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Development Document for Effluent Limitations Guidelines and Standards for the

Plastics Molding and Forming

Point Source Category

Final

DEVELOPMENT DOCUMENT
for
EFFLUENT LIMITATIONS GUIDELINES AND STANDARDS
for the
PLASTICS MOLDING AND FORMING POINT SOURCE CATEGORY

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SECTION I

SUMMARY AND CONCLUSIONS

INTRODUCTION

Pursuant to Sections 301, 304, 306, 307, 308, and 501 of the Clean Water Act and the Settlement Agreement in Natural Resources Defense Council v. Train 8 ERC 2120 (D.D.C. 1976), modified 12 ERC 1833 (D.D.C. 1979), modified by orders dated October 26, 1982, August 2, 1983; January 6, 1984; and July 5, 1984, the Environmental Protection Agency (EPA) collected and analyzed data for plants in the Plastics Molding and Forming Point Source category. (Throughout this document the Plastics Molding and Forming category is referred to as the "PM&F" category.) Proposed effluent limitations guidelines and standards for this category were published in the Federal Register on February 15, 1984 (49 FR 5862). This document and the administrative record provide the technical basis for the final effluent limitations guidelines for existing direct dischargers and standards of performance for new source direct dischargers for the PM&F category. This document also addresses EPA's consideration of pretreatment standards for new and existing indirect dischargers in the PM&F category.

In the PM&F category, there are an estimated 10,260 plants of which 1,898 use process water (i.e., water that contacts the plastic material during processing). These plants have approximately 2,587 processes that use process water. Of these processes, 810 discharge water directly to rivers and streams; 1,145 discharge to publicly owned treatment works; and 632 do not discharge process water. The other 8,362 plants in the PM&F category do not use process water (i.e., they are dry).

To collect information regarding plant size, age and production, the production processes used, and the quantity, treatment, and disposal of process water generated, EPA conducted three questionnaire surveys and a two-part telephone survey. As a result of these surveys, 382 plants were included in a data base from which were derived technical, statistical, and economic information to evaluate the PM&F category. In addition, EPA sampled PM&F processes at 18 plants: four plants were sampled in 1980; seven plants were sampled in 1983; and seven plants were sampled in 1984. Samples collected were analyzed for conventional, selected nonconventional, and priority toxic pollutants to identify and quantify pollutants present in PM&F process waters.

The Agency examined data obtained from the questionnaire surveys and the wastewater sampling programs to characterize the PM&F

category. The category is comprised of plants that employ generic processes that blend, mold, form, or otherwise process plastic materials. These processes are:

1. extrusion,
2. molding,
3. coating and laminating,
4. thermoforming,
5. calendering,
6. casting,
7. foaming,
8. cleaning, and
9. finishing.

Results of the sampling programs indicate that process water is generally used to cool or heat plastic products, to clean both the surfaces of the plastic products and the surfaces of shaping equipment that contact plastic products, or to finish plastic products. Waters used in contact cooling and heating processes, in cleaning processes, and in finishing processes have different pollutant characteristics. For this reason, the PM&F category was divided into three subcategories:

1. contact cooling and heating water subcategory;
2. cleaning water subcategory; and
3. finishing water subcategory.

The contact cooling and heating water subcategory includes those processes where process water contacts raw materials or plastic products for the purpose of heat transfer during plastics molding and forming.

The cleaning water subcategory includes those processes that use process water to clean the surface of plastic products or to clean shaping equipment surfaces that are or have been in contact with the formed plastic product. Process water used to clean the plastic product or shaping equipment includes water used in the detergent wash cycle and water used in the rinse cycle to remove detergents and other foreign matter.

The finishing water subcategory includes those processes that use process water to finish the plastic product. Finishing water consists of water used to carry away waste plastic material or to lubricate the product during the finishing operation.

Only process water that contacts the plastic material, plastic product, or surfaces of shaping equipment used to mold or form plastic materials is covered by this final regulation. Non-contact cooling water is not process water and thus is not controlled. Permit writers and control authorities will establish limitations for the discharge of non-contact cooling water and other non-process wastewater on a case-by-case basis.

Plants in the PM&F category may have processes that use only one type of water and thus fit within one subcategory. However, many plants have contact cooling and heating water, cleaning water, and finishing water processes. In this instance, plants must comply with the effluent limitations guidelines and standards for each subcategory.

EPA studied the PM&F category to characterize the pollutants in the different types of process water. The conventional and nonconventional pollutants or pollutant properties present in treatable concentrations are: (1) conventional pollutants - biochemical oxygen demand (BOD_5), oil and grease (O&G), total suspended solids (TSS), and pH, (2) nonconventional pollutants - total organic carbon, chemical oxygen demand, and total phenols. The priority toxic pollutants found in treatable concentrations in PM&F process waters are: (1) contact cooling and heating water - bis(2-ethylhexyl) phthalate, (2) cleaning water - phenol and zinc, and (3) finishing water - bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate.

The control and treatment technologies available for this category include various end-of-pipe technologies. These technologies were considered appropriate for the treatment of plastics molding and forming process waters and formed the basis for the model treatment technologies for the final PM&F regulation.

End-of-pipe technologies considered appropriate for PM&F process waters include equalization, pH adjustment, settling, the activated sludge process, the activated carbon process and filtration. Using these technologies, the Agency developed several treatment options. After consideration of these options, the Agency selected model treatment technologies as the basis for this regulation.

Equalization. Equalization involves mixing or holding of wastewater to provide an influent to a treatment process with both a relatively constant flow rate and composition.

pH Adjustment. Acidic and basic materials are used to control the pH of the wastewater. Proper pH adjustment not only controls a pollutant property but also serves to ensure proper treatment technology performance.

Settling. Settling is a process that removes solid particles from a liquid matrix by gravitational force. This is done by reducing the velocity of the flow in a large volume tank so that gravitational settling can occur. Floatable materials such as oils can also be removed in this process by skimming them from the surface of the water in the tank.

Biological Treatment (Activated Sludge). The activated sludge process is a widely used biological treatment process characterized by a suspension of microorganisms maintained in a homogeneous state by mixing and turbulence induced by aeration. The microorganisms oxidize soluble and colloidal organic material to carbon dioxide and water in the presence of molecular oxygen. This process treats dissolved pollutants such as BOD_5, total organic carbon, and total phenols. The activated sludge process, which is designed to ensure optimal removal of BOD_5, also may remove organic priority pollutants in the wastewater.

Activated sludge technology can be used with settling technologies to make a package activated sludge plant. These are self-contained plants that usually consist of a primary settling unit, an activated sludge unit, and a final settling unit. Package activated sludge plants can be used to treat flows from as low as 600 gallons per day to as high as 100,000 gallons per day.

Activated Carbon. The activated carbon process is used to remove dissolved organic contaminants from wastewater. The activated carbon removes pollutants from water by the process of adsorption, the attraction and accumulation of one substance on the surface of another. Organic compounds are preferentially adsorbed onto activated carbon; this selectivity results in a particularly effective method for the removal of soluble organic compounds from aqueous solutions.

Filtration. Filtration processes are used to remove suspended solids from process waters. Filtration processes include a wide range of technologies including screens, granular media filters, belt filters, and membrane filters. The primary difference between the various types of filters is the degree of permeability of the barrier, ranging from the coarseness of a wire screen to the selectivity of ultrafiltration membranes.

TYPE OF EFFLUENT LIMITATIONS GUIDELINES AND STANDARDS

The effluent limitations guidelines and standards in the final PM&F regulation are mass-based. They are calculated using the following equation:

$$\text{Effluent Mass} = (\text{Concentration})\ (\text{Average Process Water Usage Flow Rate})$$

The pollutant concentrations, which are based on the performance of the selected model treatment technology, are promulgated in the final rule and presented in this document. The average process water usage flow rate is the process water, including recycle, that flows through a process and contacts the plastic product. A permit writer uses the concentration values promulgated in this rule and the average process water usage flow rate, which is obtained from the permittee, to calculate the effluent pollutant mass that can be discharged.

If a plant has more than one PM&F process in the same subcategory, the average process water usage flow rate for those processes is the sum of the average process water usage flow rate for each process. This sum is used to calculate the pollutant mass for the PM&F processes at a plant in the same subcategory.

CONTACT COOLING AND HEATING WATER SUBCATEGORY

Best Practicable Technology Currently Available (BPT) Effluent Limitations Guidelines

The BPT effluent limitations guidelines for this subcategory are based on the application of good housekeeping practices. During plant visits and various sampling episodes, EPA found that good housekeeping practices are commonly employed with processes in this subcategory. Raw materials and lubricating oils are routinely segregated from the cooling and heating water, which keeps pollutants not generated during the PM&F operation out of the cooling and heating water. The final BPT effluent limitations guidelines ensure continuation of those practices because they are based on a statistical evaluation of the pollutant concentrations currently discharged by processes at plants employing good housekeeping techniques. This approach was selected at BPT because no conventional or nonconventional pollutants were found in treatable concentrations in contact cooling and heating waters.

Implementation of the final BPT effluent limitations guidelines for this subcategory will result in only minimal removals of conventional, nonconventional, and priority toxic pollutants.

Best Available Technology Economically Achievable (BAT) Effluent Limitations Guidelines

Except for bis(2-ethylhexyl) phthalate, there are no toxic pollutants present in treatable concentrations in the process water discharged by contact cooling and heating water processes. Therefore, except for bis(2-ethylhexyl) phthalate, the BAT effluent limitations guidelines are the same as the BPT effluent limitations guidelines for this subcategory.

The toxic pollutant bis(2-ethylhexyl) phthalate was found in treatable concentrations (ranging from 0.011 mg/l to 1.72 mg/l) in 52.6 percent of the contact cooling and heating water samples collected and analyzed. However, none of the technologies considered during the development of the proposed rule for this subcategory can be used to control this pollutant. Accordingly, EPA is reserving the BAT effluent limitations guidelines for bis(2-ethylhexyl) phthalate pending further study. The Agency has identified one technology (i.e., the activated carbon process) that it believes will effectively control bis(2-ethylhexyl) phthalate, but at this time does not have treatability data for phthalates for that treatment process. EPA plans to study the treatment of phthalates by the activated carbon process and, after reviewing the results of that study, to propose and promulgate BAT effluent limitations guidelines for bis(2-ethylhexyl) phthalate.

Because the BAT effluent limitations guidelines for all pollutants except bis(2-ethylhexyl) phthalate are the same as the BPT effluent limitations guidelines for those pollutants, there are no additional pollutant removals achieved by implementation of the final BAT effluent limitations guidelines.

Best Conventional Pollutant Control Technology (BCT) Effluent Limitations Guidelines

The Agency was unable to identify a technology that further reduces the concentrations of conventional pollutants found in contact cooling and heating waters. For this reason, BCT is equal to BPT for this subcategory and the BCT effluent limitations guidelines are the same as the BPT effluent limitations guidelines. Because there are no technologies available to reduce conventional pollutants in this subcategory, EPA has no reason to await promulgation of the final BCT methodology before promulgating BCT effluent limitations guidelines for this subcategory.

New Source Performance Standards (NSPS)

Except for bis(2-ethylhexyl) phthalate, the Agency is promulgating NSPS for this subcategory equal to the BPT effluent limitations guidelines. The NSPS control BOD_5, O&G, TSS, and pH.

NSPS are being promulated equal to the BPT effluent limitations guidelines because the Agency believes that the characteristics of process waters generated by new sources will be substantially the same as the characteristics of PM&F process waters generated by existing sources. Accordingly, the Agency considered the same technologies as the basis for NSPS that were considered for BPT/BAT. EPA was unable to identify additional technologies that are capable of reducing the concentrations of pollutants found in process water discharges from contact cooling and heating water processes at new sources.

The Agency believes that the concentrations of bis(2-ethylhexyl) phthalate in contact cooling and heating water discharged by new sources will be similar to the concentrations of that pollutant discharged by existing sources. As discussed earlier, the Agency found treatable concentrations of bis(2-ethylhexyl) phthalate in 52.6 percent of the contact cooling and heating water samples collected and analyzed. Because no previously-studied technologies effectively control this pollutant, NSPS for bis(2-ethylhexyl) phthalate are reserved pending completion of the phthalate treatability study discussed above.

NSPS were derived based on a statistical evaluation of the conventional pollutant concentrations in process waters discharged by existing contact cooling and heating water processes. They ensure that the same good housekeeping practices employed at existing sources will be employed at new sources.

The Agency anticipates that 14 kilograms per year of the toxic pollutants found in treatable concentrations in contact cooling and heating waters will be discharged from a "normal" new source plant for this subcategory. Implementation of NSPS is expected to result in minimal pollutant removals.

EPA has defined a "normal" new source plant for this subcategory as a plant that only contains a contact cooling and heating water process. The average process water usge flow rate for the contact cooling and heating water process at this "normal" plant is 35 gpm and the pollutant concentrations in the process water discharged from that process are assumed to be equal to the average pollutant concentrations for this subcategory.

Pretreatment Standards for Existing Sources (PSES)

The Agency is not promulgating PSES at this time for any pollutant; PSES for bis(2-ethylhexyl) phthalate are being reserved. EPA has determined that the average percentage of toxic pollutant removals nation-wide by well-operated POTWs meeting secondary treatment requirements (ranging from 35 to 99 percent) is greater than the percentage of toxic pollutant removals achieved by BAT (i.e., zero percent removals). Therefore, the toxic pollutants do not pass through a POTW. Even though categorical pretreatment standards are not being promulgated, indirect dischargers in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

PSES for bis(2-ethylhexyl) phthalate are reserved pending proposal and promulgation of the BAT effluent limitations guidelines for bis(2-ethylhexyl) phthalate. When BAT is selected, EPA will determine if that pollutant passes through a POTW.

Pretreatment Standards for New Sources (PSNS)

The Agency is not promulgating PSNS at this time for any pollutant; PSNS for bis(2-ethylhexyl) phthalate are being reserved. The Agency believes that new and existing indirect discharge sources will discharge the same pollutants in similar amounts. As discussed in the preceding subsection, the average percentage of toxic pollutants removed nation-wide by well-operated POTWs meeting secondary treatment requirements (ranging from 35 to 99 percent) is greater than the average percent removal achieved by BAT/NSPS for this subcategory (i.e., zero percent removal). Therefore, the toxic pollutants do not pass through a POTW. Even though the Agency is not promulgating categorical pretreatment standards, indirect dischargers at new sources in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

The Agency believes that the concentrations of bis(2-ethylhexyl) phthalate in contact cooling and heating water discharged from new indirect sources will be similar to the concentrations of that pollutant discharged from existing indirect sources. For this reason, the Agency is reserving PSNS for bis(2-ethylhexyl) phthalate until completion of the phthalate treatability study. When the technology basis for NSPS for that pollutant is selected, EPA will determine if bis(2-ethylhexyl) phthalate passes through a POTW.

CLEANING WATER SUBCATEGORY

Best Practicable Technology Currently Available (BPT) Effluent Limitations Guidelines

The Agency is promulgating BPT effluent limitations guidelines for this subcategory based on the performance of a package activated sludge plant with equalization and pH adjustment. The final BPT effluent limitations guidelines control BOD_5, O&G, TSS, and pH. The activated sludge process removes the toxic pollutants found in treatable concentrations in cleaning water. This technology and the effluent values for this technology were transferred from the organic chemicals, plastics, and synthetic fibers (OCPSF) point source category.

Implementation of the BPT effluent limitations guidelines for this subcategory is expected to result in an annual removal of 217,500 kilograms of conventional pollutants, 136,700 kilograms of nonconventional pollutants, and 155 kilograms of treatable priority toxic pollutants. EPA believes that the toxic pollutants in cleaning water are effectively controlled when the effluent limitations guidelines for the conventional pollutants are met.

Best Available Technology Economically Achievable (BAT) Effluent Limitations Guidelines

The Agency is not promulgating BAT effluent limitations guidelines more stringent than the BPT effluent limitations guidelines for this subcategory because there are insignificant quantities of toxic pollutants remaining in cleaning water after compliance with the applicable BPT effluent limitations guidelines. The Agency believes that the amount and toxicity of these pollutants do not justify establishing more stringent BAT effluent limitations guidelines for the toxic pollutants. Therefore, the BAT effluent limitations guidelines for this subcategory are the same as the BPT effluent limitations guidelines. No additional toxic pollutant removals are achieved by the BAT effluent limitations guidelines for this subcategory.

Best Conventional Pollutant Control Technology (BCT) Effluent Limitations Guidelines

The Agency has identified at least one technology (i.e., filtration) that can reduce the concentration of conventional pollutants remaining after the application of BPT for this subcategory. Accordingly, EPA is reserving promulgation of BCT effluent limitations guidelines for this subcategory pending promulgation of the final BCT methodology. Once that methodology is promulgated, EPA will use it to determine if additional controls for conventional pollutants are justified for this subcategory.

New Source Performance Standards (NSPS)

The Agency believes that characteristics of process waters discharged by new sources in the cleaning water subcategory will be the same as the characteristics of process waters discharged by existing sources in this subcategory. Thus, the technology option selected for new sources is the same as the technology option selected for existing sources in this final rule.

The Agency is promulgating NSPS based on the same model treatment technologies used as the basis for the promulgated BPT/BAT effluent limitations guidelines (package activated sludge plant with equalization and pH adjustment). Although the Agency also considered filtration as a model treatment technology following the package activated sludge plant, filtration was not included in the technology basis at this time for the reasons presented in

Section XII of this document. However, if the Agency finds that application of filtration is justified based on the final BCT cost test methodology, EPA may revise the technology basis for NSPS for this subcategory to include filtration as a polishing step. At this time, the Agency is not promulgating NSPS more stringent than the effluent limitations guidelines for existing sources because the amount and toxicity of the toxic pollutants remaining after treatment in the BPT/BAT treatment technologies for this subcategory do not justify more stringent controls.

Pollutants and pollutant properties controlled by NSPS include biochemical oxygen demand, oil and grease, total suspended solids, and pH. The Agency believes that the toxic pollutants in cleaning waters are effectively controlled when the NSPS for the above pollutants are met.

The Agency anticipates that 2,290 kilograms per year of conventional pollutants, 2,079 kilograms of nonconventional pollutants, and 2.3 kilograms of priority toxic pollutants will be discharged by a "normal" new source plant for this subcategory. Implementation of NSPS is expected to result in removal of 2,100 kilograms per year of conventional pollutants, 1,300 kilograms of nonconventional pollutants, and 1.5 kilograms of priority toxic pollutants.

A "normal" plant for the cleaning water subcategory is a model plant that has one cleaning process whose production, wastewater characteristics, and financial profile are typical of existing plants with cleaning processes. The process flow rate for the cleaning process in this "normal" plant is 13.5 gpm.

Pretreatment Standards for Existing Sources (PSES)

EPA is not promulgating PSES for the cleaning water subcategory because the priority toxic pollutants (i.e., phenol and zinc) found in cleaning waters in treatable concentrations do not pass through a POTW. The Agency compared the percent removal of phenol and zinc (i.e., 75 percent and 65 percent, respectively) achieved by application of BAT to the average percentage removal of those pollutants nation-wide by well-operated POTWs meeting secondary treatment requirements (99 percent for phenol and 77 percent for zinc). Because the percent removals in a POTW are greater than the BAT percent removals, phenol and zinc do not pass through a POTW. Therefore, pretreatment standards are not established for phenol and zinc.

Even though no categorical pretreatment standards are being promulgated for existing sources for this subcategory, indirect dischargers must comply with the General Pretreatment Regulations - 40 CFR Part 403.

Pretreatment Standards for New Sources (PSNS)

The Agency is not promulgating PSNS for this subcategory. The Agency believes that new and existing indirect discharge sources will discharge the same pollutants in similar amounts. As discussed in the preceding subsection, the average toxic pollutant percentage removal by well-operated POTWs meeting secondary treatment requirements is greater than the percentage of toxic pollutants removed by the model treatment technology for the BAT effluent limitations guidelines, which is the technology basis for NSPS. Therefore, the toxic pollutants do not pass through a POTW.

Even though new indirect dischargers are not subject to categorical pretreatment standards, they must comply with the General Pretreatment Reglations - 40 CFR Part 403.

FINISHING WATER SUBCATEGORY

Best Practicable Technology Currently Available (BPT) Effluent Limitations Guidelines

The Agency is promulgating BPT effluent limitations guidelines for this subcategory based on the performance of a settling unit. The BPT effluent limitations guidelines control TSS and pH.

The Agency estimates that the BPT effluent limitations guidelines for this subcategory will result in a removal of 2,520 kilograms per year of conventional pollutants from finishing process waters.

Best Available Technology Economically Achievable (BAT) Effluent Limitations Guidelines

Except for three phthalates, EPA is promulgating BAT equal to BPT for this subcategory. The BAT effluent limitations guidelines are the same as the BPT effluent limitations guidelines. There are no additional pollutant removals achieved by implementation of the BAT effluent limitations guidelines for this subcategory.

EPA was only able to identify one technology (i.e., the activated carbon process) for the removal of the three phthalates found in treatable concentrations in finishing waters. However, the Agency does not have treatability data for phthalates for the activated carbon process. The Agency plans to study the treatment of phthalates by the activated carbon process. After reviewing the results of that study, EPA plans to propose and to promulgate BAT effluent limitations guidelines for the three phthalates in finishing water. For this reason, the BAT effluent limitations guidelines for this subcategory for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved.

Best Conventional Pollutant Control Technology (BCT) Effluent Limitations Guidelines

EPA was able to identify at least one technology (i.e., filtration) that could reduce the concentration of TSS in finishing waters after the application of BPT. Accordingly, BCT effluent limitations guidelines for this subcategory are reserved pending promulgation of the final BCT methodology. That methodology will be used to determine if additional controls for conventional pollutants are justified for this subcategory.

New Source Performance Standards (NSPS)

The Agency believes that characteristics of process waters discharged from finishing processes at new sources will be the same as the characteristics of process waters discharged by those processes at existing sources. Thus, the technology option selected for new sources is the same as the one selected for existing sources.

The Agency is promulgating NSPS based on the same model treatment technology used as the basis for the BPT effluent limitations guidelines (i.e., settling). Although the Agency also considered filtration as a model treatment technology following settling, filtration was not included in the technology basis for NSPS at this time for the reasons presented in Section XII of this document. However, if the Agency finds that application of filtration is justified based on the final BCT cost test methodology, EPA may revise the technology basis for NSPS for this subcategory to include filtration as a polishing step. At this time, the Agency is not establishing NSPS more stringent than the effluent limitations guidelines for existing sources because, except for three phthalates, there are no toxic pollutants found in finishing waters in treatable concentrations. The Agency believes that the concentrations of the three phthalates in finishing waters discharged by new sources will be similar to the concentrations of those phthalates found in finishing waters discharged by existing sources. For this reason, the Agency is reserving NSPS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate for this subcategory.

Pollutants and pollutant properties controlled by new sources include TSS and pH. NSPS for this subcategory are the same as the BPT effluent limitations guidelines.

The Agency anticipates that 363 kilograms per year of conventional pollutants will be discharged by a "normal" new source plant for this subcategory. Implementation of NSPS is expected to result in the removal of 252 kilograms per year of conventional pollutants.

EPA has defined a "normal" new source plant for this subcategory as a plant that only contains a finishing water process. The average process water usage flow rate for the finishing water process at this "normal" plant is 3.15 gpm and the pollutant concentrations in the process water discharged from that process are assumed to be equal to the average pollutant concentrations for this subcategory.

Pretreatment Standards for Existing Sources (PSES)

The Agency is not promulgating PSES for this subcategory at this time for any pollutant; PSES for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved. EPA has determined that the average percentage of the toxic pollutants removed nation-wide by well-operated POTWs meeting secondary treatment requirements (ranging from 35 to 99 percent) is greater than the average percent removal achieved by application of BAT (i.e., zero percent removal). Therefore, the toxic pollutants do not pass through a POTW. Even though the Agency is not promulgating categorical pretreatment standards, indirect dischargers at existing sources in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

PSES for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved pending promulgation of the BAT effluent limitations guidelines for those pollutants. When BAT is established, EPA will determine if those three phthalates pass through a POTW.

Pretreatment Standards for New Sources (PSNS)

The Agency is not promulgating PSNS for this subcategory at this time for any pollutant; PSNS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved. The Agency believes that new and existing indirect discharge sources will discharge the same pollutants in similar amounts. As discussed in the preceding subsection, EPA has determined that the average percentage of toxic pollutants removed nation-wide by well-operated POTWs meeting secondary treatment requirements is greater than the average percent of toxic pollutants removed by the model treatment technology for BAT, which is the technology basis for NSPS. Therefore, the toxic pollutants do not pass through a POTW. Even though the Agency is not promulgating categorical pretreatment standards, indirect discharges at new sources in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

The Agency believes that the concentrations of the three phthalates in finishing waters discharged from new sources will be similar to the concentrations of those pollutants discharged from existing indirect sources. For this reason, the Agency is reserving PSNS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate until completion of the phthalate treatability study. When the technology basis for the NSPS for those pollutants is established, EPA will determine if PSNS for the three phthalates are warranted.

SECTION II

RECOMMENDATIONS

1. EPA has divided the plastics molding and forming category into three subcategories for the purpose of final effluent limitations guidelines and standards. They are:

   - contact cooling and heating water subcategory;
   - cleaning water subcategory; and
   - finishing water subcategory.

2. Best Practicable Technology Currently Available (BPT) effluent limitations guidelines for the contact cooling and heating water subcategory are based on a statistical evaluation of the pollutant concentrations in contact cooling and heating waters. For the cleaning water subcategory and the finishing water subcategory, the BPT effluent limitations guidelines are based on the performance of a package activated sludge plant with pH adjustment and a settling unit with pH adjustment, respectively.

A. BPT EFFLUENT LIMITATIONS GUIDELINES FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

The mass of the pollutants listed below that can be discharged is calculated by multiplying the average process water usage flow rate for the contact cooling and heating water processes at a point source times the following pollutant concentrations:

Contact Cooling and Heating Water

Concentration used to calculate BPT effluent limitations

Pollutant or Pollutant Property	Maximum for any 1 day (mg/l)
BOD_5	26
Oil & Grease	29
TSS	19
pH	(1)

[1] Within the range of 6.0 to 9.0 at all times.

The permit authority will obtain the average process water usage flow rate for the contact cooling and heating water processes from the permittee.

B. BPT EFFLUENT LIMITATIONS GUIDELINES FOR THE CLEANING WATER SUBCATEGORY

The mass of the pollutants listed below that can be discharged is calculated by multiplying the average process water usage flow rate for the cleaning water processes at a point source times the following pollutant concentrations:

Cleaning Water

Concentration used to calculate BPT effluent limitations

Pollutant or Pollutant Property	Maximum for any 1 day (mg/l)	Maximum for monthly average (mg/l)
BOD_5	49	22
Oil & Grease	71	17
TSS	117	36
pH	(1)	(1)

[1] Within the range of 6.0 to 9.0 at all times.

The permit authority will obtain the average process water usage flow rate for the cleaning water processes from the permittee.

C. BPT EFFLUENT LIMITATIONS GUIDELINES FOR THE FINISHING WATER SUBCATEGORY

The mass of the pollutants listed below that can be discharged is calculated by multiplying the average process water usage flow rate for the finishing water processes at a point source times the following pollutant concentrations:

Finishing Water

Concentration used to calculate BPT effluent limitations

Pollutant or Pollutant Property	Maximum for any 1 day (mg/l)	Maximum for monthly average (mg/l)
TSS	130	37
pH	(1)	(1)

[1] Within the range of 6.0 to 9.0 at all times.

The permit authority will obtain the average process water usage flow rate for the finishing water processes from the permittee.

3. Except for one phthalate in contact cooling and heating waters and three phthalates in finishing waters, best available technology economically achievable (BAT) equals BPT for each subcategory. The BAT effluent limitations guidelines are the same as the BPT effluent limitations guidelines for each subcategory. The BAT effluent limitations guidelines for phthalates in two subcategories are reserved pending further study.

A. BAT EFFLUENT LIMITATIONS GUIDELINES FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

(1) The BAT effluent limitations guidelines for bis(2-ethylhexyl) phthalate are reserved.
(2) The Agency has determined that, with the exception of bis(2-ethylhexyl) phthalate, there are no toxic pollutants in treatable concentrations in contact cooling and heating waters. Accordingly, the Agency is promulgating BAT effluent limitations guidelines equal to the BPT effluent limitations guidelines.

B. BAT EFFLUENT LIMITATIONS GUIDELINES FOR THE CLEANING WATER SUBCATEGORY

The Agency has determined that there are insignificant quantities of toxic pollutants in cleaning process waters after application of BPT. Accordingly, because the BPT level of treatment provides adequate control, the Agency is establishing BAT effluent limitations guidelines equal to the BPT effluent limitations guidelines.

C. BAT EFFLUENT LIMITATIONS GUIDELINES FOR THE FINISHING WATER SUBCATEGORY

(1) The BAT effluent limitations guidelines for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved.

(2) The Agency has determined that, with the exception of bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate, there are no toxic pollutants in treatable concentrations in finishing waters. Accordingly, the Agency is promulgating BAT effluent limitations guidelines equal to the BPT effluent limitations guidelines for this subcategory.

4. EPA could not identify a technology that would reduce the concentrations of conventional pollutants in contact cooling and heating waters. Therefore, the Agency has no reason to await promulgation of the final BCT methodology before promulgating BCT effluent limitations guidelines for the contact cooling and heating water subcategory. The BCT effluent limitations guidelines for that subcategory are the same as the BPT effluent limitations guidelines.

The Agency identified at least one technology, filtration, that could reduce the concentrations of conventional pollutants in cleaning waters and in finishing waters after application of BPT. Accordingly, BCT effluent limitations guidelines are not being promulgated for those subcategories until the final BCT methodology is promulgated.

A. BCT EFFLUENT LIMITATIONS GUIDELINES FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

The mass of the pollutants listed below that can be discharged is calculated by multiplying the average process water usage flow rate for the contact cooling and heating water processes at a point source times the following pollutant concentrations:

Contact Cooling and Heating Water

Concentration used to calculate BCT effluent limitations

Pollutant or Pollutant Property	Maximum for any 1 day (mg/l)
BOD_5	26
Oil & Grease	29
TSS	19
pH	(1)

[1] Within the range of 6.0 to 9.0 at all times.

The permit authority will obtain the average process water usage flow rate for the contact cooling and heating water processes from the permittee.

B. BCT EFFLUENT LIMITATIONS GUIDELINES FOR THE CLEANING WATER SUBCATEGORY

[Reserved]

C. BCT EFFLUENT LIMITATIONS GUIDELINES FOR THE FINISHING WATER SUBCATEGORY

[Reserved]

5. Except for one phthalate in contact cooling and heating waters and three phthalates in finishing waters, new source performance standards (NSPS) are the same as the BAT effluent limitations guidelines for each subcategory. NSPS for the phthalates in two subcategories are reserved pending further study.

A. NEW SOURCE PERFORMANCE STANDARDS FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

(1) NSPS for bis(2-ethylhexyl) phthalate are reserved.
(2) The mass of the pollutants listed below that can be discharged is calculated by multiplying the average process water usage flow rate for the contact cooling and heating water processes at a new source times the following pollutant concentrations:

Contact Cooling and Heating Water

Concentration used to calculate NSPS

Pollutant or Pollutant Property	Maximum for any 1 day (mg/l)
BOD_5	26
Oil & Grease	29
TSS	19
pH	(1)

[1] Within the range of 6.0 to 9.0 at all times.

The permit authority will obtain the average process water usage flow rate for the new source contact cooling and heating water processes from the permittee.

B. NEW SOURCE PERFORMANCE STANDARDS FOR THE CLEANING WATER SUBCATEGORY

The mass of the pollutants listed below that can be discharged is calculated by multiplying the average process water usage flow rate for cleaning processes at a new source times the following pollutant concentrations:

Cleaning Water

Concentration used to calculate NSPS

Pollutant or Pollutant Property	Maximum for any 1 day (mg/l)	Maximum for monthly average (mg/l)
BOD_5	49	22
Oil & Grease	71	17
TSS	117	36
pH	(1)	(1)

[1] Within the range of 6.0 to 9.0 at all times.

The permit authority will obtain the average process water usage flow rate for the contact cooling and heating water processes from the permittee.

C. NEW SOURCE PERFORMANCE STANDARDS FOR THE FINISHING WATER SUBCATEGORY

(1) NSPS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved.
(2) The mass of the pollutants listed below that can be discharged is calculated by multiplying the average process water usage flow rate for the finishing water processes at a new source times the following pollutant concentrations:

Finishing Water

Concentration used to calculate NSPS

Pollutant or Pollutant Property	Maximum for any 1 day (mg/l)	Maximum for monthly average (mg/l)
TSS	130	37
pH	(1)	(1)

[1] Within the range of 6.0 to 9.0 at all times.

The permit authority will obtain the average process water usage flow rate for the new source finishing water processes from the permittee.

6. Except for one phthalate in contact cooling and heating waters and three phthalates in finishing waters, the Agency is not promulgating pretreatment standards for existing sources for the PM&F category because the Agency has determined that toxic pollutants found in PM&F process waters do not pass through a well-operated secondary POTW. The PSES for the phthalates in two subcategories are reserved pending further study.

A. PRETREATMENT STANDARDS FOR EXISTING SOURCES FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

(1) PSES for bis(2-ethylhexyl) phthalate are reserved.
(2) Any existing source subject to this subpart that introduces pollutants into a publicly owned treatment works must comply with 40 CFR Part 403 - General Pretreatment Regulations.

B. PRETREATMENT STANDARDS FOR EXISTING SOURCES FOR THE CLEANING WATER SUBCATEGORY

Any existing source subject to this subpart that introduces pollutants into a publicly owned treatment works must comply with 40 CFR Part 403 - General Pretreatment Regulations.

C. PRETREATMENT STANDARDS FOR EXISTING SOURCES FOR THE FINISHING WATER SUBCATEGORY

(1) PSES for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved.
(2) Any existing source subject to this subpart that introduces pollutants into a publicly owned treatment works must comply with 40 CFR Part 403 - General Pretreatment Regulations.

7. Except for one phthalate in contact cooling and heating waters and three phthalates in finishing waters, EPA is not promulgating pretreatment standards for new sources for the PM&F category because the Agency has determined that toxic pollutants found in PM&F process waters do not pass through a well-operated secondary POTW. PSNS for the phthalates in two subcategories are reserved pending further study.

A. PRETREATMENT STANDARDS FOR NEW SOURCES FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

(1) PSNS for bis(2-ethylhexyl) phthalate are reserved.
(2) Any new source subject to this subpart that introduces pollutants into a publicly owned treatment works must comply with 40 CFR Part 403 - General Pretreatment Regulations.

B. PRETREATMENT STANDARDS FOR NEW SOURCES FOR THE CLEANING WATER SUBCATEGORY

Any new source subject to this subpart that introduces pollutants into a publicly owned treatment works must comply with 40 CFR Part 403 - General Pretreatment Regulations.

C. PRETREATMENT STANDARDS FOR NEW SOURCES FOR THE FINISHING WATER SUBCATEGORY

(1) PSNS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved.

(2) Any new source subject to this subpart that introduces pollutants into a publicly owned treatment works must comply with 40 CFR Part 403 - General Pretreatment Regulations.

SECTION III

INTRODUCTION

BACKGROUND

The Federal Water Pollution Control Act Amendments of 1972 established a comprehensive program to "restore and maintain the chemical, physical, and biological integrity of the Nation's waters," under Section 101(a). By July 1, 1977, existing industrial dischargers were required to achieve "effluent limitations requiring the application of the best practicable control technology currently available" (BPT), under Section 301(b)(1)(A); and by July 1, 1984, "effluent limitations requiring the application of the best available technology economically achievable . . . which will result in reasonable further progress toward the national goal of eliminating the discharge of all pollutants" (BAT), under Section 301(b)(2)(A). New industrial direct dischargers were required to comply with Section 306 new source performance standards (NSPS) based on best available demonstrated technology; existing and new dischargers to publicly owned treatment works (POTW) were subject to pretreatment standards under Sections 307(b) (PSES) and (c) (PSNS), respectively, of the Act.

The requirements for direct dischargers were to be incorporated into National Pollutant Discharge Elimination System (NPDES) permits issued under Section 402 of the Act while pretreatment standards were made enforceable directly against dischargers to a POTW (indirect dischargers). Although Section 402(a)(1) of the 1972 Act authorized the setting of NPDES permit requirements for direct dischargers on a case-by-case basis, Congress intended that, for the most part, effluent limitations guidelines be based on the degree of effluent reduction attainable by the application of BPT and BAT. Moreover, Sections 304(c) and 306 of the Act required promulgation of new source performance standards; and Sections 304(f), 307(b), and 307(c) required promulgation of pretreatment standards. In addition to the effluent limitations guidelines and standards for designated industry categories, Section 307(a) of the Act required the Administrator to promulgate effluent standards for toxic pollutants applicable to all dischargers of these pollutants. Finally, Section 501(a) of the Act authorized the Administrator to prescribe any additional regulations "necessary to carry out his functions" under the Act.

EPA was unable to promulgate many of the toxic pollutant standards by the dates specified in the Act. In 1976, EPA was sued by several environmental groups and in settlement of this lawsuit, EPA and the plaintiffs executed a "Settlement Agreement" that was approved by the Court. This agreement required EPA to develop a program and adhere to a schedule for promulgating effluent limitations guidelines, pretreatment standards, and new source performance standards for 65 "priority" compounds and classes of compounds for 21 major industries. See, Settlement Agreement in Natural Resources Defense Council, Inc. v. Train, 8 ERC 2120 (D.D.C. 1976), modified 12 ERC 1833 (D.D.C. 1979), modified by orders dated October 26, 1982, August 2, 1983; January 6, 1984; and July 5, 1984.

On December 27, 1977, the President signed into law amendments to the Federal Water Pollution Control Act (P.L. 95-217). The Act, as amended, is commonly referred to as the Clean Water Act. Although this Act makes several important changes in the federal water pollution control program, its most significant feature is its incorporation of several of the basic elements of the Settlement Agreement program for toxic pollution control. Sections 301(b)(2)(C) and 301(b)(2)(D) of the Act now require the achievement by July 1, 1984, of effluent limitations guidelines based on the application of BAT for toxic pollutants, including the 65 priority compounds and classes of compounds (the same toxic pollutants as listed in Natural Resources Defense Council, Inc. v. Train, supra) Congress declared toxic under Section 307(a) of the Act. Likewise, EPA's program for new source performance standards is now aimed principally at control of these toxic pollutants. Pretreatment standards control the toxic pollutants and other pollutants that are incompatible with a POTW. Moreover, to strengthen the toxics control program, Congress added Section 304(e) to the Act, authorizing the Administrator to prescribe "best management practices" (BMP) to prevent the release of toxic and hazardous pollutants from plant site runoff, spillage or leaks, sludge or waste disposal, and drainage from raw material storage associated with, or ancillary to, the manufacturing or treatment process.

In keeping with its emphasis on toxic pollutants, the Clean Water Act also revised the control program for other types of pollutants. Instead of BAT for "conventional" pollutants identified under Section 304(a)(4) (including biochemical oxygen demand, oil and grease, total suspended solids, fecal coliform, and pH), the new Section 301(b)(2)(E) requires achievement, by July 1, 1984, of "effluent limitations requiring the application of the best conventional pollutant control technology" (BCT). The factors considered in assessing BCT for an industry include a two-part "cost-resonableness" test (Section 304(b)(4)(B)). See, American Paper Institute v. EPA, 660 F.2d 954 (4th Cir. 1981). The first part compares the cost for private industry to reduce its conventional pollutant concentrations with the costs for publicly owned treatment works for similar levels of reduction of those pollutants. The second part examines the cost effectiveness of additional industrial treatment beyond BPT.

For nonconventional pollutants, Sections 301(b)(2)(A) and (b)(2)(F) require achievement of BAT effluent limitations guidelines within three years after their establishment, or not later than July 1, 1984, whichever is later, but in no case later than July 1, 1987.

PURPOSE

This document presents the information and data used to develop the final effluent limitations guidelines and standards for the plastics molding and forming (PM&F) point source catetgory.

AUTHORITY

Effluent limitations guidelines and standards for the PM&F category are promulgated under authority of Sections 301, 304, 306, 307, 308, and 501 of the Clean Water Act (the Federal Water Pollution Control Act Amendments of 1972, 33 U.S.C. 1251 et seq., as amended by the Clean Water Act of 1972, Pub. L. 95-217) (the "Act"). The PM&F regulation is also promulgated in response to the Settlement Agreement in Natural Resources Defense Council, Inc. v. Train, 8 ERC 2120 (D.D.C. 1976), modified 12 ERC 1833 (D.D.C. 1979), modified by orders dated October 26, 1982; August 2, 1983; January 6, 1984; and July 5, 1984.

STUDY APPROACH

The approach used to develop the final PM&F effluent limitations guidelines and standards included the following:

1. The Agency conducted three questionnaire surveys, a two part telephone survey, and three process water sampling programs to gather information on production, manufacturing processes, water use and dischargepractices, wastewater treatment, and process water characteristics.

2. EPA sampled 18 PM&F plants to characterize PM&F process waters. Samples were analyzed for conventional, selected nonconventional, and priority toxic pollutants.

3. A PM&F category profile was developed using information from both the questionnaire surveys and literature sources.

4. The PM&F category was subcategorized based on information from the questionnaire surveys and information from the process water sampling programs.

5. Results of the sampling programs were used to determine the pollutants in PM&F process water in treatable concentrations.

6. Control and treatment technologies that effectively control the pollutants in PM&F process waters were evaluated.

7. Costs, pollutant removals, energy, and non-water quality aspects were evaluated for the various treatment technologies.

8. A model treatment technology was selected for BPT, BAT, BCT, and NSPS.

9. Effluent concentration data for the model treatment technologies were obtained.

10. Effluent concentrations for each type of effluent limitations guidelines and standard were then established. Permit writers use those concentrations and the average process water usage flow rate for a process, which is obtained from the permittee, to calculate the mass of a pollutant that can be discharged.

EPA also evaluated the need for pretreatment standards to control discharges of pollutants that may pass through a well-operated secondary POTW. Results of that evaluation are presented in this document.

SECTION IV

CATEGORY PROFILE

The plastics molding and forming (PM&F) category covers a large, diverse industry that uses plastic materials to produce a wide variety of consumer and industrial products. Since shortly after the discovery of plastic materials, nearly 60 years ago, molding and forming processes have been used to turn those plastic materials into usable items. Originally, plastic products were typically considered to be inexpensive substitutes for wood, leather, and metal items. However, in many cases, plastic products have virtually replaced other products due to their superior characteristics, such as light weight, durability, and resistance to corrosion. New product uses for plastics as well as new plastic formulations are continually being developed. The products produced by the plastics molding and forming category are used in a wide variety of consumer and industrial markets including: automobiles, appliances and business machines, construction materials, disposables, household furnishings, housewares, and medical products.

The PM&F category is defined by both molding and forming processes and the type of material processed. Plants included in this category are generally classified by Standard Industrial Classification (SIC) 3079 (Miscellaneous Plastics Products), either as the primary or secondary SIC code. Standard Industrial Classifications are established by the Department of Commerce, Bureau of the Census. Plants in the PM&F category with a secondary SIC code of 3079 include plants in the textiles, lumber and wood products, printing and publishing, machinery, and transportation equipment industries. Classification of plants covered by the PM&F category is further discussed in Section V.

In the course of developing the effluent limitations guidelines and standards for the plastics molding and forming category, several data gathering efforts were undertaken to characterize the category. They included:

- sampling at PM&F plants,
- conducting questionnaire and telephone surveys, and
- reviewing various literature sources.

SAMPLING PROGRAM

Information on the PM&F category was gathered during three wastewater sampling programs for this regulation. Eighteen PM&F plants were sampled: seven in 1984, seven in 1983, and four in 1980. Flow measurements taken at the sampled plants provided information on water use and discharge practices. Wastewater samples were collected and analyzed for conventional, selected nonconventional, and priority toxic pollutants. A discussion of the sampling programs including analytical results is presented in Section VI and Appendix A.

QUESTIONNAIRE SURVEYS

The plastics molding and forming category was surveyed to gather information on plant size and age, production, production processes used, and the quantity, treatment, and disposal of wastewater generated at PM&F plants. This information was requested in three questionnaires mailed under authority of Section 308 of the Act to companies known or believed to be involved in plastics molding or forming. A two-part telephone survey was used to develop the sample population for the third questionnaire survey.

1978 and 1979 Questionnaire Surveys

In 1978, 8,450 firms were sent a one-page questionnaire. The names and addresses of the plants on the mailing list for this questionnaire were compiled from the following sources:

1. Dun & Bradstreet, Inc. and
2. Fortune 500.

The questionnaire asked if the company was a plastics molder and former; if process water was used, (i.e., water that contacts the plastic product); the type of discharge mode; what plastic materials were used; and what products were produced at the plant. When firms had plastics molding and forming processes at more than one location, a questionnaire was completed for each plant. A total of 5,138 questionnaires were returned: 1,114 indicated the plant uses process water in a PM&F process and 4,024 indicated the plant did not use process water.

From the 1,114 respondents to the 1978 survey that indicated they use process water, 750 plants were mailed a more detailed questionnaire in 1979. Approximately 59 percent of the companies responded to the survey. Of the 440 respondents to the survey, 407 returned completed questionnaires and 33 indicated they had responded incorrectly to the one page questionnaire and had only dry processes (i.e., process water did not contact the formed plastic product). Seventy-five of the 407 returned questionnaires contained unclear data. Therefore, only data from the other 332 questionnaires were included in the data base for this regulation.

1983 Telephone Survey

In 1983, a two-part telephone survey was conducted to screen the target population for the third questionnaire survey. The first part of the telephone survey consisted of calling:

1. Two hundred thirty-two plants that returned a completed 1979 questionnaire;
2. One hundred ninety-three randomly selected plants that received a questionnaire in 1979 but did not return it; and
3. Seven hundred thirty-four plants, which is one-half of the PM&F plants (i.e., "new plants") that entered the market between January 1, 1978, and December 31, 1981, according to Dun and Bradstreet's list of plants with a primary SIC Code 3079.

The first part of the telephone survey was designed so that the ratio of plants that returned a completed questionnaire in 1979 to those that did not return a completed 1979 questionnaire (232:193) was the same as the actual ratio of plants that returned a completed 1979 questionnaire to those that did not return a completed questionnaire (407:343). All plants called in the telephone survey were asked whether they were plastics molders and formers and if they use process water in their PM&F processes.

Table IV-1 contains the results of the first part of the telephone survey. As shown in the table, 50 percent of the new plants indicated they use process water. This number was viewed with caution because the Agency believes that many of the respondents did not completely understand the difference between contact and non-contact cooling water.

In the second part of the 1983 telephone survey, the other portion of the new PM&F plants that entered the market between January 1, 1978, and December 31, 1981, (according to Dun and Bradstreet's listing of plants with a primary SIC 3079) were contacted. They were also asked if they were plastics molders and formers and if they use process water. However, they were asked more specific questions, such as what kind of PM&F processes they employ. Because more time was spent asking detailed questions, information from this part of the survey concerning the number of processes that use process water (i.e., wet) and that do not use process water (i.e., dry) is more reliable than similar information from the first part of the telephone survey.

Table IV-1

RESULTS OF 1983 PLASTICS MOLDING AND FORMING TELEPHONE SURVEY
FIRST PART

	Total Number of Plants Contacted	Number of Plants in the PM&F Category	PM&F Plants					
			Wet	(%)	Dry	(%)	Total	(%)
Respondents to the 1979 questionnaire	232	182	182	(100)	0		182	(100)
Non-respondents to the 1979 questionnaire	193	103	29	(28)	74	(72)	103	(100)
New plants listed as entering the market between 1977 and 1981*	734	467	233	(50)	234	(50)	467	(100)

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*Based on a listing of plants with a primary SIC of 3079 obtained from Dun and Bradstreet, Inc.

In the second part of the telephone survey, 741 PM&F plants were contacted. Out of that number, 535 plants were plastic molders and formers, while the remaining 206 plants were not. Eighty-four (16 percent) of the 535 PM&F plants had wet processes and 451 (84 percent) had dry processes.

Table IV-2 contains a distribution of the wet and dry processes from the second part of the telephone survey by the type of process. The number of wet processes and the number of dry processes are larger than the number of PM&F plants because some plants had more than one PM&F process. Types of processes with the largest number of wet processes were extrusion, molding, and finishing.

Results of the second part of the telephone survey are distributed by type of wet process and discharge mode in Table IV-3. Most PM&F processes in the second part of the telephone survey discharged process water to a POTW or did not discharge process water (i.e., zero discharge).

Statistics from the 1978 single page questionnaire and the second part of the 1983 telephone survey were used to estimate the percentages of wet and dry plants in the PM&F category. These were the only two surveys not directed solely at plants believed to use process water. Of the 5,138 PM&F plants that returned the single page questionnaire in 1978, 21 percent indicated they had wet PM&F processes. This percentage was averaged with the 16 percent of the PM&F plants from the second part of the 1983 telephone survey that had wet processes to obtain an estimate of 18.5 percent of the plants in the PM&F industry that are wet (i.e., use process water). Multiplying that percentage times the estimated 10,260 plants in the PM&F category provides an estimate of 1,898 wet plants in the category.

The total number of 10,260 PM&F plants in the United States was estimated from the State Industrial Guides (Appendix B lists the guides used to develop this estimate). For the purpose of the analysis to determine the economic impact of the PM&F regulation, a sample of PM&F plants was selected from the State Industrial Guides. The sample, created by extracting every 20th plant listed as a producer of SIC 3079 products, formed a data base with 513 entries. Because one of every 20 plants was included, the 513 entries represent five percent of the category. It follows that the PM&F category is comprised of approximately 10,260 plants. (20 x 513 = 10,260). Approximately 77 percent of the 513 randomly selected plants had a primary SIC of 3079 and approximately 23 percent had a secondary SIC of 3079. Applying these percentages to the total number of plants in the PM&F industry yields 7,900 plants that are primary plastics molders and formers and 2,360 that mold and form plastics as a secondary

Table IV-2

RESULTS OF 1983 PLASTICS MOLDING AND FORMING TELEPHONE SURVEY SECOND PART

Type of Process	Wet Processes	(%)*	Dry Processes	(%)*	Total	(%)
Extrusion	52	(48)	57	(52)	109	(100)
Molding	18	(5)	329	(95)	347	(100)
Coating and Laminating	1	(3)	34	(97)	35	(100)
Thermoforming	0	(0)	61	(100)	61	(100)
Calendering	0	(0)	2	(100)	2	(100)
Casting	1	(14)	6	(86)	7	(100)
Foaming	0	(0)	11	(100)	11	(100)
Cleaning	3	(60)	2	(40)	5	(100)
Finishing	11	(13)	72	(87)	83	(100)
TOTAL	86		574		660	

	Total	%
Wet Processes	86	13
Dry Processes	574	87
	660	100

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*Percent of type of process.

Table IV-3

DISTRIBUTION OF THE NUMBER OF PLASTICS MOLDING AND FORMING PROCESSES BY DISCHARGE MODE*

Type of Wet Process	% of Total Wet Processes	Discharge Mode				Total
		Direct	Indirect	Zero	Unknown	
Extrusion	60.4	1	15	31	5	52
Molding	20.9	1	7	10	0	18
Coating and Laminating	1.2	0	0	1	0	1
Casting	1.2	0	1	0	0	1
Cleaning	3.5	0	3	0	0	3
Finishing	12.8	0	1	10	0	11
TOTAL	100.0	2	27	52	5	86

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*Based on information from second part of 1983 telephone survey.

operation. The types of plants with a secondary plastics molding and forming operation include: textiles, lumber and wood products, printing and publishing, machinery, and transportation equipment.

1983 Questionnaire Survey

To further update the questionnaire data collected in 1978 and 1979 and the telephone survey data collected in 1983, 330 questionnaires were mailed in June 1983 to PM&F plants believed to use process water. The questionnaire sample was developed based on the following criteria:

1. The sample was selected to obtain current information for plants in the category that used process water (wet plants).
2. The sample consisted of "new" PM&F plants (those entering the market between January 1, 1978, and December 31, 1981) and "old" PM&F plants that use process water.
3. The number of "new" wet plants was based on data obtained through the two-part 1983 telephone survey.
4. The number of "old" wet plants was based on data obtained from the 1978 and 1979 questionnaire surveys and from the first part of the 1983 telephone survey.

All plants entering the market between January 1, 1978, and December 31, 1981, were called during the 1983 two-part telephone survey. Results of that telephone survey indicate that there are 317 new plants that have wet processes.

As previously mentioned, a one-page questionnaire was mailed to 8,450 plants in 1978. There were 1,114 respondents to that questionnaire that indicated they had wet PM&F processes. A more detailed questionnaire was mailed to 750 of the 1,114 respondents in 1979.

Four hundred seven of the plants that received the 1979 detailed questionnaire returned a completed questionnaire and 343 did not return a completed questionnaire. Applying the percentage of the plants that returned completed questionnaires and the percentage of those that did not return completed questionnaires to the 1,114 wet plants reported in the 1978 one-page questionnaire provides an estimate of the 1,114 plants that would have returned a completed questionnaire and that would not have returned a completed questionnaire if all 1,114 wet plants were mailed a detailed questionnaire. Using those percentages, the Agency estimated that 605 of 1,114 wet plants would have returned a completed questionnaire and 509 would not have returned a completed questionnaire.

To determine the current status of the 750 plants that received the 1979 questionnaire, 425 of those plants were called in 1983. Two hundred thirty-two of the 425 plants returned a questionnaire in 1979 and 193 did not return the questionnaire. As previously mentioned, this telephone survey was designed so that the ratio of the plants that were called (i.e., 232:193) was the same ratio of the plants that returned and did not return completed 1979 detailed questionnaires (i.e., 407:343).

Results of this telephone survey indicated that 182 of the 232 plants that returned completed 1979 questionnaires were still in business and had wet PM&F processes. Twenty-nine of the 193 plants that did not return a completed 1979 questionnaire were still in business and had wet PM&F processes.

The estimated number of the 1,114 wet plants from the 1978 questionnaire survey that would have returned a detailed questionnaire (i.e., 605) and the estimated number that would not have returned the questionnaire (i.e., 509) if all 1,114 plants had been mailed a questionnaire in 1979 were adjusted using the results of the above telephone survey. Based on those results, the Agency estimates 475 (605 x 182/232) of the 1,114 wet plants would have returned the questionnaire and 76 (509 x 29/193) would not have returned the questionnaire. Therefore, the target population for the 1983 questionnaire survey was:

317	new PM&F plants
475	old PM&F plants that would have returned the 1979 questionnaire
76	old PM&F plants that would not have returned the 1979 questionnaire
868	total

The numbers in each of these strata were used to determine the distribution of the 330 detailed questionnaires that were mailed in 1983. That distribution is presented in Table IV-4.

In the 1983 questionnaire survey, companies were requested to return a questionnaire for each plastics molding and forming plant they operated. A total of 346 questionnaires were returned. Of the 346 questionnaires, 324 indicated the plant molds and forms plastic materials. One hundred sixty-four of those plants use process water (i.e., they were wet) and 160 do

Table IV-4

DISTRIBUTION OF THE 330 DETAILED 1983 QUESTIONNAIRES

Stratum	Target Population	Number of 1983 Questionnaires
New plants	317*	119
Old plants that would have returned 1979 questionnaire	475**	182
Old plants that would not have returned the 1979 questionnaire	76**	29

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*Based on results of 1983 telephone survey of new plants.

**Based on results of 1983 telephone survey of plants that did and did not return a completed questionnaire in 1979.

not use process water (i.e., they are dry), meaning 49 percent of the plants do not use process water even though the survey was directed at plants who said they did use process water in the first part of the 1983 telephone survey. This supports the Agency's contention that plants did not understand the difference between contact and non-contact cooling water during the first part of the telephone survey.

Most of the plants that received the 1979 and 1983 questionnaires have a primary SIC of 3079, which means that a plant molds and forms plastics as a primary operation. During a meeting with representatives from the Society of Plastics Industries (SPI), they indicated that additional information could be obtained from plants with a secondary SIC of 3079 (i.e., the plant molds and forms plastics as a secondary operation) by sending a questionnaire to a sample of companies on the mailing list for the magazine "Plastic World." Therefore, in August 1983, 170 questionnaires were mailed to companies on that list. As with the other questionnaire surveys, companies were requested to return a questionnaire for each plastics molding and forming plant that they operated, so that a total of 173 questionnaires were returned. Of these, 106 questionnaires indicated the plant molds and forms plastics with 56 plants using process water and 50 plants having dry processes. Because the mailing list included many subscribers not believed to mold or form plastics, such as libraries and chambers of commerce, statistical information from these questionnaires was not used to characterize the PM&F category. However, information from the questionnaires regarding water use practices at plants with wet processes was included in the data base for this regulation.

Summary of Questionnaire Data Base

The questionnaire data base for this project consists of questionnaires from both the 1979 and 1983 surveys. When a plant returned a questionnaire in 1979 and again in 1983, only the updated questionnaire from the 1983 survey was included in the data base. Thus, only 175 of the original 332 questionnaires from the 1979 questionnaire survey remain in the updated data base. The data base also contains 207 of the 220 1983 questionnaires returned by wet plants during the 1983 questionnaire survey. The other 13 questionnaires were incomplete or not applicable to these effluent limitations guidelines. For the incomplete questionnaires, it was not possible to obtain additional data through further contact with the plants. Thus, the questionnaire data base consists of 175 questionnaires from the 1979 survey and 207 questionnaires from the 1983 survey for a total of 382 questionnaires.

Table IV-5 contains a distribution of the types of processes by discharge mode reported on the 1979 and 1983 questionnaires that make up the data base. These processes use water that contacts the plastic product. Extrusion processes are the most prevalent water-users followed by cleaning processes and molding processes. Calendering processes comprise the smallest percentage of processes that use process water (0.8 percent) because most of the cooling water is contained within the calender roll and never touches the plastic product.

Each of the questionnaires in the data base for this regulation were reviewed and the following data were documented for future reference and evaluation:

- company name, plant address, and name of the contact listed in the questionnaire.
- plant discharge status (i.e., direct, indirect, or zero discharge).
- production processes present at the plant; associated wastewater flow rates; production rates; operating hours; process water treatment, reuse, or disposal methods; and the plastic materials processed.
- capital and annual treatment costs.
- any available pollutant monitoring data provided by the plant.

The summaries provided a consistent, systematic method of evaluating the information. In addition, procedures were developed to simplify subsequent analyses. Using those procedures, information in the data base was used to:

- select and list the plants containing specific production processes and associated types of process waters and treatment technologies;
- sum the number of plants containing specific processes and associated types of process waters and treatment technology combinations;
- calculate annual production associated with each process; and
- calculate water use and process water discharge rates for individual processes.

Table IV-5

WATER-USING PROCESSES IN THE PM&F CATEGORY DISTRIBUTED BY DISCHARGE MODE

	Number of Processes in the Questionnaire Data Base							
Type of Process†	Direct Discharge	(%)*	Indirect Discharge	(%)*	Zero Discharge	(%)*	Total	(%)**
Extrusion	128	(78.6)	132	(57.1)	105	(82.7)	365	(70.0)
Molding	5	(3.1)	18	(7.8)	8	(6.3)	31	(6.0)
Coating and Laminating	2	(1.2)	7	(3.0)	4	(3.1)	13	(2.5)
Thermoforming	2	(1.2)	6	(2.6)	1	(0.8)	9	(1.7)
Calendering	2	(1.2)	2	(0.9)	0	(0)	4	(0.8)
Casting	1	(0.6)	5	(2.2)	0	(0)	6	(1.2)
Cleaning	21	(12.9)	47	(20.3)	3	(2.4)	71	(13.6)
Finishing	2	(1.2)	14	(6.1)	6	(4.7)	22	(4.2)
TOTAL	163	(100)	231	(100)	127	(100)	521	(100)

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†There are no foaming processes that use water in the questionnaire data base.

*Percent of all types of processes in a discharge mode.

**Percent of the total number of processes for all types of processes.

The survey information was used to develop the PM&F category profile, to develop a subcategorization scheme, to analyze treatment and control technologies, to determine the water use and discharge practices, and to estimate statistics for the estimated 1,898 plants in the PM&F category that use process water. A more detailed description of the PM&F data base is presented in Section VI.

LITERATURE REVIEW

The literature was examined for information on plastics molding and forming processes and wastewater treatment technologies. Treatment technology effectiveness and investment and annual operation and maintenance costs were also obtained from the literature.

Many sources were reviewed for information on wastewater treatment technologies. EPA's Innovative and Alternative Technology Assessment Manual provided most of the information on treatment technologies. Treatment technology performance data were obtained from EPA's Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants. Additional data were obtained from documents supporting the proposed organic chemicals, plastics, and synthetic fibers category effluent limitations guidelines and standards. Treatment technology information obtained from these sources is presented in Section VIII. Costing information was obtained primarily from EPA's Estimating Water Treatment Costs and vendor contacts. Details on investment and operation and maintenance costs are presented in Section IX.

A great variety of general references, texts, and articles were used as sources of information on plastics molding and forming processes. The process descriptions derived from these sources are presented later in this chapter. Process information was supplemented by trip reports for numerous site visits to PM&F plants. A complete list of references used to obtain both process information and information on other aspects of the PM&F category is presented in Section XVI.

INDUSTRY DESCRIPTION

The following description of the PM&F category and the processes used to mold and form plastic products is based on information from the sources of information listed above. The literature provided the foundation on which the descriptions are based. Literature information has been augmented and updated where appropriate by data gathered during the sampling episodes and questionnaire surveys.

Plastic materials are a group of synthetic* organic materials composed of high molecular weight, long chain molecules. The molecular composition along with the degree of crosslinking and the pattern and amount of branching in the molecule determines the material's characteristics. The generic category of plastic materials includes many types of resins, resinoids, organic polymers, cellulose derivatives, casein derivatives, and proteins. Except for some specialty applications, the majority of plastic materials used in consumer and industrial products are synthetically produced organic polymers and copolymers. The PM&F effluent limitations guidelines and standards only apply to synthetic organic polymers (i.e., thermoset polymers, thermoplastic polymers, or combinations of natural polymers and thermoset or thermoplastic polymers) that are solid in their final forms and that were shaped by flow. The materials can be either homogeneous polymers or polymers combined with fillers, plasticizers, pigments, stabilizers, or other additives. Accordingly, the PM&F regulation does not apply to natural organic materials.

Plastic materials can be generally classified into two basic groups: thermoplastics and thermosets. Thermoplastics become soft when exposed to a sufficient amount of heat and they harden when cooled. The heating and cooling process can be repeated several times. Thermoplastic materials can be processed by a large number of forming processes, the most common being injection molding and extrusion. They include: acrylonitrile-butadiene-styrene, polyethylene, polypropylene, polystyrene, and polyvinyl chloride.

Thermosetting plastics are set into their permanent shape when heat and pressure are applied during molding or forming. Unlike thermoplastics, once set into shape, thermoset products cannot be softened and reformed. Thermoset plastic products are usually formed by processes such as compression molding, transfer molding, and casting. Thermoset plastic materials include alkyd resins, epoxy resins, phenolic resins, and silicone.

Some plastics can be formulated into either thermoplastics or thermosetting products depending on the extent of crosslinking permitted during their manufacture. Once produced, these materials exhibit the properties of the particular type of plastic and are processed accordingly. Polyurethene and polyester are two such plastic materials.

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* The definition of plastic materials in the PM&F regulation also includes natural polymers that are combined with synthetic organic materials, such as cellulose acetate. Wholly natural organic materials, such as regenerated cellulose, are not included in this definition.

For the purpose of regulation, the plastics industry is covered by two industrial point source categories. These categories are: (1) the organic chemicals, plastics, and synthetic fibers category which includes manufacturers who produce and formulate all the basic plastic resins and who process certain natural organic materials; and (2) the plastics molding and forming category comprised of the processors that convert the plastic materials into usable shapes.

Overlap of the organic chemicals, plastics, and synthetic fibers category and the plastics molding and forming category occurs during the production of crude intermediate plastic material, such as pelletized plastic resin. Plastics molding and forming processes (e.g., extrusion and pelletizing) used by plastics resin manufacturers to process crude intermediate plastic material for shipment off-site are excluded from the PM&F regulation and are regulated under the organic chemicals, plastics, and synthetic fibers category. Plastics molding and forming processes used by plastic resin manufacturers to process crude intermediate plastic materials that are further processed on-site into intermediate or final plastics products in molding and forming processes are controlled by the effluent limitations guidelines and standards for the plastics molding and forming category.

For example, consider a manufacturer of polyurethane who uses contact cooling water in a pelletizing operation; the pelletizing operation is the last step in the polyurethane manufacturing process. If those polyurethane pellets (crude intermediate plastic material) are shipped off-site without further molding and forming, the contact cooling water used in the pelletizing operation is regulated under the organic chemicals, plastics, and synthetic fibers category. If, however, the extruded polyurethane pellets are further extruded on-site into polyurethane tubing (intermediate or final plastic product), the contact cooling water used in both the pelletizing operation and the extrusion operation would be regulated under the plastics molding and forming category.

PM&F plants produce a wide variety of products and range from small plants with a single process and a few employees to large plants with several hundred employees. Plastics molding and forming plants tend to be located near the sales centers of the United States so that finished consumer products need not be transported over long distances. Sixty-five percent of the plants are located in one of the following four clusters:

1. New York, New Jersey, and Pennsylvania;
2. Illinois, Indiana, Michigan, and Ohio;
3. Louisiana, Oklahoma, and Texas; and
4. California and Washington.

PLASTICS MOLDING AND FORMING PROCESSES

The plastics molding and forming category consists of plants that blend, mold, form, or otherwise process a wide variety of plastic materials into intermediate or final plastic products. There are nine generic processes used to process plastic materials. They are:

1. extrusion,
2. molding,
3. coating and laminating,
4. thermoforming,
5. calendering,
6. casting,
7. foaming,
8. cleaning, and
9. finishing.

Each of these processes is described below including discussion of which PM&F processes use process water and the purpose of the water. For this regulation, process water is defined as any raw, service, recycled, or reused water that contacts the plastic product or contacts shaping equipment surfaces, such as molds and mandrels, that are or have been in contact with the plastic product. Non-contact cooling water is not process water and thus is not controlled by the final PM&F regulation. Permitting and control authorities will establish limitations for the discharge of non-contact cooling water and other non-process wastewater on a case-by-case basis.

Extrusion Processes

Extrusion processes force molten polymer under pressure through a shaping die to produce products of uniform cross-sectional area such as pipe, tubing, sheet, film, and profile. This process has a number of different applications including the compounding of polymers, the production of pellets and parisons (blow molding preforms) for later use, the production of finished and semi-finished products, and the coating of substrate materials.

A wide range of polymers are extruded. Thermoplastic polymers are most commonly used and include acrylic resins, acrylonitrile-butadiene-styrene (ABS), polyacetal, fluoroplastics, nylon, polyphenylene oxide, polybutylene, polyethylene, polypropylene, polystyrene, polyvinyl chloride, styrene-acrylonitrile, and thermoplastic polyesters.

Extruded thermoplastic foams are produced by incorporating a gas-forming expanding agent in the thermoplastic and extruding the mixture under carefully controlled conditions. This is an extrusion process with the addition of a blowing agent at the extrusion die. Packaging and building products are the major applications for extruded foam products. The primary raw materials used to produce extruded foam products are acrylonitrile-butadiene-styrene, high density polyethylene, polypropylene, polystyrene, and polyvinyl chloride.

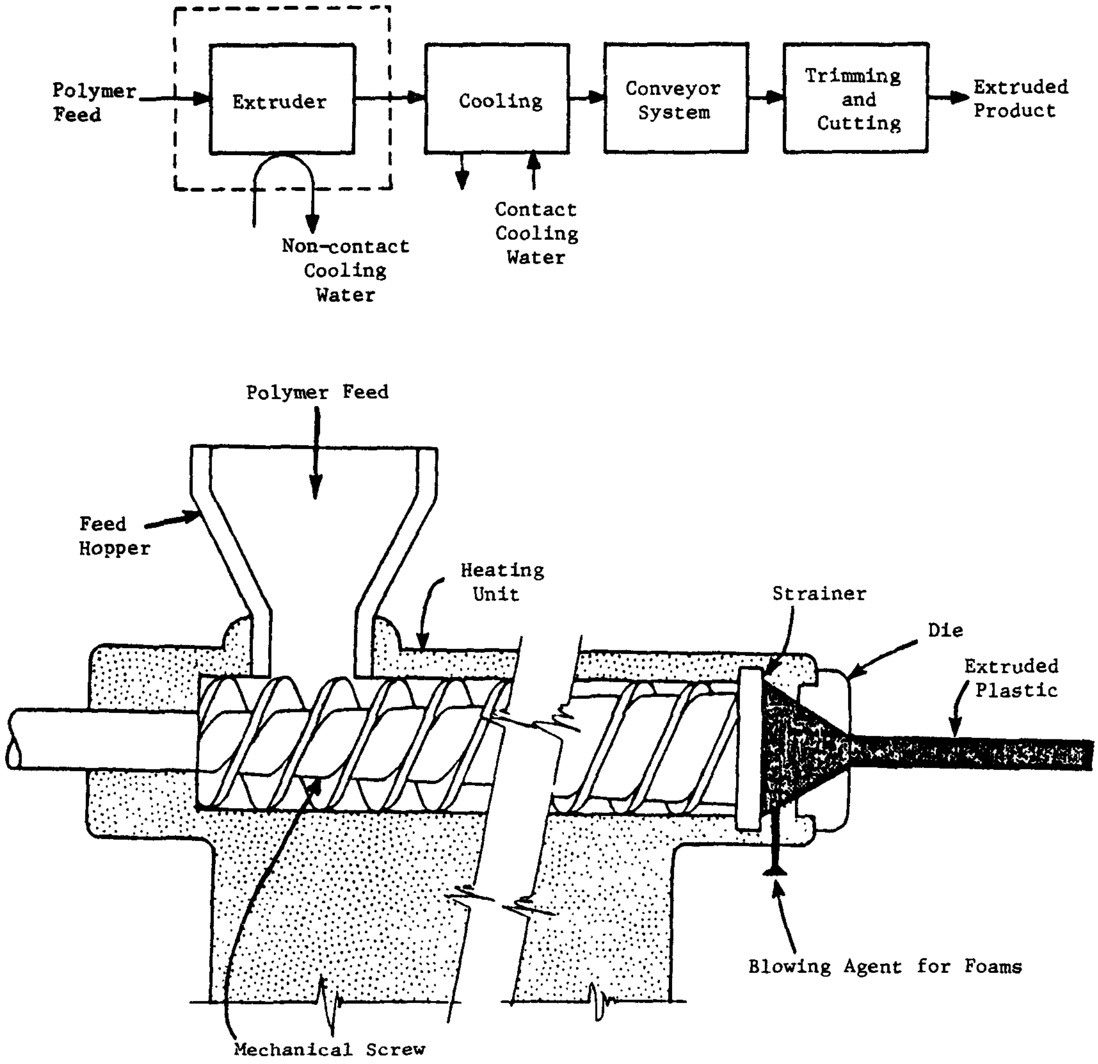
A schematic of the extrusion process is shown in Figure IV-1. Polymer granules, pellets, powder, or beads are fed into the hopper of the extruder. The polymer is picked up by a rotating screw within the extruder cylinder and is forced toward the die. Heat provided to the cylinder walls begins the softening of the polymer pellets. As the material moves along the cylinder, friction becomes the primary source of heat. During this heating and compression period, the plastic material is transformed into a homogeneous melt and is thoroughly mixed.

Prior to leaving the extruder cylinder, the melted polymer passes through a screen pack that removes dirt and provides back pressure control. The melt enters the die at high pressure. The extrusion die is a streamlined orifice that reduces the melt to the desired shape. As the extrudate leaves the extruder, it is transported over some type of roller or conveyor cooling system that cools the hot extrudate by use of air or water.

Approximately 50 percent of extrusion processes use contact cooling water. Contact cooling water is used when a high heat transfer rate is required such as for the extrusion of thick-walled products or during pelletizing operations.

Extrusion processes are often used to blend, color, and pelletize polymers. Additives required for special applications and colors desired by the processor are added to the resin and are fed to the extruder to become a homogeneous melt. A brief description of the most commonly used classes of additives and specialty chemicals is presented in Table IV-6. The melt is extruded through a multi-opening die and taken off as strands that are cut into pellets of the desired size after cooling. In many cases, the pellets are cut at the face of the die, which is submerged in water for rapid cooling. Pelletized polymers can be in the form of round, cylindrical, or cube-shaped particles and can be used as feed material for extrusion, molding, casting, foaming, and other processes. Commonly pelletized theromoplastics are ABS, polyethylene, polypropylene, and polyvinyl chloride.

Extrusion processes can use both contact and non-contact cooling water. Non-contact cooling water is used to remove excess heat from the extrusion machinery caused by friction. Direct contact cooling water is used for product quenching. Extruded profile, pipe, and tube are often cooled by direct contact cooling water.



Source: Adpated from Masson, D. (ed). <u>The Study of the Plastics Industry</u>. 1973.

Figure IV-1

EXTRUSION PROCESS

Table IV-6

COMMONLY USED ADDITIVES IN POLYMER FORMULATION USING THE EXTRUSION PROCESS

Additive	Function	Example
Antiblocking Agent	Prevents self-adhesion of films	Silicate minerals High melting point waxes
Antioxidants	Retard oxidative degradation of plastic material during processing and use	Alkylated phenols Amines Phosphates Thio compounds
Antisatic Agents	Reduce the accumulation of electronic charge on the surface of polymers	Amine Quaternary ammonium Anionic surface active agents
Catalysts	Affect the rate of chemical reactions without themselves being consumed or undergoing chemical change	Peroxides Organo-tin compounds Amines
Chemical Resistant Additives	Descrease polymer susceptibility to chemical degradation	Glass Synthetic fibers Graphite
Colorants	Impart hue (shade), volume (brightness), and chroma (strength of color) to plastics	Dyes Organic and inorganic pigments
Coupling Agents	Enhance polymer-mineral surface bonds and increase the ability of composites to retain properties during prolonged exposure to moisture	Silane compounds Titanate compounds
Cure Retardants	Reduce the cure rate for amino resins	Amines
Curing Agents	Improve the curing of thermosetting resins upon exposure to heat	Peroxides Amines Azo compounds
Fibrous Reinforcements	Impart tensile, flexural, and compressive strength to plastics	Synthetic fibers Carbon fibers Glass fibers
Fillers and Extenders	Increase the bulkiness and decrease the total cost of plastic formulations	Calcium carbonate Silica Nutshell flours
Flame Retardants	Act chemically or physically as insulators by creating endothermic cooling reactions, by coating the plastic to exclude oxygen or by influencing combustion through reaction with materials that have different physical properties	Antimony oxide Chlorinated parafins Halogenated organics
Foaming (blowing) Agents	Produce large quantities of gases upon heating that form cellular plastics	Nitrogen Pentane Azo bis formamide
Heat Stabilizers	Prevent the degradation of the plastic material during process heating and during its useful life	Barium-cadmium compounds Tin compounds

Table IV-6 (Continued)

COMMONLY USED ADDITIVES IN POLYMER FORMULATION USING THE EXTRUSION PROCESS

Additive	Function	Example
Impact Resistant Additives	Decrease a plastic materials tendency to break or crack upon impact	Acrylics ABS
Insulators	Improve the thermal or electrical insulating properties of polymers	Silaceous minerals Ceramic oxides
Lubricants	Enhance resin processibility and the appearance of the end product	Fatty acid esters Hydrocarbon oils Paraffin wax Amides
Mold Release Agents	Prevent sticking of newly formed parts to a mold	Silicon Mineral oil Wax Fatty acids Mica Talc
Plasticizers	Impart flexibility, resiliency and increasing melt flow to polymers by reducing the intramolecular forces between polymer chains	Phthalates Adipates Trimellitates Glycolates Fatty acid esters Organic phosphates
Preservatives and Biocides	Inhibit biological degradation of polymers	Fungicides Bacteriostats
Casting Promoters	Improve the cure of cast parts	Cobalt octoate Dimethyl aniline Tin salts
Sizing Agents	Coatings that protect the polymer surface	Waxes
UV Stabilizers	Absorb ultraviolet radiation and reradiate it at a harmless wavelength or consume the free radicals generated by UV light	Benzotriazoles Benzophenones

Plastic jacketed wire and cable is also passed through a water bath for direct contact cooling. The use of contact cooling water in extrusion processes is the major source of process water in the plastics molding and forming category.

Molding Processes

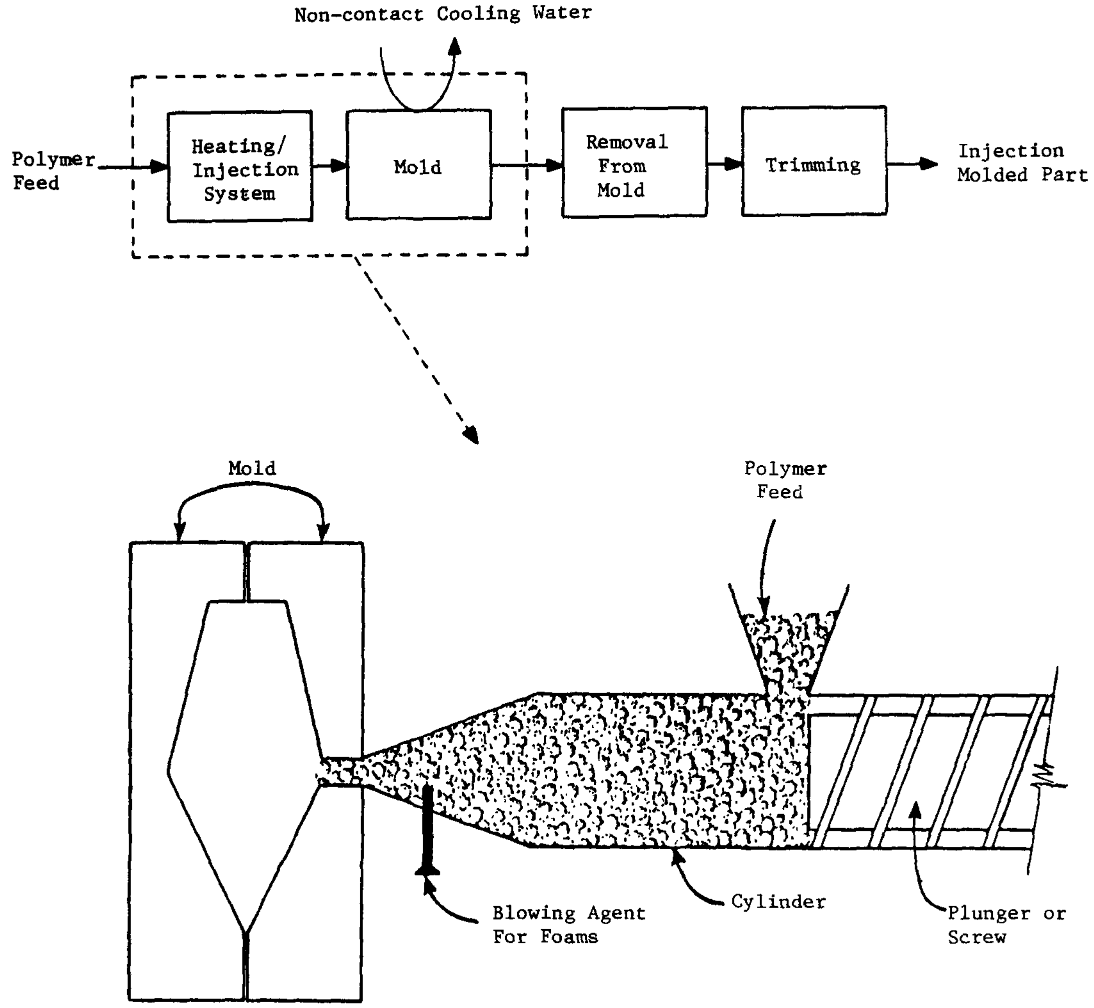
Molding is the most common process used to produce finished or semi-finished products from plastic materials. Molded parts can be solid, hollow, or foamed. Plastic objects of almost any desired shape can be produced commercially by one of seven different types of molding processes:

1. injection molding,
2. blow molding,
3. compression molding,
4. transfer molding,
5. reaction injection molding,
6. rotational molding, and
7. expandable bead foam molding.

Injection Molding. Injection molding is used to form intricate plastic parts with excellent dimensional accuracy at very high production rates. Injection molding involves the plasticating of pelletized plastic materials with heat and the subsequent injection of the melt into a mold.

Both thermoplastic and thermoset polymers are injection molded. The majority of injection molded products are produced from polyethylene, polypropylene, polystyrene, and acrylonitrile-butadiene-styrene (ABS). Other polymers that are commercially injection molded are acrylic resins, fluoroplastics, nylons, phenolic resins, polyacetal, polycarbonate, polyesters, polyphenylene sulfide, and styrene-acrylonitrile. Typical injection molded products include appliance parts, furniture parts, machine parts, office and household items, and toys and novelties. Fillers can be added during the injection molding process to produce reinforced plastic products such as appliance components and sporting goods.

A schematic of the injection molding process is shown in Figure IV-2 . The resin and additives are fed into the heating portion of the injection molding machine where the polymer is heated to the temperature at which it becomes soft enough to flow. An injection system forces the melt through a nozzle, then through sprues and runners, and finally into the cavities of the mold where high pressure is held briefly to allow the plastic to set. As thermoplastics cool in the mold, they retain the desired product shape. Thermosets require that heat be applied to the mold to complete polymerization.



Source: Adpated from Masson, D. (ed). The Study of the Plastics Industry. 1973.

Figure IV-2

INJECTION MOLDING PROCESS

Structural foam molding is an injection molding process where a blowing agent is added to either the polymer input materials or the polymer melt. Polystyrene is the major material used in structural foam molding. The following polymers are also used: acrylonitrile-butadiene-styrene, polyphenylene oxide, polycarbonate, high density polyethylene, polypropylene, and polystyrene. Uses for structural foam include furniture, business machines, and construction products.

There are four basic types of heating/injection systems used for commercial injection molding. They are: (1) conventional injection molding machines, (2) piston-type preplasticating machines, (3) screw type preplasticating machines, and (4) reciprocating-screw injection machines. The reciprocating screw injection machine is the most common machine for modern plastics processing due to its faster cycles, lower melting temperature requirements, and better mixing.

In conventional injection molding machines the plastic granules or pellets feed from a hopper into the chamber of the heating cylinder. A plunger compresses the material forcing it through progressively hotter zones of the heating cylinder. The material flows from the heating cylinder through a nozzle and into the mold. In piston-type preplasticating machines a heater is used to preplasticate the plastic granules after which the plastic is held in a holding chamber until it is molten enough to be forced into the die. A piston rams the plastic through the nozzle into the mold. In screw-type preplasticating machines, an extruder is used to plasticize the plastic material. A rotating screw feeds the pellets forward into the heated interior surface of the extruder barrel. The molten plastic is extruded into a holding chamber and is forced into the die by an injection plunger. In reciprocating screw injection machines, a rotating screw moves the plastic material forward through a heated extruder barrel. As the molten plastic material moves forward, the screw backs up to a limit switch that determines the volume of material collecting in the front of the barrel. The screw then acts as a ram and injects the plastic material into the die.

The majority of all injection molding operations use non-contact cooling water circulated through channels in both the injection equipment and the product mold. Direct contact cooling may be used, however, when molded parts require rapid cooling.

Blow Molding. Blow molding is used to produce hollow, thin wall objects from thermoplastic resins; it has become one of the major processing methods for the plastics industry for hollow articles. Blow molding involves extruding or injection molding a preformed shape that is then blown into its final form by compressed air.

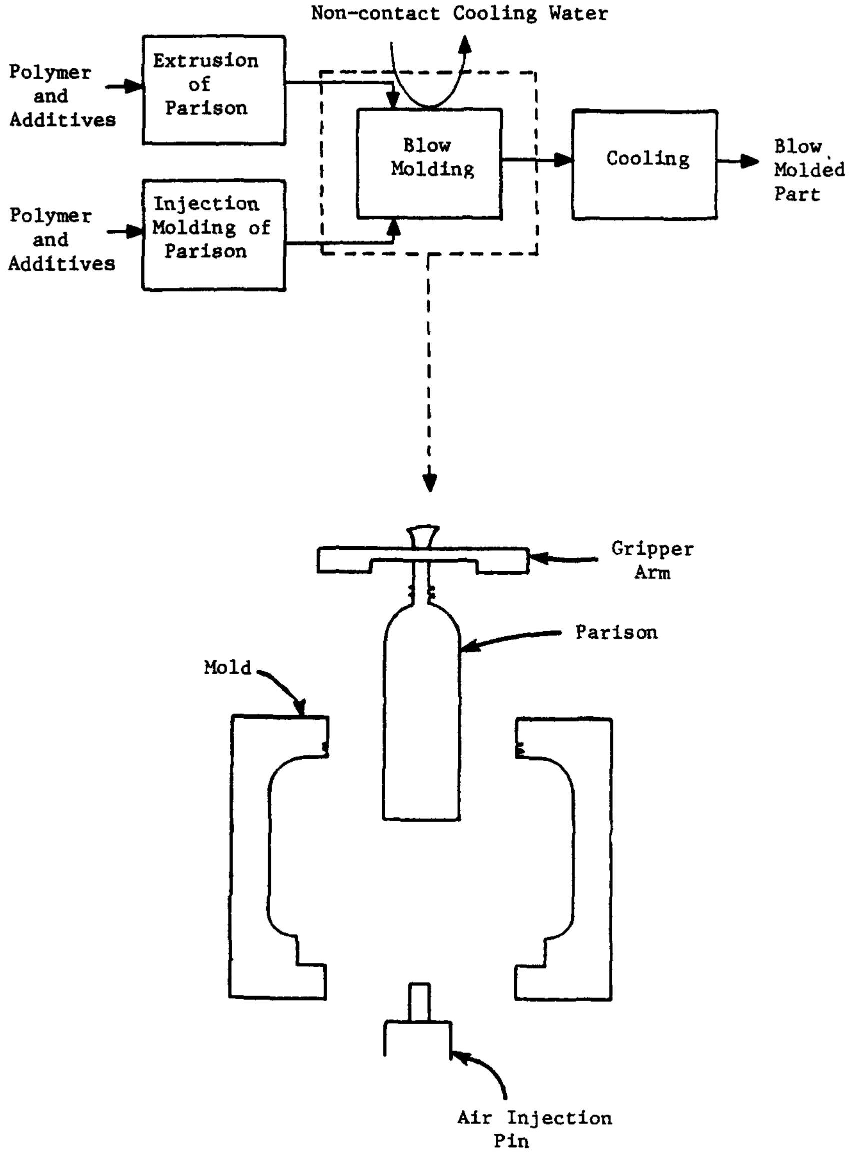
Most thermoplastic materials can be blow molded; however, high density polyethylene has traditionally been the workhorse of the blow molding industry. Other thermoplastic polymers commercially used for blow molding include acrylic resins, acrylonitrile-butadiene-styrene, polyacetal, polycarbonate, polyester, polyethylenes, polypropylene, polystyrene, and polyvinyl chloride. Blow molding processes are used to produce a wide range of hollow bottles and containers. Approximately 80 percent of the blow molding processes produce packaging items. These include household bottles and containers for cosmetics, toiletries, pharmaceuticals, chemicals, and foods, as well as industrial containers. The remaining 20 percent produce industrial products such as automobile fuel tanks, lighting fixture globes, ornaments, and toys.

A schematic of a blow molding process is shown in Figure IV-3. Blow molding processes can be divided into two major types: extrusion blow molding and injection blow molding. These two processes are similar in that they both use a parison, or preshaped sleeve, of plastic that is expanded by air pressure to fill the inside of a concave mold. The difference between the processes lies in the formation of the parison. Extrusion blow molding uses an extruder to preform parisons whereas in injection blow molding the parisons are formed in an injection mold. Blow molding processes use non-contact cooling water to cool the mold.

Compression Molding. Compression molding is one of the earliest forms of molding; it requires only one major piece of equipment: the compression press. Compression molding involves shaping a measured quantity of plastic within a mold by applying pressure and heat. This molding process is ideal for the production of parts with large areas and relatively simple shapes.

Compression molding is primarily used for processing thermoset resins, although it is used to mold thermoplastics for special applications. Polymers most commonly used in compression molding include alkyd resins, amino resins, diallyl phthalate, epoxy resins, phenolic resins, and polyester resins. Other less frequently used polymers include polytetrafluorethylene, polyurethane, silicone, and polyvinyl chloride. Fillers such as glass fibers, wood, cotton, and cellulose are often used during compression molding to produce reinforced plastic products. Typical compression molded products include novelties, knobs, handles, dinnerware, buttons, electrical and electronic components, and appliance parts. Reinforced products include large automotive and appliance parts.

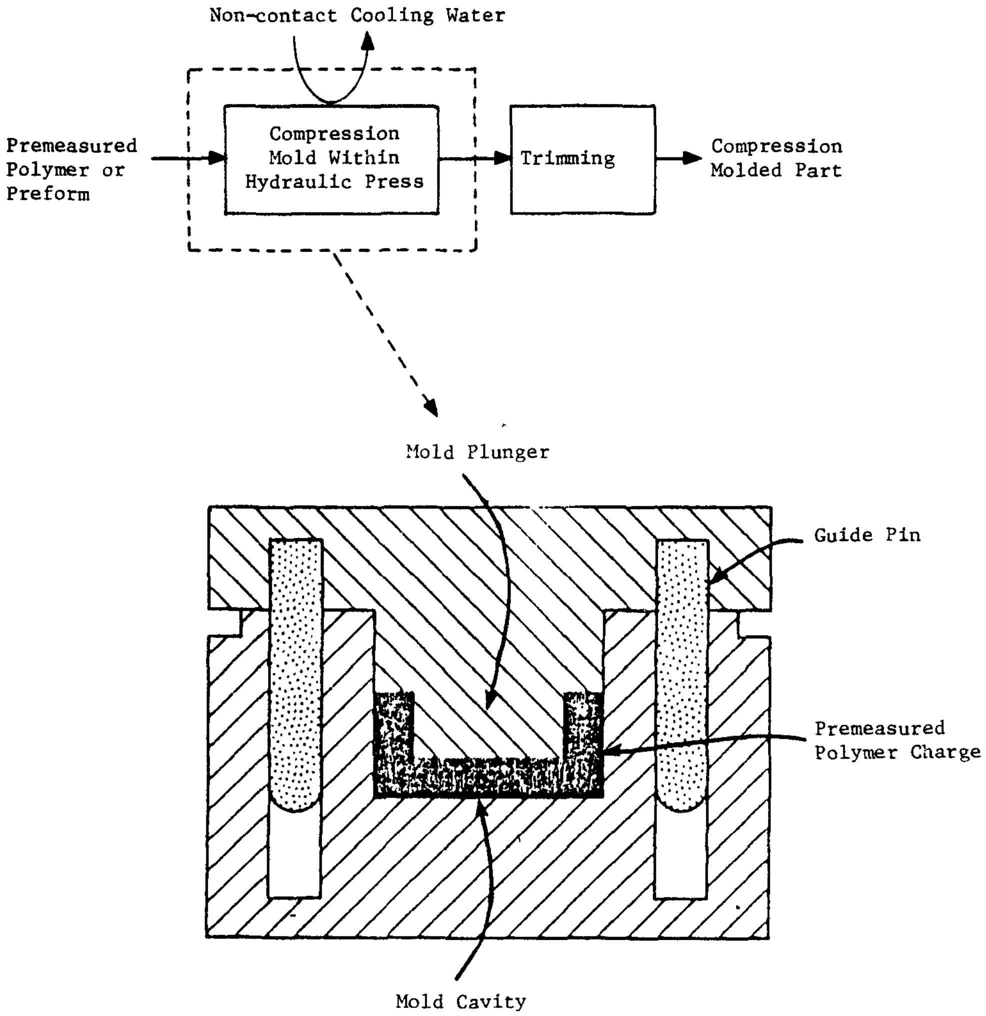
A schematic of the compression molding process is shown in Figure IV-4. The plastic material is fed to the compression mold either in granular form or as a preform. The mold halves are then



Source: Adapted from Seymour, W.B. <u>Modern Plastics Technology</u>. 1975.

Figure IV-3

BLOW MOLDING PROCESS



Source: Adapted from Masson, D. (ed). The Study of the Plastics Industry. 1973.

Figure IV-4

COMPRESSION MOLDING PROCESS

closed by a hydraulic press. Pressure is maintained and heat is applied, causing the plastic to spread to the shape of the mold.

Compression molding processes generally use non-contact cooling water to cool the mold halves. Some compression molding processes may use contact cooling water sprays to rapidly cool newly formed products.

Transfer Molding. Transfer molding is much like compression molding with the difference being that in transfer molding the resin is preheated in a separate chamber and is then forced into the mold cavity for curing.

Thermoset resins are most commonly transfer molded. These include alkyd resins, amino resins, diallyl phthalate resins, epoxy resins, phenolic resins, and polyester resins. Fillers such as cellulose, clay, glass fiber, minerals, and synthetic fibers are often used during transfer molding to produce reinforced plastic products. Transfer molding is especially well suited for the production of small intricate thermoset parts and is used extensively in the production of electrical insulating parts and connectors. Reinforced products include appliance housings and decorative parts.

A schematic of the transfer molding process is shown in Figure IV-5. Plastic preforms are preheated by heat lamps, hot air ovens, or dielectric heaters. That material is put into a chamber or "transfer pot" where it is plasticized by heat and pressure into a viscous mass. The plastic is then forced through sprues and runners into the mold cavity. The pot, sprues, runners, and cavity surfaces are maintained at a temperature suitable for rapid curing of the material. The plastic is held in the mold at its cure temperature until the part is capable of maintaining its shape. Transfer molding processes generally do not use contact water to cool the product.

Reaction Injection Molding. Reaction injection molding (RIM) involves the simultaneous high pressure injection of two or more reactive liquids into a mixing chamber followed by low pressure injection into a mold cavity. Most commercial reaction injection molding is performed with various urethane formulations. The majority of urethane formulations are comprised of two liquid intermediate feeds: the resin and isocyanate. When blowing agents are incorporated in the isocyanate feed, foam products are formed. Fillers are added during reaction injection molding to produce reinforced plastic products for the automotive industry. Reaction injection molded polyurethane products include bumper systems, panelling, automotive trim, sporting goods, and machinery housing.

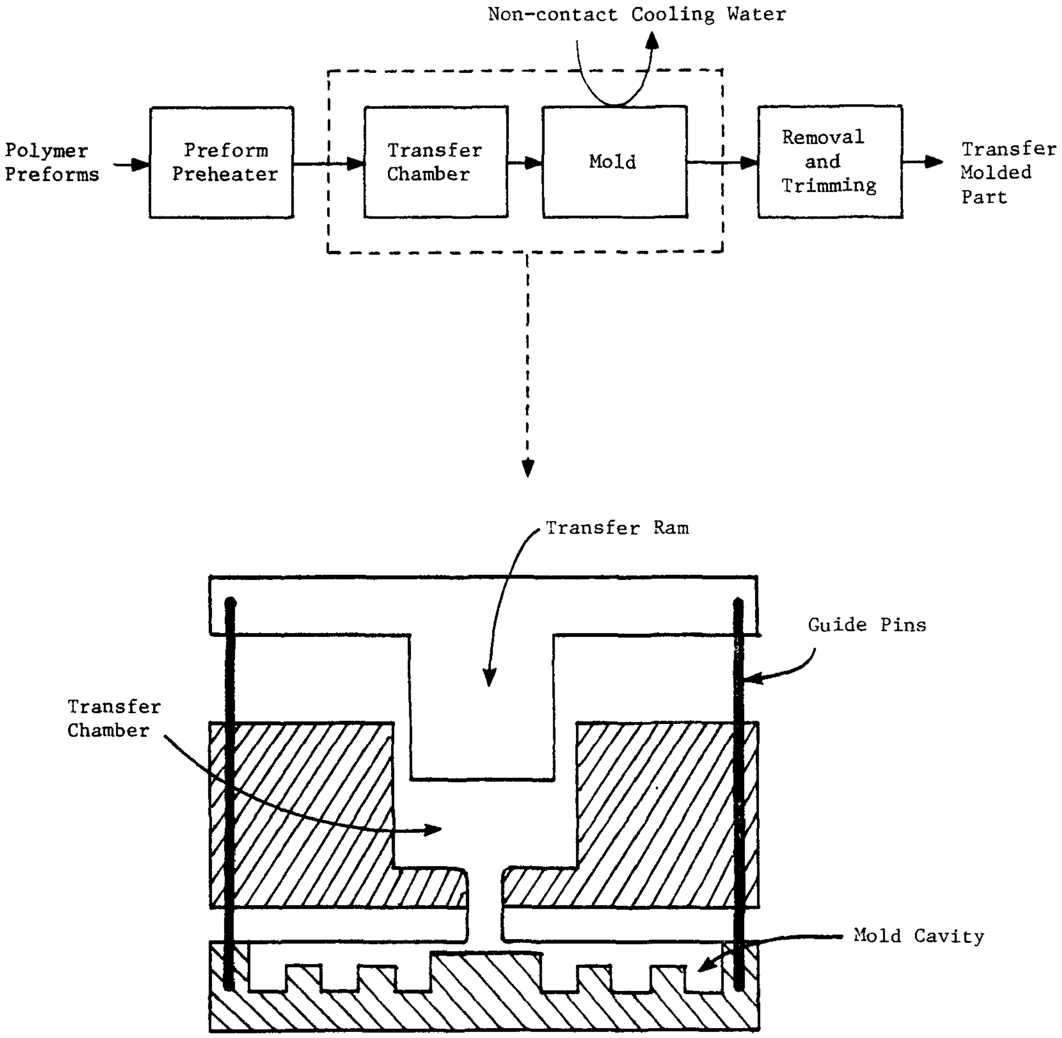


Figure IV-5

TRANSFER MOLDING PROCESS

A schematic of a reaction injection molding process is shown in Figure IV-6. A reaction injection molding process consists of four integrally related units: feed tanks, a metering system, a mixer, and the mold. The feed tanks are where the raw material components are stored and heated. Agitators, heat exchangers, low-pressure pumps, and recirculation equipment are used to maintain liquid temperature and uniformity. Liquid material from the feed tanks are metered to the mixing head where they are mixed under high-pressure. The liquids are then injected into the mold where polymerization occurs. Once the part has sufficiently cured to hold its shape, the mold is opened and the part is ejected. Contact water is not used during the reaction injection molding process. The molded parts can be sufficiently cooled by air. Non-contact water may be used to cool the mold.

Rotational Molding. Rotational molding, sometimes termed rotomolding or rotocasting, is used to make rigid or flexible thin-walled hollow objects from thermoplastic materials. Rotational molding involves rotating polymer powder or liquid in a heated hollow mold.

Rotational molding is performed almost exclusively with thermoplastic resins such as polyamide resins, polyacetal, polycarbonate, low density polyethylene, and polyvinyl chloride. The rotational molding process is used to produce a wide range of industrial and consumer goods including arm rests, toys and novelties, sporting goods, and tanks and storage bins.

A schematic of the rotational molding process is shown in Figure IV-7. Premeasured amounts of the polymer powder or liquid are put into the preheated hollow mold at the mold loading station. The mold is then put in the circulating hot air oven where it is simultaneously rotated around two perpendicular axes. The heat forces the thermoplastic to melt and the rotation uniformly distributes the polymer over the entire mold surface. The mold is then removed from the heating oven and is cooled. After the part has cooled sufficiently to hold the desired shape, the mold is opened and the part is removed.

Most rotational molding processes use non-contact cooling water to cool the outside surface of the mold. Some rotational molding processes may use direct contact water sprays when rapid cooling of the part is necessary.

Expandable Bead Foam Molding. Expandable bead foam molding processes produce a closed-cell, rigid plastic foam material characterized by fused polymer spheres. The fused polymer product is produced by expanding beads impregnated with hydrocarbon in a mold cavity. The beads puff and fuse together filling the mold cavity when heated.

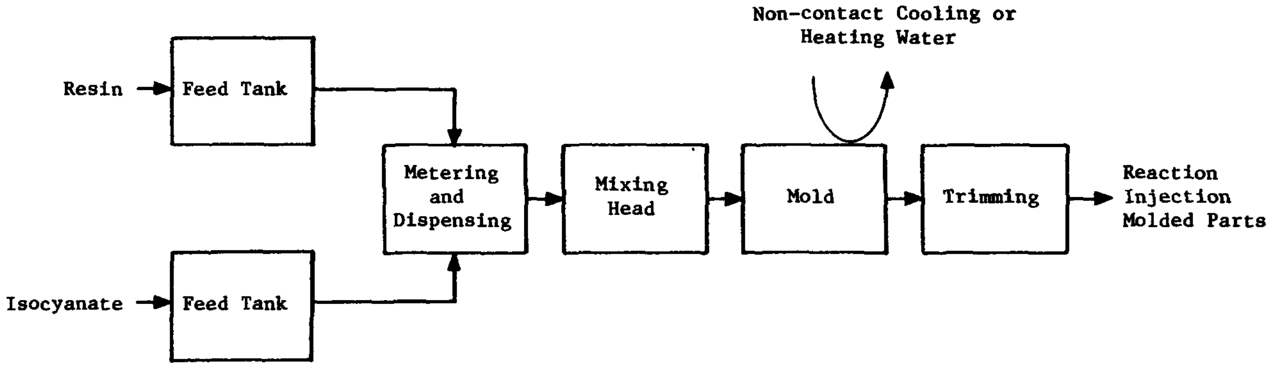


Figure IV-6

REACTION INJECTION MOLDING PROCESS

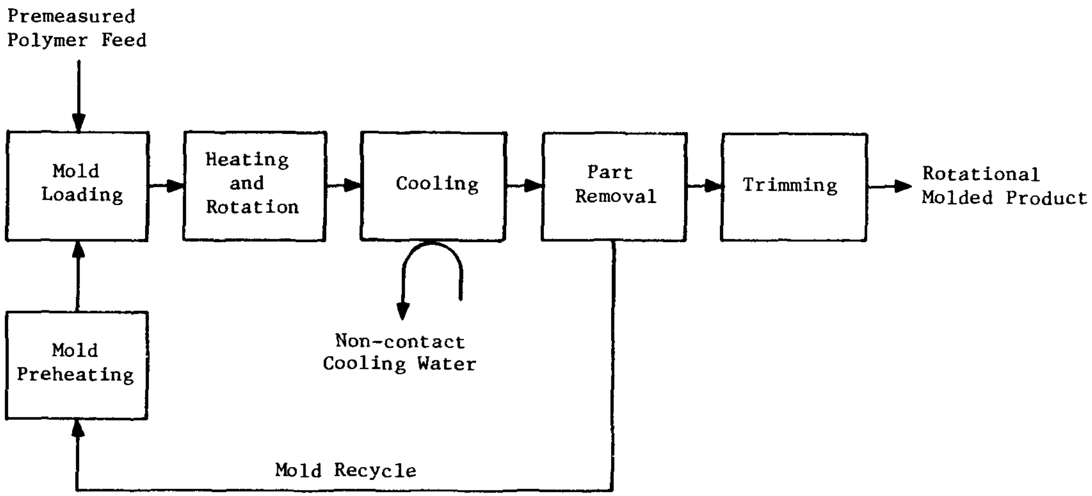


Figure IV-7

ROTATIONAL MOLDING PROCESS

Most bead foam molding processes use polystyrene or polyvinyl chloride as raw materials. Typical end products are packaging materials, flotation devices, insulation, and hot and cold containers.

A schematic of an expandable bead foam process is shown in Figure IV-8. Polystyrene beads are usually pre-expanded to a bulk density close to the desired product bulk density prior to further processing. Pre-expansion equipment commonly consists of a steam chamber with baffles and mechanical agitation. Condensate is discharged from the steam chamber.

The pre-expanded beads are fed to a preheated split cavity mold. Steam is supplied to the mold cavity through small holes in the mold. The heat supplied by the steam causes the impregnated beads to expand to fill the confines of the mold. The soft and molten bead skins fuse together to form a single polymer mass. Condensed steam (contact heating water) is discharged from the mold cavity.

Water is generally not used for the direct contact cooling of foam products. Non-contact cooling water is used to cool extruder and mold assemblies. However, the steam that heats the product becomes a source of contact heating process water when condensed.

Coating and Laminating Processes

Coating and laminating processes combine polymeric materials with other materials to produce products with special properties such as chemical resistance, toughness, humidity resistance, corrosion resistance, and electrical insulation. Heat is used in both processes. Lamination also requires high pressures.

Coating.

Polymer coatings are applied in the form of a melt, liquid, or finely divided powder onto numerous substrates including other plastic objects, metal, wood, paper, fabric, leather, glass, concrete, and ceramics. Both thermoplastic and thermoset resins can be coated. The most common resins used are: acrylic resins, epoxy resins, fluoroplastics, amino resins, polyesters, low density polyethylene, polypropylene, and polyvinyl chloride. Typical products from coating processes include automotive parts, appliance parts, electrical supplies, furniture, and housewares.

There are four types of coating processes: plastisol coating, powder coating, spread coating, and extrusion coating. A flow diagram representing plastisol and powder coating is presented in Figure IV-9. Spread coating is illustrated in Figure IV-10. A flow diagram of the extrusion coating process is presented in Figure IV-11.

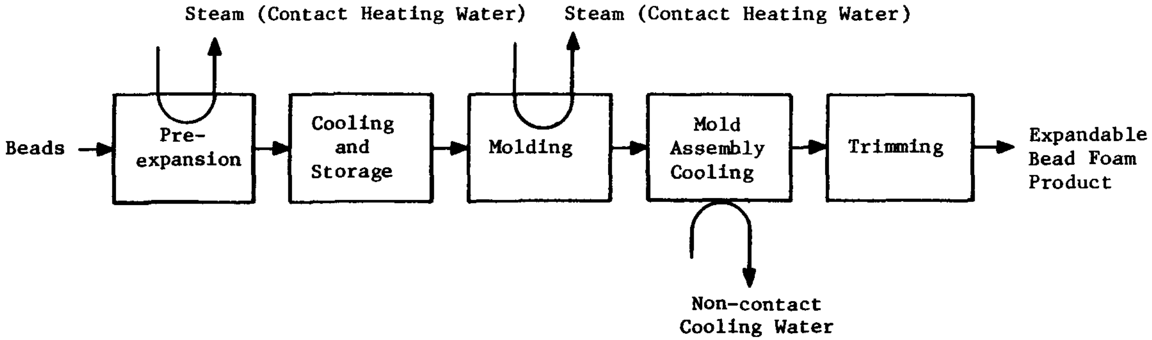


Figure IV-8

EXPANDABLE BEAD FOAM MOLDING PROCESS

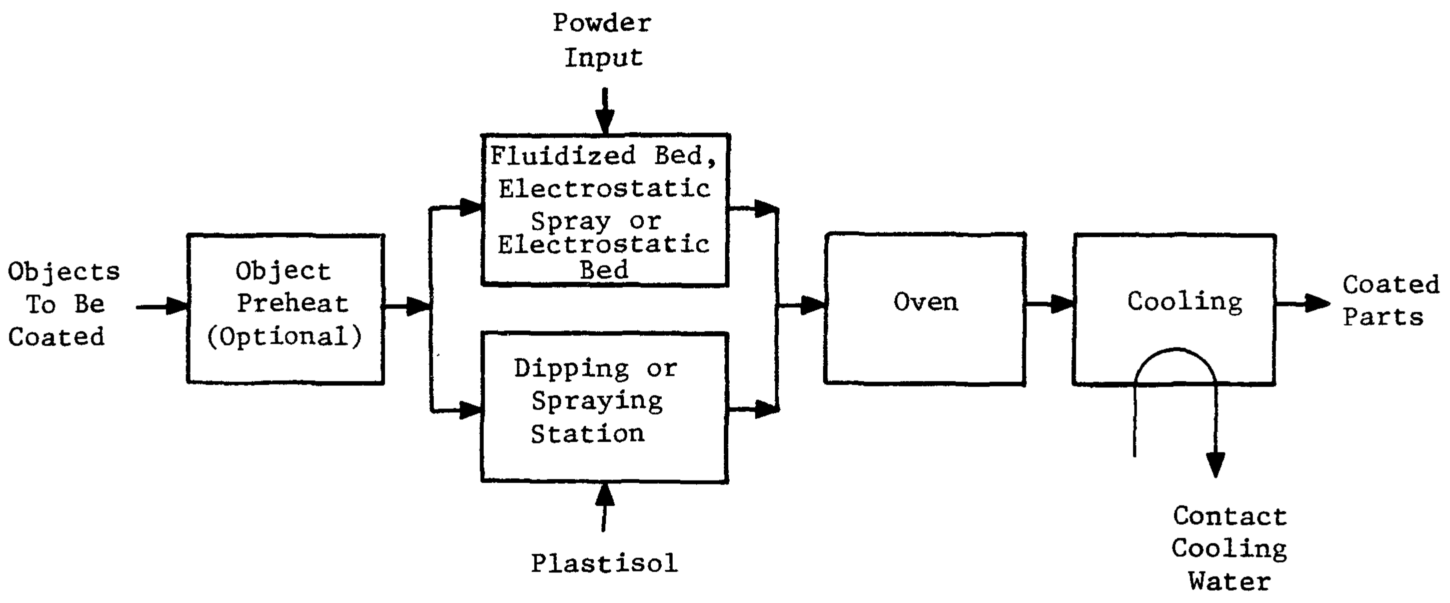


Figure IV-9

PLASTISOL AND POWDER COATING PROCESSES

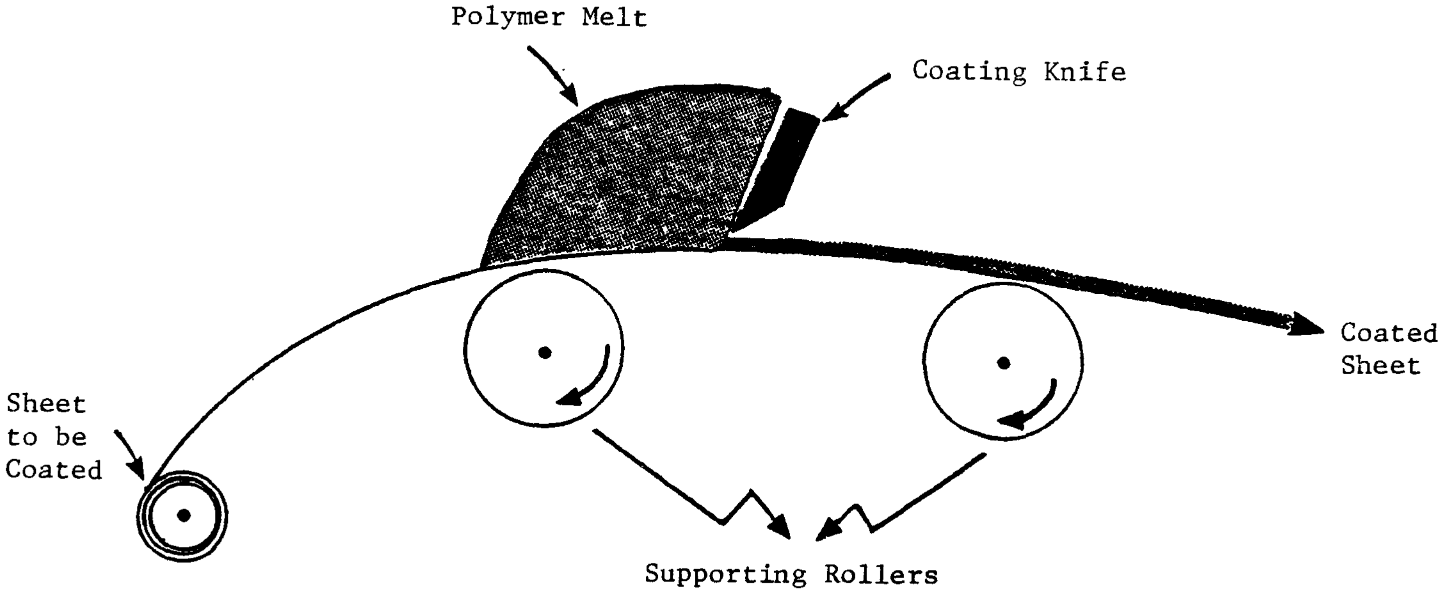


Figure IV-10

SPREAD COATING PROCESS

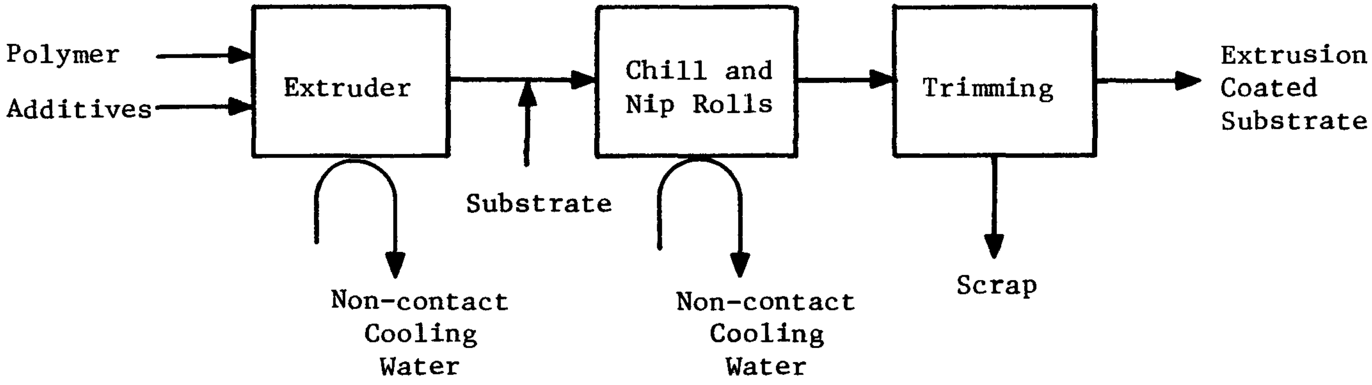


Figure IV-11

EXTRUSION COATING PROCESS

Plastisol Coating. Plastisol coating involves the use of a liquid plastisol that consists of fine particles of polyvinyl chloride (PVC) dispersed in plasticizers. Typical plastisol coated products include housewares and outdoor furniture. The plastisol is contained in a vat into which the object to be coated is dipped. The objects are sometimes preheated to assure sufficient polymer fusion. The dipped parts then pass through an oven to complete fusion. Some product applications require that the plastisol be applied to the object surface with a spray gun or a brush. Whether sprayed or brushed, the coated object must subsequently be heated in an oven to fuse the polymer coat. The dip coating process is very similar to a dip casting process. The difference lies in the nature of the mold. In dip casting, the plastic part, such as a glove, is stripped from the mold and the mold is used to form another part. In dip coating, the mold is actually part of the finished product, such as a metal patio chair that is dip coated with plastic.

Powder Coating. Powder coating involves the use of a homogeneous blend of thermoset or thermoplastic resin, pigments, fillers, and additives in the form of a dry, fine, flour-like substance. Three basic powder coating methods exist: fluidized bed, electrostatic spray, and electrostatic bed. Fluidized bed coating involves creating a fluidized bed of thermoplastic or thermoset resin powder by the flow of air through a porous plate at the bottom of a tank. Objects to be coated are preheated and are then dipped into the fluidized bed. When the resin particles touch the surface of the hot object they melt and fuse. Electrostatic spraying is performed by charging the polymer powder either positively or negatively so that it is attracted to a grounded or oppositely charged object. The electrostatic bed process is a combination of the fluidized bed and electrostatic spray methods. Electrodes located in the porous plate at the bottom of the fluidized bed tank transfer a charge to the powder particles which are then attracted to the grounded object to be coated.

Spread Coating. Knife or spread coating uses a long blade or knife to spread the molten thermoplastic polymer coating on a moving substrate. Thermoplastics such as low density polyethylene, polyvinyl chloride, and polypropylene are used to coat flexible materials such as fabric.

Extrusion Coating. Extrusion coating involves the extrusion of a thin film of polymer onto a moving substrate, which is usually either a paper web, plastic sheet, or paper sheet. Polymers such as low density polyethylene, polypropylene, and polyethylene terephthalate are used in extrusion coating processes to produce the coatings.

Laminating. Laminate structures are formed from layers of resins and fillers bonded together. Thermosetting resins are the only resin types commercially used for laminating. Typical laminating resins include alkyd resins, epoxy resins, melamine formaldehyde, and phenolic resins. Paper, cloth, glass fiber, and glass cloth are typically used as the reinforcing substrate. Lamination processes are used to produce decorative panels and items requiring good electrical insulating properties. Process water is typically not used in lamination processes.

Laminating processes can be classified into three types: lamination of flat sheets, lamination of rods and tubes, and continuous lamination. A schematic of the laminating process is shown in Figure IV-12.

Flat Sheet Lamination. Flat laminate sheets are produced by impregnating the base sheets with liquid thermosetting resin. Phenolics, melamines, alkyd, polyester, and epoxies are all commonly used. The correct number of sheets for the specific application are placed together with the resin between two platens of a hydraulic laminating press. The hydraulic press closes and pressure and heat are applied to the layers. The thermoset resin flows through the filler sheets and cures. After the sheets have sufficiently cured, the platens are allowed to cool, the press is opened, and the sheets removed.

Rod and Tube Lamination. Laminate rods and tubes are produced from filler webs impregnated with thermoset resin. Solid rods are made by winding the impregnated filler web around a very thin rod (mandrel) which is then withdrawn. The preform rods are then placed in a compression mold where heat and pressure are applied. In some operations the rods are placed in an oven and allowed to cure without pressure over a long period of time, typically 12 to 24 hours. In making a tube, the mandrel is left in during the compression molding step.

Continuous Lamination. Continuous lamination processes are used to produce large volumes of structural grade sheets for use as residential and industrial panels. Polyester resins are most commonly used in the continuous lamination process along with chopped glass fibers. Continuous lamination is performed by combining the resins and reinforcements between two moving carrier films. The films are pulled through a set of squeeze rolls to eliminate entrapped air. The laminate cures in an oven after which the carrier film is stripped from the newly formed laminate. Figure IV-13 depicts the continuous lamination process.

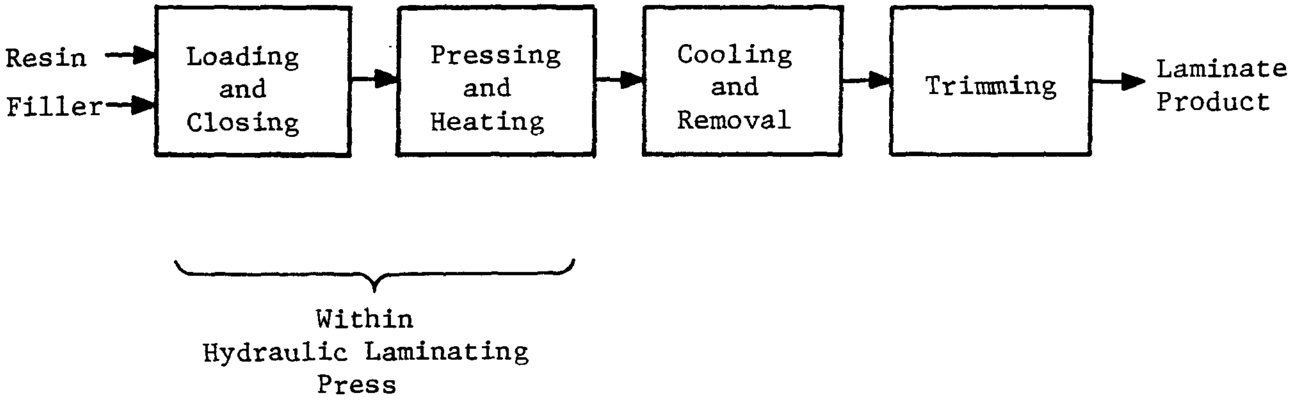


Figure IV-12

LAMINATING PROCESS

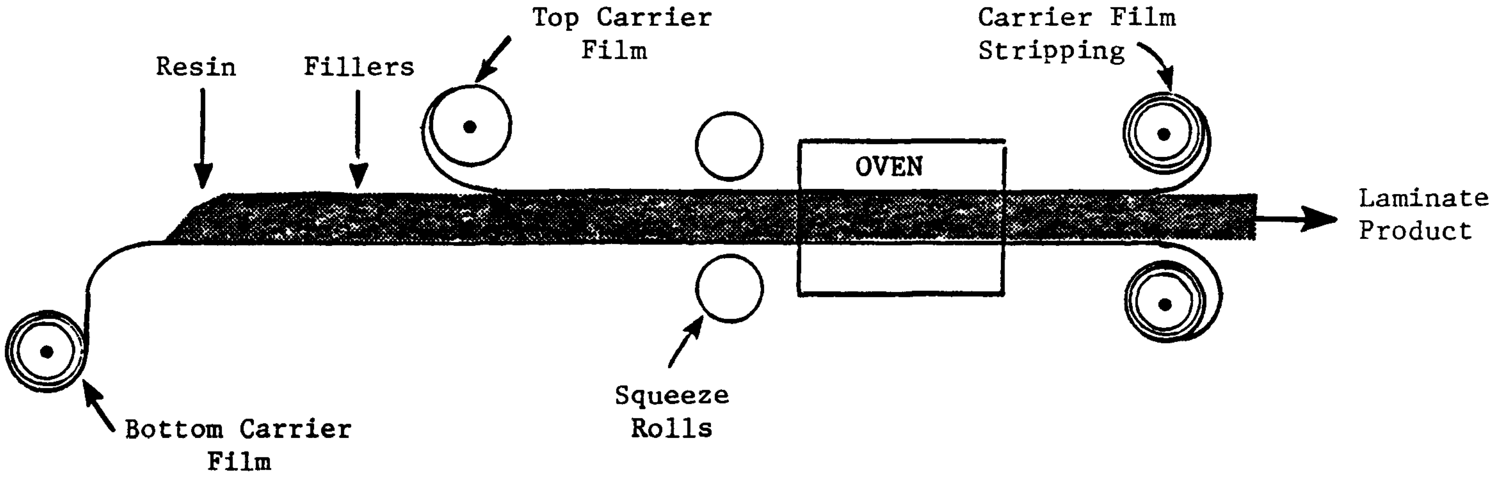


Figure IV-13

CONTINUOUS LAMINATION PROCESS

Thermoforming Processes

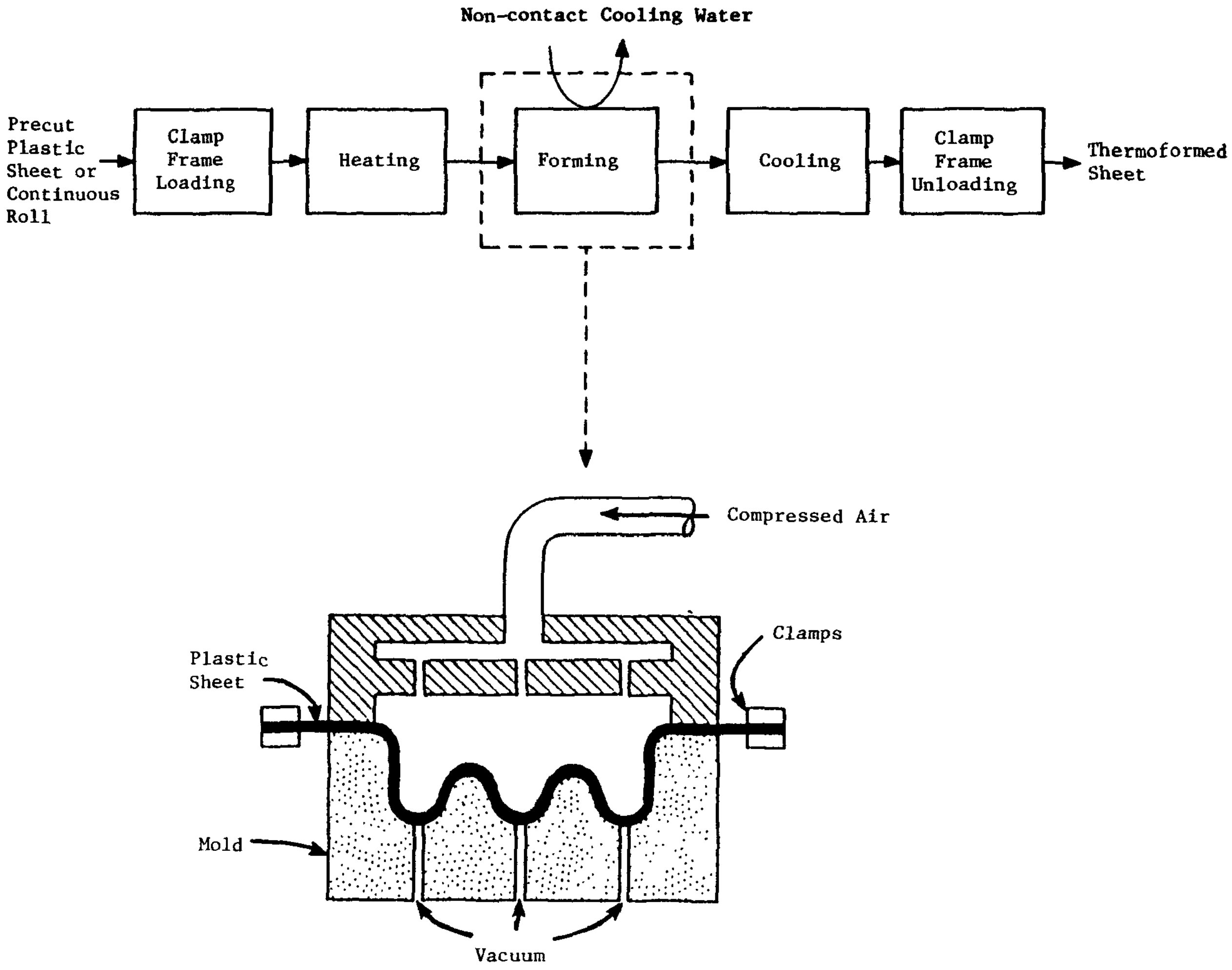
Thermoforming processes involve the heating of thermoplastic sheet or film to a pliable state and forcing it around the contours of a mold. Vacuum, air pressure, or mechanical force are employed to aid in the sheet forming. The input for thermoforming processes is foam sheet or film produced by extrusion, calendering, or casting processes. Sheet and film can be laminated or printed prior to thermoforming.

A wide variety of sheet and film plastic is suitable for thermoforming. Sheet and film for thermoforming is typically made from acrylic, acrylonitrile-butadiene-styrene, polycarbonate, polyethylenes, polypropylene, polystyrene, and polyvinyl chloride. Typical thermoformed products include appliance parts, automotive parts, lighting fixtures, packaging, and signs and displays.

A schematic of the thermoforming processes is shown in Figure IV-14. Plastic sheet is clamped into a frame prior to thermoforming to provide support for the plastic material throughout the entire process. The plastic sheet is uniformly heated before being formed to be certain of uniform stretch during forming. One of three heating methods are usually used: radiant heating, convection heating, and conduction heating, with radiant heating being the most commonly used method. When sufficiently heated, the sheet is formed into the desired shape by one of three forming processes: (1) vacuum forming, (2) pressure forming, and (3) matched mold forming.

Vacuum Forming. Vacuum forming is the most versatile and most commonly used process for thermoforming. The heated sheet is placed directly above a concave mold and pressure is used to seal the plastic material to the upper mold edge. Vacuum is applied from beneath the mold through small holes in the mold cavity forcing the sheet against the mold contours. Although many variations of vacuum forming exist, they all employ a vacuum applied from below the mold surface. Common variations are termed drape forming, snap-back forming, and plug assist vacuum forming.

Pressure Forming. Pressure forming involves the use of air pressure to force the softened plastic sheet against the mold. A sheet of plastic is clamped over a pressure box containing a concave mold and is heated. The sheet is then covered and compressed air is blown through openings in the cover. The air pressure forces the sheet against the mold contours. A variation of pressure forming termed free blowing is used to produce bubble-like forms.



Source: Adapted from Masson, D. (ed). The Study of the Plastics Industry. 1973.

Figure IV-14

THERMOFORMING PROCESS

Matched Mold Forming. Matched mold forming is used to produce products requiring excellent reproduction detail. The heated sheet material is placed between convex and concave mold halves. The halves are brought together, thereby forming the sheet into the mold shape.

Most thermoforming processes use non-contact cooling water. However, in some instances, the thermoformed product may be spray cooled with water.

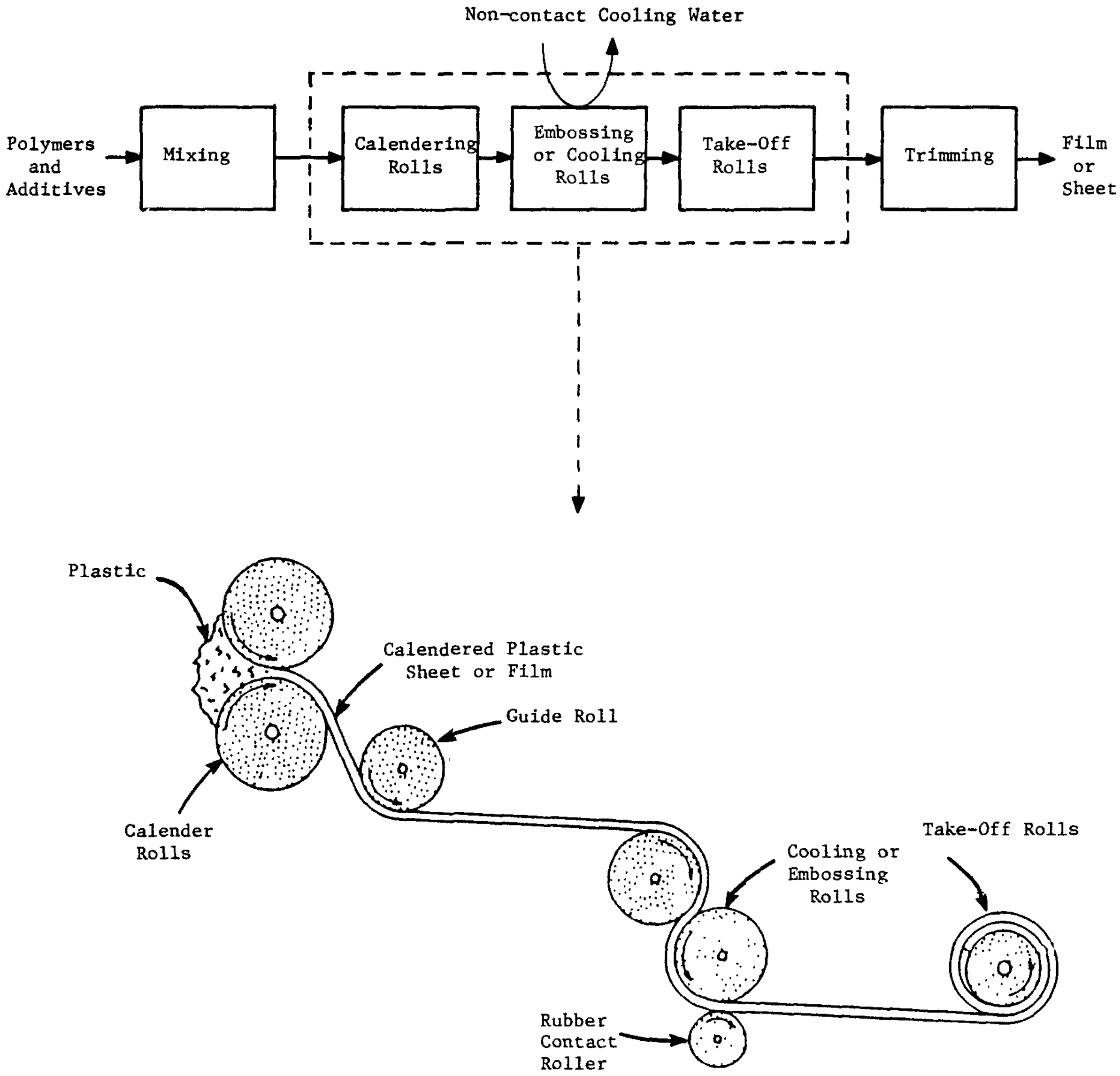
Calendering Processes

Calendering is widely used in the plastics molding and forming category to produce uniform thickness film and sheet at high production rates. Calendering processes squeeze pliable thermoplastic between a series of rotating rolls to produce the polymer film and sheet, to emboss sheet and film, to perform compounding and to coat textiles and papers.

Flexible and rigid polyvinyl chloride compounds are the most commonly used input materials for the manufacture of calendered products. Typical products include building and construction supplies, packaging supplies, and consumer and institutional goods such as toys, seats, and coverings. Acrylonitrile-butadiene-styrene, polyethylene, and polystyrene are also used to produce various films.

A schematic of a calendering process is shown in Figure IV-15. Calendering processes generally consist of five units: mixing, calendering, cooling, take-off, and trimming. The thermoplastic resin and the appropriate additives are transferred from storage facilities through a sieve to a high shear mixer or mill where heat is supplied to soften and blend the polymer mix. The polymer is then fed to the calendering unit, which usually consists of three to five heated cast iron rolls that squeeze the softened polymer into a sheet or film of desired width and thickness. The arrangement of the calender rolls is determined by the product requirements as are the number of rolls and the roll spacings. The clearance between rolls is progressively decreased to slowly reduce the thickness and increase the width of the sheet or film. Most roll arrangements are adjustable to allow versatility in production methods. Newly calendered sheet is cooled by feeding the sheet or film through a series of two to ten cooling rolls cooled with non-contact cooling water. The take-off rolls feed the sheet and film to edge trimming operations, further finishing operations, or roll-up.

Calendering is also used to coat materials such as paper and fabric with a polymer. The process is similar to that described above except that fabric or paper is fed into the calendering



Source: Adapted from Masson, D. (ed). The Study of the Plastics Industry. 1973.

Figure IV-15

CALENDERING PROCESS

rolls as the plastic film is formed. The plastic and fabric are tightly bonded together by the heat and force of the rolls and emerge from the cooling rolls as a single composite sheet.

Most calendering processes use non-contact water to cool the cooling rolls. Contact cooling water may be sprayed on both the plastic sheet and the rubber contact roller as the plastic sheet passes through the embossing rollers. Some calendering processes may also use contact cooling water to cool the newly formed sheet or film.

Casting Processes

In the plastics molding and forming industry, the term casting is used rather loosely to describe a wide variety of processes. Casting involves liquid plastic materials allowed to cure at atmospheric pressure in a mold or on a mold surface.

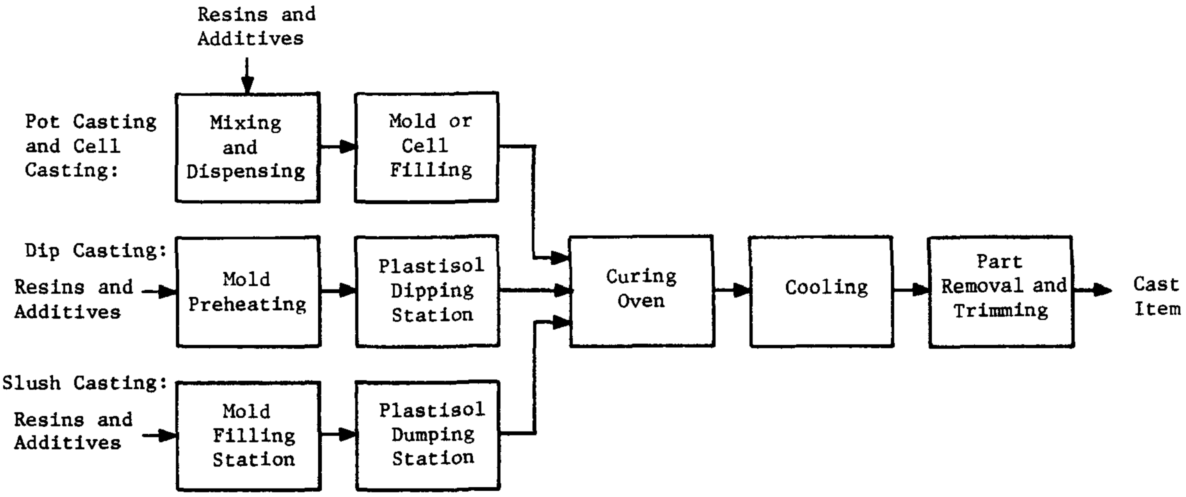
Both thermoplastic and thermoset resins can be used in casting processes. Commonly cast thermoplastics include acrylics, nylons, and polyvinyl chlorides. Commonly cast thermosets include epoxy resins, polyesters, phenolics, and polyurethanes.

Fillers are often used in casting processes to produce reinforced plastic products such as boats and recreational vehicles, troughs, ducts, bins and tubs, as well as preforms for use in the compression molding of reinforced products.

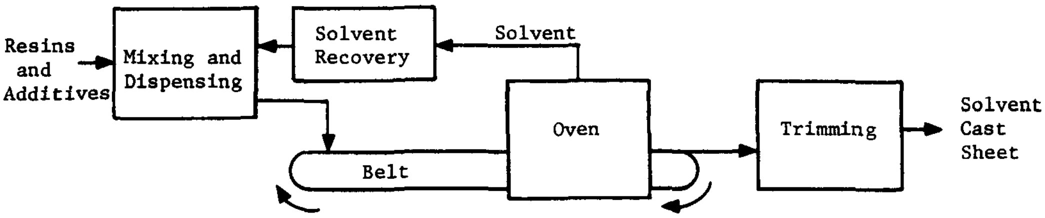
There are seven types of casting processes: pot casting, slush casting, dip casting, cell casting, chilled film casting, solvent casting, and continuous casting. A schematic of pot, slush and dip, cell, solvent, and continuous casting processes is shown in Figure IV-16. The chilled film casting process is illustrated in Figure IV-17.

Pot Casting. Pot casting is the simplest form of casting and is used to produce a wide variety of products. Polymers used in pot casting include acrylic, alkyl resins, diallyl phthalate, epoxy, nylon, phenolic, polyester, polyurethane, and silicone elastomer. During pot casting a liquid polymer or a monomer solution is poured into an open mold where is it allowed to cure. The pot cast part is cured by the addition of heat in an oven, exothermically by means of a catalyst, or by a combination of both methods. Typical pot cast products include novelties, plaques, knobs, embedments, electrical encapsulations, optical products, bearings, gears, jewelry, billiard balls, seals and gaskets, housewares, and furniture parts.

Pot, Cell, Dip, and Slush Casting



Solvent Casting



Continuous Casting

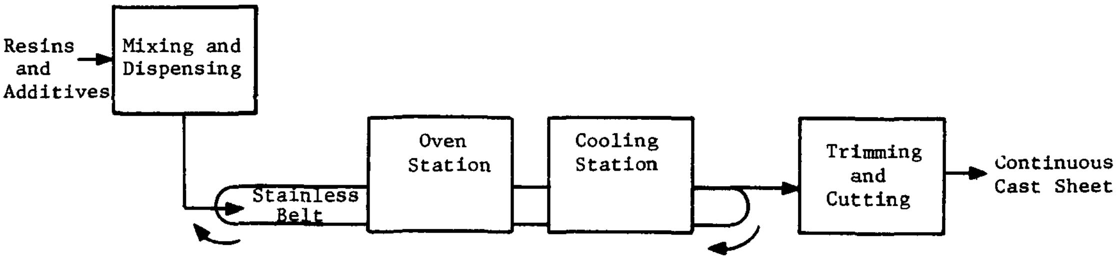


Figure IV-16

CASTING PROCESSES

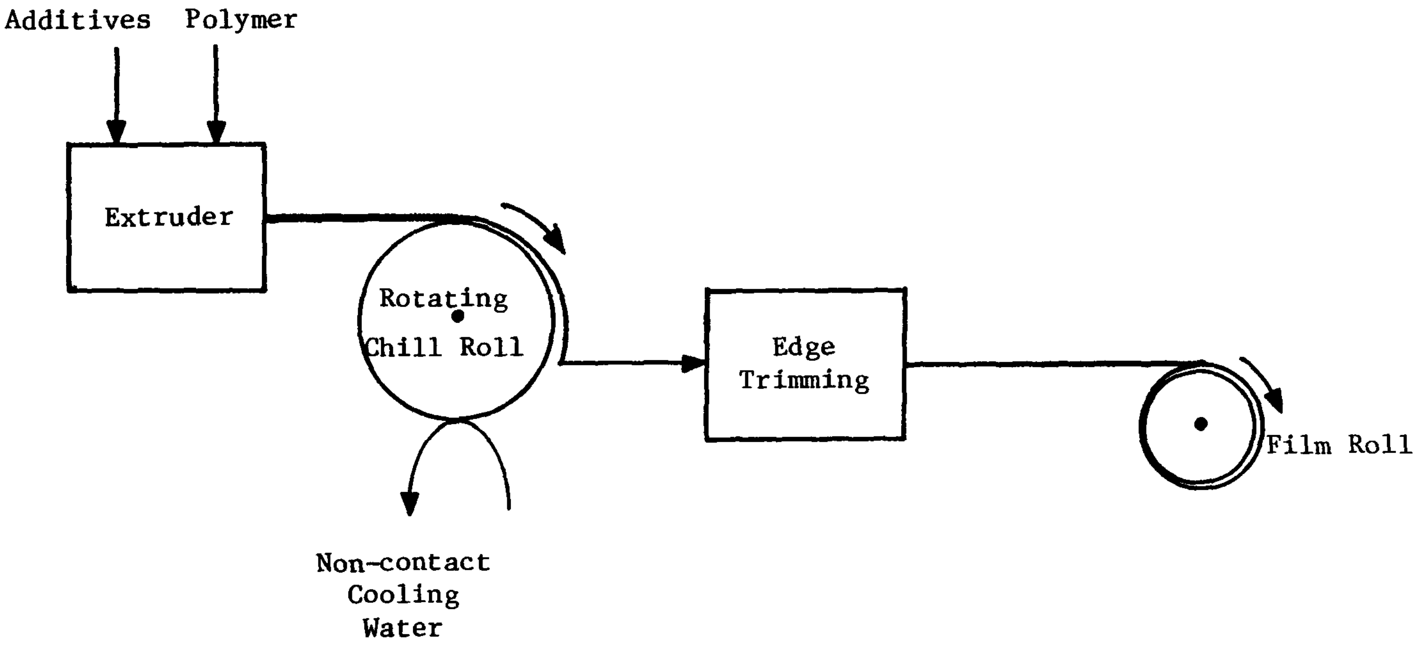


Figure IV-17

CHILLED FILM CASTING PROCESS

Slush Casting and Dip Casting. Slush casting involves the use of liquid plastisol (fine particle polyvinyl chloride dispersed in plasticizers such as dioctyl phthalate). These plastisols are viscous at room temperature. A measured amount of plastisol is poured into a hollow mold that has been preheated. The mold is rotated quickly to cover all inside surfaces and after a specific period of time, excess plastisol is poured out into a storage vat for future reuse. The thickness of the hollow part is determined by the amount of time the plastisol remains in the mold. The mold is then placed in an oven and is heated for several minutes to complete fusion. Typical slush cast products include housewares, novelties, doll heads, fish lures, and toys.

In dip casting, a mold is preheated and dipped into a liquid plastisol. A polymer coating fuses around the mold during immersion. The coated mold is then placed in an oven to complete fusion. Typical dip cast products include novelties, boots, gloves, coin purses, and eye glass cases.

Cell Casting. Cell casting is used to produce sheet, tubes, and rods. Acrylic sheet is most commonly cell cast. A premeasured amount of liquid acrylic, consisting of a small amount of polymer in a monomer and additive solution, is poured between two sheets of polished or tempered plate glass that are slightly larger than the desired acrylic sheet product. The glass cell, which is held together by tubing and spring clips, is then placed horizontally in an oven for curing.

Chilled Film Casting. Chilled film casting is a casting process used to produce non-oriented, thin, polymer films. Thermoplastic materials such as polypropylene homopolymer, propylene-ethylene copolymer, and low density polyethylene are most commonly used to produce film. The most common form of chilled film casting is termed chill roll casting. In chill roll casting, the formulated polymer is extruded through a slot die onto a rotating, chilled, polished roll. The movement of the roll draws the molten resin away from the die without significantly stretching or orienting the film. The extrudate solidifies into a film as it passes over the chilled roll surface. The film is trimmed as necessary and wound onto rolls. Chill casting processes produce high clarity film products. Process water is not used during chill roll casting.

A less commonly used film casting process is termed tubular water bath casting. A thin-walled vertical tube of formulated polymer is extruded downward from a rotating circular die over a water cooled mandrel. The tube is quenched in contact cooling water and split open to form a film. The film is then trimmed and wound on rolls.

Solvent Casting. Solvent casting, often referred to as solution casting, is used for the production of film and sheet. Polyvinyl chloride (PVC) organosols are the most commonly used polymers for this process. Organosols are formed by dispersing finely powdered PVC in plasticizer and organic solvents. The solution is poured onto a rotating drum or an endless belt that passes through an oven. The solvent is evaporated in the oven in carefully programmed heat zones and a relatively solvent free polymer film leaves the oven.

Continuous Casting. Continuous casting processes produce thin continuous acrylic sheet. They are very similar to cell casting processes except that the liquid acrylic is cured between two highly polished moving stainless steel belts. The acrylic, trapped between the stainless belts, travels through the oven and air cooling stations.

Water may be used for the direct contact cooling of cast products. Direct contact cooling water sprays can be used in slush casting and in dip casting processes and in some pot casting processes. During tubular water bath casting, direct contact cooling water is used during the product quenching step.

Foam Processes

Foamed plastics (often called cellular or expanded plastics) are made by adding a blowing agent to thermoplastics or thermosets to form a spongelike material. Blowing agents are either added to the input material and vaporize due to heat or are generated as a by-product of a cure reaction. Plastic foam products have wide commercial use for flotation devices, packaging, cushioning, and insulation. Plastic foams can be either rigid or flexible. Foamed plastic products can be classified into one of three types: extruded thermoplastic foam, structural foam, and multicomponent thermoset foam. The production of extruded thermoplastic foams is a variation of the extrusion process where either dry chemicals that foam when heated are included in the resin feed or a solvent blowing agent is injected into the polymer melt at the extrusion die. Structural foam molding is a variation of the injection molding process where chemical blowing agents or injected gases form bubbles in the molded product. Multicomponent thermoset foams are formed in a carefully controlled reaction injection molding (RIM) process where blowing agents are either generated as a by-product of the chemical reaction that takes place in the mold of a RIM process or added with the input materials and vaporized by the heat of reaction. Contact cooling water is generally not used during the molding and forming of these foamed products.

Cleaning Processes

Parts produced by the various molding and forming processes may require cleaning to become useful end products.

Cleaning. Cleaning processes wash the surfaces of plastic products to remove residual mold release agents, processing chemicals, and other matter prior to finishing, shipping, or further processing. Cleaning is generally divided into two segments; a detergent wash cycle and a rinse cycle for the removal of detergents and other foreign matter. Generally, the level of sophistication of washing processes varies with the type of product being formed and the manufacturing steps that follow. Small novelty items requiring cleaning may simply be dunked and agitated in a bucket with the bucket dumped periodically. Larger items can be cleaned in the same manner in a tank. At the large manufacturing facilities, custom designed washing equipment may be employed. Two types of automated cleaning processes are used. In the first type, a batch of plastic products is loaded into a washing machine that operates cyclically. In the first cycle, plastic products are washed with detergent water; in subsequent cycles, the plastic products are rinsed. When the wash-rinse cycle is complete, the plastic products are removed from the machine and the whole process is repeated with a new batch of products. The other type of automated washing process is a continuous staged process. The products to be cleaned are conveyed through a detergent wash stage and then through a rinse stage.

Depending on the degree of cleaning required for a final application or further processing, the cleaning process may actually employ several rinse cycles or stages. For instance, cleaning processes used to prepare surfaces for painting generally include a deionized water rinse as a final step.

Shaping equipment surfaces that contact the plastic product, such as molds and mandrels, may also be washed in a cleaning process.

Finishing Processes

Products produced by the various molding and forming processes may also require finishing to render the final product useful.

Finishing. There are three general finishing processes: machining, decorating, and assembling. Machining is used to drill, cut, mill, and otherwise shape products to match final product specifications. Decorative finishes are applied to plastic parts by a variety of methods including painting, printing, hot stamping, and vacuum metallizing. Assembling involves joining two or more plastic parts by methods such as solvent welding, ultrasonic welding, and electronic heat sealing. Process water is often used in finishing processes as a lubricant and carrier of waste particulates generated by machining processes. Decorating and assembling are dry operations.

SECTION V

SUBCATEGORIZATION

BASIS FOR SUBCATEGORIZATION SCHEME

In developing the final regulation for the plastics molding and forming category, the Agency considered whether different effluent limitations guidelines and standards are appropriate for different segments of the industry. The Act allows EPA to consider a number of factors to determine if subcategorization is needed. These factors are:

1. raw materials;
2. production processes;
3. products;
4. size and age of plants;
5. geographic location;
6. type of water use; and
7. wastewater characteristics.

The Agency determined whether any of these individual factors identified a need to subcategorize the PM&F category. The Agency also evaluated the relationship between different factors to identify a need for subcategorization. A discussion of each factor is presented below. After considering all these factors, the Agency determined that the plastics molding and forming category is most appropriately regulated using three subcategories.

FACTORS CONSIDERED

Raw Materials

The raw materials used in the plastics molding and forming category can be classified as:

- plastics and resins;
- chemical additives; and
- processing aids.

The type and combination of raw materials used in plastics molding and forming are highly dependent on the production process used and the end products desired. Plastics molders and formers can use many different raw material combinations to produce different end products at one production plant over a given period of time. Many different raw materials may also be used in any one type of PM&F process.

The concentration of pollutants in PM&F process waters varies because of the raw materials used. However, the types of pollutants in these process waters are similar regardless of the material processed. This is illustrated by reviewing the sampling data base presented in Appendix A. For cleaning process waters, the priority pollutant phenol was found in concentrations ranging from 0.002 mg/l to 6.0 mg/l in eight of the 13 cleaning water processes sampled. The 6.0 mg/l concentration was found in process water used to clean the surfaces of equipment that process phenolic resin. The 0.002 mg/l was found in process water used to wash and rinse a polyurethane product. The range in phenol concentrations for those two processes can be explained by the raw material processed. However, the range in pollutant concentration does not prevent both process waters from being treated in the same type of treatment technology. This situtation is also illustrated in the data bases for the contact cooling and heating water processes and for the finishing water processes. Therefore, a subcategorization scheme based on raw materials is not needed to ensure equitable effluent limitations guidelines and standards for the PM&F category. Further, due to the proprietary nature of the raw material combinations and the varying requirements for product quality, particularly when different raw materials are processed in the same PM&F process, the Agency believes that a subcategorization scheme based on raw materials is not feasible for the PM&F category.

Production Processes

There are nine different generic production processes used in the plastics molding and forming category. They are:

1. extrusion;
2. molding;
3. coating and laminating;
4. thermoforming;
5. calendering;
6. casting;
7. foaming;
8. cleaning; and
9. finishing.

Each of the above processes may use process water (i.e., water that contacts the plastic product). Process water is used in the first seven processes to cool or heat plastic materials and plastic products. Process water is used in cleaning processes to clean surfaces of plastic products and to clean shaping equipment surfaces; it is used in finishing processes to finish plastic products.

As indicated in the section on raw materials, sampling data presented in Appendix A indicate that the pollutants found in process waters for PM&F processes that cool or heat a plastic product (i.e., the first seven processes listed above) are similar even though the pollutant concentrations may vary. Therefore, the Agency believes that there is nothing about the different contact cooling and heating processes that significantly affects the development of equitable effluent limitations guidelines for those processes. For this reason, PM&F contact cooling and heating water processes can be addressed as a group with respect to effluent limitations guidelines and standards.

Sampling data for cleaning water processes and finishing water processes indicate that the pollutants in those two process waters are different. Those data also indicate that the pollutants in contact cooling and heating waters are different from the pollutants in either cleaning process waters or finishing process waters. For these reasons, the Agency considered three types of PM&F processes (i.e., contact cooling and heating water processes, cleaning water processes, and finishing water processes) further as the basis to subcategorize the PM&F category so that equitable effluent limitations guidelines and standards could be developed.

Products Produced

An extremely wide range of products are produced in the plastics molding and forming category. The products can be classified according to the following types:

1. packaging materials;
2. building and construction components;
3. consumer and institutional products;
4. electrical and electronics products;
5. appliances;
6. transportation products;
7. furniture;
8. industrial equipment; and
9. intermediate products.

Products within any given product type can generally be manufactured from several different plastic materials and in several different production processes. In addition, any given plant may produce a wide range of products falling into many of the above product types. The amount and type of pollutants discharged by those processes are not directly related to the type of product produced. Thus, a subcategorization scheme based on product type is not needed to ensure the development of equitable effluent limitations guidelines and standards for the PM&F category.

Size and Age of Plants

The number of employees and amount of production can be used to measure relative sizes of PM&F plants. However, neither factor provides an adequate basis for subcategorization.

The amount of wastewater discharged and the types of pollutants in the wastewater are largely independent of the number of plant employees. Variations in staff occur for many reasons including shift differences, the need for clerical and administrative support, the need for maintenance support, efficiency of plant operations, and market fluctuations. Due to these and other factors, the number of employees is constantly fluctuating. The Agency found no correlation between the number of employees at a PM&F plant and the number and range of concentrations of pollutants in wastewater discharged from PM&F processes at a plant. Therefore, a subcategorization scheme based on the number of employees at a plant is not appropriate for the PM&F category.

While plant production can be used to approximate the mass of pollutants generated, the Agency has determined that it should not be used to establish different effluent limitations guidelines and standards for the plastics molding and forming category for the following reasons:

1. The types of PM&F processes used and the characteristics of the wastewater discharged from those processes are not dependent on the total plant production.

2. While the amount of production affects the total mass of pollutants discharged, it has little effect on the types and range of concentrations of pollutants found in the wastewater. Therefore, there is little, if any, difference between the type of treatment technology required at small and large PM&F plants where process water is treated and discharged.

The plastics molding and forming industry is a relatively new industry that developed following the development of the polymer and resins formulating industry. To remain competitive in an industry that has steadily made technological improvements over the past 30 years, PM&F plants have been continually modernized. Thus, because most PM&F plants were built in the same general time frame and are continually modernized, neither plant age nor equipment age is a significant factor that requires subcategorization to ensure equitable effluent limitations guidelines and standards.

Geographic Location

Plastics molding and forming plants are not limited to any one geographical location and are generally located near distribution and sales centers so that the finished products need not be transported over long distances. A large percentage of molding and forming plants are located in the four geographical clusters of (1) New Jersey, New York, and Pennsylvania; (2) Illinois, Indiana, Michigan, and Ohio; (3) Louisiana, Oklahoma, and Texas; and (4) California and Washington.

There are no specific geographical factors that significantly affect water use at PM&F plants or characteristics of PM&F process waters. The physical space required for the treatment systems evaluated for the PM&F regulation is small compared to the overall plant size. Therefore, there are no consequences from the construction and operation of a wastewater treatment system peculiar to the different geographical areas. For these reasons, the Agency believes there is no need to subcategorize the PM&F category based on geographic location.

Types of Water Use

Results of the questionnaire surveys and the sampling programs for the PM&F regulation indicate that there are basically three types of process water used by processes in the PM&F category. They are:

1. contact cooling and heating water,
2. cleaning water, and
3. finishing water.

Contact cooling and heating water is used to either cool or heat plastic materials or plastic products. Water can be sprayed onto a product or the product can be drawn through a water bath. In either case, the water is used for heat transfer.

Cleaning water is used to clean the surfaces of plastic products or to clean shaping equipment surfaces that are or have been in contact with the plastic product. It includes water used in the washing and rinsing cycles of a cleaning process.

Finishing water is used to finish plastic products. It includes water used either to carry away waste plastic materials during a finishing operation or to lubricate a plastic product during finishing.

Sampling data indicate that the type and concentration of pollutants in PM&F process waters vary depending on how process water is used. Therefore, the development of equitable effluent limitations guidelines and standards for the PM&F category may be influenced by how the process water is used. For this reason, the Agency gave further consideration to type of water used as the basis for the PM&F subcategorization scheme.

Wastewater Characteristics

Results of the sampling programs for this regulation indicate that contact cooling and heating waters, cleaning waters, and finishing waters have different pollutant characteristics. Only one pollutant (i.e., bis(2-ethylhexyl) phthalate) was found in a treatable concentration in contact cooling and heating waters. Cleaning waters have treatable concentrations of three conventional pollutants, three nonconventional pollutants, and two priority toxic pollutants. Finishing waters have treatable concentrations of one conventional pollutant (i.e., TSS) and three priority pollutants. These different pollutants severely impact the development of equitable effluent limitations guidelines and standards for the PM&F category. Therefore, wastewater characteristics were considered further as the basis for the PM&F subcategorization scheme.

SELECTED SUBCATEGORIZATION SCHEME

The subcategorization scheme for the PM&F category is based on three types of production processes, water use, and wastewater characteristics. The three types of production processes are contact cooling and heating water processes, cleaning water processes, and finishing water processes. The water use (i.e., heat transfer, cleaning, or finishing) for those three types of processes influence the wastewater characteristics of the process water. All three factors influence the development of equitable effluent limitations guidelines and standards for the PM&F category.

The three subcategories for the PM&F category are:

1. contact cooling and heating water subcategory,
2. cleaning water subcategory, and
3. finishing water subcategory.

The contact cooling and heating water subcategory includes PM&F processes in which process water contacts plastic materials for the purpose of heat transfer. Processes that use process water to clean the surfaces of plastic products or to clean shaping equipment surfaces that are or have been in contact with the plastic product are included in the cleaning water subcategory. The finishing water subcategory includes PM&F processes that use process water during the finishing operation.

One advantage of this subcategorization scheme is that plants can easily identify the type of water used in their PM&F processes. Having only three subcategories should also make it less complicated for the permit writer to write permits for PM&F plants.

APPLICABILITY

The PM&F effluent limitations guidelines and standards apply to processes that blend, mold, form, or otherwise process intermediate or final plastic products and that discharge process water. Some molding and forming processes (e.g., extrusion and pelletizing) are used by plastic resin manufacturers to process crude intermediate plastic material. For the purpose of the PM&F regulation, plastic molding and forming processes used by plastic resin manufacturers to process crude intermediate plastic materials for shipment off-site are excluded from the PM&F regulation and regulated under the organic chemicals, plastics, and synthetic fibers category. Plastic molding and forming processes used by plastic resin manufacturers to process crude intermediate plastic materials that are processed on-site into intermediate or final plastic products by molding and forming are controlled by the effluent limitations guidelines and standards for the PM&F category. For example, a plant may manufacture a polyurethane resin. To prepare the resin for shipment, the manufacturer may extrude the resin and then pelletize it. If the polyurethane pellet is shipped off-site, the extrusion process is subject to the effluent limitations guidelines and standards for the organic chemicals, plastics, and synthetic fibers category. If the polyurethane pellet is further processed on-site in a molding and forming process, that process and the extrusion process used to obtain the pellet are subject to the PM&F effluent limitations guidelines and standards.

In several instances, particular PM&F processes and the wastewater generated by these processes may fall within this and other industrial categories for which the Agency has established effluent limitations guidelines and standards. Thus, for the purpose of regulatory coverage, the Agency has separated each process to ensure that it is clearly subject to one set of effluent limitations guidelines and standards. Processes that coat a plastic material onto a substrate may fall within the definition of electroplating and metal finishing as defined in 40 CFR Parts 413 and 433 (see 48 FR 32485; July 15, 1983). These coating operations are excluded from the effluent limitations guidelines and standards for the electroplating and metal finishing point source category and are subject to the PM&F effluent limitations guidelines and standards.

Coating of plastic material onto a formed metal substrate is also covered by the PM&F effluent limitations guidelines and standards and is not covered by the specific metal forming effluent limitations guidelines such as those for aluminum forming (40 CFR Part 467 (48 FR 49126; October 24, 1983), copper forming (40 CFR Part 468 (48 FR 36942; August 15, 1983), and nonferrous metals forming (40 CFR Part 471 (proposed 49 FR 8112, March 5, 1984)). However, the PM&F regulation applies only to the coating process; the prior forming operations are subject to the specific metal forming regulation.

Some research and development (R&D) laboratories and technical centers produce low quantities of plastic products in PM&F processes. PM&F processes at R&D laboratories are subject to the PM&F effluent limitations guidelines and standards if they discharge process water. The PM&F regulation applies to PM&F processes that discharge process waters regardless of the mass of plastic products produced by a process. The Agency considered low production PM&F processes during the development of the final PM&F regulation because there are 24 processes in the Agency's data base with very low production rates (i.e., less than 10,000 pounds per year). Information from those processes was used with information from high production processes to characterize the PM&F category.

The PM&F regulation does not apply to wastewater generated during the reticulation of polyurethane foam. Reticulation can be done by either a chemical process or a thermal process. In the chemical process, the foam is passed through a bath of sodium hydroxide and then is quenched in a series of water baths to stop the chemical reaction. In thermal reticulation, the foam is reticulated by controlled explosions inside the foam structure. Products of combustion are removed from the foam by a vacuum pump and are absorbed in the water inside the pump. Process water used in chemical and thermal reticulation is not cooling water because it is not used for heat transfer; it is not cleaning water because it does not clean the surface of either the plastic product or the equipment that contacts the plastic product; and it is not finishing water because the process water is not used to finish a plastic product. For these reasons, the PM&F effluent limitations guidelines and standards do not apply to the processes that reticulate polyurethane foam. Those processes are addressed in the effluent limitations guidelines and standards for the organic chemicals, plastics, and synthetic fibers category. If the reticulated foam is further processed in a molding and forming process, that process is subject to the PM&F regulation.

The final regulation does not apply to processes used to produce regenerated cellulose for two reasons. First, cellulose is a natural organic material, not a "plastic material" as defined by EPA. In the final PM&F regulation, a plastic material is defined as "a synthetic organic polymer . . ." [emphasis added]. Second, the final step in the xanthate process used to regenerate cellulose is to wash the regenerated cellulose to remove dissolved salts and sulfur compounds from within the cellulose. Process water used in this final step is not cleaning water as defined in the final PM&F regulation because it cleans more than just the surface of the regenerated cellulose. For these reasons, the manufacturing process for regenerated cellulose is not subject to the PM&F regulation. It is subject to the effluent limitations guidelines and standards for the organic chemicals, plastics, and synthetic fibers category.

Similarly, the final PM&F regulation also does not apply to molding and forming operations that process regenerated cellulose because regenerated cellulose is not a plastic material as defined in the final PM&F regulation. The regulation does apply, however, to molding and forming processes that use cellulose derivatives (e.g., cellulose acetate), which are plastic materials as defined in the final PM&F regulation.

Wastewater is generated by the solvent recovery operation in the solution or solvent casting process. However, this wastewater does not result from the blending, molding, forming, or any processing of the plastic material and is not a process water. It is generated when steam condensate from the solvent casting process is distilled to recover acetone. Data from the analysis of samples of this wastewater indicate that its pollutant characteristics are different from the characteristics of PM&F process waters. In addition, the Agency estimates that only eight plants in the category generate solvent recovery wastewater. For these reasons, the Agency believes that solvent recovery wastewater is best controlled on a case-by-case basis by the permit writer or control authority. Analytical data for this type of wastewater are presented in Appendix A of this technical development document and may be used as a guide by the permit writer or control authority.

Plants in the PM&F category may have processes generating only one type of wastewater and thus fit within one subcategory. However, many plants generate contact cooling and heating water, cleaning water, and finishing water. In this instance, plants must comply with the effluent limitations guidelines and standards for each subcategory.

SECTION VI

WATER USE AND WASTEWATER CHARACTERISTICS

This section discusses the water use and wastewater discharge practices for the PM&F category and presents the wastewater treatment technologies currently used by PM&F plants. Data used to characterize PM&F process waters are also presented in this section. The data were obtained from two sources:

1. questionnaires and
2. sampling and analysis programs.

QUESTIONNAIRE DATA

From the survey data base for this project described in Section IV, statistics were developed to apply to the plastics molding and forming plants that use process water. The data base contains questionnaires from 382 plants: 175 questionnaires are from the 1979 survey and 207 questionnaires are from the 1983 survey.

The 382 questionnaires were reviewed and summarized to determine the discharge mode (i.e., direct, indirect, or zero discharge) for PM&F processes. Table VI-1 contains a distribution of the 521 wet processes reported in the questionnaires by discharge mode for the types of process waters generated. As shown in the table, 31 percent of these processes are direct dischargers, 44 percent are indirect dischargers, and 25 percent have no discharge.

Table VI-2 presents the average operating hours, average production, and the average water use and discharge rates by subcategory for the different types of dischargers. The averages were calculated by summing the data for processes within a subcategory by discharge mode and dividing by the number of processes with the discharge mode. Average water use and discharge rates are given in both liters per hour and liters per year.

Table VI-3 contains a distribution of the number of wet processes in the questionnaire data base that have no discharge by the method used to obtain no discharge.

The 382 questionnaires were also reviewed to determine the treatment technologies currently used by plants in the PM&F category. A summary of those treatment technologies is presented in Table VI-4. The 17 plants listed in the table are plants where a significant portion (i.e., 50 percent or more) of the wastewater treated is from PM&F processes. Only 10 of those plants have

Table VI-1

DISCHARGE MODE FOR WET PROCESSES IN QUESTIONNAIRE DATA BASE*

Type of Process Water	Discharge Mode							
	Direct	Percent†	Indirect	Percent†	Zero	Percent†	Total	Percent
Contact Cooling and Heating Water	140	32.7	170	39.7	118	27.6	428	100
Cleaning Water	21	29.6	47	66.2	3	4.2	71	100
Finishing Water	2	9.1	14	63.6	6	27.3	22	100
TOTAL	163	31.3	231	44.3	127	24.4	521	100

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*Based on information from 1979 and 1983 questionnaire surveys.

†Percent for type of process water.

Table VI-2

QUESTIONNAIRE DATA BASE INFORMATION*

Contact Cooling and Heating Water Processes	Average Operating Hours Per Year	Average Plastic Production (kkg/yr)	Average Process Water Use		Average Process Water Discharge	
			(l/hr)	(l/yr)	(l/hr)	(l/yr)
Direct Dischargers	5,870	6,290	26,600	178,000,000	5,450	33,000,000
Indirect Dischargers	4,610	2,480	14,500	92,800,000	3,180	18,300,000
Zero Dischargers	5,210	3,160	23,200	146,000,000	0	0
Cleaning Water Processes						
Direct Dischargers	5,790	3,150	11,800	63,500,000	3,860	30,700,000
Indirect Dischargers	3,900	1,390	10,900	41,000,000	1,780	7,670,000
Zero Dischargers	6,930	3,110	600	5,280,000	0	0
Finishing Water Processes						
Direct Dischargers	4,000	46	715	2,490,000	715	2,490,000
Indirect Dischargers	3,580	2,200	2,730	7,160,000	1,590	3,800,000
Zero Dischargers	3,540	1,670	20,200	76,600,000	0	0

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*Based on information obtained from the 1979 and 1983 questionnaire surveys.

Table VI-3

DISTRIBUTION OF NUMBER OF PROCESSES IN QUESTIONNAIRE DATA BASE WITH ZERO DISCHARGE*

Zero Discharge Method	Contact Cooling and Heating Water	Cleaning Water	Finishing Water
100 Percent Recycle	83	0	3
Ponded for Evaporation	5	0	1
Septic Tank With Leach Field	10	2	0
Evaporation From Process Equipment	10	0	1
Land Application	9	0	0
Contract Haul	1	1	1
TOTAL	118	3	6

---

*Based on information obtained from the 1979 and 1983 questionnaire surveys.

Table VI-4

PM&F TREATMENT TECHNOLOGIES SUMMARY*

			Treatment Technologies													
Plant ID	Discharge Mode	% PM&F Process Water	pH Adjustment	Equalization	Oil Skimming	Solids Skimming	Filtration	Aeration	API Separator	Clarifier	Settling	Chlorinator	Activated Sludge	Carbon Adsorption	Coagulant Addition	Sludge or Solids Removal
640	Direct	100			X	X	X				X					
602195C	Direct	100							X							
564076A	Direct	100	X								X					
1400	Direct	99						X			X					
1420	Direct	88		X			X	X				X				X
1946	Direct	86	X								X					
29640A	Direct	81									X					
362544S	Direct	80					X	X			X					
580294E	Direct	61						X			X					
1330	Direct	50	X	X		X	X			X			X	X		X
583	Indirect	100					X				X					
1500	Indirect	100	X								X					X
2722	Indirect	100	X												X	
10290	Indirect	100					X									
10650	Indirect	100	X													
2500	Indirect	100	X	X			X									
480	Zero	100		X						X						X
	TOTAL		7	4	1	2	7	4	1	2	9	1	1	1	1	4

*Based on information reported in 1979 and 1983 questionnaire surveys.

treatment technologies that treat only PM&F process water. The other plants have treatment technologies that treat process water from PM&F processes with wastewater from other industrial processes. The 17 plants where a significant portion of the wastewater treated is from PM&F processes are only four percent of the plants in the data base. The other 96 percent of the plants are zero dischargers, had no treatment technology, or are plants where more than 50 percent of the wastewater treated was discharged by processes other than PM&F processes.

Of the 521 wet PM&F processes in the combined data base, 201 recycle process water. Table VI-5 contains a distribution of the number of processes that recycle process water by discharge mode. As shown in the table, 48 percent of those processes do not discharge process water, 23 percent are direct dischargers, and 28 percent are indirect dischargers.

The contact cooling and heating water subcategory was analyzed to determine the types of plastics molding and forming processes in the subcategory. Table VI-6 presents results of this analysis. As shown in the table, extrusion processes comprise the majority of processes in the subcategory with 85.0 percent. The next predominate type of process is molding with 7.5 percent. These two types of processes are 92.5 percent of the processes in this subcategory. The remaining four types of processes (i.e., calendering, casting, coating and laminating, and thermoforming) make up the remaining 7.5 percent.

PM&F Category Data

The 382 plants in the questionnaire data are distributed with respect to the processes that use a specific type of process water in the following manner:

1. Three hundred fifteen plants (82.5 percent) have processes using only contact cooling and heating water;

2. Twenty-six plants (6.8 percent) have processes using only cleaning water;

3. Nine plants (2.3 percent) have processes using only finishing water;

4. Twenty plants (5.2 percent) have processes that use contact cooling and heating water and processes that use cleaning water;

5. Five plants (1.3 percent) have processes that use contact cooling and heating water and processes that use finishing water;

Table VI-5

DISCHARGE MODE FOR PROCESSES IN QUESTIONNAIRE DATA BASE THAT RECYCLE PROCESS WATER*

	Discharge Mode							
Type of Process Water	Direct§	Percent†	Indirect	Percent†	Zero	Percent†	Total	Percent
Contact Cooling and Heating Water	44	23.4	50	26.6	94	50	188	100
Cleaning Water	3	33.3	6	66.7	0	0	9	100
Finishing Water	0	0	1	25.0	3	75.0	4	100
TOTAL	47	23.4	57	28.4	97	48.2	201	100

---

*Based on information from 1979 and 1983 questionnaire surveys.

§Direct and indirect discharge processes have a continuous or intermittent bleed or discharge from the recycle unit.

†Percent for type of process water.

Table VI-6

DISTRIBUTION OF NUMBER OF PROCESSES IN THE CONTACT COOLING AND HEATING WATER SUBCATEGORY BY TYPE OF PROCESS AND DISCHARGE MODE

Type of Process	Direct Discharge	Percent*	Indirect Discharge	Percent*	Zero Discharge	Percent*	Total	Percent*
Calendering	1	0.8	2	1.2	0	0	3	0.7
Casting	1	0.8	5	2.9	0	0	6	1.4
Coating and Laminating	2	1.4	7	4.1	4	3.4	13	3.1
Extrusion	127	90.7	132	77.7	105	89.0	364	85.0
Molding	6	4.2	18	10.6	8	6.8	32	7.5
Thermoforming	3	2.1	6	3.5	1	0.8	10	2.3
TOTAL	140	100.0	170	100.0	118	100.0	428	100.0

---

*Percent of all types of processes in a discharge mode.

6. Six plants (1.6 percent) have processes that use cleaning water and processes that use finishing water; and

7. One plant (0.3 percent) has a process that uses contact cooling and heating water, a process that uses cleaning water, and a process that uses finishing water.

Based on that information, 341 plants (315 + 20 + 5 + 1) have processes that use contact cooling and heating water, 53 plants have processes that use cleaning water (26 + 20 + 6 + 1), and 21 plants (9 + 5 + 6 + 1) have processes that use finishing water.

Estimate of Number of Plants and Processes in PM&F Category That Use Process Water

The process and plant information listed above from the questionnaire data base was applied to the estimated 1,898 wet plants in the PM&F category to obtain an estimate of the number of wet plants and processes in each subcategory. The means of arriving at the estimate of 1,898 wet plants is presented in Section IV. The calculations for the category plant estimate are:

(1,898 category wet plants) (0.825) = 1,569 plants with processes that use only contact cooling and heating water

(1,898 category wet plants) (0.068) = 129 plants with processes that use only cleaning water

(1,898 category wet plants) (0.023) = 43 plants with processes that use only finishing water

(1,898 category wet plants) (0.052) = 98 plants with processes that use contact cooling and heating water and processes that use cleaning water

(1,898 category wet plants) (0.013) = 24 plants with processes that use contact cooling and heating water and processes that use finishing water

(1,898 category wet plants) (0.016) = 30 plants with processes that use cleaning water and processes that use finishing water

(1,898 category wet plants) (0.003) = 5 plants with processes that use contact cooling and heating water, processes that use cleaning water, and processes that use finishing water

This equates to 1,696 plants (1,569 + 98 + 24 + 5) in the PM&F category with processes that use contact cooling and heating water, 262 plants (129 + 98 + 30 + 5) that use cleaning water, and 102 plants (43 + 24 + 30 + 5) that use finishing water. The total category wet process estimate is:

$$(1{,}696 \text{ category plants with processes that use contact cooling and heating water}) \times \frac{(428 \text{ data base processes})}{(341 \text{ data base plants})} = 2{,}129 \text{ processes that use contact cooling and heating water}$$

$$(262 \text{ category plants with processes that use cleaning water}) \times \frac{(71 \text{ data base processes})}{(53 \text{ data base plants})} = 351 \text{ category processes that use cleaning water}$$

$$(102 \text{ category plants with processes that use finishing water}) \times \frac{(22 \text{ data base processes})}{(21 \text{ data base plants})} = 107 \text{ category processes that use finishing water}$$

Applying the percentages for direct, indirect, and zero dischargers from Table VI-1 to the number of estimated processes gives an estimate number of processes by discharge mode. See Table VI-7 for this presentation.

Estimate of PM&F Category Process Water Use

The amount of process water use was estimated for each type of discharge mode (i.e., direct, indirect, and zero) in the PM&F category. The PM&F category uses approximately 308 billion liters (81 billion gallons) annually of process water. The following example for indirect dischargers illustrates the procedure used to estimate water use for the PM&F category.

To estimate the water use by indirect dischargers, the average amount of water used per year for each subcategory from the questionnaire data base was multiplied by the estimated number of indirect processes. These data are listed in Tables VI-2 and VI-7, respectively. The subcategory total amount of indirect water used was further divided into amounts discharged by plants with processes in only one subcategory, in two subcategories, and

Table VI-7

DISTRIBUTION OF THE NUMBER OF PM&F PROCESSES THAT USE PROCESS WATER BY TYPE OF PROCESS WATER AND DISCHARGE MODE

Type of Process Water	Direct Dischargers	Indirect Dischargers	Zero Dischargers	Total
Contact Cooling and Heating Water	696	845	588	2,129
Cleaning Water	104	232	15	351
Finishing Water	10	68	29	107
TOTAL	810	1,145	632	2,587

in three subcategories. For example, in the contact cooling and heating water subcategory questionnaire data base, indirect discharging processes are distributed as follows:

1. 90.0 percent of the contact cooling and heating water processes are at plants with only contact cooling and heating processes,
2. 7.1 percent of the contact cooling and heating water processes are at plants with contact cooling and heating water processes and cleaning processes,
3. 2.3 percent of contact cooling and heating water processes are at plants with contact cooling and heating water processes and finishing processes, and
4. 0.6 percent of contact cooling and heating water processes are at plants that have processes in the three subcategories.

These percentages were multiplied by the total amount of contact cooling and heating water used by indirect dischargers to calculate the amount of contact cooling and heating water used by indirect dischargers at the above listed combinations of processes. The same calculations were done for the cleaning water subcategory and for the finishing water subcategory. Table VI-8 summarizes the water use for the possible combinations. Likewise, water use was calculated for both the direct and zero dischargers. Tables VI-9 and VI-10 present the water use information for those discharge modes.

Estimate of PM&F Category Process Water Discharged

The amount of water discharged by PM&F processes was estimated for direct and indirect dischargers. The PM&F category discharges approximately 44 billion liters (12 billion gallons) annually of process water. The water discharge estimate was calculated in the same manner as the water use estimate, except that the average amount of water discharged from the questionnaire data base (presented in Table VI-2) was multiplied by the estimated number of processes. The distribution of process water discharged by plants with processes in one or more subcategories was calculated using the same percentages used to calculate the water use estimates. Tables VI-11 and VI-12, respectively, present the process water discharge information for direct and indirect dischargers.

SAMPLING PROGRAMS

This section discusses the sampling programs conducted during 1980, 1983, and 1984, and presents the results of the sample

Table VI-8

DISTRIBUTION OF PM&F WATER USE FOR INDIRECT DISCHARGERS

Possible Process Combination	Water Use by Indirect Dischargers (billion liters per year) Contact Cooling and Heating Water	Cleaning Water	Finishing Water	Total
1. Contact Cooling and Heating Water Processes Only	70.6	---	---	70.6
2. Cleaning Water Processes Only	---	5.47	---	5.47
3. Finishing Water Processes Only	---	---	0.174	0.174
4. Contact Cooling and Heating Water and Cleaning Water Processes	5.57	2.84	---	8.41
5. Contact Cooling and Heating Water and Finishing Water Processes	1.80	---	0.139	1.94
6. Cleaning Water and Finishing Water Processes	---	1.01	0.139	1.15
7. Contact Cooling and Heating Water, Cleaning Water, and Finishing Water Processes	0.470	0.200	0.0346	0.705
TOTAL	78.4	9.52	0.487	88.4

Table VI-9

DISTRIBUTION OF PM&F WATER USE FOR DIRECT DISCHARGERS

	Water Use by Direct Dischargers (billion liters per year)			
Possible Process Combination	Contact Cooling and Heating Water	Cleaning Water	Finishing Water	Total
1. Contact Cooling and Heating Water Processes Only	112	---	---	112
2. Cleaning Water Processes Only	---	1.88	---	1.88
3. Finishing Water Processes Only	---	---	0	0
4. Contact Cooling and Heating Water and Cleaning Water Processes	12.4	3.76	---	16.2
5. Contact Cooling and Heating Water and Finishing Water Processes	0	---	0	0
6. Cleaning Water and Finishing Water Processes	---	0.942	0.0249	0.967
7. Contact Cooling and Heating Water, Cleaning Water, and Finishing Water Processes	0	0	0	0
TOTAL	124	6.58	0.0249	131

Table VI-10

DISTRIBUTION OF PM&F WATER USE FOR ZERO DISCHARGERS

Possible Process Combination	Water Use by Zero Dischargers (billion liters per year)			
	Contact Cooling and Heating Water	Cleaning Water	Finishing Water	Total
1. Contact Cooling and Heating Water Processes Only	84.4	---	---	84.4
2. Cleaning Water Processes Only	---	0.0528	---	0.0528
3. Finishing Water Processes Only	---	---	1.85	1.85
4. Contact Cooling and Heating Water and Cleaning Water Processes	0.730	0.0264	---	0.756
5. Contact Cooling and Heating Water and Finishing Water Processes	0.730	---	0.371	1.10
6. Cleaning Water and Finishing Water Processes	---	0	0	0
7. Contact Cooling and Heating Water, Cleaning Water, and Finishing Water Processes	0	0	0	0
TOTAL	85.9	0.0792	2.22	88.2

Table VI-11

DISTRIBUTION OF PM&F PROCESS WATER DISCHARGED BY INDIRECT DISCHARGERS

	Process Water Discharged by Indirect Dischargers (billion liters per year)			
Possible Process Combination	Contact Cooling and Heating Water	Cleaning Water	Finishing Water	Total
1. Contact Cooling and Heating Water Processes Only	13.9	---	---	13.9
2. Cleaning Water Processes Only	---	1.02	---	1.02
3. Finishing Water Processes Only	---	---	0.0921	0.0921
4. Contact Cooling and Heating Water and Cleaning Water Processes	1.09	0.530	---	1.62
5. Contact Cooling and Heating Water and Finishing Water Processes	0.354	---	0.0738	0.428
6. Cleaning Water and Finishing Water Processes	---	0.189	0.0378	0.263
7. Contact Cooling and Heating Water, Cleaning Water, and Finishing Water Processes	0.0924	0.0374	0.0183	0.148
TOTAL	15.4	1.78	0.258	17.4

Table VI-12

DISTRIBUTION OF PM&F PROCESS WATER DISCHARGED BY DIRECT DISCHARGERS

	Process Water Discharged by Direct Dischargers (billion liters per year)			
Possible Process Combination	Contact Cooling and Heating Water	Cleaning Water	Finishing Water	Total
1. Contact Cooling and Heating Water Processes Only	21.0	---	---	21.0
2. Cleaning Water Processes Only	---	0.912	---	0.912
3. Finishing Water Processes Only	---	---	0	0
4. Contact Cooling and Heating Water and Cleaning Water Processes	2.33	1.82	---	4.15
5. Contact Cooling and Heating Water and Finishing Water Processes	0	---	0	0
6. Cleaning Water and Finishing Water Processes	---	0.456	0.0249	0.481
7. Contact Cooling and Heating Water, Cleaning Water, and Finishing Water Processes	0	0	0	0
TOTAL	23.3	3.19	0.0249	26.5

analyses. The results from the 1980 and 1983 sampling programs were used in developing the proposed PM&F effluent limitations guidelines and standards. The 1984 sampling effort results were incorporated with the results from the other efforts to evaluate comments and to develop the final PM&F effluent limitations guidelines and standards.

Plant Selection - Proposed Regulation

The sampling programs for the proposed PM&F regulation were undertaken to identify pollutants in the PM&F process waters. Samples were collected at plastics molding and forming plants and analyzed for conventional, selected nonconventional, and priority toxic pollutants.

Criteria used to select PM&F plants for sampling included the number and types of PM&F processes, water use and wastewater discharge practices, and differences in production processes and plastics materials used. The primary sources of this information were the questionnaire surveys. The Agency selected plants for sampling that represented a full range of PM&F processes and raw materials. Those plants usually had more than one PM&F process.

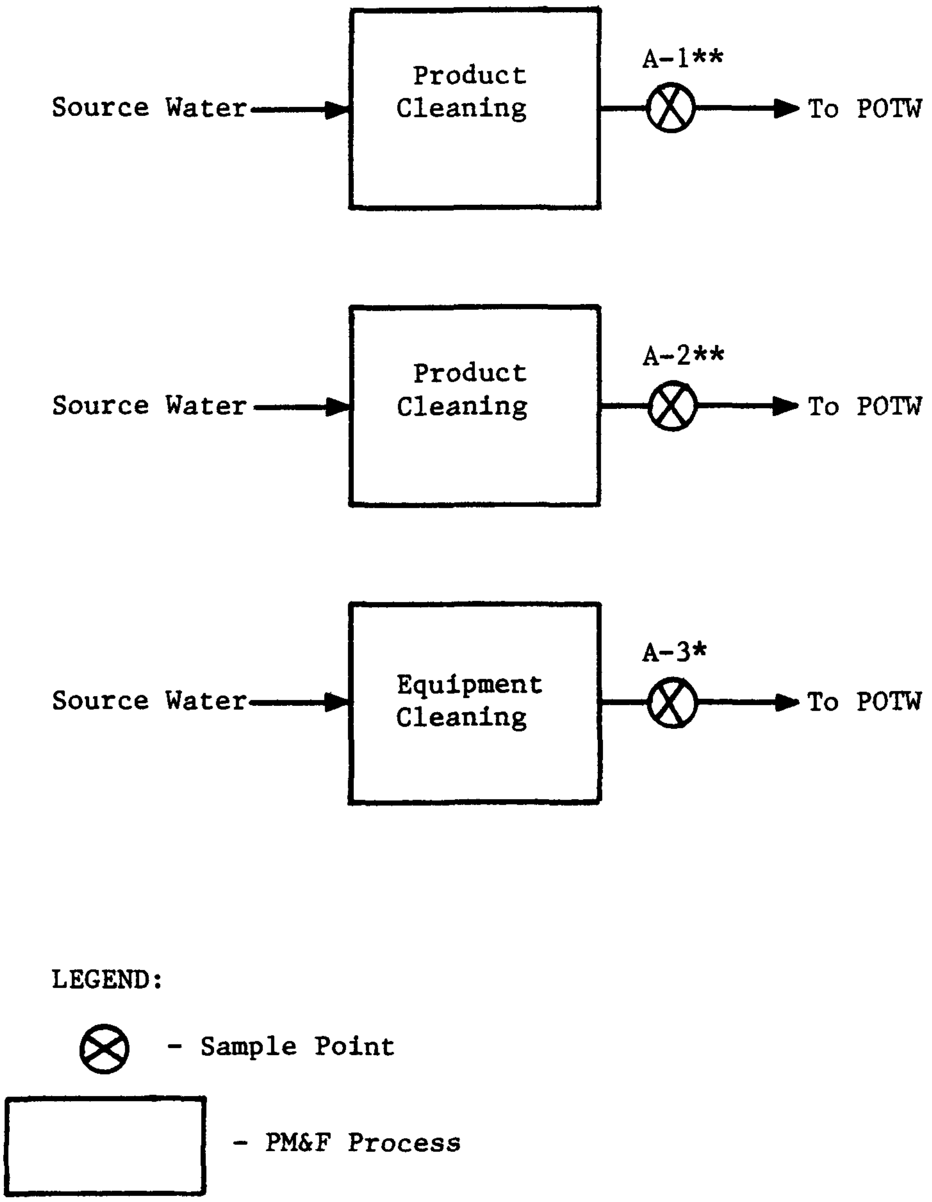
Field Sampling Programs - Proposed PM&F Regulation

After selection of candidate plants, each plant was contacted by telephone to verify their operations and to inform them that EPA had included them in the sampling program. Presampling site visits were conducted to identify sample locations, sampling conditions, and plant operations.

Eleven plants were sampled during the 1980 and 1983 episodes. Plants C, E, F, and I were sampled in 1980 and the remaining seven plants, A, B, D, G, H, J, and K, were sampled in 1983. Figures VI-1 through VI-11 present process water flow diagrams for the 11 plants indicating the location of the sample points.

The sampling data base for the proposed regulation contained data from 18 contact cooling and heating processes that were sampled at eight PM&F plants. Four different types of contact cooling and heating water processes were sampled at those plants (i.e., extrusion, molding, calendering, and thermoforming). Twelve cleaning processes were sampled at eight PM&F plants and one finishing process was sampled. These 13 processes were in the cleaning and finishing water subcategory for the proposed regulation.

Several changes were made to the pre-proposal sampling data base between proposal and promulgation. These changes include the following:



*Data from this point were not used in data analysis because production data were not available for this process.

**This is a batch process.

Figure VI-1

SAMPLING POINTS AT PLANT A

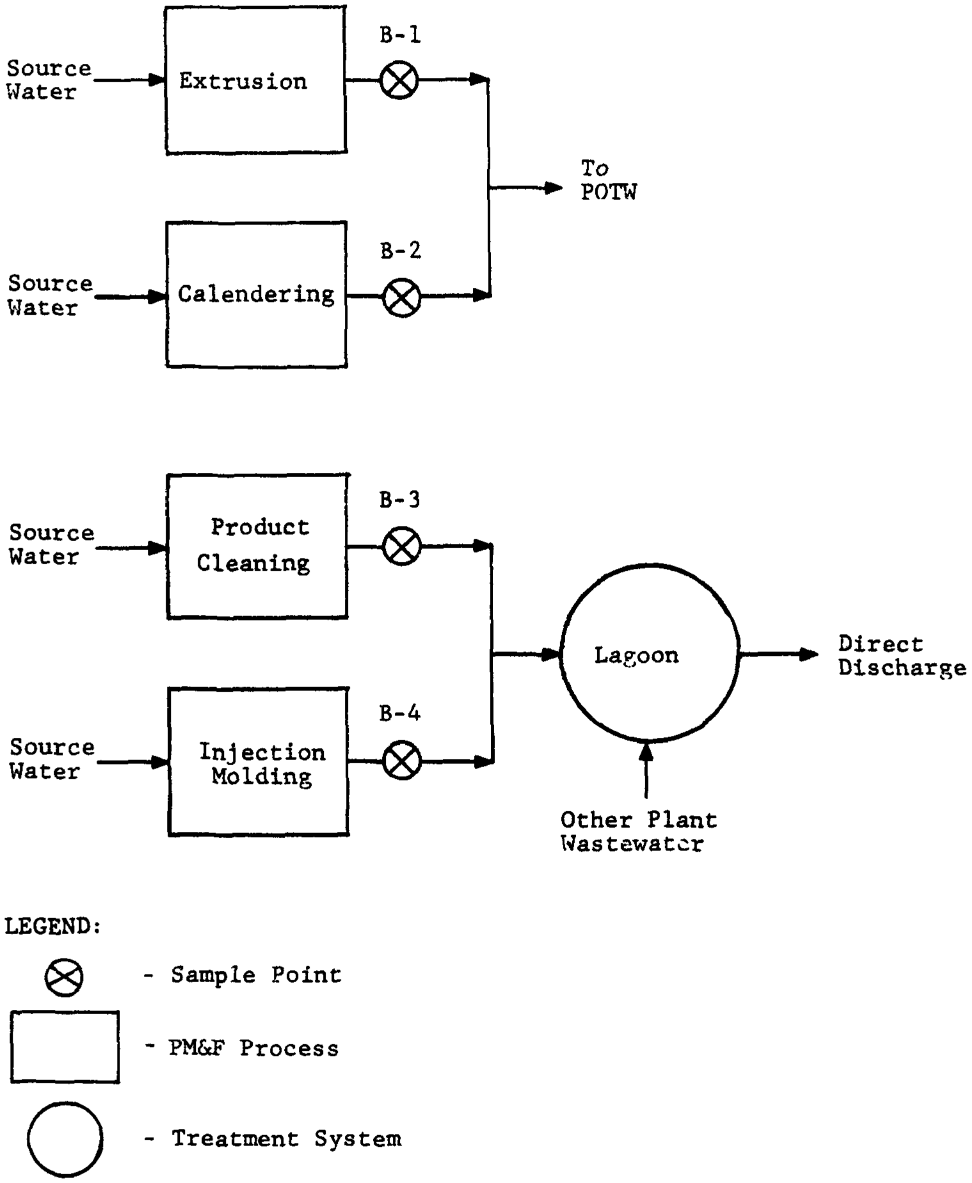
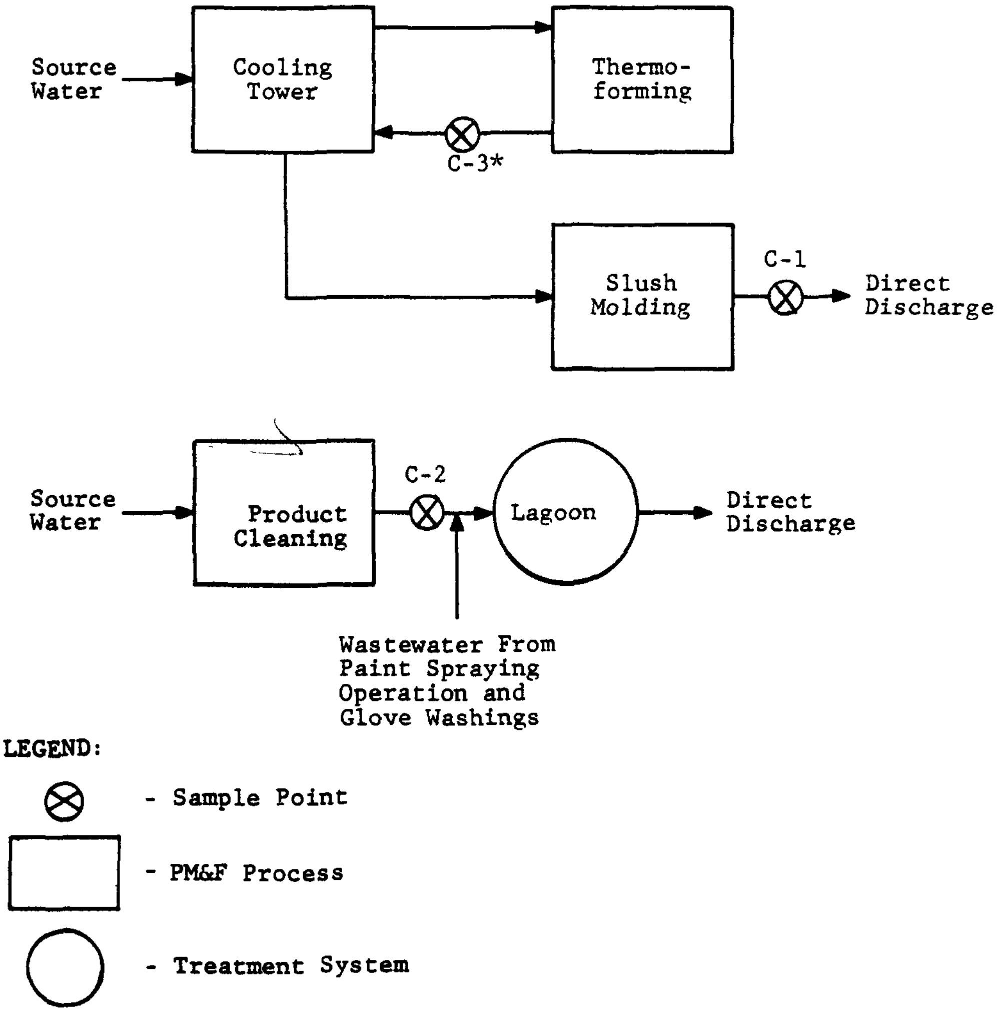


Figure VI-2

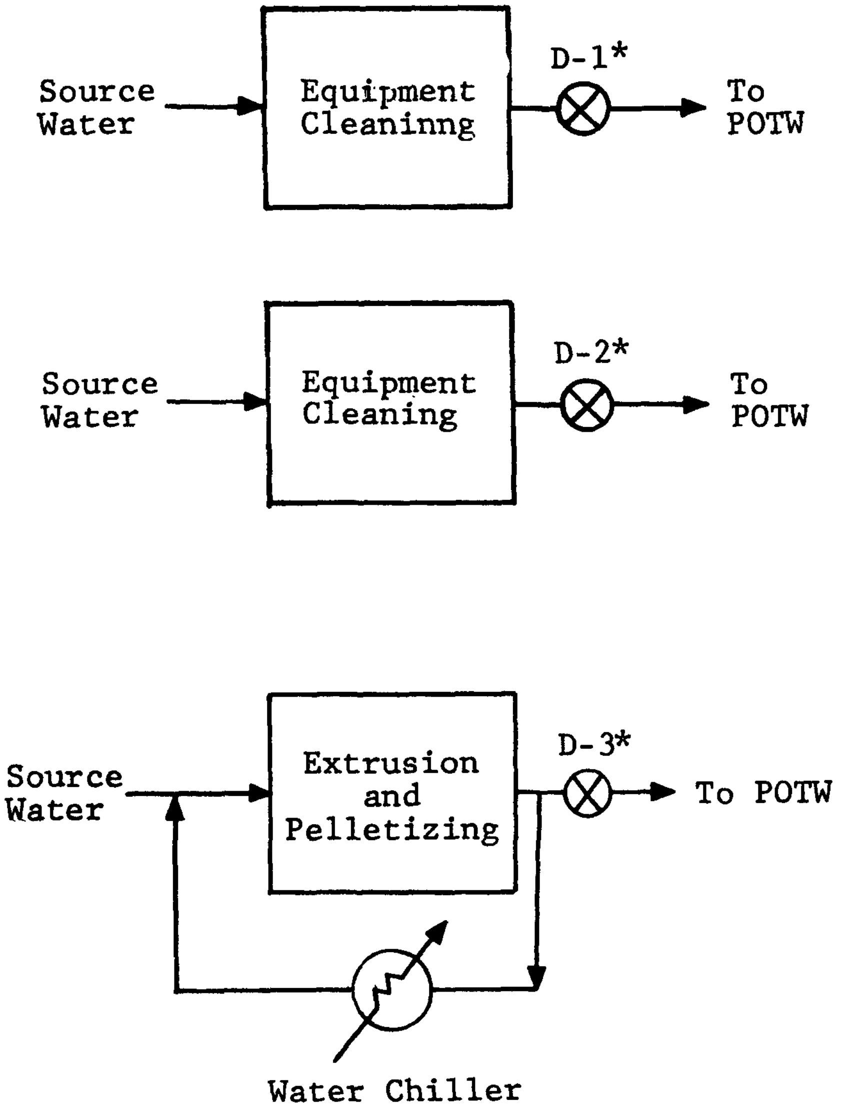
SAMPLING POINTS AT PLANT B



*Data from this point were not used in data analyses because process is no longer in operation.

Figure VI-3

SAMPLING POINTS AT PLANT C



LEGEND:

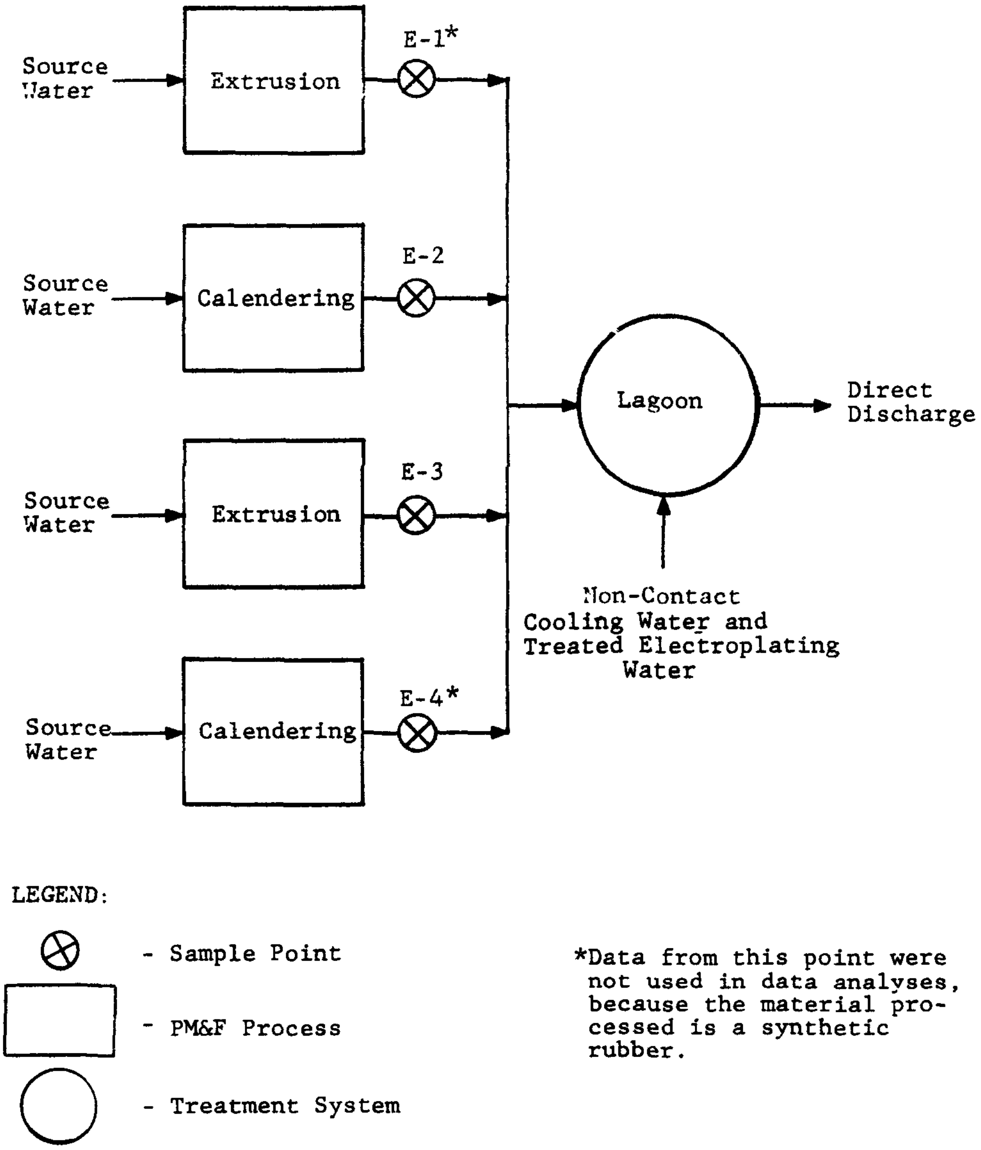
⊗ - Sample Point

☐ - PM&F Process

*Batch process was sampled when process water was discharged.

Figure VI-4

SAMPLING POINTS AT PLANT D



*Data from this point were not used in data analyses, because the material processed is a synthetic rubber.

Figure VI-5

SAMPLING POINTS AT PLANT E

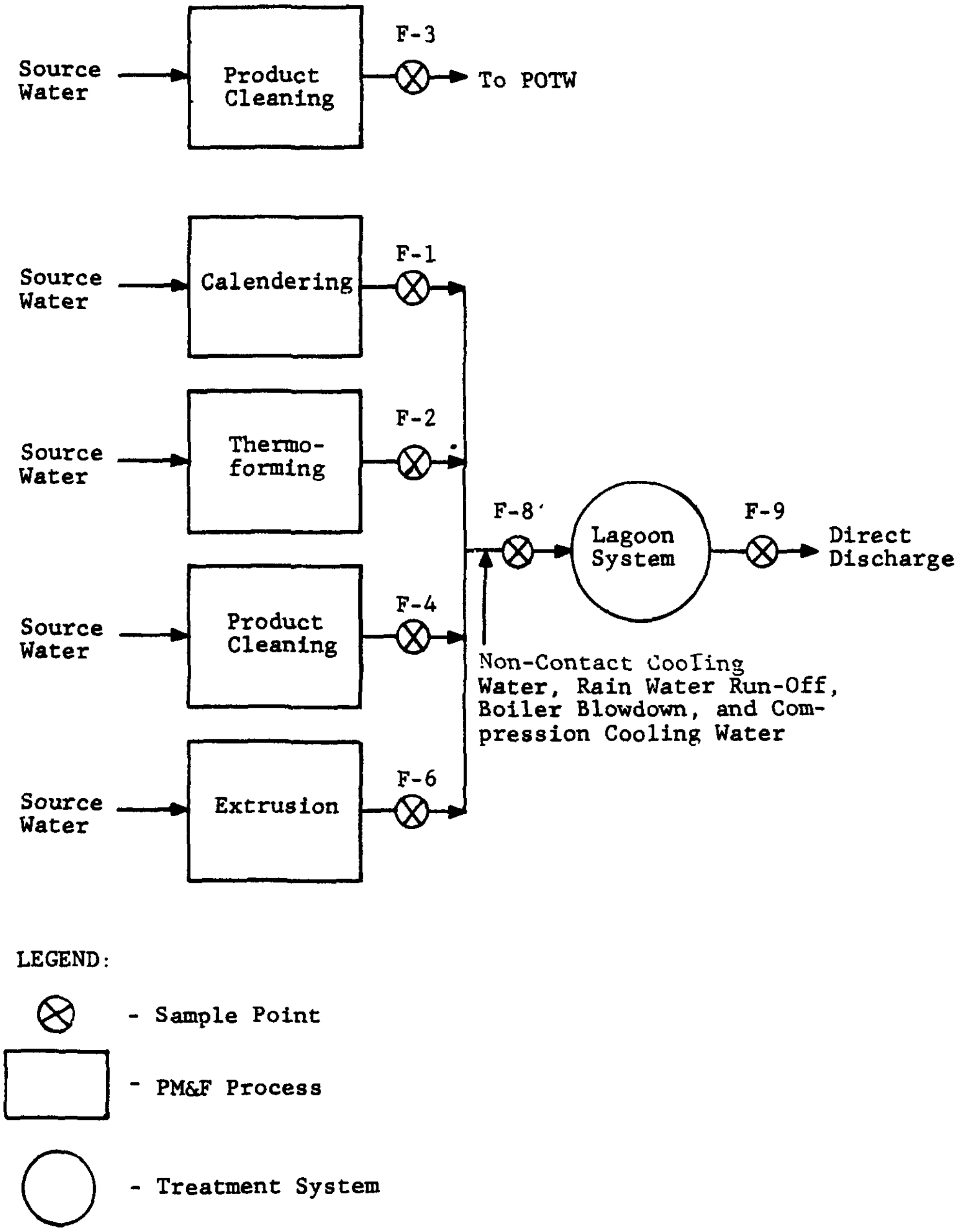
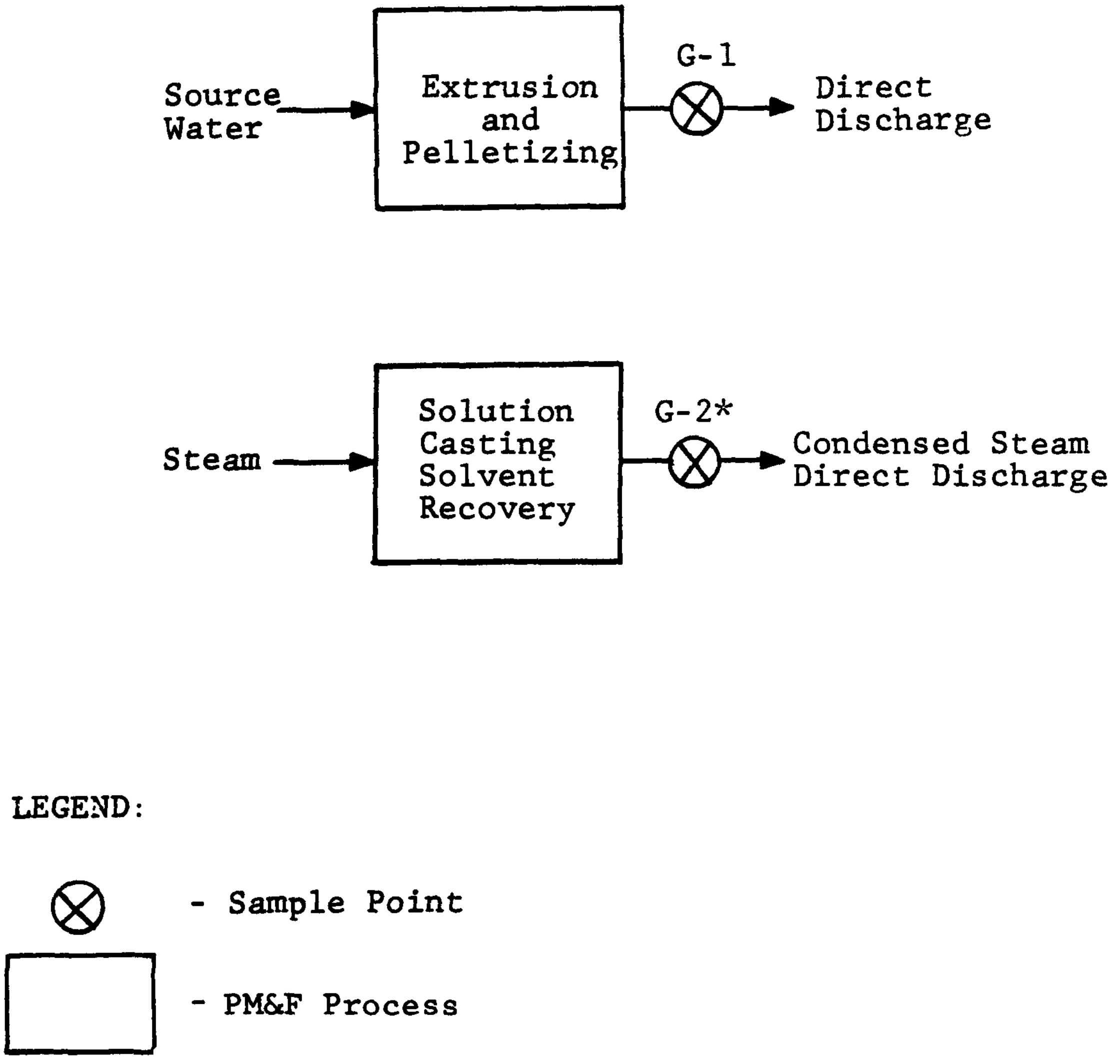


Figure VI-6

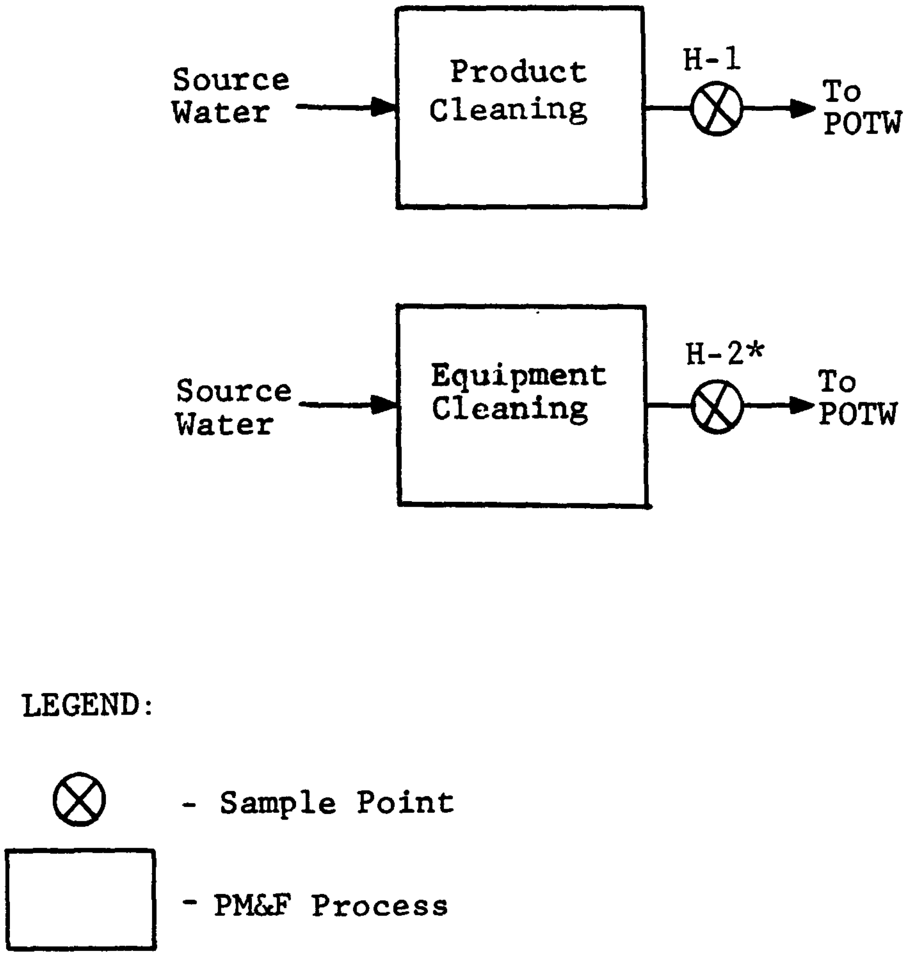
SAMPLING POINTS AT PLANT F



*Solvent recovery wastewater is not regulated by the PM&F effluent limitations guidelines and standards.

Figure VI-7

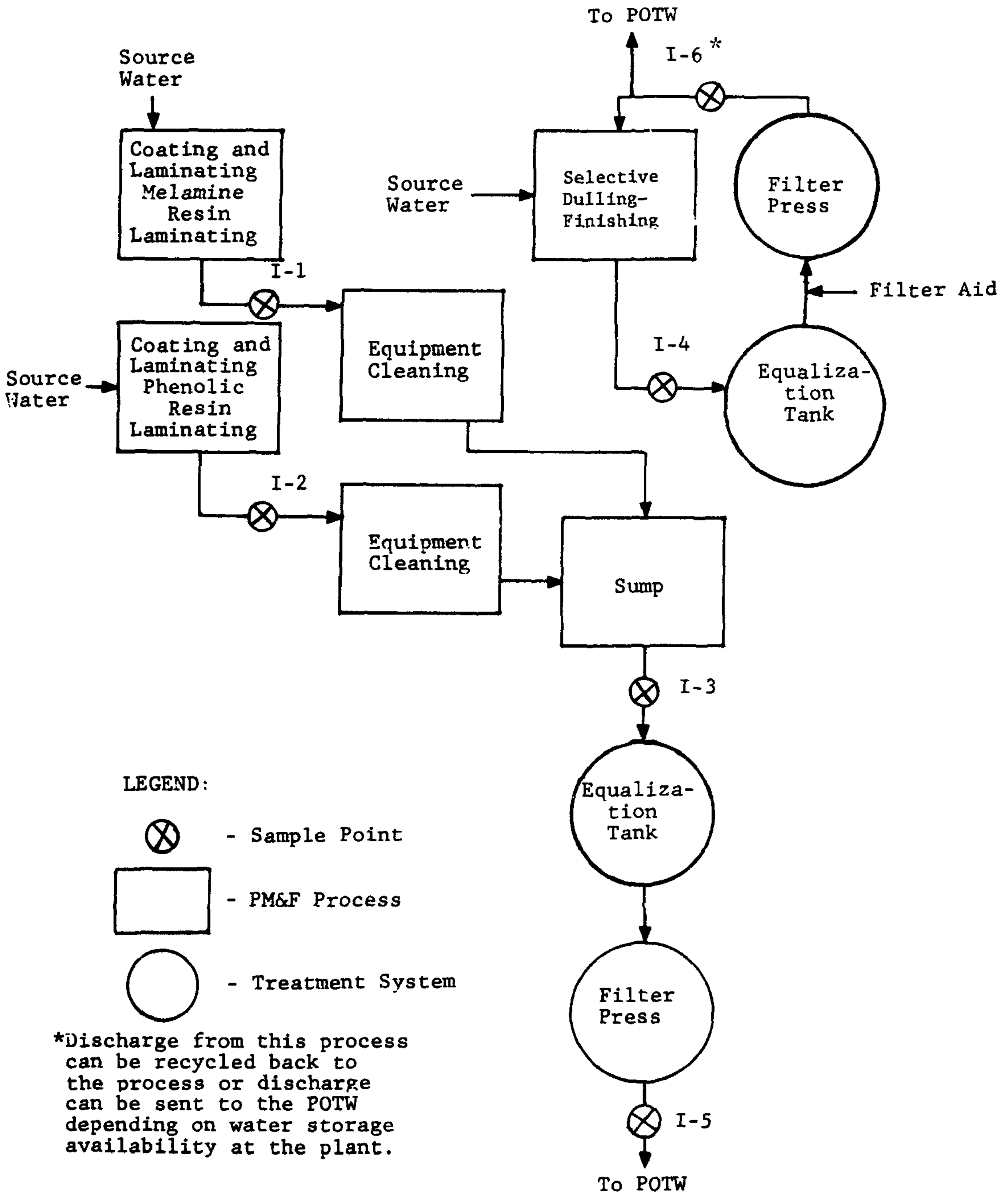
SAMPLING POINTS AT PLANT G



*Data from this point were not used in data analyses because production data were not available for this process.

Figure VI-8

SAMPLING POINTS AT PLANT H



*Discharge from this process can be recycled back to the process or discharge can be sent to the POTW depending on water storage availability at the plant.

Figure VI-9

SAMPLING POINTS AT PLANT I

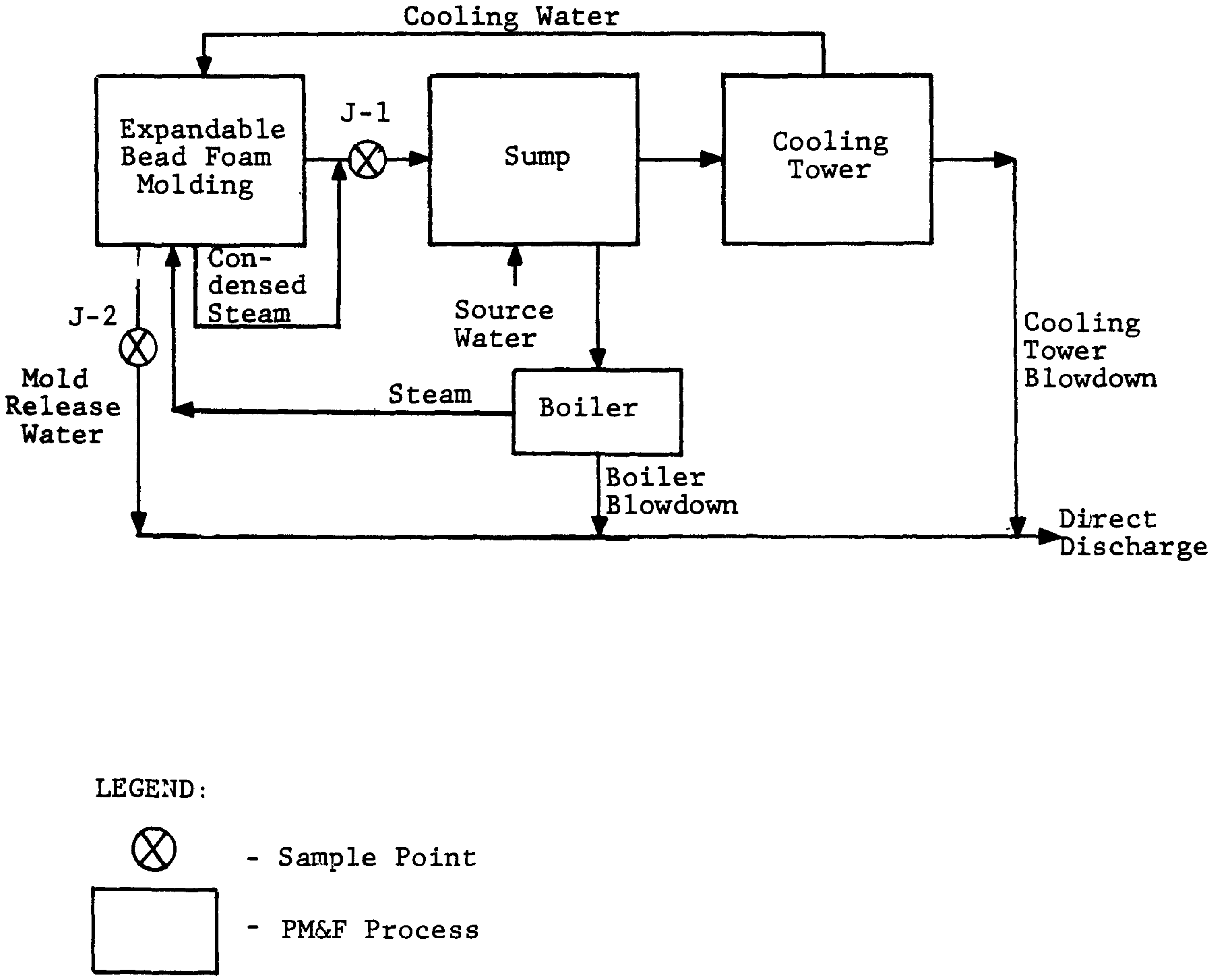


Figure VI-10

SAMPLING POINTS AT PLANT J

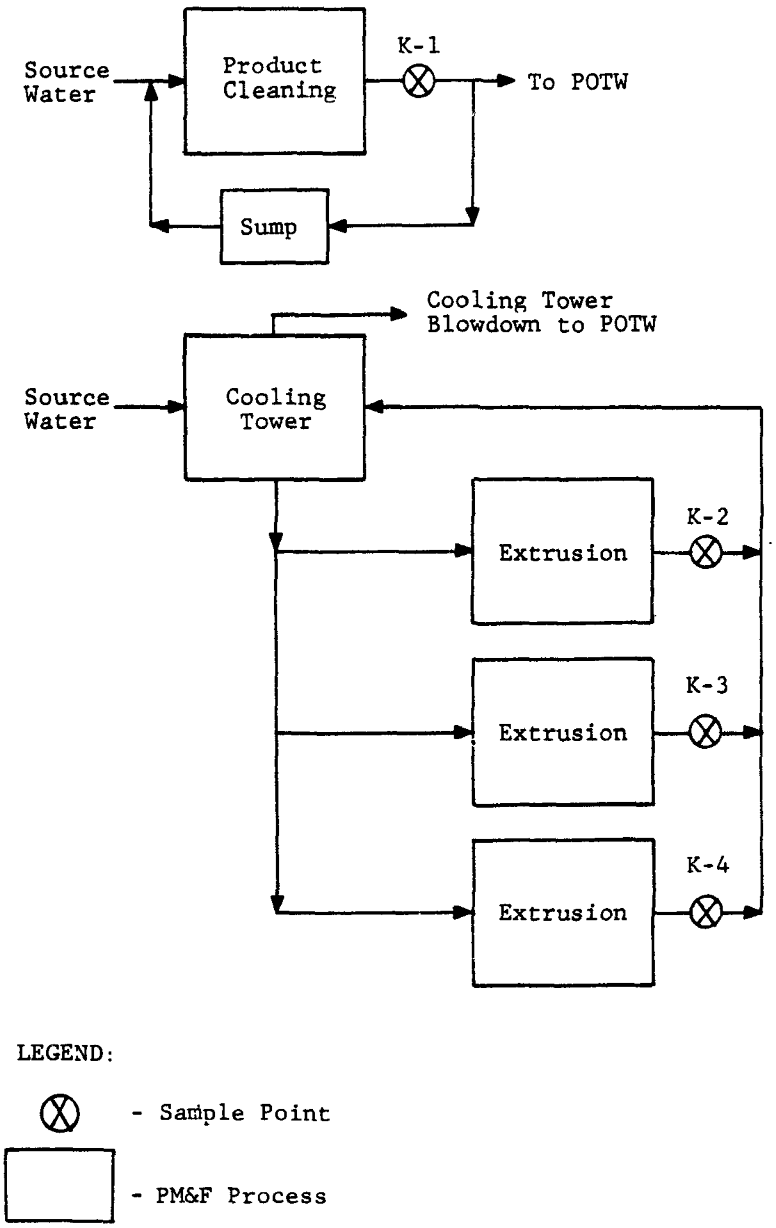


Figure VI-11

SAMPLING POINTS AT PLANT K

1. Process H-1 was moved to the cleaning water subcategory. Originally, this process was classified as a casting process in the contact cooling and heating water subcategory. The Agency determined that water was used in this process to rinse the mold release agent (glycerol) from the product after the product was stripped off a mandrel. Because this is a cleaning operation instead of a heat transfer operation, data from that process were transferred from the contact cooling and heating water data base to the cleaning water data base.

2. Process B-2 was moved to the contact cooling and heating water subcategory. At proposal, process B-2 was classified as a finishing operation because two calender rolls formed the product into its final shape. This process was subsequently moved to the contact cooling and heating water subcategory because the Agency now believes water is used to cool instead of finish the product.

3. Processes E-1 and E-4 were eliminated from the contact cooling and heating water subcategory. The material used in those processes is a synthetic rubber and not a plastic material.

4. The cleaning and finishing water subcategory was separated into the cleaning water subcategory and the finishing water subcategory.

5. Production data were calculated for process I-4 and the process was included in the finishing water subcategory.

Table VI-13 lists the processes sampled in each subcategory and the process water flow rate for each process for which data were used to develop the final PM&F regulation.

Plant Selection - Final PM&F Regulation

Effluent limitations guidelines and standards were proposed on February 15, 1984, for the PM&F point source category. At the time of the proposal, the Agency identified three areas of the industry where the collection of additional sampling data was necessary. The three areas were (1) conventional and nonconventional pollutant data for contact cooling and heating waters; (2) conventional, nonconventional, and priority pollutant data for finishing waters; and (3) characteristics of solid waste generated by PM&F wastewater treatment operations. In addition, EPA determined that some additional data were needed to fully evaluate and respond to comments on the proposed PM&F regulation.

Table VI-13

1980 AND 1983 SAMPLED PROCESSES

CONTACT COOLING AND HEATING WATER SUBCATEGORY

Process Code	Type of Process	Process Water Flow Rate (gpm)
B-1	extrusion	0.8
B-2	extrusion	1.8
B-4	injection molding	0.025
C-1	slush molding	0.28
D-3	pelletizing (extrusion)	50 gal/batch
E-2	calendering	14.0
E-3	wire coating (extrusion)	35.0
F-1	calendering	2.3
F-2	vacuum forming	1.8
F-6	extrusion	2.0
G-1	pelletizing (extrusion)	1.45
J-1	foam injection molding	120.0
J-2	molding	11.0
K-2	extrusion	4.0
K-3	extrusion	2.0
K-4	extrusion	146.0

CLEANING WATER SUBCATEGORY

Process Code	Type of Process	Process Water Flow Rate (gpm)
A-1	parts washing	10 gal/batch
A-2	oxalic acid parts washing	40 gal/batch
B-3	lens cleaning	20
C-2	parts washing	2.0
D-1	tank cleaning	15 gal/batch
D-2	tank cleaning	15 gal/batch
F-3	parts washing and rinsing	3.4
F-4	parts washing and rinsing	7.4
H-1	product rinsing	0.07
I-1	resin application equipment cleanup	1.4
I-2	resin application equipment cleanup	0.7
I-3	resin application equipment cleanup	1.6
K-1	parts washing	0.5

FINISHING WATER SUBCATEGORY

Process Code	Type of Process	Process Water Flow Rate (gpm)
I-4	product surface dulling	5.4

As for the sampling programs for the proposed regulation, types of processes, water use and wastewater discharge practices, and differences in production processes and plastic materials used were considered when selecting plants for the post-proposal sampling program. The questionnaire survey forms were the primary source of this information. Plants M, N, O, P, Q, and R were sampled in 1984. Figures VI-12 through VI-17 present process water flow diagrams for these six plants indicating the location of the sample points.

The 1984 sampling data base contains data from nine contact cooling and heating processes sampled at five plants. These processes, which include extrusion, thermoforming, and casting, were sampled and the samples were analyzed for conventional and selected nonconventional pollutants. Two finishing water processes were also sampled at two plants. Samples from those processes were analyzed for conventional, selected nonconventional, and priority pollutants. Table VI-14 presents the processes sampled in each subcategory and the process water flow rate for each process. Additionally, four solid waste samples from PM&F wastewater treatment operations were collected at three plants and analyzed to determine whether those wastes were hazardous. Refer to the energy and non-water quality impacts in Section IX for the extraction procedure (EP) toxicity test results for those samples.

Plant F was sampled in 1980 and was re-sampled in 1984 for verification of the total phenols concentrations found in the process water. The 1980 sampling episode showed total phenols levels that were magnitudes higher than levels found at the other sampled plants. Because personnel at Plant F could not explain what was contributing to the total phenols concentration, Plant F was selected for total phenols verification sampling. The results of this verification sampling are discussed at the end of this section.

Sample Collection, Preservation, and Transportation

Collection, preservation, and transportation of samples were performed in accordance with procedures outlined both in Appendix III of "Sampling and Analysis Procedures for Screening of Industrial Effluents for Priority Pollutants" (published by the Environmental Monitoring and Support Laboratory, Cincinnati, Ohio, March 1977, revised, April 1977) and in "Sampling Screening Procedure for the Measurement of Priority Pollutants" (published by the EPA Industrial Technology Division (formerly Effluent Guidelines Division), Washington, D.C., October 1976). Procedures for collection, preservation, and transportation of samples tested for conventional and nonconventional pollutants are described in the appropriate test methods (see Table VI-16).

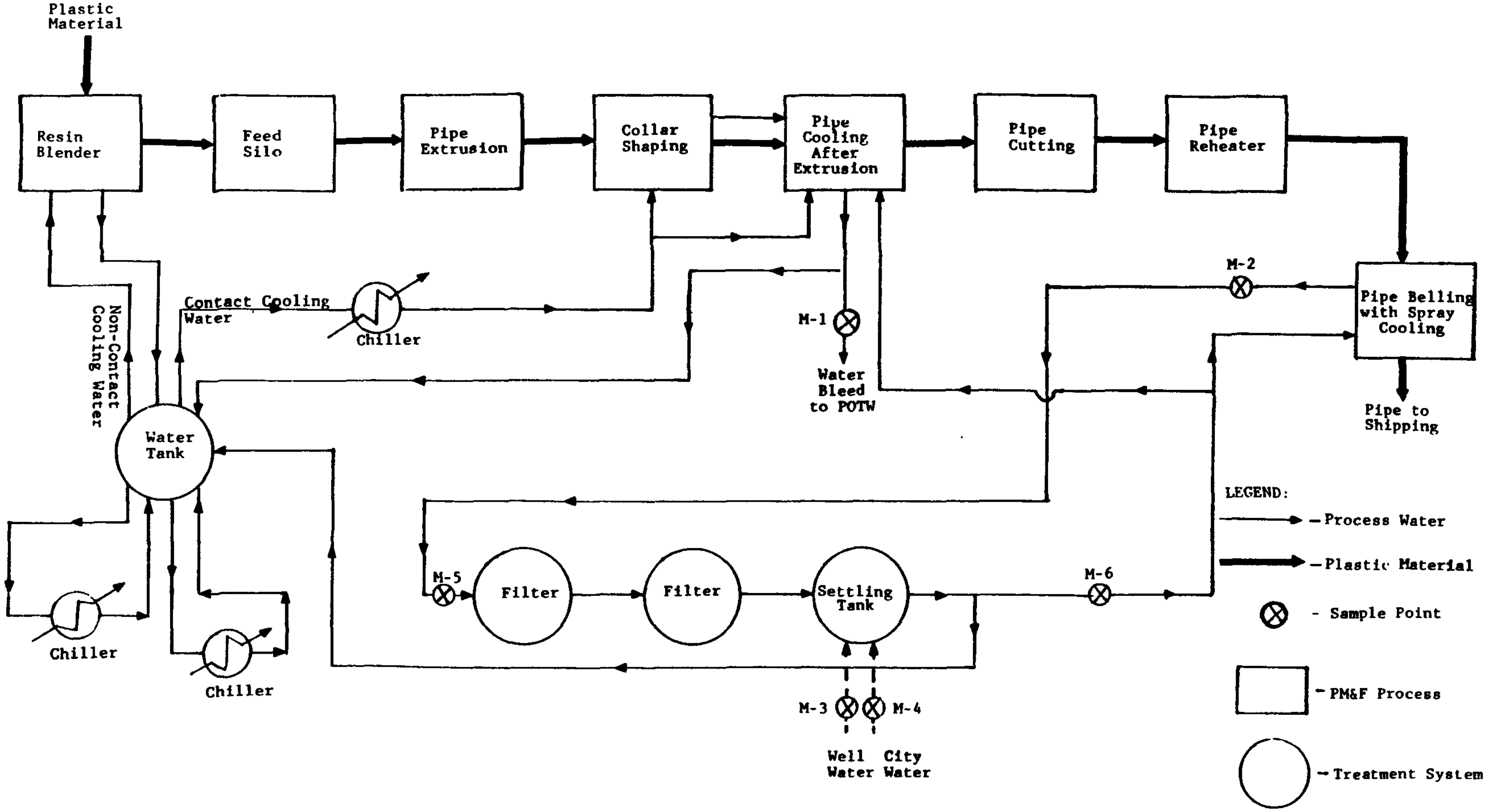
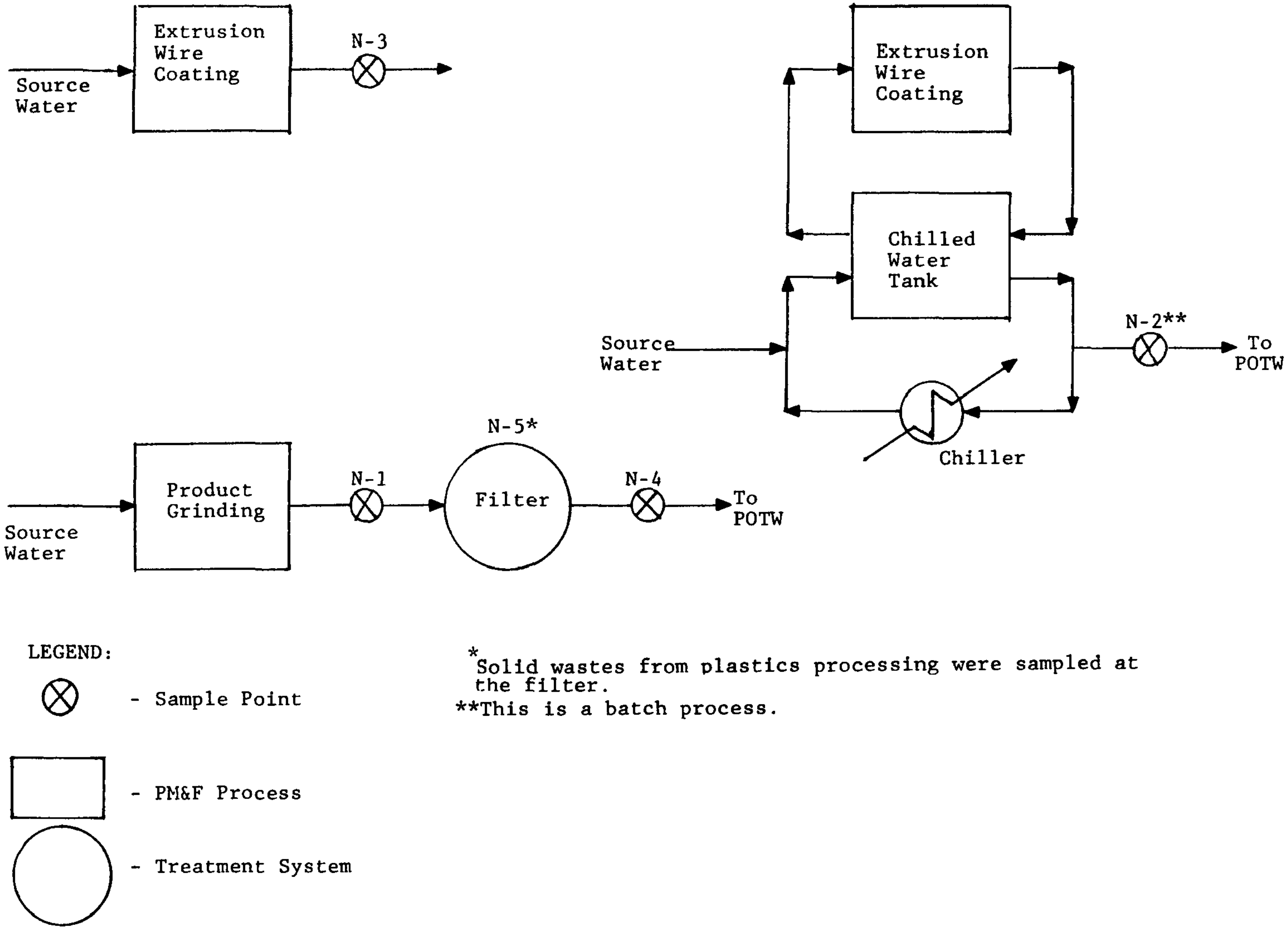


Figure VI-12

SAMPLING POINTS AT PLANT M



*Solid wastes from plastics processing were sampled at the filter.

**This is a batch process.

Figure VI-13

SAMPLING POINTS AT PLANT N

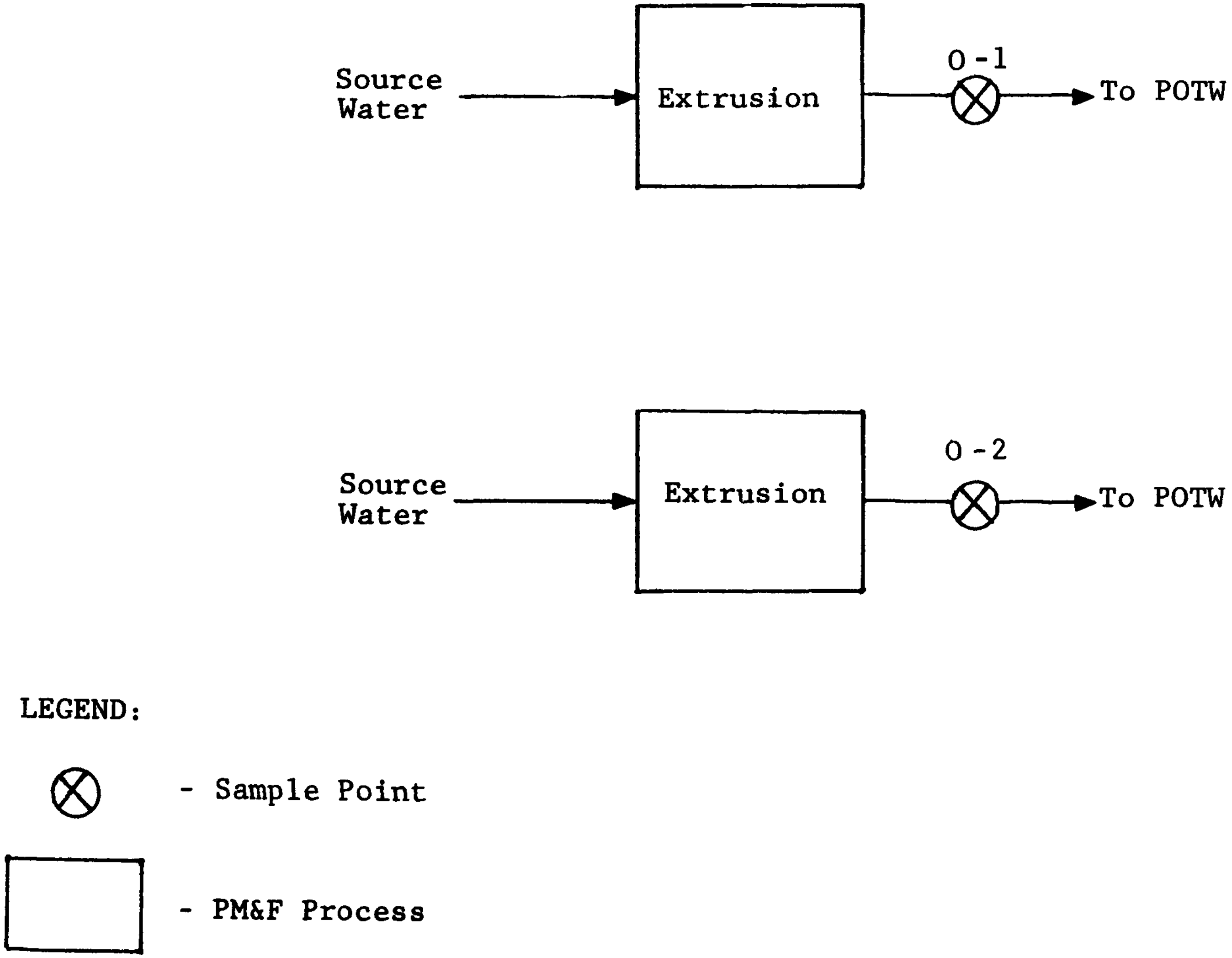


Figure VI-14

SAMPLING POINTS AT PLANT O

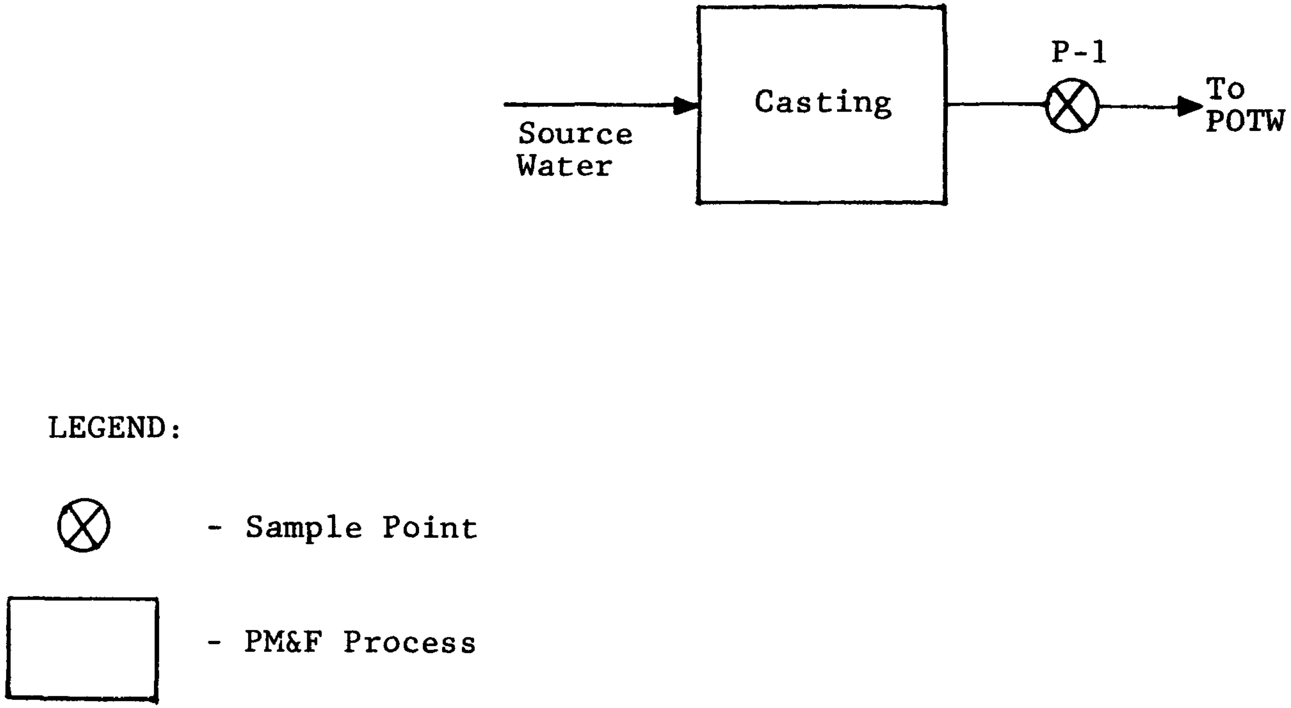


Figure VI-15

SAMPLING POINTS AT PLANT P

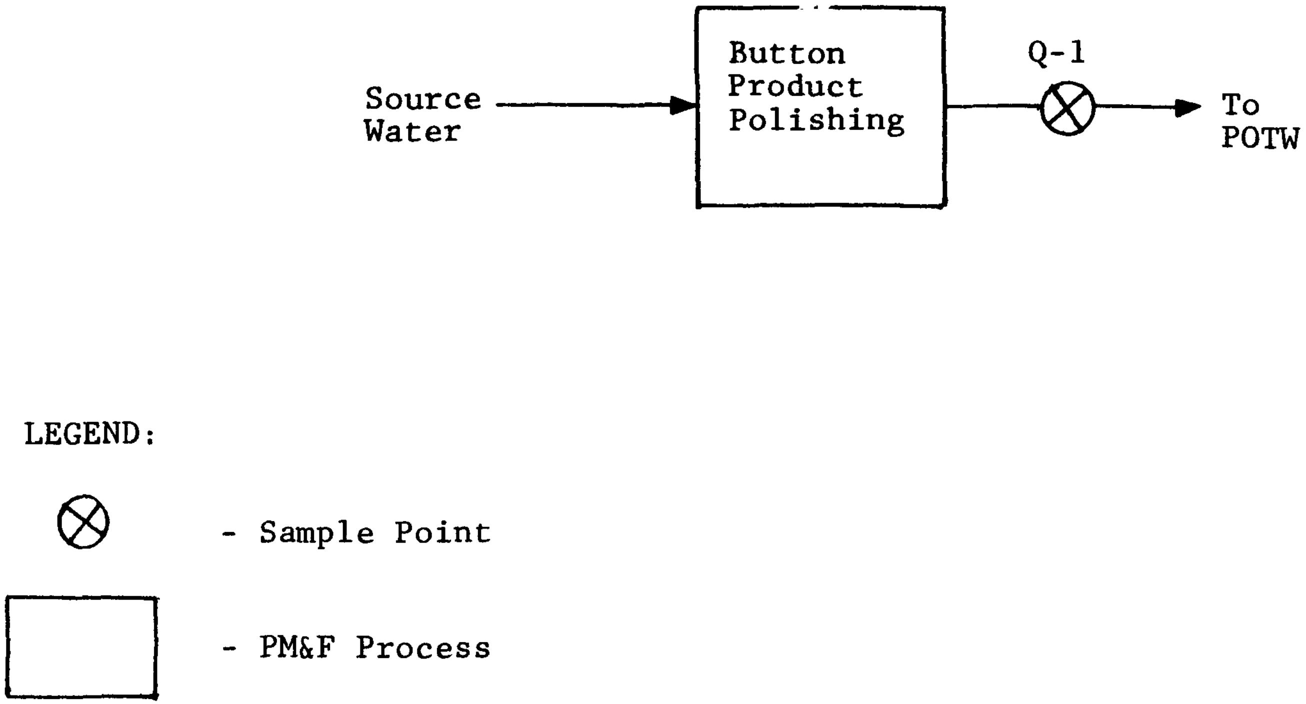
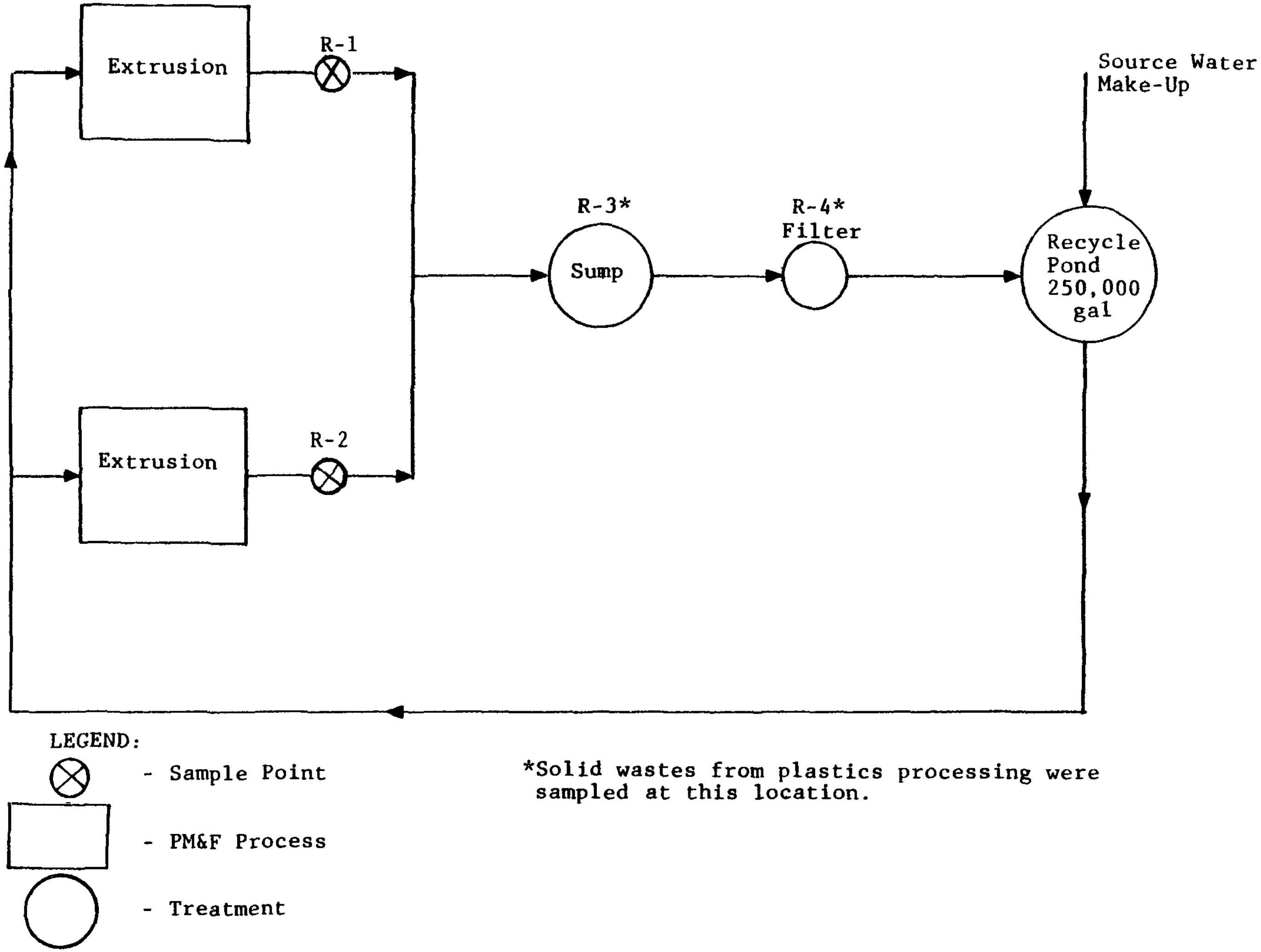


Figure VI-16

SAMPLING POINTS AT PLANT Q



*Solid wastes from plastics processing were sampled at this location.

Figure VI-17

SAMPLING POINTS AT PLANT R

Table VI-14

1984 SAMPLED PROCESSES

CONTACT COOLING AND HEATING WATER SUBCATEGORY

Process Code	Type of Process	Process Water Flow Rate (gpm)
M-1	pipe extrusion	3.6
M-2	thermoforming	5.0
N-2	extrusion	0.03
N-3	extrusion	0.94
O-1	extrusion	2.5
O-2	extrusion	1.8
P-1	casting	4.8
R-1	extrusion	3.9
R-2	extrusion	55.0

FINISHING WATER SUBCATEGORY

Process Code	Type of Process	Process Water Flow Rate (gpm)
N-1	product grinding	12.0
Q-1	product finishing	18.0

Sample Analysis

Once collected in the field, samples were prepared and shipped via overnight air express to EPA contract laboratories for analysis. Pollutants for which analyses were conducted are presented in Table VI-15. The analytical methods used are listed in Table VI-16. The analytical detection limits for the priority toxic pollutants are listed in Table VI-17.

Field Quality Assurance/Quality Control (QA/QC)

Field QA/QC procedures for the sampling programs included taking duplicate, blank, preservative blank, and source water samples.

Field Duplicates. Duplicate samples were collected at one sampling point at some of the sampled plants and were analyzed for the same pollutants that the other samples collected at that point were analyzed for. The identity of the duplicate samples was not made known to the laboratories. Oil and grease and volatile organic (VOA) samples were collected in duplicate each time samples were collected and shipped to the laboratory.

Field Blanks. As required by sampling protocol, organic-free water was flushed through each automatic sampler prior to the start of sampling at each plant. One gallon of that water was collected and shipped to the contract laboratory. This sample was the non-volatile organic pollutant blank sample.

Duplicate VOA blanks for each sampling point were supplied in 40 milliliter vials by the laboratory. Both preserved and unpreserved VOA field blanks were supplied. The VOA blanks were prepared in the laboratory, transported to the sampling site, placed at selected locations at the sampling site, and then returned to the laboratory after conclusion of the sampling period.

Preservative/Container Blanks. To verify that there was no contamination from the various chemicals used as preservatives or from the sample containers, organic-free water supplied by the laboratory was poured into the appropriate sample containers. These samples were preserved and shipped to appropriate laboratories for analysis.

Source Water Samples. To assess potential presence of conventional, nonconventional, and toxic pollutants in the source water for each plant, samples of the source water were collected, preserved, shipped to the laboratory, and analyzed for the pollutants listed in Table VI-15.

Table VI-15

POLLUTANTS FOR WHICH PM&F PROCESS WATER SAMPLES WERE ANALYZED

PRIORITY POLLUTANTS

Base/Neutral Compounds

Acenaphthene
Benzidine
1,2,4-Trichlorobenzene
Hexachlorobenzene
Hexachloroethane
bis (2-Chloroethyl) ether
1,2-Dichlorobenzene
2-Chloronaphthalene
1,3-Dichlorobenzene
1,4-Dichlorobenzene
3,3'-Dichlorobenzidine
2,4-Dinitrotoluene
2,6-Dinitrotoluene
1,2-Diphenylhydrazine
 (as azobenzene)
Fluoranthene
4-Chlorophenyl phenyl ether
4-Bromophenyl phenyl ether
bis (2-Chloroisopropyl) ether
bis (2-Chloroethoxy) methane
Hexachlorobutadiene
Hexachlorocyclopentadiene
Isophorone
Naphthalene
Nitrobenzene
N-Nitrosodimethylamine
N-Nitrosodiphenylamine
N-Nitrosodi-n-propylamine
bis (2-Ethylhexyl) phthalate
Butyl benzyl phthalate
Di-n-butyl phthalate
Di-n-octyl phthalate
Diethyl phthalate
Dimethyl phthalate
Benzo(a)anthracene
Benzo(a) pyrene
3,4-Benzofluoranthene
Benzo(k)fluoranthene
Chrysene
Acenaphthylene
Anthracene
Benzo (g,h,i)perylene
Fluorene
Phenanthrene
Dibenzo(a,h)anthracene
Indeno(1,2,3-c,d)pyrene
Pyrene
2,3,7,8-Tetrachlorodibenzo-
 p-dioxin

PRIORITY POLLUTANTS

Pesticides

Aldrin
Dieldrin
Chlordane
4,4'-DDT
4,4'-DDE
4,4'-DDD
alpha-Endosulfan
beta-Endosulfan
Endosulfan sulfate
Endrin
Endrin aldehyde
Heptachlor
Heptachlor epoxide
alpha-BHC
beta-BHC
gamma-BHC
delta-BHC
PCB-1242
PCB-1254
PCB-1221
PCB-1232
PCB-1248
PCB-1260
PCB-1016
Toxaphene

Volatiles

Acrolein
Acrylonitrile
Benzene
Carbon tetrachloride
Chlorobenzene
1,2-Dichloroethane
1,1,1-Trichloroethane
1,1-Dichloroethane
1,1,2-Trichloroethane
1,1,2,2-Tetrachloroethane
Chloroethane
bis (Chloromethyl) ether[1]
2-Chloroethylvinyl ether
Chloroform
1,1-Dichloroethylene
1,2-trans-Dichloroethylene
1,2-Dichloropropane
1,2-Dichloropropylene
Ethylbenzene
Methylene chloride
Methyl chloride
Methyl bromide
Bromoform
Dichlorobromomethane
Trichlorofluoromethane[1]
Dichlorodifluoromethane[1]
Chlorodibromomethane
Tetrachloroethylene
Toluene
Trichloroethylene
Vinyl chloride

PRIORITY POLLUTANTS

Acid Compounds

2,4,6-Trichlorophenol
p-Chloro-m-cresol
2-Chlorophenol
1,4-Dichlorophenol
2,4-Dimethylphenol
2-Nitrophenol
4-Nitrophenol
2,4-Dinitrophenol
4,5-Dinitro-o-cresol
Pentachlorophenol
Phenol

Other

Cyanide
Asbestos

Metals

Antimony
Arsenic
Beryllium
Chromium
Cadmium
Copper
Lead
Mercury
Nickel
Selenium
Silver
Thallium
Zinc

NONCONVENTIONAL POLLUTANTS

Ammonia
Boron
Bromide
Chemical Oxygen Demand (COD)
Fluoride
Free Chlorine
Nitrates
Sulfate
Sulfide
Surfactants
Total Dissolved Solids
Total Kjeldahl Nitrogen
Total Organic Carbon (TOC)
Total Phenols (4-AAP)
Total Phosphorus

NONCONVENTIONAL METAL POLLUTANTS

Aluminum
Barium
Boron
Calcium
Cobalt
Iron
Magnesium
Manganese
Molybdenum
Tin
Titanium
Vanadium
Yttrium

CONVENTIONAL POLLUTANTS

Biochemical Oxygen Demand (BOD_5)
pH
Oil and Grease
Total Suspended Solids (TSS)

---

[1] These compounds were removed from the priority pollutant list (see 46 FR 2266, January 8, 1981, and 46 FR 10723, February 4, 1981).

Table VI-16

ANALYTICAL METHODS SUMMARY

Conventional and Nonconventional Pollutants	USEPA Methods†	Standard Methods††
BOD_5	405.1	
COD	410.1, 410.2	
TOC	415.1	
TSS	160.2	
Bromide		405
Fluoride	340.1	
Ammonia	350.1	
Total Kjeldahl Nitrogen (TKN)	351.3	
Nitrate-Nitrite Nitrogen (as N)	353.2	
Oil and Grease		503C
Phosphorus (total)	365.1	
Boron		404B
Sulfate (as SO4=)	375.2	
Sulfide (as S)	376.2	
Surfactants (MBAS)	425.1	512A
pH	150.1	
Cyanide (total)	335.3	
Phenols (total)	420.2	
Metals	Inductively Coupled Plasma (ICP) Opticals - Emission Spectrometer Method (Task 1)†††	
Calcium		
Magnesium		
Sodium		
Aluminum		
Manganese		
Vanadium		
Boron		
Barium		
Molybdenum		
Tin		
Yttrium		
Cobalt		
Iron		
Titanium		

†USEPA Methods for Chemical Analysis of Water and Wastes, USEPA, Environmental Monitoring and Support Laboratory, Cincinnati, Ohio, March 1979, EPA-600/4-79-020.

††Standard Methods for the Examination of Water and Wastewater, 15 Edition, 1981.

†††Procedures are described in "Guidelines Establishing Test Procedures for Analysis of Pollutants; Proposed Regulations, Appendix IV," Federal Register, December 3, 1979, p. 69559.

Table VI-16 (Continued)

ANALYTICAL METHODS SUMMARY

Priority Toxic Pollutants	USEPA Method†
Acid Extraction	1625*
Base/Neutral Extraction	1625*
Volatile Organics	1624*
Pesticides and PCB's	608
Metals Lead Beryllium Cadmium Chromium Copper Nickel Zinc	Inductively Coupled Plasma (ICP) Optical - Emission Spectrometer Method (Task 1)††
Metals Selenium Thallium Silver Arsenic Antimony Mercury	Flameless Atomic Absorption Spectrometer Method (Task 2)†
Metals Lead Beryllium Cadmium Chromium Copper Nickel Zinc	Flame Atomic Absorption Spectrometer Method (Task 2)†

*In cases where isotopes were not available USEPA Methods 624 and 625 were used.

†USEPA Methods for Chemical Analysis of Water and Wastes, USEPA, Environmental Monitoring and Support Laboratory, Cincinnati, Ohio, March 1979, EPA-600/4-79-020.

††Procedures are described in "Guidelines Establishing Test Procedures for Analysis of Pollutants; Proposed Regulations, Appendix IV," Federal Register, December 3, 1979, p. 69559.

Table VI-17

DETECTION LIMITS FOR PRIORITY TOXIC POLLUTANTS

Pollutant	Analytical* Detection Limit (ug/l)
Base/Neutral Extractable Compounds	
N-nitrosodimethylamine	250
isophorone	50
hexachlorocyclopentadiene	250
benzidine	50
3,3'-dichlorobenzidene	50
indeno(1,2,3-cd)pyrene	25
dibenzo(ah)anthracene	25
benzo(ghi)perylene	25
all other base/neutral compounds	10
Acid Extractable Compounds	
2,4-dimethylphenol	250
2,4-dinitrophenol	250
2-methyl-4,6-dinitrophenol	250
pentachlorophenol	125
all other acid compounds	25
Volatile Compounds	
acrolein	100
acrylonitrile	100
all other volatile compounds	10
Pesticides	
aldrin	0.003
dieldrin	0.006
chlordane	0.04
4,4'-DDT	0.016
4,4'-DDE	0.006
4,4'-DDD	0.012
alpha-endosulfan	0.005
beta-endosulfan	0.010
endosulfan sulfate	0.03
endrin	0.009
endrin aldehyde	0.023
heptachlor	0.002
heptachlor epoxide	0.004

Table VI-17 (Continued)

DETECTION LIMITS FOR PRIORITY TOXIC POLLUTANTS

Pollutant	Analytical* Detection Limit (ug/l)
Pesticides (Continued)	
alpha-BHC	0.002
beta-BHC	0.004
gamma-BHC	0.004
delta-BHC	0.002
PCB-1242	0.05
PCB-1254	0.06
PCB-1221	0.10
PCB-1232	0.10
PCB-1248	0.06
PCB-1260	0.15
PCB-1016	0.04
toxaphene	0.40
Metals	
antimony	100
arsenic	53
beryllium	0.3
cadmium	4
chromium	7
copper	6
lead	42
mercury	0.1
nickel	15
selenium	75
silver	7
thallium	100
zinc	2
Others	
cyanide	20

*These analytical detection limits are from the USEPA test method for the organic acid, base neutral, and volatile pollutants. The limits for the pesticides and metals are from the Federal Register, Monday, December 3, 1979, "Guidelines Establishing Test Procedures for the Analysis of Pollutants; Proposed Regulations."

Sampling Procedure Protocols

The following procedures were used during the sampling episodes. These procedures comply with sampling method protocols.

Bottle/Glassware Preparation. Sample containers and glassware that came in contact with the process water samples were prepared according to the procedures outlined in Table VI-18. With the exceptions of grease and oil jars, volatile organic analysis vials, field blank and preservative blank containers, and the non-volatile (NVO) composite jug, sample containers were rinsed with process water prior to use.

Composite Samples. Composite samples were collected using an ISCO Model 1580 Sampler equipped with new silastic pump tubing and new teflon sample lines. An aluminum rod was used to anchor the sample line in place if necessary. The equipment was programmed to collect a minimum of nine quarts (8,516 milliliters) of process water over the duration of each sampling day. The minimum aliquot size was 100 milliliters and the maximum interval between aliquot collection was 30 minutes.

The operation of each sampler was checked periodically throughout the sampling day. Batteries used with the samplers were changed on a daily basis to avoid problems.

At the conclusion of collection of each composite sample period, contents of the jug were thoroughly mixed by shaking before being transferred to individual containers. Graduated cylinders were used to transfer the sample from the sample jug to the container to avoid spillage.

Free Chlorine Determination. A free chlorine determination was made with potassium iodide paper at each sampling point at the beginning of each sampling day. The appropriate samples were preserved if free chlorine was present in excess of 1 ppm.

Sample Preservation. All samples were maintained at 4°C during the sampling period. All preservatives were purchased fresh and placed in new containers. Cyanide and phenol samples were collected via grab samples and preserved with appropriate chemicals as soon as they were collected. Oil and grease samples were single grab samples preserved with sulfuric acid. VOA samples were individual grab samples collected four times per day and preserved with sodium metabisulfate, if necessary. Individual pipets were used for each preservative and discarded after use to avoid cross-contamination.

pH Measurement. pH was monitored at each sampling location using pH meters. The meter was buffered before use with pH 4, 7, and

Table VI-18

CONTAINER AND GLASSWARE PREPARATION PROCEDURES

Container	Type	Size	Preparation
Composite Jug	Glass	2.5-5 gallons	Scrub with hot detergent water, rinse with tap water, rinse with blank water, rinse with methylene chloride. Use Teflon liners in caps.
NVO Jug	Glass	1 gallon	
Blank Water Jug	Glass	1 gallon	
Graduated Cylinders	Glass	250/2000 ml	
VOA Vial, Septa, Screw Cap	Glass	40 ml	New containers were used each time after being cleaned according to procedures outlined above.
Phenol	Amber Glass	8 ounce	New containers, caps and Teflon liners washed with hot water, rinsed with tap water and blank water.
Cyanide	Plastic	1 quart	New containers and caps washed with hot water and rinsed with tap water and blank water.
Metals	Plastic Bottles	1 quart	New containers washed with detergent water, rinsed with tapwater, rinsed with deionized water, rinsed with 1:1 ultra-pure nitric acid.
Conventional/Nonconventional Pollutants	Plastic	0.5 gallon	New containers.
Acidified Conventional/Nonconventional Pollutants	Plastic	quart	New containers.

Table VI-18 (Continued)

CONTAINER AND GLASSWARE PREPARATION PROCEDURES

Container	Type	Size	Preparation
Sulfide	Plastic	pint	New containers.
Sulfite	Plastic	8 ounce	New containers.
Free Chlorine	Plastic	8 ounce	New containers.
Grease and Oil	Glass Widemouth	quart	New containers washed with soap and water, rinsed with tap water, rinsed with deionized water, rinsed with acetone, rinsed with freon.

10 buffering agents. If pH meters were not available, pH paper was used.

Temperature Measurement. Temperature was measured with metal dial thermometers. Mercury thermometers were not used because of potential contamination of the process water in case the thermometer broke.

Laboratory Quality Assurance/Quality Control (QA/QC)

Quality control measures used in the laboratory are presented in "Handbook for Analytical Quality Control in Water and Wastewater Laboratories" (published by EPA Environmental Monitoring and Support Laboratory, Cincinnati, Ohio, 1976). As part of the analytical quality control program, duplicates and blanks (including sealed VOA samples of blank water carried to each sampling site and returned unopened and samples of preserved and unpreserved equipment blank water) were analyzed. Standards and spiked samples were also analyzed. As part of the analytical QA/QC, all instruments (such as balances, spectrophotometers, and recorders) were routinely maintained and calibrated.

PROCESS WATER POLLUTANT CONCENTRATIONS

Analytical data for each type of process water were summarized and are presented in this section. The tables that present the data contain the following information for each pollutant:

1. Number of samples analyzed,
2. Number of times pollutant was detected,
3. Subcategory pollutant concentration range, and
4. Subcategory average pollutant concentration.

Table VI-19 presents these data for the three subcategories. Only pollutants that were detected one or more times are included in Table VI-19. The daily data used to calculate the summaries are presented in Appendix A.

Certain data editing rules were applied to the daily data; the data were then averaged by a flow-weighted averaging methodology to calculate the subcategory average concentrations listed in Table VI-19. The editing rules and averaging methodology are described below.

Data Editing Rules

The following editing rules were used to calculate the subcategory pollutant average concentrations:

Table VI-19

SUMMARY OF SAMPLE DATA

CONTACT COOLING AND HEATING WATER SUBCATEGORY

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Conventional				
biochemical oxygen demand (BOD_5)	43	43	2.3-96.9	1
oil and grease	47	47	0-75	2
pH	35	35	5.4-8.3	NA
total suspended solids (TSS)	38	38	<1-104	0.6
Nonconventional				
aluminum	34	19	ND-0.800	0.044
ammonia nitrogen	38	37	0-8.4	0.035
barium	34	22	ND-0.190	0.001
boron	34	18	ND-0.17	0.0006
bromide	21	21	<0.4-0.8	636†
calcium	34	34	2.0-406	3.59
chemical oxygen demand (COD)	47	47	<5-800	26
cobalt	34	11	ND-0.142	0.018
cyanide (amenable)	19	19	0-<0.01	0
fluoride	21	21	0.08-1.25	0.211
iron	34	32	ND-9.85	0.156
Kjeldahl nitrogen	38	32	ND-1.15	0.034
magnesium	34	34	0.7-29.8	0.412
manganese	34	14	ND-0.210	0.005
molydenum	34	5	ND-0.15	0.004
nitrate	21	21	<0.1-2.1	0.062
sodium	34	34	1.8-207	0.861
sulfate	21	21	<5-1,180	1.04

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CONTACT COOLING AND HEATING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Nonconventional (Cont.)				
sulfide	19	19	<1	0
surfactants	36	36	0-28.86	0.013
tin	34	10	ND-0.12	31†
titanium	34	17	ND-0.290	0.0004
total dissolved solids (TDS)	17	17	66-800	68.1
total organic carbon (TOC)	47	47	1-144	8
total phenols	39	39	<0.001-20.86	0.006
total phosphorus	38	38	<0.003-3.25	0.281
vanadium	35	6	ND-0.056	0.0008
yttrium	35	3	ND-0.019	75†
Priority Toxic				
1. acenaphthene	38	4	ND-<0.01	1†
4. benzene	41	22	ND-0.045	0.012
5. benzidine	37	2	ND-<0.01	9†
6. carbon tetrachloride (tetrachloromethane)	41	9	ND-0.008	92†
7. chlorobenzene	38	6	ND-0.0032	8†
10. 1,2-dichloroethane	39	1	ND-<0.01	0.07†
11. 1,1,1-trichloroethane	38	21	ND-0.093	0.024
22. parachlorometa cresol	38	16	ND-0.043	0.022
23. chloroform	41	32	ND-0.115	0.001
24. 2-chlorophenol	38	1	ND-<0.01	0.07†

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CONTACT COOLING AND HEATING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Priority Toxic (Cont.)				
25. 1,2-dichlorobenzene	38	1	ND-<0.01	0.07†
26. 1,3-dichlorobenzene	38	1	ND-<0.01	0.07†
27. 1,4-dichlorobenzene	38	1	ND-<0.01	0.07†
30. 1,2-trans-dichloroethylene	41	3	ND-0.017	0.0001
31. 2,4-dichlorophenol	38	1	ND-<0.01	0.07†
38. ethylbenzene	41	7	ND-<0.01	6†
39. fluoranthene	37	2	ND-<0.01	4†
41. 4-bromophenyl phenyl ether	38	1	ND-0.00042	23†
44. methylene chloride (dichloromethane)	41	36	ND-0.33	0.023
47. bromoform	41	10	ND-0.024	0.0003
48. dichlorobromomethane	41	18	ND-0.007	8†
49. trichlorofluoromethane	41	11	ND-0.004	18†
51. chlorodibromomethane	41	9	ND-0.001	0.0003
54, isophorone	38	1	ND-0.00096	53†
55. naphthalene	38	1	ND-0.018	2†
57. 2-nitrophenol	38	5	ND-0.003	19†
58. 4-nitrophenol	38	3	ND-0.004	0
60. 4,6-dinitro-o-cresol	38	1	ND-0.004	0.9†
61. N-nitrosodimethylamine	38	1	ND-<0.01	0.0002
62. N-nitrosodiphenylamine	38	2	ND-0.006	7†
65. phenol	38	20	ND-0.910	0.004
66. bis(2-ethylhexyl) phthalate	38	37	ND-1.72	0.098
67. butyl benzyl phthalate	38	4	ND-0.006	33†

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CONTACT COOLING AND HEATING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Priority Toxic (Cont.)				
68. di-n-butyl phthalate	38	36	ND-0.013	0.001
69. di-n-octyl phthalate	38	7	ND-0.021	0.0001
70. diethyl phthalate	38	22	ND-0.964	0.005
71. dimethyl phthalate	38	4	ND-0.087	0.0002
72. benzo(a)anthracene (1,2-benzoanthracene)	38	3	ND-<0.01	5†
73. benzo(a)pyrene (3,4-benzopyrene)	38	3	ND-0.012	99†
76. chrysene	38	1	ND-<0.01	0.07†
78. anthracene	38	6	ND-<0.01	0.002
80. fluorene	38	2	ND-<0.01	22†
81. phenanthrene	38	4	ND-<0.01	37†
85. tetrachloroethylene	38	6	ND-0.014	4†
86. toluene	41	16	ND-0.015	0.0001
87. trichloroethylene	38	8	ND-0.215	0.0003
89. aldrin	41	6	ND-<0.005	0.2†
90. dieldrin	38	6	ND-<0.005	0.2†
92. 4,4'-DDT	41	1	ND-22†	0.1†
93. 4,4'-DDE	41	2	ND-45†	9†
94. 4,4'-DDD	38	1	ND-40†	2†
97. endosulfan sulfate	38	1	ND-0.00013	0.3†
98. endrin	38	2	ND-<0.005	0.06†
99. endrin aldehyde	38	3	ND-66†	0.3†
100. heptachlor	38	3	ND-28†	0.3†
101. heptachlor epoxide	38	1	ND-0.0004	0.02†

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CONTACT COOLING AND HEATING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Priority Toxic (Cont.)				
102. alpha-BHC	38	17	ND-0.0006	36†
103. beta-BHC	38	11	ND-0.0006	9†
104. gamma-BHC	38	14	ND-349†	2†
105. delta-BHC	38	11	ND-107†	40†
114. antimony	35	8	ND-0.03	0.006
115. arsenic	34	2	ND-0.016	0.0015
117. beryllium	35	2	ND-0.003	19†
118. cadmium	34	13	ND-0.071	0.0007
119. chromium (total)	34	12	ND-0.200	0.002
120. copper	34	25	ND-2.2	0.001
121. cyanide (total)	38	36	ND-<0.02	0
122. lead	34	14	ND-0.292	0.100
123. mercury	34	3	ND-0.0007	0.1†
124. nickel	34	8	ND-3.88	0.003
125. selenium	34	6	ND-0.012	0
126. silver	34	8	ND-0.016	56†
127. thallium	34	2	ND-0.126	57†
128. zinc	34	25	ND-0.770	0.009

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CLEANING WATER SUBCATEGORY

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Conventional				
biochemical oxygen demand (BOD_5)	26	26	2.6-1,000	90
oil and grease	26	26	0-684	48
total suspended solids (TSS)	28	28	2-16,363	714
pH	26	26	1.6-11.5	NA
Nonconventional				
aluminum	25	17	ND-8.1	0.276
ammonia nitrogen	28	28	0-399	11
barium	26	19	ND-0.8	0.017
boron	26	16	ND-2.9	0.091
bromide	10	10	<0.4	0
calcium	26	25	ND-207	3.88
chemical oxygen demand (COD)	28	28	48-2,280	115
cyanide (amenable)	20	5	0-0.174	0
fluoride	10	10	<0.1-6.8	0.201
iron	26	20	ND-51.3	1.61
Kjeldahl nitrogen	28	25	0-3,070	127
magnesium	26	26	0.154-24.9	1.66
manganese	26	16	ND-0.519	0.017
molybdenum	26	3	ND-0.3	0.009
nitrate/nitrite	10	10	<0.1-2.1	0.012
sodium	26	25	ND-3,860	107
sulfate	10	10	<5-45	1.52
sulfide	9	9	<1	0
surfactants	27	26	ND-148	7.95

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CLEANING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Nonconventional (Cont.)				
tin	26	7	ND-1.2	0.033
titanium	26	17	ND-0.199	0.004
total dissolved solids (TDS)	20	17	0-13,000	928
total organic carbon (TOC)	28	28	19.5-10,038	634
total phenols	22	22	<0.001-730	36
total phosphorus	28	28	0.005-123	7
yttrium	25	3	ND-0.006	77†
Priority Toxic				
4. benzene	26	18	ND-0.099	0.002
7. chlorobenzene	26	2	ND-<0.001	24†
11. 1,1,1-trichloroethane	26	14	ND-0.020	0.0004
13. 1,1-dichloroethane	26	1	ND-0.003	65†
22. parachlorometa cresol	26	9	ND-0.042	0.0001
23. chloroform	26	12	ND-0.19	0.0004
24. 2-chlorophenol	26	1	ND-0.006	0.0001
26. 1,3-dichlorobenzene	26	1	ND-0.001	6†
30. 1,2-trans-dichloroethylene	26	2	ND-<0.010	36†
31. 2,4-dichlorophenol	26	1	ND-0.001	22†
38. ethylbenzene	26	3	ND-<0.010	58†
39. fluoranthene	26	6	ND-<0.010	76†
44. methylene chloride (dichloromethane)	26	23	ND-0.310	0.012
47. bromoform (tribromomethane)	26	3	ND-0.010	6†

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CLEANING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Priority Toxic (Cont.)				
48. dichlorobromomethane	26	2	ND-0.015	0.0001
49. trichlorofluoromethane	26	5	ND-0.034	0.004
51. chlorodibromomethane	26	2	ND-0.002	18†
55. naphthalene	26	1	ND-<0.010	42†
57. 2-nitrophenol	26	1	ND-<0.010	12†
60. 4,6-dinitro-o-cresol	26	1	ND-0.004	64†
62. N-nitrosodiphenylamine	26	13	ND-0.064	0.002
64. pentachlorophenol	26	2	ND-0.02	0.0002
65. phenol	26	19	ND-6.0	0.198
66. bis(2-ethylhexyl) phthalate	26	24	ND-0.196	0.007
67. butyl benzyl phthalate	26	2	ND-<0.010	32†
68. di-n-butyl phthalate	26	16	ND-0.023	0.002
69. di-n-octyl phthalate	26	1	ND-<0.010	7†
70. diethyl phthalate	26	14	ND-<0.010	0.0009
72. benzo(a)anthracene (1,2-benzoanthracene)	26	2	ND-<0.010	15†
73. benzo(a)pyrene (3,4-benzopyrene)	26	2	ND-<0.010	0.0008
76. chrysene	26	9	ND-<0.010	0.0003
78. anthracene	26	5	ND-<0.010	0.0001
80. fluorene	26	1	ND-<0.010	23†
81. phenanthrene	26	4	ND-<0.010	0.0001
84. pyrene	26	4	ND-<0.010	70†
85. tetrachloroethylene	26	3	ND-<0.010	0

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

CLEANING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Priority Toxic (Cont.)				
86. toluene	26	15	ND-0.69	0.013
87. trichloroethylene	26	5	ND-<0.010	73†
89. aldrin	26	4	ND-<0.005	25†
90. dieldrin	26	1	ND-<0.005	4†
97. endosulfan sulfate	26	2	ND-<0.005	5†
98. endrin	26	2	ND-<0.005	0.0004
100. heptachlor	26	4	ND-<0.005	27†
102. alpha-BHC	26	5	ND-6†	0.1†
103. beta-BHC	26	5	ND-0.0002	9†
104. gamma-BHC	26	6	ND-<0.005	66†
105. delta-BHC	26	9	ND-0.0005	70†
114. antimony	26	6	ND-0.133	0.003
115. arsenic	26	8	ND-0.12	0.0002
119. chromium (total)	26	9	ND-0.53	0.019
120. copper	26	18	ND-1.44	0.044
121. cyanide (total)	26	28	0-0.034	0
123. mercury	26	3	ND-0.0005	8†
124. nickel	26	3	ND-0.166	0.004
125. selenium	26	8	ND-0.28	0.013
126. silver	26	3	ND-0.018	0.0002
128. zinc	26	22	ND-29.8	0.598

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

FINISHING WATER SUBCATEGORY

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Conventional				
Biochemical oxygen demand (BOD_5)	9	9	3.8-14	6
oil and grease	9	6	0-19.7	8
total suspended solids (TSS)	9	7	0-1,359	95
pH	9	9	6.36-8.4	NA
Nonconventional				
aluminum	9	5	ND-9.75	2.32
barium	9	5	ND-0.065	0.022
boron	9	4	ND-0.700	
calcium	9	8	2.97-19.3	1.06
chemical oxygen demand (COD)	9	8	<5-325	17
iron	9	7	ND-9.66	1.62
magnesium	9	8	0.386-5.1	0.102
manganese	9	5	ND-0.308	0.069
sodium	9	8	11.7-318	9.73
titanium	9	3	ND-0.076	0.009
total organic carbon (TOC)	9	9	2-238	23
total phenols	9	6	<0.01-8.75	0.217
Priority Toxic				
4. benzene	9	2	ND-0.009	0.0005
8. 1,2,4-trichlorobenzene	9	2	ND-0.01945	0.006
11. 1,1,1-trichloroethane	9	1	ND-0.018	0.001
12. hexachloroethane	9	1	ND-0.00666	0

Table VI-19 (Continued)

SUMMARY OF SAMPLE DATA

FINISHING WATER SUBCATEGORY (Cont.)

Pollutant	Number of Samples	Number of Times Detected	Concentration Range (mg/l)	Flow-Weighted Average Concentration (mg/l)
Priority Toxic (Cont.)				
28. 3,3'-dichlorobenzidine	9	1	ND-0.01289	0.002
34. 2,4-dimethylphenol	9	2	ND-0.00591	0
38. ethylbenzene	9	3	ND-0.01149	0.005
44. methylene chloride (dichloromethane)	9	1	ND-0.006	0
65. phenol	9	3	ND-0.2	0.007
66. bis(2-ethylhexyl) phthalate	9	9	0.003-1.48768	0.479
68. di-n-butyl phthalate	9	6	ND-0.08085	0.031
71. dimethyl phthalate	9	2	ND-0.19438	0.034
87. trichloroethylene	9	3	ND-0.01511	0.004
114. antimony	9	2	ND-0.01	0.001
115. arsenic	9	3	ND-0.11	0.001
119. chromium (total)	9	2	ND-0.01	0.001
120. copper	9	5	ND-0.073	0.028
122. lead	9	1	ND-0.179	0.030
121. cyanide	3	2	0-0.015	0.010
123. mercury	9	3	ND-0.00025	15†
124. nickel	9	2	ND-0.04	0.004
125. selenium	9	3	ND-0.30	0.030
128. zinc	9	7	ND-0.229	0.087

NA - Average concentration is not applicable for pH.

†Concentration is in nanograms per liter.

1. All non-detected results were averaged as zero.

2. The source water concentration was subtracted from the process water concentration. If a negative number resulted, zero was used in the average.

3. Laboratory values below the method detection limit were averaged as the reported value.

4. Laboratory values reported as less than values for organic compounds were averaged as the values without the less than sign.

5. Duplicate data were treated as data for an additional sampling day.

6. For the priority toxic pollutant metals, when both the Task 1 (Inductively Coupled Plasma Optical) and Task 2 (Flame Atomic Absorption) analyses were performed, only the Task 1 test results were used in the averaging process. A metal laboratory result reported as a less than value was treated as a non-detected result in the averaging methodology.

These editing rules vary from the editing rules used to develop pollutant averages for the proposed PM&F regulation. At proposal, the following editing rules were used:

1. Non-detected values were excluded from the data base.

2. Source water concentrations were not subtracted from the process water concentration.

3. Laboratory values equal to or below the method detection limit were excluded from the data base.

4. Laboratory values reported as less than values for organic compounds were excluded from the data base. These less than values were usually equal to the method detection limit.

5. Duplicate data were treated as data for an additional sampling day.

6. For the priority metal pollutants, when both the Task 1 (Inductively Coupled Plasma Optical) and Task 2 (Flame Atomic Absorption) analyses were performed, only the Task 1 test results were used in the data base. A metal laboratory result reported as a less than value was treated as a non-detected result in the averaging methodology.

EPA's pre-proposal editing rules that excluded values in the averaging methodology lead to examination of the process water characteristics on a worse-case basis. By not considering non-detected values, the concentration average was skewed conservatively high. The post-proposal editing rule that includes all non-detected data points as zeros in the averaging of data recognizes that even though certain pollutants were not detected, the resulting data (i.e., that indicating non-detection) are valid data. These values were included in subcategory average pollutant concentration calculations to ensure proper characterization of subcategory process water instead of only characterizing a segment of the subcategory process water where pollutants were found above their detection limits.

At proposal, EPA did not subtract the source water concentration from the process water concentration prior to averaging the process water concentration because the plant's source water pollutant concentrations contribute to the overall effluent concentrations. However, EPA decided to subtract the source water concentration from the process water concentration before averaging the data for development of the final regulation. This allowed the Agency to determine the pollutants that were added to process water from the PM&F processes.

EPA used laboratory results equal to or below the method detection limit in developing the final PM&F regulation because the Agency believes that all reported values should be used to calculate average concentrations even though a value may be below a method detection limit. In addition, EPA had no reason to believe such data were not valid. Therefore, the data were used to calculate the subcategory average concentrations.

To develop the final regulation, laboratory results for organic compounds that were reported as less than values, were averaged as the value without the less than sign. As discussed above, EPA believes that all data should be used to calculate the pollutant averages for the PM&F subcategories. By using the value without the less than sign, the Agency was conservative in assuming that the pollutant was present.

The treatment of duplicate data did not change between proposal and promulgation. EPA considered duplicate data as data for an additional sampling day.

Likewise, the use of Task 1 metal analyses, instead of Task 2 metal analyses when results from both analyses were available, did not change between proposal and promulgation. EPA used Task 1 analyses results because only those results were available for all sampled processes. The use of reported less than values did not change between the proposed and promulgated regulation. A reported metal less than value was treated as a non-detected result.

Pollutant Average Concentration Methodology

For the proposed PM&F rule, EPA used subcategory average pollutant concentrations to characterize PM&F process waters and then to determine which pollutants warranted control by the effluent limitations guidelines and standards for a subcategory. The Agency estimated subcategory average pollutant concentrations by obtaining an arithmetic average of the pollutant concentrations found in PM&F process waters during several sampling episodes. Based on these estimates, EPA identified pollutants present in treatable concentrations and then selected various technology options to control those pollutants.

Several commenters on the proposal stated that the subcategory average pollutant concentrations should be estimated by flow-weighting the sampling data because arithmetic averages overestimate the concentrations of the pollutants in PM&F process waters. They claimed that flow-weighted averages should be used to account for the wide variation in the amount of process water discharged by the processes that were sampled. Commenters also stated that different average pollutant concentrations should be calculated for extrusion processes in the contact cooling and heating water subcategory and for other processes in that subcategory. According to the commenters, extrusion processes have the highest water use in that subcategory and process water from those processes does not contain pollutants in high concentrations.

EPA reviewed the variation in the amount of water discharged by processes sampled during the development of the PM&F regulation. The Agency determined that there is wide variation in the discharge rates and that the variation should be considered when subcategory average pollutant concentrations are estimated. EPA also determined that flow-weighted average pollutant concentrations provide a better estimate of the pollutant concentrations found in PM&F process waters because that type of average addresses the impact of the wide variation in discharge rates. More weight is given to high flow rate processes than to low flow rate processes when flow-weighted concentrations are calculated. When arithmetic averages are calculated, all processes are given the same weight regardless of their discharge rate. In developing the final PM&F regulation, EPA relied on flow-weighted pollutant averages to estimate the pollutant concentrations found in process water discharged from processes in each subcategory.

In response to the comment concerning separate average concentrations for the extrusion processes, the Agency proportioned the flow-weighted concentrations for the contact cooling and heating water subcategory by the number of processes for each type of contact cooling and heating water process in the questionnaire data base. This gave more weight to extrusion processes because the largest number of processes in the data base for the contact cooling and heating water subcategory are extrusion processes.

Presented below is the methodology that the Agency used to flow-weight the pollutant concentration data. This methodology uses analytical results and flow data from the sampling episode; it also uses weighting factors from the questionnaire data base to determine the predominance of a type of process in the contact cooling and heating water subcategory. Table VI-20 presents the sampling data used in the example presented below. Table VI-21 presents the questionnaire data base weighting factors that were used in the concentration averaging methodology. The methodology steps described below were applied to the data in Tables VI-20 and VI-21 in the following example:

1. The processes contributing to each type of process water are separated into similar types of processes (i.e., extrusion, molding, calendering, thermoforming, and casting processes are separated within the contact cooling and heating water subcategory).

   There are two extrusion processes and one molding process in the example. The extrusion processes are denoted as EX-1 and EX-2, and the molding process is denoted as MD-1 in Table VI-20.

2. The daily concentrations for each process are flow-weighted to obtain an average daily flow-weighted concentration. The process water usage flow rates measured on the sampling days are used to flow-weight the concentrations.

Process	Average Daily Flow-Weighted Concentration (mg/l)
EX-1	$\frac{(10\text{ mg/l})(100\text{ l/hr}) + (30\text{ mg/l})(140\text{ l/hr}) + (15\text{ mg/l})\ (100\text{ l/hr})}{(100\text{ l/hr} + 140\text{ l/hr} + 100\text{ l/hr})} = 19.7\text{ mg/l}$
EX-2	$\frac{(50\text{ mg/l})\ (300\text{ l/hr}) + (10\text{ mg/l})\ (400\text{ l/hr})}{(300\text{ l/hr} + 400\text{ l/hr})} = 27\text{ mg/l}$
MD-1	$\frac{(100\text{ mg/l})(50\text{ l/hr}) + (110\text{ mg/l})(60\text{ l/hr}) + (120\text{ mg/l})\ (60\text{ l/hr})}{(50\text{ l/hr} + 60\text{ l/hr} + 60\text{ l/hr})} = 111\text{ mg/l}$

Table VI-20

DATA FOR POLLUTANT X - CALCULATION OF AVERAGE CONCENTRATION EXAMPLE

Process	Concentration* Day 1	Flow** Day 1	Concentration Day 2	Flow Day 2	Concentration Day 3	Flow Day 3	Concentration Dup.	Flow Dup.
Extrusion (EX-1)	10	100	---	---	30	140	15	100
Extrusion (EX-2)	50	300	10	400	---	---	---	---
Molding (MD-1)	100	50	---	---	110	60	120	60

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*Concentrations are in mg/L.

**Flow rates are in l/hr.

Table VI-21

QUESTIONNAIRE DATA BASE WEIGHTING FACTORS FOR FLOW-WEIGHTED CONCENTRATION METHODOLOGY

CONTACT COOLING WATER SUBCATEGORY

Type of Process	Percentage of Processes* in Questionnaire Data Base
Extrusion	85.05
Molding	7.48
Coating and Laminating	3.04
Thermoforming	2.33
Casting	1.40
Calendering	0.70
	100.00

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*See Table VI-6.

3. For each process, the water usage flow rates measured on the sampling days are averaged. This is the average process water usage rate.

Process	Average Process Water Usage Rate (l/hr)
EX-1	$\frac{100 + 140 + 100}{3} = 113$ l/hr
EX-2	$\frac{300 + 400}{2} = 350$ l/hr
MD-1	$\frac{50 + 60 + 60}{2} = 85$ l/hr

4. The average daily flow-weighted concentrations (calculated in step 2) for all similar processes in a subcategory are flow-weighted using the average process water usage rates (calculated in step 3). For example, the average daily flow-weighted concentrations of extrusion processes within the contact cooling and heating water subcategory are flow-weighted together. This resulting concentration is the type-of-process flow-weighted concentration.

Type of Process	Type-of-Process Flow-Weighted Concentration (mg/l)
Extrusion	$\frac{(19.7 \text{ mg/l})\ (113 \text{ l/hr}) + (27 \text{ mg/l})\ (350 \text{ l/hr})}{(113 \text{ l/hr} + 350 \text{ l/hr})}$
	= 25.2 mg/l
Molding	$\frac{(111 \text{ mg/l})\ (85 \text{ l/hr})}{(85 \text{ l/hr})} = 111$ mg/l

5. The average process water usage rates (calculated in step 3) are averaged together for all similar processes to calculate a type-of-process average water usage flow rate.

Type of Process	Type-of-Process Average Water Usage Flow Rate (l/hr)
Extrusion	(113 l/hr + 350 l/hr)/2 = 232 l/hr
Molding	85 l/hr

6. The average pollutant mass for a type of process is calculated by multiplying the type-of-process flow-weighted concentration (calculated in step 4) by the type-of-process average water usage flow rate (calculated in step 5).

Type of Process	Average Pollutant Mass (mg/hr)
Extrusion	(25.2 mg/l) (232 l/hr) = 5,850 mg/hr
Molding	(111 mg/l) (85 l/hr) = 9,440 mg/hr

7. For each type of process, the average pollutant mass (calculated in step 6) is weighted by the predominance of that type of process in the questionnaire data base. The weighted average pollutant masses for the different types of processes are then summed together. Extrusion processes comprise 85.05 percent and molding processes comprise 7.48 percent of the questionnaire data base contact cooling and heating water processes (from Table VI-21).

Type of Process	Weighted Pollutant Mass (mg/hr)
Extrusion	(0.8505) (5,850 mg/hr) = 4,970
Molding	(0.0748) (9,440 mg/hr) = 706
	TOTAL 5,676 mg/hr

8. For each type of process, the type-of-process average water usage flow rate (calculated in step 5) is also weighted by the predominance of that type of process in the questionnaire data base. The weighted type-of-process average flows for the different types of processes in the contact cooling and heating water subcategory are summed together.

Type of Process	Weighted Type-of-Process Average Water Usage Flow Rate (l/hr)
Extrusion	(0.8505) (232 l/hr) = 197
Molding	(0.0748) (85 l/hr) = 6.4
	TOTAL 203.4 l/hr

9. The subcategory average concentration is calculated by dividing the total weighted pollutant mass (calculated in step 7) by the total weighted flow (calculated in step 8).

Subcategory Average Concentration (mg/l)

Pollutant X (5,676 mg/hr)/(203.4 l/hr) = 27.9 mg/l

The calculation procedure is more simplified for the cleaning water subcategory and the finishing water subcategory because these subcategories have only one type of process (i.e., cleaning or finishing processes). The same methodology is used except for proportioning the average by type of process.

SAMPLED PLANTS WITH WASTEWATER TREATMENT SYSTEMS

Wastewater treatment technologies exist at four of the plants (i.e., plants C, E, F, and I) that were sampled in 1980, at one plant (i.e., Plant B) that was sampled in 1983, and at three plants that were sampled in 1984 (i.e., plants M, N, and R). Of the sampled treatment systems, plants I, M, N, and R had a wastewater treatment system primarily for PM&F process waters.

The treatment at Plant I consists of equalization, pH adjustment, and filtration (see Figure VI-9). Treatment at Plant M consists of filtration and settling of contact cooling water. Figure VI-12 illustrates this treatment. Process water from the grinding operation at Plant N is filtered before discharge (see Figure VI-13). Treatment for recycled contact cooling water at Plant R consists of solids skimmings from a collection sump and filtration through a bag filter (see Figure VI-17). Effluent data for these treatment processes are presented in Appendix A.

The treatment process at Plants B, C, E, and F is a lagoon that treats a combined wastewater. Effluents from the lagoons at Plants E and F were sampled during this project. These effluent data were not used in the data analyses for the PM&F regulation because they treat more than just PM&F process waters. Those data are contained in the administrative record for the regulation.

SOLUTION CASTING/SOLVENT RECOVERY SAMPLING DATA

Wastewater is also generated by the solvent recovery operation in the solution or solvent casting process. However, this wastewater does not result from the blending, molding, forming, or any processing of the plastic material and is not a process water. Samples of this wastewater indicate that its pollutant characteristics are different from the characteristics of PM&F process waters. In addition, the Agency estimates that only eight plants in the category generate solvent recovery wastewater. For these reasons, the Agency believes that solvent recovery wastewater is best controlled on a case-by-case basis by the permit writer or control authority. Analytical data for this type of wastewater from the Agency's study of the plastics molding and forming category may be used as a guide by the permit writer. Appendix A presents wastewater pollutant characteristics for a solution casting process at Plant G. See Figure VI-7 for a process diagram.

TOTAL PHENOLS VERIFICATION AT PLANT F

The sample points shown in Figure VI-6 were resampled in 1984 to verify the process water total phenols concentrations at Plant F. All samples had total phenols samples of less than 0.01 mg/l. Because the concentrations from the 1980 sampling episode, ranging from <5 to 1,670 mg/l, could not be explained by plant personnel and because the 1984 sampling data do not verify the 1980 analytical results, the total phenols data from Plant F were not used to obtain a subcategory average concentration for total phenols.

SECTION VII

POLLUTANTS IN PLASTICS MOLDING AND FORMING PROCESS WATERS

The Agency studied the plastics molding and forming category to determine the presence of conventional, selected nonconventional, and priority toxic pollutants in PM&F process waters.

CONVENTIONAL POLLUTANTS

As previously mentioned, conventional pollutants are those defined in Section 304(a)(4) of the Act and any other pollutants defined by the Administrator as conventional pollutants. The list of conventional pollutants currently includes: biochemical oxygen demand (BOD), total suspended solids (TSS), fecal coliform, pH, and oil and grease.

Samples collected during the 1980, 1983, and 1984 sampling episodes for the PM&F regulation were analyzed for BOD_5, TSS, oil and grease, and pH. All of these pollutants warrant further consideration for control in the cleaning water subcategory because they were found in treatable concentrations in the cleaning process waters. In the finishing water subcategory, total suspended solids (TSS) were found in concentrations that warrant control. The contact cooling and heating water subcategory does not have treatable concentrations of BOD_5, oil and grease, or TSS. Refer to Table VII-1 for the average concentrations of the conventional pollutants that are controlled in each subcategory.

NONCONVENTIONAL POLLUTANTS

Samples collected during the 1980, 1983, and 1984 sampling episodes were also analyzed for the nonconventional pollutants listed in Table VII-2. These pollutants were selected for analysis based on knowledge of the raw materials used in the PM&F category and on the potential for those pollutants to be discharged in PM&F process waters.

Results of the sample analyses indicate that only three nonconventional pollutants were found in treatable concentrations in cleaning process waters. They are: chemical oxygen demand (COD), total organic carbon (TOC), and total phenols. Refer to Table VII-3 for the average concentrations of the nonconventional pollutants in cleaning water.

Nonconventional pollutants were not found in treatable concentrations in contact cooling and heating waters or in finishing waters.

Table VII-1

CONVENTIONAL POLLUTANT AVERAGE CONCENTRATIONS - PM&F PROCESS WATERS

	Average Concentrations (mg/l)**		
Conventional Pollutants	Contact Cooling and Heating Water	Cleaning Water	Finishing Water
BOD_5	*	90	*
Oil and Grease	*	48	*
TSS	*	714	95
pH range	5.4-8.3	1.6-11.5	*

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*Average concentrations below treatable concentrations.

**Subcategory average concentrations are from Table VI-19.

Table VII-2

NONCONVENTIONAL POLLUTANTS FOR WHICH SAMPLES WERE ANALYZED

Nonconventional Pollutant	Sampling Episode Year 1980	1983	1984
Ammonia	X	X	
Boron		X	
Bromide		X	
Chemical oxygen demand (COD)	X	X	X
Cyanide (amenable)	X		
Fluoride		X	
Free chlorine		X	X
Nitrates		X	
Sulfate		X	
Sulfide		X	
Surfactants	X	X	
Total dissolved solids	X		
Total Kjehdahl nitrogen	X	X	
Total organic carbon (TOC)	X	X	X
Total phenols	X	X	X
Total phosphorus	X	X	

Table VII-3

NONCONVENTIONAL POLLUTANT AVERAGE CONCENTRATIONS - CLEANING WATER SUBCATEGORY

Nonconventional Pollutant	Average Concentration (mg/l)*
COD	115
TOC	634
Total Phenols	36

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*Average concentrations are from Table VI-19.

In the proposed PM&F regulation, the Agency indicated that although approximately 79 percent of the mass of nonconventional pollutants in contact cooling and heating waters would be removed by the proposed BPT, EPA was going to investigate the nonconventional pollutants, particularly COD and TOC, to determine the constituents of those pollutants. Subsequent to proposal, the Agency conducted a study to determine what contributes to those pollutants.

EPA reviewed the analytical data for the contact cooling and heating water samples to determine which of the pollutants that the samples were analyzed for would contribute to the COD and TOC. By doing this, the Agency determined whether the concentrations of COD and TOC in contact cooling and heating waters were solely attributed to the organic pollutants for which analyses were conducted. Results of that work indicated that other pollutants contributed to the COD and TOC because the concentrations of COD and TOC were higher than the total of the concentrations of the organic pollutants in the contact cooling and heating waters.

The Agency believes that many different non-priority organic pollutants could have contributed to the COD and TOC concentration estimates at proposal. However, EPA could not identify those pollutants because the contact cooling and heating water samples were only analyzed for conventional, selected nonconventional, and priority toxic pollutants.

As discussed in Section VI of this development document, the Agency revised its pollutant averaging methodology for the final PM&F regulation. Flow-weighted averages were calculated for the final rule to account for the different flow rates of the sampled processes. EPA believes that flow-weighted averages provide a better estimate of the pollutant concentrations than the arithmetic averages used for the proposal.

Based on the flow-weighted subcategory average concentrations for the COD and TOC, those pollutants are not present in treatable concentrations in contact cooling and heating waters. The Agency does not believe that the masses of COD and TOC in contact cooling and heating waters calculated using the flow-weighted subcategory averages are significant.

PRIORITY TOXIC POLLUTANTS

List of Pollutants

One hundred and twenty-nine priority toxic pollutants were studied for the PM&F regulation pursuant to the requirements of the Clean Water Act of 1977. These pollutants, which are listed in Table VI-15, are members of the 65 compounds and classes of compounds referred to in Section 307(a)(1) of the Act.

From the original list of 129 priority pollutants, three pollutants were deleted in two separate amendments to 40 CFR Subchapter N, Part 401. Dichlorodifluoromethane and trichlorofluoromethane were deleted first (46 FR 79692; January 8, 1981) followed by the deletion of bis(chloromethyl) ether (46 FR 10723; February 4, 1981). The Agency concluded that deleting these compounds does not compromise adequate control over their discharge into the aquatic environment and that no adverse effects on the aquatic environment or on human health will occur as a result of deleting them from the list of priority toxic pollutants. Concentration data were obtained for these pollutants during the sampling episodes for this regulation because some of the PM&F samples were collected and analyzed prior to the deletion of these pollutants from the list of priority pollutants. These pollutants were not considered, however, for the final PM&F regulation.

Data on the concentration of asbestos in PM&F process waters are available from a small number of samples taken during the 1980 sampling program. Those data indicate that asbestos was not present or could not be interpreted because of the limited number of fibers counted. EPA did not analyze for asbestos in the 1983 and the 1984 sampling programs.

Exclusion of Pollutants and Subcategories

The modified Settlement Agreement in NRDC v. Train, supra, contains provisions that authorize the exclusion of priority toxic pollutants and industry subcategories from regulation in certain instances. These provisions are presented in Paragraph 8 of the modified Settlement Agreement. They are:

"1. For a specific pollutant or a subcategory or category, equally or more stringent protection is already provided by an effluent, new source performance standard, or pretreatment standard or by an effluent limitation and guideline promulgated pursuant to Section(s) 301, 304, 306, 307(a), 307(b), and 307(c) of the Act.

2. For a specific pollutant, except for pretreatment standards, the specific pollutant is present in the effluent discharge solely as a result of its presence in intake waters taken from the same body of water into which it is discharged and, for pretreatment standards, the specific pollutant is present in the effluent which is introduced into treatment works (as defined in Section 212 of the Act) which are publicly owned solely as a

result of its presence in the point source's intake waters, provided however, that such point source may be subject to an appropriate effluent limitation for such pollutant pursuant to the requirements of Section 307.

3. For a specific pollutant, the pollutant is not detectable (with the use of analytical methods approved pursuant to 304(h) of the Act, or in instances where approved methods do not exist, with the use of analytical methods which represent state-of-the-art capability) in the direct discharges or in the effluents which are introduced into publicly-owned treatment works from sources within the subcategory or category; or is detectable in the effluent from only a small number of sources within the subcategory and the pollutant is uniquely related to only those sources; or the pollutant is present only in trace amounts and is neither causing nor likely to cause toxic effects; or is present in amounts too small to be effectively reduced by technologies known to the Administrator; or the pollutant will be effectively controlled by the technologies upon which are based other effluent limitations and guidelines, standards of performance, or pretreatment standards.

4. For a category or subcategory, the amount and the toxicity of each pollutant in the discharge does not justify developing national regulations in accordance with the schedule contained in Paragraph 7(b)."

The basis for exclusion in subparagraph 2 above for the PM&F regulation is that if a pollutant was found in a higher concentration in the plant intake water (i.e., source water) than in the process water generated by the PM&F process, that pollutant would be excluded from control. Data obtained from the sampling episodes were reviewed, therefore, to determine which, if any, of the priority pollutants were excluded from control because of this reason.

With respect to subparagraph 3 for the PM&F regulation, a pollutant was considered not detected if the laboratory reported that it was not detected or if the laboratory reported that it was detected at or below the analytical detection limit. Pollutants were excluded from control if they were not detected or detected at or below their detection limit. Refer to Table VI-17 for analytical detection limits for the priority toxic pollutants. Also for the PM&F regulation, "detected in a small number of sources" was defined as detected in two or less samples when 20 or more samples were analyzed. If a pollutant was found in two or less samples when 20 or more samples were analyzed for that pollutant, it was excluded from further consideration. Another basis for exclusion in subparagraph 3 is that a pollutant is present in amounts too small to be effectively reduced by technologies known by the Administrator.

The PM&F category was reviewed to determine if any of the priority pollutants could be excluded based on Paragraph 8 of the Settlement Agreement. Each subcategory was also reviewed to determine if any priority pollutants could be excluded by subcategory. Results of those reviews are presented below.

PM&F Category. The Agency first applied the exclusion criterion that a pollutant was not detected or was detected at or below the analytical detection limit to exclude pollutants for the entire PM&F category. Table VII-4 lists 73 priority toxic pollutants that were not detected in any of the process water samples analyzed or were detected at or below the pollutant analytical detection limit. These pollutants are excluded from regulation for the PM&F category and were not considered further. Table VII-5 lists the priority pollutants that were considered further because they were detected above their analytical detection limit.

PM&F Subcategories. Priority pollutants listed in Table VII-5 were reviewed by subcategory to determine whether:

1. A pollutant was never detected in process water samples for this subcategory or was detected at or below the analytical detection limit;

2. A pollutant was found in a higher concentration in the plant intake water (i.e., source water) than in the process water generated by the PM&F process; and

3. A pollutant was detected in two or less samples when 20 or more samples were analyzed for that pollutant.

A pollutant was first reviewed to determine if it was found above the detection limit. If it was, the data were reviewed to determine if the pollutant was present in a higher concentration in the source water than in the process water. If the concentration was higher in the effluent, the pollutant was examined for occurrence in more than two samples if 20 or more samples were analyzed. If the pollutant passed all of these criteria, it was considered further for regulation. Table VII-6 presents an example of this exclusion methodology. Table VII-7 presents priority pollutants excluded from control for the PM&F subcategories using this methodology. Table VII-8 lists the priority pollutants that remain after the above mentioned exclusions and their subcategory average concentration (from Table VI-19).

Table VII-4

PRIORITY POLLUTANTS EXCLUDED FROM CONTROL FOR THE PM&F CATEGORY*

Priority Pollutant

1. acenaphthene
2. acrolein
3. acrylonitrile
5. benzidene
6. carbon tetrachloride
7. chlorobenzene
9. hexachlorobenzene
10. 1,2-dichloroethane
13. 1,1-dichloroethane
14. 1,1,2-trichloroethane
15. 1,1,2,2-tetrachloroethane
16. chloroethane
18. bis (2-chloroethyl) ether
19. 2-chloroethyl vinyl ether (mixed)
20. 2-chloronaphthalene
21. 2,4,6-trichlorophenol
24. 2-chlorophenol
25. 1,2-dichlorobenzene
26. 1,3-dichlorobenzene
27. 1,4-dichlorobenzene
29. 1,1-dichloroethylene
31. 2,4-dichlorophenol
32. 1,2-dichloropropane
33. 1,2-dichloropropylene (1,3-dichloropropene)
34. 2,4-dimethylphenol
35. 2,4-dinitrotoluene
36. 2,6-dinitrotoluene
37. 1,2-diphenylhydrazine
39. fluoranthene
40. 4-chlorophenyl phenyl ether
41. 4-bromophenyl phenyl ether
42. bis(2-chloroisopropyl) ether
43. bis(2-choroethoxy) methane
45. methyl chloride (chloromethane)
46. methyl bromide (bromomethane)
51. chlorodibromomethane
52. hexachlorobutadiene
53. hexachlorocyclopentadiene
54. isophorone
56. nitrobenzene
57. 2-nitrophenol
58. 4-nitrophenol
59. 2,4-dinitrophenol
60. 4,6-dinitro-o-cresol
61. N-nitrosodimethylamine
63. N-nitrosodi-n-propylamine
64. pentachlorophenol
67. butyl benzyl phthalate
72. benzo (a)anthracene (1,2-benzanthracene)
74. 3,4-benzofluoranthene
75. benzo(k)fluoranthane (11,12-benzofluoranthene)
76. chrysene
77. acenaphthylene
78. anthracene
79. benzo(ghi)perylene (1,11-benzoperylene)
80. fluorene
81. phenanthrene
82. dibenzo (a,h)anthracene (1,2,5,6-dibenzanthracene)
83. indeno (1,2,3-cd)pyrene (w,e,-o-phenylenepyrene)
84. pyrene
88. vinyl chloride (chloroethylene)
91. chlordane (technical mixture and metabolites)
95. alpha-endosulfan
106. PCB-1242 (Arochlor 1242)
107. PCB-1254 (Arochlor 1254)
108. PCB-1221 (Arochlor 1221)
109. PCB-1232 (Arochlor 1232)
110. PCB-1248 (Arochlor 1248)
111. PCB-1260 (Arochlor 1260)
112. PCB-1016 (Arochlor 1016)
113. toxaphene
116. asbestos
129. 2,3,7,8-tetra chlorodibenzo-p-dioxin (TCDD)

*Pollutants were either not detected in any process water samples or were detected at or below the pollutant analytical detection limit.

Table VII-5

PRIORITY POLLUTANTS DETECTED IN PM&F PROCESS WATERS

<u>Priority Pollutant</u>

4. benzene
8. 1,2,4-trichlorobenzene
11. 1,1,1-trichloroethane
12. hexachloroethane
22. parachlorometa cresol
23. chloroform (trichloromethane)
28. 3,3'-dichlorobenzidine
30. 1,2-trans-dichloroethylene
38. ethylbenzene
44. methylene chloride (dichloromethane)
47. bromoform (tribromomethane)
48. dichlorobromomethane
55. naphthalene
62. N-nitrosodiphenylamine
65. phenol
66. bis(2-ethylhexyl) phthalate
68. di-n-butyl phthalate
69. di-n-octyl phthalate
70. diethyl phthalate
71. dimethyl phthalate
73. benzo (a)pyrene (3,4-benzopyrene)
85. tetrachloroethylene
86. toluene
87. trichloroethylene
89. aldrin
90. dieldrin
92. 4,4'-DDT
93. 4,4'-DDE(p,p'DDX)
94. 4,4'-DDD(p,p'TDE)
96. beta-endosulfan
97. endosulfan sulfate
98. endrin
99. endrin aldehyde
100. heptachlor
101. heptachlor epoxide
102. alpha-BHC
103. beta-BHC
104. gamma-BHC
105. delta-BHC
114. antimony
115. arsenic
117. beryllium
118. cadmium
119. chromium (Total)
120. copper
121. cyanide (Total)
122. lead
123. mercury
124. nickel
125. selenium
126. silver
127. thallium
128. zinc

Table VII-6

EXCLUSION METHODOLOGY EXAMPLE - POLLUTANT X

Process	Method Detection Limit (mg/l)	Pollutant X Concentration (mg/l)					
		Source	Day 1	Day 2	Day 3	Day 4	Day 5
1	2	4	~~ND~~	(3)	~~ND~~	~~ND~~	(4)
2	2	5	(5)	~~ND~~	⑥	~~ND~~	~~ND~~
3	2	ND	~~1~~	⑦	~~ND~~	~~ND~~	~~ND~~
4	2	3	~~1~~	~~2~~	(3)	~~ND~~	~~ND~~

Exclusion Methodology

1. Data are first eliminated because the pollutant was never detected or detected at or below the analytical detection limit. See sample data that have a straight line through them.

2. Data are next eliminated if the source water concentrations are equal to or greater than the effluent concentrations. See sampled data enclosed by parentheses.

3. Data are finally eliminated if only analytical results remain for two or less samples when 20 or more samples were analyzed. See sample data that are circled.

Pollutant X was excluded because it was found in two or less samples after the other data were eliminated.

Table VII-7

PRIORITY POLLUTANTS EXCLUDED FROM CONTROL

CONTACT COOLING AND HEATING WATER SUBCATEGORY

Priority Pollutants Not Detected or Detected at or Below the Analytical Detection Limit

8. 1,2,4-trichlorobenzene
28. 3,3'-dichlorobenzidine
38. ethylbenzene
48. dichlorobromomethane
62. N-nitrosodiphenylamine
114. antimony
115. arsenic
121. cyanide (Total)
125. selenium

Priority Pollutants with Concentrations in the Plant Intake Water Equal to or Greater Than the Effluent Concentrations

47. bromoform (tribromomethane)
87. trichloroethylene

Priority Pollutants Detected in Two or Less Samples When 20 or More Samples Were Analyzed

12. hexachloroethane
30. 1,2-trans-dichloroethylene
55. naphthalene
69. di-n-octyl phthalate
70. diethyl phthalate
71. dimethyl phthalate
73. benzo (a)pyrene (3,4-benzopyrene)
85. tetrachloroethylene
92. 4,4'-DDT
93. 4,4'-DDE(p,p'DDX)
94. 4,4'-DDD(p,p'TDE)
96. beta-endosulfan
97. endosulfan sulfate
98. endrin
100. heptachlor
101. heptachlor epoxide

CLEANING WATER SUBCATEGORY

Priority Pollutants Not Detected or Detected at or Below the Analytical Detection Limit

8. 1,2,4-trichlorobenzene
12. hexachloroethane
28. 3,3'-dichlorobenzidine
30. 1,2-trans-dichloroethylene
38. ethylbenzene
47. bromoform (tribromomethane)
55. naphthalene
69. di-n-octyl phthalate
70. diethyl phthalate
71. dimethyl phthalate
73. benzo (a)pyrene (3,4-benzopyrene)
85. tetrachloroethylene
87. trichloroethylene
90. dieldrin
92. 4,4'-DDT
93. 4,4'-DDE(p,p'DDX)
94. 4,4'-DDD(p,p'TDE)
96. beta-endosulfan
97. endosulfan sulfate
99. endrin aldehyde
101. heptachlor epoxide
117. beryllium
118. cadmium
122. lead
127. thallium

Priority Pollutants with Concentrations in the Plant Intake Water Equal to or Greater Than the Effluent Concentrations

23. chloroform
121. cyanide (Total)

Priority Pollutants Detected in Two or Less Samples When 20 or More Samples Were Analyzed

11. 1,1,1-trichloroethane
48. dichlorobromomethane
68. di-n-butyl phthalate
98. endrin

Table VII-7 (Continued)

PRIORITY POLLUTANTS EXCLUDED FROM CONTROL

FINISHING WATER SUBCATEGORY

Priority Pollutants Not Detected or Detected at or Below the Analytical Detection Limit

4. benzene
12. hexachloroethane
22. parachlorometa cresol
23. chloroform (trichloromethane)
30. 1,2-trans-dichloroethylene
44. methylene chloride (dichloromethane)
47. bromoform (tribromomethane)
48. dichlorobromomethane
55. naphthalene
62. N-nitrosodiphenylamine
69. di-n-octyl phthalate
70. diethyl phthalate
73. benzo (a)pyrene (3,4-benzopyrene)
85. tetrachloroethylene
86. toluene
89. aldrin
90. dieldrin
92. 4,4'-DDT
93. 4,4'-DDE(p,p'DDX)
94. 4,4'-DDD(p,p'TDE)
96. beta-endosulfan
97. endosulfan sulfate
98. endrin
99. endrin aldehyde
100. heptachlor
101. heptachlor epoxide
102. alpha-BHC
103. beta-BHC
104. gamma-BHC
105. delta-BHC
117. beryllium
118. cadmium
126. silver
127. thallium

Priority Pollutants with Concentrations in the Plant Intake Water Equal to or Greater Than the Effluent Concentrations

There are no pollutants excluded in this subcategory for this reason.

Priority Pollutants Detected in Two or Less Samples When 20 or More Samples Were Analyzed

There are no pollutants excluded in this subcategory for this reason.

Table VII-8

PRIORITY POLLUTANTS IN PM&F PROCESS WATERS

Priority Pollutants	Average Concentrations (mg/1)**		
	Contact Cooling and Heating Water	Cleaning Water	Finishing Water
4. benzene	0.012	0.002	*
8. 1,2,4-trichlorobenzene	*	*	0.006
11. 1,1,1-trichloroethane	0.024	*	0.001
22. parachlorometa cresol	0.022	0.0001	*
23. chloroform	0.001	*	*
28. 3,3'-dichlorobenzidine	*	*	0.002
38. ethylbenzene	*	*	0.005
44. methylene chloride	0.023	0.012	*
62. N-nitrosodiphenylamine	*	0.002	*
65. phenol	0.004	0.198	0.007
66. bis(2-ethylhexyl) phthalate	0.098	0.007	0.479
68. di-n-butyl phthalate	0.001	*	0.031
71. dimethyl phthalate	*	*	0.034
86. toluene	0.0001	0.013	*
87. trichloroethylene	*	*	0.004
89. aldrin	0.2†	25†	*
90. dieldrin	0.2†	*	*
99. endrin aldehyde	0.3†	*	*
100. heptachlor	*	27†	*
102. alpha-BHC	36†	0.1†	*
103. beta-BHC	9†	9†	*
104. gamma-BHC	2†	66†	*
105. delta-BHC	40†	70†	*
114. antimony	*	0.003	0.001
115. arsenic	*	0.0002	0.001
117. beryllium	19†	*	*
118. cadmium	0.0007	*	*

Table VII-8 (Continued)

PRIORITY POLLUTANTS IN PM&F PROCESS WATERS

		Average Concentrations (mg/l)**		
	Priority Pollutants	Contact Cooling and Heating Water	Cleaning Water	Finishing Water
119.	chromium (Total)	0.002	0.019	0.001
120.	copper	0.001	0.044	0.028
121.	cyanide (Total)	*	*	0.010
122.	lead	0.100	*	0.030
123.	mercury	0.1†	8†	15†
124.	nickel	0.003	0.004	0.004
125.	selenium	*	0.013	0.030
126.	silver	56†	0.0002	*
127.	thallium	0.0008	*	*
128.	zinc	0.009	0.598	0.087

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*Pollutant is not considered further in this subcategory.

**Average concentrations are from Table VI-19.

†Concentration is in nanograms per liter.

The subcategory average concentrations for the priority pollutants were compared with treatability limits for treatment technologies most capable of effectively removing the pollutants. These treatability limits are presented in Table VII-9.

Because the treatability limits are based on "best-case" treatment technologies, priority pollutants with a concentration greater than the treatability limit were considered further for control. The priority pollutants that were present at concentrations higher than the treatable limits and their average concentrations are presented in Table VII-10. Priority pollutants with a subcategory average below the treatability limit were considered present in amounts too small to be effectively reduced by technologies known to the Administrator.

POLLUTANTS CONSIDERED FOR REGULATION

The following discussions address the pollutants listed in Tables VII-1, VII-3, and VII-8. The discussions include the source of the pollutant; whether it is a naturally occurring element, processed metal, or a manufactured product; general physical properties and the form of the pollutant; and toxic effects of the pollutant on humans and other animals.

Conventional Pollutants

Biochemical Oxygen Demand (BOD_5). Biochemical oxygen demand is not a specific pollutant, but a measure of the relative oxygen requirements of wastewaters. The BOD_5 test measures the oxygen required for the biochemical degradation of organic material (carbonaceous demand) and the oxygen used to oxidize inorganic material such as sulfides and ferrous iron. It also may measure the oxygen used to oxidize reduced forms of nitrogen (nitrogenous demand) unless their oxidation is prevented by the use of an inhibitor.

Many wastewaters contain more oxygen-demanding materials than the amount of dissolved oxygen available in air-saturated water. Therefore, it is necessary to dilute the sample, add nutrients, and maintain the pH in a range suitable for bacterial growth. When analyzing those wastewaters, complete stabilization of a sample may require a period of incubation too long for practical purposes. For this reason, a five day period was selected as the standard incubation period.

Oil and Grease. Oil and grease are taken together as one pollutant. Some of its components are:

1. Light Hydrocarbons - These include light fuels such as gasoline, kerosene, and jet fuel, and miscellaneous solvents used

Table VII-9

POLLUTANT TREATABILITY LIMITS*

	Priority Pollutant	Treatability Limit (mg/l)
4.	benzene	0.050
8.	1,2,4-trichlorobenzene	0.010
11.	1,1,1-trichloroethane	0.100
22.	parachlorometa cresol	0.050
23.	chloroform	0.100
28.	3,3'-dichlorobenzidine	0.010
38.	ethylbenzene	0.050
44.	methylene chloride	0.100
62.	N-nitrosodiphenylamine	0.001 to 0.010
65.	phenol	0.050
66.	bis(2-ethylhexyl) phthalate	0.010
68.	di-n-butyl phthalate	0.025
71.	dimethyl phthalate	0.001 to 0.010
86.	toluene	0.050
87.	trichloroethylene	0.100
89.	aldrin	0.001
90.	dieldrin	0.001
99.	endrin aldehyde	$\leq$0.001
100.	heptachlor	$\leq$0.001
102.	alpha-BHC	0.001
103.	beta-BHC	0.001
104.	gamma-BHC	0.001
105.	delta-BHC	0.001
114.	antimony	0.47
115.	arsenic	0.34
117.	beryllium	0.200
118.	cadmium	0.049
119.	chromium	0.07

Table VII-9 (Continued)

POLLUTANT TREATABILITY LIMITS*

	Priority Pollutant	Treatability Limit (mg/l)
120.	copper	0.39
121.	cyanide	0.047
122.	lead	0.080
123.	mercury	0.036
124.	nickel	0.22
125.	selenium	0.20
126.	silver	0.070
127.	thallium	0.200
128.	zinc	0.23

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*Treatability limits for organic priority pollutants (excluding pesticides) are from U.S. EPA, Treatability of Organic Priority Pollutants - Part C - Their Estimated (30-Day Ave.) Treated Effluent Concentrations - A Molecular Engineering Approach, Murray P. Strier, 11 July 1978.

Treatability limits for priority pollutant pesticides are from U.S. EPA, Treatability of Organic Priority Pollutants - Part D - The Pesticides - Their Estimated (30-Day Ave.) Treated Effluent Concentrations, Murray P. Strier, 26 December 1978.

Treatability limits for the priority metal pollutants are from the U.S. EPA, Development Document for Effluent Guidelines and Standards for the Nonferrous Metals Manufacturing Point Source Category Phase II, July 1984.

Table VII-10

PRIORITY POLLUTANTS PRESENT IN TREATABLE CONCENTRATIONS

		Average Concentration (mg/l)		
	Priority Pollutant	Contact Cooling and Heating Waters	Cleaning Waters	Finishing Waters
65.	phenol	*	0.198	*
66.	bis(2-ethylhexyl) phthalate	0.098	*	0.479
68.	di-n-butyl phthalate	*	*	0.031
71.	dimethyl phthalate	*	*	0.034
128.	zinc	*	0.598	*

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*Pollutant not found in treatable concentrations for this subcategory.

for industrial processing, degreasing, or cleaning purposes. The presence of these light hydrocarbons may make the removal of other heavier oil wastes more difficult.

2. Heavy Hydrocarbons, Fuels, and Tars - These include the crude oils, diesel oils, #6 fuel oil, residual oils, slop oils, and in some cases, asphalt and road tar.

3. Lubricants and Cutting Fluids - These generally fall into two classes: non-emulsifiable oils such as lubricating oils and greases and emulsifiable oils such as water soluble oils, rolling oils, cutting oils, and drawing compounds. Emulsifiable oils may contain fat, soap, or various other additives.

4. Vegetable and Animal Fats and Oils - These originate primarily from processing of foods and natural products.

Oil and grease can settle or float and may exist as solids or liquids depending on factors such as method of use, production process, and temperature of water.

Even in small quantities, oil and grease cause troublesome taste and odor problems. Scum lines from these pollutants are produced on treatment basin walls and on other containers. Fish and water fowl are adversely affected by oils in their habitat. Oil emulsions may adhere to the gills of fish causing suffocation, and the flesh of fish is tainted when microorganisms that were exposed to waste oil are eaten. Deposition of oil in the bottom sediments of water can inhibit normal benthic growth and oil and grease exhibit an oxygen demand.

Many of the toxic organic pollutants may be distributed between the oil phase and the aqueous phase in industrial wastewaters. The presence of phenols, PCB's, PAH's, and almost any other organic pollutant in the oil and grease make characterization of this pollutant almost impossible. The other organics add to the objectionable nature of the oil and grease.

Levels of oil and grease that are toxic to aquatic organisms vary greatly, depending on the type and the species susceptibility. Crude oil in concentrations as low as 0.3 mg/l has been reported as extremely toxic to freshwater fish. It has been recommended that public water supply sources be essentially free from oil and grease.

Oil and grease in quantities of 100 liters per square kilometer cause a sheen on the surface of a body of water. The presence of oil slicks decreases the aesthetic value of a waterway.

pH. Although not a specific pollutant, pH is related to the acidity or alkalinity of a wastewater. It is not, however, a measure of either. The term pH is used to describe the hydrogen ion concentration (or activity) present in a given solution. Values for pH range from 0 to 14; these numbers are the negative logarithms of the hydrogen ion concentrations. A pH of 7 indicates neutrality. Solutions with a pH above 7 are alkaline, while those solutions with a pH below 7 are acidic. The relationship of pH and acidity and alkalinity is not necessarily linear or direct. Knowledge of the water pH is useful in determining necessary measures for corrosion control, sanitation, and disinfection. Its value is also necessary in the treatment of industrial wastewaters to determine amounts of chemicals required to remove pollutants and to measure their effectiveness. Removal of pollutants, especially dissolved solids is affected by the pH of the wastewater.

Waters with a pH below 6.0 are corrosive to treatment facilities, distribution lines, and household plumbing fixtures and can thus add constituents to drinking water such as iron, copper, zinc, cadmium, and lead. The hydrogen ion concentration can affect the taste of the water; at a low pH water tastes sour. The bactericidal effect of chlorine is weakened as the pH increases.

Extremes of pH or rapid pH changes can exert stress conditions on or kill aquatic life. Even moderate changes from acceptable criteria limits of pH are deleterious to some aquatic species.

The relative toxicity to aquatic life of many materials is increased by changes in the water pH. For example, metallocyanide complexes can increase a thousand-fold in toxicity with a drop of 1.5 pH units.

Because of the universal nature of pH and its effect on water quality and treatment, it is controlled by the effluent limitations guidelines and standards for many industry categories. A neutral pH range (approximately 6 to 9) is generally desired because either extreme beyond this range has a deleterious effect on receiving waters and on other wastewater constituents.

Total Suspended Solids (TSS). Suspended solids include both organic and inorganic materials. The inorganic compounds include sand, silt, and clay. The organic fraction includes such materials as grease, oil, tar, and animal and vegetable waste products. These solids may settle out rapidly; bottom deposits are often a mixture of both organic and inorganic solids. Solids may be suspended in water for a time and then settle to the bed of the stream or lake. Solids discharged with domestic wastes may be inert, slowly biodegradable materials, or rapidly decomposable substances. While in suspension, suspended solids increase the turbidity of the water, reduce light penetration, and impair the photosynthetic activity of aquatic plants.

Suspended solids in water interfere with many industrial processes and cause foaming in boilers and incrustations on equipment exposed to such water, especially as the temperature rises. They are undesirable in process water used in many manufacturing processes and in cooling water systems.

Solids in suspension are aesthetically displeasing. When they settle to form sludge deposits on the stream or lake bed, they often cause damage to aquatic life. Solids, when transformed to sludge deposits, may do a variety of damaging things, including blanketing the stream or lake bed and thereby destroying the living spaces for those benthic organisms that would otherwise occupy the habitat. Organic solids use a portion or all of the dissolved oxygen available in the area and also serve as a food source for sludgeworms and associated organisms.

Suspended solids may kill fish and shellfish by causing abrasive injuries and by clogging the gills and respiratory passages of various aquatic fauna. Indirectly, suspended solids are inimical to aquatic life because they screen out light, and they promote and maintain the development of noxious conditions through oxygen depletion. This results in the killing of fish and fish food organisms. Suspended solids also reduce the recreational value of the water.

Nonconventional Pollutants

Chemical Oxygen Demand (COD). COD is a test that measures the organic matter in wastewater by chemical oxidation. It is not a measure of one particular pollutant. The oxygen equivalent (i.e., carbon dioxide, CO_2) of the organic matter that can be oxidized is measured by using a strong chemical oxidizing agent in an acidic medium. Potassium dichromate is an excellent oxidizing agent for this test. The principal reaction using dichromate as the oxidizing agent may be generally represented by the following unbalanced equation:

$$\text{Organic Matter } (C_aH_bO_c) + Cr_2O_7^{=} + H^+ \xrightarrow[\text{heat}]{\text{catalyst}}$$

$$Cr^{3+} + CO_2 + H_2O$$

The COD of wastewater is usually higher than the BOD_5 because more compounds can be chemically oxidized than can be biologically oxidized. COD can be correlated with BOD_5 for many kinds of wastewater. This can be quite useful because COD test results can be obtained in three hours versus the five days needed to obtain BOD_5 test results.

Total Organic Carbon (TOC). TOC is another test to determine the organic matter present in wastewater; it is especially applicable to small concentrations of organic matter. The test is performed by injecting a known quantity of sample into a high-temperature furnace. The organic carbon is oxidized to carbon dioxide in the presence of a catalyst and the carbon dixoide is quantitatively measured with an infrared analyzer. TOC also measures more than one pollutant.

Phenols (Total). Total phenols are measured using the 4-AAP (4-aminoantipyrene) method. This analytical procedure measures the color development of reaction products between 4-AAP and some phenols. The results are reported as phenol. Thus, "total phenols" is not actually total phenols because many phenols (notably nitrophenols) do not react. Also, because each reacting phenol contributes to the color development to a different degree and because each phenol has a molecular weight different from others and from phenol itself, analyses of several mixtures containing the same total concentration of several phenols will give different numbers depending on the proportions of the phenols in the particular mixture. Despite these limitations, the total phenols method is useful when the mix of phenols is relatively constant and an inexpensive monitoring method is desired.

Priority Toxic Pollutants

4. Benzene. Benzene (C_6H_6) is a clear, colorless liquid obtained mainly from petroleum feedstocks using several different processes. Some is recovered from light oils obtained from coal carbonization gases. Benzene boils at 80°C and has a vapor pressure of 100 mm of mercury at 26°C. It is slightly soluble in water (1.8 g/l at 25°C) and it dissolves in hydrocarbon solvents. Annual production in the United States is three to four million tons.

Most of the benzene used in the United States goes into chemical manufacture. About half of that is converted to ethylbenzene which is used to make styrene. Some benzene is used in motor fuels.

According to numerous published studies, benzene is harmful to human health. Most studies relate effects of inhaled benzene vapors. These effects include nausea, loss of muscle coordination, and excitement followed by depression and coma. Death is usually the result of respiratory or cardiac failure. Two specific blood disorders are related to benzene exposure. One of these, acute myelogenous leukemia, represents a carcinogenic effect of benzene. However, most human exposure data are based on exposure in occupational settings and benzene carcinogenesis is not firmly established.

Oral administration of benzene to laboratory animals produced leukopenia, a reduction in the number of leukocytes in the blood. Subcutaneous injection of benzene-oil solutions has produced suggestive, but not conclusive, evidence of benzene carcinogenesis.

Benzene demonstrated teratogenic effects in laboratory animals, and mutagenic effects in humans and other animals.

For maximum protection of human health from the potential carcinogenic effects of exposure to benzene through ingestion of water and contaminated aquatic organisms, the ambient water concentration is zero. Concentrations of benzene estimated to result in additional lifetime cancer risk at levels of 10^{-7}, 10^{-6}, and 10^{-5} are 0.000066 mg/l, 0.00066 mg/l, and 0.0066 mg/l, respectively.

8. 1,2,4-Trichlorobenzene. 1,2,4-Trichlorobenzene ($C_6H_3Cl_3$, 1,2,4-TCB) is a liquid at room temperature, solidifying to a crystalline solid at 17°C and boiling at 214°C. It is produced by liquid phase chlorination of benzene in the presence of a catalyst. Its vapor pressure is 4 mm Hg at 25°C. 1,2,4-TCB is insoluble in water and soluble in organic solvents. Annual United States production is in the range of 15,000 tons. 1,2,4-TCB is used in limited quantities as a solvent and as a dye carrier in the textile industry. It is also used as a heat transfer medium and as a transfer fluid. The compound can be selectively chlorinated to 1,2,4,5-tetrachlorobenzene using iodine plus antimony trichloride as catalyst.

No reports are available regarding the toxic effects of 1,2,4-TCB on humans. Limited data from studies on effects in laboratory animals fed 1,2,4-TCB indicate depression of activity at low doses and predeath extension convulsions at lethal doses. Metabolic disturbances and liver changes were also observed. Studies for the purpose of determining teratogenic or mutagenic properties of 1,2,4-TCB have not been conducted. No studies have been made of carcinogenic behavior of 1,2,4-TCB administered orally.

For the prevention of adverse effects due to the organoleptic properties of 1,2,4-trichlorobenzene in water, the water quality criterion is 0.013 mg/l.

11. 1,1,1-Trichloroethane. 1,1,1-Trichloroethane is one of the two possible trichlorethanes. It is manufactured by hydrochlorinating vinyl chloride to 1,1-dichloroethane which is then chlorinated to the desired product. 1,1,1-Trichloroethane is a liquid at room temperature with a vapor pressure of 96 mm of mercury at 20°C and a boiling point of 74°C. Its formula is CCl_3CH_3. It is slightly soluble in water (0.48 g/l) and is very soluble in

organic solvents. The United States annual production is greater than one-third of a million tons. 1,1,1-Trichloroethane is used as an industrial solvent and degreasing agent.

Most human toxicity data for 1,1,1-trichloroethane relate to inhalation and dermal exposure routes. Limited data are available for determining toxicity of ingested 1,1,1-trichloroethane, and those data are all for the compound itself, not solutions in water. No data are available regarding its toxicity to fish and aquatic organisms. For the protection of human health from the toxic properties of 1,1,1-trichloroethane ingested through the consumption of water and fish, the ambient water criterion is 18.4 mg/l. The criterion is based on results of bioassays for possible carcinogenicity.

22. Para-chloro-meta-cresol. Para-chloro-meta-cresol (ClC_7H_6OH) is thought to be a 4-chloro-3-methyl-phenol (4-chloro-meta-cresol, or 2-chloro-5-hydroxy-toluene), but is also used by some authorities to refer to 6-chloro-3-methyl-phenol (6-chloro-meta-cresol, or 4-chloro-3-hydroxy-toluene), depending on whether the chlorine is considered to be para to the methyl or to the hydroxy group. For the purposes of this document, the pollutant is assumed to be 2-chloro-5-hydroxy-toluene. This pollutant is a colorless crystalline solid melting at 66 to 68°C. It is slightly soluble in water and soluble in organic solvents. This pollutant reacts with 4-aminoantipyrene to give a colored product and contributes, therefore, to the nonconventional pollutant "total phenols." No information on manufacturing methods or volumes produced was found.

Para-chloro-meta cresol (abbreviated here as PCMC) is marketed as a microbicide and was proposed as an antiseptic and disinfectant more than 40 years ago. It is used in glues, gums, paints, inks, textiles, and leather goods.

Although no human toxicity data are available for PCMC, studies on laboratory animals have demonstrated that this pollutant is toxic when administered subcutaneously and intravenously. Death was preceded by severe muscle tremors. At high dosages kidney damage occurred. On the other hand, an unspecified isomer of chlorocresol, presumed to be PCMC, is used at a concentration of 0.15 percent to preserve mucous heparin, a natural product administered intravenously as an anticoagulant. No information was found regarding possible teratogenicity or carcinogenicity of PCMC.

23. Chloroform. Chloroform, also called trichloromethane, is a colorless liquid manufactured commercially by chlorination of methane. Careful control of conditions maximizes chloroform

production, but other products must be separated. Chloroform boils at 61°C and has a vapor pressure of 200 mm of mercury at 25°C. It is slightly soluble in water (8.22 g/l at 20°C) and readily soluble in organic solvents.

Chloroform is used as a solvent and to manufacture refrigerants, pharmaceuticals, plastics, and anesthetics. It is seldom used as an anesthetic.

Toxic effects of chloroform on humans include central nervous system depression, gastrointestinal irritation, liver and kidney damage and possible cardiac sensitization to adrenalin. Carcinogenicity has been demonstrated for chloroform using laboratory animals.

For the maximum protection of human health from the potential carcinogenic effects of exposure to chloroform through ingestion of water and contaminated aquatic organisms, the ambient water concentration is zero. Concentrations of chloroform estimated to result in additional lifetime cancer risks at the levels of 10^{-7}, 10^{-6}, and 10^{-5} are 0.000019 mg/l, 0.00019 mg/l, and 0.0019 mg/l, respectively.

28. 3,3'-Dichlorobenzidine. 3,3'-Dichlorobenzidine (DCB) or dichlorobenzidine (4,4'-diamino-3,3'-dichlorobiphenyl) is used in the production of dyes and pigments and as a curing agent for polyurethanes. The molecular formula of dichlorobenzidine is $C_{12}H_{10}Cl_2N_2$ and the molecular weight is 253.13.

DCB forms brownish needles with a melting point of 132 to 133°C. It is readily soluble in alcohol, benzene, and glacial acetic acid, slightly soluble in HCl, and sparingly soluble in water (0.7 g/l at 15°C). When combined with ferric chloride or bleaching powder, a green color is produced.

The affinity of DCB for suspended particulates in water is not clear; its basic nature suggests that it may be fairly tightly bound to humic materials in soils. Soils may be moderate to long term reservoirs for DCB.

Pyrolysis of DCB will most likely lead to the release of HCl. Because of the halogen substitution, DCB compounds probably biodegrade at a slower rate than benzidine alone. The photochemistry of DCB is not completely known. DCB may photodegrade to benzidine.

Assuming the clean air concentrations of ozone (2×10^{-9}) and an average atmospheric concentration of hydroxyl radicals (3×10^{-15} M), the half-life for oxidation of DCB by either of these chemical compounds is on the order of one and one to 10 days, respectively. Furthermore, assuming a representative concentration of 10^{-10} M for peroxy radicals in sunlit oxygenated water, the half-life for oxidation by these compounds is approximately 100 days, given the variability of environmental conditions.

The data base available for dichlorobenzidines and freshwater organisms is limited to one test on bioconcentration of 3,3'-dichlorobenzidine. No statement can be made concerning acute or chronic toxicity of this pollutant.

No saltwater organisms have been tested with any dichlorobenzidine; no statement can be made concerning acute or chronic toxicity for that pollutant on saltwater organisms.

For the maximum protection of human health from the potential carcinogenic effects due to exposure of dichlorobenzidine through ingestion of contaminated water and contaminated aquatic organisms, the ambient water concentration should be zero based on the non-threshold assumption for this chemical. However, zero level may not be attainable at the present time. Therefore, the levels that may result in incremental increase of cancer risk over the lifetime were estimated at 10^{-5}, 10^{-6}, and 10^{-7}. The corresponding recommended criteria are 0.103 ug/l, 0.010 ug/l, and 0.001 ug/l, respectively. If the above estimates are made for consumption of aquatic organisms only, excluding consumption of water, the levels are 0.204 ug/l, 0.020 ug/l, and 0.002 ug/l, respectively.

38. Ethylbenzene. Ethylbenzene is a colorless, flammable liquid manufactured commercially from benzene and ethylene. Approximately half of the benzene used in the United States goes into the manufacture of more than three million tons of ethylbenzene annually. Ethylbenzene boils at 136°C and has a vapor pressure of 7 mm Hg at 20°C. It is slightly soluble in water (0.14 g/l at 15°C) and is very soluble in organic solvents.

About 98 percent of the ethylbenzene produced in the United States goes into the production of styrene, much of which is used in the plastics and synthetic rubber industries. Ethylbenzene is a constituent of xylene mixtures used as diluents in the paint industry, agricultural insecticide sprays, and gasoline blends.

Although humans are exposed to ethylbenzene from a variety of sources in the environment, little information on effects of ethylbenzene in man or animals is available. Inhalation can irritate eyes, affect the respiratory tract, or cause vertigo. In laboratory animals, ethylbenzene exhibited low toxicity. There are no data available on teratogenicity, mutagenicity, or carcinogenicity of ethylbenzene.

Criteria are based on data derived from inhalation exposure limits. For the protection of human health from the toxic properties of ethylbenzene ingested through water and contaminated aquatic organisms, the ambient water quality criterion is 1.4 mg/l.

44. Methylene Chloride. Methylene chloride, also called dichloromethane (CH_2Cl_2), is a colorless liquid manufactured by chlorination of methane or methyl chloride followed by separation from the higher chlorinated methanes formed as coproducts. Methylene chloride boils at 40°C and has a vapor pressure of 362 mm of mercury at 20°C. It is slightly soluble in water (20 g/l at 20°C) and very soluble in organic solvents. The United States annual production is about 250,000 tons.

Methylene chloride is a common industrial solvent found in insecticides, metal cleaners, paint, and paint and varnish removers.

Methylene chloride is not generally regarded as highly toxic to humans. Most human toxicity data are for exposure by inhalation. Inhaled methylene chloride acts as a central nervous system depressant. There is also evidence that the pollutant causes heart failure when large amounts are inhaled.

Methylene chloride did produce mutation in tests for this effect. In addition, a bioassay recognized for its extremely high sensitivity to strong and weak carcinogens produced results that were marginally significant. Thus, potential carcinogenic effects of methylene chloride are not confirmed or denied, but are under continuous study. These studies are difficult to conduct for two reasons. First, the low boiling point (40°C) of methylene chloride makes it difficult to maintain the compound at 37°C during incubation. Secondly, all impurities must be removed because the impurities themselves may be carcinogenic. These complications also make the test results difficult to interpret.

62. N-nitrosodiphenylamine. N-nitrosodiphenylamine $[(C_6H_5)_2NNO]$, also called nitrous diphenylamide, is a yellow crystalline solid manufactured by nitrosation of diphenylamine. It melts at 66°C and is insoluble in water, but soluble in several organic solvents other than hydrocarbons. Production in the United States has approached 1,500 tons per year. The compound is used as a retarder for rubber vulcanization and as a pesticide for control of scorch (a fungus disease of plants).

N-nitroso compounds are acutely toxic to every animal species tested and are also poisonous to humans. N-nitrosodiphenylamine toxicity in adult rats lies in the mid range of the values for 60 N-nitroso compounds tested. Liver damage is the principal toxic effect. N-nitrosodiphenylamine, unlike many other N-nitrosoamines, does not show mutagenic activity. N-nitrosodiphenylamine has been reported by several investigations to be non-carcinogenic. However, the pollutant is capable of trans-nitrosation and could thereby convert other amines to carcinogenic N-nitrosoamines. Sixty-seven of 87 N-nitrosoamines studied were reported to have carcinogenic activity. No water quality criteria have been proposed for N-nitrosodiphenylamine.

65. Phenol. Phenol, also called hydroxybenzene and carbolic acid, is a clear, colorless, hygroscopic, deliquescent, crystalline solid at room temperature. Its melting point is 43°C and its vapor pressure at room temperature is 0.35 mm Hg. It is very soluble in water (67 gm/l at 16°C) and can be dissolved in benzene, oils, and petroleum solids. Its formula is C_6H_5OH.

Although a small percent of the annual production of phenol is derived from coal tar as a naturally occurring product, most of the phenol is synthesized. Two of the methods are fusion of benzene sulfonate with sodium hydroxide and oxidation of cumene followed by cleavage with a catalyst. Annual production in the United States is in excess of one million tons. Phenol is generated during distillation of wood and the microbiological decomposition of organic matter in the mammalian intestinal tract.

Phenol is used as a disinfectant, in the manufacture of resins, dyestuffs, and pharmaceuticals, and in the photo processing industry. In this discussion, phenol is the specific compound that is separated by methylene chloride extraction of an acidified sample and identified and quantified by GC/MS. Phenol also contributes to the "Total Phenols," discussed elsewhere, which are determined by the 4-AAP colorimetric method.

Phenol exhibits acute and sub-acute toxicity in humans and laboratory animals. Acute oral doses of phenol in humans cause sudden collapse and unconsciousness by its action on the central nervous system. Death occurs by respiratory arrest. Sub-acute oral doses in mammals are rapidly absorbed then quickly distributed to various organs, then cleared from the body by urinary excretion and metabolism. Long term exposure by drinking phenol contaminated water has resulted in statistically significant increase in reported cases of diarrhea, mouth sores, and burning of the mouth. In laboratory animals, long term oral administration at low levels produced slight liver and kidney damage. No reports were found regarding carcinogenicity of phenol administered orally - all carcinogenicity studies were skin tests.

For the protection of human health from phenol ingested through water and through contaminated aquatic organisms the concentration in water should not exceed 3.4 mg/l.

Fish and other aquatic organisms demonstrated a wide range of sensitivities to phenol concentration. However, acute toxicity values were at moderate levels when compared to other organic priority pollutants.

66-71. Phthalate Esters. Phthalic acid, or 1,2-benzenedicarboxylic acid, is one of three isomeric benzenedicarboxylic acids produced by the chemical industry. The other two isomeric forms are called isophthalic and terephthalic acids. The formula for all three acids is $C_6H_4(COOH)_2$. Some esters of phthalic acid are designated as toxic pollutants. They are discussed as a group here and specific properties of individual phthalate esters in PM&F process waters are then discussed.

Phthalic acid esters are manufactured in the United States at an annual rate in excess of one billion pounds. They are used as plasticizers - primarily in the production of polyvinyl chloride (PVC) resins. The most widely used phthalate plasticizer is bis (2-ethylhexyl) phthalate which accounts for nearly one-third of the phthalate esters produced. This particular ester is commonly referred to as dioctyl phthalate (DOP) and should not be confused with one of the less used esters, di-n-octyl phthalate, which is also used as a plasticizer. In addition to these two isomeric dioctyl phthalates, four other esters, also used primarily as plasticizers, are designated as toxic pollutants. They are: butyl benzyl phthalate, di-n-butyl phthalate, diethyl phthalate, and dimethyl phthalate.

Industrially, phthalate esters are prepared from phthalic anhydride and the specific alcohol to form the ester. Some evidence is available suggesting that phthalic acid esters also may be synthesized by certain plant and animal tissues. The extent to which this occurs in nature is not known.

Phthalate esters used as plasticizers can be present in concentrations up to 60 percent of the total weight of the plastic. The plasticizer is not linked by primary chemical bonds to the resin. Rather, it is locked into the structure of intermeshing polymer molecules and held by van der Waals forces. The result is that the plasticizer is easily extracted. Plasticizers are responsible for the odor associated with new plastic toys or flexible sheet that has been contained in a sealed package.

Although the phthalate esters are not soluble or are only very slightly soluble in water, they do migrate into aqueous solutions placed in contact with the plastic. Thus, industrial facilities with tank linings, wire and cable coverings, tubing, and sheet flooring of PVC are expected to discharge some phthalate esters in their raw waste. In addition to their use as plasticizers, phthalate esters are used in lubricating oils and pesticide carriers. These also can contribute to industrial discharge of phthalate esters.

From the accumulated data on acute toxicity in animals, phthalate esters may be considered as having a rather low order of toxicity. Human toxicity data are limited. The toxic effect of the esters is most likely due to one of the metabolic products, in particular the monoester. Oral acute toxicity in animals is greater for the lower molecular weight esters than for the higher molecular weight esters.

Orally administered phthalate esters generally produced enlarging of liver and kidney and atrophy of testes in laboratory animals. Specific esters produced enlargement of heart and brain, spleenitis, and degeneration of central nervous system tissue.

Subacute doses administered orally to laboratory animals produced some decrease in growth and degeneration of the testes. Chronic studies in animals showed similar effects to those found in acute and subacute studies, but to a much lower degree. The same organs were enlarged, but pathological changes were not usually detected.

A recent study of several phthalic esters produced suggestive but not conclusive evidence that dimethyl, diethyl, and bis(2-ethylhexyl) phthalates have a cancer liability. Phthalate esters do bioconcentrate in fish. The factors, weighted for relative consumption of various aquatic and marine food groups, are used to calculate ambient water quality criteria for phthalate esters. The values are included in the discussion of the specific esters.

Studies of toxicity of phthalate esters in freshwater and salt water organisms are scarce. A chronic toxicity test with bis(2-ethylhexyl) phthalate showed that significant reproductive impairment occurred at 0.003 mg/l in the freshwater crustacean, _Daphnia magna_. In acute toxicity studies, saltwater fish and organisms showed sensitivity differences of up to eight-fold to butyl benzyl, diethyl, and dimethyl phthalates. This suggests that each ester must be evaluated individually for toxic effects.

In addition to the general remarks and discussion on phthalate esters, specific information on bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate is presented below.

66. _Bis(2-ethylhexyl) phthalate_. Little information is available about the physical properties of bis(2-ethylhexyl) phthalate. It is a liquid boiling at 387°C at 5mm of mercury and is insoluble in water. Its formula is $C_6H_4(COOC_8H_{17})_2$. This toxic pollutant constitutes about one-third of the phthalate

ester production in the U.S. It is commonly referred to as dioctyl phthalate, or DOP, in the plastics industry where it is the most extensively used compound for the plasticization of polyvinyl chloride (PVC).

Bis(2-ethylhexyl) phthalate has been shown to induce liver tumors in both sexes of Fisher 344 rats and $B_6C_3F_1$ mice. The most sensitive animals were the male $B_6C_3F_1$ mice. Carcinogenicity bioassays, conducted for the Carcinogenesis Testing Program, National Cancer Institute (NCI)/National Toxicology Program, showed that liver tumors were associated with the administration of bis(2-ethylhexyl) phthalate (judged at least 99.5 percent pure by thin layer chromatography) in both mice and rats of either sex. In rats, the incidence of hepatocellular carcinomas and neoplastic nodules of the liver were both significantly increased ($p=0.05$) in females on the 12,000 ppm diet. Combining these two categories led to a significant increase ($p=0.01$) in males at 12,000 ppm and in females at 6,000 ($p=0.012$) and 12,000 ppm ($p=0.001$). Among mice, there was a statistically significant increase in hepatocellular carcinomas in females at 3,000 ppm ($p=0.006$) and in both sexes at 6,000 ppm ($p=0.03$). There was also evidence of an increase in hepatocellular adenomas, although not significant at $p<0.05$.

Two previous studies on Sherman rats fed diets containing 4,000 ppm DEHP and Wistar rats fed diets containing 5,000 ppm bis(2-ethylhexyl) phthalate did not show any carcinogenic effects. However, mortality was high in both studies and too few animals were maintained longer than one year to permit conclusions concerning near lifetime exposure.

For the maximum protection of human health from the potential carcinogenic effects due to exposure of bis(2-ethylhexyl) phthalate through ingestion of contaminated water and contaminated aquatic organisms, the ambient water concentrations should be zero based on the non-threshold assumption for this chemical. However, zero level may not be attainable at the present time. Therefore, levels are estimated that may result in incremental increase of cancer risk over the lifetime of 10^{-5}, 10^{-6}, and 10^{-7}. The corresponding recommended criteria are 17.5 ug/l, 1.75 ug/l, and 0.175 ug/l, respectively. If the above estimates are made for consumption of aquatic organisms only, excluding consumption of water, the levels are 58.8 ug/l, 5.88 ug/l, and 0.588 ug/l, respectively.

68. <u>Di-n-butyl Phthalate (DBP)</u>. DBP is a colorless, oily liquid, <u>boiling at 340°C.</u> <u>Its</u> water solubility at room temperature is reported to be 0.4 g/l and 4.5 g/l in two different chemistry handbooks. The formula for DBP, $C_6H_4(COOC_4H_9)_2$,

is the same as for its isomer, di-isobutyl phthalate. DBP production is one to two percent of total United States phthalate ester production.

DBP is used to a limited extent as a plasticizer for polyvinyl chloride (PVC). It is not approved for contact with food. It is used in liquid lipsticks and as a diluent for polysulfide dental impression materials. DBP is used as a plasticizer for nitrocellulose in making gun powder and as a fuel in solid propellants for rockets. Further uses are insecticides, safety glass manufacture, textile lubricating agents, printing inks, adhesives, paper coatings, and resin solvents.

For protection of human health from the toxic properties of DBP ingested through water and through contaminated aquatic organisms, the ambient water quality criterion is 34 mg/l. If contaminated aquatic organisms alone are consumed, excluding the consumption of water, the ambient water criterion is 154 mg/l.

71. Dimethyl Phthalate (DMP). DMP has the lowest molecular weight of the phthalate esters - M.W. = 194 compared to M.W. of 391 for bis(2-ethylhexyl) phthalate. DMP has a boiling point of 282°C. It is a colorless liquid, soluble in water to the extent of 5 mg/l. Its molecular formula is $C_6H_4(C)(CH_3)_2$.

Dimethyl phthalate production in the United States is just under one percent of total phthalate ester production. DMP is used to some extent as a plasticizer in cellulosics; however, its principal specific use is for dispersion of polyvinylidene fluoride (PVDF). PVDF is resistant to most chemicals and finds use as electrical insulation, chemical process equipment (particularly pipe), and as a case for long-life finishes for exterior metal siding. Coil coating techniques are used to apply PVDF dispersions to aluminum or galvanized steel siding.

For the protection of human health from the toxic properties of dimethyl phthalate ingested through water and through contaminated aquatic organisms, the ambient water criterion is 313 mg/l. If contaminated aquatic organisms alone are consumed, excluding the consumption of water, the ambient water criterion is 2,900 mg/l.

86. Toluene. Toluene is a clear, colorless liquid with a benzene-like odor. It is a naturally occuring compound derived primarily from petroleum or petrochemical processes. Some toluene is obtained from the manufacture of metallurgical coke. Toluene is also referred to as totuol, methylbenzene, methacide, and phenylmethane. It is an aromatic hydrocarbon with the formula $C_6H_5CH_3$. It boils at 111°C and has a vapor pressure of 30 mm Hg at room temperature. The water solubility of toluene

is 535 mg/l and it is miscible with a variety of organic solvents. Annual production of toluene in the United States is greater than two million metric tons. Approximately two-thirds of the toluene is converted to benzene and the remaining 33 percent is used approximately equally for the manufacture of chemicals and for use as a paint solvent and aviation gasoline additive. An estimated 5,000 metric tons are discharged to the environment annually as a constituent in wastewaters.

Most data on the effects of toluene in human and other mammals are based on inhalation exposure or dermal contact studies. There appear to be no reports of oral administration of toluene to human subjects. A long term toxicity study on female rats revealed no adverse effects on growth, mortality, appearance and behavior, organ to body weight ratios, blood-urea nitrogen levels, bone marrow counts, peripheral blood counts, or morphology of major organs. The effects of inhaled toluene on the central nervous system, both at high and low concentrations, have been studied in humans and animals. However, ingested toluene is expected to be handled differently by the body because it is absorbed more slowly and must first pass through the liver before reaching the nervous system. Toluene is extensively and rapidly metabolized in the liver. One of the principal metabolic products of toluene is benzoic acid, which itself seems to have little potential to produce tissue injury.

Toluene does not appear to be teratogenic in laboratory animals or man. Nor is there any conclusive evidence that toluene is mutagenic. Toluene has not been demonstrated to be positive in any in vitro mutagenicity or carcinogenicity bioassay system or to be carcinogenic in animals or man.

Toluene has been found in fish caught in harbor waters in the vicinity of petroleum and petrochemical plants. Bioconcentration studies have not been conducted, but bioconcentration factors have been calculated on the basis of the octanol-water partition coefficient.

For the protection of human health from the toxic properties of toluene ingested through water and through contaminated aquatic organisms, the ambient water criterion is 14.3 mg/l. If contaminated aquatic organisms alone are consumed excluding the consumption of water, the ambient water criterion is 424 mg/l. Available data show that the adverse effects on aquatic life occur at concentrations as low as 5 mg/l.

Acute toxicity tests have been conducted with toluene and a variety of freshwater fish and Daphnia magna. The latter appears to be significantly more resistant than fish. No test results have been reported for the chronic effects of toluene on freshwater fish or invertebrate species.

87. Trichloroethylene. Trichloroethylene (1,1,2-trichloroethylene or TCE) is a clear, colorless liquid boiling at 87°C. It has a vapor pressure of 77 mm Hg at room temperature and is slightly soluble in water (1 gm/l). United States production is greater than 0.25 million metric tons annually. It is produced from tetrachloroethane by treatment with lime in the presence of water.

TCE is used for vapor phase degreasing of metal parts; cleaning and drying electronic components, as a solvent for paints; as a refrigerant; for extraction of oils, fats, and waxes; and for dry cleaning. Its widespread use and relatively high volatility result in detectable levels in many parts of the environment.

Data on the effects produced by ingested TCE are limited. Most studies have been directed at inhalation exposure. Nervous system disorders and liver damage are frequent results of inhalation exposure. In the short term exposures, TCE acts as a central nervous system depressant. It was used as an anesthetic before its other long term effects were defined.

TCE has been shown to induce transformation in a highly sensitive *in vitro* Fischer rat embryo cell system (F1706) that is used for identifying carcinogens. Severe and persistent toxicity to the liver was recently demonstrated when TCE was shown to produce carcinoma of the liver in mouse strain B6C3F1. One systematic study of TCE exposure and the incidence of human cancer was based on 518 men exposed to TCE. The authors of that study concluded that although the cancer risk to man cannot be ruled out, exposure to low levels of TCE probably does not present a very serious and general cancer hazard.

TCE is bioconcentrated in aquatic species, making the consumption of such species by humans a significant source of TCE. For the protection of human health from the potential carcinogenic effects of exposure to trichloroethylene through ingestion of water and contaminated aquatic organisms, the ambient water concentration should be zero based on the non-threshold assumption of this chemical. However, zero level may not be attainable at the present time. Therefore, the levels that may result in incremental increase of cancer risk over the lifetime are estimated at 10^{-5}, 10^{-6}, and 10^{-7}. The corresponding recommended criteria are 0.027 mg/l, 0.0027 mg/l, and 0.00027 mg/l.

Only a very limited amount of data on the effects of TCE on freshwater aquatic life are available. One species of fish (fathead minnows) showed a loss of equilibrium at concentrations below those resulting in lethal effects.

89. Aldrin. Aldrin is highly toxic by ingestion and inhalation and is absorbed through the skin. It has been found to be carcinogenic to the liver of mice. For the protection of human health against the carcinogenic properties of aldrin, EPA has proposed a limit of 4.6×10^{-3} ng/l at a risk factor of 10^{-6} for the ingestion of water and contaminated aquatic organisms. Aldrin is banned from manufacture and use by EPA.

90. Dieldrin. Dieldrin is highly toxic by ingestion, inhalation, and skin absorption. Dieldrin has been found to cause cancer in the liver of mice. Dieldrin is banned from manufacture and use by EPA.

99. Endrin Aldehyde. Endrin aldehyde is likely to be present in one pesticide process as a reaction by-product. It is toxic and has no known commercial uses.

100. Heptachlor. Heptachlor is a nonsystemic stomach and contact insecticide that has fumigant action. It is a soft waxy solid with a melting range of 46 to 75°C and is practically insoluble in water. Heptachlor is very toxic to mammals with an acute oral LD50 of 100 mg/kg for male rats and an acute dermal LD50 for male rats of 195 mg/kg. Heptachlor and its epoxide bioaccumulate in fatty tissue and persist for lengthy periods of time. Several uses of hepatachlor have been discontinued to avoid contamination of milk and animal products. Heptachlor is a suspected carcinogen. The total number of tumors in both male and female rats increased in one long-term study after heptachlor exposure. It has been recommended that human daily intake of heptachlor should not exceed 0.005 mg/kg of body weight. A ban was placed on heptachlor in Canada in 1969 because of concern for residues in milk and deleterious effects on birds.

102. Alpha-BHC. Alpha-BHC is toxic by ingestion and skin absorption; is an eye and skin irritant; and is a central nervous system depressant.

103. Beta-BHC. Beta-BHC is moderately toxic by inhalation, highly toxic by ingestion, and is a strong irritant by skin absorption. It acts as a central nervous system depressant.

104. Gamma-BHC. Gamma-BHC, also known as lindane, is highly toxic by ingestion and moderately toxic by inhalation.

105. Delta-BHC. Delta-BHC is moderately toxic by inhalation and highly toxic by ingestion. It is a strong irritant to the skin and eyes; is absorbed by the skin; and is a central nervous system depressant.

114. Antimony. Antimony (chemical name - stibium, symbol Sb), classified as a non-metal or metalloid, is a silvery white, brittle crystalline solid. Antimony is found in small ore bodies throughout the world. Principal ores are oxides of mixed antimony valences and an oxysulfide ore. Complex ores with metals are important because the antimony is recovered as a by-product. Antimony melts at 631°C and is a poor conductor of electricity and heat.

Annual United States consumption of primary antimony ranges from 10,000 to 20,000 tons. About half is used in metal products, mostly antimonial lead for lead acid storage batteries, and about half in non-metal products. A principal compound is antimony trioxide which is used as a flame retardant in fabrics and as an opacifier in glass, ceramics, and enamels. Several antimony compounds are used as catalysts in organic chemicals synthesis, as fluorinating agents (the antimony fluoride), as pigments, and in fireworks.

Essentially no information on antimony-induced human health effects has been derived from community epidemiology studies. The available data are in literature relating effects observed with therapeutic or medicinal uses of antimony compounds and industrial exposure studies. Large therapeutic doses of antimonial compounds, usually used to treat schistisomiasis, have caused severe nausea, vomiting, convulsions, irregular heart action, liver damage, and skin rashes. Studies of acute industrial antimony poisoning have revealed loss of appetite, diarrhea, headache, and dizziness in addition to the symptoms found in studies of therapeutic doses of antimony.

For the protection of human health from the toxic properties of antimony ingested through water and through contaminated aquatic organisms, the ambient water criterion is 0.146 mg/l. If contaminated aquatic organisms are consumed, excluding the consumption of water, the ambient water criterion is 45 mg/l. Available data show that adverse effects on aquatic life occur at concentrations higher than those cited for human health risks.

115. Arsenic. Arsenic (chemical symbol As) is classified as a non-metal or metalloid. Elemental arsenic normally exists in the alpha-crystalline metallic form, which is steel gray and brittle, and in the beta form, which is dark gray and amorphous. Arsenic sublimes at 615°C. Arsenic is widely distributed throughout the world in a large number of minerals. The most important commercial source of arsenic is as a by-product from treatment of copper, lead, cobalt, and gold ores. Arsenic is usually marketed as the trioxide (As_2O_3). Annual United States production of the trioxide approaches 40,000 tons.

The principal use of arsenic is in agricultural chemicals (herbicides) for controlling weeds in cotton fields. Arsenicals have various applications in medicinal and vetrinary use, as wood preservatives, and in semiconductors.

The effects of arsenic in humans were known by the ancient Greeks and Romans. The principal toxic effects are gastrointestinal disturbances. Breakdown of red blood cells occurs. Symptoms of acute poisoning include vomiting, diarrhea, abdominal pain, lassitude, dizziness, and headache. Longer exposure produced dry, falling hair, brittle, loose nails, eczema, and exfoliation. Arsenicals also exhibit teratogenic and mutagenic effects in humans. Oral administration of arsenic compounds has been associated clinically with skin cancer for nearly one-hundred years. Since 1888, numerous studies have linked occupational exposure and therapeutic administration of arsenic compounds to increased incidence of respiratory and skin cancer.

For the maximum protection of human health from the potential carcinogenic effects of exposure to arsenic through ingestion of water and contaminated aquatic organisms, the ambient water concentration is zero. Concentrations of arsenic estimated to result in additional lifetime cancer risk levels of 10^{-7}, 10^{-6}, and 10^{-5} are 0.00000022 mg/l, 0.0000022 mg/l, and 0.000022 mg/l, respectively. If contaminated aquatic organisms alone are consumed, excluding the consumption of water, the water concentration should be less than 1.75×10^{-4} to keep the increased lifetime cancer risk below 10^{-5}. Available data show that adverse effects on aquatic life occur at concentrations higher than those cited for human health risks.

117. Beryllium. Beryllium is a dark gray metal of the alkaline earth family. It is relatively rare, but because of its unique properties finds widespread use as an alloying element, especially for hardening copper used in springs, electrical contacts, and non-sparking tools. World production is reported to be in the range of 250 tons annually. However, much more reaches the environment as emissions from coal burning operations. Analysis of coal indicates an average beryllium content of 3 ppm and 0.1 to 1.0 percent in coal ash or fly ash.

The principle ores are beryl ($3BeO.Al_2O_3.6SiO_2$) and bertrandite [$Be_6SiO_2O_7(OH_2)$]. Only two industrial facilities produce beryllium in the United States because of limited demand and the highly toxic character. About two-thirds of the annual production goes into alloys, 20 percent into heat sinks, and 10 percent into beryllium oxide (BeO) ceramic products.

Beryllium has a specific gravity of 1.846, making it the lightest metal with a high melting point (1,350°C). Beryllium alloys are corrosion resistant, but the metal corrodes in aqueous environments. Most common beryllium compounds are soluble in water, at least to the extent necessary to produce a toxic concentration of beryllium ions.

Most data on toxicity of beryllium are for inhalation of beryllium oxide dust. Some studies on orally administered beryllium in laboratory animals have been reported. Despite the large number of studies implicating beryllium as a carcinogen, there is no recorded instance of cancer being produced by ingestion. However, a recently convened panel of uninvolved experts concluded that epidemiologic evidence suggests that beryllium is a carcinogen in man.

In the aquatic environment, beryllium is chronically toxic to aquatic organisms at 0.0053 mg/l. Water softness has a large effect on beryllium toxicity to fish. In soft water, beryllium is reportedly 100 times as toxic as in hard water.

For the maximum protection of human health from the potential carcinogenic effects of exposure to beryllium through ingestion of water and contaminated aquatic organisms, the ambient water concentration is zero. Concentrations of beryllium estimated to result in additional lifetime cancer risk levels of 10^{-7}, 10^{-6}, and 10^{-5} are 0.00000037 mg/l, 0.0000037 mg/l, and 0.000037 mg/l, respectively. If contaminated aquatic organisms alone are consumed, excluding the consumption of water, the concentration should be less than 0.00117 mg/l to keep the increased lifetime cancer risk below 10^{-5}.

118. Cadmium. Cadmium is a relatively rare metallic element that is seldom found in sufficient quantities in a pure state to warrant mining or extraction from the earth's surface. It is found in trace amounts of about one ppm throughout the earth's crust. Cadmium is, however, a valuable by-product of zinc production.

Cadmium is used primarily as an electroplated metal and is found as an impurity in the secondary refining of zinc, lead, and copper.

Cadmium is an extremely dangerous cumulative toxicant, causing progressive chronic poisoning in mammals, fish, and probably other organisms. The metal is not excreted.

Toxic effects of cadmium on man have been reported from throughout the world. Cadmium may be a factor in the development of such human pathological conditions as kidney disease, testicular tumors, hypertension, arteriosclerosis, growth inhibition, chronic disease of old age, and cancer. Cadmium is normally ingested by humans through food and water as well as by breathing air contaminated by cadmium dust. Cadmium is cumulative in the liver, kidney, pancreas, and thyroid of humans and other animals. A severe bone and kidney syndrome known as itai-itai disease has been documented in Japan as caused by cadmium ingestion via drinking water and contaminated irrigation water. Ingestion of as little as 0.6 mg/day has produced the disease. Cadmium acts synergistically with other metals. Copper and zinc substantially increase its toxicity.

Cadmium is concentrated by marine organisms, particularly molluscs, that accumulate cadmium in calcareous tissues and in the viscera. A concentration factor of 1,000 for cadmium in fish muscle has been reported, as have concentration factors of 3,000 in marine plants and up to 29,600 in certain marine animals. The eggs and larvae of fish are apparently more sensitive than adult fish to poisoning by cadmium and crustaceans appear to be more sensitive than fish eggs and larvae.

For the protection of human health from the toxic properties of cadmium ingested through water and through contaminated aquatic organisms, the ambient water criterion is 0.010 mg/l. Available data show that adverse effects on aquatic life occur at concentrations in the same range as those cited for human health and they are highly dependent on water hardness.

119. Chromium. Chromium is an elemental metal usually found as a chromite ($FeO.Cr_2O_3$). The metal is normally produced by reducing the oxide with aluminum. A significant proportion of the chromium used is in the form of compounds such as sodium dichromate (Na_2CrO_4) and chromic acid (CrO_3), both are hexavalent chromium compounds.

Chromium is found as an alloying component of many steels and its compounds are used in electroplating baths and as corrosion inhibitors for closed water circulation systems.

The two chromium forms most frequently found in industry wastewaters are hexavalent and trivalent chromium. Hexavalent chromium is the form used for metal treatments. Some of it is reduced to trivalent chromium as part of the process reaction. The raw wastewater containing both valence states is usually treated first to reduce remaining hexavalent to trivalent chromium and second to precipitate the trivalent form as the hydroxide. The hexavalent form is not removed by lime treatment.

Chromium, in its various valence states, is hazardous to man. It can produce lung tumors when inhaled and induces skin sensitizations. Large doses of chromates have corrosive effects on the intestinal tract and can cause inflammation of the kidneys. Hexavalent chromium is a known human carcinogen. Levels of chromate ions that show no effect in man appear to be so low as to prohibit determination, to date.

The toxicity of chromium salts to fish and other aquatic life varies widely with the species, temperature, pH, valence of the chromium, and synergistic or antagonistic effects, especially the effect of water hardness. Studies have shown that trivalent chromium is more toxic to fish of some types than is hexavalent chromium. Hexavalent chromium retards growth of one fish species at 0.0002 mg/l. Fish food organisms and other lower forms of aquatic life are extremely sensitive to chromium. Therefore, both hexavalent and trivalent chromium must be considered harmful to particular fish or organisms.

For the protection of human health from the toxic properties of chromium (except hexavalent chromium) ingested through water and contaminated aquatic organisms, the ambient water quality criterion is 170 mg/l. If contaminated aquatic organisms alone are consumed, excluding the consumption of water, the ambient water criterion for trivalent chromium is 3,443 mg/l. The recommended ambient water quality criterion for hexavalent chromium is identical to the existing drinking water standard for total chromium, which is 0.050 mg/l.

120. Copper. Copper is a metallic element that sometimes is found free, as the native metal, and is also found in minerals such as cuprite (Cu_2O), malechite [$CuCO_3.Cu(OH)_2$], azurite [$2CuCO_3.Cu(OH)_2$], chalcopyrite ($CuFeS_2$), and bornite (Cu_5FeS_4). Copper is obtained from these ores by smelting, leaching, and electrolysis. It is used in the plating, electrical, plumbing, and heating equipment industries, as well as in insecticides and fungicides.

Traces of copper are found in all forms of plant and animal life and the metal is an essential trace element for nutrition. Copper is not considered to be a cumulative systemic poison for humans as it is readily excreted by the body, but it can cause symptoms of gastroenteritis, with nausea and intestinal irritations, at relatively low dosages. The limiting factor in domestic water supplies is taste. To prevent this adverse organoleptic effect of copper in water, a criterion of one mg/l has been established.

The toxicity of copper to aquatic organisms varies significantly, not only with the species, but also with the physical and chemical characteristics of the water, including temperature, hardness, turbidity, and carbon dioxide content. In hard water, the toxicity of copper salts may be reduced by the precipitation of copper carbonate or other insoluble compounds. The sulfates of copper and zinc and of copper and calcium are synergistic in their toxic effect on fish.

Relatively high concentrations of copper may be tolerated by adult fish for short periods of time; the critical effect of copper appears to be its higher toxicity to young or juvenile fish. Concentrations of 0.02 to 0.03 mg/l have proved fatal to some common fish species. In general, the salmonoids are very sensitive and the sunfishes are less sensitive to copper.

The recommended criterion to protect freshwater aquatic life is 0.0056 mg/l as a 24-hour average, and 0.012 mg/l maximum concentration at a hardness of 50 mg/l $CaCO_3$. For total recoverable copper, the criterion to protect freshwater aquatic life is 0.0056 mg/l as a 24-hour average.

Copper salts cause undesirable color reactions in the food industry and cause pitting when deposited on some other metals such as aluminum and galvanized steel. To control undesirable taste and odor quality of ambient water due to the organoleptic properties of copper, the estimated level is one mg/l for total recoverable copper.

Irrigation water containing more than minute quantities of copper can be detrimental to certain crops. Copper appears in all soils; its concentration ranges from 10 to 80 ppm. In soils, copper occurs in association with hydrous oxides of manganese and iron and also as soluble and insoluble complexes with organic matter. Copper is essential to the life of plants and the normal range of concentration in plant tissue is from 5 to 20 ppm. Copper concentrations in plants normally do not build up to high levels when toxicity occurs. For example, the concentrations of copper in snapbean leaves and pods was less than 50 and 20 mg/kg, respectively, under conditions of severe copper toxicity. Even under conditions of copper toxicity, most of the excess copper accumulates in the roots; very little is moved to the aerial part of the plant.

121. Cyanide. Cyanides are among the most toxic of pollutants commonly observed in industrial wastewaters. Introduction of cyanide into industrial processes is usually by dissolution of potassium cyanide (KCN) or sodium cyanide (NaCN) in process waters. However, hydrogen cyanide (HCN) formed when the above salts are dissolved in water, is probably the most acutely lethal compound.

The relationship of pH to hydrogen cyanide formation is very important. As pH is lowered to below 7, more than 99 percent of the cyanide is present as HCN and less than 1 percent as cyanide ions. Thus, at neutral pH, the pH of most living organisms, the more toxic form of cyanide prevails.

Cyanide ions combine with numerous heavy metal ions to form complexes. The complexes are in equilibrium with HCN. Thus, the stability of the metal-cyanide complex and the pH determine the concentration of HCN. Stability of the metal-cyanide anion complexes is extremely variable. Those formed with zinc, copper, and cadmium are not stable. They rapidly dissociate, with production of HCN, in near neutral or acid waters. Some of the complexes are extremely stable. Cobaltocyanide is very resistant to acid distillation in the laboratory. Iron cyanide complexes are also stable, but undergo photodecomposition to give HCN upon exposure to sunlight. Synergistic effects have been demonstrated for the metal cyanide complexes making zinc, copper, and cadmium cyanides more toxic than an equal concentration of sodium cyanide.

The toxic mechanism of cyanide is essentially an inhibition of oxygen metabolism (i.e., rendering the tissues incapable of exchanging oxygen). The cyanogen compounds are true noncumulative protoplasmic poisons. They arrest the activity of all forms of animal life. Cyanide shows a very specific type of toxic action. It inhibits the cytochrome oxidase system. This system is the one that facilitates electron transfer from reduced metabolites to molecular oxygen. The human body can convert cyanide to a non-toxic thiocyanate and eliminate it. However, if the quantity of cyanide ingested is too great at one time, the inhibition of oxygen utilization proves fatal before the detoxifying reaction reduces the cyanide concentration to a safe level.

Cyanides are more toxic to fish than to lower forms of aquatic organisms such as midge larvae, crustaceans, and mussels. Toxicity to fish is a function of chemical form and concentration, and is influenced by the rate of metabolism (temperature), the level of dissolved oxygen, and pH. In laboratory studies, free cyanide concentrations ranging from 0.05 to 0.14 mg/l have been proven to be fatal to sensitive fish species including trout, bluegill, and fathead minnows. Levels above 0.2 mg/l are rapidly fatal to most fish species. Long term sublethal concentrations of cyanide as low as 0.01 mg/l have been shown to affect the ability of fish to function normally (e.g., reproduce, grow, and swim).

For the protection of human health from the toxic properties of cyanide ingested through water and through contaminated aquatic organisms, the ambient water quality criterion is 0.200 mg/l.

Persistence of cyanide in water is highly variable and depends upon the chemical form of cyanide in the water, the concentration of cyanide, and the nature of other constituents. Cyanide may be destroyed by strong oxidizing agents such as permanganate and chlorine. Chlorine is commonly used to oxidize strong cyanide solutions. Carbon dioxide and nitrogen are the products of complete oxidation. But if the reaction is not complete, the very toxic compound, cyanogen chloride, may remain in the treatment system and subsequently be released to the environment. Partial chlorination may occur either as part of a POTW treatment or during the disinfection treatment of surface water for drinking water preparation.

122. Lead. Lead is a soft, malleable, ductile, blueish-gray, metallic element, usually obtained from the mineral galena (lead sulfide, PbS), anglesite (lead sulfate, $PbSO_4$), or cerussite (lead carbonate, $PbCO_3$). Because it is usually associated with minerals of zinc, silver, copper, gold, cadmium, antimony, and arsenic, special purification methods are frequently used before and after extraction of the metal from the ore concentrate by smelting.

Lead is widely used for its corrosion resistance, sound and vibration absorption, low melting point (solders), and relatively high imperviousness to various forms of radiation. Small amounts of copper, antimony and other metals can be alloyed with lead to achieve greater hardness, stiffness, or corrosion resistance than is afforded by the pure metal. Lead compounds are used in glazes and paints. About one third of United States lead consumption goes into storage batteries. About half of United States lead consumption is from secondary lead recovery. United States consumption of lead is in the range of one million tons annually.

Lead ingested by humans produces a variety of toxic effects including impaired reproductive ability, disturbances in blood chemistry, neurological disorders, kidney damage, and adverse cardiovascular effects. Exposure to lead in the diet results in permanent increase in lead levels in the body. Most of the lead entering the body eventually becomes localized in the bones where it accumulates. Lead is a carcinogen or cocarcinogen in some species of experimental animals. Lead is teratogenic in experimental animals. Mutagenicity data are not available for lead.

The recommended ambient water quality criterion for lead is identical to the existing drinking water standard for lead which is 0.050 mg/l. Available data show that adverse effects on aquatic life occur at concentrations as low as 7.5×10^{-4} mg/l of total recoverable lead as a 24-hour average with a water hardness of 50 mg/l as $CaCO_3$.

123. Mercury. Mercury is an elemental metal rarely found in nature as the free metal. Mercury is unique among metals as it remains a liquid down to about 39 degrees below zero. It is

relatively inert chemically and is insoluble in water. The principal ore is cinnabar (HgS).

Mercury is used industrially as the metal and as mercurous and mercuric salts and compounds. Mercury is used in several types of batteries. Mercury released to the aqueous environment is subject to biomethylation, conversion to the extremely toxic methyl mercury.

Mercury can be introduced into the body through the skin and the respiratory system as the elemental vapor. Mercuric salts are highly toxic to humans and can be absorbed through the gastrointestinal tract. Fatal doses can vary from 1 to 30 grams. Chronic toxicity of methyl mercury is evidenced primarily by neurological symptoms. Some mercuric salts cause death by kidney failure.

Mercuric salts are extremely toxic to fish and other aquatic life. Mercuric chloride is more lethal than copper, hexavalent chromium, zinc, nickel, and lead towards fish and aquatic life. In the food cycle, algae containing mercury up to 100 times the concentration in the surrounding sea water are eaten by fish that further concentrate the mercury. Predators that eat the fish in turn concentrate the mercury even further.

For the protection of human health from the toxic properties of mercury ingested through water and through contaminated aquatic organisms, the ambient water criterion is 0.00014 mg/l.

124. Nickel. Nickel is seldom found in nature as the pure elemental metal. It is a relatively plentiful element and is widely distributed throughout the earth's crust. It occurs in marine organisms and is found in the oceans. The chief commercial ores for nickel are pentlandite [$(Fe,Ni)_9S_8$], and a lateritic ore consisting of hydrated nickel-iron-magnesium silicate.

Nickel has many and varied uses. It is used in alloys and as the pure metal. Nickel salts are used for electroplating baths.

The toxicity of nickel to man is thought to be very low and systemic poisoning of human beings by nickel or nickel salts is almost unknown. In non-human mammals nickel acts to inhibit insulin release, depress growth, and reduce cholesterol. A high incidence of cancer of the lung and nose has been reported in humans engaged in the refining of nickel.

Nickel salts can kill fish at very low concentrations. However, nickel has been found to be less toxic to some fish than copper, zinc, and iron. Nickel is present in coastal and open ocean waters at concentrations in the range of 0.0001 to 0.006 mg/l although the most common values are 0.002 to 0.003 mg/l. Marine animals contain up to 0.4 mg/l and marine plants contain up to 3 mg/l. Higher nickel concentrations have been reported to cause reduction in photosynthetic activity of the giant kelp. A low concentration was found to kill oyster eggs.

For the protection of human health based on the toxic properties of nickel ingested through water and through contaminated aquatic organisms, the ambient water criterion is 0.0134 mg/l. If contaminated aquatic organisms are consumed, excluding consumption of water, the ambient water criterion is 0.100 mg/l. Available data show that adverse effects on aquatic life occur for total recoverable nickel concentrations as low as 0.0071 mg/l as a 24-hour average.

125. Selenium. Selenium (chemical symbol Se) is a non-metallic element existing in several allotropic forms. Gray selenium, which has a metallic appearance, is the stable form at ordinary temperatures and melts at 220°C. Selenium is a major component of 38 minerals and a minor component of 37 others found in various parts of the world. Most selenium is obtained as a by-product of precious metals recovery from electrolytic copper refinery slimes. United States annual production at one time reached one million pounds.

Principal uses of selenium are in semi-conductors, pigments, decoloring of glass, zerography, and metallurgy. It also is used to produce ruby glass used in signal lights. Several selenium compounds are important oxidizing agents in the synthesis of organic chemicals and drug products.

While results of some studies suggest that selenium may be an essential element in human nutrition, the toxic effects of selenium in humans are well established. Lassitude, loss of hair, discoloration and loss of fingernails are symptoms of selenium poisoning. In a fatal case of ingestion of a larger dose of selenium acid, peripheral vascular collapse, pulmonary edema, and coma occurred. Selenium produces mutagenic and teratogenic effects, but it has not been established as exhibiting carcinogenic activity.

For the protection of human health from the toxic properties of selenium ingested through water and through contaminated aquatic organisms, the ambient water criterion is 0.010 mg/l (i.e., the same as the drinking water standard). Available data show that adverse effects on aquatic life occur at concentrations higher than that cited for human toxicity.

126. Silver. Silver is a soft, lustrous, white metal that is insoluble in water and alkali. In nature, silver is found in the

elemental state (native silver) and combined in ores such as argentite (Ag_2S), horn silver ($AgCl$), and procisite (Ag_3AsS_3), and pyrangyrite (Ag_3SbS_3). Silver is used extensively in several industries, among them electroplating.

Metallic silver is not considered to be toxic, but most of its salts are toxic to a large number of organisms. Upon ingestion by humans, many silver salts are absorbed in the circulatory system and deposited in various body tissues, resulting in generalized or sometimes localized gray pigmentation of the skin and mucous membranes known as argyria. There is no known method for removing silver from the tissues once it is deposited and the effect is cumulative.

Silver is recognized as a bactericide and doses from 0.000001 to 0.0005 mg/l have been reported as sufficient to sterilize water. The criterion for ambient water to protect human health from the toxic properties of silver ingested through water and through contaminated aquatic organisms is 0.050 mg/l.

The chronic toxic effects of silver on the aquatic environment have not been given as much attention as many other heavy metals. Data from existing literature support the fact that silver is very toxic to aquatic organisms. Despite the fact that silver is nearly the most toxic of the heavy metals, there are insufficient data to adequately evaluate even the effects of hardness on silver toxicity. There are no data available on the toxicity of different forms of silver.

Bioaccumulation and concentration of silver from sewage sludge has not been studied to any great degree. There is some indication that silver could be bioaccumulated in mushrooms to the extent that there could be adverse physiological effects on humans if they consumed large quantities of mushrooms grown in silver enriched soil. The effect, however, would tend to be unpleasant rather than fatal.

127. Thallium. Thallium is a soft, silver-white, dense, malleable metal. Five major minerals contain 15 to 85 percent thallium, but they are not of commercial importance because the metal is produced in sufficient quantity as a by-product of lead-zinc smelting of sulfide ores. Thallium melts at 304°C. United States annual production of thallium and its compounds is estimated to be 1,500 pounds.

Industrial uses of thallium include the manufacture of alloys, electronic devices, and special glass. Thallium catalysts are used for industrial organic syntheses.

Acute thallium poisoning in humans has been widely described. Gastrointestinal pains and diarrhea are followed by abnormal sensation in the legs and arms, dizziness, and, later, loss of hair. The central nervous system is also affected. Somnolence, delerium or coma may occur. Studies on the teratogenicity of thallium appear inconclusive; no studies on mutagenicity were found; and no published reports on carcinogenicity of thallium were found.

For the protection of human health from the toxic properties of thallium ingested through water and contaminated aquatic organisms, the ambient water criterion is 0.013 mg/l.

128. Zinc. Zinc occurs abundantly in the earth's crust, concentrated in ores. It is readily refined into the pure, stable, silver-white metal. In addition to its use in alloys, zinc is used as a protective coating on steel. It is applied by hot dipping (i.e., dipping the steel in molten zinc) or by electroplating.

Zinc can have an adverse effect on man and animals at high concentrations. Zinc at concentrations in excess of five mg/l causes an undesirable taste that persists after wastewater treatment. For the prevention of adverse effects due to these organoleptic properties of zinc, five mg/l was adopted for the ambient water criterion. Available data show that adverse effects on aquatic life occur at concentrations as low as 0.047 mg/l as a 24-hour average.

Toxic concentrations of zinc compounds cause adverse changes in the morphology and physiology of fish. Lethal concentrations in the range of 0.1 mg/l have been reported. Acutely toxic concentrations induce cellular breakdown of the gills and possibly the clogging of the gills with mucous. Chronically toxic concentrations of zinc compounds cause general enfeeblement and widespread histological changes to many organs, but not to gills. Abnormal swimming behavior has been reported at 0.04 mg/l. Growth and maturation are retarded by zinc. Effects of zinc poisoning may not become apparent immediately, so that fish removed from zinc-contaminated water may die as long as 48 hours after removal.

In general, salmonoids are most sensitive to elemental zinc in soft water; the rainbow trout is the most sensitive in hard waters. A complex relationship exists between zinc concentration, dissolved zinc concentration, pH, temperature, and calcium and magnesium concentration. Prediction of harmful effects has been less than reliable and controlled studies have not been extensively documented.

The major concern with zinc compounds in marine waters is not with acute lethal effects, but rather with the long-term sublethal effects of the metallic compounds and complexes. Zinc accumulates in some marine species; marine animals contain zinc in the range of 6 to 1,500 mg/kg. From the point of view of acute lethal effects, invertebrate marine animals seem to be the most sensitive organism tested.

MASS OF POLLUTANTS

Pollutant average concentrations in the PM&F process waters were presented for the PM&F subcategories in Table VI-19. Of equal importance is the mass of pollutants in the process waters. Estimated pollutant masses generated per year are presented in this section.

Pollutant masses were estimated with a statistical methodology that combines information from both the sampling episodes and the questionnaire data base. This methodology is illustrated below. Refer to Table VII-11 for sampling data used in this example. The questionnaire survey data used in the example are presented in Table VII-12.

1. The example has two extrusion processes and one molding process in the contact cooling and heating water subcategory.

2. Calculate the average mass of pollutant discharged for each process. Use the water usage flow rates and the concentrations measured on the sampling days (see Table VII-11).

Process	Average Mass of Pollutant (mg/hr)
EX-1	$\frac{(10\ \text{mg/l})(100\ \text{l/hr})+(30\ \text{mg/l})(140\ \text{l/hr})+(15\ \text{mg/l})(100\ \text{l/hr})}{3} = 2{,}230\ \text{mg/hr}$
EX-2	$\frac{(50\ \text{mg/l})(300\ \text{l/hr}) + (10\ \text{mg/l})(400\ \text{l/hr})}{2} = 9{,}500\ \text{mg/hr}$
MD-1	$\frac{(100\ \text{mg/l})(50\ \text{l/hr})+(110\ \text{mg/l})(60\ \text{l/hr})+(120\ \text{mg/l})(60\ \text{l/hr})}{3} = 6{,}270\ \text{mg/hr}$

Table VII-11

DATA FOR POLLUTANT X - MASS CALCULATION EXAMPLE

	Contact Cooling and Heating Water Subcategory											
	Day 1			Day 2			Day 3			Duplicate		
Process	Conc. (mg/l)	Flow (l/hr)	Prod. (kg/hr)	Conc. (mg/l)	Flow (l/hr)	Prod. (kg/hr)	Conc. (mg/l)	Flow (l/hr)	Prod. (kg/hr)	Conc. (mg/l)	Flow (l/hr)	Prod. (kg/hr)
Extrusion (EX-1)	10	100	50	--	--	--	30	140	100	15	100	50
Extrusion (EX-2)	50	300	1000	10	400	900	--	--	--	--	--	--
Molding (MD-1)	100	50	100	--	--	--	110	60	130	120	60	130

Table VII-12

QUESTIONNAIRE SURVEY DATA USED TO ESTIMATE POLLUTANT MASSES

Type of Process	Estimated Number of Processes* Direct Dischargers	Estimated Number of Processes* Indirect Dischargers	Average Plastic Production (kkg/yr/process)** Direct Dischargers	Average Plastic Production (kkg/yr/process)** Indirect Dischargers
Calendering	5	10	1,980	11,000
Casting	5	25	7,300	1,580
Coating and Laminating	10	35	293	1,800
Extrusion	631	657	6,740	2,650
Molding	30	89	1,490	900
Thermoforming	15	29	2,060	2,240
Cleaning	104	232	3,150	1,390
Finishing	10	68	46	2,200

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*Calculated by applying the percentages in Table VI-6 to the total estimated number of contact cooling and heating water processes presented in Table VI-7.

**Calculated using data from the PM&F questionnaire survey data base.

3. For the processes that belong to a type of process, sum the average mass of pollutants (calculated in step 2).

Type of Process	Summed Average Mass (mg/hr)
Extrusion	2,230 mg/hr + 9,500 mg/hr = 11,730 mg/hr
Molding	6,270 mg/hr

4. For each process, calculate an average plastic production rate with measurements taken on the sampling day (see Table VII-11).

Process	Average Plastic Production Rate (kg/hr)
EX-1	$\frac{50+100+50}{3} = 67$ kg/hr
EX-2	$\frac{1,000+900}{2} = 950$ kg/hr
MD-1	$\frac{100+130+130}{3} = 120$ kg/hr

5. For the processes that belong to a type of process, sum the average plastic production rates calculated in step 4.

Type of Process	Summed Average Plastic Production Rate (kg/hr)
Extrusion	67 kg/hr + 950 kg/hr = 1,117 kg/hr
Molding	120 kg/hr

6. For each type of process, divide the summed average pollutant mass (calculated in step 3) by the summed average plastic production rate (calculated in step 5) to calculate a pollutant mass per unit of production.

Type of Process	Pollutant Mass Per Unit of Production (mg Pollutant/kg Plastic)
Extrusion	$\frac{11,730 \text{ mg/hr}}{1,117 \text{ kg/hr}} = 10.5 \frac{\text{mg}}{\text{kg}}$
Molding	$\frac{6,270 \text{ mg/hr}}{120 \text{ kg/hr}} = 52.3 \frac{\text{mg}}{\text{kg}}$

7. For each type of process, multiply the pollutant mass per unit of production (calculated in step 6) by the estimated number of processes and by the average plastic production from the questionnaire data base. This calculation estimates the pollutant mass for each type of process in the subcategory. The questionnaire data are presented in Table VII-12 for the different types of processes for both direct and indirect dischargers. This example calculation estimates the direct discharge pollutant mass. An analogous calculation for the indirect discharge pollutant mass uses the values for indirect dischargers presented in Table VII-12.

Type of Process	Estimated Direct Discharge Pollutant Mass (kg/yr)
Extrusion	(10.5 mg/kg)(631 processes)(6,740 kkg/yr/process) = 44,700 kg/yr
Molding	(52.3 mg/kg)(30 processes)(1,490 kkg/yr/process) = 2,340 kg/yr

8. In the contact cooling and heating water subcategory, an estimate of the pollutant mass per unit of production for the types of processes that have no sampling data was also calculated. This was calculated by summing the estimated pollutant masses (calculated in step 7) and then dividing by the sum of questionnaire survey factors used in the pollutant mass estimate. For example, combining the extrusion and molding results from step 7 gives the following:

$$\frac{44{,}700\ \text{kg/yr} + 2{,}340\ \text{kg/yr}}{[(631\ \text{processes})(6{,}740\ \text{kkg/yr/process}) + (30\ \text{processes})(1{,}490\ \text{kkg/yr/process})]}$$

$$= 0.011\ \frac{\text{kg pollutant}}{\text{kkg plastic}}$$

This pollutant mass per unit of production is an estimate to use for the types of processes that have no sampling data (i.e., casting, calendering, coating and laminating, and thermoforming).

9. To estimate the pollutant mass discharged for the type of processes that have no available sampling data, multiply the pollutant mass per unit of production (calculated in step 8) by the appropriate factors in Table VII-12.

Type of Process	Estimated Direct Discharge Pollutant Mass (kg/yr)
Calendering	(0.011 kg/kkg)(5 processes)(1,980 kkg/yr/process) = 109 kg/yr
Casting	(0.011 kg/kkg)(5 processes)(7,300 kkg/yr/process) = 402 kg/yr
Coating & Laminating	(0.011 kg/kkg)(10 processes)(293 kkg/yr/process) = 32 kg/yr
Thermoforming	(0.011 kg/kkg)(15 processes)(2,060 kkg/yr/process) = 340 kg/yr

10. Sum the estimated pollutant masses for both sampled and unsampled types of processes (calculated in steps 7 and 9), to obtain an estimate of the total direct discharge pollutant mass for the subcategory.

Type of Process		Estimated Direct Discharge Pollutant Mass (kg/yr)
Extrusion		44,700
Molding		2,340
Calendering		109
Casting		402
Coating & Laminating		32
Thermoforming		340
	TOTAL	47,923 kg/yr of Pollutant X

This calculation procedure is more simplified for the cleaning water subcategory and for the finishing water subcategory because these subcategories have only one type of process (i.e., cleaning or finishing processes). Calculation steps one through seven need only be performed for these subcategories.

This methodology was used to estimate the mass of pollutants discharged by direct and indirect dischargers in the three PM&F subcategories. Those estimates are presented in Table VII-13. Masses were estimated for the conventional and nonconventional pollutants in all three subcategories, even though not all of these pollutants were found in treatable concentrations for each subcategory. This was done to examine the total pollutant mass in the subcategories. Masses for the priority pollutants were calculated for the pollutants in Table VII-8. This was also done to evaluate the priority pollutant mass discharged by the industry.

Table VII-13

POLLUTANT MASSES
(CONTACT COOLING AND HEATING WATER SUBCATEGORY)

Conventional Pollutants	Direct Discharge Mass (kg/yr)	Indirect Discharge Mass (kg/yr)	Total Mass (kg/yr)
BOD_5	127,000	65,600	192,600
Oil and Grease	99,200	74,800	174,000
TSS	33,000	23,000	56,000
TOTAL	259,200	163,400	422,600
Nonconventional Pollutants			
COD	1,760,000	900,000	2,660,000
TOC	596,000	320,000	916,000
Total Phenols	441	342	783
TOTAL	2,356,441	1,220,342	3,576,783
Priority Pollutants			
4. benzene	2,040	872	2,912
11. 1,1,1-trichloroethane	3,970	1,700	5,670
22. parachlorometa cresol	3,630	1,550	5,180
23. chloroform	212	95	307
44. methylene chloride	3,810	1,640	5,450
65. phenol	662	289	951
66. bis(2-ethylhexyl) phthalate	9,470	5,460	14,930
68. di-n-butyl phthalate	211	98.7	309.7
86. toluene	21.9	13.7	35.6

Table VII-13 (Continued)

POLLUTANT MASSES
(CONTACT COOLING AND HEATING WATER SUBCATEGORY) (Continued)

Priority Pollutants	Direct Discharge Mass (kg/yr)	Indirect Discharge Mass (kg/yr)	Total Mass (kg/yr)
89. aldrin	0.022	0.033	0.055
90. dieldrin	0.022	0.055	0.077
99. endrin aldehyde	0.044	0.019	0.063
102. alpha-BHC	2.68	1.92	4.60
103. beta-BHC	1.52	0.648	2.17
104. gamma-BHC	0.278	0.173	0.451
105. delta-BHC	6.37	2.80	9.17
117. beryllium	3.24	1.38	4.66
118. cadmium	116	49.7	165.7
119. chromium	296	142	438
120. copper	165	82.1	247.1
122. lead	16,800	7,220	24,020
123. mercury	0.002	0.004	0.006
124. nickel	392	193	585
126. silver	9.28	4.00	13.28
127. thallium	136	58.1	194.1
128. zinc	567	527	1,094
TOTAL	42,500	20,000	62,500

Table VII-13 (Continued)

POLLUTANT MASSES
(CLEANING WATER SUBCATEGORY)

Conventional Pollutants	Direct Discharge Mass (kg/yr)	Indirect Discharge Mass (kg/yr)	Total Mass (kg/yr)
BOD_5	25,600	25,200	50,800
Oil and Grease	14,200	14,000	28,200
TSS	199,000	196,000	395,000
TOTAL	238,800	235,200	474,000
Nonconventional Pollutants			
COD	32,000	31,500	63,500
TOC	177,000	174,000	351,000
Total Phenols	7,400	7,290	14,690
TOTAL	216,400	212,790	429,190
Priority Pollutants			
4. benzene	0.532	0.524	1.056
22. parachlorometa cresol	0.0413	0.0406	0.0819
44. methylene chloride	3.58	3.53	7.11
62. N-nitrosodiphenylamine	0.482	0.476	0.958
65. phenol	59.2	58.3	117.5
66. bis(2-ethylhexyl) phthalate	2.21	2.18	4.39
86. toluene	3.74	3.68	7.42

Table VII-13 (Continued)

POLLUTANT MASSES
(CLEANING WATER SUBCATEGORY) (Continued)

Priority Pollutants	Direct Discharge Mass (kg/yr)	Indirect Discharge Mass (kg/yr)	Total Mass (kg/yr)
89. aldrin	0.0075	0.00739	0.01489
100. heptachlor	0.00815	0.00803	0.01618
102. alpha-BHC	0.0000182	0.0000178	0.0000360
103. beta-BHC	0.00256	0.00254	0.00510
104. gamma-BHC	0.0196	0.0193	0.0389
105. delta-BHC	0.0210	0.0206	0.0416
114. antimony	0.970	0.984	1.954
115. arsenic	0.068	0.069	0.137
119. chromium	5.62	5.53	11.15
120. copper	13.1	12.9	26.0
123. mercury	0.002	0.002	0.004
124. nickel	1.25	1.23	2.48
125. selenium	3.74	3.68	7.42
126. silver	0.0607	0.0617	0.1217
128. zinc	178	176	354
TOTAL	273	269	542

Table VII-13 (Continued)

POLLUTANT MASSES
(FINISHING WATER SUBCATEGORY)

Conventional Pollutants	Direct Discharge Mass (kg/yr)	Indirect Discharge Mass (kg/yr)	Total Mass (kg/yr)
BOD$_5$	237	76,900	77,137
Oil and Grease	287	93,000	93,287
TSS	3,630	1,180,000	1,183,630
TOTAL	4,154	1,349,900	1,354,054
Nonconventional Pollutants			
COD	640	207,000	207,640
TOC	889	288,000	288,889
Total Phenols	8.28	2,680	2,688.28
TOTAL	1,537.28	497,680	499,217.28
Priority Pollutants			
8. 1,2,4-trichlorobenzene	0.225	72.9	73.125
11. 1,1,1-trichloroethane	0.0307	9.95	9.9807
28. 3,3'-dichlorobenzidine	0.0833	27.0	27.0833
38. ethylbenzene	0.181	58.7	58.881
65. phenol	0.263	85.1	85.363
66. bis(2-ethylhexyl) phthalate	18.3	5,920	5,938.3
68. di-n-butyl phthalate	1.17	378	379.17
71. dimethyl phthalate	1.28	414	415.28
87. trichloroethylene	0.155	50.2	50.355

Table VII-13 (Continued)

POLLUTANT MASSES
(FINISHING WATER SUBCATEGORY) (Continued)

Priority Pollutants	Direct Discharge Mass (kg/yr)	Indirect Discharge Mass (kg/yr)	Total Mass (kg/yr)
114. antimony	0.0397	12.9	12.9397
115. arsenic	0.0348	11.3	11.3348
119. chromium	0.0397	12.9	12.9397
120. copper	1.08	349	350.08
121. cyanide	0.194	62.7	62.894
122. lead	1.15	374	375.15
123. mercury	0.000566	0.183	0.183566
124. nickel	0.156	50.7	50.856
125. selenium	1.15	371	372.15
128. zinc	3.33	1,080	1,083.33
TOTAL	29	9,341	9,370

SECTION VIII

WASTEWATER CONTROL AND TREATMENT TECHNOLOGIES

INTRODUCTION

This section discusses the control and treatment technologies considered in this final rulemaking for the control of pollutants in process waters generated by PM&F processes. These control and treatment technologies are unit processes that are used to develop model treatment technology options. The specific model technology options considered for BPT, BAT, NSPS, and PSES/PSNS are discussed in Sections X, XI, XII, and XIII, respectively.

Prior to publication of the proposed PM&F regulation, EPA considered a wide range of in-process control and end-of-pipe treatment technologies. These technologies are discussed in detail in the preamble to the proposed PM&F regulation (see 49 FR 5862) and in the technical development document supporting the proposed PM&F regulation. Additional information obtained subsequent to the proposal to evaluate comments and data submitted by commenters on the proposed regulation and revisions in EPA's data averaging methodology (see Section VI of this document) led to changes in technologies considered in developing model treatment technology options for the final PM&F regulation. Based on their applicability to PM&F process waters and general technical feasibility, the following control and treatment technologies, which are divided into in-plant control technologies and end-of-pipe treatment technologies, were considered for the final PM&F regulation:

- In-plant control technologies

  --Process water recycle
  --In-process measures

- End-of-pipe treatment technologies

  --Settling
  --pH adjustment
  --Activated sludge
  --Activated carbon adsorption
  --Filtration (suspended solids removal)
  --Vacuum filtration (sludge dewatering)

The remainder of this section describes each of these technologies. In particular, the following topics are discussed, where applicable, for each technology:

- Process description,
- Applications,
- Technology status,
- Limitations,
- Reliability,
- Environmental impact, and
- Treatability data.

The primary literature sources relied on during the development of this section were EPA's Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants and EPA's Innovative and Alternative Technology Assessment Manual. Metcalf and Eddy, Inc.'s Wastewater Engineering, Treatment/Disposal/Reuse served as a general reference. Refer to Section XVI for reference details.

IN-PLANT CONTROL TECHNOLOGY

The purpose of in-plant control technology for plants in the plastics molding and forming category is to reduce or eliminate the amount of process water requiring end-of-pipe treatment and thereby either reduce the size of the treatment technology or eliminate the need for the treatment technology. In-plant technologies considered for the PM&F category are: (1) process water recycle; and (2) in-process measures.

Process Water Recycle

Recycling of process water is the practice of recirculating water to be used again for the same purpose or process. Water recycle is distinguished from water reuse, which is the recirculation of process water to be used again for a different purpose or process. An example of water recycle would be to use rinse water more than once in the same rinsing operation; whereas in water reuse, the rinse water would be used again, but in a different operation. Both practices result in a reduction in the amount of process water discharged.

Applications. Two types of recycle are possible - recycle with no discharge (100 percent recycle) and recycle with a discharge (or bleed stream). One hundred percent recycle may be prohibited by the presence of dissolved solids in the process water (e.g., sulfates and chlorides). These dissolved solids precipitate if their solubility limits are exceeded and form scale on pipes and equipment. A bleed stream, either continuous or periodic, is necessary to prevent maintenance problems that would be created by the precipitation of dissolved solids. One hundred percent recycle is generally applicable to low flow rate processes and to process waters with low pollutant concentrations.

Process water that requires cooling is recycled through a unit that lowers the temperature of the water so that it can be recycled. Two types of equipment may be used for 100 percent recycle of process water that needs to be cooled. The first and simplest piece of equipment is a holding tank. Process water is held up in a tank until the temperature drops sufficiently, through passive heat transfer to the environment, to allow the water to be recycled. A holding tank is only practical for low flow rates because tank sizes increase dramatically when the flow rate increases. One hundred percent recycle of process waters that needs to be cooled may also be achieved using chillers, which cool the water by mechanical refrigeration. In a chiller, the cooling water is passed through a heat exchanger that is cooled by a low boiling, vaporized refrigerant. Chillers can be used with processes with medium flow rates because they can be purchased as self-contained units that are easy to install. At higher flow rates, the chiller's high energy usage per unit of cooling makes its use less attractive. Recycle systems such as cooling tanks or chiller units are generally cleaned out once every one or two years and thus potentially may require the disposal of some amount of waste.

Recycle with a discharge is generally practiced for processes with high flow rates. Process waters from those processes that need to be cooled can be recycled through cooling towers that lower the water temperature by evaporative cooling. In a typical cooling tower configuration, water is distributed at the top of the tower in a manner that provides a large contact area between air and water. Air circulates countercurrently to the water to be cooled. Heat is transferred from the water to the air as water evaporates. Cooling towers can be used with processes with flow rates from as low as 15 gpm to several hundred gpm.

One hundred percent recycle of process water through cooling towers is prohibited because the concentration of dissolved solids in the process waters may cause scale to form on the cooling tower. A bleed stream is needed to reduce the concentration of these solids below the concentration where they would precipitate and cause pipe plugging and scaling on the cooling tower.

Process water that requires the removal of solids and oil and grease before it can be used again in the process can be recycled through a settling tank. Generally, process water that requires removal of suspended solids and oil and grease has to be replaced after a period of time. This can be done either by replacing the small continuous discharge flow from the unit with fresh water or by periodically changing all of the process water within the recycle unit.

Technology Status. Process water recycle is currently practiced by 44 percent of the wet processes in the contact cooling and heating water subcategory, 13 percent of wet processes in the cleaning water subcategory, and 18 percent of wet processes in the finishing water subcategory. When recycle was reported, the recycle percentage generally ranged from 90 to 100 percent. Table VIII-1 contains a distribution of the number of processes with various recycle percentages by PM&F subcategory based on data from the questionnaire data base.

Limitations. A potential limitation of 100 percent recycle of process water is the buildup of dissolved solids. The presence of dissolved solids may result in scale formation on piping and equipment and may also affect product quality. Dissolved solids levels can be controlled in cases where a bleed stream is discharged by increasing the bleed flow. For recycle systems that include settling, solids removed from the settling unit require disposal. Small quantities of scale and settled solids also have to be periodically removed from recycle units with a discharge.

The percent of process water that can be recycled depends on product quality. In some cases, process water may not be recycled because product quality requires that only "potable" water be used in the process.

Reliability. Recycle units have few components with moving parts; most of the routine maintenance is needed to service the recirculating pump.

Environmental Impact. Recycle is an important water conservation measure because both the demand for raw water and the amount of water discharged are reduced when process water is recycled. A reduction in the amount of process water that requires treatment results in a reduction in the required treatment unit capacity and, therefore, the cost of end-of-pipe treatment. In addition, the performance of the treatment process, in terms of percent removal, may be improved when recycle is used because pollutants in the recycle unit discharge are more concentrated. Generally, end-of-pipe treatment perform more effectively with higher pollutant concentrations.

In-Process Measures

Two opportunities exist for plants to reduce the quantity of water used by PM&F processes. One is to decrease the quantity of water that flows through the process; the other is to modify the process so that the use of process water is no longer necessary.

Table VIII-1

DISTRIBUTION OF PM&F PROCESSES WITH RECYCLE

	Number of Processes in Questionnaire Data Base With Recycle (Percent of Total Wet Processes in Subcategory)		
Percent Recycle	Contact Cooling and Heating Water Subcategory	Cleaning Water Subcategory	Finishing Water Subcategory
100	83 (19.4)	0	3 (13.6)
95-99.9	63 (14.7)	7 (9.9)	1 (4.5)
90-94.9	15 (3.5)	1 (1.4)	0
75-89.9	14 (3.3)	1 (1.4)	0
50-74.9	9 (2.1)	0	0
0.1-49.9	4 (0.9)	0	0
0	240 (56.1)	62 (87.3)	18 (81.9)
	428 (100)	71 (100)	22 (100)

Applications. The Agency believes that, based on observations made during plant visits, some PM&F plants may not pay close attention to water use. Satisfactory operation may be achieved with smaller rinse or contact cooling water flows. The practice of shutting off process water during periods when a production unit is inoperative and adjusting flow rates during periods of low activity can reduce the volume of water to be treated or discharged. Producers with a high water use should be able to reduce their water use through simple flow reduction procedures such as more careful adjustment of process water flow rates and reduction of overflow and dragout from quench tanks.

The Agency considered process modifications for reducing process water use because approximately 80 percent of the processes in the PM&F category do not require the use of process water. The possibility of eliminating the use of process water by the other 20 percent of PM&F processes that use process water, was studied. Investigation into the specific uses of process water revealed that the 20 percent of manufacturers who are using process water need that water for efficient and effective operation of their processes. The majority of PM&F process water is contact cooling water used during extrusion processes. This water is necessary for effective heat transfer, particularly during pelletizing processes and for the extrusion of tube, pipe, profiles, or plastic coverings on wire and cable. Process water is also needed for contact cooling during other molding and forming process to maintain product integrity. It is also needed to clean both the surfaces of the plastic products and surfaces of shaping equipment used to produce those products and to finish plastic products. Water is required in cleaning processes and in finishing processes as a carrier media. PM&F processes that use process water need the water for effective operation of the process; they cannot be converted to dry processes. Therefore, process modifications to eliminate the use of process water are not appropriate for wet PM&F processes.

END-OF-PIPE TREATMENT TECHNOLOGY

This section discusses end-of-pipe treatment technologies applicable to treatment of process waters discharged by PM&F processes. End-of-pipe treatment technologies are used to reduce the concentrations of pollutants in process waters. The end-of-pipe treatment technologies that were considered will treat either some or all of the pollutants listed in Table VIII-2.

Settling

Settling is a process that removes solid particles from a liquid matrix by gravitational force. This is done by reducing the velocity of the influent flow so that gravitation settling can

Table VIII-2

POLLUTANTS AND POLLUTANT PROPERTIES FOUND IN TREATABLE CONCENTRATIONS IN PM&F PROCESS WATERS

Conventional Pollutants

- BOD_5
- Oil and Grease
- TSS
- pH

Nonconventional Pollutants

- COD
- TOC
- Total Phenols

Priority Pollutants

65. phenol
66. bis(2-ethylhexyl) phthalate
68. di-n-butyl phthalate
71. dimethyl phthalate
128. zinc

occur. Simple settling requires long retention times to achieve high removal efficiencies. Settling tanks can be designed with baffles to eliminate the turbulence caused by influent water and have sloping bottoms to aid in sludge collection. Settling tanks are often designed so that oil and grease separation also occurs. Oil and grease and other floatable materials can be removed by surface skimming.

Applications. Settling can be effectively used to treat wastewater with high concentrations of oil and grease and suspended solids. Toxic metals removals have also been achieved in settling tanks.

Technology Status. Settling has been effectively demonstrated in the treatment of numerous industrial wastewaters. It is one of the oldest wastewater treatment technologies in use. Eleven plants in the questionnaire data base for the PM&F category have settling/clarification units in place to treat PM&F process waters.

Limitations. Excessively long retention times may be required under certain conditions, particularly when the specific gravity of suspended particles is close to one or the particle sizes are small. Colloidal particles with diameters less than one micron may not be effectively settled without the addition of a flocculant or coagulating agent. Additionally, dissolved pollutants are not removed by settling.

Reliability. The lack of mechanical complexity makes this technology very reliable.

Environmental Impact. The major environmental impact associated with settling is the disposal of the solid material removed from the wastewater.

Treatability Data. Mean removal efficiencies for conventional and selected nonconventional pollutants in a settling unit are presented in Table VIII-3.

pH Adjustment

pH adjustment is the process of adjusting an acidic or a basic wastewater to a pH of an acceptable value. Adjusting the pH of the wastewater is necessary for various reasons. The pH should be adjusted to: (1) prevent metal corrosion and/or damage to equipment and structures; (2) protect aquatic life and human health; (3) ensure effective operation of a treatment process; and (4) provide neutral pH water for recycle. pH adjustment may also be needed to break emulsions, to insolubilize certain

Table VIII-3

REMOVAL EFFICIENCIES FOR CONVENTIONAL AND SELECTED NONCONVENTIONAL POLLUTANTS IN A SETTLING TANK

Pollutant	Mean Removal Efficiency (%)
BOD5	33
Oil and Grease	47
TSS	82
COD	71
TOC	40
Total Phenols	43

Source: Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, July 1980, EPA 600/8-80-042c.

chemical species, or to control chemical reaction rates (e.g., chlorination). Generally, the pH of a wastewater should be between 6.0 and 9.0.

The actual process of adjustment to a neutral pH is accomplished by the addition of a basic material to an acidic material or by adding an acid to an alkaline material. Addition of the neutralization agent must be carefully controlled to avoid large temperature increases due to the exothermic nature of most acid-base neutralization reactions. Neutralization chemicals can be added manually or automatically to a mixed tank. Continuous pH monitoring is usually included in an automatic chemical addition system.

Applications. This technology is widely applied in the treatment of wastewaters.

Technology Status. pH adjustment is widely used in industrial waste treatment. Seven PM&F plants that treat process waters from primarily PM&F processes reported that they adjusted the pH of their process waters (see Table VI-4).

Limitations. The pH adjustment rate may be limited by heat effects accompanying the neutralization reaction. In most cases, proper planning of the neutralization process with respect to concentration of the neutralizing agent, rate of addition, reaction time, and equipment design can alleviate the heat problem.

Reliability. The pH adjustment process is highly reliable if properly monitored.

Environmental Impact. The environmental impacts associated with pH adjustment are, in general, minor. However, pH adjustment may result in precipitation of dissolved pollutants in certain wastewaters. These precipitated solids may eventually settle and require disposal. In addition, when acids are added to wastewaters containing certain salts, such as sulfide, toxic gases may be produced.

Activated Sludge

The activated sludge process is an aerobic (i.e., in the presence of oxygen) decomposition process in which organic material is oxidized by microorganisms. These microorganisms utilize organic pollutants as a source of food and convert them into carbon dioxide, water, energy, and cellular material, which may be removed by liquid-solids separation. Activated sludge treatment is distinguished from other types of biological treatment by the return of settled microorganisms (i.e., the acidvated sludge) to contact with incoming wastewater. The activated sludge process is used to remove dissolved and colloidal biodegradable organic pollutants from wastewater.

A flow diagram of a conventional activated sludge process is presented in Figure VIII-1. There are two basic unit operations involved: (1) contacting of the influent wastewater and microorganisms in the presence of oxygen, and subsequently, (2) separation of the liquid/solids mixture that forms. The activated sludge process was developed as a continuous flow process because of the underlying concept of recycling activated sludge. In the first step, or the contacting phase, the microorganisms oxidize soluble and colloidal organic pollutants to carbon dioxide and water in the presence of molecular oxygen. The intimate contact required between the wastewater and microorganisms is achieved by mixing and turbulence induced by aeration. The mixture of microorganisms and wastewater (called mixed liquor) formed in the contactor or aeration basin is transferred to a gravity settling unit for liquid/solids separation. A large portion of the microorganisms that settle in the settling unit is recycled to the contactor to be mixed with incoming wastewater; the remaining excess sludge is transferred to sludge handling processes.

The mechanism of aerobic decomposition in the activated sludge process can be expressed as:

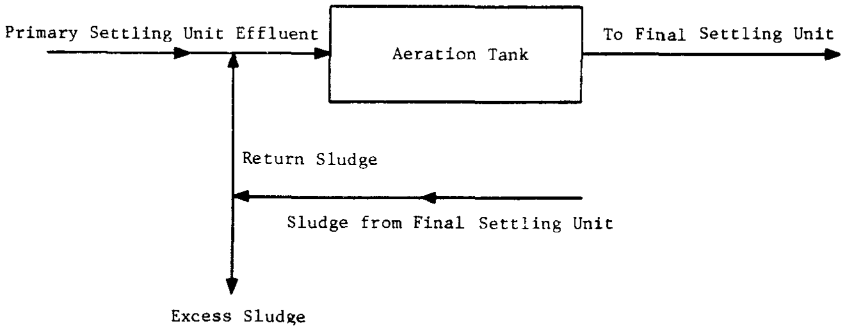
$$\text{Organic Material} + O_2 + \text{Nutrients} \xrightarrow{\text{Microorganisms}} CO_2 + H_2O + \text{Energy} + \text{Microorganisms}$$

Two separate phases actually occur in parallel; one is the synthesis of organic materials into new microorganism cells in the presence of nutrients, and the other is the oxidation of organic material to CO_2, H_2O, and energy in the presence of oxygen and microorganisms. Two primary nutrients are required for the formation of new cells in the former reaction; these are nitrogen and phosphorus. Most wastewaters contain sufficient quantities of nutrients; however, nutrients have to be added where this is not the case.

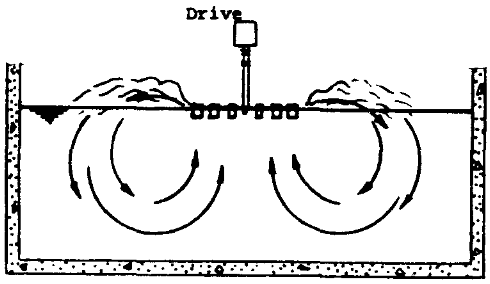
Oxygen is required in this process to support the oxidation and synthesis reactions. Various aeration methods are employed to transfer oxygen to wastewater. They include mechanical aeration and diffused aeration.

Mechanical Aeration. Mechanical aeration methods include a submerged turbine with compressed air spargers (agitator/sparger system) and surface mechanical entrainment aerators. The agitator/sparger system consists of a radial-flow turbine located below the mid-depth of the basin with compressed air supplied to the turbine through a sparger. The surface-type aerators entrain

Flow Diagram, Conventional Activated Sludge Process



Mechanical Surface Aeration



Diffused Aeration

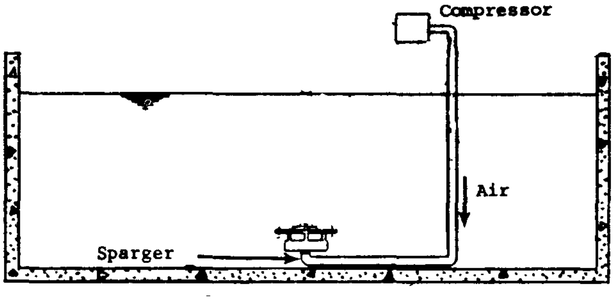


Figure VIII-1

ACTIVATED SLUDGE TREATMENT PROCESS

Figures adapted from Innovative and Alternative Technology Assessment Manual, EPA 430/9-78-009.

atmospheric air by producing a region of intense turbulence at the water surface. They are designed to pump large quantities of liquid, thus dispersing the entrained air and agitating and mixing the basin contents. Figure VIII-1 contains a schematic diagram of a mechanical surface aeration unit.

Diffused Aeration. In a diffused air system, compressors are used to supply air to a diffusion network. Diffused air systems may be classified as fine bubble or coarse bubble. Diffusers commonly used in the activated sludge process include porous ceramic plates laid in the basin bottom (fine bubble), porous ceramic domes or ceramic or plastic tubes connected to a pipe header and lateral system (fine bubble), tubes covered with synthetic fabric or wound filaments (fine or coarse bubble), and specifically designed spargers with multiple openings (coarse bubble). A diffused aeration sparger system is also depicted in Figure VIII-1.

Two modifications to the activated sludge process are pure oxygen and extended aeration:

Pure Oxygen. The use of pure oxygen for activated sludge treatment has become competitive with the use of air due to the development of efficient oxygen dissolution systems. The benefits of substituting pure oxygen for air include reduced power requirements for dissolving oxygen in the wastewater, reduced aeration tank volume, and improved biokinetics of the activated sludge. Lower amounts of excess sludge are generated; the thickening capability of pure oxygen activated sludge is generally greater than the thickening capability of the air activated sludge.

Extended Aeration. Extended aeration is a modification of the activated sludge process in which the fundamental idea is to minimize the amount of excess sludge, which represents a disposal problem. Extended aeration is distinguished from the conventional activated sludge process by longer retention times, lower food to microorganism ratios, higher oxygen consumptions, and higher concentration of microorganisms in the contactor. All of these factors lead to a decrease in the amount of sludge that has to be disposed of.

Excess sludge is formed in the activated sludge process because there is a net increase in the microoganism formation. However, there is an additional reaction that occurs in extended aeration in which the new microorganism cells undergo self-oxidation because sufficient time is allowed for further completion of the oxidation process. In the self-oxidation step, the microorganisms consume their own cell material for energy (a step also referred to as endogenous respiration). However, there is always a portion of the sludge that is non-biodegradable.

The extended aeration process is generally applicable to relatively small wastewater flows for which the additional retention time (and aeration basin volume) is less costly compared to costs of the aeration basin volume for larger flows. The application of extended aeration for small flows is usually accomplished with package treatment plants. There are a variety of proprietary extended aeration package plants available on the market today. A typical design features three chambers. The influent enters the first chamber where scum and sludge are separated. The second chamber is where the aeration occurs. The third and final compartment is a settling chamber where sludge settles by gravity and is returned to the aeration portion of the unit. Figure VIII-2 presents a diagram of an extended aeration activated sludge package plant.

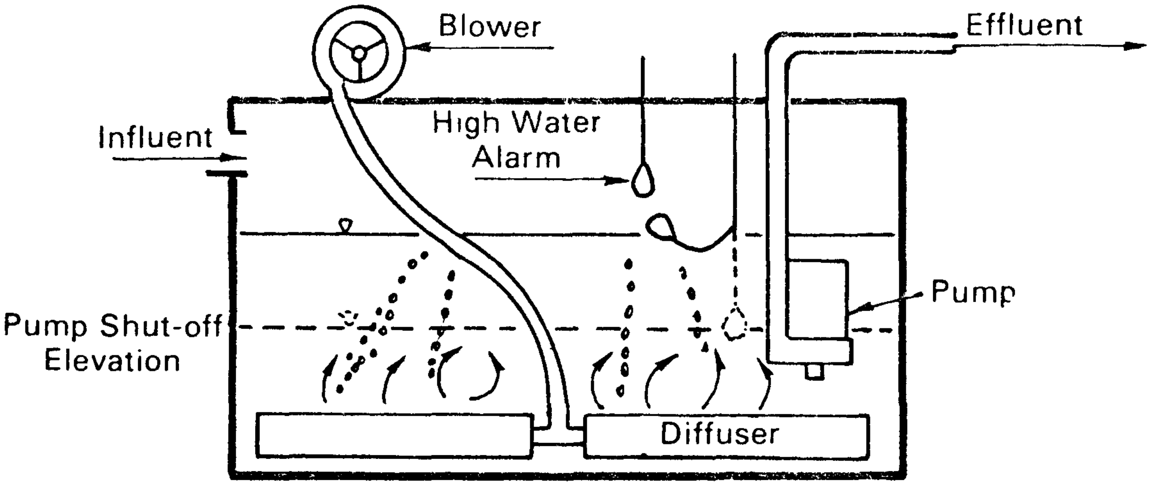
Applications. The activated sludge process is employed in domestic and industrial wastewater treatment for the removal of conventional, nonconventional, and priority organic pollutants. Limited priority pollutant metals removal has also been observed in activated sludge processes. Activated sludge processes can be used to treat PM&F process waters to remove dissolved organic pollutants found in treatable concentrations (see Table VIII-2). Industrial wastewater that is amenable to biological treatment and degradation may be jointly treated with domestic wastewater in an activated sludge process.

Technology Status. Activated sludge has not been demonstrated for the treatment of process waters generated solely by PM&F processes. However, it is a widely demonstrated, effective biological treatment process that has been used to treat wastewaters with conventional pollutant characteristics similar to the conventional pollutant characteristics of PM&F process waters.

Limitations/Reliability. Activated sludge treatment processes can be upset with variations in hydraulic and organic loads. For example, shock loads of phenolic compounds will kill the microorganisms that oxidize the organic materials and make the activated sludge process work. Under steady state conditions, phenols can be treated in concentrations up to 500 mg/l (Metcalf & Eddy, Inc.). Activated sludge processes are also not designed for an intermittent wastewater flow. Other disadvantages are high operating costs, operational complexity, and energy consumption. The activated sludge process must be well maintained for it to work properly.

Environmental Impact. The activated sludge process requires proper disposal of sludge to avoid solid waste pollution problems. Excess sludge generation is generally in the range of 0.15 to 0.7 pound per pound BOD_5 removed (EPA Treatability Manual). Energy requirements are approximately 200 kwh/yr per 1,000 gpd

Batch - Extended Aeration



Flow-Through Extended Aeration

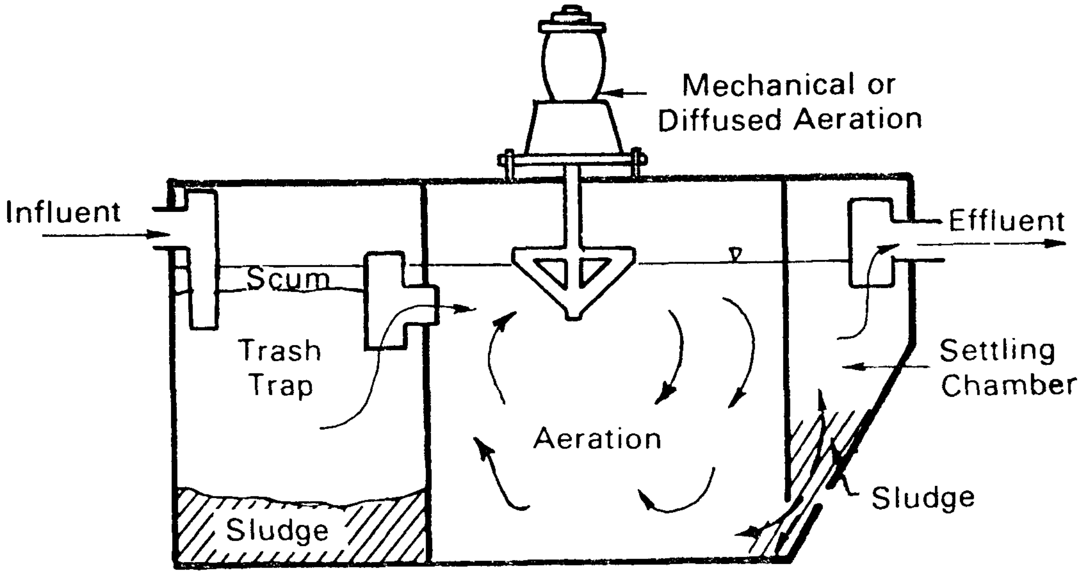


Figure VIII-2

EXTENDED AERATION ACTIVATED SLUDGE PACKAGE PLANTS treated (Innovative and Alternative Technology Assessment Manual). Improperly operated systems can cause odor problems.

Treatability Data. Treatability data for activated sludge processes treating solely PM&F process waters are not available. However, treatability data for activated sludge processes are available from several studies of other industrial categories.

For conventional pollutants (i.e., BOD_5, oil and grease, TSS), the available treatability data most applicable to the PM&F category are data from the organic chemicals, plastics, and synthetic fibers category because wastewaters generated by some processes in that subcategory and by some PM&F processes are similar with respect to conventional pollutant concentrations.

Treatability data for nonconventional pollutants (i.e., COD, TOC, total phenols) were based on percent removal values reported in EPA's Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants. These values represented mean percent removals for COD, TOC, and total phenols calculated using performance data from various industries for activated sludge processes.

For priority pollutants found above treatable concentrations, mean percent removals for the activated sludge process were obtained from EPA's Fate of Priority Pollutants in Publicly Owned Treatment Works: Volume I (440/1-82-303); they are presented in Table VIII-4. However, these percent removals are not generally applicable to the relatively low concentrations of priority pollutants characteristic of PM&F process waters. In many cases, application of these percent removals to the average influent concentrations of priority pollutants found in PM&F process waters resulted in effluent concentrations less than the pollutant analytical detection limits.

Activated Carbon Adsorption

Activated carbon removes pollutants from water by the process of adsorption (i.e., the attraction and accumulation of one substance on the surface of another). Activated carbon preferentially adsorbs organic compounds over other compounds and, because of this selectivity, is effective in removing organic pollutants from wastewaters. This sorption process occurs when wastewater is passed over the activated carbon in a packed bed.

The term activated carbon applies to any amorphous form of carbon specially treated to give high adsorption capacities. The adsorption of materials onto the active sites in the activated carbon is a reversible process, allowing the carbon to be regenerated for reuse using either heat and steam or solvents.

Table VIII-4

REMOVAL EFFICIENCIES FOR NONCONVENTIONAL POLLUTANTS AND PRIORITY POLLUTANTS FOR ACTIVATED SLUDGE PROCESSES

Nonconventional Pollutants	Mean Removal Efficiency (%)	Source
COD	63	A
TOC	63	A
Total Phenols	60	A
Priority Pollutants		
65. phenol	99+	B
66. bis(2-ethylhexyl) phthalate	72	B
67. dimethyl phthalate	No Data	
68. di-n-butyl phthalate	51	B
128. zinc	77	B

Sources:

(A) USEPA, Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, July 1980, EPA 600/8-80-042c.

(B) USEPA, Fate of Priority Pollutants in Publicly Owned Treatment Works: Volume I, September 1982, EPA 440/1-82/303.

Carbon adsorption requires preliminary treatment of the wastewater to remove excess suspended solids, oils, and greases. Suspended solids in the influent should be less than 50 mg/l to minimize backwash requirements; oil and grease should be less than 10 mg/l.

Activated carbon is available in both powdered and granular form. An adsorption column packed with granular activated carbon is depicted in Figure VIII-3. Powdered carbon is less expensive per unit weight and may have slightly higher adsorption capacity, but it is more difficult to handle and to regenerate compared with granular activated carbon.

Applications. Carbon adsorption is used primarily to remove gaseous contaminants and condensable vapors from gaseous streams. Carbon adsorption has also been used to remove dissolved organic pollutants in both municipal and industrial wastewaters. It is most effective for removing non-polar organic compounds of low molecular weight and slight solubility in the liquid phase. Many inorganic pollutants, including cyanide, chromium, mercury, and chlorine, are also effectively removed in the activated carbon process.

In general, carbon adsorption is used to treat wastewater when a high quality effluent is desired. It is used for such things as purification in industrial processes, pharmaceutical manufacture, drinking water purification, and secondary and tertiary treatment of industrial and municipal wastewaters. Typical applications include removal of phenol from drinking water supplies, sugar decolorization, and removal of mercury from industrial wastewaters. Potentially, activated carbon adsorption is almost universally applicable because trace organics are found in virtually all industrial wastewaters.

Limitations. Wastewaters treated by carbon adsorption require pretreatment if there are significant levels of suspended solids (greater than 50 mg/l) and oil and grease (greater than 10 mg/l) present. High suspended solids levels tend to quickly clog the carbon bed and result in frequent backwashings. Oil and grease tend to coat the activated carbon, interfering with reactivation and resulting in the loss of activity.

Carbon adsorption is generally least effective for the removal of organic pollutants exhibiting the following characteristics:

- Low molecular weight,
- High solubility in the liquid phase, and
- High polarity.

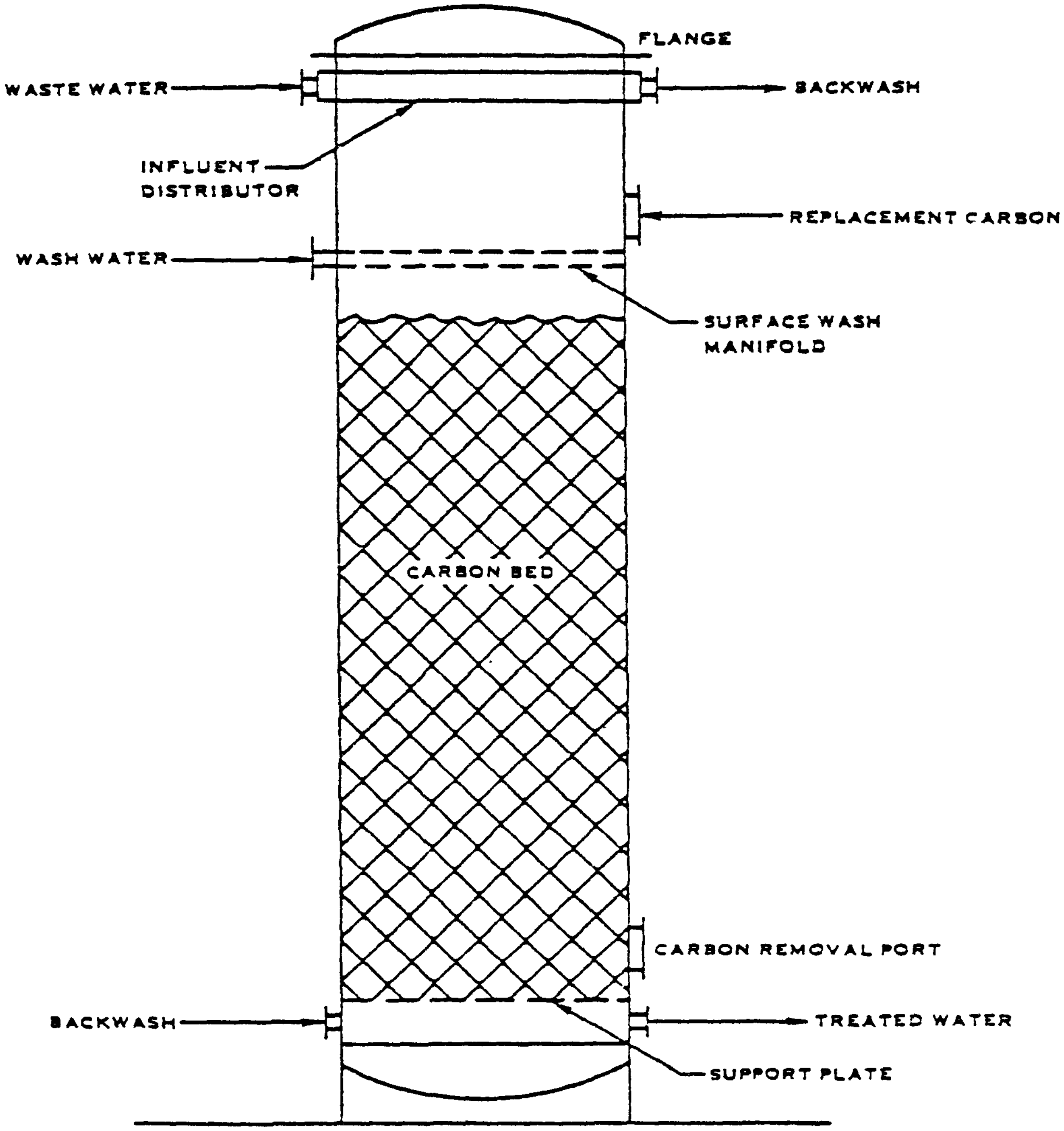


Figure VIII-3

ACTIVATED CARBON ADSORPTION COLUMN

High operating and maintenance costs are associated with carbon adsorption due to the relatively sophisticated operation and materials handling.

Reliability. Treatment of wastewater using activated carbon adsorption is moderately reliable, depending on the design, construction, and manufactured equipment quality. In addition, high levels of suspended solids and oil and grease may affect the performance.

Environmental Impact. Carbon adsorption equipment requires minimal use of land. Spent carbon may present a land disposal problem if regeneration is not feasible. There may also be an air pollution problem encountered with regeneration and production of hydrogen sulfide (leading from favorable conditions found in carbon beds).

Treatability Data. A U.S. EPA study entitled, Treatability of Organic Priority Pollutants - Part C - Their Estimated (30-Day Ave.) Treated Effluent Concentration - A Molecular Engineering Approach, indicates that bis(2-ethylhexyl) phthalate can be theoretically removed to 0.010 mg/l (30-day average) using activated carbon treatment preceded by oil-water separation and filtration. Based on consideration of chemical structure and physical and chemical properties that would affect adsorption, the treatability level for dimethyl phthalate and di-n-butyl phthalate were both estimated to be 0.025 mg/l.

Filtration (Suspended Solids Removal)

Filtration processes are used either to remove suspended solids from the effluent from other treatment technologies or as a pretreatment process. Filtration processes include a wide range of technologies including screens, granular media filters, belt filters, and membrane filters, just to name a few. Figure VIII-4 contains diagrams of different kinds of filters used to remove suspended solids from wastewater.

The performance of filters is based on a physical screening process in which a barrier* prevents the passage of suspended solids. The primary difference between the various types of filters is the degree of permeability of the barrier, ranging from the coarseness of a wire screen to the selectivity of ultrafiltration membranes.

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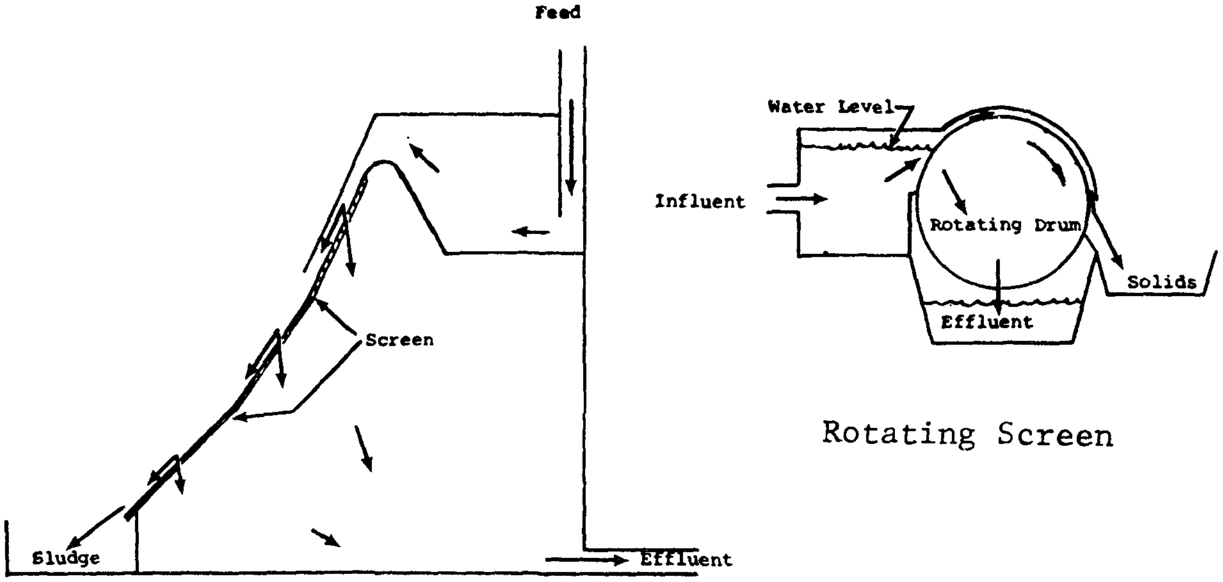
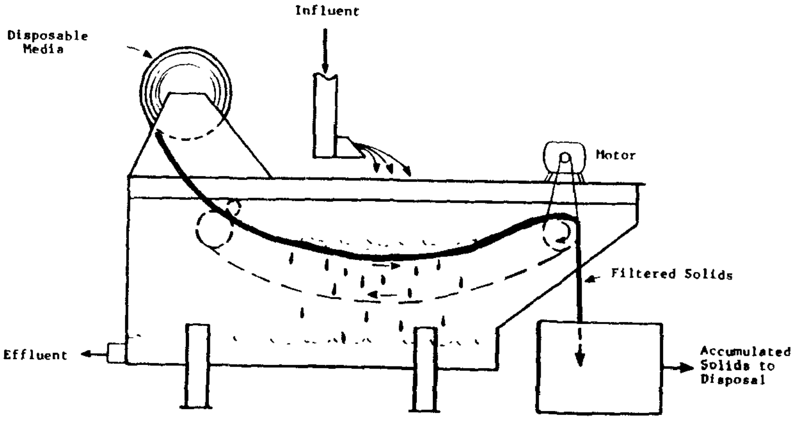
* Although processes based on barriers that have no appreciable thickness in the direction of the liquid flow are typically referred to as straining, these processes are considered as filtration processes in this discussion.

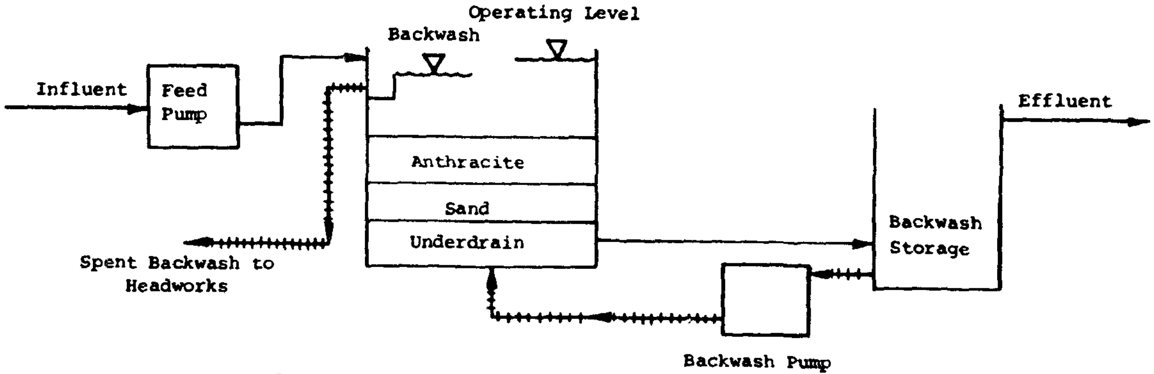


Inclined Screen

Rotating Screen



Paper Filter



Granular Media Filter

Figure VIII-4

FILTRATION TECHNOLOGIES

Filtration processes operate on either a batch or continuous basis, depending on the process. For instance, normal practice is to design certain types of filters (e.g., granular media, cartridge, bag) to operate on a batch basis with entire units taken out of service for cleaning (e.g., backwashing, filter media replacement) according to a schedule or as required. Some granular media filter designs, however, provide more or less continuous cleaning, either externally with media cycled through the bed, or in-place with techniques such as traveling backwash or air pulsing of the bed and air mixing of the liquid above it. Other types of filters, such as inclined screens and paper filters (see Figure VIII-4) usually provide continuous removal of the accumulated solids.

Applications. *Filtration can be used for a wide range of applications* including: (1) the removal of coarse solids by screening in a pretreatment process, (2) the removal of precipitated solids after chemical coagulation of wastewaters, and (3) treatment of settled effluent from other treatment technologies (e.g., the activated sludge process).

Technology Status. Several types of filters are currently used to treat PM&F process waters. Technologies observed during sampling episodes include a bag filter, a paper filter, and a belt filter.

Limitations. Economics of filtration processes can be highly dependent on consistent influent quality and flow variations. The performance of filtration processes may be limited by the filterability (e.g., particle size, floc strength, adhesive properties) of the suspended solids. The filterability may be improved by addition of filter aids such as alum to act as coagulants and to increase the floc strength.

In addition, dissolved solids are generally not removed by filtration processes, with the exception of certain processes based on selective membranes that are capable of removing dissolved solids.

Reliability. Filters typically have a high degree of reliability when properly maintained. Occasional problems may arise when the filters are not properly cleaned.

Environmental Impact. The major environmental impact of filters is the disposal of the suspended solids removed from the wastewater. Solids have to be disposed of properly to avoid negative environmental impacts. Filters usually do not contribute to other types of pollution (e.g., air pollution).

Treatability Data. Filtration is an effective and widely used technology for removing total suspended solids from wastewater. Typical percent removals for suspended solids range from 5 to 95 percent. The median percent removal for suspended solids using granular media filtration is 75 percent based on treatability data reported in Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, (EPA 600/8-80-042C). Mean removal efficiencies ranging from 10 to 25 percent for oil and grease, BOD_5, TOC, COD, and total phenols have also been achieved in filtration units.

Vacuum Filtration (Sludge Dewatering)

In wastewater treatment plants, sludge may be dewatered by vacuum filters that generally use cylindrical drum filters. These filters have a medium that may be cloth made of natural or synthetic fibers or a wire-mesh fabric. The drum is suspended above and dips into a vat of sludge. As the drum rotates slowly, part of its circumference is subject to an internal vacuum that draws sludge to the filter medium. Water is drawn through the porous filter cake to a discharge port, and the dewatered sludge, loosened by compressed air, is scraped from the filter mesh. Because the dewatering of sludge on vacuum filters is relatively expensive per kilogram of water removed, the liquid sludge is frequently thickened prior to processing. A vacuum filter is depicted in Figure VIII-5.

Applications. Vacuum filters are frequently used both in municipal treatment plants and in a wide variety of industries. They are most commonly used in larger facilities, which may have a thickener to double the solids content of sludge before vacuum filtering.

Technology Status. Vacuum filtration is a fully proven technology for sludge dewatering. It is used for sludge dewatering in many industries.

Limitations. Vacuum filters are not practical at low dewatered sludge outputs due to their high initial cost and area requirements. In addition, vacuum filters have high maintenance requirements, which are characteristic of sludge dewatering equipment. Maintenance consists of the cleaning or replacement of the filter media, drainage grids, drainage piping, filter pans, and other parts of the equipment. Experience in a number of vacuum filter plants indicates that maintenance consumes approximately 5 to 15 percent of the time of the maintenance personnel. If carbonate buildup or other problems are unusually severe, maintenance time may be as high as 20 percent. For this reason, one or more spare units should be available. If intermittent operation is used, the filter equipment should be drained

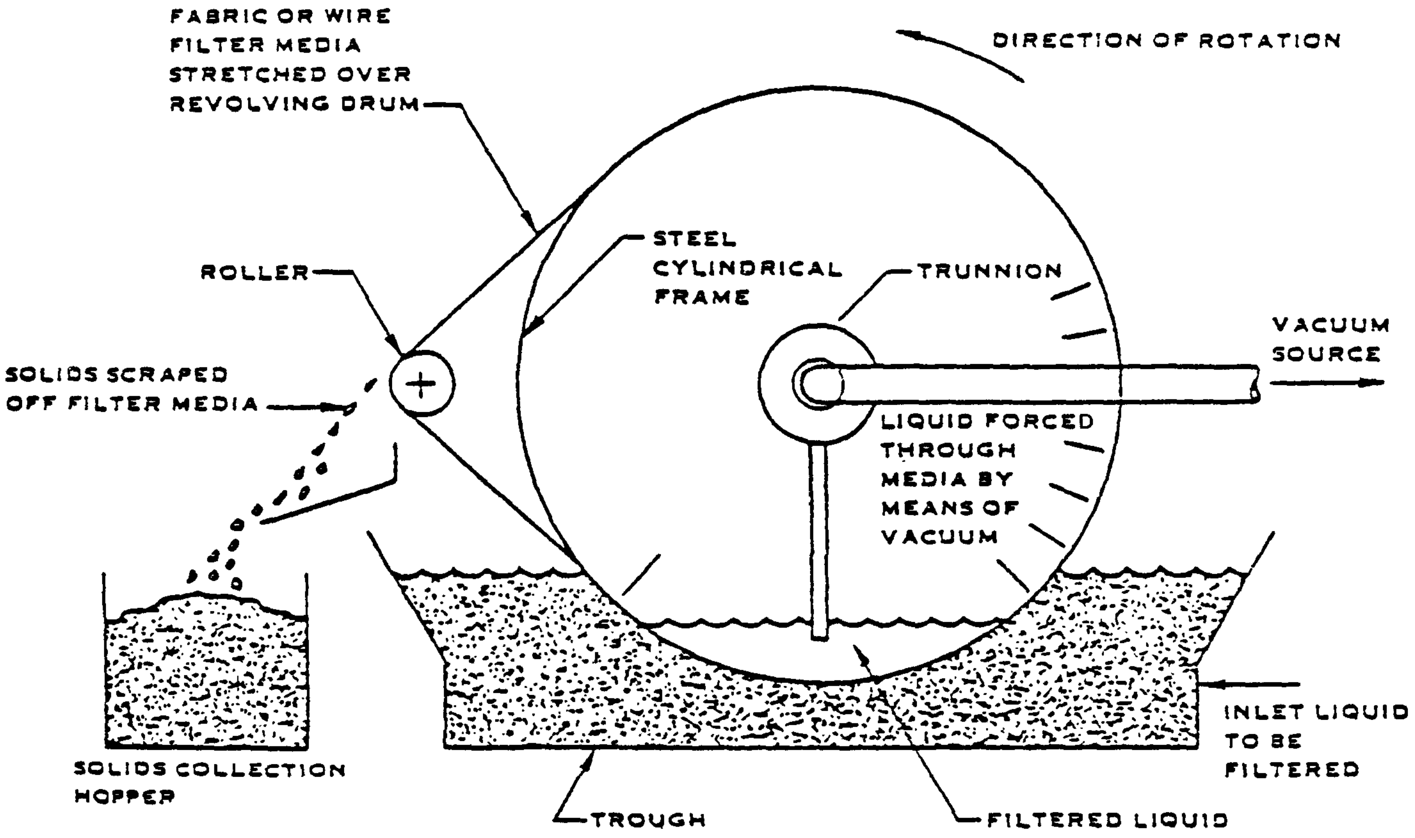


Figure VIII-5

VACUUM FILTER

and washed each time it is taken out of service. An allowance for this wash time must be made in filtering schedules.

Reliability. Vacuum filters have proven reliable at many industrial and municipal treatment facilities. At present, the largest municipal installation that uses vacuum filters is the West Southwest wastewater treatment plant in Chicago, Illinois, where 96 large filters were installed in 1925, functioned approximately 25 years, and then were replaced with larger units. Original vacuum filters at Minneapolis-St. Paul, Minnesota, now have over 28 years of continuous service.

Environmental Impact. The disposal of the solid cake generated from vacuum filtration is the only major environmental impact associated with this technology. The solid waste is usually disposed in a landfill. The characteristics of the dewatered sludge depend primarily on the raw waste characteristics of the treated wastewaters and the particular treatment technology utilized.

SECTION IX

COSTS, ENERGY, AND NON-WATER QUALITY ASPECTS

INTRODUCTION

This section presents the technical data used to develop cost estimates for the treatment technologies described in Section VIII. In addition, the methodology for estimating process-by-process treatment costs is discussed. Cost estimates obtained using information presented in this section are used to evaluate the control and treatment options for each type of effluent limitations guidelines and standards. The cost estimates are also used as the basis to estimate the economic impact of the final regulation on the PM&F category.

This section also discusses the technical basis for the Agency's estimates of (1) the energy used by the treatment technologies, (2) solid waste generation rates, and (3) other non-water quality impacts attributable to implementation of the control and treatment technologies.

COST ESTIMATES FOR TREATMENT TECHNOLOGIES

Sources of Cost Data

Capital and operation and maintenance (O&M) cost data for the treatment technologies were obtained from two sources: (1) equipment manufacturers and (2) the literature. The major sources of capital costs were contacts with equipment vendors. Most of the O&M cost information was obtained from the literature.

Cost Components

Capital costs consist of equipment costs and system costs. Equipment costs include: (1) the purchase price of the manufactured equipment and any accessories; (2) delivery charges, which account for the cost of shipping the purchased equipment a distance of 500 miles; and (3) installation charges, which include charges for labor, excavation, site work, and materials.

System capital costs include engineering, administrative, and legal costs, contingencies, and the contractor's fee. The engineering, administrative, and legal costs are expressed as a percentage of the equipment costs. Contingencies and contractor's fee are expressed as a percentage of the sum of the equipment costs and the engineering, administrative, and legal costs. Equipment costs and system costs are added to obtain the total capital costs. The components of capital costs are listed below:

Item No.	Item	Cost
1	Equipment Costs	Cost of installed equipment
2	Engineering, Administrative, and Legal	10 percent of Item 1
3	Subtotal	Item 1 and Item 2
4	Contingency	15 percent of Item 3
5	Contractor's Fee	10 percent of Item 3
6	Total Capital Cost	Items 3 through 5

Operation and maintenance costs include the following:

1. Raw materials costs - These costs are for chemicals used in the treatment processes, which include caustic, sulfuric acid, corrosion inhibitors, and biocides.

2. Operational labor costs - These costs account for the labor directly associated with operation of the process equipment. Labor requirements are estimated in terms of hours per year. A composite labor rate of $21 per hour was used to convert the annual hours to an annual cost. This composite labor rate includes a base labor rate of $9 per hour for skilled labor, 15 percent of the base labor rate for supervision, and 100 percent of the base rate for plant overhead. Nine dollars per hour is the Bureau of Labor national wage rate for skilled labor.

3. Maintenance and repair costs - These costs account for the labor and materials required for repair and routine maintenance of the equipment. Maintenance and repair costs were assumed to be five percent of the equipment costs based on information from literature sources unless more reliable data were available from vendors.

4. Energy costs - Energy or power costs were calculated based on total nominal horsepower requirements for the equipment (in kw-hrs); an electricity charge of $0.049/kilowatt-hour; and an operating schedule of 24 hours/day, 250 days/year unless specified otherwise. The electricity rate is based on the industrial electricity rate derived from the Department of Energy's Monthly Energy Review (March 1982).

In addition to O&M costs, total annualized costs include monitoring costs. Monitoring refers to periodic sampling and analysis to verify that discharge limitations are being met. Monitoring costs were based on $300 per sample for toxic pollutants (base/neutral extractables analysis via gas chromatography/mass spectrophotometry) and $50 per sample for conventional pollutants (BOD_5, TSS, oil and grease, and pH). These costs were determined from in-house literature and from a vendor quote. The costs per analysis were multiplied by the monitoring frequency (i.e., number of analyses per year) to obtain the annual monitoring costs for a particular plant. Monitoring frequencies and the annual monitoring costs for each plant are discussed in the Economic Impact Analysis of Effluent Limitations and Standards for the Plastics Molding and Forming Industry, EPA 440/2-84-025, December 1984. Amortized costs, which account for depreciation and the cost of financing, are also discussed in the economic analysis document.

Cost Update Factors

All costs were standardized by adjusting them to the first quarter of 1982. The cost indices used for particular components of costs are described below.

Capital Costs - Capital costs were adjusted using the EPA-Sewage Treatment Plant Construction Cost Index. The value of this index for March 1982 is 414.0.

Operation and Maintenance-Labor Costs - The Engineering News-Record Skilled Labor Wage Index was used to adjust the portion of operation and maintenance cost attributable to labor. The March 1982 value is 325.0.

Maintenance and Repair Costs - The producer price index published by the Department of Labor, Bureau of Statistics was used for these costs. The March 1982 value of this index is 276.5.

Raw Materials Costs - The Chemical Engineering Producer Price Index for industrial chemicals was used. This index is published biweekly in Chemical Engineering magazine. The March 1982 value of this index is 362.6.

Cost Data Correlation

To estimate capital and O&M costs for the treatment technologies, cost data from all available sources were plotted on a graph of capital or O&M costs versus a design parameter (usually flow rate). These data were distributed over a range of flows. A single line was fitted to the data points, thus arriving at a cost curve that represented an average of all the costs for either a treatment technology or a component of a treatment technology. Because the cost estimates presented in this section are applicable to treatment technologies used in varying circumstances and geographic locations, the Agency believes this statistical approach best estimates costs of the technologies considered for the final PM&F regulation. For consistency in estimating costs and accuracy in reading the final cost curves, equations were developed to represent the final cost curves. Capital and operation and maintenance cost equations are listed in Table IX-1.

DESIGN DATA FOR TREATMENT TECHNOLOGIES

Design data and cost information are presented for the following treatment and control technologies:

- Flow equalization,
- pH adjustment,
- Settling,
- Package activated sludge plant,
- Activated carbon adsorption,
- Vacuum filters, and
- Contract haul.

Flow Equalization

Flow equalization is accomplished using holding tanks sized for a retention time of eight hours and an excess capacity factor of 20 percent. Equalization costs were based on the following equipment:

1. Equalization tank (eight hour retention time)
2. Influent pump

Cost correlations are available for equalization tanks with a volume between 50 and 500,000 gallons based on vendor quotations. Three separate capital cost equations were developed, one for fiberglass tanks ranging from 50 to 1,000 gallons, another for fiberglass tanks from 1,000 to 24,000 gallons, and a third for 24,000 to 500,000 gallon steel tanks. Capital costs for steel tanks with a volume greater than 24,000 gallons include on-site fabrication, two coats of epoxy, a prime coat, and a finish coat.

O&M costs for tanks include maintenance costs (e.g., for inspection, repair) and labor costs for removing settled solids from the tank. The maintenance costs are estimated as two percent of the capital cost of the tank and the labor requirements for settled solids removal range from 1 to 4.5 hours per week, depending on the tank size.

Table IX-1

CAPITAL AND O&M COST EQUATIONS*

Equipment	Equation	Range of Validity
Activated Carbon Adsorption	$C = 19{,}280$	$CER = 0.374,\ 0 \le Y < 5$
	$C = 16{,}538.7 + 836.368\ Y - 3.40459\ Y^2$	$,\ 5 \le Y \le 75$
	$C = -60{,}242.7 + 1{,}814.97\ Y - 2.79681\ Y^2$	$,\ 75 < Y \le 310$
	$A = 3{,}140$	$,\ 0 \le Y < 1$
	$A = 3{,}112 + 209.26\ Y - 0.3526\ Y^2$	$,\ 1 \le Y < 75$
	$A = 14{,}214 + 14.668\ Y + 0.2696\ Y^2$	$,\ 75 < Y \le 310$
	$C = 19{,}220$	$CER = 3.90,\ 0 \le Y < 1$
	$C = 7{,}847 + 11{,}531.4\ Y - 98.524\ Y^2$	$,\ 1 \le Y < 15$
	$C = 132{,}579 + 1{,}738.07\ Y$	$,\ 15 \le Y \le 150$
	$A = 3{,}400$	$,\ 0 \le Y \le 0.15$
	$A = 2{,}694.5 + 2{,}787.15\ Y - 99.2586\ Y^2$	$,\ 0.15 < Y < 15$
	$A = 5{,}865.5 + 1{,}086.30\ Y$	$,\ 15 \le Y \le 150$
Agitators, C-clamp	$C = 417 + 4{,}030\ (HP)$	$0 < HP \le 0.25$
	$A = 104 + 351\ (HP)$	
	$C = 839.1 + 587.5\ (HP)$	$0.25 < HP \le 0.33$
	$A = 2{,}739.89 + 403.365\ (HP) + 0.7445\ (HP)^2$	
Agitators, Top Entry	$C = 1{,}585.55 + 125.302\ (HP) - 3.27437\ (HP)^2$	$0.33 < HP < 5.0$
	$A = 2{,}739.89 + 403.365\ (HP) + 0.7445\ (HP)^2$	
Contract Haul	$C = 0$	
	$A = 0.40\ (G)(HPY)$	Nonhazardous Wastes
Lime Feed System	$C = \exp[9.13051 + 0.114998\ \ln(F) + 0.18767\ (\ln F)^2]$	$0.01 < F < 10$
	$A = \exp[7.00162 + 0.317975\ \ln F + 0.064336\ (\ln F)^2] + 0.022\ (F)\ (HPY)$	$0.01 < F < 10$
Package Activated Sludge Plant	$C = 2{,}566$	$X < 600$
	$A = 910$	
	$C = 9{,}165$	$600 < X \le 1{,}500$
	$A = 3{,}055$	
	$C = 6{,}500 + 1.71\ X$	$1{,}500 < X \le 5{,}000$
	$A = 1{,}600 + 0.96\ X$	
	$C = \exp[1.57977 + 1.22209\ (\ln X) - 0.028484(\ln X)^2]$	$5{,}000 < X < 100{,}000$
	$A = 4{,}538.99 + 0.0737513\ (X) - 2.77111 \times 10^{-7}\ (X^2)$	
Pumps, Transfer	$C = \exp[6.31076 + 0.228887\ (\ln Y) + 0.0206172\ (\ln Y)^2]$	$3 < Y < 3{,}500$
	$A = \exp[6.67588 + 0.031335\ (\ln Y) + 0.062016\ (\ln Y)^2]$	
Tank, Fiberglass	$C = 3{,}100.44 + 1.19041\ (V) - 1.7288\times10^{-5}\ (V)^2$	$500 < V < 24{,}000$
	$A = 0.02(C) + (21)[4.17 \times 10^{-5}(V) + 0.958]$	Equalization w/settling
	$A = 0.05(C)$	Settling
	$A = 0.02(C)$	Equalization/holding w/o settling

Table IX-1 (Continued)

CAPITAL AND O&M COST EQUATIONS*

Equipment	Equation	Range of Validity
Tank, Steel	$C = 14,759.8 + 0.170817 (V) - 8.44271 \times 10^{-8} (V)^2$	$24,000 < V < 500,000$
	$A = 0.02(C) + (21)[4.17 \times 10^{-5}(V) + 0.958]$	Equalization w/settling
	$A = 0.05(C)$	Settling
	$A = 0.02(C)$	Equalization/holding w/o settling
Vacuum Filter	$C = 71,083.7 + 442.3(SA) - 0.233807(SA)^2$ $A = 17,471.4 + 677.408(SA) - 0.484647(SA)^2$	$9.4 < SA < 750$
Vacuum Filter Housing	$C = (45)[308.253 + 0.836592(SA)]$ $A = (4.96)[308.253 + 0.836592(SA)]$	$9.4 < SA < 750$

A = Operation and maintenance costs (1982 dollars/year)
C = Equipment costs (1982 dollars)
CER = Carbon exhaustion rate (pounds carbon/1,000 gallons)
F = Chemical feed rate (pounds/hour)
G = Sludge disposal rate (gallons/hour)
HP = Power requirement (horsepower)
HPY = Plant operating hours (hours/year)
SA = Filter surface area (square feet)
V = Tank capacity (gallons)
X = Wastewater flow rate (gallons/day)
Y = Wastewater flow rate (gallons/minute)

*Capital cost equations do not include system capital costs (e.g., engineering, contingency, etc.); system costs must be added to the equipment costs (calculated by the above cost equations) to obtain total capital costs. O&M cost equations do not include either monitoring or amortization costs.

Capital costs for pumps are based on vendor quotations for positive displacement pumps with a flow rate between 3 and 27 gpm and centrifugal pumps, which are more economical at higher flow rates, with a flow rate between 27 and 3,500 gpm. Pump O&M costs are based on the following:

- energy costs, which were estimated assuming a pump efficiency of 70 percent; the pump operates for the reported plant operating hours at the nominal capacity (horsepower);
- operating labor costs, which were based on 0.5 hours labor/operating day; and
- maintenance labor costs, which were based on labor requirements ranging from 0.005 to 0.03 hours labor/hour of pump operation (depending on pump capacity).

pH Adjustment

Costs were estimated for adjusting the pH of process waters from pH 5 to pH 7 by the addition of lime. An influent pH of 5 was selected based on a review of pH's from the sampling data. Adjustment of pH occurs in the equalization tank if such a tank is included in the treatment technology. If equalization is not required, pH adjustment occurs in a mix tank with an appropriately sized agitator (based on 0.5 horsepower/1,000 gallons). Costs for the following equipment were included in pH adjustment costs:

1. Mix tank (if equalization tank is not available)
2. Lime feed system
    - storage tank
    - chemical metering pump
    - pipe and valves
    - instrumentation (pH control)
3. Agitator

Capital costs for the mix tank were obtained using the cost equations used to calculate equalization tank costs, as described in the flow equalization discussion in this section. O&M costs for mix tanks are estimated as five percent of the tank capital cost and are for maintenance (e.g., periodic clean out and repair).

A capital cost equation for the lime feed system delivering between 0.01 and 10 lbs lime/hour on a continuous basis was developed from vendor quotations. The capital costs include costs for a pH monitor (flow-through pH analyzer), electrical and instrumentation (e.g., conduit, indicating controller, transducer), piping and valves (e.g., control valve and instrumentation piping), a C-clamp agitator, and a storage tank (sized to hold six percent weight lime slurry for one week).

O&M costs for lime feed systems include energy costs for the agitator, operational labor costs for preparation of chemical stock solutions and calibration of instrumentation, and maintenance costs for the tank and valving.

Lime feed system costs were included in the pH adjustment costs because PM&F process waters generally have to be adjusted from acidic to neutral conditions when pH adjustment is necessary. In cases when an acid feed system was required, the costs of an acid feed system were assumed to be equal to the costs of the lime feed system. This assumption tends to overestimate the pH adjustment costs because an acid feed system requires a less sophisticated metering system than a lime feed system.

Capital and O&M cost equations were developed for three types of agitators: (1) small C-clamp agitators (less than 0.25 hp), (2) medium-sized C-clamp agitators (between 0.25 and 0.33 hp), and (3) top-entry agitators (between 0.33 and 10 hp). The capital costs for agitators, which were based on vendor quotations, include costs of enclosed gear drives, electric motors, and 304 stainless steel shafts and propellers. Agitator O&M costs include energy costs (based on estimated horsepower requirements and 8,760 operating hours per year) and maintenance labor and materials costs (assumed to be five percent of the capital cost).

Settling

Settling tanks are used for gravity separation of suspended solids in wastewater. The settling unit was sized for eight hours of retention time. It was assumed that 82 percent influent solids were removed. This technology includes:

1. Settling tank (eight hour retention time)
2. Pump

Operating and maintenance costs include tank maintenance and settled solids removal (estimated as five percent of capital cost of tank) and O&M costs associated with the pump. Refer to previous discussion on flow equalization for information on tank capital costs and for information on pump capital and O&M costs.

Package Activated Sludge Plant

Package activated sludge plants are usually composed of three tanks (see Figure VIII-2) in which primary settling, activated sludge treatment (extended aeration), and secondary settling occur. The influent enters the first chamber where scum and settleable solids are removed. The second chamber (i.e., the activated sludge unit) is where dissolved pollutants are treated. The final chamber is a settling unit where solids settle by gravity and are either returned to the aeration unit or removed. Package activated sludge plants can be used for flows as low as 600 gallons per day.

Capital costs for a package activated sludge plant included the following:

1. Costs for a nutrient addition system

    - mix tank (retention time of eight hours for PM&F plants operating eight hours per day, 10 minutes for PM&F plants operating 16 to 24 hours per day)
    - agitator (sized based on 0.5 hp/1,000 gallons)
    - chemical feed pumps (2)
    - chemical day tanks (2)

2. Costs for the activated sludge unit

    - primary settling tank
    - aeration chamber
    - secondary settling tank

The following assumptions were made in the design of the package activated sludge plant:

1. Influent process water characteristics:

    BOD_5 = 89 mg/l
    TSS = 714 mg/l
    pH = 5

    Effluent process water characteristics:

    BOD_5 = 22 mg/l
    TSS = 36 mg/l
    pH = 7

2. "Nutrients" are added to the process water to maintain an active microorganism level. Nitrogen is added at a dosage level of 8.9 mg/l (one-tenth of the influent BOD_5 concentration) as ammonia chloride (NH_4Cl).

Phosphorus is fed at a dosage level of 0.89 mg/l (one-hundredth of the influent BOD_5 concentration) as phosphoric acid (H_3PO_4).

3. Nutrients (for maintaining the activated sludge) and lime (for adjusting the pH) are added in a mix tank. Nutrient and lime addition was accomplished on either a batchwise or continuous basis depending on which alternative was less costly. For addition of the chemicals to the high flow rate PM&F processes, a rapid mix tank (10 minute retention time) and continuous feed system was more economical compared with collection of the process water generated during the course of an operating day followed by manual addition of chemicals on a batchwise basis. For low flow rate processes, however, the batch addition scheme was more economical than continuous chemical addition due to the relatively high capital costs of continuous feed systems.

   Because the low flow rate processes were generally associated with plants with fewer number of operating hours, the selection of either batch or continuous chemical addition was based on the plant operating schedule. For plants operating eight hours per day, the mix tank is sized for eight hours of retention (in addition to 20 percent excess capacity) and chemicals are manually added on a batch basis. For plants operating 16 or 24 hours per day, chemicals are added continuously in a rapid mix tank sized for 10 minutes of retention. Costs for lime feed systems are described separately under the pH adjustment discussion in this section.

4. The design for the activated sludge treatment of industrial wastes is based on three-stage treatment, consisting of primary settling, extended aeration, and secondary settling. However, the commercially available package activated sludge units that are applicable to low flow rate processes only provide two-stage treatment (aeration followed by settling). Thus, costs for a primary settling tank sized for a retention time of eight hours were added to the costs of the two-stage package units.

5. The package activated sludge treatment plant design includes flow equalization. Flow equalization is provided in the nutrient addition mix tank for PM&F plants operating eight hours per day and in the primary settling tank for PM&F plants operating either 16 or 24 hours per day. In each case, the tank is sized for an eight hour retention time based on instantaneous influent flow rate.

6. The nominal package activated sludge treatment plant capacity is based on a continuous influent flow rate. The smallest capacity package plant for which costs were obtained is 600 gpd. If the influent flow is greater than 200 gpd but less than 600 gpd, costs for the 600 gpd package plant were assumed. Treatment costs for PM&F processes with a flow rate less than 200 gpd were based on disposal by contract haul, which is more economical than treatment in a package activated sludge plant at these flow rates. It was assumed in these cases that PM&F plants will use the less costly method of complying with the PM&F regulation.

7. Sludge production rates are based on removal of TSS from the influent concentration of 714 mg/l to a concentration of 36 mg/l, plus production of 0.6 lb sludge (dry weight) per lb of BOD_5 removed. Sludge from the settling units consists of two percent solids (TSS = 20,000 mg/l).

8. Costs are provided for sludge dewatering based on vacuum filtration of the sludge to 20 percent solids if such treatment is economical. Sludge is contract hauled without dewatering if the influent flow to the vacuum filter is less than 50 l/hr.

Activated Carbon Adsorption

Activated carbon is used to remove dissolved organic contaminants from wastewaters. As the wastewater is pumped through the carbon column, organic contaminants diffuse into the carbon particles through pores and are adsorbed onto the pore walls. As organic material accumulates, the carbon loses its effectiveness and must be replaced or regenerated periodically.

Two downflow carbon columns in series are usually used.* The leading column loses its effectiveness first because most of the organic pollutants are adsorbed in it. When breakthrough occurs (i.e., when the column effluent concentration of a specified adsorbed pollutant exceeds a specified maximum), the column is taken off-line and regenerated or replaced and the second column becomes the leading column. This configuration, known as a

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* When it was estimated that breakthrough would occur less than once every three months, two columns were not deemed necessary. Thus, costs were based on a single adsorption column in these cases.

"merry-go-round," results in a more consistent effluent quality than a single, larger column or a system where one column is active and one is on standby. During column operation, solids accumulate in the interstices of the carbon bed. To prevent the column from plugging, the bed must be periodically backwashed to remove these solids. Also, a method for replacing spent carbon is required. Either replacement with virgin carbon and disposal of the spent carbon or regeneration of the spent carbon by either off-site or on-site regeneration may be used, depending on the carbon usage rate.

Costs of the following equipment were included in the estimate of capital costs for the activated carbon process:

1. Carbon adsorption unit

   - steel adsorption columns (1 or 2 columns depending on estimated carbon exhaustion rate)
   - hydraulic loading = 2.5 gpm/ft^2
   - initial activated carbon charge
   - pump for transfer between surge tank and column
   - piping
   - instrumentation

2. Backwash facilities

   - backwash hold tank - provides 15 gpm/ft^2 per column for 15 minutes (duration length of backwash)
   - pump

3. Influent surge tank (one hour retention time)

4. Carbon replacement/regeneration facilities* for:

   - replacement (for carbon usage rates less than 1.6 lbs/hr)
   - off-site regeneration (for carbon usage rates between 1.6 and 53 lbs/hr) or
   - on-site regeneration (for carbon usage rates above 53 lbs/hr)

The capital and O&M cost equations for activated carbon adsorption systems include the costs of all four components listed above. As presented in Table IX-1, separate sets of equations were developed for different flow ranges and carbon exhaustion

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*The carbon replacement/regeneration method depends on the carbon usage rate.

rates as a function of influent flow rate. Both the carbon exhaustion rate and the influent flow rate to the activated carbon unit are dependent on whether process waters are recycled. For processes in the questionnaire data base for this regulation that recycled 90 percent or more of the process water, the influent to the activated carbon adsorption unit was assumed to be the discharge (at 90 percent recycle) from the recycle unit. For processes with reported recycle percentages of less than 90 percent, the influent to activated carbon adsorption was assumed to be the process water usage flow (i.e., once-through process data).

The carbon exhaustion rate is dependent on the influent and effluent pollutant concentrations of the process water. Recycled process waters should have higher pollutant concentrations than process waters that are not recycled. Specifically, process water recycled at 90 percent was assumed to have concentrations 10 times higher than non-recycled process waters. Based on this assumption, the following influent concentrations and carbon exhaustion rates were used to size the activated carbon unit:

	Process Water Concentration/Carbon Exhaustion Rate			
	Contact Cooling and Heating Water		Finishing Water	
Pollutant	Non-Recycled	Recycled†	Non-Recycled	Recycled†
Bis(2-ethylhexyl) phthalate (mg/l)	0.235*	2.35	0.479	4.79
Di-n-butyl phthalate (mg/l)	**	**	0.031	0.31
Dimethyl phthalate (mg/l)	**	**	0.034	0.34
Carbon Exhaustion Rate (lb/1,000 gal)	0.374	3.90	0.82	8.6

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† Based on 90 percent recycle.

* Only field sampling concentration data above the treatability level of 0.01 mg/l were used in calculating the flow-weighted pollutant average concentration in the influent to activated carbon adsorption.

** Not found above treatable concentrations in this process water.

The carbon exhaustion rates were based on published isotherm data (Reference: Carbon Adsorption Isotherms for Toxic Organics, EPA 600/8-80-023, April 1980) and an excess capacity factor of 100 percent.

Capital and O&M costs for activated carbon adsorption were based on achieving the following theoretical treatability limits:

Pollutant	Theoretical Treatability Limit (mg/l) for Activated Carbon Adsorption
Bis(2-ethylhexyl) phthalate	0.010
Di-n-butyl phthalate	0.025
Dimethyl phthalate	0.025

Source: Treatability of Organic Priority Pollutants - Part C - Their Estimated (30-Day Ave.) Treated Effluent Concentration - A Molecular Engineering Approach, U.S. EPA (internal report).

Capital costs of activated carbon adsorption units include costs based on vendor quotations for pre-assembled steel adsorption columns having a constant height of 25 feet. The diameter is based on a constant hydraulic loading of 2.5 gpm/ft^2. If the calculated column diameter is greater than the maximum allowable diameter (9 feet), multiple column trains are designed. If the predicted diameter is less than the allowable minimum diameter (2 feet), the minimum diameter is used. O&M costs for the carbon columns specifically include costs of energy for supply and backwash pumping, operating labor costs for monitoring column performance, and routine maintenance (e.g., changing pump seals, etc.). Costs for the initial activated carbon charge are based on the cost of Calgon FILTRASORB 300 and are a function of the amount of carbon purchased. Typical activated carbon costs range from $0.63 to $0.97 (March 1982) per pound.

The capital and O&M costs for the surge and backwash tanks and transfer pumps are based on the corresponding cost equations previously described in the flow equalization discussion, except that O&M tank costs are only two percent of the capital cost because solids removal is not necessary.

Selection of the carbon replacement or regeneration method depends on the carbon usage rate (lbs carbon exhausted/hr), which is a function of the influent flow rate and the carbon exhaustion rate. One of three operating schemes was chosen for each plant. Below a carbon usage rate of 1.6 lbs/hr, replacement of spent carbon with new carbon and contract haul of the spent carbon was most economical. Between 1.6 and 53 lbs/hr, regeneration by off-site regeneration was more economical. On-site regeneration facilities were more economical when the carbon usage rate was above 53 lbs/hr.

For carbon replacement, no capital investment was required. Direct annual costs consist of contract hauling the spent carbon as a hazardous waste and the purchase and installation of new carbon.

For the off-site regeneration option, direct capital costs include costs for hoppers for dewatering and storage of spent carbon. The minimum amount of carbon that can be economically regenerated off-site is 20,000 lbs. In cases where the actual inventory is less than 20,000 lbs, capital costs for purchasing additional carbon to reach the minimum level are included. O&M costs include the charge for regeneration, transportation of the carbon to and from the regeneration facility, and cost for placing carbon into the column.

For an on-site regeneration facility, direct capital costs include costs for a multiple hearth furnace and associated equipment, spent carbon storage, exhaust gas scrubbers, a carbon slurry system, quench tank, housing, and controls and instrumentation. Direct annual costs include operation and maintenance labor for the regeneration facility, maintenance materials, and electricity and natural gas costs for the building, electrical equipment, and furnace. Also included is the cost of replacing carbon lost in the regeneration process (10 percent of the spent carbon passing through the furnace) with virgin carbon.

Vacuum Filters

For the PM&F regulation, sludge from a settling unit and waste activated sludge is dewatered in a vacuum filter to reduce the amount of sludge that requires disposal. Vacuum filters can dewater sludge to a cake with 20 percent solids. Dewatered sludge is disposed of by contract haul and the filtrate is recycled to the treatment process.

The capacity of the vacuum filter, expressed as square feet of filtration area, is based on a yield of 14.6 kg of dry solids/hr per square meter of filter area (3 lbs/hr/ft^2), a solids capture of 95 percent and an excess capacity of 30 percent. The filter operates eight hours per operating day.

Cost data were compiled for vacuum filters ranging in size from 0.9 to 69.7 m^2 (9.4 to 750 ft^2) of filter surface area. Based on the results of a total annualized cost comparison, contract haul of the sludge is more economical when the sludge flow rate is 50 l/hr (0.23 gpm) or less. Therefore, when the sludge flow rate is 50 l/hr or less, costs were estimated to contract haul all of the sludge.

Costs for the vacuum filtration unit include costs for the following equipment:

1. Vacuum filter with precoat but no sludge conditioning
2. *Housing*
3. Influent transfer pump
4. Slurry holding tank
5. Sludge pumps

The vacuum filter is sized based on eight hours of operation per day. The slurry holding tank and pump are excluded when the treatment technology operates eight hours per day or less. In this case, the underflow from the settling unit directly enters the vacuum filter. For cases where the treatment technology is operated for more than eight hours per day, the underflow is stored during vacuum filter non-operating hours. The filter is sized accordingly to filter the stored slurry in an eight hour period each day. The holding tank capacity is based on the difference between the plant and vacuum filter operating hours plus an excess capacity of 20 percent. Cost equations for capital and O&M costs of vacuum filters and a vacuum filter building are presented in Table IX-1.

The following assumptions were made in developing vacuum filter capital and O&M costs:

1. O&M costs associated with the vacuum filter were developed based on continuous operation (24 hrs/day, 365 days/yr). These costs were adjusted for a plant's individual operating schedule by assuming that O&M costs are proportional to the hours the vacuum filter actually operates. Thus, O&M costs were adjusted by the ratio of actual vacuum filter operating hours per year (8 hrs/day x number days/yr) to the number of hours in a year (8,760 hrs/yr).

2. O&M vacuum filter costs include operating and maintenance labor (ranging from 200 to 3,000 hrs/yr as a function of filter size), maintenance materials (generally less than five percent of capital cost), and energy (mainly for the vacuum pumps).

3. Costs for facilities to house a vacuum filter were based on rates of $\$45/ft^2$ and $\$5/ft^2/yr$ for capital and O&M costs, respectively. These rates were applied to

the estimated floor area required by the vacuum filter system to obtain the costs of the facilities that house the vacuum filter. The O&M cost rate accounts for electrical energy requirements of the filter housing. Floor area for the housing is based on equipment dimensions reported in vendor literature, ranging from 300 ft^2 for the minimum size filters (9.4 ft^2) to 1,400 ft^2 for a vacuum filter capacity of 1,320 ft^2.

Contract Haul

Concentrated sludge and certain process waters are removed on a contract basis for off-site disposal. The cost of contract haul depends on the classification of the waste as being either hazardous or nonhazardous. For nonhazardous wastes, a rate of $0.106/liter ($0.40/ gallon) was used to estimate contract hauling costs. The cost for contract hauling hazardous wastes (i.e., spent activated carbon) was developed from a survey of waste disposal services and varies with the amount of waste hauled (e.g., $0.97/gal for disposal at 1 gal/hr of sludge to $0.76/gal for disposal at 100 gal/hr of sludge). No capital costs are associated with contract hauling. The minimum monthly charge for removal is $75.00, based on information from nonhazardous sludge haulers.

PROCESS-BY-PROCESS COST ESTIMATES

Prior to estimating treatment costs for each process in the data base for this regulation, the treatment technologies discussed in Section VIII were used to develop model treatment technology options for the various types of effluent limitations guidelines and standards. These model treatment technology options are discussed in more detail in Sections X, XI, and XII.

For the model treatment technology options considered by the Agency, each type of process water (i.e., each subcategory) requires a different treatment option.* Thus, the Agency assumed that process waters in different subcategories would not be combined for treatment. For this reason, capital and O&M costs for each type of process water were estimated separately (i.e., based on segregated treatment of each process water type), as discussed below.

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* Except for the contact cooling and heating category water and finishing water subcategory, both of which had activated carbon adsorption as the model treatment technology at BAT. However, no plant for which process water treatment costs were estimated had process waters in both of these subcategories.

First, for each of the 112 direct discharging plants in the questionnaire survey data base for which treatment costs were estimated, process waters were segregated by subcategory. Next, for the questionnaire survey plants that had more than one process water in a particular subcategory, the flows for these process waters were combined to obtain subcategory flows for each plant. Thus, it was assumed that process waters would be combined if they required the same treatment. Third, costs of the model treatment technology options were estimated for each subcategory to obtain capital and O&M costs for each of the 112 questionnaire survey plants. These process-by-process cost estimates, which are included in the public record for this regulation, were then used in the economic impact analysis to develop total capital and total annual cost estimates on a plant-by-plant basis. These cost estimates are in the Economic Impact Analysis of Effluent Limitation Guidelines and Standards for the Plastics Molding and Forming Industry, EPA 440/2-84-025, December 1984. A more detailed discussion of this process-by-process cost methodology for a plant is presented below.

Plant-Specific Treatment Technologies

The first step in the development of process-by-process cost estimates was to select the appropriate treatment technologies for a particular plant. This selection is simply based on the particular processes at a plant. For example, if a plant discharges cleaning water and finishing water, costs at BPT for this plant were estimated for the model treatment technology options at BPT for these process waters.

Process Water Characteristics

After establishing the model treatment technology for a given plant, the next step was to define the influent process water characteristics (i.e., flow and pollutant concentrations).

Because the cost equations shown in Table IX-1 are primarily dependent on flow, either directly or indirectly, the influent flow is required as an input parameter. The plant-specific flows for each process water were derived from the questionnaire surveys. For plants practicing recycle of process water, the discharge flow was used as the influent flow to end-of-pipe treatment (see discussion on activated carbon adsorption in this section for exceptions).

Costs for certain treatment technologies are affected by influent concentrations. For example, the carbon exhaustion rate is dependent on the amount of adsorbable organics removed from the influent. Influent concentration dictates how long it takes for carbon to be exhausted. These influent concentrations are also required for the calculation of pollutant removals. In general, the influent concentrations used as input to cost estimation are the flow-weighted average values calculated for each subcategory and presented in Section VI. The exception is explained in the description of the activated carbon adsorption process.

Cost Calculations

Once the model treatment technology option and process water characteristics were defined for each plant in the data base, appropriate cost equations were used to estimate capital and O&M costs of the technology. The capital and O&M cost equations are presented in Table IX-1.

Consideration of Existing Treatment

Cost estimates for the model treatment technology options are for "greenfield" plants and do not account for equipment that plants may already have in-place. To estimate the cost incurred by a plant to meet the effluent limitations guidelines, "credit" should be given for treatment in-place at that plant. The actual capital costs of a model treatment technology option were obtained by subtracting capital costs of treatment in-place (as calculated by the cost equations) from the total "greenfield" costs. O&M costs associated with treatment in-place were not subtracted, however, because these costs recur and must be borne by the facility each year.

COST ESTIMATION EXAMPLE

An example illustrating the cost estimation procedures for a single plant is presented here. Capital and O&M costs at BPT are estimated using the specific cost estimation steps previously described.

Plant Y in the PM&F category is a direct discharger at which injection molding, dip coating, plastic product cleaning, and grinding operations are performed. Both cleaning water and finishing water are discharged from the plant. Therefore, the plant has processes in both the cleaning water subcategory and the finishing water subcategory. The plant also has processes in the contact cooling and heating water subcategory (i.e., injection molding and dip coating), but these processes do not use process water.

Costs for Plant Y at BPT were estimated using the following procedure:

1. Define the treatment technology.

   The only model treatment technology option considered at BPT for the cleaning water subcategory consists of equalization and pH adjustment followed by a package activated sludge plant; for the finishing water subcategory, only settling was considered. Thus, costs for Plant Y are estimated based on the model treatment technologies shown in Figure IX-1.

2. Define the process water characteristics.

   Cleaning water influent characteristics:

   Flow = 170 l/hr (0.75 gpm)
   pH = 5
   BOD_5 = 89 mg/l
   TSS = 714 mg/l
   O&G = 48 mg/l

   Finishing water influent characteristics:

   Flow = 522 l/hr (2.3 gpm)
   TSS = 95 mg/l

   Plant operating hours = 5,914 hrs/yr

3. Cost calculation.

   The specified model treatment technology and raw waste data were used as the basis of the cost calculations. Results of the design and cost calculations are presented below.

   <u>Design Data</u>

   Finishing water (settling):

   Settling tank volume = 1,324 gal
   Contract haul volume (sludge) = 3,125 gal/yr

   Cleaning water (equalization, pH adjustment, and package activated sludge plant):

   Equalization tank volume = 432 gal
   Equalization agitator size = 0.015 hp
   Activated sludge treatment capacity = 864 gal/day

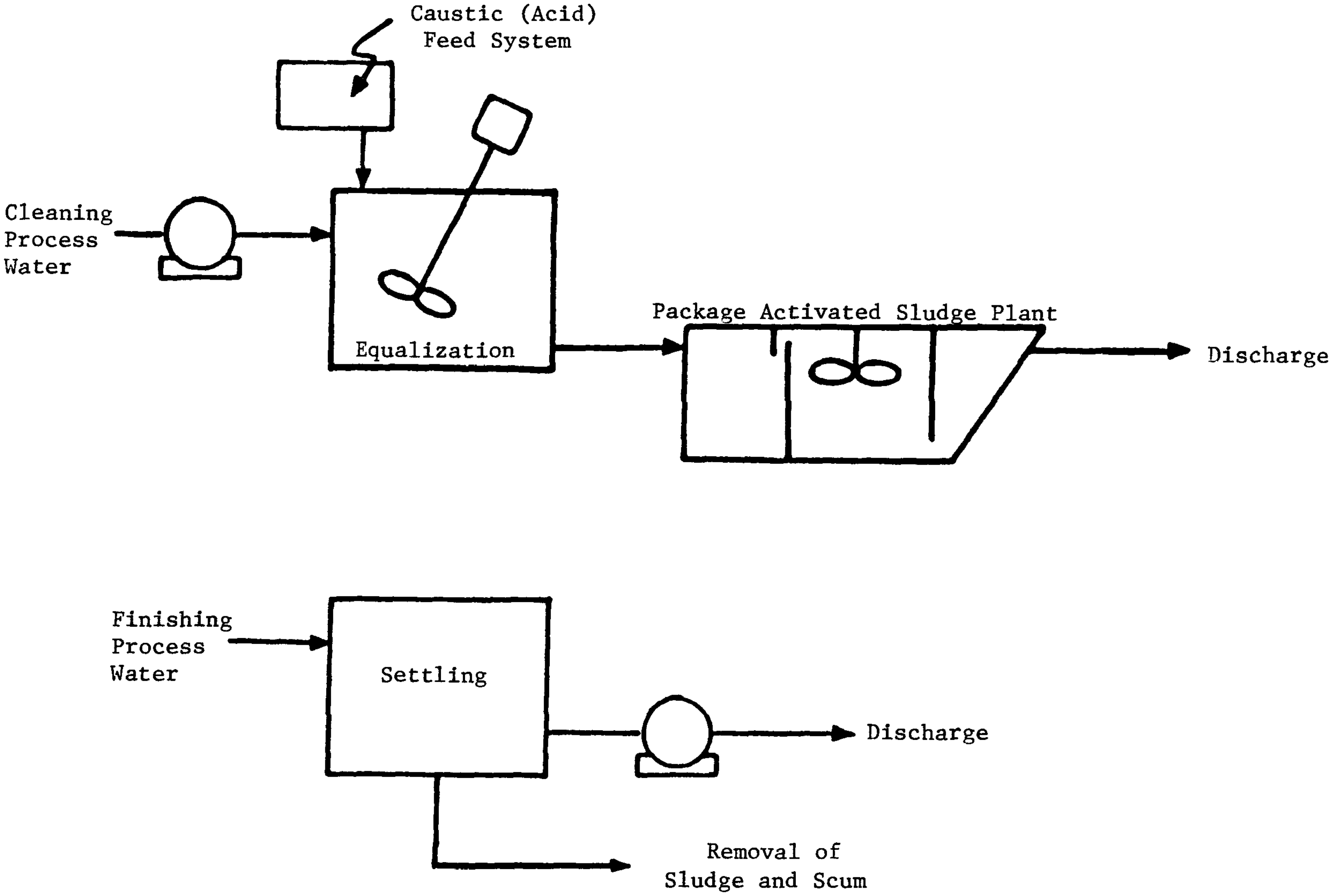

Figure IX-1

COST ESTIMATE EXAMPLE
MODEL TREATMENT TECHNOLOGIES FOR PLANT Y AT BPT

Nutrient Addition:
  Phosphoric acid application rate = 0.0012 lbs/hr
  Ammonium chloride application rate = 0.0128 lbs/hr
Lime application rate = 0.0011 lbs/hr
Contract haul volume (sludge) = 9,830 gal/yr

The estimated costs of these model treatment technologies are presented in Table IX-2.

4. Consideration of treatment in place.

   This step reduces the estimated costs to account for treatment facilities existing at Plant Y. Based on the questionnaire survey response, Plant Y has no treatment in-place. Therefore, the "greenfield costs" shown in Table IX-2 represent the actual estimated costs for Plant Y at BPT.

ESTIMATION OF ENERGY AND NON-WATER QUALITY IMPACTS

The remainder of this section discusses the methodologies used to estimate the energy and non-water quality environmental impacts associated with the regulation. The estimated energy requirements, solid wastes generation, air pollution emissions, and consumptive water losses based on the following methodologies are presented in Sections X through XIII.

Energy

The increases in electrical energy consumption attributable to application of the final PM&F effluent limitations guidelines and standards were estimated to assess the impact of the final PM&F regulation with regard to energy consumption. The estimated electrical energy consumption by the PM&F category (expressed as kw-hr/year) for the selected model treatment technology options is presented in Sections X, XI, XII, and XIII for BPT, BAT, NSPS, and PSES/PSNS, respectively. This part discusses the assumptions and steps used to derive the energy consumption estimates.

Estimation of the net increase in electrical energy consumption at BPT and BAT was accomplished as follows:

1. Energy costs for the treatment technologies were estimated using energy factors. These factors represent the percent of the annual O&M costs attributable to energy for each technology. The energy costs ($/year) were converted to energy requirements (kilowatt-hours/year) using the electricity charge rate of $0.049/kilowatt-hour.

Table IX-2

ESTIMATED CAPITAL AND O&M COSTS FOR PLANT Y AT BPT

Equipment Costs	Estimated Costs ($, 3/82) Capital	 O&M (1)
Settling	$ 5,390	$ 1,120
Equalization	1,980	1,980
Chemical Addition	16,500	4,400
Package Activated Sludge Plant	4,380	4,670
Contract Haul (Sludge)		
Cleaning Water	0	3,700
Finishing Water	0	1,270
Subtotal (Equipment Costs)	$28,250	$17,140
System Costs		
Engineering, Administrative, and Legal	2,825	-
Contingency	4,661	-
Contractor's Fee	3,108	-
Subtotal (System Costs)	10,594	-
Total Costs	$38,844	$17,140

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(1) O&M costs do not include monitoring costs.

2. Energy requirements for plants in each subcategory were estimated by applying the energy factors to the corresponding treatment technology O&M costs. This was done for each of the 112 direct discharging plants in the questionnaire survey for which costs were estimated. Estimated energy requirements for these plants were then totaled by subcategory.

3. The total energy requirement for each PM&F subcategory was estimated by scaling up the subcategory values obtained in the previous step. The scale-up was based on multiplying the subcategory value by the ratio of the estimated total number of wet PM&F plants to the number of wet plants in the PM&F questionnaire survey.

4. The energy usage for the PM&F category was estimated by adding the projected subcategory energy requirements obtained in the previous step.

At BPT, the estimated total energy requirement determined in the last step represents the total energy usage by PM&F plants attributable to the BPT effluent limitations guidelines. The significance of the energy usage attributable to the PM&F regulation is assessed by comparing it to the total current energy usage for the PM&F category, which is estimated to be 1×10^{11} kw-hr/yr. The total energy usage was projected from energy usage information supplied by plants in the questionnaire survey data base.

Air Pollution

The Agency does not expect the treatment of PM&F process waters using the technologies considered as the basis for this final PM&F regulation to create an air pollution problem. Some volatile organic compounds may be emitted to the air from the biological treatment technologies. However, those emissions are not expected to be significant. Accordingly, air pollution emissions attributable to the PM&F regulation were not estimated.

Solid Waste

The increase in solid wastes generated from application of the final effluent limitations guidelines and standards were estimated to assess the potential solid waste disposal impact of the final PM&F regulation. The estimated amounts of solid wastes (expressed as metric tons per year) generated by the PM&F category for the selected model treatment technologies are presented in Sections X, XI, XII, and XIII, for BPT, BAT, NSPS, and PSES/PSNS, respectively. This section discusses the assumptions and steps used to derive the solid wastes generation estimates.

Solid wastes generated by the control and treatment technologies considered for the PM&F category include settled solids from sedimentation processes, treatment process sludges containing biological solids and skimmed oil, and residues from periodic cleaning of tanks and other equipment that may accumulate solids. The annual sludge generation rates resulting from treatment of PM&F process waters were estimated by material balances performed around each unit treatment process. These material balances were based on the average influent pollutant levels and design assumptions for the treatment technologies discussed previously in this section. These sludge generation rates provided the basis for estimating the total amount of solid wastes generated by the PM&F category due to the final PM&F regulation:

1. Solid waste generation rates (liters/year) for treatment of each type of PM&F process water were determined for each of the 112 direct discharging plants included in the questionnaire survey data base that have no treatment in-place.* These generation rates, expressed in liters/year, were converted to metric tons/year by assuming that the solid waste has the density of water. Estimated solid waste generation rates for these plants were totaled by subcategory.

2. The total solid waste generation rates for the PM&F subcategory were estimated by scaling up the subcategory values obtained in the previous step. The scale-up was based on multiplying the subcategory values by the ratio of the estimated total number of wet PM&F plants to the number of wet plants in the PM&F questionnaire survey data base.

3. The solid waste generation rate for the PM&F category was estimated by adding the projected subcategory solid waste generation rates obtained in the previous step.

Characterization of PM&F Solid Wastes. Based on the analyses of process water solid wastes generated during treatment of PM&F process waters, the Agency believes that PM&F process water treatment residuals are not hazardous under Section 3001 of the Resource Conservation and Recovery Act (RCRA). Four solid waste samples were collected at three PM&F plants. The descriptions of

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* Only questionnaire survey plants with no treatment-in-place were included to estimate the additional amount of solid waste generated from implementation of the selected model treatment technologies (i.e., the net increase from the current level of solid waste generation attributable to this regulation).

these samples, including the PM&F subcategory, materials processed, wastewater treatment practices, and physical descriptions of the samples are presented in Table IX-3. These samples were tested for hazardous characteristics based on the extraction procedure (EP) toxicity test (see test method 1310, Test Methods for Evaluating Solid Wastes, SW-846†). This test method is designed to simulate potential leaching of toxic pollutants from the solid waste. Pollutants in solid waste samples analyzed were present in concentrations below the allowable concentration of those pollutants specified in the EP toxicity test procedures. As can be seen by the results, presented in Table IX-4, the pollutant concentrations in all extract samples were well below the pollutant concentrations considered hazardous.

In addition to passing the EP toxicity test, none of the solid wastes are specifically listed as hazardous, pursuant to 40 CFR Part 261.11 (45 FR 33121; May 1980, as amended by 45 FR 76624; November 19, 1980), nor are they likely to exhibit only hazardous waste characteristics (e.g., reactivity, ignitability).

Also, the Agency expects the solid wastes generated by the selected model treatment technologies to exhibit similar nonhazardous characteristics as these sampled wastes. Thus, the Agency believes that the solid wastes generated as a result of these guidelines will not be hazardous. Because the PM&F solid wastes are not believed to be hazardous, no estimates for treatment, storage, or disposal of the solid wastes in accordance with RCRA hazardous waste requirements were made.

Although it is the Agency's view that solid wastes generated as a result of the final PM&F regulation are not expected to be classified as hazardous under the regulations implementing Subtitle C of the Resource Conservation and Recovery Act (RCRA), generators of these wastes must test the waste to determine if they meet any of the characteristics of hazardous waste. See 40 CFR Part 262.11 (45 FR 12732-12733; February 26, 1980). The Agency may also list these sludges as hazardous pursuant to 40 CFR Part 261 (45 FR at 33121; May 19, 1980, as amended at 45 FR 76624; November 19, 1980).

If these wastes are identified as hazardous, they will come within the scope of RCRA's "cradle to grave" hazardous waste management program, requiring regulation from the point of generation to point of final disposition. EPA's generator standards require generators of hazardous wastes to meet containerization, labeling, record keeping, and reporting requirements; if plastics molders or formers dispose of hazardous wastes off-site, they

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†See also 40 CFR 261.24 (45 FR 33084; May 19, 1980).

Table IX-3

DESCRIPTION OF PM&F TREATMENT SYSTEM SOLID WASTE SAMPLES

Plant	Process Code	PM&F Subcategory	Materials Processed	Wastewater Treatment	Solid Sample Description
480*	L-5	finishing water	polyester, rubber	recycle with a DAF clarifier, and belt filtration (dewatering) of solids	dewatered solids sample
10290	N-5	finishing water	polyurethane	filtration	filter cake sample
3625445	R-3	contact cooling and heating water	polyvinyl chloride, polypropylene, polyethylene	recycle with solids skimming, filtration, and water cooling	skimmed solids sample
3625445	R-4	contact cooling and heating water	polyvinyl chloride, polypropylene, polyethylene	recycle with solids skimming, filtration, and water cooling	filter cake sample

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*Plant 480 is not included in the PM&F sampling data base (presented in Section VI), because rubber is also processed at the plant.

Table IX-4

EP TOXICITY TEST RESULTS FOR PM&F WASTEWATER TREATMENT SOLID WASTES

Pollutant	Hazardous Concentrations (ug/l)*	PM&F Solid Waste Concentration by Process Code (ug/l)			
		L-5	N-5	R-3	R-4
Metals (ICAPES)					
silver	5,000	<0.002	0.004	<0.002	<0.002
barium	100,000	0.22	0.96	0.16	0.57
cadmium	1,000	<0.002	<0.002	<0.002	0.27
chromium	5,000	<0.001	<0.001	<0.001	0.094
Metals (AA)					
arsenic	5,000	<0.002	<0.003	<0.002	<0.002
mercury	200	<0.002	<0.0002	<0.0002	<0.0002
lead	5,000	0.008	<0.002	<0.002	<0.002
selenium	1,000	<0.002	<0.003	<0.002	<0.002
Herbicides					
2,4-D	10,000	<0.1	<0.1	<0.15	<0.1
2,4,5-TP (silvex)	1,000	**	<0.01	<0.01	<0.1
Pesticides					
lindane	400	<0.1	<0.1	<4	<4
endrin	20	<0.1	<0.1	<0.2	<0.2
methoxychlor	10,000	<1	<1	<100	<100
toxaphene	500	<1	<1	<5	<5

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*These concentrations are listed in CFR Title 40, Part 261.

**Presence of large interference peak precludes detection.

would have to prepare a manifest that tracks the movement of the wastes from the generator's premises to an appropriate off-site treatment, storage, or disposal facility. See 40 CFR Part 262.20 (45 FR 33142; May 19, 1980, as amended at 45 FR 86973; December 31, 1980). The transporter regulations require transporters of hazardous wastes to comply with the manifest system to ensure that the wastes are delivered to a permitted facility. See 40 CFR Part 263.20 (45 FR 33142; May 19, 1980, as amended at 45 FR 86973; December 31, 1980). Finally, RCRA regulations establish standards for hazardous waste treatment, storage, and disposal facilities allowed to receive such wastes. See 40 CFR Part 264 (46 FR 2802; January 12, 1981, 45 FR 32274; July 26, 1982).

Even if these wastes are not identified as hazardous, they still must be disposed in a manner that will not violate the open dumping prohibition of §4005 of RCRA. The Agency has calculated as part of the costs for wastewater treatment the cost of hauling and disposing of these wastes in accordance with this requirement.

Consumptive Water Loss

Where evaporative cooling mechanisms are used for recycling water, water loss may result and contribute to water scarcity problems - a primary concern in arid and semi-arid regions. Because recycle of PM&F process waters is not a treatment and control technology used in development of the PM&F regulation, consumptive water loss associated with the regulation does not represent a potential environmental impact. Therefore, consumptive water losses were not estimated.

SECTION X

BEST PRACTICABLE CONTROL TECHNOLOGY CURRENTLY AVAILABLE

BACKGROUND

This section defines the effluent characteristics attainable through the application of best practicable control technology currently available (BPT), as required by Section 301(b)(1)(A) of the Act. Effluent limitations guidelines for the PM&F category based on BPT reflect either the existing treatment performance by plants of various sizes, ages, and manufacturing processes within the plastics molding and forming category or the performance of a treatment technology transferred from the organic chemicals, plastics, and synthetic fibers category.

The factors considered in identifying BPT include the total cost of applying the technology in relation to the effluent reduction benefits derived, the age of equipment and facilities involved, the manufacturing processes employed, energy, non-water quality environmental impacts, and other factors EPA considers appropriate. In general, the BPT level represents the average of the best existing performance of plants of various ages, sizes, processes, or other common characteristics. Where existing performance is uniformly inadequate, BPT may be transferred from a different subcategory or category. Limitations based on transfer of a technology have to be supported by a conclusion that the technology will be capable of achieving the prescribed effluent limitations guidelines (see Tanners' Council of America v. Train, 540 F.2d 1188 (4th Cir. 1976)). BPT focuses on end-of-pipe treatment rather than process changes or internal controls, except where such practices are common to the industry.

The cost-benefit inquiry for BPT is a limited balancing, committed to EPA's discretion, that does not require the Agency to quantify benefits in monetary terms. See American Iron and Steel Institute v. EPA, 526 F.2d 1027 (3rd Cir. 1975). In balancing costs in relation to effluent reduction benefits, EPA considers the volume and nature of existing discharges, the volume and nature of discharges expected after application of BPT, the general environmental effects of the pollutants, and the cost and economic impacts of the required level of pollution control. The Act does not require or permit consideration of water quality problems attributable to particular point sources or industries, or water quality improvements in particular water bodies. Accordingly, water quality considerations were not the basis for the final BPT effluent limitations guidelines for the PM&F category. See Weyerhaeuser Company v. Costle, 590 F.2d 1011 (D.C. Cir. 1978).

TECHNICAL APPROACH

The plastics molding and forming category was studied to identify the manufacturing processes used and to determine the characteristics of PM&F process waters. Results of that study were used to subcategorize the PM&F category, to determine the appropriate type of effluent limitations guidelines for the PM&F category, and to select model BPT treatment technologies.

Subcategorization. The factors reviewed to determine the subcategorization scheme for this category are:

1. Raw materials,
2. Production processes,
3. Products,
4. Size and age of plants,
5. Wastewater characteristics,
6. Water use, and
7. Geographic location of plants.

At proposal, the PM&F category was divided into two subcategories: (1) contact cooling and heating water subcategory and (2) cleaning and finishing water subcategory. In response to comments, the Agency collected additional sampling data for finishing waters subsequent to proposal. Using those data and data from previous sampling episodes, EPA determined that cleaning waters and finishing waters have different pollutant characteristics. Cleaning waters have treatable concentrations of BOD_5, O&G, TSS, COD, TOC, total phenols, phenol, and zinc, whereas finishing waters only have treatable concentrations of TSS and three phthalates. Because of these different characteristics, cleaning water processes and finishing water processes were placed in separate subcategories for the final rule.

For the purpose of the final regulation, the PM&F category is divided into three subcategories: (1) contact cooling and heating water subcategory, (2) cleaning water subcategory, and (3) finishing water subcategory. Additional information on this subcategorization scheme is presented in Section V of this document.

In making technical assessments of data, reviewing manufacturing processes, and assessing treatment technology options, both indirect and direct dischargers were considered as a single group for each subcategory. An examination of PM&F plants and processes did not indicate any process differences based on the type of discharge, whether it be direct or indirect. Therefore, data from both direct and indirect dischargers were used to make technical assessments for BPT for each subcategory.

Type of Effluent Limitations Guidelines and Standards. The Agency proposed production-based effluent limitations guidelines and standards for the PM&F category. They were calculated by multiplying the effluent pollutant concentration by a regulatory production-normalized flow (i.e., liters discharged per 1,000 kilograms of plastic product produced). After further study and evaluation, the Agency has determined that production-based effluent limitations guidelines and standards are not appropriate for the PM&F category. EPA could not establish production normalized flows for each subcategory primarily because of the wide variation in water use by PM&F processes. This variation is caused by the many different types of materials processed and by product quality requirements. The amount of water required depends on the type of material processed and the desired product quality. In some cases, many different materials are processed in the same process at the same plant thus making the establishment of a regulatory production normalized flow infeasible. This is particularly true for "custom" plastics molders and formers.

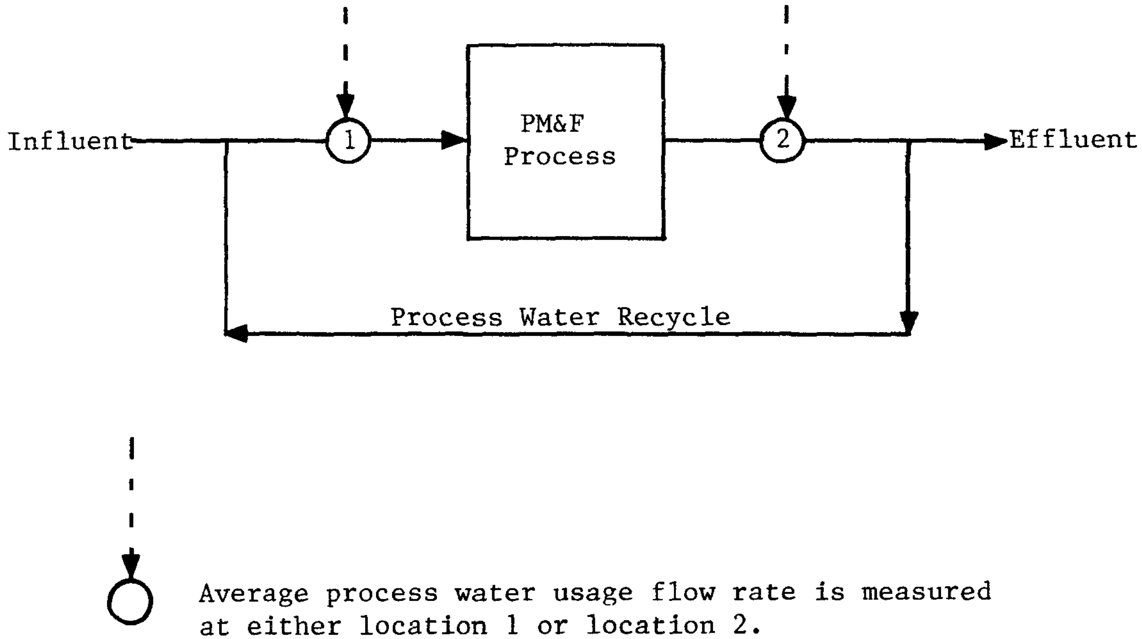
EPA considered subdividing the PM&F category based on either the plastic material processed or on product quality to account for the variability in water use caused by the different plastic materials thus allowing the establishment of subcategory production normalized flows. However, such a subcategorization scheme would be extremely complex because of the large number of plastic materials and the combination of plastic materials that are used. Such an approach is also not feasible because of the "custom" PM&F plants discussed above.

The effluent limitations guidelines and standards in this final rule for all three subcategories are mass-based. They are calculated using the following equation:

Effluent Mass = (Concentration) (Average Process Water Usage Flow Rate)

The pollutant concentrations are established based on the performance of the selected treatment technology. The average process water usage flow rate is obtained from the permittee for each process to be regulated. It is defined as the volume of process water (liters) used per year by a process divided by the number of days per year the process operates. The volume of water used is the water that flows through a process and comes in contact with the plastic product over a period of one year. Figure X-1 indicates where the average process water usage flow rate is measured.

A one year period was selected to determine the volume of water used by a process to account for any variation in water use because of seasonal operations. It also accounts for variation in the number of days that the plant operates during a year.



Average process water usage flow rate is measured at either location 1 or location 2.

Figure X-1

AVERAGE PROCESS WATER USAGE FLOW RATE

If a plant has more than one PM&F process in the same subcategory, the average process water usage flow rate for those processes is the sum of the average process water usage flow rate for each process. This sum is used to calculate the pollutant mass for the PM&F processes at a plant in the same subcategory.

Using the above equation to calculate effluent pollutant mass ensures that processes with the same average process water usage flow rate, whether water is recycled or used on a once-through basis, have the same mass limitations. If only concentration limitations were employed, processes that recycle process water may be penalized because their discharges would likely have higher concentrations than the concentrations in discharges from processes that use once-through process water.

Additional Steps. Once the subcategorization scheme and the type of effluent limitations guidelines and standards were established, the following steps were taken as part of the technical study to develop final BPT effluent limitations guidelines:

1. Select pollutants that would be controlled.
2. Select a treatment technology on which to base the BPT effluent limitations guidelines.
3. Establish effluent concentration values for the controlled pollutants achievable by the selected BPT.
4. Establish maximum concentration for any one day and maximum for monthly average concentration based on the effluent concentrations achievable by the selected BPT technology.

BPT Model Treatment Technologies

The BPT model treatment technologies were developed from the control and treatment technologies described in Section VIII. Factors considered in developing the model BPT treatment technologies included the characteristics of PM&F process waters, PM&F process water flow rates, and treatment technologies at PM&F plants.

The BPT options for each subcategory were selected from the group of model treatment technologies described below.

Technology 1: Settling and pH Adjustment (if necessary)

Settling is effective in removing insoluble pollutants such as total suspended solids (TSS) and oil and grease (O&G). However, dissolved pollutants (e.g., BOD_5) are not removed by this technology. Settling is a widely demonstrated technology used to treat PM&F process waters. If necessary, pH adjustment is used to maintain the pH of the effluent within prescribed limits.

Technology 2: Equalization, pH Adjustment (if necessary), and Package Activated Sludge Plant

This treatment technology consists of flow equalization and pH adjustment (as needed) followed by treatment in a package activated sludge plant. Flow equalization provides an influent wastewater with a relatively constant flow rate and composition. If necessary, pH adjustment is included to maintain the pH of the effluent within prescribed limits. The activated sludge technology treats dissolved and biodegradable organic compounds in the process waters. In addition, insoluble pollutants such as TSS and O&G are removed in the liquid/solids separation processes in a package activated sludge plant.

Activated sludge treatment is used only at integrated facilities where PM&F process waters and other wastewaters are combined for treatment. However, the activated sludge technology is widely demonstrated in other categories for the treatment of wastewaters with characteristics similar to the characteristics of PM&F process waters. In particular, it has been demonstrated in the treatment of wastewater generated by processes in the plastics only subcategory of the organic chemicals, plastics, and synthetic fibers category.

Technology 3: Zero Discharge by Contract Haul of the Discharge from a Recycle Unit

Disposal of the discharge from a recycle unit by contract haul eliminates the discharge of pollutants. Two plants in the PM&F questionnaire data base currently contract haul cleaning water.

At proposal, recycle was included as part of several treatment technologies. Recycle reduces the amount of process water that has to be treated and also may improve the performance of the treatment technology because technologies usually perform better with a concentrated wastewater.

The Agency considered recycle with the technologies for the final PM&F regulation, but rejected it because of the variation in water use by PM&F processes. That variation is caused by the different types of plastic materials produced and by product quality requirements. For example, a "custom" plastics molder and former may produce a polyurethane product and a polyvinyl chloride product in the same process. Those products may have different quality requirements that influence the amount of water needed to produce each product. The amount of water that could be recycled also depends on the quality requirements of the plastic product.

As mentioned above in the discussion on production-normalized flows, EPA considered subdividing the PM&F category based on either the plastic material processed or on product quality to account for the variability in water use. This approach was rejected because of its complexity.

Because of the variation in water use by PM&F processes, the Agency was unable to establish a subcategory recycle percentage that all processes in a subcategory can meet. For this reason, recycle was rejected for the final PM&F regulation. Technology 3 was not considered further for this regulation because it was considered feasible only in conjunction with extensive recycle. The Agency does not believe it is feasible to contract haul all of the process water instead of just the discharge from the recycle unit.

BPT OPTIONS

The BPT options were selected from the model treatment technologies described above. The applicability of a model treatment technology to a particular subcategory is based on the characteristics of process waters generated by processes in the subcategory. The rationale for selection or rejection of each BPT option is discussed below. In addition, the estimated costs, pollutant removals, energy requirements, and solid waste generation rates associated with the selected option for each subcategory are presented.

Contact Cooling and Heating Water Subcategory

There were no conventional pollutants found in treatable concentrations in the contact cooling and heating water subcategory (see Table VI-19). The only pollutant found in treatable concentrations in contact coolng and heating waters was bis(2-ethylhexyl) phthalate. Therefore, the Agency did not consider any of the model treatment technologies as BPT options.

At proposal, Technology 1 (settling and pH adjustment) and Technology 2 (equalization, pH adjustment, and activated sludge treatment) were considered as BPT options for this subcategory. Technology 1 was rejected for the final rule because the suspended solids concentration in the contact cooling and heating water is very low. Technology 2 was rejected for the final rule because the BOD_5 concentration in contact cooling and heating water is not high enough to support the activated sludge treatment process.

Contract haul was also included as part of a BPT option considered at proposal. That option included recycle to reduce the amount of process water that had to be hauled. As discussed earlier in this section, the Agency has determined that recycle is no longer appropriate as part of the technology basis for the effluent limitations guidelines and standards for the PM&F category. EPA believes that contract haul of contact cooling and heating water is not a feasible option unless the amount of process water that has to be hauled is reduced through the use of a recycle unit. For this reason, contract haul of process water was not considered as a BPT option for the final regulation for this subcategory.

The Agency considered one BPT option as the basis for the BPT effluent limitations guidelines for this subcategory. It is:

Option 1: Good Housekeeping Practices

The Agency found during the sampling episodes for this regulation that good housekeeping practices are employed with contact cooling and heating processes. Lubricating oils and other pollutants are kept out of the contact cooling and heating water and the processes that use that type of water are usually used only to cool or heat plastic materials. For example, in an extrusion process, the molten plastic material is forced through a dye and the resulting product is drawn through a water bath for rapid cooling. The water bath is used only to cool the plastic product. Consequently, the only opportunity for pollutants to get into the process water occurs when the plastic material is cooled.

In this option, the concentration values used to calculate the final BPT effluent limitations guidelines are based on a statistical evaluation of the pollutant concentrations in the raw process waters. This option ensures the continuation of the good housekeeping practices by limiting the pollutant concentrations to those that are currently being discharged.

Option Selected. The Agency is promulgating Option 1 as the model technology basis for BPT effluent limitations guidelines for the contact cooling and heating water subcategory. The final BPT effluent limitations guidelines control BOD_5, O&G, TSS, and pH. Appendix D describes how the concentration values promulgated in the final regulation for this subcategory were calculated.

The concentration values in the final rule are multiplied by the average process water usage flow rate for a contact cooling and heating water process to obtain the mass of pollutants that can be discharged. The average process water usage flow rate, discussed in the previous section, is obtained from the permittee.

There are only minimal pollutant removals for the selected option and only minimal costs because this option is based on current practices. The Agency has determined that the effluent reduction benefits associated with compliance with the BPT effluent limitations guidelines justify the costs.

The Agency has concluded that there will be only a minimal increase in production of solid wastes caused by the implementation of the BPT effluent limitations guidelines for this subcategory. There is also little or no increase in electrical energy usage.

Cleaning Water Subcategory

The conventional pollutants found in treatable concentrations in cleaning waters are TSS, O&G, BOD_5, and pH. Therefore, the Agency only considered model treatment technologies that remove these pollutants as BPT options for this subcategory.

At proposal, EPA considered BPT options based on recycle and contract haul of the discharge from the recycle unit and recycle with treatment of the discharge from the recycle unit in a package activated sludge plant. As discussed earlier, the Agency has determined that recycle is no longer an appropriate technology basis for the final effluent limitations guidelines for the PM&F category. Contract haul of cleaning waters was rejected as a BPT option for this subcategory for the same reasons it was rejected for the contact cooling and heating water subcategory.

The Agency identified two options as the basis for the final BPT effluent limitations guidelines for the cleaning water subcategory. These options are:

Option 1: Settling and pH Adjustment (as needed)

The technology for this option consists of a sedimentation tank in which the velocity of the process water is reduced so that solid material can settle by gravitational force. The pH of the process water is adjusted, if necessary. For the final PM&F regulation, this option was rejected early because it does not treat the dissolved pollutants (i.e., BOD_5) found in treatable concentrations in cleaning waters.

Option 2: Equalization, pH Adjustment (as needed), and Package Activated Sludge Plant

The technology for this option consists of an equalization tank followed by a package activated sludge plant with pH adjustment (if necessary). This technology treats the BOD_5, O&G, and TSS in cleaning waters (see Table VI-19). It also treats the nonconventional and priority toxic pollutants found in treatable concentrations in cleaning water. The Option 2 technology is represented in Figure X-2.

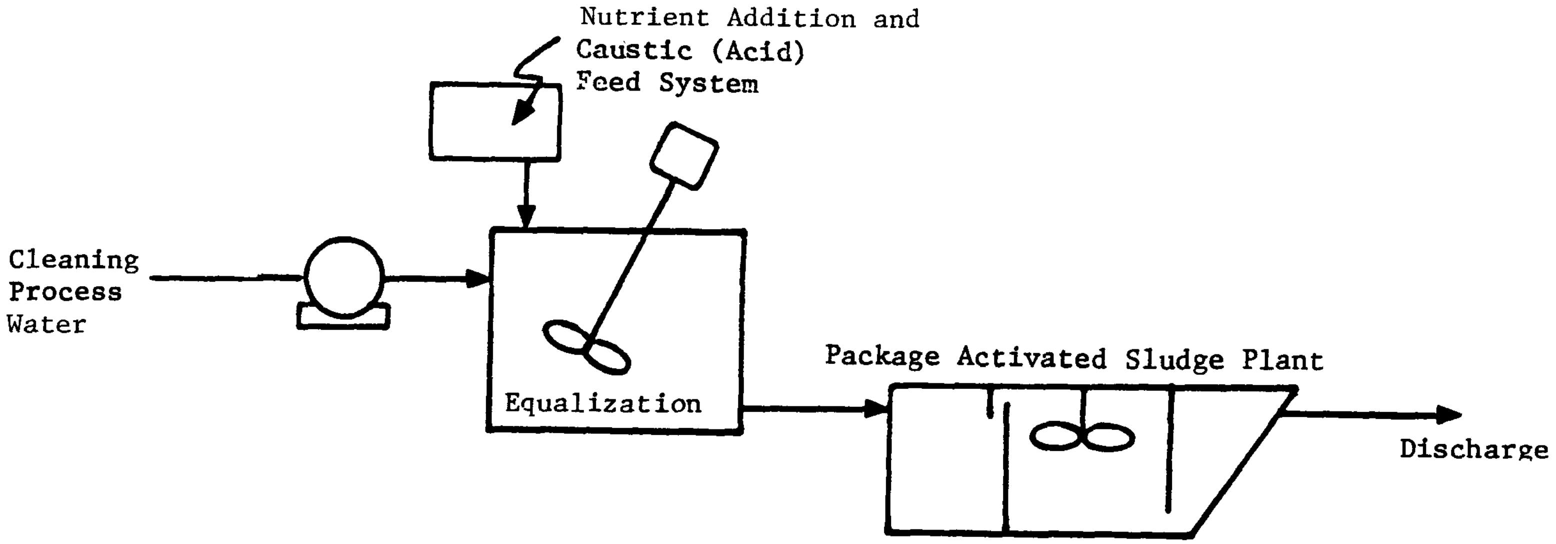


Figure X-2

SCHEMATIC OF BPT OPTION 2 - CLEANING WATER SUBCATEGORY

The estimated amounts of pollutants remaining after Option 2 are:

Type of Pollutant	Discharged in Raw Water - Direct Dischargers (kg/yr)	Remaining After Option 2 (kg/yr)
Conventional	238,800	21,300
Nonconventional	216,400	79,800
Priority Toxic	237	82

The methodology used to calculate the pollutant removals is presented in Appendix C.

The estimated investment cost and annual pollution control costs for Option 2 are:

	Cost ($ Million, 1984 Dollars) Option 2
Investment Cost	$6.9
Annual Pollution Control Costs*	4.4

*Includes depreciation and interest.

Detailed information on these costs is presented in Economic Impact Analysis of Final Effluent Limitations and Standards for the Plastics Molding and Forming Industry, EPA 440/2-84-025, December 1984.

Option Selected. The Agency is promulgating Option 2 as the technology basis for the BPT effluent limitations guidelines for this subcategory.

Data available to the Agency indicate that where cleaning waters are treated by biological treatment processes, wastewaters from other manufacturing processes are commingled with the cleaning process waters. Therefore, data are not available on the application of biological treatment to cleaning waters only. As at proposal, EPA found that treatment at plants that treat cleaning waters separately is uniformly inadequate because those plants indicated on their questionnaires that they use only sedimentation and oil skimming to treat cleaning water. These technologies do not remove the dissolved pollutants in the cleaning waters. Thus, the Agency has determined that the PM&F industry has uniformly inadequate treatment of process water discharges resulting from the cleaning processes. Accordingly, the Agency has relied on the transfer of biological treatment (i.e., the activated sludge process) from the organic chemicals, plastics, and synthetic fibers category to establish BPT effluent limitations guidelines for this subcategory. The Agency believes that such a transfer is appropriate because of the similarities between the cleaning process waters and the organic chemicals, plastics, and synthetic fibers category wastewaters.

At proposal, to evaluate the two types of wastewaters, the Agency conducted a statistical comparison of the raw wastewater conventional pollutant concentrations in PM&F process waters and the concentrations of those pollutants in raw wastewaters discharged at plants in the plastics only subcategory in the organic chemicals, plastics, and synthetic fibers category. This comparison was revised to support the final PM&F rule. After reviewing the results of the updated analysis, the Agency has concluded that the raw wastewater conventional pollutant concentrations in PM&F cleaning waters are neither significantly greater nor more variable than the raw process water conventional pollutant concentrations in wastewaters discharged by plants in the plastics only subcategory. This conclusion supports the Agency's determination that the activated sludge treatment technology can be transferred from the organic chemicals, plastics, and synthetic fibers (OCPSF) category and that the technology will treat PM&F cleaning waters to the same level that it treats OCPSF wastewaters.

Performance data for the activated sludge process were also transferred from the organic chemicals, plastics, and synthetic fibers category to the cleaning water subcategory. The transferred concentration values in the final PM&F regulation are the same as the concentration values used to calculate the production-based effluent limitations guidelines for the cleaning and finishing water subcategory at proposal. Maximum for any one day and maximum for monthly average concentrations for BOD_5, O&G, and TSS are established by the final PM&F rule. The transfer of both the activated sludge process and performance data for that process are discussed in more detail in Appendix D. The Agency believes the toxic pollutants found in treatable concentrations in cleaning waters are effectively controlled when the effluent limitations guidelines for the conventional pollutants are met.

The Agency estimates that the BPT effluent limitations guidelines for this subcategory will result in the removal of 217,500 kg/yr of conventional pollutants, 136,600 kg/yr of nonconventional pollutants, and 155 kg/yr of priority toxic pollutants from the process waters. The estimated total investment costs and total annual costs for the BPT effluent limitations guidelines are $6.9 million and $4.4 million, respectively, in 1984 dollars. The Agency has determined that the costs are justified by the effluent reduction benefits.

The Agency estimates that the implementation of the selected BPT option for the cleaning water subcategory will result in a net increase in electrical energy consumption of 4.1 million kilowatt-hours per year (kw-hr/yr) and a net increase in the solid waste generation rate of 7,300 metric tons per year (kkg/yr). The methodologies used to derive these estimates are discussed in Section IX. The net increase in electrical energy consumption is significantly less than one percent of the estimated total current energy usage for the PM&F category. The Agency has concluded that the increased production of solid wastes (which are not believed to be hazardous) associated with the selected option for this subcategory will not cause any significant negative environmental impacts. Therefore, there are no non-water quality impacts of the BPT effluent limitations guidelines for this subcategory.

Finishing Water Subcategory

The only conventional pollutant found in treatable concentrations in finishing waters was TSS. Therefore, the Agency considered only model treatment technologies that remove that pollutant as BPT options in this subcategory.

For the proposed PM&F regulation, cleaning water processes and finishing water processes were in the same subcategory. Subsequent to proposal, the Agency established separate subcategories for cleaning water processes and for finishing water processes. The activated sludge process on which the proposed BPT effluent limitations guidelines for the cleaning and finishing water subcategory were based was not considered for the final BPT effluent limitations guidelines for the finishing water subcategory because the BOD_5 concentration (i.e., 6 mg/l) in finishing waters is not high enough to support operation of a biological process. The Agency identified one BPT option for the final regulation to treat the pollutants found in treatable concentrations in finishing waters (see Tables VII-2, VII-3, and VII-10).

Option 1: Settling and pH Adjustment (as needed)

The technology for this option consists of a settling tank in which the velocity of the process water is reduced so that solid material can settle by gravitational force. The pH of the process water is adjusted if necessary. This technology removes TSS. Refer to Figure X-3 for a schematic of the Option 1 technology.

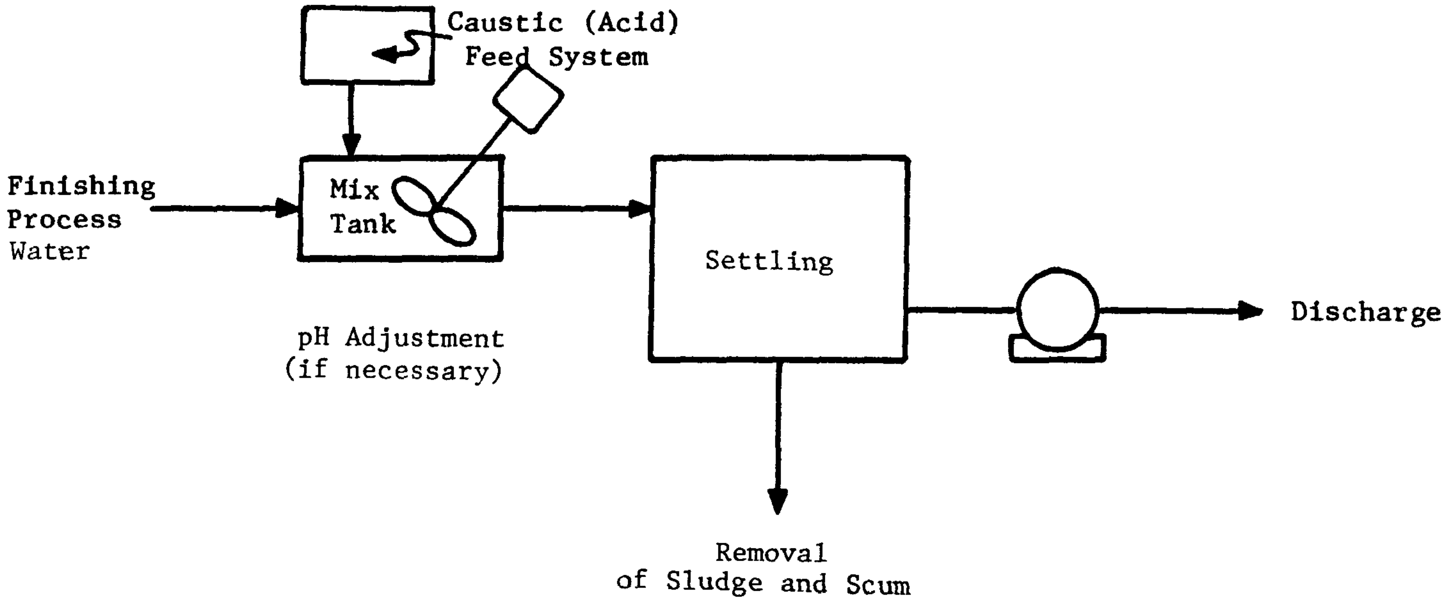


Figure X-3

SCHEMATIC OF BPT OPTION 1 - FINISHING WATER SUBCATEGORY

The estimated amounts of pollutants remaining after Option 1 are:

Type of Pollutant	Discharged in Raw Process Water - Direct Discharger (kg/yr)	Remaining After Option 1 (kg/yr)
Conventional	3,630	1,110
Priority Toxic	20	20

The methodology used to calculate the pollutant removals is presented in Appendix C.

The estimated investment cost and annual pollution controls for Option 1 are:

	Cost (1984 Dollars) Option 1
Investment Cost	$91,000
Annual Pollution Cost*	67,500

*Includes depreciation and interest.

Option Selected. The Agency is promulgating Option 1 as the technology basis for the BPT effluent limitations guidelines for this subcategory. This technology is demonstrated for the PM&F category. Twelve of the plants that treat PM&F process waters have a settling unit.

The Agency estimates that the BPT effluent limitations guidelines for this subcategory will result in the removal of 2,520 kg/yr of conventional pollutants from the process waters. The estimated total investment cost and total annual cost for the BPT effluent limitations guidelines are $91,000 and $67,500, respectively, in 1984 dollars. The Agency has determined that the costs are justified by the effluent reduction benefits.

The Agency estimates that the implementation of the selected BPT option for the finishing water subcategory will result in a net increase in electrical energy consumption of 24,000 kw-hr/yr and a solid waste generation rate of 10 metric tons per year. The methodologies used to derive these estimates are discussed in Section IX. The net increase in electrical energy consumption is significantly less than one percent of the estimated total current energy usage for the PM&F category. The Agency has concluded that the increased production of solid wastes associated with the selected option for this subcategory will not cause any significant negative environmental impacts. As discussed in Section IX of this document, EPA has determined the solid wastes are not expected to be hazardous pursuant to RCRA. There are no non-water quality impacts of the BPT effluent limitations guidelines for this subcategory.

REGULATED POLLUTANTS AND POLLUTANT PROPERTIES

Pollutants and pollutant properties selected for control in the plastics molding and forming category include biochemical oxygen demand (BOD_5), oil and grease (O&G), total suspended solids (TSS), and pH.

Biochemical oxygen demand was found in cleaning waters at concentrations up to 1,000 mg/l. BOD_5 is used to estimate the organic content of wastewater. BOD_5 is also an important control parameter for the activated sludge treatment process; the reduction of BOD_5 indicates an overall reduction of organic pollutants.

Total suspended solids was found in cleaning waters at concentrations up to 16,363 mg/l. It was found in finishing waters at concentrations up to 1,359 mg/l.

Oil and grease was detected in cleaning waters at concentrations up to 684 mg/l.

For protection of aquatic life and human welfare, pH of wastewater should be between 6.0 and 9.0. The pH of PM&F process waters is regulated because the pH of contact cooling and heating waters ranged between 5.4 and 8.3 and the pH of cleaning water ranged from 1.6 to 11.5. The pH of finishing water ranged from 6.4 to 8.4.

The Agency is establishing BPT effluent limitations guidelines for BOD_5, TSS, O&G, and pH in two subcategories and for TSS and pH in the other subcategory. The Agency estimates that when these limitations are met, approximately 63 percent of the amount of treatable nonconventional pollutants discharged by PM&F processes and approximately 65 percent of the amount of treatable priority toxic pollutants discharged will be removed. These estimates are based on removal percentages reported in the literature and previous EPA studies for the nonconventional and priority toxic pollutants. The nonconventional and priority toxic pollutants in PM&F process waters are listed in Tables VII-3 and VII-10, respectively.

EFFLUENT CONCENTRATION VALUES

Contact Cooling and Heating Water Subcategory. For the contact cooling and heating water subcategory, the concentrations used to calculate the mass of pollutants that can be discharged are based on a statistical evaluation of the raw waste concentrations in contact cooling and heating waters. Maximum for any one day concentrations were established for BOD_5, O&G, and TSS. pH is also controlled for this subcategory. Maximum for monthly average concentrations were not established for this subcategory because there is no variability associated with the performance of a treatment technology. The maximum for any one day values are based on the concentrations currently discharged and are presented in Table X-1. A discussion of the statistical evaluation of the contact cooling and heating water raw waste concentrations is presented in Appendix D.

Cleaning Water Subcategory. A package activated sludge plant is the end-of-pipe treatment technology selected as BPT for the cleaning water subcategory. The activated sludge process and performance data for that process were transferred from the organic chemicals, plastics, and synthetic fibers (OCPSF) category because wastewater generated by processes in that category and PM&F cleaning waters have similar conventional pollutant characteristics.

The transfer of the activated sludge process was evaluated by comparing the sampling data for cleaning waters obtained during the sampling program for this regulation to process wastewater data from the organic chemicals, plastics, and synthetic fibers category, particularly the plastics only subcategory. That comparison showed that the wastewaters for the cleaning water subcategory and for the OCPSF category have similar characteristics. Specifically, data on raw waste concentrations of BOD_5, TSS, and O&G were examined statistically. A detailed report on the statistical analysis is presented in Appendix D. Results of that analysis show that the concentrations for these pollutants in PM&F cleaning waters are neither significantly greater nor more variable than the concentrations of those pollutants in wastewaters generated by processes at plants that manufacture plastics. This supports the Agency's technical judgment that the activated sludge process will treat PM&F cleaning waters effectively and achieve the conventional pollutant effluent concentrations achieved by activated sludge processes that treat wastewater generated by processes at plastics manufacturing plants in the OCPSF category. The Agency's judgment that the activated sludge process will treat PM&F cleaning waters was based on the literature and knowledge of the performance of the activated sludge process.

Thus, the Agency transferred the activated sludge technology and effluent data for that technology from the OCPSF category to the PM&F cleaning water subcategory. Effluent concentration values were transferred for BOD_5, TSS, and O&G. These values are presented in Table X-1.

Table X-1

EFFLUENT CONCENTRATIONS USED TO CALCULATE THE FINAL BPT EFFLUENT LIMITATIONS GUIDELINES

Contact Cooling and Heating Water Subcategory

Pollutant	Maximum for Any One Day (mg/l)	Maximum for Monthly Average (mg/l)
BOD_5	26	(2)
Oil and Grease	29	(2)
TSS	19	(2)
pH	(1)	(1)

Cleaning Water Subcategory

Pollutant	Maximum for Any One Day (mg/l)*	Maximum for Monthly Average (mg/l)*
BOD_5	49	22
Oil and Grease	71	17
TSS	117	36
pH	(1)	(1)

Finishing Water Subcategory

Pollutant	Maximum for Any One Day (mg/l)	Maximum for Monthly Average (mg/l)
TSS	130	37
pH	(1)	(1)

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(1) Within the range 6.0 to 9.0 at all times.

(2) Not established for this subcategory.

*Transferred from the OCPSF category.

Finishing Water Subcategory. The effluent concentrations for TSS for the finishing water subcategory were obtained by multiplying the subcategory average TSS concentration by a percent removal to obtain a long-term average concentration. Variability factors were then applied to the long-term average to obtain the maximum for any one day and maximum for monthly average concentration values. Calculation of both the variability factors and the concentration values is discussed in more detail in Appendix D. The TSS concentrations used to calculate the final BPT effluent limitations guidelines for the finishing water subcategory are presented in Table X-1.

BPT EFFLUENT LIMITATIONS GUIDELINES

BPT effluent limitations guidelines are calculated by multiplying the pollutant concentrations promulgated in the final PM&F regulation by the average process water usage flow rate for a process, which is obtained from a permittee. The maximum for any one day and maximum for monthly average concentrations used to calculate the final BPT effluent limitations guidelines are presented in Table X-1.

EXAMPLE OF THE APPLICATION OF THE BPT EFFLUENT LIMITATIONS GUIDELINES

The purpose of the BPT effluent limitations guidelines is to provide a uniform basis for regulating process water discharged from processes in the plastics molding and forming category. For direct dischargers, this is accomplished through NPDES permits. The plastics molding and forming category is regulated on an individual wastewater flow "building block" approach. An example that illustrates how the effluent limitations guidelines are used to determine the amount of pollutants that can be discharged from plastics molding and forming plants is presented below.

Example

Plant X is a hypothetical plastics molder and former that is classified as a direct discharger. Plant X, which operates for eight hours a day, 250 days per year, compounds and pelletizes 1,250,000 kg of polyethylene per year. The pelletizing process uses contact cooling water. A portion of the pelletized product is extruded in a process that also uses contact cooling water. The average process water usage flow rates for both these processes are 118,100 l/day (65 gpm) and 36,400 l/day (20 gpm), respectively.

In addition, Plant X cleans injection molds; the molds are used to shape polyethylene products. The average process usage flow rate for the cleaning water process is 16,350 l/day (3 gpm). The shaped polyethylene is then trimmed in a finishing operation that uses an average of 1,900 l/day (0.34 gpm) of finishing water. Only de minimus levels of BOD_5 and oil and grease are present in the finishing water from this operation.

Based on this information, the allowable masses of pollutants that can be discharged by Plant X under the final BPT regulation are determined as follows. Plant X has processes that belong to each of the three PM&F subcategories. The two contact cooling processes are regulated under the contact cooling and heating water subcategory, the injection mold cleaning process is regulated under the cleaning water subcategory, and the trimming process is regulated under the finishing water subcategory.

The mass of BOD_5 that may be discharged from PM&F processes at Plant X is calculated as follows:

1. The total average process water usage flow rate for the contact cooling and heating water process is the sum of the reported average process water usage flow rates. For Plant X, this is equal to 118,100 l/day plus 36,400 l/day, or a total of 154,500 l/day.

2. From Table X-1, the maximum for any one day concentration value for BOD_5 is 26 mg/l.

3. Multiplying the effluent concentration (26 mg/l) by the average process water flow rate (154,500 l/day) results in the maximum for any one day mass of 4,017,000 mg/day (8.9 lbs/day) of BOD_5 that may be discharged from the contact cooling and heating water processes.

4. Using these calculation procedures (steps 1-3) for the cleaning water process results in the corresponding maximum for any one day BOD_5 discharge of 801,500 mg/day (1.8 lbs/day). The BOD_5 discharge from the finishing water is not considered because BOD_5 is not regulated in the finishing water subcategory and only de minimus levels of BOD_5 were reported in the finishing water by the permittee.

5. The total maximum for any one day discharge for BOD_5 for Plant X is the sum of 4,017,000 mg/day (from contac cooling water) and 801,150 mg/day (from cleaning water), or 4,818,150 mg/day (10.6 lbs/day).

Table X-2 illustrates the calculation of the maximum for any one day mass of pollutants that can be discharged for Plant X. Maximum for monthly average mass discharges are calculated in a similar manner.

Table X-2

ALLOWABLE DISCHARGE OF REGULATED POLLUTANTS FOR PLANT X

Process Water	Average Process Water Usage Flow Rate (l/day)	BOD$_5$		O&G		TSS	
		Effluent Concentration (mg/l)*	Maximum for Any One Day Mass (mg/day)	Effluent Concentration (mg/l)	Maximum for Any One Day Mass (mg/day)	Effluent Concentration (mg/l)	Maximum for Any One Day Mass (mg/day)
Contact Cooling Water for Pelletizing	118,100	26	3,070,600	29	3,424,900	19	2,243,900
Contact Cooling Water for Extrusion	36,400	26	946,400	29	1,055,600	19	691,600
Cleaning Water for Injection Molds	16,350	49	801,150	71	1,160,850	117	1,912,950
Finishing Water for Trimming	1,900	†	--	†	--	130	247,000
Total Maximum for Any One Day Discharge for Plant X (mg/day)			4,818,150		5,641,350		5,095,450

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*Effluent concentrations are from Table X-1.

†BOD$_5$ and O&G are not regulated in the finishing water subcategory. Additionally, the permittee reported only de minimus levels of BOD$_5$ and O&G in the process waters for the finishing operations.

SECTION XI

BEST AVAILABLE TECHNOLOGY ECONOMICALLY ACHIEVABLE

INTRODUCTION

This section defines the effluent limitations guidelines based on the performance of the best available technology economically achievable (BAT) pursuant to Section 304(b)(2)(B) of the Clean Water Act. BAT effluent limitations guidelines are applicable to process waters that are directly discharged by existing sources.

The factors considered in assessing BAT include the total cost of applying the technology in relation to the amount of pollutant removal, age of equipment and facilities involved, the process employed, process changes, non-water quality environmental impacts (including energy requirements) and the costs of applying such technology. At a minimum, the BAT level represents the best economically achievable performance of plants of various ages, sizes, processes, or other shared characteristics. As with BPT, where the Agency has found the existing treatment performance to be uniformly inadequate, BAT may be transferred from a different subcategory or category. BAT may include feasible process changes or internal controls even when not common industry practice.

The required assessment of BAT "considers" costs, but does not require a balancing of costs against effluent reduction benefits (see, Weyerhaeuser v. Costle, supra). In developing BAT, however, EPA gives substantial weight to the reasonableness of cost. The Agency considers the volume and nature of discharges expected after application of BPT, the general environmental effects of the pollutants, and the costs and economic impacts of the additional pollution control levels.

Despite this expanded consideration of costs, the primary determinant of BAT is effluent reduction capability. As a result of the Clean Water Act of 1977, the achievement of BAT effluent limitations guidelines has become the principal national means of controlling toxic pollutants. Process waters generated by PM&F processes contain five priority toxic pollutants in treatable concentrations including one toxic metal and four toxic organics.

IDENTIFICATION OF THE BEST AVAILABLE TECHNOLOGY ECONOMICALLY ACHIEVABLE

Contact Cooling and Heating Water Subcategory

The only toxic pollutant found in treatable concentrations in contact cooling and heating waters was bis(2-ethylhexyl) phthalate. It was found in treatable concentrations in 12 out of 16 processes sampled (52.6 percent of the samples analyzed) ranging from 0.011 to 1.72 mg/l. Therefore, only BAT options that remove that pollutant were considered for the final PM&F regulation.

At proposal, EPA considered a package activated sludge plant as a BAT option for this subcategory. This option was not considered for the final rule because the BOD_5 concentrations in contact cooling and heating waters are not high enough to support the operation of biological treatment.

Contract haul was also a BAT option for this subcategory at proposal. That option included recycle to reduce the amount of process water that had to be hauled. As discussed earlier, the Agency has determined that recycle is no longer appropriate as part of the technology basis for the effluent limitations guidelines and standards for the PM&F category. EPA believes that contract haul is not a feasible option unless the amount of process water that has to be hauled is reduced through the use of a recycle unit. For this reason, contract haul was not considered as a BAT option for the final regulation for this subcategory.

The Agency considered one option as the basis for the BAT effluent limitations guidelines in this subcategory. It is:

Option 1: pH Adjustment (as needed) and Activated Carbon Adsorption

The model treatment technology in Option 1 is the only technology EPA could identify to remove the bis(2-ethylhexyl) phthalate in contact cooling and heating water. Enough activated carbon was included in the design of that process to remove the phthalate to a level equal to its treatability limit (see Table VII-9). The technology for this option is shown in Figure XI-1.

The estimated amount of bis(2-ethylhexyl) phthalate discharged in contact cooling and heating water is 9,470 kg/yr. After application of the model treatment technology in Option 1, the Agency estimates that 8,500 kg/yr of this phthalate will be removed.

The estimated investment costs and annual pollution control costs for Option 1 are $34,000,000 and $13,000,000, respectively, in 1984 dollars. Detailed information on these costs is presented in *Economic Impact Analysis of Effluent Limitations and Standards for the Plastics Molding and Forming Industry*, EPA 440/2-84-025, December 1984.

Option Selected. The Agency is not selecting Option 1 as the basis for the final BAT effluent limitations guidelines for this subcategory at this time because EPA has no treatability data for the activated carbon process. The Agency plans to conduct further studies to obtain these data.

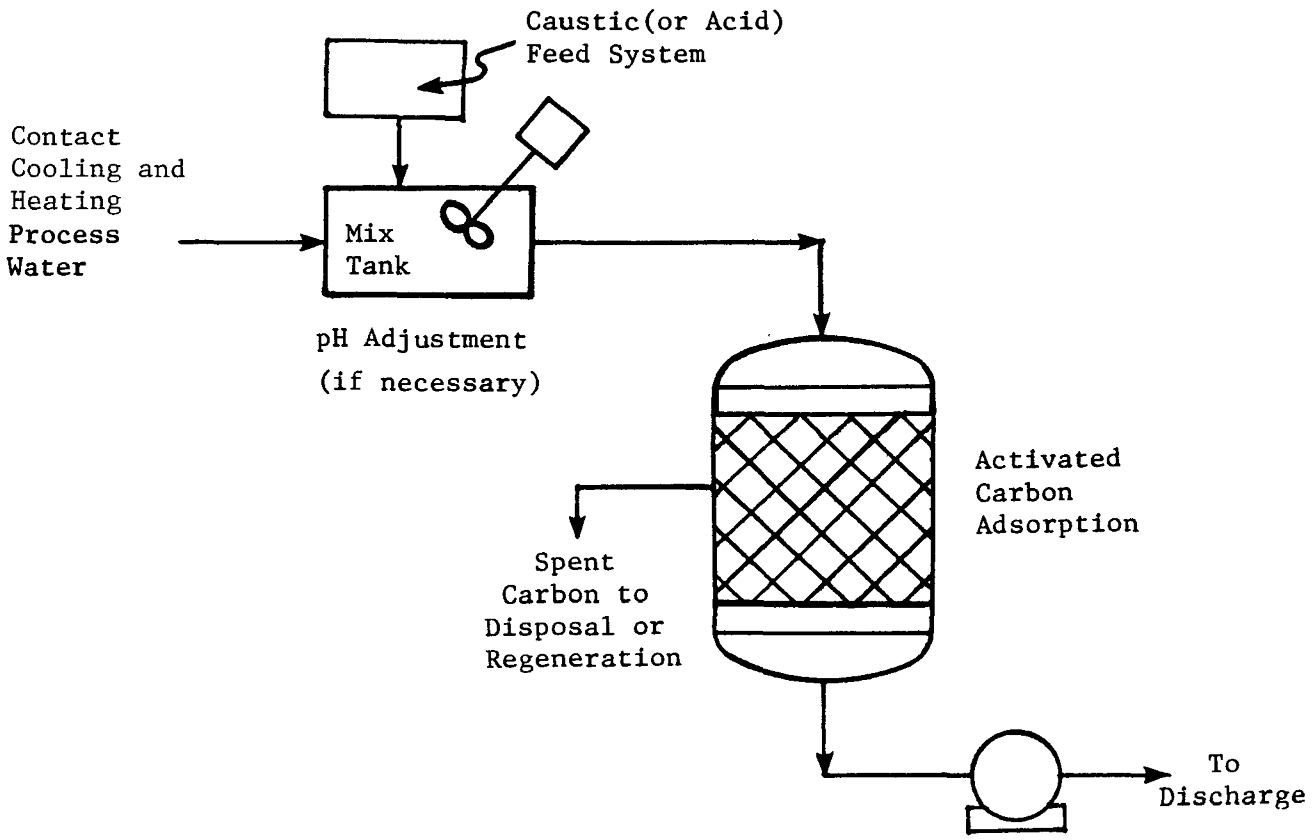

Figure XI-1

BAT OPTION 1
CONTACT COOLING AND HEATING WATER SUBCATEGORY

As part of the treatability study, EPA will collect samples at contact cooling and heating water processes. The Agency will then conduct bench-scale studies to select the type of activated carbon to use to treat contact cooling and heating water and to determine the carbon exhaustion rates. Once carbon exhaustion rates are known, EPA can design and cost the activated carbon processes for the treatment of contact cooling and heating water.

Because of the lack of performance data for the treatment of phthalates in the activated carbon process, EPA is reserving the BAT effluent limitations for bis(2-ethylhexyl) phthalate for this subcategory at this time. When the treatability study discussed above is completed, the Agency will propose and promulgate the BAT effluent limitations guidelines for the phthalate.

The Agency is promulgating BAT equal to BPT for the other priority toxic pollutants because bis(2-ethylhexyl) phthalate is the only toxic pollutant found in treatable concentrations in contact cooling and heating waters. Therefore, except for bis(2-ethylhexyl) phthalate, the BAT effluent limitations guidelines are the same as the BPT effluent limitations guidelines for this subcategory. EPA has determined that the BAT/BPT effluent limitations guidelines for this subcategory are economically achievable.

There are no net increases in energy usage or solid waste generation for BAT compared to BPT for the contact cooling and heating water subcategory because, at this time, the Agency is not promulgating BAT effluent limitations guidelines more stringent than the BPT effluent limitations guidelines for this subcategory.

Cleaning Water Subcategory

The Agency only considered one option for BAT for this subcategory. This option, which is the selected BPT, is:

Option 1: Equalization, pH Adjustment, and Package Activated Sludge Plant

At proposal, the Agency considered recycle and contract haul of the discharge from the recycle unit as a BAT option. This option was rejected for this subcategory for the final regulation for the same reasons it was rejected in the contact cooling and heating water subcategory.

The Agency is not promulgating BAT effluent limitations guidelines more stringent than the BPT effluent limitations guidelines for this subcategory because there are insignificant quantities of priority toxic pollutants remaining in cleaning waters after application of BPT. The Agency estimates that 155 kg/yr of the toxic pollutants (i.e., phenol and zinc) discharged in cleaning waters in treatable concentrations will be removed after compliance with the BPT effluent limitations guidelines. Thus, 82 kg/yr would be discharged after application of BPT. This is equal to less than 0.01 kg/day of toxic pollutants discharged per direct discharger. Table C-4 in Appendix C lists the estimated amount of phenol and zinc that would be discharged per year by direct dischargers in this subcategory after compliance with the BPT effluent limitations guidelines. Also shown on Table C-3 is the average concentration of toxic pollutants after application of BPT. The Agency has determined that the toxic pollutants are adequately controlled by the BPT effluent limitations guidelines and the amount and toxicity of those pollutants after application of BPT do not justify establishing more stringent BAT effluent limitations guidelines for toxic pollutants for this subcategory. Accordingly, EPA is excluding the toxic pollutants phenol and zinc from further national regulation for this subcategory, under Paragraph 8(a)(i) of the Settlement Agreement in NRDC v. Train, supra.

There are no net increases in energy usage or solid waste generation for BAT compared with BPT for the cleaning water subcategory because the Agency is not promulgating BAT effluent limitations guidelines more stringent than BPT effluent limitations guidelines for this subcategory. EPA has determined that the BAT/BPT effluent limitations guidelines for this subcategory are economically achievable.

Finishing Water Subcategory

Three toxic pollutants were found in finishing waters in treatable concentrations. Bis(2-ethylhexyl) phthalate was found in treatable concentrations in two of three sampled finishing processes (55.6 percent of the samples analyzed) ranging from 0.011 mg/l to 1.488 mg/l. Di-n-butyl phthalate was found in treatable concentrations in one of three sampled finishing processes (33.3 percent of the samples analyzed) ranging from 0.038 mg/l to 0.081 mg/l; dimethyl phthalate was found in treatable concentrations in one of three sampled finishing processes (11.1 percent of the samples analyzed) at 0.194 mg/l. Therefore, for this final regulation, only BAT options that remove bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate were considered.

At proposal, cleaning water processes and finishing water processes were in the same subcategory. Subsequent to proposal, those processes were placed in separate subcategories.

The BAT options considered at proposal for the cleaning and finishing water subcategory were considered for the finishing water subcategory in this final regulation. Recycle and contract haul of the discharge from the recycle unit was rejected for this subcategory for the same reasons it was rejected for the cleaning water subcategory. Recycle and treatment of the discharge from the recycle unit in a package activated sludge plant with pH adjustment was also rejected for this subcategory because the BOD_5 concentrations in finishing waters are not high enough to support the operation of a biological process.

The Agency considered one option as the basis for the BAT effluent limitations guidelines for this subcategory.

Option 1: pH Adjustment (as needed), Settling, and Activated Carbon Adsorption

The model treatment technology in Option 1 is the only technology EPA could identify to remove the phthalates in finishing waters. Enough activated carbon was included in the design of that process to remove the phthalates to a level equal to their treatability limits (see Table VII-9). The settling unit, which is the selected BPT, removes the TSS in the process water prior to treatment of the process water in the activated carbon process. The model treatment technology for this option is depicted in Figure XI-2.

The estimated amounts of pollutant remaining after Option 1 are:

Pollutant	In Raw Wastewater (kg/yr)	Pollutant Mass Removed - Option 1 (kg/yr)	Remaining After Option 1 (kg/yr)
Conventional	3,630	2,938	692
Priority Toxic	20	18.5	1.5

The estimated investment costs and annual pollution control cost for Option 1 are $311,000 and $162,000, respectively, in 1984 dollars.

Option Selected. The Agency is not selecting Option 1 as the basis for the final BAT effluent limitations for this subcategory at this time because EPA has no treatability data for phthalates for the activated carbon process. As mentioned in the discussion for the contact cooling and heating water subcategory, the Agency plans to conduct further studies to obtain these data. These studies will address the phthalates in both contact cooling and heating waters and in finishing waters.

Because of the lack of performance data for the treatment of phthalates in the activated carbon process, EPA is reserving the

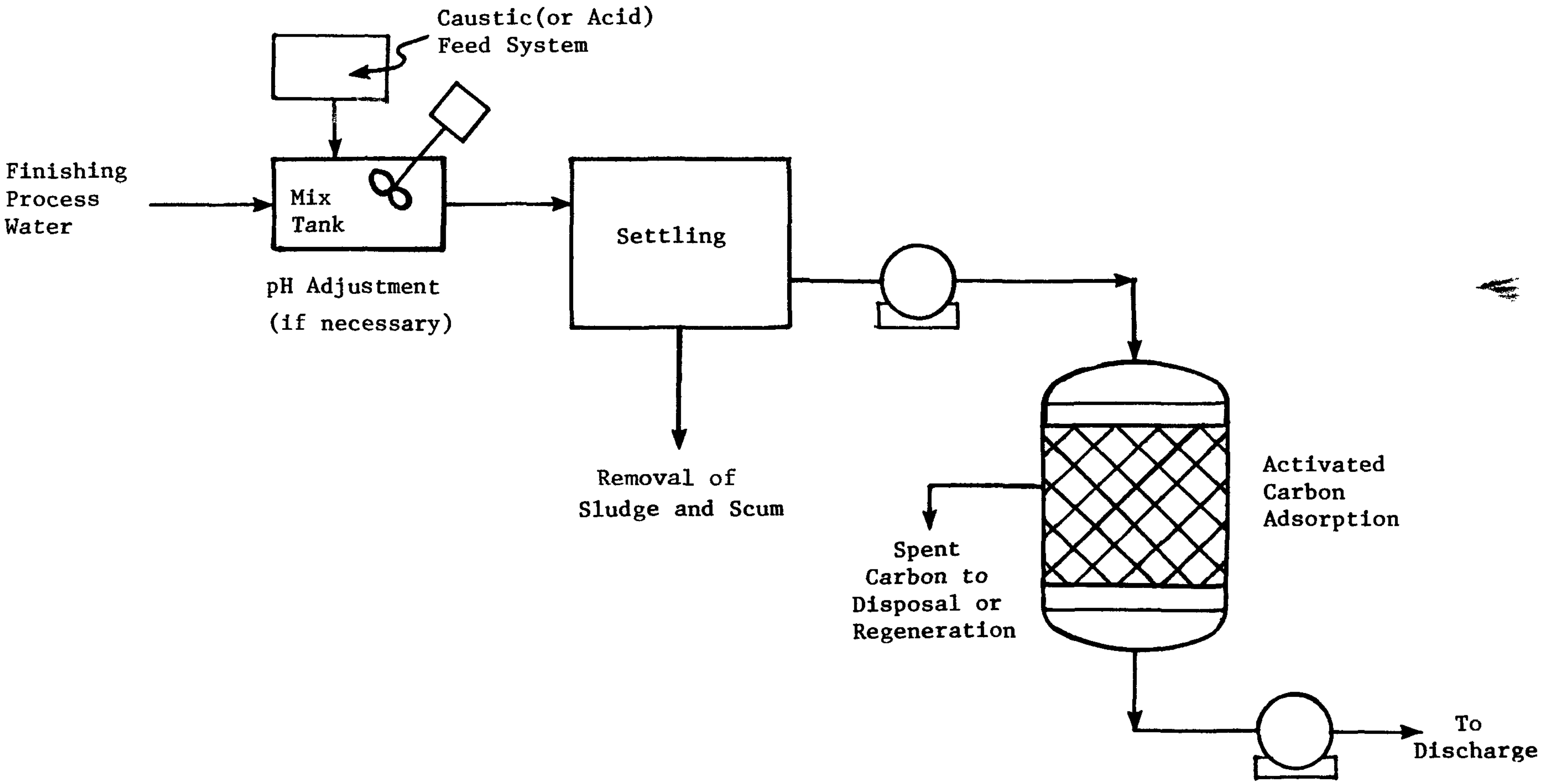

Figure XI-2

BAT OPTION 1
FINISHING WATER SUBCATEGORY

BAT effluent limitations guidelines for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate for this subcategory at this time. When the treatability study for phthalates is completed, the Agency will propose and promulgate the BAT effluent limitations guidelines for the phthalates.

The Agency is promulgating BAT equal to BPT for the other toxic pollutants because, except for the three phthalates, there are no toxic pollutants found in treatable concentrations in finishing waters. With the exception of the three phthalates listed above, the BAT effluent limitations guidelines are the same as the BPT effluent limitations guidelines for this subcategory. EPA has determined that the BAT/BPT effluent limitations guidelines for this subcategory are economically achievable.

There are no net increases in energy usage or solid waste generation for BAT compared to BPT for the finishing water subcategory because, at this time, the Agency is not promulgating BAT effluent limitations guidelines more stringent than the BPT effluent limitations guidelines for this subcategory.

SECTION XII

NEW SOURCE PERFORMANCE STANDARDS

INTRODUCTION

This section discusses new source performance standards (NSPS) for PM&F processes at new sources that discharge directly to navigable waters. New sources are defined as any building, structure, facility, or installation (including major modifications to existing sources) for which construction is started after promulgation of NSPS for the PM&F category.

The basis for NSPS under Section 306 of the Act is the best available demonstrated technology. New plants have the opportunity to design and use the best and most efficient plastics molding and forming processes and wastewater treatment technologies without facing the added costs and restrictions encountered in retrofitting an existing plant. Therefore, Congress directed EPA to consider the best demonstrated process changes, in-plant controls, and end-of-pipe treatment technologies that reduce pollution to the maximum extent feasible when developing NSPS.

TECHNICAL APPROACH TO NSPS

The Agency believes that characteristics of process waters discharged by new PM&F processes in each subcategory will be the same as the characteristics of process waters discharged by existing PM&F processes in those subcategories. Thus, the options considered for NSPS are the same as those considered for the BPT/BAT effluent limitations guidelines for each subcategory. These options are discussed in the BPT and BAT sections of this development document (Sections X and XI, respectively). The pollutants found in treatable concentrations in the process waters for each subcategory and their concentrations are presented in Tables VII-1, VII-3, and VII-10.

NSPS OPTION SELECTION

Except for phthalates in two subcategories, the Agency is promulgating NSPS based on the model treatment technologies selected as the basis for the BPT/BAT effluent limitations guidelines. EPA is not promulgating NSPS more stringent than the effluent limitations guidelines for existing sources at this time because either the amount and toxicity of the priority toxic pollutants remaining after application of the BPT/BAT model technologies do not justify more stringent controls or there are no toxic pollutants in treatable concentrations in the process waters. The mass of priority toxic pollutants remaining and their effluent concentrations after application of BPT/BAT are presented in Tables C-3 and C-5 for the cleaning water subcategory and Tables C-7 and C-10 for the finishing water subcategory, respectively. Except for one phthalate, there are no priority toxic pollutants in treatable concentrations in contact cooling and heating process waters.

EPA is reserving NSPS for bis(2-ethylhexyl) phthalate for the contact cooling and heating water subcategory pending completion of the phthalate treatability study discussed in Section XI of this development document. NSPS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are also reserved for the finishing water subcategory until the treatability study is completed. When that study is completed, EPA will propose and promulgate NSPS for the phthalates.

The technology basis for NSPS for each subcategory is:

Contact Cooling and Heating Water Subcategory

NSPS for this subcategory are based on good housekeeping practices. As discussed earlier, EPA found during the sampling episodes for development of the PM&F regulation that good housekeeping practices are employed with contact cooling and heating water processes. Lubricating oils and other pollutants are kept out of the contact cooling and heating waters and those waters are used only for plastics molding and forming. Good housekeeping practices are the basis for the NSPS for this subcategory because, except for one phthalate, there are no pollutants in contact cooling and heating wasters in treatable concentrations. NSPS ensure that good housekeeping practices will be employed at plants using new contact cooling and heating water processes because they are based on the current concentrations of pollutants discharged at existing sources where good housekeeping is practiced.

NSPS for this subcategory control BOD_5, O&G, TSS, and pH. Results of the statistical evaluation used to establish concentration values for those pollutants are presented in Appendix D. NSPS for bis(2-ethylhexyl) phthalate for this subcategory are reserved pending completion of the phthalate treatability study.

Cleaning Water Subcategory

The model treatment technology for NSPS for this subcategory consists of equalization, pH adjustment (as needed), and a package activated sludge plant. A schematic of the model treatment technology for NSPS for the cleaning water subcategory is presented in Figure XII-1. NSPS for this subcategory control BOD_5, O&G, TSS, and pH.

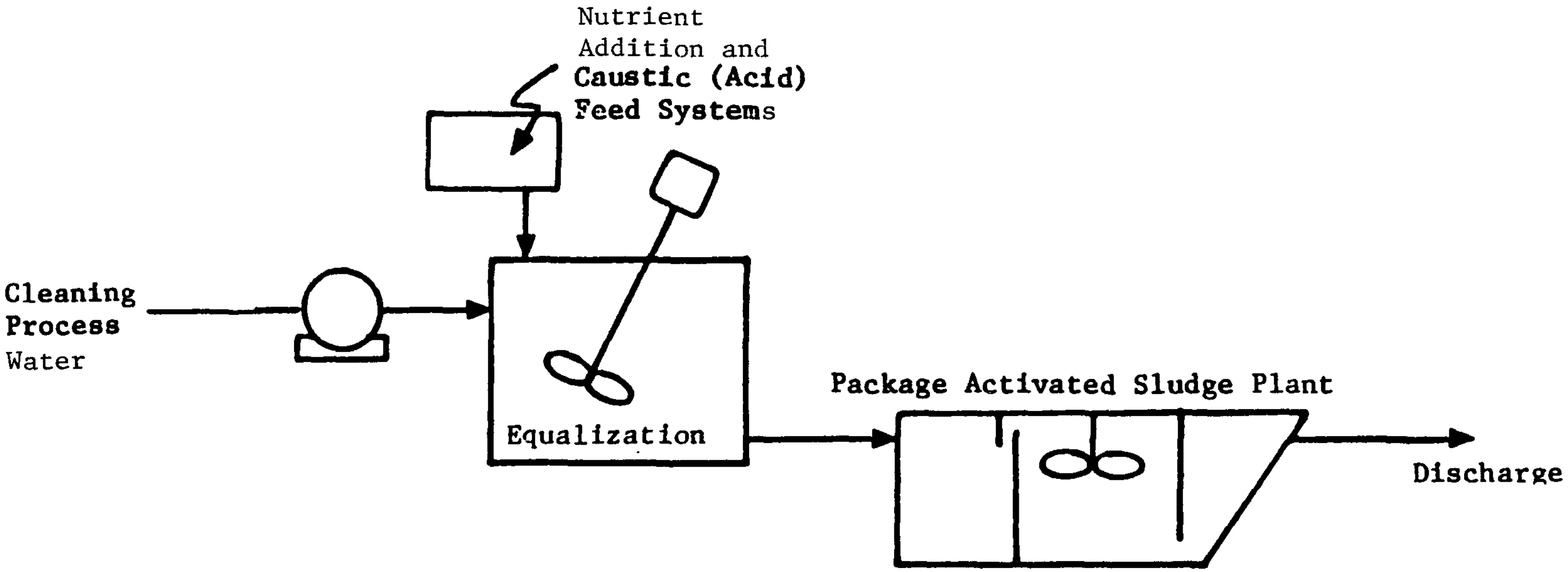

Figure XII-1

MODEL TREATMENT TECHNOLOGY FOR NSPS - CLEANING WATER SUBCATEGORY

The Agency considered a model treatment technology for NSPS for this subcategory that included a package activated sludge plant followed by a filter. However, EPA did not propose NSPS based on this more stringent technology and the Agency has no performance data using that technology for the treatment of cleaning water only. Also, EPA did not receive any comments on the proposed PM&F regulation suggesting that a filter should be included in the model technology for NSPS. This may be because, based on the "normal" plant for this subcategory discussed later in this section, the Agency estimates that 2,180 kg/yr of conventional pollutants would be removed by the activated sludge process followed by a filter (see Appendix C). This is only 80 kg/yr or 0.32 kg/day per direct discharging new source more than would be removed by a package activated sludge plant without a filter. There are no additional nonconventional and priority toxic pollutant removals by filtration, because these pollutants are dissolved, not suspended. For these reasons, EPA is not including a filter in the NSPS model technology for this subcategory at this time. However, after further study of the filtration technology for the best conventional pollutant control technology (BCT) effluent limitations guidelines for this subcategory, if the Agency finds that additional conventional pollutant removals based on the application of a filter are justified, EPA may revise NSPS for this subcategory using a model treatment technology that consists of a package activated sludge plant with pH adjustment and a filter.

Finishing Water Subcategory

The model treatment technology for NSPS for this subcategory consists of pH adjustment (if necessary) and settling. A schematic of this model treatment technology for the finishing water subcategory is presented in Figure XII-2. NSPS for this subcategory control TSS and pH.

NSPS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate for this subcategory are reserved pending completion of the phthalate treatability study discussed in Section XI. The phthalates were the only toxic pollutants found in treatable concentrations in finishing waters.

The Agency considered a model treatment technology for NSPS for this subcategory that included pH adjustment, settling, and filtration. However, EPA did not propose NSPS based on this more stringent technology and the Agency has only limited performance data using this model treatment technology to treat finishing waters only. Also, EPA did not receive any comments on the proposed PM&F regulation suggesting that a filter should be included in the model treatment technology for NSPS (cleaning water processes and finishing water processes were in the same subcategory at proposal). This may be because, based on the

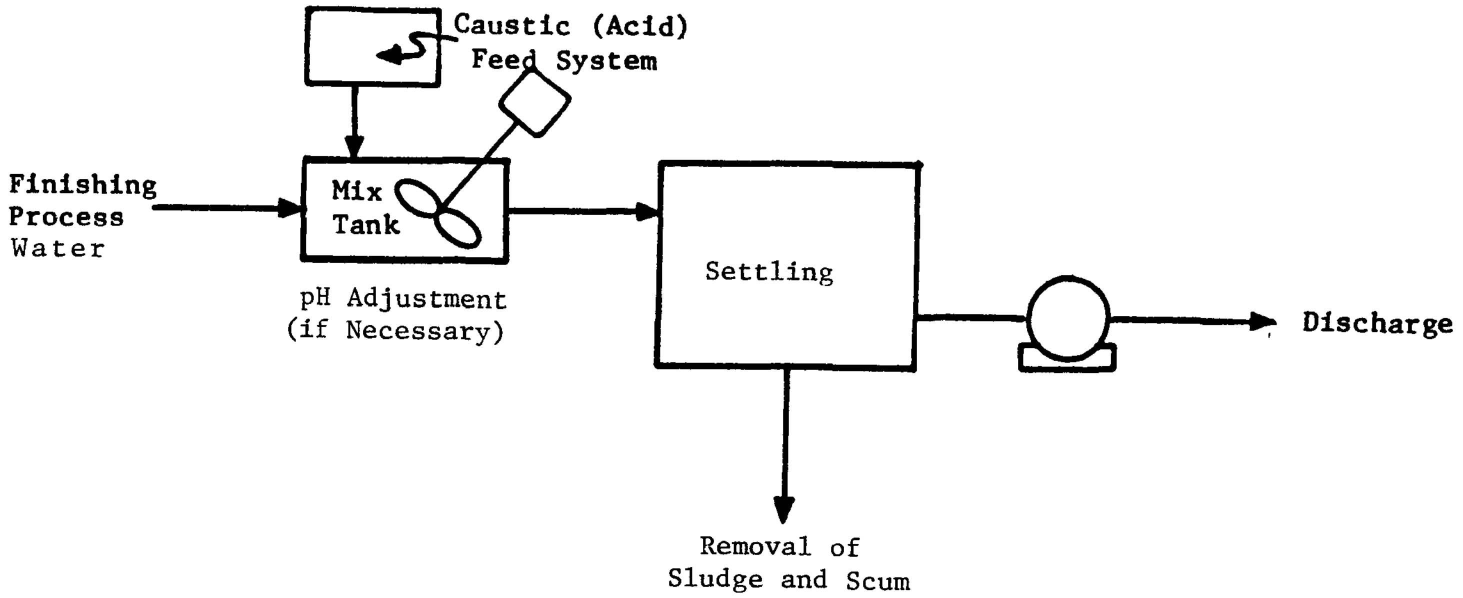

Figure XII-2

MODEL TREATMENT TECHNOLOGY FOR NSPS - FINISHING WATER SUBCATEGORY "normal" plant for this subcategory discussed later in this section, the Agency estimates that 318 kg/yr of conventional pollutants would be removed by a settling unit followed by a filter (see Appendix C). This is only 66 kg/yr or 0.26 kg/day per direct discharging new source more than would be removed by a settling unit. For these reasons, EPA is not using a filter as with the model treatment technology for NSPS for this subcategory at this time. However, after further study of the filtration technology for the BCT effluent limitations guidelines for this subcategory, if the Agency finds that additional conventional pollutant removals based on the application of a filter are justified, EPA may revise NSPS for this subcategory using filtration as part of the model treatment technology.

COSTS AND POLLUTANT REMOVALS FOR NSPS

The Agency conducted an economic analysis of the impact of the final NSPS on new PM&F plants. The analysis was based on a "normal" plant for each subcategory. A "normal" plant for a subcategory is a theoretical model plant that has one molding and forming process covered by the subcategory whose production, wastewater characteristics, and financial profile are typical of existing plants.

The process flow rates for the PM&F process in a "normal" plant are assumed to be the median values for plants in the questionnaire data base for a subcategory. The pollutant concentrations in the process waters discharged from the PM&F process at a "normal" plant are assumed to be equal to the subcategory average pollutant concentrations. Each "normal" plant is also assumed to operate 6,000 hours/year (24 hours/day for 250 days/year). Process flow rates and pollutant concentrations assumed for the "normal" plant in each subcategory are presented in Table XII-1.

The pollutant masses in the PM&F process waters for the "normal" plants are shown in Table XII-2. The pollutant removals for the NSPS model treatment technology for each "normal" plant are presented in Table XII-3. Data for the model treatment technologies used as the basis for the effluent limitations guidelines for existing sources were used to estimate the removals presented in Table XII-3.

The estimated investment cost and annual pollution control costs for the NSPS model treatment technology for each subcategory are presented in Table XII-4.

Data relied on for the economic analysis of NSPS were primarily data developed for existing sources, which include costs on a plant-by-plant basis along with retrofit costs where applicable. The Agency believes that costs could be lower for new sources

Table XII-1

CHARACTERISTICS OF PM&F "NORMAL" PLANTS

	Subcategory		
Characteristic†	Contact Cooling and Heating Water	Cleaning Water	Finishing Water
Process Flow Rate (gpm)	35	13.5	3.15
Operating Hours (hrs/yr)	6,000	6,000	6,000
Conventional Pollutants			
BOD5 (mg/l)	*	89	*
O&G (mg/l)	*	47	*
TSS (mg/l)	*	714	95
pH	5.4-8.3	1.6-11.5	6.9-8.4
Nonconventional Pollutants (mg/l)			
COD	*	115	*
TOC	*	634	*
Total Phenol	*	36	*
Priority Pollutants (mg/l)			
65. Phenol	*	0.198	*
66. Bis(2-ethylhexyl) Phthalate	0.098	*	0.479
68. Di-n-butyl phthalate	*	*	0.031
71. Dimethyl phthalate	*	*	0.034
128. Zinc	*	0.598	*

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†The average values presented here are from Tables VII-1, VII-3, and VII-10.

*Pollutant was not found in treatable concentrations in this subcategory.

Table XII-2

POLLUTANT MASS IN PROCESS WATERS FOR NSPS "NORMAL" PLANT (kg/yr)

Pollutant	Contact Cooling and Heating Water Subcategory	Cleaning Water Subcategory	Finishing Water Subcategory
Conventional	*	2,293	363
Nonconventional	*	2,079	*
Priority Toxic	13.6	2.3	2.1

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*Pollutants not found in treatable concentrations in process waters.

Table XII-3

ESTIMATED POLLUTANT REMOVALS FOR PM&F NSPS MODEL TREATMENT TECHNOLOGY (kg/yr)

Pollutant	Contact Cooling and Heating Water Subcategory*	Cleaning Water Subcategory	Finishing Water Subcategory
Conventional	0	2,094	252
Nonconventional	0	1,314	0
Priority Toxic	0	1.5	0

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*Minimal removals for this subcategory because NSPS are based on good housekeeping practices instead of performance of a treatment technology.

Table XII-4

ESTIMATED COSTS OF NSPS MODEL TREATMENT TECHNOLOGY FOR PM&F "NORMAL" PLANTS

($, 1984 Dollars)

	Contact Cooling and Heating Water Subcategory	Cleaning Water Subcategory	Finishing Water Subcategory
Investment Cost	0	$267,000	$9,100
Annual Pollution Control Costs	0	$ 83,000	$6,800

than costs for equivalent existing sources because production processes could be designed to reduce the amount of process water discharged and there would be no costs associated with retrofitting a process. The Agency does not believe that applying the model treatment technology for NSPS to new sources, including major modifications to existing sources, creates a barrier to entry into the PM&F category because new sources will expend an amount equal to, or possibly less than, the amount required by existing sources to comply with the final PM&F regulation.

REGULATED POLLUTANTS AND POLLUTANT PROPERTIES

The Agency has no reason to believe that the pollutants found in treatable concentrations in PM&F process waters from new sources will be any different than pollutants found in process waters from existing sources. Consequently, pollutants selected for regulation under NSPS are the pollutants controlled at BPT for each subcategory. They are: BOD_5, O&G, TSS, and pH in the contact cooling and heating water subcategory and in the cleaning water subcategory and TSS and pH in the finishing water subcategory. The effluent concentrations promulgated for NSPS are the same as those presented in Table X-1. Those values are multiplied by the average process water usage flow rate obtained from the permittee to obtain the mass of pollutants that can be discharged. The Agency estimates that, except for phthalates, 63 percent of the treatable nonconventional pollutant mass and 65 percent of the treatable priority toxic pollutant mass are removed when the NSPS for the conventional pollutants are met. NSPS for phthalates are reserved in two subcategories.

NEW SOURCE PERFORMANCE STANDARDS

The effluent concentration values used by a permit writer or control authority to calculate the mass of a pollutant that can be discharged are the same as those used to calculate the BPT effluent limitations guidelines. These concentration values are discussed in more detail in Section X of this development document.

The concentration values for NSPS (see Table X-1) are multiplied by the average process water usage flow rate to obtain the mass of pollutants discharged. Calculation of the effluent concentration values presented in Table X-1 is addressed in Appendix D.

The example presented in Section X, which illustrates the application of the BPT effluent limitations guidelines, is also relevant to the application of the NSPS for each subcategory for the final regulation.

NON-WATER QUALITY IMPACTS

A. Air Pollution

Model treatment technologies for NSPS will settle or biologically oxidize pollutants found in PM&F process waters. Emissions from these technologies are not expected to cause air pollution problems. Accordingly, NSPS will not create any substantial air pollution problem.

B. Solid Waste

EPA believes that the amount of solid wastes generated by a new source will be approximately the same as the amount generated by an equal-sized existing source at BPT. Therefore, for equal-sized facilities, the estimated annual average plant production of solid wastes generated in compliance with NSPS would be about the same as the annual average plant production for BPT. EPA projects that this would be about 40 metric tons per year per new source in the cleaning water subcategory and about 10 metric tons per year per new source in the finishing water subcategory. EPA anticipates that only minimal quantities of solid wastes would be generated at new sources in the contact cooling and heating water subcategory because of the characteristically low levels of TSS in process water discharges from existing sources in this subcategory. The assumptions used for estimating solid waste generation rates are presented in Section IX.

In addition, it is the Agency's view that solid wastes generated by new sources as a result of these guidelines are not expected to be classified as hazardous. This conclusion is based on the results of extraction procedure (EP) toxicity tests discussed in Section IX.

C. Consumptive Water Loss

The model treatment technologies for NSPS are not expected to cause a water loss. Therefore, NSPS are not expected to result in a consumptive water loss.

D. Energy Requirements

EPA believes that the energy used by a new direct discharging plant to comply with NSPS will be approximately the same amount as that used by an equal-sized existing source at BPT. Therefore, for equal-sized plants, the estimated annual plant energy use for NSPS would be about the same as the annual average energy use for BPT. EPA projects that this would be about 83,000 kw-hr/yr per new source in the cleaning water subcategory and about 2,400 kw-hr/yr per new source in the finishing water subcategory. EPA anticipates that only minimal quantities of energy will be required at new sources in the contact cooling and heating water subcategory because the technology basis of NSPS (the application of good housekeeping practices) would not involve the use of significant levels of energy. The assumptions used for estimating energy requirements are presented in Section IX.

These uses do not significantly add to the total energy consumption for the PM&F category. The Agency concludes that any increased energy use to comply with the NSPS is insignificant and that effluent reduction benefits outweigh the increased energy use.

SECTION XIII

PRETREATMENT STANDARDS

This section addresses pretreatment standards for existing sources (PSES) and pretreatment standards for new sources (PSNS). PSES and PSNS are applicable to PM&F process waters that are indirectly discharged (i.e., discharged to a POTW), pursuant to in Sections 307(b) and 307(c) of the Clean Water Act.

The Federal Water Pollution Control Act of 1972 stated that pretreatment standards shall prevent the discharge of any pollutant that may interfere with, pass through, or otherwise be incompatible with a POTW. The Clean Water Act of 1977 further stipulated that industrial discharges also must not interfere with the use and disposal of municipal sludges. The General Pretreatment Regulations for existing and new sources originally were published in the Federal Register (Vol. 43, No. 123; June 26, 1978) and can be found at 40 CFR Part 403. These regulations provide the general framework for categorical pretreatment standards. They describe the Agency's overall policy for establishing and enforcing categorical pretreatment standards for new and existing industrial dischargers and delineate the responsibilities and deadlines applicable to each party involved, including POTWs, States, and the involved industries. In cases where categorical pretreatment standards are not established because the Agency has determined that they are not warranted, indirect dischargers must still comply with the General Pretreatment Regulations - 40 CFR Part 403.

The remainder of this section describes the technical approach to developing PSES/PSNS for the PM&F category.

TECHNICAL APPROACH

The Agency examined the need for pretreatment standards in each of the PM&F subcategories. Specifically, the Agency considered whether the toxic pollutants discharged by the PM&F processes pass through a POTW. A pollutant is considered by the Agency to pass through a POTW when more of that pollutant can be removed by the application of BAT than can be removed by a POTW. If, for a particular pollutant, the average percentage removed nation-wide in well-operated POTWs meeting secondary treatment requirements is greater than the percentage removed by BAT, the pollutant does not pass through a POTW. Thus, a categorical pretreatment standard for that pollutant is not needed.

PRETREATMENT STANDARDS FOR EXISTING SOURCES

Contact Cooling and Heating Water Subcategory

For all pollutants except bis(2-ethylhexyl) phthalate, the Agency is not promulgating categorical PSES for this subcategory; PSES for bis(2-ethylhexyl) phthalate are being reserved pending further study. EPA has determined that the average percentage of toxic pollutant removals (ranging from 35 to 99 percent) nationwide by well-operated POTWs meeting secondary treatment requirements is greater than the percentage of toxic pollutant removals achieved by BAT (i.e., zero percent removals) in this subcategory. Therefore, the toxic pollutants do not pass through a POTW. Even though categorical pretreatment standards are not being promulgated, indirect dischargers in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

PSES for bis(2-ethylhexyl) phthalate are reserved pending proposal and promulgation of the BAT effluent limitations guidelines for that pollutant. When BAT is selected for that pollutant, EPA will determine if bis(2-ethylhexyl) phthalate passes through a POTW.

Cleaning Water Subcategory

EPA is not promulgating PSES for the cleaning water subcategory because the priority toxic pollutants found in cleaning waters in treatable concentrations (i.e., phenol and zinc) do not pass through a POTW. The Agency compared the percent removal of phenol and zinc (i.e., 75* percent and 62** percent, respectively) achieved by applying BAT to the average percentage removal of those pollutants nation-wide by well-operated POTWs

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*Percent removal was calculated based on the treatability limit from U.S. EPA's Treatability of Organic Priority Pollutants - Part C - Their Estimated (30-Day Ave.) Treated Effluent Concentration - A Molecular Engineering Approach, Murray P. Strier, July 11, 1978.

**Percent removal was derived from the treatability limit for zinc for the lime, settle and filtration technology listed in the U.S. EPA, Development Document for Effluent Limitations Guidelines and Standards for the Nonferrous Metals Manufacturing Point Source Category Phase II, July 1984.

meeting secondary treatment requirements (99† percent for phenol and 77† percent for zinc). Because the percent removals in a POTW are greater than the BAT percent removals, phenol and zinc do not pass through a POTW. Therefore, categorical pretreatment standards are not required for phenol and zinc. Even though no categorical pretreatment standards are being promulgated for existing sources for this subcategory, indirect dischargers must comply with the General Pretreatment Regulations - 40 CFR Part 403.

Finishing Water Subcategory

Except for three phthalates, the Agency is not promulgating categorical PSES for this subcategory for any pollutant; PSES for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved. EPA has determined that the average percentage of toxic pollutants removed nation-wide by well-operated POTWs meeting secondary treatment requirements (ranging from 35 to 99 percent) is greater than the average percent removal of toxic pollutants by direct dischargers applying BAT (i.e., zero percent removals). Therefore, the toxic pollutants do not pass through a POTW. Even though the Agency is not promulgating categorical pretreatment standards, indirect dischargers at existing sources in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

PSES for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved pending development of the BAT effluent limitations guidelines for those pollutants. When BAT is selected, EPA will determine if those three pollutants pass through a POTW.

PRETREATMENT STANDARDS FOR NEW SOURCES

Contact Cooling and Heating Water Subcategory

For all pollutants except bis(2-ethylhexyl) phthalate, the Agency is not promulgating categorical PSNS for the contact cooling and heating water subcategory; PSNS for bis(2-ethylhexyl) phthalate are reserved. The Agency believes that new and existing indirect discharge sources in this subcategory will discharge the same pollutants in similar amounts. As discussed in the preceding

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†POTW percent removals were obtained from Table 10, Fate of Priority Pollutants in Publicly Owned Treatment Works, Final Report, Volume 1, EPA-440/1-82/303, September 1982.

section, the average percentage of toxic pollutants removed nation-wide by well-operated POTWs meeting secondary treatment requirements (ranging from 35 to 99 percent) is greater than the average percent removal of toxic pollutants by direct dischargers applying BAT/NSPS (i.e., zero percent removals). Therefore, the toxic pollutants do not pass through a POTW. Even though the Agency is not promulgating categorical pretreatment standards at this time, indirect dischargers at new sources in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

The Agency believes that the concentrations of bis(2-ethylhexyl) phthalate in contact cooling and heating waters discharged from new indirect sources will be similar to the concentrations of that pollutant discharged from existing indirect sources. For this reason, the Agency is reserving PSNS for bis(2-ethylhexyl) phthalate until promulgation of NSPS for that pollutant. When NSPS are developed, EPA will determine if bis(2-ethylhexyl) phthalate passes through a POTW.

Cleaning Water Subcategory

The Agency is not promulgating categorical PSNS for this subcategory. The Agency believes that new and existing indirect discharging sources will discharge the same pollutants in similar amounts. As discussed in the preceding section, the average toxic pollutant percentage removed nation-wide by well-operated POTWs meeting secondary treatment requirements is greater than the percentage of toxic pollutant removals achieved by applying BAT. Therefore, the toxic pollutants do not pass through a POTW.

Even though new indirect dischargers are not subject to categorical pretreatment standards, they must comply with the General Pretreatment Regulations - 40 CFR Part 403.

Finishing Water Subcategory

Except for three phthalates, the Agency is not promulgating categorical PSNS for this subcategory for any pollutant; PSNS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate are reserved. The Agency believes that new and existing indirect discharge sources in this subcategory will discharging the same pollutants in similar amounts. As discussed in the preceding section, EPA has determined that the average percentage of toxic pollutants removed nation-wide by well-operated POTWs meeting secondary treatment requirements (ranging from 35 to 95 percent) is greater than the average percent removals achieved by applying BAT/NSPS (i.e., zero percent removals). Therefore, the toxic pollutants do not pass through a POTW. Even though the Agency is not promulgating categorical pretreatment standards, new source indirect dischargers in this subcategory must comply with the General Pretreatment Regulations - 40 CFR Part 403.

The Agency believes that the concentration of the three phthalates in finishing waters discharged from new indirect sources will be similar to the concentrations of those pollutants discharged from existing indirect sources. For this reason, the Agency is reserving PSNS for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate until NSPS for those pollutants are promulgated. When NSPS are developed, EPA will determine if the pollutants pass through a POTW.

SECTION XIV

BEST CONVENTIONAL POLLUTANT CONTROL TECHNOLOGY

This section defines the effluent limitations guidelines for the PM&F category based on the performance of the "best conventional pollutant control technology" (BCT). BCT effluent limitations guidelines are applicable to the discharge of conventional pollutants from existing industrial point sources, as established in Section 301(b)(2)(E) of the 1977 amendments to the Clean Water Act. Section 304(a)(4) designated the following as conventional pollutants: biochemical oxygen demand (BOD), total suspended solids (TSS), fecal coliform, pH, and any additional pollutants defined by the Administrator as conventional. The Administrator designated oil and grease a "conventional" pollutant on July 30, 1979 (44 FR 44501).

BCT effluent limitations guidelines are not additional limitations but replace BAT effluent limitations guidelines for the control of conventional pollutants. In addition to other factors specified in Section 304(b)(4)(B), the Act requires that BCT effluent limitations guidelines be assessed in light of a two part "cost-reasonableness" test. See, American Paper Institute v. EPA, 660 F.2d 954 (4th Cir. 1981). The first part of the test compares the cost for private industry to reduce its conventional pollutant concentrations with the cost publicly owned treatment works incur for similar levels of reduction. The second part of the test examines the cost-effectiveness of additional industrial wastewater treatment beyond BPT. EPA must find that the BCT effluent limitations guidelines are "reasonable" under both parts of the test before the BCT effluent limitations guidelines are established. In no case may the BCT effluent limitations guidelines be less stringent than the BPT effluent limitations guidelines.

EPA published its methodology for carrying out the BCT analysis on August 29, 1979 (44 FR 50732). In the case mentioned above, the Court of Appeals ordered EPA to make certain revisions. A revised methodology for the general development of BCT effluent limitations guidelines was proposed on October 29, 1982 (47 FR 49176). On September 20, 1984, the Agency issued a major notice of data availability for the BCT methodology (49 FR 37046). When the final BCT methodology is promulgated, EPA will use this methodology to determine whether BCT effluent limitations guidelines should be established for two of the three PM&F subcategories.

The Agency reviewed treatment technologies that could be used to remove additional conventional pollutants after BPT. For the contact cooling and heating water subcategory, EPA was unable to identify a technology that further reduces the concentrations of conventional pollutants found in contact cooling and heating waters. For this reason, the Agency is establishing BCT effluent limitations guidelines equal to the BPT effluent limitations guidelines for the contact cooling and heating water subcategory (presented in Table X-2). Because there are no technologies available to reduce conventional pollutants in contact cooling and heating waters, EPA has no reason to await promulgation of the final BCT methodology before promulgating BCT effluent limitations guidelines for this subcategory.

For both the cleaning water subcategory and the finishing water subcategory, the Agency has identified at least one technology (filtration) that can reduce the concentration of conventional pollutants remaining after the application of BPT. Therefore, EPA is reserving promulgation of BCT effluent limitations guidelines for those subcategories pending promulgation of the final BCT methodology. Once that methodology is promulgated, EPA will apply it to the costs and conventional pollutant removals associated with the filtration technology to determine if additional controls for conventional pollutants are justified for those two subcategories.

SECTION XV

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SECTION XVII

GLOSSARY

This section contains the definitions of the technical terms used in this document. Table XVII-1 lists some common plastic polymers and their uses and properties.

Acidity

The acidity of water is its quantitative capacity to react with a strong base to a designated pH. Various materials may contribute to the measured acidity depending on the method of determination. These materials include strong mineral acids, weak acids such as carbonic and acetic acids, and hydrolyzing salts such as ferrous or aluminum sulfates.

Alkalinity

Alkalinity of a water is its quantitative capacity to react with a strong acid to a designated pH. It is an indication of the concentration of carbonate, bicarbonate, and hydroxide ions present in the water.

Analytical Quantification Limit

The minimum concentration at which a pollutant can be accurately measured. It is also known as the method detection limit.

Average Process Water Usage Flow Rate

The average process water usage flow rate of a process in liters per day is equal to the volume of the process water (liters) used per year by a process divided by the number of days per year the process operates. The average process water usage flow rate for a plant with more than one plastics molding and forming process in a subcategory is the sum of the average process water usage flow rates for those plastics molding and forming processes.

Batch Treatment

Batch treatment is a waste treatment method where wastewater is collected over a period of time and then treated prior to discharge. Collection may be continuous even though treatment is not. Batch treatment may be used because the processes generating wastewater are operated on a batch operation mode, or the treatment system may be oversized for the amount of wastewater generated.

Table XVII-1

THE GLASS TRANSISTION AND MELTING TEMPERATURES OF SOME COMMON POLYMERS, AND THEIR MAIN USES*

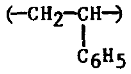
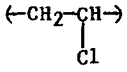
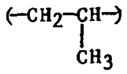
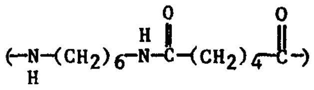
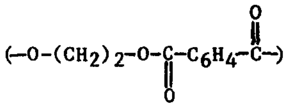
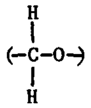
Polymer	Repeat Unit	Abbreviation	T_g (°C)	T_m (°C)	Main Uses
Linear polyethylene	$(-CH_2-CH_2-)$	HDPE	-110	134	Extruded and injection molded articles, bottles, and containers
Branched polyethylene	$(-CH_2-CH_2-)$	LDPE	-110	115	Flexible packaging film; flexible extruded and molded articles
Polystyrene	 $(-CH_2-\underset{C_6H_5}{\underset{\vert}{CH}}-)$	PS	90-100	---	Extruded and molded articles that are transparent; foamed articles
Polyvinylchoride	 $(-CH_2-\underset{Cl}{\underset{\vert}{CH}}-)$	PVC	87	---	Extruded rigid or plasticized articles, tubes, sheets, profiles
Polypropylene	 $(-CH_2-\underset{CH_3}{\underset{\vert}{CH}}-)$	PP	-10	165	Extruded and molded articles that are rigid
Nylon 6-6	 $(-\underset{H}{N}-(CH_2)_6-\overset{H}{N}-\overset{O}{\overset{\Vert}{C}}-(CH_2)_4-\overset{O}{\overset{\Vert}{C}}-)$	--	50	240	Fibers; molded and extruded rigid articles
Polyethylene terephthalate	 $(-O-(CH_2)_2-O-\underset{O}{\underset{\Vert}{C}}-C_6H_4-\overset{O}{\overset{\Vert}{C}}-)$	PET	70	260	Fibers and transparent strong films
Polyoximethylene	 $(-\overset{H}{\overset{\vert}{\underset{H}{\underset{\vert}{C}}}}-O-)$	Acetal	-50	180	Molded "engineering" structural components; tough

Table XVII-1 (Continued)

THE GLASS TRANSISTION AND MELTING TEMPERATURES OF SOME COMMON POLYMERS, AND THEIR MAIN USES*

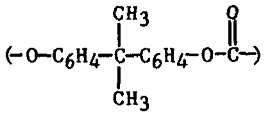
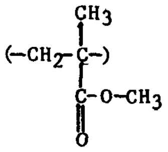
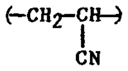
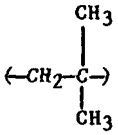
Polymer	Repeat Unit	Abbreviation	T_g (°C)	T_m (°C)	Main Uses
Polycarbonate	 $(-O-C_6H_4-\overset{CH_3}{\underset{CH_3}{C}}-C_6H_4-O-\overset{O}{\overset{\Vert}{C}}-)$	PPO	150	---	Molded tough and transparent articles; structural components
Polymethylmethacrylate	 $(-CH_2-\overset{CH_3}{\underset{\underset{\underset{O}{\Vert}}{C-O-CH_3}}{C}}-)$	PMMA	90-100	---	Cast transparent sheet; molded articles
Polytetrafluoroethylene	$(-CF_2-CF_2-)$	Teflon, PTFE	125	327	"Extruded" tubes; sintered blocks for machining; tapes; solvent resistant
Polyacrylonitrile	 $(-CH_2-\underset{CN}{CH}-)$	PAN	105	>250	High strength fibers
Polyisobutylene	 $(-CH_2-\overset{CH_3}{\underset{CH_3}{C}}-)$	PIB	-70	---	Adhesives, paper coatings; together with isoprene, butyl rubber
Polybutadiene	$(-CH_2-CH=CH-CH_2-)$	---	-88	---	Styrene-butadiene rubber (SBR); nitrile rubbers (with PAN); oil resistant

*Table is from Principles of Polymer Processing, Tadmor Z, Gogos C. G., John Wiley and Sons, 1979, pp. 38-39.

Biological Oxygen Demand (BOD$_5$)

The biological oxygen demand test for wastewaters determines the oxygen required for the biochemical degradation of organic material (carbonaceous demand) and the oxygen used to oxidize inorganic material such as sulfides and ferrous iron. The wastewater sample is incubated for a standard period of five days, hence the name BOD$_5$.

Blowing Agent

A blowing agent is the material injected into a plastic material that causes the plastic material to expand with the application of heat. Blowing agents can be gases introduced into the molten plastic or a gas producing compound that is mixed with the polymer before processing.

Blow Molding

Blow molding expands a parison into a desired shape with compressed air. Hollow, thin-wall objects from thermoplastic resins are formed.

Calendering Process

The calendering process squeezes pliable thermoplastic between a series of rolls to produce uniform quality polymer film and sheet, to emboss sheet and film, to perform compounding operations, and to coat textiles and papers.

Casting Process

A casting process forms products by allowing a liquid plastic to cure at atmospheric pressure in a mold or on a mold surface.

Chemical Oxygen Demand (COD)

The chemical oxygen demand is a measure of the oxygen equivalent of the organic matter in a wastewater sample that is susceptible to oxidation by a strong chemical oxidant.

Cleaning Process

A cleaning process is a process in which surfaces of plastic products and shaping equipment surfaces that contact the plastic product are washed to remove residual mold release agents and other matter prior to finishing or further processing. A cleaning process contains a detergent wash cycle and a rinse cycle.

Cleaning Water

Cleaning water is process water used to clean the surfaces of an intermediate or final plastic product or to clean the surfaces of equipment used in plastic molding and forming that contacts an intermediate or final product. It includes water used in both the detergent wash and rinse cycles of a cleaning process.

Coating Process

A coating process covers objects with a polymer layer that is in the form of a melt, liquid, or finely divided powder. These objects that are coated include other plastic materials, metal, wood, paper, fabric, leather, glass, concrete, and ceramics.

Compounding

Compounding is the plastics processing step where a plastic resin is mixed with additives or fillers.

Compression Molding

Compression molding shapes a measured quantity of plastic within a mold by applying heat and pressure to form products with large surface areas and relatively simple shapes.

Contact Cooling and Heating Water

Contact cooling and heating water is process water that contacts the raw materials or plastic product for the purpose of heat transfer during plastic molding and forming.

Conventional Pollutants

Conventional pollutants are the pollutants defined in Section 304(a)(4) of the Clean Water Act. They include biological oxygen demand, oil and grease, suspended solids, fecal coliform, and pH.

Cooling Trough

A cooling trough is a long open box-like container that holds water to quench a processed plastic product. It is commonly used to contact cool extruded strands before they are pelletized and to cool extruded pipe.

Crude Intermediate Plastic Material

Crude intermediate plastic material is plastic material formulated in an on-site polymerization process.

Direct Discharger

A direct discharger is an industrial water user that discharges wastewater directly to a navigable stream.

Dry Process

A dry process is a process that uses no proces water or uses only non-contact cooling water.

Effluent

Effluent is the discharge from a point source after treatment.

End-of-Pipe Treatment

End-of-pipe treatment is the treatment given wastewater before the wastewater is discharged.

Extrusion Process

Extrusion is a process that forces molten polymer under pressure through a shaping die to produce products of uniform cross-sectional area such as pipe, tubing, sheet, and film.

Filler

A filler is a material that when added to a plastic may reduce the end product cost by occupying a fraction of the volume of the plastic product. It may also act as a speciality additive to improve the final product.

Finishing Process

A finishing process renders the plastic parts useful. There are three types of finishing processes: machining, decorating, and assembling.

Finishing Water

Finishing water is process water used to remove waste plastic material generated during a finishing process or to lubricate a plastic product during a finishing process. It includes water used to machine and to assemble intermediate or final plastic products.

Foaming Agent

A foaming agent is a gas producing compound added to a polymer that causes the polymer to foam when the gas is liberated by the addition of heat or a reduction in pressure.

Foaming Process

A foaming process injects a blowing or foaming agent into a thermoplastic or thermoset to form a sponge-like material.

Glass Transition Temperature

The temperature at which a polymer changes from a brittle glassy solid to a rubber-like substance.

Indirect Discharger

An indirect discharger is an industrial source that discharges wastewater to a publicly owned treatment works.

Influent

Influent is water used in a PM&F process. It can be the source water for a plant or the source water combined with recycled water.

Injection Molding

Injection molding forms intricate plastic parts by forcing a heated plastic material into a mold cavity.

In-Process Control Technology

In-process control technology is the conservation of water throughout the production processes to reduce the amount of wastewater discharged.

Integrated Plant

An integrated plant is a plant that combines process water from all sources in the plant for treatment in a central wastewater treatment system.

Laminating Process

The laminating process combines layers of plastic materials with other materials through high pressure. These structures are formed from layers of resins and fillers bonded together as a unit with the resin used as a reinforcing agent.

Mass of Pollutant That Can Be Discharged

The mass of pollutant that can be discharged is the pollutant mass calculated by multiplying the allowable pollutant effluent concentration times the average process water usage flow rate.

Melt Temperature

The temperature at which a polymer becomes fluid.

Monomer

A monomer is a chemical compound that during a polymerization process becomes a repeating link in the polymer chain.

New Source Performance Standards (NSPS)

NSPS for new industrial direct dischargers as defined by Section 306 of the Clean Water Act are based on the best available demonstrated technology.

Nonconventional Pollutants

Nonconventional pollutants include pollutants that are not designated as either conventional pollutants or priority toxic pollutants.

Oil and Grease

Oil and grease are materials that are soluble in trichlorotrifluoroethane. They include nonvolatilized materials usch as hydrocarbons, fatty acids, soaps, fats, waxes, and oils.

Parison

A parison is a preshaped sleeve usually made by extrusion. This sleeve is an intermediate product often used as the starting material for the blow molding process.

Pelletizing

Pelletizing is a process by which long extruded strands are cut into pellets. These pellets are an intermediate product which can be the feed material for other plastic molding and forming processes.

pH

pH is the negative logarithm of the hydronium ion concentration. Values below seven represent an acid environment; a value of seven represents a neutral environment; and values greater than seven are indicative of a basic environment.

Pigments

A pigment is a compound that when well mixed with a polymer imparts color to the polymer. To impart color, the pigment must absorb light in the visible wavelength range.

Plastic Material

A plastic material is a synthetic organic polymer (i.e., a thermoset polymer, a thermoplastic polymer, or a combination of a natural polymer and a thermoset or thermoplastic polymer) that is solid in its final form and that was shaped by flow. The material can be either a homogeneous polymer or a polymer combined with fillers, plasticizers, pigments, stabilizers, or other additives.

Plasticization - Internal

A copolymerization process by which a chain is made more flexible. The chain's rigidity is caused by steric factors.

Plasticizer - External

An external plasticizer is usually a monomeric molecule that when mixed with polar or hydrogen bonded polymer results in increasing the flexibility of the rigid polymer.

Plastics Molding and Forming (PM&F) Processes

Plastic molding and forming processes are a group of manufacturing processes in which plastic materials are blended, molded, formed, or otherwise processed into intermediate or final plastic products.

Plastisol

A plastisol is a low viscosity system of dispersed polyvinyl chloride (PVC) in a plasticizer.

PM&F Category

Throughout this document, the PM&F abbreviation stands for the Plastics Molding and Forming category.

Pollutant Concentration

A measure of the mass of pollutant per volume of wastewater. Commonly used units are milligrams per liter.

Pollutant Effluent Limitations Guidelines

The pollutant effluent limitations guidelines is the mass of pollutant allowed to be discharged per unit of time. For the PM&F category, typical units are milligrams of pollutant per day. The pollutant mass is calculated by multiplying the effluent concentration times the average process water usage flow rate.

Polymer

A polymer is a macromolecule comprised of linked together repeating monomers. These macromolecules have molecular weights in the range of 10^4 to 10^7.

Polymerization

Polymerization is the chemical reaction that produces a polymer.

Priority Toxic Pollutants

Priority toxic pollutants are toxic pollutants selected for study from 65 compounds and classes of compounds Congress declared toxic under Section 307(a) of the Clean Water Act.

Process Water

Process water is any raw, service, recycled, or reused water that contacts the plastic product or contacts shaping equipment surfaces such as molds and mandrels that are, or have been, in contact with the plastic product.

Publicly Owned Treatment Works (POTW)

A POTW is a wastewater treatment facility owned by a state or municipality.

Reaction Injection Molding (RIM)

A RIM process simultaneously injects two or more reactive liquid streams at high pressure into a mixing chamber and then injects the plastic at a lower pressure into the mold cavity.

Recycle

Recycle is a water-saving technology that returns process water that has been used in a process to that process.

Regrind

Regrind is processed plastic that is scrapped and mixed with pure plastic and reprocessed.

Reinforcing Agent

A reinforcing agent primarily improves the strength and stiffness of the base polymer.

Resin

A resin is the homogeneous polymer that forms the basis of a plastic product. The resin does not include fillers, plasticizers, pigments or stabilizers.

Rotational Molding

A rotational molding process rotates a polymer powder or liquid inside a large, heated mold to form hollow objects from thermoplastic materials.

Sprue

The sprue is the entrance into the mold through which the plastic flows.

Stabilizer

A stabilizer is a compound that when added to a polymer protects it from heat, light, or oxygen.

Thermoforming Process

A thermoforming process heats a thermoplastic sheet or film to a pliable state and forces it around the contours of a mold. Vacuum, air pressure, or mechanical force form the molten sheet to the mold.

Thermoplastic Polymer

A thermoplastic polymer is a linear molecule that can melt and flow with the addition of heat and pressure.

Thermoset Polymer

A thermoset polymer has crosslinks throughout the chain making it stable to heat. The polymer will not melt or flow with heat.

Total Organic Carbon (TOC)

TOC is a measure of the organic material in a wastewater and is determined by oxidizing the organic material to carbon dioxide.

Total Phenols

Phenols are hydroxy derivatives of benzene.

Total Suspended Solids (TSS)

TSS is a measure of the solids in wastewater.

Transfer Molding

Transfer molding uses a preheated plastic material and moves it into the mold cavity with pressure through a sprue. It is similar to injection molding.

Treatability Limit

The treatability limit is the lowest concentration of a pollutant achievable by a wastewater treatment process.

Volume of Process Water Used Per Year

The volume of process water used per year is the volume of process water that flows through a process and comes in contact with the plastic product over a period of one year.

Wastewater Discharged

Wastewater discharged is process water from a PM&F process that is discharged to a navigable stream or a POTW.

Water Quench

A water quench is a contact water cooling bath used to quickly cool a material. It is often used in extrusion and injection molding to cool the products.

Water Used

Water used is water that contacts the plastic material or product. This includes any recycle and makeup water.

Wet Process

A wet process is a process in which the plastic product comes into direct contact with water.

Zero Discharger

A zero discharger is any industrial water user that does not discharge wastewater.

APPENDIX A

SAMPLING DATA

APPENDIX A

SAMPLING DATA

This appendix presents the daily concentration data for the 18 PM&F plants sampled for the final PM&F regulation. Table A-1 lists the data for the contact cooling and heating water subcategory; Table A-2 lists the data for the cleaning water subcategory; and Table A-3 presents the data for the finishing water subcategory. The concentration values for the source water sample, for process samples collected on days one, two, and three and for the duplicate samples listed in Tables A-1, A-2, and A-3 were used to develop the average concentrations presented in Table VI-19.

Processes from Plant K in Tables A-1 and A-2 have two source water concentrations listed. The first value listed represents the concentration of a make-up water flow and the second value represents a recirculated water flow to the process. Some pollutants for process K-4 from Plant K have two concentration values listed under each sampling day. The first concentration is from an unpreserved sample and the second listed value is from a preserved sample.

Wastewater treatment processes that treat primarily PM&F process waters were sampled at one plant (i.e., Plant I) in 1980. Tables A-4 and A-5 present influent and effluent data for two treatment processes at that plant (see Figure VI-9). Wastewater treatment processes that treat primarily PM&F process waters were also sampled at three plants in 1984. Refer to Tables A-6, A-7, and A-8 for influent and effluent data for these treatment processes at plants M, N, and R, respectively (see Figures VI-12, VI-13, and VI-17).

Table A-9 presents solution casting solvent recovery sampling data for Plant G. Data presented in Table A-9 may be used as a guide by the permit writer to write permits for the solvent recovery wastewater. This wastewater is not regulated by the plastics molding and forming effluent limitations guidelines and standards.

Table A-1

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD$_5$)	B-1	1	<5	<5			
	B-2	1	<5	<5			
	B-4	1	<5	<5			<5
	C-1	1	83.8	96.9	84.8	90.9	
	D-3	1	NA	NA			
	E-2	1	5.0	9.4	8.9	4.1	
	E-3	1	5	7.6	3.9	0.5	
	F-1	1	2	10	8	10	
	F-2	1	2	8	7	7	
	F-6	1	2		5	3	
	G-1	3	<5	††	††		
	J-1	2	<5	<5			
	J-2	2	<5	56			52
	K-2	3/1	<5/<5	<5	<5	<5	
	K-3	3/1	<5/<5	<5	<5	<5	<5
	K-4	3/1	<5/<5	<5	<5	<5	
	M-1	1	38	130			
	M-2	1	18	18			
	N-2	1	5.0	10			
	N-3	2	5.0		6		
	O-1	2	NA	NA			
	O-2	2	NA	NA			
	P-1	2	8.5	2.3			
	R-1	2	4	6			
	R-2	2	4	4			

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants (Continued)							
oil and grease	B-1	2	<4	<4			
	B-2	2	<4	<4			
	B-4	2	<4	4			10
	C-1	1	17.0	75.0	24.5	41.0	
	D-3	2	<4	<4			<4
	E-2	1	19.6	16.8	23.8	11.8	
	E-3	1	19.6	20.0	27.8	19.4	
	F-1	1	3	1	0	4	
	F-2	1	3	3	0	5	
	F-6	1	3		5	4	
	G-1	2	6	<4	4		
	J-1	2	<4	11			
	J-2	2	<4	73			49
	K-2	2	<4/<4	<4	<4	<4	
	K-3	2	<4/<4	<4	<4	<4	<4
	K-4	2	<4/<4	<4	<4	<4	
	M-1	1	<1	31			
	M-2	1	74	29			
	N-2	1	<1	5			
	N-3	1	<1		3		
	O-1	1	9	5			
	O-2	1	9	3			
	P-1	1	3	3			
	R-1	1	7	6			
	R-2	1	7	8			

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants (Continued)							
pH	B-1	1	5.6	5.7			
	B-2	1	5.6	5.5			
	B-4	1	5.6	5.8			5.8
	C-1	3	5.8	5.4	6.65	6.0	
	D-3	1	7.3	7.8			
	E-2	3	6.55	6.5	6.6	6.5	
	E-3	3	6.55	6.35	6.51	6.41	
	F-1	3	7.6	7.65	7.7	7.65	
	F-2	3	7.6	8.0	7.6	7.55	
	F-6	3	7.6		7.6	7.55	
	G-1	3	7.4	7.7	7.6		
	J-1	2	8.55	8.3			
	J-2	2	8.55	8.2			8.2
	K-2	3	8.0/8.0	8.2	8.3	7.9	
	K-3	3	8.0/8.0	8.0	7.9	8.0	7.9
	K-4	3	8.0/8.0	8.0	7.9	8.0	
	M-1	1	7.57	7.86			
	M-2	1	7.83	7.85			
	N-2	1	8.32	7.19			
	N-3	2	8.32		8.3		
	O-1	2	6.7	6.93			
	O-2	2	6.7	6.69			
	P-1	2	7.51	7.38			
	R-1	2	7.35	7.21			
	R-2	2	7.35	7.36			

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants (Continued)							
total suspended solids (TSS)	B-1	1	<4	<4			
	B-2	1	<4	<4			
	B-4	1	<4	4			<4
	C-1	3	0	104	77.0	18.0	
	D-3	1	<4	<4			<4
	E-2	3	1	3	4	2	
	E-3	3	1	4	2	3	
	F-1	3	2	6	3	5	
	F-2	3	2	<1	2	1	
	F-6	3	2		1	<1	
	G-1	3	16	22	4		
	J-1	2	<4	4			
	J-2	2	<4	36			38
	K-2	3	<4/6	6	4	<4	
	K-3	3	<4/<4	<4	<4	<4	<4
	K-4	3	<4/4	4	<4	4	
	M-1	1	<1	5			
	M-2	1	9	4			
	N-2	1	3	<1			
	N-3	2	3		<1		
	O-1	2	<1	<1			
	O-2	2	<1	<1			
	P-1	2	<1	2			
	R-1	2	<1	<1			
	R-2	2	<1	<1			

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants							
aluminum	B-1	1	0.100	0.800			
	B-2	1	0.100	ND			
	B-4	1	0.100	0.500			
	C-1	3	ND	0.310	0.200	0.041	
	D-3	1	0.11	0.073			
	E-2	3	0.155	0.047	0.126	0.036	
	E-3	3	0.155	0.040	0.022	ND	
	F-2	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.662	0.513		
	J-1	2	ND	0.163			
	J-2	2	ND	0.235			
	K-2	3/1	ND/0.200	0.100	0.100	0.100	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/0.1	ND	ND	0.1	
ammonia nitrogen	B-1	1	0.06	0.06			
	B-2	1	0.06	<0.05			
	B-4	1	0.06	<0.05			<0.05
	C-1	3	0	0	8.4	1.68	
	D-3	1	<0.05	<0.05			<0.05
	E-2	3	<0.05	<0.05	<0.05	0.09	
	E-3	3	<0.05	0.39	<0.05	<0.05	
	F-1	3	3.3	0.61	3.1	1.1	
	F-2	3	3.3	1.1	2.4	0.7	
	F-6	3	3.3		6.4	1.8	
	G-1	3	<0.05	<0.05	<0.05		
	J-1	2	<0.05	0.05			
	J-2	2	<0.05	0.05			0.05
	K-2	3	<0.05/0.24	0.10	0.12	0.14	
	K-3	3	<0.05/<0.05	<0.05	<0.05	<0.05	<0.05
	K-4	3	<0.05/<0.05	<0.05	<0.05	<0.05	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
barium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.190	0.180	0.180	
	D-3	1	0.034	0.035			
	E-2	3	0.014	0.020	0.035	0.016	
	E-3	3	0.014	0.014	0.014	0.015	
	F-1	3	0.043	0.063	0.085	0.100	
	F-2	3	0.043	0.052	0.088	0.110	
	F-6	3	0.043		0.14	0.17	
	G-1	3	ND	0.040	0.018		
	J-1	2	0.030	0.012			
	J-2	2	0.030	0.016			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
boron	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	ND	ND	0.030	
	D-3	1	0.050	0.038			
	E-2	3	0.207	0.016	0.007	ND	
	E-3	3	0.207	ND	0.013	0.029	
	F-1	3	0.051	0.17	0.13	0.12	
	F-2	3	0.051	0.060	0.110	0.065	
	F-6	3	0.051		0.065	0.047	
	G-1	3	ND	0.103	0.01		
	J-1	2	0.174	0.169			
	J-2	2	0.174	0.150			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
bromide	B-1	1	<0.4	<0.4			
	B-2	1	<0.4	<0.4			
	B-4	1	<0.4	<0.4			<0.4
	C-1		NA	NA	NA	NA	
	D-3	1	<0.4	<0.4			<0.4
	E-2		NA	NA	NA	NA	
	E-3		NA	NA	NA	NA	
	F-1		NA	NA	NA	NA	
	F-2		NA	NA	NA	NA	
	F-6		NA		NA	NA	
	G-1	3	0.56	0.55	0.8		
	J-1	2	<0.4	<0.4			
	J-2	2	<0.4	<0.4			<0.4
	K-2	3/1	<0.4/<0.4	<0.4	<0.4	<0.4	
	K-3	3/1	<0.4/<0.4	<0.4	<0.4	<0.4	<0.4
	K-4	3/1	<0.4/<0.4	<0.4	<0.4	<0.4	
calcium	B-1	1	2.100	2.900			
	B-2	1	2.1	2.5			
	B-4	1	2.100	2.000			
	C-1	3	6.840	11.500	11.100	10.400	
	D-3	1	21.4	16.1			
	E-2	3	9.52	9.39	9.32	8.9	
	E-3	3	9.52	9.33	9.32	9.09	
	F-1	3	33.2	48.8	73.8	90.7	
	F-2	3	33.2	38.1	75.6	93.6	
	F-6	3	33.2		87.8	90.8	
	G-1	3	0.062	394	406		
	J-1	2	25.850	16.400			
	J-2	2	25.850	17.900			
	K-2	3/1	20.4/23.8	22.2	22.9	25.6	
	K-3	3/1	20.4/20.7	20.4	20.9	20.3	
	K-4	3/1	20.4/23	19.9	20.8	21.7	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
chemical oxygen demand (COD)	B-1	1	<5	<5			
	B-2	1	<5	7			
	B-4	1	<5	<5			<5
	C-1	3	0	377.2	322.4	352.8	
	D-3	1	<5	10			14
	E-2	3	30	72.1	29.7	25.4	
	E-3	3	30	55.1	25.4	4.2	
	F-1	3	8294	645	35	81	
	F-2	3	8294	588	31	111	
	F-6	3	8294		53	461	
	G-1	3	<5	415	280		
	J-1	2	15.5	60			
	J-2	2	15.5	122			125
	K-2	3/1	<5/<5	51	12	36	
	K-3	3/1	<5/<5	192	<5	5	<5
	K-4	3/1	<5/<5	40	<5	7	
	M-1	1	90	800			
	M-2	1	46	47			
	N-2	1	20	30			
	N-3	2	20		40		
	O-1	2	60	50			
	O-2	2	60	48			
	P-1	2	90	<10			
	R-1	2	16	16			
	R-2	2	16	20			
cobolt	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.043	0.032	0.028	
	D-3	1	ND	ND			
	E-2	3	ND	0.136	0.142	0.084	
	E-3	3	ND	0.136	0.115	0.060	
	F-1	3	ND	ND	ND	ND	
	F-2	1	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.051	0.058		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
cyanide (amenable)	B-1		NA	NA			
	B-2		NA	NA			
	B-4		NA	NA			NA
	C-1	1	0	0	0	0	
	D-3		NA	NA			
	E-2	1	<0.005	<0.005	<0.005	<0.005	
	E-3	1	<0.005	<0.005	<0.005	<0.005	
	F-1	1	0	0	0	0	
	F-2	1	0	0	0	0	
	F-6	1	0		0	0	
	G-1		NA/NA	NA	NA	NA	
	J-1		NA	NA			
	J-2	2	NA	NA			NA
	K-2		NA/NA	NA	NA	NA	
	K-3		NA/NA	NA	NA	NA	NA
	K-4		NA/NA	NA	NA	NA	
fluoride	B-1	1	1.2	0.85			
	B-2	1	1.2	0.88			
	B-4	1	1.2	0.91			0.95
	C-1		NA	NA	NA	NA	
	D-3	1	0.95	0.95			1.25
	E-2		NA	NA	NA	NA	
	E-3		NA	NA	NA	NA	
	F-1		NA	NA	NA	NA	
	F-2		NA	NA	NA	NA	
	F-6		NA		NA	NA	
	G-1	3	0.46	0.08	0.18		
	J-1	2	0.595	0.54			
	J-2	2	0.595	0.36			0.48
	K-2	3	0.81/1.18	1.02	1.04	1.04	
	K-3	3	0.81/0.73	0.78	0.72	0.80	0.73
	K-4	3	0.81/1.12	1.05	0.95	1.2	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
iron	B-1	1	0.300	0.400			
	B-2	1	0.3	0.45			
	B-4	1	0.300	0.500			
	C-1	3	0.140	9.850	9.450	1.640	
	D-3	1	ND	0.066			
	E-2	3	0.094	0.112	0.172	0.110	
	E-3	3	0.094	0.132	0.126	0.094	
	F-1	3	0.036	0.47	0.37	0.074	
	F-2	3	0.036	0.064	0.19	0.30	
	F-6	3	0.036		0.038	ND	
	G-1	3	ND	0.090	0.052		
	J-1	2	ND	ND			
	J-2	2	ND	0.054			
	K-2	3/1	ND/1.05	0.85	0.80	0.75	
	K-3	3/1	ND/0.4	0.25	0.35	0.35	
	K-4	3/1	ND/0.2	0.3	0.1	0.15	
Kjeldahl nitrogen	B-1	1	<1	<1			
	B-2	1	<1	<1			
	B-4	1	<1	<1			<1
	C-1	3	0	0	0	0	
	D-3	1	<1	<1			<1
	E-2	3	<0.1	<0.1	0.1	0.22	
	E-3	3	<0.1	0.63	<0.1	<0.1	
	F-1	3	<0.02	<0.02	0.45	<0.02	
	F-2	3	<0.02	1.15	<0.02	<0.02	
	F-6	3	<0.02		0.35	0.45	
	G-1	3	<1	<1	<1		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	<1/<1	<1	<1	<1	
	K-3	3	<1/<1	<1	<1	<1	<1
	K-4	3	<1/<1	<1	<1	<1	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
magnesium	B-1	1	0.700	0.900			
	B-2	1	0.7	0.8			
	B-4	1	0.700	0.700			
	C-1	3	1.240	2.120	2.060	1.870	
	D-3	1	5.66	4.83			
	E-2	3	2.36	2.46	2.58	2.42	
	E-3	3	2.36	2.54	2.55	2.6	
	F-1	3	13.3	19.8	23.4	28.6	
	F-2	3	13.3	17.2	24.8	29.8	
	F-6	3	13.3		28.5	29.4	
	G-1	3	0.181	24.3	25.5		
	J-1	2	3.215	2.290			
	J-2	2	3.215	2.500			
	K-2	3/1	5.8/6.4	5.9	6.1	6.8	
	K-3	3/1	5.8/5.6	5.5	5.7	5.5	
	K-4	3/1	5.8/6.1	5.6	5.9	5.9	
manganese	B-1	1	ND	0.050			
	B-2	1	ND	ND			
	B-4	1	ND	0.050			
	C-1	3	0.072	0.210	0.210	0.160	
	D-3	1	0.008	0.006			
	E-2	3	0.011	0.035	0.039	0.040	
	E-3	3	0.011	0.032	0.044	0.032	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.029	0.032		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
molybdenum	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	ND	0.021	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	0.045	ND	
	E-3	3	ND	0.044	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/0.150	ND	0.15	0.15	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
nitrate	B-1	1	<0.1	<0.1			
	B-2	1	<0.1	0.1			
	B-4	1	<0.1	<0.1			<0.1
	C-1		NA	NA	NA	NA	
	D-3	1	2.0	2.1			2.1
	E-2		NA	NA	NA	NA	
	E-3		NA	NA	NA	NA	
	F-1		NA	NA	NA	NA	
	F-2		NA	NA	NA	NA	
	F-6		NA		NA	NA	
	G-1	3	5.8	6.6	6.0		
	J-1	2	1.05	0.35			
	J-2	2	1.05	0.40			0.40
	K-2	3	1.05/1.4	0.75	1.35	1.35	
	K-3	3	1.05/0.70	0.75	0.75	0.70	0.70
	K-4	3	1.05/1.2	1.1	1.1	1.15	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
sodium	B-1	1	1.800	2.100			
	B-2	1	1.8	2.1			
	B-4	1	1.800	1.800			
	C-1	3	11.400	18.600	18.900	17.400	
	D-3	1	26.2	22.3			
	E-2	3	10.8	10.8	8.71	10.7	
	E-3	3	10.8	10.7	8.82	11.2	
	F-1	3	177	169.0	119.0	91.4	
	F-2	3	177	170	117	88.9	
	F-6	3	177.0		97.2	86.5	
	G-1	3	ND	18.8	207		
	J-1	2	70.400	58.000			
	J-2	2	70.400	53.900			
	K-2	3/1	8.1/10.2	8.6	9.2	10.5	
	K-3	3/1	8.1/7.5	7.3	7.6	7.4	
	K-4	3/1	8.1/9.3	8.1	8.7	8.8	
sulfate	B-1	1	9	5			
	B-2	1	9	10			
	B-4	1	9	<5			<5
	C-1		NA	NA	NA	NA	
	D-3	1	33	33			30
	E-2		NA	NA	NA	NA	
	E-3		NA	NA	NA	NA	
	F-1		NA	NA	NA	NA	
	F-2		NA	NA	NA	NA	
	F-6		NA		NA	NA	
	G-1	3	1040	1180	890		
	J-1	2	33	25			
	J-2	2	33	25			25
	K-2	2	10/15	11	15	15	
	K-3	2	10/11	10	11	10	11
	K-4	2	10/12	10	<5	11	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate	Average
Nonconventional Pollutants (Continued)								
sulfide	B-1	1	<1	<1				
	B-2	1	<1	<1				
	B-4	1	<1	<1			<1	
	C-1		NA	NA	NA	NA		
	D-3	1	NA	NA				
	E-2		NA	NA	NA			
	E-3		NA	NA	NA			
	F-1		NA	NA	NA	NA		
	F-2		NA	NA	NA	NA		
	F-6		NA		NA	NA		
	G-1	1	<1	<1	<1			
	J-1	2	<1	<1				
	J-2	2	<1	<1			<1	
	K-2	1	<1/<1	<1	<1	<1		
	K-3	1	<1/<1	<1	<1	<1	<1	
	K-4	1	<1/<1	<1	<1	<1		
surfactants	B-1	1	<0.01	<0.01				
	B-2	1	<0.01	<0.01				
	B-4	1	<0.01	<0.01			<0.01	
	C-1	3	0.08	28.86	25.7	16.09		
	D-3		NA	NA				
	E-2	3	0.12	0	0.10	0		
	E-3	3	0.12	0	0	0.11		
	F-1	3	<0.02	6	3.3	8		
	F-2	3	<0.02	0.02	0.05	0.07		
	F-6	3	<0.02		0.02	<0.02		
	G-1	3	<0.01	<0.01	0.10			
	J-1	2	<0.015	0.045				
	J-2	2	<0.015	0.032			0.057	
	K-2	3	<0.01/ 0.01	<0.01	0.02	<0.01		
	K-3	3	<0.01/ 0.01	<0.01	<0.01	<0.01	<0.01	
	K-4	3	<0.01/ 0.01	<0.01	0.03	<0.01		

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
tin	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.012	ND	ND	
	D-3	1	ND	ND			
	E-2	3	0.051	0.043	0.058	0.052	
	E-3	3	0.051	0.032	0.042	0.042	
	F-1	3	ND	0.12	0.080	0.050	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
titanium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	0.087	0.290	0.290	0.100	
	D-3	1	0.013	0.017			
	E-2	3	ND	0.006	0.009	ND	
	E-3	3	ND	ND	0.005	ND	
	F-1	3	0.130	0.12	0.085	0.039	
	F-2	3	0.13	0.096	0.094	0.053	
	F-6	3	0.13		0.097	0.063	
	G-1	3	0.010	0.023	0.036		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
total dissolved solids (TDS)	B-1		NA	NA			
	B-2		NA	NA			
	B-4		NA	NA			NA
	C-1	3	0	150.0	140.0	110	
	D-3		NA	NA			
	E-2	3	7	103	89	68	
	E-3	3	7	98	73	66	
	F-1	3	800	700	700	500	
	F-2	3	800	800	700	400	
	F-6	3	800		700	400	
	G-1		NA	NA	NA		
	J-1		NA	NA			
	J-2		NA	NA			NA
	K-2		NA/NA	NA	NA	NA	
	K-3		NA/NA	NA	NA	NA	NA
	K-4		NA/NA	NA	NA	NA	
total organic carbon (TOC)	B-1	1	6	7			
	B-2	1	6	7			
	B-4	1	6	6			6
	C-1	1	3.0	48.0	40.5	29.5	
	D-3	1	2	6			4
	E-2	1	8.9	16	10.0	6.4	
	E-3	1	8.9	16.4	8.1	1.0	
	F-1	1	37	27	66	65	
	F-2	1	37	64	63	64	
	F-6	1	37		61	59	
	G-1	3	<1	144	88		
	J-1	2	6.5	21			
	J-2	2	6.5	46			46
	K-2	3	3.0/4	30	8	14	
	K-3	3	3/0/1	72	3	4	2
	K-4	3	3.0/2	26	5	4	
	M-1	1	<1	24			
	M-2	1	30	13			
	N-2	1	10	14			
	N-3	2	10		10		
	O-1	2	<1	<1			
	O-2	2	<1	<1			
	P-1	2	<1	18			
	R-1	2	6	6			
	R-2	2	6	5			

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
total phenols	B-1	1	<0.020	<0.020			
	B-2	1	<0.02	<0.02			
	B-4	1	<0.020	<0.020			<0.020
	C-1	1	1.42	1.08	16.42	20.86	
	D-3	1	<0.001	<0.001			<0.001
	E-2	1	<0.001	<0.001	<0.001	<0.001	
	E-3	1	<0.001	<0.001	<0.001	<0.001	
	F-1¶	1	10	36	81	238	
	F-2¶	1	10	<5	13	15	
	F-6¶	1	10		1670	108	
	G-1	2	0.023	0.100	0.220		
	J-1	2	<0.020	<0.020			
	J-2	2	<0.020	<0.020			<0.020
	K-2	2	<0.001/0.01	<0.001	0.008	0.023	
	K-3	2	<0.001/<0.001	<0.001	0.026	<0.001	<0.001
	K-4	2	<0.001/0.026	<0.008	<0.001	<0.001	
	M-1	1	<0.005	0.056			
	M-2	1	0.28	0.26			
	N-2	1	0.39	0.67			
	N-3	1	0.39	0.47			
	O-1	1	0.42	0.15			
	O-2	1	0.42	0.09			
	P-1	1	<0.005	0.096			
	R-1	1	0.4	0.42			
	R-2	1	0.4	0.34			
total phosphorus	B-1	1	0.210	0.287			
	B-2	1	0.21	0.242			
	B-4	1	0.210	0.221			0.173
	C-1	3	1.20	<0.005	<0.005	<0.003	
	D-3	1	0.10	<0.02			0.04
	E-2	3	0.24	0.24	0.16	0.20	
	E-3	3	0.24	1.04	0.16	0.24	
	F-1	3	<0.02	3.25	3.25	2.05	
	F-2	3	<0.02	0.55	1.3	<0.02	
	F-6	3	<0.02		0.85	<0.02	
	G-1	3	0.04	0.04	0.21		
	J-1	2	0.0435	0.53			
	J-2	2	0.0435	0.78			0.52
	K-2	3/1	0.04/0.51	0.39	0.63	0.51	
	K-3	3/1	0.04/0.08	<0.02	0.03	0.04	0.03
	K-4	3/1	0.04/0.35	0.31	0.17	0.42	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
vanadium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	0.038	ND			
	E-2	3	ND	0.005	0.005	ND	
	E-3	3	ND	0.005	0.003	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.053	0.056		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
yttrium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	0.006			
	E-2	3	ND	ND	ND	ND	
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.007	0.019		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants							
1. acenaphthene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	*	*	ND	
	F-2	3	ND	*	ND	*	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	
4. benzene	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	*	0.001	*	*	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	*	*	ND	*	
	F-2	2	*	*	*	*	
	F-6	2	*		*	*	
	G-1	2	ND	ND	0.019		
	J-1	2	0.003	0.004			
	J-2	2	0.003	ND			ND
	K-2	2	ND/0.008	ND	0.008	0.009	
	K-3	2	ND/0.008	ND	0.009	0.009	0.009
	K-4	2	ND/0.009	0.045/ND	0.034/ 0.008	0.005/ 0.008	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
5. benzidine	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND		
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		*	*	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
6. carbon tetrachloride	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	ND	ND	ND	ND	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	0.008	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	ND	ND	ND	ND	
	F-2	2	ND	ND	ND	ND	
	F-6	2	ND		ND	ND	
	G-1	2	0.001	*	*		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	2	0.004/0.0055	ND	0.007	0.004	
	K-3	2	0.004/0.005	0.001	0.005	ND	0.006
	K-4	2	0.004/0.0075	ND/ND	ND/0.008	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
7. chlorobenzene	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	ND	ND	ND	ND	
	D-3	2	ND	ND			
	E-2	2	ND	0.0032	ND	ND	0.0003
	E-3	2	ND	ND	ND	ND	
	F-1	2	ND	ND	ND	ND	
	F-2	2	ND	*	*	*	
	F-6	2	ND		*	ND	
	G-1	2	ND	ND	ND		
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	ND	ND	ND	ND
	K-4	2	ND/ND	ND/ND	ND/ND	ND/ND	
10. 1,2-dichloroethane	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	ND	ND	*	ND	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	ND
	F-1	2	ND	ND	ND	ND	
	F-2	2	ND	ND	ND	ND	
	F-6	2	ND		ND	ND	
	G-1	2	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	2	ND	ND	ND	ND	
	K-3	2	ND	ND	ND	ND	ND
	K-4	2	ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
11. 1,1,1-trichloroethane	B-1	2	*	0.001			
	B-2	2	*	0.0015			
	B-4	2	*	0.001			0.001
	C-1	2	ND	ND	*	ND	
	D-3	2	0.004	0.001			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	*	ND	ND	ND	
	F-2	2	*	ND	ND	ND	
	F-6	2	*		ND	ND	
	G-1	2	0.004	0.003	0.006		
	J-1	2	0.004	0.004			
	J-2	2	0.004	*			0.001
	K-2	2	0.003/0.0115	0.001	0.036	0.007	
	K-3	2	0.003/0.001	0.001	0.001	0.004	0.002
	K-4	2	0.003/0.0275	0.011/ 0.037	0.037/ 0.093	0.015/ 0.031	
22. p-chloro-m-cresol	B-1	1	0.008	0.008			
	B-2	1	0.008	0.008			
	B-4	1	0.008	0.008			0.008
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	0.008	0.008			
	J-2	2	0.008	0.008			0.008
	K-2	3	ND/0.043	0.042	0.042	0.043	
	K-3	3	ND/0.043	0.042	0.040	0.043	0.042
	K-4	3	ND/ND	0.042	0.042	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
23. chloroform	B-1	2	0.014	0.026			
	B-2	2	0.014	0.035			
	B-4	2	0.014	0.020			0.070
	C-1	2	ND	ND	ND	ND	
	D-3	2	0.019	0.010			
	E-2	2	0.068	0.048	0.058	0.070	0.115
	E-3	2	0.068	0.042	0.090	0.066	
	F-1	2	*	*	*	*	
	F-2	2	*	*	*	ND	
	F-6	2	*		*	*	
	G-1	2	0.006	0.005	0.008		
	J-1	2	0.0035	ND			
	J-2	2	0.0035	ND			ND
	K-2	2	0.1015/0.001	*	ND	ND	
	K-3	2	0.1015/0.003	0.001	0.002	0.002	0.003
	K-4	2	0.1015/0.062	0.003/ 0.015	0.003/ 0.012	0.029/ 0.024	
24. 2-chlorophenol	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	*	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
25. 1,2-dichlorobenzene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	*	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	
26. 1,3-dichlorobenzene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	*	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
27. 1,4-dichlorobenzene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	*	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	
30. 1,2-trans-dichloroethylene	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	0.008	*	ND	ND	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	ND	ND	ND	ND	
	F-2	2	ND	ND	ND	ND	
	F-6	2	ND		ND	ND	
	G-1	2	ND	0.015	0.017		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	ND	ND	ND	ND
	K-4	2	ND/ND	ND/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
31. 2,4-dichlorophenol	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	*	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	
38. ethylbenzene	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	ND	*	*	ND	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	ND	ND	ND	*	
	F-2	2	ND	*	*	*	
	F-6	2	ND		ND	*	
	G-1	2	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	ND	ND	ND	ND
	K-4	2	ND/ND	ND/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
39. fluoranthene	B-1	1	ND	*			
	B-2	1	ND	*			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	
	K-4	3	ND/ND	ND	ND	ND	
41. 4-bromophenylphenylether	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	0.00042	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
44. methylene chloride	B-1	2	0.001	ND			
	B-2	2	0.001	0.014			
	B-4	2	0.001	††			0.183
	C-1	2	*	0.009	0.038	0.011	
	D-3	2	0.017	0.008			
	E-2	2	0.00007	0.007	0.00006	0.0001	0.0029
	E-3	2	0.00007	0.00008	0.00005	0.00008	
	F-1	2	*	0.001	*	*	
	F-2	2	*	0.002	*	*	
	F-6	2	*		*	*	
	G-1	2	ND	0.33	0.024		
	J-1	2	0.005	ND			
	J-2	2	0.005	0.096			0.066
	K-2	2	0.015/0.0305	ND	0.156	0.028	
	K-3	2	0.015/0.028	0.026	0.023	0.031	0.037
	K-4	2	0.015/0.0335	0.017/ND	0.041/0.157	0.010/0.030	
47. bromoform	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	ND	ND	ND	ND	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	0.086	0.015	0.015	0.024	
	F-2	2	0.086	0.005	0.020	0.009	
	F-6	2	0.086		0.011	0.017	
	G-1	2	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	*	ND	ND	ND
	K-4	2	ND/ND	*/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
48. dichlorobromomethane	B-1	2	ND	ND			
	B-2	2	ND	0.001			
	B-4	2	ND	ND			ND
	C-1	2	ND	ND	ND	ND	
	D-3	2	0.004	0.003			
	E-2	2	0.004	ND	ND	0.006	ND
	E-3	2	0.004	ND	ND	ND	
	F-1	2	*	ND	ND	*	
	F-2	2	*	ND	ND	ND	
	F-6	2	*		*	*	
	G-1	2	ND	ND	ND		
	J-1	2	0.001	ND			
	J-2	2	0.001	0.002			0.002
	K-2	2	0.018/ND	0.007	0.006	0.005	
	K-3	2	0.018/ND	0.001	0.005	0.003	ND
	K-4	2	0.018/ND	0.001/ND	ND/0.007	0.005/ 0.006	
49. trichlorofluoromethane	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	ND	0.003	0.004	*	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	ND	ND	ND	*	
	F-2	2	ND	*	*	*	
	F-6	2	ND		*	*	
	G-1	2	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	0.001	0.002			0.002
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	ND	ND	ND	ND
	K-4	2	ND/ND	ND/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
51. chlorodibromomethane	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	ND	ND	ND	ND	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	0.002	*	*	0.001	
	F-2	2	0.002	*	*	*	
	F-6	2	0.002		*	*	
	G-1	2	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	ND	ND	ND	ND
	K-4	2	ND/ND	0.001/ND	ND/ND	ND/ND	
54. isophorone	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	0.00096	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
55. naphthalene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	0.018	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	
56. nitrobenzene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	*	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (*Continued*)							
57. 2-nitrophenol	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	0.001	0.003	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	*	0.001	0.001	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
58. 4-nitrophenol	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	0.007/*	*	ND	*	
	K-3	3	0.007/ND	ND	ND	ND	ND
	K-4	3	0.007/ND	ND	ND	0.004	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
60. 4,6-dinitro-o-cresol	B-1	1	ND	ND			
	B-2	1	ND	0.004			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
61. N-nitrosodimethylamine	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	*	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
62. N-nitrosodiphenylamine	B-1	1	ND	*			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	0.006			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	*/0.001	ND	ND	ND	
	K-3	3	*/*	ND	ND	ND	ND
	K-4	3	*/*	ND	ND	ND	
63. N-nitrosodi-n-propylamine	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	0.015	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
64. pentachlorophenol	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	4.880†††			
	J-2	2	ND	6.000†††			5.730†††
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	
65. phenol	B-1	1	0.010	0.028			
	B-2	1	0.01	0.01			
	B-4	1	0.010	0.318			0.334
	C-1	3	*	0.780	0.810	0.91	
	D-3	1	*	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	*	*	0.005	0.017	
	F-2	3	*	*	*	*	
	F-6	3	*		*	0.36	
	G-1	3	ND	0.179	0.434		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	0.012	
	K-3	3	ND/ND	ND	ND	0.0005	ND
	K-4	3	ND/ND	ND	ND	0.002	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
66. bis(2-ethylhexyl)phthalate	B-1	1	0.001	0.001			
	B-2	1	0.001	0.007			
	B-4	1	0.001	0.006			0.010
	C-1	3	0.003	0.048	0.024	0.011	
	D-3	1	0.289	0.017			
	E-2	3	0.00066	0.0017	0.00042	0.00063	0.0034
	E-3	3	0.00066	0.00085	0.002	0.00048	
	F-1	3	0.001	0.003	0.020	0.009	
	F-2	3	0.001	0.004	0.003	0.002	
	F-6	3	0.001		0.063	0.033	
	G-1	3	ND	ND	1.72		
	J-1	2	0.002	0.481			
	J-2	2	0.002	0.050			0.051
	K-2	3	0.005/0.113	0.240	0.258	1.006	
	K-3	3	0.005/0.161	0.072	0.107	0.314	0.122
	K-4	3	0.005/0.008	0.005	0.001	0.188	
67. butyl benzyl phthalate	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	0.00049	ND	
	F-1	3	ND	ND	0.006	0.004	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		*	ND	
	G-1	3	0.003	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
68. di-n-butyl phthalate	B-1	1	0.003	0.001			
	B-2	1	0.003	0.008			
	B-4	1	0.003	0.003			0.004
	C-1	3	*	0.003	0.003	0.001	
	D-3	1	0.003	0.012			
	E-2	3	0.000725	0.0011	0.00043	0.00071	0.0010
	E-3	3	0.000725	0.0078	0.0014	0.0011	
	F-1	3	*	0.001	0.003	0.003	
	F-2	3	*	0.003	0.002	0.003	
	F-6	3	*		*	*	
	G-1	3	ND	0.0010	0.0023		
	J-1	2	0.0105	0.013			
	J-2	2	0.0105	0.011			0.012
	K-2	3	0.005/ND	0.004	0.004	0.011	
	K-3	3	0.005/0.004	0.009	0.004	ND	0.005
	K-4	3	0.005/ND	0.006	0.007	ND	
69. di-n-octyl phthalate	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	0.004	0.004	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	0.00032	ND	
	F-1	3	ND	*	ND	0.002	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	0.005	ND	0.020		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	0.021	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
70. diethyl phthalate	B-1	1	*	0.002			
	B-2	1	*	0.001			
	B-4	1	*	*			*
	C-1	3	ND	*	*	ND	
	D-3	1	ND	ND			
	E-2	3	0.00082	0.0013	0.00054	0.00074	0.00094
	E-3	3	0.00082	0.0011	0.0018	0.00080	
	F-1	3	ND	*	ND	ND	
	F-2	3	ND	*	ND	ND	
	F-6	3	ND		*	ND	
	G-1	3	ND	0.621	0.964		
	J-1	2	0.0005	ND			
	J-2	2	0.005	0.001			0.001
	K-2	3	ND/ND	ND	ND	*	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/*	ND	*	ND	
71. dimethyl phthalate	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	0.003	0.002	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.001	0.087		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/0.003	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/1)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
72. benzo(a)anthracene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	*	ND	ND	
	D-3	1	ND	ND			
	E-2	3	*	ND	ND	ND	ND
	E-3	3	ND	ND	0.00053	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	*	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
73. benzo(a)pyrene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	0.012			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	*	ND		
	J-1	2	ND	0.001			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/*	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
76. chrysene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	*	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/0.004	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
78. anthracene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	*	*	*	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	0.00019	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	0.004	0.004	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
80. fluorene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	*	ND	
	D-3	1	*	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	0.00039	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
81. phenanthrene	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	*	*	*	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	0.00067	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
85. tetrachloroethylene	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	0.019	*	*	*	
	D-3	2	ND	ND			
	E-2	2	ND	ND	ND	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	ND	ND	ND	ND	
	F-2	2	ND	ND	ND	ND	
	F-6	2	ND		ND	ND	
	G-1	2	0.012	0.004	0.014		
	J-1	2	ND	ND			
	J-2	2	0.001	ND			ND
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	ND	ND	ND	ND
	K-4	2	ND/ND	0.001/ND	ND/ND	ND/ND	
86. toluene	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	*	0.006	0.005	0.002	
	D-3	2	ND	ND			
	E-2	2	ND	0.0022	ND	ND	0.0025
	E-3	2	ND	ND	ND	ND	
	F-1	2	*	*	*	*	
	F-2	2	*	0.008	0.015	0.002	
	F-6	2	*		0.002	*	
	G-1	2	ND	ND	ND		
	J-1	2	0.012	ND			
	J-2	2	0.012	ND			ND
	K-2	2	ND/0.016	ND	ND	ND	
	K-3	2	ND/ND	ND	0.016	0.016	0.016
	K-4	2	ND/ND	ND/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
87. trichloroethylene	B-1	2	ND	ND			
	B-2	2	ND	ND			
	B-4	2	ND	ND			ND
	C-1	2	0.004	ND	*	ND	
	D-3	2	ND	ND			
	E-2	2	ND	ND	0.0011	ND	ND
	E-3	2	ND	ND	ND	ND	
	F-1	2	ND	ND	ND	ND	
	F-2	2	ND	ND	ND	ND	
	F-6	2	ND		ND	ND	
	G-1	2	0.343	0.146	0.215		
	J-1	2	0.050	ND			
	J-2	2	0.050	0.003			0.002
	K-2	2	ND/ND	ND	ND	ND	
	K-3	2	ND/ND	0.001	ND	ND	ND
	K-4	2	ND/0.0095	0.001/ND	ND/ND	ND/ND	
89. aldrin	B-1	1	ND	0.000003			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	**	**	**	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	0.0003	ND	ND	
	F-2	3	ND	**	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	0.000023
	K-4	3	ND/ND	ND/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
90. dieldrin	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	**	**	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	0.000086	ND	0.000034
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	**	ND	**	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND/ND	ND/ND	ND/ND	
92. 4,4'-DDT	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	0.000022	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
93. 4,4'-DDE	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	0.000027
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/0.000023	ND	ND	0.000045	ND
	K-4	3	ND/ND	ND/ND	ND/ND	ND/ND	
94. 4,4'-DDD	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	0.000040	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND/ND	ND/ND	ND/ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
97. endosulfan sulfate	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	0.00013	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
98. endrin	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	**	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	**	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND	ND	ND	ND	
	K-3	3	ND	ND	ND	ND	ND
	K-4	3	ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
99. endrin aldehyde	B-1	1	ND	0.000066			
	B-2	1	ND	ND			
	B-4	1	ND	0.000031			0.000066
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
100. heptachlor	B-1	1	0.000003	0.000002			
	B-2	1	0.000003	ND			
	B-4	1	0.000003	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	0.000026	0.000028	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
101. heptaclor expoxide	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	0.00004	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/ND	ND	ND	ND	
	K-3	3	ND/ND	ND	ND	ND	ND
	K-4	3	ND/ND	ND	ND	ND	
102. alpha-BHC	B-1	1	0.000003	0.000005			
	B-2	1	0.000003	0.000004			
	B-4	1	0.000003	0.000004			0.000007
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	0.000121	ND	ND	0.000108	ND
	E-3	3	0.000121	0.000182	0.000178	0.000194	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	0.0006	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	0.000009		
	J-1	2	0.0000025	0.00022			
	J-2	2	0.0000025	0.00029			ND
	K-2	3	0.000021/ 0.000008	0.000036	0.000134	0.000191	
	K-3	3	ND/0.000083	ND	0.000078	0.000113	ND
	K-4	3	ND/0.000076	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
103. beta-BHC	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	0.0006	
	D-3	1	0.000181	0.00014			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	0.000166	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			ND
	K-2	3	ND/0.000025	0.000062	0.000072	0.000335	
	K-3	3	0.000021/ 0.000046	0.000035	0.000047	0.000183	0.000043
	K-4	3	0.000021/ 0.000050	0.000025	0.000041	ND	
104. gamma-BHC	B-1	1	ND	0.000002			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	**	ND	ND	
	D-3	1	0.000006	0.000099			
	E-2	3	0.000110	ND	0.000349	0.000057	ND
	E-3	3	0.00011	0.000122	ND	0.000096	
	F-1	3	**	ND	ND	ND	
	F-2	3	**	ND	0.0003	ND	
	F-6	3	**		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	0.0000025	ND			
	J-2	2	0.0000025	ND			ND
	K-2	3	0.000018/ND	0.000032	0.000038	0.000076	
	K-3	3	ND/0.000027	0.000018	ND	0.000061	0.000022
	K-4	3	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
105. delta-BHC	B-1	1	0.000005	0.000009			
	B-2	1	0.000005	0.000006			
	B-4	1	0.000005	0.000005			0.000005
	C-1	3	**	**	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	ND
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	0.0000085	0.000035			
	J-2	2	0.0000085	ND			ND
	K-2	3	0.000018/ND	ND	0.000039	ND	
	K-3	3	0.000018/ND	ND	0.000027	ND	ND
	K-4	3	0.000018/ND	0.000058	0.000061	0.000107	
114. antimony	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	0.002	0.002	0.004	0.003	
	E-3	3	0.002	ND	0.003	0.003	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/0.04	0.02	0.03	0.03	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
115. arsenic	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	
	E-3	3	ND	ND	ND	0.001	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	0.016			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
117. beryllium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			ND
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.003	0.003		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
118. cadmium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.025	0.019	0.015	
	D-3	1	ND	ND			
	E-2	3	0.005	0.006	0.005	0.006	
	E-3	3	0.005	0.006	0.003	0.006	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		0.053	0.071	
	G-1	3	ND	ND	ND		
	J-1	2	0.018	0.014			
	J-2	2	0.018	0.017			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
119. chromium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.200	0.170	0.012	
	D-3	1	0.010	0.015			
	E-2	3	ND	0.007	0.008	0.003	
	E-3	3	ND	0.009	0.008	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	0.073	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.143	0.077		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/0.02	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
120. copper	B-1	1	2.600	1.200			
	B-2	1	2.6	2.2			
	B-4	1	2.600	1.550			
	C-1	3	0.068	0.940	0.530	0.310	
	D-3	1	0.106	0.106			
	E-2	3	0.196	0.058	0.055	0.066	
	E-3	3	0.196	0.058	0.061	0.060	
	F-1	3	0.700	0.034	0.026	0.036	
	F-2	3	0.7	0.016	ND	ND	
	F-6	3	0.7		0.022	0.041	
	G-1	3	ND	0.06	0.045		
	J-1	2	ND	ND			
	J-2	2	ND	0.037			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/0.1	0.05	0.1	0.1	
	K-4	3/1	ND/0.1	ND	ND	ND	
121. cyanide (total)	B-1	1	<0.01	<0.01			
	B-2	1	<0.01	<0.01			
	B-4	1	<0.01	<0.01			<0.01
	C-1	1	0	0	0	0	
	D-3	1	<0.02	<0.02			<0.02
	E-2	1	<0.01	<0.01	<0.01	<0.01	
	E-3	1	<0.01	<0.01	<0.01	<0.01	
	F-1	1	<0.02	<0.02	<0.02	<0.02	
	F-2	1	<0.02	<0.02	<0.02	<0.02	
	F-6	1	<0.02		<0.02	<0.02	
	G-1	2	<0.02	<0.02	<0.02		
	J-1	2	<0.01	<0.01			
	J-2	2	<0.01	ND			ND
	K-2	1	<0.02/<0.02	<0.02	<0.02	<0.02	
	K-3	1	<0.02/<0.02	<0.02	<0.02	<0.02	<0.02
	K-4	1	<0.02/<0.02	<0.02	<0.02	<0.02	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
122. lead	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.260	0.160	ND	
	D-3	1	ND	ND			
	E-2	3	0.080	0.122	0.292	0.126	
	E-3	3	0.080	0.057	0.059	0.064	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/0.25	0.15	0.15	0.10	
	K-3	3/1	ND/0.05	0.1	ND	0.1	
	K-4	3/1	ND/ND	ND	ND	0.5	
123. mercury	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.0007	0.0003	0.0003	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND	ND	ND	ND	
	K-3	3/1	ND	ND	ND	ND	
	K-4	3/1	ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
124. nickel	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	3.880	3.240	2.770	
	D-3	1	ND	ND			
	E-2	3	ND	0.012	0.021	ND	
	E-3	3	ND	0.021	0.014	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.073	ND		
	J-1	2	ND	ND			
	J-2	2	ND	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
125. selenium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	0.002	0.001	0.002	0.001	
	E-3	3	0.002	0.002	ND	0.001	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	0.0345	0.012			
	J-2	2	0.0345	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR CONTACT COOLING AND HEATING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
126. silver	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	0.012	0.0088	ND	
	D-3	1	ND	ND			
	E-2	3	0.001	0.001	0.001	ND	
	E-3	3	0.001	0.001	ND	0.002	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	ND	ND		
	J-1	2	0.016	0.016			
	J-2	2	0.016	0.014			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	
127. thallium	B-1	1	ND	ND			
	B-2	1	ND	ND			
	B-4	1	ND	ND			
	C-1	3	ND	ND	ND	ND	
	D-3	1	ND	ND			
	E-2	3	ND	ND	ND	ND	
	E-3	3	ND	ND	ND	ND	
	F-1	3	ND	ND	ND	ND	
	F-2	3	ND	ND	ND	ND	
	F-6	3	ND		ND	ND	
	G-1	3	ND	0.126	0.126		
	J-1	2	0.1385	ND			
	J-2	2	0.1385	ND			
	K-2	3/1	ND/ND	ND	ND	ND	
	K-3	3/1	ND/ND	ND	ND	ND	
	K-4	3/1	ND/ND	ND	ND	ND	

Table A-1 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CONTACT COOLING AND HEATING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
128. zinc	B-1	1	0.120	0.180			
	B-2	1	0.12	0.16			
	B-4	1	0.120	0.120			
	C-1	3	ND	0.750	0.770	0.490	
	D-3	1	0.017	0.018			
	E-2	3	1.46	0.627	0.658	0.637	
	E-3	3	1.46	0.664	0.662	0.712	
	F-1	3	0.015	ND	ND	ND	
	F-2	3	0.015	0.14	0.21	0.21	
	F-6	3	0.015		ND	ND	
	G-1	3	ND	0.067	0.125		
	J-1	2	ND	0.054			
	J-2	2	ND	0.125			
	K-2	3/1	ND/0.08	0.06	0.06	0.08	
	K-3	3/1	ND/0.04	ND	0.04	0.04	
	K-4	3/1	ND/0.36	ND	ND	ND	

†Sample Type

1 - grab
2 - grab composite
3 - automatic composite

§See Figures VI-1 through VI-17.
††Value was not used because it was suspected to be result of laboratory contamination.
†††Pentachlorophenol was added to plant J's cooling tower as an algicide. Its use as an algicide was recently discontinued at plant J. For this reason, these data were not used in this project.
*Indicates a reported less than value of <0.001 mg/l.
**Indicates a reported less than value of <0.0001 mg/l.

¶Total phenols data from plant F were not used based on verification sampling.

NA - Pollutant was not analyzed.

ND - Not detected.

Table A-2

SAMPLING DATA BY POLLUTANT FOR CLEANING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD$_5$)	A-1	1	<5	9			
	A-2	1	<5	450			
	B-3	1	<5	48	46	52	
	C-2	1	83.8	84.8	48.5	72.7	
	D-1		NA	NA			
	D-2		NA	NA			
	F-3	1	2	510	247	52	
	F-4	1	2	198	34	26	
	H-1	1	<5.0	1000	630		850
	I-1	1	1.7	6.3	6.1	6.2	
	I-2	1	1.7	2.6	5.95	5.65	
	I-3	1	1.7	3.2		6.6	
	K-1	2	<5	20			
oil and grease	A-1	2	<4	<4			
	A-2	2	<4	<4			
	B-3	2	<4	<4	<4	<4	
	C-2	1	17.0	31.0	0	17.5	
	D-1	2	<4	<4			
	D-2	2	<4	<4			
	F-3	1	3	548	684		
	F-4	1	3	3	89		
	H-1	2	<4.0	<4.0	<4.0		<4.0
	I-1	1	0	18	7	44.7	
	I-2	1	0	234.5	21.8	174.1	
	I-3	1	0	21.2		7.8	
	K-1	2	<4	<4			
pH	A-1	1	8.6	9.2			
	A-2	1	8.6	1.6			
	B-3	3	6.8	7.1	7.1	6.2	
	C-2	3	5.8	6.85	6.25	6.55	
	D-1		NA	NA			
	D-2		NA	NA			
	F-3	3	7.6	7.9	8.1	8.0	
	F-4	3	7.6	7.9	8.5	8.4	
	H-1	1	5.7	4.8	5.7		4.8
	I-1	3	6.6	7.2	7.5	7.5	
	I-2	1	6.6	11.5	10.0	10.8	
	I-3	1	6.6	11.0		8.0	
	K-1	2	8.0	9.3			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants (Continued)							
total suspended solids (TSS)	A-1	1	8	12			
	A-2	1	8	39			
	B-3	3	<4	<4	<4	<4	
	C-2	3	0	8.0	2.0	11.0	
	D-1	1	<4	13			
	D-2	1	<4	8			
	F-3	3	2	198	274	466	
	F-4	3	2	90	1310	68	
	H-1	1	5.0	11.0	<4.0		10.0
	I-1	3	56.0	16363	11738	12597	
	I-2	1	56.0	5825	244	1039	
	I-3	1	56.0	1136		5671	
	K-1	2	<4	6			
Nonconventional Pollutants							
aluminum	A-1	1	ND	ND			
	A-2	1	ND	0.1			
	B-3	1	0.2	0.2	0.2	0.1	
	C-2	3	ND	ND	ND	ND	
	D-1	1	0.11	0.07			
	D-2	1	0.11	ND			
	F-3	3	ND	0.1	0.058		
	F-4	3	ND	ND	0.071		
	H-1	1	ND	ND	ND		
	I-1	3	0.2	0.2	0.1	0.2	
	I-2	1	0.2	8.1	0.3	5	
	I-3	1	0.2	4.2		5.2	
	K-1	2	ND	0.1			
ammonia nitrogen	A-1	1	<0.1	<0.1			
	A-2	1	<0.1	<0.1			
	B-3	3	<0.05	0.06	0.06	0.17	
	C-2	3	0	0	9.52	5.60	
	D-1	1	<0.05	399			
	D-2	1	<0.05	198			
	F-3	1	3.3	<1	2.7	1.1	
	F-4	1	3.3	1.5	4.0	1.4	
	H-1	1	0.09	<0.05	0.05		0.07
	I-1	1	0.20	137.5	75.0	93.1	
	I-2	1	0.20	20.4	51.25	4.25	
	I-3	1	0.20	75.0		67.5	
	K-1	2	<0.05	0.66			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR CLEANING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
barium	A-1	1	ND	0.014			
	A-2	1	ND	0.062			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	0.012	0.012	0.015	
	D-1	1	0.034	0.035			
	D-2	1	0.034	0.035			
	F-3	3	0.043	0.065	0.091		
	F-4	3	0.043	0.047	0.037		
	H-1	1	ND	ND	ND		ND
	I-1	3	0.03	0.04	0.04	0.03	
	I-2	1	0.03	0.8	0.09	0.65	
	I-3	1	0.03	0.16		0.05	
	K-1	2	ND	ND			
boron	A-1	1	ND	ND			
	A-2	1	ND	0.024			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	0.050	0.034			
	D-2	1	0.050	0.053			
	F-3	3	0.051	0.19	0.18		
	F-4	3	0.051	0.14	0.15		
	H-1	1	ND	ND	ND		ND
	I-1	3	0.050	0.06	0.12	0.06	
	I-2	1	0.050	0.23	0.07	0.21	
	I-3	1	0.050	0.52		0.58	
	K-1	2	ND	2.9			
bromide	A-1	1	<0.4	<0.4			
	A-2	1	<0.4	<0.4			
	B-3	3	<0.4	<0.4	<0.4	<0.4	
	C-2		NA	NA	NA	NA	
	D-1	1	<0.4	<0.4			
	D-2		NA	NA			
	F-3		NA	NA	NA	NA	
	F-4		NA	NA	NA	NA	
	H-1	1	<0.4	<0.4	<0.4		<0.4
	I-1		NA	NA	NA	NA	
	I-2		NA	NA	NA	NA	
	I-3		NA	NA		NA	
	K-1	2	<0.4	<0.4			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
calcium	A-1	1	4.8	5.0			
	A-2	1	4.8	7.58			
	B-3	1	4.5	4.3	4.3	4.8	
	C-2	3	6.84	6.86	6.46	6.58	
	D-1	1	21.4	16.0			
	D-2	1	21.4	16.6			
	F-3	3	33.2	40.7	72.7		
	F-4	3	33.2	34.3	20.5		
	H-1	1	0.194	0.073	ND		0.123
	I-1	3	51.3	46.3	47.9	45.9	
	I-2	1	51.3	182.0	30.7	207.0	
	I-3	1	51.3	45.2		26.8	
	K-1	2	20.4	5.7			
chemical oxygen demand (COD)	A-1	1	19	460			
	A-2	1	19	958			
	B-3	1	<5	96	86	62	
	C-2	3	0	453.9	278.5	148.8	
	D-1	1	<5	48			
	D-2	1	<5	172			
	F-3	3	8294	1321	261	983	
	F-4	3	8294	380	346	111	
	H-1	1	<5.0	2280	1150		2220
	I-1	3	290	680	1150	640	
	I-2	1	290	480	520	560	
	I-3	1	290	200		950	
	K-1	2	<5	195			
cyanide (amenable)	A-1	1	NA	NA			
	A-2	1	NA	NA			
	B-3		NA	NA	NA	NA	
	C-2	1	0	0	0	0	
	D-1		NA	NA			
	D-2	1	NA	NA			
	F-3	1	0	0	0	0	
	F-4	1	0	0	0	0	
	H-1		NA	NA	NA		
	I-1	1	0.6	0.025	0.174	0.01	
	I-2	1	0.6	0	0.034	0	
	I-3	1	0.6	0		0.01	
	K-1		NA	NA			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
fluoride	A-1	1	0.20	0.19			
	A-2	1	0.20	6.8			
	B-3	3	0.44	0.12	0.37	0.11	
	C-2		NA	NA	NA	NA	
	D-1	1	0.95	0.99			
	D-2		0.95	0.99			
	F-3		NA	NA	NA	NA	
	F-4		NA	NA	NA	NA	
	H-1	1	0.14	<0.1	0.14		<0.1
	I-1		NA	NA	NA	NA	
	I-2		NA	NA	NA	NA	
	I-3		NA	NA			
	K-1	2	0.81	0.27			
iron	A-1	1	0.171	1.95			
	A-2	1	0.171	2.20			
	B-3	1	0.1	0.1	0.05	0.05	
	C-2	3	0.14	1.44	1.15	1.25	
	D-1	1	ND	0.118			
	D-2	1	ND	ND			
	F-3	3	0.036	1.49	1.31		
	F-4	3	0.036	1.46	2.63		
	H-1	1	ND	ND	ND		ND
	I-1	3	0.067	0.538	ND	0.269	
	I-2	1	0.067	51.3	0.023	39.1	
	I-3	1	0.067	10.6		4.73	
	K-1	2	ND	ND			
Kjeldahl nitrogen	A-1	1	<1	21.6			
	A-2	1	<1	<1			
	B-3	3	<1	<1	<1	<1	
	C-2	3	0	0	0	0	
	D-1	1	<1	361			
	D-2	1	<1	210			
	F-3	3	<0.02	7.55	3.7	2.5	
	F-4	3	<0.02	0.65	1.05	0.25	
	H-1	1	<1.0	<1.0	<1.0		<1.0
	I-1	3	3.85	3070	1248	1718	
	I-2	1	3.85	45.5	1153	60.1	
	I-3	1	3.85	1310		1188	
	K-1	2	<1	12			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
magnesium	A-1	1	0.820	0.847			
	A-2	1	0.820	0.83			
	B-3	1	1.4	1.4	1.4	1.4	
	C-2	3	1.24	1.16	1.17	1.15	
	D-1	1	5.66	4.82			
	D-2	1	5.66	4.97			
	F-3	3	13.3	18.7	24.9		
	F-4	3	13.3	17.3	14.9		
	H-1	1	0.179	0.154	0.167		0.198
	I-1	3	7.17	7.03	7.04	6.89	
	I-2	1	7.17	17.5	4.26	13.4	
	I-3	1	7.17	6.42		5.27	
	K-1	2	5.8	0.2			
manganese	A-1	1	ND	0.02			
	A-2	1	ND	0.176			
	B-3	1	ND	ND	ND	ND	
	C-2	3	0.072	0.070	0.072	0.071	
	D-1	1	0.008	0.01			
	D-2	1	0.008	0.003			
	F-3	3	ND	0.020	0.016		
	F-4	3	ND	0.011	0.024		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	0.022	ND	ND	
	I-2	1	ND	0.519	ND	0.424	
	I-3	1	ND	0.111		0.084	
	K-1	2	ND	ND			
molybdenum	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	0.021	0.065		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	0.3	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR CLEANING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
nitrate/nitrite	A-1	1	<0.1	<0.1			
	A-2	1	<0.1	<0.1			
	B-3	3	0.25	0.25	0.20	0.28	
	C-2		NA	NA	NA	NA	
	D-1	1	2.0	2.1			
	D-2		2.0	2.1			
	F-3		NA	NA	NA	NA	
	F-4		NA	NA	NA	NA	
	H-1	1	<0.1	0.2	<0.1		<0.1
	I-1		NA	NA	NA	NA	
	I-2		NA	NA	NA	NA	
	I-3		NA	NA		NA	
	K-1	2	1.05	<0.1			
sodium	A-1	1	12.8	58.1			
	A-2	1	12.8	15.1			
	B-3	1	11.1	11.3	10.6	12.0	
	C-2	3	11.4	13.6	12.6	14.4	
	D-1	1	26.2	24.3			
	D-2	1	26.2	24.2			
	F-3	3	17.7	358	311		
	F-4	3	17.7	198	180		
	H-1	1	ND	5.93	ND		5.57
	I-1	3	12.4	24.5	24.0	19.7	
	I-2	1	12.4	1830	3860	510	
	I-3	1	12.4	272		317	
	K-1	2	8.1	0.8			
sulfate	A-1	1	12	40			
	A-2	1	12	45			
	B-3	3	11	12	10	10	
	C-2		NA	NA	NA	NA	
	D-1	1	33	33			
	D-2		33	30			
	F-3		NA	NA	NA	NA	
	F-4		NA	NA	NA	NA	
	H-1	1	<5.0	<5.0	<5.0		<5.0
	I-1		NA	NA	NA	NA	
	I-2		NA	NA	NA	NA	
	I-3		NA	NA		NA	
	K-1	2	10	<5			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
sulfide	A-1	1	<1	<1			
	A-2	1	<1	<1			
	B-3	1	<1	<1	<1	<1	
	C-2		NA	NA	NA	NA	
	D-1		NA	NA			
	D-2		NA	NA			
	F-3		NA	NA	NA	NA	
	F-4		NA	NA	NA	NA	
	H-1	1	<1.0	<1.0	<1.0		<1.0
	I-1		NA	NA	NA	NA	
	I-2		NA	NA	NA	NA	
	I-3		NA	NA		NA	
	K-1	2	<1	<1			
surfactants	A-1	1	<0.01	0.020			
	A-2	1	<0.01	<0.01			
	B-3	3	<0.01	<0.01	<0.01	<0.01	
	C-2	3	0.08	0.92	0.04	1.06	
	D-1		NA	NA			
	D-2	1	NA	NA			
	F-3	3	<0.02	148	66	50	
	F-4	3	<0.02	0.05	0.15	0.07	
	H-1	1	<0.01	<0.01	<0.01		<0.01
	I-1	3	0.15	0.10	0.112	0.05	
	I-2	1	0.15	0.05	0.40	0.025	
	I-3	1	0.15	0.15		0.112	
	K-1	2	<0.01	0.03			
tin	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	0.042	ND	0.021	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	0.077	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	1.1	
	I-2	1	ND	0.9	1.1	1.2	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
titanium	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	0.087	0.081	0.095	0.084	
	D-1	1	0.013	0.021			
	D-2	1	0.013	0.018			
	F-3	3	0.13	0.12	0.027		
	F-4	3	0.13	0.092	0.085		
	H-1	1	ND	0.01	ND		0.01
	I-1	3	ND	0.016	ND	0.041	
	I-2	1	ND	0.199	ND	0.174	
	I-3	1	ND	0.06		0.075	
	K-1	2	ND	ND			
total dissolved solids (TDS)	A-1	1	NA	NA			
	A-2	1	NA	NA			
	B-3		NA	NA	NA	NA	
	C-2	3	0	5.0	100	5.0	
	D-1		NA	NA			
	D-2	1	NA	NA			
	F-3	3	800	1300	1300	900	
	F-4	3	800	800	1400	600	
	H-1		NA	NA	NA		
	I-1	3	201.5	221	227.5	214.5	
	I-2	1	201.5	4907.5	3250	1430	
	I-3	1	201.5	13000		812.5	
	K-1		NA	NA			
total organic carbon (TOC)	A-1	1	13	150			
	A-2	1	13	1010			
	B-3	3	5	36	34	39	
	C-2	1	3.0	74.0	19.5	30	
	D-1	1	2	22			
	D-2	1	2	56			
	F-3	1	37	875	455	242	
	F-4	1	37	70	103	52	
	H-1	1	2.0	800	600		792
	I-1	1	11.0	9267	5412	10038	
	I-2	1	11.0	1472	3282	2604	
	I-3	1	11.0	5316		4998	
	K-1	2	3	58			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
total phenols	A-1	1	<0.020	<0.020			
	A-2	1	<0.020	<0.050			
	B-3	1	<0.02	<0.02	<0.02	<0.02	
	C-2	1	1.42	0.1	20.86	1.42	
	D-1	1	<0.001	<0.001			
	D-2	1	<0.001	<0.001			
	F-3††	1	10	32	82	222	
	F-4††	1	10	30	62	16	
	H-1	1	<0.02	<0.02	<0.02		<0.02
	I-1	1	2.7	2.95	3.13	3.75	
	I-2	1	2.7	585	575	284.5	
	I-3	1	2.7	730		0.83	
	K-1	2	<0.001	0.31			
total phosphorus	A-1	1	0.03	0.04			
	A-2	1	0.03	0.14			
	B-3	3	<0.02	0.052	<0.02	<0.02	
	C-2	3	1.2	<0.005	0.345	1.06	
	D-1	1	0.1	0.03			
	D-2	1	<0.1	<0.03			
	F-3	3	<0.02	10.5	23.85	13.4	
	F-4	3	<0.02	15.95	20.75	13.55	
	H-1	1	<0.02	<0.02	0.04		0.05
	I-1	3	3.18	6.13	10.45	5.5	
	I-2	1	3.18	103.4	28.77	123	
	I-3	1	3.18	32.1		5.17	
	K-1	2	0.04	0.17			
vanadium	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	0.038	ND			
	D-2	1	0.038	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	0.077	ND	ND		
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
yttrium	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	0.006			
	D-2	1	ND	0.006			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	0.005	ND		
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
Priority Pollutants							
4. benzene	A-1	2	0.005	0.006			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	*	0.003	*	*	
	D-1	2	ND	0.018			
	D-2	2	ND	0.018			
	F-3	2	*	0.01	0.005		
	F-4	2	*	*	*		
	H-1	2	ND	ND	ND		ND
	I-1	2	0.007	0.099	0.012	ND	
	I-2	2	0.007	0.011	0.012	0.009	
	I-3	2	0.007	0.01		0.009	
	K-1	2	ND	0.008			
6. carbon tetrachloride	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	ND	ND	ND	
	D-1	2	ND	ND			
	D-2	2	ND	ND			
	F-3	2	ND	ND	ND		
	F-4	2	ND	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	0.004	ND			

Table A-2

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
7. chlorobenzene	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	ND	ND	ND	
	D-1	2	ND	ND			
	D-2	2	ND	0.0004			
	F-3	2	ND	ND	ND		
	F-4	2	ND	ND	*		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	ND	ND			
11. 1,1,1-trichloroethane	A-1	2	0.003	*			
	A-2	2	0.003	0.010			
	B-3	2	*	0.001	0.001	0.001	
	C-2	2	ND	ND	ND	ND	
	D-1	2	0.004	0.003			
	D-2	2	0.004	0.001			
	F-3	2	*	ND	ND		
	F-4	2	*	ND	ND		
	H-1	2	*	0.001	0.002		0.001
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	0.011	0.010	0.020	
	I-3	2	ND	ND		ND	
	K-1	2	0.003	0.009			
13. 1,1-dichloroethane	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	ND	ND	ND	
	D-1	2	ND	ND			
	D-2	2	ND	ND			
	F-3	2	ND	ND	ND		
	F-4	2	ND	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	0.003		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
22. p-chloro-m-cresol	A-1	1	0.042	0.042			
	A-2	1	0.042	0.042			
	B-3	3	0.008	0.005	0.008	0.008	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	0.014			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	0.008	0.042	0.040		0.042
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
23. chloroform	A-1	2	0.087	0.038			
	A-2	2	0.087	*			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	ND	ND	ND	
	D-1	2	0.019	0.048			
	D-2	2	0.019	0.053			
	F-3	2	*	ND	*		
	F-4	2	*	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	0.12	0.013	0.007	ND	
	I-2	2	0.12	0.005	0.004	0.019	
	I-3	2	0.12	0.004		0.002	
	K-1	2	0.1015	ND			
24. 2-chlorophenol	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	0.006		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
26. 1,3-dichlorobenzene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.001	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
30. 1,2-trans-dichloroethylene	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	0.008	*	*	ND	
	D-1	2	ND	ND			
	D-2	2	ND	ND			
	F-3	2	ND	ND	ND		
	F-4	2	ND	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	ND	ND			
31. 2,4-dichlorophenol	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	0.001		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
38. ethylbenzene	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	*	*	ND	
	D-1	2	ND	ND			
	D-2	2	ND	ND			
	F-3	2	ND	ND	0.001		
	F-4	2	ND	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	ND	ND			
39. fluoranthene	A-1	1	*	*			
	A-2	1	*	*			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	*			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.006	ND	0.002	
	I-3	1	ND	0.0004		ND	
	K-1	2	ND	ND			
44. methylene chloride	A-1	2	0.029	0.084			
	A-2	2	0.029	0.310			
	B-3	2	0.002	0.039	0.005	0.003	
	C-2	2	*	*	*	*	
	D-1	2	0.017	0.019			
	D-2	2	0.017	0.018			
	F-3	2	*	*	0.002		
	F-4	2	*	0.002	*		
	H-1	2	0.003	0.003	0.043		0.008
	I-1	2	0.005	0.005	ND	0.016	
	I-2	2	0.005	0.005	0.005	ND	
	I-3	2	0.005	0.005		ND	
	K-1	2	0.015	0.032			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
47. bromoform	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	ND	ND	ND	
	D-1	2	ND	ND			
	D-2	2	ND	0.001			
	F-3	2	0.086	ND	0.010		
	F-4	2	0.086	0.004	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	ND	ND			
48. dichlorobromomethane	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	ND	ND	ND	
	D-1	2	0.004	0.015			
	D-2	2	0.004	0.011			
	F-3	2	*	ND	ND		
	F-4	2	*	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	0.009	ND	ND	ND	
	I-2	2	0.009	ND	ND	ND	
	I-3	2	0.009	ND		ND	
	K-1	2	0.018	ND			
49. trichlorofluoromethane	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	0.017	0.034	0.017	
	D-1	2	ND	ND			
	D-2	2	ND	ND			
	F-3	2	ND	ND	ND		
	F-4	2	ND	0.003	*		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
51. chlorodibromomethane	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	ND	ND	ND	ND	
	D-1	2	ND	0.001			
	D-2	2	ND	0.002			
	F-3	2	0.002	ND	ND		
	F-4	2	0.002	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	0.004	ND	ND	ND	
	I-2	2	0.004	ND	ND	ND	
	I-3	2	0.004	ND		ND	
	K-1	2	ND	ND			
55. naphthalene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	*	ND			
	F-3	3	ND	*	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
56. nitrobenzene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	*	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR CLEANING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
57. 2-nitrophenol	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	*			
58. 4-nitrophenol	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	0.007	ND			
60. 4,6-dinitro-o-cresol	A-1	1	ND	ND			
	A-2	1	ND	0.004			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
62. N-nitrosodiphenylamine	A-1	1	0.001	0.001			
	A-2	1	0.001	0.028			
	B-3	3	ND	*	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	0.006			
	D-2	1	ND	0.006			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	*	*		*
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	0.005	0.064	
	I-3	1	ND	0.016		0.001	
	K-1	2	*	0.004			
64. pentachlorophenol	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	0.020	0.001	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
65. phenol	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	0.001	0.11	0.1	0.1	
	C-2	3	*	0.022	0.014	0.012	
	D-1	1	*	ND			
	D-2	1	*	ND			
	F-3	3	*	0.005	0.006		
	F-4	3	*	0.002	*		
	H-1	1	ND	ND	ND		ND
	I-1	3	0.030	0.051	0.030	0.062	
	I-2	1	0.030	2.8	6.0	5.1	
	I-3	1	0.030	2.6		0.74	
	K-1	2	ND	0.214			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
66. bis(2-ethylhexyl)phthalate	A-1	1	ND	ND			
	A-2	1	ND	0.025			
	B-3	3	0.057	*	*	0.046	
	C-2	3	0.003	0.013	0.018	0.011	
	D-1	1	0.289	0.032			
	D-2	1	0.289	0.029			
	F-3	3	0.001	0.032	0.013		
	F-4	3	0.001	0.004	ND		
	H-1	1	*	0.134	0.085		0.196
	I-1	3	0.001	0.002	0.004	0.140	
	I-2	1	0.001	0.080	0.001	0.062	
	I-3	1	0.001	0.004		0.007	
	K-1	2	0.005	0.083			
67. butyl benzyl phthalate	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	0.002	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
68. di-n-butyl phthalate	A-1	1	ND	ND			
	A-2	1	ND	0.002			
	B-3	3	0.001	0.003	0.003	0.003	
	C-2	3	*	0.002	0.003	*	
	D-1	1	0.003	0.008			
	D-2	1	0.003	0.008			
	F-3	3	*	*	0.023		
	F-4	3	*	*	ND		
	H-1	1	ND	ND	0.001		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	0.001	ND	
	I-3	1	ND	ND		0.006	
	K-1	2	0.005	0.007			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR CLEANING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
69. di-n-octyl phthalate	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
70. diethyl phthalate	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	*	0.001	*	
	C-2	3	ND	*	*	*	
	D-1	1	ND	*			
	D-2	1	ND	0.001			
	F-3	3	ND	*	ND		
	F-4	3	ND	*	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	0.002	0.002	0.002	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	*			
72. benzo(a)anthracene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	ND	ND	
	D-1	1	*	ND			
	D-2	1	*	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	0.001	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
73. benzo(a)pyrene	A-1	1	ND	ND			
	A-2	1	ND	*			
	B-3	3	ND	0.005	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
76. chrysene	A-1	1	0.004	0.004			
	A-2	1	0.004	0.004			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	0.001	ND		
	H-1	1	ND	0.004	0.004		0.004
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.005	ND	0.001	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
78. anthracene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	*	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.008	ND	0.003	
	I-3	1	ND	ND		ND	
	K-1	2	ND	0.003			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR CLEANING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
80. fluorene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	*	ND	
	D-1	1	ND	ND			
	D-2	1	*	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
81. phenanthrene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	*	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.008	ND	0.003	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
84. pyrene	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	*	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.006	ND	0.002	
	I-3	1	ND	0.0004		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
85. tetrachloroethylene	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	0.019	*	0.003	*	
	D-1	2	ND	ND			
	D-2	2	ND	ND			
	F-3	2	ND	ND	ND		
	F-4	2	ND	ND	ND		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	ND	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	ND	ND			
86. toluene	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	*	0.001	0.001	*	
	D-1	2	ND	0.036			
	D-2	2	ND	0.033			
	F-3	2	*	0.032	0.030		
	F-4	2	*	*	*		
	H-1	2	ND	ND	ND		ND
	I-1	2	ND	0.002	ND	0.003	
	I-2	2	ND	0.69	0.11	0.25	
	I-3	2	ND	0.15		ND	
	K-1	2	ND	ND			
87. trichloroethylene	A-1	2	ND	ND			
	A-2	2	ND	ND			
	B-3	2	ND	ND	ND	ND	
	C-2	2	0.004	*	ND	ND	
	D-1	2	ND	0.001			
	D-2	2	ND	0.001			
	F-3	2	ND	ND	ND		
	F-4	2	ND	ND	ND		
	H-2	2	ND	ND	ND		ND
	I-1	2	ND	ND	ND	0.003	
	I-2	2	ND	ND	ND	ND	
	I-3	2	ND	ND		ND	
	K-1	2	ND	0.002			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
89. aldrin	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	0.000006	
	C-2	3	**	**	ND	0.0001	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	0.0001	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
90. dieldrin	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	**	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
97. endosulfan sulfate	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	**	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	**	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR CLEANING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
98. endrin	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	0.00227	
	C-2	3	ND	**	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
100. heptachlor	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	0.000004	
	C-2	3	ND	**	ND	0.0001	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	**	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
102. alpha-BHC	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	3	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	0.000004			
	D-2	1	ND	0.000006			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	0.000002	0.000002	0.000003		0.000003
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
103. beta-BHC	A-1	1	0.000264	0.000005			
	A-2	1	ND	ND			
	B-3	3	0.000008	ND	0.00001	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	0.000181	ND			
	D-2	1	0.000181	ND			
	F-3	3	ND	0.0002	ND		
	F-4	3	ND	ND	ND		
	H-1	1	0.000013	0.000016	ND		0.000012
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	0.000021	ND			
104. gamma-BHC	A-1	1	ND	ND			
	A-2	1	ND	0.000003			
	B-3	3	ND	ND	ND	0.000005	
	C-2	3	ND	**	ND	**	
	D-1	1	0.000006	ND			
	D-2	1	0.000006	ND			
	F-3	3	**	0.0016	ND		
	F-4	3	**	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	0.000002			
105. delta-BHC	A-1	1	0.000009	0.000015			
	A-2	1	0.000009	0.000033			
	B-3	3	0.000009	ND	ND	0.000013	
	C-2	3	**	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	0.0005	ND		
	F-4	3	ND	0.0002	ND		
	H-1	1	0.000006	0.000011	0.000135		0.000012
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	0.000018	0.000008			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
114. antimony	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	0.009	ND	0.081	0.010	
	I-2	1	0.009	0.105	ND	0.133	
	I-3	1	0.009	0.035		0.019	
	K-1	2	ND	ND			
115. arsenic	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	0.080	0.095	0.050	0.004	
	I-2	1	0.080	0.040	0.120	0.010	
	I-3	1	0.080	0.080		0.080	
	K-1	2	ND	ND			
119. chromium	A-1	1	ND	ND			
	A-2	1	ND	0.077			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	0.049	ND	
	D-1	1	0.010	ND			
	D-2	1	0.010	0.013			
	F-3	3	ND	ND	0.030		
	F-4	3	ND	0.020	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	0.070	ND	ND	
	I-2	1	ND	0.510	ND	0.53	
	I-3	1	ND	0.12		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
120. copper	A-1	1	ND	0.054			
	A-2	1	ND	0.626			
	B-3	1	0.15	ND	ND	ND	
	C-2	3	0.068	0.055	0.028	0.046	
	D-1	1	0.106	0.207			
	D-2	1	0.106	0.156			
	F-3	3	0.700	0.045	0.055		
	F-4	3	0.700	0.021	0.042		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	0.01	ND	0.01	
	I-2	1	ND	1.44	ND	0.91	
	I-3	1	ND	0.23		0.03	
	K-1	2	ND	0.85			
121. cyanide (total)	A-1	1	<0.01	<0.01			
	A-2	1	<0.01	<0.01			
	B-3	1	<0.01	<0.01	<0.01	<0.01	
	C-2	1	0	0	0	0	
	D-1	1	<0.02	<0.02			
	D-2	1	<0.02	<0.02			
	F-3	1	<0.02	<0.02	<0.02	<0.02	
	F-4	1	<0.02	<0.02	<0.02	<0.02	
	H-1	1	<0.01	<0.01	<0.01		<0.01
	I-1	1	0.7	0.025	0.18	0.01	
	I-2	1	0.7	0	0.034	0	
	I-3	1	0.7	0		0.014	
	K-1	2	<0.02	<0.02			
122. lead	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	0.1	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	ND	ND	ND	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
123. mercury	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.0005	ND	0.0003	
	I-3	1	ND	0.0001		ND	
	K-1	2	ND	ND			
124. nickel	A-1	1	ND	ND			
	A-2	1	ND	0.166			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.110	ND	0.1	
	I-3	1	ND	ND		ND	
	K-1	2	ND	ND			
125. selenium	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	0.020	0.010	0.050	0.110	
	I-2	1	0.020	0.030	0.110	0.220	
	I-3	1	0.020	0.220		0.28	
	K-1	2	ND	ND			

Table A-2 (Continued)

SAMPLING DATA BY POLLUTANT FOR
CLEANING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
126. silver	A-1	1	ND	ND			
	A-2	1	ND	ND			
	B-3	1	ND	ND	ND	ND	
	C-2	3	ND	ND	ND	ND	
	D-1	1	ND	ND			
	D-2	1	ND	ND			
	F-3	3	ND	ND	ND		
	F-4	3	ND	ND	ND		
	H-1	1	ND	ND	ND		ND
	I-1	3	ND	ND	ND	ND	
	I-2	1	ND	0.018	ND	0.006	
	I-3	1	ND	0.002		ND	
	K-1	2	ND	ND			
128. zinc	A-1	1	ND	0.108			
	A-2	1	ND	0.71			
	B-3	1	0.06	0.02	ND	0.02	
	C-2	3	ND	0.12	0.080	0.10	
	D-1	1	0.017	0.033			
	D-2	1	0.017	0.027			
	F-3	3	0.015	0.38	0.45		
	F-4	3	0.015	0.029	0.20		
	H-1	1	ND	ND	ND		ND
	I-1	3	1.13	0.253	0.99	0.269	
	I-2	1	1.13	29.8	0.583	17.0	
	I-3	1	1.13	11.9		0.43	
	K-1	2	ND	0.16			

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†Sample Type

1 - grab
2 - grab composite
3 - automatic composite

§See Figures VI-1 through VI-11.
*Indicates a reported less than value of <0.001 mg/l.
**Indicates a reported less than value of <0.0001 mg/l.
††Total phenols data from plant F were not used based on verification sampling.

NA - Pollutant was not analyzed.

ND - Not detected.

Table A-3

SAMPLING DATA BY POLLUTANT FOR FINISHING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD_5)	I-4	3	0.75	3.8	6.4	5.7	
	N-1	3	5	7	7		8
	Q-1	3	1	11	6		14
oil and grease	I-4	1	0	2.4	2.0	19.7	
	N-1	1	<1	22	16		19
	Q-1	1	<1	<1	<1		<1
pH	I-4	3	7.8	8.4	8.0	8.4	
	N-1	3	8.32	7.89	7.63		7.92
	Q-1	3	5.99	6.36	6.59		6.41
total suspended solids (TSS)	I-4	3	33	63	289	1359	
	N-1	3	3	7	<1		<1
	Q-1	3	<1	9.1	6.3		16
Nonconventional Pollutants							
aluminum	I-4	3	0.20	6.7	9.75	10.9	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	2.48	0.574		2.640
barium	I-4	3	0.03	0.03	0.04	0.03	
	N-1	3	ND	ND	ND		0.010
	Q-1	3	ND	0.062	ND		0.065
boron	I-4	3	0.70	0.70	0.59	0.62	
	N-1	3	ND	ND	ND		0.012
	Q-1	3	ND	ND	ND		0.018
calcium	I-4	3	7.04	12.4	13.6	11.3	
	N-3	3	22.1	2.97	19.3		3.04
	Q-1	3	16.3	17.0	12.9		17.2
chemical oxygen demand (COD)	I-4	3	225	170	325	290	
	N-1	3	20	20	20		25
	Q-1	3	16	47	<5		31

Table A-3 (Continued)

SAMPLING DATA BY POLLUTANT FOR
FINISHING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
iron	I-4	3	0.247	5.04	8.61	9.66	
	N-1	3	ND	0.051	ND		1.13
	Q-1	3	0.218	1.09	0.386		1.130
magnesium	I-4	3	3.05	3.58	3.82	3.63	
	N-1	3	3.19	0.386	2.96		0.401
	Q-1	3	5.050	5.050	3.46		5.100
manganese	I-4	3	0.009	0.084	0.064	0.152	
	N-1	3	ND	ND	ND		ND
	Q-1	3	0.186	0.304	0.266		0.308
sodium	I-4	3	359.0	317.0	318.0	326.0	
	N-1	3	34.3	67.3	37.2		60.8
	Q-1	3	8.28	11.70	15.6		11.900
titanium	I-4	3	0.01	0.054	0.076	0.076	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	ND		0.030
total organic carbon (TOC)	I-4	3	1.7	11.2	27.0	238	
	N-1	3	10	14	14		14
	Q-1	3	<1	15	2		26
total phenols	I-4	1	4.5	2.55	8.75	1.22	
	N-1	1	0.39	0.39	0.45		0.51
	Q-1	1	<0.01	<0.01	<0.01		<0.01
Priority Pollutants							
4. benzene	I-4	2	0.003	ND	0.009	0.007	
	N-1	2	ND	ND	ND		ND
	Q-1	2	ND	ND	ND		ND
8. 1,2,4-trichlorobenzene	I-4	3	ND	ND	ND	ND	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	0.015377	ND		0.019457

Table A-3 (Continued)

SAMPLING DATA BY POLLUTANT FOR
FINISHING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
11. 1,1,1-trichloroethane	I-4	2	ND	0.018	ND	ND	
	N-1	2	ND	ND	ND		ND
	Q-1	2	ND	ND	ND		ND
12. hexachloroethane	I-4	3	ND	ND	ND	ND	
	N-1	3	0.00706	0.006641	ND		ND
	Q-1	3	ND	ND	ND		ND
28. 3,3'-dichlorobenzidine	I-4	3	ND	ND	ND	ND	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	0.012897	ND		ND
34. 2,4-dimethyl phenol	I-4	3	ND	ND	ND	ND	
	N-1	3	ND	ND	ND		ND
	Q-1	3	0.006066	0.005919	0.005775		ND
38. ethylbenzene	I-4	2	ND	ND	ND	ND	
	N-1	2	ND	ND	ND		ND
	Q-1	2	ND	0.007981	0.011498		0.008547
44. methylene chloride	I-4	2	0.0090	ND	0.0060	ND	
	N-1	2	ND	ND	ND		ND
	Q-1	2	ND	ND	ND		ND
65. phenol	I-4	3	0.081	0.014	0.073	0.20	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	ND		ND
66. bis(2-ethylhexyl)phthalate	I-4	3	ND	0.005	0.040	0.014	
	N-1	3	ND	0.003189	0.006894		0.008537
	Q-1	3	0.00613	1.31412	0.011232		1.48768
68. di-n-butyl phthalate	I-4	3	ND	0.014	ND	0.017	
	N-1	3	ND	ND	0.009198		ND
	Q-1	3	0.003012	0.038445	0.080856		0.056065
71. dimethyl phthalate	I-4	3	ND	ND	ND	ND	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	0.003509	0.194388		ND

Table A-3 (Continued)

SAMPLING DATA BY POLLUTANT FOR FINISHING WATER SUBCATEGORY (RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
87. trichloroethylene	I-4	2	ND	ND	ND	ND	
	N-1	2	ND	0.009976	0.015113		0.010828
	Q-1	2	ND	ND	ND		ND
114. antimony	I-4	3	ND	ND	0.01	0.01	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	ND		ND
115. arsenic	I-4	3	0.10	0.11	0.11	0.01	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	ND		ND
119. chromium	I-4	3	ND	ND	0.01	0.01	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	ND		ND
120. copper	I-4	3	ND	ND	0.02	0.01	
	N-1	3	ND	ND	ND		0.018
	Q-1	3	ND	0.073	ND		0.072
121. cyanide	I-4	1	0	0.015	0	0.013	
	N-1			NA			
	Q-1			NA			
122. lead	I-4	3	ND	ND	ND	ND	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	0.179		ND
123. mercury	I-4	3	ND	0.0002	ND	0.0001	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	0.00025	ND		ND
124. nickel	I-4	3	ND	0.04	ND	0.04	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	ND		ND

Table A-3 (Continued)

SAMPLING DATA BY POLLUTANT FOR
FINISHING WATER SUBCATEGORY
(RAW WASTEWATER)

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
125. selenium	I-4	3	0.06	0.20	0.30	0.28	
	N-1	3	ND	ND	ND		ND
	Q-1	3	ND	ND	ND		ND
128. zinc	I-4	3	ND	0.084	0.229	0.176	
	N-1	3	ND	ND	ND		0.009
	Q-1	3	0.022	0.196	0.028		0.204

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†Sample Type

1 - grab
2 - grab composite
3 - automatic composite

§See Figures VI-9, VI-12, and VI-15.

NA - Pollutant was not analyzed.

ND - Not detected.

Table A-4

SAMPLING DATA BY POLLUTANT FOR
WASTEWATER TREATMENT SYSTEM ONE
(PLANT I)

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD_5)	I-3	1	1.7	3.2	6.6		
	I-5	1	1.7	5.1	1.6	4.4	
oil and grease	I-3	1	0	21.2	7.8		
	I-5	1	0	13.4	11.6	8.3	
pH	I-3	1	6.6	11.0	8.0		
	I-5	1	6.6	11.1	8.0	9.0	
total suspended solids (TSS)	I-3	1	56	1136	5671		
	I-5	1	56	356	305	329	
Nonconventional Pollutants							
aluminum	I-3	1	0.2	4.2	5.2		
	I-5	1	0.2	0.4	0.4	0.3	
ammonia nitrogen	I-3	1	0.2	75.0	67.5		
	I-5	1	0.2	95	40.3	166.2	
barium	I-3	1	0.03	0.16	0.05		
	I-5	1	0.03	0.07	0.07	ND	
boron	I-3	1	0.05	0.52	0.58		
	I-5	1	0.05	0.061	0.07	0.20	
calcium	I-3	1	51.3	45.2	26.8		
	I-5	1	51.3	36.0	31.5	7.23	
chemical oxygen demand (COD)	I-3	1	290	200	950		
	I-5	1	290	320	880	600	
cyanide amenable	I-3	1	0.6	0	0.01		
	I-5	1	0.6	0.021	0.021	0.022	
iron	I-3	1	0.067	10.6	4.73		
	I-5	1	0.067	0.404	0.202	0.224	

Table A-4 (Continued)

SAMPLING DATA BY POLLUTANT FOR
WASTEWATER TREATMENT SYSTEM ONE
(PLANT I)

Pollutant	Process Code†	Sample Type††	Source	Day 1	Day 2	Day 3	Duplicate
			Concentrations (mg/l)				
Nonconventional Pollutants (Continued)							
Kjeldahl nitrogen	I-3	1	3.85	1310	1188		
	I-5	1	3.85	1377	84.7	4750	
magnesium	I-3	1	7.17	6.42	5.27		
	I-5	1	7.17	3.28	49.3	1.12	
manganese	I-3	1	ND	0.111	0.084		
	I-5	1	ND	ND	ND	ND	
sodium	I-3	1	12.4	272	317		
	I-5	1	12.4	3970	2320	958	
surfactants	I-3	1	0.15	0.15	0.112		
	I-5	1	0.15	0.70	0.125	0.07	
tin	I-3	1	ND	ND	ND		
	I-5	1	ND	ND	ND	0.8	
titanium	I-3	1	ND	0.060	0.075		
	I-5	1	ND	ND	ND	ND	
total dissolved solids (TDS)	I-3	1	201.5	13000	812.5		
	I-5	1	201.5	4517.5	3315	1950	
total organic carbon (TOC)	I-3	1	11.0	5316	4998		
	I-5	1	11.0	2813	4628	5250	
total phenols	I-3	1	2.7	730	0.83		
	I-5	1	2.7	322	591	0.72	
total phosphorus	I-3	1	3.18	32.1	5.17		
	I-5	1	3.18	99.6	224	45.2	
vanadium	I-3	1	ND	ND	ND		
	I-5	1	ND	0.022	0.022	0.022	
Priority Pollutants							
4. benzene	I-3	2	0.007	0.01	0.009		
	I-5	2	0.007	0.009	0.010	0.003	0.010

Table A-4 (Continued)

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM ONE (PLANT I)

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
11. 1,1,1-trichloroethane	I-3	2	ND	ND	ND		
	I-5	2	ND	0.002	0.003	ND	ND
15. 1,1,2,2-tetrachloroethane	I-3	2	ND	ND	ND		
	I-5	2	ND	ND	ND	ND	0.002
21. 2,4,6-trichlorophenol	I-3	1	ND	ND	ND		
	I-5	1	ND	0.001	0.0005	ND	0.002
23. chloroform	I-3	2	0.12	0.004	0.002		
	I-5	2	0.12	ND	0.007	0.010	0.006
24. 2-chlorophenol	I-3	1	ND	0.006	ND		
	I-5	1	ND	0.014	0.005	0.002	0.009
31. 2,4-dichlorophenol	I-3	1	ND	0.001	ND		
	I-5	1	ND	0.005	0.002	ND	0.006
39. fluoranthene	I-3	1	ND	0.004	ND	ND	
	I-5	1	ND	ND	ND	ND	ND
44. methylene chloride	I-3	2	0.005	0.005	ND		
	I-5	2	0.005	0.010	ND	ND	ND
48. dichlorobromomethane	I-3	2	0.009	ND	ND		
	I-5	2	0.009	ND	ND	ND	ND
51. chlorodibromomethane	I-3	2	0.004	ND	ND		
	I-5	2	0.004	ND	ND	ND	ND
62. N-nitrosodiphenylamine	I-3	1	ND	0.016	0.001		
	I-5	1	ND	0.004	0.004	0.006	0.003
64. pentachlorophenol	I-3	1	ND	ND	ND		
	I-5	1	ND	0.002	ND	ND	0.001
65. phenol	I-3	1	0.030	2.6	0.74		
	I-5	1	0.030	7.7	2.0	1.5	2.7
66. bis(2-ethylhexyl)phthalate	I-3	1	0.001	0.004	0.007		
	I-5	1	0.001	0.0007	0.006	0.012	0.003

Table A-4 (Continued)

SAMPLING DATA BY POLLUTANT FOR
WASTEWATER TREATMENT SYSTEM ONE
(PLANT I)

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
68. di-n-butyl phthalate	I-3	1	ND	ND	0.006		
	I-5	1	ND	0.002	0.002	0.002	0.004
84. pyrene	I-3	1	ND	0.0004	ND		
	I-5	1	ND	ND	ND	ND	ND
86. toluene	I-3	2	ND	0.15	ND		
	I-5	2	ND	0.11	0.039	0.032	0.103
114. antimony	I-3	1	0.009	0.035	0.019		
	I-5	1	0.009	0.141	0.038	0.087	
115. arsenic	I-3	1	0.080	0.080	0.080		
	I-5	1	0.080	0.095	0.22	0.036	
119. chromium	I-3	1	ND	0.12	ND		
	I-5	1	ND	ND	ND	ND	
121. cyanide (total)	I-3	1	0.700	0	0.014		
	I-5	1	0.700	0.024	0.017	0.018	
123. mercury	I-3	1	ND	0.0001	ND		
	I-5	1	ND	ND	ND	0.0001	
124. nickel	I-3	1	ND	ND	ND		
	I-5	1	ND	ND	ND	0.110	
125. selenium	I-3	1	0.020	0.220	0.28		
	I-5	1	0.020	0.110	0.090	0.16	
126. silver	I-3	1	ND	0.002	ND		
	I-5	1	ND	ND	ND	ND	

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†I-3 is influent, I-5 is effluent; see Figure VI-9.

††Sample Type

1 - grab
2 - grab composite

ND - Not detected.

Table A-5

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM TWO (PLANT I)

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD_5)	I-4	3	0.75	3.8	6.4	5.7	
	I-6	1	0.75	2.65	3.8	5.6	
oil and grease	I-4	1	0	2.4	2.0	19.7	
	I-6	1	0	0	0	0	
pH	I-4	3	7.8	8.4	8.0	8.4	
	I-6	1	7.8	9.1	6.5	7.5	
total suspended solids (TSS)	I-4	3	33	63	289	1359	
	I-6	1	33	12	7	0	
Nonconventional Pollutants							
aluminum	I-4	3	0.200	6.7	9.75	10.9	
	I-6	1	0.200	0.200	0.200	0.300	
ammonia nitrogen	I-4	3	0.45	0.25	57.5	3.0	
	I-6	1	0.45	0.38	0.35	0	
barium	I-4	3	0.030	0.030	0.040	0.030	
	I-6	1	0.030	0.030	ND	0.030	
boron	I-4	3	0.700	0.700	0.590	0.620	
	I-6	1	0.700	0.520	0.520	0.730	
calcium	I-4	3	7.04	12.4	13.6	11.3	
	I-6	1	7.04	17.1	11.6	11.4	
chemical oxygen demand (COD)	I-4	3	225	170	325	290	
	I-6	1	225	125	295	40	
cyanide amenable	I-4	3	0	0.013	0	0.013	
	I-6	1	0	0.008	0.006	0.006	
iron	I-4	3	0.247	5.04	8.61	9.66	
	I-6	1	0.247	0.089	0.314	0.089	

Table A-5 (Continued)

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM TWO (PLANT I)

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
Kjeldahl nitrogen	I-4	3	8.55	4.5	1380	51.9	
	I-6	1	8.55	7.22	6.2	1.76	
magnesium	I-4	3	3.05	3.58	3.82	3.63	
	I-6	1	3.05	3.76	3.24	3.22	
manganese	I-4	3	0.009	0.084	0.064	0.152	
	I-6	1	0.009	0.016	ND	ND	
sodium	I-4	3	359	317	318	326	
	I-6	1	359	291	325	328	
surfactants	I-4	3	0.25	0.20	0.20	0.30	
	I-6	1	0.25	0.15	0.15	0.10	
tin	I-4	3	ND	ND	ND	ND	
	I-6	1	ND	1.9	ND	ND	
titanium	I-4	3	0.010	0.054	0.076	0.076	
	I-6	1	0.010	ND	ND	ND	
total dissolved solids (TDS)	I-4	3	981.5	1040	910	910	
	I-6	1	981.5	715	897	981.5	
total organic carbon (TOC)	I-4	3	1.7	11.2	27.0	238	
	I-6	1	1.7	25.2	1.3	5.6	
total phenols	I-4	3	4.5	2.55	8.75	1.22	
	I-6	1	4.5	15.10	0.08	4.93	
total phosphorus	I-4	3	0.52	0.10	0.96	1.94	
	I-6	1	0.52	4.22	1.06	0	
vanadium	I-4	3	ND	ND	ND	0.006	
	I-6	1	ND	ND	ND	ND	
Priority Pollutants							
4. benzene	I-4	2	0.003	ND	0.009	0.007	
	I-6	2	0.003	0.008	0.008	ND	

Table A-5 (Continued)

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM TWO (PLANT I)

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
11. 1,1,1-trichloroethane	I-4	2	ND	0.018	ND	ND	
	I-6	2	ND	ND	ND	ND	
44. methylene chloride	I-4	2	0.009	ND	0.006	ND	
	I-6	2	0.009	0.004	0.014	ND	
65. phenol	I-4	3	0.081	0.014	0.073	0.200	
	I-6	1	0.081	0.016	0.250	0.130	
66. bis(2-ethylhexyl)phthalate	I-4	3	ND	0.005	0.040	0.014	
	I-6	1	ND	0.020	0.002	ND	
68. di-n-butyl phthalate	I-4	3	ND	0.014	ND	0.017	
	I-6	1	ND	ND	0.012	ND	
69. di-n-octyl phthalate	I-4	3	ND	ND	ND	ND	
	I-6	1	ND	ND	0.053	ND	
70. diethyl phthalate	I-4	3	ND	ND	ND	ND	
	I-6	1	ND	ND	0.0009	ND	
86. toluene	I-4	2	ND	ND	ND	ND	
	I-6	2	ND	0.001	ND	ND	
114. antimony	I-4	3	ND	ND	0.010	0.010	
	I-6	1	ND	ND	0.005	0.009	
115. arsenic	I-4	3	0.100	0.110	0.110	0.010	
	I-6	1	0.100	0.095	0.110	0.018	
119. chromium	I-4	3	ND	ND	0.010	0.010	
	I-6	1	ND	ND	ND	ND	
120. copper	I-4	3	ND	ND	0.020	0.010	
	I-6	1	ND	ND	ND	ND	
121. cyanide (total)	I-4	1	0	0.015	0	0.013	
	I-6	1	0	0.008	0.006	0.006	
123. mercury	I-4	3	ND	0.0002	ND	0.0001	
	I-6	1	ND	ND	0.0001	0.0004	

Table A-5 (Continued)

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM TWO (PLANT I)

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
124. nickel	I-4	3	ND	0.040	ND	0.040	
	I-6	1	ND	ND	0.040	ND	
125. selenium	I-4	3	0.060	0.200	0.300	0.280	
	I-6	1	0.060	0.160	0.060	0.090	
128. zinc	I-4	3	ND	0.084	0.229	0.176	
	I-6	1	ND	0.015	ND	ND	

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†I-4 is influent, I-6 is effluent; see Figure VI-9.

††Sample Type

1 - grab
2 - grab composite
3 - automatic composite

ND - Not detected.

Table A-6

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM AT PLANT M

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD$_5$)	M-3	1	38	3.5			
	M-4	1	38	18			
oil and grease	M-3	1	<1	72			
	M-4	1	<1	74			
pH	M-3	1	7.57	7.99			
	M-4	1	7.57	7.83			
total suspended solids (TSS)	M-3	1	<1	23			
	M-4	1	<1	9			
Nonconventional Pollutants							
chemical oxygen demand (COD)	M-3	1	90	<10			
	M-4	1	90	46			
total organic carbon (TOC)	M-3	1	<1	21			
	M-4	1	<1	30			
total phenols	M-3	1	<0.005	0.075			
	M-4	1	<0.005	0.280			

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†M-3 is influent, M-4 is effluent; see Figure VI-13.

††Sample Type

1 - grab

Table A-7

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM AT PLANT N

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD$_5$)	N-1	3	5	7	7		8
	N-4	3	5	7	9		
oil and grease	N-1	1	<1	22	16		19
	N-4	1	<1	15	<1		
pH	N-1	3	8.32	7.89	7.63		7.92
	N-4	3	8.32	7.9	7.21		
total suspended solids (TSS)	N-1	3	3	9	<1		<1
	N-4	3	3	4	8		
Nonconventional Pollutants							
chemical oxygen demand (COD)	N-1	3	20	20	20		25
	N-4	3	20	30	25		
total organic carbon (TOC)	N-1	3	10	14	14		14
	N-4	3	10	14	13		
total phenols	N-1	1	0.39	0.39	0.45		0.51
	N-4	1	0.39	0.38	7.49		

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†N-1 is influent, N-4 is effluent; see Figure VI-13.

††Sample Type

1 - grab
3 - grab composite

Table A-8

SAMPLING DATA BY POLLUTANT FOR WASTEWATER TREATMENT SYSTEM AT PLANT R

Pollutant	Process Code†	Sample Type††	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD_5)	R-1	2	4	6			
	R-2	2	4	4			
	R-4	1	4	4			
oil and grease	R-1	2	9	6			
	R-2	2	9	8			
	R-4	1	9	7			
pH	R-1	1	7.35	7.21			
	R-2	1	7.35	7.36			
	R-4	1	7.35	7.35			
total suspended solids (TSS)	R-1	2	<1	<1			
	R-2	2	<1	<1			
	R-4	1	<1	<1			
Nonconventional Pollutants							
chemical oxygen demand (COD)	R-1	2	50	16			
	R-2	2	50	20			
	R-4	1	50	16			
total organic carbon (TOC)	R-1	2	7	6			
	R-2	2	7	5			
	R-4	1	7	6			
total phenols	R-1	1	0.17	0.42			
	R-2	1	0.17	0.34			
	R-4	1	0.17	0.40			

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†R-1 and R-2 are influent, R-4 is recycle; see Figure VI-17.

††Sample Type

1 - grab
2 - grab composite

Table A-9

SOLVENT RECOVERY WASTEWATER DATA - PLANT G

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Conventional Pollutants							
biological oxygen demand (BOD_5)	G-2	3	<5.0	7.0	††	††	10.0
oil and grease	G-2	2	6.0	8.0	8.0	<4.0	<4.0
pH	G-2	2	7.4	3.6	3.6	3.6	3.6
total suspended solids	G-2	3	16.0	14.0	14.0	<4.0	18.0
Nonconventional Pollutants							
acetone	G-2	3	NA	0.020	0.077	0.144	0.027
ammonia nitrogen	G-2	3	<0.05	<0.05	0.19	0.05	<0.05
boron	G-2	3	ND	0.042	ND	ND	
bromide	G-2	3	0.56	<0.4	<0.4	0.8	<0.4
calcium	G-2	3	0.062	0.041	0.144	0.044	
chemical oxygen demand (COD)	G-2	3	<5.0	435	465	482	470
fluoride	G-2	3	0.46	0.13	0.18	0.25	0.18
iron	G-2	3	ND	1.009	0.886	0.862	
Kjeldahl nitrogen	G-2	3	<1.0	<1.0	<1.0	<1.0	<1.0
magnesium	G-2	3	0.181	0.163	0.17	0.167	
nitrate/nitrite	G-2	3	5.8	<0.1	0.2	<0.1	<0.1
sodium	G-2	3	ND	ND	ND	ND	
sulfate	G-2	2	1040	<5.0	<5.0	<5.0	<5.0
sulfide	G-2	3	<1.0	<1.0	<1.0	<1.0	<1.0
surfactants	G-2	3	<0.01	<0.01	0.02	0.03	<0.01

Table A-9 (Continued)

SOLVENT RECOVERY WASTEWATER DATA - PLANT G

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l) Source	Day 1	Day 2	Day 3	Duplicate
Nonconventional Pollutants (Continued)							
titanium	G-2	3	0.01	ND	0.008	0.011	
total organic carbon (TOC)	G-2	3	<1.0	165	179	174	178
total phenols	G-2	2	0.023	0.170	0.19	0.15	0.150
total phosphorus	G-2	3	0.04	0.04	0.04	<0.02	0.04
vanadium	G-2	3	ND	0.046	ND	ND	
yttrium	G-2	3	ND	ND	ND	ND	
Priority Pollutants							
1. acenaphthene	G-2	3	ND	ND	0.094	ND	ND
6. carbon tetrachloride	G-2	2	0.001	ND	0.018	ND	ND
11. 1,1,1-trichloroethane	G-2	2	0.004	0.001	0.002	0.001	0.001
18. bis(2-chloroethyl)ether	G-2	3	ND	0.001	ND	ND	0.003
23. chloroform	G-2	2	0.006	0.002	0.004	0.001	0.002
44. methylene chloride	G-2	2	0.001	0.008	0.026	0.007	0.008
47. bromoform	G-2	2	ND	ND	*	ND	*
62. N-nitrosodiphenylamine	G-2	3	ND	ND	*	*	ND
65. phenol	G-2	3	ND	0.011	*	0.090	ND
66. bis(2-ethylhexyl)phthalate	G-2	3	0.015	0.005	0.003	0.004	0.116
68. di-n-butyl phthalate	G-2	3	0.003	0.007	0.012	0.008	0.003
70. diethyl phthalate	G-2	3	0.005	0.136	0.439	0.177	ND
71. dimethyl phthalate	G-2	3	ND	0.002	0.0730	.043	ND

Table A-9 (Continued)

SOLVENT RECOVERY WASTEWATER DATA - PLANT G

Pollutant	Process Code§	Sample Type†	Concentrations (mg/l)				
			Source	Day 1	Day 2	Day 3	Duplicate
Priority Pollutants (Continued)							
72. benzo(a)anthracene	G-2	3	ND	*	*	*	ND
73. benzo(a)pyrene	G-2	3	ND	*	0.002	*	0.002
80. fluorene	G-2	3	ND	ND	*	ND	ND
84. pyrene	G-2	3	ND	ND	ND	*	ND
85. tetrachloroethylene	G-2	2	0.012	ND	ND	ND	ND
86. toluene	G-2	3	ND	ND	ND	ND	0.001
87. trichloroethylene	G-2	2	0.343	ND	ND	0.001	ND
100. heptachlor	G-2	3	ND	0.000150	ND	ND	ND
101. heptachlor epoxide	G-2	3	ND	ND	0.000084	ND	ND
102. alpha-BHC	G-2	3	ND	ND	ND	0.000006	ND
103. beta-BHC	G-2	3	0.000166	0.000225	ND	ND	0.000011
120. copper	G-2	3	ND	0.037	0.086	0.072	
121. cyanide (total)	G-2	2	<0.02	<0.02	<0.02	<0.02	<0.02
128. zinc	G-2	3	ND	0.026	0.004	ND	

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†Sample Type

2 - grab composite
3 - automatic composite

§See Figures VI-1 through VI-11.

††Value not used in the subcategory average calculation because it was suspected to be result of laboratory contamination.

*Indicates a reported less than value of <0.001 mg/l.

NA - Pollutant was not analyzed.

ND - Not detected.

APPENDIX B

STATE INDUSTRIAL GUIDES

APPENDIX B

STATE INDUSTRIAL GUIDES

This appendix lists the State Industrial Guides used to estimate the size of the PM&F category. This estimate is described in Section IV.

State	Edition	Title and Publisher
Alabama	1980-81	Alabama Director of Mining and Manufacturing, Industrial Research Department, Alabama Development Office
Arizona	1982	Arizona Directory of Manufacturers, Pheonix Metropolitan Chamber of Commerce
Arkansas	1982	Arkansas Directory of Manufacturers, Arkansas Industrial Development Foundation
California	1983	California Manufacturer's Register, California Manufacturer's Association
Colorado	1982	Directory of Colorado Manufacturers, University of Colorado, Boulder, Business Division, College of Business and Administration
Connecticut	1982	MacRae's Connecticut State Industrial Directory
Delaware	1981-82	Delaware Directory of Commerce and Industry, Delaware State Chamber of Commerce
Florida	1982	Directory of Florida Industries, The Florida Chamber of Commerce c 1981
Georgia	1980-81	Georgia Manufacturing Directory, Georgia Department of Industry and Trade, c. 1980

State	Edition	Title and Publisher
Idaho	1982	Idaho Manufacturing Directory University of Idaho Center for Business Development and Research
Illinois	1983	Illinois Manufacturers Directory, Manufacturer's News Inc., Chicago, IL Editor, Louise M. West
Indiana	1983	Harris Indiana Marketer's Industrial Directory, Harris Publishing Company (1983, Ohio), State Directory Division
Iowa	1981-82	Directory of Iowa Manufacturers, Iowa Development Commission
Kansas	1981-82	Directory of Kansas Manufacturers and Products, Kansas Department of Economic Development
Kansas	1981-82	Directory of Kansas Manufacturers and Products, Kansas Economic Development Commission
Kentucky	1983	Kentucky Directory of Manufacturers, Kentucky Department of Economic Development
Louisiana	1982	Directory of Louisiana Manufacturers, Louisiana Department of Commerce
Maine	1981-82	Directory of New England Manufacturers, New England Council, George D. Hall Company
Maryland	1981-82	The Directory of Maryland Manufacturers, State of Maryland, Department of Economic and Community Development
Massachusetts	1981-82	Directory of Massachusetts Manufacturers, George D. Hall's Association Industires of Mass c. 1981
Michigan	1982	The Directory of Michigan Manufacturers, Pick Publications, Inc.
Minnesota	1981	Minnesota Directory of Manufacturers, Minnesota Department of Economic Development

State	Edition	Title and Publisher
Mississippi	1980	Mississippi Manufacturers Directory Mississippi Research and Development Center, printed 1979
Missouri	1982	Missouri Directory, Mining and Manufacturing Industires Services and Supplies, Information Data Company
Nebraska	1982-83	A Directory of Nebraska Manufacturers and Their Products, Nebraska Department of Economic Development
Nevada	1981	Nevada Industrial Directory, Nevada Department of Economic Development
New Hampshire	1982-83	Made in New Hampshire, State of New Hampshire, Office of Industrial Development, Division of Economic Development
New Jersey	1983	New Jersey State Industrial Directory MacRae's Blue Book, Inc.
New York	1983	New York State Industrial Directory, MacRae's Blue Book, Inc. Editor, Barbara Sadic
North Carolina	1981-82	Directory of North Carolina Manufacturing Firms, North Carolina Department of Commerce
North Dakota	1978-79	Directory of North Dakota Manufacturing, North Dakota Business and Industrial Development Department
Ohio	1983	Ohio Marketers Industrial Directory, Harris Publishing Company
Oklahoma	1980	Oklahoma Directory of Manufacturers and Products, Industrial Development Department
Pennsylvania	1982	MacRae's Pennsylvania State Industrial Directory
Rhode Island	1981-82	Rhode Island Directory of Manufacturers, Rhode Island Directory of Economic Development

State	Edition	Title and Publisher
South Carolina	1983	South Carolina 1983 Industrial Directory, South Carolina State Development Board
South Dakota	1981-82	South Dakota Manufacturers & Processors Directory, Department of Economic and Tourism Development
Tennessee	1982	Tennessee Directory of Manufacturers, Tennessee Department of Economic and Community Development
Texas	1983	Directory of Texas Manufacturers, Bureau of Business Research, University of Texas, Austin
Virginia	1981-82	Virginia Industrial Directory, Virginia State Chamber of Commerce
Washington	1982-83	Washington Manufacturers Register, Times Mirror Press, Washington State Department of Commerce and Economic Development
West Virginia	1980	West Virginia Manufacturer's Directory, Governor's Office of Economic and Community Development Department
Wisconsin	1983	Classified Directory of Wisconsin Manufacturers, Wisconsin Association of Manufacturers and Commerce

APPENDIX C

POLLUTANT REMOVALS

APPENDIX C

POLLUTANT REMOVALS

This appendix explains how PM&F subcategory pollutant mass removals were calculated for the model treatment technologies. These removals apply to the BPT and BAT effluent limitations guidelines and to NSPS. Table C-1 contains the subcategory pollutant average concentrations and total estimated direct discharge masses for pollutants found in treatable concentrations for each subcategory.

CONTACT COOLING AND HEATING WATER SUBCATEGORY

BPT Effluent Limitations Guidelines Pollutant Mass Removals

No model treatment technology was selected as the basis for the BPT effluent limitations guidelines for this subcategory. BPT effluent limitations guidelines were established to ensure that plants continue the good housekeeping practices observed during the sampling episodes conducted during development of this regulation. They are based on the results of a statistical evaluation of the pollutant concentrations in contact cooling and heating process waters. There are only minimal costs associated with the final BPT effluent limitations guidelines and there are only minimal pollutant mass removals. See Section X for a discussion of the BPT effluent limitation guidelines for this subcategory.

BAT Effluent Limitations Guidelines Pollutant Mass Removals

BAT effluent limitations guidelines for this subcategory are equal to BPT effluent limitations guidelines except for the priority pollutant bis(2-ethylhexyl) phthalate. BAT effluent limitations guidelines are reserved for bis(2-ethylhexyl) phthalate. After further study, EPA will propose and promulgate BAT effluent limitations guidelines for this pollutant. The technology considered to treat bis(2-ethylhexyl) phthalate is activated carbon adsorption.

To estimate mass removals at BAT for bis(2-ethylhexyl) phthalate, the theoretical treatability limit for this pollutant presented in Table VII-9 was used. This limit was based on technology that includes activated carbon adsorption. Refer to Table C-2 for the influent and effluent concentrations and the estimated pollutant mass removals for the activated carbon process.

The influent and effluent concentrations listed on Table C-2 are from Tables C-1 and VII-9, respectively. The percentage removal (i.e., 89.8 percent) based on these concentrations was applied to

Table C-1

AVERAGE CONCENTRATIONS AND ESTIMATED MASSES FOR POLLUTANTS FOUND IN TREATABLE CONCENTRATIONS

	Average Concentrations (mg/l)			Estimated Pollutant Mass for Direct Dischargers (kg/yr)		
Conventional Pollutants	Contact Cooling and Heating Water	Cleaning Water	Finishing Water	Contact Cooling and Heating Water	Cleaning Water	Finishing Water
BOD_5	*	90	*	*	25,600	*
Oil and Grease	*	48	*	*	14,200	*
TSS	*	714	*	*	199,000	3,630
pH Range	5.4-8.3	1.6-11.5	6.0-8.4	NA	NA	NA
Nonconventional Pollutants						
COD	*	115	*	*	32,000	*
TOC	*	634	*	*	177,000	*
Total Phenols	*	36	*	*	7,400	*
Priority Pollutants						
65. phenol	*	0.198	*	*	59	*
66. bis(2-ethylhexyl) phthalate	0.098	*	0.479	9,470	*	18
68. di-n-butyl phthalate	*	*	0.031	*	*	1
71. dimethyl phthalate	*	*	0.034	*	*	1
128. zinc	*	0.598	*	*	178	*

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*Average concentration is below treatability limit.

NA - Not applicable.

Table C-2

POLLUTANT REMOVAL - ACTIVATED CARBON ADSORPTION CONTACT COOLING AND HEATING WATER SUBCATEGORY

Priority Pollutant	Influent Concentration (mg/l)	Effluent Concentration (mg/l)	Pollutant* % Removal	Pollutant Mass in Process Water (kg/yr)	Pollutant Mass Removal (kg/yr)	Pollutant Mass Remaining After Treatment (kg/yr)
66. bis(2-ethylhexyl) phthalate	0.098	0.010	89.8	9,470	8,500	970

---

*Pollutant percent removal is based on treatability limit (i.e., 0.010 mg/l) of bis(2-ethylhexyl) phthalate from U.S. EPA, Treatability of Organic Priority Pollutants - Part C - Their Estimated (30-Day Ave.) Treated Effluent Concentration - A Molecular Engineering Approach, Murray P. Strier, 11 July 1978.

the mass of bis(2-ethylhexyl) phthalate in contact cooling and heating waters listed in Table C-1 to estimate the pollutant mass removal.

NSPS Pollutant Mass Removals

NSPS are equal to BPT effluent limitations guidelines except for bis(2-ethylhexyl) phthalate. NSPS are reserved for bis(2-ethylhexyl) phthalate. After further study, EPA will propose and promulgate NSPS for this pollutant. The model treatment technology considered to treat bis(2-ethylhexyl) phthalate is pH adjustment (as needed) and activated carbon adsorption.

NSPS ensure that the good housekeeping practices observed during the sampling episodes conducted during development of this regulation will be employed at new sources. They are based on the results of a statistical evaluation of pollutant concentrations in contact cooling and heating waters. The pollutant concentrations used to calculate NSPS for this subcategory are presented in Table X-1. There are only minimal costs and there are minimal pollutant mass removals for NSPS for this subcategory.

CLEANING WATER SUBCATEGORY

BPT Effluent Limitations Guidelines Pollutant Mass Removals

The model treatment technology for the BPT effluent limitations guidelines for the cleaning water subcategory consists of equalization, pH adjustment, and a package activated sludge plant. Table C-3 presents the model treatment technology influent and effluent pollutant concentrations and the treatment technology percent removals. The sources of the pollutant percent removals are also listed in Table C-3.

The percent removal for the priority pollutant zinc is based on a technology that includes lime addition, settling, and filtration. The treatability limit for this technology is 0.230 mg/l.

There are no treatability data for zinc removal in activated sludge. However, literature does report a percent removal (99 percent). This percent removal, when applied to the influent concentration of 0.598 mg/l, gives an effluent concentration of 0.006 mg/l. Because this concentration is well below the treatability limit of the technology described above to treat metals (i.e., lime addition, settle, and filter), the effluent concentration for zinc was adjusted to 0.230 mg/l and the percent removal was correspondingly adjusted to 61.5 percent.

The percent removals in Table C-3 were applied to the cleaning water pollutant masses presented in Table C-1 to estimate the

Table C-3

POLLUTANT CONCENTRATIONS AND PERCENT REMOVALS
BPT MODEL TREATMENT TECHNOLOGY
CLEANING WATER SUBCATEGORY

Conventional Pollutants	Influent Concentration (mg/l)	Effluent Concentration (mg/l)	Pollutant % Removal	% Removal Source
BOD_5	90	22	76	1
Oil and Grease	48	17	65	1
TSS	714	36	95	1
Nonconventional Pollutants				
COD	115	43	63	2
TOC	634	234	63	2
Total Phenols	36	14	60	2
Priority Pollutants				
65. phenol	0.198	0.050	74.7	3
128. zinc	0.598	0.230	61.5	4

---

1. Percent removals were calculated using the effluent concentration data transferred from the organic chemicals, plastics, and synthetic fibers category. Refer to Appendix D for details.

2. Percent removals are from U.S. EPA, Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, July 1980, EPA 600/8-80-842c.

3. Percent removal was calculated using the pollutant treatability limit from U.S. EPA, Treatability of Organic Priority Pollutants - Part C - Their Estimated (30-Day Ave.) Treated Effluent Concentration - A Molecular Engineering Approach, Murray P. Strier, 11 July 1978.

4. Percent removal was calculated from treatability limit for lime, settle, and filtration technology in the U.S. EPA Development Document for Effluent Guidelines and Standards for the Nonferrous Metals Manufacturing Point Source Category Phase II, July, 1984.

pollutant mass removals for the BPT effluent limitations guidelines. Table C-4 lists the estimated cleaning water subcategory pollutant mass removals at BPT and the mass of pollutants remaining after BPT.

BAT Effluent Limitations Guidelines Pollutant Mass Removals

For the cleaning water subcategory, BAT effluent limitations guidelines are equal to BPT effluent limitations guidelines. Consequently, the BAT pollutant mass removals are equal to BPT removals as listed in Table C-4.

NSPS Pollutant Mass Removals

Pollutant mass removals for direct dischargers at a new plant in the cleaning water subcategory were based on the performance of the model treatment technology that was selected at BPT. To estimate the pollutant masses discharged and the pollutant mass removals for NSPS, the pollutant masses at BPT were divided by the estimated number of direct discharging cleaning processes (i.e., 104 cleaning processes). This approach assumes that process waters at a new discharging source have the same pollutant influent and effluent concentrations as listed in Table C-3. Hence, the pollutant percent removals are the same. Refer to Table C-5 for the cleaning water subcategory new source pollutant masses, mass removals, and masses remaining after treatment.

EPA considered NSPS based on the performance of a package activated sludge plant followed by a filter. Refer to Table C-6 for the filter pollutant mass removals and for filter influent and effluent concentrations. The mass of pollutants in the influent to the filter and the filter influent pollutant concentrations are equal to the pollutant masses remaining after activated sludge treatment (see Table C-5) and the effluent concentrations presented on Table C-3, respectively.

FINISHING WATER SUBCATEGORY

BPT Effluent Limitations Guidelines Pollutant Mass Removals

The model treatment technology (i.e., settling) for BPT for this subcategory removes total suspended solids (TSS). Table C-7 presents the TSS influent and effluent concentrations, the TSS percent removal, the pollutant mass removals based on the percent removal, and the pollutant mass remaining after treatment. The TSS pollutant mass removal for the BPT effluent limitations guidelines is 2,520 kg/yr.

The TSS percent removal is 69.5 percent. This removal was calculated using the influent concentration of 95 mg/l and the median

Table C-4

BPT POLLUTANT MASS REMOVALS
CLEANING WATER SUBCATEGORY

Conventional Pollutants	Pollutant Mass in Process Waters (kg/yr)	Pollutant Mass Removal (kg/yr)	Pollutant Mass Remaining After Treatment (kg/yr)
BOD_5	25,600	19,300	6,300
Oil and Grease	14,200	9,170	5,030
TSS	199,000	189,000	10,000
TOTAL	238,800	217,470	21,330
Nonconventional Pollutants			
COD	32,000	20,200	11,800
TOC	177,000	112,000	65,000
Total Phenols	7,400	4,440	3,040
TOTAL	216,400	136,640	79,840
Priority Pollutants			
65. phenol	59	44.3	14.7
128. zinc	178	110	68.0
TOTAL	237	154.3	82.7

Table C-5

NSPS POLLUTANT MASS REMOVALS CLEANING WATER SUBCATEGORY

Conventional Pollutant	New Source* Pollutant Mass (kg/yr)	Pollutant Mass Removal (kg/yr)	Pollutant Mass Remaining After Treatment (kg/yr)
BOD_5	246	186	60
Oil and Grease	137	88.2	48.8
TSS	1,910	1,820	90
TOTAL	2,293	2,094.2	198.8
Nonconventional Pollutant			
COD	308	194	114
TOC	1,700	1,080	620
Total Phenols	71	42.7	28.3
TOTAL	2,079	1,316.7	762.3
Priority Pollutant			
65. phenol	0.569	0.426	0.143
128. zinc	1.71	1.06	0.650
TOTAL	2.279	1.486	0.793

---

*Obtained by dividing the pollutant mass listed in Table C-1 for the cleaning water subcategories by the estimated number of direct discharging cleaning water processes.

Table C-6

NSPS CONVENTIONAL POLLUTANT MASS REMOVALS FOR FILTRATION CLEANING WATER SUBCATEGORY

Conventional Pollutants	Pollutant Mass Entering Filter from Package Activated Sludge Plant Unit (kg/yr)	Influent Concentration (mg/l)*	Percent Removal†	Effluent Concentration (mg/l)**	Filter Pollutant Mass Removal (kg/yr)
BOD_5	60	22	13.6	19	10
Oil and Grease	48.8	17	20.0	13.6	10
TSS	90	36	67	12	60
TOTAL	198.8				80

---

*Effluent from package activated sludge plant.

†Percent removals for BOD_5 and TSS were calculated using the median effluent concentrations for granular media filtration in the U.S. EPA, Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, July 1980, EPA 600/8-80-842c.

The oil and grease percent removal is the median percent removal for granular media filtration from the same source.

**Calculated by multiplying the influent concentration times one minus the percent removal.

Table C-7

TOTAL SUSPENDED SOLIDS CONCENTRATIONS AND MASS REMOVALS FINISHING WATER SUBCATEGORY

TSS Influent Concentration	95 mg/l
TSS Effluent Concentration	29 mg/l
TSS Percent Removal*	69.5 %
TSS Mass	3,630 kg/yr
TSS Mass Removal	2,520 kg/yr
TSS Mass Remaining After Treatment	1,110 kg/yr

---

*Percent removal is based on a median effluent concentration of 29 mg/l for settling technology. This is the median effluent concentration for settling technology in the U.S. EPA, Treatability Manual, Volume III, Technologies for Control/ Removal of Pollutants, July 1980, EPA 600/8-80-842c.

effluent concentration of 29 mg/l from the U.S. EPA, Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, July 1980, EPA 600/8-80-842C for settling technology.

BAT Effluent Limitations Guidelines Pollutant Mass Removals

BAT effluent limitations guidelines for this subcategory are equal to BPT effluent limitations guidelines for all pollutants except for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate. Therefore, the estimated pollutant removals are the same as at BPT.

The three phthalates are reserved at BAT. The technology identified for treatment of the phthalates is settling followed by activated carbon adsorption. The activated carbon also removes additional quantities of TSS. The Agency estimated the amounts of the three phthalates that would be removed by the activated carbon process so that the technology could be evaluated economically. Refer to Table C-8 for the activated carbon adsorption process influent and effluent concentrations and the percent removals for the three phthalates.

The pollutant removals for the settling unit are equal to the removals at BPT and the TSS concentration of the process water entering the activated carbon adsorption process is equal to the TSS concentration in the settling unit effluent (i.e., 29 mg/l from Table C-7).

The pollutant mass removals for the finishing water subcategory are presented in Table C-9. These removals reflect the pollutant removals for the settling and activated carbon adsorption technologies. Also presented in Table C-9 are the finishing water subcategory pollutant masses remaining after treatment.

NSPS Pollutant Mass Removals

NSPS for this subcategory are equal to BPT effluent limitations guidelines except for bis(2-ethylhexyl) phthalate, di-n-butyl phthalate, and dimethyl phthalate. NSPS are reserved for the phthalates pending completion of a phthalate treatability study.

Estimated pollutant mass removals for direct discharge finishing water processes at a new plant were based on two model treatment technologies:

1. Settling (the selected technology for BPT and BAT) and
2. Settling followed by filtration.

To estimate the pollutant masses discharged and the pollutant mass removals for NSPS, the pollutant masses at BPT were divided

Table C-8

POLLUTANT CONCENTRATIONS AND PERCENT REMOVALS - ACTIVATED CARBON PROCESS FINISHING WATER SUBCATEGORY

Conventional Pollutant	Influent Concentration from Settling Unit (mg/l)	Effluent Concentration from Activated Carbon Adsorption (mg/l)	Pollutant Percent Removal	Pollutant Percent Removal Source
TSS	29	12	37.7	1
Priority Pollutant				
66. bis(2-ethylhexyl) phthalate	0.479	0.010	97.9	2
68. di-n-butyl phthalate	0.031	0.025	19.4	2
71. dimethyl phthalate	0.034	0.025	25.5	2

---

1. Percent removal is based on the median effluent concentration for granular activated carbon technology presented in the U.S. EPA, Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, July 1980, EPA 600/8-80-842c.

2. Percent removal is based on the pollutant treatability limit from U.S. EPA, Treatability of Organic Priority Pollutants - Part C - Their Estimated (30-Day Ave.) Treated Effluent Concentration - A Molecular Engineering Approach, Murray P. Strier, 11 July 1978.

Table C-9

BAT MASS REMOVALS
FINISHING WATER SUBCATEGORY

	Conventional Pollutant	Pollutant Mass Removal - Settling Unit (kg/yr)	Pollutant Mass Removal - Activated Carbon Adsorption (kg/yr)	Total Pollutant Mass Removal (kg/yr)	Pollutant Mass Remaining After Treatment (kg/yr)
TSS		2,520	418	2,938	692
	Priority Pollutant				
66.	bis(2-ethylhexyl) phthalate	0	17.9	17.9	0.1
67.	di-n-butyl phthalate	0	0.227	0.227	0.773
71.	dimethyl phthalate	0	0.339	0.339	0.661
TOTAL		0	18.5	18.5	1.53

by the estimated number of finishing processes (i.e., 10 finishing processes). This approach assumes that settling units at new discharging sources have the influent and effluent concentrations listed on Table C-7. Hence, the pollutant percent removal is the same for a settling unit at an existing source and at a new source. Table C-10 presents the mass removals for the settling technology for the finishing water subcategory.

EPA considered a model treatment technology for NSPS that included a settling unit followed by filtration. The filter influent and effluent concentrations and pollutant mass removals are presented in Table C-11. The filter influent TSS concentration and influent TSS mass are equal to the effluent TSS concentration and effluent TSS mass from the settling unit at BPT (see Table C-7).

Table C-10

NSPS MASS REMOVALS - SETTLING UNIT FINISHING WATER SUBCATEGORY

Conventional Pollutant	New Source Pollutant Mass (kg/yr)*	Pollutant Mass Removal (kg/yr)**	Pollutant Mass Remaining After Treatment (kg/yr)
TSS	363	252	111

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*Calculated by dividing the estimated subcategory pollutant mass for TSS by the estimated number of finishing processes.

**For settling unit, based on percent removal presented in Table C-7.

Table C-11

NSPS MASS REMOVALS - FILTER FINISHING WATER SUBCATEGORY*

TSS Influent Concentration	29 mg/l
TSS Effluent Concentration	12 mg/l
TSS Percent Removal**	59 percent
TSS Pollutant Mass	111 kg/yr
TSS Pollutant Mass Removal	65.5 kg/yr
TSS Mass Remaining After Treatment	45.5 kg/yr

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*For a filter following the settling unit.

**Percent removal was calculated using the median effluent concentration for granular media filtration from U.S. EPA, Treatability Manual, Volume III, Technologies for Control/ Removal of Pollutants, July 1980, EPA 600/8-80-842c.

APPENDIX D

POLLUTANT CONCENTRATIONS USED TO CALCULATE THE BEST PRACTICABLE TECHNOLOGY (BPT) EFFLUENT LIMITATIONS GUIDELINES

UNITED STATES ENVIRONMENTAL PROTECTION AGENCY
WASHINGTON, D.C. 20460

MEMORANDUM

SUBJECT: Calculation of Final Best Practicable Technology (BPT) Limitations Guidelines - Plastics Molding and Forming (PM&F)

FROM: R. Clifton Bailey, Statistician
Analysis and Evaluation Division (WH-586) R. CB.

TO: Robert M. Southworth, PM&F Project Officer
Industrial Technology Division (WH-552)

Purpose

This memorandum describes the development of the final BPT effluent limitations guidelines for the PM&F category. Pollutants regulated by the effluent limitations guidelines are biochemical oxygen demand (BOD$_5$), oil and grease (O&G), and total suspended solids (TSS).

Background

Proposed BPT effluent limitations guidelines for the PM&F category were published in the Federal Register on February 15, 1984 (49 FR 5862). They control BOD$_5$, O&G, and TSS in two subcategories. The limitations were based on concentration values that were transferred from the organic chemicals, plastics, and synthetic fibers (OCPSF) category and a production normalized flow calculated using information from two questionnaire surveys of the PM&F industry.

In response to comments, the Agency collected additional pollutant concentration data and calculated flow-weighted subcategory pollutant average concentrations using both the new sampling data and data from previous sampling episodes. Based on the flow-weighted average concentrations and information provided by commenters, the Agency determined that the PM&F category should be divided into three subcategories for the final PM&F regulation. They are:

- ° contact cooling and heating water subcategory;
- ° cleaning water subcategory; and
- ° finishing water subcategory.

This memorandum discusses the concentration values used to calculate the final BPT effluent limitations guidelines for each subcategory. These concentrations are multiplied by the average process water usage flow rate for a process to determine the mass of pollutants that can be discharged from a process.

The final BPT effluent limitations guidelines for the contact cooling and heating water subcategory are based on a statistical evaluation of the raw waste concentrations of BOD_5, O&G, and TSS in contact cooling and heating water. This approach was used because the concentrations of BOD_5 in contact cooling and heating water are too low to support the operation of the proposed technology for BPT (i.e., the activated sludge process) and the Agency could not identify any other technology that would reduce those concentrations.

Final BPT effluent limitations guidelines for the cleaning water subcategory are based on the application of a package activated sludge plant with equalization and pH adjustment because the BOD_5 concentrations found in cleaning water are high enough to support biological treatment. However, no effluent data on activated sludge treatment of cleaning water only were available. Therefore, as at proposal, we compared the cleaning water untreated concentration data for BOD_5, O&G, and TSS to data from those pollutants in wastewater generated at plastics manufacturing plants (PMP) in the organic chemicals, plastics, and synthetic fibers category (OCPSF) category. Results of that comparison are presented in this memorandum. Because wastewaters from cleaning processes at PM&F plants and wastewaters generated at PMP plants have similar BOD_5, O&G, and TSS characteristics, it is appropriate to use activated sludge effluent data from those pollutants from the OCPSF category to determine effluent limitations guidelines for the PM&F cleaning water subcategory. Those data are presented in Appendices I and IIA to this memorandum.

For the finishing water subcategory, only TSS was present in treatable concentrations. For this reason, the BPT effluent limitations guidelines for this subcategory are based on the performance of a settling unit. Calculation of the maximum TSS concentration for any one-day and the maximum TSS concentration for the monthly average is discussed in this memorandum.

Data

Plastics Molding and Forming Process Sample Data

Samples of untreated process water were collected at 18 plastics molding and forming (PM&F) plants. BOD_5, O&G, and TSS concentrations found in these samples are presented in Appendix I. Concentration data are presented for all three subcategories.

Plastics Manufacturing Plant Data

The BPT effluent limitations guidelines for the cleaning water subcategory are based on data from well-operated activated sludge processes at six plastics manufacturing plants (Nos. 9, 44, 45, 96, 111, 126). These well-operated treatment processes were identified through an engineering analysis of the performance data for those processes (see page 190 of the OCPSF technical development document-proposal for a summary). BOD_5 and TSS data were available from effluent samples collected at five of the six plants (Nos. 9, 44, 45, 111, 126). These data are presented in Appendix IIA.

Oil and grease (O&G) data were not available for the six well-operated wastewater treatment processes at the plastics manufacturing plants in the plastics only subcategory. Therefore, the PM&F effluent limitations guidelines for O&G were developed based on data from four plants (Nos. 3, 61, 124, 170) in the OCPSF data base that manufacture plastics (not necessarily plastics only plants) and that use activated sludge treatment. Those data are also presented in Appendix IIA.

Subsequent to proposal, we investigated using an expanded data base for the OCPSF category to see if the transferred effluent concentrations for the final regulation for the cleaning water subcategory should be based on the expanded data base. Although additional data had been collected for the OCPSF category, those data had neither been input to the data base nor been verified. Because the estimated date for completion of the expanded and verified data base was after the promulgation date for the final PM&F regulation, we used the same data base for the transfer of the activated sludge performance data for the final PM&F regulation that was used for the proposed regulation. This data base is the only verified data base available for the development of the PM&F regulation. Because it is a verified data base, the Agency believes it is appropriate to use that data base for the final PM&F Regulation.

The final BPT effluent limitations guidelines for the cleaning water subcategory were developed based on a log-normal distribution fit to the data. The goodness-of-fit of the log-normal model for O&G effluent data was examined using a graphical procedure described in Appendix III. As stated, the plots presented in Appendix IIC support the log-normal distribution as a model for the O&G effluent data. The graphical procedure used to demonstrate log-normality for O&G was the same procedure used to demonstrate log-normality for BOD_5 and TSS for the proposed OCPSF Regulation (see the technical development document for the proposed OCPSF regulation).

Performance Data Transfer - Cleaning Water Subcategory

Effluent concentration values for BOD_5, O&G, and TSS for the cleaning water subcategory were developed in a manner similar to the effluent concentrations for those pollutants for the cleaning and finishing water subcategory at proposal. However, as discussed above, cleaning water processes and finishing water processes are in separate subcategories for the final regulation. Therefore, only PM&F cleaning water data were used for the comparison with the influent data from PMP in the OCPSF category. The revised data summary shown in Table 1 presents the plant average pollutant concentrations and log-variances for plants in the cleaning water subcategory and for the PMP plants used in the comparisons.

As at proposal, the statistical comparisons use a nonparametric test, the Mann-Whitney U/Wilcoxon Test, for independent samples. The revised comparisons (summarized in Table 2) were made separately for the plant means and plant log-variances. In these tests, neither the medians of the PM&F means nor the medians of the PM&F log-variances were found to be significantly greater than the corresponding PMP values. Consequently, the process water for the PM&F cleaning water subcategory is neither significantly greater nor more variable than the PMP process wastewater with respect to BOD_5, TSS, and O&G concentrations.

Results of the statistical analysis also support the judgement that BOD_5, TSS, and O&G effluent concentrations for activated sludge treatment of cleaning water should neither be greater nor more variable than effuent concentrations for those pollutants for an activated sludge process used to treat PMP process wastewater. We conclude, therefore, that the cleaning water concentration values shown in Table 6 of this memorandum can be met using the activated sludge process to treat PM&F wastewater.

TABLE 1

RANK COMPARISON OF MEAN POLLUTANT CONCENTRATIONS AND LOG-VARIANCES: PLASTICS MOLDING AND FORMING (PM&F) PLANTS IN THE CLEANING WATER SUBCATEGORY AND PLASTICS MANUFACTURING (PMP) PLANTS

POLLUTANT	PLANT TYPE	PLANT ID	SAMPLE SIZE	CONCENTRATION (mg/l): MEAN	RANK
BOD_5	PMF	I	8	5.33	1
	PMF	K	1	20.00	2
	PMF	B	3	48.67	3
	PMF	C	3	62.89	4
	PMP	9	23	84.74	5
	PMP	111	157	94.82	6
	PMF	F	6	200.97	7
	PMF	A	2	361.52	8
	PMP	45	148	381.14	9
	PMP	44	45	754.00	10
	PMF	H	2	777.50	11
	PMP	126	247	1087.47	12
O&G	PMF	A	2	4.000	3
	PMF	R	3	4.000	3
	PMF	D	2	4.000	3
	PMF	H	2	4.000	3
	PMF	K	1	4.000	3
	PMF	C	3	12.544	6
	PMP	61	234	17.393	7
	PMP	124	59	22.902	8
	PMP	3	157	41.139	9
	PMP	1	8	54.215	10
	PMP	170	203	79.277	11
	PMF	F	4	133.321	12
TSS	PMF	B	3	4.00	1
	PMF	K	1	6.00	2
	PMF	C	3	6.24	3
	PMF	H	2	7.25	4
	PMF	D	2	10.50	5
	PMP	9	23	27.25	6
	PMF	A	2	33.58	7
	PMP	111	157	42.84	8
	PMF	F	6	234.65	9
	PMP	45	148	304.32	10
	PMP	126	247	557.00	11
	PMP	44	45	3780.76	12
	PMF	I	8	7360.98	13

TABLE 1 (CONT'D)

POLLUTANT	PLANT TYPE	PLANT ID	SAMPLE SIZE	LOG-VARIANCE OF POLLUTANT CONCENTRATION:	
				MEAN	RANK
BOD_5	PMF	K	1	.	.
	PMF	B	3	0.00387	1
	PMF	H	2	0.07376	2
	PMF	C	3	0.08329	3
	PMP	44	45	0.12644	4
	PMF	I	8	0.12665	5
	PMP	III	157	0.16975	6
	PMP	45	148	0.17588	7
	PMP	126	247	0.26334	8
	PMP	9	23	0.67626	9
	PMF	F	6	1.46832	10
	PMF	A	2	7.65196	11
O&G	PMF	K	1	.	.
	PMF	A	2	0.0000	2.5
	PMF	B	3	0.0000	2.5
	PMF	D	2	0.0000	2.5
	PMF	H	2	0.0000	2.5
	PMP	61	234	0.39147	5.0
	PMP	170	203	0.39781	6.0
	PMP	3	157	0.61599	7.0
	PMP	124	59	1.11618	8.0
	PMF	C	3	1.48186	9.0
	PMF	I	8	1.69834	10.0
	PMF	F	4	6.30013	11.0
TSS	PMF	K	1	.	.
	PMF	B	3	0.0000	1
	PMF	D	2	0.11786	2
	PMP	111	157	0.17684	3
	PMF	H	2	0.46569	4
	PMP	126	247	0.55877	5
	PMP	9	23	0.56581	6
	PMF	A	2	0.69461	7
	PMF	C	3	0.82157	8
	PMF	F	6	1.18541	9
	PMP	45	148	1.47319	10
	PMF	I	8	2.25857	11
	PMP	44	45	2.61015	12

TABLE 2

RESULTS OF THE COMPARISON OF POLLUTANT CONCENTRATION IN PMP PROCESS WASTEWATER AND IN PROCESS WASTEWATER FOR THE PM&F CLEANING WATER SUBCATEGORY

Using Wilcoxon - T Test for 2 Independent Samples

One-Tailed Test H_O: PMF $\leq$ PMP

H_A: PMF > PMP

	POLLUTANT	NUMBER OF PLANTS PMF	NUMBER OF PLANTS PMP	RANK MEAN PMF	RANK MEAN PMP	T_x[1]	P	
PLANT MEANS RANKED	BOD_5	7	5	5.14	8.40	42	.926	NS[2]
	O&G	8	4	5.38	8.75	35	.923	NS
	TSS	8	5	5.50	9.40	47	.953	NS
PLANT LOG-VARIANCES RANKED	BOD_5	6	5	5.53	6.80	40	.959	NS
	O&G	7	4	5.71	6.50	26	.606	NS
	TSS	7	5	6.00	7.20	36	.681	NS

1 As defined by Gibbons, J.D., "Nonparametric Methods for Quantitative Analysis," Holt, Rinehard and Winston, 1976, p. 163.

2 NS - Not significant.

[This updates Table 3, page D-11, technical development document for the proposed PM&F regulations].

Statistical Evaluation of Raw Waste Concentrations - Contact Cooling and Heating Water Subcategory

The final BPT effluent limitations guidelines for BOD_5, O&G, and TSS for the contact cooling and heating water subcategory are based on the raw waste concentrations of those pollutants in contact cooling and heating waters. This approach was used because commenters correctly pointed out that the concentrations of BOD_5 in contact cooling and heating water were too low to support the proposed activated sludge treatment. Furthermore, during the sampling episodes for this regulation, the Agency found that, for contact cooling and heating water, the industry employed good housekeeping practices such as keeping lubricating oil and other pollutants out of the process water. A regulation based on the raw waste concentrations ensures the continuation of the good housekeeping practices. An evaluation of the raw waste concentrations, shown in Table 3, was selected as the basis for the final BPT effluent limitations guidelines for this subcategory because the Agency could not identify a technology that would reduce the low BOD_5, O&G and TSS concentrations in contact cooling and heating waters.

TABLE 3

PM&F DATA FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

```
                                        PM&F DATA FOR CONTACT COOLING AND HEATING SUBCATEGORY
                                                   STREAMS M-1 AND M-2 DELETED

POLLUTANT PROCESS STREAM        DAY1         DAY2         DAY3  DF      LOGMEAN SUM SQUARE        EIJ          VIJ      AVG FLOW

  BOD5
          CALEND   B-2         5.0000         .            .     0       1.6094     0.0000      5.2985       3.4523    410.0000
          CALEND   E-2         9.4000       8.9000       4.1000  2       1.9459     0.4307      7.4180       6.7667   3157.0000
          CALEND   F-1        10.0000       8.0000      10.0000  2       2.2282     0.0332      9.8374      11.9005    530.0000

                        PROC POOLED SD =    0.3406                2                          FLOW TOT =    4097.00
                             PROC EXPECTED VALUE = 7.518854                  PROCESS WGTED VARIANCE = 7.099109

          CAST     P-1         2.3000         .            .     0       0.8329     0.0000      2.6362       2.1801   1090.0000

                        PROC POOLED SD =    0.5224                                           FLOW TOT =    1090.00
                             PROC EXPECTED VALUE = 2.636193                  PROCESS WGTED VARIANCE = 2.180112

          EXTRUDE  A-1         5.0000         .            .     0       1.6094     0.0000      6.2978      23.2623    181.0000
          EXTRUDE  D-3           .            .            .     .         .        0.0000        .            .        23.7000
          EXTRUDE  E-3         7.6000       3.9000       0.5000  2       0.8987     4.0233      3.0939       5.6141   8040.0000
          EXTRUDE  F-6           .          5.0000       3.0000  1       1.3540     0.1305      4.8783      13.9574    454.0000
          EXTRUDE  G-1           .            .            .     .         .        0.0000        .            .       313.5000
          EXTRUDE  K-2         5.0000       5.0000       5.0000  2       1.6094     0.0000      6.2978      23.2623    908.0000
          EXTRUDE  K-3         5.0000       5.0000       5.0000  2       1.6094     0.0000      6.2978      23.2623    454.0000
          EXTRUDE  K-4         5.0000       5.0000       5.0000  2       1.6094     0.0000      6.2978      23.2623  33154.0000
          EXTRUDE  N-2        10.0000         .            .     0       2.3026     0.0000     12.5957      93.0493      6.6000
          EXTRUDE  N-3           .          6.0000         .     0       1.7918     0.0000      7.5574      33.4978    213.0000
          EXTRUDE  O-1           .            .            .     .         .        0.0000        .            .       559.0000
          EXTRUDE  O-2           .            .            .     .         .        0.0000        .            .       416.0000
          EXTRUDE  R-1         6.0000         .            .     0       1.7918     0.0000      7.5574      33.4978    881.0000
          EXTRUDE  R-2         4.0000         .            .     0       1.3863     0.0000      5.0383      14.8879  12400.0000

                        PROC POOLED SD =    0.6794                                           FLOW TOT =   58003.80
                             PROC EXPECTED VALUE = 5.455343                  PROCESS WGTED VARIANCE = 18.6277

          MOLD     B-4         5.0000         .            .     0       1.6094     0.0000      5.0111       0.1120      5.6000
          MOLD     C-1        96.9000      84.8000      90.9000  2       4.5079     0.0069     90.9343      36.8824     63.6000
          MOLD     J-1         5.0000         .            .     0       1.6094     0.0000      5.0111       0.1120  27260.0000
          MOLD     J-2        54.0000         .            .     0       3.9890     0.0000     54.1203      13.0642   2010.0000

                        PROC POOLED SD =    0.0667                                           FLOW TOT =   29339.20
                             PROC EXPECTED VALUE = 8.561618                  PROCESS WGTED VARIANCE = 1.07906

          THERM    F-2         8.0000       7.0000       7.0000  2       1.9904     0.0119      7.3404       0.3212    408.0000

                        PROC POOLED SD =    0.0771                                           FLOW TOT =     408.00
                             PROC EXPECTED VALUE = 7.340393                  PROCESS WGTED VARIANCE = 0.3211999
```

PROCESS STREAMS M1 AND M2 DELETED BECAUSE CONTAMINATED.

TABLE 3

PM&F DATA FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

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                                         PM&F DATA FOR CONTACT COOLING AND HEATING SUBCATEGORY
                                                     STREAMS M-1 AND M-2 DELETED

POLLUTANT PROCESS STREAM      DAY1        DAY2        DAY3  DF     LOGMEAN SUM SQUARE      EIJ        VIJ     AVG FLOW

 O&G
          CALEND   B-2      4.0000         .           .     0      1.3863     0.0000    4.8414    10.8985   410.0000
          CALEND   E-2     16.8000     23.8000     11.8000   2      2.8197     0.2461   20.3003   191.6133  3157.0000
          CALEND   F-1      1.0000      1.0000      4.0000   2      0.4621     1.2812    1.9213     1.7164   530.0000

                     PROC POOLED SD =    0.6179                                            FLOW TOT =     4097.00
                          PROC EXPECTED VALUE = 16.37574                 PROCESS WGTED VARIANCE = 148.9629

          CAST     P-1      3.0000      1.0000         .     1      0.5493     0.6035    2.3421     4.5444  1090.0000

                     PROC POOLED SD =    0.7768                                            FLOW TOT =     1090.00
                          PROC EXPECTED VALUE = 2.342089                 PROCESS WGTED VARIANCE = 4.544424

          EXTRUDE  B-1      4.0000         .           .     0      1.3863     0.0000    4.0210     0.1698   181.0000
          EXTRUDE  D-3      4.0000         .           .     0      1.3863     0.0000    4.0210     0.1698    23.7000
          EXTRUDE  E-3     20.0000     27.8000     19.4000   2      3.0953     0.0796   22.2107     5.1819  8040.0000
          EXTRUDE  F-6         .        5.0000      4.0000   1      1.4979     0.0249    4.4956     0.2123   454.0000
          EXTRUDE  G-1      4.0000      4.0000         .     1      1.3863     0.0000    4.0210     0.1698   313.5000
          EXTRUDE  K-2      4.0000      4.0000      4.0000   2      1.3863     0.0000    4.0210     0.1698   906.0000
          EXTRUDE  K-3      4.0000      4.0000      4.0000   2      1.3863     0.0000    4.0210     0.1698   454.0000
          EXTRUDE  K-4      4.0000      4.0000      4.0000   2      1.3863     0.0000    4.0210     0.1698 33154.0000
          EXTRUDE  N-2      5.0000         .           .     0      1.6094     0.0000    5.0262     0.2654     6.6000
          EXTRUDE  N-3         .        3.0000         .     0      1.0986     0.0000    3.0157     0.0955   213.0000
          EXTRUDE  O-1      5.0000         .           .     0      1.6094     0.0000    5.0262     0.2654   559.0000
          EXTRUDE  O-2      3.0000         .           .     0      1.0986     0.0000    3.0157     0.0955   416.0000
          EXTRUDE  P-1      6.0000         .           .     0      1.7918     0.0000    6.0314     0.3821   881.0000
          EXTRUDE  R-2      8.0000         .           .     0      2.0794     0.0000    8.0419     0.6793 12400.0000

                     PROC POOLED SD =    0.1022                                            FLOW TOT =    58003.80
                          PROC EXPECTED VALUE = 7.435005                 PROCESS WGTED VARIANCE = 0.9771765

          MOLD     B-4      7.0000         .           .     0      1.9459     0.0000    8.1883    24.6966     5.6000
          MOLD     C-1     75.0000     24.5000     41.0000   2      3.7432     0.6272   49.4046   899.0445    63.6000
          MOLD     J-1     11.0000         .           .     0      2.3979     0.0000   12.8674    60.9854 27260.0000
          MOLD     J-2     61.0000         .           .     0      4.1109     0.0000   71.3554  1875.4264  2010.0000

                     PROC POOLED SD =    0.5600                                            FLOW TOT =    29339.20
                          PROC EXPECTED VALUE = 16.95263                 PROCESS WGTED VARIANCE = 187.1007

          THERM    F-2      3.0000         .        5.0000   1      1.3540     0.1305    4.1341     2.3818   408.0000

                     PROC POOLED SD =    0.3612                                            FLOW TOT =      408.00
                          PROC EXPECTED VALUE = 4.134063                 PROCESS WGTED VARIANCE = 2.381821
```

PROCESS STREAMS M1 AND M2 DELETED BECAUSE CONTAMINATED.

TABLE 3

PM&F DATA FOR THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

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                                    PM&F DATA FOR CONTACT COOLING AND HEATING SUBCATEGORY
                                                 STREAMS M-1 AND M-2 DELETED

POLLUTANT PROCESS STREAM       DAY1         DAY2         DAY3  DF    LOGMEAN SUM SQUARE      EIJ        VIJ     AVG FLOW

 TSS
          CALEND   B-2       4.0000          .            .     0     1.3863    0.0000     4.2584     2.4183   410.0000
          CALEND   E-2       3.0000       4.0000       2.0000   2     1.0594    0.2425     3.0708     1.2576  3157.0000
          CALEND   F-1       6.0000       3.0000       5.0000   2     1.4999    0.2582     4.7709     3.0355   530.0000

                     PROC POOLED SD =    0.3538                                       FLOW TOT =     4097.00
                          PROC EXPECTED VALUE = 3.409589                 PROCESS WGTED VARIANCE = 1.603742

          CAST     P-1       2.0000          .            .     0     0.6931    0.0000     2.2591     1.4082  1090.0000

                     PROC POOLED SD =    0.4936                                       FLOW TOT =     1090.00
                          PROC EXPECTED VALUE = 2.259137                 PROCESS WGTED VARIANCE = 1.408235

          EXTRUDE  B-1       4.0000          .            .     0     1.3863    0.0000     4.3778     3.7918   181.0000
          EXTRUDE  D-3       4.0000          .            .     0     1.3863    0.0000     4.3778     3.7918    23.7000
          EXTRUDE  E-3       4.0000       2.0000       3.0000   2     1.0594    0.2425     3.1570     1.9718  8040.0000
          EXTRUDE  F-6          .         1.0000       1.0000   1     0.0000    0.0000     1.0945     0.2370   454.0000
          EXTRUDE  G-1      22.0000       4.0000          .     1     2.2387    1.4531    10.2669    20.8546   313.5000
          EXTRUDE  K-2       6.0000       4.0000       4.0000   2     1.5214    0.1096     5.0114     4.9686   908.0000
          EXTRUDE  K-3       4.0000       4.0000       4.0000   2     1.3863    0.0000     4.3778     3.7918   454.0000
          EXTRUDE  K-4       4.0000       4.0000       4.0000   2     1.3863    0.0000     4.3778     3.7918 33154.0000
          EXTRUDE  N-2       1.0000          .            .     0     0.0000    0.0000     1.0945     0.2370     6.6000
          EXTRUDE  N-3          .         1.0000          .     0     0.0000    0.0000     1.0945     0.2370   213.0000
          EXTRUDE  O-1       1.0000          .            .     0     0.0000    0.0000     1.0945     0.2370   559.0000
          EXTRUDE  O-2       1.0000          .            .     0     0.0000    0.0000     1.0945     0.2370   416.0000
          EXTRUDE  R-1       1.0000          .            .     0     0.0000    0.0000     1.0945     0.2370   881.0000
          EXTRUDE  R-2       1.0000          .            .     0     0.0000    0.0000     1.0945     0.2370 12400.0000

                     PROC POOLED SD =    0.4249                                       FLOW TOT =    58003.80
                          PROC EXPECTED VALUE = 3.405251                 PROCESS WGTED VARIANCE = 2.735168

          MOLD     H-4       4.0000          .            .     0     1.3863    0.0000     6.2105    54.4100     5.6000
          MOLD     C-1     104.0000      77.0000      18.0000   2     3.9595    1.7598    81.4080  9348.8067    63.6000
          MOLD     J-1       4.0000          .            .     0     1.3863    0.0000     6.2105    54.4100 27260.0000
          MOLD     J-2      36.0000          .            .     0     3.5835    0.0000    55.8947  4407.2072  2010.0000

                     PROC POOLED SD =    0.9360                                       FLOW TOT =    29339.20
                          PROC EXPECTED VALUE = 9.777343                 PROCESS WGTED VARIANCE = 372.7638

          THERM    F-2       1.0000       2.0000       1.0000   2     0.2310    0.3203     1.3650     0.3236   408.0000

                     PROC POOLED SD =    0.4002                                       FLOW TOT =      408.00
                          PROC EXPECTED VALUE = 1.364959                 PROCESS WGTED VARIANCE = 0.3236007
```

PROCESS STREAMS M1 AND M2 DELETED BECAUSE CONTAMINATED.

In basing the effluent limitations guidelines for BOD_5, O&G, and TSS on the raw waste concentrations, the Agency developed effluent limitations that reflect the distribution of the process-types within the contact cooling and heating water subcategory. To do this, EPA used the PM&F data for the questionnaire surveys of the industry to estimate the relative number of processes by process-type within the contact cooling and heating water subcategory. The relative number of processes by process-type establishes a weight for each process-type which is the ratio of the number of processes of each type to the total number of processes in the survey data base for this subcategory. The weights are:

Type of Process	Weight
Calendering	0.0093
Casting	0.0140
Extrusion	0.8528
Molding	0.0724
Thermoforming	0.0211
Coating & Laminating	0.0304.

Consequently, the extrusion process type has the most weight because the largest number of processes for the contact cooling and heating water subcategory are extrusion processes. Within each process type, process streams were flow-weighted. As suggested by commenters, flow-weighting gives more weight to sampled process streams where water use was most intense. To obtain the flow-weight for a process stream within a process type, the average process stream flow (shown in Table 3) is normalized to sum to one within the process-type by dividing the process stream flow by the total stream flow within the process-type. For the limitations computation, each process stream is assigned a weight that is the product of the weight for the process type (shown above) and the individual flow-weight within the process-type. For example, to compute the weight for extrusion process stream, E3, of 0.1182 shown in Table IV.A.1 in Appendix IVA to this memorandum, we use the weight for the extrusion process-type of 0.8528 shown above, the average stream flow for E3 of 8040 l/hr. (Table 3) and the total flow for sampled extrusion processes of 58003.8 l/hr. (Table 3). The weight for process stream E3 is determined by:

Extrusion weight x flow for E3/total flow for extrusion processes

$$\begin{aligned} &= 0.8528 \times 8040/58003.8 \\ &= 0.8528 \times 0.1386 \\ &= 0.1182. \end{aligned}$$

The resulting process stream weights used in the limitations computations are displayed in Appendix IVA.

The 99th percentile daily limitations for the contact cooling and heating water subcategory were computed according to the methodology shown in Appendix IVA. This methodology was used to represent the subcategory process-types and the flow within the process-types. The daily 99th percentile concentration values for this subcategory are shown in Table 6.

Calculation of TSS Concentration - Finishing Water Subcategory

The only pollutant regulated in the finishing water subcategory is TSS. Since proposal, the cleaning and finishing water subcategory was split into two subcategories. In response to comments, the Agency collected additional data and found that TSS was the only pollutant present in treatable concentrations in finishing water. The Agency based the TSS concentration values shown in Table 6 for the finishing water subcategory on settling technology. The TSS effluent concentrations were obtained by multiplying the estimated long-term average TSS effluent concentration for a settling unit by the daily and monthly variability factors described below.

Long-Term Average TSS Concentration

A long-term average TSS effluent concentration for a settling unit was calculated by multiplying the flow-weighted TSS concentration in finishing water (see Table 4) times a percent removal. The percent removal (i.e., 82 percent) was reported in the technical development document for the proposed PM&F regulation (pg. 194). It was obtained from the Treatability Manual, Volume III, Technologies for Control/Removal of Pollutants, July 1980, US EPA 600-8-80-042C. The estimated long-term TSS effluent concentration for the settling unit is:

$$91 \text{ mg/l} \times 0.18 = 16 \text{ mg/l}.$$

This concentration was used to calculate the maximum for one day and the maximum of monthly average concentrations for TSS because effluent data for the treatment of finishing water alone in a settling unit are not available.

Variability Factors

In the absence of effluent data for a settling unit that treats only finishing water, we considered the transfer of variability factors from other industrial categories. However, we were unable to find an appropriate data base for the transfer of those factors. For this reason, the variability factors used to calculate the final BPT effluent limitations guidelines for the finishing water subcategory are based on the variability of the raw TSS concentrations found in finishing waters.

The TSS daily variability factor, VF(1), for the finishing processes is the ratio of the flow-weighted average of the lognormal 99-th percentile estimates to the flow-weighted average of the lognormal expectations. In Appendix IVB, we shown that this ratio is

$$VF(1) = \exp(2.326\hat{\sigma} - \hat{\sigma}^2/2)$$

when a pooled estimate of σ is used. In this case $\hat{\sigma} = 1.216$ and

$$VF(1) = 8.1.$$

The Central Limit Theorem was used to compute the 95th percentile variability factor for an average of 30 samples. For this approximation, we used the flow weighted averages of the log-normal expectations and the variances to compute a subcategory expectation and variance. As shown in Appendix IVB, the monthly variability factor is

$$\begin{aligned} VF(30) &= 1 + 1.6449(V/30)^{.5}/E \\ &= 1 + 1.6449(1.89781 \times 10^5/30)^{.5}/102.4 \\ &= 2.3 \end{aligned}$$

The maximum for one day and the maximum for average monthly pollutant concentrations used to calculate the final BPT effluent limitations guidelines for TSS for the finishing water subcategory are presented in Table 5.

BPT Effluent Limitations Guidelines

The concentrations used to calculate the final BPT effluent limitations guidelines for the PM&F category are presented in Table 6. These concentrations are multiplied by the average process water usage flow rate for a process to obtain the mass of a pollutant that can be discharged from that process.

TABLE 4

SUMMARY OF TSS CONCENTRATION DATA FOR THE FINISHING WATER SUBCATEGORY

Process	TSS (mg/l)*			Average (mg/l)	Log Mean (μ_i)	Sum Squares (SS_i)	D.F. (ν_i)**	Flow (l/hr.)
	Day 1	Day 2	Day 3					
I-4	63	289	1359	570.3	5.675	4.717	2	1220
N-1	4	1	-	2.5	0.693	0.961	1	2760
Q-1	12.55	6.3	-	9.4	2.185	0.237	1	4160

Pooled standard deviation	1.216
Flow-weighted:	
Average Concentration	91 mg/l
Average log-normal expectation, E	102.4 mg/l
Average of log-normal 99th percentiles	827.4 mg/l
Average log-normal variance, V	$1.89781 \times 10^5 (mg/l)^2$

* Duplicate concentrations for TSS samples were averaged.

** Degrees of freedom equal to number of samples for the process minus one.

TABLE 5

EFFLUENT TSS CONCENTRATIONS - FINISHING WATER SUBCATEGORIES

	Variability Factor	Long-Term Average	Concentration*
Maximum for One Day	8.1	16 mg/l	130 mg/l
Maximum for Monthly Average	2.3	16 mg/l	37 mg/l

* Long-term average multiplied by variability factor.

TABLE 6

CONCENTRATIONS USED TO CALCULATE THE FINAL BPT EFFLUENT LIMITATIONS GUIDELINES*

Subcategory	Pollutant	Maximum for One Day (mg/l)	Maximum for Monthly Averages (mg/l)
Cooling & Heating Water	BOD5	26	-
	O&G	29	-
	TSS	19	-
Cleaning Water	BOD5	49	22
	O&G	71	17
	TSS	117	36
Finishing Water	TSS	130	37

* These values are multiplied by the average process water usage flow rate for a process to obtain the mass of pollutants that can be discharged from the process.

APPENDIX I

BOD_5, O&G and TSS Data for Untreated PM&F Process Water by Subcategory

P M & F DATA BASE - RAW VALUES

SUBCAT=CC & H

POLL	SAMPTYPE	PROCESS	STREAM	SOURCE	DETECTS	DAY1	DETECT1	FLOW1	DAY2	DETECT2	FLOW2	DAY3	DETECT3	FLOW3	DUPLICAT	DETECTD
BOD5	1	CALEND	B-2	5.0	<	5.0	<	410.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	1	CALEND	E-2	5.0		9.4		3157.0	8.9		3157.0	4.1		3157.0	0	NS
BOD5	1	CALEND	F-1	2.0		10.0		568.0	8.0		454.0	10.0		568.0	0	NS
BOD5	2	CAST	P-1	8.5		2.3		1090.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	1	EXTRUDE	B-1	5.0	<	5.0	<	181.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	1	EXTRUDE	D-3	0.0	NS	0.0	NS	23.7	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	1	EXTRUDE	E-3	5.0		7.6		8040.0	3.9		8040.0	0.5		8040.0	0	NS
BOD5	1	EXTRUDE	F-6	2.0		0.0	NS	0.0	5.0		454.0	3.0		454.0	0	NS
BOD5	3	EXTRUDE	G-1	5.0	<	0.0	NS	414.0	0.0	NS	213.0	0.0	NS	0.0	0	NS
BOD5	3	EXTRUDE	K-2	5.0	<	5.0	<	908.0	5.0	<	908.0	5.0	<	908.0	0	NS
BOD5	3	EXTRUDE	K-3	5.0	<	5.0	<	454.0	5.0	<	454.0	5.0	<	454.0	5	<
BOD5	3	EXTRUDE	K-4	5.0	<	5.0	<	37854.0	5.0	<	33217.0	5.0	<	28391.0	0	NS
BOD5	1	EXTRUDE	M-1	38.0		130.0		818.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	1	EXTRUDE	N-2	5.0		10.0		6.6	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	2	EXTRUDE	N-3	5.0		0.0	NS	0.0	6.0		213.0	0.0	NS	0.0	0	NS
BOD5	2	EXTRUDE	O-1	0.0	NA	0.0	NA	559.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	2	EXTRUDE	O-2	0.0	NA	0.0	NA	416.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	2	EXTRUDE	R-1	4.0		6.0		881.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	2	EXTRUDE	R-2	4.0		4.0		12400.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	1	MOLD	B-4	5.0	<	5.0	<	5.6	0.0	NS	0.0	0.0	NS	0.0	5	<
BOD5	1	MOLD	C-1	83.8		96.9		63.6	84.8		63.6	90.9		63.6	0	NS
BOD5	2	MOLD	J-1	5.0	<	5.0	<	27260.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
BOD5	2	MOLD	J-2	5.0	<	56.0		2010.0	0.0	NS	0.0	0.0	NS	0.0	52	
BOD5	1	THERM	F-2	2.0		8.0		408.0	7.0		408.0	7.0		408.0	0	NS
BOD5	1	THERM	M-2	18.0		18.0		1140.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
O&G	2	CALEND	B-2	4.0	<	4.0	<	410.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
O&G	1	CALEND	E-2	19.6		16.8		3157.0	23.8		3157.0	11.8		3157.0	0	NS
O&G	1	CALEND	F-1	3.0		1.0		568.0	0.0		454.0	4.0		568.0	0	NS
O&G	1	CAST	P-1	3.0		3.0		1090.0	0.0	NS	0.0	0.0	NS	0.0	0	NS

P M & F DATA BASE - RAW VALUES

-- SUBCAT=CC & H --

POLL	SAMPTYPE	PROCESS	STREAM	SOURCE	DETECTS	DAY1	DETECT1	FLOW1	DAY2	DETECT2	FLOW2	DAY3	DETECT3	FLOW3	DUPLICAT	DETECTD
O&G	2	EXTRUDE	B-1	4.000	<	4.000	<	181.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	2	EXTRUDE	D-3	4.000	<	4.000	<	23.7	0.00	NS	0.0	0.000	NS	0.0	4.000	<
O&G	1	EXTRUDE	E-3	19.600		20.000		8040.0	27.80		8040.0	19.400		8040.0	0.000	NS
O&G	1	EXTRUDE	F-6	3.000		0.000	NS	0.0	5.00		454.0	4.000		454.0	0.000	NS
O&G	2	EXTRUDE	G-1	6.000		4.000	<	414.0	4.00		213.0	0.000	NS	0.0	0.000	NS
O&G	2	EXTRUDE	K-2	4.000	<	4.000	<	908.0	4.00	<	908.0	4.000	<	908.0	0.000	NS
O&G	2	EXTRUDE	K-3	4.000	<	4.000	<	454.0	4.00	<	454.0	4.000	<	454.0	4.000	<
O&G	2	EXTRUDE	K-4	4.000	<	4.000	<	37854.0	4.00	<	33217.0	4.000	<	28391.0	0.000	NS
O&G	1	EXTRUDE	M-1	1.000	<	31.000		818.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	1	EXTRUDE	N-2	1.000	<	5.000		6.6	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	1	EXTRUDE	N-3	1.000	<	0.000	NS	0.0	3.00		213.0	0.000	NS	0.0	0.000	NS
O&G	1	EXTRUDE	O-1	9.000		5.000		559.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	1	EXTRUDE	O-2	9.000		3.000		416.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	1	EXTRUDE	R-1	7.000		6.000		881.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	1	EXTRUDE	R-2	7.000		8.000		12400.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	2	MOLD	B-4	4.000	<	4.000		5.6	0.00	NS	0.0	0.000	NS	0.0	10.000	
O&G	1	MOLD	C-1	17.000		75.000		63.6	24.50		63.6	41.000		63.6	0.000	NS
O&G	2	MOLD	J-1	4.000	<	11.000		27260.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS
O&G	2	MOLD	J-2	4.000	<	73.000		2010.0	0.00	NS	0.0	0.000	NS	0.0	49.000	
O&G	1	THERM	F-2	3.000		3.000		408.0	0.00		408.0	5.000		408.0	0.000	NS
O&G	1	THERM	M-2	74.000		29.000		1140.0	0.00	NS	0.0	0.000	NS	0.0	0.000	NS

P M & F DATA BASE - RAW VALUES

SUBCAT=CC & H

POLL	SAMPTYPE	PROCESS	STREAM	SOURCE	DETECTS	DAY1	DETECT1	FLOW1	DAY2	DETECT2	FLOW2	DAY3	DETECT3	FLOW3	DUPLICAT	DETECTD
TSS	1	CALEND	B-2	4.000	<	4.000	<	410.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	3	CALEND	E-2	1.000		3.000		3157.0	4.0		3157.0	2.0		3157.0	0	NS
TSS	3	CALEND	F-1	2.000		6.000		568.0	3.0		454.0	5.0		568.0	0	NS
TSS	2	CAST	P-1	1.000	<	2.000		1090.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	1	EXTRUDE	B-1	4.000	<	4.000	<	181.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	1	EXTRUDE	D-3	4.000	<	4.000	<	23.7	0.0	NS	0.0	0.0	NS	0.0	4	<
TSS	3	EXTRUDE	E-3	1.000		4.000		8040.0	2.0		8040.0	3.0		8040.0	0	NS
TSS	3	EXTRUDE	F-6	2.000		0.000	NS	0.0	1.0		454.0	1.0	<	454.0	0	NS
TSS	3	EXTRUDE	G-1	16.000		22.000		414.0	4.0		213.0	0.0	NS	0.0	0	NS
TSS	3	EXTRUDE	K-2	4.000	<	6.000		908.0	4.0		908.0	4.0	<	908.0	0	NS
TSS	3	EXTRUDE	K-3	4.000	<	4.000	<	454.0	4.0	<	454.0	4.0	<	454.0	4	<
TSS	3	EXTRUDE	K-4	4.000	<	4.000		37854.0	4.0	<	33217.0	4.0		28391.0	0	NS
TSS	1	EXTRUDE	M-1	1.000	<	5.000		818.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	1	EXTRUDE	N-2	3.000		1.000	<	6.6	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	2	EXTRUDE	N-3	3.000		0.000	NS	0.0	1.0	<	213.0	0.0	NS	0.0	0	NS
TSS	2	EXTRUDE	O-1	1.000	<	1.000	<	559.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	2	EXTRUDE	O-2	1.000	<	1.000	<	416.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	2	EXTRUDE	R-1	1.000	<	1.000	<	881.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	2	EXTRUDE	R-2	1.000	<	1.000	<	12400.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	1	MOLD	B-4	4.000	<	4.000		5.6	0.0	NS	0.0	0.0	NS	0.0	4	<
TSS	3	MOLD	C-1	0.000		104.000		63.6	77.0		63.6	18.0		63.6	0	NS
TSS	2	MOLD	J-1	4.000	<	4.000		27260.0	0.0	NS	0.0	0.0	NS	0.0	0	NS
TSS	2	MOLD	J-2	4.000	<	36.000		2010.0	0.0	NS	0.0	0.0	NS	0.0	38	
TSS	3	THERM	F-2	2.000		1.000	<	408.0	2.0		408.0	1.0		408.0	0	NS
TSS	1	THERM	M-2	9.000		4.000		1140.0	0.0	NS	0.0	0.0	NS	0.0	0	NS

P M & F DATA BASE - RAW VALUES

SUBCAT=CLEAN

POLL	SAMPTYPE	PROCESS	STREAM	SOURCE	DETECTS	DAY1	DETECT1	FLOW1	DAY2	DETECT2	FLOW2	DAY3	DETECT3	FLOW3	DUPLICAT	DETECTD
BOD5	1	CLEAN	A-1	5.00	<	9.00		37.9	0.00	NS	0.0	0.00	NS	0	0.00	NS
BOD5	1	CLEAN	A-2	5.00	<	450.00		151.0	0.00	NS	0.0	0.00	NS	0	0.00	NS
BOD5	1	CLEAN	B-3	5.00	<	48.00		4540.0	46.00		4540.0	52.00		4540	0.00	NS
BOD5	1	CLEAN	C-2	83.80		84.80		200.0	48.50		649.0	72.70		505	0.00	NS
BOD5	0	CLEAN	D-1	0.00	NS	0.00	NS	56.8	0.00	NS	0.0	0.00	NS	0	0.00	NS
BOD5	0	CLEAN	D-2	0.00	NS	0.00	NS	56.8	0.00	NS	0.0	0.00	NS	0	0.00	NS
BOD5	1	CLEAN	F-3	2.00		510.00		780.0	247.00		519.0	52.00		1110	0.00	NS
BOD5	1	CLEAN	F-4	2.00		198.00		4540.0	34.00		397.0	26.00		113	0.00	NS
BOD5	1	CLEAN	H-1	5.00	<	1000.00		15.1	630.00		15.1	0.00	NS	0	850.00	
BOD5	1	CLEAN	I-1	1.70		6.30		228.0	6.10		355.0	6.20		344	0.00	NS
BOD5	1	CLEAN	I-2	1.70		2.60		178.0	5.95		77.6	5.65		234	0.00	NS
BOD5	1	CLEAN	I-3	1.70		3.20		405.0	0.00	NS	0.0	6.60		344	0.00	NS
BOD5	2	CLEAN	K-1	5.00	<	20.00		115.0	0.00	NS	0.0	0.00	NS	0	0.00	NS
O&G	2	CLEAN	A-1	4.00	<	4.00	<	37.9	0.00	NS	0.0	0.00	NS	0	0.00	NS
O&G	2	CLEAN	A-2	4.00	<	4.00	<	151.0	0.00	NS	0.0	0.00	NS	0	0.00	NS
O&G	2	CLEAN	B-3	4.00	<	4.00	<	4540.0	4.00	<	4540.0	4.00	<	4540	0.00	NS
O&G	1	CLEAN	C-2	17.00		31.00		200.0	0.00		649.0	17.50		505	0.00	NS
O&G	2	CLEAN	D-1	4.00	<	4.00	<	56.8	0.00	NS	0.0	0.00	NS	0	0.00	NS
O&G	2	CLEAN	D-2	4.00	<	4.00	<	56.8	0.00	NS	0.0	0.00	NS	0	0.00	NS
O&G	1	CLEAN	F-3	3.00		548.00		780.0	684.00		519.0	0.00	NS	1110	0.00	NS
O&G	1	CLEAN	F-4	3.00		3.00		4540.0	89.00		397.0	0.00	NS	113	0.00	NS
O&G	2	CLEAN	H-1	4.00	<	4.00	<	15.1	4.00	<	15.1	0.00	NS	0	4.00	<
O&G	1	CLEAN	I-1	0.00		18.00		228.0	7.00		355.0	44.70		344	0.00	NS
O&G	1	CLEAN	I-2	0.00		234.50		178.0	21.80		77.6	174.10		234	0.00	NS
O&G	1	CLEAN	I-3	0.00		21.20		405.0	0.00	NS	0.0	7.80		344	0.00	NS
O&G	2	CLEAN	K-1	4.00	<	4.00	<	115.0	0.00	NS	0.0	0.00	NS	0	0.00	NS

P M & F DATA BASE - RAW VALUES

SUBCAT=CLEAN

POLL	SAMPTYPE	PROCESS	STREAM	SOURCE	DETECTS	DAY1	DETECT1	FLOW1	DAY2	DETECT2	FLOW2	DAY3	DETECT3	FLOW3	DUPLICAT	DETECTD
TSS	1	CLEAN	A-1	8.000		12.0		37.9	0.0	NS	0.0	0.0	NS	0	0.00	NS
TSS	1	CLEAN	A-2	8.000		39.0		151.0	0.0	NS	0.0	0.0	NS	0	0.00	NS
TSS	3	CLEAN	B-3	4.000	<	4.0	<	4540.0	4.0	<	4540.0	4.0	<	4540	0.00	NS
TSS	3	CLEAN	C-2	0.000		8.0		200.0	2.0		649.0	11.0		505	0.00	NS
TSS	1	CLEAN	D-1	4.000	<	13.0		56.8	0.0	NS	0.0	0.0	NS	0	0.00	NS
TSS	1	CLEAN	D-2	4.000	<	8.0		56.8	0.0	NS	0.0	0.0	NS	0	0.00	NS
TSS	3	CLEAN	F-3	2.000		198.0		780.0	274.0		519.0	466.0		1110	0.00	NS
TSS	3	CLEAN	F-4	2.000		90.0		4540.0	1310.0		397.0	68.0		113	0.00	NS
TSS	1	CLEAN	H-1	5.000		11.0		15.1	4.0	<	15.1	0.0	NS	0	10.00	
TSS	3	CLEAN	I-1	56.000		16363.0		228.0	11738.0		355.0	12597.0		344	0.00	NS
TSS	1	CLEAN	I-2	56.000		5825.0		178.0	244.0		77.6	1039.0		234	0.00	NS
TSS	1	CLEAN	I-3	56.000		1136.0		405.0	0.0	NS	0.0	5671.0		344	0.00	NS
TSS	2	CLEAN	K-1	4.000	<	6.0		115.0	0.0	NS	0.0	0.0	NS	0	0.00	NS

```
                                                         P M & F DATA BASE - RAW VALUES

------------------------------------------------------------ SUBCAT=FINISH -------------------------------------------------------------

    POLL SAMPTYPE PROCESS STREAM  SOURCE DETECTS     DAY1 DETECT1 FLOW1     DAY2 DETECT2 FLOW2  DAY3    DETECT3 FLOW3 DUPLICAT DETECTD

    TSS     3     FINISH   I-4   33.0000          63.0000          1100  289.000              1140  1359.00           1420   0.0000    NS
    TSS     3     FINISH   N-1    3.0000           7.0000          2880    1.000     <        2640     0.00    NS        0   1.0000    <
    TSS     3     FINISH   Q-1    1.0000    <      9.1000          4160    6.300              4160     0.00    NS        0  16.0000
```

APPENDIX II

Plastics Manufacturing Plants (PMP)

A) PM&P Data: Influent and Effluent BOD5, O&G and TSS

B) Summary Statistics for PMP Data

C) Probit Plots for PMP Oil and Grease Data

APPENDIX IIA

PMP Data: Influent and Effluent BOD, O&G and TSS

```
                                    LISTING OF PMP DATA BY POLLUTANT

------------------------------------------------------------- POLL=BOD --------------------------------------------------------------------------------
                          OBS      PLANT      DATE        FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

                            1        9       101575        0.05              56                 4
                            2        9       102275        0.05              70                 5
                            3        9       111275        0.25             194                 5
                            4        9       111975        0.07              54                 1
                            5        9       121075        0.06              49                 5
                            6        9       121775        0.06              32                 5
                            7        9       010776        0.10              71                14
                            8        9       011476         .               120                 5
                            9        9       021176        0.07              59                 4
                           10        9       021876         .               226                 2
                           11        9       031076        0.08              52                 7
                           12        9       032576         .                 .                 7
                           13        9       0[illegible]1476        0.06              20                 4
                           14        9       042176         .               108                 8
                           15        9       051276        0.09             192                 4
                           16        9       051976         .                17                 8
                           17        9       060976        0.13              56                 3
                           18        9       061676        0.13              54                 6
                           19        9       072176        0.07              92                10
                           20        9       072876        0.09              80                 7
                           21        9       080476        0.05               9                 4
                           22        9       081876        0.06             132                10
                           23        9       090876        0.02              27                 4
                           24        9       092276         .               179                 5
                           25       44       060179        0.92               .                13
                           26       44       060479        0.88               .                 6
                           27       44       060579        1.00               .                14
                           28       44       060679        0.80               .                15
                           29       44       060779        0.38               .                 9
                           30       44       060879        0.83               .                16
                           31       44       061179        0.94               .                 4
                           32       44       061279        0.79               .                 5
                           33       44       061379        0.80               .                18
                           34       44       061479        1.13               .                18
                           35       44       061579        0.45               .                17
                           36       44       061879        0.57               .                 1
                           37       44       061979        0.71               .                16
                           38       44       062079        0.39               .                17
                           39       44       062179        0.57               .                16
                           40       44       062279        0.36               .                14
                           41       44       062579        0.83               .                 3
                           42       44       062679        0.68               .                13
                           43       44       062779        0.60               .                12
                           44       44       062879        0.62               .                10
                           45       44       062979        0.80               .                14
                           46       44       070279        0.81               .                 2
                           47       44       070379        0.63            1000                 5
                           48       44       070479        0.51               .                10
                           49       44       070579        0.25               .                10
                           50       44       070679        0.34               .                13
                           51       44       070979        0.79               .                 8
                           52       44       071079        0.71               .                17
                           53       44       071179        0.73               .                 8
                           54       44       071279        0.74               .                27
```

```
------------------------------------------------------ POLL=BOD ------------------------------------------------------

        OBS     PLANT     DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

         55      44      071379       0.80               .                14
         56      44      071679       0.74               .                 7
         57      44      071779       0.79               .                 8
         58      44      071879       0.73               .                 3
         59      44      071979       0.73               .                15
         60      44      072079       0.90               .                22
         61      44      072379       0.54               .                 5
         62      44      072479       0.69               .                 4
         63      44      072579       0.73               .                15
         64      44      072679       0.81               .                29
         65      44      072779       0.71               .                22
         66      44      073079       0.79               .                 4
         67      44      073179       0.43               .                11
         68      44      080179       0.38             769                 4
         69      44      080279       0.46               .                 7
         70      44      080379       0.66               .                 4
         71      44      080679       0.74               .                 5
         72      44      080779       0.26               .                 6
         73      44      080879       0.56            1090                13
         74      44      080979       0.73               .                 9
         75      44      081079       0.75               .                 9
         76      44      081379       0.74               .                 7
         77      44      081479       0.65               .                24
         78      44      081579       0.79            1689                16
         79      44      081679       0.73               .                20
         80      44      081779       0.84               .                21
         81      44      082079       0.83               .                10
         82      44      082179       0.85               .                22
         83      44      082279       0.73            1311                13
         84      44      082379       0.67               .                31
         85      44      082479       0.94               .                21
         86      44      082779       0.96               .                 3
         87      44      082879       0.96               .                15
         88      44      082979       0.91             700                13
         89      44      083079       0.90               .                14
         90      44      083179        .                 .                 9
         91      44      090379       0.10             622                 7
         92      44      090479       0.34               .                 5
         93      44      090579       0.28               .                 7
         94      44      090679       0.38               .                 8
         95      44      090779       0.33               .                 9
         96      44      091079       0.62               .                11
         97      44      091179       0.70               .                13
         98      44      091279       0.67               .                 9
         99      44      091379       0.72               .                13
        100      44      091479       0.85               .                13
        101      44      091779       0.88             304                11
        102      44      091879       0.88               .                13
        103      44      091979       0.46             648                 5
        104      44      092079       0.33               .                 4
        105      44      092179       0.43               .                 4
        106      44      092479       0.31             225                 5
        107      44      092579       0.27               .                 3
        108      44      092679       0.37               .                 3
```

```
                              LISTING OF PMP DATA BY POLLUTANT

-------------------------------------------- POLL=BOD --------------------------------------------

          OBS     PLANT     DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

          109      44      092779       0.36             .                8
          110      44      092879       0.35             .                9
          111      44      100179       0.55            794               7
          112      44      100279       0.57             .                8
          113      44      100379       0.45             .                8
          114      44      100479       0.36             .                6
          115      44      100579       0.57             .                7
          116      44      100879       0.96            806               4
          117      44      100979       0.46             .                7
          118      44      101079       0.64             .                9
          119      44      101179       0.70             .                6
          120      44      101279       0.68             .                6
          121      44      101579       0.23            500               3
          122      44      101679       0.67             .                8
          123      44      101779       0.67             .                6
          124      44      101879       0.60             .                5
          125      44      101979       0.62             .                8
          126      44      102279       0.60            369               3
          127      44      102379       0.68             .                7
          128      44      102479       0.69             .                6
          129      44      102579       0.60             .               11
          130      44      102679       0.59             .                8
          131      44      102979       0.60             .               10
          132      44      103079       0.67             .               17
          133      44      103179       0.10             .               18
          134      44      110179       0.52           1019              11
          135      44      110279       0.72             .               11
          136      44      110579       0.58             .                4
          137      44      110679       0.59             .                7
          138      44      110779       0.68             .                9
          139      44      110879       0.68            816              10
          140      44      110979       0.53             .                9
          141      44      111279       0.66             .               11
          142      44      111379       0.98             .                9
          143      44      111479       0.65             .               11
          144      44      111579       0.5[illegible]            781               8
          145      44      111679       0.5[illegible]             .               11
          146      44      111979       0.72             .               15
          147      44      112079       0.78             .               15
          148      44      112179       0.78             .               12
          149      44      112279       0.35            906              14
          150      44      112379       0.11             .                5
          151      44      112679       0.58             .                5
          152      44      112779       0.78             .                5
          153      44      112879       0.69             .                5
          154      44      112979       0.70            925              13
          155      44      113079       0.78             .                6
          156      44      120379       0.74            654               1
          157      44      120479       0.55             .                7
          158      44      120579       0.60             .                6
          159      44      120679       0.66             .                4
          160      44      120779       0.70             .                4
          161      44      121079       1.12            721               5
          162      44      121179       0.63             .               14
```

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                              LISTING OF PMP DATA BY POLLUTANT

---------------------------------------------------- POLL=BOD --------------------------------------------------------

      OBS      PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

      163       44       121279       0.79               .                4
      164       44       121379       0.60               .                3
      165       44       121479       0.63               .                5
      166       44       121779       0.61             956                3
      167       44       121879       0.58               .                4
      168       44       121979       0.57               .                5
      169       44       122079       0.52               .                5
      170       44       122179       0.65               .                8
      171       44       122479       0.36            1020                9
      172       44       122579       0.47               .               14
      173       44       122679       0.41               .               10
      174       44       122779       0.30               .                7
      175       44       122879       0.41               .                8
      176       44       123179       0.63               .                6
      177       44       010180       0.53             697               15
      178       44       010280       0.15               .               20
      179       44       010380       0.59               .               10
      180       44       010480       0.50               .               13
      181       44       010780       0.67             587               14
      182       44       010880       0.63            1157                7
      183       44       010980       0.65               .                5
      184       44       011080       0.47               .                6
      185       44       011180       0.69               .                8
      186       44       011480       0.32               .                3
      187       44       011580       0.60             722               13
      188       44       011680       0.76               .                7
      189       44       011780       0.74               .               10
      190       44       011880       0.56               .               11
      191       44       012180       0.62               .                3
      192       44       012280       0.60            1010               10
      193       44       012380       0.85               .               14
      194       44       012480       0.53               .               12
      195       44       012580       0.61               .               11
      196       44       012880       0.56               .                5
      197       44       012980       0.48               .               10
      198       44       013080       0.48               .                9
      199       44       013180       0.54               .                6
      200       44       020180       0.67             611                5
      201       44       020480       0.87               .               12
      202       44       020580       0.55               .                8
      203       44       020680       0.49               .                6
      204       44       020780       0.46               .                5
      205       44       020880       0.94             802               10
      206       44       021180       0.69               .                5
      207       44       021280       0.25               .                6
      208       44       021380       0.51               .               10
      209       44       021480       0.63               .                7
      210       44       021580       0.57             855                8
      211       44       021880       0.47               .               10
      212       44       021980       0.65               .               14
      213       44       022080       0.69               .               13
      214       44       022180       0.74               .               13
      215       44       022280       0.71             590               15
      216       44       022580       0.89                                6
```

```
                                   LISTING OF FMP DATA BY POLLUTANT                                              5

---------------------------------------------------------- POLL=BOD --------------------------------------------------------------

                 OBS     PLANT      DATE       FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

                 217      44       022680        0.85             .                 9
                 218      44       022780        0.78             .                 6
                 219      44       022880        0.58             .                 3
                 220      44       022980        0.46             .                 3
                 221      44       030380        0.44            710                9
                 222      44       030480        0.50             .                 9
                 223      44       030580        0.57             .                 5
                 224      44       030680        0.61             .                12
                 225      44       030780        1.04             .                 7
                 226      44       031080        0.79            666               10
                 227      44       031180        0.64             .                 8
                 228      44       031280        0.63             .                 8
                 229      44       031380        0.82             .                 9
                 230      44       031480        0.80             .                 8
                 231      44       031780        0.91            599                8
                 232      44       031880        0.86             .                 7
                 233      44       031980        0.82             .                 3
                 234      44       032080        1.00             .                 8
                 235      44       032180        0.97             .                 8
                 236      44       032480        0.62            618                4
                 237      44       032580        0.78             .                 3
                 238      44       032680        0.75             .                 3
                 239      44       032780        0.71             .                 3
                 240      44       032880        0.82             .                 3
                 241      44       033180        0.73             .                 3
                 242      44       040180        0.81            552               12
                 243      44       040280        0.82             .                 3
                 244      44       040380        0.56             .                 7
                 245      44       040480        0.21             .                10
                 246      44       040780        0.64             .                 4
                 247      44       040880        0.90            736                3
                 248      44       040980        0.71             .                 3
                 249      44       041080        0.92             .                 3
                 250      44       041180        0.93             .                 3
                 251      44       041480        0.95             .                 3
                 252      44       041580        0.70            583                3
                 253      44       041680        0.74             .                 7
                 254      44       041780        0.87             .                 6
                 255      44       041880        0.86             .                 3
                 256      44       042180        0.76             .                 4
                 257      44       042280        0.55            549                5
                 258      44       042380        0.73             .                 3
                 259      44       042480        0 73             .                 3
                 260      44       042580        0.59             .                 3
                 261      44       042880        0.62             .                 4
                 262      44       042980        0.60             .                 6
                 263      44       043080        0.62             .                 7
                 264      44       050180        0.70            675                4
                 265      44       050280        0.67             .                 4
                 266      44       050580        0.87             .                 5
                 267      44       050680        0.96             .                10
                 268      44       050780        0.87             .                14
                 269      44       050880        0.32            911               13
                 270      44       050980        0.60             .                15
```

```
------------------------------------------------ POLL=BOD ------------------------------------------------

OBS    PLANT    DATE     FLOW(MGD)   INFLUENT(PPM)   EFFLUENT(PPM)

271     44     051280      0.72            .               8
272     44     051380      0.80            .              12
273     44     051480      0.64            .              11
274     44     051580      0.35          555               9
275     44     051680      0.60            .               9
276     44     051980      0.50            .               5
277     44     052080      0.25            .               8
278     44     052180      0.11            .               9
279     44     052280      0.57          576              11
280     44     052380      0.44            .              11
281     44     052680      0.30            .               7
282     44     052780      0.48            .               6
283     44     052880      0.54            .               7
284     44     052980       .            544              10
285     44     053080       .              .               5
286     45     062879      3.31          350               1
287     45     070379      1.73          360               2
288     45     070479      1.46          308               2
289     45     070579      2.13          175               2
290     45     071079      2.35          368              11
291     45     071179      2.84          325               7
292     45     071279      2.95          288               5
293     45     071779      2.07          278               2
294     45     071879      2.43          280               2
295     45     071979      2.70          338               2
296     45     072479      3.49          310               5
297     45     072579      3.17          375               6
298     45     072679      3.26          393               5
299     45     073179      3.12            .               1
300     45     080179      3.03          165               2
301     45     080279      2.87          170               3
302     45     080779      2.94          245               1
303     45     080879      3.04          205               1
304     45     080979      2.48          283               2
305     45     081479      2.71            .               1
306     45     081579      2.56          358               5
307     45     081679      2.82          458               1
308     45     082179      3.41          315               4
309     45     082279      3.62          325               3
310     45     082379      3.56          403               2
311     45     082879      2.63          325               3
312     45     082979      2.56          308               2
313     45     083079      3.40          372               1
314     45     090479      1.61          195               2
315     45     090579      2.21          240               1
316     45     090679      2.86          200               2
317     45     091179      2.44          293               2
318     45     091279      1.92          313               1
319     45     091379      1.85          240               2
320     45     091879      2.39          331               1
321     45     091979      1.86          323               2
322     45     092079      3.04          313               2
323     45     092579      2.85          345               1
324     45     092679      2.77          325               1
```

```
---------------------------------------------------- POLL=BOD --------------------------------------------------------

OBS    PLANT    DATE     FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

325     45     092779      2.52           298               1
326     45     100279      2.24           288               2
327     45     100379      2.27           255               2
328     45     100479      2.66           288               3
329     45     100979      2.19           353               4
330     45     101079      2.52           420               2
331     45     101679      2.10             .               5
332     45     101779      1.95           468               4
333     45     101879      1.42           479               3
334     45     102379      2.26             .               6
335     45     102479      1.22             .               8
336     45     102579      1.55             .               2
337     45     103079      2.26             .               3
338     45     103179      1.86           320               3
339     45     110179      1.56           345               2
340     45     110679      1.59           395               5
341     45     110779      1.57           520               5
342     45     110879      1.73           425               3
343     45     111379      2.17           570               6
344     45     111479      1.41           678               4
345     45     111579      1.19           435               3
346     45     112079      1.65           385               2
347     45     112179      1.49           410               3
348     45     112279      0.96           430               3
349     45     112779      1.36           260               1
350     45     112879      1.48           303               1
351     45     112979      2.01           330               5
352     45     120479      1.36           273               1
353     45     120579      1.98           400               4
354     45     120679      1.54           315               3
355     45     121179      2.12           425               4
356     45     121279      2.03           477               6
357     45     121379      2.21           528               3
358     45     121879      2.09           487               4
359     45     121979      2.20           360               6
360     45     122079      2.22           513               3
361     45     122579      1.04           330               4
362     45     122679      1.65           320               4
363     45     122779      2.09           305               4
364     45     010180      0.74           430               3
365     45     010280      2.06           483               4
366     45     010380      1.93           482               6
367     45     010880      1.61           545               4
368     45     010980      1.74           660               3
369     45     011080      1.60           680               4
370     45     011580      1.59           450               4
371     45     011680      1.55           344               6
372     45     011780      1.53           365               2
373     45     012280      1.72           550              12
374     45     012380      1.91           760               4
375     45     012480      1.47           495               3
376     45     012980      1.80           510               5
377     45     013080      1.66           495               9
378     45     013180      1.64           518               6
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------------------------------------------------------- POL.=BOD ---------------------------------------------------------------------

                OBS     PLANT      DATE       FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

                379      45       020580        1.64             570                 3
                380      45       020680        1.48             475                 7
                381      45       020780        1.98             378                 3
                382      45       021280        2.02             390                 4
                383      45       021380        2.15             533                 3
                384      45       021480        1.92             513                 2
                385      45       021980        1.93             465                 3
                386      45       022080        2.13             425                 3
                387      45       022180        1.66             645                 2
                388      45       022680        1.40             470                 5
                389      45       022780        1.70               .                 3
                390      45       022880        1.06             455                 3
                391      45       030480        1.57             593                 3
                392      45       030580        1.72             497                 3
                393      45       030680        1.55             472                 3
                394      45       031180        2.58             583                 6
                395      45       031280        2.20             492                 4
                396      45       031380        2.05             542                 3
                397      45       031880        2.03             595                 2
                398      45       031980        2.23             690                 2
                399      45       032080        2.40             508                 4
                400      45       032580        1.55             540                 3
                401      45       032680        1.68             458                 4
                402      45       032780        1.67             483                 3
                403      45       040180        2.07             410                 3
                404      45       040280        1.54             420                 2
                405      45       040380        1.53             588                 3
                406      45       040880        1.85             493                 3
                407      45       040980        1.86             473                 4
                408      45       041080        1.83             370                 3
                409      45       041580        1.67             330                 1
                410      45       041680        2.80             535                 1
                411      45       041780        2.51             440                 2
                412      45       042280        2.01             425                 4
                413      45       042380        1.93             410                 1
                414      45       042480        1.44             413                 2
                415      45       042980        1.76             475                 1
                416      45       043080        2.05             310                 1
                417      45       050180        1.72             323                 1
                418      45       050680        1.91             468                 5
                419      45       050780        2.30             368                 5
                420      45       050880        2.14             333                 5
                421      45       051380        1.88             343                 2
                422      45       051480        1.93             390                 1
                423      45       051580        1.53             435                 2
                424      45       052080        1.23             305                 1
                425      45       052180        1.17             330                 2
                426      45       052280        0.87             230                 1
                427      45       052780        1.30              55                 3
                428      45       052880        1.67              79                 1
                429      45       052980        0.99             128                 1
                430      45       060380        1.01             116                 3
                431      45       060480        0.93             160                 3
                432      45       060580        0.90             140                 3
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---------------------------------------------------------- POL=BOD ----------------------------------------------------------------------

        OBS     PLANT     DATE     FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

        433      45      061080      1.45           215               1
        434      45      061180      1.48           210               1
        435      45      061280      1.66           210               1
        436      45      061780      1.34           100               1
        437      45      061880      1.41           195               1
        438      45      061980      1.45           170               2
        439      45      062480      1.26           293               1
        440      45      062580      1.21           270               1
        441      45      062680      1.64           320               2
        442      96      093075      3.20            .                5
        443      96      100375      3.20            .                4
        444      96      100775      3.20            .                4
        445      96      101075      3.10            .               11
        446      96      101475      3.10            .                9
        447      96      101775      3.20            .                5
        448      96      102175      3.00            .                6
        449      96      102475      3.20            .                8
        450      96      102875      3.20            .                8
        451      96      110175      3.20            .                6
        452      96      110475      3.40            .                1
        453      96      110775      3.40            .                1
        454      96      111175      3.10            .                2
        455      96      111475      3.10            .                2
        456      96      111875      3.40            .                2
        457      96      112175      3.40            .                1
        458      96      112475      3.40            .                1
        459      96      112775      3.30            .                2
        460      96      120175      3.30            .                2
        461      96      120475      3.30            .                2
        462      96      120875      3.40            .                1
        463      96      121175      3.20            .                1
        464      96      121575      3.00            .                2
        465      96      121875      3.10            .                2
        466      96      122275      3.30            .                1
        467      96      122575      3.50            .                3
        468      96      122975      3 50            .                3
        469      96      010176      3.50            .                2
        470      96      010576      3.60            .                3
        471      96      010876      3.50            .                2
        472      96      011276      3.60            .                2
        473      96      011576      3.50            .                3
        474      96      012076      3.40            .                9
        475      96      012276      3.20            .                3
        476      96      012676      3.30            .                5
        477      96      012976      3.20            .                2
        478      96      020276      3.20            .                2
        479      96      020576      3.30            .                3
        480      96      020976      3.20            .                2
        481      96      021276      3.50            .                1
        482      96      021676      3.50            .                1
        483      96      021976      3.20            .                3
        484      96      022376      3.50            .                2
        485      96      022676      3.20            .                1
        486      96      030176      3.40            .                2
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                                        LISTING OF PMP DATA BY POLLUTANT

------------------------------------------------------------ POLL=BOD ------------------------------------------------------------

                  OBS     PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

                  487      96       030476        3.4             .                3
                  488      96       030876        3.3             .                1
                  489      96       031176        3.1             .                2
                  490      96       031576        3.5             .                3
                  491      96       031876        3.2             .                3
                  492      96       032276        3.2             .                1
                  493      96       032676        3.2             .                2
                  494      96       033076        3.1             .                2
                  495      96       040176        3.2             .                2
                  496      96       040576        3.4             .                2
                  497      96       040876        3.1             .                2
                  498      96       041276        3.0             .                1
                  499      96       041576        3.8             .                2
                  500      96       041976        3.5             .                2
                  501      96       042276        3.2             .                1
                  502      96       042676        3.0             .                2
                  503      96       042976        3.0             .                3
                  504      96       050376        3.1             .                3
                  505      96       050676        3.2             .                1
                  506      96       051076        3.1             .                2
                  507      96       051376        3.0             .                1
                  508      96       051776        3.2             .                3
                  509      96       052076        3.0             .                1
                  510      96       052476        3.0             .                2
                  511      96       052776        2.9             .                1
                  512      96       053176        3.1             .                1
                  513      96       060376        3.0             .                1
                  514      96       060776        3.0             .                4
                  515      96       061076        3.1             .                3
                  516      96       061476        3.2             .                3
                  517      96       061776        3.1             .                4
                  518      96       062176        3.1             .                2
                  519      96       062476        2.9             .                2
                  520      96       062876        2.9             .                2
                  521      96       070176        3.4             .                1
                  522      96       070576        3.1             .                2
                  523      96       070876        3.0             .                1
                  524      96       071276        3.0             .                2
                  525      96       071576        3.0             .                1
                  526      96       071976        3.0             .                2
                  527      96       072276        2.8             .                1
                  528      96       072676        2.9             .                1
                  529      96       072976        2.8             .                1
                  530      96       080276        2.8             .                2
                  531      96       080576        2.7             .                2
                  532      96       080976        2.9             .                1
                  533      96       081276        3.1             .                1
                  534      96       081676        3.1             .                1
                  535      96       081976        2.9             .                2
                  536      96       082376        2.7             .                1
                  537      96       082676        2.8             .                1
                  538      96       083076        2.6             .                1
                  539      96       090276        2.6             .                2
                  540      96       090676        1.7             .                1
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------------------------------------------ POLL=BOD ------------------------------------------

OBS    PLANT     DATE     FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

541      96     090976      2.50             .                1
542      96     091376      2.20             .                2
543      96     091676      2.60             .                2
544      96     092076      2.50             .                1
545      96     092376      2.20             .                1
546      96     092776      2.60             .                1
547     111     010477      0.83            55               12
548     111     010577      0.96            65               11
549     111     010677      0.93            80                6
550     111     011177      0.91           105               10
551     111     011277      0.83            90               10
552     111     011377      0.70            87               12
553     111     011877      0.78            65               10
554     111     011977      0.98            80                9
555     111     012077      0.65           100                6
556     111     012577      0.84            79                8
557     111     012677      0.99            76               13
558     111     012777      0.98            75               13
559     111     020177      0.63            80                7
560     111     020277      0.61           100               12
561     111     020377      0.73            90                6
562     111     020877      0.87            80                6
563     111     020977      0.99            85                5
564     111     021077      0.96            88                6
565     111     021577      0.92            65               10
566     111     021677      0.69            65                8
567     111     021777      1.00            60               20
568     111     022277      0.74            85                8
569     111     022377      1.14            90                6
570     111     022477      1.08           100                5
571     111     030177      0.74            80                8
572     111     030277      0.68            90               10
573     111     030377      0.43            80                5
574     111     030877      0.73            88                9
575     111     030977      0.57            83               10
576     111     031077      1.15            75                8
577     111     031577      1.37            50               10
578     111     031677      1.01            75                8
579     111     031777      1.18            84               12
580     111     032277      1.11            75               18
581     111     032377      1.06            68                8
582     111     032477      0.96            65                8
583     111     032977      0.98            70                8
584     111     033077      0.89            80                6
585     111     033177      0.95            80                6
586     111     040477      0.93            95               12
587     111     040577      1.15            70                6
588     111     040677      0.74            80                5
589     111     041277      0.92            53               10
590     111     041377      1.10            60               10
591     111     041477      0.87            55                8
592     111     041977      0.45            60                8
593     111     042077      0.94            70                8
594     111     042177      1.02            64                8
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------------------------------------------------- POLL=BOD -------------------------------------------------

OBS    PLANT    DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

595    111     042677     0.83          68               8
596    111     042777     0 96          77               6
597    111     042877     0.55          75               6
598    111     050377     0.77          68               6
599    111     050477     0.65          65               8
600    111     050577     0.81          64               6
601    111     051077     0.82          95               8
602    111     051177     0.72         100               8
603    111     051277     0.75         100               8
604    111     051777     0.93          58               8
605    111     051877     0.93          60               6
606    111     051977     0.87          60               7
607    111     052477     0.98          36               7
608    111     052577     1.07          32               7
609    111     052677     1.17          32               6
610    111     053177     1.03          32               5
611    111     060177     0.85          40               6
612    111     060277     1.17          45               7
613    111     060777     1.09          32              15
614    111     060877     1.08          40               8
615    111     060977     0.77          38               8
616    111     061477     0.85          37               5
617    111     061577     0.82          40               4
618    111     061677     0.84          50               6
619    111     062177     0 42          32               5
620    111     062277     0.92          24               4
621    111     062377     1.01          32               4
622    111     062877     1.01          73              14
623    111     062977     0.62          75              10
624    111     063077     0.87          90               8
625    111     070577     0.66         160               4
626    111     070677     0.74         120               4
627    111     070777     0.67         115               4
628    111     071277     0.82         130               4
629    111     071377     0.99         118               5
630    111     071477     1.01         125               4
631    111     071977     0.88         140               5
632    111     072077     0.85         120               4
633    111     072177     0.97         100               4
634    111     072677     0.74         110               8
635    111     072777     0.96         100               4
636    111     072877     0.93         100               5
637    111     080277     1 08         110              16
638    111     080377     1 09         117              14
639    111     080477     1.09         118              12
640    111     080977     1.03         102               4
641    111     081077     0.93          88               4
642    111     081177     0.92         110               4
643    111     081677     0.99          75               2
644    111     081777     0.87          89               3
645    111     081877     1.16          80               3
646    111     082377     0.75         116               4
647    111     082477     0.74         120               3
648    111     082577     0.94         125               4
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POLL=BOD

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
649	111	083077	0.85	125	4
650	111	083177	0.80	110	5
651	111	090177	0.76	120	4
652	111	090677	1.00	119	3
653	111	090777	1.01	98	3
654	111	090877	0.84	95	4
655	111	091377	1.15	108	4
656	111	091477	0.97	130	4
657	111	091577	0.67	142	5
658	111	092077	1.10	106	5
659	111	092177	1.12	93	4
660	111	092277	1.30	94	5
661	111	092777	0.67	94	4
662	111	092877	0.95	107	3
663	111	092977	0.91	115	4
664	111	100477	0.76	108	3
665	111	100577	1.02	110	3
666	111	100677	0.88	109	3
667	111	101177	0.76	115	3
668	111	101277	0.86	111	3
669	111	101377	1.04	110	2
670	111	101877	1.10	92	3
671	111	101977	0.58	104	3
672	111	102077	0.85	113	3
673	111	102577	0.36	119	4
674	111	102677	0.92	120	3
675	111	102777	0.72	145	3
676	111	110177	0.81	138	3
677	111	110277	0.93	124	3
678	111	110377	1.18	123	4
679	111	110877	0.87	100	3
680	111	110977	1.01	100	3
681	111	111077	1.02	110	3
682	111	111577	0.91	147	4
683	111	111677	0.75	150	3
684	111	111777	0.88	165	3
685	111	112077	0.72	186	3
686	111	112177	0.82	200	2
687	111	112277	0.79	340	7
688	111	112377	0.65	180	13
689	111	112977	0.84	175	2
690	111	113077	1.15	130	2
691	111	120177	0.97	130	2
692	111	120677	1.03	120	2
693	111	120777	1.11	120	2
694	111	120877	0.68	110	3
695	111	121377	0.91	105	8
696	111	121477	1.06	95	7
697	111	121577	0.68	95	4
698	111	121977	0.73	100	3
699	111	122077	0.86	100	3
700	111	122177	0.92	95	3
701	111	122777	0.79	130	4
702	111	122877	0.71	128	3

POLL=BOD

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
703	111	122977	0.86	127	3.0
704	126	100275	0.38	1500	6.8
705	126	100575	0.28	640	4.4
706	126	100675	0.33	670	4.5
707	126	100775	0.30	460	6.2
708	126	100875	0.38	1500	6.2
709	126	100975	0.34	1800	6.9
710	126	101275	0.32	1300	4.7
711	126	101375	0.36	1100	5.1
712	126	101475	0.38	1100	4.4
713	126	101575	0.43	1100	4.4
714	126	101675	0.49	1200	4.7
715	126	101975	0.38	460	3.1
716	126	102075	0.32	330	4.8
717	126	102175	0.33	500	3.9
718	126	102275	0.31	1100	5.9
719	126	102375	0.32	1000	3.5
720	126	102675	0.30	1200	6.2
721	126	102775	0.44	1300	4.4
722	126	102875	0.53	1300	4.0
723	126	102975	0.41	910	4.4
724	126	103075	0.36	1100	3.9
725	126	110275	0.29	530	2.2
726	126	110375	0.30	540	2.5
727	126	110475	0.30	430	2.1
728	126	110575	0.37	1500	2.4
729	126	110675	0.39	1500	2.6
730	126	110975	0.44	1400	4.1
731	126	111075	0.58	1500	3.1
732	126	111175	0.48	1500	2.4
733	126	111275	0.45	1500	2.4
734	126	111375	0.49	1000	3.4
735	126	111675	0.41	1200	3.3
736	126	111775	0.43	660	1.7
737	126	111875	0.44	1100	2.5
738	126	111975	0.46	1100	1.8
739	126	112075	0.46	1500	1.6
740	126	112375	0.36	910	1.7
741	126	112475	0.38	1000	2.3
742	126	112575	0.41	370	2.4
743	126	112775	0.40	300	1.6
744	126	113075	0.35	570	2.0
745	126	120175	0.38	910	0.9
746	126	120275	0.33	900	1.7
747	126	120375	0.33	690	1.1
748	126	120475	0.40	490	2.6
749	126	120775	0.38	410	0.6
750	126	120875	0.35	760	1.1
751	126	120975	0.40	500	2.4
752	126	121075	0.30	570	1.5
753	126	121175	0.26	360	1.5
754	126	121475	0.39	520	2.0
755	126	121575	0.38	670	3.0
756	126	121675	0.35	750	1.4

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------------------------------------------------------------- POLL=BOD -------------------------------------------------------------------------

      OBS     PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

      757      126      121775       0.33             720               2.9
      758      126      121875       0.36             490               3.2
      759      126      122175       0.25             560               2.0
      760      126      122275       0.31             370               2.7
      761      126      122375       0.34             410               2.1
      762      126      122575       0.43             370               5.7
      763      126      122875       0.45             700               1.7
      764      126      122975       0.45             330               1.1
      765      126      123075       0.42             720               1.8
      766      126      010176       0.29             720               3.7
      767      126      010476       0.45             520              13.0
      768      126      010576       0.42             400               5.3
      769      126      010676       0.43             430               3.5
      770      126      010776       0.32             370               4.4
      771      126      010876       0.35             770               4.1
      772      126      011176       0.39            1700               3.2
      773      126      011276       0.40             830               3.2
      774      126      011376       0.37            1000               3.8
      775      126      011476       0.35            1500               1.8
      776      126      011576       0.32            1700               2.0
      777      126      011876       0.30             430               2.1
      778      126      011976       0.34             660               5.5
      779      126      012076       0.35             440               2.1
      780      126      012176       0.36            1000               2.5
      781      126      012276       0.33             660               1.3
      782      126      012576       0.39             370               2.0
      783      126      012676       0.35             970               3.3
      784      126      012776       0.35            1300               1.6
      785      126      012876       0.46            1200               9.9
      786      126      012976       0.44            1500               4.4
      787      126      020176       0.45            1700               5.0
      788      126      020276       0.34            2100               4.0
      789      126      020376       0.37             890               4.2
      790      126      020476       0.38            2000               4.5
      791      126      020576       0.41             500               7.2
      792      126      020876       0.46             800               4.3
      793      126      020976       0.42             630               3.3
      794      126      021076       0.35            1700               4.4
      795      126      021176       0.37            1200               3.9
      796      126      021276       0.34             930               4.3
      797      126      021676       0.35            1900               5.9
      798      126      021776       0.34            2400               4.6
      799      126      021876       0.36            1400               4.7
      800      126      021976       0.41            1100               4.7
      801      126      022276       0.27            1000               4.3
      802      126      022376       0.31             430               4.0
      803      126      022476       0.33             540               4.0
      804      126      022576       0.21             540               3.3
      805      126      022676       0.30             560               3.9
      806      126      022976       0.29             760               3.7
      807      126      030176       0.25             310               3.6
      808      126      030276       0.31             420               7.6
      809      126      030376       0.33             430               5.4
      810      126      030476       0.29             470               5.6
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                                   LISTING OF PMP DATA BY POLLUTANT

------------------------------------------------------------- POLL=BOD ------------------------------------------------------------------

              OBS     PLANT       DATE       FLOW(MGD)     INFLUENT(PPM,      EFFLUENT(PPM)

              811      126       030776        0.23             820                6.9
              812      126       030876        0.38             820                7.2
              813      126       030976        0.45             820                8.0
              814      126       031076        0.37            1500                7.7
              815      126       031176        0.39            1300                7.5
              816      126       031476        0.24            1400               12.0
              817      126       031576        0.33            1800               10.0
              818      126       031676        0.40            1100               12.0
              819      126       031776        0.35             930                9.2
              820      126       031876        0.29            1600                9.2
              821      126       032176        0.26            2200               19.0
              822      126       032276        0.25             630               18.0
              823      126       032376        0.26            1500               11.0
              824      126       032476        0.27            1300               12.0
              825      126       032576        0.27            1300               14.0
              826      126       032876        0.26             490               13.0
              827      126       032976        0.32             660               11.0
              828      126       033076        0.39            1600               13.0
              829      126       033176        0.51            1154               19.0
              830      126       040176        0.44            1500               16.0
              831      126       040476        0.38            1800               15.0
              832      126       040576        0.30            1800               20.0
              833      126       040676        0.23            2000               18.0
              834      126       040776        0.26            2600               15.0
              835      126       040876        0.25            2500               14.0
              836      126       041176        0.23            1600               11.0
              837      126       041276        0.23            1000                8.4
              838      126       041376        0.26            1500               14.0
              839      126       041476        0.27             600                7.8
              840      126       041876        0.28             640               11.0
              841      126       041976        0.33             660               13.0
              842      126       042076        0.36             840               12.0
              843      126       042176        0.33            1100               12.0
              844      126       042276        0.33            1800               12.0
              845      126       042576        0.31             820                5.4
              846      126       042676        0.33             930                6.6
              847      126       042776        0.28             730                5.7
              848      126       042876        0.29            1200                7.5
              849      126       050576        0.30            2300               18.0
              850      126       050676        0.40            1900               15.0
              851      126       050976        0.33            1300               11.0
              852      126       051076        0.37            1300               12.0
              853      126       051176        0.39            1300                9.1
              854      126       051276        0.32            1100                8.5
              855      126       051376        0.43             930                6.9
              856      126       051676        0.19            1200                6.6
              857      126       051776        0.36             560                6.3
              858      126       051876        0.35            1700                4.6
              859      126       051976        0.34            2100                8.1
              860      126       052076        0.34            2600                7.7
              861      126       052376        0.25            2000               10.0
              862      126       052476        0.20            1600                8.7
              863      126       052576        0.22            1600               10.0
              864      126       052676        0.20            1100                8.3
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---------------------------------------------------- POLL=BOD ----------------------------------------------------

 OBS     PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

 865      126      052776       0.28            2100              4.6
 866      126      053176       0.20            1000              8.0
 867      126      060176       0.25             640              9.9
 868      126      060276       0.41             840              8.3
 869      126      060376       0.27             850              7.7
 870      126      060676       0.23             540              9.2
 871      126      060776       0.23            1100             12.0
 872      126      060876       0.23             600             12.0
 873      126      060976       0.24             530             11.0
 874      126      061076       0.27            1200             13.0
 875      126      061376       0.27            1600              6.9
 876      126      061476       0.41            1800              5.6
 877      126      061576       0.28            1000              9.3
 878      126      061676       0.38             400              5.3
 879      126      061776       0.45             540              6.9
 880      126      062076       0.37            1600              6.2
 881      126      062176       0.42            2100             10.0
 882      126      062276       0.50            1500              5.9
 883      126      062376       0.43            1800              4.5
 884      126      062476       0.37            1300              3.5
 885      126      062776       0.33             910              4.2
 886      126      062876       0.37            1500              8.3
 887      126      062976       0.39             950              6.3
 888      126      063076       0.35            1400              5.0
 889      126      070176       0.27            1000              6.8
 890      126      070576       0.28            1200              2.4
 891      126      070676       0.30            1800              8.3
 892      126      070776       0.42            2200              4.4
 893      126      070876       0.38            1100              4.3
 894      126      071176       0.27            1800             12.0
 895      126      071276       0.29            2300             14.0
 896      126      071376       0.25            1900             10.0
 897      126      071476       0.30            1100              6.0
 898      126      071576       0.37            1300              8.0
 899      126      071876       0.29               .              5.9
 900      126      071976       0.28            1000              4.1
 901      126      072076       0.28             600              6.0
 902      126      072176       0.28            2000              5.0
 903      126      072276       0.37            1400              5.1
 904      126      072576       0.38               .              2.8
 905      126      072676       0.41            2300              8.4
 906      126      072776       0.46            2400              5.4
 907      126      072876       0.38            2200              8.4
 908      126      072976       0.72             730             11.0
 909      126      080176       0.41            1000              8.7
 910      126      080276       0.33             950              5.3
 911      126      080376       0.35             930              5.1
 912      126      080476       0.33            1300              6.3
 913      126      080576       0.37            1300              5.3
 914      126      080876       0.33             700              5.1
 915      126      080976       0.31             890              5.9
 916      126      081076       0.28             820              4.1
 917      126      081176       0.28             640              2.4
 918      126      081276       0.36             530              4.2
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---------------------------------------------------- POLL=BOD ----------------------------------------------------

            OBS     PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

            919      126      081576       0.40            530              5.1
            920      126      081676       0.43            710              3.6
            921      126      081776       0.35           2000              7.4
            922      126      081876       0.33           2000             11.0
            923      126      081976       0.31           1500              8.0
            924      126      082276       0.21            540              6.9
            925      126      082376       0.24            870              4.8
            926      126      082476       0.25            980              3.8
            927      126      082576       0.29           1200              6.3
            928      126      082676       0.37            980             12.0
            929      126      082976       0.28            640              2.0
            930      126      083076       0.32            670              1.9
            931      126      083176       0.38            930              2.8
            932      126      090176       0.42           1400              3.8
            933      126      090276       0.54           1300              2.6
            934      126      090676       0.33           1400              2.3
            935      126      090776       0.46            400              2.7
            936      126      090876       0.38            870              2.7
            937      126      090976       0.30            870              4.2
            938      126      091276       0.43           1100              3.0
            939      126      091376       0.52            840              4.2
            940      126      091476       0.55            570              2.1
            941      126      091576       0.63            640              3.1
            942      126      091676       0.45            440              3.3
            943      126      091976       0.34            530              2.0
            944      126      092076       0.47            610              3.2
            945      126      092176       0.53           1800              2.0
            946      126      092276       0.52            890              2.0
            947      126      092376       0.47           1500              2.1
            948      126      092676       0.45            870              2.3
            949      126      092776       0.53            930              1.8
            950      126      092876       0.43           1100              1.2
            951      126      092976       0.38            630              1.1
            952      126      093076       0.47            980              1.5

---------------------------------------------------- POLL=OAG ----------------------------------------------------

            OBS     PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

            953        3      010377       0.19             .              27.0
            954        3      011077       0.20           52.0               .
            955        3      011677       0.19           86.5               .
            956        3      012477       0.17           62.0               .
            957        3      013177       0.16           46.0               .
            958        3      020777       0.18           82.0               .
            959        3      021477       0.16           52.0             12.0
            960        3      022177       0.20           39.0               .
            961        3      022877       0.20           31.0               .
            962        3      030777       0.21           62.0               .
            963        3      031477       0.18           62.0               .
            964        3      031777       0.20             .              22.0
            965        3      032177       0.24           44.0               .
            966        3      032877       0.22           38.0               .
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------------------------------------------------------------- POLL=OAG -------------------------------------------------------------

                 OBS     PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

                 967       3       040477       0.23           119.0                .
                 968       3       041177       0.20            83.0                .
                 969       3       041477       0.22              .               17.5
                 970       3       041877       0.21            46.0                .
                 971       3       042577       0.22            44.0                .
                 972       3       050277       0.26            43.0              12.0
                 973       3       050977       0.21            61.0                .
                 974       3       051677       0.27            27.0                .
                 975       3       052377       0.26            35.0                .
                 976       3       060677       0.26            56.0              27.5
                 977       3       061377       0.29            52.0                .
                 978       3       062077       0.26            35.0                .
                 979       3       062777       0.25            23.0                .
                 980       3       070477       0.30            44.0                .
                 981       3       071177       0.31            31.0                .
                 982       3       071877       0.26            29.0                .
                 983       3       072577       0.29            24.0              16.0
                 984       3       080877       0.27            41.0               7.0
                 985       3       081577       0.25            37.0                .
                 986       3       082277       0.32            16.0                .
                 987       3       082977       0.27            27.0                .
                 988       3       090577       0.27            30.0              22.0
                 989       3       091277       0.26            38.0                .
                 990       3       091977       0.28            75.0                .
                 991       3       092677       0.26            61.0                .
                 992       3       101077       0.26            31.0                .
                 993       3       102477       0.32            41.0              22.0
                 994       3       103177       0.33            24.0                .
                 995       3       110777       0.26            21.0                .
                 996       3       111477       0.27            30.5                .
                 997       3       111577       0.29              .               12.5
                 998       3       112177       0.26            27.0                .
                 999       3       112877       0.26            37.0                .
                1000       3       120577       0.28            36.5              12.5
                1001       3       121277       0.28            31.0                .
                1002       3       121977       0.29            46.5                .
                1003       3       122777       0.29            32.5                .
                1004       3       010978       0.28            25.0                .
                1005       3       011678       0.31            10.5               8.5
                1006       3       012378       0.34            12.0                .
                1007       3       013078       0.23            36.0                .
                1008       3       020678       0.24            16.0              13.0
                1009       3       021378       0.25            19.0                .
                1010       3       022778       0.24            26.0                .
                1011       3       030678       0.26           225.0                .
                1012       3       030778       0.26              .               26.0
                1013       3       031378       0.26           188.0                .
                1014       3       032078       0.26            56.0               3.3
                1015       3       032178       0.25              .               11.0
                1016       3       032778       0.26            42.0                .
                1017       3       040378       0.32            41.0                .
                1018       3       041078       0.34            36.5                .
                1019       3       041778       0.26            38.0                .
                1020       3       042478       0.25            36.0              11.0
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                                   LISTING OF PMP DATA BY POLLUTANT                                   20

----------------------------------------------------- POLL=OAG --- -----------------------------------------------------

              OBS      PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

              1021       3       050178       0.25           56.5               .
              1022       3       050278       0.25             .              31.0
              1023       3       050878       0.24           32.0               .
              1024       3       051578       0.23            8.0               .
              1025       3       052278       0.22            6.0               .
              1026       3       062678       0.26          312.0               .
              1027       3       062778       0.24             .              16.5
              1028       3       070378       0.27          133.0               .
              1029       3       071078       0.29           67.5               .
              1030       3       071178       0.27             .              20.5
              1031       3       071778       0.26           78.5               .
              1032       3       073178       0.27           85.0               .
              1033       3       080778       0.27           65.9               .
              1034       3       080978       0.30             .              22.5
              1035       3       081478       0.33           77.5               .
              1036       3       082178       0.30          100.5               .
              1037       3       082878       0.29           93.0               .
              1038       3       090478       0.27          230.0               .
              1039       3       091178       0.33           16.0               .
              1040       3       091278       0.29             .              10.0
              1041       3       091878       0.28           47.0               .
              1042       3       092578       0.29           99.0               .
              1043       3       100278       0.30           99.5               .
              1044       3       100978       0.27           61.5               .
              1045       3       101678       0.28           55.0              12.0
              1046       3       102378       0.28           57.5               .
              1047       3       103078       0.29            9.9               .
              1048       3       110678       0.30           48.0               .
              1049       3       111378       0.31           10.1               .
              1050       3       111578       0.32             .               3.0
              1051       3       112078       0.33           12.5               .
              1052       3       112778       0.32           15.0               .
              1053       3       120478       0.32            7.5               5.0
              1054       3       121178       0.27            9.1               .
              1055       3       121878       0.30            8.7               .
              1056       3       122578       0.30           11.9               .
              1057       3       010879       0.27            9.2               8.8
              1058       3       011579       0.29           16.0               .
              1059       3       012279       0.31           17.1               .
              1060       3       012979       0.29           15.3               .
              1061       3       020579       0.38           17.2               .
              1062       3       021279       0.28           24.4               .
              1063       3       021979       0.30           10.5               .
              1064       3       022779       0.31           11.7               4.2
              1065       3       030579       0.32           37.9               .
              1066       3       031279       0.31           22.0               .
              1067       3       031979       0.33           21.8               .
              1068       3       032879       0.32             .              18.6
              1069       3       032979       0.32             .              26.1
              1070       3       033079       0.30           26.1               .
              1071       3       040279       0.36           27.8               .
              1072       3       040979       0.37           34.0               .
              1073       3       041679       0.27           46.0               .
              1074       3       042479       0.30           30.0              14.7
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----------------------------------------------------- POLL=OAG -----------------------------------------------------------

OBS      PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

1075       3       050779       0.33            39.6               .
1076       3       051479       0.33            38.2               .
1077       3       052179       0.31            37.0              24.5
1078       3       052879       0.31            30.9               .
1079       3       060479       0.34            28.9              12.9
1080       3       061179       0.31            35.6               .
1081       3       061879       0.34            13.5               .
1082       3       062579       0.34            32.6               .
1083       3       070279       0.35            38.2               .
1084       3       070979       0.30             2.3               1.7
1085       3       071779       0.36            14.2               .
1086       3       073079       0.33            25.9               .
1087       3       080679       0.36            29.0              21.0
1088       3       081379       0.39            28.6               .
1089       3       081679       0.34              .                6.7
1090       3       082079       0.30            25.6               .
1091       3       082779       0.35            26.0               .
1092       3       090379       0.31            23.8               .
1093       3       091079       0.38            28.3               .
1094       3       091779       0.38            19.0               .
1095       3       092479       0.36             9.9               1.4
1096       3       100179         .             23.0               .
1097       3       100879       0.31             6.2               .
1098       3       100979       0.36              .                2.3
1099       3       102279       0.30             4.3               .
1100       3       102979       0.32            11.0               .
1101       3       110579       0.31            17.0               .
1102       3       110679       0.30              .                3.7
1103       3       111979       0.32            32.9               .
1104       3       112679       0.33            28.1               .
1105       3       120379       0.30             5.7               1.4
1106       3       121079       0.29            22.4               .
1107       3       121779       0.23            38.2               .
1108       3       011080       0.34            20.6              17.3
1109       3       011180       0.34              .               21.9
1110       3       011480       0.35            32.4               .
1111       3       012180       0.29            28.6               .
1112       3       012880       0.28            33.1               .
1113       3       020480       0.35            46.9               .
1114       3       021280       0.29            82.8               .
1115       3       021380       0.30              .                1.3
1116       3       021980       0.26            58.5               .
1117       3       022580       0.28            37.3               .
1118       3       030380       0.28            37.3               .
1119       3       031080       0.32            24.0               .
1120       3       031280       0.34             3.6               .
1121       3       031780       0.35              .                0.4
1122       3       032480       0.30            24.5               .
1123       3       033180       0.35            34.7               .
1124       3       040780       0.30            18.8               .
1125       3       041480       0.36            13.9               .
1126       3       041580       0.32              .                5.0
1127       3       042880       0.32            27.6               .
1128       3       050580       0.28            11.3               .
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POLL=OAG

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
1129	3	051280	0.29	11.1	.
1130	3	051380	0.30	.	2
1131	3	051980	0.28	16.9	.
1132	61	010375	.	.	28
1133	61	010675	.	.	18
1134	61	010875	.	.	16
1135	61	011575	.	.	26
1136	61	012075	.	.	49
1137	61	012275	.	.	50
1138	61	012975	.	.	18
1139	61	020375	.	.	130
1140	61	020575	.	.	21
1141	61	021075	.	.	21
1142	61	021275	.	.	30
1143	61	021775	.	.	24
1144	61	021975	.	.	31
1145	61	022475	.	.	46
1146	61	022675	.	.	19
1147	61	030375	.	.	4
1148	61	030575	.	.	6
1149	61	031075	.	.	6
1150	61	031275	.	.	7
1151	61	031775	.	.	11
1152	61	031975	.	.	76
1153	61	032475	.	.	7
1154	61	032675	.	.	14
1155	61	040175	.	.	11
1156	61	040275	.	.	7
1157	61	040375	.	.	9
1158	61	040475	.	.	10
1159	61	040775	.	.	20
1160	61	040875	.	.	19
1161	61	040975	.	.	11
1162	61	041075	.	.	22
1163	61	041175	.	.	11
1164	61	041475	.	.	31
1165	61	041575	.	.	42
1166	61	041675	.	.	18
1167	61	041775	.	.	23
1168	61	041875	.	.	5
1169	61	042175	.	.	10
1170	61	042275	.	.	13
1171	61	042375	.	.	12
1172	61	042475	.	.	19
1173	61	042575	.	.	5
1174	61	042875	.	.	29
1175	61	042975	.	.	16
1176	61	043075	.	.	38
1177	61	050175	.	.	13
1178	61	050275	.	.	6
1179	61	050575	.	.	11
1180	61	050675	.	.	13
1181	61	050775	.	.	14
1182	61	050875	.	.	10

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------------------------------------------------------------ POLL=OAG ------------------------------------------------------------

          OBS     PLANT     DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

          1183     61      050975         .               .                 3
          1184     61      051275         .               .                 9
          1185     61      051375         .               .                13
          1186     61      051475         .               .                24
          1187     61      051575         .               .                11
          1188     61      051675         .               .                13
          1189     61      051975         .               .                 9
          1190     61      052075         .               .                17
          1191     61      052175         .               .                36
          1192     61      052275         .               .                14
          1193     61      052375         .               .                16
          1194     61      052675         .               .                75
          1195     61      052775         .               .                19
          1196     61      052875         .               .               265
          1197     61      052975         .               .                13
          1198     61      053075         .               .                14
          1199     61      060275         .               .                15
          1200     61      060375         .               .                13
          1201     61      060975         .               .                 9
          1202     61      061675         .               .                 6
          1203     61      061875         .               .                13
          1204     61      062075         .               .                 3
          1205     61      062475         .               .                17
          1206     61      062675         .               .                10
          1207     61      062775         .               .                16
          1208     61      070175         .               .                14
          1209     61      070275         .               .                12
          1210     61      070375         .               .                11
          1211     61      070475         .               .                15
          1212     61      070875         .               .                 8
          1213     61      071075         .               .                13
          1214     61      071175         .               .                 5
          1215     61      071575         .               .                 5
          1216     61      071675         .               .                 4
          1217     61      071775         .               .                 5
          1218     61      071875         .               .                11
          1219     61      072275         .               .                15
          1220     61      072475         .               .                14
          1221     61      072575         .               .                14
          1222     61      072875         .               .                12
          1223     61      072975         .               .                25
          1224     61      073075         .               .                10
          1225     61      080675         .               .                 6
          1226     61      080775         .               .                11
          1227     61      080875         .               .                12
          1228     61      081175         .               .                13
          1229     61      081275         .               .                 8
          1230     61      081375         .               .                17
          1231     61      081475         .               .                11
          1232     61      081575         .               .                20
          1233     61      081875         .               .                29
          1234     61      081975         .               .                10
          1235     61      082075         .               .                11
          1236     61      082175         .               .                10
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------------------------------------------------------ POLL=OAG ------------------------------------------------------

     OBS     PLANT     DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

     1237     61      082275        .               .                55
     1238     61      082575        .               .                 9
     1239     61      082675        .               .                 6
     1240     61      082775        .               .                14
     1241     61      082875        .               .                 7
     1242     61      082975        .               .                 6
     1243     61      090175      2.73              9                 6
     1244     61      090275      2.73              9                 7
     1245     61      090375      2.73             26                 8
     1246     61      090475      2.73             12                10
     1247     61      090575      2.73             17                 8
     1248     61      090875      2.73             21                13
     1249     61      090975      2.59              .                13
     1250     61      091075      2.73             28                12
     1251     61      091175      2.59             13                11
     1252     61      091275      2.59             12                 .
     1253     61      091575      2.88              6                 .
     1254     61      091775      2.88             12                 .
     1255     61      091875      2.88              8                12
     1256     61      091975      2.88              8                 8
     1257     61      092275      2.88              7                11
     1258     61      092375      2.88              8                14
     1259     61      092475      2.88             12                 7
     1260     61      092575      3.60              7                 5
     1261     61      092975      1.58              .                17
     1262     61      093075      1.87             10                 9
     1263     61      100275      2.01             12                 8
     1264     61      100375      2.01             58                 .
     1265     61      100675      1.65             16                 8
     1266     61      100775      1.64             22                 7
     1267     61      100875      1.64             14                10
     1268     61      100975      1.65             12                 8
     1269     61      101075      1.72             13                14
     1270     61      101375      2.16             17                11
     1271     61      101475      2.59             23                 6
     1272     61      101575      2.59             24                12
     1273     61      101675      2.59             11                17
     1274     61      101775      2.59              8                 7
     1275     61      102075      2.01             14                 6
     1276     61      102175      2.01             11                 5
     1277     61      102375      1.44             11                 7
     1278     61      102475      1.87              7                 .
     1279     61      102775      2.59             35                20
     1280     61      102875      2.59              7                 6
     1281     61      102975      2.59              9                 5
     1282     61      103075      2.59             13                 7
     1283     61      103175      2.59              8                 7
     1284     61      110375      2.59             10                12
     1285     61      110475      2.59              5                 5
     1286     61      110575      2.59             21                 6
     1287     61      110675      2.44             14                 6
     1288     61      110775      2.44              7                 3
     1289     61      111175      2.44             19                 5
     1290     61      111275      2.44             14                 9
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------------------------------------------------ POLL=OAG ------------------------------------------------------------

    OBS      PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

    1291      61       111375     • 2.44              .                 8
    1292      61       111475       2.44              6                 .
    1293      61       111775       2.44              9                 3
    1294      61       111875       2.44              6                 4
    1295      61       111975       2.52             63                 4
    1296      61       112075       2.59              2                 5
    1297      61       112175       2.59              3                 4
    1298      61       112475       2.16              4                 9
    1299      61       112575       2.30             15                 9
    1300      61       112675       2.59             13                 4
    1301      61       120275       2.52             12                 .
    1302      61       120375       2.59              9                 7
    1303      61       120475       2.44              .                 8
    1304      61       120575       2.30              .                64
    1305      61       120875        .                7                 9
    1306      61       120975       2.66              8                 8
    1307      61       121075       2.73              4                 5
    1308      61       121175       2.66              6                 6
    1309      61       121275       2.59              8                 6
    1310      61       121575       2.59              9                 6
    1311      61       121675       2.73              8                 6
    1312      61       121775       2.80              9                 7
    1313      61       121975       2.73              9                 5
    1314      61       122275       2.73              9                 8
    1315      61       122975       2.73              8                 8
    1316      61       123075       2.73              6                 8
    1317      61       123175       2.73             15                11
    1318      61       010276       2.91              7                10
    1319      61       010576       2.88             15                18
    1320      61       010676       2.73              9                 8
    1321      61       010776       2.88              9                 9
    1322      61       010876       2.88              .                10
    1323      61       011276       2.89             11                14
    1324      61       011376       2.88             19                 8
    1325      61       011576       2.95              6                 9
    1326      61       011676       2.80              7                 3
    1327      61       011976       2.08              8                 5
    1328      61       012076       2.09              3                 4
    1329      61       012176       2.37              8                 8
    1330      61       012276       2.66             10                 7
    1331      61       012376       2.66              7                 7
    1332      61       013076       3.09              .                 9
    1333      61       020376       2.80              5                 5
    1334      61       020476       2.30              6                 9
    1335      61       020576       2.01              8                 8
    1336      61       020676       2.44              5                 .
    1337      61       020976       2.59             12                 9
    1338      61       021176       2.30              7                 6
    1339      61       021376       2.09              9                14
    1340      61       021675       2.16              .                13
    1341      61       021776       2.16              9                 9
    1342      61       021876       2.01             20                10
    1343      61       022376       2.44              7                16
    1344      61       022476       2.37              9                10
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--------------------------------------------------------- POLL=OAG ---------------------------------------------------------

 OBS     PLANT     DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

 1345     61      022576       2.23              .                 7
 1346     61      022776       2.23              9                 6
 1347     61      030176       1.58             10                 9
 1348     61      030276       1.58              8                 6
 1349     61      030476       1.58              8                10
 1350     61      030576       1.58              .                10
 1351     61      030876       2.03              6                 4
 1352     61      030976       2.30             11                 7
 1353     61      031076       2.44              5                 8
 1354     61      031176       2.44              8                 2
 1355     61      031276       2.44             10                 7
 1356     61      031576       2.73              6                 8
 1357     61      031776       2.16             14                 6
 1358     61      031876       1.72             14                11
 1359     61      031976       1.58              7                12
 1360     61      032276       2.01             19                 8
 1361     61      032376       2.30             17                 8
 1362     61      032476       2.37             20                 8
 1363     61      032576       2.52             13                 6
 1364     61      032676       2.59             10                 6
 1365     61      032976       2.59              8                 9
 1366     61      033076       2.59             13                10
 1367     61      033176       2.59             10                 8
 1368     61      040176       2.59              8                12
 1369     61      040576       2.30             12                 9
 1370     61      040676       2.30             12                 8
 1371     61      040776       2.30              8                 6
 1372     61      040876       2.30             11                 7
 1373     61      041176       2.30              8                 8
 1374     61      041276       2.30             20                 3
 1375     61      041376       2.01             22                 7
 1376     61      041476       2.01             16                10
 1377     61      041875       1.87              9                12
 1378     61      041976       1.67             14                 7
 1379     61      042076       1.87             17                 8
 1380     61      042276       2.47             18                10
 1381     61      042576       2.30              .                 8
 1382     61      042676       2.30             18                13
 1383     61      042776       2.44             26                 9
 1384     61      042876       2.52             27                 7
 1385     61      042976       2.12             17                15
 1386     61      050276       2.13             31                 9
 1387     61      050376       2.23             10                10
 1388     61      050476       2.30             12                 9
 1389     61      050576       2.30             21                11
 1390     61      050676       2.44              5                10
 1391     61      050976       2.88             28                11
 1392     61      051076       2.88              6                 1
 1393     61      051176       2.88              9                 4
 1394     61      051276       2.88             27                 5
 1395     61      051376       2.88              8                 2
 1396     61      051676       1.87             14                 6
 1397     61      051776       1.87             12                 5
 1398     61      051876       2.10             10                31
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----------------------------------------------------- POLL=OAG ------------------------------------------------------------

 OBS      PLANT      DATE       FLOW(MGD)     INFLUENT(PPM)      EFFLUENT(PPM)

 1399      61       051976        2.10              9                  6
 1400      61       052076        1.97              9                  5
 1401      61       052376        1.72             11                  7
 1402      61       052476        1.58             10                  5
 1403      61       052576        1.58             11                  7
 1404      61       052676        2.16             11                  8
 1405      61       052776        2.05             10                  3
 1406      61       053076        1.80             12                  6
 1407      61       053176        2.26             20                  7
 1408      61       060176        2.79              7                  4
 1409      61       060276        2.88              7                  9
 1410      61       060376        2.88             17                 21
 1411      61       060676        2.16             17                 11
 1412      61       060776        2.37             20                 18
 1413      61       060876        2.37             20                 10
 1414      61       060976        2.37             20                 13
 1415      61       061076        2.37             23                 13
 1416      61       061376        1.88             46                 41
 1417      61       061476        1.69             36                 45
 1418      61       061576        2.14             16                 31
 1419      61       061676        2.69             42                 31
 1420      61       061776        2.88             44                 41
 1421      61       062076        2.88             19                 22
 1422      61       062176        2.88             20                 11
 1423      61       062276        2.88             26                 23
 1424      61       062376        2.88             22                 19
 1425      61       062476        2.88             26                 26
 1426      61       062776        2.88             22                 20
 1427      61       062876        2.88             18                 18
 1428      61       062976        2.88             19                 17
 1429      61       063076        2.88             23                 23
 1430      61       070176        2.88             19                 27
 1431      61       070576        2.88             25                 17
 1432      61       070676        2.88             31                 29
 1433      61       071176        2.88             35                 22
 1434      61       071276        2.80             39                 33
 1435      61       071376        1.62             29                 31
 1436      61       071476        2.01             22                 29
 1437      61       071876        2.35             28                 10
 1438      61       071976        2.86             28                 16
 1439      61       072076        2.85             30                 26
 1440      61       072176        2.88             30                 29
 1441      61       072276        2.88             30                 19
 1442      61       072576        2.88             33                 29
 1443      61       072676        2.88             28                 27
 1444      61       072776        2.24             17                 14
 1445      61       072876        2.10             16                 13
 1446      61       072976        2.59             19                 16
 1447      61       073076        2.01              .                 13
 1448      61       080176        2.01             14                 13
 1449      61       080376        2.70             26                 14
 1450      61       080476        2.56             31                  4
 1451      61       080576        2.44             31                 16
 1452      61       080876        2.27             31                 18
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------------------------------------------------ POLL=OAG ------------------------------------------------

  OBS     PLANT      DATE      FLOW(MGD)      INFLUENT(PPM)      EFFLUENT(PPM)

 1453       61      080976       1.90              22                15.0
 1454       61      081076       1.65              34                17.0
 1455       61      081176       1.58              32                19.0
 1456       61      081276       1.69              27                15.0
 1457       61      081576       2.16              27                19.0
 1458       61      081676       2.16              25                19.0
 1459       61      081776       2.16              26                20.0
 1460       61      081876       2.26              33                22.0
 1461       61      081976       2.45              41                24.0
 1462       61      082276       2.10              31                17.0
 1463       61      082376       1.62              34                16.0
 1464       61      082476       2.16              25                15.0
 1465       61      082576       2.16              21                14.0
 1466       61      082676       2.16              22                21.0
 1467       61      082976       2.16              28                12.0
 1468       61      083076       2.16              30                  .
 1469       61      083176       2.23              23                14.0
 1470       61      090176       2.32              25                12.0
 1471       61      090276       2.62             230                18.0
 1472       61      090776       2.72              19                12.0
 1473       61      090876       2.70              30                  .
 1474       61      090976       2.70              30                24.0
 1475       61      091276       2.70              22                20.0
 1476       61      091376       2.70              28                25.0
 1477       61      091476       2.67              19                27.0
 1478       61      091576       2.66              25                24.0
 1479       61      091676       2.66              14                11.0
 1480       61      091976       2.72              16                13.0
 1481       61      092076       2.73               8                17.0
 1482       61      092176       2.73              12                10.0
 1483       61      092276       2.75              14                12.0
 1484       61      092376       2.80              13                18.0
 1485       61      092676       2.85              22                11.0
 1486       61      092776       2.85              13                15.0
 1487       61      092876       2.85              15                 9.0
 1488       61      092976       2.85              23                15.0
 1489       61      093076       2.85               .                13.0
 1490      124      011475        .                 .                 1.3
 1491      124      012375       0.28               .                 6.4
 1492      124      012875       0.20               .                 1.5
 1493      124      013075       0.18               .                 9.0
 1494      124      020475        .                 .                 1.5
 1495      124      020675        .                 .                 7.8
 1496      124      021175        .                 .                13.3
 1497      124      021375        .                 .                 3.0
 1498      124      021475        .                 .                 3.0
 1499      124      031375        .                 .                 0.4
 1500      124      031875        .                 .                 0.8
 1501      124      032575        .                 .                 0.6
 1502      124      041175        .                 8                  .
 1503      124      041375        .                 .                 2.6
 1504      124      041875        .                 .                 4.0
 1505      124      042075        .                 .                11.9
 1506      124      042275        .                 .                11.1
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------------------------------------------ POLL=OAG ------------------------------------------

 OBS     PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

 1507     124      042775         .              .               3.2
 1508     124      042975         .              .              11.1
 1509     124      050475         .              .               1.6
 1510     124      051175         .              .               0.8
 1511     124      051675         .              .               0.9
 1512     124      051875         .              .               8.5
 1513     124      052075         .              .               3.8
 1514     124      052375         .              .               0.5
 1515     124      052575         .              .               1.4
 1516     124      052775         .              .               0.8
 1517     124      060175         .              .               0.4
 1518     124      060675         .             4.0               .
 1519     124      061075         .              .               2.0
 1520     124      062075         .              .               0.4
 1521     124      062275         .              .               5.9
 1522     124      062375         .              .               0.3
 1523     124      062775         .              .               2.7
 1524     124      062975         .              .               0.6
 1525     124      070475         .              .               0.9
 1526     124      070675         .              .               2.8
 1527     124      070875         .              .               0.2
 1528     124      071375         .              .               0.3
 1529     124      071575         .              .               4.5
 1530     124      072275         .              .               0.2
 1531     124      072575         .              .               5.7
 1532     124      072775         .              .               3.6
 1533     124      072975         .              .               4.0
 1534     124      080175         .              .              17.3
 1535     124      080375         .              .               7.3
 1536     124      080575         .              .              14.2
 1537     124      080875         .             1.8              5.2
 1538     124      081075         .              .              23.5
 1539     124      081275         .              .              15.8
 1540     124      081575         .              .               1.0
 1541     124      081775         .              .              36.0
 1542     124      081975         .              .               2.7
 1543     124      082275         .            33.0             10.8
 1544     124      082475         .            51.1              1.2
 1545     124      082675         .              .              17.0
 1546     124      082775         .            14.2               .
 1547     124      082975         .              .              21.2
 1548     124      083175         .              .              20.4
 1549     124      090175         .            52.4               .
 1550     124      090275         .              .               1.2
 1551     124      090575         .            16.7              6.2
 1552     124      090775         .              .              29.3
 1553     124      090975         .              .              34.4
 1554     124      091275         .              .               1.2
 1555     124      091475         .              .               1.8
 1556     124      091675         .              .               6.1
 1557     124      091975         .              .               4.4
 1558     124      092175         .              .               4.6
 1559     124      092375         .              .               1.0
 1560     124      092675         .              .               1.9
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-------------------------------------- POLL=OAG --------------------------------------

 OBS     PLANT     DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

 1561     124     092875        .              .                4.0
 1562     124     093075        .              .                3.2
 1563     124     100375        .              .                3.8
 1564     124     100575        .              .                0.4
 1565     124     101075        .            13.2               .
 1566     124     101475        .            24.3               .
 1567     124     102175        .            55.2               .
 1568     124     102875        .            23.1               1.1
 1569     124     110475        .            15.7               4.1
 1570     124     111175        .             3.5               2.3
 1571     124     111875        .            24.9               .
 1572     124     112575        .            15.8               0.1
 1573     124     120275        .            13.1               5.4
 1574     124     120975        .            17.2               .
 1575     124     121675        .            40.2               1.1
 1576     124     122375        .            60.6               .
 1577     124     123075        .            22.1               4.0
 1578     124     010676        .            30.5               3.3
 1579     124     011376        .            30.7               2.4
 1580     124     012076        .             7.1               .
 1581     124     012776        .             9.0               2.9
 1582     124     020376      0.36            6.7               0.7
 1583     124     021076      0.57            7.9               .
 1584     124     021776      0.60           13.2               .
 1585     124     022476      0.17           45.1               0.5
 1586     124     030276      0.29           26.6               0.2
 1587     124     030976      0.31           37.4               0.6
 1588     124     031676      0.35           12.5               0.6
 1589     124     032376      0.47           20.6               2.4
 1590     124     033076      0.42           17.9               2.2
 1591     124     040676      0.37            8.4               2.4
 1592     124     041376      0.53           25.2               .
 1593     124     042076      0.39           76.3               .
 1594     124     042776        .           103.2               1.1
 1595     124     050476      0.33           11.1               3.0
 1596     124     051176      0.51           17.2               2.6
 1597     124     051876      0.44           14.9               3.5
 1598     124     052576      0.29           26.1               .
 1599     124     060176      0.41           39.2               .
 1600     124     060876      0.30            0.4               .
 1601     124     061576      0.36            1.9               .
 1602     124     062276        .            25.8               .
 1603     124     062976      0.31           10.1               .
 1604     124     070676        .            11.0               .
 1605     124     071276      0.32           16.1               .
 1606     124     071376      0.27             .                5.1
 1607     124     072076      0.59           10.7               1.8
 1608     124     072776      0.58           18.7               0.1
 1609     124     080376      0.40           18.3               .
 1610     124     081076      0.46            0.4               .
 1611     124     082476      0.38           11.6               .
 1612     124     082676      0.34             .               17.6
 1613     124     082776        .              .                0.1
 1614     124     083176      0.24           23.6               .
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POLL=OAG

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
1615	124	090776	0.29	46.4	2.4
1616	124	091476	0.81	17.3	.
1617	124	092176	0.46	23.6	0.7
1618	124	092876	0.66	18.4	.
1619	170	060478	3.58	48.6	2.2
1620	170	060778	4.18	62.4	15.6
1621	170	061178	2.47	28.6	3.6
1622	170	061478	3.17	55.8	9.6
1623	170	061878	3.42	50.8	2.4
1624	170	062178	3.02	81.8	6.6
1625	170	062578	3.66	134.6	2.0
1626	170	062978	3.49	42.2	8.0
1627	170	070478	3.82	35.8	6.0
1628	170	070578	3.16	61.0	3.0
1629	170	070978	3.02	52.0	9.0
1630	170	071278	2.66	64.0	3.0
1631	170	071678	3.17	12.0	3.0
1632	170	071978	3.06	52.0	6.0
1633	170	072378	3.15	24.0	8.8
1634	170	072678	3.14	71.0	2.4
1635	170	073078	2.86	34.0	5.4
1636	170	080278	2.99	159.8	17.8
1637	170	080678	2.74	50.0	4.6
1638	170	080978	2.74	64.2	7.2
1639	170	081378	2.96	33.0	4.0
1640	170	081678	2.59	29.0	9.0
1641	170	082078	2.66	167.0	7.0
1642	170	082378	2.98	32.0	4.0
1643	170	082778	2.66	76.6	3.8
1644	170	083078	3.58	53.6	0.6
1645	170	090378	2.51	102.6	2.4
1646	170	090678	2.64	91.0	9.0
1647	170	091078	3.02	104.2	5.6
1648	170	091378	3.64	58.8	14.6
1649	170	092078	2.64	34.0	8.0
1650	170	092178	2.88	28.0	7.0
1651	170	092478	2.75	72.0	11.0
1652	170	092778	2.62	65.4	7.2
1653	170	100178	2.62	107.0	20.0
1654	170	100478	2.83	26.0	6.0
1655	170	100878	3.05	84.0	17.0
1656	170	101178	2.66	168.0	5.0
1657	170	101578	2.86	95.0	8.0
1658	170	101878	3.35	20.0	5.0
1659	170	102278	2.76	115.0	19.0
1660	170	102578	2.90	31.0	5.0
1661	170	102978	3.19	27.0	1.0
1662	170	110178	2.33	71.0	13.0
1663	170	110578	2.33	19.2	2.0
1664	170	110878	2.33	127.0	20.0
1665	170	111278	2.62	31.6	12.4
1666	170	111578	2.98	147.2	11.6
1667	170	111978	2.40	21.0	6.0
1668	170	112278	2.04	143.0	7.4

POLL=OAG

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
1669	170	112678	2.50	38.0	13.0
1670	170	112978	2.54	67.0	11.0
1671	170	120378	2.86	75.6	10.2
1672	170	120678	2.82	64.0	6.4
1673	170	121078	3.32	85.1	10.0
1674	170	121378	2.73	89.8	21.8
1675	170	121778	3.01	104.0	9.0
1676	170	122078	2.55	95.0	5.0
1677	170	122478	2.45	180.0	6.0
1678	170	122778	3.02	88.0	6.0
1679	170	123178	3.29	.	11.0
1680	170	010379	3.00	109.0	17.0
1681	170	010779	3.00	176.0	10.0
1682	170	011079	3.00	187.0	13.0
1683	170	011479	3.00	43.0	10.0
1684	170	011779	3.00	40.0	7.0
1685	170	012179	3.20	52.0	4.0
1686	170	012479	2.71	123.0	15.0
1687	170	012879	2.72	109.0	28.0
1688	170	013179	2.89	32.0	7.0
1689	170	020479	3.13	65.0	8.0
1690	170	020779	2.86	92.0	4.6
1691	170	021179	2.72	140.0	12.0
1692	170	021479	3.50	58.0	10.0
1693	170	021879	2.32	276.0	12.0
1694	170	022179	3.28	246.0	.
1695	170	022579	3.43	110.0	25.0
1696	170	022879	3.47	66.0	16.0
1697	170	030479	2.60	43.0	13.0
1698	170	030779	2.53	94.0	15.3
1699	170	031179	1.75	54.0	18.0
1700	170	031579	2.22	70.0	17.0
1701	170	031879	2.32	94.0	26.0
1702	170	032179	1.74	70.0	18.0
1703	170	032579	3.05	95.0	29.0
1704	170	032879	2.42	146.0	35.0
1705	170	040179	3.12	116.0	14.0
1706	170	040479	1.34	73.0	12.0
1707	170	040879	2.04	62.0	6.0
1708	170	041179	2.78	71.0	4.0
1709	170	041579	2.54	326.0	8.0
1710	170	041879	2.50	137.0	3.0
1711	170	042279	2.50	56.0	5.0
1712	170	042579	2.48	85.0	6.0
1713	170	042979	2.27	40.0	8.0
1714	170	050279	2.53	231.0	14.0
1715	170	050679	2.08	80.0	20.0
1716	170	050979	2.03	75.0	18.0
1717	170	051379	3.48	51.8	23.0
1718	170	051679	2.52	81.9	6.8
1719	170	052079	2.66	71.0	11.0
1720	170	052379	2.94	56.0	8.0
1721	170	052779	2.63	70.0	12.0
1722	170	053079	2.68	52.0	3.2

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---------------------------------------------------------- POLL=OAG ----------------------------------------------------------------------

 OBS      PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

 1723      170      060379       2.74             78.6              17.8
 1724      170      060679       2.21             39.0              17.0
 1725      170      061079       2.96            163.0              24.0
 1726      170      061379       2.30            409.0              39.0
 1727      170      061779       3.90            202.0              28.0
 1728      170      062079       2.99             56.4               3.2
 1729      170      062479       2.90            106.0               8.0
 1730      170      062779       2.57            200.0              10.6
 1731      170      070179       3.22             56.0              19.6
 1732      170      070479       3.64             46.0              11.0
 1733      170      070879       1.97             56.0               9.0
 1734      170      071179       2.90             54.0              16.0
 1735      170      071579       2.51             49.0               2.0
 1736      170      071879       3.36             61.0              10.0
 1737      170      072279       3.00             42.0              13.0
 1738      170      072579       3.01             82.0              11.0
 1739      170      072979       3.32             42.0              12.0
 1740      170      080179       3.32            139.8              21.2
 1741      170      080579       2.90             86.4               5.4
 1742      170      080879       2.30             98.0               5.2
 1743      170      081279       2.83             58.2              14.6
 1744      170      081579       2.57             20.8               2.8
 1745      170      081979       3.70             40.0               7.0
 1746      170      082279       3.44             56.0              16.0
 1747      170      082679       2.78             95.0              18.0
 1748      170      082979       3.71             55.0              17.8
 1749      170      090279       3.19             47.2               6.2
 1750      170      090579       3.19             28.6               5.8
 1751      170      090979       3.05             56.8              18.6
 1752      170      091279       3.10             50.2              10.6
 1753      170      091679       3.05             79.4               8.8
 1754      170      091979       3.05            111.0              10.2
 1755      170      092379       3.57             95.6              11.2
 1756      170      092679       2.64             85.8              15.4
 1757      170      093079       3.05             68.2              14.2
 1758      170      100379       3.77             25.0               7.6
 1759      170      100779       3.37             67.0              11.0
 1760      170      101079       3.36             37.0               9.0
 1761      170      101479       2.90             22.0              10.0
 1762      170      101779       2.90             42.6              13.0
 1763      170      102379       2.86             29.4               8.2
 1764      170      102579       2.78             21.2               1.4
 1765      170      103079       3.05             90.8               1.2
 1766      170      110179       2.38             32.0               8.0
 1767      170      110679       3.07            149.4              10.8
 1768      170      110879       2.40            168.0              10.4
 1769      170      111379       3.41             26.0               6.0
 1770      170      111579       2.90             52.0               3.0
 1771      170      112079       2.86             32.0               2.0
 1772      170      112279       2.93             44.0               4.2
 1773      170      112779       2.89             96.0               9.0
 1774      170      112979       2.79            194.0              10.2
 1775      170      120479       3.17            150.0              18.0
 1776      170      120679       3.19                               22.0
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------------------------------------------------ POLL=OAG ----------------------------------------------------------------

      OBS     PLANT     DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

      1777     170     121179       3.23           257.0             18.0
      1778     170     121379       3.48             .               22.0
      1779     170     121879       2.63           126.0              7.4
      1780     170     122079       2.83            66.0             13.0
      1781     170     122579       3.43            80.6             23.4
      1782     170     122779       2.86            34.0             10.0
      1783     170     010180       3.38            18.2               .
      1784     170     010380       2.90           108.0               .
      1785     170     010880       3.05            30.0               .
      1786     170     011080       3.19           101.0               .
      1787     170     011680       3.31            75.0               .
      1788     170     011780       3.31            90.0               .
      1789     170     012280       2.90            26.0               .
      1790     170     012480       2.62            92.0               .
      1791     170     012980       3.01            96.0               .
      1792     170     013180       3.25            26.0               .
      1793     170     020580       3.14            62.0               .
      1794     170     021280       3.19           160.0               .
      1795     170     021480       2.95            29.4               .
      1796     170     021980       2.84            50.0               .
      1797     170     022280       3.20            87.0               .
      1798     170     022680       2.97            88.0               .
      1799     170     022880       3.04            86.0               .
      1800     170     030480       3.29            84.0               .
      1801     170     030680       3.46            96.0               .
      1802     170     031180       2.94           105.0               .
      1803     170     031380       3.42            52.0               .
      1804     170     031880       3.50            68.0               .
      1805     170     032080       3.78            67.6               .
      1806     170     032580       3.45            34.0               .
      1807     170     032780       1.96            25.0               .
      1808     170     040180       3.40            82.6               .
      1809     170     040380       3.37            64.2               .
      1810     170     040880       3.66            37.4               .
      1811     170     041680       2.90            18.0               .
      1812     170     041780       3.05            30.2               .
      1813     170     042280       3.31            49.0               .
      1814     170     042480       2.10            54.0               .
      1815     170     042980       2.70            94.2               .
      1816     170     050180       2.33            51.4               .
      1817     170     050680       2.47            20.0               .
      1818     170     050980       2.33            61.0               .
      1819     170     051380       2.16            22.2               .
      1820     170     051580       2.09            62.0               .
      1821     170     052080       2.94            28.0               .
      1822     170     052280       2.25            27.0               .
      1823     170     052780       2.00           108.0               .
      1824     170     052980       2.18            94.0               .
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---------------------------------------------- POLL=TSS -----------------------------------------------------------------

        OBS      PLANT       DATE       FLOW(MGD)      INFLUENT(PPM)      EFFLUENT(PPM)

        1825       9        101575        0.05              36                31.0
        1826       9        102275        0.05              28                21.0
        1827       9        111275        0.25              41                47.0
        1828       9        111975        0.07              14                45.0
        1829       9        121075        0.06              22                 6.0
        1830       9        121775        0.06               4                13.0
        1831       9        010776        0.10              13                13.0
        1832       9        011476         .                50                52.0
        1833       9        021176        0.07              31                20.0
        1834       9        021876         .                50                16.0
        1835       9        031076        0.08              25                41.0
        1838       9        032576         .                49                53.0
        1837       9        041476        0.06              19                20.0
        1838       9        042176         .                49                47.0
        1839       9        051276        0.09              27                17.0
        1840       9        051976         .                20                50.0
        1841       9        060976        0.13              57                41.2
        1842       9        061676        0.13              12                17.0
        1843       9        072176        0.07              14                15.0
        1844       9        072876        0.09              20                40.0
        1845       9        080476        0.05              11                40.0
        1846       9        081876        0.06              48                17.0
        1847       9        090876        0.02              10                17.0
        1848       9        092276         .                 4                19.0
        1849      44        060179        0.92              88                 3.0
        1850      44        060479        0.88             224                10.0
        1851      44        060579        1.00             268                 9.0
        1852      44        060679        0.80             306                20.0
        1853      44        060779        0.38             212                 6.0
        1854      44        060879        0.83             512                20.0
        1855      44        061179        0.94              18                11.0
        1856      44        061279        0.79             138                33.0
        1857      44        061379        0.80            3944                47.0
        1858      44        061479        1.13            1234                18.0
        1659      44        061579        0.45             508                22.0
        1860      44        061879        0.57             760                10.0
        1861      44        061979        0.71            1016                82.0
        1862      44        062079        0.39               .                33.0
        1863      44        062179        0.57               .                 8.0
        1864      44        062279        0.36               .                16.0
        1865      44        062579        0.83               .                 5.0
        1866      44        062679        0.68               .                21.0
        1867      44        062779        0.60               .                 4.0
        1868      44        062879        0.62               .                 9.0
        1869      44        062979        0.80               .                 5.0
        1870      44        070279        0.81             176                17.0
        1871      44        070379        0.63              82                11.0
        1872      44        070479        0.51             896                17.0
        1873      44        070579        0.25             450                16.0
        1874      44        070679        0.34             602                30.0
        1875      44        070979        0.79             182                 4.0
        1876      44        071079        0.71             300                 7.0
        1877      44        071179        0.73             138                11.0
        1878      44        071279        0.74             390                 8.0
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POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
1879	44	071379	0.80	830	5
1880	44	071679	0.74	342	4
1881	44	071779	0.79	5478	1
1882	44	071879	0.73	10050	7
1883	44	071979	0.73	15150	10
1884	44	072079	0.90	11900	4
1885	44	072379	0.54	410	4
1886	44	072479	0.69	662	13
1887	44	072579	0.73	1078	9
1888	44	072679	0.81	15400	19
1889	44	072779	0.71	10300	17
1890	44	073079	0.79	17660	5
1891	44	073179	0.43	314	5
1892	44	080179	0.38	508	5
1893	44	080279	0.46	690	18
1894	44	080379	0.66	1258	3
1895	44	080679	0.74	792	4
1896	44	080779	0.26	272	7
1897	44	080879	0.56	248	28
1898	44	080979	0.73	1440	2
1899	44	081079	0.75	2084	13
1900	44	081379	0.74	1176	2
1901	44	081479	0.65	2502	6
1902	44	081579	0.79	20700	2
1903	44	081679	0.73	17160	3
1904	44	081779	0.84	20700	2
1905	44	082079	0.83	17380	11
1906	44	082179	0.85	21270	8
1907	44	082279	0.73	11000	16
1908	44	082379	0.67	706	8
1909	44	082479	0.94	1846	13
1910	44	082779	0.96	9000	10
1911	44	082879	0.96	69600	14
1912	44	082979	0.91	2160	11
1913	44	083079	0.90	7320	54
1914	44	083179	.	.	10
1915	44	090379	0.19	3320	2
1916	44	090479	0.34	8212	3
1917	44	090579	0.28	3980	2
1918	44	090679	0.39	2580	1
1919	44	090779	0.33	1052	2
1920	44	091079	0.62	430	5
1921	44	091179	0.70	7140	2
1922	44	091279	0.67	10560	1
1923	44	091379	0.72	18940	2
1924	44	091479	0.85	18820	2
1925	44	091779	0.88	13380	25
1926	44	091879	0.88	2860	83
1927	44	091979	0.48	1900	10
1928	44	092079	0.33	1080	6
1929	44	092179	0.43	3240	14
1930	44	092479	0.31	2900	3
1931	44	092579	0.27	16100	5
1932	44	092679	0.37	4020	2

POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
1933	44	092779	0.36	11440	65
1934	44	092879	0.35	19280	95
1935	44	100179	0.55	4120	20
1936	44	100279	0.57	3300	24
1937	44	100379	0.45	182	34
1938	44	100479	0.36	204	37
1939	44	100579	0.57	680	4
1940	44	100879	0.96	5420	6
1941	44	100979	0.46	360	13
1942	44	101079	0.64	5280	19
1943	44	101179	0.70	1920	9
1944	44	101279	0.68	4940	16
1945	44	101579	0.23	10540	11
1946	44	101679	0.67	9800	15
1947	44	101779	0.67	12120	33
1948	44	101879	0.60	6200	16
1949	44	101979	0.62	12740	35
1950	44	102279	0.60	13500	16
1951	44	102379	0.68	20440	18
1952	44	102479	0.69	14960	20
1953	44	102579	0.60	1700	38
1954	44	102679	0.59	560	34
1955	44	102979	0.60	7360	25
1956	44	103079	0.67	16060	6
1957	44	103179	0.10	1380	28
1958	44	110179	0.52	640	18
1959	44	110279	0.72	1180	9
1960	44	110579	0.58	2640	16
1961	44	110679	0.59	1780	2
1962	44	110779	0.68	3520	12
1963	44	110879	0.68	2640	22
1964	44	110979	0.53	580	4
1965	44	111279	0.66	2460	7
1966	44	111379	0.98	5640	24
1967	44	111479	0.65	8160	22
1968	44	111579	0.51	340	26
1969	44	111679	0.51	760	4
1970	44	111979	0.72	1260	21
1971	44	112079	0.78	2560	9
1972	44	112179	0.78	2100	4
1973	44	112279	0.35	560	4
1974	44	112379	0.11	640	3
1975	44	112679	0.58	2620	1
1976	44	112779	0.78	1750	12
1977	44	112879	0.69	1185	1
1978	44	112979	0.70	1480	5
1979	44	113079	0.73	2620	2
1980	44	120379	0.74	2300	2
1981	44	120479	0.55	4360	5
1982	44	120579	0.60	2060	1
1983	44	120679	0.66	240	4
1984	44	120779	0.70	920	2
1985	44	121079	1.12	2080	1
1986	44	121179	0.63	1360	1

POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
1987	44	121279	0.79	1240	4
1988	44	121379	0.60	3760	1
1989	44	121479	0.63	5080	9
1990	44	121779	0.61	1000	2
1991	44	121879	0.58	1480	4
1992	44	121979	0.57	378	2
1993	44	122079	0.52	880	4
1994	44	122179	0.65	3880	1
1995	44	122479	0.36	100	2
1996	44	122579	0.47	940	5
1997	44	122679	0.41	720	5
1998	44	122779	0.30	380	6
1999	44	122879	0.41	400	8
2000	44	123179	0.63	.	12
2001	44	010180	0.53	1600	3
2002	44	010280	0.15	670	16
2003	44	010380	0.59	920	6
2004	44	010480	0.50	154	7
2005	44	010780	0.67	150	680
2006	44	010880	0.63	180	18
2007	44	010980	0.65	790	6
2008	44	011080	0.47	1255	4
2009	44	011180	0.69	744	14
2010	44	011480	0.32	160	7
2011	44	011580	0.60	360	6
2012	44	011680	0.76	480	2
2013	44	011780	0.74	720	6
2014	44	011880	0.56	1040	7
2015	44	012180	0.62	1440	4
2016	44	012280	0.60	940	3
2017	44	012380	0.65	280	25
2018	44	012480	0.53	220	2
2019	44	012580	0.61	280	2
2020	44	012880	0.56	260	2
2021	44	012980	0.48	186	11
2022	44	013080	0.43	340	2
2023	44	013180	0.54	160	1
2024	44	020180	0.67	100	2
2025	44	020480	0.87	90	17
2026	44	020580	0.55	122	4
2027	44	020680	0.49	55740	7
2028	44	020780	0.45	13400	2
2029	44	020880	0.34	1280	41
2030	44	021180	0.69	340	15
2031	44	021280	0.25	34100	3
2032	44	021380	0.51	80	2
2033	44	021480	0.63	180	3
2034	44	021580	0.57	260	4
2035	44	021880	0.47	13300	3
2036	44	021980	0.65	380	2
2037	44	022080	0.63	2780	2
2038	44	022180	0.74	3340	6
2039	44	022280	0.71	3520	65
2040	44	022580	0.89	3920	7

POLL=133

OBS	PLANT	DATE	FLOW(MCD)	INFLUENT(PPM)	EFFLUENT(PPM)
2041	44	022680	0.85	1840	10
2042	44	022780	0.78	5500	2
2043	44	022880	0.58	4320	6
2044	44	030380	0.44	1920	7
2045	44	030480	0.50	8080	7
2046	44	030580	0.57	120	2
2047	44	030680	0.61	15060	3
2048	44	030780	1.04	2440	4
2049	44	031080	0.79	1080	9
2050	44	031180	0.64	340	2
2051	44	031280	0.63	820	2
2052	44	031380	0.82	140	2
2053	44	031480	0.80	1060	2
2054	44	031780	0.91	2940	2
2055	44	031880	0.86	620	6
2056	44	031980	0.82	760	8
2057	44	032080	1.00	100	5
2058	44	032180	0.97	7064	3
2059	44	032480	0.62	3560	3
2060	44	032580	0.78	1480	15
2061	44	032680	0.75	2280	7
2062	44	032780	0.71	1860	5
2063	44	032880	0.82	3604	3
2064	44	033180	0.73	.	4
2065	44	040180	0.81	86	10
2066	44	040280	0.82	4640	2
2067	44	040380	0.56	800	7
2068	44	040480	0.21	460	2
2069	44	040780	0.64	1460	2
2070	44	040880	0.90	4780	11
2071	44	040980	0.71	1780	5
2072	44	041080	0.92	1340	2
2073	44	041180	0.93	1260	2
2074	44	041480	0.95	780	3
2075	44	041580	0.70	280	2
2076	44	041680	0.74	580	2
2077	44	041780	0.87	280	2
2078	44	041860	0.86	780	2
2079	44	042180	0.76	420	5
2080	44	042280	0.55	160	2
2081	44	042380	0.73	500	2
2082	44	042480	0.73	460	2
2083	44	042580	0.59	740	2
2084	44	042880	0.62	680	7
2085	44	042980	0.60	600	2
2086	44	043080	0.62	380	4
2087	44	050180	0.70	500	2
2088	44	050280	0.67	460	2
2089	44	050580	0.87	1460	2
2090	44	050680	0.96	940	2
2091	44	050780	0.87	260	10
2092	44	050880	0.32	240	18
2093	44	050980	0.60	80	9
2094	44	051280	0.72	420	10

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------------------------------------------------ POLL=TSS ------------------------------------------------

   OBS     PLANT     DATE     FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

   2095     44      051380      0.80           120                4
   2096     44      051480      0.64           440                5
   2097     44      051580      0.35           520               10
   2098     44      051680      0.60           720                7
   2099     44      051980      0.50           350                3
   2100     44      052080      0.25            80                2
   2101     44      052180      0.11            30               12
   2102     44      052280      0.57            20              320
   2103     44      052380      0.44           310               25
   2104     44      052680      0.30           310               10
   2105     44      052780      0.48            60                2
   2106     44      052880      0.54            30                2
   2107     44      052980       .              20               44
   2108     44      053080       .              40               59
   2109     45      070279      2.17            12                2
   2110     45      070379      1.73             6                4
   2111     45      070479      1.46            26               22
   2112     45      070579      2.13            26               10
   2113     45      070679      1.90             .               12
   2114     45      070779      2.11             .               10
   2115     45      070879      2.24            14               16
   2116     45      070979      2.26            90               64
   2117     45      071079      2.33           306               54
   2118     45      071179      2.84           110               26
   2119     45      071279      2.95           136               46
   2120     45      071379      3.26             .               10
   2121     45      071479      3.43             .                6
   2122     45      071579      2.49            44               12
   2123     45      071679      2.47            22                8
   2124     45      071779      2.07            66               10
   2125     45      071879      2.43            40               10
   2126     45      071979      2.70            38                8
   2127     45      072079      2.55             .                4
   2128     45      072179      2.48             .               10
   2129     45      072279      2.45            60                6
   2130     45      072379      3.28             6               10
   2131     45      072479      3.43            20               16
   2132     45      072579      3.17           522               22
   2133     45      072679      3.26           980               10
   2134     45      072779      3.24             .                4
   2135     45      072879      3.07             .                4
   2136     45      072979      3.20            94                6
   2137     45      073079      3.20            62               10
   2138     45      073179      3.12           496                6
   2139     45      080179      3.03           104                4
   2140     45      080279      2.87           534                6
   2141     45      080379      2.97             .                6
   2142     45      080479      3.18             .                6
   2143     45      080579      2.98           446                4
   2144     45      080679      3.10           320                4
   2145     45      060779      2.94           556               30
   2146     45      080879      3.04           668                8
   2147     45      080979      2.48           618               10
   2148     45      081079      3.21             .               46
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----------- ---------------------------------------------- POLL=TSS ---------------------------------------------------------------------------

        OBS     PLANT     DATE     FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

        2149     45      081279      2.90            672               44
        2150     45      081379      2.66            480               42
        2151     45      081479      2.71            564               20
        2152     45      081579      2.56            398               14
        2153     45      081679      2.82            412                4
        2154     45      081779      2.73              .               20
        2155     45      081879      2.63              .                6
        2156     45      081979      2.52            494                2
        2157     45      082079      2.87            512               10
        2158     45      082179      3.41            482                4
        2159     45      082279      3.62            552               10
        2160     45      082379      3.56            398                8
        2161     45      082479      3.58              .                8
        2162     45      082579      3.29              .               12
        2163     45      082679      2.55             64                8
        2164     45      082779      3.01             36               10
        2165     45      082879      2.63             80                4
        2166     45      082979      2.56             82                6
        2167     45      083079      3.40            128               18
        2168     45      083179      2.72              .               20
        2169     45      090179      2.21              .               14
        2170     45      090279      2.00             86               16
        2171     45      090379      0.63           1118                6
        2172     45      090479      1.61             72               18
        2173     45      090579      2.21             74                8
        2174     45      090679      2.86             52                4
        2175     45      090779      2.82              .               30
        2176     45      090879      2.34              .               46
        2177     45      090979      1.88            202               20
        2178     45      091079      2.39            224                6
        2179     45      091179      2.44             48                4
        2180     45      091279      1.92             48               14
        2181     45      091379      1.85             68                4
        2182     45      091479      1.98              .               28
        2183     45      091579      2.40              .               32
        2184     45      091679      2.44             82               40
        2185     45      091779      2.37             44               10
        2186     45      091879      2.39             26                4
        2187     45      091979      1.86             24                6
        2188     45      092079      3.04             74                2
        2189     45      092179      2.91              .               12
        2190     45      092279      3.06              .               14
        2191     45      092379      2.73            220               10
        2192     45      092479      2.52             56               12
        2193     45      092579      2.85             72               14
        2194     45      092679      2.77             70                4
        2195     45      092779      2.52             44               10
        2196     45      092879      2.45              .               24
        2197     45      092979      2.60              .               14
        2198     45      093079      2.49             36               22
        2199     45      100179      2.32             54               14
        2200     45      100279      2.24             92               28
        2201     45      100379      2.27             62                8
        2202     45      100479      2.66             12                6
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------------------------------------------------------------ POLL=TSS ------------------------------------------------------------

OBS     PLANT     DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

2203     45      100579       2.44             .               72
2204     45      100679       2.19             .               66
2205     45      100779       2.01           128               48
2206     45      100879       1.90            70               40
2207     45      100979       2.18            48               44
2208     45      101079       2.52            28               18
2209     45      101179       2.18            66                6
2210     45      101279       1.96             .                6
2211     45      101379       1.70             .                6
2212     45      101479       1.65            60                8
2213     45      101579       1.46           298               10
2214     45      101679       2.10           350               34
2215     45      101779       1.95           130               18
2216     45      101879       1.42           500                8
2217     45      101979       1.46             .               42
2218     45      102079       1.59             .               38
2219     45      102179       1.57           274               28
2220     45      102279       1.61           284               32
2221     45      102379       2.26           278                2
2222     45      102479       1.22           206                2
2223     45      102579       1.55           264                2
2224     45      102679       1.50             .               22
2225     45      102779       1.20             .               12
2226     45      102879       0.84           204               16
2227     45      102979       1.15           446                6
2228     45      103079       2.26           234               10
2229     45      103179       1.86           110                4
2230     45      110179       1.56            74               18
2231     45      110279       1.57             .                4
2232     45      110379       1.31             .                8
2233     45      110479       0.70           280                6
2234     45      110579       0.92           108                6
2235     45      110679       1.59           132               24
2236     45      110779       1.57           492               46
2237     45      110879       1.73           122               10
2238     45      110979       1.78             .               12
2239     45      111079       1.68             .                6
2240     45      111179       1.40            18               10
2241     45      111279       2.35           146               26
2242     45      111379       2.17            76                4
2243     45      111479       1.41           216               12
2244     45      111579       1.19           142               30
2245     45      111679       2.02             .               10
2246     45      111779       2.03             .               18
2247     45      111879       1.55           470               12
2248     45      111979       1.19            72               22
2249     45      112079       1.65            76               18
2250     45      112179       1.49             .                8
2251     45      112279       0.96            82               10
2252     45      112379       0.93             .               36
2253     45      112479       2.06             .               28
2254     45      112579       2.11            74               26
2255     45      112679       1.30            70               54
2256     45      112779       1.36            52               30
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---------------------------------------------------- POL =TSS ----------------------------------------------------

OBS     PLANT     DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

2257     45      112879       1.48            64               14
2258     45      112979       2.01            76               10
2259     45      113079       1.93             .               14
2260     45      120179       1.77             .               10
2261     45      120279       1.63             6                6
2262     45      120379       1.56           322                6
2263     45      120479       1.36           318               20
2264     45      120579       1.98           304               36
2265     45      120679       1.54           190                6
2266     45      120779       1.80             .               28
2267     45      120879       1.65             .               18
2268     45      120979       1.37           214               10
2269     45      121079       2.14           138                2
2270     45      121179       2.12           180                4
2271     45      121279       2.03           534                6
2272     45      121379       2.21           208               16
2273     45      121479       2.23             .               34
2274     45      121579       1.73             .               22
2275     45      121679       1.80           312               26
2276     45      121779       1.78           436               14
2277     45      121879       2.09           198               22
2278     45      121979       2.20           226                4
2279     45      122079       2.22            22               14
2280     45      122179       1.95             .               16
2281     45      122279       1.52             .               12
2282     45      122379       1.55           214                8
2283     45      122479       0.88             .               14
2284     45      122579       1.04            50               34
2285     45      122679       1.65           266               24
2286     45      122779       2.09           238                2
2287     45      122879       1.93             .               46
2288     45      122979       1.70             .               46
2289     45      123079       1.24           318               42
2290     45      123179       0.35             .                4
2291     45      010180       0.74           604                4
2292     45      010280       2.06           166               18
2293     45      010380       1.93           300                4
2294     45      010480       1.57             .                2
2295     45      010580       1.43             .                2
2296     45      010680       1.62            88                4
2297     45      010780       1.79            52                2
2298     45      010880       1.61           554                4
2299     45      010980       1.74           132                4
2300     45      011080       1.60           432                2
2301     45      011180       1.72             .                6
2302     45      011280       1.82             .                2
2303     45      011380       1.80            24                4
2304     45      011480       1.60            22                2
2305     45      011580       1.59             2                4
2306     45      011680       1.55           458                2
2307     45      011780       1.53           128                6
2308     45      011880       1.87             .               32
2309     45      011980       1.39             .               28
2310     45      012080       1.35           708               18
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---------------------------------------------- POL=TSS ----------------------------------------------

OBS     PLANT     DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

2311     45      012180       1.59            416                28
2312     45      012280       1.72             90                42
2313     45      012380       1.91             74                10
2314     45      012480       1.47            164                 2
2315     45      012580       1.67              .                 4
2316     45      012680       1.55              .                 2
2317     45      012780       1.53            356                 2
2318     45      012880       1.66            182                 2
2319     45      012980       1.80            190                 2
2320     45      013080       1.66            250                28
2321     45      013180       1.64            426                48
2322     45      020180       1.95              .                26
2323     45      020280       1.40              .                14
2324     45      020380       1.69            594                26
2325     45      020480       1.98           1336                 2
2326     45      020580       1.64            472                46
2327     45      020680       1.48            482                 2
2328     45      020780       1.98            504                 2
2329     45      020880       1.90              .                 6
2330     45      020980       2.02              .                 2
2331     45      021080       1.80            260                 2
2332     45      021180       1.68            380                 2
2333     45      021280       2.02            206                 4
2334     45      021380       2.15             20                 4
2335     45      021480       1.92             50                 6
2336     45      021580       1.70              .                 6
2337     45      021680       2.36              .                 4
2338     45      021780       2.25            456                 4
2339     45      021880       1.36            422                10
2340     45      021980       1.93             74                18
2341     45      022080       2.13            256                 8
2342     45      022180       1.66            294                 8
2343     45      022280       1.28              .                28
2344     45      022380       1.88              .                14
2345     45      022480       1.57            262                 2
2346     45      022580       2.02            392                 8
2347     45      022680       1.40            398                50
2348     45      022780       1.70            422                74
2349     45      022880       1.00            256                28
2350     45      022980       1.51              .                36
2351     45      030180       1.80              .                62
2352     45      030280       1.61            404                24
2353     45      030380       2.23            432                 6
2354     45      030480       1.57            420                14
2355     45      030580       1.72            346                32
2356     45      030680       1.55            326                42
2357     45      030780       2.49              .                20
2358     45      030880       2.21              .                 4
2359     45      030980       1.60             28                 6
2360     45      031080       1.88            300                56
2361     45      031180       2.58           2692                20
2362     45      031280       2.20             22                 6
2363     45      031380       2.05            102                42
2364     45      031480       2.63              .                16
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POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
2365	45	031580	2.48	.	8
2366	45	031680	2.18	256	8
2367	45	031780	1.53	320	2
2368	45	031880	2.03	62	18
2369	45	031980	2.23	232	14
2370	45	032080	2.40	60	26
2371	45	032180	2.51	.	2
2372	45	032280	2.08	.	4
2373	45	032380	2.23	358	2
2374	45	032480	1.55	372	2
2375	45	032580	1.55	296	58
2376	45	032680	1.68	72	2
2377	45	032780	1.67	516	32
2378	45	032880	2.18	.	22
2379	45	032980	2.52	.	22
2380	45	033080	2.17	10	14
2381	45	033180	2.00	200	10
2382	45	040180	2.07	16	4
2383	45	040280	1.54	134	48
2384	45	040380	1.53	60	36
2385	45	040480	0.41	.	40
2386	45	040580	0.60	.	38
2387	45	040680	2.33	162	30
2388	45	040790	1.76	272	2
2389	45	040880	1.85	124	36
2390	45	040980	1.86	46	8
2391	45	041090	1.83	152	18
2392	45	041180	1.77	.	24
2393	45	041280	1.77	.	30
2394	45	041380	2.04	122	14
2395	45	041480	2.08	90	12
2396	45	041580	1.67	152	94
2397	45	041680	2.80	80	8
2398	45	041780	2.51	152	18
2399	45	041880	1.82	.	24
2400	45	041980	1.50	.	34
2401	45	042080	1.70	70	44
2402	45	042180	1.99	62	42
2403	45	042280	2.01	866	4
2404	45	042380	1.93	12	2
2405	45	042480	1.44	70	6
2406	45	042580	1.43	.	24
2407	45	042680	1.42	.	18
2408	45	042780	1.48	254	20
2409	45	042880	1.45	550	2
2410	45	042980	1.76	100	20
2411	45	043080	2.05	102	48
2412	45	050180	1.72	480	4
2413	45	050280	1.41	.	2
2414	45	050380	1.89	.	2
2415	45	050480	2.29	346	4
2416	45	050580	1.60	46	14
2417	45	050680	1.91	40	2
2418	45	050780	2.30	32	2

POL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
2419	45	050880	2.14	94	18
2420	45	050980	1.42	.	4
2421	45	051080	1.32	.	2
2422	45	051180	1.25	56	2
2423	45	051280	1.66	120	2
2424	45	051380	1.88	452	72
2425	45	051480	1.93	76	38
2426	45	051580	1.53	748	48
2427	45	051680	1.66	.	6
2428	45	051780	1.79	.	2
2429	45	051880	1.60	988	4
2430	45	051980	1.22	282	56
2431	45	052080	1.23	700	54
2432	45	052180	1.17	336	2
2433	45	052280	0.87	558	20
2434	45	052380	1.26	.	18
2435	45	052480	1.61	.	10
2436	45	052580	1.13	.	18
2437	45	052660	0.85	688	112
2438	45	052780	1.30	2334	72
2439	45	052880	1.67	3758	36
2440	45	052980	0.99	930	4
2441	45	053080	1.05	.	2
2442	45	053160	1.15	.	6
2443	45	060180	1.32	590	12
2444	45	060280	1.11	278	8
2445	45	060380	1.01	378	22
2446	45	060480	0.93	1076	56
2447	45	060580	0.90	530	14
2448	45	060680	1.02	.	2
2449	45	060780	1.45	.	4
2450	45	060880	1.20	2692	6
2451	45	060980	1.24	898	72
2452	45	061080	1.45	1014	58
2453	45	061180	1.48	794	32
2454	45	061280	1.66	234	10
2455	45	061380	1.17	.	4
2456	45	061480	1.35	.	10
2457	45	061580	1.40	302	12
2458	45	061680	1.36	666	84
2459	45	061780	1.34	140	50
2460	45	061880	1.41	510	48
2461	45	061980	1.45	680	82
2462	45	062080	1.48	.	24
2463	45	062180	1.82	.	26
2464	45	062280	1.70	447	24
2465	45	062380	1.49	86	8
2466	45	062480	1.26	124	2
2467	45	062580	1.21	366	2
2468	45	062680	1.64	902	6
2469	45	062780	2.19	.	38
2470	45	062880	1.91	.	42
2471	45	062980	1.68	598	26
2472	45	063080	1.53	720	2

POL.=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
2527	96	082776	2.70	.	16
2528	96	083076	2.60	.	3
2529	96	090176	2.60	.	10
2530	96	090276	2.60	.	8
2531	96	090776	1.60	.	14
2532	96	091376	2.20	.	18
2533	96	091476	2.30	.	21
2534	96	091676	2.60	.	16
2535	96	092076	2.50	.	19
2536	96	092276	2.30	.	17
2537	96	092876	2.60	.	11
2538	96	092976	2.40	.	19
2539	111	010177	1.01	.	10
2540	111	010277	0.90	.	3
2541	111	010377	1.05	.	7
2542	111	010477	0.83	70	30
2543	111	010577	0.96	90	20
2544	111	010677	0.93	100	6
2545	111	010777	0.93	.	7
2546	111	010877	0.93	.	3
2547	111	010977	0.99	.	19
2548	111	011077	0.90	.	5
2549	111	011177	0.91	80	5
2550	111	011477	1.16	.	2
2551	111	011577	0.93	.	17
2552	111	011677	1.10	.	14
2553	111	011777	1.11	.	3
2554	111	011877	0.78	40	3
2555	111	011977	0.98	70	45
2556	111	012077	0.65	80	7
2557	111	012177	1.08	.	16
2558	111	012277	1.06	.	17
2559	111	012377	1.12	.	24
2560	111	012577	0.84	60	8
2561	111	012677	0.99	50	11
2562	111	012777	0.98	70	9
2563	111	012877	1.08	.	6
2564	111	012977	0.96	.	10
2565	111	013077	0.97	.	12
2566	111	013177	0.97	.	3
2567	111	020177	0.69	65	3
2568	111	020277	0.61	75	7
2569	111	020377	0.73	70	9
2570	111	020477	0.59	.	3
2571	111	020577	1.09	.	9
2572	111	020677	1.14	.	9
2573	111	020777	1.13	.	15
2574	111	020977	0.99	52	16
2575	111	021077	0.96	55	7
2576	111	021177	0.77	.	20
2577	111	021277	0.73	.	35
2578	111	021377	0.82	.	25
2579	111	021477	0.78	.	38
2580	111	021577	0.92	40	6

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------------------------------------------------------- POLL=TSS --------------------------------------------------------

        OBS     PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

        2473     96       100875        3.2             .                28
        2474     96       101375        3.2             .                46
        2475     96       102775        3.2             .                43
        2476     96       110375        3.3             .                18
        2477     96       111075        3.3             .                15
        2478     96       111475        3.1             .                 3
        2479     96       111875        3.4             .                 4
        2480     96       112575        3.4             .                 2
        2481     96       120275        3.4             .                18
        2482     96       120475        3.3             .                12
        2483     96       120775        3.4             .                 7
        2484     96       120875        3.4             .                 9
        2485     96       121275        3.0             .                17
        2486     96       121575        3.0             .                33
        2487     96       121675        3.0             .                16
        2488     96       121875        3.1             .                 9
        2489     96       122275        3.3             .                 9
        2490     96       122975        3.5             .                19
        2491     96       010776        3.4             .                 8
        2492     96       010976        3.4             .                12
        2493     96       012076        3.4             .                10
        2494     96       020576        3.3             .                15
        2495     96       022476        3.4             .                 8
        2496     96       030276        3.5             .                13
        2497     96       030976        3.2             .                 4
        2498     96       031176        3.1             .                10
        2499     96       032676        3.2             .                 6
        2500     96       040576        3.4             .                 5
        2501     96       041276        3.0             .                 3
        2502     96       041976        3.5             .                11
        2503     96       042376        3.1             .                20
        2504     96       050476        3.1             .                11
        2505     96       051376        3.0             .                 8
        2506     96       051976        3.1             .                 5
        2507     96       052576        3.1             .                12
        2508     96       060376        3.0             .                 6
        2509     96       060776        3.0             .                14
        2510     96       060976        3.1             .                 5
        2511     96       061576        3.1             .                 7
        2512     96       061876        3.0             .                10
        2513     96       062476        2.9             .                 9
        2514     96       062976        3.1             .                11
        2515     96       070876        3.0             .                 4
        2516     96       071276        3.0             .                10
        2517     96       071576        3.0             .                20
        2518     96       071976        3.0             .                14
        2519     96       072276        2.8             .                 7
        2520     96       072676        2.9             .                 6
        2521     96       072876        2.8             .                 6
        2522     96       080476        2.8             .                11
        2523     96       081276        3.1             .                 6
        2524     96       081676        3.1             .                 3
        2525     96       082376        2.7             .                 6
        2526     96       082676        2.8             .                11
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POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
2527	96	082776	2.70	.	16
2528	96	083076	2.60	.	3
2529	96	090176	2.60	.	10
2530	96	090276	2.60	.	8
2531	96	090776	1.60	.	14
2532	96	091376	2.20	.	18
2533	96	091476	2.30	.	21
2534	96	091676	2.60	.	16
2535	96	092076	2.50	.	19
2536	96	092276	2.30	.	17
2537	96	092876	2.60	.	11
2538	96	092976	2.40	.	19
2539	111	010177	1.01	.	10
2540	111	010277	0.90	.	3
2541	111	010377	1.05	.	7
2542	111	010477	0.83	70	30
2543	111	010577	0.96	90	20
2544	111	010677	0.93	100	6
2545	111	010777	0.93	.	7
2546	111	010877	0.93	.	3
2547	111	010977	0.99	.	19
2548	111	011077	0.90	.	5
2549	111	011177	0 91	80	5
2550	111	011477	1.16	.	2
2551	111	011577	0.93	.	17
2552	111	011677	1.10	.	14
2553	111	011777	1.11	.	3
2554	111	011877	0.78	40	3
2555	111	011977	0.98	70	45
2556	111	012077	0.65	80	7
2557	111	012177	1.08	.	16
2558	111	012277	1.06	.	17
2559	111	012377	1.12	.	24
2560	111	012577	0.84	60	8
2561	111	012677	0.99	50	11
2562	111	012777	0.98	70	9
2563	111	012877	1.08	.	6
2564	111	012977	0.98	.	10
2565	111	013077	0.97	.	12
2566	111	013177	0.97	.	3
2567	111	020177	0.69	65	3
2568	111	020277	0.61	75	7
2569	111	020377	0.73	70	9
2570	111	020477	0.59	.	3
2571	111	020577	1.09	.	9
2572	111	020677	1.14	.	9
2573	111	020777	1.13	.	15
2574	111	020977	0.99	52	16
2575	111	021077	0.96	55	7
2576	111	021177	0.77	.	20
2577	111	021277	0.73	.	35
2578	111	021377	0.82	.	25
2579	111	021477	0.78	.	38
2580	111	021577	0.92	40	6

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            OBS      PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

            2581      111      021677       0.69            45               8.0
            2582      111      021777       1.00            38              12.0
            2583      111      021877       0.88             .              20.0
            2584      111      021977       1.09             .              50.0
            2585      111      022077       0.87             .               3.0
            2586      111      022177       0.90             .               7.0
            2587      111      022277       0.74            45              18.0
            2588      111      022377       1.14            42              16.0
            2589      111      022477       1.08            50               6.0
            2590      111      022577       1.19             .               4.0
            2591      111      022677       1.06             .               5.0
            2592      111      022777       0.90             .               5.0
            2593      111      022877       0.82             .               5.0
            2594      111      030177       0.74            40               0.5
            2595      111      030277       0.68            43               5.0
            2596      111      030377       0.43            40              13.0
            2597      111      030577       0.99             .              16.0
            2598      111      030677       0.88             .               6.0
            2599      111      030777       0.85             .               5.0
            2600      111      030877       0.73            45               5.0
            2601      111      030977       0.57            40              12.0
            2602      111      031077       1.15            30               4.0
            2603      111      031177       1.33             .              14.0
            2604      111      031277       1.31             .               4.0
            2605      111      031377       1.29             .              16.0
            2606      111      031477       1.01             .               4.0
            2607      111      031577       1.37            20              10.0
            2608      111      031677       1.01            33              71.0
            2609      111      031777       1.18            35              19.0
            2610      111      031877       1.07             .               6.0
            2611      111      031977       1.25             .              19.0
            2612      111      032077       1.21             .              11.0
            2613      111      032177       1.19             .              14.0
            2614      111      032277       1.11            20               1.0
            2615      111      032377       1.06            18              13.0
            2616      111      032477       0.96            22               7.0
            2617      111      032577       0.95             .               7.0
            2618      111      032777       1.07             .               6.0
            2619      111      032877       1.15             .               5.0
            2620      111      032977       0.98            20              15.0
            2621      111      033077       0.80            30               2.0
            2622      111      033177       0.95            33               2.0
            2623      111      040177       0.93             .               8.0
            2624      111      040277       1.04             .               8.0
            2625      111      040377       1.13             .               9.0
            2626      111      040477       0.93            45               5.0
            2627      111      040577       1.15            35               9.0
            2628      111      040677       0.74            37               5.0
            2629      111      040777       1.34             .               8.0
            2630      111      040877       1.22             .               9.0
            2631      111      040977       1.28             .              17.0
            2632      111      041077       1.17             .              13.0
            2633      111      041177       1.23             .               5.0
            2634      111      041277       0.92            35               2.0
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----------------------------------------------------------- POLL=TSS -----------------------------------------------------------

OBS     PLANT     DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

2635     111     041377       1.10            31               36
2636     111     041477       0.87            34               16
2637     111     041577       1.06             .               15
2638     111     041677       1.03             .               12
2639     111     041777       0.90             .               13
2640     111     041877       1.04             .                5
2641     111     041977       0.45            16                8
2642     111     042077       0.94            27                5
2643     111     042177       1.02            36                7
2644     111     042277       0.87             .                9
2645     111     042377       0.96             .                2
2646     111     042477       0.80             .               16
2647     111     042577       0.69             .               16
2648     111     042677       0.83            29                5
2649     111     042777       0.96            30                4
2650     111     042877       0.55            26                1
2651     111     043077       1.19             .                7
2652     111     050177       0.90             .                3
2653     111     050277       0.74             .                1
2654     111     050777       1.11             .                1
2655     111     050877       0.79             .                3
2656     111     050977       1.00             .                1
2657     111     051077       0.82            20                1
2658     111     051177       0.72            10                3
2659     111     051277       0.75            20                6
2660     111     051377       0.75             .                7
2661     111     051477       1.18             .                2
2662     111     051577       1.16             .                2
2663     111     051677       0.91             .               10
2664     111     051777       0.93            20                8
2665     111     051877       0.93            18               19
2666     111     051977       0.87            14                4
2667     111     052077       0.95             .               11
2668     111     052177       0.91             .               15
2669     111     052277       0.94             .               26
2670     111     052377       0.95             .               13
2671     111     052477       0.98            19                5
2672     111     052577       1.07            10               10
2673     111     052677       1.17            17                9
2674     111     052777       0.98             .                9
2675     111     052877       1.10             .                8
2676     111     052977       1.16             .               13
2677     111     053077       1.09             .                8
2678     111     053177       1.03            32                1
2679     111     060177       0.85            39                2
2680     111     060277       1.17            64                5
2681     111     060377       0.96             .                5
2682     111     060477       1.06             .                1
2683     111     060577       0.98             .                1
2684     111     060677       0.98             .               16
2685     111     060777       1.09            31               13
2686     111     060877       1.08            36                9
2687     111     060977       0.77            40               16
2688     111     061077       1.08             .                9
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------------------------------------------------------------ POLL=TSS ------------------------------------------------------------

   OBS      PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

   2689      111      061177       0.99              .                11
   2690      111      061277       0.89              .                22
   2691      111      061377       1.10              .                13
   2692      111      061477       0.85             15                 5
   2693      111      061577       0.82             21                16
   2694      111      061677       0.84             19                14
   2695      111      061777       0.86              .                 5
   2696      111      061877       0.76              .                 9
   2697      111      061977       0.76              .                11
   2698      111      062077       0.68              .                 8
   2699      111      062177       0.42             35                 7
   2700      111      062277       0.92             40                 7
   2701      111      062377       1.01             45                 9
   2702      111      062477       0.98              .                17
   2703      111      062577       0.84              .                12
   2704      111      062677       1.13              .                25
   2705      111      062777       1.05              .                 7
   2706      111      062877       1.01             37                 6
   2707      111      062977       0.62             42                 6
   2708      111      070177       1.08              .                 4
   2709      111      070277       0.80              .                 3
   2710      111      070377       0.83              .                13
   2711      111      070477       0.80              .                13
   2712      111      070577       0.66             58                 6
   2713      111      070677       0.74             45                11
   2714      111      070777       0.67             29                16
   2715      111      070877       0.58              .                12
   2716      111      070977       0.76              .                 6
   2717      111      071077       0.93              .                 9
   2718      111      071177       0.83              .                10
   2719      111      071277       0.82             60                 9
   2720      111      071377       0.99             40                 3
   2721      111      071477       1.01             54                 2
   2722      111      071577       0.86              .                 1
   2723      111      071677       0.94              .                 2
   2724      111      071777       0.89              .                 8
   2725      111      071877       0.88              .                 5
   2726      111      071977       0.88             43                 7
   2727      111      072077       0.85             50                 4
   2728      111      072177       0.97             44                 4
   2729      111      072277       0.87              .                 8
   2730      111      072377       1.17              .                10
   2731      111      072477       1.12              .                 6
   2732      111      072577       1.00              .                13
   2733      111      072677       0.74             27                37
   2734      111      072777       0.96             26                10
   2735      111      072877       0.93             37                48
   2736      111      072977       0.61              .                 7
   2737      111      073077       1.11              .                 2
   2738      111      073177       1.01              .                15
   2739      111      080177       0.79              .                10
   2740      111      080277       1.08             34                 4
   2741      111      080377       1.09             43                 5
   2742      111      080477       1.09             50                 5
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------------------------------------------------------------ POLL=TSS ------------------------------------------------------------

  OBS     PLANT     DATE     FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

  2743     111     080577      1.20              .                 9
  2744     111     080677      1.15              .                 5
  2745     111     080777      1.27              .                16
  2746     111     080877      1.11              .                 5
  2747     111     080977      1.03             42                 5
  2748     111     081077      0.93             38                25
  2749     111     081177      0.92             40                 9
  2750     111     081277      0.97              .                 2
  2751     111     081377      1.07              .                 5
  2752     111     081477      0.90              .                 5
  2753     111     081577      0.88              .                 2
  2754     111     081677      0.99             42                 1
  2755     111     081777      0.87             48                 7
  2756     111     081877      1.16             40                32
  2757     111     081977      1.02              .                 5
  2758     111     082077      0.96              .                26
  2759     111     082177      0.91              .                 4
  2760     111     082277      0.83              .                 1
  2761     111     082377      0.75             38                 2
  2762     111     082477      0.74             51                 6
  2763     111     082677      1.11              .                18
  2764     111     082777      0.85              .                 6
  2765     111     082877      0.97              .                 2
  2766     111     082977      0.81              .                 6
  2767     111     083077      0.85             47                 2
  2768     111     083177      0.80             48                10
  2769     111     090177      0.76             40                 7
  2770     111     090277      0.95              .                 8
  2771     111     090377      1.06              .                 6
  2772     111     090477      1.06              .                 2
  2773     111     090577      0.88              .                 5
  2774     111     090677      1.00             37                 6
  2775     111     090777      1.01             32                 1
  2776     111     090877      0.84             33                 3
  2777     111     090977      1.23              .                 9
  2778     111     091077      1.08              .                 3
  2779     111     091177      0.89              .                 1
  2780     111     091277      0.88              .                14
  2781     111     091377      1.15             22                 1
  2782     111     091477      0.97             64                 5
  2783     111     091577      0.67             32                 1
  2784     111     091677      0.80              .                 2
  2785     111     091777      0.91              .                 3
  2786     111     091877      0.78              .                 6
  2787     111     091977      0.84              .                 7
  2788     111     092077      1.10             38                 6
  2789     111     092177      1.12             33                 6
  2790     111     092277      1.30             30                 3
  2791     111     092377      1.05              .                 7
  2792     111     092477      1.31              .                 4
  2793     111     092577      1.10              .                 5
  2794     111     092677      0.74              .                10
  2795     111     092777      0.67             35                 3
  2796     111     092877      0.95             40                14
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POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
2797	111	092977	0.91	36	44
2798	111	093077	1.02	.	6
2799	111	100177	0.97	.	3
2800	111	100277	0.90	.	8
2801	111	100377	1.00	.	9
2802	111	100477	0.76	43	16
2803	111	100577	1.02	42	7
2804	111	100677	0.88	45	4
2805	111	100777	0.94	.	2
2806	111	100877	0.96	.	5
2807	111	100977	0.91	.	7
2808	111	101077	0.84	.	6
2809	111	101177	0.76	49	2
2810	111	101277	0.86	48	10
2811	111	101377	1.04	47	10
2812	111	101477	1.03	.	3
2813	111	101577	0.90	.	7
2814	111	101677	1.13	.	8
2815	111	101777	0.91	.	13
2816	111	101877	1.10	40	11
2817	111	101977	0.58	39	10
2818	111	102077	0.85	37	13
2819	111	102177	1.02	.	13
2820	111	102277	1.05	.	20
2821	111	102377	0.91	.	33
2822	111	102477	1.03	.	24
2823	111	102577	0.86	36	22
2824	111	102677	0.92	47	11
2825	111	102777	0.72	54	18
2826	111	102977	0.88	.	4
2827	111	103077	0.99	.	6
2828	111	103177	0.85	.	4
2829	111	110177	0.81	41	15
2830	111	110277	0.93	56	19
2831	111	110377	1.18	48	15
2832	111	110477	1.14	.	14
2833	111	110577	1.05	.	10
2834	111	110677	1.07	.	18
2835	111	110777	0.96	.	8
2836	111	110877	0.87	42	2
2837	111	110977	1.01	33	11
2838	111	111077	1.02	40	7
2839	111	111277	0.90	.	20
2840	111	111377	0.93	.	14
2841	111	111477	0.76	.	9
2842	111	111577	0.91	69	5
2843	111	111777	0.88	58	11
2844	111	111877	0.88	.	7
2845	111	112077	0.72	48	1
2846	111	112177	0.82	73	1
2847	111	112277	0.79	55	12
2848	111	112377	0.65	50	10
2849	111	112477	0.87	.	32
2850	111	112577	0.78	.	35

```
------------------------------------------------------- POLL=TSS ------------------------------------------------------------

           OBS      PLANT      DATE      FLOW(MGD)    INFLUENT(PPM)    EFFLUENT(PPM)

           2851      111      112677       0.72              .               12
           2852      111      112777       0.72              .                2
           2853      111      112877       0.78              .                3
           2854      111      112977       0.84             83               14
           2855      111      113077       1.15             46                8
           2856      111      120177       0.97             43                8
           2857      111      120277       0.81              .                6
           2858      111      120377       0.88              .               11
           2859      111      120477       0.87              .                9
           2860      111      120577       0.80              .                1
           2861      111      120677       1.03             62               13
           2862      111      120777       1.11             70               11
           2863      111      120877       0.68             70               14
           2864      111      120977       0.72              .               28
           2865      111      121077       0.74              .               15
           2866      111      121177       0.78              .               14
           2867      111      121277       0.90              .               38
           2868      111      121377       0.91             30               16
           2869      111      121477       1.06             35                5
           2870      111      121577       0.68             55                8
           2871      111      121677       0.88              .                6
           2872      111      121777       0.78              .                5
           2873      111      121877       0.90              .                4
           2874      111      121977       0.73             66                3
           2875      111      122077       0.86             73               10
           2876      111      122177       0.92             70               62
           2877      111      122277       0.95              .                2
           2878      111      122377       0.79              .                2
           2879      111      122477       0.82              .               31
           2880      111      122677       0.84              .                9
           2881      111      122777       0.79             50                6
           2882      111      122877       0.71             60                9
           2883      111      122977       0.86             60                5
           2884      111      123077       0.94              .               13
           2885      111      123177       0.89              .                9
           2886      126      100275       0.38            426               33
           2887      126      100575       0.28            671               20
           2888      126      100675       0.33            783               19
           2889      126      100775       0.30            364               25
           2890      126      100875       0.38           1180               38
           2891      126      100975       0.34           2000               24
           2892      126      101275       0.32           5988               14
           2893      126      101375       0.36           7000               46
           2894      126      101475       0.38          14600               23
           2895      126      101575       0.43            422               30
           2896      126      101675       0.49            333               26
           2897      126      101975       0.38            600               23
           2898      126      102075       0.32            544               29
           2899      126      102175       0.33            683               10
           2900      126      102275       0.31           1260               28
           2901      126      102375       0.32           1220               20
           2902      126      102675       0.30            453               30
           2903      126      102775       0.44            443               33
           2904      126      102875       0.53            447               31
```

POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
2905	126	102975	0.41	430	30
2906	126	103075	0.36	813	38
2907	126	110275	0.29	743	20
2908	126	110375	0.30	738	32
2909	126	110475	0.30	393	25
2910	126	110575	0.37	264	18
2911	126	110675	0.39	144	19
2912	126	110975	0.44	550	21
2913	126	111075	0.58	469	18
2914	126	111175	0.48	276	3
2915	126	111275	0.45	560	25
2916	126	111375	0.49	950	30
2917	126	111675	0.41	691	16
2918	126	111775	0.43	379	26
2919	126	111875	0.44	300	20
2920	126	111975	0.46	310	17
2921	126	112075	0.46	475	13
2922	126	112375	0.36	593	15
2923	126	112475	0.38	356	21
2924	126	112575	0.41	293	17
2925	126	112775	0.40	448	22
2926	126	113075	0.35	156	11
2927	126	120175	0.38	308	13
2928	126	120275	0 33	260	10
2929	126	120375	0.33	268	7
2930	126	120475	0.40	376	11
2931	126	120775	0.38	300	10
2932	126	120875	0.35	412	14
2933	126	120975	0.40	538	15
2934	126	121075	0.30	508	26
2935	126	121175	0.26	221	11
2936	126	121475	0.39	265	7
2937	126	121575	0.38	226	20
2938	126	121675	0.35	268	10
2939	126	121775	0.33	260	20
2940	126	121875	0.36	254	21
2941	126	122175	0.25	320	18
2942	126	122275	0.31	287	10
2943	126	122375	0.34	350	13
2944	126	122575	0.43	333	12
2945	126	122875	0.45	360	10
2946	126	122975	0.45	406	11
2947	126	123075	0.42	205	10
2948	126	010176	0.29	240	10
2949	126	010476	0.45	213	19
2950	126	010576	0.42	168	22
2951	126	010676	0.43	64	11
2952	126	010776	0.32	140	16
2953	126	010876	0.35	380	10
2954	126	011176	0.39	360	10
2955	126	011276	0.40	472	12
2956	126	011376	0.37	243	10
2957	126	011476	0.35	260	11
2958	126	011576	0.32	212	8

POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
2959	126	011876	0.30	392	11
2960	126	011976	0.34	311	14
2961	126	012076	0.35	306	11
2962	126	012176	0.36	300	10
2963	126	012276	0.33	304	10
2964	126	012576	0.39	367	6
2965	126	012676	0.35	429	10
2966	126	012776	0.35	256	11
2967	126	012876	0.36	343	34
2968	126	012976	0.44	435	29
2969	126	020176	0.45	245	12
2970	126	020276	0.34	310	38
2971	126	020376	0.37	392	15
2972	126	020476	0.38	245	13
2973	126	020576	0.41	239	10
2974	126	020876	0.46	246	11
2975	126	020976	0.42	324	15
2976	126	021076	0.35	246	3
2977	126	021176	0.37	444	17
2978	126	021276	0.34	269	4
2979	126	021676	0.35	248	20
2980	126	021776	0.34	104	3
2981	126	021876	0.36	160	10
2982	126	021976	0.41	120	11
2983	126	022276	0.27	154	17
2984	126	022376	0.31	160	10
2985	126	022476	0.33	324	11
2986	126	022576	0.21	168	10
2987	126	022676	0.30	143	12
2988	126	022976	0.29	322	10
2989	126	030176	0.25	123	5
2990	126	030276	0.31	367	12
2991	126	030376	0.33	139	10
2992	126	030476	0.29	161	8
2993	126	030776	0.23	300	21
2994	126	030876	0.38	236	14
2995	126	030976	0.45	216	10
2996	126	031076	0.37	224	11
2997	126	031176	0.39	144	11
2998	126	031476	0.24	256	25
2999	126	031576	0.33	416	11
3000	126	031676	0.40	197	24
3001	126	031776	0.35	126	15
3002	126	031876	0.29	233	14
3003	126	032176	0.26	186	21
3004	126	032276	0.25	148	39
3005	126	032376	0.26	160	29
3006	126	032476	0.27	2089	38
3007	126	032576	0.27	2370	51
3008	126	032876	0.26	400	30
3009	126	032976	0.32	393	50
3010	126	033076	0.39	328	24
3011	126	033176	0.51	268	39
3012	126	040176	0.44	1064	23

```
-------------------------------------------------------- POLL=TSS ----------------------------------------------------------

        OBS      PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

        3013      126      040476       0.38            179                11
        3014      126      040576       0.30            260                14
        3015      126      040676       0.23            499                16
        3016      126      040776       0.26            514                27
        3017      126      040876       0.25            347                20
        3018      126      041176       0.23            952                53
        3019      126      041276       0.23            231                42
        3020      126      041376       0.26            205                31
        3021      126      041476       0.27            171                47
        3022      126      041876       0.28            148                49
        3023      126      041976       0.33            133                61
        3024      126      042076       0.36            129                28
        3025      126      042176       0.33            340                50
        3026      126      042276       0.33            324                54
        3027      126      042576       0.31            196                58
        3028      126      042676       0.33            435                80
        3029      126      042776       0.28            258                50
        3030      126      042876       0.29            244                75
        3031      126      042976       0.31            144                46
        3032      126      050276       0.33            190                56
        3033      126      050376       0.36            224                38
        3034      126      050476       0.39            214                45
        3035      126      050576       0.30            236                44
        3036      126      050676       0.40            566                38
        3037      126      050976       0.33            710                40
        3038      126      051076       0.37            364                18
        3039      126      051176       0.38            507                40
        3040      126      051276       0.32            390                30
        3041      126      051376       0.43            393                22
        3042      126      051676       0.19            200                24
        3043      126      051776       0.36            313                36
        3044      126      051876       0.35            140                29
        3045      126      051976       0.34            325                25
        3046      126      052076       0.34            500                35
        3047      126      052376       0.25            295                27
        3048      126      052476       0.20           1325                26
        3049      126      052576       0.22           1266                23
        3050      126      052676       0.20           1692                25
        3051      126      052776       0.28            430                37
        3052      126      053176       0.20           1700                12
        3053      126      060176       0.25            400                35
        3054      126      060276       0.41            525                36
        3055      126      060376       0.27           1270                80
        3056      126      060676       0.23           1740                34
        3057      126      060776       0.23           1400                32
        3058      126      060876       0.23           2988                70
        3059      126      060976       0.24           1614                38
        3060      126      061076       0.27            350                31
        3061      126      061376       0.27            230                25
        3062      126      061476       0.41            103                11
        3063      126      061576       0.28            400                40
        3064      126      061676       0.38            213                13
        3065      126      061776       0.45            163                14
        3066      126      062076       0.37            225                29
```

POLL=TSS

OBS	PLANT	DATE	FLOW(MGD)	INFLUENT(PPM)	EFFLUENT(PPM)
3067	126	062176	0.42	480	11
3068	126	062276	0.50	922	28
3069	126	062376	0.43	5160	22
3070	126	062476	0.37	2456	47
3071	126	062776	0.33	520	20
3072	126	062876	0.37	480	11
3073	126	062976	0.39	341	24
3074	126	063076	0.35	292	19
3075	126	070176	0.27	307	20
3076	126	070576	0.28	400	22
3077	126	070676	0.30	200	30
3078	126	070776	0.42	1170	22
3079	126	070876	0.38	188	18
3080	126	071176	0.27	112	12
3081	126	071276	0.29	333	50
3082	126	071376	0.25	343	50
3083	126	071476	0.30	327	35
3084	126	071576	0.37	208	57
3085	126	071876	0.29	.	13
3086	126	071976	0.28	480	25
3087	126	072076	0.28	250	13
3088	126	072176	0.28	230	11
3089	126	072276	0.37	413	27
3090	126	072576	0.38	.	11
3091	126	072676	0.41	292	31
3092	126	072776	0.46	206	21
3093	126	072876	0.38	143	15
3094	126	072976	0.72	117	20
3095	126	080176	0.41	192	21
3096	126	080276	0.33	176	10
3097	126	080376	0.35	208	20
3098	126	080476	0.33	500	28
3099	126	080576	0.37	378	18
3100	126	080876	0.33	295	15
3101	126	080976	0.31	152	12
3102	126	081076	0.28	381	11
3103	126	081176	0.28	240	13
3104	126	081276	0.36	190	15
3105	126	081576	0.40	565	25
3106	126	081676	0.43	358	43
3107	126	081776	0.35	542	49
3108	126	081876	0.33	387	20
3109	126	081976	0.31	230	21
3110	126	082276	0.21	295	18
3111	126	082376	0.24	540	31
3112	126	082476	0.25	263	19
3113	126	082576	0.29	500	23
3114	126	082676	0.37	280	14
3115	126	082976	0.26	160	19
3116	126	083076	0.32	393	39
3117	126	083176	0.36	445	28
3118	126	090176	0.42	390	19
3119	126	090276	0.54	875	15
3120	126	090676	0.33	413	9

```
------------------------------------------------------------- POLL=TSS -------------------------------------------------------------

        OBS      PLANT      DATE      FLOW(MGD)     INFLUENT(PPM)     EFFLUENT(PPM)

        3121      126      090776       0.46             226                16
        3122      126      090876       0.38             313                 9
        3123      126      090976       0.30             299                17
        3124      126      091276       0.43             400                15
        3125      126      091376       0.52             430                13
        3126      126      091476       0.55             347                17
        3127      126      091576       0.63             313                40
        3128      126      091676       0.45            1083                37
        3129      126      091976       0.34             360                20
        3130      126      092076       0.47             131                11
        3131      126      092176       0.53             133                14
        3132      126      092276       0.52             182                17
        3133      126      092376       0.47             362                10
        3134      126      092676       0.45             400                10
        3135      126      092776       0.53             310                21
        3136      126      092876       0.49             345                 7
        3137      126      092976       0.38             230                11
        3138      126      093076       0.47             839                48
```

APPENDIX II B

Summary Statistics for PMP Data

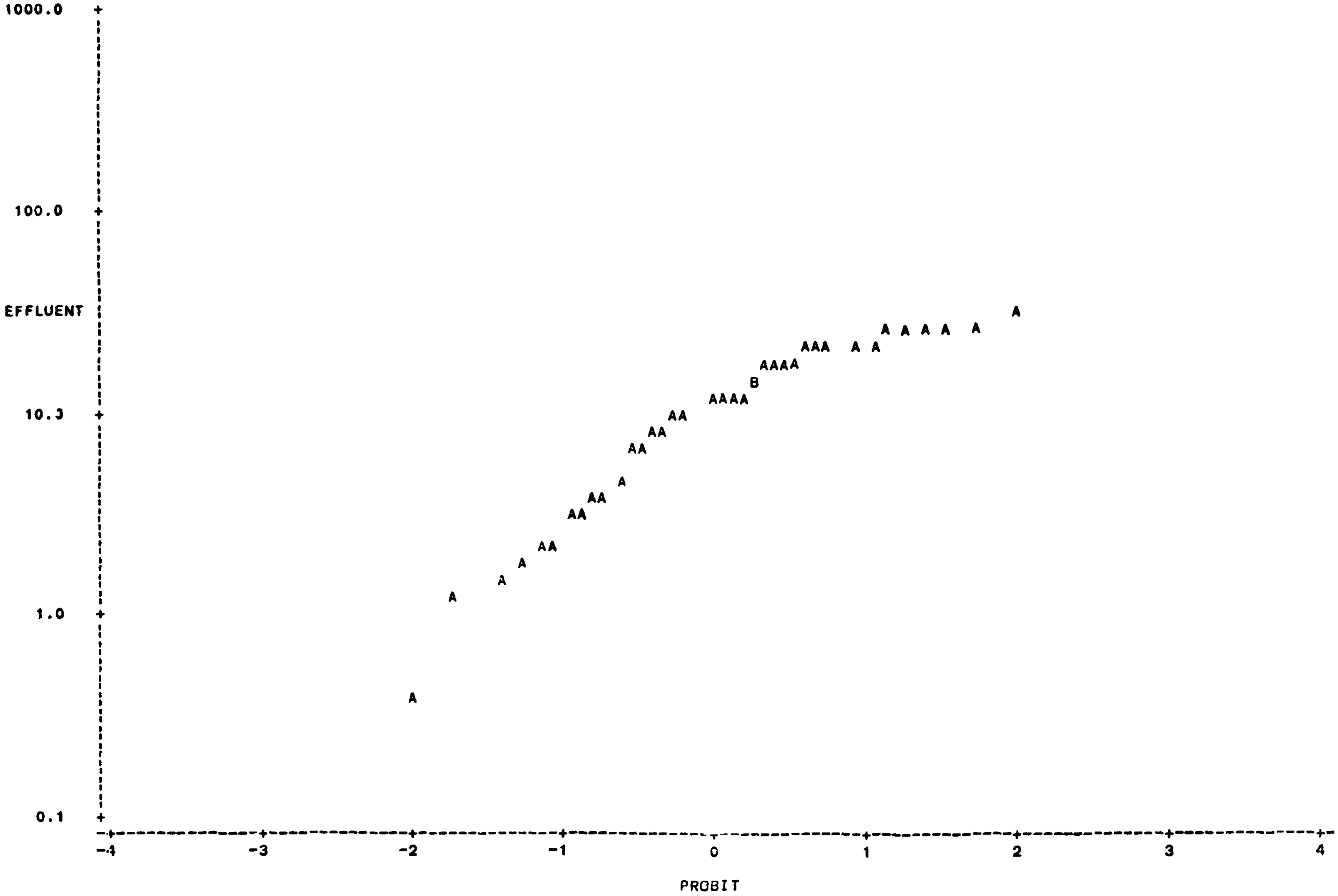
```
                              SUMMARY STATISTICS ON PMP DATA BY POLLUTANT                                                    1
                               INFLUENT AND EFFLUENT CONCENTRATION(PPM)

------------------------------------------------------------ POLL=BOD -----------------------------------------------------------

 PLANT    NINF    MEANINF    MEDINF    STDINF    MININF    MAXINF    NEFF    MEANEFF    MEDEFF    STDEFF    MINEFF    MAXEFF

     9      23      84.74        59    61.779         9       226      24    5.70633       5.0   2.83578       1.0        14
    44      45     754.00       710   259.794       225      1689     261    8.86590       8.0   5.04148       1.0        31
    45     148     381.14       369   132.375        55       760     156    3.04487       3.0   1.90532       1.0        12
    96       0          .         .         .         .         .     105    2.36190       2.0   1.87146       1.0        11
   111     157      94.82        95    38.166        24       340     157    6.19108       5.0   3.43462       2.0        20
   126     247    1087.47      1000   534.181       300      2600     249    5.96225       4.7   4.01444       0.6        20

------------------------------------------------------------ POLL=OAG -----------------------------------------------------------

 PLANT    NINF    MEANINF    MEDINF    STDINF    MININF    MAXINF    NEFF    MEANEFF    MEDEFF     STDEFF    MINEFF    MAXEFF

     3     157    41.1395      32.0   40.3825       2.3     312.0      46    13.0261     12.25     8.6642       0.4   [illegible]
    61     234    17.3932      14.0   17.1321       2.0     230.0     348    14.5833     11.00    17.9715       1.0       265
   124      59    22.9017      17.3   19.0899       0.4     103.2     100     5.1670      2.65     7.1238       0.1        30
   170     203    79.2773      66.0   55.2835      12.0     409.0     163    10.7859      9.60     6.9133       0.6        39

------------------------------------------------------------ POLL=TSS -----------------------------------------------------------

 PLANT    NINF    MEANINF    MEDINF    STDINF    MININF    MAXINF    NEFF    MEANEFF    MEDEFF    STDEFF    MINEFF    MAXEFF

     9      24      27.25      23.5     16.43         4        57      24    29.0917      20.5   15.1753       6.0        53
    44     249    3780.76    1040.0   7466.80        18     69600     260    14.4615       6.0   47.6527       1.0       580
    45     257     304.32     202.0    410.49         2      3758     364    17.9945      10.0   17.9430       2.0       112
    96       0          .         .         .         .         .      66    12.2273      10.5    8.3974       2.0   [illegible]
   111     148      42.84      40.0     16.62        10       100     347    10.0735       8.0    9.2436       0.5        71
   126     251     557.00     324.0   1155.43        64     14600     253    23.1344    , 20.0   14.1249       3.0        60
```

APPENDIX II C

Probit Plots for PMP Oil and Grease Data

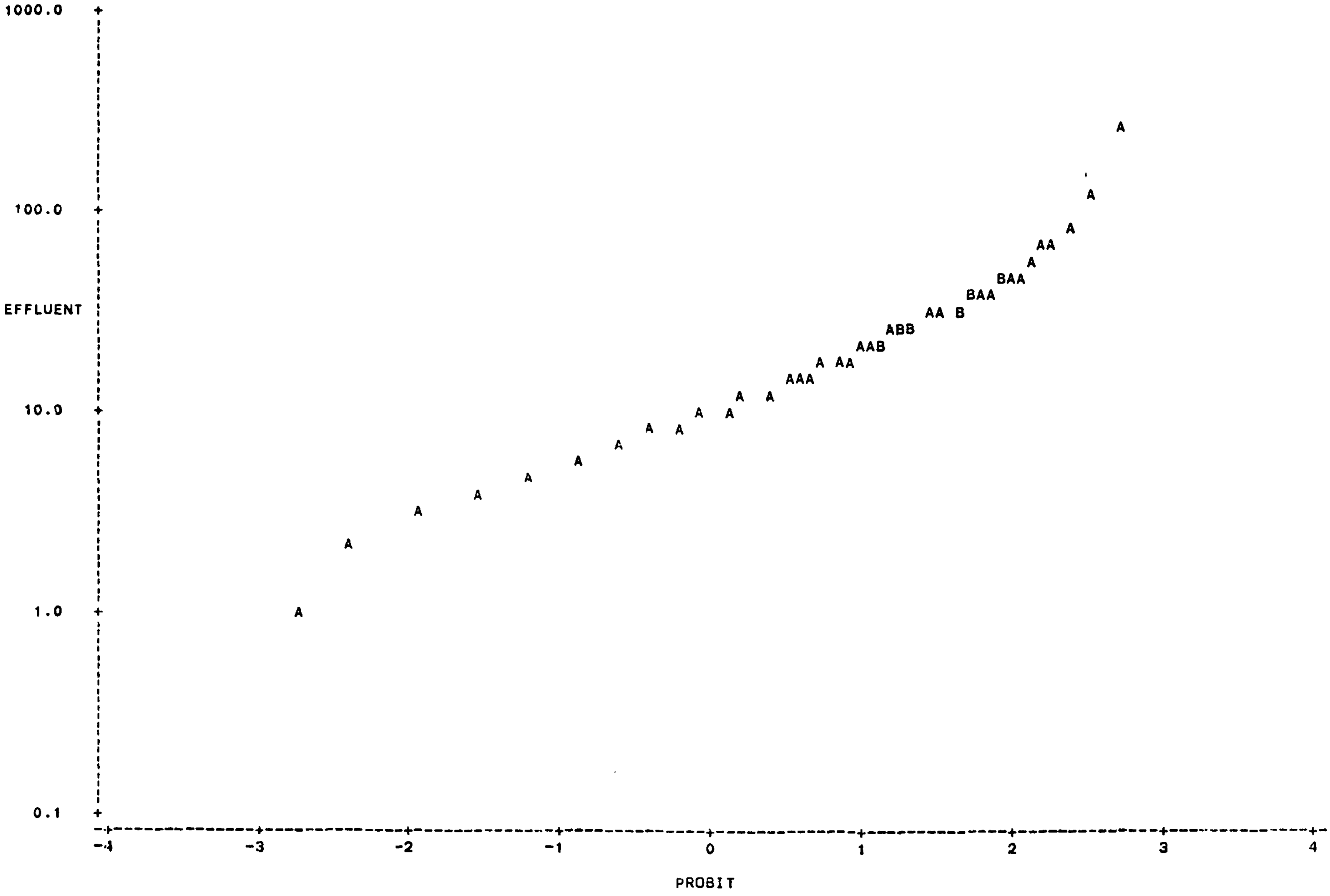
PROBABILITY PLOT OF OIL & GREASE(PPM)
PLANT=3

PLOT OF EFFLUENT*PROBIT   LEGEND: A = 1 OBS, B = 2 OBS, ETC.



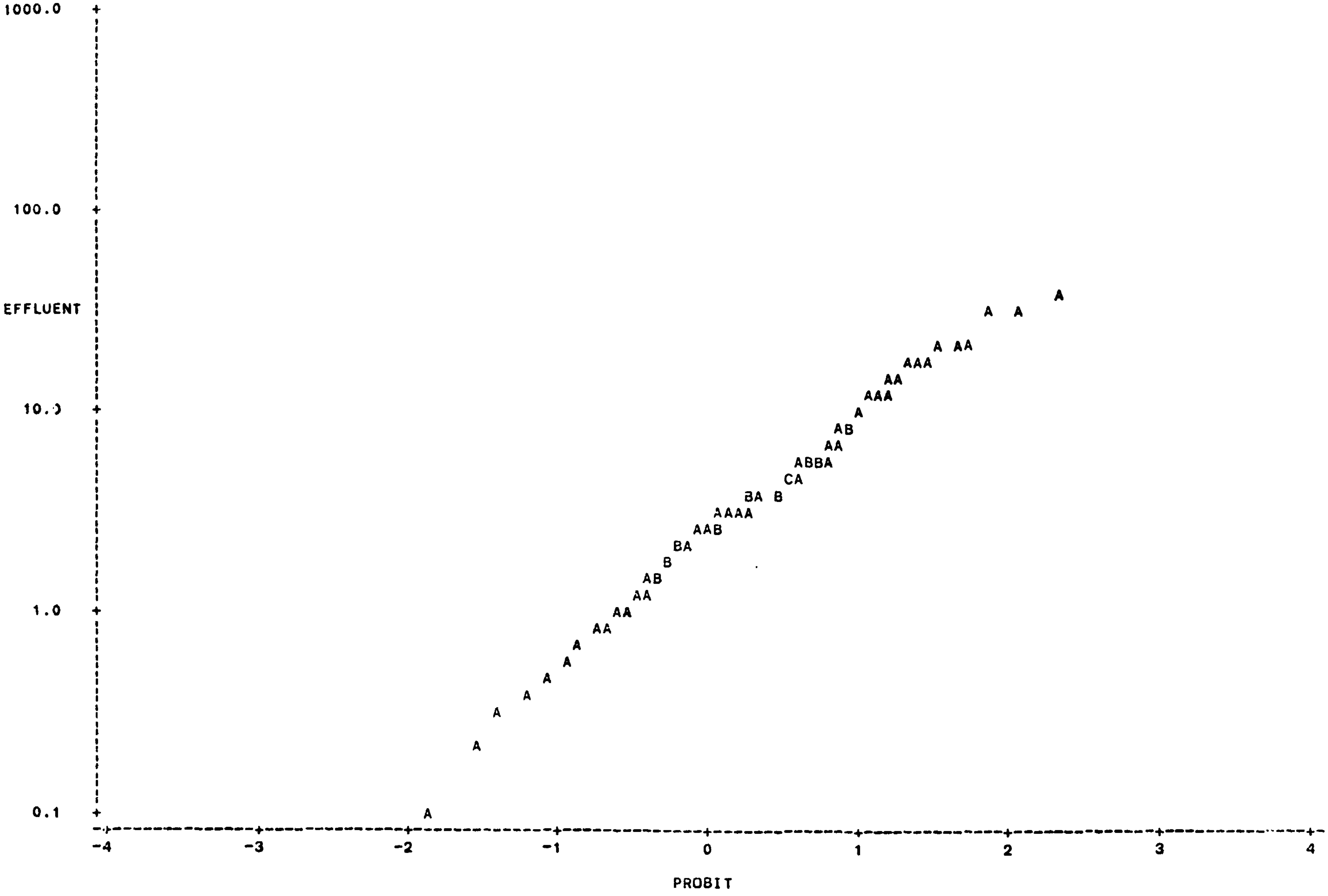
PROBABILITY PLOT OF OIL & GREASE(PPM)
PLANT=61

PLOT OF EFFLUENT*PROBIT LEGEND: A = 1 OBS, B = 2 OBS, ETC.



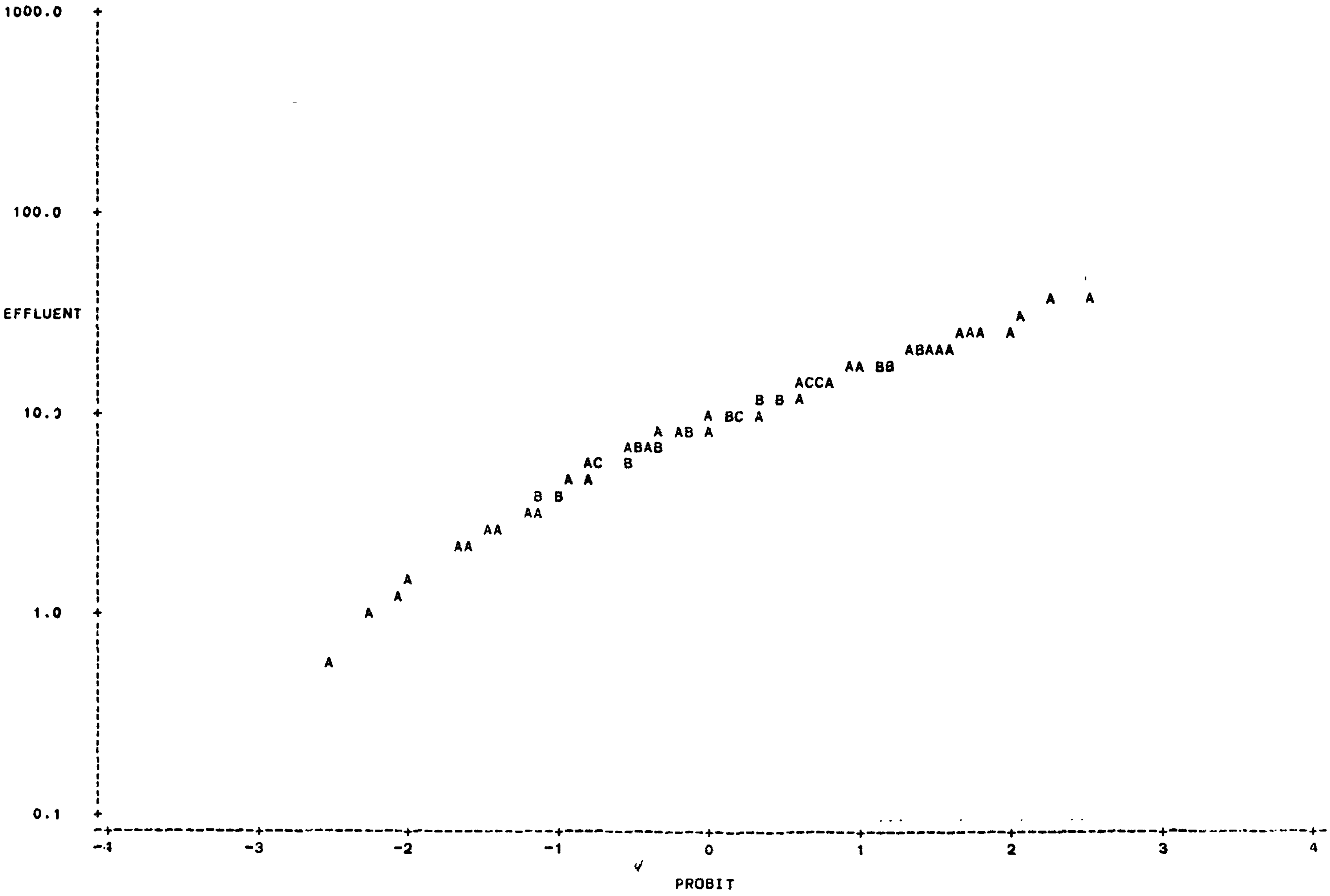
PROBABILITY PLOT OF OIL & GREASE(PPM)
PLANT=124

PLOT OF EFFLUENT*PROBIT   LEGEND: A = 1 OBS, B = 2 OBS, ETC.



PROBABILITY PLOT OF OIL & GREASE(PPM)
PLANT=170

PLOT OF EFFLUENT*PROBIT LEGEND: A = 1 OBS, B = 2 OBS, ETC.



APPENDIX III

Statistical Procedures

Statistical Procedures

Descriptive Statistics

Some of the more commonly employed descriptive statistics are defined as follows:

(1) N - number of valid observations used in a particular analysis (e.g., the total number of effluent samples at a particular plant for a particular pollutant)

(2) Mean - arithmetic average: $\bar{X} = \sum_{i=1}^{N} X_i/N$

(3) Variance - standard unbiased estimate: $S^2 = \frac{1}{N-1} \sum_{i=1}^{N} (X_i - \bar{X})^2$

Log-variance - variance with $X_i = \log_e$ (observation)

Daily variability factors depend directly on the log-variance (see the section of this Appendix below on Variability Factors).

(The standard deviation is $S = \sqrt{S^2}$.)

(4) Minimum - the smallest value in a set of N observations.

(5) Maximum - the largest value in a set of N observations.

(6) Range - the minimum subtracted from the maximum.

(7) Median - the middle value in a set of N observations. If N is odd (N = 2k - 1 for some integer k), the median is the kth order statistic, C(k). If N is even (N = 2k), the median is

$$[C(k) + (C(k + 1)]/2$$

(8) Stream Average - flow weighted average of sample concentrations

$$\bar{X} = \sum W_i X_i$$

where

$$W_i = f_i/\sum f_i$$

for sample concentration X_i and stream flow f_i.

(9) Plant Average - flow weighted averages of stream concentrations

$$\bar{X} = \sum W_i X_i$$

where

$$W_i = f_i / \sum f_i$$

for sample average concentration x_i and stream average f_i. When flows are missing the plant average is the plant mean.

Goodness-of-Fit

The goodness-of-fit of the lognormal model for the O&G effluent data (PMP) was checked through a graphical procedure called a probability plot. Let $X_1, \ldots, X_n$ denote the n observation daily values fo the parameter of interest (the BOD or measurements from a given plant). Denote the rth largest of the n values by $X_{(r)}$, and define a corresponding score called the "probit" by

$$\text{Probit } [X_{(r)}] = \Phi^{-1}[r/(n + 1)],$$

where $\Phi^{-1}(.)$ is the inverse of the standard normal cumulative distribution function. The probit score is the normal deviation (z-value) equivalent to the value $X_{(r)}$. Probit scores are useful because plots of X values versus corresponding probit scores tend to be straight lines when X is normally distributed; this fact is the basis for probability plots. If X has a lognormal distribution, a log-scale plot of X values versus probit scores tends to be a straight line. Daniel and Wood (1971) give simulated examples of probability plots to indicate the degree of random departure from a straight line to expect for different sample sizes when X is normally distributed. Probability plots for BOD and TSS are presented in Figures B-1 to B-28 of the BPT Development Document. Similar plots for O&G are presented in Appendix IIC of this memorandum.

Based on the probability plots, it was concluded that the lognormal distribution was a reasonable model for the PMP oil and grease effluent data.

Variability Factors for the Cleaning Subcategory

Assuming that the distribution of the concentration c is lognormal, then $y = \log(c)$ is normally distributed with mean μ and variance σ^2 (Aitchison and Brown, pages 8-9). Thus, the 99th percentile on the natural log scale is

$$y_{0.99} = \mu + 2.326\ \sigma\ ,$$

and the 99th percentile on the concentration scale is

$$c_{0.99} = \exp(y_{0.99}) = e^{\mu + 2.326\ \sigma}\ .$$

The mean and variance on the concentration scale are:

$$\mu_c = e^{\mu + 1/2\ \sigma^2}$$

and

$$\sigma^2_c = e^{2\mu + \sigma^2} (e^{\sigma^2} - 1).$$

Hence, the daily maximum variability factor under the lognormal model is

$$VF(1) = \frac{c_{0.99}}{\mu_c} = \exp(2.326\ \sigma - 0.5\ \sigma^2). \qquad (2)$$

Estimates of any of the above quantities are calculated by substituting the mean and variance of natural logs of the observations for μ and σ^2, respectively, Consequently, the daily maximum variability factors depends directly on the log-variance of the concentration.

Variability factors for 30-day average concentrations, VF(30), are based on the distribution of an average of values drawn from the distribution of daily values and take day-to-day correlation into account. Positive autocorrelation between concentrations measured on consecutive days means that such concentrations tend to be similar. The following formulas incorporate the autocorrelation between concentrations values measured on adjacent days.

The correlation (ρ) between adjacent days' measurements (i.e., the lag-1 autocorrelation) was estimated using the available data. Then using the first-order autoregressive model commonly found to be appropriate in water pollution modeling, the mean and variance of an average of n daily values, denoted by $\bar{c}$, were approximated by:

$$\mu_{\bar{c}} = \exp(\mu + \sigma^2/2) \qquad (3)$$

and

$$\sigma^2_{\bar{c}} = \frac{\sigma^2_{\bar{c}}}{n}\ fn\ (\rho), \qquad (4)$$

with

$$f_n(\rho) = 1 + (2/n) \sum_{k=1}^{n-1} (n-k)(\exp(\rho^k\ \sigma^2) - 1)/(\exp\ \sigma^2 - 1).$$

It can be seen in (4) that $\sigma^2_{\bar{c}}$ equals the variance of an average of n uncorrelated observations, $\sigma^2_{\bar{c}}$ /n, multiplied by a factor, fn(ρ) that adjusts for the presence of autocorrelation. For oil and grease effluent data, the estimate for the lag-1 autocorrelation between logs of the concentration measurements was 0.5095 and the adjustment factor is 2.665.

Similar adjustments were made in the Organics BPT Development Document for BOD_5 and TSS concentration values.

Finally, since $\bar{c}$ is approximately normally distributed by the Central Limit Theorem, the 95th percentile and variability factors of a 30-day average are approximately

$$\bar{c}_{0.99} = \mu_{\bar{c}} + 1.645\ \sigma_{\bar{c}} \qquad (5)$$

and

$$VF(30) = c_{0.95}/\mu_{\bar{c}}$$

$$= 1 + 1.645[e^{\sigma^2} - 1)f_{30}(\rho)/30]^{1/2} \qquad (6)$$

with $\mu_{\bar{c}}$ and $\sigma^2_{\bar{c}}$ defined by equations (3) and (4). Estimates of $\bar{c}_{0.95}$ or VF(30) are calculated by substituting estimates of μ, σ^2, and ρ into the formulas above.

References

Aitchison, J., and J.A.C. Brown (1957). The Lognormal Distribution, Cambridge University Press, London, 8-9.

Daniel, C., and F.S. Wood (1971). Fitting Equations to Data, Wiley, New York, 34-43.

APPENDIX IV

A) Statistical Procedures for Calculation of a 99th Percentile Limitations for the PM&F Subcategory: Contact Cooling and Heating

B) Statistical Procedure for Calculation of the TSS Effluent Concentration Limits for the PM&F Subcategory: Finishing Water

IV.A. Statistical Procedures for Calculation of a 99th Percentile Limitations for the PM&F Subcategory: Contact Cooling and Heating

For the PM&F contact cooling and heating water subcategory the 99th percentile limitations use the weights for process-type and the process flow within the process-type. To do this each process stream is assigned a weight that is the product of the weight for the process type and the flow weight normalized within the process-type. These weights (Table IV.A.1) are designated by w_i ($i = 1, 2, \ldots, k$) where k is the number of process streams. An example of computation of the weights is shown in the text of this memorandum. Within a stream, pollutant values were assumed to follow the lognormal distribution.

To use the log-normal with the PM&F process data, we estimate the log-normal parameters μ_i and $\sigma_i{}^2$ for each process stream. Generally, for n_i observations on the ith stream, the log mean is

$$\hat{\mu}_i = \sum_{j=1}^{n_i} \ln X_i/n_i$$

and the log-variance $\hat{\sigma}_i{}^2$ is the within process type pooled estimate of σ^2 . This is obtained by computing the sum of squares SS_i, for each stream in a process type

$$SS_i = \sum_{j=1}^{n_i} (\ln X_{i_j} - \hat{\mu}_i)^2$$

and the corresponding degrees of freedom, $\nu_i = n_i - 1$. To obtain the pooled estimate for σ^2 for a process type, we sum the sum of squares and corresponding degrees of freedom for each process stream. Then,

$$\sigma^2_{\text{process-type}} = SS_{\text{process-type}}/D.F._{\text{process-type}}.$$

Pooled estimates for the log-variance of each process type were used because there were at most three data values for a process stream. By assuming processes of the same type have similar log-variances, a more reliable estimate is obtained for σ_i^2 .

When the total degrees of freedom, D.F., for all streams within a process-type is zero, the ratio of the total sum of squares and the total degrees of freedom over all streams in the subcategory is used to estimate pooled variance for the subcategory. The pooled variance estimate for the subcategory is then used for process-types with zero degrees of freedom.

The 99th percentile estimate is the solution, x_{99}, of

$$0.99 = \int_0^{x_{99}} f(x)dx,$$

where

$$f(x) = \sum_{i=1}^{k} w_i f_i(x, \hat{\mu}_i, \hat{\sigma}_i)$$

and the component density functions denoted by f_i are log-normal with estimated parameters $\hat{\mu}_i$ and $\hat{\sigma}_i^2$, respectively. The solution x_{99}, found interatively, is the 99th percentile of the mixture distribution $f(x)$. A summary of the weights w_i, and parameters estimates $\hat{\mu}_i$ and $\hat{\sigma}_i^2$ is given in Table IV A.1.

The expected value, E, and the variance, V, for the log-normal component distributions, f_i are

$$E_i = \exp(\hat{\mu}_i + 0.5\, \hat{\sigma}_i^2)$$

$$V_i = E_i^2(\exp \hat{\sigma}_i^2 - 1).$$

TABLE IV.A.1

A SUMMARY OF THE WEIGHTS, AND LOGNORMAL PARAMETER ESTIMATES BY PROCESS STREAM USED TO CALCULATE THE 99TH PERCENTILES OF THE MIXTURE DISTRIBUTION FOR BOD$_5$, O&G AND TSS IN THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

```
                 PM&F LIMITATIONS COMPUTED
           AS ITERATED SUBCATEGORY 99TH PERCENTILE
         FOR CONTACT COOLING AND HEATING SUBCATEGORY
                STREAMS M-1 AND M-2 DELETED

                     POLLUTANT = BOD5

              POOLED SIGMA =  0.5224

PROCESS   STREAM   WEIGHT      MU      D.F.     SIGMA
-------   ------   ------   --------   ----   --------
 CALEND    B-2     0.0009    1.6094     0      0.3406
 CALEND    E-2     0.0072    1.9459     2      0.3406
 CALEND    F-1     0.0012    2.2282     2      0.3406
 CAST      P-1     0.0140    0.8329     0      0.5224
 EXTRUDE   B-1     0.0027    1.6094     0      0.6794
 EXTRUDE   D-3     0.0003    1.6823     0      0.6794
 EXTRUDE   E-3     0.1182    0.8987     2      0.6794
 EXTRUDE   F-6     0.0067    1.3540     1      0.6794
 EXTRUDE   G-1     0.0046    1.6823     0      0.6794
 EXTRUDE   K-2     0.0133    1.6094     2      0.6794
 EXTRUDE   K-3     0.0067    1.6094     2      0.6794
 EXTRUDE   K-4     0.4874    1.6094     2      0.6794
 EXTRUDE   N-2     0.0001    2.3026     0      0.6794
 EXTRUDE   N-3     0.0031    1.7918     0      0.6794
 EXTRUDE   O-1     0.0082    1.6823     0      0.6794
 EXTRUDE   O-2     0.0061    1.6823     0      0.6794
 EXTRUDE   R-1     0.0130    1.7918     0      0.6794
 EXTRUDE   R-2     0.1823    1.3863     0      0.6794
 MOLD      B-4     0.0000    1.6094     0      0.0667
 MOLD      C-1     0.0002    4.5079     2      0.0667
 MOLD      J-1     0.0673    1.6094     0      0.0667
 MOLD      J-2     0.0050    3.9890     0      0.0667
 THERM     F-2     0.0211    1.9904     2      0.0771
 OTHERS            0.0304    2.0475     0      0.5224
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THE 99TH PERCENTILE IS 26.1148
```

TABLE IV.A.1

A SUMMARY OF THE WEIGHTS, AND LOGNORMAL PARAMETER ESTIMATES BY PROCESS STREAM USED TO CALCULATE THE 99TH PERCENTILES OF THE MIXTURE DISTRIBUTION FOR BOD_5, O&G AND TSS IN THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

```
                  PM&F LIMITATIONS COMPUTED
           AS ITERATED SUBCATEGORY 99TH PERCENTILE
         FOR CONTACT COOLING AND HEATING SUBCATEGORY
                STREAMS M-1 AND M-2 DELETED

                     POLLUTANT = O&G

              POOLED SIGMA =  0.4078

PROCESS  STREAM  WEIGHT     MU     D.F.     SIGMA
-------  ------  ------  --------  ----   --------
 CALEND    B-2   0.0009   1.3863    0      0.6179
 CALEND    E-2   0.0072   2.8197    2      0.6179
 CALEND    F-1   0.0012   0.4621    2      0.6179
 CAST      P-1   0.0140   0.5493    1      0.7768
 EXTRUDE   B-1   0.0027   1.3863    0      0.1022
 EXTRUDE   D-3   0.0003   1.3863    0      0.1022
 EXTRUDE   E-3   0.1182   3.0953    2      0.1022
 EXTRUDE   F-6   0.0067   1.4979    1      0.1022
 EXTRUDE   G-1   0.0046   1.3863    1      0.1022
 EXTRUDE   K-2   0.0133   1.3863    2      0.1022
 EXTRUDE   K-3   0.0067   1.3863    2      0.1022
 EXTRUDE   K-4   0.4874   1.3863    2      0.1022
 EXTRUDE   N-2   0.0001   1.6094    0      0.1022
 EXTRUDE   N-3   0.0031   1.0986    0      0.1022
 EXTRUDE   O-1   0.0082   1.6094    0      0.1022
 EXTRUDE   O-2   0.0061   1.0986    0      0.1022
 EXTRUDE   R-1   0.0130   1.7918    0      0.1022
 EXTRUDE   R-2   0.1823   2.0794    0      0.1022
 MOLD      B-4   0.0000   1.9459    0      0.5600
 MOLD      C-1   0.0002   3.7432    2      0.5600
 MOLD      J-1   0.0673   2.3979    0      0.5600
 MOLD      J-2   0.0050   4.1109    0      0.5600
 THERM     F-2   0.0211   1.3540    1      0.3612
 OTHERS          0.0304   2.4068    0      0.4078
----------------------------------------------------------
```

THE 99TH PERCENTILE IS 28.6541

TABLE IV.A.1

A SUMMARY OF THE WEIGHTS, AND LOGNORMAL PARAMETER ESTIMATES BY PROCESS STREAM USED TO CALCULATE THE 99TH PERCENTILES OF THE MIXTURE DISTRIBUTION FOR BOD_5, O&G AND TSS IN THE CONTACT COOLING AND HEATING WATER SUBCATEGORY

```
                 PM&F LIMITATIONS COMPUTED
            AS ITERATED SUBCATEGORY 99TH PERCENTILE
          FOR CONTACT COOLING AND HEATING SUBCATEGORY
                STREAMS M-1 AND M-2 DELETED

                     POLLUTANT = TSS

               POOLED SIGMA =  0.4936

PROCESS   STREAM   WEIGHT     MU      D.F.    SIGMA
-------   ------   ------  --------   ----  --------
 CALEND     B-2    0.0009   1.3863      0    0.3538
 CALEND     E-2    0.0072   1.0594      2    0.3538
 CALEND     F-1    0.0012   1.4999      2    0.3538
 CAST       P-1    0.0140   0.6931      0    0.4936
 EXTRUDE    B-1    0.0027   1.3863      0    0.4249
 EXTRUDE    D-3    0.0003   1.3863      0    0.4249
 EXTRUDE    E-3    0.1182   1.0594      2    0.4249
 EXTRUDE    F-6    0.0067   1.9636      1    0.4249
 EXTRUDE    G-1    0.0046   2.2387      1    0.4249
 EXTRUDE    K-2    0.0133   1.5214      2    0.4249
 EXTRUDE    K-3    0.0067   1.3863      2    0.4249
 EXTRUDE    K-4    0.4874   1.3863      2    0.4249
 EXTRUDE    N-2    0.0001   1.9636      0    0.4249
 EXTRUDE    N-3    0.0031   1.9636      0    0.4249
 EXTRUDE    O-1    0.0082   1.9636      0    0.4249
 EXTRUDE    O-2    0.0061   1.9636      0    0.4249
 EXTRUDE    R-1    0.0130   1.9636      0    0.4249
 EXTRUDE    R-2    0.1823   1.9636      0    0.4249
 MOLD       B-4    0.0000   1.3863      0    0.9380
 MOLD       C-1    0.0002   3.9595      2    0.9380
 MOLD       J-1    0.0673   1.3863      0    0.9380
 MOLD       J-2    0.0050   3.5835      0    0.9380
 THERM      F-2    0.0211   0.2310      2    0.4002
 OTHERS            0.0304   1.8037      0    0.4936
-------------------------------------------------------
```

THE 99TH PERCENTILE IS 19.1426

IV. B. Statistical Procedure for Calculating the TSS Effluent Concentration Limits for the PM&F Subcategory: Finishing Water

The lognormal 99th percentile for the i-th stream in the finishing water PM&F subcategory is

$$L_i = \exp(\hat{\mu}_i + 2.326\,\hat{\sigma}_i)$$

where $\hat{\mu}_i$ and $\hat{\sigma}_i$ are the estimated log-mean and the log-variance for the i-th stream in the finishing water subcategory. A pooled log-variance was used for the finishing subcategory because of the small number of degrees of freedom for each stream.

The lognormal expectation for the i-th stream is

$$E_i = \exp(\hat{\mu}_i + 0.5\,\hat{\sigma}_i^2)$$

and the lognormal variance for the i-th stream is

$$V_i = E_i^2(\exp\hat{\sigma}^2 - 1).$$

The daily variability factor is

$$VF(1) = (\Sigma\ w_i L_i)/(\Sigma\ w_i E_i)$$

where w_i is the flow weight for the i-th stream normalized so that

$$\Sigma\ wi = 1.$$

That is

$$wi = f_i/\Sigma f_i$$

where f_i is the average flow for the i-th stream. In this case, the daily variability factor is

$$VF(1) = \exp(2.326\,\hat{\sigma} - 0.5\,\hat{\sigma}^2)$$

$$= 8.1$$

because the pooled estimate, $\hat{\sigma} = 1.216$, is used.

The 30-day variability factors based on the central limit theorem approximation for an average of 30 samples is

$$VF(30) = 1 + 1.6449(V/30)^{.5}/E$$

$$= 2.3$$

where

$$E = \Sigma\ w_i E_i = 102.4\ \text{mg/l},$$