



# Optimizing Nutrient Removal in Oxidation Ditches

US EPA sponsored webinar for Wastewater Treatment Plant Operators  
January 27, 2022

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# Optimizing Nutrient Removal & Wastewater Excellence

**Optimizing Nutrient Removal in:**

**Oxidation Ditches**

(Today)

**Sequencing Batch Reactors**

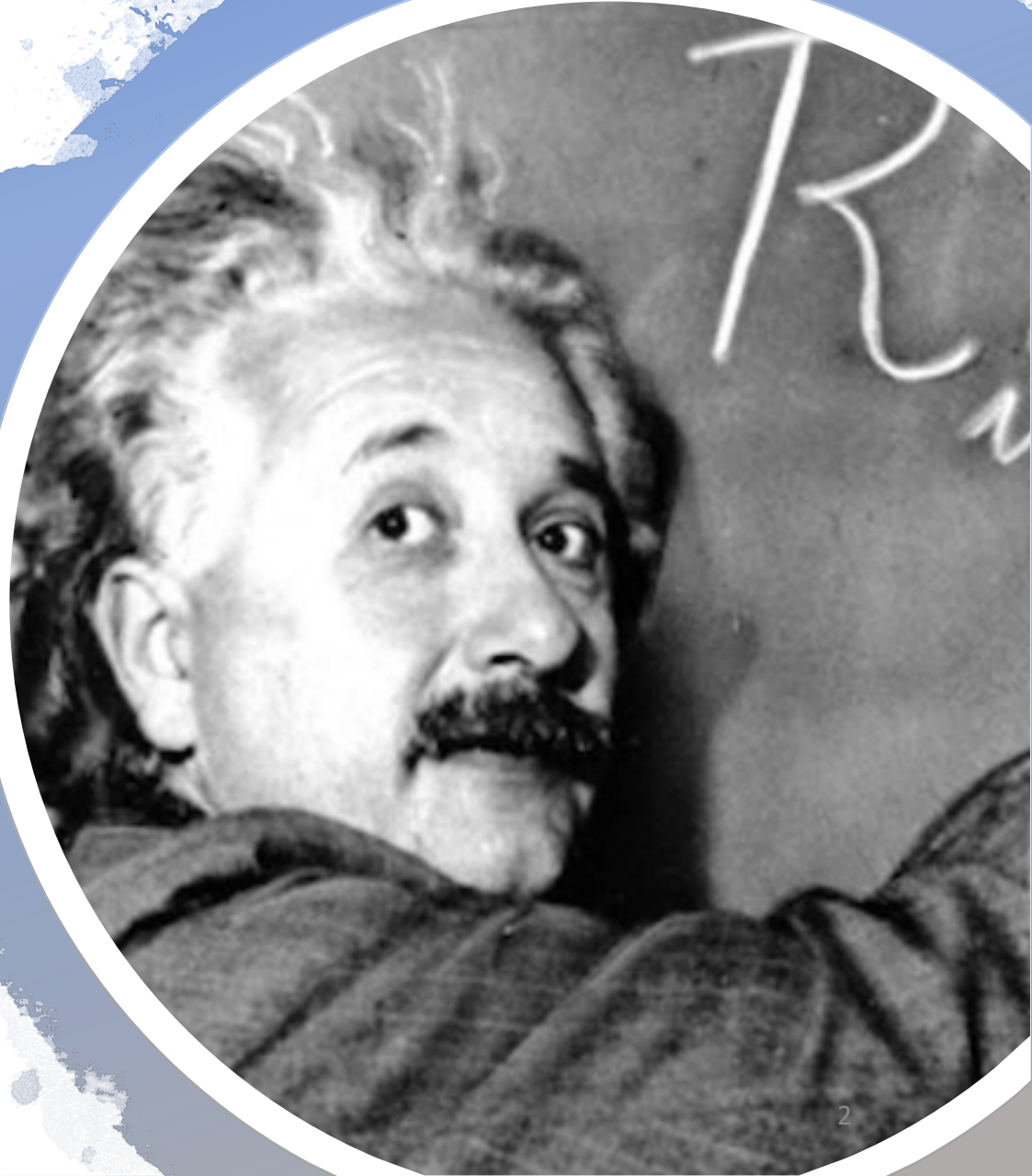
(February 17, 2022)

**Conventional / Extended Air Activated Sludge**

(March 31, 2022)

**Transitioning from Permit Compliance to  
Wastewater Excellence**

(April 28, 2022)



**TODAY**

# ***Optimizing Nutrient Removal in Oxidation Ditches***

## **Review**

Biological Nutrient Removal

    Nitrogen Removal

    Phosphorus Removal

Oxidation Ditch Design Concepts

## **Case Studies**

Wastewater treatment plants operating differently than designed to improve N&P removal

    Cookeville, Tennessee

    Chinook, Montana

    Great Bend, Kansas

    Oneida, Tennessee

    Basehor, Kansas

## **Discussion**



**KEEP  
CALM  
AND  
BLAME  
ME FOR EVERYTHING**

## Acknowledgements

**BASEHOR, KANSAS** Gene Myracle, Jr.

**CHINOOK, MONTANA** Eric Miller & Cory Fox

**COOKEVILLE, TENNESSEE** Ronnie Kelly, Tom Graham & John Buford

**GREAT BEND, KANSAS** Jason Cauley, Reuben Martin, April Batts & James Gaunt

**ONEIDA, TENNESSEE** Greg Burchfield, Chad McDowell & Greg Overton

**EPA** Peter Bahor, Laura Paradise, Paul Shriner & Tony Tripp (**HQ**), Brendon Held & Craig Hesterlee (**R4**), Andrea Schaller & Sydney Weiss (**R5**), Tina Laidlaw (**R8**),

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7

**N**

**Nitrogen**

## ***Step 1: Convert Ammonia ( $\text{NH}_4$ ) to Nitrate ( $\text{NO}_3$ )***

Oxygen-rich Aerobic Process

Don't need BOD for bacteria to grow

Bacteria are sensitive to pH and temperature

## ***Step 2: Convert Nitrate ( $\text{NO}_3$ ) to Nitrogen Gas ( $\text{N}_2$ )***

Oxygen-poor Anoxic Process

Do need BOD for bacteria to grow

Bacteria are hardy





# Ammonia Removal - 1<sup>st</sup> Step of N Removal

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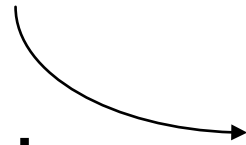
# Ammonia Removal

Ammonia ( $\text{NH}_4$ ) is converted to Nitrate ( $\text{NO}_3$ )

Ammonia  
( $\text{NH}_4$ )

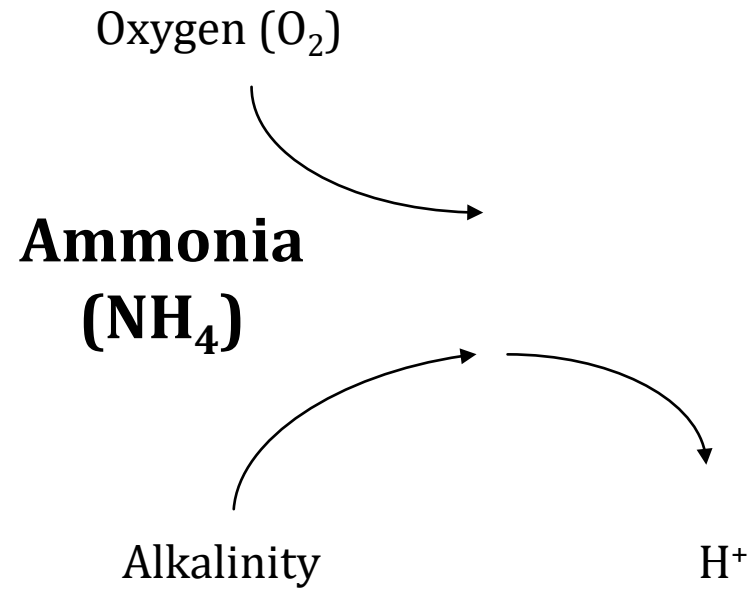
# Ammonia Removal

Oxygen ( $O_2$ )



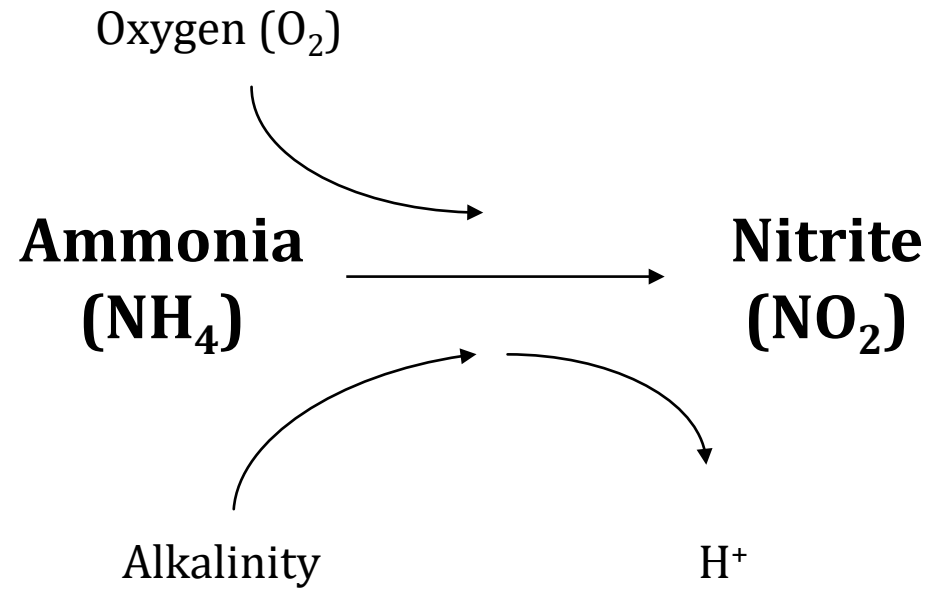
**Ammonia**  
**( $NH_4$ )**

# Ammonia Removal

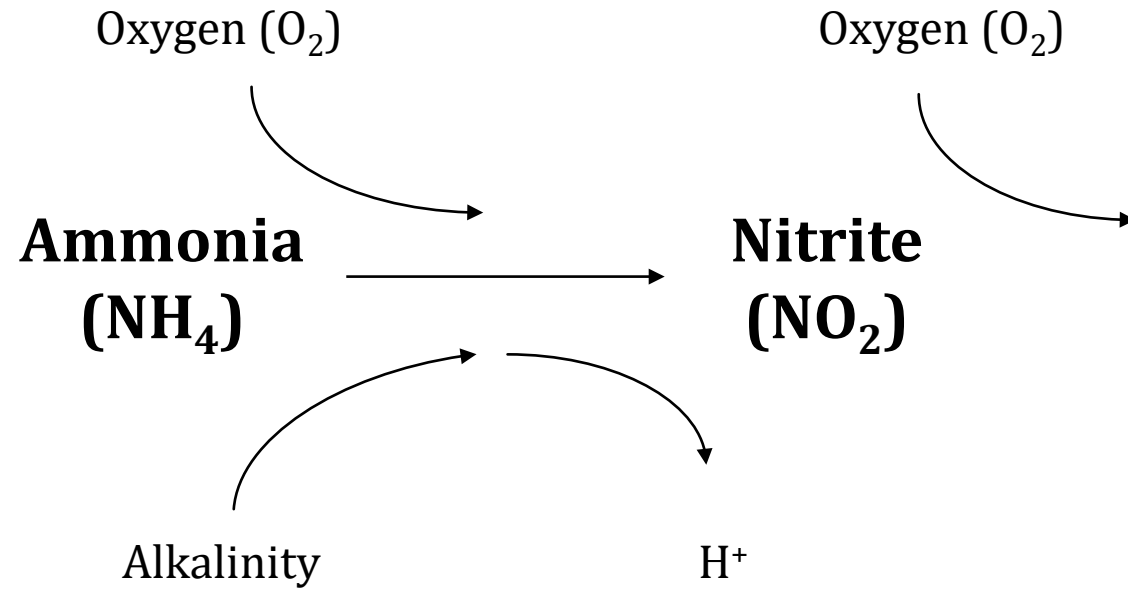




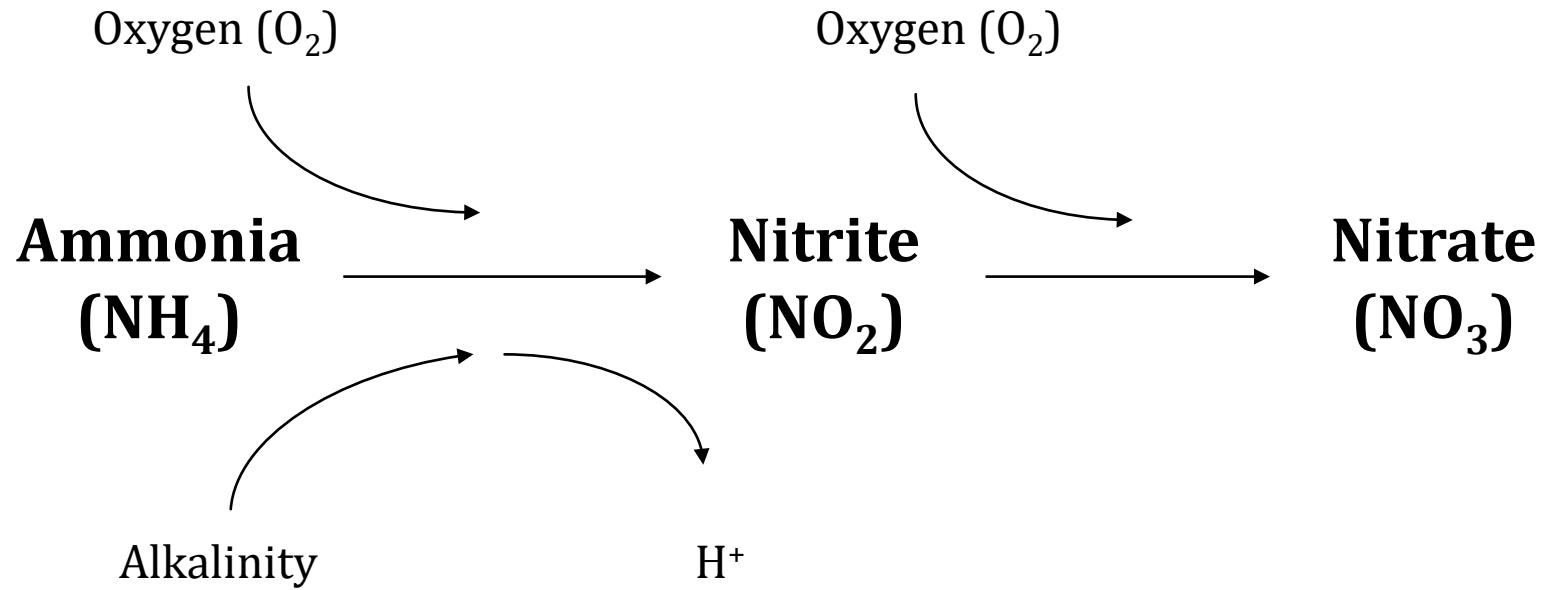
# Ammonia Removal



# Ammonia Removal



# Ammonia Removal



Nitrate  
Removal - 2<sup>nd</sup>  
Step of N  
removal



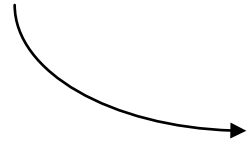


# Nitrate Removal

Nitrate  
(NO<sub>3</sub>)

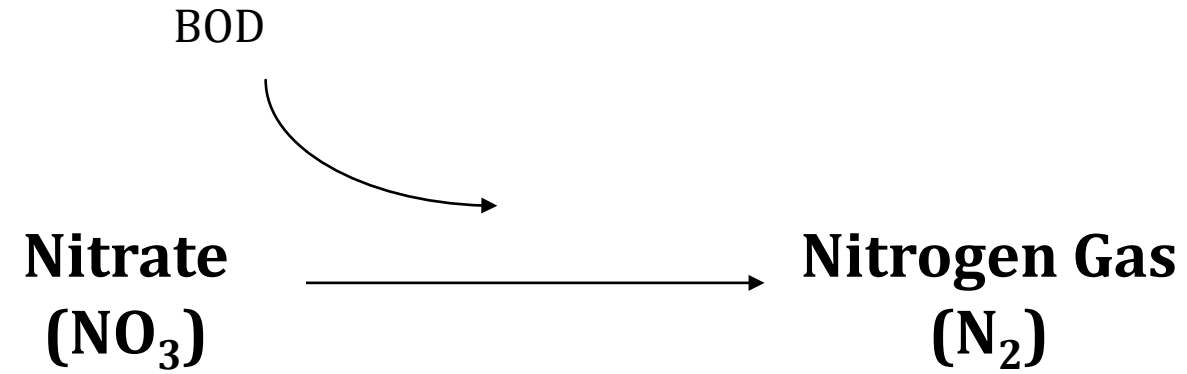
# Nitrate Removal

BOD

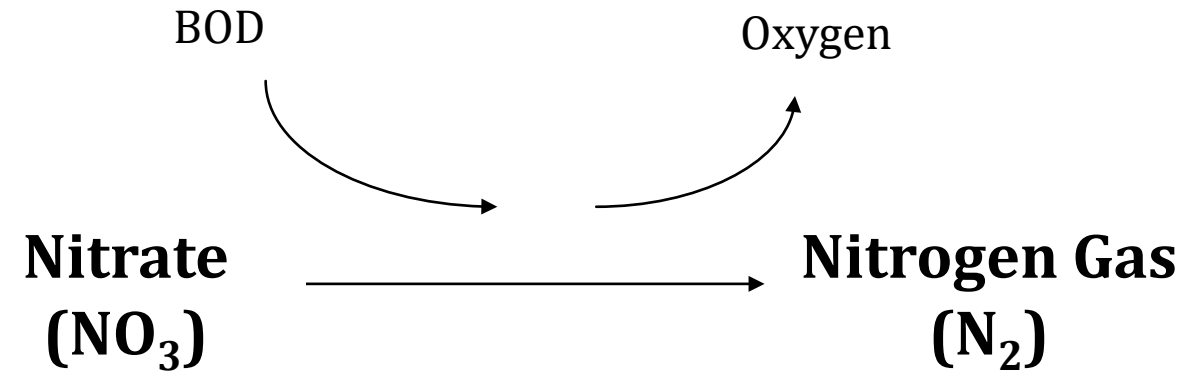


**Nitrate**  
**(NO<sub>3</sub>)**

# Nitrate Removal

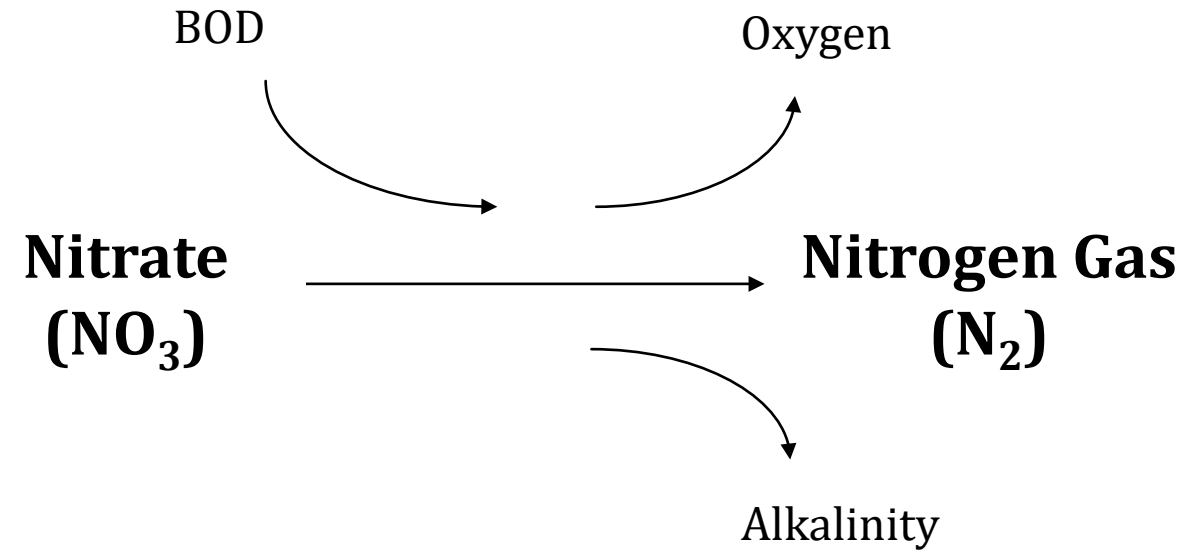


# Nitrate Removal





# Nitrate Removal



Questions?

Comments?





Phosphorus

15

P

30.974

# ***Phosphorus Removal: What an Operator needs to know***

ONE. Convert soluble phosphorus to TSS (total suspended solids)...

Biologically

Chemically

TWO. Remove TSS





# ***Biological Phosphorus Removal***

## Step 1: prepare “dinner”

VFA (volatile fatty acids) production in septic conditions

## Step 2: “eat”

Bio-P bugs (PAOs, “phosphate accumulating organisms”) eat VFAs in septic conditions ... temporarily releasing more phosphorus into the water

## Step 3: “breathe” and grow

In oxygen-rich conditions, bio-P bugs (PAOs) take in almost all of the soluble phosphorus as they reproduce and grow

Questions?

Comments?

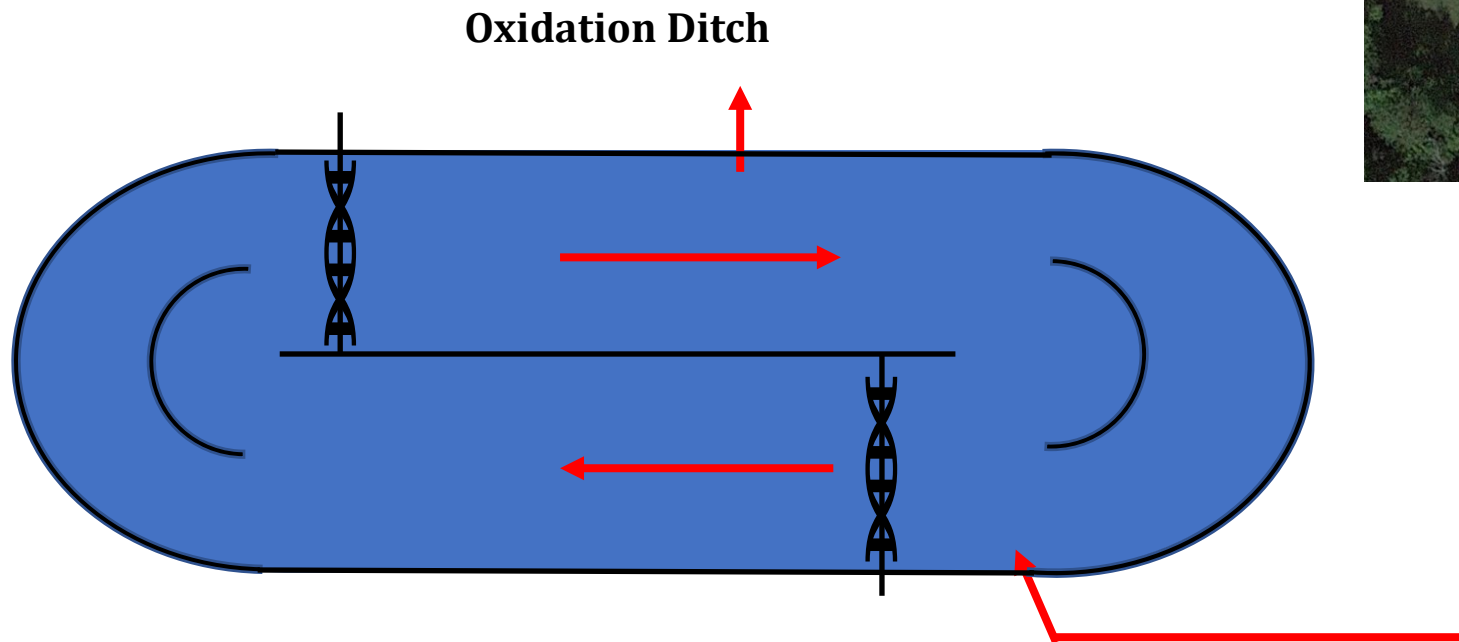






Oxidation Ditches Designed for  
Neither Nitrogen Removal nor  
Phosphorus Removal

# *Oxidation Ditch with no Anoxic Zone and no Anaerobic Zone*



**Oxidation Ditch:**  
BOD and Ammonia removal (Nitrification)

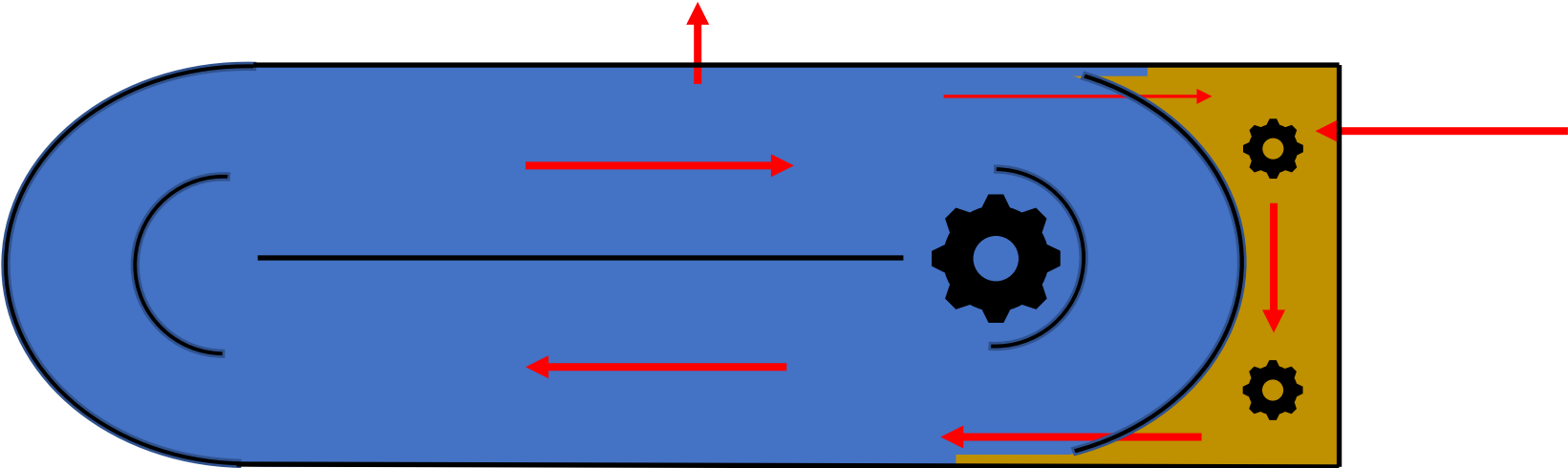


Oxidation Ditches Designed for  
Nitrogen Removal but not for  
Phosphorus Removal

***Oxidation Ditch with Anoxic Zone***

**Anoxic Zone:**  
Nitrate removal (Denitrification)

**Oxidation Ditch:**  
BOD and Ammonia removal (Nitrification)



**Oxidation Ditch**

**Anoxic Zone**

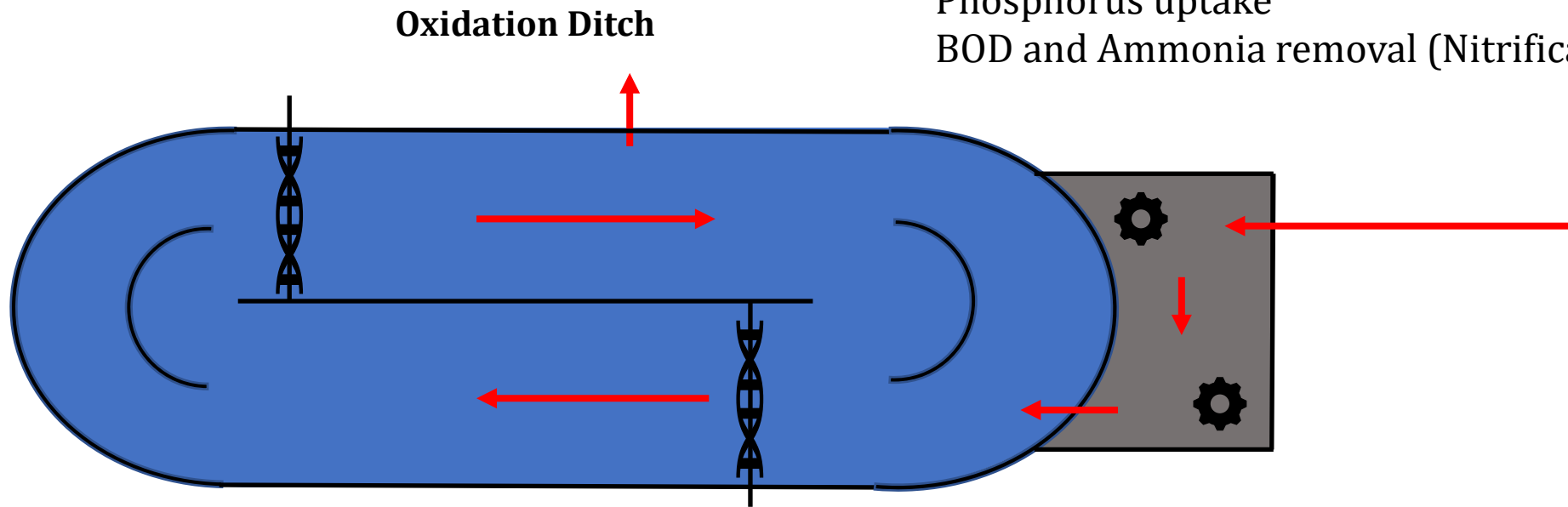
# 3

Oxidation Ditches Designed for  
Phosphorus Removal but not  
Nitrogen Removal

# *Oxidation Ditch with Anaerobic Zone*

**Anaerobic Zone:**  
VFA production / VFA uptake / Phosphorus release

**Oxidation Ditch:**  
Phosphorus uptake  
BOD and Ammonia removal (Nitrification)





Oxidation Ditches Designed to  
Remove both Nitrogen and  
Phosphorus

# *Oxidation Ditch with Anaerobic and Anoxic Zones*

## **Anaerobic Zone:**

VFA production / VFA uptake / Phosphorus release

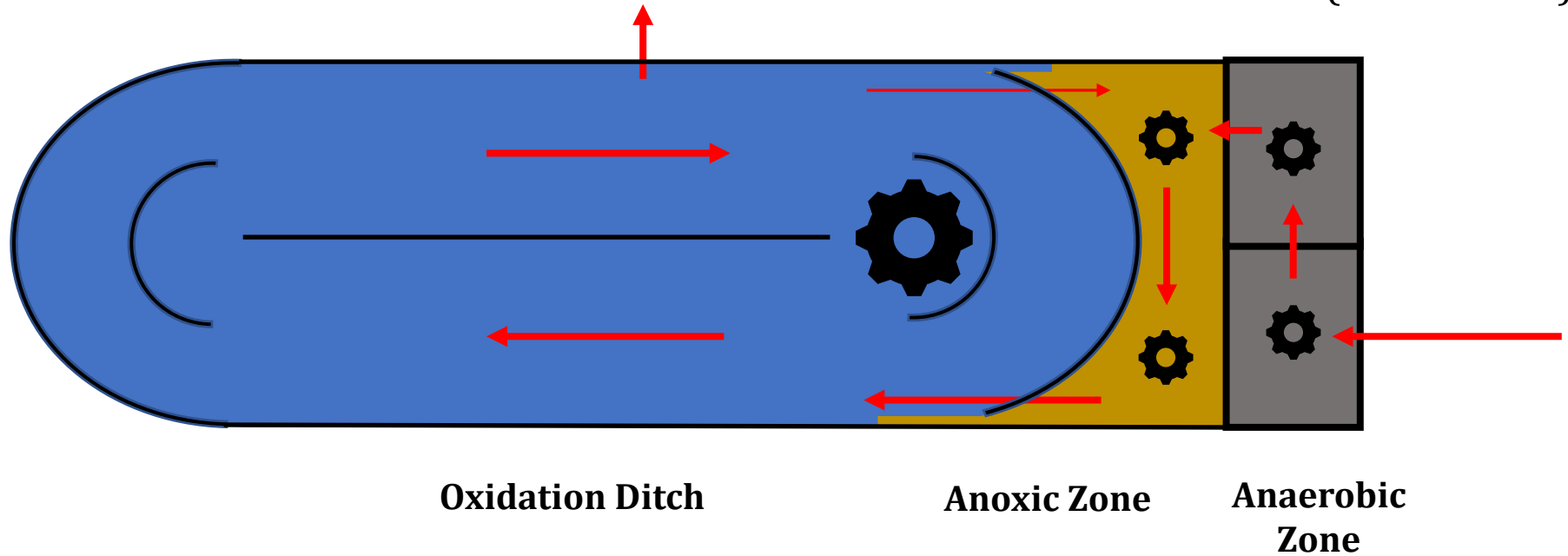
## **Anoxic Zone:**

Nitrate removal (Denitrification)

## **Oxidation Ditch:**

Phosphorus uptake

BOD and Ammonia removal (Nitrification)





## *Orbal Oxidation Ditch*



Questions?

Comments?





7

**N**

**Nitrogen**

# ***Options for Optimizing Nitrogen Removal in Oxidation Ditches***

## **1. Create Zones**

Oxygen-rich aerobic zone(s) for ammonia conversion to nitrate

Oxygen-poor anoxic zone(s) for nitrate conversion to nitrogen gas

## **2. Cycle Air On & Off**

Aerate long enough to convert ammonia to nitrate

Air-off long enough to convert nitrate to nitrogen gas

# ***Options for Optimizing Nitrogen Removal in Oxidation Ditches***

## **1. Create Zones**

Oxygen-rich aerobic zone(s) for ammonia conversion to nitrate

Oxygen-poor anoxic zone(s) for nitrate conversion to nitrogen gas

## **2. Cycle Air On & Off**

Aerate long enough to convert ammonia to nitrate

Air-off long enough to convert nitrate to nitrogen gas





Cookeville, Tennessee

Population: 33,500

15 MGD design flow





Cookeville





Cookeville, Tennessee





Cookeville, Tennessee





Cookeville, Tennessee





Cookeville, Tennessee





Cookeville, Tennessee

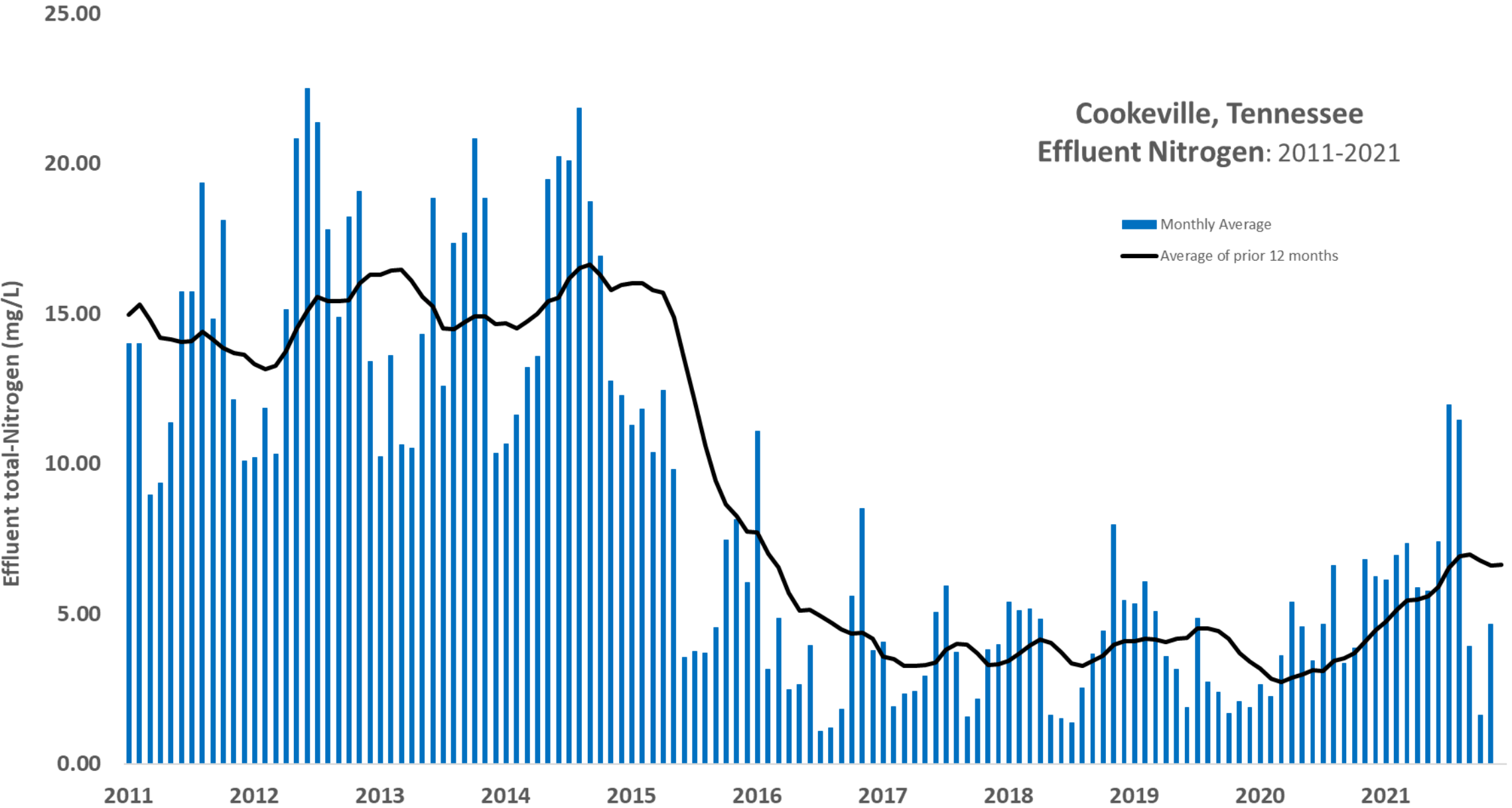




Cookeville, Tennessee

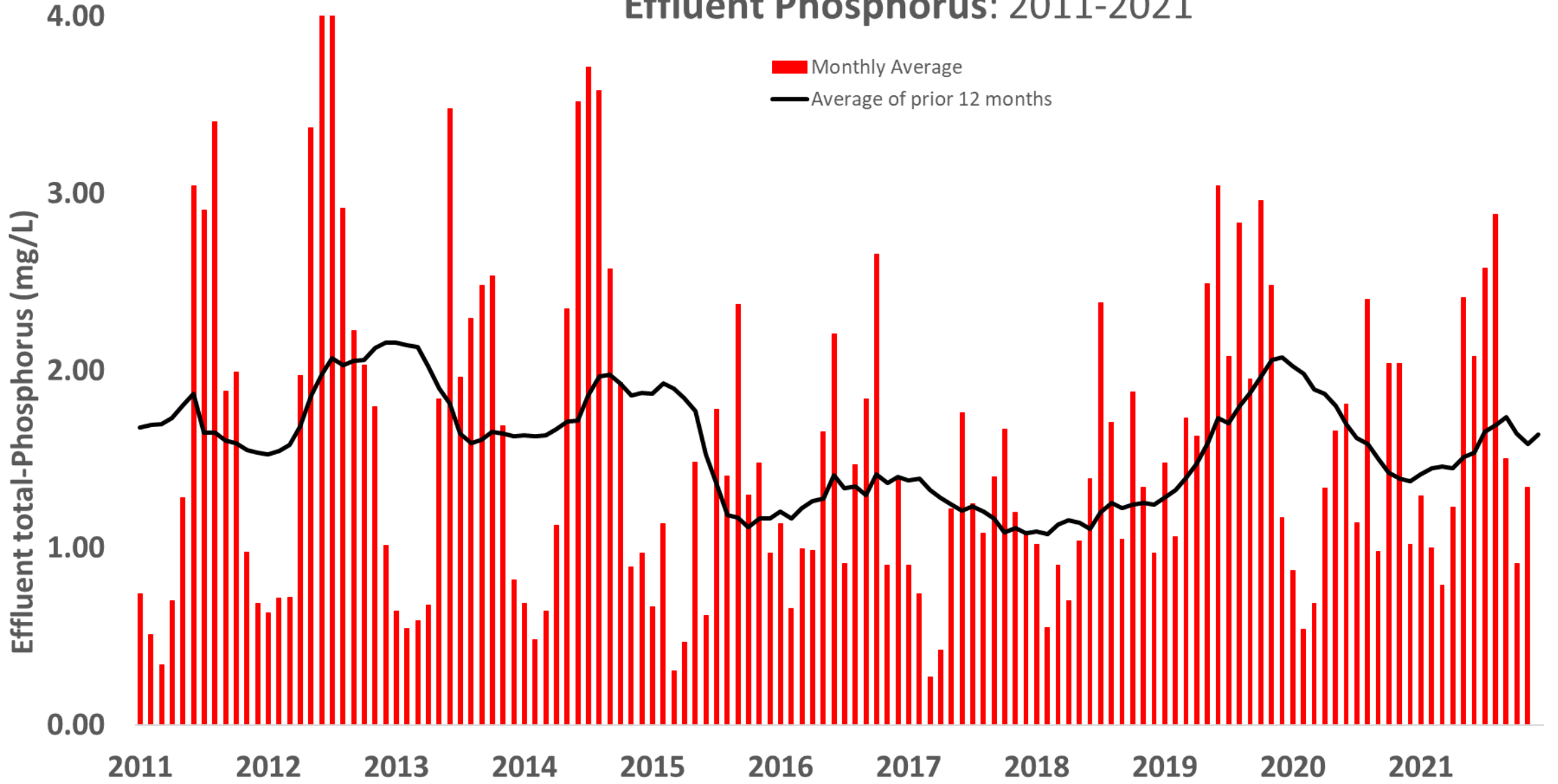


### Cookeville, Tennessee Effluent Nitrogen: 2011-2021



# Cookeville, Tennessee

## Effluent Phosphorus: 2011-2021





# ***Cookeville, Tennessee***

## **Nitrogen**

Now: 5.5 mg/L

Was: 15 mg/L

## **Phosphorus**

Little to no change: 1.5 mg/L

## **Sustainable**

No new construction

Less electricity is used

## **Ratepayer savings**

\$10,000 investment in aeration timers and in-house lab equipment

\$250,000 per year electrical savings

\$4+ million facility upgrade no longer necessary

Questions?

Comments?

# ***Options for Optimizing Nitrogen Removal in Oxidation Ditches***

## **1. Create Zones**

Oxygen-rich aerobic zone(s) for ammonia conversion to nitrate

Oxygen-poor anoxic zone(s) for nitrate conversion to nitrogen gas

## **2. Cycle Air On & Off**

Aerate long enough to convert ammonia to nitrate

Air-off long enough to convert nitrate to nitrogen gas





Chinook, Montana

Population: 1,250

0.5 MGD design flow



**Chinook, Montana**



River



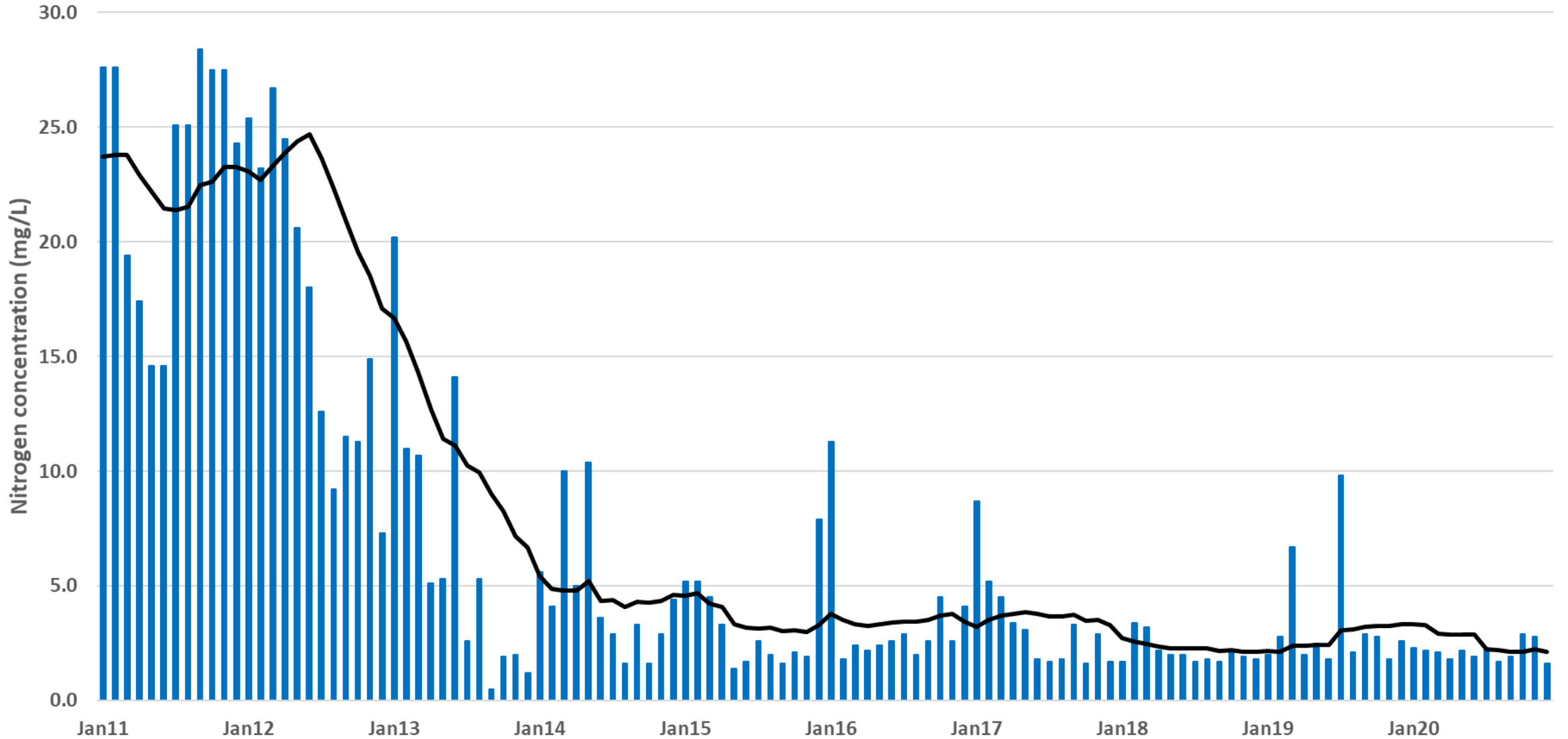
**Chinook, Montana**





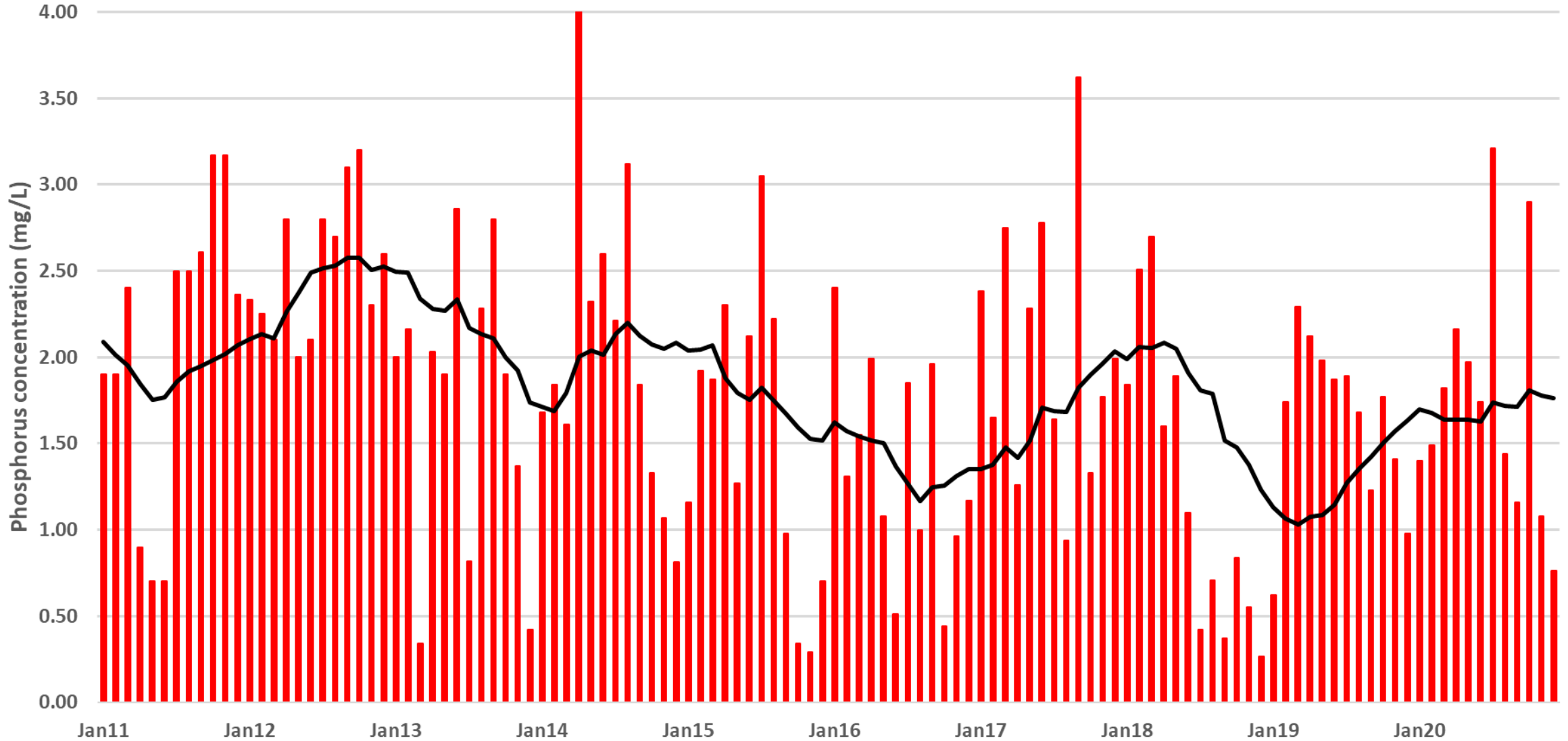
# Effluent total-Nitrogen (mg/L) Chinook, Montana

Monthly average tN    Rolling AVG tN



# Effluent total-Phosphorus (mg/L) Chinook, Montana

total-P Rolling 12-mo AVG



# ***Chinook, Montana***

## **Nitrogen**

Now: 3 mg/L

Was: 20+ mg/L

## **Phosphorus**

Now: 1.5 mg/L

Was: 2.0+ mg/L

## **Sustainable**

No new construction

Less electricity is used

## **Ratepayer savings**

\$15,000 investment in in-line instruments and SCADA programming

Electrical savings

Reduced scope of facility upgrade

Questions?

Comments?





Phosphorus

15

P

30.974



# ***Options for Optimizing Phosphorus Removal in Oxidation Ditches***

## **1. Create Zones**

A. Septic conditions ahead of ditch to ...

create the “food” that bio-P bugs “eat” ... that is, VFA (volatile fatty acid) formation

bio-P bugs living in the MLSS (mixed liquor suspended solids) “eat” the VFAs ... the bio-P bugs being PAOs, phosphate accumulating organisms

B. Followed by aerobic zone(s) in main body of ditch for for luxury uptake by energized bio-P bugs

## **2. Create Sludge Blankets in Ditch During Air Off cycles**

Allow mixed liquor to settle during the air-off cycle and make the air-off cycles long enough for the settled sludge to go septic enough to create VFAs

When resuspended, energized bio-P bugs will pull phosphorus out of solution

## **3. Sidestream P Removal**

Create a septic conditions in sludge holding tank and return approximately 10% of the waste sludge back into the oxidation ditch

# ***Options for Optimizing Phosphorus Removal in Oxidation Ditches***

## **1. Create Zones**

A. Septic conditions ahead of ditch to ...

- i. create the “food” that bio-P bugs “eat” ... that is, VFA (volatile fatty acid) formation
- ii. bio-P bugs living in the MLSS (mixed liquor suspended solids) “eat” the VFAs ... the bio-P bugs being PAOs, phosphate accumulating organisms

B. Followed by aerobic zone(s) in main body of ditch for for luxury uptake by energized bio-P bugs



Great Bend, Kansas

Population: 13,400

3.6 MGD design flow



# *Great Bend, Kansas*

## **Nitrogen Removal in Ditch**

**Rotor equipped with VFD and controlled by in-tank DO probe**

**Ammonia → Nitrate**

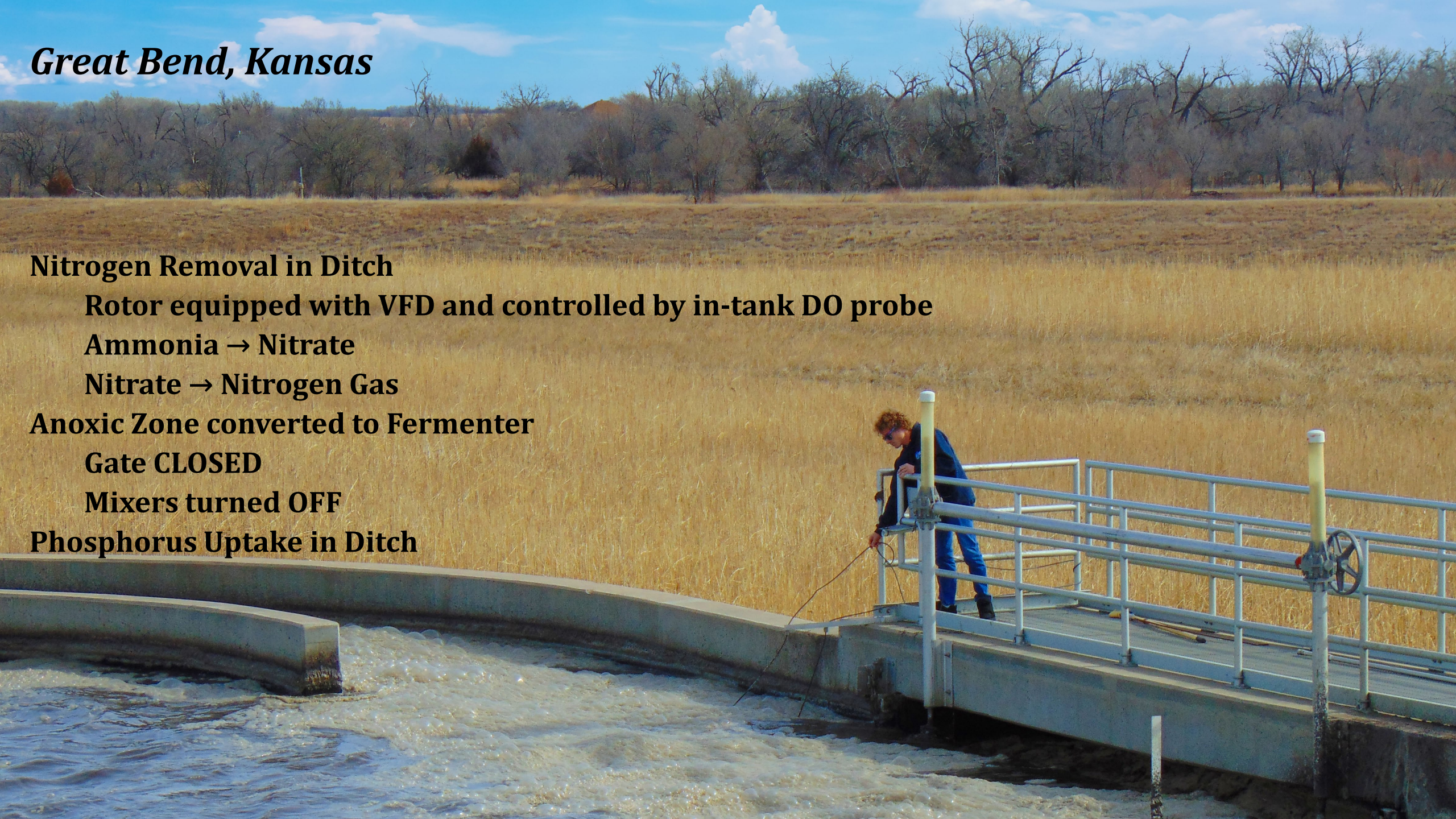
**Nitrate → Nitrogen Gas**

**Anoxic Zone converted to Fermenter**

**Gate CLOSED**

**Mixers turned OFF**

**Phosphorus Uptake in Ditch**





# Great Bend, KS

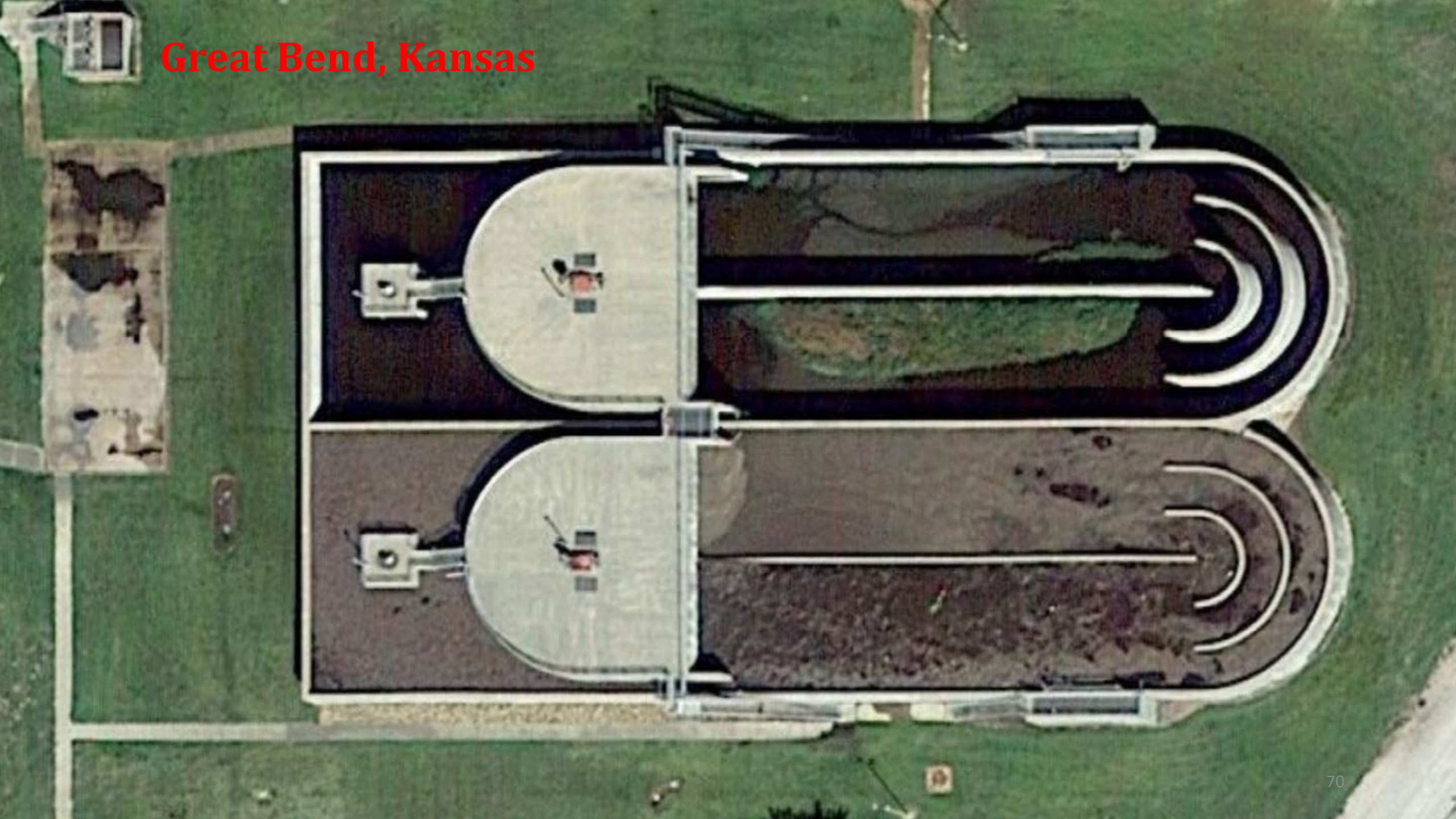


2nd St

Great Bend  
Sewage Treatment

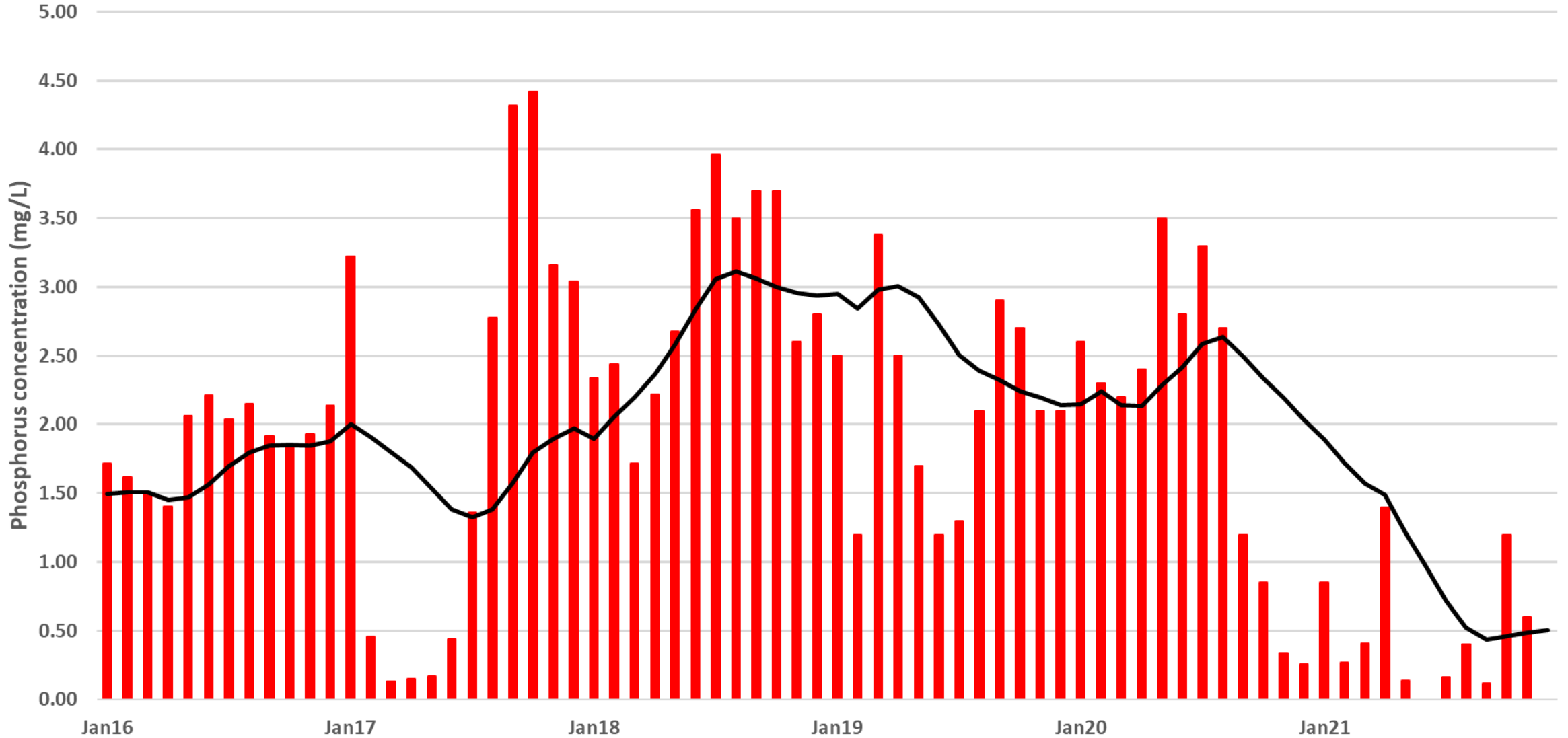


**Great Bend, Kansas**



# Effluent total-Phosphorus Great Bend, Kansas

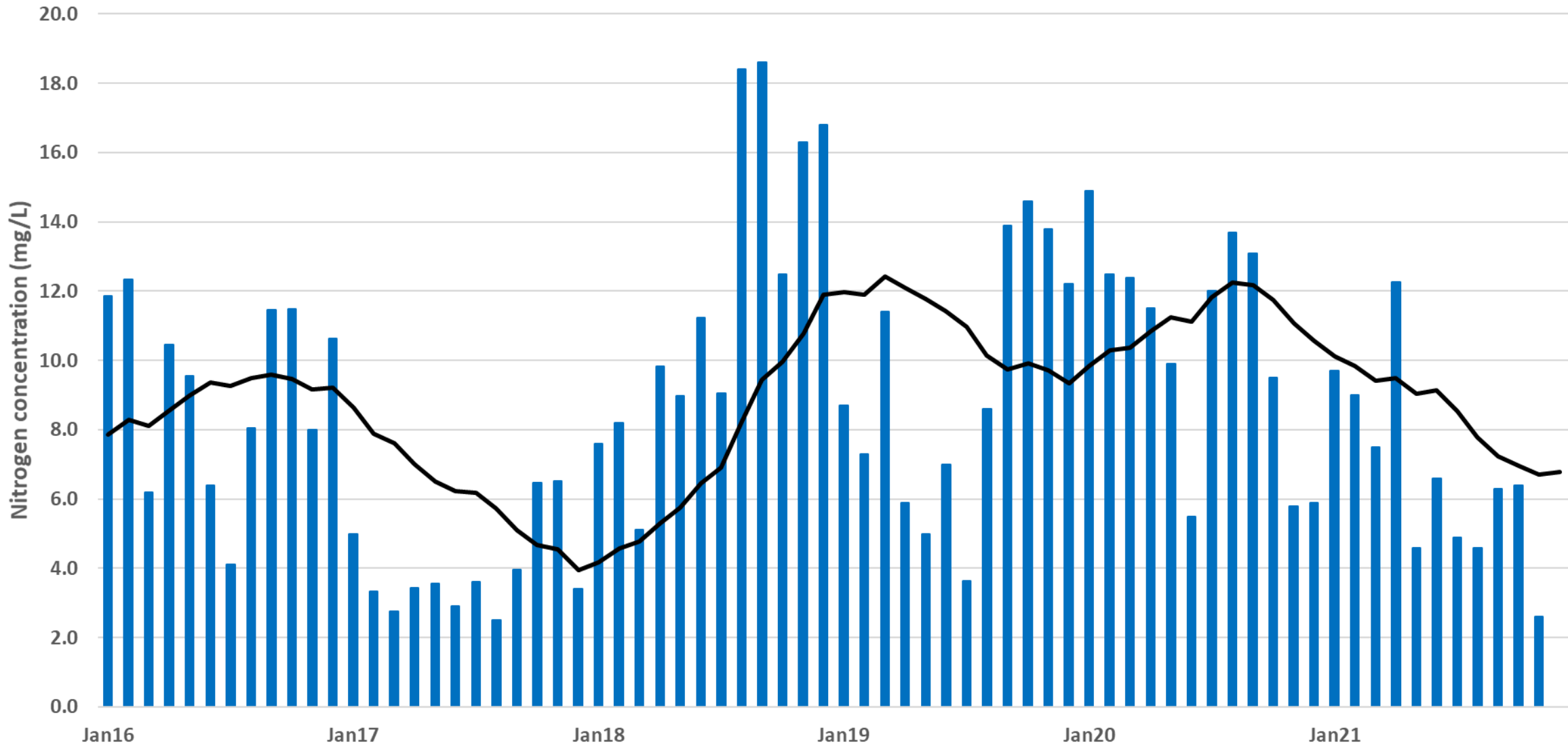
total-P Rolling 12-mo AVG





# Effluent total-Nitrogen Great Bend, Kansas

Monthly average tN    Rolling AVG tN



# *Great Bend, Kansas*

## **Phosphorus**

Now: 0.5 mg/L

Was: 2+ mg/L

## **Nitrogen**

Now: 6 mg/L

Was: 10+ mg/L

## **Sustainable**

No new construction

Less electricity is used

## **Ratepayer savings**

\$50,000 investment in VFD, in-line DO, and SCADA

Electrical savings

\$6 million facility upgrade no longer necessary

Questions?

Comments?



# ***Options for Optimizing Phosphorus Removal in Oxidation Ditches***

## **1. Create Zones**

A. Septic conditions ahead of ditch to ...

- i. create the “food” that bio-P bugs “eat” ... that is, VFA (volatile fatty acid) formation
- ii. bio-P bugs living in the MLSS (mixed liquor suspended solids) “eat” the VFAs ... the bio-P bugs being PAOs, phosphate accumulating organisms

B. Followed by aerobic zone(s) in main body of ditch for for luxury uptake by energized bio-P bugs

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Allow mixed liquor to settle during the air-off cycle and make the air-off cycles long enough for the settled sludge to go septic enough to create VFAs

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Create a septic conditions in sludge holding tank and return approximately 10% of the waste sludge back into the oxidation ditch



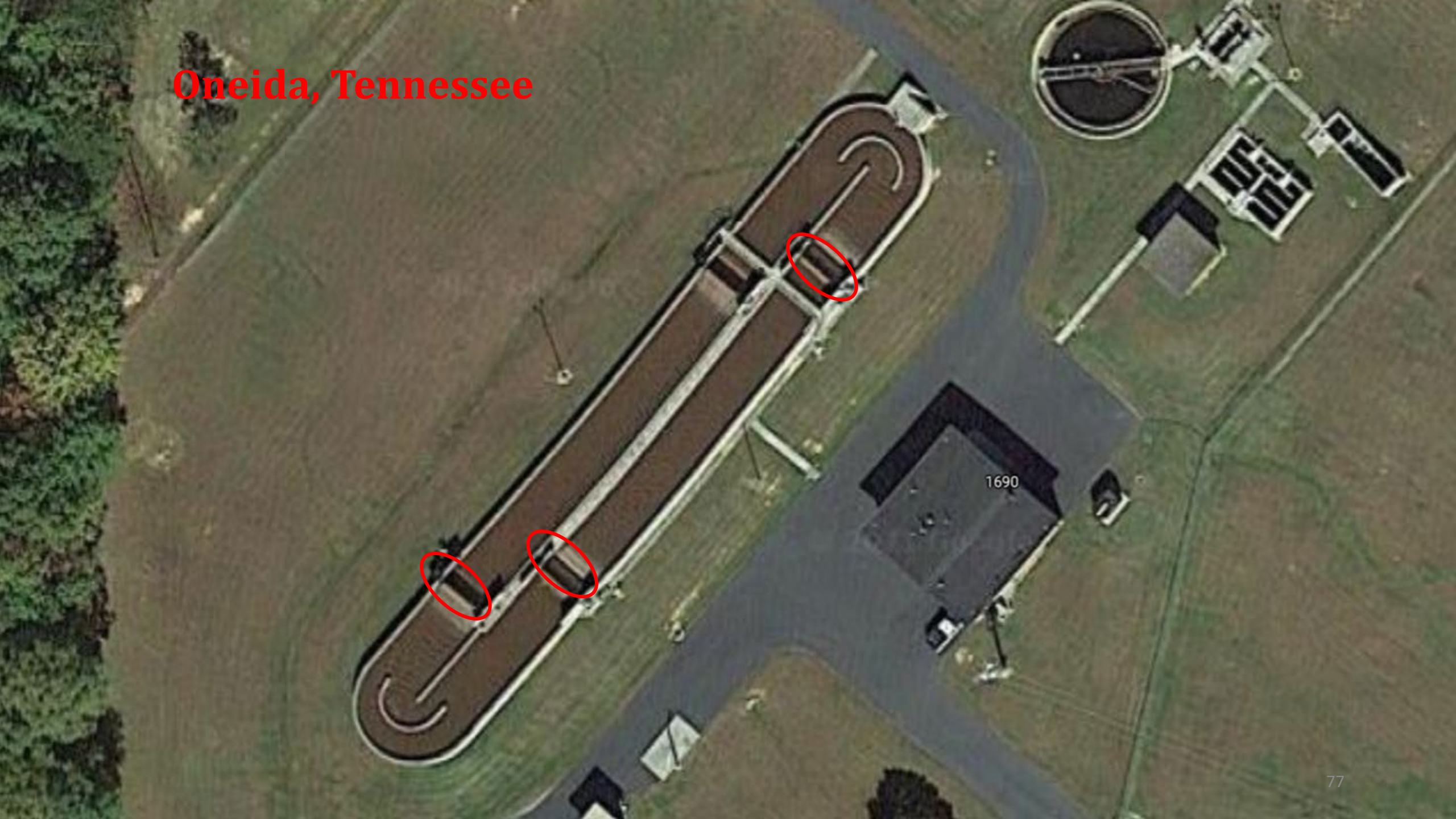
Oneida, Tennessee

Population: 3,700

0.998 MGD design flow



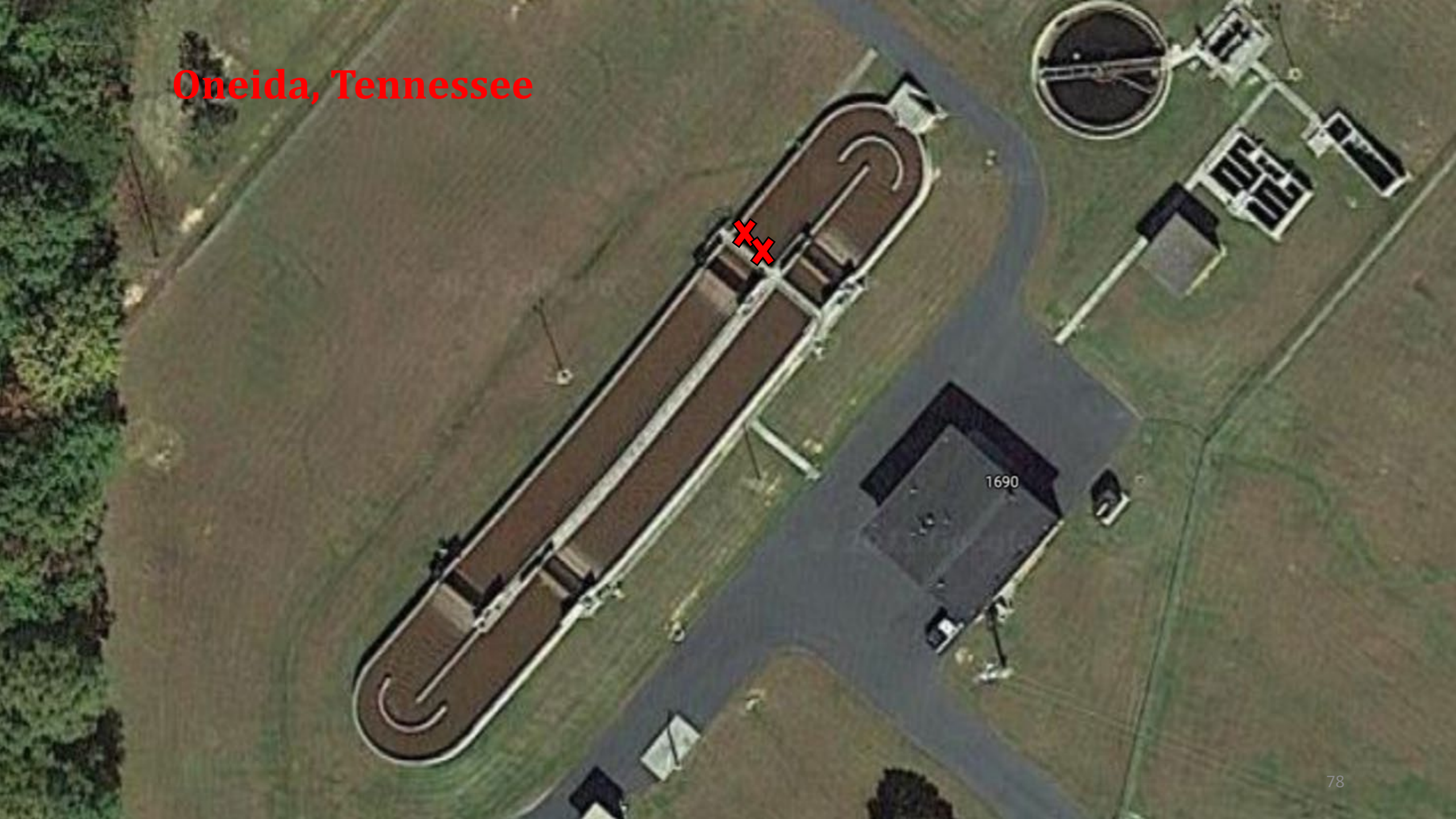
**Oneida, Tennessee**



1690



**Oneida, Tennessee**

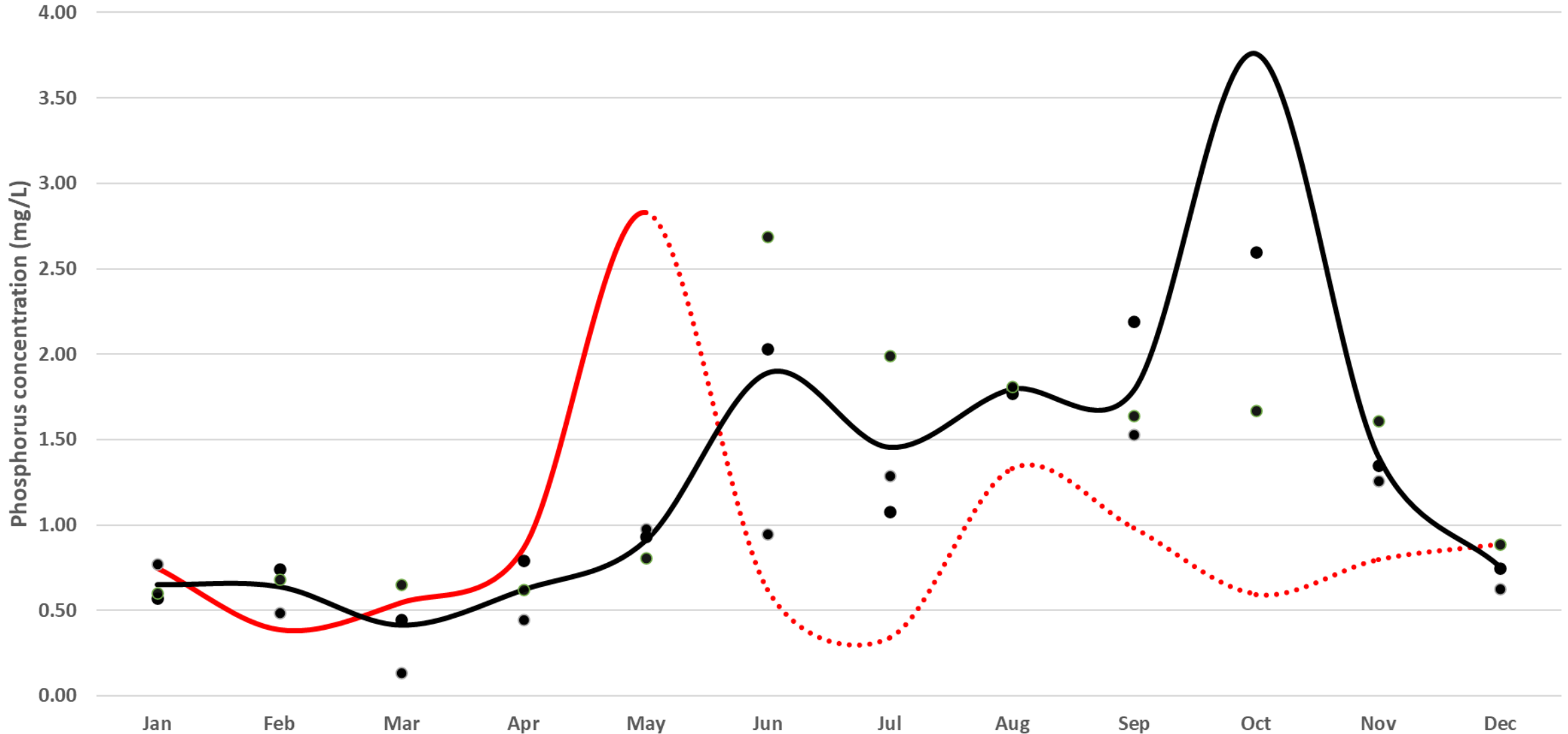


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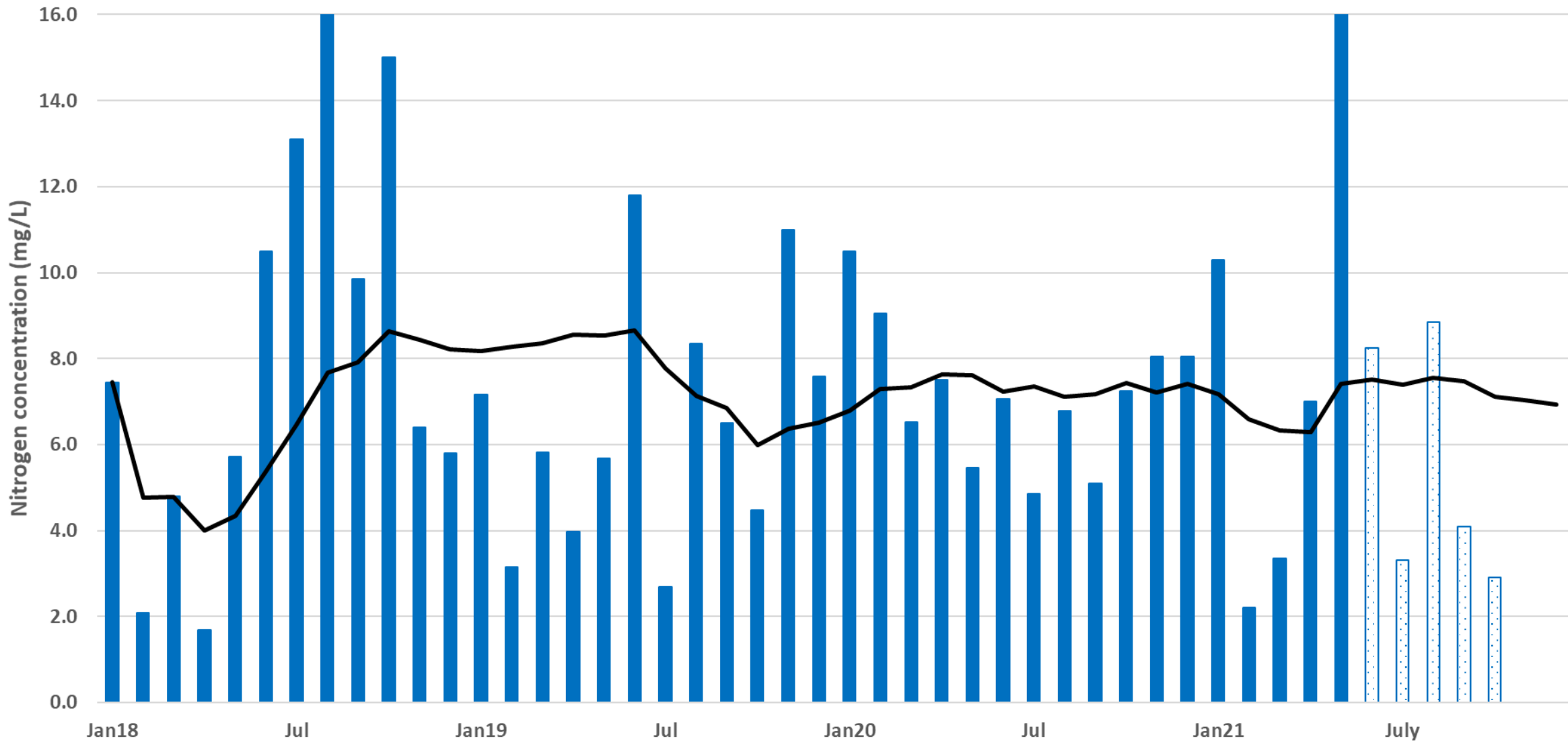
# Effluent total-Phosphorus Oneida, Tennessee

● 2018 ● 2019 ● 2020 — 2021 — 2018-2020 average



# Effluent total-Nitrogen Oneida, Tennessee

Monthly average tN    Rolling AVG tN





# *Oneida, Tennessee*

## **Nitrogen**

Now: 8 mg/L

## **Phosphorus**

Now: summer peaks of less than 1.5 mg/L

Was: summer peaks of more than 3.0 mg/L

## **Sustainable**

No new construction

Less electricity is used

## **Ratepayer savings**

Electrical savings

Unlikely that a facility upgrade will be required





**TrickedOut**







Basehor, Kansas

Population: 6,000

1.12 MGD design flow



N 158th St



202

WATER  
TREATMENT  
PLANT



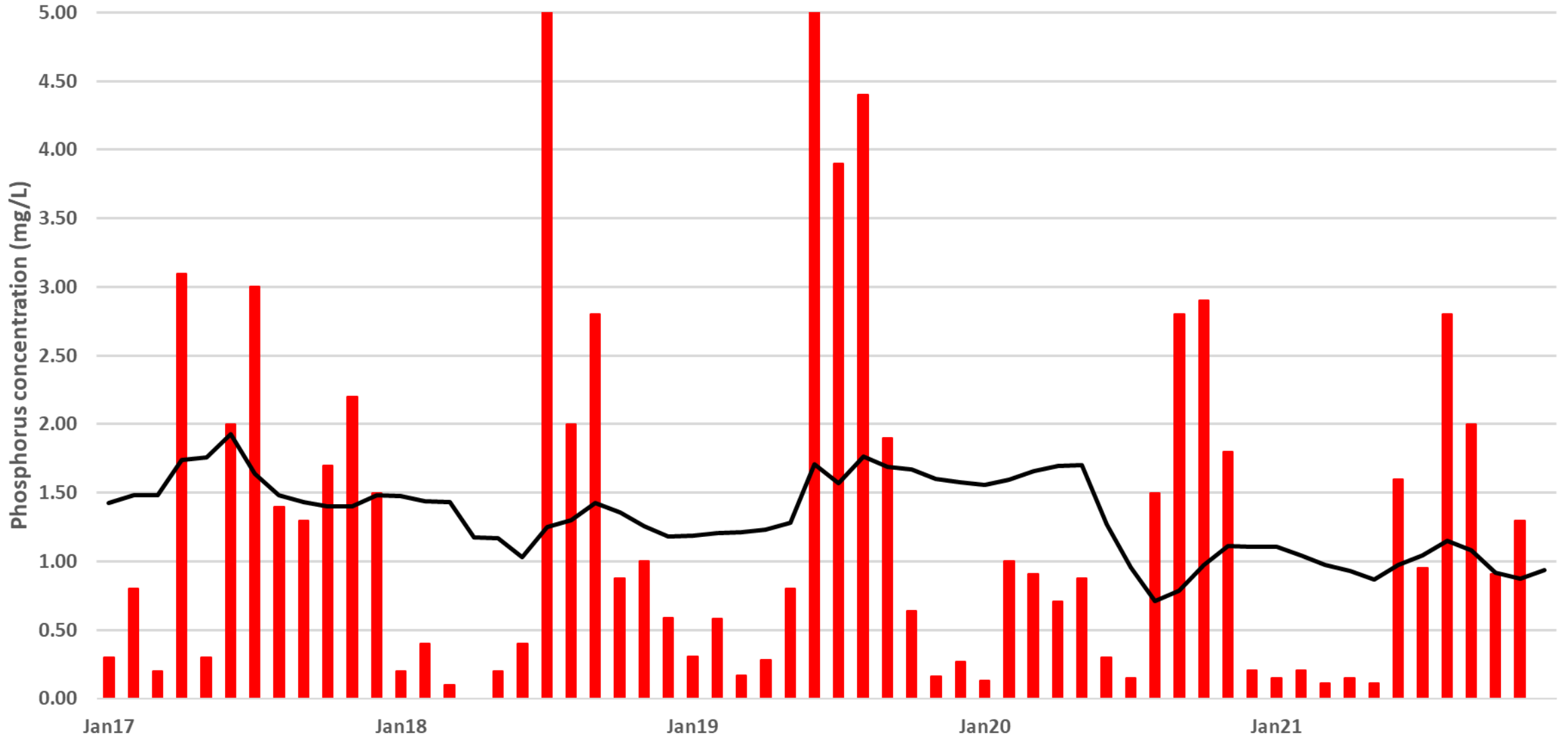


N 158th St



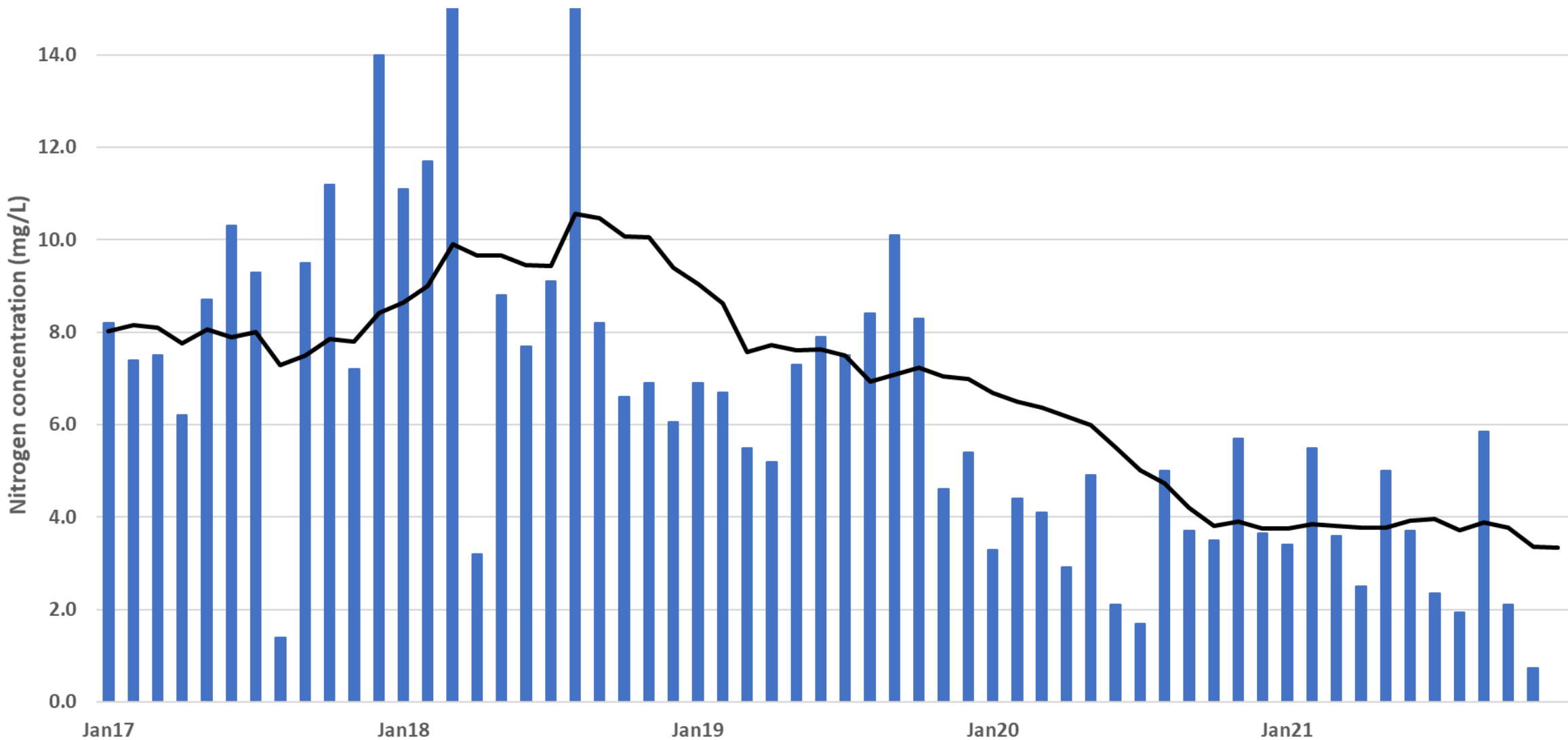
# Effluent total-Phosphorus Basehor, Kansas

Monthly Average    Rolling 12-mo AVG



# Effluent total-Nitrogen Basehor, Kansas

Monthly average tN    Rolling AVG tN



# ***Basehor, Kansas***

## **Nitrogen**

Now: 4 mg/L

Was: 8 mg/L

## **Phosphorus**

Now: 1.0 mg/L with summer peaks less than 3 mg/L

Was: 1.5 mg/L with summer peaks more than 3 mg/L

## **Sustainable**

No new construction

DO control in aeration basin

Less mixing of anoxic and anaerobic tanks

## **Ratepayer savings**

Electrical savings from less mixing

Possible elimination of near-term facility upgrade





## ***Optimizing Nutrient Removal & Wastewater Excellence***

### ***Optimizing Nutrient Removal***

February 17: Optimizing Nutrient Removal in SBRs

March 31: Optimizing Nutrient Removal in Conventional and Extended Aeration Activated Sludge wwtps

### ***Wastewater Excellence***

April 28: Transitioning from Permit Compliance to Wastewater Excellence

Comments &  
Questions

