

2.2 Sewage Sludge Incineration

There are approximately 170 sewage sludge incineration (SSI) plants units from 86 facilities in operation in the United States. Three main types of incinerators are used:- multiple hearth, fluidized bed, and electric infrared. Some sludge is co-fired with municipal solid waste in combustors based on refuse combustion technology (see Section 2.1). Refuse co-fired with sludge in combustors based on sludge incinerating technology is limited to multiple hearth incinerators only.

Over 80 percent of the identified operating sludge incinerators are of the multiple hearth design. About 15 percent are fluidized bed combustors and 3 percent are electric. The remaining combustors co-fire refuse with sludge. Most sludge incinerators are located in the Eastern United States, though there are a significant number on the West Coast. Facilities are located in 24 states and Puerto Rico. New York has the largest number of facilities with 33. Pennsylvania 18. Ohio and Michigan New Jersey have the next-largest numbers of facilities with 211 and 4910 sites, respectively.

~~Sewage sludge incinerator emissions are currently regulated under 40 CFR Part 60, Subpart O and 40 CFR Part 61, Subparts C and E. Subpart O in Part 60 establishes a New Source Performance Standard for particulate matter. Subparts C and E of Part 61 National Emission Standards for Hazardous Air Pollutants (NESHAP) establish emission limits for beryllium and mercury, respectively.~~

In 1989, technical standards for the use and disposal of sewage sludge were proposed as 40 CFR Part 503, under authority of Section 405 of the Clean Water Act. Subpart G of this proposed Part 503 proposes to establish national emission limits for arsenic, beryllium, cadmium, chromium, lead, mercury, nickel, and total hydrocarbons from sewage sludge incinerators. The proposed limits for mercury and beryllium are based on the assumptions used in developing the NESHAPs for these pollutants, and no additional controls were proposed to be required. Carbon monoxide emissions were examined, but no limit was proposed.

~~In 2011, EPA established new source performance standards (NSPS) and emission guidelines (EG), and in 2016 EPA established a federal implementation plan (FIP) for sewage sludge incineration units (SSI) located at wastewater treatment facilities designed to treat domestic sewage sludge. Sewage sludge incineration units (SSI) are regulated under 40 CFR Part 60 subpart LLLL, 40 CFR Part 60 subpart MMMM and 40 CFR Part 62 subpart LLL These final rules set limits for nine pollutants under CAA section 129: cadmium, carbon monoxide, hydrogen chloride, lead, mercury, nitrogen oxides, particulate matter, polychlorinated dibenzo-p-dioxins and polychlorinated dibenzofurans, and sulfur dioxide.~~

2.2.1 Process ~~Description~~^{1,2}Description^{1,2}

~~Types of incineration described in this section include:~~

- Multiple hearth,
- Fluidized bed, and
- Electric.

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Single hearth cyclone, rotary kiln, and wet air oxidation are also briefly discussed.

2.2.1.1 The Source Classification Codes (SCC) for this sector are:

- 50100801 - Waste Disposal; Solid Waste Disposal – Government; Sewage Sludge Incineration; Incinerator
- 50100802 - Waste Disposal; Solid Waste Disposal – Government; Sewage Sludge Incineration; Multiple Hearth Furnaces–Incinerator
- 50100803 - Waste Disposal; Solid Waste Disposal – Government; Sewage Sludge Incineration; Fluidized Bed Combustor
- 50100804 - Waste Disposal; Solid Waste Disposal – Government; Sewage Sludge Incineration; Electric Infrared Incinerator
- 50301101 - Waste Disposal; Solid Waste Disposal – Industrial; Sewage Sludge Incineration; Incinerator
- 50301102 - Waste Disposal; Solid Waste Disposal – Industrial; Sewage Sludge Incineration; Multiple Hearth Incinerator
- 50301103 - Waste Disposal; Solid Waste Disposal – Industrial; Sewage Sludge Incineration; Fluidized Bed Combustor
- 50301104 - Waste Disposal; Solid Waste Disposal – Industrial; Sewage Sludge Incineration; Electric Infrared Incinerator
- 50600701 - Waste Disposal; Solid Waste Disposal – Commercial; Sewage Sludge Incineration; Incinerator
- 50600702 - Waste Disposal; Solid Waste Disposal – Commercial; Sewage Sludge Incineration; Multiple Hearth Incinerator
- 50600703 - Waste Disposal; Solid Waste Disposal – Commercial; Sewage Sludge Incineration; Fluidized Bed Combustor
- 50600704 - Waste Disposal; Solid Waste Disposal – Commercial; Sewage Sludge Incineration; Electric Infrared Incinerator
- 50700701 - Waste Disposal; Solid Waste Disposal – Institutional; Sewage Sludge Incineration; Incinerator
- 50700702 - Waste Disposal; Solid Waste Disposal – Institutional; Sewage Sludge Incineration; Multiple Hearth Incinerator
- 50700703 - Waste Disposal; Solid Waste Disposal – Institutional; Sewage Sludge Incineration; Fluidized Bed Combustor
- 50700704 - Waste Disposal; Solid Waste Disposal – Institutional; Sewage Sludge Incineration; Electric Infrared Incinerator

2.2.1.1 Multiple Hearth Furnaces

The multiple hearth furnace was originally developed for mineral ore roasting nearly a century ago. The air-cooled variation has been used to incinerate sewage sludge since the 1930s. –A cross-sectional diagram of a typical multiple hearth furnace is shown in Figure 2.2-1. –The basic multiple hearth furnace (MHF) is a vertically oriented cylinder.– The outer shell is constructed of steel, lined with refractory, and surrounds a series of horizontal refractory hearths. –A hollow cast iron rotating shaft runs through the center of the hearths. –Cooling air is introduced into the shaft which extend above the hearths.– Each rabble arm is equipped with a number of teeth, approximately 6 inches in length, and spaced about 10 inches apart. –The teeth are shaped to rake the sludge in a spiral motion, alternating in direction from the outside in, to the

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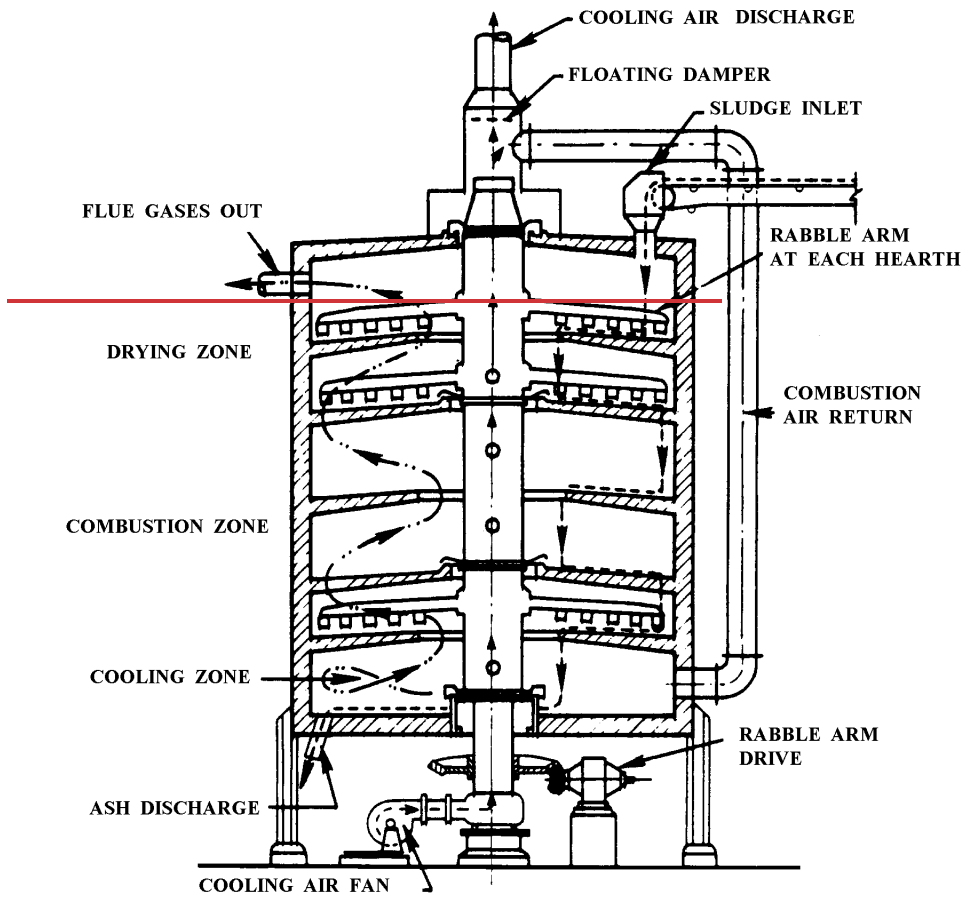


Figure 2.2-1. Cross Section of a Multiple Hearth Furnace

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inside out, between hearths. Typically, the upper and lower hearths are fitted with four rabble arms, and the middle hearths are fitted with two. Burners, providing auxiliary heat, are located in the sidewalls of the hearths.

In most ~~multiple hearth furnaces~~ MHFs, partially dewatered sludge is fed onto the perimeter of the top hearth. The rabble arms move the sludge through the incinerator by raking the sludge toward the center shaft where it drops through holes located at the center of the hearth. In the next hearth the sludge is raked in the opposite direction. This process is repeated in all of the subsequent hearths. The effect of the rabble motion is to break up solid material to allow better surface contact with heat and oxygen. A sludge depth of about 1 inch is maintained in each hearth at the design sludge flow rate.

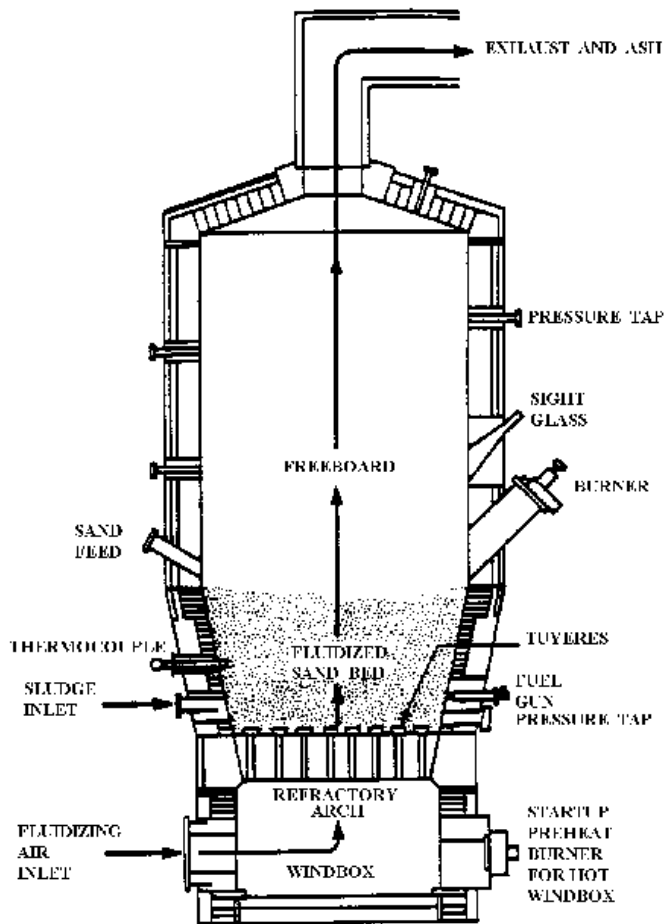
Scum may also be fed to one or more hearths of the incinerator. Scum is the material that floats on wastewater. It is generally composed of vegetable and mineral oils, grease, hair, waxes, fats, and other materials that will float. Scum may be removed from many treatment units including ~~preaeration~~ pre-aeration tanks, skimming tanks, and sedimentation tanks. Quantities of scum are generally small compared to those of other wastewater solids.

Ambient air is first ducted through the central shaft and its associated rabble arms. A portion, or all, of this air is then taken from the top of the shaft and recirculated into the lowermost hearth as preheated combustion air. Shaft cooling air which is not circulated back into the furnace is ducted into the stack downstream of the air pollution control devices. The combustion air flows upward through the drop holes in the hearths, countercurrent to the flow of the sludge, before being exhausted from the top hearth. Air enters the bottom to cool the ash. Provisions are usually made to inject ambient air directly into the middle hearths as well.

From the standpoint of the overall incineration process, ~~multiple hearth furnaces~~ MHFs can be divided into three zones. The upper hearths comprise the drying zone where most of the moisture in the sludge is evaporated. The temperature in the drying zone is typically between 425 and 760°C (800 and 1400°F). Sludge combustion occurs in the middle hearths (second zone) as the temperature is increased to about 925°C (1700°F). The combustion zone can be further subdivided into the upper-middle hearths where the volatile gases and solids are burned, and the lower-middle hearths where most of the fixed carbon is combusted. The third zone, made up of the lowermost hearth(s), is the cooling zone. In this zone the ash is cooled as ~~its~~ heat is transferred to the incoming combustion air.

~~Multiple hearth furnaces~~ MHFs are sometimes operated with afterburners to further reduce odors and concentrations of unburned hydrocarbons. In afterburning, furnace exhaust gases are ducted to a chamber where they are mixed with supplemental fuel and air and completely combusted. Some incinerators have the flexibility to allow sludge to be fed to a lower hearth, thus allowing the upper hearth(s) to function essentially as an afterburner.

Under normal operating condition, 50 to 100 percent excess air must be added to an MHF ~~in order~~ to ensure complete combustion of the sludge. Besides enhancing contact between fuel and oxygen in the furnace, these relatively high rates of excess air are necessary to compensate for normal variations in both the organic characteristics of the sludge feed and the rate at which it enters the incinerator. When an inadequate amount of excess air is available, only partial oxidation of the carbon will occur, with a resultant increase in emissions of carbon monoxide, soot, and hydrocarbons. Too much excess air, on the other hand, can cause increased entrainment of particulate and unnecessarily high auxiliary fuel consumption.



Multiple-hearth furnace (MHF) emissions are usually controlled by a venturi scrubber, an impingement tray scrubber, or a combination of both. Wet cyclones and dry cyclones are also used. Wet electrostatic

Figure 2.2-2. Cross Section of a Fluidized Bed Furnace

precipitators (Wet ESPs) are being installed as retrofits where tighter limits on particulate matter and metals are required by State regulations.

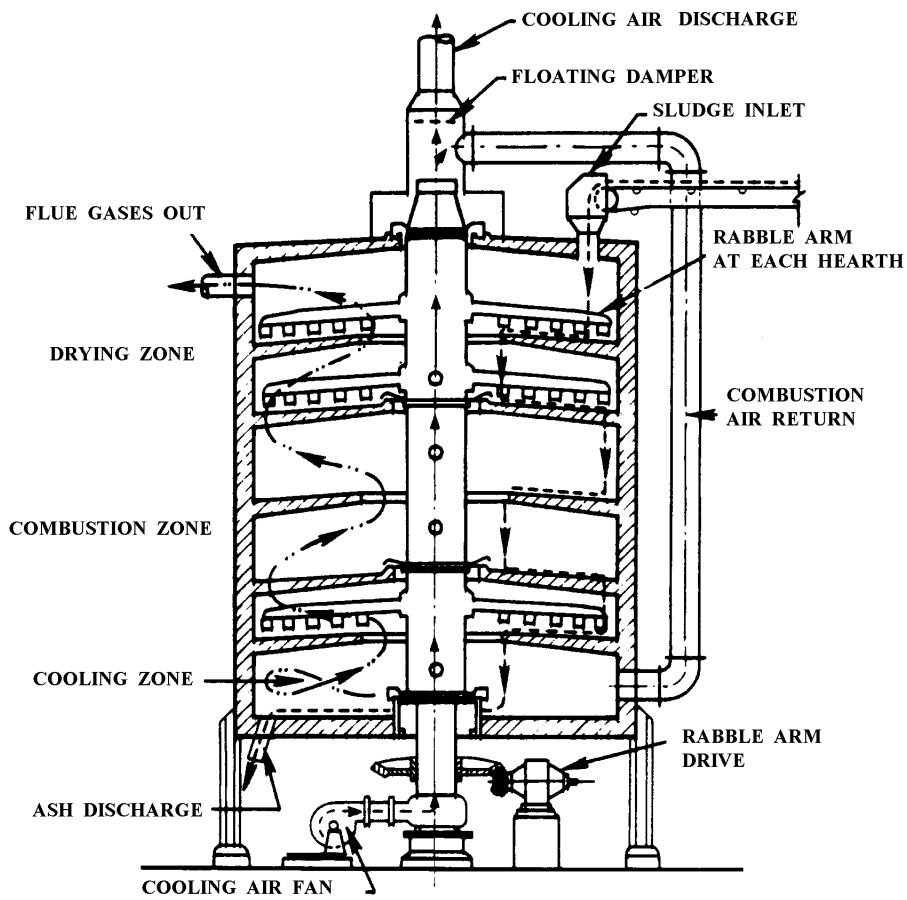


Figure 2.2-1. Cross Section of a Multiple Hearth Furnace

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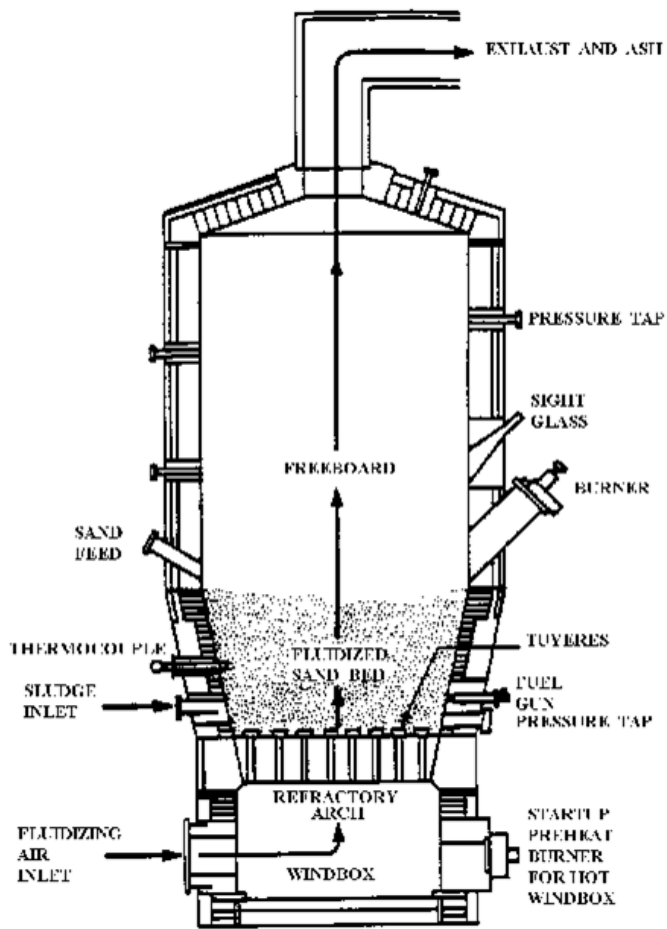


Figure 2-2-2. Cross Section of a Fluidized Bed Incinerator-Furnace

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2.2.1.2 Fluidized Bed Incinerators

Fluidized bed technology was first developed by the petroleum industry to be used for catalyst regeneration. Figure 2.2-2 shows the cross-section diagram of a fluidized bed furnace. Fluidized bed combustors (FBCs) consist of a vertically oriented outer shell constructed of steel and lined with refractory. Tuyeres (nozzles designed to deliver blasts of air) are located at the base of the furnace within a refractory-lined grid. A bed of sand, approximately 0.75 meters (2.5 feet) thick, rests upon the grid. Two general configurations can be distinguished on the basis of how the fluidizing air is injected into the furnace. In the "hot windbox" design the combustion air is first preheated by passing through a heat exchanger where heat is recovered from the hot flue gases. Alternatively, ambient air can be injected directly into the furnace from a cold windbox.

Partially dewatered sludge is fed into the lower portion of the furnace. Air injected through the tuyeres, at pressures of from 20 to 35 kilopascals (3 to 5 pounds per square inch gauge), simultaneously fluidizes the bed of hot sand and the incoming sludge. Temperatures of 750 to 925°C (1400 to 1700°F) are maintained in the bed. Residence times are typically 2 to 5 seconds. As the sludge burns, fine ash particles are carried out the top of the furnace. Some sand is also removed in the air stream; sand make-up requirements are on the order of 5 percent for every 300 hours of operation.

Combustion of the sludge occurs in two zones. Within the bed itself (Zone 1), evaporation of the water and pyrolysis of the organic materials occur nearly simultaneously as the temperature of the sludge is rapidly raised. In the second zone (freeboard area), the remaining free carbon and combustible gases are burned. The second zone functions essentially as an afterburner.

Fluidization achieves nearly ideal mixing between the sludge and the combustion air and the turbulence facilitates the transfer of heat from the hot sand to the sludge. The most noticeable impact of the better burning atmosphere provided by a fluidized bed incinerator is seen in the limited amount of excess air required for complete combustion of the sludge. Typically, FBCs can achieve complete combustion with 20 to 50 percent excess air, about half the excess air required by ~~multiple hearth furnaces~~-MHFs. As a consequence, FBC incinerators have generally lower fuel requirements compared to MHF incinerators.

Fluidized bed incinerators most often have venturi scrubbers or venturi/impingement tray scrubber combinations for emissions control.

2.2.1.3 Electric Infrared Incinerators

The first electric infrared furnace was installed in 1975, and their use is not common. Electric infrared incinerators consist of a horizontally oriented, insulated furnace. A woven wire belt conveyor extends the length of the furnace and infrared heating elements are located in the roof above the conveyor belt. Combustion air is preheated by the flue gases and is injected into the discharge end of the furnace. Electric infrared incinerators consist of a number of prefabricated modules, which can be linked together to provide the necessary furnace length. A cross section of an electric furnace is shown in Figure 2.2-3. The dewatered sludge cake is conveyed into one end of the incinerator. An internal roller mechanism levels the sludge into a continuous layer approximately one inch thick across the width of the belt. The sludge is sequentially dried and then burned as it moves beneath the infrared heating elements. Ash is discharged into a hopper at the opposite end of the furnace. The preheated combustion air enters the furnace above the ash hopper and is further heated by the outgoing ash. The direction of air flow is

countercurrent to the movement of the sludge along the conveyor. -Exhaust gases leave the furnace at the feed end.- Excess air rates vary from 20 to 70 percent.

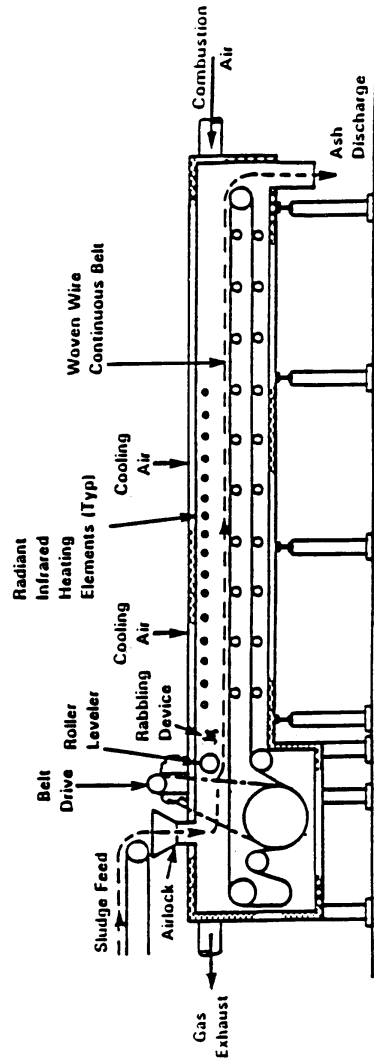


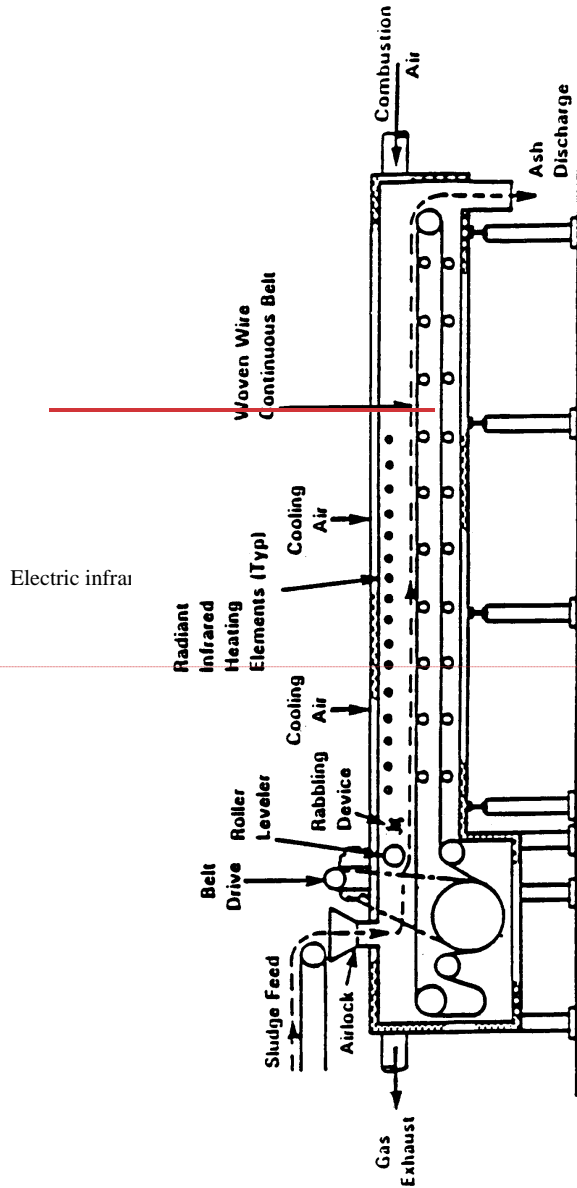
Figure 1.2-3. Cross Section of an Electric Infrared Furnace.

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Compared to MHF and FBC technologies, the electric infrared furnace offers the advantage of lower capital cost,

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especially smaller systems. - However, electricity in some may make electric furnace infeasible.- other concern is replacement various components as the woven wire and infrared heaters, have 3- to 5-year lifetimes.

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Figure 2.2-3. Cross Section of an Electric Infrared Furnace.
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2.2.1.4 –Other Technologies–

A number of other technologies have been used for incineration of sewage sludge, including cyclonic reactors, rotary kilns, and wet oxidation reactors. –These processes are not in widespread use in the United States and will be discussed only briefly.

The cyclonic reactor is designed for small capacity applications. It is constructed of a vertical cylindrical chamber that is lined with refractory. Preheated combustion air is introduced into the chamber tangentially at high velocities. –The sludge is sprayed radially toward the hot refractory walls. Combustion is rapid:– The residence time of the sludge in the chamber is on the order of 10 seconds. The ash is removed with the flue gases.

Rotary kilns are also generally used for small capacity applications. –The kiln is inclined slightly from the horizontal plane, with the upper end receiving both the sludge feed and the combustion air. A burner is located at the lower end of the kiln. –The circumference of the kiln rotates at a speed of about 15 centimeters (cm) per second (6 inches per second). –Ash is deposited into a hopper located below the burner.

The wet oxidation process is not strictly one of incineration; it instead utilizes oxidation at elevated temperature and pressure in the presence of water (flameless combustion). –Thickened sludge, at about 6 percent solids, is first ground and mixed with a stoichiometric amount of compressed air. –The slurry is then pressurized.– The mixture is then circulated through a series of heat exchangers before entering a pressurized reactor. –The temperature of the reactor is held between 175 and 315E°C (350 and 600E°F).– The pressure is normally 7,000 to 12,500 kilopascals (1,000 to 1,800 pounds per square inch grade). –Steam is usually used for auxiliary heat.– The water and remaining ash are circulated out the reactor and are finally separated in a tank or lagoon. –The liquid phase is recycled to the treatment plant. ~~Offgases~~Off-gases must be treated to eliminate odors: –wet scrubbing, afterburning, or carbon absorption may be used.

2.2.1.5 Co-incineration and Co-firing–

Wastewater treatment plant sludge generally has a high–water content and in some cases, fairly high levels of inert materials. –As a result, its net fuel value is often low.– If sludge is combined with other combustible materials in a co-incineration scheme, a furnace feed can be created that has both a low water concentration and a heat value high enough to sustain combustion with little or no supplemental fuel.

Virtually any material that can be burned can be combined with sludge in a co-incineration process. –Common materials for co-combustion are coal, municipal solid waste (MSW), wood waste and agriculture waste. –Thus, a municipal or industrial waste can be disposed of while providing an autogenous (self-sustaining) sludge feed, thereby solving two disposal problems.

There are two basic approaches to combusting sludge with MSW: (1) use of MSW combustion technology by adding dewatered or dried sludge to the MSW combustion unit, and (2) use of sludge combustion technology by adding processed MSW as a supplemental fuel to the sludge furnace. –With the latter, MSW is processed by removing ~~noncombustibles~~non-combustibles, shredding, air classifying, and screening. Waste that is more finely processed is less likely to cause problems such as severe erosion of the hearths, poor temperature control, and refractory failures.

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2.2.2 –Emissions ~~And Controls~~^{and Controls}¹⁻³

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Sewage sludge incinerators potentially emit significant quantities of pollutants. The major pollutants emitted are: –(1) particulate matter, (2) metals, (3) carbon monoxide (CO), (4) nitrogen oxides (NO_x), (5) sulfur dioxide (SO₂), and (6) unburned hydrocarbons. –Partial combustion of sludge can result in emissions of intermediate products of incomplete combustion (PIC), including toxic organic compounds.

Uncontrolled particulate emission rates vary widely depending on the type of incinerator, the volatiles and moisture content of the sludge, and the operating practices employed. Generally, uncontrolled particulate emissions are highest from fluidized bed incinerators because suspension burning results in much of the ash being carried out of the incinerator with the flue gas. –Uncontrolled emissions from multiple hearth and fluidized bed incinerators are extremely variable, however. –Electric incinerators appear to have the lowest rates of uncontrolled particulate release of the three major furnace types, possibly because the sludge is not disturbed during firing. –In general, higher airflow rates increase the opportunity for particulate matter to be entrained in the exhaust gases. –Sludge with low volatile content or high moisture content may compound this situation by requiring more supplemental fuel to burn. As more fuel is consumed, the amount of air flowing through the incinerator is also increased. However, no direct correlation has been established between airflow and particulate emissions.

Metal emissions are affected by metal content of the sludge, fuel bed temperature, and the level of particulate matter control. –Since metals which are volatilized in the combustion zone condense in the exhaust gas stream, most metals (except mercury) are associated with fine particulate and are removed as the fine particulates are removed.

Carbon monoxide is formed when available oxygen is insufficient for complete combustion or when excess air levels are too high, resulting in lower combustion temperatures.

Emissions of nitrogen and sulfur oxides are primarily the result of oxidation of nitrogen and sulfur in the sludge. –Therefore, these emissions can vary greatly based on local and seasonal sewage characteristics.

Emissions of volatile organic compounds (VOC) also vary greatly with incinerator type and operation. Incinerators with countercurrent airflow such as multiple hearth designs provide the greatest opportunity for unburned hydrocarbons to be emitted. In the MHF, hot air and wet sludge feed are contacted at the top of the furnace. –Any compounds distilled from the solids are immediately vented from the furnace at temperatures too low to completely destruct them.

Particulate emissions from sewage sludge incinerators have historically been controlled by wet scrubbers, since the associated sewage treatment plant provides both a convenient source and a good disposal option for the scrubber water. –The types of existing sewage sludge incinerator controls range from low pressure drop spray towers and wet cyclones to higher pressure drop venturi scrubbers and venturi/impingement tray scrubber combinations. –Electrostatic precipitators and baghouses are employed primarily where sludge is co-fired with municipal solid waste. –The most widely used control device applied to a multiple hearth incinerator is the impingement tray scrubber. –Older units use the tray scrubber alone while combination venturi/impingement tray scrubbers are widely applied to newer multiple hearth incinerators and to fluidized bed incinerators. –Most electric incinerators and many fluidized bed incinerators use venturi scrubbers only.

In a typical combination venturi/impingement tray scrubber, hot gas exits the incinerator and enters the precooling or quench section of the scrubber. Spray nozzles in the quench section cool the

incoming gas and the quenched gas then enters the venturi section of the control device. Venturi water is usually pumped into an inlet weir above the quencher. –The venturi water enters the scrubber above the throat and floods the throat completely.– This eliminates build-up of solids and reduces abrasion. Turbulence created by high gas velocity in the converging throat section deflects some of the water traveling down the throat into the gas stream. –Particulate matter carried along with the gas stream impacts on these water particles and on the water wall. –As the scrubber water and flue gas leave the venturi section, they pass into a flooded elbow where the stream velocity decreases, allowing the water and gas to separate. Most venturi sections come equipped with variable throats. –By restricting the throat area within the venturi, the linear gas velocity is increased, and the pressure drop is subsequently increased.– Up to a certain point, increasing the venturi pressure drop increases the removal efficiency. Venturi scrubbers typically maintain 60 to 99 percent removal efficiency for particulate matter, depending on pressure drop and particle size distribution.

At the base of the flooded elbow, the gas stream passes through a connecting duct to the base of the impingement tray tower. Gas velocity is further reduced upon entry to the tower as the gas stream passes upward through the perforated impingement trays. –Water usually enters the trays from inlet ports on opposite sides and flows across the tray.– As gas passes through each perforation in the tray, it creates a jet which bubbles up the water and further entrains solid particles. –At the top of the tower is a mist eliminator to reduce the carryover of water droplets in the stack effluent gas. –The impingement section can contain from one to four trays, but most systems for which data are available have two or three trays.

~~Emission factors and Tables containing emission factor ratings factors for multiple hearth sewage sludge incinerators are shown in Tables 2.2-1, 2.2-2, 2.2-3, 2.2-4, and 2.2-5. Tables 2.2-6, 2.2-7, and 2.2-8 present emission factors, for fluidized bed sewage sludge incinerators. Table 2.2-9 presents the available emission factors and for electric infrared incinerators. Tables 2.2-10 and 2.2-11 present the cumulative particle size distribution and size specific emission factors for sewage sludge incinerators. Figure 2.2-4, Figure 2.2-5, and Figure 2.2-6 present cumulative particle size distribution and size specific emission factors for multiple hearth, fluidized bed, and electric infrared incinerators, respectively. are listed below:~~

- ~~Table 2.2-1 (Metric and English Units). CRITERIA POLLUTANT EMISSION FACTORS FOR MULTIPLE HEARTH SEWAGE SLUDGE INCINERATORS~~
- ~~Table 2.2-2 (Metric and English Units). ACID GAS EMISSION FACTORS FOR MULTIPLE HEARTH SEWAGE SLUDGE INCINERATORS~~
- ~~Table 2.2-3 (Metric and English Units). CHLORINATED DIBENZO-P-DIOXIN (CDD) AND CHLORINATED DIBENZOFURAN (CDF) EMISSION FACTORS FOR MULTIPLE HEARTH SEWAGE SLUDGE INCINERATORS~~
- ~~Table 2.2-4 (Metric and English Units). SUMMARY OF ORGANIC COMPOUND EMISSIONS FROM MULTIPLE HEARTH SEWAGE SLUDGE INCINERATORS~~
- ~~Table 2.2-5 (Metric and English Units). SUMMARY OF METAL EMISSIONS FROM MULTIPLE HEARTH SEWAGE SLUDGE INCINERATORS~~
- ~~Table 2.2-6 (Metric and English Units). CRITERIA POLLUTANT EMISSION FACTORS FOR FLUIDIZED BED SEWAGE SLUDGE INCINERATORS~~
- ~~Table 2.2-7 (Metric and English Units). ACID GAS AND ORGANIC COMPOUND EMISSION FACTORS FOR FLUIDIZED BED SEWAGE SLUDGE INCINERATORS~~
- ~~Table 2.2-8 (Metric and English Units). METAL EMISSION FACTORS FOR FLUIDIZED BED SEWAGE SLUDGE INCINERATORS~~

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- Table 2.2-9 (Metric and English Units). SUMMARY OF EMISSION FACTORS FOR ELECTRIC INFRARED SEWAGE SLUDGE INCINERATORS
- Table 2.2-10 (Metric and English Units). CARBON DIOXIDE EMISSION FACTORS FOR SEWAGE SLUDGE INCINERATORS
- Table 2.2-11 (Metric and English Units). CUMULATIVE PARTICLE SIZE DISTRIBUTION FOR SEWAGE SLUDGE INCINERATORS
- Table 2.2-12 (Metric and English Units). CUMULATIVE PARTICLE SIZE-SPECIFIC EMISSION FACTORS FOR SEWAGE SLUDGE INCINERATORS

2.2.3 Updates to the Section

January 2023:

- Updated/added 66 emission factors
- Updated Source Classification Codes (SCCs): The SCCs used in the previous version of this chapter have been retired. The following SCCs have replaced the existing SCCs:
 - SCC 5-01-005-15 has been replaced with SCC 5-01-008-02
 - SCC 5-01-005-16 has been replaced with SCC 5-01-008-03
 - SCC 5-01-005-17 has been replaced with SCC 5-01-008-04
 - SCC 5-02-005-15 has been replaced with SCC 5-06-007-02
- New quality ratings have been given to factors new/revised based on approaches contained in the revised Emissions Factors Procedures Document. Factors are given quality ratings based on representativeness of factor (e.g., Highly, Moderately, Minimally).

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Table 2.2-1 (continued).

Source Category	Nitrogen Oxides (NO _x)				Sulfur Dioxide (SO ₂)				
	lb/MMBtu Heat Input	kg/Mg	lb/ton	EMISSION FACTOR RATING	lb/MMBtu Heat Input CO ₂	lb/MMBtu Heat Input O ₂	kg/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	-	2.5 E+00	5.0 E+00	C	-	-	1.4 E+01	2.8 E+01	B
Controlled	-	-	-	-	-	-	-	-	-
Afterburner/scrubber ^{ad}	-	-	-	-	-	-	-	-	-
Afterburner/wet scrubber	-	2.8 E+00 ⁱ	5.6 E+00 ⁱ	Moderately	-	-	1.5 E-01 ^{ag}	3.0 E-01 ^{ag}	Minimally
Afterburner/ESP/regenerative thermal oxidizer/scrubber ^o /wet ESP	2.2 E-01 ^{m,n}	-	-	Moderately	-	-	-	-	-
Afterburner/ESP/scrubber ^o /wet ESP	-	2.6 E+00 ^p	5.2 E+00 ^p	Moderately	-	-	-	-	-
Afterburner/scrubber ^r /wet ESP	4.0 E-02 ^{u,v,n}	-	-	Moderately	-	-	-	-	-
Afterburner/scrubber ^r /regenerative thermal oxidizer/wet ESP	5.6 E-02 ^{w,v,s}	-	-	Moderately	1.8 E-02 ^{ah,v}	2.3 E-02 ^{av}	-	-	Moderately
Afterburner/ESP/regenerative thermal oxidizer/scrubber ^o /wet ESP	2.1 E-01 ^{ts}	-	-	Moderately	-	-	-	-	-
Cyclone	-	-	-	-	-	-	2.8 E+00	5.6 E+00	E
Impingement	-	3.5 E+00 ^k	6.9 E+00 ^k	Minimally	-	-	3.2 E-01	6.4 E-01	D
Venturi	-	-	-	-	-	-	2.3 E+00	4.6 E+00	E
Venturi/impingement	-	-	-	-	-	-	1.0 E-01	2.0 E-01	E

^aUnits are pollutants emitted of ~~dry~~dried sludge ~~burned~~fed unless otherwise stated. Source Classification Code (SCC) 5-01-005-15008-02 unless otherwise stated. Blanks indicate no data.

^bWet ESP = wet^bESP = electrostatic precipitator.

^cUncontrolled emission factors for NO_x and CO apply to all air pollution control device types.

^dReference 132

^eHazardous air pollutants listed in the Clean Air Act.

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- ^c[Reference 117](#)
- ^d[Reference 86](#)
- ^e[Reference 87](#)
- ^h[Impingement type wet scrubber/packed bed scrubber/scrubber/wet scrubber/venturi scrubber](#)
- ⁱ[Reference 113](#)
- ^j[Reference 91](#)
- ^k[Reference 92](#)
- ^l[Scrubber/spray scrubber/venturi scrubber/wet scrubber](#)
- ^m[Reference 120](#)
- ⁿ[lb/MMBtu Heat Input CO₂](#)
- ^o[Impingement type wet scrubber/scrubber/wet scrubber/venturi scrubber](#)
- ^p[Reference 124](#)
- ^q[Scrubber/spray scrubber/venturi scrubber/wet scrubber](#)
- ^r[Reference 146](#)
- ^s[lb/MMBtu Heat Input O₂](#)
- ^t[Impingement venturi spray scrubber/wet scrubber](#)
- ^u[Reference 121](#)
- ^v[SCC 5-06-007-02](#)
- ^w[Reference 123](#)
- ^x[Reference 96](#)
- ^y[Reference 94](#)
- ^z[Reference 97](#)
- ^{aa}[Reference 95](#)
- ^{ab}[Reference 127](#)
- ^{ac}[Reference 128](#)
- ^{ad}[Scrubber/wet scrubber/venturi scrubber](#)
- ^{ae}[Reference 129](#)
- ^{af}[Reference 100](#)
- ^{ag}[Reference 102](#)
- ^{ah}[Reference 130](#)
- ^{ai}[Reference 101](#)

Table 2.2-3 (cont.)

Source Category	1,2,3,4,6,7,8,9- Octachlorodibenzo- p-dioxin		1,2,3,4,6,7,8- Heptachlorodibenzo- p-dioxin		Other Hexachlorodibenzo- p-dioxins		Total TEQ		
	µg/Mg	lb/ton	µg/Mg	lb/ton	µg/Mg	lb/ton	lb/MMBtu Heat Input O ₂	µg/Mg	lb/ton
Uncontrolled	-	-	-	-	-	-	-	-	-
Controlled	-	-	-	-	-	-	-	-	-
Afterburner/venturi/wet scrubber	-	-	-	-	4.2 E-02 ^{h,s}	8.4 E-11 ^{h,s}	-	-	-
Afterburner/scrubber ^a / regenerative thermal oxidizer/ wet ESP	-	-	-	-	-	-	-	2.9 E-02 ^{o,f}	5.7 E-11 ^{o,f}
Afterburner/scrubber ^a /wet ESP	-	-	-	-	-	-	1.5 E-10 ^{o,f}	-	-
Afterburner/wet scrubber	9.5 E-0 ^{h,s}	1.9 E-10 ^{h,s}	2.9 E-02 ^{h,s}	5.8 E-11 ^{h,s}	-	-	-	-	-

^aUnits are pollutant emitted of ~~dry~~dried sludge ~~burned~~fed unless otherwise noted. Source Classification Code (SCC) ~~5-01-005-15-008-02~~ unless otherwise specified. Blanks indicate no data.

^bWet ESP = wet^bESP = electrostatic precipitator.

^cHazardous air pollutants listed in the *Clean Air Act*.

^dHazardous air pollutants listed in the *Clean Air Act*.

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Table 2.2-4 (cont.)

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Table 2.2-4 (cont.)

Source Category ^b	1,2-Dichlorobenzene			1,3-Dichlorobenzene			1,4-Dichlorobenzene ^c		
	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	3.7 E-01	7.4 E-04	E				4.1 E-01	8.2 E-04	E
Controlled									
—Cyclone									
—Cyclone/impingement									
—Cyclone/venturi				5.0 E-02	1.0 E-04	E	7.0 E-03	1.4 E-05	E
—Cyclone/venturi/impingement									
—Electrostatic precipitator									
—Fabric filter									
—Impingement									
—Venturi									
—Venturi/impingement/ —afterburner									
-	1,2-Dichlorobenzene	-	-	1,3-Dichlorobenzene	-	-	1,4-Dichlorobenzene ^c	-	-
Source Category	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	3.7 E-01	7.4 E-04	E	-	-	-	4.1 E-01	8.2 E-04	E
Controlled	-	-	-	-	-	-	-	-	-
—Cyclone	-	-	-	-	-	-	-	-	-
—Cyclone/impingement	-	-	-	-	-	-	-	-	-
—Cyclone/venturi	-	-	-	5.0 E-02	1.0 E-04	E	7.0 E-03	1.4 E-05	E
—Cyclone/venturi/impingement	-	-	-	-	-	-	-	-	-
—Electrostatic precipitator	-	-	-	-	-	-	-	-	-
—Fabric filter	-	-	-	-	-	-	-	-	-
—Impingement	-	-	-	-	-	-	-	-	-
—Venturi	-	-	-	-	-	-	-	-	-
—Venturi/impingement/	-	-	-	-	-	-	-	-	-

Table 2.2-4 (cont.)

Source Category ^b	2-Nitrophenol			Acetaldehyde ^c			Acetone		
	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	6.0 E+00	1.2 E-02	E						
Controlled									
Cyclone									
Cyclone/impingement									
Cyclone/venturi	3.8 E-01	7.6 E-04	E						
Cyclone/venturi/impingement									
Electrostatic precipitator									
Fabric filter									
Impingement				1.6 E-01	3.2 E-04	E			
Venturi							3.2 E+00	6.4 E-03	E
Venturi/impingement/afterburner									
Venturi/impingement	1.2 E+00	2.4 E-03	E						
Venturi/impingement/Wet ESP									
Venturi/Wet ESP									

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Table 2.2-4 (cont.)

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Source Category ^b	Perchloroethylene ^c			Phenol ^c			Tetrachloroethane ^c		
	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	4.0 E-01	8.0 E-04	E	2.2 E+01	4.4 E-02	E			
Controlled									
—Cyclone									
—Cyclone/impingement									
—Cyclone/venturi	3.0 E-01	6.0 E-04	E						
—Cyclone/venturi/impingement									
—Electrostatic precipitator									
—Fabric filter									
—Impingement									
—Venturi	2.0 E-01	4.0 E-04	E				1.2 E+01	2.4 E-02	E
—Venturi/impingement/afterburner									
—Venturi/impingement				1.8 E+00	3.6 E-03	E			
—Venturi/impingement/Wet-ESP									
—Venturi/Wet-ESP									

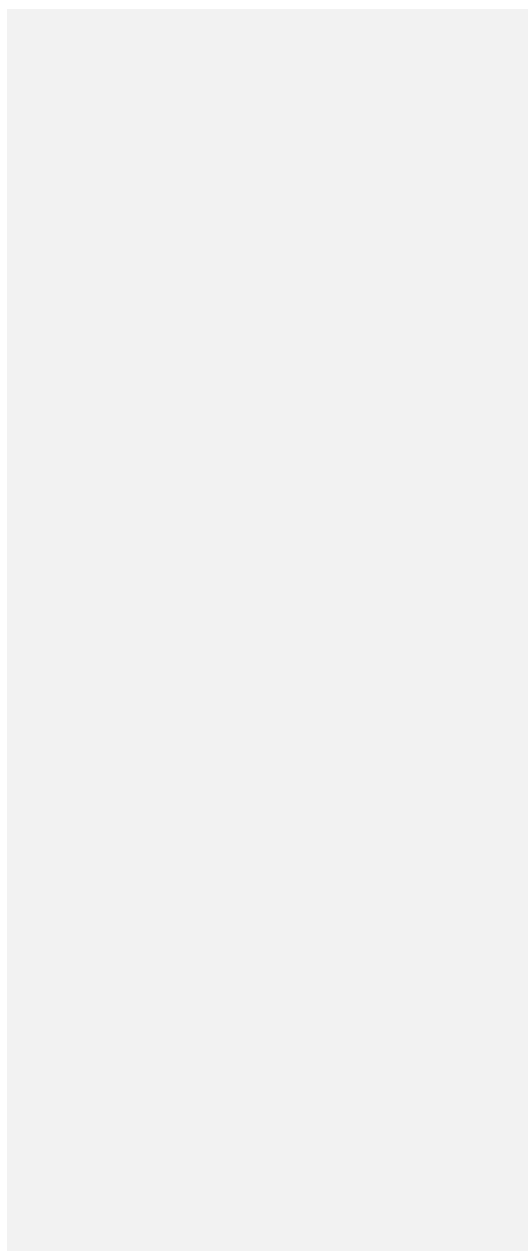


Table 2.2-4. (cont.)

Source Category	Vinyl Chloride ^c			Xylene, m.p. ^c			Xylene (total) ^c		
	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	6.6 E+00	1.3 E-02	E	-	-	-	9.5 E-01	1.9 E-03	E
Controlled	-	-	-	-	-	-	-	-	-
Cyclone	-	-	-	-	-	-	-	-	-
Cyclone/impingement	-	-	-	-	-	-	-	-	-
Cyclone/venturi	1.0 E+00	2.0 E-03	E	-	-	-	-	-	-
Cyclone/venturi/impingement	-	-	-	-	-	-	-	-	-
Electrostatic precipitator	8.0 E-01	1.6 E-03	E	-	-	-	-	-	-
Fabric filter	-	-	-	-	-	-	-	-	-
Impingement	-	-	-	-	-	-	-	-	-
Venturi	-	-	-	2.0 E+00	4.0 E-03	E	-	-	-
Venturi/impingement/afterburner	-	-	-	-	-	-	-	-	-
Venturi/impingement	3.7 E+00	7.4 E-03	D	-	-	-	-	-	-
Venturi/impingement/Wet ESP	-	-	-	-	-	-	-	-	-
Venturi/Wet ESP	-	-	-	-	-	-	-	-	-

^aUnits are pollutants emitted of ~~dry~~dried sludge ~~burned~~fed. Source Classification Code (SCC) 5-01-~~005~~15008-02. Blanks indicate no data.

^bWet ESP = wet^bESP = electrostatic precipitator.

^cHazardous air pollutants in the *Clean Air Act*.

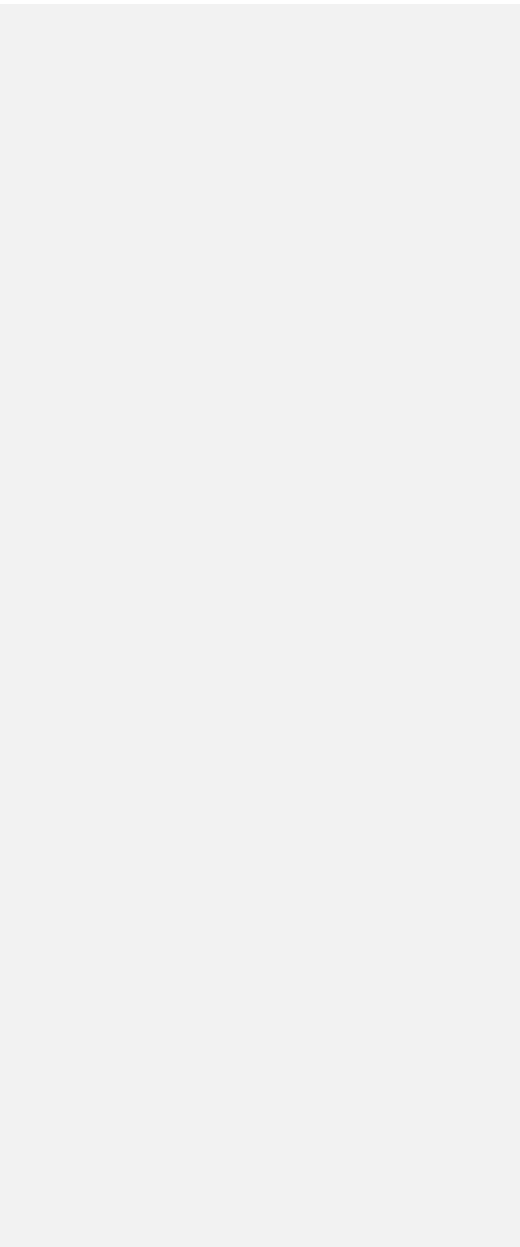
^dReference 88

^eReference 104

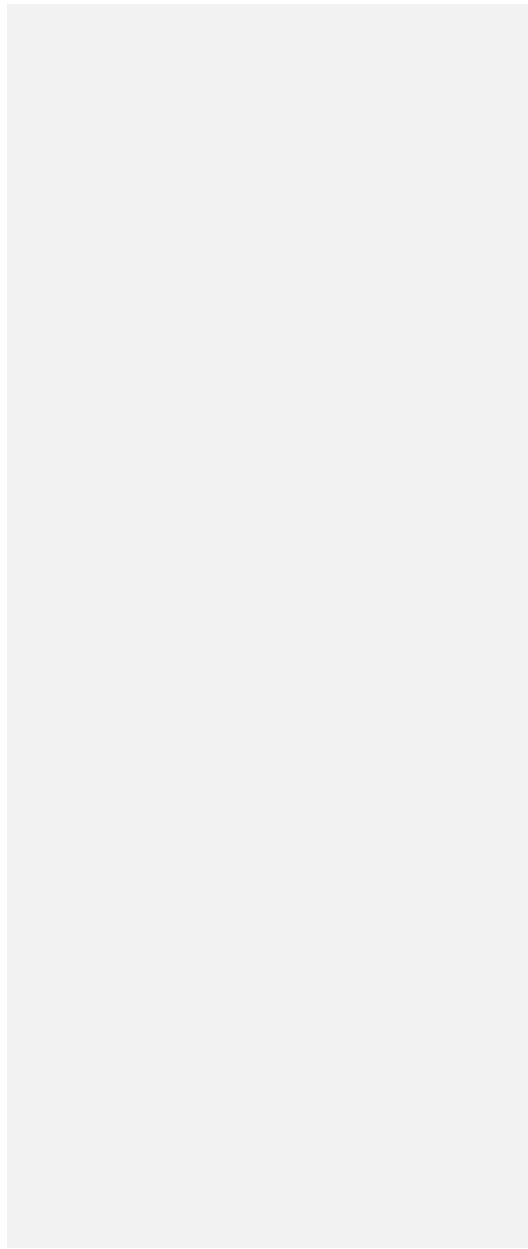
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Table 2.2-5 (cont.)

Source Category ^a	Calcium			Chromium ^e			Cobalt ^e		
	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	7.0 E+02	1.4 E+00	C	1.4 E+01	2.9 E-02	B	9.0 E-01	1.8 E-03	C
Controlled									
—Cyclone	1.2 E+00	2.4 E-03	E	1.9 E+00	3.8 E-03	D	2.0 E-01	4.0 E-04	E
—Cyclone/impingement				4.0 E-02	8.0 E-05	E			
—Cyclone/venturi				5.0 E-01	1.0 E-03	E			
—Cyclone/venturi/impingement				1.1 E+01	2.7 E-02	E			
—Electrostatic precipitator	3.5 E+02	7.0 E-01	E	1.4 E+00	2.8 E-03	E	3.8 E-01	7.6 E-04	E
—Fabric filter	8.0 E-02	1.6 E-04	E	4.0 E-02	8.0 E-05	E	6.0 E-03	1.2 E-05	E
—Impingement				9.8 E+00	1.9 E-02	E			
—Venturi				5.0 E-01	1.0 E-03	E			
—Venturi/impingement/ —afterburner				4.9 E+00	9.8 E-03	E			
—Venturi/impingement	2.6 E+02	5.2 E-01	D	2.1 E+00	4.2 E-03	E	4.5 E-01	9.0 E-04	D
—Venturi/impingement/Wet-ESP				1.1 E-01	2.2 E-04	E			
—Venturi/Wet-ESP				1.0 E-02	2.0 E-05	E			



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~~Table 2.2.5 (cont.)~~

Source Category ^b	Titanium			Vanadium			Zinc		
	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING

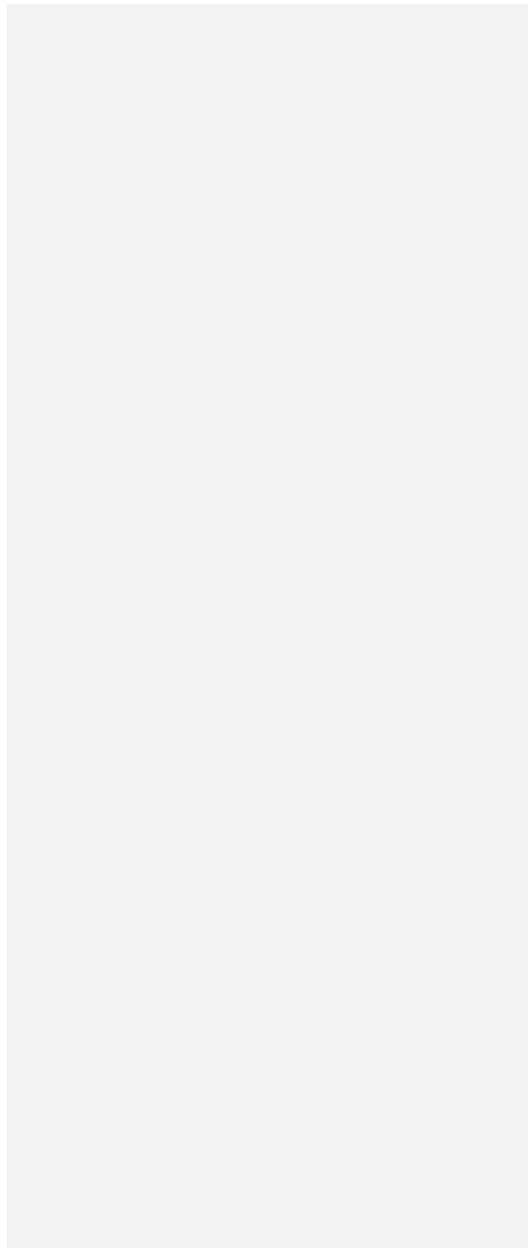
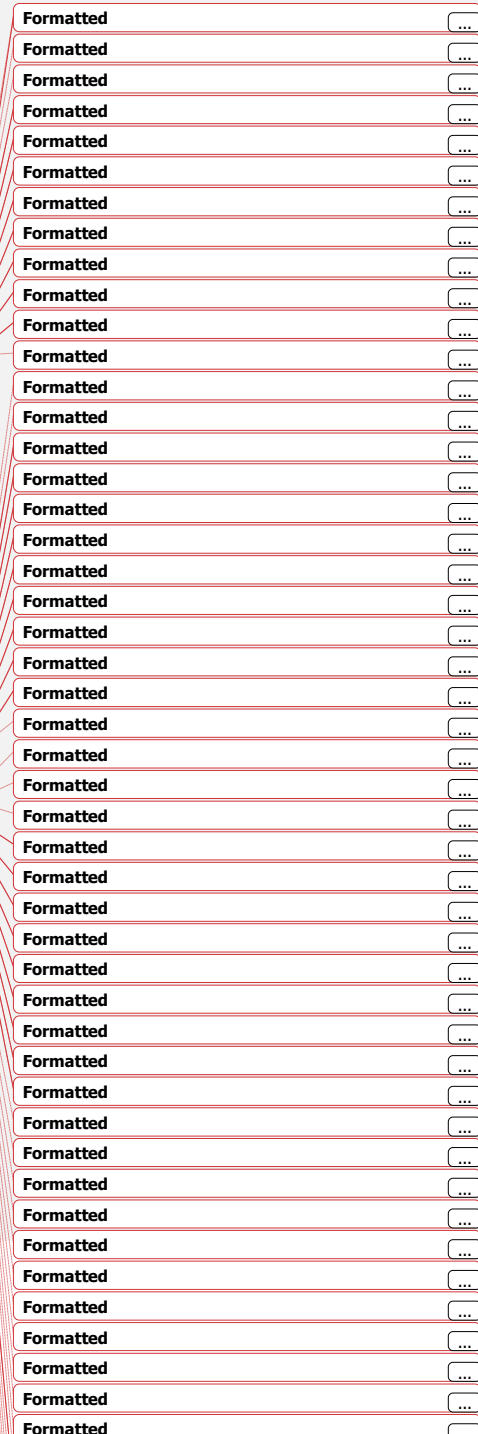


Table 2.2-5 (cont.).

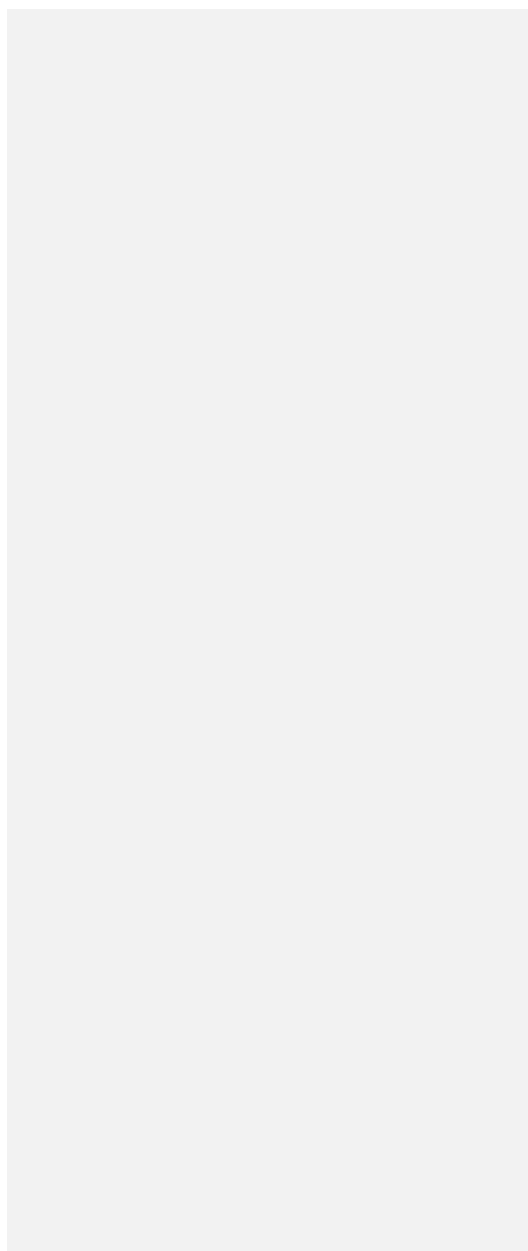
Source Category	Titanium			Vanadium			Zinc		
	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING	g/Mg	lb/ton	EMISSION FACTOR RATING
Uncontrolled	5.1 E+01	1.0 E-01	C	3.3 E+00	6.6 E-03	C	6.6 E+01	1.3 E-01	C
Controlled							1.1 E+01	2.2 E-02	E
–Cyclone	1.0 E-01	2.0 E-04	E	3.0 E-01	6.0 E-04	E			
–Cyclone/impingement									
–Cyclone/venturi							3.8 E+01	7.6 E-02	E
–Cyclone/venturi/impingement									
Controlled							1.1 E+01	2.2 E-02	E
–Cyclone	1.0 E-01	2.0 E-04	E	3.0 E-01	6.0 E-04	E	-	-	-
–Cyclone/impingement	-	-	-	-	-	-	-	-	-
–Cyclone/venturi	-	-	-	-	-	-	3.8 E+01	7.6 E-02	E
–Cyclone/venturi/impingement	-	-	-	-	-	-	-	-	-
Electrostatic precipitator	9.0 E-01	1.8 E-03	E	9.9 E-01	2.0 E-03	E	3.9 E-01	7.8 E-04	E
Fabric filter	6.0 E-03	1.2 E-05	E	2.0 E-03	4.0 E-06	E	4.0 E-02	8.0 E-05	E
Impingement	-	-	-	-	-	-	-	-	-
Venturi	-	-	-	-	-	-	4.4 E+00	8.8 E-03	E
Venturi/impingement/afterburner	-	-	-	-	-	-	3.3 E+01	6.6 E-02	E
Venturi/impingement	3.1 E+00	6.2 E-03	D	8.0 E-01	1.6 E-03	E	2.4 E+01	4.8 E-02	C
Venturi/impingement/Wet ESP	-	-	-	-	-	-	-	-	-
Venturi/Wet ESP	-	-	-	-	-	-	2.0 E-01	4.0 E-04	E

^aUnits are pollutants emitted of ~~dry~~dried sludge ~~burned~~fed unless otherwise specified. Source Classification Code (SCC) 5-01-005-15008-02. Blanks indicate no data.

^bWet ESP = wet^cESP = electrostatic precipitator.



^cHazardous air pollutants listed in the *Clean Air Act*.



^b~~Wet ESP = wet~~^bESP = electrostatic precipitator-

^c~~Uncontrolled Emission Factors for NO_x and CO apply to all Air Pollution Control Device Types.~~

^cACI = activated carbon injection

^dHazardous air pollutants listed in the *Clean Air Act*.

^eScrubber pressure drop/scrubber water pH/tray tower scrubber/venturi scrubber/wet scrubber

^fReference 145

^gModerately representative emission factor

^hScrubber pressure drop/scrubber water pH/spray scrubber/tray scrubber/venturi scrubber

ⁱReference 147

^jlb/MMBtu heat input O₂

^kImpingement scrubber/venturi scrubber

^lHighly representative emission factor

^mReference 89

ⁿImpingement scrubber/scrubber/venturi scrubber

^oReference 115

^pImpingement scrubber/tray scrubber/venturi scrubber/wet scrubber

^qMinimally representative emission factor

^rScrubber water pH/wet scrubber

^sReference 122

^tReference 125

^uImpingement scrubber/scrubber/venturi scrubber/wet scrubber

^vScrubber/impingement type wet scrubber/venturi scrubber/wet scrubber

^wReference 98

^xReference 99

^yImpingement scrubber/scrubber pressure drop/tray scrubber/venturi scrubber

^zReference 137

^{aa}Reference 130

^{ab}lb/MMBtu heat input CO₂

^{ac}Reference 131

^{ad}Reference 133

^{ae}Scrubber/impingement type wet scrubber/venturi scrubber

Carbon Tetrachloride ^b					1.2 E-02	2.4 E-05		
Chlorobenzene ^b					5.0 E-03	1.0 E-05		

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Table 2.2-7 (cont.).

Pollutant	ACI/Average Bed Temperature/Baghouse/Incinerator/Scrubber ^d /Wet ESP		Average bed temperature/ESP/tray type gas absorption column/scrubber ^g		Adsorption – activated carbon or other/average bed temperature/ESP/selective non-catalytic reduction/cyclones/incinerator/tray-type gas absorption column/wet ESP/scrubber ^l	
	g/Mg	lb/ton	g/Mg	lb/ton	g/Mg	lb/ton
Hydrogen Chloride (HCl) ^b	4.0 E+00 ^{e,f}	7.9 E-03 ^{e,f}	-	-	-	-
Total TCDD	-	-	9.5 E-06 ^{h,i}	1.9 E-08 ^{h,i}	-	-
Total TEQ	-	-	-	-	3.3 E-07 ^{m,f}	6.6 E-10 ^{m,f}

^aUnits are pollutants emitted of ~~drydried~~ ~~sludge burned~~ ~~fed~~. Source Classification Code (SCC) 5-01-005-16008-03. Blanks indicate no data.

^bHazardous air pollutants listed in the *Clean Air Act*.

^cACI = activated carbon injection; ESP = electrostatic precipitator

^dScrubber water pH/ tray scrubber/venturi scrubber/wet scrubber

^eReference 112

^fHighly representative emission factor

^gScrubber pressure drop/scrubber water pH/tray scrubber/venturi scrubber/wet scrubber

^hReference 138

ⁱModerately representative emission factor

^jReference 135

^kScrubber, venturi scrubber/wet scrubber

^lScrubber/impingement type wet scrubber/venturi scrubber/wet scrubber

^mReference 140

ⁿImpingement scrubber/tray scrubber/venturi scrubber

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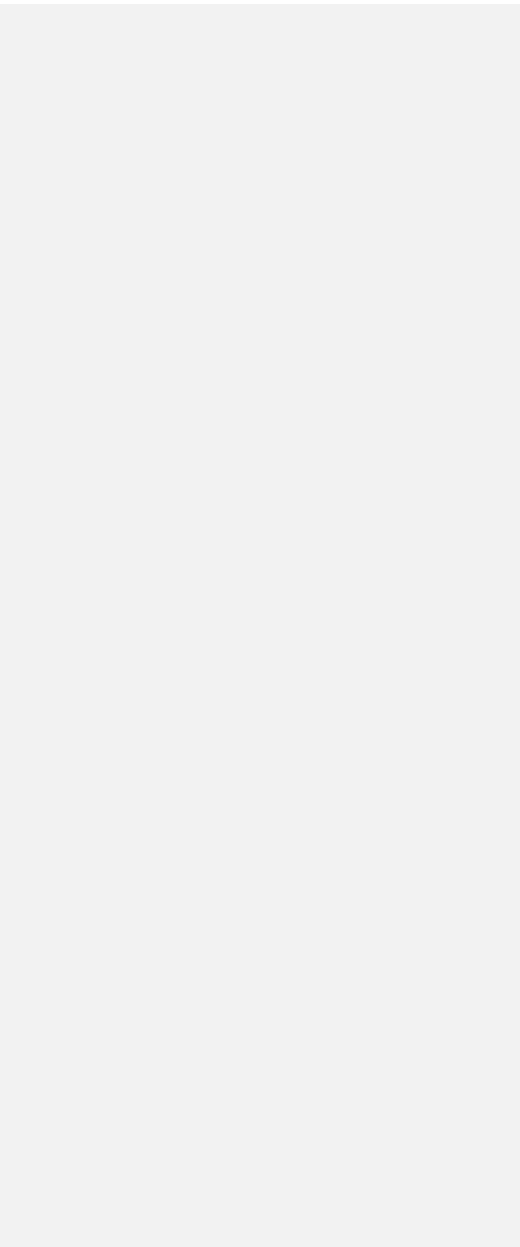


Table 2.2-8 (cont.).

Pollutant	ACI/ Average Bed Temperature/Baghouse/Cyclones/Wet ESP/ ESP/SNCR ^s / Incinerator/ Tray- Type Gas Absorption/ Scrubber ^d		Average Bed Temperature/Scubber ^f / Wet ESP	
	g/Mg	lb/ton	g/Mg	lb/ton
Aluminum	-	-	-	-
Arsenic ^c	-	-	-	-
Barium	-	-	-	-
Beryllium ^c	-	-	-	-
Cadmium ^c	<u>1.7 E-03^{k,p}</u>	<u>3.3 E-06^{k,p}</u>	-	-
Calcium ^c	-	-	-	-
Chromium ^c	-	-	<u>1.8 E-02^{m,h}</u>	<u>3.6 E-05^{m,h}</u>
Copper	-	-	-	-
Manganese ^c	-	-	-	-
Magnesium	-	-	-	-
Mercury ^c	-	-	-	-
Nickel ^c	-	-	-	-
Potassium	-	-	-	-
Selenium ^c	-	-	-	-
Silicon	-	-	-	-
Sulfur	-	-	-	-
Tin	-	-	-	-
Titanium	-	-	-	-
Zinc	-	-	-	-

Table 2.2-8 (cont.).

Pollutant	Incinerator/Venturi		ACI/ Average Bed Temperature/Baghouse/Cyclone/ Incinerator/ESP/Wet ESP/Scrubber/ Tray-Type Gas Absorption Column	
	g/Mg	lb/ton	g/Mg	lb/ton
Aluminum	-	-	-	-
Arsenic ^c	-	-	-	-
Barium	-	-	-	-
Beryllium ^c	-	-	-	-
Cadmium ^c	-	-	-	-
Calcium ^c	-	-	-	-
Chromium ^c	-	-	-	-
Copper	-	-	-	-
Manganese ^c	-	-	-	-
Magnesium	-	-	-	-
Mercury ^c	2.4 E-01 ^{n,h}	4.8 E-04 ^{n,h}	1.2 E-01 ^{f,p}	2.3 E-04 ^{f,p}
Nickel ^c	-	-	-	-
Potassium	-	-	-	-
Selenium ^c	-	-	-	-
Silicon	-	-	-	-
Sulfur	-	-	-	-
Tin	-	-	-	-
Titanium	-	-	-	-
Zinc	-	-	-	-

^aUnits are pollutants emitted of ~~dry~~ dried sludge ~~burned~~. Source Classification Code (SCC) 5-01-005-16008-03. Blanks indicate no data.

^bWet ESP = wet^bESP = electrostatic precipitator.

^cHazardous air pollutants listed in the *Clean Air Act*.

^fReference 116

^gSNCR = selective non-catalytic reduction

^hModerately representative emission factor

ⁱACI = Activated Carbon Injection

^jScrubber/scrubber water pH/tray scrubber/venturi scrubber

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^k[Reference 141](#)

^l[Impingement type wet scrubber/scrubber pressure drop/scrubber water pH/tray scrubber/venturi scrubber/wet scrubber](#)

^m[Reference 110](#)

ⁿ[Reference 90](#)

^o[Venturi scrubber/scrubber/tray scrubber/](#)

^p[Highly representative emission factor](#)

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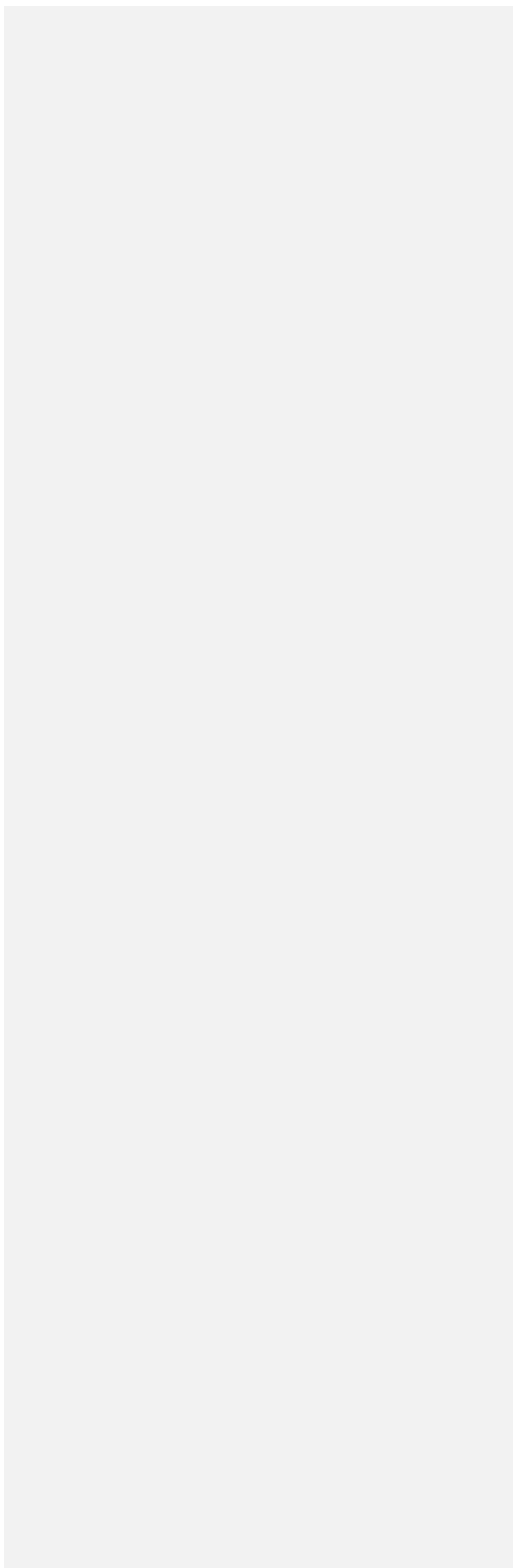


Table 2.2-10 (Metric and English Units). CARBON DIOXIDE EMISSION FACTORS FOR SEWAGE SLUDGE INCINERATORS.

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Source Category	Carbon Dioxide		
	lb/MMbtu Heat Input	kg/Mg ^a	lb/ton ^a
Uncontrolled	-	-	-
Controlled (SCC 5-01-008-02)	-	-	-
Afterburner/ESP ^a /Scrubber ^b /Wet ESP ^p / Regenerative Thermal Oxidizer	-	1.8 E+03 ^{e,i}	3.5 E+03 ^{e,i}
Afterburner/ESP/Scrubber ^c /Wet ESP	1.6 E+02 ^{d,i,g}	-	-
Controlled (SCC 5-01-008-03)	-	-	-
Average Bed Temperature/ Incinerator/Scrubber ^b /Wet ESP	-	1.5 E+03 ^{j,i}	2.9 E+03 ^{j,i}
Average Bed Temperature/ESP/Tray-Type Gas Absorption Column/Scrubber ^k /Wet ESP	1.9 E+02 ^{l,m,i}	-	-
Controlled (SCC 5-06-007-02)	-	-	-
Afterburner/Scrubber ⁿ /Wet ESP	1.6 E+02 ^{o,i,g}	-	-

^aUnits are in dried sludge fed.

^bVenturi scrubber/wet scrubber/tray scrubber/impingement plate scrubber

^cVenturi scrubber/wet scrubber

^dReference 106

^eReference 107

^fMinimally representative emission factor

^glb/MMbtu heat input O₂

^hScrubber water pH/venturi scrubber/wet scrubber

ⁱModerately representative emission factor

^jReference 108

^kScrubber/scrubber pressure drop/scrubber water pH, tray scrubber, venturi scrubber

^lReference 105

^mlb/MMbtu heat input CO₂

ⁿImpingement venturi tray scrubber/wet scrubber

^oReference 136

^pESP = electrostatic precipitator

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Table 2.2-11 (Metric and English Units), CUMULATIVE PARTICLE SIZE DISTRIBUTION FOR SEWAGE SLUDGE INCINERATORS^a

EMISSION FACTOR RATING: E

Particle Size (µm) (µm)	Cumulative Mass % Stated Size					
	Uncontrolled			Controlled (Scrubber)		
	MH ^b	EI ^c		MH	FB ^d	EI
15	15	43		30	7.7	60
10	10	30		27	7.3	50
5.0	5.3	17		25	6.7	35
2.5	2.8	10		22	6.0	25
1.0	1.2	6.0		20	5.0	18
0.625	0.75	5.0		17	2.7	15

^aReference 5.

^bMH = multiple hearth incinerator. Source Classification Code (SCC) 5-01-~~005-15008-02~~.

^cEI = electric infrared incinerator. SCC- 5-01-~~005-17008-04~~.

^dFB = fluidized bed incinerator. SCC 5-01-~~005-16008-03~~.

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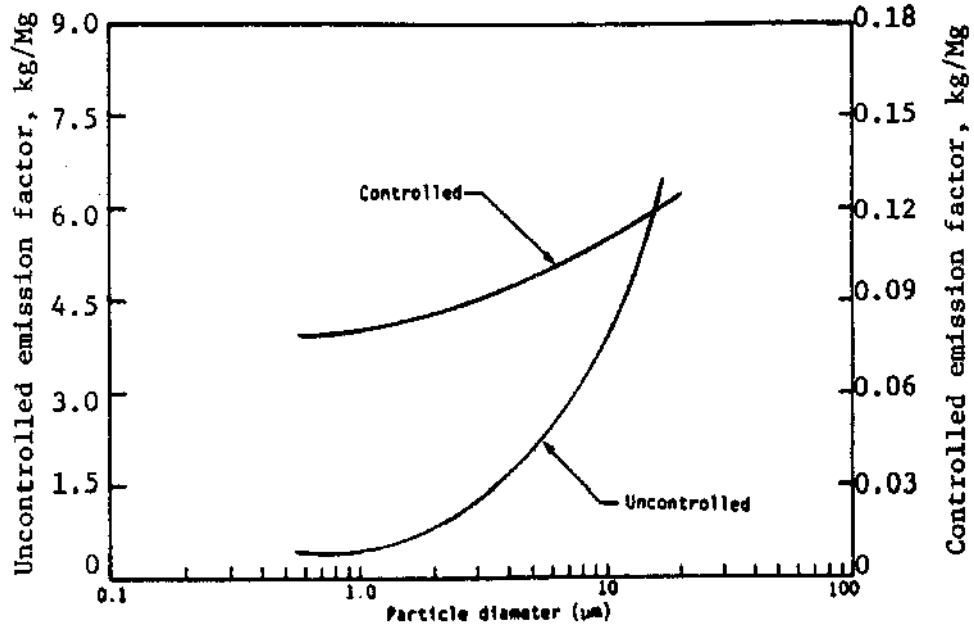
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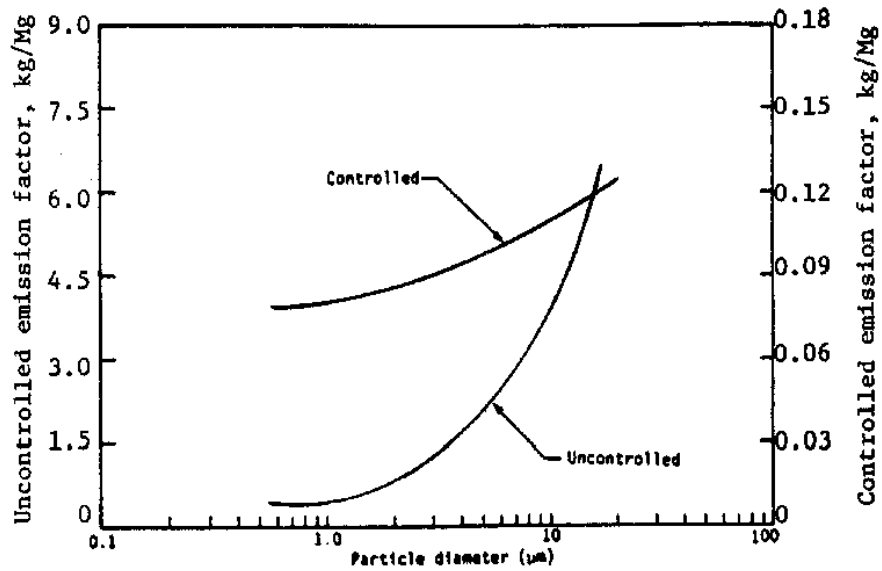
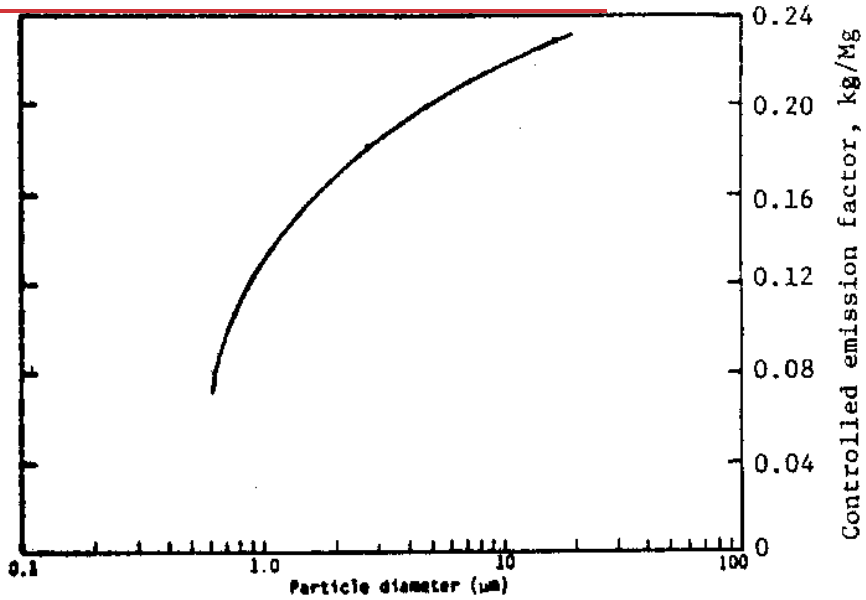


Figure 2.2-4. Cumulative Particle Size Distribution and Size-Specific Emission Factors for Multiple-Health Incinerators



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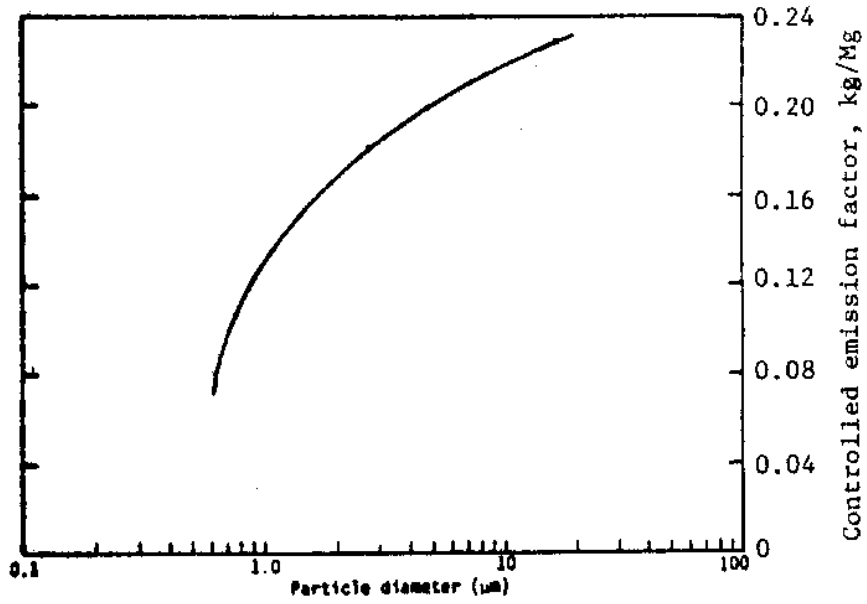


Figure 2.2-5. Cumulative Particle Size Distribution and Size-Specific Emission Factors for Fluidized-Bed Incinerators

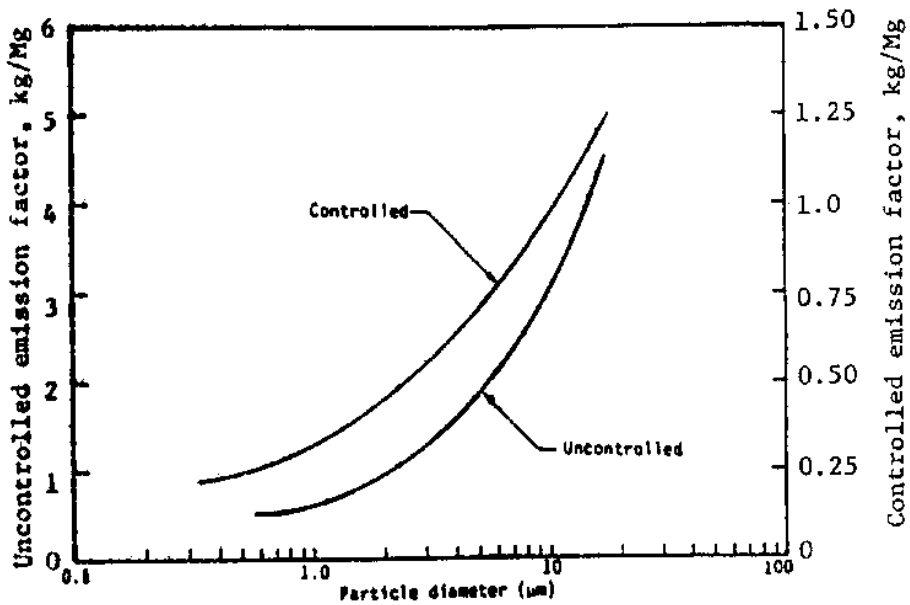
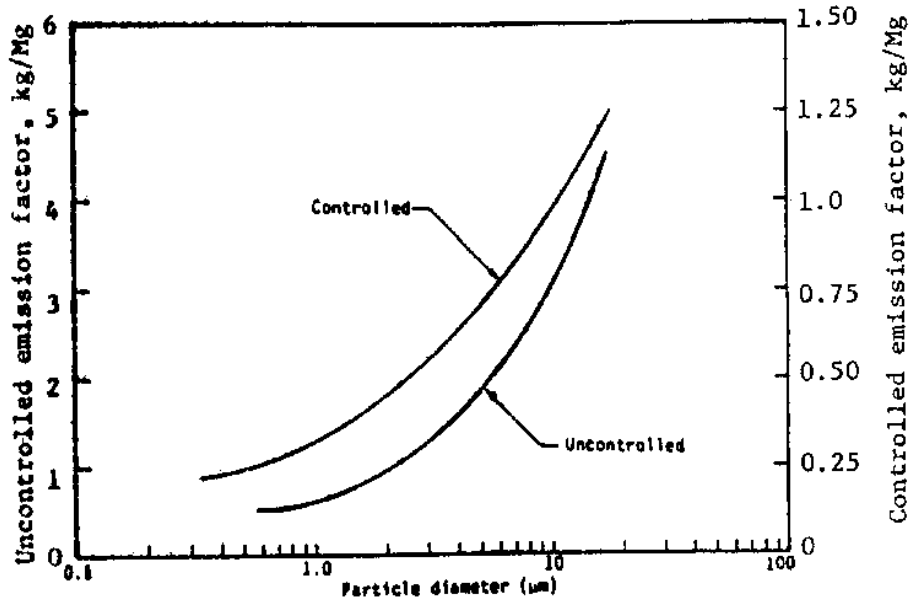


Figure 2.2-6. Cumulative Particle Size Distribution and

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125. NOx stack test data submitted to CEDRI for SCC/control device combination. Each individual test report can be obtained via WebFIRE.

126. Other Hexachlorodibenzo-p-dioxins stack test data submitted to CEDRI for SCC/control device combination. Each individual test report can be obtained via WebFIRE.

127. PM, Filterable stack test data submitted to CEDRI for SCC/control device combination. Each individual test report can be obtained via WebFIRE.

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134. Tetrachlorodibenzo-p-dioxins, total stack test data submitted to CEDRI for SCC/control device combination. Each individual test report can be obtained via WebFIRE.

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