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Technologies and Costs for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water

Technologies and Costs for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water

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Acronyms and Abbreviations

ANSI	American National Standards Institute
BV	bed volumes
DOC	dissolved organic carbon
EBCT	empty bed contact time
EPA	U.S. Environmental Protection Agency
GAC	granular activated carbon
gfd	gallons per day per square foot
g/mol	grams per mole
gpm	gallons per minute
IX	ion exchange
LSI	Langelier saturation index
MCL	maximum contaminant level
MGD	million gallons per day
mg/L	milligrams per liter
MWCO	molecular weight cut off
NF	nanofiltration
ng/L	nanograms per liter
NPDES	National Pollutant Discharge Elimination System
NSF	NSF International, The Public Health and Safety Company ¹
O&M	operating and maintenance
PFAS	per- and polyfluoroalkyl substances
POE	point-of-entry
POU	point-of-use
RCRA	Resource Conservation and Recovery Act
RO	reverse osmosis
RSSCT	rapid small-scale column test
SDI	silt density index
SDWA	Safe Drinking Water Act
TDP	Technology Design Panel
TOC	total organic carbon
WBS	Work Breakdown Structure
WWTP	wastewater treatment plant

See also Table 1-1 for abbreviations for individual PFAS compounds.

¹ Formerly National Sanitation Foundation

1.0 Introduction

1.1 Background

Per- and polyfluoroalkyl substances (PFAS) are a broad class of approximately 10,000 synthetic chemicals (Rogers et al., 2021; Weaver, 2020; USEPA, 2021d). Because of their water-resistant, stain-resistant, and non-stick properties, they are incorporated in or used as coatings for a variety of products. Household and industrial PFAS applications include use in carpeting, clothing, cookware, cosmetics, electronics, fire-fighting foam, glass, and packaging. The manufacture of PFAS and PFAS-containing products, along with the use and disposal of these products, have resulted in releases to air, soil, and water (ATSDR, 2021; Rogers et al., 2021; Weaver, 2020). The same properties that make PFAS useful in industry and commerce also make them stable and persistent in the environment (ATSDR, 2021).

The U.S. Environmental Protection Agency (EPA) is proposing a regulation for certain PFAS under the Safe Drinking Water Act (SDWA). To assist in evaluating and developing the national costs associated with the proposed regulation, this document describes treatment technologies that are known to effectively remove PFAS from drinking water. It also presents estimated costs associated with the engineering, installation, and operation and maintenance of these technologies. EPA is proposing MCLGs for perfluorooctanesulfonic acid (PFOS) and perfluorooctanoic acid (PFOA) at zero and the enforceable Maximum Contaminant Level (MCL) at 4.0 nanograms per liter (ng/L) or parts per trillion (ppt) for each of these contaminants. EPA is also proposing regulation of hexafluoropropylene oxide dimer acid (HFPO-DA), perfluorobutane sulfonic acid (PFBS), perfluorononanoic acid (PFNA), and perfluorohexane sulfonic acid (PFHxS) through a Hazard Index (HI) approach. EPA is proposing to set the MCLG as a HI of 1.0 (unitless) and the enforceable MCL equal to the MCLG. Table 1-1 lists PFAS for which treatability data are available in the literature included in EPA's Drinking Water Treatability Database (USEPA, 2021a; 2021b; 2021c).

The two most frequently studied PFAS are PFOA, which refers to perfluorooctanoic acid or perfluorooctane carboxylate, and PFOS, which refers to perfluorooctane sulfonic acid or perfluorooctane sulfonate.² Figure 1-1 shows the chemical structure of these two PFAS. Both molecules incorporate a chain of fully fluorinated (perfluorinated) carbon atoms but differ in the functional group attached at the end of the chain. In PFOA, the terminal functional group is carboxylic acid (CO₂H) or carboxylate (CO₂⁻) in the anion form. In PFOS, the terminal functional group is sulfonic acid (SO₃H) or sulfonate (SO₃⁻) in the anion form.

Both PFOA and PFOS include a total of eight carbon atoms in their molecular chain. There are other perfluorinated PFAS that incorporate the same terminal functional groups but have a different number of carbon atoms in the chain. For example, PFHxA refers to a perfluorinated six-carbon compound with a carboxylic acid or carboxylate functional group. PFHxS refers to a perfluorinated six-carbon compound with a sulfonic acid or sulfonate functional group. In general, degree of fluorination, functional group, and chain length provide a means of classifying PFAS compounds, as shown in Table 1-2. Buck et al. (2011) and ITRC (2020) provide a more

² Although different sources within the literature may use the names for the acid and anion forms of PFOA, PFOS, and other perfluorinated PFAS interchangeably, they most frequently occur in the environment in their anion form (ITRC, 2020).

detailed and nuanced categorization of PFAS, but for purposes of discussing treatment technologies and costs this simplified categorization is useful.

Table 1-1. PFAS with Treatability Data

Abbreviation	Full Name	Chemical Abstract Service (CAS) Number
ADONA	Ammonium 4,8-dioxo-3H-perfluorononanoate	958445-44-8 or 919005-14-4 (as acid)
F-53B	A combination of 9-chlorohexadecafluoro-3-oxanone-1-sulfonic acid and 11-chloroeicosafluoro-3-oxaundecane-1-sulfonic acid	756426-58-1 and 763051-92-9 (respectively)
FtS 4:2	Fluorotelomer sulfonate 4:2	414911-30-1
FtS 6:2	Fluorotelomer sulfonate 6:2	27619-97-2
FtS 8:2	Fluorotelomer sulfonate 8:2	39108-34-4
HFPO-DA*	Ammonium perfluoro-2-methyl-3-oxahexanoate, Perfluoro-2-methyl-3-oxahexanoic acid	62037-80-3 (as ammonium salt), 13252-13-6 (as acid)
Nafion BP2	Perfluoro-2-[[perfluoro-3-(perfluoroethoxy)-2-propanyl]oxy]ethanesulfonic acid	749836-20-2
N-EtFOSAA	2-(N-Ethyl-perfluorooctanesulfonamido)acetate	2991-50-6
N-MeFOSAA	2-(N-Methylperfluorooctanesulfonamido)acetate	909405-48-7 or 2355-31-9 (as acid)
PFBA	Perfluorobutanoic acid	375-22-4
PFBS	Perfluorobutyl sulfonic acid	375-73-5
PFBSA	Perfluorobutylsulfonamide	30334-69-1
PFDA	Perfluorodecanoic acid	335-76-2
PFDoA	Perfluorododecanoic acid	307-55-1
PFDS	Perfluorodecyl sulfonic acid	335-77-3
PFECHS	Perfluoro-4-(perfluoroethyl)cyclohexylsulfonate	80988-54-1
PFHpA	Perfluoroheptanoic acid	375-85-9
PFHpS	Perfluoroheptyl sulfonic acid	375-92-8
PFHxA	Perfluorohexanoic acid	307-24-4
PFHxS	Perfluorohexyl sulfonic acid	355-46-4
PFHxSA	Perfluorohexanesulfonamide	41997-13-1
PFMOAA	Difluoro(perfluoromethoxy)acetic acid, also known as perfluoro-2-methoxyacetic acid	674-13-5
PFMOBA	Perfluoro-4-methoxybutanoic acid	863090-89-5
PFMOPrA	Perfluoro-3-methoxypropanoic acid	377-73-1
PFNA	Perfluorononanoic acid	375-95-1
PFNS	Perfluorononane sulfonic acid	68259-12-1
PFO2HxA	Perfluoro-3,5-dioxahexanoic acid	39492-88-1
PFO3OA	Perfluoro-3,5,7-trioxaoctanoic acid	39492-89-2
PFO4DA	Perfluoro-3,5,7,9-butaoadecanoic acid	39492-90-5
PFOA	Perfluorooctanoic acid	335-67-1
PFOS	Perfluorooctane sulfonic acid	1763-23-1
PFOSA	Perfluorooctanesulfonamide	754-91-6
PFPeA	Perfluoropentanoic acid	2706-90-3
PFPrS	Perfluoropropane sulfonate	110676-15-8

Abbreviation	Full Name	Chemical Abstract Service (CAS) Number
PFTriA	Perfluorotridecanoic acid	72629-94-8
PFUnA	Perfluoroundecanoic acid	2058-94-8

* HFPO-DA is used in a processing aid technology developed by DuPont to make fluoropolymers without using PFOA. The chemicals associated with this process are commonly known as GenX Chemicals and the term is often used interchangeably for HFPO-DA along with its ammonium salt
 Sources: USEPA, 2021a; 2021b; 2021c

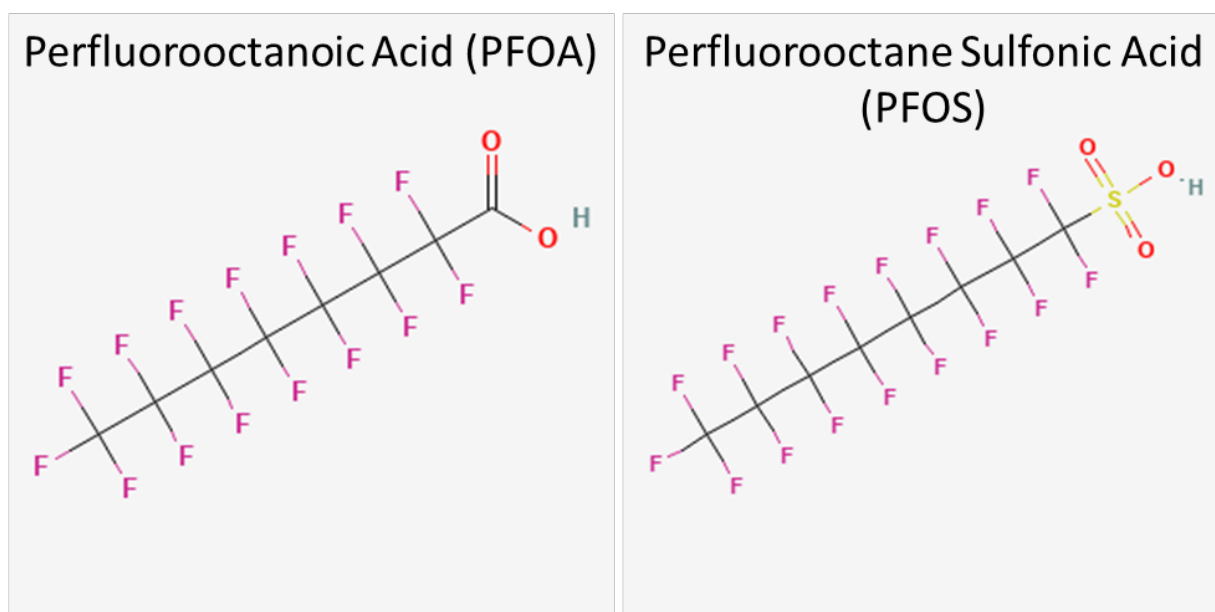


Figure 1-1. Chemical Structure of PFOA and PFOS

Sources: NCBI, 2021a; 2021b

Table 1-2. PFAS Classified by Functional Group and Chain Length

Number of Carbons	Perfluorinated Carboxylic Acids/Carboxylates	Perfluorinated Sulfonic Acids/Sulfonates	Other Perfluorinated	Polyfluorinated
3		PFPrS		PFMOAA
4	PFBA	PFBS	PFBSA	FtS 4:2, PFO2HxA, PFMOPrA
5	PFPeA	PFPeS		PFO3OA, PFMOBA
6	PFHxA	PFHxS	HFPO-DA, PFHxSA	FtS 6:2, PFO4DA
7	PFHpA	PFHpS		ADONA, Nafion BP2
8	PFOA	PFOS	PFOSA, PFECHS	FtS 8:2

Number of Carbons	Perfluorinated Carboxylic Acids/Carboxylates	Perfluorinated Sulfonic Acids/Sulfonates	Other Perfluorinated	Polyfluorinated
9	PFNA	PFNS		
10	PFDA	PFDS		
11	PFUnA			N-MeFOSAA
12	PFDoA			N-EtFOSAA
13	PFTriA			

Sources: ITRC, 2020; USEPA, 2021a; 2021b; 2021c

1.2 Organization and Overview

This report is organized as follows:

- Evaluation of treatment and nontreatment compliance options for potential PFAS standards (Chapters 2 through 6)
- Costs for treatment and nontreatment (Chapter 7).

The technology evaluations in Chapter 2 through 5 describe treatment technologies that can effectively remove PFAS from drinking water. Specifically, they address effectiveness for the following treatment technologies:

- Granular activated carbon (GAC) (Chapter 2)
- Ion exchange (IX) (Chapter 3)
- Reverse osmosis and nanofiltration (RO/NF) (Chapter 4)
- Point-of-use/point-of-entry (POU/POE) treatment (Chapter 5).³

For each technology, the corresponding chapter provides an overview of how the technology operates and summarizes its effectiveness for removal or destruction of PFAS. Each technology summary also incorporates available findings with respect to effectiveness under different source water conditions. Information on process waste characterization, handling, and management is also provided. Each summary concludes with a compilation of the PFAS-specific engineering design specifications obtained from the treatability literature reviewed.

Chapter 6 discusses nontreatment options that might be used in lieu of treatment options to comply with the proposed PFAS regulation. Chapter 7 (in combination with Appendices A and B) presents estimated costs associated with engineering, installation, operation, and maintenance of each of the treatment and nontreatment options discussed in Chapters 2 through 6. Appendix A provides complete cost equations for the treatment and nontreatment options. Appendix B

³ POU devices are not currently a compliance option because the regulatory options under consideration require treatment to concentrations below the current NSF International/American National Standards Institute (NSF/ANSI) certification standard for POU device removal of PFAS. However, POU treatment might become a compliance option for small systems in the future if NSF/ANSI develop a new certification standard that mirrors EPA's proposed regulatory standard.

presents example cost model outputs for selected flow rates, allowing review of individual cost line items.

1.3 Information Sources

The information presented in this document is a summary of EPA's literature search to evaluate the state of science with respect to treatment options for PFAS-contaminated drinking source water. The objectives of the literature review were to:

- identify what technologies are being studied and tested
- summarize the data regarding effectiveness
- characterize other factors relevant for drinking water treatment (e.g., pre- and post-treatment requirements and waste characterization and management options)
- identify key research gaps.

1.4 References

Agency for Toxic Substances and Disease Registry (ATSDR). 2021. *Toxicological Profile for Perfluoroalkyls*. U.S. Department of Health and Human Services. Retrieved from <https://www.atsdr.cdc.gov/toxprofiles/tp200.pdf>

Buck, R.C., Franklin, J., Berger, U., Conder, J.M., Cousins, I.T., de Voogt, P., Jensen, A.A., Kurunthachalam, K., Mabury, S.S., and van Leeuwen, S.P. 2011. Perfluoroalkyl and polyfluoroalkyl substances in the environment: terminology, classification, and origins. *Integr Environ Assess Manag*, 7(4), 513-541. <https://doi.org/10.1002/ieam.258>

Interstate Technology Regulatory Council (ITRC). 2020. Naming Conventions and Physical and Chemical Properties of Per- and Polyfluoroalkyl Substances (PFAS). Retrieved from https://pfas-1.itrcweb.org/fact_sheets_page/PFAS_Fact_Sheet_Naming_Conventions_April2020.pdf

National Center for Biotechnology Information (NCBI). 2021a. *PubChem Compound Summary for CID 9554, Perfluorooctanoic acid*. Retrieved from <https://pubchem.ncbi.nlm.nih.gov/compound/9554#section=2D-Structure>

NCBI. 2021b. *PubChem Compound Summary for CID 74483, Perfluorooctanesulfonic acid*. Retrieved from <https://pubchem.ncbi.nlm.nih.gov/compound/Perfluorooctanesulfonic-acid#section=2D-Structure>

Rogers, R.D., Reh, C.M., and Breysse, P. 2021. Advancing per- and polyfluoroalkyl substances (PFAS) research: an overview of ATSDR and NCEH activities and recommendations. *J Expo Sci Environ Epidemiol*, 31(6), 961-971. <https://doi.org/10.1038/s41370-021-00316-6>

U.S. Environmental Protection Agency (USEPA). 2021a. *Drinking Water Treatability Database: Per- and Polyfluoroalkyl Substances*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=11020>

USEPA. 2021b. *Drinking Water Treatability Database: Perfluorooctane Sulfonate*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10940>

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USEPA. 2021c. *Drinking Water Treatability Database: Perfluorooctanoic Acid*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10520>

USEPA. 2021d. *CompTox Chemicals Dashboard: PFAS structures in DSSTox (update August 2021)*. Retrieved from <https://comptox.epa.gov/dashboard/chemical-lists/PFASSTRUCTv4>

Weaver, J. 2020. PFAS should be managed as a single class of chemicals, experts say. *Environmental Factor*. National Institute of Environmental Health Sciences. Retrieved from <https://factor.niehs.nih.gov/2020/8/papers/pfas/index.htm>

2.0 Granular Activated Carbon (GAC)

2.1 Operating Principle

GAC is a porous adsorptive media with extremely high internal surface area. GAC is manufactured from a variety of raw materials with porous structures including bituminous coal, lignite coal, peat, wood, coconut shells, and others. Physical and/or chemical manufacturing processes are applied to these raw materials to create and/or enlarge pores, resulting in a porous structure with a large surface area per unit mass.

When water is treated with GAC, it passes through treatment columns or beds containing GAC. The process separates dissolved contaminants from the water through adsorption to the surfaces in the pores of the GAC. In the case of PFAS, the literature suggests that the primary mechanisms of adsorption include both hydrophobic and electrostatic interactions (Ateia et al., 2019). In addition to removing PFAS, GAC can remove contaminants including taste and odor compounds, natural organic matter, volatile organic compounds, synthetic organic compounds, disinfection byproduct precursors, and radon. Organic compounds with high molecular weights are also readily adsorbable.

The contaminants are adsorbed by GAC until the carbon is no longer able to adsorb additional molecules at the influent feed concentration. At this point, the result is reduced removal of the contaminant, referred to as “breakthrough.” Figure 2-1 is a conceptual diagram of the GAC treatment process, from initial adsorption to breakthrough. Once the contaminant concentration in the treated water reaches an unacceptable level, the carbon is considered “spent” and must be replaced by virgin or reactivated GAC. The length of time between GAC replacement events is known as “bed life,” discussed in more detail in Section 2.2.2. Reactivation⁴ is a process that removes adsorbed contaminants from adsorption sites on GAC so that it can be reused. Although different methods are available for GAC reactivation, the process most commonly involves high temperature thermal treatment in a specialized facility such as a multiple hearth furnace or rotary kiln (Matthis and Carr, 2018; USEPA, 2022). Section 2.5 provides more information on the fate of PFAS in the reactivation process.

GAC beds typically also require periodic backwash to prevent head loss or biomass accumulation. The backwash process must be designed to remove accumulated solids, while preventing the spent carbon at the top of the column from mixing with the unspent carbon at the bottom, creating a mixed bed and the possibility of “leakage” of the target contaminant.

⁴ The terms “reactivation” and “regeneration” are sometimes used interchangeably in the drinking water industry. GAC vendors, however, make a distinction between the two processes. The appropriate term for the process used on spent GAC containing adsorbed PFAS is reactivation (Matthis and Carr, 2018).

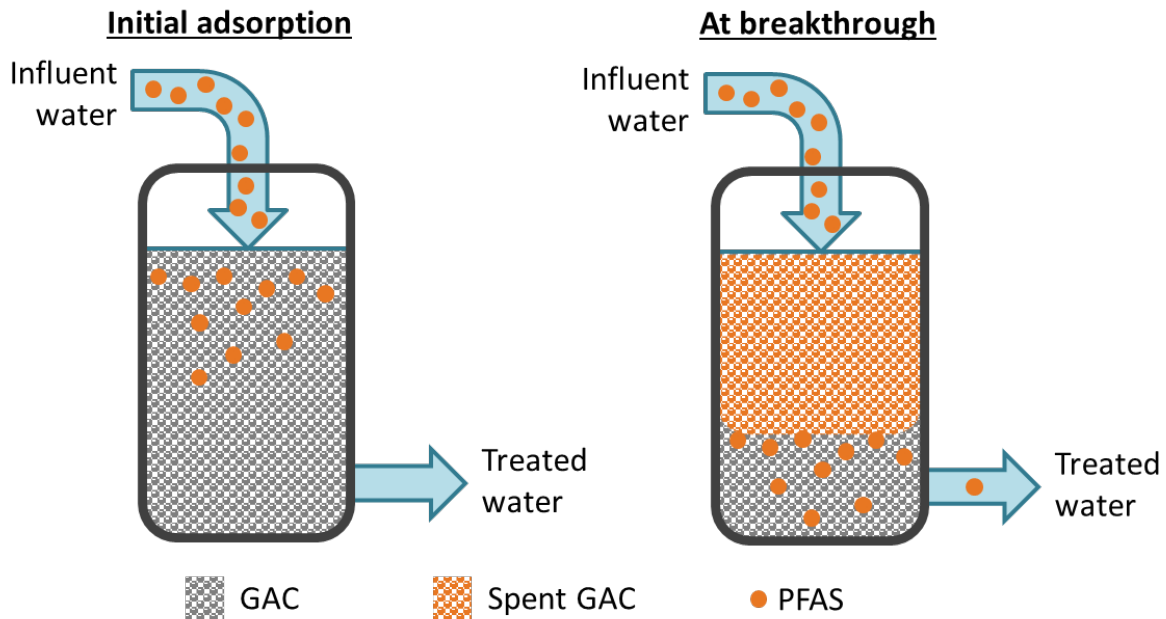


Figure 2-1. Conceptual Diagram of the GAC Treatment Process

The specific design of a GAC treatment facility depends on the type of contactor and the system configuration used. GAC can be set up in a single-stage, series, or parallel system. In drinking water treatment, GAC configuration generally is a downflow fixed (packed) bed system. The system can have single or multiple adsorbers operated under pressure or fed by gravity (Brady and Moran, 2012; Summers et al., 2011). Pressure contactors are more cost effective for small systems because they can be purchased off the shelf as prefabricated, packaged units. Pressure GAC systems can be operated at higher suspended solids concentrations with less frequent backwashing and over a wide range of flow rates due to the allowable pressure variances. Pressure GAC systems are also enclosed, so there is no visual observation of the system. Gravity contactor designs are generally used in larger installations (Brady and Moran, 2012; Summers et al., 2011). Gravity contactors can be sized larger than off-the-shelf pressure vessels and because common wall design can minimize space requirements. A gravity contactor design is better for systems that do not have large variances in flow, pressure, or turbidity (Summers et al., 2011). Figure 2-2 and Figure 2-3, respectively, provide schematic drawings for a pressure GAC facility and a gravity GAC facility.

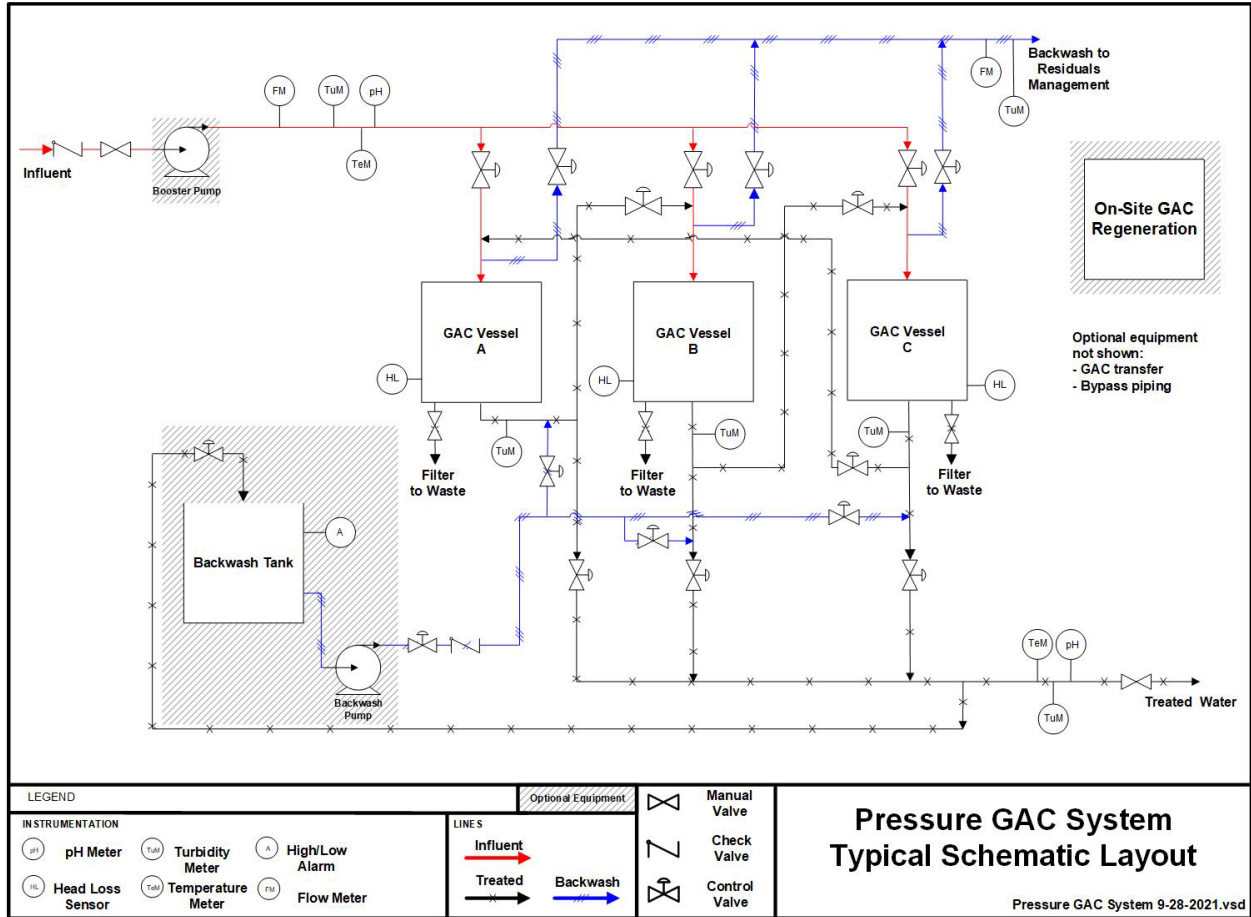


Figure 2-2. Typical Schematic Layout for Pressure GAC Treatment Facility

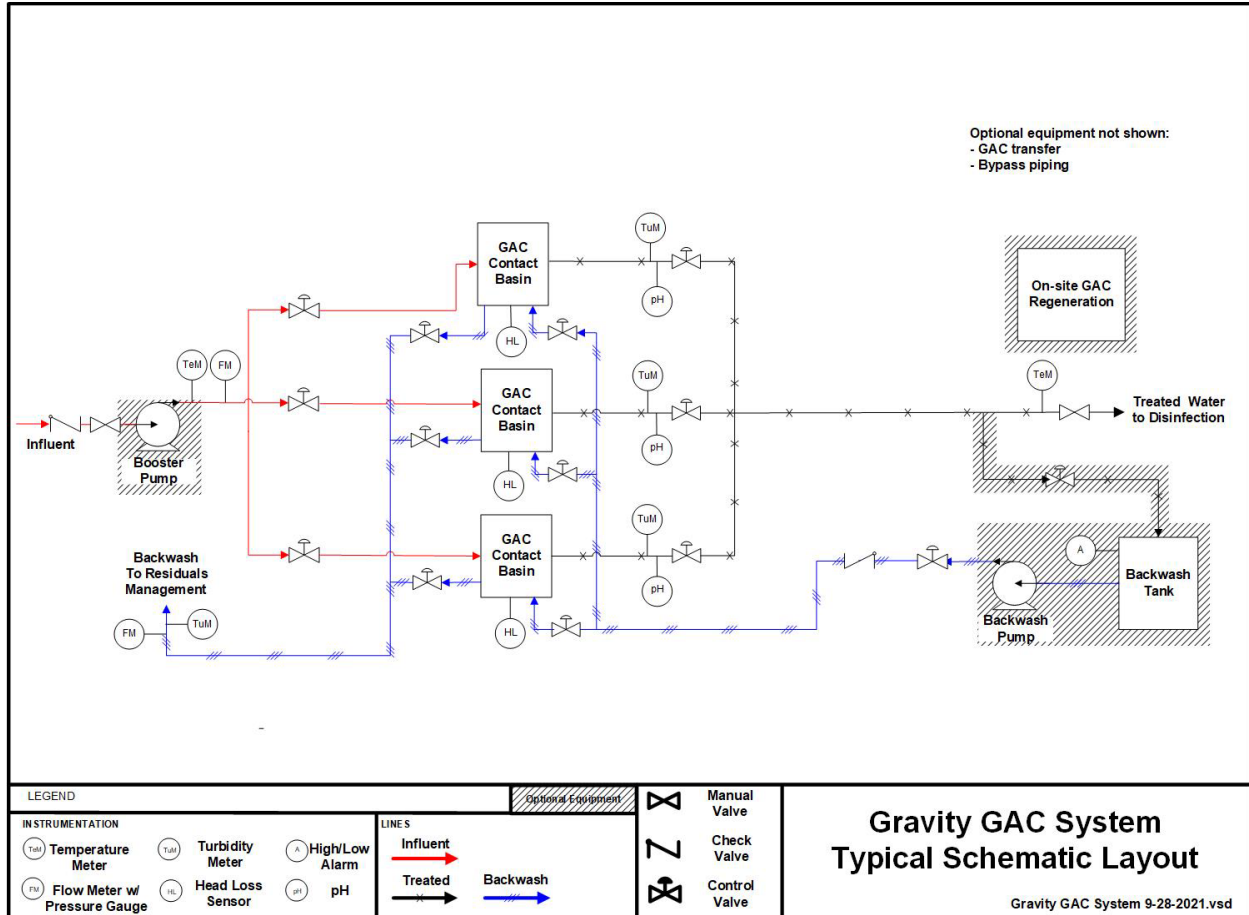


Figure 2-3. Typical Schematic Layout for Gravity GAC Treatment Facility

2.2 Effectiveness for PFAS Removal

2.2.1 Removal Efficiency

EPA’s Drinking Water Treatability Database (USEPA, 2021a; 2021b; 2021c) includes extensive data from the literature on PFAS removal by GAC. Results are available from studies conducted in the laboratory, in the field at pilot scale, and in full-scale application, as shown in Table 2-1, Table 2-2, and Table 2-3.⁵ These tables present the number of studies at each scale, along with a key benchmark of technology effectiveness: maximum removal efficiency. Removal efficiency is the percentage of the influent concentration removed through treatment.

The literature demonstrates maximum GAC removal efficiencies of 90 percent or greater for all the carboxylate and sulfonate PFAS compounds for which data are available. The literature also shows that the technology often removes these compounds to levels below analytical detection limits. For PFOA and PFOS, maximum removal efficiencies are greater than 99 percent, also to below analytical detection limits and lower than the regulatory thresholds currently under consideration. There are fewer studies of GAC performance for other (non-carboxylate and non-

⁵ Data shown in these tables are as of December 2021. EPA frequently updates the Drinking Water Treatability Database, so parties interested in results from recently published literature may wish to access the database directly at <https://tdb.epa.gov/tdb/home>.

sulfonate) PFAS compounds, but the available data show maximum removal efficiency of 90 percent or greater for many of these compounds, including HFPO-DA.

Table 2-1. Studies of GAC Treatment for Carboxylate PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFBA	4	8	5	5	99.5	Westreich et al. 2018
PFPeA	5	7	5	5	90	Appleman et al. 2013; McCleaf et al. 2017; Park et al. 2017; Lombardo et al. 2018; Kempisty et al. 2019; Liu et al. 2019; Park et al. 2020
PFHxA	6	12	6	6	99.5	Westreich et al. 2018
PFHpA	7	9	5	7	>99	Zeng et al 2020
PFOA	8	23	9	17	>99.8	Forrester and Bostardi 2019
PFNA	9	6	3	8	>99	Zeng et al 2020
PFDA	10	6	1	4	97	Appleman et al. 2013
PFUnA	11	1	0	1	90	McCleaf et al. 2017
PFDoA	12	3	0	0	90	McCleaf et al. 2017; Park et al. 2017
PFTriA	13	1	0	0	90	McCleaf et al. 2017

Sources: USEPA, 2021a; 2021c

Table 2-2. Studies of GAC Treatment for Sulfonate PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum Removal Efficiency	Source for Maximum Removal Efficiency
PFPrS	3	0	1	0	90	Liu et al. 2019
PFBS	4	13	7	8	99.5	Westreich et al. 2018
PFPeS	5	2	2	0	90	Liu et al. 2019
PFHxS	6	13	7	11	99.5	Westreich et al. 2018
PFHpS	7	2	4	1	>99	Belkouteb et al. 2020
PFOS	8	24	10	15	99.7	Woodard et al. 2017
PFNS	9	1	0	0	95.82	Wang et al. 2020

Sources: USEPA, 2021b; 2021c

Table 2-3. Studies of GAC Treatment for Other PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum Removal Efficiency	Source for Maximum Removal Efficiency
PFMOAA	3	0	0	1	70	Hopkins et al. 2018
FtS 4:2	4	0	1	0	Not reported	
PFBSA	4	1	0	0	56	Yan et al. 2020
PFO2HxA	4	0	0	1	90	Hopkins et al. 2018
PFO3OA	5	0	0	1	90	Hopkins et al. 2018
FtS 6:2	6	1	3	0	88	Casey et al. 2018
HFPO-DA	6	1	1	1	93	Hopkins et al. 2018
PFHxSA	6	1	1	0	80	Rodowa et al. 2020
PFO4DA	6	0	0	1	90	Hopkins et al. 2018
Nafion BP2	7	0	1	1	>99	Hopkins et al. 2018
FtS 8:2	8	1	3	0	88	Woodard et al. 2017
PFOSA	8	3	1	0	95	Kothawala et al. 2017
PFECHS	8	1	0	0	65	Yan et al. 2020

Source: USEPA, 2021c

2.2.2 Bed Life

In addition to removal efficiency, the effectiveness of GAC depends on bed life, which is the length of time the technology can maintain a target removal efficiency (e.g., 80 percent, 95 percent) or predefined concentration limit (such as an MCL). Bed life can be expressed as the number of days or months between GAC replacement events. It can also be expressed in bed volumes (BV), which is a measure of throughput: the volume of water treated during the bed life divided by the volume of the GAC bed. With either measure, a higher number indicates a longer bed life and more effective treatment.⁶ Figure 2-4 illustrates the concepts of breakthrough and bed life on a typical “S-shaped” GAC breakthrough curve.

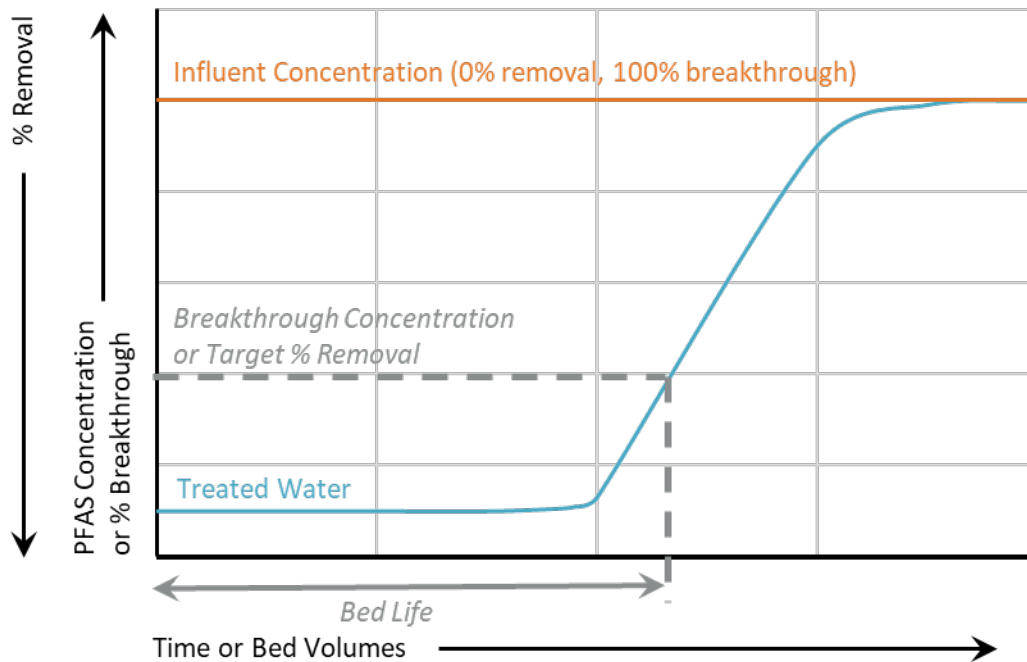


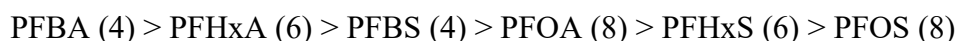
Figure 2-4. Typical GAC Breakthrough Curve

There is a consensus in the literature that GAC’s capacity for a given PFAS compound is strongly influenced by chain length (i.e., number of carbon atoms) and functional group (i.e., carboxylate versus sulfonate). In general, all other factors (see below) being equal, GAC exhibits a greater capacity for longer chain compounds than shorter chain compounds and a greater capacity for sulfonate PFAS than carboxylate PFAS. The greater capacity translates to longer bed life and lower treatment costs (Appleman et al., 2013; Appleman et al., 2014; Berretta et al., 2021; Inyang and Dickenson, 2017; McCleaf et al., 2017; Zeng et al., 2020).

For GAC, chain length appears to be the more important factor, followed by functional group. The results from Berretta et al. (2021) provide an example of a typical order of breakthrough.

⁶ A related measure is carbon use rate, which is often expressed in units of pounds of carbon used per 1,000 gallons of water treated. A lower carbon use rate reflects a longer bed life and more effective treatment. To avoid confusion, this document does not present data on carbon use rate.

From earliest breakthrough to latest, this typical sequence is as follows (with number of carbon atoms shown in parenthesis for ease of reference):



In addition to chain length and functional group, estimates of GAC bed life for PFAS removal depend on multiple factors. These additional factors can include the following:

- The target removal efficiency or predefined concentration at which the treated water quality is considered unacceptable (i.e., the “breakthrough” concentration)
- The influent concentration of the target PFAS compound(s)
- Other raw water quality parameters (see Section 2.3)
- Size of the GAC bed relative to the flow of water to be treated, measured by empty bed contact time (EBCT) (see Section 2.6.1)
- Adsorption properties of the specific GAC media (e.g., type of carbon, surface area, pore size distribution, and surface chemistry).

Because of these varying factors, comparing GAC bed life results across multiple studies is difficult. Section 2.6.3 discusses methods to estimate bed life as a critical parameter in the design and operation of GAC treatment.

2.2.3 Full-Scale Applications

Additional support for the effectiveness of GAC for PFAS removal is evident from the number of full-scale facilities that are currently using the technology. As indicated in Section 2.1.1, there are numerous studies of GAC performance for PFAS removal at full-scale facilities. These effectiveness studies include results for GAC facilities designed specifically to target PFAS, in addition to facilities originally designed for other contaminants. In total, the literature identifies more than 30 full-scale GAC facilities that specifically target the removal of PFAS from drinking water. Table 2-4 identifies these facilities.

Table 2-4. Full-scale GAC Systems Removing PFAS from Drinking Water

Location	Flow rate (MGD)	Groundwater or Surface Water	Year of Startup	Sources
Moose Creek, Fairbanks North Star Borough, Alaska	2.2	Groundwater	2016	Alaska Community Action on Toxics 2019; Forrester 2019
Gustavus, Alaska	Not reported	Groundwater	2018-2019	Alaska Community Action on Toxics 2019
Airline/Lambert Water Treatment Campus, Marana, Pima County, Arizona	Not reported	Groundwater	Not reported	Marana Water 2019
Liberty Utilities, Litchfield Park, Arizona	1.58	Groundwater	2017	ADEQ 2021; Forrester 2019
Picture Rocks Water Treatment Campus, Marana, Pima County, Arizona	Not reported	Groundwater	Not reported	Marana Water 2019
Municipal Services Commission of the City of New Castle, New Castle, Delaware	0.50	Groundwater	2015	Mordock 2016; Forrester 2019

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Location	Flow rate (MGD)	Groundwater or Surface Water	Year of Startup	Sources
Emerald Coast Utilities Authority, Pensacola, Escambia County, Florida	1.44	Groundwater	2017	Robinson 2018; Forrester 2019
Rome Water and Sewer Division, Rome, Georgia	9	Groundwater	Not reported	Forrester 2019; City of Rome 2019
Former Naval Air Station, Brunswick, Maine	Not reported	Not reported	2011	Danko 2018
Kennebunk, Kennebunkport & Wells Water District, Kennebunk, Maine	2.90	Groundwater	2020	Berretta et al. 2021; Business Wire 2018
Mary Dunn Water Supply Wells, Hyannis & Town of Barnstable, Massachusetts	1.44	Groundwater	2015	Gallagher 2017; Forrester 2019
City of Westfield Department of Public Works, Westfield, Massachusetts	Not reported	Groundwater	2018	Westfield 2019
Plainfield Township, Kent County, Michigan	9	Groundwater	2018	Biolchini 2018
Ann Arbor Water Treatment Plant, Ann Arbor, Michigan	50	Surface Water	2018	Stanton 2019; Page 2020
Oakdale Public Works, Oakdale, Minnesota	3.6	Groundwater	2006	MDH 2010; ATSDR 2008
Merrimack Village District Water Works, Merrimack, Hillsborough County, New Hampshire	Not reported	Groundwater	2020	Cronin 2020
Pease International Tradeport Drinking Water System, Portsmouth, New Hampshire	0.72	Groundwater	2019	City of Portsmouth 2020; Forrester 2019
Montclair Water Bureau, Montclair, New Jersey	0.72	Groundwater	Not reported	Forrester 2019; PFAS Project Lab 2021
Passaic Valley Water Commission, Garfield, New Jersey	0.5	Groundwater	Not reported	Forrester 2019; Sobko 2021
Hampton Bays Water District, Suffolk County, New York	9	Groundwater	2018	Gordon 2018
Suffolk County Water Authority, New York	Not reported	Groundwater	2017	SCWA 2018
Town of Petersburg Water District, Petersburg/Rensselaer County, New York	0.07	Not reported	2017	Forrester 2019; NYS DEC 2020a
Washington Lake Filtration Plant, Newburgh, New York	8.86	Groundwater	2017	Forrester 2019; NYS DEC 2020b
Little Hocking Water Association, Little Hocking, Ohio	Not reported	Groundwater	2007	Cummings et al 2015
Village of Hoosick Falls, New York	1.01	Groundwater	Not reported	Forrester 2019; NYS DEC 2021

Location	Flow rate (MGD)	Groundwater or Surface Water	Year of Startup	Sources
Sweeny Water Treatment Plant, Cape Fear Public Utilities Authority, North Carolina	44	Surface Water	2022	Vandermeijden and Hagerty 2020
Wright-Patterson Air Force Base, Dayton, Ohio	2.74	Groundwater	2017	Barber 2017; Forrester 2019
Aqua Pennsylvania, Chalfont Borough, Pennsylvania	0.58	Groundwater	Not reported	Forrester 2019; Chalfont Borough 2021
Horsham Water and Sewer Authority, Horsham, Montgomery County, Pennsylvania	1.44	Groundwater	2017	Boodoo et al. 2019; Montgomery News 2017; Forrester 2019
Warrington Township Water and Sewer Department, Warrington, Pennsylvania	0.58	Groundwater	Not reported	Forrester 2019; Warrington Township 2017
City of El Campo Water Department, El Campo, Texas	Not reported	Groundwater	2017	Sullivan 2018
Airway Heights Water System, City of Airway Heights, Washington	Not reported	Groundwater	2018	ATSDR 2020
Joint Base Lewis-McChord, Washington	Not reported	Groundwater	Not reported	Sullivan 2018
Issaquah, Washington	4.32	Groundwater	2016	City of Issaquah 2020; Mende 2019; Kwan and York 2017
Parkersburg Utility Board, Parkersburg, West Virginia	Not reported	Not reported	Not reported	USEPA 2009

MGD = million gallons per day

2.3 Raw Water Quality Considerations

Natural organic matter, often measured as dissolved organic carbon (DOC) or total organic carbon (TOC), can interfere with GAC's capacity to adsorb PFAS (Appleman et al., 2013; Ateia et al., 2019; Berretta et al., 2021; Gagliano et al., 2020; Kothawala et al., 2017). The significance of this interference may depend on the specific type of natural organic matter present (Gagliano et al., 2020; Kothawala et al., 2017). However, in general, it does not necessarily reduce the maximum removal effectiveness of GAC. Instead, it shortens the time to breakthrough, meaning more frequent GAC replacement can be required at higher TOC concentrations, all other factors being equal. Therefore, it should be possible to reliably manage the impact of natural organic matter through piloting, selection of design parameters, and operational monitoring. For purposes of estimating national costs for GAC, EPA used a method to estimate bed life that explicitly includes consideration of influent TOC (see Sections 2.6.3 and 7.2.1).

The presence of other adsorbable contaminants can reduce GAC capacity for a target contaminant, as the contaminants compete for adsorption sites on the media. The extent of this competition depends on the relative concentrations and adsorbability of the contaminants. However, when a poorly adsorbed contaminant is present and not a treatment target, the system can allow the contaminant to breakthrough, reducing its impact on GAC capacity for the target

contaminant(s) (Stenzel and Merz, 1989). When multiple target contaminants (e.g., multiple PFAS compounds) are present, GAC operation, specifically the selection of bed life, should consider competition among these contaminants. In extreme cases, where the GAC bed becomes highly saturated with contaminants, preferred contaminants in the influent can displace previously adsorbed, less preferred contaminants. Such cases can result in a phenomenon known as chromatographic peaking, where the treated concentration of a less preferred contaminant exceeds its influent concentration (Brady and Moran, 2012). Appleman et al. (2014) reported this phenomenon for PFBA at a full-scale GAC system removing PFAS. McCleaf et al. (2017) observed similar behavior for PFBA and PFPeA in column tests. Like TOC, the impact of competition among target contaminants, including the potential for chromatographic peaking, can be managed through piloting, selection of design parameters, and operational monitoring. For purposes of estimating national costs for GAC, EPA used a method to estimate bed life that is based on data from studies where multiple PFAS compounds were present in concentrations typical of PFAS-contaminated drinking water (see Sections 2.6.3 and 7.2.1).

2.4 Pre- and Post-Treatment Needs

Because GAC also works as a filtration medium, solids in influent water can accumulate in the GAC bed, causing excess pressure drop and increased backwash frequency. Therefore, under some circumstances, pre-filtration should be included. Such circumstances are site-specific, but examples include when upstream treatment includes coagulant addition for solids removal or when there is the potential for formation of iron and manganese precipitates (Stenzel and Merz, 1989; Summers et al., 2011). Chlorination prior to GAC treatment is not generally recommended because of the potential for the chlorine compounds to react with adsorbed compounds or the GAC itself (Brady and Moran, 2012; Summers et al., 2011).

In some cases, there can be temporary water chemistry changes immediately following GAC changeout, such as leaching of metals (e.g., arsenic, antimony), increases in pH, or release of fines which are small particles or powdered materials (Brady and Moran, 2012). These effects are readily managed by using pre-treated GAC media or diverting the first few bed volumes of treated water to waste and do not typically require post-treatment.

2.5 Waste Generation and Residuals Management Needs

The most likely management option for spent GAC containing adsorbed PFAS is reactivation. There are a number GAC vendor-operated reactivation facilities available, including some that hold Resource Conservation and Recovery Act (RCRA) permits to treat spent GAC that is classified as hazardous waste (USEPA, 2020; Matthis and Carr, 2021). Matthis and Carr (2021) report results from leaching tests on GAC used to remove PFAS from drinking water at full-scale after reactivation, also in a full-scale facility. They found that 15 of the 16 PFAS compounds analyzed were below analytical limits in the leachate. PFBA was present, but only at 1.9 parts per trillion. These results suggest that reactivated GAC should be suitable for reuse.

The full-scale study in Matthis and Carr (2021), however, did not fully address the fate of PFAS in the GAC reactivation process. There are a limited number of smaller scale studies that have examined whether PFAS compounds are transformed, volatilized, or destroyed/defluorinated during the process (e.g., Watanabe et al., 2016; Watanabe et al., 2018; Xiao, 2020). These studies suggest that the fate of PFAS in GAC reactivation depends on factors including PFAS chain

length, reactivation temperature, and combustion atmosphere (Baghirzade et al., 2021). Additional full-scale research might be needed if future air quality regulations address PFAS emissions from GAC reactivation facilities. The results of this research might necessitate changes to spent GAC management practices. Future RCRA hazardous waste regulations for PFAS could also limit the available management options.

GAC systems also intermittently generate a liquid residual in the form of spent backwash. Like conventional filters, GAC contactors must be backwashed periodically to remove solids, maintain the desired hydraulic properties of the bed, and possibly to control biological growth. Backwash does not remove adsorbed contaminants from the GAC bed, although some attrition or loss of actual GAC particles may occur during the backwash process. Therefore, spent backwash water contains primarily suspended solids and not target contaminants. The interval between backwash occurrences is mainly a function of the turbidity in the influent water. Management options for spent backwash include discharge to surface water under a National Pollutant Discharge Elimination System (NPDES) permit, discharge to a wastewater treatment plant (WWTP), or recycle to the head of the treatment plant. For some small systems, another option may be discharge to an on-site septic system.

When averaged over the time between generation events, backwash flow is relatively low. Instantaneous flow during a backwash event, however, is much higher. If spent backwash is recycled to the head of a treatment plant, recommended engineering practice is that the recycle stream should be no more than 5 to 10 percent of total system flow (USEPA, 2002; USEPA, 1996). Thus, when backwash is recycled, the system should include a spent backwash holding tank to prevent recycle flow from exceeding this recommendation. Holding tanks also may be advisable for other backwash management options (e.g., to prevent instantaneous flow from overwhelming the capacity of a WWTP).

2.6 Critical Design Parameters

Critical design parameters for GAC systems removing PFAS are:

- EBCT
- Contactor configuration (number of vessels in series)
- Bed life
- Residuals management options.

Section 2.5 discusses residuals management options. The sections below discuss EBCT, contactor configuration, and bed life in more detail, including the data available in the literature for these parameters. Section 7.2.1 identifies the specific values for each parameter used in EPA's cost estimates. Values for other GAC design parameters (e.g., loading rate, backwash frequency), while not specifically addressed here, are well documented for GAC treatment in general. EPA has no reason to expect a significant difference in these parameters for GAC systems treating PFAS compounds.

2.6.1 Empty Bed Contact Time

For a given set of site-specific conditions, there is a minimum EBCT required to produce water of a target quality. EBCT, measured in minutes, is defined by the following equation:

$$EBCT \text{ (in minutes)} = \frac{\text{Volume of GAC Bed}}{\text{Volumetric Flow Rate (per minute)}}$$

The minimum EBCT required varies depending on the specific contaminant treated, the required contaminant removal percentage, the type of GAC used, and other influent water characteristics. Full-scale GAC treatment systems that are purpose-built for PFAS removal and for which EBCT data are available use EBCTs between 7.6 and 26 minutes (Appleman et al., 2014; Boodoo, 2018; Forrester and Mathis, 2018; Kwan and York, 2017; Vandermeiden and Hagerty, 2020). GAC vendors commonly recommend a minimum EBCT of 20 minutes for PFAS removal (Calgon Carbon, 2018; Forrester and Mathis, 2017; 2018).

2.6.2 Contactor Configuration

GAC treatment systems with multiple contactors can be configured in parallel or in series. The schematic diagrams in Section 2.1 show contactors in parallel (in Figure 2-2) and in series (in Figure 2-3). In a series (or lead/lag) configuration, water flows first through an initial contactor that serves as a roughing contactor, then through subsequent contactors that serve as polishing contactors. Each contactor in the series typically has an equal EBCT such that the total EBCT of the series provides the design EBCT. In a parallel configuration, flow is divided equally among the contactors, each of which provides the design EBCT (Brady and Moran, 2012).

A series (or lead/lag) configuration serves the purpose of treating a greater water volume than one contactor with similar bed volume. When GAC in the roughing contactor is spent, this media is replaced and the polishing contactor moves to the start of the series, becoming the roughing contactor. The use of vessels in series can allow the carbon in the lead vessel to reach saturation, increasing total capacity (Brady and Moran, 2012; Summers et al., 2011).

A parallel configuration can also increase total capacity by staggering GAC replacement events. In this arrangement, individual contactors can approach saturation, providing lower removal efficiency, while other, more recently replaced contactors are exceeding the required removal efficiency. Correctly operated, the resulting blended flow will meet the treatment goal (Brady and Moran, 2012; Summers et al., 2011). Systems can use a configuration that combines series and parallel operation (i.e., multiple trains in parallel, each train with contactors in series).

Full-scale GAC treatment systems that are purpose-built for PFAS removal and for which configuration data are available are pressure systems that use two vessels in series (Appleman et al., 2014; Berretta et al., 2021; Boodoo, 2018; Forrester and Mathis, 2018; Kwan and York, 2017; Vandermeiden and Hagerty, 2020). For pressure systems removing PFAS, design engineers and GAC vendors commonly recommend two vessels in series (Anderson et al., 2021; Calgon Carbon, 2018; Forrester and Mathis, 2017; 2018). Gravity systems typically do not use series operation.

2.6.3 Bed Life

As discussed in Section 2.2.2, GAC bed life depends on a number of factors. Designers should select EBCT and contactor configuration to maximize bed life. Although bed life data are available from full-scale systems removing PFAS, these data are of limited usefulness because of one or more of the following factors:

- Influent PFAS concentrations that are highly variable over time, with frequent non-detections
- A limited number of PFAS compounds monitored
- GAC reactivation or replacement prior to PFAS detection in treated water.

More extensive data are available in the literature from pilot studies and rapid small scale column tests (RSSCTs). RSSCTs are laboratory tests designed and operated under hydraulic and influent water conditions that are calibrated to simulate those in full-scale adsorbers. The simulation considers fluid dynamic parameters such as flow rate, GAC particle size, Reynolds number, diffusivity and others (Crittenden et al., 1991). RSSCTs have the advantage of being less time-consuming than pilot-studies or full-scale studies, where reaching breakthrough can require months or years.

Comparing and synthesizing bed life data from pilot studies and RSSCTs is complicated by variations in study design (e.g., water quality, EBCT, type of GAC). To develop a practical method of estimating bed life for purposes of estimating national costs for GAC, EPA used data from six studies covering 10 water quality conditions. EPA selected these studies for the following reasons:

- The studies are peer-reviewed publications
- Bed life data were tabulated in or readily interpolated from the published literature
- Multiple PFAS compounds were present in concentrations typical of PFAS-contaminated drinking water
- The studies measured natural organic matter (as TOC or DOC) and it was present in concentrations typical of drinking water sources
- The studies presented data for a EBCT of 10 minutes, providing a consistent and comparable measure of bed volumes across the studies.

Table 2-5. Studies Used to Develop GAC Bed Life Estimates

Study	Study Type	Number of Water Quality Conditions	Influent TOC (mg/L)	PFAS Compounds Present and Monitored
Burkhardt et al., 2022	Pilot	3	1.8 to 3.2(a)	PFBA(b), PFPeA(b), PFHxA, PFOA, PFNA(b), PFDA(b), PFBS, PFPeS(b), PFHxS, PFOS, PFNS(b), HFPO-DA(c)
Liu et al., 2019	Pilot	1	2.7(d)	PFPeA(b), PFHxA, PFHpA, PFOA, PFPrS(b), PFBS, PFPeS(b), PFHpS(b), PFHxS, PFOS
McNamara et al., 2018	CD-RSSCT	1	1.42	PFOA, PFOS
Park et al., 2020	CD-RSSCT	2	0.53 and 0.78	PFPeA(b), PFHxA, PFHpA, PFOA, PFBS, PFOS
Patterson et al., 2018	CD-RSSCT	1	2.3 to 2.4	PFHpA, PFOA, PFNA(b), PFBS, PFHxS, PFOS
Zeng et al., 2020	CD-RSSCT	2	0.4 and 0.88(d)	PFHxA, PFHpA, PFOA, PFBS, PFHxS, PFOS

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CD-RSSCT = constant diffusivity rapid small scale column test; DOC = dissolved organic carbon; TOC = total organic carbon
 Notes:

- (a) Includes unpublished TOC data from PFAS pilot study
- (b) EPA was not able to develop a breakthrough relationship for this compound
- (c) Other non-carboxylate, non-sulfonate PFAS were also present and monitored
- (d) Influent DOC

EPA pooled the data from all the studies. When the studies compared different types of GAC, EPA selected the data for the best performing GAC, assuming that systems would not use underperforming media in practice. EPA then used multiple linear regression to develop a model that results in compound-specific bed life equations.

EPA recognizes that PFAS breakthrough curves are not linear. However, to develop the equations, EPA specifically used the data from the last point of non-detection to the first instance of complete breakthrough (or the end of the study, whichever came first). By limiting the data to this range, EPA sought to characterize the portion of the breakthrough curve where bed life changes rapidly with removal efficiency. This portion of the curve is of most interest in selecting a target bed life for purposes of cost estimating and is expected to be more approximately linear than the curve overall. Figure 2-5 shows this concept graphically in relation to a typical theoretical breakthrough curve.

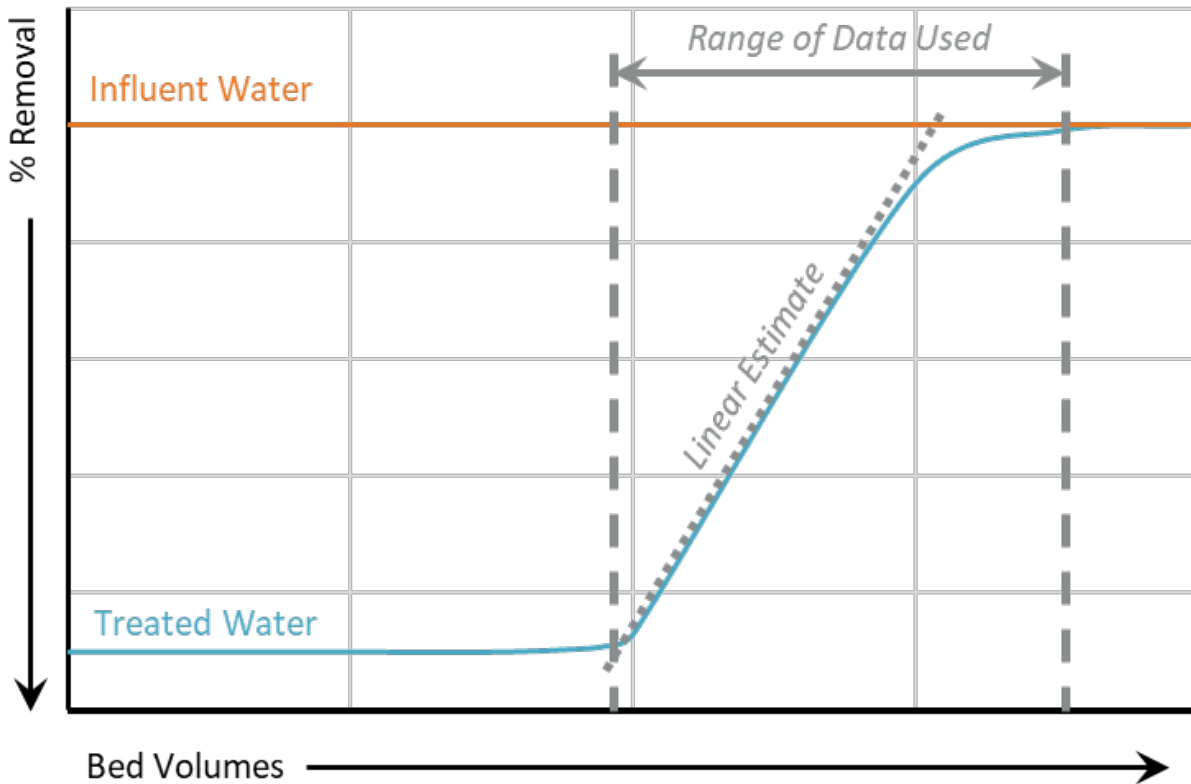


Figure 2-5. Linear Bed Life Estimate in Relation to a Typical Breakthrough Curve

The resulting PFAS compound-specific bed life equations for GAC take the following form:

$$BV_{contam,GAC} = A_{TOC} \times TOC + A_{R,GAC} \times \%R_{contam} + B_{contam,GAC}$$

Where:

- $BV_{\text{contam,GAC}}$ = GAC bed life for a given PFAS contaminant in BV
- TOC = influent TOC in milligrams per liter (mg/L)
- $\%R_{\text{contam}}$ = target percent removal of a given PFAS as a decimal (e.g., 0.8, 0.95)
- A_{TOC} , $A_{\text{R,GAC}}$, and $B_{\text{contam,GAC}}$ are parameters derived in the regression analysis. Table 2-6 shows their estimated values.

Table 2-6. Estimated Parameter Values for GAC Bed Life Equations

Parameter	GAC Model Value
A_{TOC}	-37,932
A_{R}	-36,309
$B_{\text{HFPO-DA}}$	113,034
B_{PFHxA}	113,967
B_{PFBS}	129,357
B_{PFHpA}	129,357
B_{PFHxS}	129,357
B_{PFOA}	139,862
B_{PFOS}	143,731

The parameter values result in the following order of breakthrough from earliest to latest, given a constant influent TOC and target percent removal:

$$\text{HFPO-DA} > \text{PFHxA} > \text{PFBS} = \text{PFHpA} = \text{PFHxS} > \text{PFOA} > \text{PFOS}$$

This result is generally consistent with the typical expectation, as discussed in Section 2.2.2, that shorter chain compounds break through before longer chain compounds and carboxylates break through before sulfonates. The equations predict identical bed lives for PFBS, PFHpA, and PFHxS because the intercept terms for these compounds (B_{PFBS} , B_{PFHpA} , and B_{PFHxS}) were not significantly different from each other statistically. All compounds share the same slope term (A_{TOC}) for influent TOC (in mg/L) and the same slope term (A_{R}) for percent removal of the PFAS compound (as a decimal) because specifying the model this way results in a consistent order of breakthrough across the range of possible influent TOC values and percent removal values. The model has an adjusted R^2 of 0.62. The overall model and individual coefficients are statistically significant. Note that the equations are valid only up to a TOC of 3.2 mg/L, the maximum value in the data set used.

Because the equations are based on pooled data, they reflect central tendency results under varying water quality conditions. As such, the EPA believes they represent the best approach for estimating national cost given the data currently available in the literature. However, these equations should not be used in lieu of site-specific engineering analyses or pilot studies to guide the design or operation of specific treatment systems.

As discussed above, the equations are based in part on RSSCT data. For PFAS removal, there is no consensus in the literature regarding methods to scale up GAC from RSSCTs to full-scale.

There are concerns that RSSCT results may, in some cases, overestimate full-scale bed life (Hopkins, 2021; Kempisty et al., 2019; Meng et al., 2021; Redding et al., 2019). The degree of this potential overestimation is not certain. To compensate for this potential overestimation, when applying the bed life equations, EPA did not incorporate the increase in bed life that would be expected from operating multiple contactors in series or parallel (see Section 2.6.2). Section 7.2.1 discusses this topic, and the application of the bed life equations generally, in more detail.

2.7 References

- Alaska Community Action on Toxics. DeFazio, D. and Tynan, T. 2019. *Threats To Drinking Water and Public Health In Alaska: The Scope Of The PFAS Problem, Consequences Of Regulatory Inaction, And Recommendations*. Retrieved from: <https://www.akaction.org/wp-content/uploads/Report-Threats-to-Drinking-Water-and-Public-Health-in-Alaska-FINAL-web-version-9-24-19.pdf>
- Agency for Toxic Substances and Disease Registry (ATSDR). 2008. *Perfluorochemical Contamination in Lake Elmo Final Release and Oakdale, Washington County, Minnesota*. Retrieved from: https://www.atsdr.cdc.gov/HAC/pha/PFCsLakeElmo/PFCs_in_Lake_Elmo_PHA_8-29-2008_508.pdf
- Agency for Toxic Substances and Disease Registry (ATSDR). 2020. *PFAS Exposure Assessment Airway Heights, Spokane County, WA*. Retrieved from: <https://www.atsdr.cdc.gov/pfas/docs/factsheet/Spokane-Factsheet-508.pdf>
- Anderson, J., Meng, P., Sidnell, T., and Ross, I. 2021. Advances in Remediation of PFAS-impacted Waters. In Kempisty, D.M. and Racz, L. (Eds.), *Forever Chemicals: Environmental, Economic, and Social Equity Concerns with PFAS in the Environment* (pp. 189-209). CRC Press. <https://doi.org/10.1201/9781003024521>
- Appleman, T.D., Higgins, C.P., Quinones, Q., Vanderford, B.J., Kolstad, C., Zeigler-Holady, J.C., and Dickenson, E.R.V. 2014. Treatment of poly- and perfluoroalkyl substances in U.S. full-scale water treatment systems. *Water Research*, 51(2014), 246-255. <http://dx.doi.org/10.1016/j.watres.2013.10.067>
- Appleman, T.D., Dickenson, E.R.V., Bellona, C., and Higgins, C.P. 2013. Nanofiltration and granular activated carbon treatment of perfluoroalkyl acids. *Journal of Hazardous Materials*, 260(2013), 740-746. <http://dx.doi.org/10.1016/j.jhazmat.2013.06.033>
- Arizona Department of Environmental Quality (ADEQ). 2021. *Public Water System PFAS Data (Luke Air Force Base Area), PFAS Resources*. Retrieved from: <https://www.azdeq.gov/public-water-system-pfas-data-luke-air-force-base-area-pfas-resources>
- Ateia, M., Maroli, A., Tharayil, N., and Karanfil, T. 2019. The overlooked short- and ultrashort-chain poly- and perfluorinated substances: A review. *Chemosphere*, 220(2019), 866-882. <https://doi.org/10.1016/j.chemosphere.2018.12.186>
- Baghirzade, B.S., Zhang, Y., Reuther, J. F., Saleh, N. B., Venkatesan, A. K., and Apul, O. G. 2021. Thermal Regeneration of Spent Granular Activated Carbon Presents an Opportunity to

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Break the Forever PFAS Cycle. *Environmental Science & Technology*, 2021, 55, 5608–5619.
<https://doi.org/10.1021/acs.est.0c08224>

Barber, B. 2017. *Wright-Patt treating tainted water in contaminated drinking wells*. Dayton Daily News. Retrieved from: <https://www.daytondailynews.com/news/local/wright-patt-treating-tainted-water-contaminated-drinking-wells/WigOWMcSdQHNMYYE2bHCOK/>

Belkouteb, N., Franke, V., McCleaf, P., Kohler, S., and Ahrens, L. 2020. Removal of per- and polyfluoroalkyl substances (PFASs) in a full-scale drinking water treatment plant: Long-term performance of granular activated carbon (GAC) and influence of flow-rate. *Water Research*, 182(2020), 115913. <https://doi.org/10.1016/j.watres.2020.115913>

Berretta, C., Mallmann, T., Trewitz, K., and Kempisty, D.M. 2021. Removing PFAS from Water: From Start to Finish. In Kempisty, D.M. and Racz, L. (Eds.), *Forever Chemicals: Environmental, Economic, and Social Equity Concerns with PFAS in the Environment* (pp. 235-253). CRC Press. <https://doi.org/10.1201/9781003024521>

Biolchini, A. 2018. *First PFAS filters in place at Plainfield Township water plant*. MLive. Retrieved from: <https://www.mlive.com/news/grand-rapids/2018/06/first-pfas-filters-in-place-at.html>

Boodoo, F., Begg, T., Funk, T., Kessler, T., Shaw, E., and Pickel, M. 2019. *Polishing PFAS To Non-Detect Levels Using PFAS Selective Resin*. Water Online. Retrieved from: <https://www.wateronline.com/doc/polishing-pfas-to-non-detect-levels-using-pfas-selective-resin-0001>

Boodoo, F. 2018. *Short & Long Chain PFAS Removal to Non-Detect Level with Single-Use PFA694E Resin*. Presentation by Purolite Corporation. Retrieved from: <https://docs.house.gov/meetings/IF/IF18/20180906/108649/HHRG-115-IF18-20180906-SD027.pdf>

Brady, R. and Moran, M. 2012. Activated Carbon Adsorption. In Randtke, S.J. and Horsley, M.B. (Eds.), *Water Treatment Plant Design, Fifth Edition* (pp. 16.1-16.45). American Water Works Association/American Society of Civil Engineers.

Burkhardt, J.B., Burns, N., Mobley, D., Pressman, J.G., Magnuson, M.L, and Speth, T.F. 2022. Modeling PFAS Removal Using Granular Activated Carbon for Full-Scale System Design. *J. Environ. Eng.*, 148(3), 04021066. [https://doi.org/10.1061/\(ASCE\)EE.1943-7870.0001964](https://doi.org/10.1061/(ASCE)EE.1943-7870.0001964)

Business Wire. 2018. *Kennebunkport and Wells Water District to Remove PFAS with Evoqua's Granular Activated Carbon (GAC) System*. Business Wire. Retrieved from: <https://www.businesswire.com/news/home/20180521005092/en/Kennebunkport-Wells-Water-District-Remove-PFAS-Evoqua%E2%80%99s>

Calgon Carbon. 2018. *Calgon Carbon Overview and PFAS Specific Experience*. Presentation for EPA.

Casey, D., Goetz, B., Martin, B. 2018. *Case Study: Moving Beyond Carbon for More Effective PFAS Removal*. AWWA Water Quality Technology Conference. Toronto, ON.

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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Chalfont Borough. 2021. *Public Water Quality*. Borough Services for Chalfont Borough. Retrieved from: <https://www.chalfontborough.com/information/public-water-quality/>

City of Issaquah. 2020. *PFAS*. Retrieved from: <https://www.issaquahwa.gov/1742/PFAS>

City of Portsmouth – Department of Public Works. 2019. *Portsmouth Water System PFAS Update*. Retrieved from: <https://www.cityofportsmouth.com/publicworks/water/portsmouth-water-system-pfas-update>

City of Rome. 2019. *ROME WATER AND SEWER DIVISION – EPA UPDATE BRIEF (PFOA / PFOS)*. Retrieved from: <https://www.romeqa.us/DocumentCenter/View/204/PFAS-Update-2019-PDF>

City of Westfield Department of Public Works Water Division. 2019. *DRINKING WATER HEALTH ADVISORY UPDATE: Westfield Public Drinking Water System*. Retrieved from: <https://westfielddevelopment.com/DocumentCenter/View/8884/Drinking-Water-Health-Advisory---October-2019>

Crittenden, J. C., Reddy, P.S., Arora, H., Trynoski J., Hand, D.W., Perram, D.L., and Summers, R.S. 1991. Predicting GAC performance with Rapid Small-Scale Column Tests. *Journal AWWA*, 83(1), 77-87. <https://doi.org/10.1002/j.1551-8833.1991.tb07088.x>

Cronin, M. 2020. *Water filtration facility under construction to filter PFAS from Merrimack water*. WMUR9. Retrieved from: <https://www.wmur.com/article/water-filtration-facility-under-construction-to-filter-pfas-from-merrimack-water/30616073#>

Cummings, L., Matarazzo, A., Nelson, N., Sickels, F., and Storms, C. 2015. *Recommendation on Perfluorinated Compound Treatment Options for Drinking Water*. New Jersey Drinking Water Quality Institute Treatment Subcommittee. Retrieved from: <https://www.nj.gov/dep/watersupply/pdf/pfna-pfc-treatment.pdf>

Danko, A. 2018. *Treatment Technologies for PFAS Site Management*. Retrieved from: <https://frtr.gov/pdf/meetings/nov18/presentations/handouts/danko-handout.pdf>

Forrester, E. 2019. *Calgon Carbon PFAS Experience*. Calgon Carbon.

Forrester, E. and Bostardi, C. 2019. *PFAS Removal: GAC & IX*. Calgon Carbon Corporation. Webinar. April 23, 2019.

Forrester, E. and Mathis, J. 2018. *Treatment Solutions for PFAS Removal: Evaluating Total Cost*. Presentation by Calgon Carbon.

Forrester, E. and Mathis, J. 2017. *Treatment of Short Chain PFCs with Granular Activated Carbon*. Presentation by Calgon Carbon.

Gallagher, A. 2017. *NEWMOA Workshop: PFAS in the Northeast: State of Practice & Regulatory Perspectives*. Retrieved from: www.newmoa.org/events/docs/259_227/GallagherMA_May2017_final.pdf

Gordon, V. 2018. *Hampton Bays Water District Gets Green Light to Turn On Two Of Three Wells*. The Southampton Press. Retrieved from: <https://www.27east.com/southampton-press/southampton-news/hampton-bays-water-district-gets-green-light-to-turn-on-two-of-three-wells-1568745/>

Hopkins, Z.R. 2021. *Granular Activated Carbon Adsorption of Per- and Polyfluoroalkyl Substances - from Scale-Up to Factors Affecting Performance*. Doctoral Dissertation, North Carolina State University. ProQuest Dissertations Publishing. 29004569.

Hopkins, Z.R., Sun, M., DeWitt, J.C., and Knappe, D.R.U. 2018. Recently Detected Drinking Water Contaminants: GenX and Other Per- and Polyfluoroalkyl Ether Acids. *Journal AWWA*, 110(7), 13-28. <https://doi.org/10.1002/awwa.1073>

Inyang, M. and Dickenson, E.R.V. 2017. The use of carbon adsorbents for the removal of perfluoroalkyl acids from potable reuse systems. *Chemosphere*, 184, 167-175. <http://dx.doi.org/10.1016/j.chemosphere.2017.05.161>

Kempisty, D.M., Arevalo, E., Reinert, A., Edeback, V., Dickenson, E., Husted, C. Higgins, C.P., Summers, R.S., and Knappe, D.R.U. 2019. *Adsorption of per and polyfluoroalkyl acids from ground and surface water by granular activated carbon*. AWWA Water Quality Technology Conference, Dallas, TX.

Kothawala, D.N., Kohler, S.J., Ostlund, A., Wiberg, K., and Ahrens, L. 2017. Influence of dissolved organic matter concentration and composition on the removal efficiency of perfluoroalkyl substances (PFASs) during drinking water treatment. *Water Research*, 121(2017), 320-328. <http://dx.doi.org/10.1016/j.watres.2017.05.047>

Kwan, P., and York, B. 2017. *City of Issaquah's Treatment Response after Detecting Perfluorinated Compounds*. AWWA Water Quality Technology Conference, Portland, OR.

Liu, Y.-L. and Sun, M. 2021. Ion exchange removal and resin regeneration to treat per- and polyfluoroalkyl ether acids and other emerging PFAS in drinking water. *Water Research*, 207(2021), 117781. <https://doi.org/10.1016/j.watres.2021.117781>

Liu, C., Werner, D., and Bellona, C. 2019. Removal of per- and polyfluoroalkyl substances (PFASs) from contaminated groundwater using granular activated carbon: a pilot-scale study with breakthrough modeling. *Environ. Sci.: Water Res. Technol.*, 2019(11). <https://doi.org/10.1039/c9ew00349e>

Lombardo, J., Berretta, C., Redding, A., Swanson, C., and Mallmann, T. 2018. *Carbon and Resin Solutions for PFAS Removal*. Evoqua Water Technologies Webinar. March 6.

Marana Water. 2019. *Updates: April/May 2019*. Retrieved from: <https://www.maranaaz.gov/water-project-water>

Matthis, J. and Carr, S. 2018. Reactivation of Spent Activated Carbon Used for PFAS Adsorption. In Kempisty, D.M, Xing, Y., and Racz, L. (Eds.), *Perfluoroalkyl Substances in the Environment: Theory, Practice, and Innovation* (pp. 303-323). Taylor & Francis. <https://doi.org/10.1201/9780429487125>

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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McCleaf, P., Englund, S., Ostlund, A., Lindegren, K., Wiberg, K., and Ahrens, L. 2017. Removal Efficiency of Multiple Poly- and Perfluoroalkyl Substances (PFASs) in Drinking Water using Granular Activated Carbon (GAC) and Anion Exchange (AE) Column Tests. *Water Research*, 120: 77-87. <http://dx.doi.org/10.1016/j.watres.2017.04.057>

McNamara, J., Franco, R., Mimna, R., and Zappa, L. 2018. Comparison of Activated Carbons for Removal of Perfluorinated Compounds from Drinking Water. *Journal AWWA*, 110(1), E2-E14. <https://doi.org/10.5942/jawwa.2018.110.0003>

Mende, B. 2019. *Acting Fast to Remove PFAS*. AWWA Water Quality Technology Conference, Dallas, TX.

Meng, P., Hopkins, Z., Tang, T., Liu, C., Bellona, C., and Knappe, D.R.U. 2021. *PFAS removal by GAC: What are drivers for GAC use rate?* AWWA Water Quality Technology Conference, Tacoma, WA.

Minnesota Department of Health (MDH). 2010. *Oakdale and 3M Work Together to Remove Perfluorochemicals*. Waterline. Retrieved from: <https://www.health.state.mn.us/communities/environment/water/waterline/featurestories/oakdale.html>

Montgomery News. 2017. *Horsham Township Council members inspect new water filter*. The Reporter. Retrieved from: <https://www.thereporteronline.com/news/times-chronicle-public-spirit/>

Mordock, J. 2016. *In Delaware, C8 contamination blamed on firefighting foam*. The News Journal. Retrieved from: <https://www.delawareonline.com/story/money/2016/04/01/delaware-c8-contamination-blamed-firefighting-foam/81538418/>

New York State Department of Environmental Conservation (NYS DEC). 2021. *Hoosick Falls Area Information for Communities Impacted by Per- and Poly-fluorinated Alkyl Substances (PFAS)*. Retrieved from: <https://www.dec.ny.gov/chemical/108791.html>

NYS DEC. 2020a. *Newburgh Information for Communities Impacted by Per- and Polyfluoroalkyl Substances (PFAS)*. Retrieved from: <https://www.dec.ny.gov/chemical/108825.html>

NYS DEC. 2020b. *Petersburgh Information for Communities Impacted by Perfluorinated Compounds (PFCs)*. Retrieved from: <https://www.dec.ny.gov/chemical/108820.html>

Page, S. 2020. *Quantifying GAC Performance for PFAS Removal at a Surface Water Treatment Plant*. Retrieved from: https://cdn.ymaws.com/mi-water.site-ym.com/resource/resmgr/docs/borchardt_2020_presentations/07_-_borchardtconf-quantgacp.pdf

Park, M., Wu, S., Lopez, I., and Snyder, S. 2017. *Granular activated carbon (GAC) adsorption for perfluorinated alkylsubstances (PFASs) attenuation in groundwater*. AWWA Water Quality Technology Conference. Portland, OR.

Park, M., Wu, S., Lopez, I.J., Chang, J.Y., Karanfil, T., and Snyder, S.A. 2020. Adsorption of perfluoroalkyl substances (PFAS) in groundwater by granular activated carbons: Roles of

hydrophobicity of PFAS and carbon characteristics. *Water Research*, 170(2020), 115364.
<https://doi.org/10.1016/j.watres.2019.115364>

Patterson, C., Burkhardt, J., Schupp, D., Krishnan, R., Dymont, S., Merritt, S., Zintek, L., and Kleinmaier, D. 2018. Effectiveness of point-of-use/point-of-entry systems to remove per- and polyfluoroalkyl substances from drinking water. *AWWA Water Science*, 1(2), e1131.
<https://doi.org/10.1002/aws2.1131>

PFAS Project Lab. 2021. *Montclair, New Jersey*. Retrieved from:
<https://pfasproject.com/montclair-new-jersey/>

Redding, A., Grieco, S., Roth, J., and Forrester, E. 2019. *Validation of Rapid Small-Scale Column Tests (RSSCTs) to Replicate Large Scale Systems for PFAS*. AWWA Water Quality Technology Conference, Dallas, TX.

Robinson, K. 2018. *ECUA sues national manufacturers over contamination of Escambia water wells*. Pensacola News Journal. Retrieved from:
<https://www.pnj.com/story/news/2018/06/26/ecua-sues-over-contaminated-water-wells/731268002/>

Rodowa, A. E., Knappe, D. R., Chiang, S. Y. D., Pohlmann, D., Varley, C., Bodour, A., and Field, J. A. 2020. Pilot scale removal of per-and polyfluoroalkyl substances and precursors from AFFF-impacted groundwater by granular activated carbon. *Environmental Science: Water Research & Technology*, 2020(6), 1083. <https://doi.org/10.1039/c9ew00936a>

Sobko, K. 2021. *Garfield faces \$2M tab after contamination of water supply exceeds standards*. North Jersey. Retrieved from:
<https://www.northjersey.com/story/news/bergen/garfield/2021/07/22/garfield-nj-water-contamination-cleanup-chemicals/8046381002/>

Stanton, R. 2019. *Ann Arbor spending another \$950K on PFAS filters for water plant*. MLive. Retrieved from: <https://www.mlive.com/news/ann-arbor/2019/06/ann-arbor-spending-another-950k-on-pfas-filters-for-water-plant.html>

Stenzel, M.H. and Merz, W.J. 1989. Use of carbon adsorption processes in groundwater treatment. *Environmental Progress & Sustainable Energy*, 8(4), 257-264.
<https://doi.org/10.1002/ep.3300080420>

Suffolk County Water Authority (SCWA). 2018. *2018 Drinking Water Quality Report*. Retrieved from: <https://www.scwa.com/water-quality/water-quality-reports/>

Sullivan, M. 2018. *Addressing Perfluorooctane Sulfonate (PFOS) and Perfluorooctanoic Acid (PFOA)*. U.S. Department of Defense. Retrieved from:
<https://denix.osd.mil/derp/home/documents/pfos-pfoa-briefing-to-the-hasc/>

Summers, R.S., Knappe, D.R.U., and Snoeyink, V.L. 2011. Adsorption of Organic Compounds by Activated Carbon. In Edzwald, J.K. (Ed.), *Water Quality & Treatment: A Handbook on Drinking Water, Sixth Edition* (pp. 14.1-14.105). American Water Works Association.

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

U.S. Environmental Protection Agency (USEPA). 2022. *Drinking Water Treatability Database: Granular Activated Carbon*. Retrieved from <https://tdb.epa.gov/tdb/treatmentprocess?treatmentProcessId=2074826383>

USEPA. 2021a. *Drinking Water Treatability Database: Perfluorooctanoic Acid*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10520>

USEPA. 2021b. *Drinking Water Treatability Database: Perfluorooctane Sulfonate*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10940>

USEPA. 2021c. *Drinking Water Treatability Database: Per- and Polyfluoroalkyl Substances*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=11020>

USEPA. 2020. *Interim Guidance on the Destruction and Disposal of Perfluoroalkyl and Polyfluoroalkyl Substances and Materials Containing Perfluoroalkyl and Polyfluoroalkyl Substances*. EPA-HQ-OLEM-2020-0527-0002.

USEPA. 2009. *DuPont Agrees to Lower Limit of PFOA in Drinking Water*. Retrieved from: <https://www.epa.gov/sites/default/files/2016-05/documents/dupont-fs0309.pdf>

USEPA. 2002. *Filter Backwash Recycling Rule: Technical guidance manual*. Office of Groundwater and Drinking Water. EPA 816-R-02-014.

USEPA. 1996. *Technology Transfer Handbook: Management of Water Treatment Plant Residuals*. Office of Research and Development. EPA 625-R-95-008.

Vandermeiden, C. and Hagerty, V. 2020. Managing PFAS: A North Carolina Utility Story. *Journal AWWA*, 112(10), 10-18. <https://doi.org/10.1002/awwa.1590>

Wang, R., Ching, C., Dichtel, W.R., and Helbling, D.E. 2020. Evaluating the Removal of Per- and Polyfluoroalkyl Substances from Contaminated Groundwater with Different Adsorbents Using a Suspect Screening Approach. *Environmental Science and Technology Letters*, 2020(7), 954-960. <https://doi.org/10.1021/acs.estlett.0c00736>

Watanabe, N., Takata, M., Takemine, S., and Yamamoto, K. 2018. Thermal mineralization behavior of PFOA, PFHxA, and PFOS during reactivation of granular activated carbon (GAC) in nitrogen atmosphere. *Environmental Science and Pollution Research*, 25, 7200–7205. <https://doi.org/10.1007/s11356-015-5353-2>

Watanabe, N., Takemine, S., Yamamoto, K., Haga, Y., and Takata, M. 2016. Residual organic fluorinated compounds from thermal treatment of PFOA, PFHxA and PFOS adsorbed onto granular activated carbon (GAC). *Journal of Material Cycles & Waste Management*, 18, 625–630. <https://doi.org/10.1007/s10163-016-0532-x>

Warrington Township. 2017. *Water Contamination Information*. Retrieved from: <https://www.warringtontownship.org/departments/water-sewer/water-contamination-info/>

Westreich, P., Mimna, R., Brewer, J., and Forrester, F. 2018. The removal of short-chain and long-chain perfluoroalkyl acids and sulfonates via granular activated carbons: A comparative column study. *Remediation*, 29(1), 19-26. <https://doi.org/10.1002/rem.21579>

Woodard, S., Berry, J., and Newman, B. 2017. Ion exchange resin for PFAS removal and pilot test comparison to GAC. *Remediation*, 27, 19-27. <https://doi.org/10.1002/rem.21515>

Xiao, F., Sasi, P.C., Yao, B., Kubatova, A., Golovko, S.A., Golovko, M.Y., and Soli, D. 2020. Thermal Stability and Decomposition of Perfluoroalkyl Substances on Spent Granular Activated Carbon. *Environmental Science and Technology Letters*, 2020, 7, 343–350. <https://dx.doi.org/10.1021/acs.estlett.0c00114>

Yan, B., Munoz, G., Sauvé, S., and Liu, J. 2020. Molecular mechanisms of per- and polyfluoroalkyl substances on a modified clay: a combined experimental and molecular simulation study. *Water Research*, 184(2020), 116166. <https://doi.org/10.1016/j.watres.2020.116166>

Zeng, C., Atkinson, A., Sharma, N., Ashani, H., Hjelmstad, A., Venkatesh, K., and Westerhoff, P. 2020. Removing per-and polyfluoroalkyl substances from groundwaters using activated carbon and ion exchange resin packed columns. *AWWA Water Science*, 2(1), e1172. <https://doi.org/10.1002/aws2.1172>

3.0 Ion Exchange (IX)

3.1 Operating Principle

IX is a physical/chemical separation process in which stronger binding ions such as PFAS in the feed water are exchanged for weaker binding ions (typically chloride) on a resin generally made of synthetic beads or gel. In application, feed water passes through a bed of resin in a vessel or column. In the case of PFAS removal, the IX process is categorized as anion exchange (as opposed to cation exchange), because the ions involved (PFAS compounds and chloride) are negatively charged. To remove PFAS compounds, vendors generally recommend using special PFAS-selective resins (Boodoo, 2018a; Boodoo et al., 2019; Lombardo et al., 2018; Woodard et al., 2017).

The IX process continues until the resin does not have sufficient exchange sites available for the target PFAS compounds. At this point, the result is reduced contaminant removal, referred to as “breakthrough.” Figure 3-1 is a conceptual diagram of the IX treatment process, from initial adsorption to breakthrough. Once the contaminant concentration in the treated water reaches an unacceptable level, the resin is considered “spent.” In IX processes removing more traditional anions (e.g., nitrate), the capacity of the spent resin is often restored by rinsing the media with a concentrated chloride solution. However, conventional regeneration solutions are not effective for restoring the capacity of PFAS-selective resins (Liu and Sun, 2021). Therefore, in drinking water applications using PFAS-selective resin, design engineers and IX vendors recommend a single-use approach where the spent resin is disposed and replaced with fresh resin (Anderson et al., 2021; Boodoo, 2018a; Lombardo et al., 2018). Section 3.5 provides more information on the management of spent PFAS-selective resin. The length of time between resin replacement events is known as “bed life,” discussed in more detail in Section 3.2.2.

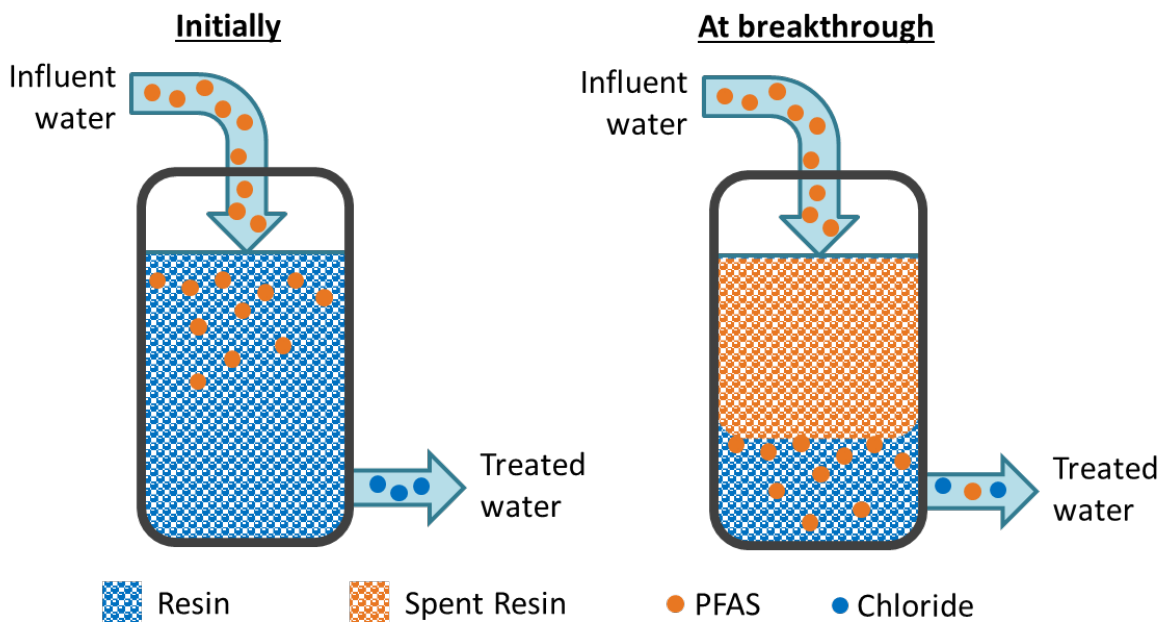


Figure 3-1. Conceptual Diagram of the IX Treatment Process

Figure 3-2 provides a schematic drawing for an IX system using disposable resin (i.e., without regeneration). The schematic shows a system with piping designed to enable operation with vessels in series, which is recommended for PFAS removal (see Section 3.6.1). In conventional IX processes, an optional backwashing step can be performed periodically during the resin's service cycle as needed to remove debris from the resin. In applications using PFAS-selective resins, backwashing is not recommended (Berretta et al., 2021). However, the resin often requires rinsing upon initial installation, with each replacement, and, in some cases, after periods of inactivity (Gottlieb and Watkins, 2012). Thus, the schematic shows optional tanks and pumps that may be required by some systems to accomplish this rinse.

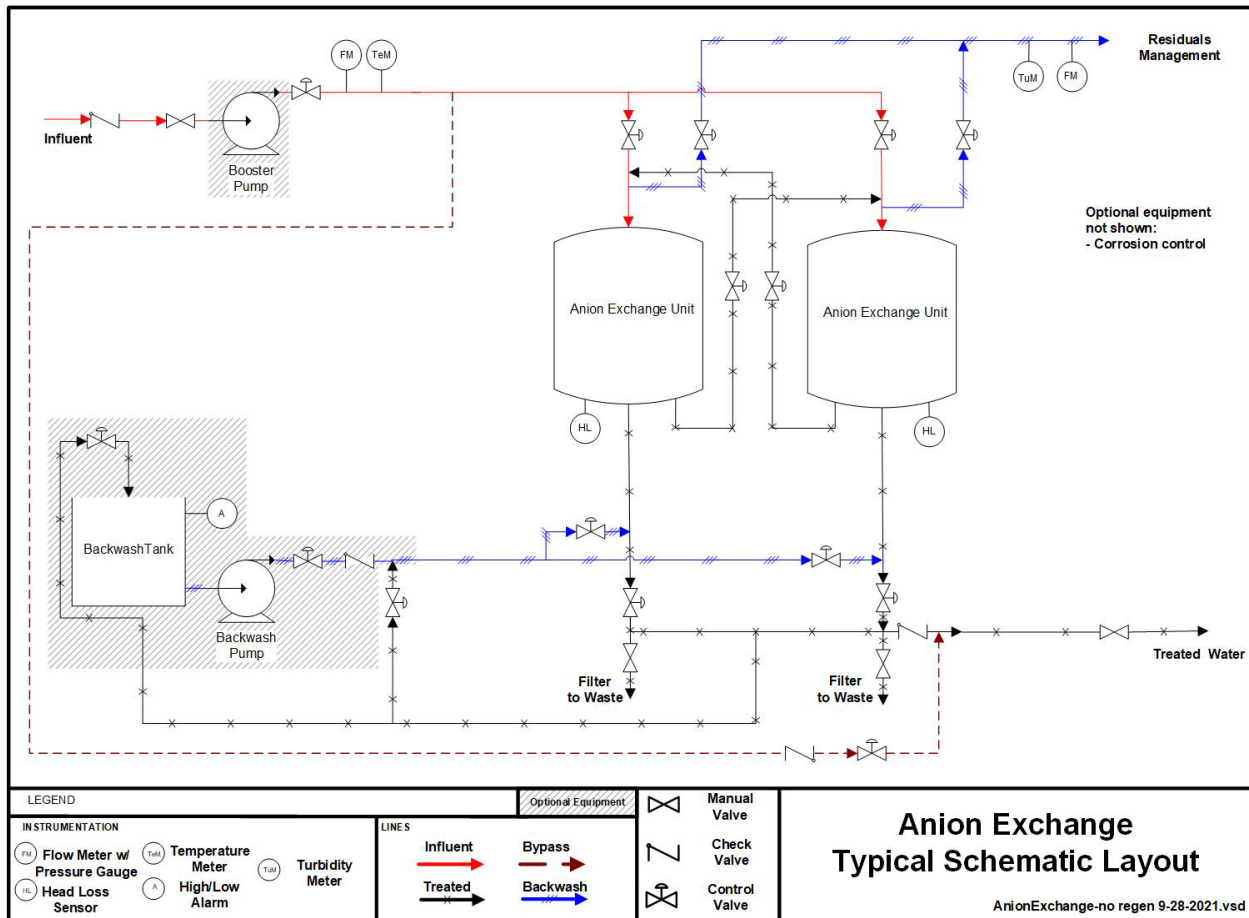


Figure 3-2. Typical Schematic Layout for IX with Resin Disposal

3.2 Effectiveness for PFAS Removal

3.2.1 Removal Efficiency

EPA's Drinking Water Treatability Database (USEPA, 2021a; 2021b; 2021c) includes extensive data from the literature on PFAS removal by IX. Results are available from studies conducted in the laboratory, in the field at pilot scale, and in full-scale application, as shown in Table 3-1,

Table 3-2, and Table 3-3. ⁷ These tables present the number of studies at each scale, along with a key benchmark of technology effectiveness: maximum removal efficiency. Removal efficiency is the percentage of the influent concentration removed through treatment.

The literature demonstrates maximum IX removal efficiencies of 90 percent or greater from most of the carboxylate and sulfonate PFAS compounds for which data are available.⁸ The literature also shows that the technology often removes these compounds to levels below analytical detection limits. For PFOA and PFOS, maximum removal efficiencies are greater than 99 percent, also to below analytical detection limits and lower than the regulatory thresholds currently under consideration. There are fewer studies of IX performance for other (non-carboxylate and non-sulfonate) PFAS compounds, but the available data show maximum removal efficiency of 97 percent or greater for all the other compounds for which data are available, including HFPO-DA.⁹

Table 3-1. Studies of IX Treatment for Carboxylate PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFBA	4	11	5	2	99.3	Dixit et al. 2020; Dixit et al. 2021
PFPeA	5	7	3	2	95.5	Schaefer et al. 2019
PFHxA	6	11	4	3	>97	Liu 2017
PFHpA	7	9	6	4	>99	Zeng et al. 2020
PFOA	8	15	7	4	99.3	Mohseni et al. 2019; Dixit et al. 2020; Dixit et al. 2021
PFNA	9	6	3	2	>99	Zeng et al. 2020; Kumarasamy et al. 2020
PFDA	10	7	0	0	>99	Kumarasamy et al. 2020
PFUnA	11	1	0	0	90	McCleaf et al. 2017
PFDoA	12	2	0	0	99.3	Dixit et al. 2021
PFTriA	13	1	0	0	90	McCleaf et al. 2017

Sources: USEPA, 2021a; 2021c

⁷ Data shown in these tables are as of December 2021. EPA frequently updates the Drinking Water Treatability Database, so parties interested in results from recently published literature may wish to access the database directly at <https://tdb.epa.gov/tdb/home>.

⁸ Exceptions are PFPeS and PFNS, but data for removal of these compounds by IX are available only from laboratory experiments in batch mode (Wang et al., 2020; Yan et al., 2020). These experiments are not designed to simulate the operation of an IX treatment process and, thus, may not reflect the result achievable at full scale.

⁹ Note, however, that data are not available to estimate IX bed life for HFPO-DA, as discussed in Section 3.6.3.

Table 3-2. Studies of IX Treatment for Sulfonate PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFBS	4	12	8	4	99.3	Dixit et al. 2020; Dixit et al. 2021
PFPeS	5	2	0	0	74	Yan et al. 2020
PFHxS	6	11	7	4	>99	Zeng et al. 2020; Boodoo 2018a; Arevalo et al. 2014; Kumarasamy et al. 2020
PFHpS	7	2	3	0	93	Yan et al. 2020
PFOS	8	16	8	4	99.7	Woodard et al. 2017
PFNS	9	1	0	0	54.9	Wang et al. 2020

Sources: USEPA, 2021b; 2021c

Table 3-3. Studies of IX Treatment for Other PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFBSA	4	1	0	0	98	Yan et al. 2020
PFMOPrA	4	1	0	0	99.3	Dixit et al. 2021
PFMOBA	5	1	0	0	99.3	Dixit et al. 2021
FtS 6:2	6	2	2	0	99.3	Dixit et al. 2021
HFPO-DA	6	4	1	0	99.3	Dixit et al. 2020; Dixit et al. 2021
PFHxSA	6	1	0	0	99	Yan et al. 2020
FtS 8:2	8	2	2	0	99.3	Dixit et al. 2021
PFOSA	8	3	0	1	98	Yan et al. 2020
PFECHS	8	1	0	0	97	Yan et al. 2020

Source: USEPA, 2021c

3.2.2 Bed Life

In addition to removal efficiency, the effectiveness of IX depends on bed life, which is the length of time the technology can maintain a target removal efficiency (e.g., 80 percent, 95 percent) or predefined concentration limit (such as an MCL). Bed life can be expressed as the number of days or months between resin replacement events. It can also be expressed in BV, which is a measure of throughput: the volume of water treated during the bed life divided by the volume of

the resin bed. With either measure, a higher number indicates a longer bed life and more effective treatment. Figure 3-3 illustrates the concepts of breakthrough and bed life on a typical “S-shaped” IX breakthrough curve.

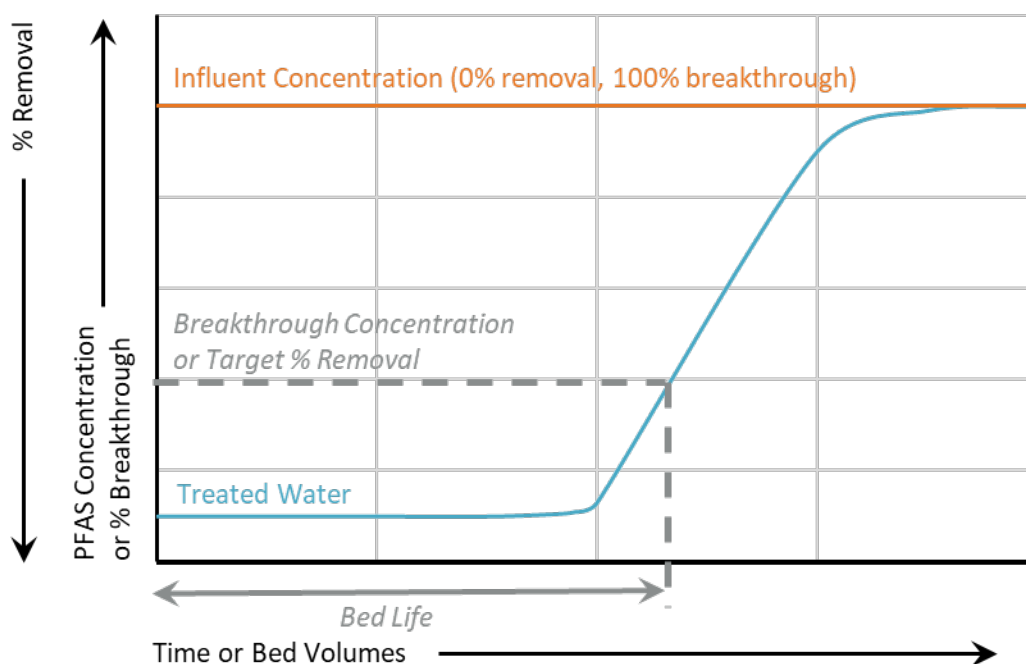
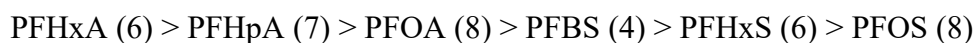


Figure 3-3. Typical IX Breakthrough Curve

There is a consensus in the literature that the capacity of IX resin for a given PFAS compound is strongly influenced by chain length (i.e., number of carbon atoms) and functional group (i.e., carboxylate versus sulfonate). In general, all other factors (see below) being equal, IX exhibits a greater capacity for sulfonate PFAS than carboxylate PFAS. Within these categories, the technology exhibits a greater capacity for longer chain compounds than shorter chain compounds. The greater capacity translates to longer bed life and lower treatment costs (Arevalo et al., 2014; Berretta et al., 2021; McCleaf et al., 2017; Schaefer et al., 2019; Zaggia et al., 2016; Zeng et al., 2020).

For IX, functional group is more significant than chain length, with carboxylates breaking through before sulfonates (Arevalo et al., 2014; Berretta et al., 2021; Schaefer et al., 2019; Zeng et al., 2020). An example IX breakthrough sequence from Zeng et al. (2020) is as follows (with number of carbon atoms shown in parenthesis for ease of reference):



In addition to chain length and functional group, estimates of IX bed life for PFAS removal depend on multiple factors. These additional factors can include the following:

- The target removal efficiency or predefined concentration at which the treated water quality is considered unacceptable (i.e., the “breakthrough” concentration)
- The influent concentration of the target PFAS compound(s)
- Other raw water quality parameters (see Section 3.3)

- Size of the IX bed relative to the flow of water to be treated, measured by EBCT (see Section 3.6.2)
- The specific IX resin being employed.

Because of these varying factors, comparing IX bed life results across multiple studies is difficult. Section 3.6.3 discusses methods to estimate bed life as a critical parameter in the design and operation of IX treatment.

3.2.3 Full-Scale Applications

Additional support for the effectiveness of IX for PFAS removal is evident from the number of full-scale facilities that are currently using the technology. Table 3-4 lists full-scale IX facilities identified in the literature. The effectiveness studies enumerated in Section 3.1.1 include results for some of these facilities. The first full-scale system treating drinking water using PFAS-selective IX commenced operation in 2017 (WWSD, 2018). Since that time, a number of additional drinking water systems have begun using the technology at full scale. Although IX remains a less common choice for PFAS removal than GAC, these recent installations suggest an increasing trend in the share of systems choosing IX. According to Berretta et al. (2021): “[n]ew suppliers are creating PFAS-selective resins, while those already in the market are improving their existing products.”

Table 3-4. Full-scale IX Systems Removing PFAS from Drinking Water

Location	Flow rate (MGD)	Groundwater or Surface Water	Year of Startup	Sources
Security Water and Sanitation Districts, Security, Colorado	9	Groundwater	2019	Jent 2020
Stratmoor Hills Water District, Stratmoor Hills, El Paso County, Colorado	1	Groundwater	Not reported	Berretta et al. 2021
Widefield Water and Sanitation District, Widefield, Colorado	Not reported	Groundwater	2017	WWSD 2018
City of Stuart, Florida	4	Groundwater	2018	Aqueous Vets 2019
Pease International Tradeport Drinking Water System, Portsmouth, New Hampshire	Not reported	Groundwater	2019	City of Portsmouth 2020
Horsham Water and Sewer Authority, Horsham, Montgomery County, Pennsylvania	0.14	Groundwater	2021	Boodoo 2018a; Boodoo et al. 2019; HWSA 2021
Warminster Municipal Authority, Warminster, Pennsylvania	Not reported	Not reported	Not reported	Boodoo 2018a; Boodoo 2018b

MGD = million gallons per day

3.3 Raw Water Quality Considerations

PFAS-selective IX resin is less sensitive to TOC than GAC (Berretta et al., 2021; Boodoo, 2018; Lombardo et al., 2018). For IX, the greater concern is the presence of competing anions, such as

nitrate, sulfate, bicarbonate, and chloride. PFAS-selective resins are designed to have higher affinity for PFAS than these other anions. However, these anions can be present in drinking water at concentrations many orders of magnitude higher than PFAS. Therefore, they can compete with PFAS for available exchange sites on the resin (Ateia et al., 2019; Berretta et al., 2021; Boodoo, 2021). Individual PFAS compounds also potentially compete with one another. In extreme cases, as more of the resin's exchange sites become occupied by influent anions, preferred anions in the influent can displace previously accumulated, less preferred anions. Such cases can result in a phenomenon known as chromatographic peaking, where the treated concentration of a less preferred anion exceeds its influent concentration (Clifford et al., 2011). McCleaf et al. (2017) observed this phenomenon for carboxylate PFAS in column tests that included both carboxylate and sulfonate PFAS in the influent.

In general, competition does not necessarily reduce the maximum removal effectiveness of the resin for PFAS. Instead, it shortens the time to breakthrough, meaning more frequent resin replacement may be required in the presence of competing anions, all other factors being equal. Therefore, it should be possible to reliably manage the impact of competition among anions, including the potential for chromatographic peaking, through piloting, selection of design parameters, and operational monitoring. As discussed in Section 3.6.3, for purposes of estimating national costs, EPA used a method to estimate bed life that explicitly includes consideration of total influent PFAS concentration. The inclusion of total PFAS concentration is intended to account for competition among PFAS compounds. The method to estimate bed life also is based on data from experiments where other competing anions, specifically nitrate and sulfate, were present in concentrations typical of drinking water.

3.4 Pre- and Post-Treatment Needs

In general, IX treatment can increase treated water corrosivity because of chloride ion addition and/or carbonate along with bicarbonate removal (Gottlieb and Watkins, 2012). For example, Berlien (2003) reported this problem with a full-scale application of IX for perchlorate treatment. However, for PFAS-selective resins specifically, one vendor reports that corrosivity effect is limited to the first 200 BV of treatment for their product. During this initial period, pH in treated water will decrease by 1 to 1.5 units; then the alkalinity and pH of the treated water returns to normal (Boodoo, 2018b). In cases where increased corrosivity is a longer-term problem, it might require post-treatment corrosion control or alterations to existing corrosion control.

3.5 Waste Generation and Residuals Management Needs

There are no known full-scale studies of spent resin from IX facilities specifically for the removal of PFAS. In general, however, the characteristics and quantities of spent resin are predictable. The spent resin contains the PFAS compounds and other anions removed from the treated water. The generation rate of spent resin is a function of bed volume and replacement frequency.

In IX processes removing more traditional contaminants (e.g., nitrate), the capacity of the spent resin is often restored by rinsing the media with a concentrated chloride solution. However, conventional regeneration solutions are not effective for restoring the capacity of PFAS-selective resins (Liu and Sun, 2021). Therefore, in drinking water applications using PFAS-selective resin, design engineers and IX vendors recommend a single-use approach where the spent resin is

disposed and replaced with fresh resin (Anderson et al., 2021; Boodoo, 2018a; Lombardo et al., 2018). Regeneration of selective resins may be possible using organic solvents (Boodoo, 2018a; Zaggia et al., 2016) or proprietary methods (Woodard et al., 2017). These alternative regeneration practices are generally practical or cost-effective only with very high influent concentrations, such as in remediation settings (Anderson et al., 2021; Boodoo, 2018a).

Under current regulations, spent resin is typically incinerated (Boodoo, 2018b). The literature is inconclusive regarding the fate of PFAS during incineration in general (USEPA, 2020) and there are no studies specific to incineration of IX resin. Additional full-scale research might be needed if future air quality regulations address PFAS emissions from incineration facilities. The results of this research might necessitate changes to spent resin management practices. Future RCRA hazardous waste regulations could also limit the available management options.

Although backwashing is not recommended for PFAS-selective resin (Berretta et al., 2021), IX systems also intermittently generate a liquid residual in the form of spent rinse water. Because the rinse follows immediately after fresh resin is installed, before the bed restarts service, it should not contain target contaminants. Management options for spent rinse water include discharge to surface water under a NPDES permit or discharge to a WWTP. When averaged over the time between generation events, spent rinse water flow is relatively low. Instantaneous flow during a rinse event, however, is much higher. Therefore, holding tanks might be advisable under certain conditions (e.g., to prevent instantaneous flow from overwhelming the capacity of a WWTP).

3.6 Critical Design Parameters

Critical design parameters that are specific to IX systems removing PFAS with selective resin are:

- EBCT
- Vessel configuration (i.e., number of vessels in series)
- Bed life
- Residuals management options.

Section 3.5 discusses residuals management options. The sections below discuss EBCT, vessel configuration, and bed life in more detail, including the data available in the literature for these parameters. Section 7.3.1 identifies the specific values for each parameter used in EPA's cost estimates. Values for other IX design parameters (e.g., loading rate, bed depth constraints, resin density), while not specifically addressed here, are well documented for IX treatment in general. EPA has no reason to expect a significant difference in these parameters for IX systems treating PFAS compounds.

3.6.1 Empty Bed Contact Time

For a given set of site-specific conditions, there is a minimum EBCT required to produce water of a target quality. EBCT, measured in minutes, is defined by the following equation:

$$EBCT \text{ (in minutes)} = \frac{\text{Volume of Resin Bed}}{\text{Volumetric Flow Rate (per minute)}}$$

The minimum EBCT required varies depending on the specific contaminant treated, the required contaminant removal percentage, the type of resin used, and other influent water characteristics (e.g., the presence of competing chemical species). Limited data are available on the EBCT employed at full-scale anion exchange systems that are purpose-built for PFAS removal. One pilot system was later permitted for permanent operation using two vessels in series with a total EBCT of 5.6 minutes (Boodoo et al., 2019). A common vendor recommendation is to use a total EBCT of 3 to 6 minutes (Boodoo, 2019; Boodoo et al., 2019; Boodoo, 2018; Lombardo et al., 2018).

3.6.2 Vessel Configuration

IX treatment systems with multiple vessels can be configured in series or in parallel. In a parallel configuration, flow is divided equally among the vessels, each of which provides the design EBCT. In a series (or lead/lag) configuration, water flow first through an initial vessel that serves as a roughing vessel, then through subsequent vessels that serve as polishing vessels (Clifford et al., 2011). Each vessel in the series typically has an equal EBCT such that the total EBCT of the series provides the design EBCT. A series (or lead/lag) configuration serves the purpose of treating a greater water volume than one vessel with similar bed volume. When resin in the roughing vessel is spent, this resin is replaced and the polishing vessel moves to the start of the series, becoming the roughing vessel. The use of vessels in series can allow the resin in the lead vessel to reach greater exhaustion, increasing total capacity (Clifford et al., 2011). For larger flow rates, systems can use a configuration that combines series and parallel operation (i.e., multiple trains in parallel, each train with contactors in series).

For PFAS removal, design engineers and vendors commonly recommend two vessels in series (Anderson et al., 2012; Berretta et al., 2021; Boodoo, 2019; Boodoo et al., 2019; Boodoo, 2018; Lombardo et al., 2018). Full-scale IX treatment systems for PFAS removal for which configuration data are available use two vessels in series (Aqueous Vets, 2019; Boodoo et al., 2019; WWSD, 2018). The schematic diagram (Figure 3-2) in Section 3.1 shows a system configured to operate with vessels in series. A system designed for operation with vessels in parallel (which is not typical for PFAS removal) would not require piping between the two anion exchange units.

3.6.3 Bed Life

As discussed in Section 3.2.2, IX bed life depends on a number of factors. Designers should select EBCT and vessel configuration to maximize bed life. Bed life data are not available for full-scale IX exchange systems using PFAS-selective resins. Although bed life data from pilot studies are available, comparing and synthesizing these data is complicated by variations in study design (e.g., water quality, EBCT, type of resin). For certain pilot studies, the bed life data have been presented, published, or otherwise provided to EPA, but are not from a peer-reviewed publications (e.g., Boodoo, 2018a; Boodoo et al., 2019; Lombardo et al., 2018). In other cases, the pilot study data reflect treatment of water with very high PFAS concentrations, more reflective of remediation conditions than drinking water (Newman and Berry, 2019; Woodard et al., 2017).

To develop a practical method of estimating bed life for purposes of estimating national costs for IX, EPA used data from Zeng et al. (2020). These data are from RSSCTs of IX treating actual

groundwater, intended to simulate a full-scale EBCT of 3.3 minutes. The RSSCTs covered six different water quality conditions (different groundwater sources) and two different PFAS-selective resins. In each groundwater source, multiple PFAS compounds were present in concentrations typical of PFAS-contaminated drinking water. PFAS compounds monitored in the IX RSSCTs were: PFHxA, PFHpA, PFOA, PFNA,¹⁰ PFBS, PFHxS, and PFOS. EPA pooled the data from the individual RSSCTs and used multiple linear regression to develop a model that results in compound-specific bed life equations.

EPA recognizes that PFAS breakthrough curves are not linear. However, to develop the equations, EPA specifically used the data from the last point of non-detection to the first instance of complete breakthrough (or the end of the study, whichever came first). By limiting the data to this range, EPA sought to characterize the portion of the breakthrough curve where bed life changes rapidly with removal efficiency. This portion of the curve is most interest in selecting a target bed life for purposes of cost estimating and is expected to be more approximately linear than the curve overall. Figure 3-4 shows this concept graphically in relation to a typical theoretical breakthrough curve.

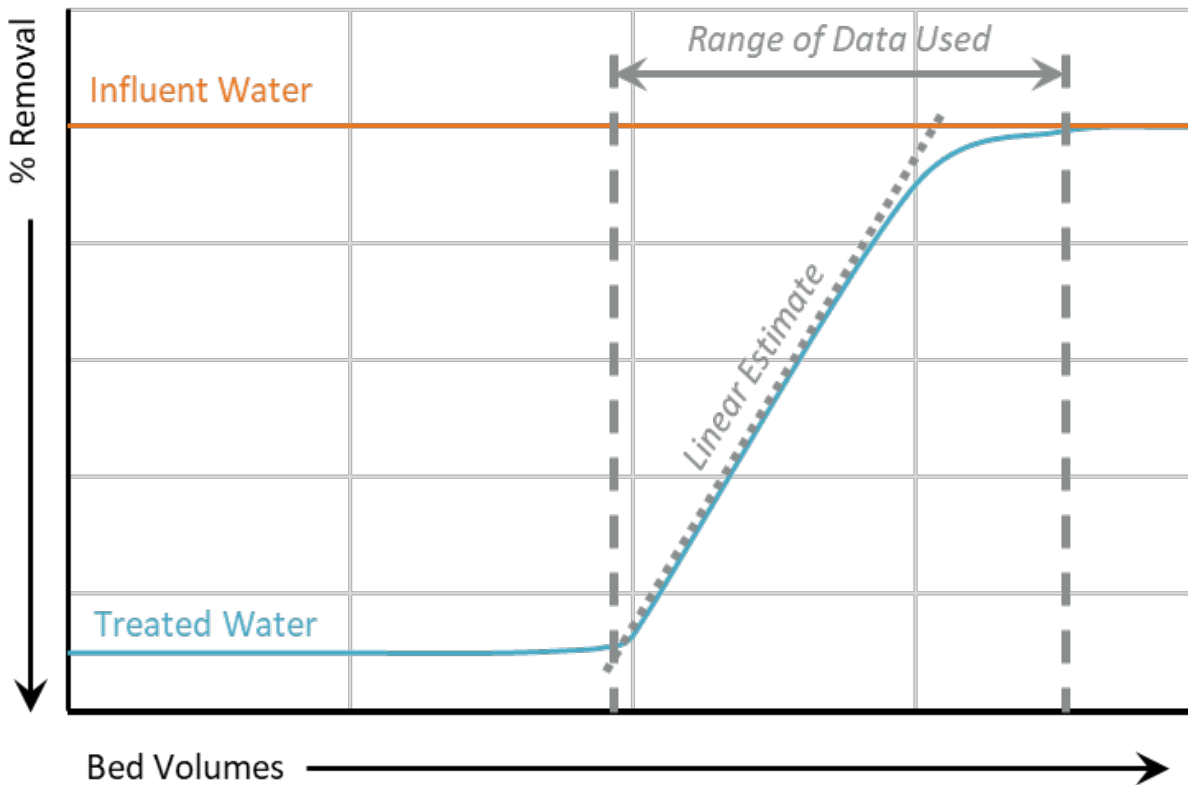


Figure 3-4. Linear Bed Life Estimate in Relation to a Typical Breakthrough Curve

The resulting PFAS compound-specific bed life equations for IX take the following form:

$$BV_{contam,IX} = A_{PFAS} \times PFAS_{total} + A_{R,IX} \times \%R_{contam} + B_{contam,IX}$$

¹⁰ EPA was not able to develop a breakthrough relationship for this compound.

Where:

- $BV_{\text{contam,IX}}$ = IX bed life for a given PFAS contaminant in BV
- $PFAS_{\text{total}}$ = total influent concentration of PFAS compounds in ng/L
- $\%R_{\text{contam}}$ = target percent removal of a given PFAS as a decimal (e.g., 0.8, 0.95)
- A_{PFAS} , $A_{R,IX}$, and $B_{\text{contam,IX}}$ are parameters derived in the regression analysis. Table 3-5 shows their estimated values.

Table 3-5. Estimated Parameter Values for IX Bed Life Equations

Parameter	IX Model Value
A_{PFAS}	-6.04
A_R	-198,242
B_{PFHxA}	212,867
B_{PFBS}	439,515
B_{PFHpA}	319,511
B_{PFHxS}	439,515
B_{PFOA}	390,787
B_{PFOS}	439,515

The parameter values result in the following order of breakthrough from earliest to latest, given a constant total influent PFAS concentration and target percent removal:

$$PFHxA > PFHpA > PFOA > PFBS = PFHxS = PFOS$$

This result is generally consistent with the typical expectation, as discussed in Section 3.2.2, that carboxylates break through before sulfonates and shorter chain compounds break through before longer chain compounds. The equations predict identical bed lives for the three sulfonate compounds included in the analysis because the intercept terms for these compounds (B_{PFBS} , B_{PFHxS} , and B_{PFOS}) were not significantly different from each other statistically. All compounds share the same slope term (A_{PFAS}) for total influent PFAS (in ng/L) and the same slope term (A_R) for percent removal of the PFAS compound (as a decimal) and because specifying the model this way results in a consistent order of breakthrough across the range of possible influent PFAS values and percent removal values.

The model has an adjusted R^2 of 0.71. The overall model and individual coefficients are statistically significant. Although the effect of total PFAS concentration on bed life (A_{PFAS}) is small, it remains statistically significant and is included in the model to account for competition among PFAS compounds. Note that the equations are valid only up to a total influent PFAS of 7,044 ng/L, the maximum value in the data set used. Other competing anions, specifically nitrate and sulfate, were present in the water sources studied and measured by Zeng et al. (2020). However, the range of concentrations for these anions across the RSSCTs was not wide. Therefore, EPA was not able to incorporate them into the IX bed life model. Also note that, unlike the bed life model for GAC (see Section 2.6.3), data were not available to incorporate HFPO-DA into the IX model.

Because the equations are based on pooled data, they reflect central tendency results under varying water quality conditions. As such, the EPA believes they represent the best approach for estimating national cost given the data currently available in the literature. However, these equations should not be used in lieu of site-specific engineering analyses or pilot studies to guide the design or operation of specific treatment systems.

The use of RSSCTs to predict IX performance for PFAS removal is a recent development (Najm et al., 2021; Schaefer et al., 2019; Zeng et al., 2020), so there are no validated methods to scale up from these bench-scale results. When RSSCTs are used to estimate the performance of GAC for PFAS, there are concerns that the results may, in some cases, overestimate full-scale bed life (Hopkins, 2021; Kempisty et al., 2019; Meng et al., 2021; Redding et al., 2019). To compensate for the potential for similar overestimation concerns for IX, when applying the bed life equations, EPA did not incorporate the increase in bed life that would be expected from operating multiple vessels in series (see Section 3.6.2). Section 7.2.1 discusses this topic, and the application of the bed life equations generally, in more detail.

3.7 References

- Anderson, J., Meng, P., Sidnell, T., and Ross, I. 2021. Advances in Remediation of PFAS-impacted Waters. In Kempisty, D.M. and Racz, L. (Eds.), *Forever Chemicals: Environmental, Economic, and Social Equity Concerns with PFAS in the Environment* (pp. 189-209). CRC Press. <https://doi.org/10.1201/9781003024521>
- Aqueous Vets. 2019. The City of Stuart, Florida Installs 4 MGD Ion Exchange System to Address PFAS Contamination. AVP-0016 Rev.2 9/19/2019. Retrieved from http://www.aqueousvets.com/uploads/9/8/8/7/98870448/avp-0016_pfas_treatment_system_-_stuart_fl_-_09.19.19.pdf
- Arevalo, E., Strynar, M., Lindstorm, A., McMillan, L., and Knappe, D. 2014. Removal of Perfluorinated Compounds by Anion Exchange Resins: Identifying Effective Resin Regeneration Strategies. AWWA Annual Conference and Exposition. Boston, MA.
- Ateia, M., Maroli, A., Tharayil, N., and Karanfil, T. 2019. The overlooked short- and ultrashort-chain poly- and perfluorinated substances: A review. *Chemosphere*, 220(2019), 866-882. <https://doi.org/10.1016/j.chemosphere.2018.12.186>
- Berlien, M. J. 2003. *La Puente Valley County Water District's Experience with ISEP* Presentation of Carollo Engineers, Inc. and Association of California Water Agencies.
- Berretta, C., Mallmann, T., Trewitz, K., and Kempisty, D.M. 2021. Removing PFAS from Water: From Start to Finish. In Kempisty, D.M. and Racz, L. (Eds.), *Forever Chemicals: Environmental, Economic, and Social Equity Concerns with PFAS in the Environment* (pp. 235-253). CRC Press. <https://doi.org/10.1201/9781003024521>
- Boodoo, F. 2021. Personal Communication (E-mail). June 7, 2021.
- Boodoo, F. 2019. Personal Communication (E-mail). February 22, 2019.

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Boodoo, F., Begg, T., Funk, T., Kessler, T., Shaw, E., and Pickel, M. 2019. *Polishing PFAS To Non-Detect Levels Using PFAS Selective Resin*. Water Online. Retrieved from: <https://www.wateronline.com/doc/polishing-pfas-to-non-detect-levels-using-pfas-selective-resin-0001>

Boodoo, F. 2018a. *Short & Long Chain PFAS Removal to Non-Detect Level with Single-Use PFA694E Resin*. Presentation by Puralite Corporation. Retrieved from: <https://docs.house.gov/meetings/IF/IF18/20180906/108649/HHRG-115-IF18-20180906-SD027.pdf>

Boodoo, F. 2018b. Personal Communication (E-mail). July 12, 2018.

City of Portsmouth – Department of Public Works. 2019. *Portsmouth Water System PFAS Update*. Retrieved from: <https://www.cityofportsmouth.com/publicworks/water/portsmouth-water-system-pfas-update>

Clifford, D., Sorg, T.J., and Ghurye, G.L. 2011. Ion Exchange and Adsorption of Inorganic Contaminants. In Edzwald, J.K. (Ed.), *Water Quality & Treatment: A Handbook on Drinking Water, Sixth Edition* (pp. 12.1-12.97). American Water Works Association.

Dixit, F., Barbeau, B., Mostafavi, S.G., and Madjid, M. 2020. Removal of legacy PFAS and other fluorotelomers: Optimized regeneration strategies in DOM-rich waters. *Water Research*, 183(2020), 116098. <https://doi.org/10.1016/j.watres.2020.116098>

Dixit, F., Barbeau, B., Mostafavi, S.G., and Mohseni, M. 2021. PFAS and DOM removal using an organic scavenger and PFAS-specific resin: Trade-off between regeneration and faster kinetics. *Science of the Total Environment*, 754(2021), 142107. <https://doi.org/10.1016/j.scitotenv.2020.142107>

Gottlieb, M.C. and Watkins, G.S. 2012. Ion Exchange Applications in Water Treatment. In Randtke, S.J. and Horsley, M.B. (Eds.), *Water Treatment Plant Design, Fifth Edition* (pp. 14.1-14.71). American Water Works Association/American Society of Civil Engineers.

Hopkins, Z.R. 2021. *Granular Activated Carbon Adsorption of Per- and Polyfluoroalkyl Substances - from Scale-Up to Factors Affecting Performance*. Doctoral Dissertation, North Carolina State University. ProQuest Dissertations Publishing. 29004569.

Horsham Water and Sewer Authority (HWSA). 2021. *PFAS Summary*. Retrieved from: <https://www.horshamwater-sewer.com/pfas-summary>

Jent, H. 2020. *Crews near completion on new ion-exchange treatment plant to purify water in Security*. The Gazette. Retrieved from: https://gazette.com/news/crews-near-completion-on-new-ion-exchange-treatment-plant-to-purify-water-in-security/article_2bf7d0ce-0410-11eb-8776-8306994433b3.html

Kempisty, D.M., Arevalo, E., Reinert, A., Edeback, V., Dickenson, E., Husted, C. Higgins, C.P., Summers, R.S., and Knappe, D.R.U. 2019. *Adsorption of per and polyfluoroalkyl acids from ground and surface water by granular activated carbon*. AWWA Water Quality Technology Conference, Dallas, TX.

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Kumarasamy, E., Manning, I. M., Collins, L. B., Coronell, O., and Leibfarth, F. A. 2020. Ionic Fluorogels for Remediation of Per-and Polyfluorinated Alkyl Substances from Water. *ACS Central Science*, 2020(6), 487–492. <https://doi.org/10.1021/acscentsci.9b01224>

Liu, C. 2017. *Removal of Perfluorinated Compounds in Drinking Water Treatment: A Study of Ion Exchange Resins and Magnetic Nanoparticles*. Doctoral Dissertation, University of Waterloo. Retrieved from <http://hdl.handle.net/10012/12660>

Lombardo, J., Berretta, C., Redding, A., Swanson, C., and Mallmann, T. 2018. Carbon and Resin Solutions for PFAS Removal. Evoqua Water Technologies Webinar. March 6.

McCleaf, P., Englund, S., Ostlund, A., Lindegren, K., Wiberg, K., and Ahrens, L. 2017. Removal Efficiency of Multiple Poly- and Perfluoroalkyl Substances (PFASs) in Drinking Water using Granular Activated Carbon (GAC) and Anion Exchange (AE) Column Tests. *Water Research*, 120: 77-87. <http://dx.doi.org/10.1016/j.watres.2017.04.057>

Mohseni, M., Dixit, F., Barbeau, B. 2019. *Optimized Regeneration Strategies for Ion Exchange Resins During PFAS Removal from Natural Waters*. AWWA Water Quality Technology Conference. Dallas, TX.

Newman, B. and Berry, J. 2019. Case Study: Pilot Testing Synthetic Media and Granular Activated Carbon for Treatment of Poly- and Perfluorinated Alkyl Substances in Groundwater. In Kempisty, D.M, Xing, Y., and Racz, L. (Eds.), *Perfluoroalkyl Substances in the Environment: Theory, Practice, and Innovation*. Taylor & Francis. <https://doi.org/10.1201/9780429487125>

Schaefer, C.E., Nguyen, D., Ho, P., Im, J., and LeBlanc, A. 2019. Assessing Rapid Small-Scale Column Tests for Treatment of Perfluoroalkyl Acids by Anion Exchange Resin. *Ind. Eng. Chem. Res.*, 2019(58), 9701–9706. <https://doi.org/10.1021/acs.iecr.9b00858>

U.S. Environmental Protection Agency (USEPA). 2021a. *Drinking Water Treatability Database: Perfluorooctanoic Acid*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10520>

USEPA. 2021b. *Drinking Water Treatability Database: Perfluorooctane Sulfonate*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10940>

USEPA. 2021c. *Drinking Water Treatability Database: Per- and Polyfluoroalkyl Substances*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=11020>

USEPA. 2020. *Interim Guidance on the Destruction and Disposal of Perfluoroalkyl and Polyfluoroalkyl Substances and Materials Containing Perfluoroalkyl and Polyfluoroalkyl Substances*. EPA-HQ-OLEM-2020-0527-0002.

Wang, R., Ching, C., Dichtel, W.R., and Helbling, D.E. 2020. Evaluating the Removal of Per- and Polyfluoroalkyl Substances from Contaminated Groundwater with Different Adsorbents Using a Suspect Screening Approach. *Environmental Science and Technology Letters*, 2020(7), 954-960. <https://doi.org/10.1021/acs.estlett.0c00736>

Woodard, S., Berry, J., and Newman, B. 2017. Ion exchange resin for PFAS removal and pilot test comparison to GAC. *Remediation*, 27, 19-27. <https://doi.org/10.1002/rem.21515>

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Widefield Water and Sanitation District (WWSD). 2018. *From Pilot to Full-Scale: A Case Study for the Treatment of Perfluorinated Compounds (PFCs) with Ion Exchange*. AWWA Water Quality Technology Conference, Toronto, ON, Canada.

Yan, B., Munoz, G., Sauvé, S., and Liu, J. 2020. Molecular mechanisms of per- and polyfluoroalkyl substances on a modified clay: a combined experimental and molecular simulation study. *Water Research*, 184(2020), 116166.
<https://doi.org/10.1016/j.watres.2020.116166>

Zeng, C., Atkinson, A., Sharma, N., Ashani, H., Hjelmstad, A., Venkatesh, K., and Westerhoff, P. 2020. Removing per-and polyfluoroalkyl substances from groundwaters using activated carbon and ion exchange resin packed columns. *AWWA Water Science*, 2(1), e1172.
<https://doi.org/10.1002/aws2.1172>

4.0 Reverse Osmosis and Nanofiltration (RO/NF)

4.1 Operating Principle

RO and NF are membrane processes that separate contaminants from drinking water. These processes separate solutes such as PFAS compounds from solution by forcing the solvent to flow through a membrane at a pressure greater than the normal osmotic pressure. In drinking water treatment, these membranes are most often used in a spiral-wound configuration that consists of several membrane envelopes, layered with feed spacers and rolled together in around a central collection tube.

The membrane is semi-permeable, transporting different molecular species at different rates. The application of pressure splits the influent water passing over the membrane into two streams:

- Treated water or “permeate” that passes through the membrane layers along with solutes of lower molecular weight into the central collection tube
- Water containing higher molecular weight solutes that remains outside the membrane layers, called “reject,” “concentrate,” or “brine.”

“Recovery rate” and “rejection rate” are the percentages of influent water that are recovered as permeate and lost as reject, respectively.¹¹ Figure 4-1 is a conceptual diagram of this process as applied to water containing PFAS.

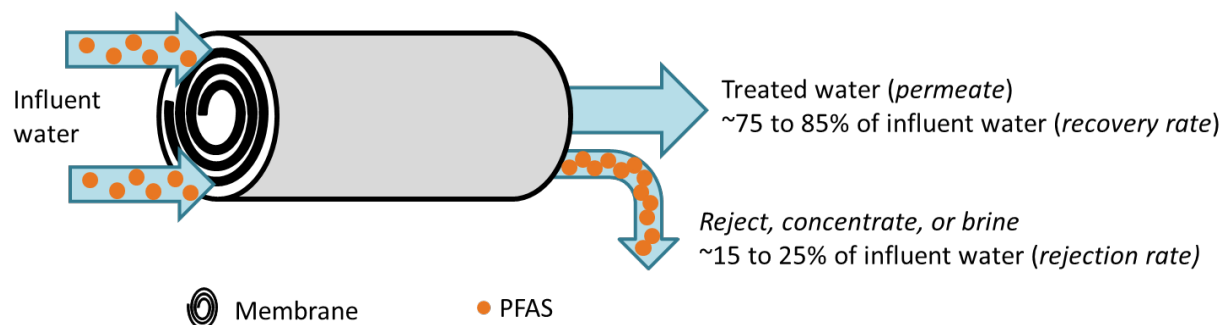


Figure 4-1. Conceptual Diagram of the RO Treatment Process

Specific membranes differ in the size of dissolved contaminants they can remove. In general, RO membranes are effective for smaller contaminants than NF membranes. However, even within the categories of RO and NF, individual membranes from different manufacturers vary in the minimum size and weight of contaminants they reject, as shown in Table 4-1. Membranes that remove smaller contaminants require higher feed pressure. Feed pressures for NF membranes are typically in the range of 50 to 150 pounds per square inch (psi). Feed pressures for RO membranes are in the range of 125 to 300 psi in low pressure applications targeting relatively large contaminants (such as PFAS compounds) but can be as high as 1,200 psi in applications such as seawater desalination (Bergman et al., 2012; USEPA, 2022c). As discussed in Section 4.2.1, both RO and NF membranes have the capacity to remove PFAS.

¹¹ Note that recovery and rejection rates are not directly related to removal efficiency, which is the percentage of influent PFAS removed from the treated water.

Table 4-1. Minimum Effective Ranges for RO/NF Membranes

Technology	Contaminant Size (microns)	Contaminant Molecular Weight (g/mol)
RO	0.0001 to ~0.0015	<100 to ~200
NF	0.001 to ~0.006	200 to 1,000

~ = approximately; g/mol = grams per mole; NF = nanofiltration; RO = reverse osmosis
 Sources: Bergman et al., 2012; DuPont, 2021; Duranceau and Taylor, 2011

A treatment system using RO or NF will employ multiple membrane elements, placed within a pressure vessel. To achieve a high recovery rate and contaminant removal efficiency, these pressure vessels often are arranged in sequential stages, typically up to three depending on the recovery to be achieved (Bergman et al., 2012; DuPont, 2021). When multiple stages are used, the number of pressure vessels decreases from stage to stage. Treated permeate is collected from each pressure vessel. The concentrate from the first membrane stage serves as the feed to the second and the concentrate from the second stage serves as the feed to the third. Consequently, each successive stage of the process increases the total system recovery. As the feed water travels through the membrane system and becomes more concentrated, its osmotic pressure increases. The feed pressure must overcome this osmotic pressure. The final concentration in the concentrate therefore has a major effect on the required feed pressure and energy use.

The membrane stages in combination make up an RO treatment train. A treatment system may have multiple trains. Figure 4-2 provides a schematic drawing for an RO treatment facility; each rectangular box within a train represents a pressure vessel that contains multiple membrane elements. An NF treatment facility would be nearly identical, with the primary difference being the type of membranes used and the operating pressures.

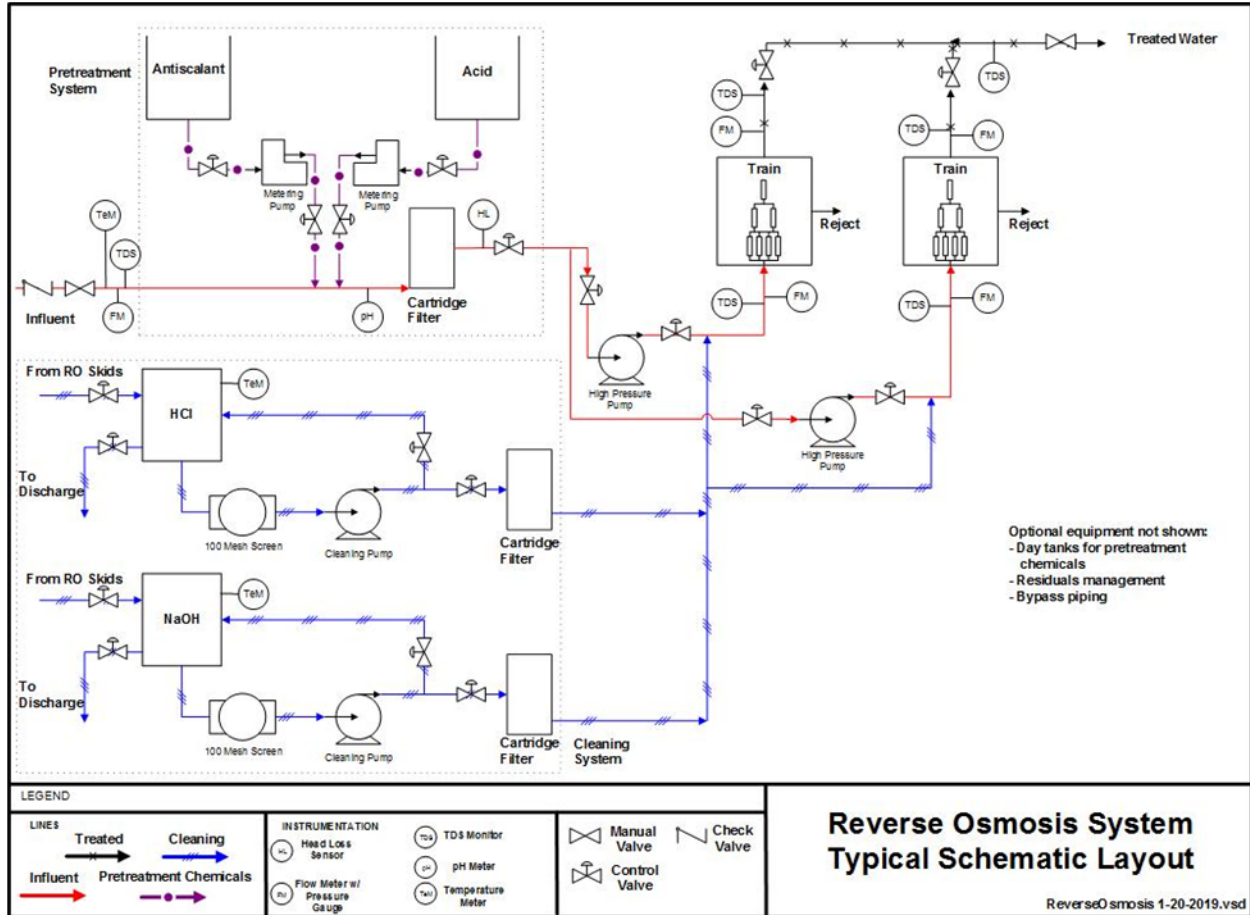


Figure 4-2. Typical Schematic Layout for RO/NF

4.2 Effectiveness for PFAS Removal

4.2.1 Removal Efficiency

EPA’s Drinking Water Treatability Database (USEPA, 2021a; 2021b; 2021c) includes extensive data from the literature on PFAS removal by RO and NF. Results are available from studies conducted in the laboratory, in the field at pilot scale, and in full-scale application, as shown in Table 4-2, Table 4-3, and Table 4-4.¹² These tables present the number of studies at each scale, along with a key benchmark of technology effectiveness: maximum removal efficiency.

Removal efficiency is the percentage of the influent concentration removed through treatment.

¹² Data shown in these tables are as of December 2021. EPA frequently updates the Drinking Water Treatability Database, so parties interested in results from recently published literature may wish to access the database directly at <https://tdb.epa.gov/tdb/home>.

Table 4-2. Studies of RO/NF Treatment for Carboxylate PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum NF Removal Efficiency	Maximum RO Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFBA	4	2	1	2	99	99.9	Lipp et al. 2010
PFPeA	5	2	3	2	>99	>99	Horst et al. 2018; Liu et al. 2021; Dickenson and Higgins 2016
PFHxA	6	3	4	4	>98	99.2	Liu et al. 2021
PFHpA	7	1	2	3	99	>99	Steinle-Darling et al. 2008; Liu et al. 2021
PFOA	8	4	4	5	99.9	99.9	Boonya-Atichart et al. 2016; Lipp et al. 2010
PFNA	9	2	1	4	99	>98	Steinle-Darling et al. 2008; Dickenson and Higgins 2016; Appleman et al. 2014
PFDA	10	2	0	4	99	>99	Steinle-Darling et al. 2008; Dickenson and Higgins 2016; Appleman et al. 2014
PFUnA	11	1	0	2	99	>77	Steinle-Darling et al. 2008; Dickenson and Higgins 2016; Appleman et al. 2014
PFDoA	12	0	0	2	-	>87	Dickenson and Higgins 2016; Appleman et al. 2014

- = no data; NF = nanofiltration; RO = reverse osmosis
 Sources: USEPA, 2021a; 2021c

Table 4-3. Studies of RO/NF Treatment for Sulfonate PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum NF Removal Efficiency	Maximum RO Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFPrS	3	0	1	0	>98	>99	Liu et al. 2021
PFBS	4	3	4	3	99.8	99.8	Lipp et al. 2010
PFPeS	5	0	1	0	>98	>99	Liu et al. 2021
PFHxS	6	2	4	4	>99	>99	Appleman et al. 2013; Thompson et al. 2011; Liu et al. 2021

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum NF Removal Efficiency	Maximum RO Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFHpS	7	0	1	0	>98	>99	Liu et al. 2021
PFOS	8	6	4	5	>99.9	99.9	Lipp et al. 2010; 2163
PFDS	10	1	0	0	99	-	Steinle-Darling et al. 2008

- = no data; NF = nanofiltration; RO = reverse osmosis
 Sources: USEPA, 2021b; 2021c

Table 4-4. Studies of RO/NF Treatment for Other PFAS

PFAS Compound	Number of Carbons	Number of Bench Studies	Number of Pilot Studies	Number of Full-scale Studies	Maximum NF Removal Efficiency	Maximum RO Removal Efficiency	Source(s) for Maximum Removal Efficiency
PFMOAA	3	0	1	0	-	>98.5	CDM Smith 2018
PFO2HxA	4	0	1	0	-	>80.8	CDM Smith 2018
PFO3OA	5	0	1	0	-	>67.2	CDM Smith 2018
FtS 6:2	6	1	2	1	99.5	>65.5	Steinle-Darling et al. 2008; CDM Smith 2018
HFPO-DA	6	0	1	0	-	>64.2	CDM Smith 2018
PFOSA	8	2	0	1	98.5	>13	Steinle-Darling et al. 2008; Dickenson and Higgins 2016
N-MeFOSAA	11	0	0	2	-	>84	Dickenson and Higgins 2016
N-EtFOSAA	12	0	0	2	-	>58	Dickenson and Higgins 2016

- = no data; NF = nanofiltration; RO = reverse osmosis
 Source: USEPA, 2021c

The literature demonstrates RO and NF removal efficiencies in the high 90 percent range for nearly all the carboxylate and sulfonate PFAS compounds for which data are available. The literature also shows that the technology often removes these compounds to levels below analytical detection limits. For PFOA and PFOS, maximum removal efficiencies are greater than 99 percent to levels lower than the regulatory thresholds currently under consideration. There are fewer studies of RO/NF performance for other (non-carboxylate and non-sulfonate) PFAS compounds. The apparently low removal values for these other PFAS compounds (e.g., greater than 64.2 percent removal for HFPO-DA) are an artifact of low influent levels relative to the detection or quantitation limits. As discussed below, higher removals than the values shown in Table 4-3 could be achievable for other PFAS that are similar in size and weight to the carboxylate and sulfonate compounds.

PFAS removal efficiency for specific membranes appears to be closely related to the characteristics of the membrane relative to the molecular weight of the target compound. For example, Yu et al. (2016) found only 55 percent removal of PFOS by a membrane with a membrane with a molecular weight cutoff (MWCO) of 1,000 grams per mole (g/mol), which is larger than the molecular weight of PFOS (500.13 g/mol). In the same study, a membrane with an MWCO of 200 g/mol achieved 95.5 to 97 percent removal of PFOS. Appleman et al. (2013) and Steinle-Darling and Reinhard (2008) also observed the effect of molecular weight on PFAS removal by NF, finding somewhat lower removal of lower molecular weight, shorter chain PFAS than higher molecular weight, longer chain PFAS. Accordingly, PFAS removal efficiency by NF membranes is not expected to vary substantially by functional group or chain length except to the extent that these factors influence molecular size and weight. RO membranes have a lower MWCO than NF membranes, often less than 100 g/mol (DuPont, 2021). Therefore, RO removal efficiency also is not expected to vary substantially by functional group or chain length. In addition, unlike GAC and IX, RO and NF do not exhibit “breakthrough” behavior. That is, removal efficiency tends to be steady-state and does not vary over time.

4.2.2 Full-Scale Applications

Two drinking water systems, in North Carolina (Dowbiggin et al., 2021) and Alabama (Wetzel, 2021; WHNT News, 2019), recently constructed full-scale treatment plants using low-pressure (or “loose”) RO. These are the first two treatment plants utilizing membrane technology specifically targeted at PFAS removal from drinking water. Although performance data are not yet available from these facilities, the effectiveness studies enumerated in Section 4.2.1 include results from full-scale facilities using membrane separation to treat other contaminants.

4.3 Raw Water Quality Considerations

In general, water quality affects the design (e.g., concentrate volume, cleaning frequency, antiscalant selection) of RO and NF systems, but not removal efficiency. The literature specifically for PFAS removal by membranes supports this conclusion. For example, Appleman et al. (2013) found that the effectiveness of NF for PFAS removal was not impaired by the presence of humic acid. Similarly, Steinle-Darling and Reinhard (2008) found that ionic strength did not have a significant effect on removal performance. Although these authors noted a significant effect from pH, this effect was observed at pH 2.8, substantially lower than typical drinking water influent. Boonya-Atichart et al. (2016) found no significant effect within a more typical range of pH (5.5 to 10). Although they observed a slight decrease in effectiveness with increasing total dissolved solids, this effect was not significant.

4.4 Pre- and Post-Treatment Needs

In general, pretreatment requirements for membrane technologies depend on influent water quality as well as the type of membrane used. Most RO and NF processes include a prescreen or cartridge filter to remove sediment that could damage the membranes. RO and NF membranes also often require pre-treatment acid or antiscalant addition for scaling control (Bergman et al., 2012; Duranceau and Taylor, 2011). Pretreatment requirements, however, typically are independent of the specific contaminant targeted for removal. Calculations such as the silt density index (SDI), found in ASTM standard D4189, can provide insight into the fouling problems that are inherent in any membrane system (Bergman et al., 2012; Duranceau and

Taylor, 2011). SDI measures the fouling potential of suspended solids. Manufacturers typically specify maximum SDIs of 3 to 5 for RO and NF elements (Bergman et al., 2012). In addition, it is important to model and conduct pilot studies to assess the potential for fouling from substances such as natural organic matter, calcium carbonate, silica, calcium fluoride, barium sulfate, calcium sulfate, strontium sulfate, and calcium phosphate. The Langelier saturation index (LSI), described in ASTM standard D3738, characterizes the potential for CaCO₃ scaling. The LSI is used to indicate the tendency of water to precipitate, dissolve, or be in equilibrium with calcium carbonate, and what pH change is required to bring the water back to equilibrium (Bergman et al., 2012). The scaling potential of other substances may be determined from a saturation calculation. There is nothing unique about PFAS removal by RO/NF that suggests a different relationship between the major water quality parameters and typical pretreatment and cleaning requirements.

The permeate from RO and, in some cases, NF can be corrosive. The extent of this impact is site-specific (Bergman et al., 2012). In other drinking water treatment applications, the permeate is often blended with untreated water to produce a less corrosive finished water (Mickley, 2018). If the source water has a sufficiently low concentration of PFAS and other contaminants, blending may reduce post-treatment requirements. In instances where blending is not possible, post-treatment (e.g., sodium hydroxide or lime addition) can be required to control corrosion impacts (Lipp et al., 2010).

4.5 Waste Generation and Residuals Management Needs

There are no full-scale studies of residuals from RO or NF facilities specifically for the removal of PFAS. In general, however, the characteristics of membrane concentrates are predictable, and handling and treatment options are well understood. This waste stream contains the PFAS compounds and other dissolved solids removed from the treated water. The two full-scale facilities identified in Section 4.2.2 are designed for recovery rates of 85 to 92 percent (Dowbiggin et al., 2021; Wetzel, 2021; WHNT News, 2019), which means that concentrate flows at these facilities would account for 8 to 15 percent of influent (i.e., 100 percent minus the recovery rate). Assuming these facilities achieve 95 percent removal efficiency, PFAS concentrations in this waste stream would be approximately 6 to 12 times the concentration in influent water.¹³

For disposal of membrane concentrate, most systems use surface water discharge or discharge to sanitary sewer. Deep well injection is common in Florida. A small percentage of systems use land application, evaporation ponds, or recycling (Mickley, 2018). The large volume of residuals is a well-known obstacle to adoption of membrane separation technology, in general. In the case of PFAS removal, the high PFAS concentration in the residuals might limit the disposal options or require additional treatment prior to disposal, depending on state and local discharge regulations.

Studies specific to treatment of concentrate containing PFAS currently are limited to lab- or pilot-scale (Franke et al. 2021; Tow et al., 2021). The Alabama facility identified under Question 4.2.1 initially planned to treat membrane concentrate through its existing GAC filters prior to

¹³ The concentration in the reject stream can be calculated as the concentration in influent times the removal efficiency, divided by the rejection rate. In this example, $0.95 / 0.15 = 6.33$ and $0.95 / 0.08 = 11.88$.

discharge (WHNT News, 2019). More recent reports (Wetzel, 2021) do not address concentrate treatment at this facility. The North Carolina facility includes the construction of a discharge pipeline to a point “several miles” away, downstream of any drinking water intakes (Dowbiggin et al., 2021).

Periodic cleaning of the membrane system is necessary to recover productivity lost to fouling. This cleaning may include cycles of acid and caustic wash, depending on the nature of the fouling. Since the spent cleaning solution is generated infrequently and in small amounts, it is typically diluted by and handled with the concentrate.

4.6 Critical Design Parameters

Critical design parameters for membrane systems removing PFAS are:

- Pretreatment and cleaning requirements
- Membrane type
- Flux rate
- Recovery rate
- Residuals management options.

As discussed in Section 4.4, assumptions about pretreatment requirements and cleaning procedures, in general, are determined based on major water quality parameters, such as hardness parameters, chloride, sulfate, silica, pH, SDI, and total dissolved solids. They typically are not affected by trace contaminant influent concentrations or removal requirements. There is nothing unique about PFAS removal by membrane separation that suggests a different relationship between the major water quality parameters and typical pretreatment and cleaning requirements. Section 4.5 discusses residuals management options. The sections below discuss membrane type, flux rate, and recovery rate in more detail, including the range of values reported in the literature for these parameters. Section 7.4 identifies the specific values for each parameter used in EPA’s cost estimates.

4.6.1 Membrane Type

As discussed in Section 4.2.1, both RO and NF membranes can be effective at removing PFAS compounds. More specifically, RO membranes shown to be effective include those in the “loose” or low-pressure end of the RO category (Dowbiggin et al., 2021; Lipp et al., 2010). NF membranes shown to be effective are at the “tight” or low MWCO end of that category (Appleman et al., 2013; Steinle-Darling and Reinhard, 2008; Yu et al., 2016). The two current full-scale membrane system specifically designed for PFAS treatment both utilize RO membranes (Dowbiggin et al., 2021; Wetzel, 2021).

4.6.2 Flux Rate

The flux of an RO/NF system is the rate of permeate water per unit of membrane area, typically measured in gallons per square foot per day (gfd). While each stage of a membrane system will have a different flux, the average flux over all elements is a fundamental design parameter. In general, the higher the quality of the feed water, the higher the flux that may be achieved. Operating with excessively high flux, however, leads to fouling of the membrane elements. Depending on the nature of the fouling, it may be reversed by cleaning, or may require

replacement of the elements. As shown in Table 4-5, flux values found in the literature range from 6 to 44 gfd including bench scale studies. Data are not available for the flux rate employed at the two full-scale RO facilities constructed specifically for PFAS removal. Dickenson and Higgins (2016) report full-scale flux rates of approximately 12 gfd, but these are for potable reuse facilities. Bench-scale studies (Appleman et al., 2013; Lipp, 2010) show that RO and NF remain effective for PFAS removal at higher flux rates.

Table 4-5. Flux Rates for PFAS Treatment Reported in the Literature

Study Scale and Membrane Type	Source Water	Flux (gfd)	Source
Full Scale RO	WWTP	12	Dickenson and Higgins, 2016
Full Scale RO	WWTP	11.6	Dickenson and Higgins, 2016
Bench Scale NF	Lab	10 to 44	Appleman et al., 2013
Bench Scale RO	Lab	17.6 to 23.5	Lipp et al., 2010
Bench Scale NF	Lab	6 to 41	Lipp et al., 2010

gfd = gallons per square foot per day; NF = nanofiltration; RO = reverse osmosis; WWTP = potable reuse facility receiving water from wastewater treatment plant

4.6.3 Recovery Rate

As discussed in Section 4.1, the recovery rate is the percentage of the influent flow that is recovered as permeate. Increasing the recovery rate will increase the concentration of dissolved solids in the membrane reject water and will thus increase the required feed pressure and the potential for membrane scaling. Thus, the achievable recovery rate depends on the quality of the source water as well as the pretreatment of the water, and systems with high levels of total dissolved solids in their feed water will typically operate at lower recovery rates than systems with lower levels. As shown in Table 4-6, recovery rates found in the literature range from 78 to 92 percent.

Table 4-6. Recovery Rates for PFAS Treatment Reported in the Literature

Study Scale and Membrane Type	Source Water	Recovery Rate	Source(s)
Full Scale RO	WWTP	85%	Thompson et al., 2011
Full Scale RO	WWTP	85%	Dickenson and Higgins, 2016
Full Scale RO	WWTP	80%	Dickenson and Higgins, 2016
Full Scale RO	Surface	90%	Wetzel, 2021; WHNT News, 2019
Pilot Scale NF	Ground	78%	Franke et al., 2019
Full Scale RO	Surface	85 to 92%	Dowbiggin et al., 2021
Bench Scale NF	Ground	84%	Boonya-Atichart et al., 2016

NF = nanofiltration; RO = reverse osmosis; WWTP = potable reuse facility receiving water from wastewater treatment plant

4.7 References

- Appleman, T.D., Dickenson, E.R.V., Bellona, C., and Higgins, C.P. 2013. Nanofiltration and granular activated carbon treatment of perfluoroalkyl acids. *Journal of Hazardous Materials*, 260(2013), 740-746. <http://dx.doi.org/10.1016/j.jhazmat.2013.06.033>
- Appleman, T.D., Higgins, C.P., Quinones, Q., Vanderford, B.J., Kolstad, C., Zeigler-Holady, J.C., and Dickenson, E.R.V. 2014. Treatment of poly- and perfluoroalkyl substances in U.S. full-scale water treatment systems. *Water Research*, 51(2014), 246-255. <http://dx.doi.org/10.1016/j.watres.2013.10.067>
- Bergman, R.A., Garcia-Aleman, J., and Morgan, R. 2012. Membrane Processes. In Randtke, S.J. and Horsley, M.B. (Eds.), *Water Treatment Plant Design, Fifth Edition* (pp. 15.1-15.61). American Water Works Association/American Society of Civil Engineers.
- Boonya-Atichart, A., Boontanon, S. K., and Boontanon, N. 2016. Removal of perfluorooctanoic acid (PFOA) in groundwater by nanofiltration membrane. *Water Science and Technology*, 74 (11), 2627–2633. <https://doi.org/10.2166/wst.2016.434>
- CDM Smith. 2018. *Advanced Treatment Options for the Northwest Water Treatment Plant*. Final Report. Prepared for Brunswick County Public Utilities.
- Dickenson, E.R.V. and Higgins, C. 2016. *Treatment Mitigation Strategies for Poly- and Perfluoroalkyl Substances*. Web Report #4322. Water Research Foundation.
- Dowbiggin, B., Treadway, J., Nichols, J. and Walker G. 2021. Exploring Treatment Options for PFAS Removal in Brunswick County, North Carolina. *Journal AWWA*, 113(4), 10-19. <https://doi.org/10.1002/awwa.1705>
- DuPont. 2021. *FilmTec™ Reverse Osmosis Membranes Technical Manual*. Version 10. Retrieved from <https://www.dupont.com/content/dam/dupont/amer/us/en/water-solutions/public/documents/en/RO-NF-FilmTec-Manual-45-D01504-en.pdf>
- Duranceau, S.J. and Taylor, J.S. 2011. Membranes. In Edzwald, J.K. (Ed.), *Water Quality & Treatment: A Handbook on Drinking Water, Sixth Edition* (pp. 11.1-11.106). American Water Works Association.
- Franke, V., Ullberg, M., McCleaf, P., Wälinder, M., Köhler, S.J., and Ahrens, L. 2021. The Price of Really Clean Water: Combining Nanofiltration with Granular Activated Carbon and Anion Exchange Resins for the Removal of Per- And Polyfluoroalkyl Substances (PFASs) in Drinking Water Production. *ACS ES&T Water*, 2021(1), 782-795. <https://doi.org/10.1021/acsestwater.0c00141>
- Horst, J., McDonough, J., Ross, I., Dickson, M., Miles, J., Hurst, J., and Storch, P. 2018. Water Treatment Technologies for PFAS: The Next Generation. *Groundwater Monitoring & Remediation*, 38(2), 13-23. <https://doi.org/10.1111/gwmr.12281>
- Lipp, P., Sacher, F., and Baldauf, G. 2010. Removal of organic micro-pollutants during drinking water treatment by nanofiltration and reverse osmosis. *Desalination and Water Treatment*, 13(2010), 226-237. <http://doi.org/10.5004/dwt.2010.1063>

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Liu, C.J., Strathmann, T.J. and Bellona, C. 2021. Rejection of per- and polyfluoroalkyl substances (PFASs) in aqueous film-forming foam by high-pressure membranes. *Water Research*, 188(2021), 116546. <https://doi.org/10.1016/j.watres.2020.116546>

Mickley, M. 2018. *Updated and Extended Survey of U.S. Municipal Desalination Plants*. Desalination and Water Purification Research and Development Program Report No. 207. U.S. Department of the Interior, Bureau of Reclamation.

Steinle-Darling, E., and Reinhard, M. 2008. Nanofiltration for Trace Organic Contaminant Removal: Structure, Solution, and Membrane Fouling Effects on the Rejection of Perfluorochemicals. *J. Environ. Sciences*, 42, 5292–5297. <https://doi.org/10.1021/es703207s>

Thompson, J., Eaglesham, G., Reungoat, J., Poussade, Y., Bartkowf, M., Lawrence, M. and Mueller, J.F. 2011. Removal of PFOS, PFOA and other perfluoroalkyl acids at water reclamation plants in South East Queensland Australia. *Chemosphere*, 82(2011), 9-17. <https://doi.org/10.1016/j.chemosphere.2010.10.040>

Tow, E.W., Ersan, M.S., Kum, S., Lee, T., Speth, T.F., Owen, C. Bellona, C., Nadagouda, M.N., Mikelonis, A.M., Westerhoff, P., Mysore, C., Frenkel, V.S., DeSilva, V., Walker, S.W., Safulko, A.K., and Ladner, D.A. 2021. Managing and treating per- and polyfluoroalkyl substances (PFAS) in membrane concentrates. *AWWA Water Science*, 3(5), e1233. <https://doi.org/10.1002/aws2.1233>

U.S. Environmental Protection Agency (USEPA). 2021a. *Drinking Water Treatability Database: Perfluorooctanoic Acid*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10520>

USEPA. 2021b. *Drinking Water Treatability Database: Perfluorooctane Sulfonate*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=10940>

USEPA. 2021c. *Drinking Water Treatability Database: Per- and Polyfluoroalkyl Substances*. Retrieved from <https://tdb.epa.gov/tdb/contaminant?id=11020>

Wetzel, M. 2021. *Reverse osmosis filtration facility near completion*. The Moulton Advertiser. Retrieved from: https://www.moultonadvertiser.com/news/article_dd221c14-fabf-11eb-801f-c3b7ff0b4dc4.html

WHNT News. 2019. *WMEL water authority approves \$30.5 million contract for Reverse Osmosis treatment system*. Nexstar Media Inc. Retrieved from: <https://whnt.com/news/wmel-water-authority-approves-30-5-million-contract-for-reverse-osmosis-treatment-system/>

Yu, Y., Zhao, C., Yu, L., Li, P., Wang, T., and Xu, Y. 2016. Removal of perfluorooctane sulfonates from water by a hybrid coagulation–nanofiltration process. *Chemical Engineering Journal*, 289(1), 7-16. <https://doi.org/10.1016/j.cej.2015.12.048>.

5.0 Point-of-Use/Point-of-Entry Treatment

5.1 Operating Principle

A POU/POE device uses a miniaturized version of a centralized treatment process to meet water quality standards at the household level. POU devices are sized to treat water for consumption at individual taps (e.g., a kitchen sink). POE devices are designed to treat water where the service line enters the house (e.g., in the basement). When a system installs, controls (i.e., owns), and maintains POU/POE devices at all customer locations where water is consumed (e.g., residences), it can forego centralized treatment (USEPA, 2006). Because POU/POE devices treat a fraction of the water delivered by a system, a compliance program that relies on POU/POE devices may be more cost-effective for smaller systems.

The NSF¹⁴ committee of stakeholders has updated the NSF/American National Standards Institute (NSF/ANSI) standards applicable to POU/POE devices to incorporate requirements for PFAS removal. To be certified under the standards a device must reduce the total concentration of PFOA and PFOS to below 70 ng/L (NSF International, 2019). Several organizations (e.g., NSF International, Underwriters Laboratories, Water Quality Association) provide third-party testing and certification that POU/POE devices meet drinking water treatment standards.

The discussion in this section focuses on POU/POE RO devices because these are the most common type of device certified for PFAS removal. The operating principle for POU/POE RO devices is the same as centralized RO: they separate solutes such as PFAS compounds from solution by forcing the solvent to flow through a membrane at a pressure greater than the normal osmotic pressure. In addition to an RO membrane for dissolved contaminant removal, POU/POE RO devices often have a sediment pre-filter and a carbon filter in front of the RO membrane, a 3- to 5-gallon treated water storage tank, and a carbon filter between the tank and the tap.

POU/POE devices are not currently a compliance option because the regulatory options under consideration require treatment to concentrations below the current certification standard of 70 ng/L total of PFOA and PFOS. However, POU/POE treatment might become a compliance option for small systems in the future if NSF/ANSI develop a new certification standard that mirrors EPA's proposed regulatory standard. To meet a PFAS drinking water standard, a system would need to purchase, install, and maintain certified devices for all customers. Usually, a system would install a single POU RO device at the kitchen tap for each residential customer. Nonresidential customers might require multiple POU devices (e.g., for drinking fountains) or a single POE device. Installation requires retrofitting the device into existing plumbing fixtures (e.g., tapping into the water supply line to insert a treated water line with a dedicated tap and adding a wastewater connection for the RO membrane concentrate or reject). Maintenance primarily consists of filter replacement, often on a fixed schedule that varies by filter type. Monitoring water quality at individual treated water taps will also be necessary to demonstrate compliance with a perchlorate drinking water standard.

¹⁴ Formerly National Sanitation Foundation

5.2 Effectiveness for PFAS Removal

As discussed above, POU/POE devices certified under the current NSF/ANSI standards remove PFOA and PFOS to a total of less than 70 ng/L. There is evidence in the literature that POU/POE RO devices can achieve even lower concentrations. Patterson et al. (2019) tested three such RO devices for removal of PFBS, PFHxS, PFHpA, PFOS, PFOA, and PFNA. The devices were sized for POU use, but plumbed with additional equipment (storage tanks, booster pumps) to simulate POE usage. Two of the devices removed each of the PFAS compounds tested to below the quantitation limit (10 ng/L) throughout the test period. The third device removed the compounds to below the quantitation limit except for one sampling event. During this sampling event, which took place immediately upon startup after a five-day stagnation period, all the PFAS compounds except PFBS were detected in the treated water at concentrations from 11 to 77 ng/L. The concentrations returned to levels below the quantitation limit during the next sampling event four hours later. Additional support for the effectiveness of POU/POE programs for PFAS removal is evident from the number of community-scale applications of the technology, as listed in Table 5-1.

Table 5-1. Community-Scale Applications of POU/POE Treatment to Remove PFAS from Drinking Water

Location	Number of Households	POU/POE	Year of Startup	Sources
Camp Grayling, Crawford County, Michigan	Not reported	Not reported	2018	Michigan DEGLE 2021b
House Street Disposal Area, Belmont, Kent County, Michigan	781	546 POE and 235 POU	2020	Michigan DEGLE 2021c
Alpena Combat Readiness Training Center, Alpena County, Michigan	31	Not reported	Not reported	Michigan DEGLE 2021a
Former Washington County Landfill, Lake Elmo, Minnesota	57	POE	2007	ATSDR 2008
Deepwater, Salem County, New Jersey	Not reported	Not reported	2011	Dunn 2011
Bennington and North Bennington, Vermont	255	POE	2020	Danko 2018; VDEC 2020
Hoosick Falls, New York	>800	POE	Not reported	NYS DEC 2021

POE = Point-of Entry; POU = Point-of-Use

5.3 Raw Water Quality Considerations

Because the POU/POE RO devices will be installed at service taps that are downstream of a system's entry point to the distribution system, EPA assumes that the raw water entering a POU/POE RO device will be water that is suitable for consumption except for an exceedance of the proposed perchlorate regulatory standard. As noted in the next section, POU/POE RO devices include pre-filters to address potential interference of delivered water quality with RO performance.

5.4 Pre- and Post-Treatment Needs

POU/POE RO devices include various filters to address pre- and post-treatment concerns. Most devices include a sediment filter for solids removal to prevent membrane fouling and a pre-RO carbon filter to remove chlorine and organic compounds that could impair membrane function. They also include a carbon filter after the membrane and storage tank to remove any organics that may remain or bacterial growth that occurs during storage. Because the POU device is installed at the tap, there are no potential adverse impacts on the distribution system.

5.5 Waste Generation and Residuals Management Needs

The treatment process waste comprises wastewater and used filter cartridges. Waste disposal methods must comply with state and local requirements. The wastewater connection is generally plumbed to the household sewer system, which uses either an on-site septic system or a centralized wastewater collection system for disposal. Depending on state and local regulations, the used cartridge filters may be included in household solid waste (USEPA, 2006).

5.6 Critical Design Parameters

EPA's cost estimates for POU/POE treatment programs assume the use of POU, as opposed to POE, devices because ingestion is the primary route of concern for exposure to PFAS. In addition to the POU devices themselves, there are several components to the design of a POU program that are primary cost drivers. These include the following:

- POU RO device installation
- Public education program development
- POU device monitoring
- POU device maintenance.

Chapter 7 discusses each of these parameters in more detail and identifies the specific values for each used in EPA's cost estimates.

5.7 References

Agency for Toxic Substances and Disease Registry (ATSDR). 2008. *Perfluorochemical Contamination in Lake Elmo Final Release and Oakdale, Washington County, Minnesota*.

Retrieved from:

https://www.atsdr.cdc.gov/HAC/pha/PFCsLakeElmo/PFCs_in_Lake_Elmo_PHA_8-29-2008_508.pdf

Gascoyne, J. 2018. *2018 PFAS Sampling Summary Report*. ATC Group Services LLC. Retrieved from:

<https://anrweb.vt.gov/PubDocs/DEC/Hazsites/20184763.SVRA.2018.DW.SamplingSummary.rpt.pdf>

Danko, A. 2018. *Treatment Technologies for PFAS Site Management*. Retrieved from:

<https://frtr.gov/pdf/meetings/nov18/presentations/handouts/danko-handout.pdf>

Michigan Department of Environment, Great Lakes, and Energy (DEGLE). 2021a. *PFAS Response and Investigations - Alpena County, Alpena, Alpena Combat Readiness Training*

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March 2024

Center (CRTC). Michigan PFAS Action Response Team. Retrieved from:
https://www.michigan.gov/pfasresponse/0,9038,7-365-86511_82704_84544---,00.html

Michigan DEGLE. 2021b. *PFAS Response and Investigations - Crawford County, Grayling, Camp Grayling - Lake Margrethe*. Michigan PFAS Action Response Team. Retrieved from:
https://www.michigan.gov/pfasresponse/0,9038,7-365-86511_82704-488777--,00.html

Michigan Department of Environment, Great Lakes, and Energy (DEGLE). 2021c. *PFAS Response and Investigations - House Street Disposal Area, Belmont, Kent County*. Michigan PFAS Action Response Team. Retrieved from:
https://www.michigan.gov/pfasresponse/0,9038,7-365-86511_82704_83030---,00.html

Dunn, P. 2011. *DuPont settles suit over claims chemical tainted drinking water around Salem County plant*. Today's Sunbeam. Retrieved from:
https://www.nj.com/salem/2011/03/dupont_settles_suit_over_claim.html

NSF International. 2019. *PFOA/PFOS Reduction Claims Requirements Added to NSF Standards for Drinking Water Treatment Devices*. Retrieved from: <https://www.nsf.org/news/pfoa-pfos-reduction-claims-requirements-added-to-nsf-standards>

New York State Department of Environmental Conservation (NYS DEC). 2021. *Hoosick Falls Area Information for Communities Impacted by Per- and Poly-fluorinated Alkyl Substances (PFAS)*. Retrieved from: <https://www.dec.ny.gov/chemical/108791.html>

Patterson, C., Burkhardt, J., Schupp, D., Krishnan, R., Dymment, S., Merritt, S., Zintek, L., and Kleinmaier, D. 2018. Effectiveness of point-of-use/point-of-entry systems to remove per- and polyfluoroalkyl substances from drinking water. *AWWA Water Science*, 1(2), e1131.
<https://doi.org/10.1002/aws2.1131>

Sullivan, M. 2018. *Addressing Perfluorooctane Sulfonate (PFOS) and Perfluorooctanoic Acid (PFOA)*. U.S. Department of Defense. Retrieved from:
<https://denix.osd.mil/derp/home/documents/pfos-pfoa-briefing-to-the-hasc/>

USEPA. 2006. *Point-of-Use or Point-of-Entry Treatment Options for Small Drinking Water Systems*. Office of Ground Water and Drinking Water. EPA-815-R-06-010.

Vermont Department of Environmental Conservation (VDEC). 2020. *Bennington PFAS Sampling and Treatment System Maintenance Considering Ongoing COVID-19 Emergency*. Retrieved from: <https://dec.vermont.gov/pfas/pfoa>

6.0 Nontreatment Alternatives

6.1 Application Principle

For small water utilities that lack the financial and/or technical capacity to implement a new treatment-based compliance strategy, nontreatment options may offer a more cost-effective path to compliance. Nontreatment options essentially replace the contaminated water source with water that meets drinking water standards, including new standards for PFAS compounds.

Nontreatment solutions for drinking water compliance include the following (USEPA, 2006):

- well rehabilitation
- contaminant source elimination
- new well construction
- interconnecting with another system to purchase water.

The feasible nontreatment options will depend on site-specific circumstances such as system size, source water type, contaminant reduction needs, and proximity to alternative water sources. For small systems, neither well rehabilitation nor source elimination (e.g., remediation of PFAS-contaminated soils or groundwater) is likely to be feasible and cost-effective. Another option – blending water from existing wells – may be a feasible, low-cost option for systems that have multiple wells including some with PFAS concentrations substantially below the new standards. For systems that cannot blend water from existing sources to comply with the new PFAS regulations, two feasible nontreatment options include the following:

1. a new well to replace the contaminated source water
2. interconnection to purchase water from a supplier.

These two options (new wells and interconnection) are likely to have higher costs than the other options (well rehabilitation and source elimination) (USEPA, 2006).

The costs associated with drilling a new well include the initial hydrological assessment, pilot hole drilling, developing the final well design, drilling the well bore, installing well casings, screens, and filters, development of the well, and installation of the pump and power source (Harter, 2003). A hydrological assessment identifies groundwater sources of suitable quality and adequate long-term supply. When replacing an existing well, the costs will also include connecting the well to the existing water distribution system.

The interconnection option involves laying a pipeline to connect the affected system to the distribution network of a neighboring system that can provide adequate water that meets all applicable drinking water standards. Costs include the cost of purchased water as well as construction and maintenance of the interconnection pipeline. Pipeline costs will depend on proximity of the neighboring system, topography of the distance to be covered, and right-of-way requirements for pipes and booster pump stations.

6.2 Compliance Effectiveness

Nontreatment options achieve compliance by replacing a PFAS-contaminated water source with an alternative water source that complies with the new PFAS regulations. This strategy is

inherently compliant if the new water source is not at risk for PFAS contamination. If the wholesale supplier of purchased water has PFAS contamination, it must implement an effective treatment process because the water it sells must comply with the PFAS standard before it can be distributed to the purchasing system.

Drinking water systems have successfully used nontreatment options to alleviate PFAS concerns. In response to PFAS contamination near Peterson Air Force Base in Colorado, three water districts turned off their wells and are purchasing surface water from another source (Sullivan, 2018). In March 2016, Fort Drum Public Works in New York took two drinking water wells out of service following detection of PFAS. Fort Drum dug five new wells with a maximum capacity of 2.2 MGD in August 2016 (Fort Drum, 2019).

6.3 Raw Water Quality Considerations

A system will need to determine whether the change in source water may affect other existing treatment processes (e.g., chlorination), or if changes in water quality may affect the distribution system (e.g., purchased water has a different pH). Changes in delivered water chemistry that trigger major process additions or adjustments could diminish the cost-effectiveness of nontreatment options.

6.4 Pre- and Post-Treatment Needs

By definition, there are no pre-treatment needs to consider with a change in source water. All treatment adjustments to account for differences in source water quality would necessarily occur after the point of source water connection. If the alternative water source has chemical parameters that differ substantially from the original source water and may affect water quality elsewhere in the system, then there may be additional treatment needs to adjust water chemistry.

6.5 Waste Generation and Residuals Management Needs

An interconnection or new well should not have incremental wastes or residuals requiring management.

6.6 Critical Design Assumptions

For new wells, key design parameters are the following:

- Total flow rate requirements and flow per well
- Well depth (and screened depth)
- Distance from well to distribution system.

For an interconnection option, key design parameters include:

- Flow rate requirements
- Distance to interconnection water supply
- Pressure at water supply source
- Cost of purchased water.

Chapter 7 discusses each of these parameters in more detail and identifies the specific values for each used in EPA's cost estimates.

6.7 References

Fort Drum Public Works (FDPW). 2019. *2018 Annual Drinking Water Quality Report*. Retrieved from:

https://home.army.mil/drum/application/files/8615/5535/5022/2018_Fort_Drum_AWQR.pdf

Harter, T. 2003. *Water Well Design and Construction*. University of California, Division of Agricultural and Natural Resources.

Sullivan, M. 2018. *Addressing Perfluorooctane Sulfonate (PFOS) and Perfluorooctanoic Acid (PFOA)*. U.S. Department of Defense. Retrieved from:

<https://denix.osd.mil/derp/home/documents/pfos-pfoa-briefing-to-the-hasc/>

U.S. Environmental Protection Agency (USEPA). 2006. *Technology and Cost Document for the Final Ground Water Rule*. EPA-815-R-06-015.

7.0 Costs for Treatment and Nontreatment Options

7.1 Introduction

7.1.1 Overview and Cost Modeling Approach

This chapter presents estimated costs for installing and operating the technologies and nontreatment options discussed in Chapters 2 through 6. Based on the information in those chapters, particularly the data on engineering design specifications, EPA developed work breakdown structure (WBS) cost estimating models for each of the PFAS treatment technologies. The WBS models are spreadsheet-based engineering models for individual treatment technologies, linked to a central database of component unit costs. EPA developed the WBS model approach as part of an effort to address recommendations made by the Technology Design Panel (TDP), which convened in 1997 to review the Agency's methods for estimating drinking water compliance costs (USEPA, 1997). The TDP consisted of nationally recognized drinking water experts from the EPA, water treatment consulting companies, public and private water utilities and suppliers, equipment vendors, and Federal and State regulators in addition to cost estimating professionals.

In general, the WBS approach involves breaking a process down into discrete components for the purpose of estimating unit costs. The WBS models represent improvements over past cost estimating methods by increasing comprehensiveness, flexibility, and transparency. By adopting a WBS-based approach to identify the components that should be included in a cost analysis, the models produce a more comprehensive assessment of the capital and operating requirements for a treatment system. The documentation for the individual WBS models (USEPA, 2024a; 2024b; 2024c; 2024d) provides complete details on the structure, content, and use of the models. EPA used the WBS models to develop the costs presented in this chapter. The models and their documentation can be accessed at: <https://www.epa.gov/dwregdev/drinking-water-treatment-technology-unit-cost-models-and-overview-technologies>.

The remainder of this section provides a brief overview of the common elements of all the WBS models and information on the anticipated accuracy of the resulting cost estimates. Subsequent sections describe how EPA used each individual technology specific WBS model to estimate costs for PFAS treatment and present the resulting cost estimates.

7.1.2 Work Breakdown Structure (WBS) Models

Each WBS model contains the work breakdown for a particular treatment process and preprogrammed engineering criteria and equations that estimate equipment requirements for user-specified design requirements (e.g., system size and influent water quality). Each model also provides unit and total cost information by component (e.g., individual items of capital equipment) and totals the individual component costs to obtain a direct capital cost. Additionally, the models estimate add-on costs (permits, pilot study, and land acquisition costs for each technology), indirect capital costs, and annual operation and maintenance (O&M) costs, thereby producing a complete compliance cost estimate.

Primary inputs common to all the WBS models include design flow and average flow in million gallons per day (MGD). Each WBS model has default designs (input sets) that correspond to specified categories of flow, but the models can generate designs for many other combinations of flows. To estimate costs for PFAS compliance, EPA fit cost curves to the WBS estimates for up to 49 different flow rates.¹⁵ Thus, the cost estimates in Sections 7.2 through 7.5, and Appendix A are in the form of equations.

Another input common to all the WBS models is “component level” or “cost level.” This input drives the selection of materials for items of equipment that can be constructed of different materials. For example, a low-cost system might include fiberglass pressure vessels and PVC piping. A high-cost system might include stainless steel pressure vessels and stainless-steel piping. The component level input also drives other model assumptions that can affect the total cost of the system, such as building quality and heating and cooling. The component level input has three possible values: low cost, mid cost, and high cost. To estimate costs for PFAS treatment, EPA generated separate cost equations for each of the three component levels, thus creating a range of cost estimates for use in national compliance cost estimates.

The third input common at all the WBS models is system automation, which allows the design of treatment systems that are operated manually or with varying degrees of automation (i.e., with control systems that reduce the need for operator intervention). The cost estimates in the technology-specific sections below are for systems that are fully automated, minimizing the need for operator intervention and reducing operator labor costs.

The WBS models generate cost estimates that include a consistent set of capital, add-on, indirect, and O&M costs. Table 7-1 identifies these cost elements, which are common to all the WBS models and included in the cost estimates below. Sections 7.2 through 7.5 identify the technology-specific cost elements included in each model. The documentation for the WBS models (USEPA, 2024a; 2024b; 2024c; 2024d) provide more information on the methods and assumptions used in the WBS models to estimate the costs for both the technology-specific and common cost elements.

¹⁵ Specifically, for each scenario modeled and separately for total capital and for O&M costs, EPA fit up to three curves: one covering small systems (less than 1 MGD design flow), one covering medium systems (1 MGD to less than 10 MGD design flow), and one covering large systems (10 MGD design flow and greater). For each curve fit, EPA chose from among several possible equation forms: linear, quadratic, cubic, power, exponential, and logarithmic. EPA chose the form that resulted in the best correlation coefficient (R^2), subject to the requirement that the equation must be monotonically increasing over the appropriate range of flow rates (i.e., within the flow rate category, the equation must always result in higher estimated costs for higher flow systems than for lower flow systems).

Table 7-1. Cost Elements Included in All WBS Models

Cost Category	Components Included
Direct Capital Costs	<ul style="list-style-type: none"> • Technology-specific equipment (e.g., vessels, basins, pumps, treatment media, piping, valves) • Instrumentation and system controls • Buildings • Residuals management equipment
Add-on Costs	<ul style="list-style-type: none"> • Land • Permits • Pilot testing
Indirect Capital Costs	<ul style="list-style-type: none"> • Mobilization and demobilization • Architectural fees for treatment building • Equipment delivery, installation, and contractor’s overhead and profit • Sitework • Yard piping • Geotechnical • Standby power • Electrical infrastructure • Process engineering • Contingency • Miscellaneous allowance • Legal, fiscal, and administrative • Sales tax • Financing during construction • Construction management
O&M Costs: Technology-specific	<ul style="list-style-type: none"> • Operator labor for technology-specific tasks (e.g., managing backwash and media replacement) • Materials for O&M of technology-specific equipment • Technology-specific chemical usage • Replacement of technology-specific equipment that occurs on an annual basis (e.g., treatment media) • Energy for operation of technology-specific equipment (e.g., mixers)
O&M Costs: Labor	<ul style="list-style-type: none"> • Operator labor for O&M of process equipment • Operator labor for building maintenance • Managerial and clerical labor
O&M Costs: Materials	<ul style="list-style-type: none"> • Materials for maintenance of booster or influent pumps • Materials for building maintenance
O&M Costs: Energy	<ul style="list-style-type: none"> • Energy for operation of booster or influent pumps • Energy for lighting, ventilation, cooling, and heating
O&M Costs: Residuals	<ul style="list-style-type: none"> • Residuals management operator labor, materials, and energy • Residuals disposal and discharge costs

In addition to costs, the models also output an estimated useful life, in years, for each WBS component. The useful lives vary by component type (e.g., buildings generally last longer than mechanical equipment) and by material (e.g., steel tanks generally last longer than plastic tanks). The models use the component useful lives to calculate an average useful life for the entire system. The calculation uses a reciprocal weighted average approach, which is based on the relationship between a component’s cost (C), its useful life (L) and its annual depreciation rate

(A) under a straight-line depreciation method. The formula below shows the reciprocal weighted average calculation:

$$\text{Average Useful Life} = \frac{\sum_{n=1}^N C_n}{\sum_{n=1}^N A_n} = \frac{C}{A}$$

where:

C_n denotes the cost of component n , $n=1$ to N

C denotes total cost of all N components

A_n denotes the annual depreciation for component n , which equals C_n/L_n

A denotes total annual depreciation for the N components.

7.1.3 WBS Model Accuracy

Costs for a given system can vary depending on site-specific conditions (e.g., raw water quality, climate, local labor rates, and location relative to equipment suppliers). The costs presented here are based on national average assumptions and include a range (represented by low-, mid-, and high-cost equations) intended to encompass the variation in costs that systems would incur to remove PFAS. To validate the engineering design methods used by the WBS models and increase the accuracy of the resulting cost estimates, EPA has subjected the individual models to a process of external peer review by nationally recognized technology experts.

The GAC model underwent peer review in 2006. Two of the three reviewers felt they had enough experience with GAC cost estimates to evaluate the model's accuracy. One of these reviewers expressed the opinion that resulting cost estimates would be in the range of budget estimates (+30 to -15 percent). The other reviewer did not provide a precise estimate of the model's accuracy range but commented that the resulting cost estimates were reasonable. EPA made substantial revisions to the GAC model in response to the peer review.

The IX model underwent peer review in 2005, during an early stage of its development. One peer reviewer responded that resulting cost estimates were in the range of budget estimates (+30 to -15 percent). The other two reviewers thought the estimates were order of magnitude estimates (+50 to -30 percent), with an emphasis on the estimates being high. The IX model has since undergone extensive revision, both in response to the peer review and to adapt it for PFAS treatment using selective resin.

The RO/NF model underwent peer review in 2007. The majority of peer reviewers who evaluated the model expressed the opinion that resulting cost estimates would be in the range of budget estimates (+30 to -15 percent). The RO model has since undergone substantial revision in response to the peer review comments.

EPA received peer review comments on the non-treatment model in May 2012. The first reviewer responded that cost estimates resulting from the non-treatment model were in the range of budget estimates (+30 to -15 percent). The second reviewer thought the cost estimates were order of magnitude estimates (+50 to -30 percent). The third reviewer felt the cost estimates were

definitive (+15 to -5 percent), except for land costs, which were difficult to assess due to regional variations. EPA revised the nontreatment model in response to the peer review recommendations.

7.1.4 Model Updates for Final Rule

In response to public comments on the proposed PFAS rule, EPA made a number of updates to the WBS models. First, EPA updated the models' cost outputs to 2022 dollars. The Agency accomplished this by escalating unit costs using indices including the Bureau of Labor Statistics producer price indices (USBLS, 2010). EPA updated each unit cost using the change in the relevant price index from year 2020 to 2022. For example, the EPA applied the percent increase of the price of metal tanks and vessels to the price of metal tanks and vessels in the WBS cost models. The EPA also collected new vendor price quotes for cost driver equipment components (e.g., pressure vessels, treatment media). In addition, EPA made the following adjustments to the models' inputs and assumptions:

- EPA updated the pilot study costs included in each of the treatment technology models. As part of this update, EPA increased the estimated length of the pilot study and the frequency of sampling during the pilot study. Additionally, EPA added a full year of confirmation sampling after full-scale installation to the estimated pilot study costs.
- EPA changed its assumptions regarding contingency. Specifically, EPA incorporated contingency at all cost levels, not just the high-cost level. EPA also increased the complexity factor applied to estimate contingency for systems using GAC and non-treatment options. Taken together, these changes result in a contingency factor of 5 to 10 percent depending on total project cost at all cost levels.
- EPA changed the input assumptions for the nontreatment interconnection option to incorporate booster pumps designed to account for friction loss in interconnecting piping (see Section 7.6.3.3).

7.2 Costs for GAC

7.2.1 Model Components and Assumptions

USEPA (2024a) provides a complete description of the engineering design process used by the WBS model for GAC. The model can generate costs for two types of design:

- Pressure designs where the GAC bed is contained in stainless steel, carbon steel, or fiberglass pressure vessels
- Gravity designs where the GAC bed is contained in open concrete basins.

Table 7-2 shows the technology-specific capital equipment and O&M requirements included in the GAC model. These items are in addition to the common WBS cost elements listed in Table 7-1.

Table 7-2. Technology-Specific Cost Elements Included in the GAC Model

Cost Category	Major Components Included
Direct Capital Costs	<ul style="list-style-type: none"> • Booster pumps for influent water (for gravity GAC designs) • Contactors (either pressure vessels or concrete basins) that contain the GAC bed • Tanks and pumps for backwashing the contactors • GAC transfer and storage equipment • Spent GAC reactivation facilities (if on-site reactivation is selected) • Associated piping, valves and instrumentation
O&M Costs: Labor	<ul style="list-style-type: none"> • Operator labor for contactor maintenance (for gravity GAC designs) • Operator labor for managing backwash events • Operator labor for backwash pump maintenance (if backwash occurs weekly or more frequently) • Operator labor for GAC transfer and replacement
O&M Costs: Materials	<ul style="list-style-type: none"> • Materials for contactor maintenance (accounts for vessel relining in pressure designs, because GAC can be corrosive, and for concrete and underdrain maintenance in gravity designs) • Materials for backwash pump maintenance (if backwash occurs weekly or more frequently) • Replacement virgin GAC (limited to loss replacement only if reactivation is selected)
O&M Costs: Energy	<ul style="list-style-type: none"> • Operating energy for backwash pumps
O&M Costs: Residuals	<ul style="list-style-type: none"> • Discharge fees for spent backwash • Fees for reactivating spent GAC (if off-site reactivation is selected) • Labor, materials, energy, and natural gas for reactivation facility (if on-site reactivation is selected) • Disposal of spent GAC (if disposal is selected)

For small systems (less than 1 MGD) using pressure designs, the GAC model assumes the use of package treatment systems that are pre-assembled in a factory, mounted on a skid, and transported to the site. The model estimates costs for package systems by costing all individual equipment line items (e.g., vessels, interconnecting piping and valves, instrumentation, and system controls) in the same manner as custom-engineered systems. This approach is based on vendor practices of partially engineering these types of package plants for specific systems (e.g., selecting vessel size to meet flow and treatment criteria). The model applies a variant set of design inputs and assumptions that are intended to simulate the use of a package plant and that reduce the size and cost of the treatment system. USEPA (2024a) provides complete details on the variant design assumptions used for package plants.

The paragraphs below describe the specific inputs and assumptions that EPA used to generate the costs in Section 7.2.2. Other inputs and assumptions not discussed below (e.g., loading rate, number of booster pumps, backwash frequency, bed expansion) remained as described in USEPA (2024a).

7.2.1.1 Design Type

Systems often choose between pressure and gravity GAC designs based on cost (Brady and Moran, 2012; Summers et al., 2011). However, groundwater systems are more likely to choose pressure designs to maintain their existing pressure head. For these systems, use of gravity contactors would entail installation and operation of new pumps to restore pressure after GAC

treatment (Summers et al., 2011). Therefore, for treatment of groundwater, EPA generated cost equations for pressure designs only. For treatment of surface water, EPA generated separate cost equations for pressure and gravity designs.

7.2.1.2 EBCT and Contactor Configuration

For pressure designs, the estimates below and in Appendix A assume two vessels in series with a minimum total EBCT of 20 minutes (i.e., 10 minutes per vessel). For gravity designs, they assume contactors in parallel with a minimum total EBCT of 20 minutes. These assumptions are consistent with design engineer and GAC vendor recommendations for PFAS removal as discussed in Sections 2.6.1 and 2.6.2. The EBCT per vessel is also consistent with the data used to derive the bed life equations (10 minutes).

7.2.1.3 Bed Life

As discussed in Sections 2.2.2 and 2.6.3, GAC bed life depends on factors including target removal efficiency, influent water quality (particularly natural organic matter), and the specific PFAS compound(s) targeted. To accommodate variations in these factors, EPA generated separate cost equations at 5,000 BV increments for bed lives ranging from 5,000 to 75,000 BV. Each 5,000 BV increment corresponds to a 2- to 5-month shift in changeout frequency, depending on system size. To estimate national costs, EPA selected from among these cost equations using the bed life equations described in Section 2.6.3. EPA rounded results from the bed life equations down to the nearest 5,000 BV, which errs on the side of higher costs.

The bed life equations are based on data representative of a single contactor with an EBCT of 10 minutes. As discussed in Section 7.2.1.1, the estimates below assume two contactors in series, each with an EBCT of 10 minutes (for pressure systems) or multiple contactors in parallel, each with an EBCT of 20 minutes (for gravity systems). Either of these configurations should result in a longer bed life than estimated for a single, 10-minute EBCT contactor (see Section 2.6.2). EPA did not adjust the bed life results to account for the more efficient contactor configuration assumptions. Not incorporating an adjustment for configuration errs on the side of higher costs and is intended to compensate for the fact that the bed life equations are based in part on RSSCT data, which might overestimate full-scale bed life (see Section 2.6.3). Note that EPA does not have data on the degree to which RSSCTs might overestimate bed life or to quantify the bed life extension resulting from contactor configuration. Therefore, the net result of this compensating adjustment is uncertain.

7.2.1.4 Residuals Management

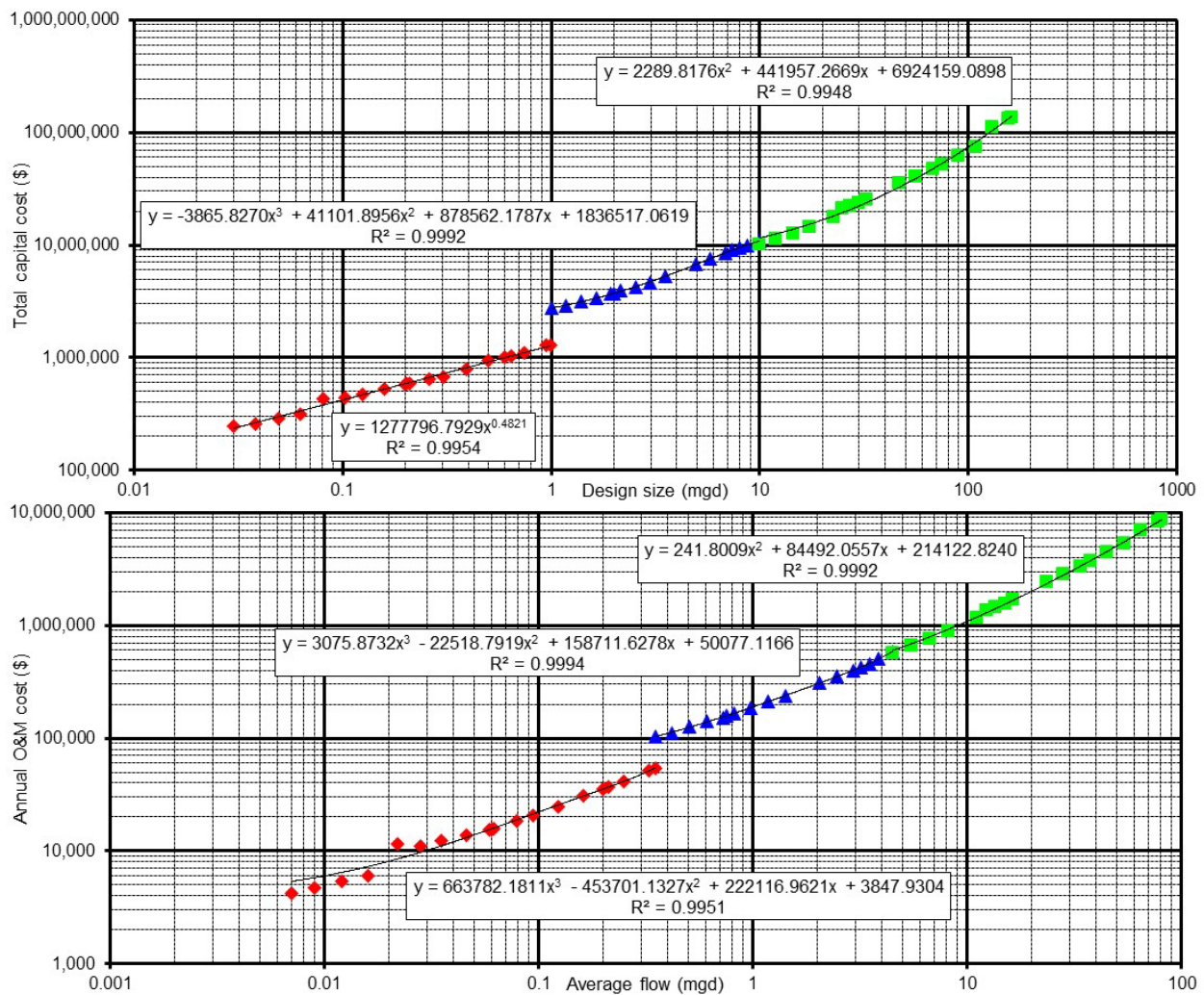
EPA generated separate cost equations for two spent GAC management scenarios:

- Off-site reactivation under current RCRA non-hazardous waste regulations
- Off-site disposal as a hazardous waste and replacement with virgin GAC (i.e., single use operation).

The first scenario reflects typical management practices under current regulations. The second scenario provides an upper bound on other options that might emerge under future air quality regulations (e.g., off-site disposal as a non-hazardous waste and replacement with virgin GAC) or RCRA hazardous waste regulations (e.g., off-site reactivation as a hazardous waste,).

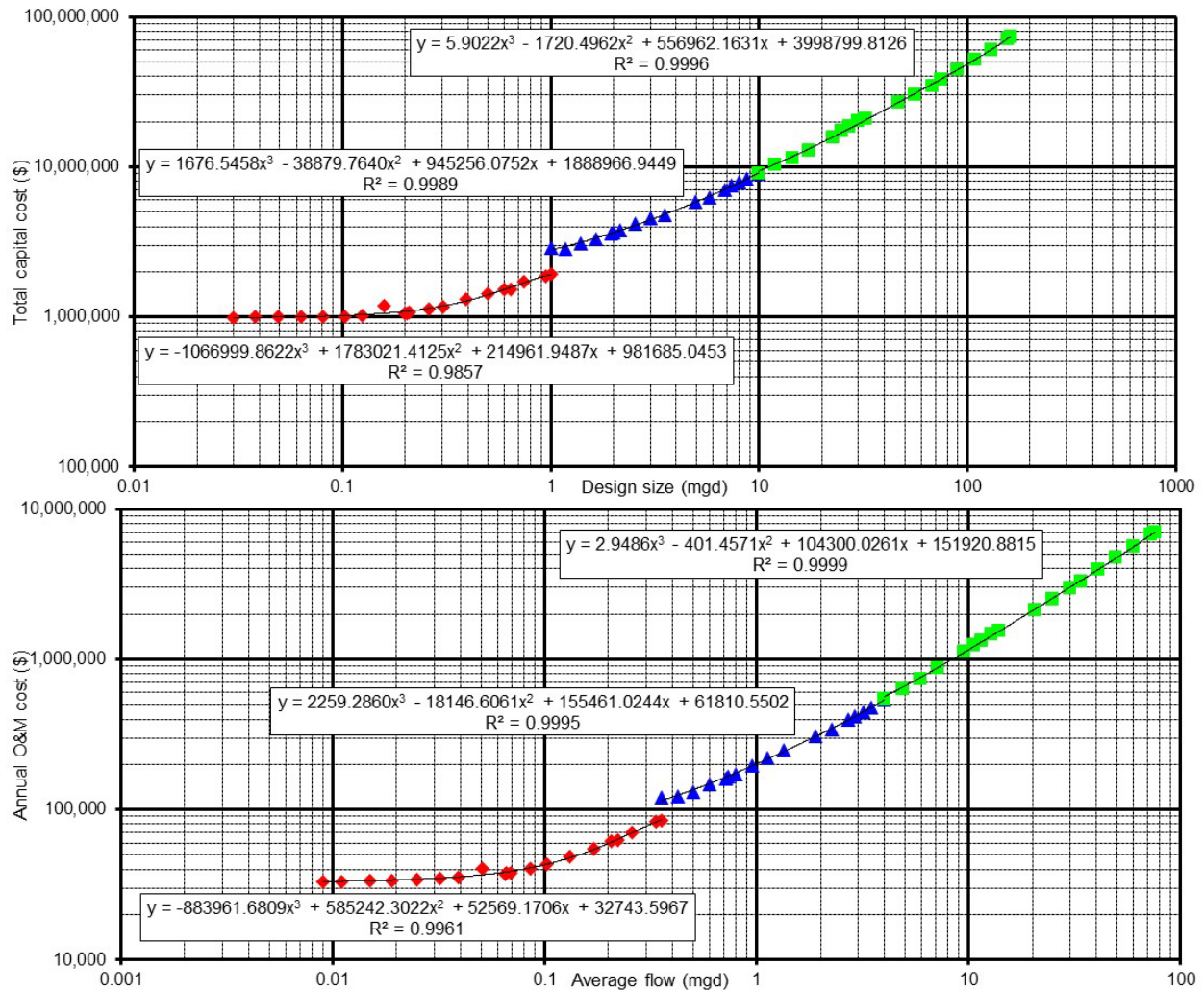
7.2.2 Cost Estimates

The graphs below plot WBS cost model results in 2022 dollars at the mid cost level for removal of PFAS from groundwater using pressure GAC (Figure 7-1) and surface water using gravity GAC (Figure 7-2), assuming a bed life of 50,000 BV and off-site GAC reactivation as a non-hazardous waste. In these exhibits, note that costs increase at 1 MGD design flow (0.355 MGD average flow) because of the transition from package systems (used by small systems) to custom-engineered systems (used by large systems). Appendix A provides complete cost equations for across the range of bed life and residuals management scenarios, including the high, mid, and low-cost levels and for treatment of groundwater and surface water. Appendix B presents example WBS model outputs at selected flow rates, allowing review of individual cost line items.



Note: costs shown assume bed life of 50,000 BV and off-site reactivation of spent GAC as a non-hazardous waste

Figure 7-1. Mid Cost Results for Removal of PFAS from Groundwater Using Pressure GAC (2022 dollars)



Note: costs shown assume bed life of 50,000 BV and off-site reactivation of spent GAC as a non-hazardous waste

Figure 7-2. Mid Cost Results for Removal of PFAS from Surface Water Using Gravity GAC (2022 dollars)

7.3 Costs for IX

7.3.1 Model Components and Assumptions

USEPA (2024d) provides a complete description of the engineering design process used by the WBS model for PFAS-selective IX. Table 7-3 shows the technology-specific capital equipment and O&M requirements included in the model. These items are in addition to the common WBS cost elements listed in Table 7-1.

Table 7-3. Technology-Specific Cost Elements Included in the PFAS-selective IX Model

Cost Category	Major Components Included
Direct Capital Costs	<ul style="list-style-type: none"> • Pre-treatment cartridge filters • Pressure vessels that contain the resin bed • Tanks and pumps for initial rinse and (optionally) backwash of the resin bed • Tanks (with secondary containment), pumps and mixers for delivering sodium hydroxide for use in post-treatment corrosion control (optional) • Associated piping, valves, and instrumentation
O&M Costs: Labor	<ul style="list-style-type: none"> • Operator labor for pre-treatment filters • Operator labor for managing backwash/rinse events • Operator labor for backwash pump maintenance (only if backwash occurs weekly or more frequently) • Operator labor for resin replacement
O&M Costs: Materials	<ul style="list-style-type: none"> • Replacement cartridges for pre-treatment filters • Materials for backwash pump maintenance (only if backwash occurs weekly or more frequently) • Chemical usage (if post-treatment corrosion control is selected) • Replacement virgin PFAS-selective resin
O&M Costs: Energy	<ul style="list-style-type: none"> • Operating energy for backwash/rinse pumps
O&M Costs: Residuals	<ul style="list-style-type: none"> • Disposal of spent cartridge filters • Discharge fees for spent backwash/rinse • Disposal of spent resin

For small systems (less than 1 MGD), the PFAS-selective IX model assumes the use of package treatment systems that are pre-assembled in a factory, mounted on a skid, and transported to the site. The model estimates costs for package systems by costing all individual equipment line items (e.g., vessels, interconnecting piping and valves, instrumentation, and system controls) in the same manner as custom-engineered systems. This approach is based on vendor practices of partially engineering these types of package plants for specific systems (e.g., selecting vessel size to meet flow and treatment criteria). The model applies a variant set of design inputs and assumptions that are intended to simulate the use of a package plant and that reduce the size and cost of the treatment system. USEPA (2024d) provides complete details on the variant design assumptions used for package plants.

The paragraphs below describe the specific inputs and assumptions that EPA used to generate the costs in Section 7.3.2. Other inputs and assumptions not discussed below (e.g., number of booster pumps, treated water corrosion control, bed expansion) remained as described in USEPA (2024d).

7.3.1.1 EBCT and Vessel Configuration

The estimates below and in Appendix A assume two vessels in series with a minimum total EBCT of 6 minutes (i.e., 3 minutes per vessel). The use of two vessels in series is consistent with full-scale practice and design engineer and IX vendor recommendations for PFAS removal as discussed in Section 3.6.2. The total EBCT is at the upper bound of the recommended range discussed in Section 3.6.1 and, therefore, errs on the side of higher cost. It also results in an EBCT per vessel roughly consistent with the data used to derive the bed life equations (3.3 minutes).

7.3.1.2 *Bed Life*

As discussed in Sections 3.2.2 and 3.6.3, IX bed life depends on factors including target removal efficiency, influent water quality, and the specific PFAS compound(s) targeted. To accommodate variations in these factors, EPA generated separate cost equations at 20,000 BV increments for bed lives ranging from 20,000 to 260,000 BV. Each 20,000 BV increment corresponds to a 3- to 4-month shift in changeout frequency, depending on system size. To estimate national costs, EPA selected from among these cost equations using the bed life equations described in Section 2.6.3. EPA rounded results from the bed life equations down to the nearest 20,000 BV, which errs on the side of higher costs.

The bed life equations are based on data representative of a single vessel with an EBCT of 3.3 minutes. As discussed in Section 7.3.1.1, the estimates below assume two vessel in series, each with an EBCT of 3 minutes. The use of vessels in series should result in a longer bed life than estimated for a single, 3.3-minute EBCT vessel (see Section 3.6.2). EPA did not adjust the bed life results to account for the more efficient vessel configuration. Not incorporating an adjustment for configuration errs on the side of higher costs and is intended to compensate for the fact that the bed life equations are based on RSSCT data, which might overestimate full-scale bed life (see Section 3.6.3). Note that EPA does not have data on the degree to which RSSCTs might overestimate bed life or to quantify the bed life extension resulting from vessel configuration. Therefore, the net result of this compensating adjustment is uncertain.

7.3.1.3 *Residuals Management*

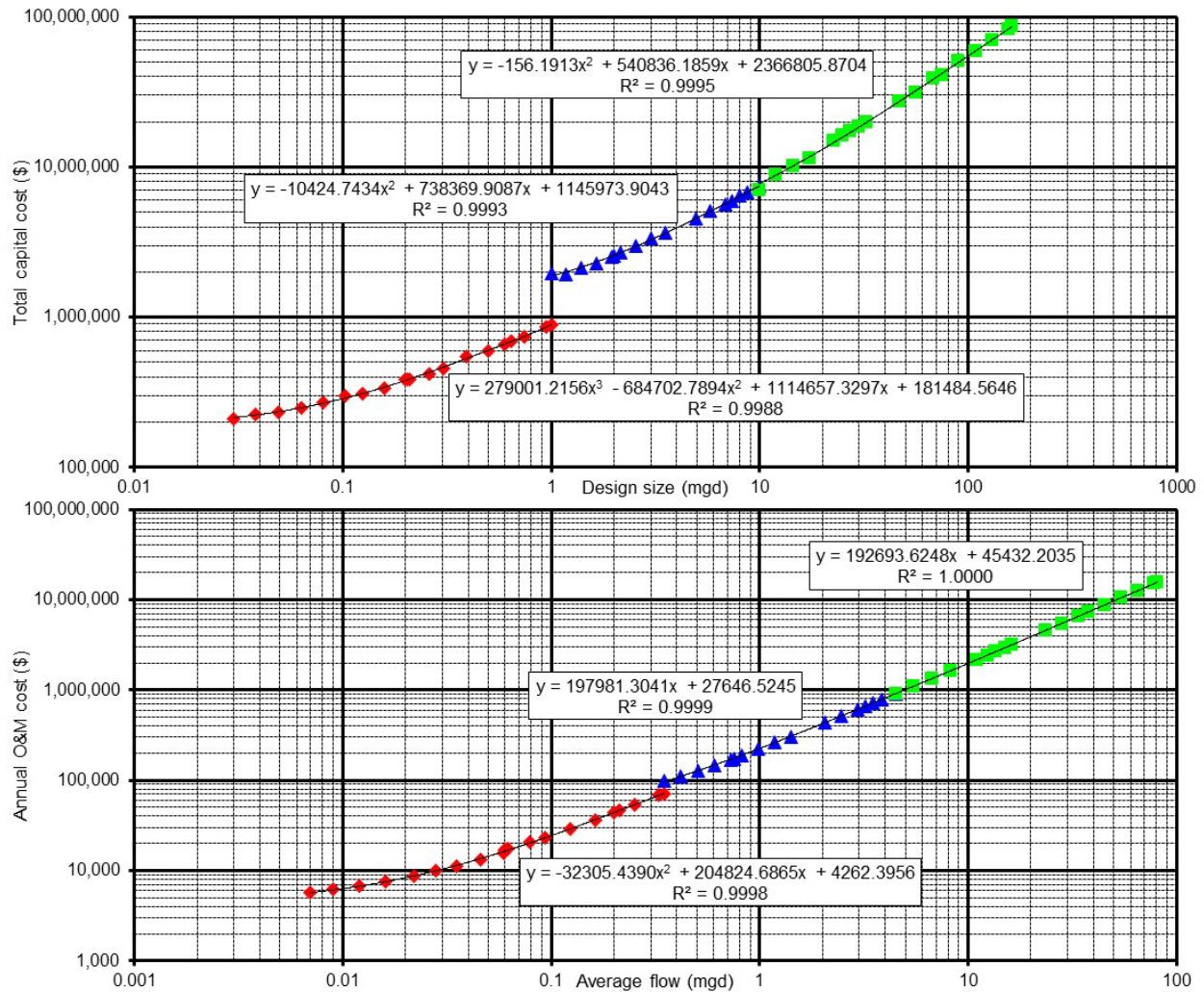
EPA generated separate cost equations for two spent resin management scenarios:

- Spent resin managed as non-hazardous and sent off-site for incineration
- Spent resin managed as hazardous and sent off-site for incineration.

In both cases, the spent resin is replaced with virgin resin. The first scenario reflects typical management practices under current regulations. The second scenario provides an upper bound on other options that might emerge under future air quality regulations (e.g., off-site disposal in a non-hazardous waste landfill) or RCRA hazardous waste regulations (e.g., off-site disposal in a hazardous waste landfill).

7.3.2 *Cost Estimates*

The graphs below (Figure 7-4) plot WBS cost model results in 2022 dollars at the mid cost level for removal of PFAS from groundwater using PFAS-selective IX, assuming a bed life of 160,000 BV. In the exhibit, note that costs increase at 1 MGD design flow (0.355 MGD average flow) because of the transition from package systems (used by small systems) to custom-engineered systems (used by large systems). Appendix A provides complete cost equations for across the range of bed life and residuals management scenarios, including the high, mid, and low-cost levels and for treatment of groundwater and surface water. Appendix B presents example WBS model outputs at selected flow rates, allowing review of individual cost line items.



Note: costs shown assume bed life of 120,000 BV and incineration of spent resin as a non-hazardous waste

Figure 7-3. Mid Cost Results for Removal of PFAS from Groundwater Using IX (2022 dollars)

7.4 Costs for RO/NF

7.4.1 Model Components and Assumptions

USEPA (2024c) provides a complete description of the engineering design process used by the WBS model for RO/NF. Table 7-4 shows the technology-specific capital equipment and O&M requirements included in the model. These items are in addition to the common WBS cost elements listed in Table 7-1.

Table 7-4. Technology-Specific Cost Elements Included in the RO/NF Model

Cost Category	Major Components Included
Direct Capital Costs	<ul style="list-style-type: none"> • High-pressure pumps for influent water and (optionally) interstage pressure boost • Pre-treatment cartridge filters • Tanks, pumps, and mixers for pretreatment chemicals • Pressure vessels, membrane elements, piping, connectors, and steel structure for the membrane racks • Valves for concentrate control and (optionally) per-stage throttle • Tanks, pumps, screens, cartridge filters, and heaters for membrane cleaning • Equipment, including dedicated concentrate discharge piping, for managing RO concentrate and spent cleaning chemicals • Associated pipes, valves, and instrumentation
O&M Costs: Labor	<ul style="list-style-type: none"> • Operator labor for pre-treatment filters • Operator labor for routine O&M of membrane units • Operator labor to maintain membrane cleaning equipment
O&M Costs: Materials	<ul style="list-style-type: none"> • Replacement cartridges for pre-treatment filters • Chemical usage for pretreatment • Maintenance materials for pre-treatment, membrane process, and cleaning equipment • Replacement membrane elements • Chemical usage for cleaning
O&M Costs: Energy	<ul style="list-style-type: none"> • Energy for high-pressure pumping
O&M Costs: Residuals	<ul style="list-style-type: none"> • Disposal costs for spent cartridge filters and membrane elements • Concentrate discharge fees*

* Not applicable under the residuals management used in the estimates below (direct discharge to a non-potable water body).

The paragraphs below describe specific inputs and assumptions that EPA used to generate the costs in Section 7.4.2. Other inputs and assumptions not discussed below (e.g., cleaning interval, permeate throttling and interstage boost, membrane life) were as described in USEPA (2024c).

7.4.1.1 Water Type

The WBS model for RO/NF includes three default groundwaters and three default surface waters, ranging from high to low quality (i.e., from low to high total dissolved solids and scaling potential). The default water parameters are based on a survey of membrane feed water characteristics in the literature. The cost estimates below and in Appendix A are intended to reflect the incremental cost of removing PFAS from otherwise potable water using RO/NF. Therefore, the estimates use the default high quality water parameters built in to the WBS model. Total dissolved solids for the high-quality surface water is approximately 360 mg/L; for high-quality groundwater, total dissolved solids is approximately 500 mg/L. USEPA (2024c) documents the other relevant characteristics of these default waters.

7.4.1.2 Membrane Type

The WBS model includes the option of NF, low-pressure RO, or brackish water RO membrane elements, with a diameter of 4 inches, 8 inches, or 16 to 18 inches.¹⁶ As discussed in Section 4.6.1, both low MWCO (or “tight”) NF membranes and low-pressure (or “loose”) RO membranes are effective for PFAS removal. Therefore, EPA used the WBS model to compare

¹⁶ Not all manufacturers use the same size for their largest diameter elements, but the model is independent of the exact diameter.

costs using NF membranes to those using low-pressure (or “loose”) RO membranes, holding the other inputs and assumptions documented here constant. The difference in annualized cost between the two membrane types varied by system size, component level, and water source (groundwater versus surface water), but was at most 10 percent. For simplicity, given the small difference in cost, the cost estimates below and in Appendix A assume use of low-pressure (or “loose”) RO membrane elements. This assumption tends to err on the side of higher cost, because RO was more frequently (although not always) the more expensive option in EPA’s comparisons. This assumption is also consistent with the types of membrane elements used at the two full-scale membrane facilities designed for PFAS removal (see Section 4.6.1). For very small systems, the cost estimates use 4-inch diameter elements; for larger systems, the estimates use 8-inch elements. The switch from 4-inch to 8-inch elements takes place at a flow rate of about 75,000 gallons per day.

7.4.1.3 Flux Rate

The flux rate, in combination with the system design flow, determines the total membrane area in the system, and therefore the total number of membrane elements to be used. Flux rates are based on the recommendations of various manufacturers for waters of different challenge. For groundwater, the cost estimates below and in Appendix A use a flux rate of 19 gfd. For surface water, the rates are 15 to 16 gfd. These flux rates fall within the range reported in the literature for PFAS removal (see Section 4.6.3).

7.4.1.4 Target Recovery Rate

For systems larger than approximately 0.5 MGD, the cost estimates below and in Appendix A use target recovery rates of 80 percent for groundwater and 85 percent for surface water.¹⁷ These recovery rates fall within the range reported in the literature for PFAS removal (see Section 4.6.3). At small flows, the minimum size of membrane elements limits flexibility in the system design; therefore, estimates up to about 500,000 gallons per day may use recovery rates as low as 70 to 75 percent.

7.4.1.5 Residuals Management

The cost estimates below and in Appendix A assume direct discharge of concentrate to a permitted outfall on a non-potable water body (e.g., ocean or brackish estuary) via 10,000 feet of buried dedicated piping. As discussed in Section 4.5, this assumption is consistent with the management practice planned at the full-scale membrane facility in North Carolina designed for PFAS removal. It is also the most common management practice for RO/NF facilities in general. Since spent cleaning solution is generated infrequently and in small amounts, the estimates here assume that it will be diluted and discharged with membrane concentrate.

7.4.2 Cost Estimates

The graphs below (Figure 7-4) plot WBS cost model results in 2022 dollars at the mid cost level for removal of PFAS from groundwater using RO. Because RO/NF can continuously achieve high removal efficiencies for PFAS, systems that require lower removals may be able to treat a portion of their total flow and blend treated water and untreated water to meet a regulatory

¹⁷ Note that recovery rate is the percent of influent flow that is recovered as useable treated water (permeate), as opposed to lost as residual concentrate. It is not directly related to percent removal of PFAS

standard. When blending is possible, it will reduce treatment costs and potential post-treatment requirements (see Section 4.4). EPA assumes systems using RO/NF will employ blending when they require less than 95 percent removal. Because RO/NF can achieve greater than 95 percent removal efficiency for most PFAS compounds (see Section 4.2.1), this assumption errs on the side of higher costs. The flow rates shown on the x-axes in Figure 7-4 and as the independent variables in the equations below and in Appendix A are treatment process flows. To account for blending in the cost estimates, these treatment process flows should be calculated from entry point flows by incorporating a blending ratio as follows:

$$B = \frac{\%R_{required}}{0.95}$$

$$Q_{treated,design} = B \times Q_{total,design}$$

$$Q_{treated,average} = B \times Q_{total,design}$$

Where:

- B = the blending ratio expressed as a decimal
- %R_{required} = removal required to meet regulatory standard, expressed as a decimal
- 0.95 = assumption about the continuous removal achieved by RO/NF (see above)
- Q_{treated} = treated portion of entry point flow in MGD
- Q_{total} = total entry point flow in MGD

Appendix A provides complete cost equations for the high, mid, and low-cost levels and for treatment of groundwater and surface water. Appendix B presents example WBS model outputs at selected flow rates, allowing review of individual cost line items.

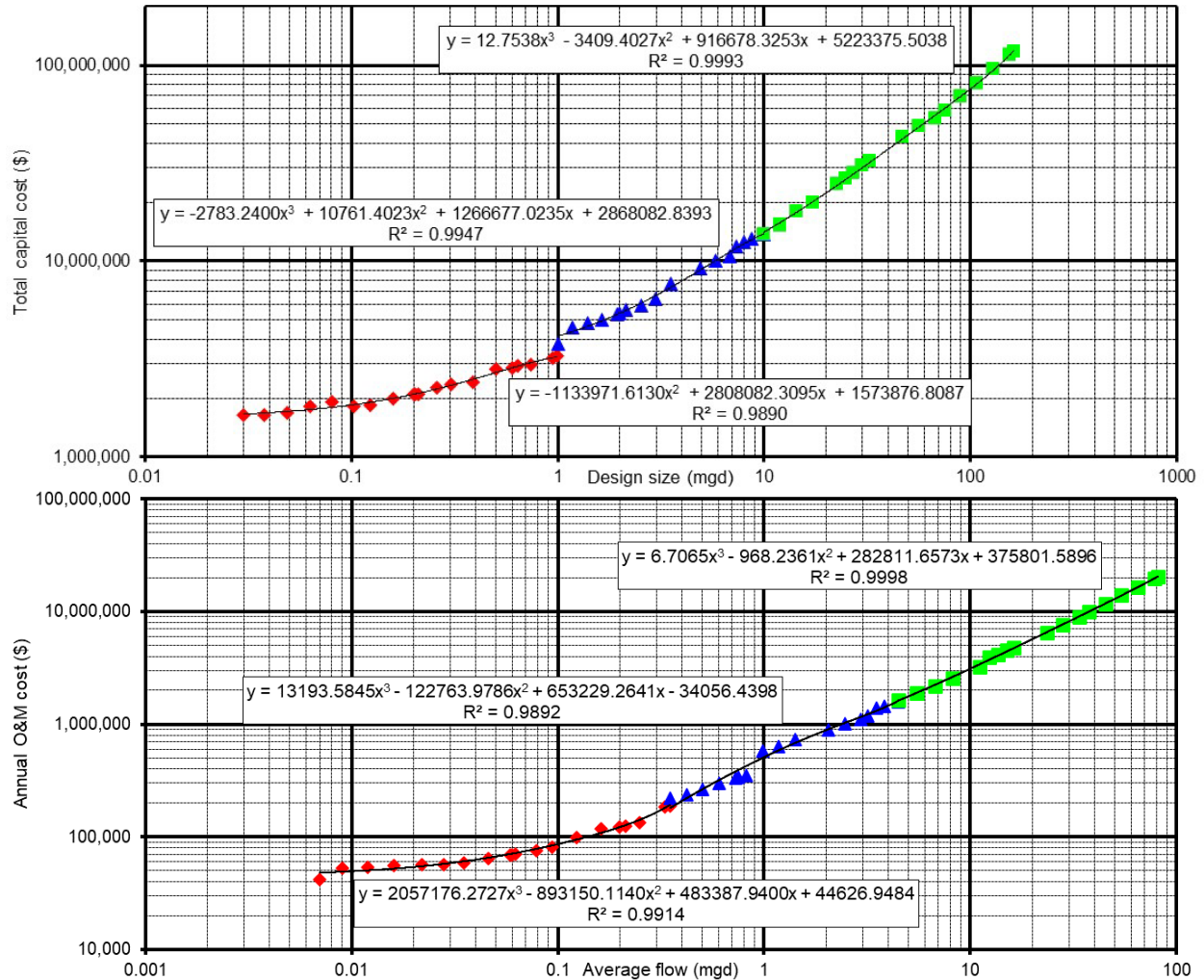


Figure 7-4. Mid Cost Results for Removal of PFAS from Groundwater Using Reverse Osmosis (2022 dollars)

7.5 Costs for POU Treatment

7.5.1 Model Components and Assumptions

The document *Cost Evaluation of Point-of-Use and Point-of-Entry Treatment Units for Small Systems: Cost Estimating Tool and User Guide* (USEPA, 2023) provides a complete description of the WBS model for POU/POE technologies. The POU/POE model is capable of estimating equipment costs for a variety of POU/POE devices. To use the POU/POE model in estimating costs for PFAS, EPA selected a program using POU RO devices. EPA assumed the use of POU, as opposed to POE, devices because ingestion is the primary route of concern for exposure to PFAS. In addition to the costs of the POU RO devices and replacement filters, the WBS model also includes the cost of the following other components of a complete POU program:

- POU RO device installation

- Public education program development
- POU device monitoring
- POU device maintenance.

Because only small systems would be expected to use POU programs, the model does not cover systems serving greater than 3,300 people (greater than 1 MGD design flow). Also, the model does not include assumptions or materials of construction that vary based on a “component level” or “cost level” input. Therefore, unlike the other models, it does not generate separate estimates for low-, mid-, and high-cost scenarios.

To use the model for PFAS removal, EPA collected cost data for POU RO devices certified for PFOA and PFOS removal under the current standard. EPA also updated all other unit costs (e.g., analytical costs, labor rates, printed material costs). Table 7-5 identifies the values used for parameters other than unit costs that drive the costs of a POU RO program. EPA developed these assumptions based on EPA guidance (USEPA, 2006) and case study data, as discussed in detail in the paragraphs below.

Table 7-5. POU Model Assumptions for PFAS Removal

Parameter Category	Value
Installation labor time	<ul style="list-style-type: none"> • Plumber installation time: 2 hours per POU device (NSF International, 2005) • Scheduling time: 0.5 hours per household (USEPA, 2006)
Public education program	<ul style="list-style-type: none"> • Public meeting-related time: 20 hours • Other outreach time (e.g., program updates in a billing mailer): 4 hours
Monitoring requirements	<ul style="list-style-type: none"> • Initial monitoring for all units; annual monitoring for 1/3 of units (USEPA, 2006) • Sampling time: 0.25 hours per sampling event (NSF International, 2005)
Filter replacement	<ul style="list-style-type: none"> • Replacement schedule: RO element (3 years); post-RO carbon filter (1 year); pre-RO filters (9 months) (manufacturer recommendations) • Filter replacement time: 0.5 hour per change-out (NSF International, 2005) • Scheduling time: 0.5 hours per household (USEPA, 2006)

7.5.1.1 POU RO Device Installation

Installation of the POU RO devices will be the responsibility of the water system. The utility can, however, hire a licensed plumber or representative of the product manufacturer to install the devices. Based on the variety of plumbing issues encountered among older housing units in a rural community, NSF International (2005) recommends using an experienced plumber to perform the installations.

The POU model contains a default estimate of two hours per household to install the POU RO. A variety of factors such as existing plumbing conditions and travel distance will affect installation times across sites. The estimate is consistent with case study data. In a Grimes, California, arsenic demonstration program (NSF International, 2005), POU adsorptive filter installation times ranged from 15 minutes to 3 hours depending on the accessibility of piping and the need for additional lines (e.g., to provide treated water to ice-makers). The mean device installation time was one hour, but total plumber billing records indicated that twice as much time was spent on all installation-related activities (e.g., additional time to obtain special plumbing fittings and return visits to homes when residents missed their appointments).

Installation costs also include administrative time for system staff to contact homeowners to schedule an installation appointment. EPA assumed an average of 30 minutes (0.5 hours) per household to schedule an appointment. Scheduling effort is likely to vary across customers, with some being relatively easy to schedule while others may require multiple calls to identify and contact the correct homeowners or to handle situations such as homeowner reluctance to participate or language barriers (USEPA, 2006).

7.5.1.2 Public Education Program

EPA guidance (2006) recommends that systems implement a public education program to obtain and maintain customer participation and long-term customer satisfaction with the POU program. The two main program elements recommended in USEPA (2006) are: public meetings prior to installing any POU devices to educate customers about the regulatory compliance requirements and the role of the POU devices; and POU program updates in billing mailers and on information flyers posted in public locations such as a post office, a public library, or a website. The POU model includes labor costs for the following program elements:

- preparing information for one public meeting
- attending the meeting
- preparing an additional billing mailer with program updates.

Public education program costs are not available from POU case studies. USEPA (2023) provides a detailed breakdown of the assumptions used to generate the time estimates shown in Table 7-5. It also describes the costs for materials such as information flyers for the public meeting, meeting announcements, and billing mailers.

7.5.1.3 POU Device Monitoring

A system that implements a POU compliance strategy will need to monitor the quality of water produced by the treatment devices to demonstrate compliance with a PFAS standard. The system will need to work with the appropriate regulatory agency to establish an approved compliance-monitoring schedule (USEPA, 2006). The resulting monitoring schedule may have sampling rates in initial year that differ from sampling rates in subsequent years. EPA Guidance (2006) provides an example of a monitoring schedule in which samples are taken from every unit during the first year to confirm that the units are working properly, and then monitoring frequency declines to one-third of units each subsequent year. EPA's cost estimates incorporate these monitoring frequencies.

Monitoring costs include sampling time, shipping fees, and laboratory analysis fees. The average sampling is 15 minutes (0.25 hours). To minimize the burden on households as well as system resources, EPA assumes that sampling occurs during installation or maintenance trips. The assumption is consistent with the Grimes case study cost analysis (NSF International, 2005) used an estimate of 15 minutes per sampling event.

7.5.1.4 POU Device Maintenance

Maintenance for the POU RO device primarily includes replacing the four filters: RO membrane, two carbon filters, and the sediment filter. Replacement schedules reflect average useful lives based on vendor recommendations. On average, the RO membrane is replaced once every three

years based on average replacement schedules across vendors, and the other filter cartridges are changed once per year.

In addition to replacement filter costs, maintenance costs include scheduling time and time to change filters. The Grimes case study cost analysis (NSF International, 2005) used an estimate of 15 minutes per filter change out. EPA assumed the average length of a maintenance call 30 minutes (0.5 hours) because the most frequent type of visit involves changing two filters. EPA used the same 30-minute scheduling time assumption that it used for initial installation.

7.5.2 *Cost Estimates*

POU RO is not currently a compliance option because the regulatory options under consideration require treatment to concentrations below 70 ng/L total of PFOA and PFOS, the current certification standard for POU devices. However, POU treatment might become a compliance option for small systems in the future if NSF/ANSI develops a new certification standard that mirrors or is more stringent than EPA's proposed regulatory standard. The cost estimates presented here for POU RO reflect the costs of devices certified under the current testing standard, which might differ from the costs of devices certified under a future standard. Therefore, the POU RO costs should be considered preliminary estimates. Additionally, EPA notes that it did not develop estimates for POU GAC devices; however, these may also potentially be a future compliance option if they are certified to the new testing standard.

Figure 7-5 plots WBS cost model results in 2022 dollars for removal of PFAS from groundwater using POU treatment. EPA limits the POU model to a maximum of approximately 1,000 households served because implementing and maintaining a POU program for a greater number of households is likely to be impractical. Therefore, the graphs do not extend beyond a maximum of 1 MGD design flow, which corresponds to this limit on the number of households. As discussed above, the POU model also does not generate separate high, mid, and low-cost estimates. Appendix A contains complete cost equations for POU treatment, including for groundwater and surface water. Appendix B presents example WBS model outputs for selected flow rates, allowing review of individual cost line items.

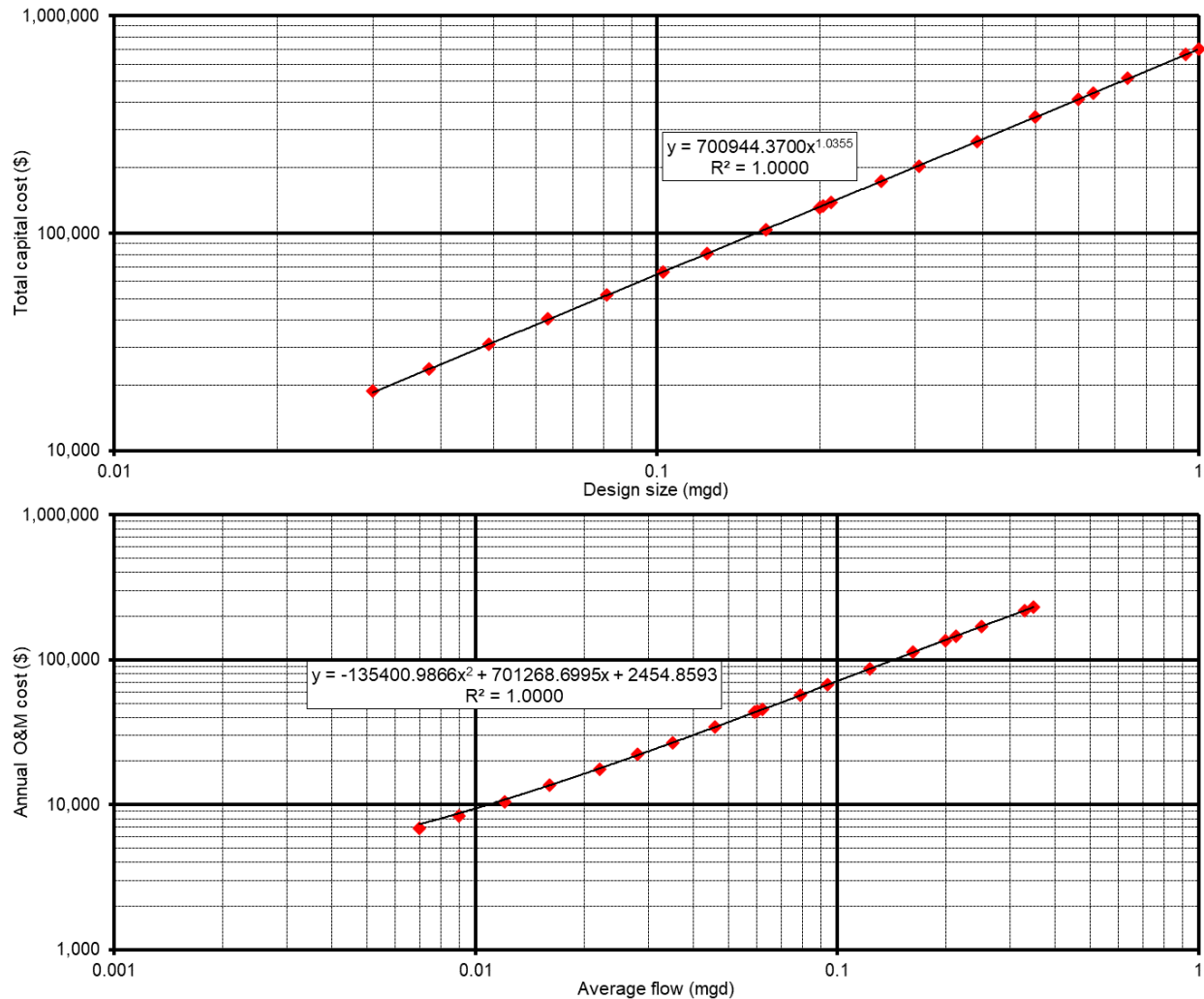


Figure 7-5. Cost Results for POU RO Removal of PFAS from Groundwater (2022 dollars)

7.6 Costs for Nontreatment Options

7.6.1 Model Components

USEPA (2024b) provides a complete description of the engineering design process used by the WBS model for nontreatment actions. The model can estimate costs for two nontreatment alternatives: interconnection with another system and drilling new wells to replace a contaminated source. Table 7-6 shows the technology-specific capital equipment and O&M requirements included in the model for each alternative. The interconnection alternative does not include any buildings. It includes all the indirect capital costs shown in Table 7-1 except for yard piping, site work, and architectural fees. The new well alternative includes a small shed or other low-cost building at the well site along with materials and labor for maintenance of this building. It includes all the indirect capital costs shown in Table 7-1 except for yard piping

Table 7-6. Technology-Specific Cost Elements Included in the Non-treatment Model

Cost Category	Major Components Included for Interconnection	Major Components Included for New Wells
Direct Capital Costs	<ul style="list-style-type: none"> Booster pumps or pressure reducing valves (depending on pressure at supply source) Concrete vaults (buried) for booster pumps or pressure reducing valves Interconnecting piping (buried) and valves 	<ul style="list-style-type: none"> Well casing, screens, and plugs Well installation costs including drilling, development, gravel pack, and surface seals Well pumps Piping (buried) and valves to connect the new well to the system
O&M Costs: Labor	<ul style="list-style-type: none"> Operator labor for O&M of booster pumps or pressure reducing valves (depending on pressure at supply source) and interconnecting valves 	<ul style="list-style-type: none"> Operator labor for operating and maintaining well pumps and valves
O&M Costs: Materials	<ul style="list-style-type: none"> Cost of purchased water Materials for maintaining booster pumps (if required by pressure at supply source) 	<ul style="list-style-type: none"> Materials for maintaining well pumps
O&M Costs: Energy	<ul style="list-style-type: none"> Energy for operating booster pumps (if required by pressure at supply source) 	<ul style="list-style-type: none"> Energy for operating well pumps

Nontreatment options are less likely to be available for larger systems because of the large water quantities required. Therefore, EPA’s WBS nontreatment cost model generates costs only for systems serving less than 10,000 people. As discussed in Section 6.1, the two options covered by the WBS nontreatment model (new wells or interconnection) are likely to have higher costs than other nontreatment options available for PFAS. The sections below describe the specific inputs and assumptions that EPA used to generate the costs for each option in Section 7.6.4. For both options, the cost estimates assume that systems choosing a nontreatment option do so because they have an alternative source that will not require additional water treatment to address changes in raw water quality (i.e., no post-treatment). Because of this, they further assume no incremental waste or residuals management costs.

7.6.2 Assumptions for New Wells

The sections below describe specific inputs and assumptions used to generate costs under the new well nontreatment option. Other inputs and assumptions not discussed below (e.g., pump type, gravel pack and grout requirement, screen and casing length ratios, well pressure and footprint) were as described in USEPA (2024b).

7.6.2.1 Total Flow Rate Requirements and Flow per Well

As with other WBS models, design and average flow are inputs to the nontreatment model. In the case of nontreatment approaches, however, “design” flow is the peak flow required by the system, rather than the design capacity of a treatment plant. In the new well nontreatment option, the flow rate requirements determine the number of new wells required. The cost estimates below and in Appendix A assume a maximum well capacity of 500 gallons per minute (gpm), such that one new well is installed per 500 gpm of water production capacity required.

7.6.2.2 Well Depth

Well depth will vary for each site depending on the geological formations and aquifer depths. Geophysical studies prior to well installation will provide guidance on optimum well depths. The WBS model has cost data for pumps to serve wells up to 1,350 feet in depth. The cost estimates below and in Appendix A assume a 250-foot well depth.

7.6.2.3 Distance from Well to Distribution System

The distance between a new well and the distribution system affects pipe installation costs. Distance will vary depending on distribution system geography relative to the extent of aquifer contamination. The cost estimates below and in Appendix A assume a distance of 500 feet.

7.6.3 Assumptions for Interconnection

The sections below describe specific inputs and assumptions used to generate costs under the interconnection nontreatment option. Other inputs and assumptions not discussed below (e.g., trench dimensions, concrete thickness) were as described in USEPA (2024b).

7.6.3.1 Flow Rate Requirements

As with other WBS models, design and average flow are inputs to the nontreatment model. In the case of nontreatment approaches, however, “design” flow is the peak flow required by the system, rather than the design capacity of a treatment plant. In the interconnection nontreatment option, the flow rate requirements determine a number of system and equipment parameters, including pipeline and valve size and pump capacity and energy use (if required by pressure at the supply source).

7.6.3.2 Distance to Interconnection Water Supply

For utilities able to purchase water from a neighboring system, the capital cost of the interconnection project will depend on the distance between the two systems. If the systems are far apart geographically, the cost of installing a pipeline may be too high to make an interconnection project feasible. Also, a larger booster pump will be required to overcome friction losses along longer pipelines. The cost estimates below and in Appendix A assume an average interconnection distance of 10,000 feet, based on comments from the peer review of the nontreatment model.

7.6.3.3 Pressure at Supply Water Source

The water pressure of purchased water may require adjustment prior to entering the purchasing system’s distribution network (e.g., to account for elevation differences). If the wholesale supplier does not have enough pressure to meet the distribution needs of the interconnection project, then booster pumps are needed to move water from the supply source into the distribution system. The booster pump size is based on flow rate as well as distance and grade to the distribution system. If the supply source has more pressure than necessary, then pressure reducing valves are needed. The cost estimates below and in Appendix A assume that differences in pressure between the supplier and the purchasing system are minimal, but that booster pumps are still needed to overcome friction loss in the interconnecting piping between the two systems.

7.6.3.4 Cost of Purchased Water

An interconnection project will include one or more water rates paid to the wholesale system by the purchasing system. The model assumption is a single water rate for the average cost in dollars per thousand gallons of purchased water. The cost estimates below and in Appendix A assume a higher cost of purchased water of \$3.17 per thousand gallons, based on recent data from wholesaling and purchasing systems that published their agreed rates online.

7.6.4 Cost Estimates

The graphs below plot WBS cost model results in 2022 dollars at the mid cost level for the two nontreatment options for systems using groundwater: new wells (Figure 7-6) and interconnection (Figure 7-7). The graphs do not extend beyond 3.536 MGD design flow, because the nontreatment model does not generate costs for larger systems. Appendix A provides complete cost equations for both nontreatment options, including the high, mid, and low-cost levels and for interconnection of groundwater and surface water systems. Appendix B presents example WBS model outputs for selected flow rates, allowing review of individual cost line items.

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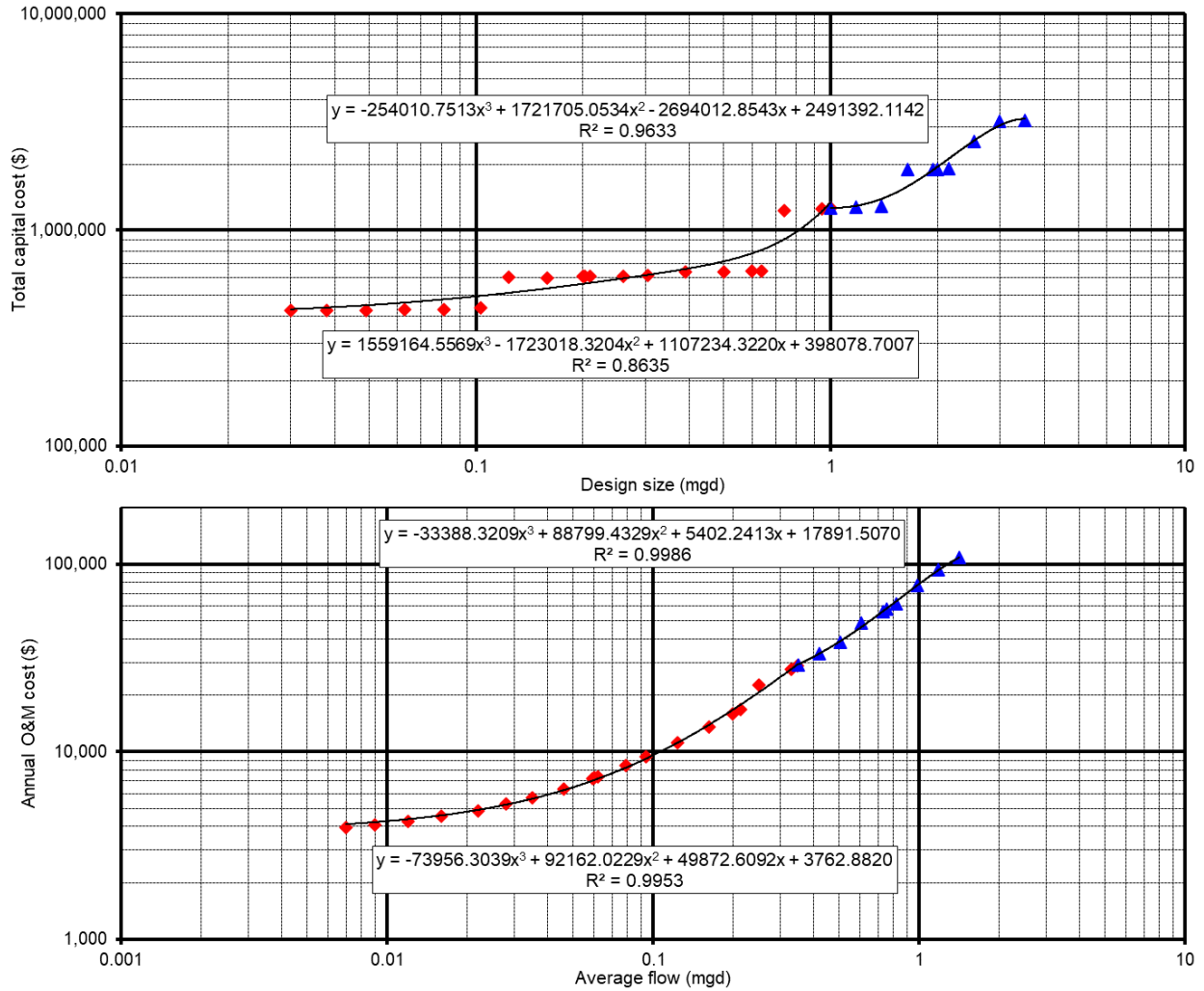


Figure 7-6. Mid Cost Results for PFAS Compliance Using New Wells at Groundwater Systems (2022 dollars)

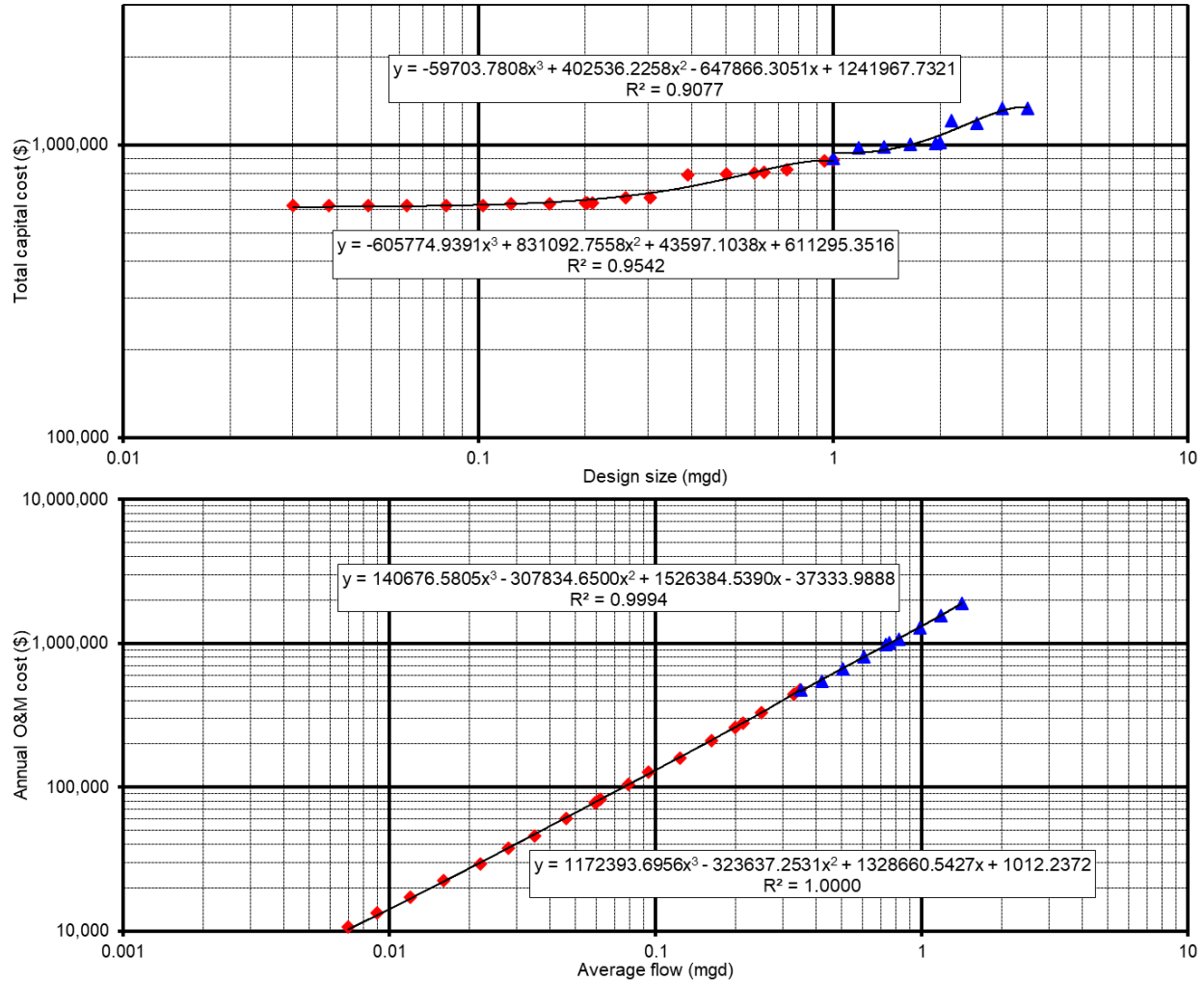


Figure 7-7. Mid Cost Results for PFAS Compliance Using Interconnection at Groundwater Systems (2022 dollars)

7.7 References

Brady, R. and Moran, M. 2012. Activated Carbon Adsorption. In Randtke, S.J. and Horsley, M.B. (Eds.), *Water Treatment Plant Design, Fifth Edition* (pp. 16.1-16.45). American Water Works Association/American Society of Civil Engineers.

NSF International. 2005. *Feasibility of Economically Sustainable Point-of-Use/Point-of-Entry Decentralized Public Water System*. Ann Arbor, MI: NSF International.

Summers, R.S., Knappe, D.R.U., and Snoeyink, V.L. 2011. Adsorption of Organic Compounds by Activated Carbon. In Edzwald, J.K. (Ed.), *Water Quality & Treatment: A Handbook on Drinking Water, Sixth Edition* (pp. 14.1-14.105). American Water Works Association.

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USEPA. 1997. *Discussion Summary: EPA Technology Design Workshop*. Washington, D.C.: USEPA, Office of Groundwater and Drinking Water.

USEPA. 2006. *Point-of-Use or Point-of-Entry Treatment Options for Small Drinking Water Systems*. Office of Ground Water and Drinking Water. EPA-815-R-06-010.

USEPA. 2023. *Cost Evaluation of Point-of-Use and Point-of-Entry Treatment Units for Small Systems: Cost Estimating Tool and User Guide*. Office of Water.

USEPA. 2024a. *Work Breakdown Structure-Based Cost Model for Granular Activated Carbon Drinking Water Treatment*. Office of Water.

USEPA. 2024b. *Work Breakdown Structure-Based Cost Model for Nontreatment Options for Drinking Water Compliance*. Office of Water.

USEPA. 2024c. *Work Breakdown Structure-Based Cost Model for Reverse Osmosis/Nanofiltration Drinking Water Treatment*. Office of Water.

USEPA. 2024d. *Work Breakdown Structure-Based Cost Model for Ion Exchange Treatment of Per- and Polyfluoroalkyl Substances (PFAS) in Drinking Water*. Forthcoming.

Appendix A. Cost Equations

Notes:

- Cost equations presented here take one of the following forms, identified by which coefficients (C1 through C10) are nonzero:

$$Cost = C1 Q^{C2}$$

or $Cost = C3 Ln(Q) + C4$

or $Cost = C5 e^{(C6 Q)}$

or $Cost = C7 Q^3 + C8 Q^2 + C9 Q + C10$

where Q is design flow in MGD for total capital costs, or average flow in MGD for annual O&M costs. Resulting costs are in 2022 dollars.

- Equations are designated as for small, medium, or large systems. These equations apply as follows:
 - Small system equations apply where design flow (Q) is less than 1 MGD
 - Medium system equations apply where design flow (Q) is 1 MGD or greater, but less than 10 MGD
 - Large system equations apply where design flow (Q) is 10 MGD or greater, but less than 162 MGD

Note: although the independent variable Q in the O&M equations is average flow, selection between O&M equations for small, medium, and large systems is made based on design flow.

- EPA developed each equation using the method described in Section 7.1.
- For GAC, equations are not presented for gravity designs for groundwater systems, because groundwater systems are unlikely to use this design type.
- For POU RO, costs do not vary by component level input (high, mid, low); equations are not presented for medium and large systems.
- For Nontreatment, medium system size curves are valid only up to 3.536 MGD design flow (1.417 MGD groundwater average flow and 1.345 MGD surface water average flow); equations are not presented for systems of greater size.

A.1 Capital and Annual O&M Cost Equation Parameters for GAC

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	Low	Pressure	5000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	5000	non-haz	Total Capital	34.018	0	0	0	0	0	0	-2486.3578	27414.1362	747627.6848	1517889.733
GW	Large	Low	Pressure	5000	non-haz	Total Capital	35.758	0	0	0	0	0	0	8.4254	-429.7729	541257.9754	3500298.704
GW	Small	Mid	Pressure	5000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	5000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	5000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1721	-239.2412	605710.8055	4654699.52
GW	Small	High	Pressure	5000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	5000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	5000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0331	-691.4953	859964.47	6895608.343
GW	Small	Low	Pressure	10000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	10000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	10000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.466	-440.2387	541837.5065	3493395.48
GW	Small	Mid	Pressure	10000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	10000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	10000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.2128	-249.7072	606290.3518	4647796.121
GW	Small	High	Pressure	10000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	10000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	10000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0727	-701.7678	860535.54	6888790.727
GW	Small	Low	Pressure	15000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	15000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	15000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	15000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	15000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	15000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815
GW	Small	High	Pressure	15000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	15000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	15000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	20000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	20000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	20000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	20000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	20000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	20000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815
GW	Small	High	Pressure	20000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	20000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	20000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	25000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	25000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	25000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	25000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	25000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	25000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815

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Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	25000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	25000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	25000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	5000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	3501541.999	-2165452.331	877869.7948	3263.1157
GW	Medium	Low	Pressure	5000	non-haz	Annual O&M	34.018	0	0	0	0	0	0	3250.4356	-23665.12	561526.7756	43752.593
GW	Large	Low	Pressure	5000	non-haz	Annual O&M	35.758	0	0	0	0	0	0	0	252.5515	486878.1261	218860.293
GW	Small	Mid	Pressure	5000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	3113884.66	-1945691.778	853757.4075	3978.2238
GW	Medium	Mid	Pressure	5000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3424.1855	-24777.0461	565525.6523	46646.6871
GW	Large	Mid	Pressure	5000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	263.1991	486763.8627	220014.9753
GW	Small	High	Pressure	5000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	3284292.916	-2055922.467	881706.9102	4989.1575
GW	Medium	High	Pressure	5000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	0	-2327.4254	531454.5345	68105.0319
GW	Large	High	Pressure	5000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	331.5468	487871.3966	243989.805
GW	Small	Low	Pressure	10000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1163798.788	-956594.5385	521753.5662	3212.0126
GW	Medium	Low	Pressure	10000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	0	969.2297	285541.4468	67721.8084
GW	Large	Low	Pressure	10000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	239.8974	263461.4869	215052.1595
GW	Small	Mid	Pressure	10000	non-haz	Annual O&M	21.815	272277.1609	0.7634	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	10000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	2222.7632	-14796.6698	318314.1199	57626.1513
GW	Large	Mid	Pressure	10000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	251.2656	263284.0211	216656.4233
GW	Small	High	Pressure	10000	non-haz	Annual O&M	24.3	270585.7863	0.7334	0	0	0	0	0	0	0	0
GW	Medium	High	Pressure	10000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	1605.1331	-12529.8744	324256.8748	60919.5312
GW	Large	High	Pressure	10000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.4754	15.1504	274030.553	176296.6942
GW	Small	Low	Pressure	15000	non-haz	Annual O&M	21.59	206605.9939	0.7477	0	0	0	0	0	0	0	0
GW	Medium	Low	Pressure	15000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	1825.2098	-11514.6751	233300.3448	59869.4318
GW	Large	Low	Pressure	15000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	235.6792	188989.2911	213782.4452
GW	Small	Mid	Pressure	15000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	691543.6845	-571481.5178	382986.5369	3892.2745
GW	Medium	Mid	Pressure	15000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	2008.9206	-12691.1516	237388.4202	62712.6846
GW	Large	Mid	Pressure	15000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.1787	-21.9534	197385.7524	158121.9551
GW	Small	High	Pressure	15000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	862231.7763	-681929.6582	410966.5325	4902.4442
GW	Medium	High	Pressure	15000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	1371.455	-10316.7192	243231.1483	66015.6036
GW	Large	High	Pressure	15000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	317.5582	189729.6626	240710.6887
GW	Small	Low	Pressure	20000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1059149.591	-733383.2022	349657.4428	3161.0361
GW	Medium	Low	Pressure	20000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2078.4966	-13333.9665	199191.3219	59530.7251
GW	Large	Low	Pressure	20000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	233.5701	151753.1858	213147.8234
GW	Small	Mid	Pressure	20000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	671818.9964	-513793.35	325560.0534	3876.0166
GW	Medium	Mid	Pressure	20000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	2261.8236	-14507.3435	203271.6442	62375.6333
GW	Large	Mid	Pressure	20000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	245.2989	151544.1032	214976.8352
GW	Small	High	Pressure	20000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	842340.7288	-624162.4319	353530.0089	4886.4332
GW	Medium	High	Pressure	20000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	1614.331	-12078.3942	209063.6135	65682.8412
GW	Large	High	Pressure	20000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.4526	12.7192	162137.5397	175667.6539
GW	Small	Low	Pressure	25000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1053276.065	-707093.9765	315190.3657	3151.4118
GW	Medium	Low	Pressure	25000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2435.2004	-16095.8916	182512.996	57615.2662
GW	Large	Low	Pressure	25000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	232.3049	129411.5	212767.1982
GW	Small	Mid	Pressure	25000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	665773.6095	-487425.8037	291085.3975	3866.5236
GW	Medium	Mid	Pressure	25000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	2618.2081	-17266.6799	186587.5011	60460.8336
GW	Large	Mid	Pressure	25000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	244.1057	129196.1015	214641.3671

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Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	25000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	836343.5993	-597800.2384	319049.6204	4877.2396
GW	Medium	High	Pressure	25000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	1964.7923	-14805.5973	192349.6102	63770.941
GW	Large	High	Pressure	25000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	314.7601	130101.3384	240054.6892
SW	Small	Low	Pressure	5000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	5000	non-haz	Total Capital	34.018	0	0	0	0	0	0	-2492.0991	27485.0084	747380.7199	1518120.093
SW	Large	Low	Pressure	5000	non-haz	Total Capital	35.758	0	0	0	0	0	0	8.4199	-428.2096	541142.2803	3500765.618
SW	Small	Mid	Pressure	5000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	5000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	5000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1667	-237.6853	605595.6021	4655161.709
SW	Small	High	Pressure	5000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	5000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	5000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0276	-689.8981	859843.855	6896164.069
SW	Small	Low	Pressure	10000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	10000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	10000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4606	-438.6757	541721.8267	3493862.219
SW	Small	Mid	Pressure	10000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	10000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	10000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.2074	-248.1514	606175.1485	4648258.31
SW	Small	High	Pressure	10000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	10000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	10000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0673	-700.1708	860414.9396	6889346.279
SW	Small	Low	Pressure	15000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	15000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	15000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	15000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	15000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	15000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004
SW	Small	High	Pressure	15000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	15000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	15000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	20000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	20000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	20000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	20000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	20000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	20000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004
SW	Small	High	Pressure	20000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	20000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	20000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	25000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	25000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	25000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	25000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	25000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	25000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	25000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	25000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	25000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	5000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	3302567.774	-2081398.277	870268.9005	2938.6808
SW	Medium	Low	Pressure	5000	non-haz	Annual O&M	34.018	0	0	0	0	0	0	4313.4488	-27486.8763	570649.6103	40003.1272
SW	Large	Low	Pressure	5000	non-haz	Annual O&M	35.758	0	0	0	0	0	0	0	221.9261	494506.3018	215974.1184
SW	Small	Mid	Pressure	5000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	2944918.421	-1870870.423	845780.859	3710.478
SW	Medium	Mid	Pressure	5000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4569.1534	-28952.3395	575248.9642	42671.8935
SW	Large	Mid	Pressure	5000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	233.3974	494442.9562	216763.0629
SW	Small	High	Pressure	5000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	3098112.413	-1972311.373	872697.3103	4665.8707
SW	Medium	High	Pressure	5000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3574.3541	-25007.3054	579438.2808	46607.892
SW	Large	High	Pressure	5000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	304.6488	496178.8936	238680.4656
SW	Small	Low	Pressure	10000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1093428.716	-920680.956	517235.5887	2834.5612
SW	Medium	Low	Pressure	10000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2700.7403	-15285.9116	320511.2896	52086.6939
SW	Large	Low	Pressure	10000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	208.7677	271054.2329	212814.7354
SW	Small	Mid	Pressure	10000	non-haz	Annual O&M	21.815	280824.6354	0.7841	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	10000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	2965.0399	-16801.6269	325173.1824	54721.0283
SW	Large	Mid	Pressure	10000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	221.0012	270928.9862	213992.647
SW	Small	High	Pressure	10000	non-haz	Annual O&M	24.3	279844.8693	0.7557	0	0	0	0	0	0	0	0
SW	Medium	High	Pressure	10000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	0	0	306120.8072	68664.6156
SW	Large	High	Pressure	10000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	293.7762	272541.1358	236688.5244
SW	Small	Low	Pressure	15000	non-haz	Annual O&M	21.59	214214.9983	0.7723	0	0	0	0	0	0	0	0
SW	Medium	Low	Pressure	15000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2504.9836	-13374.8687	240156.1568	56910.5463
SW	Large	Low	Pressure	15000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	204.3817	196570.2069	211761.5245
SW	Small	Mid	Pressure	15000	non-haz	Annual O&M	21.815	215132.9271	0.766	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	15000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	2768.0717	-14881.3544	244797.3115	59549.7187
SW	Large	Mid	Pressure	15000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	3.0439	-133.5236	206771.9515	150482.5302
SW	Small	High	Pressure	15000	non-haz	Annual O&M	24.3	215424.7458	0.7334	0	0	0	0	0	0	0	0
SW	Medium	High	Pressure	15000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	1661.7265	-10369.0046	248430.1075	63575.3329
SW	Large	High	Pressure	15000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.2632	-85.4788	209088.137	168930.2015
SW	Small	Low	Pressure	20000	non-haz	Annual O&M	21.59	176686.4915	0.7532	0	0	0	0	0	0	0	0
SW	Medium	Low	Pressure	20000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2835.7301	-15509.6714	206207.3203	56658.0803
SW	Large	Low	Pressure	20000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0896	-153.4612	169831.0651	147709.2076
SW	Small	Mid	Pressure	20000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	613007.1981	-476871.8362	319262.4672	3577.2498
SW	Medium	Mid	Pressure	20000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3098.138	-17011.1381	210837.5923	59299.6617
SW	Large	Mid	Pressure	20000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	3.035	-134.5656	169489.3809	150203.6821
SW	Small	High	Pressure	20000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	766445.309	-578490.4263	346197.5326	4532.3768
SW	Medium	High	Pressure	20000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	1977.7496	-12427.1976	214399.5842	63336.7015
SW	Large	High	Pressure	20000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	288.3396	160722.2831	235692.1656
SW	Small	Low	Pressure	25000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	960644.7055	-658812.2569	308974.9826	2800.5673
SW	Medium	Low	Pressure	25000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3390.0666	-19518.8507	191722.1325	53879.3413
SW	Large	Low	Pressure	25000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0829	-154.008	147463.1415	147530.9253
SW	Small	Mid	Pressure	25000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	603083.5751	-448355.8108	284492.5907	3572.3717
SW	Medium	Mid	Pressure	25000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3652.1782	-21018.2377	196347.947	56521.342
SW	Large	Mid	Pressure	25000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	3.0297	-135.188	147119.7477	150037.0852

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																		
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10	
SW	Small	High	Pressure	25000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	756298.5321	-549863.178	311413.059	4527.8226	
SW	Medium	High	Pressure	25000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2523.3883	-16391.2858	199866.8573	60565.9163	
SW	Large	High	Pressure	25000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.2561	-87.5621	149427.3076	168544.487	
GW	Small	Low	Pressure	30000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
GW	Medium	Low	Pressure	30000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017	
GW	Large	Low	Pressure	30000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173	
GW	Small	Mid	Pressure	30000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
GW	Medium	Mid	Pressure	30000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062	
GW	Large	Mid	Pressure	30000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815	
GW	Small	High	Pressure	30000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
GW	Medium	High	Pressure	30000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209	
GW	Large	High	Pressure	30000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619	
GW	Small	Low	Pressure	35000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
GW	Medium	Low	Pressure	35000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017	
GW	Large	Low	Pressure	35000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173	
GW	Small	Mid	Pressure	35000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
GW	Medium	Mid	Pressure	35000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062	
GW	Large	Mid	Pressure	35000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815	
GW	Small	High	Pressure	35000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
GW	Medium	High	Pressure	35000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209	
GW	Large	High	Pressure	35000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619	
GW	Small	Low	Pressure	40000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
GW	Medium	Low	Pressure	40000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017	
GW	Large	Low	Pressure	40000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173	
GW	Small	Mid	Pressure	40000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
GW	Medium	Mid	Pressure	40000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062	
GW	Large	Mid	Pressure	40000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815	
GW	Small	High	Pressure	40000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
GW	Medium	High	Pressure	40000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209	
GW	Large	High	Pressure	40000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619	
GW	Small	Low	Pressure	45000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
GW	Medium	Low	Pressure	45000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017	
GW	Large	Low	Pressure	45000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173	
GW	Small	Mid	Pressure	45000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
GW	Medium	Mid	Pressure	45000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062	
GW	Large	Mid	Pressure	45000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815	
GW	Small	High	Pressure	45000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
GW	Medium	High	Pressure	45000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209	
GW	Large	High	Pressure	45000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619	
GW	Small	Low	Pressure	50000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
GW	Medium	Low	Pressure	50000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017	
GW	Large	Low	Pressure	50000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173	
GW	Small	Mid	Pressure	50000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
GW	Medium	Mid	Pressure	50000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062	
GW	Large	Mid	Pressure	50000	non-haz	Total Capital	34.463	0	0	0	0	0	0	0	2289.8176	441957.2669	6924159.09	

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	50000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	50000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	50000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	30000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1051141.904	-692934.4954	292190.9296	3145.5028
GW	Medium	Low	Pressure	30000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2767.7757	-18932.5039	174322.7649	54468.6203
GW	Large	Low	Pressure	30000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.1726	-37.029	123088.1148	155258.537
GW	Small	Mid	Pressure	30000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	663764.4023	-473327.8748	268092.018	3860.3504
GW	Medium	Mid	Pressure	30000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	2950.5643	-20101.5473	178393.16	57315.1854
GW	Large	Mid	Pressure	30000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	243.3099	114297.4674	214417.3268
GW	Small	High	Pressure	30000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	834373.5222	-583736.1006	296062.6744	4871.1499
GW	Medium	High	Pressure	30000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2293.2451	-17619.4796	184136.7044	60626.2742
GW	Large	High	Pressure	30000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	314.0608	115194.2438	239890.8457
GW	Small	Low	Pressure	35000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1050701.23	-684671.0949	275779.2456	3140.7884
GW	Medium	Low	Pressure	35000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2989.8076	-21043.9416	169305.4423	51442.9965
GW	Large	Low	Pressure	35000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.1684	-37.1164	112432.7865	155186.8196
GW	Small	Mid	Pressure	35000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	663295.9165	-465035.0621	251673.4867	3856.0778
GW	Medium	Mid	Pressure	35000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3172.4462	-22211.7175	173372.7568	54290.288
GW	Large	Mid	Pressure	35000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	242.7417	103655.5653	214257.384
GW	Small	High	Pressure	35000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	833873.4295	-575424.0179	279640.7141	4866.652
GW	Medium	High	Pressure	35000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2512.2641	-19714.0549	179101.4647	57602.9132
GW	Large	High	Pressure	35000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.4428	11.6775	114183.3942	175398.0029
GW	Small	Low	Pressure	40000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1050650.785	-679339.9491	263456.6527	3137.7255
GW	Medium	Low	Pressure	40000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3025.6693	-21863.7255	164727.9711	49178.799
GW	Large	Low	Pressure	40000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	230.4062	95899.0549	212195.5581
GW	Small	Mid	Pressure	40000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	663367.5014	-459784.2717	239364.5068	3852.4774
GW	Medium	Mid	Pressure	40000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3208.3008	-23031.3452	168794.49	52026.0338
GW	Large	Mid	Pressure	40000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.148	-23.1372	104148.2091	157530.4598
GW	Small	High	Pressure	40000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	833834.5078	-570107.4833	267320.266	4863.568
GW	Medium	High	Pressure	40000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2545.9635	-20521.9677	174512.3998	55339.6614
GW	Large	High	Pressure	40000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.4412	11.5051	106190.9781	175353.6841
GW	Small	Low	Pressure	45000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1051045.013	-675883.4231	253890.9976	3134.8134
GW	Medium	Low	Pressure	45000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2934.6611	-21541.0477	159218.15	48095.5502
GW	Large	Low	Pressure	45000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	230.0551	89693.0039	212090.1986
GW	Small	Mid	Pressure	45000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	663481.7506	-456191.4893	229781.4541	3850.1469
GW	Medium	Mid	Pressure	45000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3117.1448	-22707.6083	163282.4621	50943.3523
GW	Large	Mid	Pressure	45000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.146	-23.218	97932.4374	157490.538
GW	Small	High	Pressure	45000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	834103.4367	-566589.0825	257747.8571	4860.6901
GW	Medium	High	Pressure	45000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2453.0981	-20188.8066	168990.8939	54258.3791
GW	Large	High	Pressure	45000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.4399	11.3689	99974.7456	175318.1043
GW	Small	Low	Pressure	50000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1051207.181	-673322.271	246214.8668	3133.234
GW	Medium	Low	Pressure	50000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2893.5592	-21353.4903	154649.9594	47228.3517
GW	Large	Low	Pressure	50000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.156	-36.5863	93225.7735	155340.7325
GW	Small	Mid	Pressure	50000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	663782.1811	-453701.1327	222116.9621	3847.9304
GW	Medium	Mid	Pressure	50000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3075.8732	-22518.7919	158711.6278	50077.1166
GW	Large	Mid	Pressure	50000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	241.8009	84492.0557	214122.824

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	50000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	834539.0852	-564173.3772	250093.156	4858.4905
GW	Medium	High	Pressure	50000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2410.6022	-19993.5814	164415.1863	53391.7044
GW	Large	High	Pressure	50000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.434	11.9469	94974.379	175571.9043
SW	Small	Low	Pressure	30000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	30000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	30000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	30000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	30000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	30000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004
SW	Small	High	Pressure	30000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	30000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	30000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	35000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	35000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	35000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	35000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	35000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	35000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004
SW	Small	High	Pressure	35000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	35000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	35000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	40000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	40000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	40000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	40000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	40000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	40000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004
SW	Small	High	Pressure	40000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	40000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	40000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	45000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	45000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	45000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	45000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	45000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	45000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004
SW	Small	High	Pressure	45000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	45000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	45000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	50000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
SW	Medium	Low	Pressure	50000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377
SW	Large	Low	Pressure	50000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913
SW	Small	Mid	Pressure	50000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	50000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876
SW	Large	Mid	Pressure	50000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	50000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	50000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	50000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	30000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	955965.2204	-643254.5548	285786.8427	2797.4999
SW	Medium	Low	Pressure	30000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3816.278	-22964.8201	184626.3964	50276.4631
SW	Large	Low	Pressure	30000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0784	-154.3709	132551.1557	147411.9536
SW	Small	Mid	Pressure	30000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	598433.4043	-432810.7858	261305.5919	3569.1401
SW	Medium	Mid	Pressure	30000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4078.0859	-24461.9644	189247.631	52919.2762
SW	Large	Mid	Pressure	30000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	3.0261	-135.6065	132206.7702	149925.1606
SW	Small	High	Pressure	30000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	751655.1286	-534327.8711	288228.0663	4524.4536
SW	Medium	High	Pressure	30000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2943.6423	-19806.3099	192738.3336	56968.538
SW	Large	High	Pressure	30000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	286.5277	123449.3073	235360.4482
SW	Small	Low	Pressure	35000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	953505.3376	-633867.9327	269220.1286	2795.2815
SW	Medium	Low	Pressure	35000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3914.4434	-24359.674	178584.8408	47598.3294
SW	Large	Low	Pressure	35000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0753	-154.6315	121899.7621	147326.9488
SW	Small	Mid	Pressure	35000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	596060.3449	-423476.1233	244747.3907	3566.5944
SW	Medium	Mid	Pressure	35000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4176.0443	-25855.2067	183202.4108	50242.1327
SW	Large	Mid	Pressure	35000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	3.0236	-135.9023	121554.5476	149845.9022
SW	Small	High	Pressure	35000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	749225.2399	-524948.0294	271659.5722	4522.4061
SW	Medium	High	Pressure	35000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3037.8493	-21180.8968	186676.3684	54293.0442
SW	Large	High	Pressure	35000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.253	-88.4546	123858.3753	168379.3967
SW	Small	Low	Pressure	40000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	952133.0586	-627820.4304	256802.0682	2793.3344
SW	Medium	Low	Pressure	40000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3850.247	-24522.6197	172809.5532	45826.9615
SW	Large	Low	Pressure	40000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	198.8992	103465.1699	210445.2031
SW	Small	Mid	Pressure	40000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	594582.4798	-417366.3086	232320.4832	3565.0348
SW	Medium	Mid	Pressure	40000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4111.7833	-26017.6931	177426.1941	48470.4455
SW	Large	Mid	Pressure	40000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	3.0217	-136.1257	113565.4428	149785.8976
SW	Small	High	Pressure	40000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	747995.476	-518983.8208	259253.1904	4520.4163
SW	Medium	High	Pressure	40000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2970.54	-21327.6173	180883.826	52524.6784
SW	Large	High	Pressure	40000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.2521	-88.7344	115868.1112	168327.5636
SW	Small	Low	Pressure	45000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	951264.0907	-623670.9617	247142.4408	2792.0187
SW	Medium	Low	Pressure	45000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3823.5285	-24545.0403	167711.4627	44594.5756
SW	Large	Low	Pressure	45000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0647	-154.1576	107667.6308	147498.7525
SW	Small	Mid	Pressure	45000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	593666.1209	-413187.2858	222655.5888	3563.9621
SW	Medium	Mid	Pressure	45000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4084.777	-26038.1494	172324.1606	47239.6459
SW	Large	Mid	Pressure	45000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	3.0139	-135.4792	107321.4126	150024.6267
SW	Small	High	Pressure	45000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	746966.487	-514755.1408	249583.304	4519.2441
SW	Medium	High	Pressure	45000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2941.213	-21336.2678	175770.2134	51295.7591
SW	Large	High	Pressure	45000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.2451	-88.1312	109623.187	168572.3915
SW	Small	Low	Pressure	50000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	950618.3806	-620670.7397	239410.1623	2790.7886
SW	Medium	Low	Pressure	50000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3982.0822	-25543.5244	165110.7659	42934.5469
SW	Large	Low	Pressure	50000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0464	-152.0757	102615.6846	148224.9821
SW	Small	Mid	Pressure	50000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	593126.7025	-410248.3687	214931.5065	3562.4396
SW	Medium	Mid	Pressure	50000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4243.3673	-27036.7421	169723.3838	45579.2149
SW	Large	Mid	Pressure	50000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.9958	-133.4133	102269.0808	150753.5222

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	50000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	746406.5724	-511800.3213	241858.6306	4517.8884
SW	Medium	High	Pressure	50000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3097.9246	-22325.1882	173159.521	49637.1184
SW	Large	High	Pressure	50000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.2276	-86.0997	104570.1034	169306.4934
GW	Small	Low	Pressure	55000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	55000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	55000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	55000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	55000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	55000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815
GW	Small	High	Pressure	55000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	55000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	55000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	60000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	60000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	60000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	60000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	60000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	60000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815
GW	Small	High	Pressure	60000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	60000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	60000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	65000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	65000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	65000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	65000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	65000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	65000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815
GW	Small	High	Pressure	65000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	65000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	65000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	70000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	70000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	70000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	70000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	70000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	70000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815
GW	Small	High	Pressure	70000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	70000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	70000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	75000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049
GW	Medium	Low	Pressure	75000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2523.6675	28012.9376	745181.4392	1520377.017
GW	Large	Low	Pressure	75000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4227	-431.4662	541371.2133	3499016.173
GW	Small	Mid	Pressure	75000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	75000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3865.827	41101.8956	878562.1787	1836517.062
GW	Large	Mid	Pressure	75000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1694	-240.9347	605824.0587	4653416.815

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	75000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
GW	Medium	High	Pressure	75000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8303.065	98339.2387	1117284.869	2553290.209
GW	Large	High	Pressure	75000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0278	-692.6687	860051.8917	6894620.619
GW	Small	Low	Pressure	55000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1051487.85	-671495.3174	239941.5572	3131.4827
GW	Medium	Low	Pressure	55000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	2998.2731	-22105.5277	152596.27	45725.9479
GW	Large	Low	Pressure	55000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.1414	-34.783	89084.1176	156068.482
GW	Small	Mid	Pressure	55000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	664042.2761	-451861.7824	215839.0456	3846.5693
GW	Medium	Mid	Pressure	55000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3180.6831	-23271.5188	156659.2527	48573.7688
GW	Large	Mid	Pressure	55000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.125	-20.8072	88790.5215	158470.9514
GW	Small	High	Pressure	55000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	834746.977	-562323.0152	243816.8128	4856.9243
GW	Medium	High	Pressure	55000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2514.2357	-20739.6958	162355.7008	51889.7037
GW	Large	High	Pressure	55000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.4201	13.6971	90832.2101	176304.8982
GW	Small	Low	Pressure	60000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1051928.601	-670233.6193	234725.6653	3129.9095
GW	Medium	Low	Pressure	60000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3079.9742	-22724.4535	150910.5624	44396.2028
GW	Large	Low	Pressure	60000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.1283	-33.1649	85627.6546	156738.2673
GW	Small	Mid	Pressure	60000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	664488.9941	-450598.222	210623.526	3844.9784
GW	Medium	Mid	Pressure	60000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3262.3048	-23889.6464	154971.4487	47244.7886
GW	Large	Mid	Pressure	60000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.1122	-19.2076	85334.0544	159140.9232
GW	Small	High	Pressure	60000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	835165.1069	-561030.7638	238595.4854	4855.5342
GW	Medium	High	Pressure	60000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2594.8965	-21352.521	160662.5334	50561.6169
GW	Large	High	Pressure	60000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	312.8143	77876.8354	240428.6751
GW	Small	Low	Pressure	65000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1052140.665	-669181.4993	230300.7575	3128.8802
GW	Medium	Low	Pressure	65000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3125.9312	-23145.3942	149431.5651	43215.621
GW	Large	Low	Pressure	65000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.1031	-29.7577	82618.5538	158243.3079
GW	Small	Mid	Pressure	65000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	664689.8822	-449526.034	206194.2018	3843.9901
GW	Medium	Mid	Pressure	65000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3308.2587	-24310.4691	153491.9113	46064.3463
GW	Large	Mid	Pressure	65000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	242.1217	74090.7367	215651.2511
GW	Small	High	Pressure	65000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	835414.6956	-560011.9572	234177.1846	4854.0687
GW	Medium	High	Pressure	65000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2640.305	-21770.6708	159181.7676	49380.495
GW	Large	High	Pressure	65000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.383	18.6403	84365.878	178487.2218
GW	Small	Low	Pressure	70000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1052485.171	-668417.4884	226510.8158	3127.9062
GW	Medium	Low	Pressure	70000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3149.1213	-23418.0077	148047.4413	42207.4667
GW	Large	Low	Pressure	70000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.0845	-27.2669	80056.8966	159342.7227
GW	Small	Mid	Pressure	70000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	665040.8806	-448776.385	202408.9398	3842.7964
GW	Medium	Mid	Pressure	70000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3331.3959	-24582.7754	152107.2619	45056.3122
GW	Large	Mid	Pressure	70000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.0687	-13.3332	79763.0556	161747.892
GW	Small	High	Pressure	70000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	835725.9595	-559224.6179	230382.2482	4853.4064
GW	Medium	High	Pressure	70000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2662.7004	-22038.9572	157793.3837	48372.5616
GW	Large	High	Pressure	70000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	2.3649	21.0925	81804.1441	179587.854
GW	Small	Low	Pressure	75000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	1052836.508	-667858.8762	223237.2973	3126.7443
GW	Medium	Low	Pressure	75000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	3152.5713	-23524.8441	146552.403	41443.6053
GW	Large	Low	Pressure	75000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.0684	-25.0936	77834.9085	160343.4075
GW	Small	Mid	Pressure	75000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	665299.3562	-448183.9852	199131.0486	3841.9003
GW	Medium	Mid	Pressure	75000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	3334.6995	-24688.4978	150609.8777	44293.4464
GW	Large	Mid	Pressure	75000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	0	242.511	69442.7456	216845.7353

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																		
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10	
GW	Small	High	Pressure	75000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	835948.2948	-558596.8236	227098.4232	4852.419	
GW	Medium	High	Pressure	75000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	2665.4201	-22141.4758	156292.7991	47610.199	
GW	Large	High	Pressure	75000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	0	313.5505	70314.212	242499.6385	
SW	Small	Low	Pressure	55000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
SW	Medium	Low	Pressure	55000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377	
SW	Large	Low	Pressure	55000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913	
SW	Small	Mid	Pressure	55000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
SW	Medium	Mid	Pressure	55000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876	
SW	Large	Mid	Pressure	55000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004	
SW	Small	High	Pressure	55000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
SW	Medium	High	Pressure	55000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247	
SW	Large	High	Pressure	55000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171	
SW	Small	Low	Pressure	60000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
SW	Medium	Low	Pressure	60000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377	
SW	Large	Low	Pressure	60000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913	
SW	Small	Mid	Pressure	60000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
SW	Medium	Mid	Pressure	60000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876	
SW	Large	Mid	Pressure	60000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004	
SW	Small	High	Pressure	60000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
SW	Medium	High	Pressure	60000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247	
SW	Large	High	Pressure	60000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171	
SW	Small	Low	Pressure	65000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
SW	Medium	Low	Pressure	65000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377	
SW	Large	Low	Pressure	65000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913	
SW	Small	Mid	Pressure	65000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
SW	Medium	Mid	Pressure	65000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876	
SW	Large	Mid	Pressure	65000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004	
SW	Small	High	Pressure	65000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
SW	Medium	High	Pressure	65000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247	
SW	Large	High	Pressure	65000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171	
SW	Small	Low	Pressure	70000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
SW	Medium	Low	Pressure	70000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377	
SW	Large	Low	Pressure	70000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913	
SW	Small	Mid	Pressure	70000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
SW	Medium	Mid	Pressure	70000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876	
SW	Large	Mid	Pressure	70000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004	
SW	Small	High	Pressure	70000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306	
SW	Medium	High	Pressure	70000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247	
SW	Large	High	Pressure	70000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171	
SW	Small	Low	Pressure	75000	non-haz	Total Capital	21.59	0	0	0	0	0	0	155873.3869	-801906.4663	1575613.983	150079.049	
SW	Medium	Low	Pressure	75000	non-haz	Total Capital	34.029	0	0	0	0	0	0	-2529.4088	28083.8097	744934.4742	1520607.377	
SW	Large	Low	Pressure	75000	non-haz	Total Capital	35.763	0	0	0	0	0	0	8.4173	-429.9031	541255.5335	3499482.913	
SW	Small	Mid	Pressure	75000	non-haz	Total Capital	21.815	1277796.793	0.4821	0	0	0	0	0	0	0	0	
SW	Medium	Mid	Pressure	75000	non-haz	Total Capital	33.359	0	0	0	0	0	0	-3871.5568	41172.6101	878315.7892	1836746.876	
SW	Large	Mid	Pressure	75000	non-haz	Total Capital	34.463	0	0	0	0	0	0	10.1641	-239.3788	605708.8553	4653879.004	

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	75000	non-haz	Total Capital	24.3	0	0	0	0	0	0	925760.6399	-2223622.419	2700805.487	376429.0306
SW	Medium	High	Pressure	75000	non-haz	Total Capital	35.282	0	0	0	0	0	0	-8308.7991	98410.0174	1117038.242	2553520.247
SW	Large	High	Pressure	75000	non-haz	Total Capital	35.505	0	0	0	0	0	0	21.0223	-691.0717	859931.2914	6895176.171
SW	Small	Low	Pressure	55000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	950092.0731	-618391.689	233070.6105	2790.634
SW	Medium	Low	Pressure	55000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	4117.4978	-26502.795	163436.6769	41273.0511
SW	Large	Low	Pressure	55000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0219	-149.1208	98434.2177	149310.834
SW	Small	Mid	Pressure	55000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	592637.4292	-407992.379	208596.0103	3562.1402
SW	Medium	Mid	Pressure	55000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4378.7314	-27995.6544	168048.6336	43917.7999
SW	Large	Mid	Pressure	55000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.9716	-130.4739	98087.3514	151841.0148
SW	Small	High	Pressure	55000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	746088.1792	-509620.5717	235529.7626	4517.2656
SW	Medium	High	Pressure	55000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3231.6757	-23275.8786	171476.466	47977.1551
SW	Large	High	Pressure	55000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.2039	-83.188	100387.7581	170398.3601
SW	Small	Low	Pressure	60000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	949787.6394	-616725.9835	227804.7086	2789.5582
SW	Medium	Low	Pressure	60000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	4186.1387	-27086.7101	161803.2371	39894.6085
SW	Large	Low	Pressure	60000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.9921	-145.3879	94900.9922	150711.1839
SW	Small	Mid	Pressure	60000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	592347.5938	-406335.5071	203331.5653	3560.9672
SW	Medium	Mid	Pressure	60000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4447.1753	-28578.257	166412.5954	42540.338
SW	Large	Mid	Pressure	60000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.942	-126.7549	94553.9088	153243.2467
SW	Small	High	Pressure	60000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	745742.9278	-507935.0201	230259.8365	4516.483
SW	Medium	High	Pressure	60000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3298.9504	-23852.5656	169834.8393	46600.4764
SW	Large	High	Pressure	60000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.1746	-79.4923	96853.8186	171803.9049
SW	Small	Low	Pressure	65000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	949554.8885	-615417.3828	223341.6858	2789.0941
SW	Medium	Low	Pressure	65000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	4212.2868	-27417.5551	160215.5626	38750.3239
SW	Large	Low	Pressure	65000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.9694	-142.5621	91923.256	151791.1841
SW	Small	Mid	Pressure	65000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	592017.1141	-404975.9893	198861.671	3560.8398
SW	Medium	Mid	Pressure	65000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4473.4515	-28909.7759	164825.7147	41395.5749
SW	Large	Mid	Pressure	65000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.9194	-123.9348	91575.8336	154325.4757
SW	Small	High	Pressure	65000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	745476.595	-506604.85	225794.7019	4516.0066
SW	Medium	High	Pressure	65000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3324.1222	-24178.6815	168243.4119	45455.9618
SW	Large	High	Pressure	65000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.1525	-76.694	93875.3771	172888.7017
SW	Small	Low	Pressure	70000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	949479.7863	-614438.2948	219526.3145	2788.3379
SW	Medium	Low	Pressure	70000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	4184.3886	-27384.6656	158308.9578	37955.7208
SW	Large	Low	Pressure	70000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.9478	-139.8365	89357.4594	152890.9067
SW	Small	Mid	Pressure	70000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	592089.2104	-404062.1835	195051.5266	3560.0089
SW	Medium	Mid	Pressure	70000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4445.4153	-28875.9823	162917.5472	40601.4264
SW	Large	Mid	Pressure	70000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.8981	-121.2188	89009.8736	155426.7095
SW	Small	High	Pressure	70000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	745306.413	-505584.7727	221974.8855	4515.3339
SW	Medium	High	Pressure	70000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3295.1688	-24140.071	166330.046	44662.9419
SW	Large	High	Pressure	70000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.1314	-73.9976	91309.1417	173991.8195
SW	Small	Low	Pressure	75000	non-haz	Annual O&M	21.59	0	0	0	0	0	0	949302.455	-613591.1715	216213.0828	2787.8809
SW	Medium	Low	Pressure	75000	non-haz	Annual O&M	34.029	0	0	0	0	0	0	4062.3849	-26778.8205	155796.5998	37555.9996
SW	Large	Low	Pressure	75000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.9323	-137.8857	87149.5367	153683.0801
SW	Small	Mid	Pressure	75000	non-haz	Annual O&M	21.815	0	0	0	0	0	0	591810.0308	-403155.9502	191729.2146	3559.8187
SW	Medium	Mid	Pressure	75000	non-haz	Annual O&M	33.359	0	0	0	0	0	0	4323.3091	-28269.2417	160402.9802	40202.825
SW	Large	Mid	Pressure	75000	non-haz	Annual O&M	34.463	0	0	0	0	0	0	2.8826	-119.2754	86801.8137	156219.7272

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	75000	non-haz	Annual O&M	24.3	0	0	0	0	0	0	745048.072	-504701.3898	218656.7362	4515.0366
SW	Medium	High	Pressure	75000	non-haz	Annual O&M	35.282	0	0	0	0	0	0	3172.2839	-23529.4898	163811.9583	44264.8187
SW	Large	High	Pressure	75000	non-haz	Annual O&M	35.505	0	0	0	0	0	0	3.1162	-72.0675	89100.692	174787.9504
SW	Small	Low	Gravity	5000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	5000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2215.9319	-47607.7405	905378.5464	1498796.203
SW	Large	Low	Gravity	5000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	5000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	5000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	5000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	5000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	5000	non-haz	Total Capital	34.735	0	0	0	0	0	0	1747.5957	-40783.7296	1021445.793	2016353.85
SW	Large	High	Gravity	5000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	10000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	10000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2215.9319	-47607.7405	905378.5464	1498796.203
SW	Large	Low	Gravity	10000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	10000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	10000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	10000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	10000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	10000	non-haz	Total Capital	34.735	0	0	0	0	0	0	1747.5957	-40783.7296	1021445.793	2016353.85
SW	Large	High	Gravity	10000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	15000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	15000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	15000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	15000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	15000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	15000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	15000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	15000	non-haz	Total Capital	34.735	0	0	0	0	0	0	1747.5957	-40783.7296	1021445.793	2016353.85
SW	Large	High	Gravity	15000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	20000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	20000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	20000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	20000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	20000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	20000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	20000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	20000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	20000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	25000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	25000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	25000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	25000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	25000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	25000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	25000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	25000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	25000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	5000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	1553949.451	-941766.8848	688128.7417	28094.6299
SW	Medium	Low	Gravity	5000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	0	0	513388.8313	77224.2648
SW	Large	Low	Gravity	5000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	0	0	491422.8766	266976.5986
SW	Small	Mid	Gravity	5000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	1468267.845	-875616.7882	683466.1672	32890.4998
SW	Medium	Mid	Gravity	5000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	0	0	516837.2312	80596.7135
SW	Large	Mid	Gravity	5000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	0	0	491762.1239	261806.4982
SW	Small	High	Gravity	5000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	1456223.479	-861545.1655	686493.8491	34783.2849
SW	Medium	High	Gravity	5000	non-haz	Annual O&M	34.735	0	0	0	0	0	0	0	0	516776.5238	80843.8182
SW	Large	High	Gravity	5000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	0	492327.3661	258618.4294
SW	Small	Low	Gravity	10000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-655303.9056	218997.6708	335086.1423	27990.8175
SW	Medium	Low	Gravity	10000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	0	0	289485.5994	76609.9675
SW	Large	Low	Gravity	10000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	0	-64.0104	272817.0482	217003.2373
SW	Small	Mid	Gravity	10000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-740910.4421	285105.4996	330420.1886	32786.6026
SW	Medium	Mid	Gravity	10000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	0	0	292910.9422	79968.9438
SW	Large	Mid	Gravity	10000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	0	0	268372.5944	259801.6116
SW	Small	High	Gravity	10000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-752949.8049	299131.2227	333447.1147	34679.0468
SW	Medium	High	Gravity	10000	non-haz	Annual O&M	34.735	0	0	0	0	0	0	0	0	292667.775	80353.2715
SW	Large	High	Gravity	10000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	0	268933.9874	256193.2518
SW	Small	Low	Gravity	15000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-751960.4934	391063.6776	219511.3385	27970.303
SW	Medium	Low	Gravity	15000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	0	0	214010.0674	78884.2913
SW	Large	Low	Gravity	15000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.1063	-421.9722	208947.5263	151995.2586
SW	Small	Mid	Gravity	15000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-837704.5411	457220.6587	214842.2504	32766.1011
SW	Medium	Mid	Gravity	15000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	0	0	217550.3678	82107.4056
SW	Large	Mid	Gravity	15000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.9574	-402.2759	208570.5531	152504.0607
SW	Small	High	Gravity	15000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-849615.2934	471182.5701	217870.8876	34658.6047
SW	Medium	High	Gravity	15000	non-haz	Annual O&M	34.735	0	0	0	0	0	0	0	-1270.5219	222367.9636	79291.6673
SW	Large	High	Gravity	15000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0435	-407.9239	209105.8333	150142.6098
SW	Small	Low	Gravity	20000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-778132.9298	452322.1283	161597.3902	27961.7537
SW	Medium	Low	Gravity	20000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	0	0	176291.9677	80242.4254
SW	Large	Low	Gravity	20000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	0	-64.597	161173.3565	215294.8982
SW	Small	Mid	Gravity	20000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-863805.9837	518451.297	156927.9439	32757.4523
SW	Medium	Mid	Gravity	20000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	0	0	179840.8933	83450.2078
SW	Large	Mid	Gravity	20000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.9625	-403.0647	171370.9449	151920.3755
SW	Small	High	Gravity	20000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-875945.8327	532521.2453	159943.4493	34650.1788
SW	Medium	High	Gravity	20000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	0	-1358.7924	184867.9854	80535.6235
SW	Large	High	Gravity	20000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0482	-408.7308	171908.9806	149450.0447
SW	Small	Low	Gravity	25000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-788043.8064	480858.0533	126819.2983	27957.146
SW	Medium	Low	Gravity	25000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	1639.6414	-12072.3682	178644.5597	69404.543
SW	Large	Low	Gravity	25000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	0	-64.7145	138844.6306	214952.8326
SW	Small	Mid	Gravity	25000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-873705.9321	546961.6412	122156.7658	32752.6553
SW	Medium	Mid	Gravity	25000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	1704.2299	-12327.776	182293.9488	72697.2791
SW	Large	Mid	Gravity	25000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	0	-62.1558	138969.6671	212547.342

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	25000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-885729.7813	560967.9696	125178.4708	34645.4088
SW	Medium	High	Gravity	25000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	0	-1804.6317	164050.9995	80446.4376
SW	Large	High	Gravity	25000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	0	-57.9972	139218.9217	211767.9863
SW	Small	Low	Gravity	30000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	30000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	30000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	30000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	30000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	30000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	30000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	30000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	30000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	35000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	35000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	35000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	35000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	35000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	35000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	35000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	35000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	35000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	40000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	40000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	40000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	40000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	40000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	40000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	40000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	40000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	40000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	45000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	45000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	45000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	45000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	45000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	45000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	45000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	45000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	45000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	50000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	50000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	50000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	50000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	50000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	50000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	50000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	50000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	50000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	30000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-792740.8478	496414.8729	103633.3399	27953.766
SW	Medium	Low	Gravity	30000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2047.557	-15421.1073	171442.7273	65831.0802
SW	Large	Low	Gravity	30000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.1102	-422.8136	134531.6902	150775.723
SW	Small	Mid	Gravity	30000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-878471.3832	562564.7983	98963.68	32749.4115
SW	Medium	Mid	Gravity	30000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2118.0777	-15704.8655	175123.9301	69114.0348
SW	Large	Mid	Gravity	30000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	0	-62.2335	124082.8211	212356.094
SW	Small	High	Gravity	30000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-890499.1756	576568.7048	101984.1109	34642.1435
SW	Medium	High	Gravity	30000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1644.9738	-13172.3627	171270.7288	70698.2142
SW	Large	High	Gravity	30000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.053	-409.5376	134712.1612	148756.874
SW	Small	Low	Gravity	35000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-795216.6807	505806.6316	87066.7389	27951.5145
SW	Medium	Low	Gravity	35000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2132.5829	-16745.919	165323.9016	63174.8008
SW	Large	Low	Gravity	35000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.1108	-422.9335	123900.8299	150601.9529
SW	Small	Mid	Gravity	35000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-880846.5024	571910.0793	82399.2614	32747.429
SW	Medium	Mid	Gravity	35000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2207.463	-17050.8762	169029.9264	66449.6158
SW	Large	Mid	Gravity	35000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.9692	-404.0768	123542.8391	151170.0719
SW	Small	High	Gravity	35000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-892855.2136	585898.0543	85423.5131	34639.8375
SW	Medium	High	Gravity	35000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1731.4305	-14505.7019	165157.4931	68040.4418
SW	Large	High	Gravity	35000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0544	-409.7709	124084.5918	148558.1653
SW	Small	Low	Gravity	40000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-796693.6716	511916.2254	74639.3036	27950.1144
SW	Medium	Low	Gravity	40000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2058.7078	-16857.3892	159492.2997	61419.2535
SW	Large	Low	Gravity	40000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.1112	-423.022	115927.6642	150471.5136
SW	Small	Mid	Gravity	40000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-882321.9354	578003.3076	69976.3566	32745.6989
SW	Medium	Mid	Gravity	40000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2136.7483	-17177.4629	163215.5664	64688.3825
SW	Large	Mid	Gravity	40000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.9703	-404.2462	115571.4953	151045.2538
SW	Small	High	Gravity	40000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-894441.0717	592070.9271	72985.6315	34638.4544
SW	Medium	High	Gravity	40000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1658.5773	-14623.25	159329.8202	66283.5528
SW	Large	High	Gravity	40000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0554	-409.9439	116113.8503	148409.4416
SW	Small	Low	Gravity	45000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-797502.071	516042.7921	64980.425	27948.7228
SW	Medium	Low	Gravity	45000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2024.1324	-16837.7963	154347.2972	60200.2876
SW	Large	Low	Gravity	45000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.1052	-422.2712	109696.076	150654.8602
SW	Small	Mid	Gravity	45000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-883279.2412	582206.4885	60308.6259	32744.4316
SW	Medium	Mid	Gravity	45000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2104.7814	-17170.7089	158085.9229	63464.3535
SW	Large	Mid	Gravity	45000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.9649	-403.5568	109341.2889	151233.0796
SW	Small	High	Gravity	45000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-895261.9097	596197.9994	63326.6218	34637.1461
SW	Medium	High	Gravity	45000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1624.7661	-14608.1542	154186.9743	65064.5713
SW	Large	High	Gravity	45000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0499	-409.2575	109884.0834	148579.4744
SW	Small	Low	Gravity	50000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-798180.1361	519054.1014	57247.895	27947.6639
SW	Medium	Low	Gravity	50000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2176.7898	-17805.0707	151713.082	58549.3672
SW	Large	Low	Gravity	50000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.0886	-420.1243	104653.7158	151339.7045
SW	Small	Mid	Gravity	50000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-883961.6809	585242.3022	52569.1706	32743.5967
SW	Medium	Mid	Gravity	50000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2259.286	-18146.6061	155461.0244	61810.5502
SW	Large	Mid	Gravity	50000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.9486	-401.4571	104300.0261	151920.8815

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	50000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-895889.3295	599181.0501	55597.6706	34636.1334
SW	Medium	High	Gravity	50000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1777.9698	-15578.522	151553.7949	63413.5349
SW	Large	High	Gravity	50000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.0337	-407.1606	104843.1765	149253.1411
SW	Small	Low	Gravity	55000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	55000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	55000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	55000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	55000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	55000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	55000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	55000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	55000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	60000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	60000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	60000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	60000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	60000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	60000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	60000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	60000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	60000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	65000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	65000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	65000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	65000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	65000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	65000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	65000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	65000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	65000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	70000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	70000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	70000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	70000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	70000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	70000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813
SW	Small	High	Gravity	70000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	70000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	70000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	75000	non-haz	Total Capital	30.095	0	0	0	0	0	0	-1281459.361	2163339.033	-89735.902	829825.997
SW	Medium	Low	Gravity	75000	non-haz	Total Capital	34.024	0	0	0	0	0	0	2323.6228	-49013.6019	910462.7037	1493951.594
SW	Large	Low	Gravity	75000	non-haz	Total Capital	35.621	0	0	0	0	0	0	6.5064	-1948.8489	565732.9385	2532745.806
SW	Small	Mid	Gravity	75000	non-haz	Total Capital	29.22	0	0	0	0	0	0	-1066999.862	1783021.413	214961.9487	981685.0453
SW	Medium	Mid	Gravity	75000	non-haz	Total Capital	33.482	0	0	0	0	0	0	1676.5458	-38879.764	945256.0752	1888966.945
SW	Large	Mid	Gravity	75000	non-haz	Total Capital	35.079	0	0	0	0	0	0	5.9022	-1720.4962	556962.1631	3998799.813

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	75000	non-haz	Total Capital	31.155	0	0	0	0	0	0	-841567.548	1416348.991	453411.6132	1037706.132
SW	Medium	High	Gravity	75000	non-haz	Total Capital	34.729	0	0	0	0	0	0	1718.4988	-40235.0004	1018912.538	2019122.046
SW	Large	High	Gravity	75000	non-haz	Total Capital	35.763	0	0	0	0	0	0	6.9161	-2183.0783	643185.9908	4001841.938
SW	Small	Low	Gravity	55000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-798709.8227	521316.6563	50915.3064	27946.7883
SW	Medium	Low	Gravity	55000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2307.2584	-18738.2912	150011.3168	56895.3275
SW	Large	Low	Gravity	55000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.0656	-417.1154	100480.0918	152391.2826
SW	Small	Mid	Gravity	55000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-884184.3144	587338.0875	46258.8618	32742.2695
SW	Medium	Mid	Gravity	55000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2391.3872	-19087.5486	153767.6283	60153.962
SW	Large	Mid	Gravity	55000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.926	-398.4906	100127.3529	152975.2363
SW	Small	High	Gravity	55000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-896340.1072	601395.1837	49273.3809	34634.9209
SW	Medium	High	Gravity	55000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1908.8452	-16513.9601	149851.7392	61760.2244
SW	Large	High	Gravity	55000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	3.011	-404.1937	100670.7427	150296.0063
SW	Small	Low	Gravity	60000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-798896.9431	522929.4901	45653.1341	27945.9024
SW	Medium	Low	Gravity	60000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2371.6519	-19299.5146	148352.5729	55524.1078
SW	Large	Low	Gravity	60000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.0369	-413.3366	96953.3533	153763.7771
SW	Small	Mid	Gravity	60000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-884586.5539	589066.5937	40979.2476	32741.8711
SW	Medium	Mid	Gravity	60000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2457.1279	-19655.1467	152115.8062	58780.8074
SW	Large	Mid	Gravity	60000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.8976	-394.7458	96601.3844	154350.1202
SW	Small	High	Gravity	60000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-896499.9137	603004.741	44008.3979	34634.2059
SW	Medium	High	Gravity	60000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1973.7208	-17078.1529	148195.5015	60387.9226
SW	Large	High	Gravity	60000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.9825	-400.4507	97145.0546	151660.4727
SW	Small	Low	Gravity	65000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-799019.5728	524173.5958	41200.0943	27945.095
SW	Medium	Low	Gravity	65000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2394.4022	-19612.4851	146745.9935	54384.9443
SW	Large	Low	Gravity	65000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	3.0152	-410.472	93981.1132	154820.1533
SW	Small	Mid	Gravity	65000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-884762.6872	590315.3621	36532.4174	32740.5935
SW	Medium	Mid	Gravity	65000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2481.0166	-19973.6181	150515.6671	57639.317
SW	Large	Mid	Gravity	65000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.8762	-391.9073	93629.7202	155408.7094
SW	Small	High	Gravity	65000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-896841.4237	604375.4337	39537.7676	34633.8644
SW	Medium	High	Gravity	65000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1996.7203	-17392.4915	146588.6921	59249.2033
SW	Large	High	Gravity	65000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.961	-397.614	94173.6072	152710.8236
SW	Small	Low	Gravity	70000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-799118.2751	525170.0815	37381.2242	27944.5198
SW	Medium	Low	Gravity	70000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2363.4202	-19562.9464	144820.4818	53595.8589
SW	Large	Low	Gravity	70000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	2.9945	-407.7157	91420.1207	155899.0953
SW	Small	Mid	Gravity	70000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-884975.2452	591384.0789	32700.2692	32740.6734
SW	Medium	Mid	Gravity	70000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2451.1416	-19929.7702	148597.5566	56847.7182
SW	Large	Mid	Gravity	70000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.8557	-389.1765	91069.297	156489.3416
SW	Small	High	Gravity	70000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-897102.2317	605439.2713	35712.2536	34633.2716
SW	Medium	High	Gravity	70000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1966.1943	-17345.7537	144666.0297	58458.9849
SW	Large	High	Gravity	70000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.9406	-394.8844	91613.3536	153784.3556
SW	Small	Low	Gravity	75000	non-haz	Annual O&M	30.095	0	0	0	0	0	0	-799441.3448	526106.8602	34053.1854	27944.3783
SW	Medium	Low	Gravity	75000	non-haz	Annual O&M	34.024	0	0	0	0	0	0	2238.9038	-18943.6832	142293.3968	53200.4987
SW	Large	Low	Gravity	75000	non-haz	Annual O&M	35.621	0	0	0	0	0	0	2.9797	-405.7372	89216.3198	156673.3209
SW	Small	Mid	Gravity	75000	non-haz	Annual O&M	29.22	0	0	0	0	0	0	-885151.1359	592235.4329	29385.5761	32740.0709
SW	Medium	Mid	Gravity	75000	non-haz	Annual O&M	33.482	0	0	0	0	0	0	2327.2884	-19313.2678	146072.378	56452.1888
SW	Large	Mid	Gravity	75000	non-haz	Annual O&M	35.079	0	0	0	0	0	0	2.8411	-387.2179	88865.9545	157265.0755

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	75000	non-haz	Annual O&M	31.155	0	0	0	0	0	0	-897249.4508	606285.2461	32395.6695	34632.7775
SW	Medium	High	Gravity	75000	non-haz	Annual O&M	34.729	0	0	0	0	0	0	1841.7892	-16726.9892	142137.5816	58064.6618
SW	Large	High	Gravity	75000	non-haz	Annual O&M	35.763	0	0	0	0	0	0	2.9259	-392.9276	89410.1847	154553.8478
GW	Small	Low	Pressure	5000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	5000	haz	Total Capital	34.165	0	0	0	0	0	0	-2204.6567	23830.3241	793506.3115	1504948.47
GW	Large	Low	Pressure	5000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5738	-476.4487	581178.4286	3451620.657
GW	Small	Mid	Pressure	5000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	5000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	5000	haz	Total Capital	34.7	0	0	0	0	0	0	10.1298	-237.2104	642538.8427	4627318.984
GW	Small	High	Pressure	5000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	5000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	5000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3087	-748.0259	900892.6186	6851542.74
GW	Small	Low	Pressure	10000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	10000	haz	Total Capital	34.165	0	0	0	0	0	0	-2204.6567	23830.3241	793506.3115	1504948.47
GW	Large	Low	Pressure	10000	haz	Total Capital	35.979	0	0	0	0	0	0	8.6145	-486.9148	581757.9749	3444717.259
GW	Small	Mid	Pressure	10000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	10000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	10000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1705	-247.6765	643118.3891	4620415.585
GW	Small	High	Pressure	10000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	10000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	10000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3483	-758.2982	901463.688	6844725.123
GW	Small	Low	Pressure	15000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	15000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	15000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	15000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	15000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	15000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	15000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	15000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	15000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	20000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	20000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	20000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	20000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	20000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	20000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	20000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	20000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	20000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	25000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	25000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	25000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	25000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	25000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	25000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	25000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	25000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	25000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	5000	haz	Annual O&M	21.605	0	0	0	0	0	0	3285811.774	-1884614.614	992203.0012	14540.3991
GW	Medium	Low	Pressure	5000	haz	Annual O&M	34.165	0	0	0	0	0	0	3670.2654	-27110.0642	789604.6564	46659.716
GW	Large	Low	Pressure	5000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	251.4776	706757.962	224250.4486
GW	Small	Mid	Pressure	5000	haz	Annual O&M	21.865	0	0	0	0	0	0	2898587.198	-1664639.247	967989.6747	15253.2076
GW	Medium	Mid	Pressure	5000	haz	Annual O&M	33.482	0	0	0	0	0	0	3851.1402	-28284.4413	793768.0138	49438.6324
GW	Large	Mid	Pressure	5000	haz	Annual O&M	34.7	0	0	0	0	0	0	0	262.125	706643.7074	225405.3004
GW	Small	High	Pressure	5000	haz	Annual O&M	24.33	0	0	0	0	0	0	3068948.195	-1774852.693	995939.8754	16264.2607
GW	Medium	High	Pressure	5000	haz	Annual O&M	35.324	0	0	0	0	0	0	3326.9129	-26499.0659	800046.1726	52798.2026
GW	Large	High	Pressure	5000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	330.4724	707751.2699	249379.4795
GW	Small	Low	Pressure	10000	haz	Annual O&M	21.605	0	0	0	0	0	0	2081176.324	-1413690.873	644829.5458	7806.4536
GW	Medium	Low	Pressure	10000	haz	Annual O&M	34.165	0	0	0	0	0	0	2856.565	-20721.0328	442852.841	44606.206
GW	Large	Low	Pressure	10000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	239.3601	373401.431	217746.9589
GW	Small	Mid	Pressure	10000	haz	Annual O&M	21.865	0	0	0	0	0	0	1696739.621	-1195173.088	620777.3535	8518.8389
GW	Medium	Mid	Pressure	10000	haz	Annual O&M	33.482	0	0	0	0	0	0	3056.0727	-22015.2897	447177.6246	47333.3259
GW	Large	Mid	Pressure	10000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	250.7288	373223.9263	219351.7504
GW	Small	High	Pressure	10000	haz	Annual O&M	24.33	0	0	0	0	0	0	1867181.477	-1305464.053	648736.9652	9529.4393
GW	Medium	High	Pressure	10000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	0	408618.1177	72942.7622
GW	Large	High	Pressure	10000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	320.5178	374205.0545	244225.0083
GW	Small	Low	Pressure	15000	haz	Annual O&M	21.605	0	0	0	0	0	0	1196707.509	-910060.6597	476002.5482	6445.1888
GW	Medium	Low	Pressure	15000	haz	Annual O&M	34.171	0	0	0	0	0	0	2419.6735	-17225.3409	323953.9255	46012.0459
GW	Large	Low	Pressure	15000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	235.3214	262282.5426	215579.5436
GW	Small	Mid	Pressure	15000	haz	Annual O&M	21.865	0	0	0	0	0	0	813050.7627	-691948.7761	451995.9777	7157.5312
GW	Medium	Mid	Pressure	15000	haz	Annual O&M	33.482	0	0	0	0	0	0	2606.3426	-18426.8915	328104.6116	48813.6144
GW	Large	Mid	Pressure	15000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	246.9299	262084.01	217333.6852
GW	Small	High	Pressure	15000	haz	Annual O&M	24.33	0	0	0	0	0	0	983652.2656	-802333.0567	479964.4663	8168.0709
GW	Medium	High	Pressure	15000	haz	Annual O&M	35.324	0	0	0	0	0	0	1980.1897	-16105.5618	333960.5309	52146.5982
GW	Large	High	Pressure	15000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	317.1999	263022.9602	242507.3443
GW	Small	Low	Pressure	20000	haz	Annual O&M	21.605	0	0	0	0	0	0	1140974.411	-812524.1342	401294.8294	5612.7464
GW	Medium	Low	Pressure	20000	haz	Annual O&M	34.171	0	0	0	0	0	0	1906.3315	-13038.943	258558.2515	50636.6859
GW	Large	Low	Pressure	20000	haz	Annual O&M	35.979	0	0	0	0	0	0	2.2281	-42.0438	215513.024	155778.7925
GW	Small	Mid	Pressure	20000	haz	Annual O&M	21.865	0	0	0	0	0	0	757707.9488	-594628.022	377313.8654	6324.9529
GW	Medium	Mid	Pressure	20000	haz	Annual O&M	33.482	0	0	0	0	0	0	2091.7803	-14230.1686	262683.4462	53450.8223
GW	Large	Mid	Pressure	20000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	245.0305	206514.0567	216324.5611
GW	Small	High	Pressure	20000	haz	Annual O&M	24.33	0	0	0	0	0	0	928431.2688	-705077.0014	405288.7887	7335.5771
GW	Medium	High	Pressure	20000	haz	Annual O&M	35.324	0	0	0	0	0	0	1452.7697	-11841.0226	268484.9258	56781.3304
GW	Large	High	Pressure	20000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	315.5406	207431.9414	241648.0166
GW	Small	Low	Pressure	25000	haz	Annual O&M	21.605	0	0	0	0	0	0	1115441.217	-765254.1605	356449.8008	5113.7132
GW	Medium	Low	Pressure	25000	haz	Annual O&M	34.171	0	0	0	0	0	0	1648.4901	-10873.4609	219891.7785	53404.5979
GW	Large	Low	Pressure	25000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	232.0899	173387.4837	213845.1138
GW	Small	Mid	Pressure	25000	haz	Annual O&M	21.865	0	0	0	0	0	0	732677.9165	-547602.5568	332495.7345	5825.6666
GW	Medium	Mid	Pressure	25000	haz	Annual O&M	33.482	0	0	0	0	0	0	1833.2475	-12059.0903	224003.2961	56225.4992
GW	Large	Mid	Pressure	25000	haz	Annual O&M	34.711	0	0	0	0	0	0	2.1918	-26.9695	181818.7861	157959.0742

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	25000	haz	Annual O&M	24.33	0	0	0	0	0	0	903105.4377	-657899.375	360449.0258	6836.7152
GW	Medium	High	Pressure	25000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	0	208047.2175	70457.075
GW	Large	High	Pressure	25000	haz	Annual O&M	35.642	0	0	0	0	0	0	2.4807	7.9757	183863.9531	175758.0129
GW	Small	Low	Pressure	30000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	30000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	30000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	30000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	30000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	30000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	30000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	30000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	30000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	35000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	35000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	35000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	35000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	35000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	35000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	35000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	35000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	35000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	40000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	40000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	40000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	40000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	40000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	40000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	40000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	40000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	40000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	45000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	45000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	45000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	45000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	45000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	45000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	45000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	45000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	45000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	50000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	50000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	50000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	50000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	50000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	50000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	50000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	50000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	50000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	30000	haz	Annual O&M	21.605	0	0	0	0	0	0	1101251.169	-738527.8953	326552.953	4780.7093
GW	Medium	Low	Pressure	30000	haz	Annual O&M	34.171	0	0	0	0	0	0	1618.2908	-10474.3191	196127.7573	54687.4971
GW	Large	Low	Pressure	30000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	231.2821	151163.7209	213411.5815
GW	Small	Mid	Pressure	30000	haz	Annual O&M	21.865	0	0	0	0	0	0	718568.0164	-520908.42	302598.3397	5493.1154
GW	Medium	Mid	Pressure	30000	haz	Annual O&M	33.482	0	0	0	0	0	0	1802.6081	-11656.055	200229.4727	57513.0856
GW	Large	Mid	Pressure	30000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	243.1308	150944.1091	215315.6385
GW	Small	High	Pressure	30000	haz	Annual O&M	24.33	0	0	0	0	0	0	889193.3837	-631314.1166	330567.1825	6503.7062
GW	Medium	High	Pressure	30000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	0	185524.1248	71001.4732
GW	Large	High	Pressure	30000	haz	Annual O&M	35.642	0	0	0	0	0	0	2.4722	8.3629	161593.998	175638.299
GW	Small	Low	Pressure	35000	haz	Annual O&M	21.605	0	0	0	0	0	0	1092344.139	-721804.8905	305195.6377	4543.151
GW	Medium	Low	Pressure	35000	haz	Annual O&M	34.171	0	0	0	0	0	0	1708.9666	-11040.3143	180897.2984	54945.9382
GW	Large	Low	Pressure	35000	haz	Annual O&M	35.979	0	0	0	0	0	0	2.1918	-40.1558	143936.3114	155341.768
GW	Small	Mid	Pressure	35000	haz	Annual O&M	21.865	0	0	0	0	0	0	709612.879	-504186.2669	281244.6344	5255.5251
GW	Medium	Mid	Pressure	35000	haz	Annual O&M	33.482	0	0	0	0	0	0	1892.8691	-12218.7814	184991.3478	57775.2345
GW	Large	Mid	Pressure	35000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	242.5883	135066.9753	215027.1845
GW	Small	High	Pressure	35000	haz	Annual O&M	24.33	0	0	0	0	0	0	880329.7582	-614632.6979	309216.8012	6266.0274
GW	Medium	High	Pressure	35000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	-889.8801	173319.4724	68955.7446
GW	Large	High	Pressure	35000	haz	Annual O&M	35.642	0	0	0	0	0	0	2.4662	8.6385	145686.9073	175552.735
GW	Small	Low	Pressure	40000	haz	Annual O&M	21.605	0	0	0	0	0	0	1086251.157	-710570.0411	289178.6981	4365.0519
GW	Medium	Low	Pressure	40000	haz	Annual O&M	34.171	0	0	0	0	0	0	1867.0334	-12185.5992	171104.2014	54299.3673
GW	Large	Low	Pressure	40000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	230.2721	123384.0258	212869.3839
GW	Small	Mid	Pressure	40000	haz	Annual O&M	21.865	0	0	0	0	0	0	703550.7018	-492984.0388	265234.5988	5077.1823
GW	Medium	Mid	Pressure	40000	haz	Annual O&M	33.482	0	0	0	0	0	0	2050.7025	-13362.046	175192.9549	57131.6563
GW	Large	Mid	Pressure	40000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	242.181	123159.1407	214810.8664
GW	Small	High	Pressure	40000	haz	Annual O&M	24.33	0	0	0	0	0	0	874196.844	-603396.8446	293202.7476	6087.9336
GW	Medium	High	Pressure	40000	haz	Annual O&M	35.324	0	0	0	0	0	0	1392.556	-10872.1882	180914.7001	60457.1982
GW	Large	High	Pressure	40000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	313.0522	124045.3645	240359.7897
GW	Small	Low	Pressure	45000	haz	Annual O&M	21.605	0	0	0	0	0	0	1081624.069	-702512.3398	276712.6855	4226.4445
GW	Medium	Low	Pressure	45000	haz	Annual O&M	34.171	0	0	0	0	0	0	2037.9582	-13478.6488	164461.6167	53217.2043
GW	Large	Low	Pressure	45000	haz	Annual O&M	35.979	0	0	0	0	0	0	2.181	-39.5963	122728.3986	155212.1184
GW	Small	Mid	Pressure	45000	haz	Annual O&M	21.865	0	0	0	0	0	0	698992.175	-484951.1709	252768.5712	4938.7754
GW	Medium	Mid	Pressure	45000	haz	Annual O&M	33.482	0	0	0	0	0	0	2221.4044	-14653.0322	168544.9848	56052.0861
GW	Large	Mid	Pressure	45000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	241.8644	113897.4831	214642.7825
GW	Small	High	Pressure	45000	haz	Annual O&M	24.33	0	0	0	0	0	0	869714.251	-595396.5428	280739.1672	5949.4919
GW	Medium	High	Pressure	45000	haz	Annual O&M	35.324	0	0	0	0	0	0	1561.1847	-12152.4767	174259.2478	59376.3143
GW	Large	High	Pressure	45000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	312.7756	114780.204	240216.5051
GW	Small	Low	Pressure	50000	haz	Annual O&M	21.605	0	0	0	0	0	0	1078400.583	-696708.3029	266758.4471	4115.1883
GW	Medium	Low	Pressure	50000	haz	Annual O&M	34.171	0	0	0	0	0	0	2203.3087	-14755.626	159745.5173	51982.009
GW	Large	Low	Pressure	50000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	229.6666	106716.1619	212544.6376
GW	Small	Mid	Pressure	50000	haz	Annual O&M	21.865	0	0	0	0	0	0	695771.0923	-479141.9062	242811.6575	4827.8253
GW	Medium	Mid	Pressure	50000	haz	Annual O&M	33.482	0	0	0	0	0	0	2386.7205	-15929.7597	163828.0943	54817.3424
GW	Large	Mid	Pressure	50000	haz	Annual O&M	34.711	0	0	0	0	0	0	2.1607	-25.4067	115012.1689	157567.8858

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	50000	haz	Annual O&M	24.33	0	0	0	0	0	0	866345.0556	-589523.5063	270777.4909	5838.5553
GW	Medium	High	Pressure	50000	haz	Annual O&M	35.324	0	0	0	0	0	0	1724.7951	-13420.145	169534.8175	58141.6034
GW	Large	High	Pressure	50000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	312.5546	107368.0533	240102.0653
GW	Small	Low	Pressure	55000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	55000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	55000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	55000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	55000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	55000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	55000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	55000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	55000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	60000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	60000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	60000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	60000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	60000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	60000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	60000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	60000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	60000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	65000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	65000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	65000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	65000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	65000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	65000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	65000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	65000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	65000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	70000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	70000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	70000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	70000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	70000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	70000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
GW	Small	High	Pressure	70000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	70000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	70000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	75000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
GW	Medium	Low	Pressure	75000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
GW	Large	Low	Pressure	75000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
GW	Small	Mid	Pressure	75000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
GW	Medium	Mid	Pressure	75000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
GW	Large	Mid	Pressure	75000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	75000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
GW	Medium	High	Pressure	75000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
GW	Large	High	Pressure	75000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
GW	Small	Low	Pressure	55000	haz	Annual O&M	21.605	0	0	0	0	0	0	1075515.641	-692112.1552	258595.8439	4024.6782
GW	Medium	Low	Pressure	55000	haz	Annual O&M	34.171	0	0	0	0	0	0	2396.8344	-16288.149	157037.703	50384.589
GW	Large	Low	Pressure	55000	haz	Annual O&M	35.979	0	0	0	0	0	0	2.1742	-39.2415	109232.4883	155129.4071
GW	Small	Mid	Pressure	55000	haz	Annual O&M	21.865	0	0	0	0	0	0	693299.4201	-474752.2609	234673.9645	4736.6583
GW	Medium	Mid	Pressure	55000	haz	Annual O&M	33.482	0	0	0	0	0	0	2580.0342	-17460.6307	161116.4324	53221.9092
GW	Large	Mid	Pressure	55000	haz	Annual O&M	34.711	0	0	0	0	0	0	2.1579	-25.2659	108938.88	157532.2266
GW	Small	High	Pressure	55000	haz	Annual O&M	24.33	0	0	0	0	0	0	863752.9907	-585061.296	262628.2431	5747.7697
GW	Medium	High	Pressure	55000	haz	Annual O&M	35.324	0	0	0	0	0	0	1916.7185	-14943.7378	166817.5799	56545.5598
GW	Large	High	Pressure	55000	haz	Annual O&M	35.642	0	0	0	0	0	0	2.4529	9.2394	110980.573	175365.676
GW	Small	Low	Pressure	60000	haz	Annual O&M	21.605	0	0	0	0	0	0	1073308.67	-688554.8895	251796.0847	3949.3629
GW	Medium	Low	Pressure	60000	haz	Annual O&M	34.171	0	0	0	0	0	0	2551.1818	-17523.5722	154742.4822	48993.0812
GW	Large	Low	Pressure	60000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	229.2626	95604.2888	212327.7746
GW	Small	Mid	Pressure	60000	haz	Annual O&M	21.865	0	0	0	0	0	0	691038.1543	-471164.7043	227869.8097	4661.4595
GW	Medium	Mid	Pressure	60000	haz	Annual O&M	33.482	0	0	0	0	0	0	2734.2339	-18694.8488	158818.4998	51831.6247
GW	Large	Mid	Pressure	60000	haz	Annual O&M	34.711	0	0	0	0	0	0	2.1555	-25.1488	103877.8418	157501.7994
GW	Small	High	Pressure	60000	haz	Annual O&M	24.33	0	0	0	0	0	0	861848.6207	-581690.0709	255857.8485	5671.569
GW	Medium	High	Pressure	60000	haz	Annual O&M	35.324	0	0	0	0	0	0	2069.7629	-16171.8988	164514.9368	55154.9051
GW	Large	High	Pressure	60000	haz	Annual O&M	35.642	0	0	0	0	0	0	2.451	9.3265	105919.2395	175338.3943
GW	Small	Low	Pressure	65000	haz	Annual O&M	21.605	0	0	0	0	0	0	1071743.115	-685844.0678	246063.8973	3884.8817
GW	Medium	Low	Pressure	65000	haz	Annual O&M	34.171	0	0	0	0	0	0	2659.0441	-18396.1353	152457.752	47902.3891
GW	Large	Low	Pressure	65000	haz	Annual O&M	35.979	0	0	0	0	0	0	2.1695	-38.9958	99889.1588	155072.3305
GW	Small	Mid	Pressure	65000	haz	Annual O&M	21.865	0	0	0	0	0	0	689263.914	-468367.6915	222130.3133	4597.2236
GW	Medium	Mid	Pressure	65000	haz	Annual O&M	33.482	0	0	0	0	0	0	2842.0031	-19566.5392	156531.4821	50742.0732
GW	Large	Mid	Pressure	65000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	241.0855	91099.5221	214228.9703
GW	Small	High	Pressure	65000	haz	Annual O&M	24.33	0	0	0	0	0	0	859811.9176	-578721.3285	250088.1805	5608.0875
GW	Medium	High	Pressure	65000	haz	Annual O&M	35.324	0	0	0	0	0	0	2176.4972	-17038.0233	162222.7943	54065.9791
GW	Large	High	Pressure	65000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	312.095	91973.6221	239864.0016
GW	Small	Low	Pressure	70000	haz	Annual O&M	21.605	0	0	0	0	0	0	1070021.56	-683428.5497	241122.7437	3830.2835
GW	Medium	Low	Pressure	70000	haz	Annual O&M	34.171	0	0	0	0	0	0	2734.2814	-19013.0776	150239.138	47034.6904
GW	Large	Low	Pressure	70000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	228.9738	87667.2478	212172.6554
GW	Small	Mid	Pressure	70000	haz	Annual O&M	21.865	0	0	0	0	0	0	687715.4419	-466021.8537	217194.5419	4542.6289
GW	Medium	Mid	Pressure	70000	haz	Annual O&M	33.482	0	0	0	0	0	0	2917.1851	-20183.1488	154312.1986	49874.6058
GW	Large	Mid	Pressure	70000	haz	Annual O&M	34.711	0	0	0	0	0	0	2.1518	-24.9642	95924.7173	157454.9004
GW	Small	High	Pressure	70000	haz	Annual O&M	24.33	0	0	0	0	0	0	858466.1508	-576498.7779	245172.2671	5553.0164
GW	Medium	High	Pressure	70000	haz	Annual O&M	35.324	0	0	0	0	0	0	2250.9296	-17650.8327	160001.2786	53197.4986
GW	Large	High	Pressure	70000	haz	Annual O&M	35.642	0	0	0	0	0	0	2.448	9.4625	97965.7632	175294.9723
GW	Small	Low	Pressure	75000	haz	Annual O&M	21.605	0	0	0	0	0	0	1068823.161	-681555.232	236859.0566	3782.5948
GW	Medium	Low	Pressure	75000	haz	Annual O&M	34.171	0	0	0	0	0	0	2796.4715	-19546.0465	148377.3514	46210.5023
GW	Large	Low	Pressure	75000	haz	Annual O&M	35.979	0	0	0	0	0	0	2.166	-38.8151	93037.3837	155030.2859
GW	Small	Mid	Pressure	75000	haz	Annual O&M	21.865	0	0	0	0	0	0	686549.9831	-464173.0724	212934.0728	4494.8488
GW	Medium	Mid	Pressure	75000	haz	Annual O&M	33.482	0	0	0	0	0	0	2979.2482	-20715.0917	152448.0697	49051.58
GW	Large	Mid	Pressure	75000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	240.8516	84260.1517	214104.8537

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	Pressure	75000	haz	Annual O&M	24.33	0	0	0	0	0	0	857117.2271	-574550.5218	240897.9619	5505.635
GW	Medium	High	Pressure	75000	haz	Annual O&M	35.324	0	0	0	0	0	0	2312.2738	-18179.062	158134.6934	52373.7192
GW	Large	High	Pressure	75000	haz	Annual O&M	35.642	0	0	0	0	0	0	2.4468	9.5181	94784.3396	175277.9677
SW	Small	Low	Pressure	5000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	5000	haz	Total Capital	34.165	0	0	0	0	0	0	-2204.6567	23830.3241	793506.3115	1504948.47
SW	Large	Low	Pressure	5000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5738	-476.4487	581178.4286	3451620.657
SW	Small	Mid	Pressure	5000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	5000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	5000	haz	Total Capital	34.7	0	0	0	0	0	0	10.1298	-237.2104	642538.8427	4627318.984
SW	Small	High	Pressure	5000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	5000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	5000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3087	-748.0259	900892.6186	6851542.74
SW	Small	Low	Pressure	10000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	10000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	10000	haz	Total Capital	35.979	0	0	0	0	0	0	8.6145	-486.9148	581757.9749	3444717.259
SW	Small	Mid	Pressure	10000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	10000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	10000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1705	-247.6765	643118.3891	4620415.585
SW	Small	High	Pressure	10000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	10000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	10000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3483	-758.2982	901463.688	6844725.123
SW	Small	Low	Pressure	15000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	15000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	15000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	15000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	15000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	15000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	15000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	15000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	15000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	20000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	20000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	20000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	20000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	20000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	20000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	20000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	20000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	20000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	25000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	25000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	25000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	25000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	25000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	25000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	25000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	25000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	25000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	5000	haz	Annual O&M	21.605	0	0	0	0	0	0	2890926.402	-1670769.014	956710.8322	16629.4625
SW	Medium	Low	Pressure	5000	haz	Annual O&M	34.165	0	0	0	0	0	0	4929.6376	-31983.6205	799889.4083	42534.8851
SW	Large	Low	Pressure	5000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	221.0659	714369.4437	220811.0287
SW	Small	Mid	Pressure	5000	haz	Annual O&M	21.865	0	0	0	0	0	0	2532635.499	-1459462.205	932043.4326	17400.6598
SW	Medium	Mid	Pressure	5000	haz	Annual O&M	33.482	0	0	0	0	0	0	5194.9748	-33526.0301	804674.9625	45081.0048
SW	Large	Mid	Pressure	5000	haz	Annual O&M	34.7	0	0	0	0	0	0	0	232.5375	714306.0752	221600.1435
SW	Small	High	Pressure	5000	haz	Annual O&M	24.33	0	0	0	0	0	0	2685714.58	-1560847.612	958955.2788	18356.132
SW	Medium	High	Pressure	5000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	0	750295.6461	76080.7752
SW	Large	High	Pressure	5000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	303.7888	716042.0219	243517.3907
SW	Small	Low	Pressure	10000	haz	Annual O&M	21.605	0	0	0	0	0	0	2019366.736	-1372032.785	634940.6118	8390.8391
SW	Medium	Low	Pressure	10000	haz	Annual O&M	34.171	0	0	0	0	0	0	3819.1009	-24101.7936	451592.7703	40990.8607
SW	Large	Low	Pressure	10000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	208.3377	380985.7991	215233.19
SW	Small	Mid	Pressure	10000	haz	Annual O&M	21.865	0	0	0	0	0	0	1664210.968	-1162418.922	610476.6453	9160.6073
SW	Medium	Mid	Pressure	10000	haz	Annual O&M	33.482	0	0	0	0	0	0	4089.3901	-25663.1268	456358.4549	43559.9785
SW	Large	Mid	Pressure	10000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	220.5709	380860.5644	216411.1249
SW	Small	High	Pressure	10000	haz	Annual O&M	24.33	0	0	0	0	0	0	1817408.027	-1263901.629	637397.7058	10115.863
SW	Medium	High	Pressure	10000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	-1724.1421	424759.679	62767.5285
SW	Large	High	Pressure	10000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	293.3462	382472.6998	239107.0445
SW	Small	Low	Pressure	15000	haz	Annual O&M	21.605	0	0	0	0	0	0	1075855.772	-841832.2426	464424.0859	6787.1082
SW	Medium	Low	Pressure	15000	haz	Annual O&M	34.171	0	0	0	0	0	0	3202.7614	-19659.3262	331558.2597	42741.2435
SW	Large	Low	Pressure	15000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	204.0949	269857.9315	213373.5803
SW	Small	Mid	Pressure	15000	haz	Annual O&M	21.865	0	0	0	0	0	0	721729.6563	-632772.5865	440026.3297	7556.488
SW	Medium	Mid	Pressure	15000	haz	Annual O&M	33.482	0	0	0	0	0	0	3469.7484	-21195.9149	336268.8414	45336.4075
SW	Large	Mid	Pressure	15000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	216.582	269712.0631	214681.3858
SW	Small	High	Pressure	15000	haz	Annual O&M	24.33	0	0	0	0	0	0	874986.8192	-734316.2616	466959.2727	8511.4242
SW	Medium	High	Pressure	15000	haz	Annual O&M	35.324	0	0	0	0	0	0	2379.5739	-16756.3053	339936.2909	49384.6496
SW	Large	High	Pressure	15000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	289.8654	271282.914	237637.1565
SW	Small	Low	Pressure	20000	haz	Annual O&M	21.605	0	0	0	0	0	0	1023546.939	-747267.0123	390780.7556	5785.9255
SW	Medium	Low	Pressure	20000	haz	Annual O&M	34.171	0	0	0	0	0	0	2466.936	-14221.7036	264346.2365	48039.167
SW	Large	Low	Pressure	20000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	201.9738	214293.9674	212444.4452
SW	Small	Mid	Pressure	20000	haz	Annual O&M	21.865	0	0	0	0	0	0	670002.4158	-538524.6035	366425.3494	6554.621
SW	Medium	Mid	Pressure	20000	haz	Annual O&M	33.482	0	0	0	0	0	0	2732.2733	-15745.9421	269029.4726	50647.2651
SW	Large	Mid	Pressure	20000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	214.5879	214137.7846	213816.6608
SW	Small	High	Pressure	20000	haz	Annual O&M	24.33	0	0	0	0	0	0	823164.8135	-639985.2779	393336.8626	7510.3042
SW	Medium	High	Pressure	20000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	0	250891.2807	64575.8752
SW	Large	High	Pressure	20000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	288.1247	215688.0524	236901.686
SW	Small	Low	Pressure	25000	haz	Annual O&M	21.605	0	0	0	0	0	0	1000038.313	-701714.3863	346559.4451	5185.6192
SW	Medium	Low	Pressure	25000	haz	Annual O&M	34.171	0	0	0	0	0	0	2103.8421	-11450.1471	224765.5493	51179.5438
SW	Large	Low	Pressure	25000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	200.7009	180955.6073	211886.5957
SW	Small	Mid	Pressure	25000	haz	Annual O&M	21.865	0	0	0	0	0	0	646618.5232	-493042.1035	322209.0159	5954.6807
SW	Medium	Mid	Pressure	25000	haz	Annual O&M	33.482	0	0	0	0	0	0	2368.3564	-12967.7543	229432.8491	53795.3041
SW	Large	Mid	Pressure	25000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	213.3914	180793.2197	213298.1493

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	25000	haz	Annual O&M	24.33	0	0	0	0	0	0	799783.5367	-594538.5988	349131.2948	6909.938
SW	Medium	High	Pressure	25000	haz	Annual O&M	35.324	0	0	0	0	0	0	0	0	217242.7092	64826.5446
SW	Large	High	Pressure	25000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	287.0805	182331.1243	236460.6054
SW	Small	Low	Pressure	30000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	30000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	30000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	30000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	30000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	30000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	30000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	30000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	30000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	35000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	35000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	35000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	35000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	35000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	35000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	35000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	35000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	35000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	40000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	40000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	40000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	40000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	40000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	40000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	40000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	40000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	40000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	45000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	45000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	45000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	45000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	45000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	45000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	45000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	45000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	45000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	50000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	50000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	50000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	50000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	50000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	50000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	50000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	50000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	50000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	30000	haz	Annual O&M	21.605	0	0	0	0	0	0	986869.2019	-675992.3584	317062.7512	4785.9369
SW	Medium	Low	Pressure	30000	haz	Annual O&M	34.171	0	0	0	0	0	0	2113.6374	-11286.1063	201355.7255	52445.103
SW	Large	Low	Pressure	30000	haz	Annual O&M	35.979	0	0	0	0	0	0	3.1071	-157.8156	169292.5148	147628.3044
SW	Small	Mid	Pressure	30000	haz	Annual O&M	21.865	0	0	0	0	0	0	633906.7037	-467560.0613	292741.8788	5554.3607
SW	Medium	Mid	Pressure	30000	haz	Annual O&M	33.482	0	0	0	0	0	0	2377.366	-12797.9694	206010.7635	55066.3453
SW	Large	Mid	Pressure	30000	haz	Annual O&M	34.711	0	0	0	0	0	0	3.0548	-139.0496	168948.0618	150142.2971
SW	Small	High	Pressure	30000	haz	Annual O&M	24.33	0	0	0	0	0	0	787081.0177	-569048.1749	319660.9646	6509.7182
SW	Medium	High	Pressure	30000	haz	Annual O&M	35.324	0	0	0	0	0	0	1251.2875	-8180.5148	209522.1061	59125.8332
SW	Large	High	Pressure	30000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	286.3842	160093.1637	236166.7669
SW	Small	Low	Pressure	35000	haz	Annual O&M	21.605	0	0	0	0	0	0	978856.237	-660094.0225	296011.9364	4499.4376
SW	Medium	Low	Pressure	35000	haz	Annual O&M	34.171	0	0	0	0	0	0	2278.2451	-12276.927	186807.5069	52425.1561
SW	Large	Low	Pressure	35000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	199.2463	142854.6166	211249.0464
SW	Small	Mid	Pressure	35000	haz	Annual O&M	21.865	0	0	0	0	0	0	625847.5558	-451650.4404	271691.1889	5268.1248
SW	Medium	Mid	Pressure	35000	haz	Annual O&M	33.482	0	0	0	0	0	0	2541.6061	-13785.9422	191455.7972	55049.9154
SW	Large	Mid	Pressure	35000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	212.0239	142685.1476	212705.3888
SW	Small	High	Pressure	35000	haz	Annual O&M	24.33	0	0	0	0	0	0	779110.2715	-553181.2539	298612.7971	6223.6016
SW	Medium	High	Pressure	35000	haz	Annual O&M	35.324	0	0	0	0	0	0	1410.133	-9141.2771	194941.5394	59112.1271
SW	Large	High	Pressure	35000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	285.887	144208.9135	235956.5428
SW	Small	Low	Pressure	40000	haz	Annual O&M	21.605	0	0	0	0	0	0	973281.1373	-649373.6409	280204.474	4285.7078
SW	Medium	Low	Pressure	40000	haz	Annual O&M	34.171	0	0	0	0	0	0	2510.2309	-13816.9867	177578.0054	51549.1067
SW	Large	Low	Pressure	40000	haz	Annual O&M	35.979	0	0	0	0	0	0	3.0944	-157.4074	141467.1487	147426.0405
SW	Small	Mid	Pressure	40000	haz	Annual O&M	21.865	0	0	0	0	0	0	620498.1994	-441039.6389	255895.2922	5054.2087
SW	Medium	Mid	Pressure	40000	haz	Annual O&M	33.482	0	0	0	0	0	0	2773.1589	-15322.8765	182219.6537	54176.8164
SW	Large	Mid	Pressure	40000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	211.5965	130776.3909	212519.7663
SW	Small	High	Pressure	40000	haz	Annual O&M	24.33	0	0	0	0	0	0	773720.0047	-542562.373	282819.9726	6009.4074
SW	Medium	High	Pressure	40000	haz	Annual O&M	35.324	0	0	0	0	0	0	1637.9059	-10659.5942	185689.357	58240.1381
SW	Large	High	Pressure	40000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	285.5143	132295.7057	235799.1894
SW	Small	Low	Pressure	45000	haz	Annual O&M	21.605	0	0	0	0	0	0	969188.2219	-641785.4522	267911.5758	4119.0252
SW	Medium	Low	Pressure	45000	haz	Annual O&M	34.171	0	0	0	0	0	0	2802.9337	-15849.1183	172169.2986	49994.1316
SW	Large	Low	Pressure	45000	haz	Annual O&M	35.979	0	0	0	0	0	0	3.0902	-157.2758	132192.1589	147357.856
SW	Small	Mid	Pressure	45000	haz	Annual O&M	21.865	0	0	0	0	0	0	616531.5626	-433525.6869	243614.5333	4887.1181
SW	Medium	Mid	Pressure	45000	haz	Annual O&M	33.482	0	0	0	0	0	0	3065.6836	-17353.2976	176806.3348	52624.3419
SW	Large	Mid	Pressure	45000	haz	Annual O&M	34.711	0	0	0	0	0	0	3.0393	-138.5947	131845.8898	149883.9721
SW	Small	High	Pressure	45000	haz	Annual O&M	24.33	0	0	0	0	0	0	769840.61	-535090.874	270543.198	5842.3218
SW	Medium	High	Pressure	45000	haz	Annual O&M	35.324	0	0	0	0	0	0	1927.3526	-12674.9055	180263.1488	56688.1915
SW	Large	High	Pressure	45000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	285.224	123029.9063	235676.5093
SW	Small	Low	Pressure	50000	haz	Annual O&M	21.605	0	0	0	0	0	0	966212.2017	-636278.384	258089.519	3985.4487
SW	Medium	Low	Pressure	50000	haz	Annual O&M	34.171	0	0	0	0	0	0	3063.5142	-17699.2944	168407.3354	48376.4542
SW	Large	Low	Pressure	50000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	198.1551	114278.8914	210770.7357
SW	Small	Mid	Pressure	50000	haz	Annual O&M	21.865	0	0	0	0	0	0	613543.3051	-428003.6619	233787.4532	4753.9807
SW	Medium	Mid	Pressure	50000	haz	Annual O&M	33.482	0	0	0	0	0	0	3326.0389	-19201.9666	173041.3544	51007.7675
SW	Large	Mid	Pressure	50000	haz	Annual O&M	34.711	0	0	0	0	0	0	3.0362	-138.5055	124425.4834	149832.3021

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	50000	haz	Annual O&M	24.33	0	0	0	0	0	0	766669.1461	-529476.1454	260704.5452	5709.2522
SW	Medium	High	Pressure	50000	haz	Annual O&M	35.324	0	0	0	0	0	0	2185.4553	-14512.3438	176488.2952	55072.377
SW	Large	High	Pressure	50000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	284.9919	115617.255	235578.6756
SW	Small	Low	Pressure	55000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	55000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	55000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	55000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	55000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	55000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	55000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	55000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	55000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	60000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	60000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	60000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	60000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	60000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	60000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	60000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	60000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	60000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	65000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	65000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	65000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	65000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	65000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	65000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	65000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	65000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	65000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	70000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	70000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	70000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	70000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	70000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	70000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279
SW	Small	High	Pressure	70000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	70000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	70000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	75000	haz	Total Capital	21.605	0	0	0	0	0	0	218205.7779	-879696.1705	1619582.503	149347.4904
SW	Medium	Low	Pressure	75000	haz	Total Capital	34.171	0	0	0	0	0	0	-2241.9665	24429.1255	791060.0658	1507435.754
SW	Large	Low	Pressure	75000	haz	Total Capital	35.979	0	0	0	0	0	0	8.5711	-478.1422	581291.6818	3450337.952
SW	Small	Mid	Pressure	75000	haz	Total Capital	21.865	1300023.414	0.4864	0	0	0	0	0	0	0	0
SW	Medium	Mid	Pressure	75000	haz	Total Capital	33.482	0	0	0	0	0	0	-3706.0774	39849.5823	913457.546	1835718.028
SW	Large	Mid	Pressure	75000	haz	Total Capital	34.711	0	0	0	0	0	0	10.1271	-238.9039	642652.0959	4626036.279

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	75000	haz	Total Capital	24.33	0	0	0	0	0	0	906888.8213	-2194035.54	2716802.713	377083.5384
SW	Medium	High	Pressure	75000	haz	Total Capital	35.324	0	0	0	0	0	0	-8214.9816	97767.571	1153481.446	2550759.106
SW	Large	High	Pressure	75000	haz	Total Capital	35.642	0	0	0	0	0	0	21.3034	-749.1992	900980.0398	6850555.015
SW	Small	Low	Pressure	55000	haz	Annual O&M	21.605	0	0	0	0	0	0	963767.8412	-632020.7847	250041.0491	3876.4248
SW	Medium	Low	Pressure	55000	haz	Annual O&M	34.171	0	0	0	0	0	0	3336.3605	-19675.8926	166355.8921	46531.7191
SW	Large	Low	Pressure	55000	haz	Annual O&M	35.979	0	0	0	0	0	0	3.084	-157.0782	118701.0923	147259.6674
SW	Small	Mid	Pressure	55000	haz	Annual O&M	21.865	0	0	0	0	0	0	611075.8724	-423739.0678	225738.2937	4645.0162
SW	Medium	Mid	Pressure	55000	haz	Annual O&M	33.482	0	0	0	0	0	0	3598.618	-21176.5874	170985.7551	49165.0171
SW	Large	Mid	Pressure	55000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	210.7808	108041.4559	212166.0538
SW	Small	High	Pressure	55000	haz	Annual O&M	24.33	0	0	0	0	0	0	764497.1217	-525361.468	252674.1438	5599.9552
SW	Medium	High	Pressure	55000	haz	Annual O&M	35.324	0	0	0	0	0	0	2456.0581	-16477.1153	174423.7373	53230.4908
SW	Large	High	Pressure	55000	haz	Annual O&M	35.642	0	0	0	0	0	0	3.2659	-91.1444	120654.6075	168347.3055
SW	Small	Low	Pressure	60000	haz	Annual O&M	21.605	0	0	0	0	0	0	961783.4013	-628705.0085	243337.9145	3785.5637
SW	Medium	Low	Pressure	60000	haz	Annual O&M	34.171	0	0	0	0	0	0	3522.784	-21040.1066	164130.0309	45127.8597
SW	Large	Low	Pressure	60000	haz	Annual O&M	35.979	0	0	0	0	0	0	0	197.7308	103166.1062	210584.9877
SW	Small	Mid	Pressure	60000	haz	Annual O&M	21.865	0	0	0	0	0	0	609315.5293	-420547.7401	219053.4562	4553.4736
SW	Medium	Mid	Pressure	60000	haz	Annual O&M	33.482	0	0	0	0	0	0	3784.7942	-22539.1289	168756.516	47762.8022
SW	Large	Mid	Pressure	60000	haz	Annual O&M	34.711	0	0	0	0	0	0	3.0315	-138.3687	113294.8012	149755.1487
SW	Small	High	Pressure	60000	haz	Annual O&M	24.33	0	0	0	0	0	0	762611.2107	-522085.8239	245972.9061	5509.2068
SW	Medium	High	Pressure	60000	haz	Annual O&M	35.324	0	0	0	0	0	0	2640.6431	-17832.105	172189.0703	51827.6361
SW	Large	High	Pressure	60000	haz	Annual O&M	35.642	0	0	0	0	0	0	3.2642	-91.1078	115594.7666	168315.6357
SW	Small	Low	Pressure	65000	haz	Annual O&M	21.605	0	0	0	0	0	0	960135.4373	-626021.5858	237657.8204	3708.7404
SW	Medium	Low	Pressure	65000	haz	Annual O&M	34.171	0	0	0	0	0	0	3650.15	-21984.7006	161863.8582	44039.9406
SW	Large	Low	Pressure	65000	haz	Annual O&M	35.979	0	0	0	0	0	0	3.0797	-156.9425	109361.1719	147191.0892
SW	Small	Mid	Pressure	65000	haz	Annual O&M	21.865	0	0	0	0	0	0	607556.9523	-417810.0117	213365.0682	4477.1505
SW	Medium	Mid	Pressure	65000	haz	Annual O&M	33.482	0	0	0	0	0	0	3912.1813	-23483.6765	166489.8108	46674.9609
SW	Large	Mid	Pressure	65000	haz	Annual O&M	34.711	0	0	0	0	0	0	0	210.4457	98714.3291	212020.8786
SW	Small	High	Pressure	65000	haz	Annual O&M	24.33	0	0	0	0	0	0	761053.4143	-519472.6105	240305.7888	5432.1176
SW	Medium	High	Pressure	65000	haz	Annual O&M	35.324	0	0	0	0	0	0	2766.5165	-18768.8194	169914.1223	50741.5143
SW	Large	High	Pressure	65000	haz	Annual O&M	35.642	0	0	0	0	0	0	3.2628	-91.0763	111313.3621	168288.422
SW	Small	Low	Pressure	70000	haz	Annual O&M	21.605	0	0	0	0	0	0	958787.5976	-623871.8389	232795.7258	3642.9355
SW	Medium	Low	Pressure	70000	haz	Annual O&M	34.171	0	0	0	0	0	0	3749.3399	-22754.8195	159928.244	43047.1421
SW	Large	Low	Pressure	70000	haz	Annual O&M	35.979	0	0	0	0	0	0	3.078	-156.886	105691.8112	147165.0078
SW	Small	Mid	Pressure	70000	haz	Annual O&M	21.865	0	0	0	0	0	0	606341.7162	-415725.1036	208509.8501	4411.2676
SW	Medium	Mid	Pressure	70000	haz	Annual O&M	33.482	0	0	0	0	0	0	4011.324	-24253.2956	164552.7432	45683.0346
SW	Large	Mid	Pressure	70000	haz	Annual O&M	34.711	0	0	0	0	0	0	3.0282	-138.272	105344.3711	149699.5207
SW	Small	High	Pressure	70000	haz	Annual O&M	24.33	0	0	0	0	0	0	759623.94	-517283.9302	235438.2792	5366.4686
SW	Medium	High	Pressure	70000	haz	Annual O&M	35.324	0	0	0	0	0	0	2864.5197	-19532.8815	167972.5947	49749.4955
SW	Large	High	Pressure	70000	haz	Annual O&M	35.642	0	0	0	0	0	0	0	284.3956	96556.1183	235326.9234
SW	Small	Low	Pressure	75000	haz	Annual O&M	21.605	0	0	0	0	0	0	957710.6467	-622138.859	228589.2907	3585.4977
SW	Medium	Low	Pressure	75000	haz	Annual O&M	34.171	0	0	0	0	0	0	3852.2364	-23617.3076	158817.4489	41881.607
SW	Large	Low	Pressure	75000	haz	Annual O&M	35.979	0	0	0	0	0	0	3.0765	-156.8393	102511.7662	147141.9184
SW	Small	Mid	Pressure	75000	haz	Annual O&M	21.865	0	0	0	0	0	0	605239.6298	-413976.8568	204302.4117	4353.8888
SW	Medium	Mid	Pressure	75000	haz	Annual O&M	33.482	0	0	0	0	0	0	4113.876	-25113.4517	163437.594	44519.3666
SW	Large	Mid	Pressure	75000	haz	Annual O&M	34.711	0	0	0	0	0	0	3.0269	-138.2329	102164.1469	149678.0902

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Pressure	75000	haz	Annual O&M	24.33	0	0	0	0	0	0	758522.8602	-515534.8091	231228.6167	5309.2146
SW	Medium	High	Pressure	75000	haz	Annual O&M	35.324	0	0	0	0	0	0	2966.0938	-20388.3053	166853.6582	48585.6621
SW	Large	High	Pressure	75000	haz	Annual O&M	35.642	0	0	0	0	0	0	3.2605	-91.0247	104463.0547	168245.6235
SW	Small	Low	Gravity	5000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	5000	haz	Total Capital	34.318	0	0	0	0	0	0	2305.6323	-47510.7565	970665.0402	1507746.82
SW	Large	Low	Gravity	5000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	5000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	5000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	5000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	5000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	5000	haz	Total Capital	34.953	0	0	0	0	0	0	1733.4111	-39746.9636	1086122.427	2021702.383
SW	Large	High	Gravity	5000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	10000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	10000	haz	Total Capital	34.318	0	0	0	0	0	0	2305.6323	-47510.7565	970665.0402	1507746.82
SW	Large	Low	Gravity	10000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	10000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	10000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	10000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	10000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	10000	haz	Total Capital	34.947	0	0	0	0	0	0	1710.5042	-39314.9705	1084128.094	2023881.676
SW	Large	High	Gravity	10000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	15000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	15000	haz	Total Capital	34.318	0	0	0	0	0	0	2305.6323	-47510.7565	970665.0402	1507746.82
SW	Large	Low	Gravity	15000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	15000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	15000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	15000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	15000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	15000	haz	Total Capital	34.947	0	0	0	0	0	0	1710.5042	-39314.9705	1084128.094	2023881.676
SW	Large	High	Gravity	15000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	20000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	20000	haz	Total Capital	34.318	0	0	0	0	0	0	2305.6323	-47510.7565	970665.0402	1507746.82
SW	Large	Low	Gravity	20000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	20000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	20000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	20000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	20000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	20000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	20000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	25000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	25000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	25000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	25000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	25000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	25000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	25000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	25000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	25000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	5000	haz	Annual O&M	30.19	0	0	0	0	0	0	1430890.047	-607724.481	790430.8213	33781.7538
SW	Medium	Low	Gravity	5000	haz	Annual O&M	34.318	0	0	0	0	0	0	3900.0251	-28227.7788	790146.1782	55129.5735
SW	Large	Low	Gravity	5000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	0	711199.4198	270134.9983
SW	Small	Mid	Gravity	5000	haz	Annual O&M	29.295	0	0	0	0	0	0	1346987.762	-542189.6111	785872.9296	38574.7787
SW	Medium	Mid	Gravity	5000	haz	Annual O&M	33.771	0	0	0	0	0	0	3855.0968	-28100.9759	793659.5509	58387.2114
SW	Large	Mid	Gravity	5000	haz	Annual O&M	35.7	0	0	0	0	0	0	0	0	711552.5541	264208.9841
SW	Small	High	Gravity	5000	haz	Annual O&M	31.24	0	0	0	0	0	0	1335162.41	-528214.2694	788917.2038	40467.3302
SW	Medium	High	Gravity	5000	haz	Annual O&M	34.953	0	0	0	0	0	0	3578.0134	-26343.2737	790593.5323	59809.8904
SW	Large	High	Gravity	5000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	0	712099.7813	262005.3046
SW	Small	Low	Gravity	10000	haz	Annual O&M	30.19	0	0	0	0	0	0	417681.0738	-271908.3328	460833.1774	29543.3928
SW	Medium	Low	Gravity	10000	haz	Annual O&M	34.318	0	0	0	0	0	0	0	0	400879.427	74115.9984
SW	Large	Low	Gravity	10000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	0	377936.3502	266007.9695
SW	Small	Mid	Gravity	10000	haz	Annual O&M	29.295	0	0	0	0	0	0	0	-31106.6477	433217.7308	34891.0934
SW	Medium	Mid	Gravity	10000	haz	Annual O&M	33.771	0	0	0	0	0	0	0	0	404200.0209	77576.1303
SW	Large	Mid	Gravity	10000	haz	Annual O&M	35.7	0	0	0	0	0	0	0	0	378274.4814	260645.316
SW	Small	High	Gravity	10000	haz	Annual O&M	31.24	0	0	0	0	0	0	320653.6944	-191936.3269	459228.79	36231.0225
SW	Medium	High	Gravity	10000	haz	Annual O&M	34.947	0	0	0	0	0	0	2045.5686	-16331.3178	440193.7569	59861.3858
SW	Large	High	Gravity	10000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	0	378820.1876	257886.9068
SW	Small	Low	Gravity	15000	haz	Annual O&M	30.19	0	0	0	0	0	0	-572923.2279	270587.5938	287716.7552	29272.7914
SW	Medium	Low	Gravity	15000	haz	Annual O&M	34.318	0	0	0	0	0	0	1742.9522	-13695.2371	320074.6439	57079.7327
SW	Large	Low	Gravity	15000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	-64.5206	271655.64	216828.7558
SW	Small	Mid	Gravity	15000	haz	Annual O&M	29.295	0	0	0	0	0	0	-658019.7952	336510.9611	283085.4427	34067.6325
SW	Medium	Mid	Gravity	15000	haz	Annual O&M	33.771	0	0	0	0	0	0	1720.9617	-13656.3651	323538.6312	60386.8618
SW	Large	Mid	Gravity	15000	haz	Annual O&M	35.7	0	0	0	0	0	0	0	0	267181.7865	259457.4779
SW	Small	High	Gravity	15000	haz	Annual O&M	31.24	0	0	0	0	0	0	-670018.8695	350515.7455	286110.8822	35960.2387
SW	Medium	High	Gravity	15000	haz	Annual O&M	34.947	0	0	0	0	0	0	0	-2815.7091	304410.8133	68582.8542
SW	Large	High	Gravity	15000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	0	267726.9961	256513.9085
SW	Small	Low	Gravity	20000	haz	Annual O&M	30.19	0	0	0	0	0	0	-648968.2182	371417.8195	212754.4958	28938.7052
SW	Medium	Low	Gravity	20000	haz	Annual O&M	34.318	0	0	0	0	0	0	0	-1801.0629	241521.5694	67358.5244
SW	Large	Low	Gravity	20000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1116	-422.8647	226701.686	152040.821
SW	Small	Mid	Gravity	20000	haz	Annual O&M	29.295	0	0	0	0	0	0	-734161.7435	437376.6622	208113.6969	33733.697
SW	Medium	Mid	Gravity	20000	haz	Annual O&M	33.771	0	0	0	0	0	0	0	-1897.3957	245203.5696	70575.7178
SW	Large	Mid	Gravity	20000	haz	Annual O&M	35.7	0	0	0	0	0	0	0	-62.6223	216300.9903	212466.4821
SW	Small	High	Gravity	20000	haz	Annual O&M	31.24	0	0	0	0	0	0	-746239.6027	451406.8775	211136.1843	35626.1863
SW	Medium	High	Gravity	20000	haz	Annual O&M	34.953	0	0	0	0	0	0	0	0	237283.4584	75898.2724
SW	Large	High	Gravity	20000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	-57.8984	216494.0017	212930.3297
SW	Small	Low	Gravity	25000	haz	Annual O&M	30.19	0	0	0	0	0	0	-686686.2807	420685.9188	167751.5742	28738.4701
SW	Medium	Low	Gravity	25000	haz	Annual O&M	34.318	0	0	0	0	0	0	0	-1634.5978	207112.0291	68283.1264
SW	Large	Low	Gravity	25000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1121	-423.0218	193384.4828	151544.1887
SW	Small	Mid	Gravity	25000	haz	Annual O&M	29.295	0	0	0	0	0	0	-772055.9228	486708.4954	163102.4582	33533.6622
SW	Medium	Mid	Gravity	25000	haz	Annual O&M	33.771	0	0	0	0	0	0	0	-1518.7439	210083.2867	71882.5568
SW	Large	Mid	Gravity	25000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.9788	-405.6184	193106.8501	150788.6256

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	25000	haz	Annual O&M	31.24	0	0	0	0	0	0	-784169.9158	500763.7248	166116.2936	35426.6152
SW	Medium	High	Gravity	25000	haz	Annual O&M	34.953	0	0	0	0	0	0	0	-2096.5894	212110.4302	70890.512
SW	Large	High	Gravity	25000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0532	-409.4974	193555.7366	149635.7467
SW	Small	Low	Gravity	30000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	30000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	30000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	30000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	30000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	30000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	30000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	30000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	30000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	35000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	35000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	35000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	35000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	35000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	35000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	35000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	35000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	35000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	40000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	40000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	40000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	40000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	40000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	40000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	40000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	40000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	40000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	45000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	45000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	45000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	45000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	45000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	45000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	45000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	45000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	45000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	50000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	50000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	50000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	50000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	50000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	50000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	50000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	50000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	50000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	30000	haz	Annual O&M	30.19	0	0	0	0	0	0	-709196.2955	448835.512	137736.6189	28605.2837
SW	Medium	Low	Gravity	30000	haz	Annual O&M	34.318	0	0	0	0	0	0	0	-1441.2403	183769.8892	69567.1796
SW	Large	Low	Gravity	30000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	-64.8521	160592.6543	215207.3545
SW	Small	Mid	Gravity	30000	haz	Annual O&M	29.295	0	0	0	0	0	0	-794529.666	514837.4045	133086.5805	33400.6437
SW	Medium	Mid	Gravity	30000	haz	Annual O&M	33.771	0	0	0	0	0	0	0	-1317.3739	186708.9037	73183.7538
SW	Large	Mid	Gravity	30000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.9806	-405.893	170899.4056	150464.5781
SW	Small	High	Gravity	30000	haz	Annual O&M	31.24	0	0	0	0	0	0	-806572.3044	528846.5315	136109.3429	35293.0815
SW	Medium	High	Gravity	30000	haz	Annual O&M	34.953	0	0	0	0	0	0	0	0	181075.798	77040.0261
SW	Large	High	Gravity	30000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0547	-409.7748	171349.594	149257.7323
SW	Small	Low	Gravity	35000	haz	Annual O&M	30.19	0	0	0	0	0	0	-723954.714	466496.1952	116312.5789	28509.4686
SW	Medium	Low	Gravity	35000	haz	Annual O&M	34.318	0	0	0	0	0	0	0	-1389.3427	167430.6551	70348.4185
SW	Large	Low	Gravity	35000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	-64.8993	144726.4983	214975.9265
SW	Small	Mid	Gravity	35000	haz	Annual O&M	29.295	0	0	0	0	0	0	-809435.2463	532569.4971	111652.9968	33304.9954
SW	Medium	Mid	Gravity	35000	haz	Annual O&M	33.771	0	0	0	0	0	0	0	-1259.6444	170346.1251	73977.6576
SW	Large	Mid	Gravity	35000	haz	Annual O&M	35.7	0	0	0	0	0	0	0	-62.8355	144900.1458	211544.7824
SW	Small	High	Gravity	35000	haz	Annual O&M	31.24	0	0	0	0	0	0	-821537.3002	546621.5496	114667.4149	35197.6814
SW	Medium	High	Gravity	35000	haz	Annual O&M	34.953	0	0	0	0	0	0	0	-1821.1465	172272.2837	73037.6901
SW	Large	High	Gravity	35000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	-58.2055	145099.8283	211820.2739
SW	Small	Low	Gravity	40000	haz	Annual O&M	30.19	0	0	0	0	0	0	-734605.5015	478549.7906	100228.0297	28438.1746
SW	Medium	Low	Gravity	40000	haz	Annual O&M	34.318	0	0	0	0	0	0	0	-1443.7247	155591.011	70616.0689
SW	Large	Low	Gravity	40000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	-64.9347	132826.88	214802.3395
SW	Small	Mid	Gravity	40000	haz	Annual O&M	29.295	0	0	0	0	0	0	-820076.7308	544601.9474	95571.4598	33233.5587
SW	Medium	Mid	Gravity	40000	haz	Annual O&M	33.771	0	0	0	0	0	0	0	-1309.7295	158489.2406	74254.2121
SW	Large	Mid	Gravity	40000	haz	Annual O&M	35.7	0	0	0	0	0	0	0	-62.8711	133000.013	211391.159
SW	Small	High	Gravity	40000	haz	Annual O&M	31.24	0	0	0	0	0	0	-832157.1618	558633.0026	98589.2549	35126.2271
SW	Medium	High	Gravity	40000	haz	Annual O&M	34.953	0	0	0	0	0	0	0	-1866.1049	160383.7189	73330.9648
SW	Large	High	Gravity	40000	haz	Annual O&M	36.221	0	0	0	0	0	0	0	-58.2567	133200.7987	211635.3631
SW	Small	Low	Gravity	45000	haz	Annual O&M	30.19	0	0	0	0	0	0	-742541.8574	487108.5107	87726.9115	28382.4104
SW	Medium	Low	Gravity	45000	haz	Annual O&M	34.318	0	0	0	0	0	0	1029.6676	-8268.1208	158859.3801	65365.144
SW	Large	Low	Gravity	45000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.113	-423.3051	134154.052	150660.2181
SW	Small	Mid	Gravity	45000	haz	Annual O&M	29.295	0	0	0	0	0	0	-828098.323	553217.583	83058.7308	33178.3437
SW	Medium	Mid	Gravity	45000	haz	Annual O&M	33.771	0	0	0	0	0	0	1180.4778	-9108.4343	163504.0701	68256.3772
SW	Large	Mid	Gravity	45000	haz	Annual O&M	35.7	0	0	0	0	0	0	0	-62.8989	123744.3568	211271.7521
SW	Small	High	Gravity	45000	haz	Annual O&M	31.24	0	0	0	0	0	0	-840256.9384	567287.2897	86071.7804	35071.1264
SW	Medium	High	Gravity	45000	haz	Annual O&M	34.953	0	0	0	0	0	0	0	-2007.3883	151596.2321	73246.4668
SW	Large	High	Gravity	45000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0573	-410.2336	134339.224	148629.0446
SW	Small	Low	Gravity	50000	haz	Annual O&M	30.19	0	0	0	0	0	0	-748770.3461	493518.6015	77715.3472	28338.3235
SW	Medium	Low	Gravity	50000	haz	Annual O&M	34.318	0	0	0	0	0	0	1281.6919	-10074.3516	155058.9874	63779.2959
SW	Large	Low	Gravity	50000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1131	-423.3374	126750.1484	150550.3987
SW	Small	Mid	Gravity	50000	haz	Annual O&M	29.295	0	0	0	0	0	0	-834286.9579	559570.3028	73061.7484	33133.5255
SW	Medium	Mid	Gravity	50000	haz	Annual O&M	33.771	0	0	0	0	0	0	1434.1383	-10922.5149	159711.5222	66668.7351
SW	Large	Mid	Gravity	50000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.9842	-406.4414	126484.4917	149816.9148

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	50000	haz	Annual O&M	31.24	0	0	0	0	0	0	-846364.3144	573613.9926	76073.8415	35026.3668
SW	Medium	High	Gravity	50000	haz	Annual O&M	34.953	0	0	0	0	0	0	0	-2173.6854	144823.2723	72936.9971
SW	Large	High	Gravity	50000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0579	-410.3248	126937.144	148503.0647
SW	Small	Low	Gravity	55000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	55000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	55000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	55000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	55000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	55000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	55000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	55000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	55000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	60000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	60000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	60000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	60000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	60000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	60000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	60000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	60000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	60000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	65000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	65000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	65000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	65000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	65000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	65000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	65000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	65000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	65000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	70000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	70000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	70000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	70000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	70000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	70000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37
SW	Small	High	Gravity	70000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	70000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	70000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	75000	haz	Total Capital	30.19	0	0	0	0	0	0	-1290650.747	2183545.961	-44745.7357	831220.478
SW	Medium	Low	Gravity	75000	haz	Total Capital	34.318	0	0	0	0	0	0	2438.6353	-49247.0571	976944.1976	1501763.516
SW	Large	Low	Gravity	75000	haz	Total Capital	36.221	0	0	0	0	0	0	6.7058	-2008.5071	656104.6466	2291190.469
SW	Small	Mid	Gravity	75000	haz	Total Capital	29.295	0	0	0	0	0	0	-1076120.098	1802620.601	259930.1507	983021.2525
SW	Medium	Mid	Gravity	75000	haz	Total Capital	33.771	0	0	0	0	0	0	1894.7388	-41884.8618	1029811.453	1874136.517
SW	Large	Mid	Gravity	75000	haz	Total Capital	35.7	0	0	0	0	0	0	6.137	-1786.4645	647268.4015	3787188.37

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	75000	haz	Total Capital	31.24	0	0	0	0	0	0	-850266.0535	1435347.569	498569.2441	1039031.084
SW	Medium	High	Gravity	75000	haz	Total Capital	34.953	0	0	0	0	0	0	1748.1779	-39470.2013	1081870.567	2028101.829
SW	Large	High	Gravity	75000	haz	Total Capital	36.221	0	0	0	0	0	0	6.3666	-2105.3529	726477.3605	3837805.245
SW	Small	Low	Gravity	55000	haz	Annual O&M	30.19	0	0	0	0	0	0	-753826.5767	498462.6422	69522.8939	28302.1371
SW	Medium	Low	Gravity	55000	haz	Annual O&M	34.318	0	0	0	0	0	0	1547.4196	-12014.0256	152973.52	61962.5501
SW	Large	Low	Gravity	55000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1132	-423.366	120692.4695	150460.1927
SW	Small	Mid	Gravity	55000	haz	Annual O&M	29.295	0	0	0	0	0	0	-839264.4939	564486.5963	64869.5053	33097.3735
SW	Medium	Mid	Gravity	55000	haz	Annual O&M	33.771	0	0	0	0	0	0	1701.2723	-12868.9941	157633.2406	64849.7131
SW	Large	Mid	Gravity	55000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.9847	-406.5172	120427.9559	149728.1761
SW	Small	High	Gravity	55000	haz	Annual O&M	31.24	0	0	0	0	0	0	-851373.7293	578523.424	67887.4348	34989.9743
SW	Medium	High	Gravity	55000	haz	Annual O&M	34.953	0	0	0	0	0	0	1160.4777	-9909.5472	153156.0211	66660.7073
SW	Large	High	Gravity	55000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0583	-410.4006	120880.9234	148400.0628
SW	Small	Low	Gravity	60000	haz	Annual O&M	30.19	0	0	0	0	0	0	-757885.6705	502305.5133	62706.9977	28271.5758
SW	Medium	Low	Gravity	60000	haz	Annual O&M	34.318	0	0	0	0	0	0	1727.7584	-13346.696	150718.5671	60581.8019
SW	Large	Low	Gravity	60000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1132	-423.3871	115644.3366	150385.3312
SW	Small	Mid	Gravity	60000	haz	Annual O&M	29.295	0	0	0	0	0	0	-843348.6609	568359.3136	58045.9036	33067.0804
SW	Medium	Mid	Gravity	60000	haz	Annual O&M	33.771	0	0	0	0	0	0	1882.6612	-14206.7284	155383.6335	63467.1506
SW	Large	Mid	Gravity	60000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.9851	-406.5801	115380.8211	149654.5421
SW	Small	High	Gravity	60000	haz	Annual O&M	31.24	0	0	0	0	0	0	-855363.945	582341.5104	61069.546	34959.7398
SW	Medium	High	Gravity	60000	haz	Annual O&M	34.953	0	0	0	0	0	0	1340.358	-11235.0627	150874.3407	65293.2054
SW	Large	High	Gravity	60000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0586	-410.4631	115834.0436	148314.3156
SW	Small	Low	Gravity	65000	haz	Annual O&M	30.19	0	0	0	0	0	0	-761264.4588	505409.1873	56934.6204	28245.9731
SW	Medium	Low	Gravity	65000	haz	Annual O&M	34.318	0	0	0	0	0	0	1850.4101	-14267.3281	148432.4491	59511.4575
SW	Large	Low	Gravity	65000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1133	-423.4124	111373.0331	150320.971
SW	Small	Mid	Gravity	65000	haz	Annual O&M	29.295	0	0	0	0	0	0	-846895.5962	571524.1654	52269.6631	33041.5324
SW	Medium	Mid	Gravity	65000	haz	Annual O&M	33.771	0	0	0	0	0	0	2006.0157	-15130.2946	153099.0901	62396.9941
SW	Large	Mid	Gravity	65000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.9855	-406.6311	111110.0853	149592.9427
SW	Small	High	Gravity	65000	haz	Annual O&M	31.24	0	0	0	0	0	0	-858925.4612	585533.2347	55287.3509	34934.2148
SW	Medium	High	Gravity	65000	haz	Annual O&M	34.953	0	0	0	0	0	0	1462.3373	-12148.0472	148563.0443	64235.5151
SW	Large	High	Gravity	65000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0589	-410.514	111563.5683	148242.149
SW	Small	Low	Gravity	70000	haz	Annual O&M	30.19	0	0	0	0	0	0	-764130.4573	507950.182	51988.3524	28223.9884
SW	Medium	Low	Gravity	70000	haz	Annual O&M	34.318	0	0	0	0	0	0	1945.1833	-15014.2301	146474.3711	58536.2482
SW	Large	Low	Gravity	70000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1134	-423.4289	107711.7962	150266.3529
SW	Small	Mid	Gravity	70000	haz	Annual O&M	29.295	0	0	0	0	0	0	-849818.7944	574092.5785	47319.4272	33019.7083
SW	Medium	Mid	Gravity	70000	haz	Annual O&M	33.771	0	0	0	0	0	0	2101.9039	-15883.334	151149.6667	61418.2862
SW	Large	Mid	Gravity	70000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.9858	-406.6786	107449.6092	149538.7299
SW	Small	High	Gravity	70000	haz	Annual O&M	31.24	0	0	0	0	0	0	-861862.1753	588110.4729	50335.3112	34912.3704
SW	Medium	High	Gravity	70000	haz	Annual O&M	34.953	0	0	0	0	0	0	1556.8234	-12890.2175	146586.719	63269.4969
SW	Large	High	Gravity	70000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0592	-410.5609	107903.2388	148179.5654
SW	Small	Low	Gravity	75000	haz	Annual O&M	30.19	0	0	0	0	0	0	-766599.3915	510047.3296	47707.5709	28204.7397
SW	Medium	Low	Gravity	75000	haz	Annual O&M	34.318	0	0	0	0	0	0	2044.1762	-15856.2408	145343.9392	57386.0757
SW	Large	Low	Gravity	75000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.1134	-423.4404	104538.6286	150219.7718
SW	Small	Mid	Gravity	75000	haz	Annual O&M	29.295	0	0	0	0	0	0	-852306.3978	576210.5083	43035.3266	33000.3067
SW	Medium	Mid	Gravity	75000	haz	Annual O&M	33.771	0	0	0	0	0	0	2201.4646	-16727.8702	150021.2677	60267.7096
SW	Large	Mid	Gravity	75000	haz	Annual O&M	35.7	0	0	0	0	0	0	2.986	-406.7174	104277.0895	149492.9147

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for GAC																	
GW/SW	Size Category	Comp Level	Design Type	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	Gravity	75000	haz	Annual O&M	31.24	0	0	0	0	0	0	-864209.306	590152.131	46061.3542	34892.8944
SW	Medium	High	Gravity	75000	haz	Annual O&M	34.953	0	0	0	0	0	0	1655.5058	-13727.7496	145439.8751	62127.283
SW	Large	High	Gravity	75000	haz	Annual O&M	36.221	0	0	0	0	0	0	3.0594	-410.5992	104730.9097	148125.6365

A.2 Capital and Annual O&M Cost Equation Parameters for IX

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	Low	20000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	20000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	20000	non-haz	Total Capital	36.511	0	0	0	0	0	0	0	-138.0534	520295.2314	2097973.873
GW	Small	Mid	20000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	20000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	20000	non-haz	Total Capital	36.047	0	0	0	0	0	0	0	-154.0817	540783.5033	2366181.96
GW	Small	High	20000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	20000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	20000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-203.4804	693808.3856	3816368.881
GW	Small	Low	40000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	40000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	40000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-136.6756	519963.9788	2105105.946
GW	Small	Mid	40000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	40000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	40000	non-haz	Total Capital	36.053	0	0	0	0	0	0	0	-152.704	540452.2565	2373313.916
GW	Small	High	40000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	40000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	40000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-202.1057	693478.446	3823469.173
GW	Small	Low	60000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	60000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	60000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-138.1552	520116.175	2102649.929
GW	Small	Mid	60000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	60000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	60000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-154.1836	540604.4527	2370857.899
GW	Small	High	60000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	60000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	60000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-203.5853	693630.6422	3821013.156
GW	Small	Low	80000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	80000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	80000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	80000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	80000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	80000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	80000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	80000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	80000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	100000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	100000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	100000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	100000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	100000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	100000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	100000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	100000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	100000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	20000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	0	1064723.853	4675.891
GW	Medium	Low	20000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	1068385.932	26095.6274
GW	Large	Low	20000	non-haz	Annual O&M	36.511	0	0	0	0	0	0	0	0	1064120.695	43944.6759
GW	Small	Mid	20000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	0	1064729.974	4663.4818
GW	Medium	Mid	20000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	1068957.152	27422.7465
GW	Large	Mid	20000	non-haz	Annual O&M	36.047	0	0	0	0	0	0	0	0	1064398.826	41319.191
GW	Small	High	20000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	0	1066125.186	4745.1175
GW	Medium	High	20000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	1069190	26924.9391
GW	Large	High	20000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	1064974.626	34924.4203
GW	Small	Low	40000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-30138.106	552285.9443	4297.6004
GW	Medium	Low	40000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	545808.3357	26229.6665
GW	Large	Low	40000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	541179.6902	45589.3443
GW	Small	Mid	40000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29112.2037	551957.6386	4300.2747
GW	Medium	Mid	40000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	546371.5684	27557.1583
GW	Large	Mid	40000	non-haz	Annual O&M	36.053	0	0	0	0	0	0	0	0	541400.35	43365.7935
GW	Small	High	40000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30689.569	553867.8181	4361.7912
GW	Medium	High	40000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	546577.1301	27097.0258
GW	Large	High	40000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	541860.8292	37800.2376
GW	Small	Low	60000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	0	368373.2371	4678.2524
GW	Medium	Low	60000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	371615.8462	26274.3289
GW	Large	Low	60000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	366855.7558	46312.9986
GW	Small	Mid	60000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	0	368379.563	4668.6211
GW	Medium	Mid	60000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	372176.3948	27601.8267
GW	Large	Mid	60000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	367046.99	44398.8966
GW	Small	High	60000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	0	369773.2427	4750.2218
GW	Medium	High	60000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	372372.8373	27154.4911
GW	Large	High	60000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	367448.4879	39460.7017
GW	Small	Low	80000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-32422.4192	291900.9894	4269.51
GW	Medium	Low	80000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	284519.5327	26296.8118
GW	Large	Low	80000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	279705.0725	46478.8316
GW	Small	Mid	80000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-31512.6076	291610.6109	4271.7118
GW	Medium	Mid	80000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	285078.8952	27623.9473
GW	Large	Mid	80000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	279870.3118	44915.4253
GW	Small	High	80000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-33098.6247	293521.5326	4333.293
GW	Medium	High	80000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	285270.7183	27183.1163
GW	Large	High	80000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	280242.3235	40290.6772
GW	Small	Low	100000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-32866.5403	239817.8443	4264.2081
GW	Medium	Low	100000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	232261.8317	26310.0878
GW	Large	Low	100000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	227407.8657	46696.2751
GW	Small	Mid	100000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-31986.6029	239537.2918	4266.2738
GW	Medium	Mid	100000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	232820.3085	27637.5622
GW	Large	Mid	100000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	227564.2981	45225.4834

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	100000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-33583.7301	241454.8296	4327.3424
GW	Medium	High	100000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	233009.4792	27200.328
GW	Large	High	100000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	227918.6218	40788.7716
SW	Small	Low	20000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	20000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	20000	non-haz	Total Capital	36.511	0	0	0	0	0	0	0	-138.0534	520295.2314	2097973.873
SW	Small	Mid	20000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	20000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	20000	non-haz	Total Capital	36.047	0	0	0	0	0	0	0	-154.0817	540783.5033	2366181.96
SW	Small	High	20000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	20000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	20000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-203.4804	693808.3856	3816368.881
SW	Small	Low	40000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	40000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	40000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-136.6756	519963.9788	2105105.946
SW	Small	Mid	40000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	40000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	40000	non-haz	Total Capital	36.053	0	0	0	0	0	0	0	-152.704	540452.2565	2373313.916
SW	Small	High	40000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	40000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	40000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-202.1057	693478.446	3823469.173
SW	Small	Low	60000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	60000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	60000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-138.1552	520116.175	2102649.929
SW	Small	Mid	60000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	60000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	60000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-154.1836	540604.4527	2370857.899
SW	Small	High	60000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	60000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	60000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-203.5853	693630.6422	3821013.156
SW	Small	Low	80000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	80000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	80000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	80000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	80000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	80000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	80000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	80000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	80000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	100000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	100000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	100000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	100000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	100000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	100000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	100000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	100000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	100000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	20000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	0	1064266.215	4689.7346
SW	Medium	Low	20000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	1071107.126	24446.2211
SW	Large	Low	20000	non-haz	Annual O&M	36.511	0	0	0	0	0	0	0	0	1065231.958	60706.4346
SW	Small	Mid	20000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	0	1064269.612	4677.299
SW	Medium	Mid	20000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	1071747.413	25731.5582
SW	Large	Mid	20000	non-haz	Annual O&M	36.047	0	0	0	0	0	0	0	0	1065525.652	58259.0692
SW	Small	High	20000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	0	1065648.754	4752.4664
SW	Medium	High	20000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	1072005.198	25219.1389
SW	Large	High	20000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	1066133.339	52256.6105
SW	Small	Low	40000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	0	542127.5219	4642.0763
SW	Medium	Low	40000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	548527.6053	24576.6829
SW	Large	Low	40000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	542286.5529	62212.0042
SW	Small	Mid	40000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	0	542131.5543	4631.8186
SW	Medium	Mid	40000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	549159.9235	25862.2108
SW	Large	Mid	40000	non-haz	Annual O&M	36.053	0	0	0	0	0	0	0	0	542516.5272	60209.4175
SW	Small	High	40000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	0	543510.2393	4706.9878
SW	Medium	High	40000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	549389.3484	25387.7067
SW	Large	High	40000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	542996.4236	55118.3653
SW	Small	Low	60000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-29091.8475	377812.3059	4222.5195
SW	Medium	Low	60000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	374334.5154	24619.9539
SW	Large	Low	60000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	367963.2854	62838.1265
SW	Small	Mid	60000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-28121.2039	377491.9025	4226.451
SW	Medium	Mid	60000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	374963.9123	25906.1196
SW	Large	Mid	60000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	368163.8659	61108.5217
SW	Small	High	60000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-29400.8472	379296.0441	4284.2095
SW	Medium	High	60000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	375184.0142	25443.8034
SW	Large	High	60000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	368584.8766	56570.2412
SW	Small	Low	80000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-29482.7766	290918.001	4209.2912
SW	Medium	Low	80000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	287237.9703	24641.6485
SW	Large	Low	80000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	280813.8532	62961.7627
SW	Small	Mid	80000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-28558.6135	290613.2665	4212.9641
SW	Medium	Mid	80000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	287866.231	25927.5102
SW	Large	Mid	80000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	280987.5434	61557.941
SW	Small	High	80000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-29845.5249	292422.6578	4270.2018
SW	Medium	High	80000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	288081.3102	25472.0596
SW	Large	High	80000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	281379.1135	57296.0667
SW	Small	Low	100000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-29710.15	238782.0626	4201.198
SW	Medium	Low	100000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	234980.0984	24654.6213
SW	Large	Low	100000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	228516.8401	63149.8734
SW	Small	Mid	100000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-28809.2271	238485.1626	4204.7415
SW	Medium	Mid	100000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	235607.355	25940.7848
SW	Large	Mid	100000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	228681.7426	61827.6959

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	100000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30114.2164	240299.6672	4261.9344
SW	Medium	High	100000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	235819.6943	25488.9673
SW	Large	High	100000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	229055.6548	57731.5199
GW	Small	Low	120000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	120000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	120000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	120000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	120000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	120000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	120000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	120000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	120000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	140000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	140000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	140000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	140000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	140000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	140000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	140000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	140000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	140000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	160000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	160000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	160000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	160000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	160000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	160000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	160000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	160000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	160000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	180000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	180000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	180000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	180000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	180000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	180000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	180000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	180000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	180000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	120000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33173.7674	205101.4462	4260.3771
GW	Medium	Low	120000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	197423.3529	26318.9393
GW	Large	Low	120000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	192543.0476	46841.6819
GW	Small	Mid	120000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32305.439	204824.6865	4262.3956
GW	Medium	Mid	120000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	197981.3041	27646.5245
GW	Large	Mid	120000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	192693.6248	45432.2035

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	120000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-33895.2093	206738.1821	4323.6841
GW	Medium	High	120000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	198168.53	27211.9235
GW	Large	High	120000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	193036.1521	41121.0624
GW	Small	Low	140000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	35681.5845	-51721.7763	182631.0521	4205.9804
GW	Medium	Low	140000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-880.1279	176426.3238	23722.2794
GW	Large	Low	140000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	167639.6152	46945.2426
GW	Small	Mid	140000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32540.2454	180030.313	4259.6831
GW	Medium	Mid	140000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	-890.3845	177029.1365	25019.671
GW	Large	Mid	140000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	167786.0028	45579.7341
GW	Small	High	140000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34138.93	181947.0208	4320.9262
GW	Medium	High	140000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	230.0847	-2590.2057	180688.3221	22967.8686
GW	Large	High	140000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	168120.1043	41358.2373
GW	Small	Low	160000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33554.2091	161702.2379	4255.8323
GW	Medium	Low	160000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	153875.1246	26330.3668
GW	Large	Low	160000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	148962.0377	47022.8481
GW	Small	Mid	160000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32707.3957	161432.3752	4257.7921
GW	Medium	Mid	160000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	154432.4544	27657.7623
GW	Large	Mid	160000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	149105.2866	45690.2555
GW	Small	High	160000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34306.6957	163349.3479	4319.0205
GW	Medium	High	160000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	154617.4865	27226.2958
GW	Large	High	160000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	149433.0726	41535.8937
GW	Small	Low	180000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33688.3305	147239.4745	4254.0898
GW	Medium	Low	180000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-883.6657	143262.3106	23720.6991
GW	Large	Low	180000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	134435.0337	47083.4506
GW	Small	Mid	180000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32848.1732	146971.8524	4256.0081
GW	Medium	Mid	180000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	-894.0329	143865.0956	25017.6807
GW	Large	Mid	180000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	134575.8435	45776.4166
GW	Small	High	180000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34440.1492	148885.8696	4317.44
GW	Medium	High	180000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	-947.713	144286.5944	24428.1293
GW	Large	High	180000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	134898.7126	41674.1754
SW	Small	Low	120000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	120000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	120000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	120000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	120000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	120000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	120000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	120000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	120000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	140000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	140000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	140000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	140000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	140000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	140000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	140000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	140000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	140000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	160000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	160000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	160000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	160000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	160000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	160000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	160000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	160000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	160000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	180000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	180000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	180000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	180000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	180000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	180000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	180000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	180000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	180000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	120000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-29870.3672	204025.3474	4195.945
SW	Medium	Low	120000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-785.3175	203307.1247	22656.9849
SW	Large	Low	120000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	193652.1592	63275.6516
SW	Small	Mid	120000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-28986.1033	203733.9984	4199.4099
SW	Medium	Mid	120000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	-788.917	203948.4194	23933.6705
SW	Large	Mid	120000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	193811.2144	62007.4224
SW	Small	High	120000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30287.3573	205549.1764	4256.4363
SW	Medium	High	120000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	-853.9895	204421.3476	23317.9075
SW	Large	High	120000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	194173.3414	58021.967
SW	Small	Low	140000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-29988.8551	179202.1335	4191.7844
SW	Medium	Low	140000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	175256.5747	24669.8708
SW	Large	Low	140000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	168748.8189	63365.4619
SW	Small	Mid	140000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29116.2113	178914.7017	4195.1846
SW	Medium	Mid	140000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	175883.0472	25955.6205
SW	Large	Mid	140000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	168903.691	62136.0331
SW	Small	High	140000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30422.1307	180729.2743	4252.4421
SW	Medium	High	140000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	176092.2195	25508.1987
SW	Large	High	140000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	169257.4064	58229.3041
SW	Small	Low	160000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-30070.9946	160581.1649	4189.0431
SW	Medium	Low	160000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	156593.12	24674.2441
SW	Large	Low	160000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	150071.3192	63432.5207
SW	Small	Mid	160000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29204.9321	160296.0166	4192.3927
SW	Medium	Mid	160000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	157219.2857	25960.0878
SW	Large	Mid	160000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	150223.0494	62232.2821

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	160000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30503.2219	162109.5074	4249.6393
SW	Medium	High	160000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	-859.2921	160891.3121	23318.614
SW	Large	High	160000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	150570.4554	58385.0229
SW	Small	Low	180000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-30133.6436	146098.465	4186.9389
SW	Medium	Low	180000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	142076.9559	24677.9414
SW	Large	Low	180000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	135544.3644	63485.0017
SW	Small	Mid	180000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29279.2012	145817.234	4190.2238
SW	Medium	Mid	180000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	142702.8819	25964.0623
SW	Large	Mid	180000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	135693.6582	62307.2731
SW	Small	High	180000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30567.8121	147627.0909	4247.6496
SW	Medium	High	180000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	142910.1884	25518.9507
SW	Large	High	180000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	136036.1583	58506.1043
GW	Small	Low	200000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	200000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	200000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	200000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	200000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	200000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	200000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	200000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	200000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	220000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	220000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	220000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	220000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	220000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	220000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	220000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	220000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	220000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	240000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	240000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	240000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	240000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	240000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	240000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	240000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	240000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	240000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	260000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	260000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	260000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	260000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	260000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	260000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	260000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	260000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	260000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
GW	Small	Low	200000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33798.2383	135669.7703	4252.67
GW	Medium	Low	200000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	127746.3893	26336.7118
GW	Large	Low	200000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	122813.4321	47131.7902
GW	Small	Mid	200000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32969.69	135405.9409	4254.5411
GW	Medium	Mid	200000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	128303.1611	27664.6285
GW	Large	Mid	200000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	122952.2806	45845.4708
GW	Small	High	200000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34551.2737	137315.3692	4316.2833
GW	Medium	High	200000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	128486.8527	27234.9565
GW	Large	High	200000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	123271.2207	41784.9972
GW	Small	Low	220000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33868.8508	126196.8521	4251.9422
GW	Medium	Low	220000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-885.8967	122157.9913	23719.0935
GW	Large	Low	220000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	113304.8412	47171.4792
GW	Small	Mid	220000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-33040.3026	125933.0227	4253.8132
GW	Medium	Mid	220000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	-896.4758	122761.3683	25015.6484
GW	Large	Mid	220000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	113442.0975	45901.667
GW	Small	High	220000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34634.165	127847.5618	4315.1813
GW	Medium	High	220000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	-949.9843	123180.9943	24428.3505
GW	Large	High	220000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	113757.8195	41875.5432
GW	Small	Low	240000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33956.2504	118312.7024	4250.6317
GW	Medium	Low	240000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	110326.9847	26341.5783
GW	Large	Low	240000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	105381.0235	47204.4006
GW	Small	Mid	240000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-33127.7021	118048.8729	4252.5027
GW	Medium	Mid	240000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	110883.6108	27669.1069
GW	Large	Mid	240000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	105516.9518	45948.4232
GW	Small	High	240000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34713.1249	119959.5503	4314.0969
GW	Medium	High	240000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	111066.4262	27240.6392
GW	Large	High	240000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	105829.9857	41951.0947
GW	Small	Low	260000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-34011.6325	111633.5752	4250.2699
GW	Medium	Low	260000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-887.4488	107547.1826	23718.5241
GW	Large	Low	260000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	98676.2546	47232.1872
GW	Small	Mid	260000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-33183.0843	111369.7458	4252.1409
GW	Medium	Mid	260000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	-898.0611	108150.6294	25014.7053
GW	Large	Mid	260000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	98811.0468	45988.4927
GW	Small	High	260000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34768.944	113282.5745	4313.5132
GW	Medium	High	260000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	-951.5776	108569.3121	24428.6524
GW	Large	High	260000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	99121.8235	42014.7232
SW	Small	Low	200000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	200000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	200000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	200000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	200000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	200000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	200000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	200000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	200000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	220000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	220000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	220000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	220000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	220000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	220000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	220000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	220000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	220000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	240000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	240000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	240000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	240000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	240000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	240000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	240000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	240000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	240000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	260000	non-haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	260000	non-haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	260000	non-haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	260000	non-haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	260000	non-haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	260000	non-haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	260000	non-haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	260000	non-haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	260000	non-haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.5931	693862.3754	3816961.127
SW	Small	Low	200000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-30194.3778	134516.8087	4184.8201
SW	Medium	Low	200000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-793.8364	133664.2158	22652.5618
SW	Large	Low	200000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	123922.8044	63526.8681
SW	Small	Mid	200000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29351.5556	134239.4948	4188.0403
SW	Medium	Mid	200000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	-797.8781	134306.2869	23928.0697
SW	Large	Mid	200000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	124070.1545	62367.0703
SW	Small	High	200000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30627.7053	136044.6805	4245.5961
SW	Medium	High	200000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	-862.6789	134774.1228	23318.4116
SW	Large	High	200000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	124408.7274	58602.6347
SW	Small	Low	220000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-30232.6951	125034.6276	4183.5207
SW	Medium	Low	220000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-795.1449	124167.9595	22651.7415
SW	Large	Low	220000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	114414.2607	63560.9425
SW	Small	Mid	220000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29389.8729	124757.3137	4186.741
SW	Medium	Mid	220000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	121588.2765	25969.0497
SW	Large	Mid	220000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	114560.0013	62416.3472

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	220000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30680.8907	126568.1362	4244.1152
SW	Medium	High	220000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	121794.5032	25525.6587
SW	Large	High	220000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	114895.3639	58681.9855
SW	Small	Low	240000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	34111.3809	-48204.2389	119495.4572	4125.4844
SW	Medium	Low	240000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	-796.0656	116253.8965	22651.0577
SW	Large	Low	240000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	106490.4701	63589.5704
SW	Small	Mid	240000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29437.7121	116863.1798	4185.3777
SW	Medium	Mid	240000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	-800.0942	116895.6647	23926.6584
SW	Large	Mid	240000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	106634.8768	62457.2321
SW	Small	High	240000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30730.8174	118673.543	4242.7044
SW	Medium	High	240000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	-864.7682	117362.0011	23318.7766
SW	Large	High	240000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	106967.5648	58748.0391
SW	Small	Low	260000	non-haz	Annual O&M	18.625	0	0	0	0	0	0	0	-30306.5688	110454.9454	4181.2444
SW	Medium	Low	260000	non-haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	106344.9169	24686.9299
SW	Large	Low	260000	non-haz	Annual O&M	36.516	0	0	0	0	0	0	0	0	99785.7195	63613.8768
SW	Small	Mid	260000	non-haz	Annual O&M	19.55	0	0	0	0	0	0	0	-29468.7854	110179.2654	4184.4506
SW	Medium	Mid	260000	non-haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	106970.4309	25972.8474
SW	Large	Mid	260000	non-haz	Annual O&M	36.058	0	0	0	0	0	0	0	0	99929.01	62491.7234
SW	Small	High	260000	non-haz	Annual O&M	21.435	0	0	0	0	0	0	0	-30745.8108	111984.3804	4241.9855
SW	Medium	High	260000	non-haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	107175.8448	25530.443
SW	Large	High	260000	non-haz	Annual O&M	36.211	0	0	0	0	0	0	0	0	100259.4392	58803.5869
GW	Small	Low	20000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	20000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	20000	haz	Total Capital	36.495	0	0	0	0	0	0	0	-150.8093	522541.2956	2067509.667
GW	Small	Mid	20000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	20000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	20000	haz	Total Capital	36.026	0	0	0	0	0	0	0	-172.5454	543990.233	2331807.921
GW	Small	High	20000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	20000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	20000	haz	Total Capital	36.195	0	0	0	0	0	0	0	-256.1575	703098.5076	3662722.799
GW	Small	Low	40000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	40000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	40000	haz	Total Capital	36.5	0	0	0	0	0	0	0	-149.4315	522210.043	2074641.74
GW	Small	Mid	40000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	40000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	40000	haz	Total Capital	36.053	0	0	0	0	0	0	0	-176.9949	544836.3714	2291858.692
GW	Small	High	40000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	40000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	40000	haz	Total Capital	36.205	0	0	0	0	0	0	0	-207.7629	694310.5292	3821848.318
GW	Small	Low	60000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	60000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	60000	haz	Total Capital	36.511	0	0	0	0	0	0	0	-153.5159	522888.5227	2051140.741
GW	Small	Mid	60000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	60000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	60000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-154.1836	540604.4527	2370857.899

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	60000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	60000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	60000	haz	Total Capital	36.205	0	0	0	0	0	0	0	-209.2425	694462.7254	3819392.301
GW	Small	Low	80000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	80000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	80000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	80000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	80000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	80000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	80000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	80000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	80000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	100000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	100000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	100000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	100000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	100000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	100000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	100000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	100000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	100000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	20000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	0	1132465.103	13709.2584
GW	Medium	Low	20000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	1137724.597	31072.6805
GW	Large	Low	20000	haz	Annual O&M	36.495	0	0	0	0	0	0	0	2292.4161	1126369.202	25983.9344
GW	Small	Mid	20000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	0	1132470.871	13692.0872
GW	Medium	Mid	20000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	1138294.683	32403.5805
GW	Large	Mid	20000	haz	Annual O&M	36.026	0	0	0	0	0	0	0	2295.4536	1126398.055	26004.3217
GW	Small	High	20000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	0	1133864.645	13773.7777
GW	Medium	High	20000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	1138531.44	31895.4706
GW	Large	High	20000	haz	Annual O&M	36.195	0	0	0	0	0	0	0	2303.1177	1126282.481	30701.0611
GW	Small	Low	40000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-50293.4697	592728.4597	8559.9633
GW	Medium	Low	40000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	580477.7028	28717.9842
GW	Large	Low	40000	haz	Annual O&M	36.5	0	0	0	0	0	0	0	1148.4666	572123.0632	39211.2295
GW	Small	Mid	40000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-48983.9971	592307.5766	8563.7776
GW	Medium	Mid	40000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	581040.3428	30047.5296
GW	Large	Mid	40000	haz	Annual O&M	36.053	0	0	0	0	0	0	0	1152.5943	571987.8749	41646.3404
GW	Small	High	40000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-50566.9793	594219.927	8625.1866
GW	Medium	High	40000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	581247.8772	29582.3025
GW	Large	High	40000	haz	Annual O&M	36.205	0	0	0	0	0	0	0	1147.9067	572899.984	34073.9924
GW	Small	Low	60000	haz	Annual O&M	18.625	0	0	0	0	0	0	122493.1151	-108031.2566	413657.567	6942.6325
GW	Medium	Low	60000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	394728.8393	27933.0818
GW	Large	Low	60000	haz	Annual O&M	36.511	0	0	0	0	0	0	0	767.0541	387365.3749	44057.421
GW	Small	Mid	60000	haz	Annual O&M	19.55	0	0	0	0	0	0	108982.9597	-99949.046	412409.3797	6965.3688
GW	Medium	Mid	60000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	395288.9627	29262.1589
GW	Large	Mid	60000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	763.6199	387888.1306	39523.5666

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	60000	haz	Annual O&M	21.435	0	0	0	0	0	0	109900.112	-102007.6368	414379.5813	7025.9161
GW	Medium	High	60000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	395486.6706	28811.3389
GW	Large	High	60000	haz	Annual O&M	36.205	0	0	0	0	0	0	0	768.0014	387922.1561	39429.2806
GW	Small	Low	80000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-42504.0836	312121.9359	6400.8146
GW	Medium	Low	80000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	301854.2032	27541.0821
GW	Large	Low	80000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	572.6012	295345.0426	42721.5719
GW	Small	Mid	80000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-41454.9632	311786.0448	6403.5835
GW	Medium	Mid	80000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	302413.2703	28869.4486
GW	Large	Mid	80000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	574.1815	295383.6898	42554.8397
GW	Small	High	80000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-43043.0386	313698.7428	6465.0197
GW	Medium	High	80000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	302606.0853	28425.7369
GW	Large	High	80000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	576.2445	295568.8722	41776.6191
GW	Small	Low	100000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-40944.0833	256000.1505	5968.7789
GW	Medium	Low	100000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	246129.6134	27305.3883
GW	Large	Low	100000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	459.0429	239842.7739	44540.9458
GW	Small	Mid	100000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-39948.0553	255681.6708	5971.3172
GW	Medium	Mid	100000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	246687.8583	28633.8044
GW	Large	Mid	100000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	460.5186	239881.0109	44374.0576
GW	Small	High	100000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-41534.8612	257594.0324	6032.9111
GW	Medium	High	100000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	246877.8538	28194.3394
GW	Large	High	100000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	462.6563	240046.7066	43453.3144
GW	Small	Low	120000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	120000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	120000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	120000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	120000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	120000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	120000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	120000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	120000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	140000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	140000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	140000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	140000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	140000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	140000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	140000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	140000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	140000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	160000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	160000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	160000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	160000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	160000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	160000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	160000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	160000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	160000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	180000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	180000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	180000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	180000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	180000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	180000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	180000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	180000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	180000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	120000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-39896.7686	218582.633	5681.1796
GW	Medium	Low	120000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	208979.7041	27148.6036
GW	Large	Low	120000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	383.3372	202841.2893	45753.4555
GW	Small	Mid	120000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-38933.8646	218274.8432	5683.612
GW	Medium	Mid	120000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	209537.5087	28476.8022
GW	Large	Mid	120000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	384.7431	202879.2466	45586.4222
GW	Small	High	120000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-40522.3364	220188.9822	5744.9019
GW	Medium	High	120000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	209725.5435	28040.1752
GW	Large	High	120000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	386.9311	203031.9133	44571.1588
GW	Small	Low	140000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-39166.0171	191862.1159	5475.3864
GW	Medium	Low	140000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	182444.1765	27036.4567
GW	Large	Low	140000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	329.262	176411.6174	46620.0948
GW	Small	Mid	140000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-38228.0344	191562.5998	5477.6885
GW	Medium	Mid	140000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	183001.5174	28364.7147
GW	Large	Mid	140000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	330.6177	176449.4169	46452.4731
GW	Small	High	140000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-39810.4962	193474.0953	5539.2778
GW	Medium	High	140000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	183188.2598	27929.9142
GW	Large	High	140000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	332.8416	176592.7649	45370.0295
GW	Small	Low	160000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-38609.9431	171819.5852	5321.0546
GW	Medium	Low	160000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	-796.2984	166059.8652	24597.289
GW	Large	Low	160000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	288.7054	156589.3905	47269.6799
GW	Small	Mid	160000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-37695.1785	171527.6546	5323.2621
GW	Medium	Mid	160000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	-806.4886	166661.8556	25895.464
GW	Large	Mid	160000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	290.0236	156627.0422	47102.2133
GW	Small	High	160000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-39268.8513	173436.0934	5384.8829
GW	Medium	High	160000	haz	Annual O&M	35.459	0	0	0	0	0	0	209.888	-2362.5219	170039.7217	23969.6138
GW	Large	High	160000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	292.2746	156763.4065	45968.9184
GW	Small	Low	180000	haz	Annual O&M	18.625	0	0	0	0	0	0	78068.9263	-78282.0736	161326.5979	5087.8603
GW	Medium	Low	180000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	147063.4792	26886.8773
GW	Large	Low	180000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	257.1614	141172.0956	47774.9908
GW	Small	Mid	180000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-37272.9131	155941.3656	5203.2539
GW	Medium	Mid	180000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	147620.3149	28215.2097
GW	Large	Mid	180000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	258.4507	141209.6341	47607.4356

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	180000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-38861.8381	157854.8108	5264.8788
GW	Medium	High	180000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	147805.0507	27783.2698
GW	Large	High	180000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	260.7223	141340.5837	46434.6796
GW	Small	Low	200000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	200000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	200000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	200000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	200000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	200000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	200000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	200000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	200000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	220000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	220000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	220000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	220000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	220000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	220000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	220000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	220000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	220000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	240000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	240000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	240000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	240000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	240000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	240000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	240000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	240000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	240000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	260000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
GW	Medium	Low	260000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
GW	Large	Low	260000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
GW	Small	Mid	260000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
GW	Medium	Mid	260000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
GW	Large	Mid	260000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
GW	Small	High	260000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
GW	Medium	High	260000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
GW	Large	High	260000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
GW	Small	Low	200000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-37831.5372	143758.8355	5105.2822
GW	Medium	Low	200000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	-816.2719	138285.6377	24420.5624
GW	Large	Low	200000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	231.9265	128838.2344	48179.5795
GW	Small	Mid	200000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-36939.9907	143474.4904	5107.3952
GW	Medium	Mid	200000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	-826.5915	138887.9876	25718.2024
GW	Large	Mid	200000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	233.1925	128875.6834	48011.898

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	High	200000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-38518.7319	145385.5363	5168.6993
GW	Medium	High	200000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	-880.7598	139311.2399	25127.3351
GW	Large	High	200000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	235.4805	129002.3241	46807.4062
GW	Small	Low	220000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-37540.5642	133552.1076	5026.6995
GW	Medium	Low	220000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	124548.3337	26791.8558
GW	Large	Low	220000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	211.2795	118746.9247	48510.2016
GW	Small	Mid	220000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-36660.6268	133271.5551	5028.7653
GW	Medium	Mid	220000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	125105.0141	28119.9349
GW	Large	Mid	220000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	212.5263	118784.2966	48342.5463
GW	Small	High	220000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-38245.2789	135183.9941	5090.3023
GW	Medium	High	220000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	125288.4993	27690.1004
GW	Large	High	220000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	214.8279	118907.3981	47112.1926
GW	Small	Low	240000	haz	Annual O&M	18.625	0	0	0	0	0	0	72528.9363	-74565.592	129783.4891	4856.3968
GW	Medium	Low	240000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	-829.4844	119769.0458	24303.2381
GW	Large	Low	240000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	194.0736	110337.4978	48785.7821
GW	Small	Mid	240000	haz	Annual O&M	19.55	0	0	0	0	0	0	61702.8777	-68129.2204	128797.7545	4874.1543
GW	Medium	Mid	240000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	116661.7765	28084.2212
GW	Large	Mid	240000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	195.3045	110374.8269	48617.6724
GW	Small	High	240000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-38012.8869	126681.6138	5024.8796
GW	Medium	High	240000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	-894.0657	120794.0535	25010.5832
GW	Large	High	240000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	197.6175	110494.9585	47365.7587
GW	Small	Low	260000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-37096.1693	117851.5198	4906.1034
GW	Medium	Low	260000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	-834.6212	112647.6343	24257.6439
GW	Large	Low	260000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	179.5149	103221.8169	49019.1355
GW	Small	Mid	260000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-36221.1848	117572.5195	4908.1634
GW	Medium	Mid	260000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	-845.2031	113250.7518	25554.3797
GW	Large	Mid	260000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	180.7325	103259.0856	48851.0268
GW	Small	High	260000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-37809.7182	119484.8867	4969.6955
GW	Medium	High	260000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	-899.1682	113671.8617	24966.0901
GW	Large	High	260000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	183.0554	103376.6913	47581.3258
SW	Small	Low	20000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	20000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	20000	haz	Total Capital	36.495	0	0	0	0	0	0	0	-150.8093	522541.2956	2067509.667
SW	Small	Mid	20000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	20000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	20000	haz	Total Capital	36.026	0	0	0	0	0	0	0	-172.5454	543990.233	2331807.921
SW	Small	High	20000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	20000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	20000	haz	Total Capital	36.195	0	0	0	0	0	0	0	-256.1575	703098.5076	3662722.799
SW	Small	Low	40000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	40000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	40000	haz	Total Capital	36.511	0	0	0	0	0	0	0	-152.0363	522736.3265	2053596.758
SW	Small	Mid	40000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	40000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	40000	haz	Total Capital	36.053	0	0	0	0	0	0	0	-176.9949	544836.3714	2291858.692

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	40000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	40000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	40000	haz	Total Capital	36.205	0	0	0	0	0	0	0	-207.7629	694310.5292	3821848.318
SW	Small	Low	60000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	60000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	60000	haz	Total Capital	36.511	0	0	0	0	0	0	0	-153.5159	522888.5227	2051140.741
SW	Small	Mid	60000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	60000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	60000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-154.1836	540604.4527	2370857.899
SW	Small	High	60000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	60000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	60000	haz	Total Capital	36.205	0	0	0	0	0	0	0	-209.2425	694462.7254	3819392.301
SW	Small	Low	80000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	80000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	80000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	80000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	80000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	80000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	80000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	80000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	80000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	100000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	100000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	100000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	100000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	100000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	100000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	100000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	100000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	100000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	20000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	0	1127565.43	15190.8237
SW	Medium	Low	20000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	1140259.936	29511.3306
SW	Large	Low	20000	haz	Annual O&M	36.495	0	0	0	0	0	0	0	2333.0175	1136975.889	-11493.1372
SW	Small	Mid	20000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	0	1127567.203	15173.3724
SW	Medium	Mid	20000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	1140898.477	30801.3688
SW	Large	Mid	20000	haz	Annual O&M	36.026	0	0	0	0	0	0	0	2336.4828	1137005.279	-11422.7473
SW	Small	High	20000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	0	1128945.407	15248.5963
SW	Medium	High	20000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	1141160.969	30277.7233
SW	Large	High	20000	haz	Annual O&M	36.195	0	0	0	0	0	0	0	2344.6023	1136936.744	-7684.5959
SW	Small	Low	40000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-40372.6016	587279.479	9332.6657
SW	Medium	Low	40000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	583103.929	27109.2544
SW	Large	Low	40000	haz	Annual O&M	36.511	0	0	0	0	0	0	0	1160.0166	578626.5735	22700.2023
SW	Small	Mid	40000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-39013.455	586828.1732	9338.745
SW	Medium	Mid	40000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	583735.3861	28397.2601
SW	Large	Mid	40000	haz	Annual O&M	36.053	0	0	0	0	0	0	0	1163.4006	578598.4996	23151.8542

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	40000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-40309.8755	588640.9229	9396.0306
SW	Medium	High	40000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	583967.0983	27917.0455
SW	Large	High	40000	haz	Annual O&M	36.205	0	0	0	0	0	0	0	1158.1616	579538.7787	16218.4027
SW	Small	Low	60000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-37152.7767	401607.3829	7611.0782
SW	Medium	Low	60000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	397385.341	26308.5463
SW	Large	Low	60000	haz	Annual O&M	36.511	0	0	0	0	0	0	0	767.7803	392611.2986	32435.4587
SW	Small	Mid	60000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-35984.5909	401220.3866	7616.1089
SW	Medium	Mid	60000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	398014.4663	27595.6301
SW	Large	Mid	60000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	764.2051	393129.1073	28511.9361
SW	Small	High	60000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-37262.9915	403025.1764	7673.7138
SW	Medium	High	60000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	398235.9186	27129.9121
SW	Large	High	60000	haz	Annual O&M	36.205	0	0	0	0	0	0	0	768.6568	393203.101	28120.3998
SW	Small	Low	80000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-35529.903	308766.4718	6750.4741
SW	Medium	Low	80000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	-550.8987	306746.7604	24500.7429
SW	Large	Low	80000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	568.3848	299893.0895	34981.0376
SW	Small	Mid	80000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-34454.6782	308410.8133	6754.9876
SW	Medium	Mid	80000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	-553.8979	307386.7869	25779.6526
SW	Large	Mid	80000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	569.9745	299948.3367	34755.1763
SW	Small	High	80000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-35743.6805	310220.6897	6812.4206
SW	Medium	High	80000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	305370.2349	26736.6176
SW	Large	High	80000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	572.2209	300151.5081	33937.4031
SW	Small	Low	100000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-34556.6593	253061.8726	6234.2492
SW	Medium	Low	100000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	248810.5844	25667.8628
SW	Large	Low	100000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	451.9539	243985.4043	38725.1007
SW	Small	Mid	100000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-33532.9539	252723.5169	6238.49
SW	Medium	Mid	100000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	249437.6047	26954.651
SW	Large	Mid	100000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	453.4356	244039.9172	38500.5095
SW	Small	High	100000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34817.9626	254531.5492	6296.0361
SW	Medium	High	100000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	249650.8648	26500.6689
SW	Large	High	100000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	455.731	244225.8463	37536.9871
SW	Small	Low	120000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	120000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	120000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	120000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	120000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	120000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	120000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	120000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	120000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	140000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	140000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	140000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	140000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	140000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	140000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	140000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	140000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	140000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	160000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	160000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	160000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	160000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	160000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	160000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	160000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	160000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	160000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	180000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	180000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	180000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	180000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	180000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	180000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	180000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	180000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	180000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	120000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33900.4382	215924.0368	5890.0342
SW	Medium	Low	120000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	211666.7607	25507.7665
SW	Large	Low	120000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	374.3328	206713.6466	41220.6732
SW	Small	Mid	120000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32918.1745	215599.7161	5894.0304
SW	Medium	Mid	120000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	212293.369	26794.4102
SW	Large	Mid	120000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	375.7431	206767.6276	40997.6054
SW	Small	High	120000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-34205.6675	217407.2924	5951.6382
SW	Medium	High	120000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	212504.7011	26343.0173
SW	Large	High	120000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	378.0706	206942.1029	39936.2611
SW	Small	Low	140000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-33439.3211	189399.3522	5644.1269
SW	Medium	Low	140000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	-660.5507	187798.374	23705.5598
SW	Large	Low	140000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	318.8896	180090.9314	43003.9659
SW	Small	Mid	140000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32480.2976	189082.8661	5647.9938
SW	Medium	Mid	140000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	-664.1618	188439.1035	24982.8715
SW	Large	Mid	140000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	320.2488	180144.5379	42781.5828
SW	Small	High	140000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-33769.9418	190891.5498	5705.6276
SW	Medium	High	140000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	-730.1226	188914.9671	24365.1968
SW	Large	High	140000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	322.5993	180310.8197	41650.5338
SW	Small	Low	160000	haz	Annual O&M	18.625	0	0	0	0	0	0	63488.5129	-66457.9691	173889.5337	5354.3148
SW	Medium	Low	160000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	165237.1063	25307.4841
SW	Large	Low	160000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	277.307	160123.92	44340.8107
SW	Small	Mid	160000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-32146.4113	169192.4714	5463.6098
SW	Medium	Mid	160000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	165863.1827	26593.8867
SW	Large	Mid	160000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	278.6275	160177.2595	44119.0894

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	160000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-33437.2181	171001.8918	5521.288
SW	Medium	High	160000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	166071.8611	26146.4553
SW	Large	High	160000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	280.9959	160337.3635	42936.0562
SW	Small	Low	180000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-32817.3744	154030.5068	5316.3073
SW	Medium	Low	180000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	149760.5538	25240.7839
SW	Large	Low	180000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	244.965	144594.0105	45380.8076
SW	Small	Mid	180000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-31893.2113	153725.7723	5319.9801
SW	Medium	Mid	180000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	150386.333	26527.2055
SW	Large	Mid	180000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	246.2556	144647.1468	45159.37
SW	Small	High	180000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-33193.2691	155537.8739	5377.427
SW	Medium	High	180000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	150594.2405	26080.9857
SW	Large	High	180000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	248.6372	144802.4835	43935.5475
SW	Small	Low	200000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	200000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	200000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	200000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	200000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	200000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	200000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	200000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	200000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	220000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	220000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	220000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	220000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	220000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	220000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	220000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	220000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	220000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	240000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	240000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	240000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	240000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	240000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	240000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87
SW	Small	High	240000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	240000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	240000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	260000	haz	Total Capital	18.625	0	0	0	0	0	0	-123193.7377	-79962.4309	875448.755	145384.5687
SW	Medium	Low	260000	haz	Total Capital	34.653	0	0	0	0	0	0	0	-6421.767	658890.1107	1055907.247
SW	Large	Low	260000	haz	Total Capital	36.516	0	0	0	0	0	0	0	-142.3532	520600.7049	2094177.562
SW	Small	Mid	260000	haz	Total Capital	19.55	0	0	0	0	0	0	279001.2156	-684702.7894	1114657.33	181484.5646
SW	Medium	Mid	260000	haz	Total Capital	34.335	0	0	0	0	0	0	0	-10424.7434	738369.9087	1145973.904
SW	Large	Mid	260000	haz	Total Capital	36.058	0	0	0	0	0	0	0	-156.1913	540836.1859	2366805.87

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water March 2024

Cost Equation Parameters for IX																
GW/SW	Size Category	Comp Level	Bed Volumes	Spent Media	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	High	260000	haz	Total Capital	21.435	0	0	0	0	0	0	942863.789	-1917858.317	2035549.745	296537.0341
SW	Medium	High	260000	haz	Total Capital	35.459	0	0	0	0	0	0	0	-11186.2438	943432.6253	1827403.638
SW	Large	High	260000	haz	Total Capital	36.211	0	0	0	0	0	0	0	-205.4211	693814.6627	3820071.758
SW	Small	Low	200000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-32612.8967	141654.1386	5201.6989
SW	Medium	Low	200000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	137379.3115	25187.6006
SW	Large	Low	200000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	219.0913	132170.0842	46212.6382
SW	Small	Mid	200000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-31700.3538	141353.3214	5205.3071
SW	Medium	Mid	200000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	138005.0096	26473.7442
SW	Large	Mid	200000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	220.3583	132223.0395	45991.888
SW	Small	High	200000	haz	Annual O&M	21.435	0	0	0	0	0	0	47582.6992	-58001.1186	146451.4913	5183.5116
SW	Medium	High	200000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	138212.1074	26028.447
SW	Large	High	200000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	222.7507	132374.5332	44735.9563
SW	Small	Low	220000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-32443.0172	131529.127	5107.445
SW	Medium	Low	220000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	127249.091	25143.9686
SW	Large	Low	220000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	197.922	122005.0527	46893.7223
SW	Small	Mid	220000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-31547.1331	131233.8608	5110.9746
SW	Medium	Mid	220000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	127874.7079	26430.1872
SW	Large	Mid	220000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	199.1691	122057.8891	46672.7612
SW	Small	High	220000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-32824.4526	133038.9559	5168.6688
SW	Medium	High	220000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	-782.9687	131237.5948	23985.0851
SW	Large	High	220000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	201.5707	122206.2415	45390.2146
SW	Small	Low	240000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-32286.9815	123086.1834	5029.46
SW	Medium	Low	240000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	118807.5267	25107.196
SW	Large	Low	240000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	180.2811	113534.1838	47460.8947
SW	Small	Mid	240000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-31396.1364	122792.551	5032.9755
SW	Medium	Mid	240000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	119432.8595	26393.5887
SW	Large	Mid	240000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	181.5122	113586.8837	47240.2875
SW	Small	High	240000	haz	Annual O&M	21.435	0	0	0	0	0	0	0	-32686.3565	124602.8057	5090.3449
SW	Medium	High	240000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	0	119639.0762	25949.6259
SW	Large	High	240000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	183.9209	113732.6369	45935.8979
SW	Small	Low	260000	haz	Annual O&M	18.625	0	0	0	0	0	0	0	-32150.6672	115941.1012	4963.2928
SW	Medium	Low	260000	haz	Annual O&M	34.653	0	0	0	0	0	0	0	0	111664.4849	25076.5171
SW	Large	Low	260000	haz	Annual O&M	36.516	0	0	0	0	0	0	0	165.3538	106366.5505	47940.7627
SW	Small	Mid	260000	haz	Annual O&M	19.55	0	0	0	0	0	0	0	-31266.4033	115649.7522	4966.7577
SW	Medium	Mid	260000	haz	Annual O&M	34.335	0	0	0	0	0	0	0	0	112289.8773	26362.694
SW	Large	Mid	260000	haz	Annual O&M	36.058	0	0	0	0	0	0	0	166.5714	106419.1291	47720.7135
SW	Small	High	260000	haz	Annual O&M	21.435	0	0	0	0	0	0	42655.2744	-54989.4188	120410.252	4953.2804
SW	Medium	High	260000	haz	Annual O&M	35.459	0	0	0	0	0	0	0	-797.2389	115709.1932	23882.7022
SW	Large	High	260000	haz	Annual O&M	36.211	0	0	0	0	0	0	0	168.9858	106562.7197	46396.821

A.3 Capital and Annual O&M Cost Equation Parameters for RO/NF

Cost Equation Parameters for RO/NF														
GW/SW	Size Category	Comp Level	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	Low	Total Capital	23.115	0	0	0	0	0	0	437053.0639	-1156916.569	1967488.564	1463918.156
GW	Medium	Low	Total Capital	28.99411765	0	0	0	0	0	0	-2261.2437	7544.8133	1088868.815	2219118.011
GW	Large	Low	Total Capital	29.67368421	0	0	0	0	0	0	0	-162.9871	693831.825	4788367.47
GW	Small	Mid	Total Capital	22.415	0	0	0	0	0	0	0	-1133971.613	2808082.31	1573876.809
GW	Medium	Mid	Total Capital	27.92941176	0	0	0	0	0	0	-2783.24	10761.4023	1266677.024	2868082.839
GW	Large	Mid	Total Capital	28.66315789	0	0	0	0	0	0	12.7538	-3409.4027	916678.3253	5223375.504
GW	Small	High	Total Capital	25.465	0	0	0	0	0	0	712817.9297	-2529832.211	3763165.486	1868182.212
GW	Medium	High	Total Capital	30.34705882	0	0	0	0	0	0	-2435.4521	2389.2312	1333865.778	3447474.127
GW	Large	High	Total Capital	30.17894737	0	0	0	0	0	0	3.8507	-1269.4529	844084.419	6296610.515
GW	Small	Low	Annual O&M	23.115	0	0	0	0	0	0	2063047.154	-897216.0192	484242.8872	44574.8113
GW	Medium	Low	Annual O&M	28.99411765	0	0	0	0	0	0	13193.5845	-122763.9786	653229.2641	-34056.4398
GW	Large	Low	Annual O&M	29.67368421	0	0	0	0	0	0	6.7065	-968.2361	282811.6573	375801.5896
GW	Small	Mid	Annual O&M	22.415	0	0	0	0	0	0	2057176.273	-893150.114	483387.94	44626.9484
GW	Medium	Mid	Annual O&M	27.92941176	0	0	0	0	0	0	13193.5845	-122763.9786	653229.2641	-34056.4398
GW	Large	Mid	Annual O&M	28.66315789	0	0	0	0	0	0	6.7065	-968.2361	282811.6573	375801.5896
GW	Small	High	Annual O&M	25.465	0	0	0	0	0	0	2067561.843	-900342.6879	484900.339	44534.718
GW	Medium	High	Annual O&M	30.34705882	0	0	0	0	0	0	13193.5845	-122763.9786	653229.2641	-34056.4398
GW	Large	High	Annual O&M	30.17894737	0	0	0	0	0	0	6.7065	-968.2361	282811.6573	375801.5896
SW	Small	Low	Total Capital	23.17	0	0	0	0	0	0	792516.8148	-2008873.791	2491357.216	1428953.402
SW	Medium	Low	Total Capital	29.3	0	0	0	0	0	0	3012.7737	-81899.4104	1466243.733	1847192.192
SW	Large	Low	Total Capital	30.78947368	0	0	0	0	0	0	0	-290.3761	644985.4841	4675860.549
SW	Small	Mid	Total Capital	22.445	0	0	0	0	0	0	4158066.618	-7581773.041	5272114.206	1424299.434
SW	Medium	Mid	Total Capital	28.21764706	0	0	0	0	0	0	10041.0742	-208062.7703	2260952.426	1637438.777
SW	Large	Mid	Total Capital	29.5	0	0	0	0	0	0	8.3787	-2744.4363	851006.8369	4837119.648
SW	Small	High	Total Capital	25.54	0	0	0	0	0	0	2628171.02	-5820941.321	5245655.252	1790788.574
SW	Medium	High	Total Capital	30.46470588	0	0	0	0	0	0	7631.6394	-169559.7783	2107573.492	2557744.787
SW	Large	High	Total Capital	31.04210526	0	0	0	0	0	0	0	-484.018	737323.2359	6841317.778
SW	Small	Low	Annual O&M	23.17	0	0	0	0	0	0	0	-153633.167	551973.2284	45651.642
SW	Medium	Low	Annual O&M	29.3	0	0	0	0	0	0	17482.5751	-161274.0615	821907.5954	-56588.3578
SW	Large	Low	Annual O&M	30.78947368	0	0	0	0	0	0	11.4871	-1669.1707	338108.3881	486893.4377
SW	Small	Mid	Annual O&M	22.445	0	0	0	0	0	0	2480041.671	-1391655.414	686771.0419	42971.874
SW	Medium	Mid	Annual O&M	28.21764706	0	0	0	0	0	0	18853.7351	-171558.7816	844811.586	-70541.8011
SW	Large	Mid	Annual O&M	29.5	0	0	0	0	0	0	11.4871	-1669.1707	338108.3881	486893.4377
SW	Small	High	Annual O&M	25.54	0	0	0	0	0	0	1479601.694	-893288.7439	632978.4064	44029.8274
SW	Medium	High	Annual O&M	30.46470588	0	0	0	0	0	0	17842.5314	-163974.0014	827920.3403	-60251.4092
SW	Large	High	Annual O&M	31.04210526	0	0	0	0	0	0	11.4871	-1669.1707	338108.3881	486893.4377

A.4 Capital and Annual O&M Cost Equation Parameters for POU RO

Cost Equation Parameters for POU RO														
GW/SW	Size Category	Comp Level	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	n/a	Total Capital	10	700944.37	1.0355	0	0	0	0	0	0	0	0
GW	Small	n/a	Annual O&M	10	0	0	0	0	0	0	0	-135400.9866	701268.6995	2454.8593
SW	Small	n/a	Total Capital	10	705013.194	1.0465	0	0	0	0	0	0	0	0
SW	Small	n/a	Annual O&M	10	0	0	0	0	0	0	0	0	652386.1744	690.4192

A.5 Capital and Annual O&M Cost Equation Parameters for Nontreatment Options

Cost Equation Parameters for Nontreatment Options															
GW/SW	Size Category	Comp Level	Design Type	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
GW	Small	Low	Interconnection	Total Capital	17.21	0	0	0	0	0	0	-560032.442	771721.5229	51365.9263	600231.0091
GW	Medium	Low	Interconnection	Total Capital	22.05	0	0	0	0	0	0	-55058.6273	363044.7555	-566594.58	1173013.79
GW	Small	Mid	Interconnection	Total Capital	17.23	0	0	0	0	0	0	-605774.9391	831092.7558	43597.1038	611295.3516
GW	Medium	Mid	Interconnection	Total Capital	22.17	0	0	0	0	0	0	-59703.7808	402536.2258	-647866.3051	1241967.732
GW	Small	High	Interconnection	Total Capital	33.93	0	0	0	0	0	0	0	-631069.7282	1385198.056	1313780.871
GW	Medium	High	Interconnection	Total Capital	38.17	0	0	0	0	0	0	0	-116324.7782	965237.1476	1292920.326
GW	Small	Low	Interconnection	Annual O&M	17.21	0	0	0	0	0	0	1172393.696	-323637.2531	1328660.543	1012.2372
GW	Medium	Low	Interconnection	Annual O&M	22.05	0	0	0	0	0	0	140676.5805	-307834.65	1526384.539	-37333.9888
GW	Small	Mid	Interconnection	Annual O&M	17.23	0	0	0	0	0	0	1172393.696	-323637.2531	1328660.543	1012.2372
GW	Medium	Mid	Interconnection	Annual O&M	22.17	0	0	0	0	0	0	140676.5805	-307834.65	1526384.539	-37333.9888
GW	Small	High	Interconnection	Annual O&M	33.93	0	0	0	0	0	0	964898.8074	-258272.7146	1319201.805	1130.9069
GW	Medium	High	Interconnection	Annual O&M	38.17	0	0	0	0	0	0	122049.6952	-267262.8612	1494257.446	-32645.9798
GW	Small	Low	New Well Construction	Total Capital	24.83	0	0	0	0	0	0	628206.1808	-605771.3415	437758.3298	220003.705
GW	Medium	Low	New Well Construction	Total Capital	28.36	0	0	0	0	0	0	-128668.7397	872536.2865	-1339364.867	1258633.582
GW	Small	Mid	New Well Construction	Total Capital	25.75	0	0	0	0	0	0	1559164.557	-1723018.32	1107234.322	398078.7007
GW	Medium	Mid	New Well Construction	Total Capital	29.01	0	0	0	0	0	0	-254010.7513	1721705.053	-2694012.854	2491392.114
GW	Small	High	New Well Construction	Total Capital	26.23	0	0	0	0	0	0	1765114.84	-2018136.542	1397596.137	422042.282
GW	Medium	High	New Well Construction	Total Capital	29.84	0	0	0	0	0	0	-296012.9238	2006412.029	-3148814.65	2912158.263
GW	Small	Low	New Well Construction	Annual O&M	24.83	0	0	0	0	0	0	-73956.3039	92162.0229	49872.6092	3762.882
GW	Medium	Low	New Well Construction	Annual O&M	28.36	0	0	0	0	0	0	-33388.3209	88799.4329	5402.2413	17891.507
GW	Small	Mid	New Well Construction	Annual O&M	25.75	0	0	0	0	0	0	-73956.3039	92162.0229	49872.6092	3762.882
GW	Medium	Mid	New Well Construction	Annual O&M	29.01	0	0	0	0	0	0	-33388.3209	88799.4329	5402.2413	17891.507
GW	Small	High	New Well Construction	Annual O&M	26.23	0	0	0	0	0	0	-73956.3039	92162.0229	49872.6092	3762.882
GW	Medium	High	New Well Construction	Annual O&M	29.84	0	0	0	0	0	0	-33388.3209	88799.4329	5402.2413	17891.507
SW	Small	Low	Interconnection	Total Capital	17.21	0	0	0	0	0	0	-560032.442	771721.5229	51365.9263	600231.0091
SW	Medium	Low	Interconnection	Total Capital	22.05	0	0	0	0	0	0	-55058.6273	363044.7555	-566594.58	1173013.79
SW	Small	Mid	Interconnection	Total Capital	17.23	0	0	0	0	0	0	-605774.9391	831092.7558	43597.1038	611295.3516
SW	Medium	Mid	Interconnection	Total Capital	22.17	0	0	0	0	0	0	-59703.7808	402536.2258	-647866.3051	1241967.732
SW	Small	High	Interconnection	Total Capital	33.93	0	0	0	0	0	0	0	-631069.7282	1385198.056	1313780.871
SW	Medium	High	Interconnection	Total Capital	38.17	0	0	0	0	0	0	0	-116324.7782	965237.1476	1292920.326
SW	Small	Low	Interconnection	Annual O&M	17.21	0	0	0	0	0	0	0	271230.0319	1251910.323	2876.94
SW	Medium	Low	Interconnection	Annual O&M	22.05	0	0	0	0	0	0	164523.1139	-347590.2383	1546276.037	-40406.7767
SW	Small	Mid	Interconnection	Annual O&M	17.23	0	0	0	0	0	0	0	271230.0319	1251910.323	2876.94
SW	Medium	Mid	Interconnection	Annual O&M	22.17	0	0	0	0	0	0	164523.1139	-347590.2383	1546276.037	-40406.7767
SW	Small	High	Interconnection	Annual O&M	33.93	0	0	0	0	0	0	1174540.783	-386902.7001	1337372.888	723.1604
SW	Medium	High	Interconnection	Annual O&M	38.17	0	0	0	0	0	0	142753.0832	-301809.514	1511610.796	-35345.6582
SW	Small	Low	New Well Construction	Total Capital	24.83	0	0	0	0	0	0	628206.1808	-605771.3415	437758.3298	220003.705
SW	Medium	Low	New Well Construction	Total Capital	28.36	0	0	0	0	0	0	-128668.7397	872536.2865	-1339364.867	1258633.582
SW	Small	Mid	New Well Construction	Total Capital	25.75	0	0	0	0	0	0	1559164.557	-1723018.32	1107234.322	398078.7007
SW	Medium	Mid	New Well Construction	Total Capital	29.01	0	0	0	0	0	0	-254010.7513	1721705.053	-2694012.854	2491392.114
SW	Small	High	New Well Construction	Total Capital	26.23	0	0	0	0	0	0	1765114.84	-2018136.542	1397596.137	422042.282
SW	Medium	High	New Well Construction	Total Capital	29.84	0	0	0	0	0	0	-296012.9238	2006412.029	-3148814.65	2912158.263

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Cost Equation Parameters for Nontreatment Options															
GW/SW	Size Category	Comp Level	Design Type	Cost Type	Useful Life	C1	C2	C3	C4	C5	C6	C7	C8	C9	C10
SW	Small	Low	New Well Construction	Annual O&M	24.83	0	0	0	0	0	0	-35362.6715	73214.0449	51411.2015	3756.6482
SW	Medium	Low	New Well Construction	Annual O&M	28.36	0	0	0	0	0	0	-41326.1706	106550.8195	-5783.4687	20024.7684
SW	Small	Mid	New Well Construction	Annual O&M	25.75	0	0	0	0	0	0	-35362.6715	73214.0449	51411.2015	3756.6482
SW	Medium	Mid	New Well Construction	Annual O&M	29.01	0	0	0	0	0	0	-41326.1706	106550.8195	-5783.4687	20024.7684
SW	Small	High	New Well Construction	Annual O&M	26.23	0	0	0	0	0	0	-35362.6715	73214.0449	51411.2015	3756.6482
SW	Medium	High	New Well Construction	Annual O&M	29.84	0	0	0	0	0	0	-41326.1706	106550.8195	-5783.4687	20024.7684

Appendix B. Example WBS Model Outputs

Notes:

- To show the variations among both system size and cost level, the examples chosen for each scenario modeled typically include a low-cost small system, a mid-cost medium system, and a high-cost large system.
- Each of the examples is among the individual flow rate-specific estimates used to generate the cost equations presented in Appendix A (see Section 7.1 for details on the method used to develop the equations).

B.1 Example Outputs for GAC

**Granular Activated Carbon(GAC), design 0.500 mgd, average 0.162 mgd
 Groundwater**

Low-Cost Components

Design Type: Pressure

Bed Volumes: 50000

Spent Media: regen off-site (non-haz) (Default)

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1.1	Pressure Vessels - Carbon Steel - Plastic Internals	160,077	30
2.2.1	Residuals Holding Tanks/Basins - Fiberglass Tanks	87,354	20
3.1.1	Process Piping - PVC	969	17
3.2.1	Backwash Piping - PVC	1,646	17
3.3.1	Influent and Treated Water Piping - PVC	969	17
3.4.1	Residuals Piping - PVC	168	17
3.4.2	Residuals Piping - Excavation	1,006	17
3.4.3	Residuals Piping - Bedding	46	17
3.4.5	Residuals Piping - Backfill and Compaction	607	17
3.4.6	Residuals Piping - Thrust Blocks	122	17
4.1.1	Motor/Air Operated (on/off) Valves - Process - Polypropylene/PVC	12,880	20
4.1.2	Motor/Air Operated (on/off) Valves - Backwash - Polypropylene/PVC	12,788	20
4.1.3	Motor/Air Operated (on/off) Valves - Residuals - Polypropylene/PVC	2,163	20
4.2.1	Manual Valves - Influent and treated water - Polypropylene/PVC	1,791	20
4.2.2	Manual Valves - Process - Polypropylene/PVC	1,791	20
4.3.1	Check Valves - Backwash - Polypropylene/PVC	2,167	20
4.3.2	Check Valves - Residuals - Polypropylene/PVC	240	20
4.3.5	Check Valves - Influent - Polypropylene/PVC	1,306	20
5.3	Pumps - Residuals	9,616	17
6.1.1	Instrumentation - Flow Meters - Influent and Treated Water - Propeller	4,796	14
6.3.1	Instrumentation - Flow Meters - Backwash - Propeller	5,645	14
6.4.1	Instrumentation - Flow Meters - Residuals - Propeller	2,238	14
6.7	High/Low Alarm (for holding tanks)	644	14
6.12.1	Sampling Ports - Carbon Steel	250	22
7.1.1	System Controls - PLC Units - PLC racks/power supplies	1,020	8
7.1.2	System Controls - PLC Units - CPUs	851	8
7.1.3	System Controls - PLC Units - I/O discrete input modules	430	8
7.1.4	System Controls - PLC Units - I/O discrete output modules	382	8
7.1.5	System Controls - PLC Units - I/O combination analog modules	1,879	8
7.1.6	System Controls - PLC Units - Ethernet modules	3,016	8
7.1.9	System Controls - PLC Units - UPSs	986	8
7.2.1	System Controls - Operator Equipment - Drive controllers	2,790	14
7.2.2	System Controls - Operator Equipment - Operator interface units	10,492	8
9.1	Media - Initial GAC Charge	55,512	N/A
12.1	Solids drying pad	493	37
14.1.1	Building Structures and HVAC - Building 1 - Low Quality	55,667	37

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
14.5	Building Structures and HVAC - Concrete Pad	3,449	37
Indirect	Indirect and Add-On Costs (contingency from model)	333,296	37
	Process Cost	448,246	
	System Cost	781,542	
	O&M Cost	29,459	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Mobilization and Demobilization	0
Architectural Fees for Treatment Building	0
Site Work	9,590
Yard Piping	3,988
Geotechnical	0
Standby Power	0
Electrical (including yard wiring)	38,913
Contingency	71,372
Process Engineering	89,649
Construction Management and GC Overhead	9,248
Permits	4,141
Pilot Study	51,042
Land Cost	1,564
Installation, Transportation, and O&P (0.0%)	0
Miscellaneous Allowance (10.0%)	44,825
Legal, Fiscal, and Administrative (2.0%)	8,965
Sales Tax (0.0%)	0
Financing during Construction (0.0%)	0

Breakdown of O&M costs	
Manager (14 hrs/yr @ \$52.3563/hr)	716
Clerical (14 hrs/yr @ \$34.0099/hr)	465
Operator (137 hrs/yr @ \$35.3133/hr)	4,831
Materials for residuals pumps (calculated as a percentage of capital)	96
Materials for GAC contactors (calculated as a percentage of capital)	1,601
Building and HVAC maintenance (materials and labor) (550 sf @ \$6.6975/sf/yr)	3,684
Makeup GAC (1403 lbs/yr @ \$2.4322/lb)	3,413
Off-site GAC regeneration (3275 lbs/yr @ \$1.9491/lb)	6,383
Energy for backwash pumps (0 Mwh/yr @ \$0.1225/kWh)	15
Energy for residuals pumps (0 Mwh/yr @ \$0.1225/kWh)	26
Energy for lighting (0 Mwh/yr @ \$0.1225/kWh)	3
Energy for ventilation (0 Mwh/yr @ \$0.1225/kWh)	46
POTW discharge fees (887471 gal/yr @ \$0.0062/gal)	5,490
Holding tanks solids disposal (0 ton/yr @ \$119.7706/ton)	11
Miscellaneous Allowance (0 @ \$)	2,678

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Granular Activated Carbon(GAC), design 5.809 mgd, average 2.455 mgd

Groundwater

Mid-Cost Components

Design Type: Pressure

Bed Volumes: 50000

Spent Media: regen off-site (non-haz) (Default)

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1.1	Pressure Vessels - Carbon Steel - Plastic Internals	1,528,099	35
2.1.1	Backwash Tanks/Basins - Fiberglass Tanks	83,665	25
2.2.1	Residuals Holding Tanks/Basins - Fiberglass Tanks	131,466	25
3.1.1	Process Piping - CPVC	15,770	22
3.2.1	Backwash Piping - CPVC	40,951	22
3.3.1	Influent and Treated Water Piping - CPVC	42,529	22
3.4.1	Residuals Piping - CPVC	3,153	22
3.4.2	Residuals Piping - Excavation	1,089	22
3.4.3	Residuals Piping - Bedding	51	22
3.4.5	Residuals Piping - Backfill and Compaction	658	22
3.4.6	Residuals Piping - Thrust Blocks	252	22
4.1.1	Motor/Air Operated (on/off) Valves - Process - Cast Iron	299,736	25
4.1.2	Motor/Air Operated (on/off) Valves - Backwash - Cast Iron	401,768	25
4.1.3	Motor/Air Operated (on/off) Valves - Residuals - Cast Iron	7,700	25
4.2.1	Manual Valves - Influent and treated water - Cast Iron	5,870	25
4.2.2	Manual Valves - Process - Cast Iron	20,540	25
4.3.1	Check Valves - Backwash - Cast Iron	21,096	25
4.3.2	Check Valves - Residuals - Cast Iron	1,508	25
4.3.5	Check Valves - Influent - Cast Iron	14,924	25
5.2	Pumps - Backwash	66,971	20
5.3	Pumps - Residuals	11,072	20
6.1.1	Instrumentation - Flow Meters - Influent and Treated Water - Venturi	4,557	15
6.3.1	Instrumentation - Flow Meters - Backwash - Venturi	4,025	15
6.4.1	Instrumentation - Flow Meters - Residuals - Venturi	2,396	15
6.6	High/Low Alarms (for backwash tanks)	644	15
6.7	High/Low Alarm (for holding tanks)	644	15
6.8	pH Meters	6,094	15
6.9	Temperature meters	1,590	15
6.1	Turbidity meters	18,551	15
6.11	Head loss sensors	33,445	15
6.12.1	Sampling Ports - Stainless Steel	850	35
7.1.1	System Controls - PLC Units - PLC racks/power supplies	3,060	10
7.1.2	System Controls - PLC Units - CPUs	851	10
7.1.3	System Controls - PLC Units - I/O discrete input modules	860	10
7.1.4	System Controls - PLC Units - I/O discrete output modules	382	10
7.1.5	System Controls - PLC Units - I/O combination analog modules	8,767	10
7.1.6	System Controls - PLC Units - Ethernet modules	3,016	10

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
7.1.7	System Controls - PLC Units - Base expansion modules	321	10
7.1.8	System Controls - PLC Units - Base expansion controller modules	618	10
7.1.9	System Controls - PLC Units - UPSs	986	10
7.2.1	System Controls - Operator Equipment - Drive controllers	8,371	15
7.2.2	System Controls - Operator Equipment - Operator interface units	3,537	10
7.2.3	System Controls - Operator Equipment - PC Workstations	4,326	10
7.2.4	System Controls - Operator Equipment - Printers - laser jet	391	10
7.3.1	System Controls - Controls Software - Operator interface software	91	10
7.3.2	System Controls - Controls Software - PLC programming software	622	10
7.3.3	System Controls - Controls Software - PLC data collection software	671	10
7.3.4	System Controls - Controls Software - Plant intelligence software	20,681	10
8.1.1	Solids Transfer - Eductors for GAC Transfer	11,195	45
9.1	Media - Initial GAC Charge	683,428	N/A
12.1	Solids drying pad	986	40
14.1.1	Building Structures and HVAC - Building 1 - Medium Quality	849,810	40
14.1.3.1	Building Structures and HVAC - Building 1 - Heating and Cooling System - Heat pump	8,152	25
14.5	Building Structures and HVAC - Concrete Pad	81,304	40
Indirect	Indirect and Add-On Costs (contingency from model)	3,147,862	40
	Process Cost	4,464,088	
	System Cost	7,611,950	
	O&M Cost	353,108	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Mobilization and Demobilization	218,818
Architectural Fees for Treatment Building	65,749
Site Work	157,888
Yard Piping	43,634
Geotechnical	0
Standby Power	5,940
Electrical (including yard wiring)	352,482
Contingency	521,172
Process Engineering	535,691
Construction Management and GC Overhead	281,613
Permits	10,308
Pilot Study	166,936
Land Cost	28,735
Installation, Transportation, and O&P (0.0%)	0
Miscellaneous Allowance (10.0%)	446,409
Legal, Fiscal, and Administrative (2.0%)	89,282
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	223,204

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Breakdown of O&M costs	
Manager (79 hrs/yr @ \$66.7054/hr)	5,240
Clerical (79 hrs/yr @ \$43.9163/hr)	3,450
Operator (786 hrs/yr @ \$39.756/hr)	31,233
Materials for backwash pumps (calculated as a percentage of capital)	670
Materials for residuals pumps (calculated as a percentage of capital)	111
Materials for GAC contactors (calculated as a percentage of capital)	15,281
Building and HVAC maintenance (materials and labor) (9160 sf @ \$6.9362/sf/yr)	63,535
Makeup GAC (21268 lbs/yr @ \$2.0848/lb)	44,340
Off-site GAC regeneration (49625 lbs/yr @ \$1.2355/lb)	61,311
Energy for backwash pumps (2 Mwh/yr @ \$0.1225/kWh)	197
Energy for residuals pumps (3 Mwh/yr @ \$0.1225/kwh)	344
Energy for lighting (4 Mwh/yr @ \$0.1225/kwh)	529
Energy for ventilation (9 Mwh/yr @ \$0.1225/kwh)	1,134
Heat pump (cooling mode) (51 Mwh/yr @ \$0.1225/kwh)	6,294
Heat pump (146 Mwh/yr @ \$0.1225/kwh)	17,900
POTW discharge fees (11628900 gal/yr @ \$0.006/gal)	69,269
Holding tanks solids disposal (1 ton/yr @ \$119.7706/ton)	168
Miscellaneous Allowance (0 @ \$)	32,101

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Granular Activated Carbon(GAC), design 56.271 mgd, average 24.863 mgd

Surface Water

High-Cost Components

Design Type: Gravity

Bed Volumes: 50000

Spent Media: regen off-site (non-haz) (Default)

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.2.1	GAC Contact Basins - Concrete	979,731	40
1.2.2	GAC Contact Basins - Internals (Underdrain/Backwash System)	4,336,193	40
1.2.3	GAC Contact Basins - Aluminum Railing	40,920	40
1.2.4	GAC Contact Basins - Aluminum Stairs	6,900	40
1.2.5	GAC Contact Basins - Excavation	418,200	40
1.2.6	GAC Contact Basins - Backfill and Compaction	83,827	40
2.2.1	Residuals Holding Tanks/Basins - Steel Tanks	165,120	35
3.1.1	Process Piping - CPVC	76,552	22
3.2.1	Backwash Piping - PVC	26,200	22
3.3.1	Influent and Treated Water Piping - PVC	32,276	22
3.4.1	Residuals Piping - CPVC	17,347	22
3.4.2	Residuals Piping - Excavation	1,326	22
3.4.3	Residuals Piping - Bedding	64	22
3.4.5	Residuals Piping - Backfill and Compaction	801	22
3.4.6	Residuals Piping - Thrust Blocks	1,316	22
4.1.1	Motor/Air Operated (on/off) Valves - Process - Cast Iron	609,373	25
4.1.2	Motor/Air Operated (on/off) Valves - Backwash - Cast Iron	931,909	25
4.1.3	Motor/Air Operated (on/off) Valves - Residuals - Cast Iron	21,410	25
4.2.1	Manual Valves - Influent and treated water - Cast Iron	37,235	25
4.3.1	Check Valves - Backwash - Cast Iron	118,377	25
4.3.2	Check Valves - Residuals - Cast Iron	7,979	25
4.3.5	Check Valves - Influent - Stainless Steel	49,272	25
5.1	Pumps - Booster	783,275	20
5.2	Pumps - Backwash	315,622	20
5.3	Pumps - Residuals	20,205	20
6.1.1	Instrumentation - Flow Meters - Influent and Treated Water - Magnetic	25,132	15
6.3.1	Instrumentation - Flow Meters - Backwash - Magnetic	16,128	15
6.4.1	Instrumentation - Flow Meters - Residuals - Magnetic	6,629	15
6.5	Level Switches/Alarms (for vessels)	9,011	15
6.7	High/Low Alarm (for holding tanks)	644	15
6.8	pH Meters	42,660	15
6.9	Temperature meters	1,590	15
6.1	Turbidity meters	98,939	15
6.11	Head loss sensors	33,445	15
6.12.1	Sampling Ports - Stainless Steel	850	35
7.1.1	System Controls - PLC Units - PLC racks/power supplies	3,060	10
7.1.2	System Controls - PLC Units - CPUs	851	10

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
7.1.3	System Controls - PLC Units - I/O discrete input modules	1,720	10
7.1.4	System Controls - PLC Units - I/O discrete output modules	382	10
7.1.5	System Controls - PLC Units - I/O combination analog modules	10,019	10
7.1.6	System Controls - PLC Units - Ethernet modules	3,016	10
7.1.7	System Controls - PLC Units - Base expansion modules	321	10
7.1.8	System Controls - PLC Units - Base expansion controller modules	618	10
7.1.9	System Controls - PLC Units - UPSs	986	10
7.2.1	System Controls - Operator Equipment - Drive controllers	23,717	15
7.2.2	System Controls - Operator Equipment - Operator interface units	3,537	10
7.2.3	System Controls - Operator Equipment - PC Workstations	4,326	10
7.2.4	System Controls - Operator Equipment - Printers - laser jet	391	10
7.3.1	System Controls - Controls Software - Operator interface software	91	10
7.3.2	System Controls - Controls Software - PLC programming software	622	10
7.3.3	System Controls - Controls Software - PLC data collection software	671	10
7.3.4	System Controls - Controls Software - Plant intelligence software	20,681	10
8.1.1	Solids Transfer - Eductors for GAC Transfer	96,667	45
9.1	Media - Initial GAC Charge	6,610,302	N/A
12.1	Solids drying pad	5,420	40
14.1.1	Building Structures and HVAC - Building 1 - Medium Quality	2,120,933	40
14.1.2.1	Building Structures and HVAC - Building 1 - Heating System - Natural gas condensing furnace	93,485	25
14.1.3.1	Building Structures and HVAC - Building 1 - Cooling System - Air conditioner	42,794	25
14.2.1	Building Structures and HVAC - Building 2 - Medium Quality	532,409	40
14.2.2.1	Building Structures and HVAC - Building 2 - Heating System - Natural gas condensing furnace	53,140	25
14.2.3.1	Building Structures and HVAC - Building 2 - Cooling System - Air conditioner	94,831	25
14.5	Building Structures and HVAC - Concrete Pad	272,984	40
Indirect	Indirect and Add-On Costs (contingency from model)	11,145,151	40
	Process Cost	19,314,431	
	System Cost	30,459,582	
	O&M Cost	2,522,462	

Totals are computed before component costs are rounded

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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Breakdown of indirect and add-on costs	
Mobilization and Demobilization	475,842
Architectural Fees for Treatment Building	199,056
Site Work	534,800
Yard Piping	116,303
Geotechnical	185,650
Standby Power	99,082
Electrical (including yard wiring)	1,610,386
Contingency	1,764,733
Process Engineering	1,545,155
Construction Management and GC Overhead	819,367
Permits	24,819
Pilot Study	166,936
Land Cost	319,568
Installation, Transportation, and O&P (0.0%)	0
Miscellaneous Allowance (10.0%)	1,931,443
Legal, Fiscal, and Administrative (2.0%)	386,289
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	965,722

Breakdown of O&M costs	
Manager (310 hrs/yr @ \$83.1618/hr)	25,755
Clerical (310 hrs/yr @ \$43.9163/hr)	13,601
Operator (3097 hrs/yr @ \$48.511/hr)	150,240
Materials for booster pumps (calculated as a percentage of capital)	7,833
Materials for backwash pumps (calculated as a percentage of capital)	3,156
Materials for residuals pumps (calculated as a percentage of capital)	202
Materials for GAC contactors (calculated as a percentage of capital)	53,637
Building and HVAC maintenance (materials and labor) (30660 sf @ \$6.9362/sf/yr)	212,663
Makeup GAC (215391 lbs/yr @ \$1.8028/lb)	388,315
Off-site GAC regeneration (502578 lbs/yr @ \$1.2355/lb)	620,930
Energy for booster pumps (1672 Mwh/yr @ \$0.1225/kwh)	204,732
Energy for backwash pumps (11 Mwh/yr @ \$0.1225/kWh)	1,334
Energy for residuals pumps (19 Mwh/yr @ \$0.1225/kwh)	2,331
Energy for lighting (57 Mwh/yr @ \$0.1225/kwh)	6,977
Energy for ventilation (56 Mwh/yr @ \$0.1225/kwh)	6,850
Air conditioning (467 Mwh/yr @ \$0.1225/kwh)	57,141
Natural gas condensing furnace (71192 therms/yr @ \$0.9468/therm)	67,402
POTW discharge fees (78840000 gal/yr @ \$0.0059/gal)	468,345
Holding tanks solids disposal (14 ton/yr @ \$119.7706/ton)	1,701
Miscellaneous Allowance (0 @ \$)	229,315

B.2 Example Outputs for IX

Anion Exchange for PFAS (AX_PFAS), design 0.500 mgd, average 0.162 mgd
Groundwater

Low-Cost Components

Bed Volumes: 120000

Spent Media: incineration (non-hazardous)

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1	Pressure Vessels - Carbon Steel - Plastic Internals	105,615	30
2.1	Ion Exchange Resin - PFAS-Selective	92,584	N/A
4.1	Cartridge Filters - Cartridge Filters	21,811	30
5.1.1	Backwash Piping - PVC	525	17
5.3.1	Process Piping - PVC	646	17
5.5.1	Influent and Treated Water Piping - PVC	646	17
5.7.1	Residuals Piping - PVC	301	17
5.7.2	Residuals Piping - Excavation	1,057	17
5.7.3	Residuals Piping - Bedding	49	17
5.7.4	Residuals Piping - Backfill and Compaction	638	17
5.7.5	Residuals Piping - Thrust Blocks	118	17
6.1.1	Valves and Fittings - Motor/Air Operated (on/off) - Process - Polypropylene/PVC	12,880	20
6.1.2	Valves and Fittings - Motor/Air Operated (on/off) - Backwash - Polypropylene/PVC	8,385	20
6.2.1	Valves and Fittings - Manual - Influent and treated water - Polypropylene/PVC	1,791	20
6.2.2	Valves and Fittings - Manual - Process - Polypropylene/PVC	1,791	20
6.3.2	Valves and Fittings - Check Valves - Influent and Treated Water - Polypropylene/PVC	2,611	20
6.3.5	Valves and Fittings - Check Valves - Residuals - Polypropylene/PVC	246	20
11.1.1	Instrumentation and Controls - Flow Meters - Influent and Treated Water - Propeller	4,796	14
11.3.1	Instrumentation and Controls - Flow Meters - Backwash - Propeller	3,860	14
11.4.1	Instrumentation and Controls - Flow Meters - Residuals - Propeller	2,812	14
11.12	Instrumentation and Controls - Head loss sensors	4,778	14
11.13.1	Instrumentation and Controls - Sampling Ports - Stainless Steel	250	30
12.1.1	System Controls - PLC Units - PLC racks/power supplies	1,020	8
12.1.2	System Controls - PLC Units - CPUs	851	8
12.1.3	System Controls - PLC Units - I/O discrete input modules	430	8
12.1.5	System Controls - PLC Units - I/O combination analog modules	1,879	8
12.1.6	System Controls - PLC Units - Ethernet modules	3,016	8
12.1.9	System Controls - PLC Units - UPSs	986	8
12.2.2	System Controls - Operator Equipment - Operator interface units	10,492	8
13.1.1	Building Structures and HVAC - Building 1 - Small Low Cost Shed	17,160	20
13.3	Building Structures and HVAC - Concrete Pad	1,971	37
Indirect	Indirect and Add-On Costs (contingency from model)	247,902	20
	Process Cost	305,996	

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
	System Cost	553,898	
	O&M Cost	36,008	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Construction Management	6,630
Process Engineering	61,199
Site Work	5,137
Yard Piping	3,723
Geotechnical	0
Standby Power	0
Electrical (including yard wiring)	28,686
Mobilization and Demobilization	0
Architectural Fees for Treatment Building	0
Permits	2,949
Pilot Study	51,042
Land Cost	1,232
Contingency	50,583
Installation, Transportation, and O&P (0.0%)	0
Miscellaneous Allowance (10.0%)	30,600
Legal, Fiscal, and Administrative (2.0%)	6,120
Sales Tax (0.0%)	0
Financing during Construction (0.0%)	0
Instrumentation and Control (0.0%)	0

Breakdown of O&M costs	
Manager (7 hrs/yr @ \$52.3563/hr)	385
Clerical (7 hrs/yr @ \$34.0099/hr)	250
Operator (73 hrs/yr @ \$35.3133/hr)	2,593
Cartridge filter replacement (7 filters/yr @ \$207.9779/sf/yr)	1,497
Building and HVAC maintenance (materials and labor) (300 sf @ \$6.6975/sf/yr)	2,009
PFAS-selective (66 cf/yr @ \$328.9104/cf)	21,667
Energy for backwash/rinse pumps (0 Mwh/yr @ \$0.1225/kwh)	0
Energy for lighting (0 Mwh/yr @ \$0.1225/kwh)	1
Energy for ventilation (0 Mwh/yr @ \$0.1225/kwh)	10
POTW discharge fees (848 gal/yr @ \$0.5134/gal)	435
Spent resin disposal (1 ton/yr @ \$2737.1421/ton)	3,877
Spent cartridge filter disposal (0 ton/yr @ \$119.7706/ton)	10
Miscellaneous Allowance (0 @ \$)	3,273

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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Anion Exchange for PFAS(AX_PFAS), design 5.809 mgd, average 2.455 mgd

Groundwater

Mid-Cost Components

Bed Volumes: 160000

Spent Media: incineration (non-hazardous)

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1	Pressure Vessels - Carbon Steel - Plastic Internals	617,823	35
2.1	Ion Exchange Resin - PFAS-Selective	1,243,192	N/A
3.1.1	Backwash/Rinse Tanks - Fiberglass	36,246	25
4.1	Cartridge Filters - Cartridge Filters	128,792	35
5.1.1	Backwash Piping - CPVC	13,799	22
5.3.1	Process Piping - CPVC	16,663	22
5.5.1	Influent and Treated Water Piping - CPVC	29,770	22
5.7.1	Residuals Piping - CPVC	3,216	22
5.7.2	Residuals Piping - Excavation	1,115	22
5.7.3	Residuals Piping - Bedding	53	22
5.7.4	Residuals Piping - Backfill and Compaction	674	22
5.7.5	Residuals Piping - Thrust Blocks	248	22
6.1.1	Valves and Fittings - Motor/Air Operated (on/off) - Process - Cast Iron	43,481	25
6.1.2	Valves and Fittings - Motor/Air Operated (on/off) - Backwash - Cast Iron	128,458	25
6.2.1	Valves and Fittings - Manual - Influent and treated water - Cast Iron	5,870	25
6.2.2	Valves and Fittings - Manual - Process - Cast Iron	13,695	25
6.3.1	Valves and Fittings - Check Valves - Backwash - Cast Iron	7,979	25
6.3.2	Valves and Fittings - Check Valves - Influent and Treated Water - Cast Iron	29,848	25
6.3.5	Valves and Fittings - Check Valves - Residuals - Cast Iron	1,066	25
7.2	Pumps - Backwash/Rinse	22,639	20
11.1.1	Instrumentation and Controls - Flow Meters - Influent and Treated Water - Venturi	4,557	15
11.3.1	Instrumentation and Controls - Flow Meters - Backwash - Venturi	3,077	15
11.4.1	Instrumentation and Controls - Flow Meters - Residuals - Venturi	2,483	15
11.6	Instrumentation and Controls - High/Low Alarm (for backwash tanks)	644	15
11.11	Instrumentation and Controls - Temperature meters	795	15
11.12	Instrumentation and Controls - Head loss sensors	23,889	15
11.13.1	Instrumentation and Controls - Sampling Ports - Carbon Steel	500	25
11.17	Instrumentation and Controls - Turbidity meters	6,184	15
12.1.1	System Controls - PLC Units - PLC racks/power supplies	2,040	10
12.1.2	System Controls - PLC Units - CPUs	851	10
12.1.3	System Controls - PLC Units - I/O discrete input modules	430	10
12.1.4	System Controls - PLC Units - I/O discrete output modules	382	10
12.1.5	System Controls - PLC Units - I/O combination analog modules	4,383	10
12.1.6	System Controls - PLC Units - Ethernet modules	3,016	10
12.1.7	System Controls - PLC Units - Base expansion modules	160	10
12.1.8	System Controls - PLC Units - Base expansion controller modules	309	10
12.1.9	System Controls - PLC Units - UPSs	986	10
12.2.1	System Controls - Operator Equipment - Drive controllers	2,790	15

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
12.2.2	System Controls - Operator Equipment - Operator interface units	3,537	10
12.2.3	System Controls - Operator Equipment - PC Workstations	4,326	10
12.2.4	System Controls - Operator Equipment - Printers - laser jet	391	10
12.3.1	System Controls - Controls Software - Operator interface software	91	10
12.3.2	System Controls - Controls Software - PLC programming software	622	10
12.3.3	System Controls - Controls Software - PLC data collection software	671	10
12.3.4	System Controls - Controls Software - Plant intelligence software	20,681	10
13.1.1	Building Structures and HVAC - Building 1 - Medium Quality	439,853	40
13.1.3.1	Building Structures and HVAC - Building 1 - Heating and Cooling System - Heat pump	4,970	25
13.3	Building Structures and HVAC - Concrete Pad	37,942	40
Indirect	Indirect and Add-On Costs (contingency from model)	2,165,457	40
	Process Cost	2,915,191	
	System Cost	5,080,648	
	O&M Cost	518,460	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Construction Management	187,285
Process Engineering	349,823
Site Work	75,691
Yard Piping	36,395
Geotechnical	0
Standby Power	2,640
Electrical (including yard wiring)	243,243
Mobilization and Demobilization	142,587
Architectural Fees for Treatment Building	38,621
Permits	2,942
Pilot Study	166,936
Land Cost	17,072
Contingency	406,639
Installation, Transportation, and O&P (0.0%)	0
Miscellaneous Allowance (10.0%)	291,519
Legal, Fiscal, and Administrative (2.0%)	58,304
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	145,760
Instrumentation and Control (0.0%)	0

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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Breakdown of O&M costs	
Manager (39 hrs/yr @ \$66.7054/hr)	2,572
Clerical (39 hrs/yr @ \$43.9163/hr)	1,693
Operator (386 hrs/yr @ \$39.756/hr)	15,330
Cartridge filter replacement (96 filters/yr @ \$225.0723/sf/yr)	21,607
Building and HVAC maintenance (materials and labor) (4420 sf @ \$6.9362/sf/yr)	30,658
PFAS-selective (998 cf/yr @ \$328.9104/cf)	328,352
Energy for backwash/rinse pumps (0 Mwh/yr @ \$0.1225/kwh)	0
Energy for lighting (1 Mwh/yr @ \$0.1225/kwh)	125
Energy for ventilation (3 Mwh/yr @ \$0.1225/kwh)	399
Heat pump (cooling mode) (15 Mwh/yr @ \$0.1225/kwh)	1,874
Heat pump (52 Mwh/yr @ \$0.1225/kwh)	6,379
POTW discharge fees (8164 gal/yr @ \$0.4228/gal)	3,452
Spent resin disposal (21 ton/yr @ \$2737.1421/ton)	58,749
Spent cartridge filter disposal (1 ton/yr @ \$119.7706/ton)	138
Miscellaneous Allowance (0 @ \$)	47,133

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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Anion Exchange for PFAS (AX_PFAS), design 56.271 mgd, average 24.863 mgd

Surface Water

High-Cost Components

Bed Volumes: 120000

Spent Media: incineration (non-hazardous)

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1	Pressure Vessels - Stainless Steel	7,661,480	35
2.1	Ion Exchange Resin - PFAS-Selective	11,733,230	N/A
4.1	Cartridge Filters - Cartridge Filters	884,649	35
5.1.1	Backwash Piping - Stainless Steel	138,044	45
5.3.1	Process Piping - Stainless Steel	166,329	45
5.5.1	Influent and Treated Water Piping - Stainless Steel	419,669	45
5.7.1	Residuals Piping - Stainless Steel	34,728	45
5.7.2	Residuals Piping - Excavation	1,180	45
5.7.3	Residuals Piping - Bedding	57	45
5.7.4	Residuals Piping - Backfill and Compaction	713	45
5.7.5	Residuals Piping - Thrust Blocks	504	45
6.1.1	Valves and Fittings - Motor/Air Operated (on/off) - Process - Stainless Steel	1,272,989	25
6.1.2	Valves and Fittings - Motor/Air Operated (on/off) - Backwash - Stainless Steel	599,105	25
6.2.1	Valves and Fittings - Manual - Influent and treated water - Cast Iron	37,235	25
6.2.2	Valves and Fittings - Manual - Process - Stainless Steel	79,944	25
6.3.1	Valves and Fittings - Check Valves - Backwash - Stainless Steel	9,520	25
6.3.2	Valves and Fittings - Check Valves - Influent and Treated Water - Stainless Steel	98,545	25
6.3.5	Valves and Fittings - Check Valves - Residuals - Stainless Steel	1,672	25
7.2	Pumps - Backwash/Rinse	46,124	20
11.1.1	Instrumentation and Controls - Flow Meters - Influent and Treated Water - Magnetic	25,132	15
11.3.1	Instrumentation and Controls - Flow Meters - Backwash - Magnetic	7,811	15
11.4.1	Instrumentation and Controls - Flow Meters - Residuals - Magnetic	5,493	15
11.11	Instrumentation and Controls - Temperature meters	795	15
11.12	Instrumentation and Controls - Head loss sensors	102,724	15
11.13.1	Instrumentation and Controls - Sampling Ports - Carbon Steel	1,500	25
11.17	Instrumentation and Controls - Turbidity meters	6,184	15
12.1.1	System Controls - PLC Units - PLC racks/power supplies	4,080	10
12.1.2	System Controls - PLC Units - CPUs	851	10
12.1.3	System Controls - PLC Units - I/O discrete input modules	1,290	10
12.1.4	System Controls - PLC Units - I/O discrete output modules	382	10
12.1.5	System Controls - PLC Units - I/O combination analog modules	13,777	10
12.1.6	System Controls - PLC Units - Ethernet modules	3,016	10
12.1.7	System Controls - PLC Units - Base expansion modules	481	10
12.1.8	System Controls - PLC Units - Base expansion controller modules	927	10
12.1.9	System Controls - PLC Units - UPSs	986	10
12.2.1	System Controls - Operator Equipment - Drive controllers	2,790	15

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
12.2.2	System Controls - Operator Equipment - Operator interface units	3,537	10
12.2.3	System Controls - Operator Equipment - PC Workstations	4,326	10
12.2.4	System Controls - Operator Equipment - Printers - laser jet	391	10
12.3.1	System Controls - Controls Software - Operator interface software	91	10
12.3.2	System Controls - Controls Software - PLC programming software	622	10
12.3.3	System Controls - Controls Software - PLC data collection software	671	10
12.3.4	System Controls - Controls Software - Plant intelligence software	20,681	10
13.1.1	Building Structures and HVAC - Building 1 - High Quality	2,217,211	40
13.1.2.1	Building Structures and HVAC - Building 1 - Heating System - Natural gas condensing furnace	67,071	25
13.1.3.1	Building Structures and HVAC - Building 1 - Cooling System - Air conditioner	26,109	25
13.2.1	Building Structures and HVAC - Building 2 - High Quality	307,005	40
13.2.3.1	Building Structures and HVAC - Building 2 - Heating and Cooling System - Heat pump	4,103	25
13.3	Building Structures and HVAC - Concrete Pad	195,622	40
Indirect	Indirect and Add-On Costs (contingency from model)	14,498,491	40
	Process Cost	26,211,376	
	System Cost	40,709,867	
	O&M Cost	4,888,971	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Construction Management	1,104,901
Process Engineering	2,096,910
Site Work	379,994
Yard Piping	488,667
Geotechnical	31,500
Standby Power	15,906
Electrical (including yard wiring)	2,339,426
Mobilization and Demobilization	641,760
Architectural Fees for Treatment Building	174,661
Permits	2,973
Pilot Study	166,936
Land Cost	240,321
Contingency	2,358,603
Installation, Transportation, and O&P (0.0%)	0
Miscellaneous Allowance (10.0%)	2,621,138
Legal, Fiscal, and Administrative (2.0%)	524,228
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	1,310,569
Instrumentation and Control (0.0%)	0

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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Breakdown of O&M costs	
Manager (195 hrs/yr @ \$83.1618/hr)	16,257
Clerical (195 hrs/yr @ \$43.9163/hr)	8,585
Operator (1955 hrs/yr @ \$48.511/hr)	94,831
Cartridge filter replacement (672 filters/yr @ \$234.0797/sf/yr)	157,302
Building and HVAC maintenance (materials and labor) (22190 sf @ \$6.9362/sf/yr)	153,914
PFAS-selective (10110 cf/yr @ \$328.9104/cf)	3,325,379
Energy for backwash/rinse pumps (0 Mwh/yr @ \$0.1225/kwh)	4
Energy for lighting (52 Mwh/yr @ \$0.1225/kwh)	6,374
Energy for ventilation (26 Mwh/yr @ \$0.1225/kwh)	3,198
Air conditioning (73 Mwh/yr @ \$0.1225/kwh)	8,934
Heat pump (cooling mode) (73 Mwh/yr @ \$0.1225/kwh)	8,934
Heat pump (20 Mwh/yr @ \$0.1225/kwh)	2,425
Natural gas condensing furnace (31092 therms/yr @ \$0.9468/therm)	29,437
POTW discharge fees (93663 gal/yr @ \$0.3524/gal)	33,003
Spent resin disposal (217 ton/yr @ \$2737.1421/ton)	594,976
Spent cartridge filter disposal (8 ton/yr @ \$119.7706/ton)	966
Miscellaneous Allowance (0 @ \$)	444,452

B.3 Example Outputs for RO/NF

**Reverse Osmosis / Nanofiltration (RONF), design 0.500 mgd, average 0.162 mgd
 Groundwater**

Low-Cost Components

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1	Membrane Process - Membrane Elements	50,119	N/A
1.2	Membrane Process - RO Pressure Vessels	17,677	17
1.3.1	Membrane Process - Feed Line Connectors - Victaulic, Painted	3,037	20
1.5.1	Membrane Process - Piping On Rack - Feed - Stainless Steel	13,214	40
1.5.2	Membrane Process - Piping On Rack - Permeate - PVC	504	17
1.5.3	Membrane Process - Piping On Rack - Concentrate - Stainless Steel	8,773	40
1.6	Membrane Process - Vessel Support Rack - Steel Beams	15,861	20
1.7	Membrane Process - Markup for Rack Assembly	36,574	23.03638685
2.1.1	Pretreatment Acid Storage Tanks - Plastic (HXLPE)	977	7
2.1.2	Pretreatment Acid Storage Tanks - Secondary Containment - Concrete Curbing	1,479	37
2.1.3	Pretreatment Acid Storage Tanks - Secondary Containment - Chemical Resistant Coating	389	10
2.2.1	Pretreatment Acid Day Tanks - Plastic/XLPE	806	7
2.2.2	Pretreatment Acid Day Tanks - Secondary Containment - Concrete Curbing	740	37
2.2.3	Pretreatment Acid Day Tanks - Secondary Containment - Chemical Resistant Coating	389	10
2.3.1	Pretreatment Antiscalant Tanks - Plastic (XLPE)	814	7
2.3.2	Pretreatment Antiscalant Tanks - Secondary Containment - Concrete Curbing	740	37
2.3.3	Pretreatment Antiscalant Tanks - Secondary Containment - Chemical Resistant Coating	389	10
2.7.1	Cleaning Solution Makeup Tanks - Plastic (XLPE)	2,167	7
2.8.1	Cleaning Chemical Storage Tanks - Acid - Plastic (XLPE)	794	7
2.8.2	Cleaning Chemical Storage Tanks - Acid - Secondary Containment - Concrete Curbing	740	37
2.8.3	Cleaning Chemical Storage Tanks - Acid - Secondary Containment - Chemical Resistant Coating	389	10
2.8.4	Cleaning Chemical Storage Tanks - High pH - Plastic (XLPE)	794	7
2.8.5	Cleaning Chemical Storage Tanks - High pH - Secondary Containment - Concrete Curbing	740	37
2.8.6	Cleaning Chemical Storage Tanks - High pH - Secondary Containment - Chemical Resistant Coating	389	10
3.1.1	Influent and Treated Water Piping - PVC	1,293	17
3.2.1	Cleaning System Piping - PVC	420	17
3.3.1	Residuals Piping - PVC	111,214	17
3.3.2	Residuals Piping - Excavation	308,438	17
3.3.3	Residuals Piping - Bedding	14,937	17
3.3.4	Residuals Piping - Backfill and Compaction	186,281	17
3.3.5	Residuals Piping - Thrust Blocks	59,263	17
4.1.1	Motor/Air Operated (on/off) Valves - Pretreatment acid - Polypropylene/PVC	1,891	20
4.1.2	Motor/Air Operated (on/off) Valves - Antiscalant - Polypropylene/PVC	1,891	20

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
4.1.3	Motor/Air Operated (on/off) Valves - Feed line - Polypropylene/PVC	8,587	20
4.1.4	Motor/Air Operated (on/off) Valves - Concentrate control - Cast Iron	5,134	20
4.1.10	Motor/Air Operated (on/off) Valves - Cleaning - Polypropylene/PVC	40,248	20
4.2.1	Manual Valves - Influent and treated water - Polypropylene/PVC	1,791	20
4.3.1	Check Valves - Residuals - Polypropylene/PVC	665	20
4.3.2	Check Valves - Influent - Polypropylene/PVC	1,306	20
4.3.4	Check Valves - Feed pumps - Polypropylene/PVC	2,611	20
4.3.5	Check Valves - Cleaning - Polypropylene/PVC	1,996	20
5.1.1	Acid Metering Pumps for Pretreatment - PVC - Electric	2,510	15
5.2.1	Antiscalant Metering Pumps for Pretreatment - PVC - Electric	2,419	15
5.4	Pumps - Feed Water	57,482	17
5.7	Pumps - Cleaning Pumps (separate for acid and caustic)	1,138	17
6.1	Screens and Filters - Cartridge Filters for Feed	27,306	30
6.2.1	Screens and Filters - Security Screens for Cleaning - Simplex Basket Screens	7,431	30
6.3	Screens and Filters - Cartridge Filters for Cleaning	16,126	30
8.1	Teflon Immersion Heaters for Cleaning Tanks	4,307	14
9.1.1	Instrumentation - Flow Meters - Influent and Treated Water Line - Propeller	9,592	14
9.2.1	Instrumentation - Flow Meters - Membrane Trains - Feed Line - Propeller	9,592	14
9.3.1	Instrumentation - Flow Meters - Membrane Trains - Permeate Line - Propeller	7,719	14
9.3.1	Instrumentation - Flow Meters - Membrane Trains - Concentrate Line - Propeller	6,171	14
9.4.1	Instrumentation - Flow Meters - Cleaning - Propeller	14,388	14
9.5.1	Instrumentation - Propeller	3,860	14
9.6	Instrumentation - Level Switches/Alarms (for cleaning tanks)	1,287	14
9.7	Instrumentation - High/Low Alarms (for pretreatment chemical tanks)	1,287	14
9.8	Instrumentation - High/Low Alarms (for cleaning chemical storage tanks)	1,287	14
9.1	Instrumentation - pH meters	12,188	14
9.11	Instrumentation - Temperature meters	2,384	14
9.12	Instrumentation - Conductivity meters	18,244	14
9.13	Instrumentation - Head loss sensors	9,556	14
9.14.1	Instrumentation - Sampling ports - Carbon Steel	900	22
10.1.1	System Controls - PLC Units - PLC racks/power supplies	2,040	8
10.1.2	System Controls - PLC Units - CPUs	851	8
10.1.3	System Controls - PLC Units - I/O discrete input modules	860	8
10.1.4	System Controls - PLC Units - I/O discrete output modules	382	8
10.1.5	System Controls - PLC Units - I/O combination analog modules	5,636	8
10.1.6	System Controls - PLC Units - Ethernet modules	3,016	8
10.1.7	System Controls - PLC Units - Base expansion modules	160	8
10.1.8	System Controls - PLC Units - Base expansion controller modules	309	8
10.1.9	System Controls - PLC Units - UPSs	986	8
10.2.1	System Controls - Operator Equipment - Drive controllers	12,556	14
10.2.2	System Controls - Operator Equipment - Operator interface units	10,492	8

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
11.1.1	Building Structures and HVAC - Building 1 - Low Quality	142,973	37
11.4	Building Structures and HVAC - Concrete Pad	13,797	37
Indirect	Indirect and Add-On Costs (contingency from model)	955,062	37
	Process Cost	1,317,693	
	System Cost	2,272,755	
	O&M Cost	117,342	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Mobilization and Demobilization	79,800
Construction Management and GC Overhead	87,042
Contingency	181,904
Process Engineering	263,539
Site Work	26,714
Yard Piping	3,725
Geotechnical	0
Standby Power	0
Electrical (including yard wiring)	116,092
Architectural Fees for Treatment Building	0
Pilot Study	1,243
Land Cost	2,559
Permits	34,321
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	131,769
Legal, Fiscal, and Administrative (2.0%)	26,354
Sales Tax (0.0%)	0
Financing during Construction (0.0%)	0

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Breakdown of O&M costs	
Manager (124 hrs/yr @ \$52.3563/hr)	6,496
Administrative (124 hrs/yr @ \$34.0099/hr)	4,220
Operator (1241 hrs/yr @ \$35.3133/hr)	43,815
Materials for pretreatment (calculated as a percentage of capital)	322
Cartridge filter replacement (19 filters/yr @ \$188.4333/filter)	3,553
Materials for membrane process (calculated as a percentage of capital)	501
Membrane replacement (10 element/yr @ \$668.2566/element)	6,873
Materials for cleaning (calculated as a percentage of capital)	247
Materials for feed water and booster pumps (calculated as a percentage of capital)	575
Building and HVAC maintenance (materials and labor) (1560 sf @ \$6.6975/sf/yr)	10,448
Sulfuric Acid - Small Qty (23565 lbs/yr @ \$0.223/lb)	5,256
Antiscalant - Basic (2468 lbs/yr @ \$3.3516/lb)	8,271
Membrane Cleaner - Low pH Sulfate Control (13 gal/yr @ \$39.192/gal)	497
Membrane Cleaner - High pH Detergent (13 gal/yr @ \$44.8439/gal)	569
Energy for feed water and booster pumps (119 Mwh/yr @ \$0.1225/kwh)	14,533
Energy for lighting (1 Mwh/yr @ \$0.1225/kwh)	71
Energy for ventilation (3 Mwh/yr @ \$0.1225/kwh)	367
Spent cartridge filter disposal (0 ton/yr @ \$119.7706/ton)	37
Spent membrane element disposal (0 ton/yr @ \$119.7706/ton)	23
Miscellaneous Allowance (0 @ \$)	10,667

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**Reverse Osmosis / Nanofiltration(RO/NF), design 5.809 mgd, average 2.455 mgd
Groundwater**

Mid-Cost Components

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1	Membrane Process - Membrane Elements	803,996	N/A
1.2	Membrane Process - RO Pressure Vessels	264,211	22
1.3.1	Membrane Process - Feed Line Connectors - Victaulic, Galvanized	52,755	25
1.5.1	Membrane Process - Piping On Rack - Feed - Stainless Steel	242,957	45
1.5.2	Membrane Process - Piping On Rack - Permeate - PVC	10,663	22
1.5.3	Membrane Process - Piping On Rack - Concentrate - Stainless Steel	181,692	45
1.6	Membrane Process - Vessel Support Rack - Steel Beams	66,014	25
1.7	Membrane Process - Markup for Rack Assembly	371,978	30.76375793
2.1.1	Pretreatment Acid Storage Tanks - Fiberglass	15,193	10
2.1.2	Pretreatment Acid Storage Tanks - Secondary Containment - Concrete Curbing	2,958	40
2.1.3	Pretreatment Acid Storage Tanks - Secondary Containment - Chemical Resistant Coating	1,167	10
2.2.1	Pretreatment Acid Day Tanks - Fiberglass	3,778	10
2.2.2	Pretreatment Acid Day Tanks - Secondary Containment - Concrete Curbing	740	40
2.2.3	Pretreatment Acid Day Tanks - Secondary Containment - Chemical Resistant Coating	389	10
2.3.1	Pretreatment Antiscalant Tanks - Fiberglass	5,386	10
2.3.2	Pretreatment Antiscalant Tanks - Secondary Containment - Concrete Curbing	1,479	40
2.3.3	Pretreatment Antiscalant Tanks - Secondary Containment - Chemical Resistant Coating	389	10
2.4.1	Pretreatment Antiscalant Day Tanks - Fiberglass	1,369	10
2.4.2	Pretreatment Antiscalant Day Tanks - Secondary Containment - Concrete Curbing	740	40
2.4.3	Pretreatment Antiscalant Day Tanks - Secondary Containment - Chemical Resistant Coating	389	10
2.7.1	Cleaning Solution Makeup Tanks - Fiberglass	39,164	10
2.8.1	Cleaning Chemical Storage Tanks - Acid - Fiberglass	2,595	10
2.8.2	Cleaning Chemical Storage Tanks - Acid - Secondary Containment - Concrete Curbing	740	40
2.8.3	Cleaning Chemical Storage Tanks - Acid - Secondary Containment - Chemical Resistant Coating	389	10
2.8.4	Cleaning Chemical Storage Tanks - High pH - Fiberglass	2,595	10
2.8.5	Cleaning Chemical Storage Tanks - High pH - Secondary Containment - Concrete Curbing	2,219	40
2.8.6	Cleaning Chemical Storage Tanks - High pH - Secondary Containment - Chemical Resistant Coating	389	10
3.1.1	Influent and Treated Water Piping - CPVC	42,422	22
3.2.1	Cleaning System Piping - CPVC	3,531	22
3.3.1	Residuals Piping - CPVC	1,266,369	22
3.3.2	Residuals Piping - Excavation	375,051	22
3.3.3	Residuals Piping - Bedding	19,102	22
3.3.4	Residuals Piping - Backfill and Compaction	226,512	22

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
3.3.5	Residuals Piping - Thrust Blocks	208,364	22
4.1.1	Motor/Air Operated (on/off) Valves - Pretreatment acid - Stainless Steel	990	25
4.1.2	Motor/Air Operated (on/off) Valves - Antiscalant - Stainless Steel	990	25
4.1.3	Motor/Air Operated (on/off) Valves - Feed line - Cast Iron	69,907	25
4.1.4	Motor/Air Operated (on/off) Valves - Concentrate control - Stainless Steel	21,371	25
4.1.10	Motor/Air Operated (on/off) Valves - Cleaning - Stainless Steel	222,326	25
4.2.1	Manual Valves - Influent and treated water - Cast Iron	10,552	25
4.3.1	Check Valves - Residuals - Cast Iron	6,898	25
4.3.2	Check Valves - Influent - Cast Iron	20,013	25
4.3.4	Check Valves - Feed pumps - Cast Iron	27,592	25
4.3.5	Check Valves - Cleaning - Cast Iron	5,532	25
5.1.1	Acid Metering Pumps for Pretreatment - PVC - Electric	3,467	20
5.2.1	Antiscalant Metering Pumps for Pretreatment - Stainless Steel - Electric	4,927	20
5.4	Pumps - Feed Water	532,976	20
5.7	Pumps - Cleaning Pumps (separate for acid and caustic)	6,253	20
6.1	Screens and Filters - Cartridge Filters for Feed	153,356	35
6.2.1	Screens and Filters - Security Screens for Cleaning - Simplex Basket Screens	38,236	35
6.3	Screens and Filters - Cartridge Filters for Cleaning	93,117	35
8.1	Teflon Immersion Heaters for Cleaning Tanks	30,166	15
9.1.1	Instrumentation - Flow Meters - Influent and Treated Water Line - Venturi	10,244	15
9.2.1	Instrumentation - Flow Meters - Membrane Trains - Feed Line - Venturi	10,590	15
9.3.1	Instrumentation - Flow Meters - Membrane Trains - Permeate Line - Venturi	9,230	15
9.3.1	Instrumentation - Flow Meters - Membrane Trains - Concentrate Line - Venturi	9,230	15
9.4.1	Instrumentation - Flow Meters - Cleaning - Venturi	76,828	15
9.5.1	Instrumentation - Venturi	3,530	15
9.6	Instrumentation - Level Switches/Alarms (for cleaning tanks)	1,287	15
9.7	Instrumentation - High/Low Alarms (for pretreatment chemical tanks)	1,287	15
9.8	Instrumentation - High/Low Alarms (for cleaning chemical storage tanks)	1,287	15
9.1	Instrumentation - pH meters	12,188	15
9.11	Instrumentation - Temperature meters	2,384	15
9.12	Instrumentation - Conductivity meters	25,085	15
9.13	Instrumentation - Head loss sensors	14,334	15
9.14.1	Instrumentation - Sampling ports - Stainless Steel	8,650	35
10.1.1	System Controls - PLC Units - PLC racks/power supplies	4,080	10
10.1.2	System Controls - PLC Units - CPUs	851	10
10.1.3	System Controls - PLC Units - I/O discrete input modules	3,440	10
10.1.4	System Controls - PLC Units - I/O discrete output modules	382	10
10.1.5	System Controls - PLC Units - I/O combination analog modules	10,019	10
10.1.6	System Controls - PLC Units - Ethernet modules	3,016	10
10.1.7	System Controls - PLC Units - Base expansion modules	481	10
10.1.8	System Controls - PLC Units - Base expansion controller modules	927	10

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
10.1.9	System Controls - PLC Units - UPSs	986	10
10.2.1	System Controls - Operator Equipment - Drive controllers	32,088	15
10.2.2	System Controls - Operator Equipment - Operator interface units	3,537	10
10.2.3	System Controls - Operator Equipment - PC Workstations	4,326	10
10.2.4	System Controls - Operator Equipment - Printers - laser jet	391	10
10.3.1	System Controls - Controls Software - Operator interface software	91	10
10.3.2	System Controls - Controls Software - PLC programming software	622	10
10.3.3	System Controls - Controls Software - PLC data collection software	671	10
10.3.4	System Controls - Controls Software - Plant intelligence software	20,681	10
11.1.1	Building Structures and HVAC - Building 1 - Medium Quality	524,472	40
11.1.2.1	Building Structures and HVAC - Building 1 - Heating System - Natural gas condensing furnace	64,500	25
11.4	Building Structures and HVAC - Concrete Pad	58,637	40
Indirect	Indirect and Add-On Costs (contingency from model)	3,634,458	40
	Process Cost	6,386,707	
	System Cost	10,021,165	
	O&M Cost	1,005,211	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs		
Mobilization and Demobilization		248,717
Construction Management and GC Overhead		265,845
Contingency		577,576
Process Engineering		603,798
Site Work		91,959
Yard Piping		15,910
Geotechnical		0
Standby Power		128,125
Electrical (including yard wiring)		447,100
Architectural Fees for Treatment Building		39,246
Pilot Study		72,728
Land Cost		19,439
Permits		38,274
Installation, Transportation, and O&P (0.0%)		0
Instrumentation and Control (0.0%)		0
Miscellaneous Allowance (10.0%)		638,671
Legal, Fiscal, and Administrative (2.0%)		127,734
Sales Tax (0.0%)		0
Financing during Construction (5.0%)		319,335

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Breakdown of O&M costs	
Manager (604 hrs/yr @ \$66.7054/hr)	40,263
Administrative (604 hrs/yr @ \$43.9163/hr)	26,508
Operator (6036 hrs/yr @ \$39.756/hr)	239,968
Materials for pretreatment (calculated as a percentage of capital)	1,594
Cartridge filter replacement (96 filters/yr @ \$231.2489/filter)	22,200
Materials for membrane process (calculated as a percentage of capital)	8,040
Membrane replacement (165 element/yr @ \$626.4905/element)	103,371
Materials for cleaning (calculated as a percentage of capital)	1,376
Materials for feed water and booster pumps (calculated as a percentage of capital)	5,330
Building and HVAC maintenance (materials and labor) (5370 sf @ \$6.8511/sf/yr)	36,790
Sulfuric Acid - Small Qty (253899 lbs/yr @ \$0.223/lb)	56,630
Antiscalant - Basic (28052 lbs/yr @ \$3.3516/lb)	94,022
Membrane Cleaner - Low pH Sulfate Control (203 gal/yr @ \$39.192/gal)	7,959
Membrane Cleaner - High pH Detergent (203 gal/yr @ \$44.8439/gal)	9,107
Energy for feed water and booster pumps (1872 Mwh/yr @ \$0.1225/kwh)	229,218
Energy for lighting (10 Mwh/yr @ \$0.1225/kwh)	1,191
Energy for ventilation (15 Mwh/yr @ \$0.1225/kwh)	1,858
Natural gas condensing furnace (29515 therms/yr @ \$0.9468/therm)	27,944
Spent cartridge filter disposal (2 ton/yr @ \$119.7706/ton)	197
Spent membrane element disposal (2 ton/yr @ \$119.7706/ton)	263
Miscellaneous Allowance (0 @ \$)	91,383

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Reverse Osmosis / Nanofiltration (RONF), design 56.271 mgd, average 24.863 mgd

Surface Water

High-Cost Components

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1	Membrane Process - Membrane Elements	6,459,814	N/A
1.2	Membrane Process - RO Pressure Vessels	2,006,152	22
1.3.1	Membrane Process - Feed Line Connectors - Victaulic, Galvanized	370,881	25
1.5.1	Membrane Process - Piping On Rack - Feed - Stainless Steel	1,708,064	45
1.5.2	Membrane Process - Piping On Rack - Permeate - PVC	74,966	22
1.5.3	Membrane Process - Piping On Rack - Concentrate - Stainless Steel	1,277,350	45
1.6	Membrane Process - Vessel Support Rack - Steel Beams	486,047	25
1.7	Membrane Process - Markup for Rack Assembly	2,785,737	30.42915982
2.1.1	Pretreatment Acid Storage Tanks - Fiberglass	68,975	10
2.1.2	Pretreatment Acid Storage Tanks - Secondary Containment - Concrete Curbing	21,449	40
2.1.3	Pretreatment Acid Storage Tanks - Secondary Containment - Chemical Resistant Coating	5,059	10
2.2.1	Pretreatment Acid Day Tanks - Fiberglass	16,724	10
2.2.2	Pretreatment Acid Day Tanks - Secondary Containment - Concrete Curbing	3,698	40
2.2.3	Pretreatment Acid Day Tanks - Secondary Containment - Chemical Resistant Coating	1,557	10
2.3.1	Pretreatment Antiscalant Tanks - Stainless Steel	14,625	35
2.3.2	Pretreatment Antiscalant Tanks - Secondary Containment - Concrete Curbing	2,958	40
2.3.3	Pretreatment Antiscalant Tanks - Secondary Containment - Chemical Resistant Coating	1,167	10
2.4.1	Pretreatment Antiscalant Day Tanks - Stainless Steel	2,210	35
2.4.2	Pretreatment Antiscalant Day Tanks - Secondary Containment - Concrete Curbing	740	40
2.4.3	Pretreatment Antiscalant Day Tanks - Secondary Containment - Chemical Resistant Coating	389	10
2.7.1	Cleaning Solution Makeup Tanks - Stainless Steel	45,951	35
2.8.1	Cleaning Chemical Storage Tanks - Acid - Fiberglass	4,712	10
2.8.2	Cleaning Chemical Storage Tanks - Acid - Secondary Containment - Concrete Curbing	1,479	40
2.8.3	Cleaning Chemical Storage Tanks - Acid - Secondary Containment - Chemical Resistant Coating	389	10
2.8.4	Cleaning Chemical Storage Tanks - High pH - Stainless Steel	2,897	35
2.8.5	Cleaning Chemical Storage Tanks - High pH - Secondary Containment - Concrete Curbing	4,438	40
2.8.6	Cleaning Chemical Storage Tanks - High pH - Secondary Containment - Chemical Resistant Coating	778	10
3.1.1	Influent and Treated Water Piping - Stainless Steel	447,647	45
3.2.1	Cleaning System Piping - Stainless Steel	29,245	45
3.3.1	Residuals Piping - Steel	2,945,204	35
3.3.2	Residuals Piping - Excavation	533,347	22
3.3.3	Residuals Piping - Bedding	28,372	22
3.3.4	Residuals Piping - Backfill and Compaction	322,116	22

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
3.3.5	Residuals Piping - Thrust Blocks	721,352	22
4.1.1	Motor/Air Operated (on/off) Valves - Pretreatment acid - Stainless Steel	990	25
4.1.2	Motor/Air Operated (on/off) Valves - Antiscalant - Stainless Steel	990	25
4.1.3	Motor/Air Operated (on/off) Valves - Feed line - Stainless Steel	493,999	25
4.1.4	Motor/Air Operated (on/off) Valves - Concentrate control - Stainless Steel	142,470	25
4.1.5	Motor/Air Operated (on/off) Valves - Stage 2 boost - Stainless Steel	21,371	25
4.1.10	Motor/Air Operated (on/off) Valves - Cleaning - Stainless Steel	658,743	25
4.2.1	Manual Valves - Influent and treated water - Cast Iron	37,235	25
4.3.1	Check Valves - Residuals - Stainless Steel	15,557	25
4.3.2	Check Valves - Influent - Stainless Steel	49,272	25
4.3.4	Check Valves - Feed pumps - Stainless Steel	138,044	25
4.3.5	Check Valves - Cleaning - Stainless Steel	5,015	25
5.1.1	Acid Metering Pumps for Pretreatment - PVC - Motor Driven	14,074	20
5.2.1	Antiscalant Metering Pumps for Pretreatment - PVC - Motor Driven	7,570	20
5.4	Pumps - Feed Water	1,535,722	20
5.5	Pumps - Booster pumps, stage 2	77,650	20
5.7	Pumps - Cleaning Pumps (separate for acid and caustic)	7,007	20
6.1	Screens and Filters - Cartridge Filters for Feed	1,022,414	35
6.2.1	Screens and Filters - Security Screens for Cleaning - Simplex Basket Screens	42,748	35
6.3	Screens and Filters - Cartridge Filters for Cleaning	100,666	35
8.1	Teflon Immersion Heaters for Cleaning Tanks	33,585	15
9.1.1	Instrumentation - Flow Meters - Influent and Treated Water Line - Magnetic	50,265	15
9.2.1	Instrumentation - Flow Meters - Membrane Trains - Feed Line - Magnetic	156,229	15
9.3.1	Instrumentation - Flow Meters - Membrane Trains - Permeate Line - Magnetic	132,579	15
9.3.1	Instrumentation - Flow Meters - Membrane Trains - Concentrate Line - Magnetic	132,579	15
9.4.1	Instrumentation - Flow Meters - Cleaning - Magnetic	427,252	15
9.5.1	Instrumentation - Magnetic	13,094	15
9.6	Instrumentation - Level Switches/Alarms (for cleaning tanks)	1,287	15
9.7	Instrumentation - High/Low Alarms (for pretreatment chemical tanks)	1,287	15
9.8	Instrumentation - High/Low Alarms (for cleaning chemical storage tanks)	1,287	15
9.1	Instrumentation - pH meters	12,188	15
9.11	Instrumentation - Temperature meters	2,384	15
9.12	Instrumentation - Conductivity meters	141,389	15
9.13	Instrumentation - Head loss sensors	90,780	15
9.14.1	Instrumentation - Sampling ports - Stainless Steel	60,000	35
10.1.1	System Controls - PLC Units - PLC racks/power supplies	15,300	10
10.1.2	System Controls - PLC Units - CPUs	851	10
10.1.3	System Controls - PLC Units - I/O discrete input modules	18,919	10
10.1.4	System Controls - PLC Units - I/O discrete output modules	765	10
10.1.5	System Controls - PLC Units - I/O combination analog modules	41,330	10

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WBS #	Item	Total Cost (\$)	Useful Life (yrs)
10.1.6	System Controls - PLC Units - Ethernet modules	3,016	10
10.1.7	System Controls - PLC Units - Base expansion modules	2,244	10
10.1.8	System Controls - PLC Units - Base expansion controller modules	4,327	10
10.1.9	System Controls - PLC Units - UPSs	986	10
10.2.1	System Controls - Operator Equipment - Drive controllers	73,943	15
10.2.2	System Controls - Operator Equipment - Operator interface units	3,537	10
10.2.3	System Controls - Operator Equipment - PC Workstations	21,632	10
10.2.4	System Controls - Operator Equipment - Printers - laser jet	782	10
10.3.1	System Controls - Controls Software - Operator interface software	91	10
10.3.2	System Controls - Controls Software - PLC programming software	3,110	10
10.3.3	System Controls - Controls Software - PLC data collection software	3,355	10
10.3.4	System Controls - Controls Software - Plant intelligence software	103,404	10
10.3.5	System Controls - Controls Software - Early warning software	116,745	10
11.1.1	Building Structures and HVAC - Building 1 - High Quality	740,869	40
11.1.2.1	Building Structures and HVAC - Building 1 - Heating System - Natural gas condensing furnace	148,374	25
11.1.3.1	Building Structures and HVAC - Building 1 - Heating and Cooling System - Air conditioner	580,415	25
11.2.1	Building Structures and HVAC - Building 2 - High Quality	382,285	40
11.2.3.1	Building Structures and HVAC - Building 2 - Heating and Cooling System - Heat pump	3,719	25
11.3.1	Building Structures and HVAC - Building 3 - High Quality	1,883,430	40
11.3.3.1	Building Structures and HVAC - Building 3 - Heating and Cooling System - Heat pump	5,535	25
11.4	Building Structures and HVAC - Concrete Pad	310,925	40
Indirect	Indirect and Add-On Costs (contingency from model)	15,495,113	40
	Process Cost	30,494,099	
	System Cost	45,989,212	
	O&M Cost	7,976,137	

Totals are computed before component costs are rounded

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of indirect and add-on costs	
Mobilization and Demobilization	620,762
Construction Management and GC Overhead	1,049,501
Contingency	2,283,454
Process Engineering	1,989,857
Site Work	427,600
Yard Piping	102,278
Geotechnical	0
Standby Power	956,084
Electrical (including yard wiring)	2,191,608
Architectural Fees for Treatment Building	183,343
Pilot Study	152,123
Land Cost	295,730
Permits	58,777
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	3,049,410
Legal, Fiscal, and Administrative (2.0%)	609,882
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	1,524,705

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of O&M costs	
Manager (3074 hrs/yr @ \$83.1618/hr)	255,674
Administrative (3074 hrs/yr @ \$43.9163/hr)	135,017
Operator (30744 hrs/yr @ \$48.511/hr)	1,491,431
Materials for pretreatment (calculated as a percentage of capital)	10,400
Cartridge filter replacement (1440 filters/yr @ \$235.0601/filter)	338,487
Materials for membrane process (calculated as a percentage of capital)	64,598
Membrane replacement (1856 element/yr @ \$626.4905/element)	1,162,766
Materials for cleaning (calculated as a percentage of capital)	1,504
Materials for feed water and booster pumps (calculated as a percentage of capital)	16,134
Building and HVAC maintenance (materials and labor) (24970 sf @ \$6.9362/sf/yr)	173,196
Sulfuric Acid - Large Qty (4008879 lbs/yr @ \$0.1567/lb)	628,329
Antiscalant - Basic (201471 lbs/yr @ \$3.3516/lb)	675,261
Membrane Cleaner - Low pH Sulfate Control (2194 gal/yr @ \$39.192/gal)	85,970
Membrane Cleaner - High pH Detergent (2194 gal/yr @ \$44.8439/gal)	98,368
Energy for feed water and booster pumps (15114 Mwh/yr @ \$0.1225/kwh)	1,850,830
Energy for lighting (66 Mwh/yr @ \$0.1225/kwh)	8,036
Energy for ventilation (97 Mwh/yr @ \$0.1225/kwh)	11,826
Air conditioning (1258 Mwh/yr @ \$0.1225/kwh)	154,057
Heat pump (31 Mwh/yr @ \$0.1225/kwh)	3,803
Heat pump (96 Mwh/yr @ \$0.1225/kwh)	11,720
Natural gas condensing furnace (71125 therms/yr @ \$0.9468/therm)	67,339
Spent cartridge filter disposal (17 ton/yr @ \$119.7706/ton)	2,070
Spent membrane element disposal (35 ton/yr @ \$119.7706/ton)	4,216
Miscellaneous Allowance (0 @ \$)	725,103

B.4 Example Outputs for POU RO

Point of Use/Point of Entry(POU), design 0.500 mgd, average 0.162 mgd (481 households)

Groundwater

Contaminant: PFAS

Treatment Technology: POU Reverse Osmosis

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1	Installed Treatment Equipment - POU/POE Unit Purchase	112,927	10
1.2	Installed Treatment Equipment - POU/POE Installation	44,933	10
1.3	Installed Treatment Equipment - Scheduling Time	8,400	N/A
2.1.1	Public Education - Technical Labor - Develop materials	353	N/A
2.1.3	Public Education - Technical Labor - Meetings	71	N/A
2.1.4	Public Education - Technical Labor - Post-meeting	71	N/A
2.2.1	Public Education - Clerical Labor - Develop materials	204	N/A
2.2.3	Public Education - Clerical Labor - Meetings	68	N/A
2.2.4	Public Education - Clerical Labor - Post-meeting	68	N/A
2.3.1	Public Education - Printed Material - Meeting flyers	19	N/A
2.3.2	Public Education - Printed Material - Meeting ads	74	N/A
2.3.4	Public Education - Printed Material - Meeting handouts	277	N/A
2.3.5	Public Education - Printed Material - Billing mailers	185	N/A
3.1	Initial Year Monitoring 1 - Sampling time	2,905	N/A
3.3	Initial Year Monitoring 1 - Analysis	102,708	N/A
3.4	Initial Year Monitoring 1 - Analysis (total coliform)	11,128	N/A
3.5	Initial Year Monitoring 1 - Shipping	1,033	N/A
Indirect	Indirect and Add-On Costs (contingency from model)	56,529	10
	Process Cost	285,425	
	System Cost	341,954	
	O&M Cost	112,626	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Permitting	4,988
Pilot Testing	4,988
Legal	4,988
Engineering	24,939
Contingency	16,626

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Breakdown of O&M costs	
POU/POE Maintenance	11,339
Information updates	424
Maintenance Scheduling	10,921
Information updates	408
Sediment Pre-Filter	6,683
Pre-GAC Filter Cartridge	11,425
Post-GAC Filter Cartridge	6,480
RO Membrane	5,602
Billing mailers	277
Sampling time	1,457
Analysis	51,510
Shipping	519

B.5 Example Outputs for Nontreatment Options

Non-Treatment(NON), design 0.500 mgd, average 0.162 mgd

Groundwater

Low-Cost Components

Design Type: Interconnection

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
2.1.1	Vaults - Booster Pump - Concrete	4,911	37
2.1.2	Vaults - Booster Pump - Excavation	5,789	37
2.1.3	Vaults - Booster Pump - Backfill and Compaction	2,317	37
3.1.1	Piping - Interconnect - PVC	161,565	17
3.1.2	Piping - Interconnect - Excavation	90,543	17
3.1.3	Piping - Interconnect - Backfill and Compaction	54,684	17
3.1.4	Piping - Interconnect - Asphalt Patch	93,519	17
4.1.1	Valves - Isolation and Street - Ductile Iron	22,950	20
4.2.1	Valves - Motor/Air Operated (on/off) - Booster Pump - Polypropylene/PVC	1,791	20
5.1	Pumps - Interconnect Booster Pump	22,852	17
6.1.1	Instrumentation - Flow Meters - Interconnect - Propeller	4,796	14
7.1	System Controls - Remote Telemetry Units (RTUs)	1,215	8
7.3	System Controls - Drive Controllers	1,395	14
Indirect	Indirect and Add-On Costs (contingency from model)	310,723	17
	Process Cost	468,328	
	System Cost	779,051	
	O&M Cost	211,778	

Totals are computed before component costs are rounded

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of indirect and add-on costs	
Contingency	48,821
Process Engineering	93,387
Construction Management and GC Overhead	37,608
Site Work	0
Yard Piping	0
Geotechnical	0
Standby Power	0
Electrical (including yard wiring)	46,693
Mobilization and Demobilization	28,016
Architectural Fees for Treatment Building	0
Permits	0
Pilot Study	0
Land Cost	0
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	46,833
Legal, Fiscal, and Administrative (2.0%)	9,367
Sales Tax (0.0%)	0
Financing during Construction (0.0%)	0

Breakdown of O&M costs	
Manager (3 hrs/yr @ \$52.3563/hr)	164
Administrative (3 hrs/yr @ \$35.3133/hr)	111
Operator (31 hrs/yr @ \$34.0099/hr)	1,066
Purchased Water (59130 K gal @ \$3.1748K gal)	187,729
Booster pump (calculated as a percentage of capital)	229
Energy for booster pumps (26 Mwh/yr @ \$0.1225/kwh)	3,228
Miscellaneous Allowance (0 @ \$)	19,253

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Non-Treatment(NON), design 0.500 mgd, average 0.162 mgd

Groundwater

Low-Cost Components

Design Type: New Well Construction

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1.1	Well Items - Well Casing - PVC	13,474	27
1.2.1	Well Items - Well screen - PVC Schedule 40	14,356	27
1.3.1	Well Items - Plugs - PVC	312	27
1.4	Well Items - Well Drilling	72,085	27
1.5	Well Items - Gravel Pack	10,244	27
1.6	Well Items - Well Development	770	27
1.7	Well Items - Grout Seal	3,072	27
3.2.1	Piping - Well - PVC	8,078	17
3.2.2	Piping - Well - Excavation	4,527	17
3.2.3	Piping - Well - Backfill and Compaction	2,734	17
4.2.2	Valves - Motor/Air Operated (on/off) - Well Pump - Polypropylene/PVC	1,791	20
5.2	Pumps - Well Pump	16,821	17
6.2.1	Instrumentation - Flow Meters - Well - Propeller	4,796	14
7.1	System Controls - Remote Telemetry Units (RTUs)	1,215	8
7.2	System Controls - Well Pump - Soft Start Control	418	8
7.3	System Controls - Drive Controllers	1,395	14
8.1.1	Building Structures - Building 1 - Small Low Cost Shed	11,440	20
Indirect	Indirect and Add-On Costs (contingency from model)	167,015	27
	Process Cost	167,528	
	System Cost	334,542	
	O&M Cost	13,630	

Totals are computed before component costs are rounded

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of indirect and add-on costs	
Contingency	20,879
Process Engineering	33,143
Construction Management and GC Overhead	18,963
Site Work	3,425
Yard Piping	0
Geotechnical	22,180
Standby Power	0
Electrical (including yard wiring)	15,427
Mobilization and Demobilization	11,166
Architectural Fees for Treatment Building	0
Permits	0
Pilot Study	0
Land Cost	21,727
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	16,753
Legal, Fiscal, and Administrative (2.0%)	3,351
Sales Tax (0.0%)	0
Financing during Construction (0.0%)	0

Breakdown of O&M costs	
Manager (4 hrs/yr @ \$52.3563/hr)	223
Administrative (4 hrs/yr @ \$35.3133/hr)	150
Operator (43 hrs/yr @ \$34.0099/hr)	1,448
Building maintenance (materials and labor) (200 sf @ \$6.6975/sf/yr)	1,339
Well pump (calculated as a percentage of capital)	168
Energy for well pumps (74 Mwh/yr @ \$0.1225/kwh)	9,062
Miscellaneous Allowance (0 @ \$)	1,239

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Non-Treatment(NON), design 1.000 mgd, average 0.350 mgd

Groundwater

Mid-Cost Components

Design Type: Interconnection

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
2.1.1	Vaults - Booster Pump - Concrete	8,546	40
2.1.2	Vaults - Booster Pump - Excavation	9,050	40
2.1.3	Vaults - Booster Pump - Backfill and Compaction	3,015	40
3.1.1	Piping - Interconnect - PVC	161,565	22
3.1.2	Piping - Interconnect - Excavation	90,543	22
3.1.3	Piping - Interconnect - Backfill and Compaction	54,684	22
3.1.4	Piping - Interconnect - Asphalt Patch	93,519	22
4.1.1	Valves - Isolation and Street - Ductile Iron	22,950	25
4.2.1	Valves - Motor/Air Operated (on/off) - Booster Pump - Cast Iron	14,273	25
5.1	Pumps - Interconnect Booster Pump	75,685	20
6.1.1	Instrumentation - Flow Meters - Interconnect - Venturi	3,077	15
7.1	System Controls - Remote Telemetry Units (RTUs)	1,215	10
7.3	System Controls - Drive Controllers	1,395	15
Indirect	Indirect and Add-On Costs (contingency from model)	361,760	22
	Process Cost	539,516	
	System Cost	901,275	
	O&M Cost	476,182	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Contingency	49,319
Process Engineering	64,574
Construction Management and GC Overhead	42,998
Site Work	0
Yard Piping	0
Geotechnical	0
Standby Power	32,220
Electrical (including yard wiring)	53,812
Mobilization and Demobilization	27,119
Architectural Fees for Treatment Building	0
Permits	0
Pilot Study	0
Land Cost	0
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	53,952
Legal, Fiscal, and Administrative (2.0%)	10,790
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	26,976

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of O&M costs	
Manager (3 hrs/yr @ \$59.8839/hr)	188
Administrative (3 hrs/yr @ \$37.6596/hr)	118
Operator (31 hrs/yr @ \$34.0099/hr)	1,066
Purchased Water (127750 K gal @ \$3.1748K gal)	405,587
Booster pump (calculated as a percentage of capital)	757
Energy for booster pumps (206 Mwh/yr @ \$0.1225/kwh)	25,178
Miscellaneous Allowance (0 @ \$)	43,289

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Non-Treatment(NON), design 1.000 mgd, average 0.350 mgd

Groundwater

Mid-Cost Components

Design Type: New Well Construction

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1.1	Well Items - Well Casing - Stainless Steel	377,507	30
1.2.1	Well Items - Well screen - PVC Schedule 80	33,038	30
1.3.1	Well Items - Plugs - PVC	623	30
1.4	Well Items - Well Drilling	144,169	30
1.5	Well Items - Gravel Pack	20,489	30
1.6	Well Items - Well Development	1,540	30
1.7	Well Items - Grout Seal	6,143	30
3.2.1	Piping - Well - PVC	16,156	22
3.2.2	Piping - Well - Excavation	9,054	22
3.2.3	Piping - Well - Backfill and Compaction	5,468	22
4.2.2	Valves - Motor/Air Operated (on/off) - Well Pump - Cast Iron	28,546	25
5.2	Pumps - Well Pump	33,641	20
6.2.1	Instrumentation - Flow Meters - Well - Venturi	3,077	15
7.1	System Controls - Remote Telemetry Units (RTUs)	2,430	10
7.2	System Controls - Well Pump - Soft Start Control	835	10
7.3	System Controls - Drive Controllers	2,790	15
8.1.1	Building Structures - Building 1 - Small Low Cost Shed	22,880	25
Indirect	Indirect and Add-On Costs (contingency from model)	552,043	30
	Process Cost	708,388	
	System Cost	1,260,431	
	O&M Cost	28,953	

Totals are computed before component costs are rounded

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of indirect and add-on costs	
Contingency	68,865
Process Engineering	84,572
Construction Management and GC Overhead	55,230
Site Work	6,850
Yard Piping	0
Geotechnical	44,360
Standby Power	27,563
Electrical (including yard wiring)	68,188
Mobilization and Demobilization	36,888
Architectural Fees for Treatment Building	2,059
Permits	0
Pilot Study	0
Land Cost	37,043
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	70,839
Legal, Fiscal, and Administrative (2.0%)	14,168
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	35,419

Breakdown of O&M costs	
Manager (9 hrs/yr @ \$59.8839/hr)	510
Administrative (9 hrs/yr @ \$37.6596/hr)	321
Operator (85 hrs/yr @ \$34.0099/hr)	2,897
Building maintenance (materials and labor) (400 sf @ \$6.6975/sf/yr)	2,679
Well pump (calculated as a percentage of capital)	336
Energy for well pumps (160 Mwh/yr @ \$0.1225/kwh)	19,578
Miscellaneous Allowance (0 @ \$)	2,632

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Non-Treatment(NON), design 3.536 mgd, average 1.345 mgd

Surface Water

High-Cost Components

Design Type: Interconnection

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
2.1.1	Vaults - Booster Pump - Concrete	10,277	40
2.1.2	Vaults - Booster Pump - Excavation	10,579	40
2.1.3	Vaults - Booster Pump - Backfill and Compaction	3,296	40
3.1.1	Piping - Interconnect - Ductile Iron	1,442,458	40
3.1.2	Piping - Interconnect - Excavation	102,616	40
3.1.3	Piping - Interconnect - Backfill and Compaction	61,975	40
3.1.4	Piping - Interconnect - Asphalt Patch	105,988	40
4.1.1	Valves - Isolation and Street - Ductile Iron	61,530	25
4.2.1	Valves - Motor/Air Operated (on/off) - Booster Pump - Stainless Steel	56,849	25
5.1	Pumps - Interconnect Booster Pump	106,073	20
6.1.1	Instrumentation - Flow Meters - Interconnect - Magnetic	9,045	15
7.1	System Controls - Remote Telemetry Units (RTUs)	1,215	10
7.3	System Controls - Drive Controllers	2,790	15
Indirect	Indirect and Add-On Costs (contingency from model)	1,235,017	40
	Process Cost	1,974,692	
	System Cost	3,209,708	
	O&M Cost	1,799,495	

Totals are computed before component costs are rounded

Breakdown of indirect and add-on costs	
Contingency	175,779
Process Engineering	236,628
Construction Management and GC Overhead	128,519
Site Work	0
Yard Piping	0
Geotechnical	0
Standby Power	63,993
Electrical (including yard wiring)	197,190
Mobilization and Demobilization	97,211
Architectural Fees for Treatment Building	0
Permits	0
Pilot Study	0
Land Cost	0
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	197,469
Legal, Fiscal, and Administrative (2.0%)	39,494
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	98,735

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of O&M costs	
Manager (6 hrs/yr @ \$66.7054/hr)	412
Administrative (6 hrs/yr @ \$39.756/hr)	245
Operator (62 hrs/yr @ \$43.9163/hr)	2,712
Purchased Water (490925 K gal @ \$3.1748K gal)	1,558,612
Booster pump (calculated as a percentage of capital)	1,061
Energy for booster pumps (595 Mwh/yr @ \$0.1225/kwh)	72,863
Miscellaneous Allowance (0 @ \$)	163,590

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
March 2024

Non-Treatment(NON), design 3.536 mgd, average 1.417 mgd

Groundwater

High-Cost Components

Design Type: New Well Construction

WBS #	Item	Total Cost (\$)	Useful Life (yrs)
1.1.1	Well Items - Well Casing - Stainless Steel	943,768	30
1.2.1	Well Items - Well screen - Stainless Steel	216,209	30
1.3.1	Well Items - Plugs - PVC	1,558	30
1.4	Well Items - Well Drilling	360,423	30
1.5	Well Items - Gravel Pack	51,222	30
1.6	Well Items - Well Development	3,850	30
1.7	Well Items - Grout Seal	15,358	30
3.2.1	Piping - Well - Ductile Iron	223,135	40
3.2.2	Piping - Well - Excavation	22,636	40
3.2.3	Piping - Well - Backfill and Compaction	13,671	40
4.2.2	Valves - Motor/Air Operated (on/off) - Well Pump - Stainless Steel	71,235	25
5.2	Pumps - Well Pump	112,124	20
6.2.1	Instrumentation - Flow Meters - Well - Magnetic	6,629	15
7.1	System Controls - Remote Telemetry Units (RTUs)	6,075	10
7.2	System Controls - Well Pump - Soft Start Control	2,088	10
7.3	System Controls - Drive Controllers	6,976	15
8.1.1	Building Structures - Building 1 - Low Quality	95,613	40
Indirect	Indirect and Add-On Costs (contingency from model)	1,576,160	30
	Process Cost	2,152,569	
	System Cost	3,728,729	
	O&M Cost	108,570	

Totals are computed before component costs are rounded

Technologies and Cost for Removing Per- and Polyfluoroalkyl Substances (PFAS) from Drinking Water
 March 2024

Breakdown of indirect and add-on costs	
Contingency	203,829
Process Engineering	257,221
Construction Management and GC Overhead	139,398
Site Work	17,125
Yard Piping	0
Geotechnical	110,900
Standby Power	65,959
Electrical (including yard wiring)	204,789
Mobilization and Demobilization	110,265
Architectural Fees for Treatment Building	8,605
Permits	1,449
Pilot Study	0
Land Cost	90,684
Installation, Transportation, and O&P (0.0%)	0
Instrumentation and Control (0.0%)	0
Miscellaneous Allowance (10.0%)	215,257
Legal, Fiscal, and Administrative (2.0%)	43,051
Sales Tax (0.0%)	0
Financing during Construction (5.0%)	107,628

Breakdown of O&M costs	
Manager (21 hrs/yr @ \$66.7054/hr)	1,420
Administrative (21 hrs/yr @ \$39.756/hr)	846
Operator (213 hrs/yr @ \$43.9163/hr)	9,351
Building maintenance (materials and labor) (1000 sf @ \$6.6975/sf/yr)	6,697
Well pump (calculated as a percentage of capital)	1,121
Energy for well pumps (647 Mwh/yr @ \$0.1225/kwh)	79,264
Miscellaneous Allowance (0 @ \$)	9,870