

# FLORIDA DEPARTMENT OF Environmental Protection

Ron DeSantis Governor

Alexis A. Lambert Secretary

Northwest District 160 W. Government St., Suite 308 Pensacola, FL 32502

Electronic Mail – Received Receipt Requested

Shane Fowler Taminco US LLC 4575 Highway 90 East Pace, FL 32571-0467

Re: Permit No. 1130004-046-AV Taminco Pace Plant Title V Permit Renewal

Dear Mr. Fowler:

Enclosed is the draft permit package to renew the Title V air operation permit for the Taminco Pace Plant. This facility is located in Santa Rosa County at 4575 Highway 90 East, Pace, Florida. The permit package includes the following documents:

- The Statement of Basis, which summarizes the facility, the equipment, the primary rule applicability, and the changes since the last Title V renewal.
- The renewed draft Title V air operation permit, which includes the specific permit conditions that regulate the emissions units covered by the proposed project.
- The Written Notice of Intent to Issue Air Permit provides important information regarding: the Permitting Authority's intent to issue an air permit for the proposed project; the requirements for publishing a Public Notice of the Permitting Authority's intent to issue an air permit; the procedures for submitting comments on the draft permit; the process for filing a petition for an administrative hearing; and the availability of mediation.
- The Public Notice of Intent to Issue Air Permit is the actual notice that you must have published in the legal advertisement section of a newspaper of general circulation in the area affected by this project. The Public Notice of Intent to Issue Title V Air Permit must be published as soon as possible and the proof of publication must be provided to the Department within seven days of the date of publication.

If you have any questions, about the enclosed permitting package or if you wish to submit comments regarding the draft permit during the comment period, please contact the Project Engineer, Luke Kimmel, by telephone at 850-595-0576 or by email at Luke.Kimmel@FloridaDEP.gov.

Executed in Pensacola, Florida.

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Kimberly R. Allen Permitting Program Administrator

3/17/2025 Date

KRA/lk

In the Matter of an *Application for Title V Air Operation Permit by:* 

Taminco US LLC 4575 Highway 90 East Pace, Florida 32571-0467

Responsible Official: Shane Fowler, Site Manager Permit No. 1130004-046-AV Facility ID No. 1130004 Taminco Pace Plant Title V Air Operation Permit Renewal Santa Rosa County, Florida

**Facility Location**: Taminco US LLC operates the Taminco Pace Plant, which is located in Santa Rosa County at 4575 Highway 90 East, Pace, Florida.

**Project**: The purpose of this project is to renew the Title V air operation permit No. 1130004-035-AV. Details of the project are provided in the application and the referenced Statement of Basis.

**Permitting Authority**: Applications for Title V air operation permits are subject to review in accordance with the provisions of Chapter 403, Florida Statutes (F.S.) and Chapters 62-4, 62-210 and 62-213 of the Florida Administrative Code (F.A.C.). The proposed project is not exempt from air permitting requirements and a Title V air operation permit is required to operate the facility. The Northwest District is the Permitting Authority responsible for making a permit determination for this project. The Permitting Authority's physical address is: 160 W. Government Street, Suite 308, Pensacola, Florida 32502-5740. The Permitting Authority's mailing address is: 160 W. Government Street, Suite 308, Pensacola, Florida 32502-5740. The Permitting Authority's telephone number is (850) 595-8300.

**Project File**: A complete project file is available for public inspection during the normal business hours of 8:00 a.m. to 5:00 p.m., Monday through Friday (except legal holidays), at the address indicated above for the Permitting Authority. The complete project file includes the draft permit, the Statement of Basis, the application, and the information submitted by the applicant, exclusive of confidential records under Section 403.111, F.S. Interested persons may view the draft permit by visiting the following website:

<u>https://fldep.dep.state.fl.us/air/emission/apds/default.asp</u> and entering the permit number shown above. Interested persons may contact the Permitting Authority's project review engineer for additional information at the address or phone number listed above.

**Notice of Intent to Issue Permit**: The Permitting Authority gives notice of its intent to issue a Title V air operation permit renewal to the applicant for the project described above. The applicant has provided reasonable assurance that continued operation of the existing equipment will not adversely impact air quality and that the project will comply with all appropriate provisions of Chapters 62-4, 62-204, 62-210, 62-212, 62-213, 62-296 and 62-297, F.A.C. The Permitting Authority will issue a proposed permit and subsequent final permit in accordance with the conditions of the draft permit unless a response received in accordance with the following procedures results in a different decision or a significant change of terms or conditions.

**Public Notice**: Pursuant to Section 403.815, F.S. and Rules 62-110.106 and 62-210.350, F.A.C., you (the applicant) are required to publish at your own expense the enclosed Public Notice of Intent to Issue Air Permit (Public Notice). The Public Notice shall be published one time only as soon as possible in the legal advertisement section of a newspaper of general circulation in the area affected by this project. The newspaper used must meet the requirements of Sections 50.011 and 50.031, F.S. in the county where the activity is to take place. If you are uncertain that a newspaper meets these requirements, please contact the Permitting Authority at the above address or phone number. Pursuant to Rule 62-110.106(5) and (9), F.A.C., the applicant shall provide proof of publication to the Permitting Authority at the above address within 7 days of publication. Failure to publish the notice and provide proof of publication may result in the denial of the permit pursuant to Rule 62-110.106(11), F.A.C.

**Comments**: The Permitting Authority will accept written comments concerning the draft Title V air operation permit for a period of 30 days from the date of publication of the Public Notice. Written comments must be

received by the close of business (5:00 p.m.), on or before the end of this 30-day period by the Permitting Authority at the above address. As part of his or her comments, any person may also request that the Permitting Authority hold a public meeting on this permitting action. If the Permitting Authority determines there is sufficient interest for a public meeting, it will publish notice of the time, date, and location in the Florida Administrative Register (FAR). If a public meeting is requested within the 30-day comment period and conducted by the Permitting Authority, any oral and written comments received during the public meeting will also be considered by the Permitting Authority. If timely received written comments or comments received at a public meeting result in a significant change to the draft permit, the Permitting Authority shall issue a revised draft permit and require, if applicable, another Public Notice. All comments filed will be made available for public inspection. For additional information, contact the Permitting Authority at the above address or phone number.

**Petitions**: A person whose substantial interests are affected by the proposed permitting decision may petition for an administrative hearing in accordance with Sections 120.569 and 120.57, F.S. Petitions filed by the applicant or any of the parties listed below must be filed within 14 days of receipt of this written notice of Intent to Issue Air Permit. Petitions filed by any persons other than those entitled to written notice under Section 120.60(3), F.S., must be filed within 14 days of publication of the attached Public Notice or within 14 days of receipt of this written notice of Intent to Issue Air Permit, whichever occurs first. Under Section 120.60(3), F.S., however, any person who asked the Permitting Authority for notice of agency action may file a petition within 14 days of receipt of that notice, regardless of the date of publication. A petitioner shall mail a copy of the petition to the applicant at the address indicated above, at the time of filing. A petition for administrative hearing must contain the information set forth below and must be filed (received) with the Agency Clerk in the Office of General Counsel, 3900 Commonwealth Boulevard, MS 35, Tallahassee, Florida 32399-3000, <u>Agency Clerk@dep.state.fl.us</u>, before the deadline. The failure of any person to file a petition within the appropriate time period shall constitute a waiver of that person's right to request an administrative determination

appropriate time period shall constitute a waiver of that person's right to request an administrative determination (hearing) under Sections 120.569 and 120.57, F.S., or to intervene in this proceeding and participate as a party to it. Any subsequent intervention (in a proceeding initiated by another party) will be only at the approval of the presiding officer upon the filing of a motion in compliance with Rule 28-106.205, F.A.C.

A petition that disputes the material facts on which the Permitting Authority's action is based must contain the following information: (a) The name and address of each agency affected and each agency's file or identification number, if known; (b) The name, address, any email address, telephone number and any facsimile number of the petitioner; the name, address, any email address, telephone number, and any facsimile number of the petitioner's representative, if any, which shall be the address for service purposes during the course of the proceeding; and an explanation of how the petitioner's substantial interests will be affected by the agency determination; (c) A statement of when and how each petitioner received notice of the agency action or proposed decision; (d) A statement of all disputed issues of material fact. If there are none, the petition must so indicate; (e) A concise statement of the ultimate facts alleged, including the specific facts the petitioner contends warrant reversal or modification of the agency's proposed action; (f) A statement of the specific rules or statutes the petitioner contends require reversal or modification of the agency's proposed action including an explanation of how the alleged facts relate to the specific rules or statutes; and, (g) A statement of the relief sought by the petitioner, stating precisely the action the petitioner wishes the agency to take with respect to the agency's proposed action. A petition that does not dispute the material facts upon which the Permitting Authority's action is based shall state that no such facts are in dispute and otherwise shall contain the same information as set forth above, as required by Rule 28-106.301, F.A.C.

Because the administrative hearing process is designed to formulate final agency action, the filing of a petition means that the Permitting Authority's final action may be different from the position taken by it in this written notice of Intent to Issue Air Permit. Persons whose substantial interests will be affected by any such final decision of the Permitting Authority on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth above.

**Extension of Time**: Under Rule 62-110.106(4), F.A.C., a person whose substantial interests are affected by the Department's action may also request an extension of time to file a petition for an administrative hearing. The

#### WRITTEN NOTICE OF INTENT TO ISSUE AIR PERMIT

Department may, for good cause shown, grant the request for an extension of time. Requests for extension of time must be filed with the Office of General Counsel of the Department at 3900 Commonwealth Boulevard, Mail Station 35, Tallahassee, Florida 32399-3000, or via electronic correspondence at <u>Agency\_Clerk@dep.state.fl.us</u>, before the deadline for filing a petition for an administrative hearing. A timely request for extension of time shall toll the running of the time period for filing a petition until the request is acted upon.

Mediation: Mediation is not available in this proceeding.

**Objections**: Finally, pursuant to 42 United States Code (U.S.C.) Section 7661d(b)(2), any person may petition the Administrator of the EPA within 60 days of the expiration of the Administrator's 45-day review period as established at 42 U.S.C. Section 7661d(b)(1), to object to the issuance of any Title V air operation permit. Any petition shall be based only on objections to the permit that were raised with reasonable specificity during the 30-day public comment period provided in the Public Notice, unless the petitioner demonstrates to the Administrator of the EPA that it was impracticable to raise such objections within the comment period or unless the grounds for such objection arose after the comment period. Filing of a petition with the Administrator of the EPA does not stay the effective date of any permit properly issued pursuant to the provisions of Chapter 62-213, F.A.C. Petitions filed with the Administrator of EPA must meet the requirements of 42 U.S.C. Section 7661d(b)(2) and must be filed with the Administrator of the EPA at: U.S. Environmental Protection Agency, Office of the Administrator, 1200 Pennsylvania Avenue, N.W., Mail Code: 1101A, Washington, DC 20460. For more information regarding EPA review and objections, visit EPA's Region 4 web site at <u>https://www.epa.gov/caa-permitting/florida-proposed-title-v-permits</u>.

Executed in Pensacola, Florida.

Kimberly RAlle

Kimberly R. Allen Permitting Program Administrator

3/17/2025 Date

#### **CERTIFICATE OF SERVICE**

The undersigned duly designated deputy agency clerk hereby certifies that this written notice of Intent to Issue the Title V Air Operation Permit Renewal (including the Public Notice, the Statement of Basis, and the draft permit), or a link to these documents available electronically on a publicly accessible server, was sent by electronic mail with received receipt requested to the persons listed below:

Shane Fowler, Taminco US LLC, <u>sfowler@eastman.com</u> Maria Edwards, Taminco US LLC, <u>medwards@eastman.com</u> Tim Musick, Taminco US LLC, <u>tmusick@eastman.com</u> Amy Adams, <u>amyadams@eastman.com</u> Daren Edwards, Taminco US LLC, <u>darenedwards@eastman.com</u> Keith Jahn, Taminco US LLC, <u>keithjahn@eastman.com</u>

#### FILING AND ACKNOWLEDGMENT FILED, on

this date, pursuant to Section 120.52(7), Florida Statutes, with the designated agency clerk, receipt of which is hereby acknowledged.

Mutille Suldet

3/17/2025

Clerk

Date

#### PUBLIC NOTICE OF INTENT TO ISSUE AIR PERMIT

Florida Department of Environmental Protection Northwest Distrist Draft Permit No. 1130004-046-AV Taminco US LLC, Taminco Pace Plant Santa Rosa County, Florida

**Applicant**: The applicant for this project is Taminco US LLC. The applicant's responsible official and mailing address are: Shane Fowler, Site Manager, Taminco US LLC, Taminco Pace Plant, 4575 Highway 90 East, Pace, Florida 32571-0467.

**Facility Location**: The applicant operates the existing Taminco Pace Plant, which is located in Santa Rosa County at 4575 Highway 90 East in Pace, Florida.

**Project**: The applicant applied on February 24, 2025 to the Department for a Title V air operation permit renewal. This is a renewal of Title V Air Operation Permit No. 1130004-035-AV. The existing facility consists of five chemical manufacturing units. Plant Nos. 1 and 4 produce methylamines; Plant No. 2 produces a variety of higher amines, including alkylamines and amylamines; Plant No. 3 processes higher amines; and the DIMLA Plant produces dimethyl laurylamine (DIMLA12), dimethyl myristylamine (DIMLA14), dimethyl hexadecylamine (DIMLA16) and a blend of DIMLA12, DIMLA14, and/or DIMLA16 (e.g. DIMLA1214). The utilities area contains two boilers and three cogeneration units. The cogeneration units are owned by Florida Power & Light (FP&L) but operated by Taminco.

**Permitting Authority**: Applications for Title V air operation permits are subject to review in accordance with the provisions of Chapter 403, Florida Statutes (F.S.) and Chapters 62-4, 62-210 and 62-213, of the Florida Administrative Code (F.A.C.). The proposed project is not exempt from air permitting requirements and a Title V air operation permit is required to operate the facility. The Northwest District is the Permitting Authority responsible for making a permit determination for this project. The Permitting Authority's physical address is: 160 W. Government Street, Suite 308, Pensacola, Florida 32502-5740. The Permitting Authority's mailing address is: 160 W. Government Street, Suite 308, Pensacola, Florida 32502-5740. The Permitting Authority's telephone number is (850) 595-8300.

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**Notice of Intent to Issue Permit**: The Permitting Authority gives notice of its intent to issue a renewed Title V air operation permit to the applicant for the project described above. The applicant has provided reasonable assurance that continued operation of the existing equipment will not adversely impact air quality and that the project will comply with all appropriate provisions of Chapters 62-4, 62-204, 62-210, 62-212, 62-213, 62-296 and 62-297, F.A.C. The Permitting Authority will issue a proposed permit and subsequent final permit in accordance with the conditions of the draft permit unless a response received in accordance with the following procedures results in a different decision or a significant change of terms or conditions.

**Comments**: The Permitting Authority will accept written comments concerning the draft Title V air operation permit for a period of 30 days from the date of publication of the Public Notice. Written comments must be received by the close of business (5:00 p.m.), on or before the end of this 30-day period by the Permitting Authority at the above address. As part of his or her comments, any person may also request that the Permitting Authority hold a public meeting on this permitting action. If the Permitting Authority determines there is sufficient interest for a public meeting, it will publish notice of the time, date, and location in the Florida Administrative Register (FAR). If a public meeting is requested within the 30-day comment period and

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# Taminco US LLC Taminco Pace Plant

## Facility ID No. 1130004 Santa Rosa County

Title V Air Operation Permit Renewal

**Permit No. 1130004-046-AV** (Renewal of Title V Air Operation Permit No. 1130004-035-AV)



## Permitting and Compliance Authority:

State of Florida Department of Environmental Protection Northwest District

160 W. Government Street, Suite 308 Pensacola, Florida 32502-5740

> Telephone. (850) 595-8300 Fax. (850) 595-8393

Permitting Authority: <u>NWDAIR@floridadep.gov</u> Compliance Authority: <u>NWDAIR@floridadep.gov</u>

# Title V Air Operation Permit Renewal Permit No. 1130004-046-AV

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# FLORIDA DEPARTMENT OF Environmental Protection

Ron DeSantis Governor

Alexis A. Lambert Secretary

Northwest District 160 W. Government St., Suite 308 Pensacola, FL 32502

**PERMITTEE:** Taminco US LLC 4575 Highway 90 East Pace, Florida 32571-0467 Permit No. 1130004-046-AV Taminco Pace Plant Facility ID No. 1130004 Title V Air Operation Permit Renewal

The purpose of this permit is to renew the Title V air operation permit for the above referenced facility. The existing Taminco Pace Plant is located in Santa Rosa County at 4575 Highway 90 East in Pace, Florida. UTM Coordinates are Zone 16, 486.91 km East and 3382.67 km North. Latitude is: 30° 34" 41.0064' and Longitude is: 87° 08" 16.3870'.

The Title V air operation permit is issued under the provisions of Chapter 403, Florida Statutes (F.S.), and Florida Administrative Code (F.A.C.) Chapters 62-4, 62-210 and 62-213. The above named permittee is hereby authorized to operate the facility in accordance with the terms and conditions of this permit.

1130004-046-AV Effective Date: DATE, 20xx Renewal Application Due Date: Exp. DATE -225, 20zz Expiration Date: Eff. DATE + 5 years, 20zz

#### (Draft)

Kimberly R. Allen Permitting Program Administrator Date

KRA/lk

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#### Subsection A. Facility Description.

Taminco Pace Plant is an existing Chemical Processing Plant, which is categorized under Standard Industrial Classification Code No. 2869. The existing Taminco Pace Plant is comprised of five chemical manufacturing units. Plant Nos. 1 and 4 produce methylamines; Plant No. 2 produces a variety of higher amines, including alkylamines and amylamines; Plant No. 3 processes higher amines; and the DIMLA Plant produces dimethyl laurylamine (DIMLA12), dimethyl myristylamine (DIMLA14), dimethyl hexadecylamine (DIMLA16) and a blend of DIMLA12, DIMLA14 and/or DIMLA16 (e.g. DIMLA1214). The Utilities area contains two boilers and three cogeneration units. The cogeneration units are owned by Florida Power & Light Company but operated by Taminco and permitted separately under Facility ID No. 1130173.

#### Methylamines Plant Nos. 1 and 4

At Methylamines (MA) Plants Nos. 1 and 4, methanol is continuously reacted with ammonia to yield methylamines. A natural gas-fired preheater is used to reach reaction temperature. Volatile off-gases from the low-pressure absorbers are controlled with the Amines Plants Flare (EU 005) or the boilers (EU 001 and EU 003). Process gases from the high-pressure absorber vents can be routed to the boilers or to the Amines Plants Flare. Visible emissions from the gas-fired heater and the flare are controlled by proper combustion. Wastewater generated is treated in the wastewater treatment system.

#### Higher Amines Plant Nos. 2 and 3

At Higher Amines Plant Nos. 2 and 3, alcohols, ammonia, ethers, aldehydes, ketones and other amines are reacted to yield various alkylamines and amylamines. A natural gas-fired preheater is used to bring the mixture to reaction temperature. The volatile off-gases from the low-pressure absorbers are controlled by the Amines Plants Flare or the boilers. Process gases from the high-pressure absorber vent in Higher Amines Plant No. 2 can be routed to the boilers or to the Amines Plants Flare. Visible emissions from the gas-fired heater and the flare are controlled by proper combustion. Wastewater generated is treated in the wastewater treatment system.

#### **Amines Plants Flare**

The Amines Plants Flare is a non-assisted flare with a natural gas pilot. Off-gases from the product absorbers at MA Plants, the Higher Amines Plants and the DIMLA Plant, as well as other process vents at the facility, are continuously released to the flare for destruction. An infra-red and a flame strength camera are utilized to continuously monitor the flame. The flame strength will alarm the control room operator if the flame goes out. The flare pilot will not relight itself. An alarm delay is built into the computer logic to avoid false alarms during brief instances when weather conditions may disrupt the flame viewed by the camera. Natural gas is fed with process gas in a ratio of 0.3:1 for streams that do not have direct BTU measurement to ensure that the minimum net heating value of gas being combusted by the flare is maintained, and a high flow alarm on the gas flow to the flare ensures that the maximum allowable flare exit velocity is not exceeded.

#### **DIMLA Plant**

At the DIMLA Plant, Dimethyl Laurylamine is manufactured from a C12 alcohol (lauryl alcohol), a C14 alcohol (myristyl alcohol), a C16 straight chain alcohol (Hexadecyl alcohol) or a mixture of the C12, C14, and/or C16 alcohols. The alcohol feed (ROH) is reacted with dimethylamine (DMA) in a catalyzed reaction with hydrogen present. Vent streams from the amines absorption column, the amines reactor and the amines desorption column are sent to the low-pressure absorber in the MA Plant No. 1 or in the MA Plant No. 4 or directly to the flare header. Wastewater from the amines desorption column can go to the wastewater treatment system. The water phase from the decanters is also sent to the wastewater treatment system via the wastewater recycle tank TK-62057 or the wastewater tank TK-62099. Residue from the ROH evaporator and a portion of the DIMLA purification column residue are sold or disposed of offsite. Off gases from the vacuum system are recovered using an atmospheric scrubber that feeds the amines absorption column.

#### Boilers

The Riley Stoker boiler (EU 001) and B&W boiler (EU 003) are designed to burn natural gas and off gases from the amines and dimethyl laurylamine processes. The vent gases are fed through annular burners with natural gas to ensure complete combustion. Each boiler is designed for a maximum firing rate of 130 million British thermal units per hour (MMBtu/hr) and is capable of producing about 90,000 pounds per hour (lb/hr) of 600 pounds per square inch gauge (psig) steam. Flue Gas Recirculation (FGR) has been added to the Riley Stoker boiler for control of NOx emissions. An estimated 50% control of NOx is expected; however, the Riley Stoker Boiler is not required to operate the FGR to stay in compliance because emissions calculations were done without taking the FGR NOx reduction into account.

Florida Power & Light Company owns three cogeneration units located within the Taminco Pace Plant boundaries. Taminco personnel operate the units, but Florida Power & Light Company maintains compliance with a separate Title V air operation permit under Facility ID No. 1130173.

#### **Reciprocating Internal Combustion Engines**

The Taminco Pace Plant operates four *existing* stationary, emergency, diesel fueled, compression ignition, reciprocating internal combustion engines (CI RICE):

Equip. I.D.	Area/Location	Existing or New	Construction Commenced Date	Brake hp	Fuel Type
PG24101C	B-Area well water pump	Existing	04/19/1994	234	Diesel
PG24101B	No. 2 well water pump	Existing	04/06/1994	234	Diesel
D24018	Plant emergency generator	Existing	06/07/1991	330	Diesel
PG24121	South Foxtrot fire water pump	Existing	04/15/1994	340	Diesel

These engines are *existing* stationary reciprocating internal combustion engines [per 40 CFR 63.6590(a)(1)(ii)] with a rating of less than 500 brake horsepower (Hp), located at a major source of hazardous air pollutants (HAP) and constructed before June 12, 2006. These stationary CI RICE are subject to 40 CFR 63 Subpart ZZZZ, National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines and must comply with the applicable emission limitations in Table 2c to 40 CFR 63 Subpart ZZZZ for Emergency Stationary CI RICE.

Taminco also operates one *new* stationary, emergency, diesel fueled, compression ignition, reciprocating internal combustion engine:

Equip. I.D.	Area/Location	Existing or New	Construction Commenced Date	Brake hp	Fuel Type
PG24114	Main fire water pump	New	06/2016	268	Diesel

This new CI RICE is regulated by 40 CFR 60, Subpart IIII, Standards of Performance for Stationary Compression Ignition Internal Combustion Engines. The fire pump engine is a "new" stationary emergency CI RICE with a displacement of less than 30 liters per cylinder, located at a major source of HAP, commenced construction on or after 6/12/2006, and has a post-2007 model year.

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#### Subsection B. Summary of Emissions Units.

EU No.	Brief Description
Regulated	Emissions Units
	Methanol Storage:
029	Methylamines Plant Nos. 1 and 4 HON Group 1 Storage Tanks (Methanol)
047	Methanol Storage HON Maintenance Wastewater
048	Methylamines Plants Sample Points (HON)

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EU No.	Brief Description	
	Boilers:	
001	Riley Stoker Boiler	
003	B & W Boiler	
	Methylamines Plant No. 1:	
005	Amines Plants Flare	
006	Methylamines Plant No. 1 Gas Fired Heater	
036	Methylamines Plant Nos. 1 and 4 HON Equipment Leaks	
046	Sitewide HON Heat Exchangers	
049	Methylamines Plant No. 1 Process Vents	
050	Methylamines Plant No. 1 Wastewater	
051	Methylamines Plant No. 1 HON Maintenance Wastewater	
054	Methylamines Plant Nos. 1 and 4 NSPS Storage Tanks	
	Higher Amines Plants:	
007	Higher Amines Plant No. 2 Gas-Fired Heater	
055	72-inch Batch Column Process Vent	
056	72-inch Batch Column Maintenance Wastewater	
059	72-inch Batch Column Wastewater	
070	Higher Amines Plant Process Vents	
	Methylamines Plant No. 4:	
060	Methylamines Plant No. 4 Gas-Fired Heater	
033	Methylamines Plant No. 4 Process Vents	
034	Methylamines Plant No. 4 Wastewater	
035	Methylamines Plant No. 4 HON Maintenance Wastewater	
037	Methylamines Plant No. 4 VOC Equipment Leaks	
053	Methylamines Plant Nos. 1 and 4 HON Group 2 Storage Tanks	
	DIMLA Plant:	
058	DIMLA MON Group 2 Storage Tank	
071	DIMLA MON Maintenance Wastewater	
072	DIMLA MON Wastewater	
077	DIMLA MON Equipment Leaks	
078	DIMLA VOC Equipment Leaks	
079	DIMLA Scrubber	
	Plant Wide:	
080	Existing Emergency Reciprocating Internal Combustion Engines (Before 2006)	
081	New Emergency Reciprocating Internal Combustion Engine (After 2007)	
Unregulate	ed Emissions Units and Activities (see Appendix U, List of Unregulated Emissions Units and/or Activities)	
062	Facility-Wide Equipment Leak Fugitives	
063	Cooling Towers (4) (that do not use chromium-based water treatment chemicals)	
075	Wastewater Treatment Plant Fugitives	
076	DIMLA Storage Tanks and Loading	

Also included in this permit are miscellaneous insignificant emissions units and/or activities (see Appendix I, List of Insignificant Emissions Units and/or Activities).

#### Subsection C. Applicable Regulations.

Based on the Title V air operation permit renewal application received February 24, 2025, this facility is a major source of hazardous air pollutants (HAP). The existing facility is a prevention of significant deterioration (PSD) major source of air pollutants in accordance with Rule 62-212.400, F.A.C.

A summary of applicable regulations is shown in the following table.

Regulation	EU No(s).
Federal Rule Cite	ations
40 CFR 60, Subpart A, NSPS General Provisions	005, 054
40 CFR 60, Subpart Kb, NSPS for Volatile Organic Liquid Storage Vessels After July 23, 1984	054
40 CFR 60, Subpart VVa, NSPS for Equipment Leaks of VOC After November 7, 2006	037, 078
40 CFR 60, Subpart IIII, Standards of Performance for Stationary CI RICE	081
40 CFR 63, Subpart A, NESHAP General Provisions	005, 029
40 CFR 63, Subpart F, NESHAP for the Synthetic Organic Chemical Manufacturing Industry	005, 029, 033, 034, 035, 046, 047, 049, 050, 051, 053
40 CFR 63, Subpart G, NESHAP for Process Vents-Stg Vessels- Transfer Ops-Wastewater	005, 029, 033, 034, 035, 046, 047, 049, 050, 051, 053
40 CFR 63, Subpart H, NESHAP for Equipment Leaks	005, 036, 037, 048
40 CFR 63, Subpart SS	005
40 CFR 63, Subpart FFFF, NESHAP for Miscellaneous Organic Chemical Manufacturing	005, 058, 071, 072, 077, 079
40 CFR 63, Subpart ZZZZ, NESHAP for Stationary Reciprocating Internal Combustion Engines	080
40 CFR 63, Subpart DDDDD, NESHAP for Boilers and Process Heaters	001, 003, 006, 007, 060
State Rule Citat	tions
Rule 62-210.200(Definitions), F.A.C.	Facility-Wide
Rule 62-210.370, F.A.C., Emissions Computation and Reporting	Facility-Wide
Rule 62-210.900, F.A.C., Forms and Instructions	Facility-Wide
Rule 62-212.400(12), F.A.C., Source Obligation	Facility-Wide
Rule 62-213.205, F.A.C., Annual Emissions Fee	Facility-Wide
Rule 62-296.320(1), (2) & (4), F.A.C., General Pollutant Emission Limiting Standards	Facility-Wide
Rule 62-210.370(3), F.A.C., Annual Operating Report (AOR)	Facility-Wide
Rule 62-213.440, F.A.C., Permit Content	Facility-Wide
Rule 62-210.300(2)(a), F.A.C., Minimum Requirements for All Air Operation Permits	001, 003
Rule 62-210.700, F.A.C., Excess Emissions	054
Rule 62-212.300(1)(e), F.A.C., Actual Emissions Recordkeeping and Reporting Requirements	029, 001, 003
Rule 62-213.440(1), F.A.C., Standard Permit Requirements	029, 001, 003, 006, 007, 060
Rule 62-4.070(3), F.A.C.,	029, 001, 003, 005, 006, 007, 035, 058, 060, 077, 078, 079

#### SECTION I. FACILITY INFORMATION.

Regulation	<u>EU No(s).</u>
Rule 62-204.800, F.A.C., Compliance Assurance, Standards Adopted: NSPS and NESHAP	001, 003, 005, 006, 007, 029, 033, 034, 035, 036, 037, 046, 047, 048, 049, 050, 051, 053, 054, 058, 060, 071, 072, 077, 078, 079, 080
Rule 62-296.406(1), F.A.C., Visible Emissions Requirement for Fossil Fuel Steam Generators with Less Than 250 Million Btu Per Hour Heat Input	001, 003
Rule 62-297.310, F.A.C., General Emissions Test Requirements	001, 003

#### **Definitions:**

'<u>HON</u>' is an abbreviation for Hazardous Organic NESHAP (National Emission Standards for Hazardous Air Pollutants).

'MON' is an abbreviation for Miscellaneous Organic NESHAP.

'<u>Group 1 wastewater stream</u>' means a wastewater stream consisting of process wastewater at an existing or new source that meets the criteria for Group 1 status in 40 CFR 63.2485(c) for compounds in Tables 8 and 9 of 40 CFR 63, Subpart FFFF and/or a wastewater stream consisting of process wastewater at a new source that meets the criteria for Group 1 status in 40 CFR 63.132(d) for compounds in Table 8 of 40 CFR 63, Subpart G.

*<u>'Group 2 wastewater stream</u>'* means any process wastewater stream that does not meet the definition of a Group 1 wastewater stream.

'<u>The MON Rule</u>': 40 CFR 63, Subpart FFFF, National Emissions Standards for Hazardous Air Pollutants, applies to new and existing Miscellaneous Organic Chemical (MON) manufacturers. This regulation indicates that all pressure relief devices (PRDs) in HAP service (except as specified in paragraphs (e)(4) and (5) of 40 CFR 63.2480) must be equipped with a monitoring device by August 12, 2023.

The regulation applies to all existing and new Miscellaneous Organic Chemicals manufacturing process units that have the possibility of emitting Hazardous Air Pollutants. The list of HAPs emitted from the DIMLA MON manufacturing facility includes (but is not limited to) methanol and formaldehyde.

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#### The following conditions apply facility-wide to all emission units and activities:

**FW1.** <u>Appendices</u>. The permittee shall comply with all documents identified in Section V, Appendices, listed in the Table of Contents. Each document is an enforceable part of this permit unless otherwise indicated. [Rule 62-213.440, F.A.C.]

#### **Emissions and Controls**

- **FW2.** <u>Not federally Enforceable.</u> Objectionable Odor Prohibited. No person shall cause, suffer, allow or permit the discharge of air pollutants, which cause or contribute to an objectionable odor. An "objectionable odor" means any odor present in the outdoor atmosphere which by itself or in combination with other odors, is or may be harmful or injurious to human health or welfare, which unreasonably interferes with the comfortable use and enjoyment of life or property, or which creates a nuisance.
  - a. The facility will strive for odor and leak free operations by using best available technology and best management practices where feasible to reduce potential odor sources.
  - b. The facility will perform plant-wide leak checks on a regular basis. The facility shall keep a log of these leak checks recording at a minimum; leak check date, initials of person who performed the leak checks, leaks or problems found if any, corrective action to be taken, and date corrective action was completed.
  - c. Should an objectionable odor be reported or detected outside the property boundary, the facility will make all reasonable efforts to promptly identify and secure the source of the objectionable odor should the facility determine the odor originated from the plant.
  - d. The facility will notify the Department within 3 business days after the facility becomes aware of an objectionable odor outside the property boundary after confirming it is the source.

[Rule 62-296.320(2), 62-210.200(Definitions), and 62-213.440(1) F.A.C.]

**FW3.** <u>General Volatile Organic Compounds (VOC) Emissions or Organic Solvents (OS) Emissions</u>. The permittee shall allow no person to store, pump, handle, process, load, unload or use in any process or installation, volatile organic compounds or organic solvents without applying known and existing vapor emission control devices or systems deemed-necessary and ordered by the Department. [Rule 62-296.320(1), F.A.C.]</u>

*{Permitting Note: Nothing is deemed necessary and ordered at this time.}* 

- **FW4.** <u>General Visible Emissions</u>. No person shall cause, let, permit, suffer or allow to be discharged into the atmosphere the emissions of air pollutants from any activity equal to or greater than 20% opacity. This regulation does not impose a specific testing requirement. [Rule 62-296.320(4)(b), F.A.C.]
- **FW5.** <u>Unconfined Particulate Matter</u>. No person shall cause, let, permit, suffer or allow the emissions of unconfined particulate matter from any activity, including vehicular movement; transportation of materials; construction; alteration; demolition or wrecking; or industrially related activities such as loading, unloading, storing or handling; without taking reasonable precautions to prevent such emissions. Reasonable precautions to prevent emissions of unconfined particulate matter at this facility include:
  - a. Construction Activities. Stockpiled soils will be wetted down with water or another dust suppressant to control emissions.
  - b. Road Dust. Plant speed limit on all roads except the mile of paved road between Area A and Area B is 20 miles per hour. The speed limit on the paved road to Area B is 30 miles per hour. All of the main roads in the plant are paved.
  - c. Abrasive Cleaning. Tarping is used extensively to reduce particulate emissions generated by sandblasting activities in the process areas. When possible and practical, equipment that must be sandblasted is taken to a location that is protected on nearly all sides by trees, which help to knock down any fugitive dust.

Furthermore, when the maintenance experts advise against the use of sandblasting or recommend for the use of other cleaning methods such as needle-gunning or scraping, these alternative methods are employed where possible.

d. Chromium NESHAP Cooling Towers. Particulate emissions from cooling towers are controlled using drift eliminators to catch the entrained droplets, coalesce them, and allow the water to drain back into the cooling tower. In addition, the louvers are designed with an inward slope towards the tower so that any droplets that impinge on the louvers will also drain back into the tower. Finally, since the droplets are wet and heavier than air, most of the relatively few droplets that do escape from the tower fall to the ground a short distance from the tower, before they can evaporate and contribute to airborne particulate emissions.

[Rule 62-296.320(4)(c), F.A.C.; and Permit No. 1130004-010-AC]

#### **Reports and Fees**

See Appendix RR, Facility-wide Reporting Requirements for additional details.

FW6. Electronic Annual Operating Report and Title V Annual Emissions Fees. The information required by the Annual Operating Report for Air Pollutant Emitting Facility [Including Title V Source Emissions Fee Calculation] (DEP Form No. 62-210.900(5)) shall be submitted by April 1 of each year, for the previous calendar year, to the Department of Environmental Protection's (DEP) Division of Air Resource Management. Each Title V source shall submit the annual operating report using the DEP's Electronic Annual Operating Report (EAOR) software, unless the Title V source claims a technical or financial hardship by submitting DEP Form No. 62-210.900(5) to the DEP Division of Air Resource Management instead of using the reporting software. Emissions shall be computed in accordance with the provisions of subsection 62-210.370(2), F.A.C. Each Title V source must pay between January 15 and April 1 of each year an annual emissions fee in an amount determined as set forth in subsection 62-213.205(1), F.A.C. The annual fee shall only apply to those regulated pollutants, except carbon monoxide and greenhouse gases, for which an allowable numeric emission-limiting standard is specified in the source's most recent construction permit or operation permit. Upon completing the required EAOR entries, the EAOR Title V Fee Invoice can be printed by the source showing which of the reported emissions are subject to the fee and the total Title V Annual Emissions Fee that is due. The submission of the annual Title V emissions fee payment is also due (postmarked) by April 1st of each year. A copy of the system-generated EAOR Title V Annual Emissions Fee Invoice and the indicated total fee shall be submitted to: Major Air Pollution Source Annual Emissions Fee, Post Office Box 3070, Tallahassee, Florida 32315-3070. Additional information is available by accessing the Title V Annual Emissions Fee On-line Information Center at the following Internet web site: http://www.dep.state.fl.us/air/emission/tyfee.htm. [Rules 62-210.370(3), 62-210.900 & 62-213.205, F.A.C.; and, §403.0872(11), Florida Statutes (2013)]

{*Permitting Note: Resources to help you complete your AOR are available on the electronic AOR (EAOR) website at:* <u>http://www.dep.state.fl.us/air/emission/eaor</u>. If you have questions or need assistance after reviewing the information posted on the EAOR website, please contact the Department by phone at (850) 717-9000 or email at <u>eaor@dep.state.fl.us.</u>}

{Permitting Note: The Title V Annual Emissions Fee form (DEP Form No. 62-213.900(1)) has been repealed. A separate Annual Emissions Fee form is no longer required to be submitted by March 1st each year.}

**FW7.** <u>Annual Statement of Compliance</u>. The permittee shall submit an annual statement of compliance to the compliance authority at the address shown on the cover of this permit and to the US. EPA at the address shown below within 60 days after the end of each calendar year during which the Title V air operation permit was effective. (See also Appendix RR, Conditions RR1 and RR7.) [Rules 62-213.440(3)(a)2. & 3. and (b), F.A.C.]

#### SECTION II. FACILITY-WIDE CONDITIONS.

U.S. Environmental Protection Agency, Region 4 Atlanta Federal Center 61 Forsyth Street, SW Atlanta, Georgia 30303 Attn: Air Enforcement Branch

#### FW8. <u>Prevention of Accidental Releases (Section 112(r) of CAA)</u>.

- a. As required by Section 112(r)(7)(B)(iii) of the CAA and 40 CFR 68, the owner or operator shall submit an updated Risk Management Plan (RMP) to the Chemical Emergency Preparedness and Prevention Office (CEPPO) RMP Reporting Center. (See paragraph e., below.)
- b. As required under Section 252.941(1)(c), F.S., the owner or operator shall report to the appropriate representative of the Division of Emergency Management, as established by department rule, within one working day of discovery of an accidental release of a regulated substance from the stationary source, if the owner or operator is required to report the release to the United States Environmental Protection Agency under Section 112(r)(6) of the CAA.
- c. The owner or operator shall submit the required annual registration fee to the Division of Emergency Management on or before April 1, in accordance with Part IV, Chapter 252, F.S., and Rule 27P-21, F.A.C.
- d. Any required written reports, notifications, certifications, and data required to be sent to the Division of Emergency Management, should be sent to: Division of Emergency Management, 2555 Shumard Oak Boulevard, Tallahassee, FL 32399-2100, Telephone: (850) 413-9970, Fax: (850) 488-1739.
- e. Any Risk Management Plans, original submittals, revisions, or updates to submittals, should be sent electronically through EPA's Central Data Exchange system at the following address: <a href="https://cdx.epa.gov">https://cdx.epa.gov</a>. Information on electronically submitting risk management plans using the Central Data Exchange system is available at: <a href="https://www.epa.gov/rmp">https://cdx.epa.gov</a>. Information on electronically submitting risk management plans using the Central Data Exchange system is available at: <a href="https://www.epa.gov/rmp">https://www.epa.gov/rmp</a>. The RMP Reporting Center can be contacted at: RMP Reporting Center, Post Office Box 10162, Fairfax, VA 22038, Telephone: (703) 227-7650.
- f. Any required reports to be sent to the National Response Center, should be sent to: National Response Center, EPA Office of Solid Waste and Emergency Response, 1200 Pennsylvania Avenue Northwest, Mail Code: USEPA (5101T), Washington, DC 20460, Telephone: (800) 424-8802.
- g. Send the required annual registration fee using approved forms made payable to: Cashier, Division of Emergency Management, State Emergency Response Commission, 2555 Shumard Oak Boulevard, Tallahassee, FL 32399-2149

[Part IV, Chapter 252, F.S.; and, Rule 27P-21, F.A.C.]

FW9. <u>Semi-Annual Reports</u>. The permittee shall monitor compliance with the terms and conditions of this permit and shall submit reports at least every six months to the compliance office. Each semi-annual report shall cover the 6-month periods of January 1 – June 30 and July 1 – December 31. The reports shall be submitted by the 60<sup>th</sup> day following the end of each calendar half (i.e., March 1<sup>st</sup> and August 29<sup>th</sup> of every year). All instances of deviations from permit requirements (including conditions in the referenced Appendices) must be clearly identified in such reports, including reference to the specific requirement and the duration of such deviation. If there are no deviations during the reporting period, the report shall so indicate. Any semi-annual reporting requirements contained in applicable federal NSPS or NESHAP requirements may be submitted as part of this report. The submittal dates specified above shall replace the submittal dates specified in the federal rules. All additional reports submitted as part of this report should be clearly identified according to the specific federal requirement. All reports shall include a certification by a responsible official, pursuant to subsection 62-213.420(4), F.A.C. (See also Conditions RR2. – RR4. of Appendix RR, Facility-wide Reporting Requirements, for additional reporting requirements related to

deviations.) [Rule 62-213.440(1)(b)3.a., F.A.C.; and, 40 CFR 60.19(d), 40 CFR 61.10(h) & 40 CFR 63.10(a)(5)]

{*Permitting Note: EPA has clarified that, pursuant to 40 CFR 70.6(a)(3), the word "monitoring" is used in a broad sense and means monitoring (i.e., paying attention to) the compliance of the source with all emissions limitations, standards, and work practices specified in the permit.*}

#### **Other Requirements**

- FW10. <u>Actual Emissions Monitoring Reporting</u>. Permit No. 1130004-038-AC (DIMLA Plant expansion project) and Permit No. 1130004-040-AC (Higher Amines Plants expansion project) were based on an analysis that compared baseline actual emissions with projected actual emissions and avoided the requirements of subsection 62-212.400(4) through (12), F.A.C., for several pollutants. Therefore, pursuant to Rule 62-212.300(1)(e), F.A.C., the Permittee is subject to the following monitoring, reporting and recordkeeping provisions.
  - a. The permittee shall monitor the emissions of any PSD pollutant that the Department identifies could increase as a result of the construction or modification and that is emitted by any emissions unit that could be affected; and, using the most reliable information available, calculate and maintain a record of the annual emissions, in tons per year on a calendar year basis, for a period of 10 years following resumption of regular operations after the change. Emissions shall be computed in accordance with the provisions in Rule 62-210.370, F.A.C.
  - b. The permittee shall report to the Department within 60 days after the end of each calendar year during the 10-year period setting out the unit's annual emissions during the calendar year that preceded submission of the report. The report shall contain the following:
    - (1) The name, address and telephone number of Permittee of the major stationary source;
    - (2) The annual emissions as calculated pursuant to the provisions of 62-210.370, F.A.C.
    - (3) If the emissions differ from the preconstruction projection, an explanation as to why there is a difference;
    - (4) And any other information that the Permittee wishes to include in the report.
  - c. The information required to be documented and maintained pursuant to subparagraphs 62-212.300(1)(e)1 and 2, F.A.C., shall be submitted to the Department, which shall make it available for review to the general public.

**For Permit No. 1130004-038-AC, DIMLA Plant Expansion project**, the Department requires the annual reporting of actual nitrogen oxide (NOx) and volatile organic compound (VOC) emissions *for the portion of the following emissions units that are related to DIMLA production*. The method used to estimate emissions shall be the same method used to obtain actual emissions estimates for the construction permit application unless alternative methods are approved in writing by the Department.

EU ID No.	Emissions Unit Description
EU 001	Riley Stoker Boiler
EU 003	B & W Boiler
EU 005	Amines Plants Flare
EU 077	DIMLA MON Equipment Leaks
EU 062	Facility-Wide Equipment Leak Fugitives (Unregulated)
EU 063	Cooling Towers (Unregulated)
EU 076	DIMLA Storage Tanks and Loading (Unregulated)
EU 075	Wastewater Treatment Plant Fugitives (Unregulated)

#### SECTION II. FACILITY-WIDE CONDITIONS.

EU 078	DIMLA VOC Equipment Leaks
EU 058	DIMLA MON Group 2 Storage Tank
EU 071	DIMLA MON Maintenance Wastewater
EU 072	DIMLA MON Wastewater
EU 079	DIMLA Scrubber
N/A	Cogeneration units

[Permit No 1130004-038-AC; and Rules 62-212.300(1)(e) and 62-210.370, F.A.C.]

**For Permit No. 1130004-040-AC, Higher Amines Plants Expansion project**, the Department requires the annual reporting of actual volatile organic compound (VOC) emissions *for the portion of the following emissions units that are related to Higher Amines production.* The method used to estimate emissions shall be the same method used to obtain actual emissions estimates for the construction permit application unless alternative methods are approved in writing by the Department.

EU ID No.	Emissions Unit Description
EU 001	Riley Stoker Boiler
EU 003	B & W Boiler
EU 005	Amines Plants Flare
EU 007	Higher Amines Plant No. 2 Gas-Fired Heater
EU 055	72-inch Batch Column Process Vent
EU 056	72-inch Batch Column Maintenance Wastewater
EU 059	72-inch Batch Column Wastewater
EU 070	Higher Amines Plants Process Vents
EU 062	Facility-Wide Equipment Leak Fugitives (Unregulated)
EU 063	Cooling Towers (Unregulated)
EU 075	Wastewater Treatment Plant Fugitives (Unregulated)
N/A	Cogeneration units
N/A	D-68201, 68202, 68205, 68206, 68209, 68211, 68213, 68214 (Unregulated)
N/A	D-67116E, I, M, Q and D-67141 (Insignificant Emissions)

[Permit No. 1130004-040-AC; and Rules 62-212.300(1)(e) and 62-210.370, F.A.C.]

{Permitting Note: The annual actual emissions results for these projects may be reported to the Department using the Project Emissions Increase (PEI) Report form included as Figure 2 – PEI Report, in Section V – Appendices. The DIMLA Plant Expansion project and the Higher Amines Plants Expansion project are operationally and financially independent of one another. Therefore, the annual actual emissions for these projects must be reported separately (i.e. a separate project emissions increase (PEI) report must be submitted for each project.).}

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#### Subsection A. Emissions Unit 029

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
029	Methylamines Plant Nos. 1 and 4 HON Group 1 Storage Tanks (Methanol)

Storage tanks TK-53401B, TK-53405 and TK-53407 are used to store methanol used in the Methylamines Plants. The tanks are painted white, and emissions are controlled by an internal floating roof with double wiper seals and slotted guide pole covers on each tank. Also, the deck is in contact with the liquid surface and pontoons mounted on the top side of the deck keep the deck afloat. Automatic bleeder vents are designed to remain normally closed except when the roof is being floated off or landed on the leg supports. Deck fittings are gasketed or equipped with flexible fabric sleeves to minimize air emissions.

{Permitting Notes: This facility is a participant in EPA's Storage Tank Emission Reduction Partnership Program (STERP) [Federal Register Notice 19891 (April 13, 2000)]. This emissions unit is regulated by 40 CFR 63 Subpart G, National Emission Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.). <u>Group 1 storage tank</u> means a storage tank with a capacity greater than or equal to 10,000 gal storing material that has a maximum true vapor pressure of total HAP greater than or equal to 6.9 kilopascals at an existing source or greater than or equal to 0.69 kilopascals at a new source, per 40 CFR 63.2550 (Definitions)}

#### **Essential Potential to Emit (PTE) Parameters**

A.1. <u>Hours of Operation</u>. This emission unit may operate continuously (8,760 hours/year). [Rule 62-210.200(PTE), F.A.C.]

#### **Equipment Limitations and Standards**

- A.2. <u>Group 1 Storage Tanks Equipped with an Internal Floating Roof</u>. Permittee shall reduce hazardous air pollutants emissions to the atmosphere by operating and maintaining a fixed roof and internal floating roof as follows:
  - a. The internal floating roof shall be floating on the liquid surface at all times except when the floating roof must be supported by the leg supports.
  - b. When the floating roof is resting on the leg supports, the process of filling, emptying, or refilling shall be continuous and shall be accomplished as soon as practical.
  - c. Each internal floating roof shall be equipped with a closure device between the wall of the storage vessel and the roof edge. The closure device shall consist of a metallic shoe seal as defined in 40 CFR63.111 of 40 CFR 63 Subpart G.
  - d. Automatic bleeder vents are to be closed at all times when the roof is floating, except when the roof is being floated off or is being landed on the roof leg supports.
  - e. Each internal floating roof shall meet the specifications listed in paragraphs (b)(5)(i) through (b)(5)(vii) of 40 CFR 63.119.
  - f. Each cover or lid on any opening in the internal floating roof shall be closed (i.e., no visible gaps), except when the cover or lid must be open for access.

[Rule 62-204.800(11)., F.A.C., and 40 CFR 63.119(a)(1) and (b)(1) through (b)(6)]

- A.3. The EPA's Storage Tank Emission Reduction Partnership Program (STERP).
  - a. The sliding cover shall be in place over the slotted guide pole opening through the floating roof at all times except when the sliding cover must be removed for access.

b. Tanks taken out of hydrocarbon service, for any reason, do not have to have any controls in place during the time they are out of service.

[Federal Register Notice 19891 (April 13, 2000)]

**A.4.** This emissions unit is subject to the emission limitations and standards contained in Section IV, Common Conditions:

C.C.1. Startup, Shutdown, and Malfunction Plan.

C.C.4. Excess Emissions and Data Obtained During Startups, Shutdowns, and Malfunctions.

#### **Test Methods and Procedures**

- Inspection Requirements. Permittee shall visually inspect the internal floating roofs and the secondary A.5. seals through manholes and roof hatches on each fixed roof at least once every 12 months after January 27, 1998. Also, Permittee shall visually inspect each internal floating roof, the primary and secondary seals, gaskets, slotted membranes, and sleeve seals (if any) each time the storage vessel is emptied and degassed, and at least once every ten years after April 22, 1997. If during an inspection, an internal floating roof is not resting on the surface of the liquid inside the storage vessel and is not resting on the leg supports; or there is liquid on the floating roof; or the seal is detached; or there are holes or tears in the seal fabric; or there are visible gaps between the seal and the wall of the storage vessel, repairs shall be made to the equipment or storage vessel must be emptied and removed from service within 45 calendar days. If a failure is detected that cannot be repaired within 45 calendar days and if the vessel cannot be emptied within 45 calendar days, Permittee may utilize up to two extensions of up to 30 additional calendar days each, provided that documentation of a decision to utilize an extension is maintained that includes a description of the failure, that documents that alternate storage capacity is unavailable, and that specifies a schedule of actions that will ensure that the control equipment will be repaired or the vessel will be emptied as soon as practicable. If during the inspections, the internal floating roof has defects; or the primary seal has holes, tears, or other openings in the seal or the seal fabric; or the secondary seal has holes, tears, or other openings in the seal or the seal fabric; or the gaskets no longer close off the liquid surface from the atmosphere; or the slotted membrane has more than 10 percent open area, the repairs shall be made before the vessel is refilled with organic HAP. [Rule 62-204.800(11), F.A.C., 40 CFR 63.120(a)(2), (4) & (7)]
- A.6. <u>Storage Tank Emission Reduction Partnership Program (STERP)</u>. Permittee shall visually inspect the deck fitting for the slotted guide pole at least once every ten years and each time the vessel is emptied and degassed. If the slotted guide pole deck fitting or control devices have defects, or if a gap of more than 0.32 centimeters (1/8 inch) exists between any gasket required for control of the slotted guide pole deck fitting and any surface that is intended to seal, such items shall be repaired before filling or refilling the storage vessel with regulated material. [Federal Register Notice 19891 (April 13, 2000)]

#### **Recordkeeping and Reporting Requirements**

A.7. <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Periodic Reports	Semi-Annual	A.9.
Notifications	30 Days Prior to Event	A.10.
Other Reporting Requirements	As required by Administrator	A.12.

[Rule 62-213.440(1)(b), F.A.C.]

#### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection A. Emissions Unit 029

- **A.8.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- A.9. <u>Periodic Reports</u>. Periodic reports are to include a summary of the results of each internal or external inspection conducted in which a failure was detected with the date of the inspection, identification of the storage vessel in which a failure was detected and a description of the failure. Also, the nature of and date the repair was made or the date the storage vessel was emptied is to be documented. [Rule 62-204.800(11), F.A.C., 40 CFR 63.122(a)(4) & (5), (d), and 40 CFR 63.123(a), (c) & (g)]
- A.10. <u>Notification Requirements</u>. Except as provided below, for all the inspections, Permittee shall notify the Department in writing at least 30 calendar days prior to the refilling of each storage vessel to afford the Department the opportunity to have an observer present. If the required inspections are not planned and Permittee could not have known about the inspection 30 calendar days in advance of refilling the vessel, Permittee shall notify the Department at least seven calendar days prior to the refilling of the storage vessel. Notification made by telephone shall be immediately followed by written documentation demonstrating why the inspection was unplanned. Documentation pertaining to the utilization of any extensions is to be included. Alternatively, the notification including the written documentation may be made in writing and sent so that it is received by the Department at least seven calendar days prior to refilling. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.120(a)(5) & (6)]
- A.11. <u>Tank Records</u>. Records showing each tank's dimensions and capacities and records of each inspection shall be maintained as long as the tank retains Group 1 status under the HON and is in operation. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.123(a) & (c)]
- A.12. <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:

C.C.1. Startup, Shutdown, and Malfunction Plan

- C.C.3. Recordkeeping and Reporting of Startups, Shutdowns, and Malfunctions
- C.C.5. General Recordkeeping Requirements
- C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G
- C.C.8. Schedule of Reporting for Specific Sources Subject to 40 CFR 63 Subparts F, G and H

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#### Subsection B. Emissions Unit 046

#### The specific conditions in this section apply to the following emission unit:

EU No.	Brief Description
046	Sitewide HON Heat Exchangers

This emissions unit is comprised of non-contact heat exchangers E-671119 and E-67032 used to cool process fluids at the Amines Plants.

{Permitting Note: This emissions unit is subject to 40 CFR 63 Subpart F, National Emission Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry, Hazardous Organic NESHAP (HON) (adopted and incorporated by reference in Rule 62-204.800(11)(b)1., F.A.C.).}

#### The following specific conditions apply to the emissions unit listed above:

#### **Essential Potential to Emit (PTE) Parameters**

**B.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

#### **Operating Conditions and Standards**

- **B.2.** <u>Heat Exchangers Monitoring Requirements</u>. All sitewide heat exchange systems not meeting the conditions specified in 40 CFR 63.104(a)(1) through (6), shall be monitored by inspecting the cooling water for the presence of one or more organic HAPs or other representative substance whose presence in cooling water indicates a leak as specified in 40 CFR 63.104(b)(1) through (6), or by using a surrogate indicator of heat exchanger system leaks as specified in 40 CFR 63.104(c)(1) through (3). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.104(a), (b), & (c)]
- **B.3.** <u>Heat Exchanger Repair Requirements</u>. Any leaks that are detected shall be repaired as soon as practical but not later than 45 days after Permittee receives results of monitoring tests indicating a leak. After repair, Permittee shall confirm that the heat exchange system has been repaired within seven calendar days of the repair or startup, whichever is later. Repairs may be delayed beyond 45 days if the criteria specified in 40 CFR 63.104(e) are met. [Rule 62-204.800(11), F.A.C., 40 CFR 63.104(d) & (e)]

#### **Recordkeeping and Reporting Requirements**

**B.4.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Periodic Reports	Semi-Annual - only if permittee invokes the delay of repair	B.6
Other Reporting Requirements	As required by Administrator	<b>B.</b> 7

[Rule 62-213.440(1)(b), F.A.C.]

- **B.5.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **B.6.** <u>Heat Exchanger Recordkeeping Requirements</u>. Permittee shall maintain records of required monitoring, leaks detected, the date when leak was detected, (if demonstrated not to be a leak, the basis for that determination), the dates of efforts to repair leaks, and the method or procedures used to confirm repair of a leak and the date the repair was confirmed. Periodic reports are required only if Permittee invokes the delay of repair. Periodic reports shall include information required by 40 CFR 63.104(f)(2). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.104(f)]

**B.7.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the limitations and standards contained in Section IV, Common Conditions:

**C.C.5.** General Recordkeeping Requirements

- C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G
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#### Subsection C. Emission Unit 047

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
047	Methanol Storage HON Maintenance Wastewater

Methanol storage equipment is flushed out in order to prepare the equipment for maintenance. Emission estimates of HAP are based on all methanol tanks flushed and cleaned during the same year, and ancillary equipment (i.e., pumps, piping and valves) cleaned and flushed more frequently. This emissions unit is composed of the methanol-containing wastewater resulting from the flushing activity. The Methanol Storage HON Maintenance Wastewater is treated in the plant wastewater system.

EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{*Permitting Note: This emissions unit is regulated by 40 CFR 63 subpart F, National Emission Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry, Hazardous Organic NESHAP (HON) (adopted and incorporated by reference in Rule 62-204.800(11)(b)1., F.A.C.).*}

#### **Essential Potential to Emit (PTE) Parameters**

C.1. <u>Hours of Operation</u>. This emissions unit is allowed to operate on an as-needed basis. [Rule 62-210.200(PTE), F.A.C.]

#### **Operational Conditions and Standards**

- C.2. <u>Management of Wastewaters Containing HAP</u>. Permittee shall maintain a record of maintenance procedures for management of wastewaters containing those organic HAPs listed in Table 9 of 40 CFR 63 Subpart G, which are generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdowns (i.e., routine maintenance). The record of maintenance procedures shall:
  - a. Specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities,
  - b. Specify procedures that will be followed to properly manage the wastewater and control organic HAP emissions to the atmosphere, and
  - c. Specify the procedures to be followed when clearing materials from process equipment.

The permittee shall modify and update the maintenance procedures as needed.

[Rule 62-204.800(11), F.A.C., 40 CFR 63.105(b) & (c)]

#### **Recordkeeping and Reporting Requirements**

C.3. <u>Startup, Shutdown, and Malfunction Plan Records</u>. Permittee shall incorporate the procedures and maintain a record of the information required by 40 CFR 63.105(b) & (c) as part of the startup, shutdown, and malfunction plan required under 40 CFR 63.6(e)(3). Plans shall be maintained and kept readily available for inspection for the life of the source, or until 40 CFR 63 standards no longer apply to the source. Previous versions of plans shall also be maintained for a period of five years following revision. No notification or periodic reporting of maintenance wastewater activities is required. [Rule 62-204.800(11), F.A.C., 40 CFR 63.105(d) & (e)]

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#### Subsection D. Emission Unit 048

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
048	Methylamines Plants Sample Points (HON)

This emissions unit is composed of points in the process where the methanol is sampled for testing and consists solely of various sample points in the process.

{Permitting Notes: This emissions unit is regulated by 40 CFR 63 Subpart H, National Emission Standards for Organic Hazardous Air Pollutants for Equipment Leaks, Hazardous Organic NESHAP (HON) (adopted and incorporated by reference in Rule 62-204.800(11)(b)3., F.A.C.). HON requires that sample purges be contained and returned to the process.}

#### **Essential Potential to Emit (PTE) Parameters**

**D.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

#### **Operating Conditions and Standards**

- **D.2.** <u>Sampling Points in Organic HAP Service</u>. Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent system. Gases displaced during filling of the sample container are not required to be collected or captured. Each sampling system shall meet one of the following specifications:
  - a. Return the purged process fluid directly to the process line; or
  - b. Collect and recycle the purged process fluid to a process; or
  - c. Be designed and operated to capture and transport the purged process fluid to a control device that complies with the requirements of 40 CFR 63.172; or
  - d. Collect, store, and transport the purged process fluid to a system or facility identified below:
    - (1) A waste management unit, or
    - (2) A treatment, storage, or disposal facility, or
    - (3) A facility permitted, licensed, or registered by a State to manage municipal or industrial solid waste, if the process fluids are not hazardous waste.
  - [Rule 62-204.800(11), F.A.C., and 40 CFR 63.166]

#### **Recordkeeping and Reporting Requirements**

**D.3.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	<b>Related Condition(s)</b>
Title V Semiannual Progress Reports	Semi-Annual - any instances of non- compliance must be included in report	D.5.

[Rule 62-213.440(1)(b), F.A.C.]

- **D.4.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- D.5. <u>Title V Semiannual Progress Reports</u>. Permittee shall maintain records specified in 40 CFR 63.181(b)(1)(i) and no periodic reporting is required under 40 CFR 63.182. Notwithstanding, Title V semiannual progress reports shall be submitted that identify any instances of non-compliance and annual Title V compliance certification reports must certify whether or not compliance with applicable requirements has been achieved. [Rule 62-204.800(11), F.A.C. and 40 CFR 63.181] Back to Table of Contents

#### Subsection E. Emission Unit 001

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description	
001	Riley Stoker Boiler	

The Riley Stoker Boiler produces up to 90,000 pounds per hour of 600 psig steam, which is equivalent to 128 MMBtu per hour heat input (1,121,280 MMBtu per year), assuming 80% boiler efficiency. The boiler startup date was November 26, 1955. The boiler is fueled by natural gas and process off-gases.

The boiler burns only gaseous fuels, as defined in 40 CFR 63.7575, which includes, but is not limited to, natural gas and process gas. The boiler is in the subcategory of 'units designed to burn gas 1 fuels'. Boilers in the subcategory of units designed to burn gas 1 fuels are not subject to the emission limits in Tables 1 and 2 or 11 through 13 to 40 CFR 63 Subpart DDDDD, or the operating limits in Table 4 to Subpart DDDDD, per 40 CFR 63.7500(e). Fuel gas system means the offsite and onsite piping and flow and pressure control system that gathers gaseous stream(s) generated by onsite operations, may blend them with other sources of gas, and transports the gaseous stream for use as fuel gas in combustion devices or in-process combustion equipment, such as furnaces and gas turbines, either singly or in combination.

{Permitting Notes: This emissions unit is regulated by Rule 62-296.406, F.A.C. – Fossil Fuel Steam Generators with Less than 250 Million Btu Per Hour Heat Input. This emissions unit is also regulated by 40 CFR 63, Subpart DDDDD – National Emissions Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters (Boiler MACT) (adopted and incorporated by reference in Rule 62-204.800(11)(b)86., F.A.C.).}

#### **Essential Potential to Emit (PTE) Parameters**

- E.1. <u>Capacity</u>. The maximum allowable operating rate of the Riley Stoker Boiler is 128 MMBtu per hour, averaged daily. [Rules 62-210.200 (PTE), 62-213.440(1), F.A.C.; Permit No. 1130004-019-AC]
- **E.2.** <u>Methods of Operation (Fuel)</u>. The boiler may operate using natural gas and process off-gases. Process liquids and used oil are not permitted to be burned in this unit. [Rule 62-210.200(PTE), F.A.C.; Permit No. 1130004-019-AC; and Permit No. 1130004-029-AC]
- **E.3.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year. [Rule 62-210.200(PTE), F.A.C.]

#### **Emission Limitations and Standards**

Unless otherwise specified, the averaging times are based on the specified averaging time of the applicable test method.

**E.4.** <u>Visible Emissions</u>. Visible emissions shall not exceed 20 percent opacity except for one six-minute period per one-hour period during which opacity shall not exceed 27 percent. [Rule 62-296.406(1), F.A.C.]

#### **Test Methods and Procedures**

E.5. <u>Test Methods</u>. Required tests shall be performed in accordance with the following reference method:

EPA Method	Description of Method and Comments
9	Visual Determination of the Opacity of Emissions from Stationary Sources

The above method is described in 40 CFR 60, Appendix A, and adopted by reference in Rule 62-204.800, F.A.C. No other method may be used unless prior written approval is received from the Department. [Rule 62-204.800, F.A.C.]

#### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection E. Emission Unit 001

**E.6.** <u>Common Testing Requirements</u>. Unless otherwise specified, tests shall be conducted in accordance with the requirements and procedures specified in Appendix TR, Facility-Wide Testing Requirements, of this permit. [Rule 62-297.310, F.A.C.]

{Permitting Note: Air compliance test notifications can now be completed online in the Department's Business Portal. To access this online process, go to <u>http://www.fldepportal.com/go/home</u> and sign in (or register if you're a new user) from the link in the upper right corner of the page. On the Welcome page select the Submit option, then select Registration/Notification, and then click on Air Compliance Test Notifications. Once in the process, just carefully read the instructions on each screen (and under the Help tabs) to complete the notification.}

E.7. <u>Compliance Tests Prior To Renewal</u>. Except as provided in subparagraph 62-297.310(8)(b)3., F.A.C. (see condition TR7.b.(3) in Appendix TR – Facility-wide Testing Requirements), compliance tests shall be performed for visible emissions (VE) prior to obtaining a renewed operation permit to demonstrate compliance with the visible emissions limits in Specific Condition E.4. Visible Emissions [Rules 62-210.300(2)(a) and 62-297.310(8)(b), F.A.C.]

*{Permitting Note: Tests which are only required once during the term of a permit prior to obtaining a renewed permit should be performed roughly five years from the previous test.}* 

#### **Work Practice Standards**

**E.8.** <u>Operation and Maintenance</u>. At all times, the Permittee must operate and maintain any affected source (as defined in 40 CFR 63.7490), including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator that may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7500(a)(3)]

#### **Compliance Requirements**

- **E.9.** <u>General Requirements</u>. At all times you must be in compliance with the work practice standards in 40 CFR 63 Subpart DDDDD except for the periods noted in 40 CFR 63.7500(f). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7505(a)]
- **E.10.** <u>Annual Tune Ups Required</u>. Permittee must conduct an annual performance tune-up according to 40 CFR 63.7540(a)(10). Each annual tune-up specified in 40 CFR 63.7540(a)(10) must be conducted no more than 13 months after the previous tune-up. [Rule 62-204.800(11)(b)86., F.A.C., and 40 CFR 63.7515(d)]
- **E.11.** <u>Tune-Up Procedures</u>. Permittee must conduct a tune-up of the boiler to demonstrate continuous compliance as specified in paragraphs (a)(10)(i) through (vi) 40 CFR 63.7540. You must conduct the tune-up while burning the type of fuel (or fuels in case of units that routinely burn a mixture) that provided the majority of the heat input to the boiler over the 12 months prior to the tune-up.
  - a. As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;
  - b. Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;

#### Subsection E. Emission Unit 001

- c. Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;
- d. Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any NOx requirement to which the unit is subject;
- e. Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and
- f. Maintain on-site and submit, if requested by the Administrator, a report containing the information in paragraphs (a)(10)(vi)(A) through (C) of 40 CFR 63.7540.
  - (1) The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
  - (2) A description of any corrective actions taken as a part of the tune-up; and
  - (3) The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7540(a)(10); and Table 3 (Item 3) to Subpart DDDDD of Part 63]

*{Permitting Note: The initial tune-up and the one-time energy assessment for the Riley Stoker Boiler (EU 001) was completed in January 2018.}* 

**E.12.** <u>Fuel Specifications</u>. Permittee shall demonstrate that all gaseous fuels other than natural gas or refinery gas qualifies as an "other gas 1 fuel" unit as defined in 40 CFR 63.7575. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7530(g)]

*{Permitting Note: <u>Other gas 1 fuel</u> means a gaseous fuel that is not natural gas or refinery gas and does not exceed a maximum concentration of 40 micrograms/cubic meters of mercury.}* 

- **E.13.** <u>Fuel Analysis Procedures</u>. Permittee shall conduct an initial fuel specification analysis for mercury according to the procedures in 40 CFR 63.7521(f) through (i) and according to the frequency listed in 40 CFR 63.7540(c).
  - a. To demonstrate that a gaseous fuel other than natural gas or refinery gas qualifies as an other gas 1 fuel, as defined in 40 CFR 63.7575, the Permittee must conduct a fuel specification analyses for mercury according to the procedures in paragraphs (g) through (i) of 40 CFR 63.7521 and Table 6 to 40 CFR 63 Subpart DDDDD, as applicable, except as specified in paragraph (f)(1) through (4) of 40 CFR 63.7521, or as an alternative where fuel specification analysis is not practical, the Permittee must measure mercury concentration in the exhaust gas when firing only the gaseous fuel to be demonstrated as an other gas 1 fuel in the boiler according to the procedures in Table 6 to 40 CFR 63 Subpart DDDDD.
    - (1) You are not required to conduct the fuel specification analyses in paragraphs (g) through (i) of 40 CFR 63.7521 for natural gas or refinery gas.
    - (2) You are not required to conduct the fuel specification analyses in paragraphs (g) through (i) of 40 CFR 63.7521 for gaseous fuels that are subject to another subpart of part 63, part 60, part 61, or part 65.

#### Subsection E. Emission Unit 001

[Rule 62-204.800(11), F.A.C., and 40 CFR 63.7521(f)]

- **E.14.** <u>Fuel Analysis Plan</u>. The Permittee must develop a site-specific fuel analysis plan for other gas 1 fuels according to the following procedures and requirements in paragraphs (g)(1) & (2) of 40 CFR 63.7521.
  - a. If you intend to use an alternative analytical method other than those required by Table 6 to 40 CFR 63 Subpart DDDDD, you must submit the fuel analysis plan to the Administrator for review and approval no later than 60 days before the date that you intend to conduct the initial compliance demonstration described in 40 CFR 63.7510.
  - b. The Permittee must include the information contained in paragraphs (g)(2)(i) through (vi) of 40 CFR 63.7521 in your fuel analysis plan.
    - (1) The identification of all gaseous fuel types other than those exempted from fuel specification analysis under (f)(1) through (3) of 40 CFR 63.7521 anticipated to be burned in each boiler.
    - (2) For each anticipated fuel type, the identification of whether you or a fuel supplier will be conducting the fuel specification analysis.
    - (3) For each anticipated fuel type, a detailed description of the sample location and specific procedures to be used for collecting and preparing the samples if your procedures are different from the sampling methods contained in Table 6 to 40 CFR 63 Subpart DDDDD. Samples should be collected at a location that most accurately represents the fuel type, where possible, at a point prior to mixing with other dissimilar fuel types. If multiple boilers are fueled by a common fuel stream it is permissible to conduct a single gas specification at the common point of gas distribution.
    - (4) For each anticipated fuel type, the analytical methods from Table 6 to 40 CFR 63 Subpart DDDDD, with the expected minimum detection levels, to be used for the measurement of mercury.
    - (5) If you request to use an alternative analytical method other than those required by Table 6 to 40 CFR 63 Subpart DDDDD, you must also include a detailed description of the methods and procedures that you are proposing to use. Methods in Table 6 to 40 CFR 63 Subpart DDDDD shall be used until the requested alternative is approved.
    - (6) If you will be using fuel analysis from a fuel supplier in lieu of site-specific sampling and analysis, the fuel supplier must use the analytical methods required by Table 6 to 40 CFR 63 Subpart DDDDD. When using a fuel supplier's fuel analysis, Permittee is not required to submit the information in 40 CFR 63.7521(g)(2)(iii).

[Rule 62-204.800(11), F.A.C., and 40 CFR 63.7521(g)]

- **E.15.** <u>Fuel Sampling Requirements</u>. The Permittee must obtain a single fuel sample for each fuel type for fuel specification of gaseous fuels. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7521(h)]
- **E.16.** <u>Mercury Concentration</u>. The Permittee must determine the concentration in the fuel of mercury, in units of micrograms per cubic meter, dry basis, of each sample for each other gas 1 fuel type according to the procedures in Table 6 to 40 CFR 63 Subpart DDDDD. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7521(i)]
- **E.17.** <u>Notification of Compliance Status</u>. Permittee must submit the Notification of Compliance Status containing the results of the initial compliance demonstration according to the requirements in 40 CFR 63.7545(e). [Rule 62-204.800(11)(b)86., F.A.C., and 40 CFR 63.7530(f)]
- **E.18.** <u>Fuel Analysis Requirements</u>. If you elect to demonstrate that a gaseous fuel meets the specifications of another gas 1 fuel as defined in 40 CFR 63.7575, you must conduct an initial fuel specification analysis according to 40 CFR 63.7521(f) through (i) and according to the frequency listed in 40 CFR 63.7540(c) and maintain records of the results of the testing as outlined in 40 CFR 63.7555(g). For samples where the initial

#### Subsection E. Emission Unit 001

mercury specification has not been exceeded, you will include a signed certification with the Notification of Compliance Status that the initial fuel specification test meets the gas specification outlined in the definition of other gas 1 fuels. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7530(g)]

#### Notification, Reports, and Records

**E.19.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Compliance Reports	Annual - no later than January 31	<b>E.23.</b> and <b>E.24</b> .
Notifications	As required by Administrator	E.17., E.21. and E.22.

[Rule 62-213.440(1)(b), F.A.C.]

- **E.20.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- E.21. <u>Notifications General</u>. The Permittee must submit to the Administrator all of the notifications in 40 CFR 63.7(b) & (c), 63.8(e), (f)(4) & (6), and 63.9(b) through (h) that apply to you by the dates specified. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7545(a)]
- **E.22.** Notification of Alternative Fuel Use. If you operate a unit designed to burn natural gas, refinery gas, or other gas 1 fuels that is subject to 40 CFR 63 Subpart DDDDD, and you intend to use a fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart of part 63, part 60, 61, or 65, or other gas 1 fuel to fire the affected unit during a period of natural gas curtailment or supply interruption, as defined in 40 CFR 63.7575, you must submit a notification of alternative fuel use within 48 hours of the declaration of each period of natural gas curtailment or supply interruption, as defined in 40 CFR 63.7575. The notification must include the information specified in paragraphs (f)(1) through (5) of 40 CFR 63.7545.
  - a. Company name and address.
  - b. Identification of the affected unit.
  - c. Reason you are unable to use natural gas or equivalent fuel, including the date when the natural gas curtailment was declared or the natural gas supply interruption began.
  - d. Type of alternative fuel that you intend to use.
  - e. Dates when the alternative fuel use is expected to begin and end.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7545(f)]

- **E.23.** <u>Compliance Report Schedule</u>. Unless the EPA Administrator has approved a different schedule for submission of reports under 40 CFR 63.10(a), you must submit each report, according to paragraph (h) of 40 CFR 63.7550, by the date in Table 9 to 40 CFR 63 Subpart DDDDD and according to the requirements in paragraphs (b)(1) through (4) of 40 CFR 63.7550. For units that are subject only to a requirement to conduct subsequent annual tune-up according to 40 CFR 63.7540(a)(10), and not subject to emission limits or Table 4 operating limits, you may submit only an annual compliance report, as applicable, as specified in paragraphs (b)(1) through (4) of 40 CFR 63.7550, instead of a semi-annual compliance report.
  - a. Annual compliance reports must cover the period from January 1 to December 31.
  - b. Annual compliance reports must be postmarked or submitted no later than January 31.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7550(b)]

#### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection E. Emission Unit 001

- **E.24.** <u>Compliance Report Contents</u>. Permittee must submit a compliance report with the information in paragraphs (c)(5)(i) through (iii), (xiv) & (xvii) of 40 CFR 63.7550 as follows:
  - a. Company and Facility name and address.
  - b. Process unit information, emissions limitations, and operating parameter limitations.
  - c. Date of report and beginning and ending dates of the reporting period.
  - d. Include the date of the most recent tune-up for each unit subject to only the requirement to conduct an annual tune-up according to 40 CFR 63.7540(a)(10). Include the date of the most recent burner inspection if it was not done annually and was delayed until the next scheduled or unscheduled unit shutdown.
  - e. Statement by a responsible official with that official's name, title, and signature, certifying the truth, accuracy, and completeness of the content of the report.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7550(c)]

- **E.25.** <u>Records Requirements</u>. The Permittee must keep records according to paragraphs (a)(1) & (2) of 40 CFR 63.7555.
  - a. A copy of each notification and report that you submitted to comply with 40 CFR 63 Subpart DDDDD, including all documentation supporting any Initial Notification or Notification of Compliance Status or annual compliance report that you submitted, according to the requirements in 40 CFR 63.10(b)(2)(xiv).
  - b. Records of performance tests, fuel analyses, or other compliance demonstrations and performance evaluations as required in 40 CFR 63.10(b)(2)(viii).

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7555(a)]

- **E.26.** <u>Fuel Specification Records</u>. If you elected to demonstrate that the unit meets the specification for mercury for the unit designed to burn gas 1 subcategory, you must maintain monthly records (or at the frequency required by 40 CFR 63.7540(c)) of the calculations and results of the fuel specification for mercury in Table 6. [Rule 62-204.800(11)(b)86., F.A.C.; 40 CFR 63.7555(g)]
- **E.27.** <u>Records of Alternate Fuel Usage</u>. If you operate a unit in the unit designed to burn gas 1 subcategory that is subject to this subpart, and you use an alternative fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart under this part, other gas 1 fuel, or gaseous fuel subject to another subpart of this part or part 60, 61, or 65, you must keep records of the total hours per calendar year that alternative fuel is burned and the total hours per calendar year that the unit operated during periods of gas curtailment or gas supply emergencies. [Rule 62-204.800(11)(b)86., F.A.C.; 40 CFR 63.7555(h)]
- **E.28.** <u>Records Retention</u>. Permittee shall maintain records of compliance information in accordance with 40 CFR 63.7560.
  - a. Your records must be in a form suitable and readily available for expeditious review, according to 40 CFR 63.10(b)(1).
  - b. As specified in 40 CFR 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.
  - c. The Permittee must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to 40 CFR 63.10(b)(1). You can keep the records off site for the remaining 3 years.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7560] <sup>1</sup> Back to Table of Contents

#### Subsection F. Emission Unit 003

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
003	B & W Boiler

The B & W Boiler produces 90,000 pounds per hour of steam at 600 psig, which is considered equivalent to 128 MMBtu per hour heat input (1,121,280 MMBtu per year), assuming 80% boiler efficiency. The boiler is fueled by natural gas and process off-gases.

The boiler burns only gaseous fuels, as defined in 40 CFR 63.7575, which includes, but is not limited to, natural gas and process gas. The boiler is in the subcategory of 'units designed to burn gas 1 fuels'. Boilers in the subcategory of units designed to burn gas 1 fuels are not subject to the emission limits in Tables 1 and 2 or 11 through 13 to 40 CFR 63 Subpart DDDDD, or the operating limits in Table 4 to Subpart DDDDD, per 40 CFR 63.7500(e). Fuel gas system means the offsite and onsite piping and flow and pressure control system that gathers gaseous stream(s) generated by onsite operations, may blend them with other sources of gas, and transports the gaseous stream for use as fuel gas in combustion devices or in-process combustion equipment, such as furnaces and gas turbines, either singly or in combination.

{Permitting Note: This emissions unit is regulated by Rule 62-296.406, F.A.C. – Fossil Fuel Steam Generators with Less than 250 Million Btu Per Hour Heat Input. This emissions unit is also regulated by 40 CFR 63, Subpart DDDDD – National Emissions Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters (Boiler MACT) (adopted and incorporated by reference in Rule 62-204.800(11)(b)86., F.A.C.).}

#### **Essential Potential to Emit (PTE) Parameters**

- **F.1.** <u>Capacity</u>. Maximum allowable operating rate of the B & W Boiler is 128 MMBtu per hour, averaged daily. [Rules 62-210.200 (PTE), 62-213.440(1), F.A.C., and Permit No. 1130004-019-AC]
- **F.2.** <u>Methods of Operation (Fuel)</u>. The boiler may operate using natural gas and process off-gases. [Rule 62-210.200(PTE), F.A.C.]
- **F.3.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year. [Rule 62-210.200(PTE), F.A.C.]

#### **Emission Limitations and Standards**

Unless otherwise specified, the averaging times are based on the specified averaging time of the applicable test method.

**F.4.** <u>Visible Emissions</u>. Visible emissions shall not exceed 20 percent opacity except for one six-minute period per one-hour period during which opacity shall not exceed 27 percent. [Rule 62-296.406(1), F.A.C.]

#### **Test Methods and Procedures**

F.5. <u>Test Methods</u>. Required tests shall be performed in accordance with the following reference methods:

EPA Method	Description of Method and Comments
9	Visual Determination of the Opacity of Emissions from Stationary Sources

The above method is described in 40 CFR 60, Appendix A, and adopted by reference in Rule 62-204.800, F.A.C. No other method may be used unless prior written approval is received from the Department.

**F.6.** <u>Common Testing Requirements</u>. Unless otherwise specified, tests shall be conducted in accordance with the requirements and procedures specified in Appendix TR, Facility-Wide Testing Requirements, of this permit. [Rule 62-297.310, F.A.C.]
#### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection F. Emission Unit 003

{Permitting Note: Air compliance test notifications can now be completed online in the Department's Business Portal. To access this online process, go to <u>http://www.fldepportal.com/go/home</u> and sign in (or register if you're a new user) from the link in the upper right corner of the page. On the Welcome page select the Submit option, then select Registration/Notification, and then click on Air Compliance Test Notifications. Once in the process, just carefully read the instructions on each screen (and under the Help tabs) to complete the notification.}

**F.7.** <u>Compliance Tests Prior To Renewal</u>. Except as provided in subparagraph 62-297.310(8)(b)3., F.A.C. (see condition TR7.b.(3) in Appendix TR – Facility-wide Testing Requirements), compliance tests shall be performed for visible emissions (VE) prior to obtaining a renewed operation permit to demonstrate compliance with the visible emissions limits in **Specific Condition F.4. Visible Emissions**. [Rules 62-210.300(2)(a) and 62-297.310(8)(b), F.A.C.]

{*Permitting Note: Tests which are only required once during the term of a permit prior to obtaining a renewed permit should be performed roughly five years from the previous test.*}

# **Work Practice Standards**

**F.8.** <u>Operation and Maintenance</u>. At all times, the Permittee must operate and maintain any affected source (as defined in 40 CFR 63.7490), including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator that may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7500(a)(3)]

## **Compliance Requirements**

- **F.9.** <u>General Requirements</u>. At all times you must be in compliance with the work practice standards in 40 CFR 63 Subpart DDDDD except for the periods noted in 40 CFR 63.7500(f). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7505(a)]
- **F.10.** <u>Annual Tune-Ups Required</u>. Permittee must conduct an annual performance tune-up according to 40 CFR 63.7540(a)(10). Each annual tune-up specified in 40 CFR 63.7540(a)(10) must be conducted no more than 13 months after the previous tune-up. [Rule 62-204.800(11)(b)86., F.A.C., and 40 CFR 63.7515(d)]
- F.11. <u>Tune-Up Procedures</u>. Permittee shall conduct an annual tune-up of the boiler as specified in 40 CFR 63.7540. Units in the Gas 1 subcategory will conduct this tune-up as a work practice for all regulated emissions under 40 CFR 63 Subpart DDDDD. You must conduct an annual tune-up of the boiler to demonstrate continuous compliance as specified in paragraphs (a)(10)(i) through (vi) of 40 CFR 63.7540. You must conduct the tune-up while burning the type of fuel (or fuels in case of units that routinely burn a mixture) that provided the majority of the heat input to the boiler or process heater over the 12 months prior to the tune-up.
  - a. As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;
  - b. Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;

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- c. Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;
- d. Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any NOx requirement to which the unit is subject;
- e. Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and
- f. Maintain on-site and submit, if requested by the Administrator, a report containing the information in paragraphs (a)(10)(vi)(A) through (C) of 40 CFR 63.7540.
  - i. The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
  - ii. A description of any corrective actions taken as a part of the tune-up; and
- iii. The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7540(a)(10); and Table 3 (Item 3) to Subpart DDDDD of Part 63]

*{Permitting Note: The initial tune-up and the one-time energy assessment for the B & W Boiler (EU 003) was completed in January 2016.}* 

**F.12.** <u>Fuel Specifications</u>. Permittee shall demonstrate that all gaseous fuels other than natural gas or refinery gas qualifies as an "other gas 1 fuel" unit as defined in 40 CFR 63.7575. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7530(g)]

{*Permitting Note:* <u>Other gas 1 fuel</u> means a gaseous fuel that is not natural gas or refinery gas and does not exceed a maximum concentration of 40 micrograms/cubic meters of mercury.}

- **F.13.** <u>Fuel Analysis Procedures</u>. Permittee shall conduct an initial fuel specification analysis for mercury according to the procedures in 40 CFR 63.7521(f) through (i) as follows and according to the frequency listed in 40 CFR 63.7540(c) (See Specific Condition F.18. Fuel Analysis Requirements) as follows:
  - a. To demonstrate that a gaseous fuel other than natural gas or refinery gas qualifies as an other gas 1 fuel, as defined in 40 CFR 63.7575, you must conduct a fuel specification analyses for mercury according to the procedures in paragraphs (g) through (i) of 40 CFR 63.7521 and Table 6 to 40 CFR 63 Subpart DDDDD, as applicable, except as specified in paragraph (f)(1) through (4) of 40 CFR 63.7521, or as an alternative where fuel specification analysis is not practical, you must measure mercury concentration in the exhaust gas when firing only the gaseous fuel to be demonstrated as an other gas 1 fuel in the boiler or process heater according to the procedures in Table 6 to 40 CFR 63 Subpart DDDDD.
  - i. You are not required to conduct the fuel specification analyses in paragraphs (g) through (i) of 40 CFR 63.7521 for natural gas or refinery gas.
  - ii. You are not required to conduct the fuel specification analyses in paragraphs (g) through (i) of 40 CFR 63.7521 for gaseous fuels that are subject to another subpart of part3 63, 60, 61, or part 65.

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[Rule 62-204.800(11), F.A.C. and 40 CFR 63.7521(f) and 40 CFR 63.7530(g)]]

- **F.14.** <u>Fuel Analysis Plan</u>. The Permittee must develop a site-specific fuel analysis plan for other gas 1 fuels according to the following procedures and requirements in paragraphs (g)(1) & (2) of 40 CFR 63.7521.
  - a. If you intend to use an alternative analytical method other than those required by Table 6 to 40 CFR 63 Subpart DDDDD, you must submit the fuel analysis plan to the Administrator for review and approval no later than 60 days before the date that you intend to conduct the initial compliance demonstration described in 40 CFR 63.7510.
  - b. The Permittee must include the information contained in paragraphs (g)(2)(i) through (vi) of 40 CFR 63.7521 in your fuel analysis plan.
    - i. The identification of all gaseous fuel types other than those exempted from fuel specification analysis under (f)(1) through (3) of 40 CFR 63.7521 anticipated to be burned in each boiler or process heater.
    - ii. For each anticipated fuel type, the identification of whether you or a fuel supplier will be conducting the fuel specification analysis.
  - iii. For each anticipated fuel type, a detailed description of the sample location and specific procedures to be used for collecting and preparing the samples if your procedures are different from the sampling methods contained in Table 6 to 40 CFR 63 Subpart DDDDD. Samples should be collected at a location that most accurately represents the fuel type, where possible, at a point prior to mixing with other dissimilar fuel types. If multiple boilers or process heaters are fueled by a common fuel stream it is permissible to conduct a single gas specification at the common point of gas distribution.
  - iv. For each anticipated fuel type, the analytical methods from Table 6 to 40 CFR 63 Subpart DDDDD, with the expected minimum detection levels, to be used for the measurement of mercury.
  - v. If you request to use an alternative analytical method other than those required by Table 6 to 40 CFR 63 Subpart DDDDD, you must also include a detailed description of the methods and procedures that you are proposing to use. Methods in Table 6 to 40 CFR 63 Subpart DDDDD shall be used until the requested alternative is approved.
  - vi. If you will be using fuel analysis from a fuel supplier in lieu of site-specific sampling and analysis, the fuel supplier must use the analytical methods required by Table 6 to 40 CFR 63 Subpart DDDDD. When using a fuel supplier's fuel analysis, Permittee is not required to submit the information in 40 CFR 63.7521(g)(2)(iii).

[Rule 62-204.800(11), F.A.C. and 40 CFR 63.7521(g)]

- **F.15.** <u>Fuel Sampling Requirements</u>. The Permittee must obtain a single fuel sample for each fuel type for fuel specification of gaseous fuels. [Rule 62-204.800(11), F.A.C. and 40 CFR 63.7521(h)]
- **F.16.** <u>Mercury Concentration</u>. The Permittee must determine the concentration in the fuel of mercury, in units of microgram per cubic meter, dry basis, of each sample for each other gas 1 fuel type according to the procedures in Table 6 to 40 CFR 63 Subpart DDDDD. [Rule 62-204.800(11), F.A.C. and 40 CFR 63.7521(i)]
- **F.17.** <u>Notification of Compliance Status</u>. Permittee must submit the Notification of Compliance Status containing the results of the initial compliance demonstration according to the requirements in 40 CFR 63.7545(e). [Rule 62-204.800(11)(b)86., F.A.C., and 40 CFR 63.7530(f)]
- **F.18.** <u>Fuel Analysis Requirements</u>. If you elect to demonstrate that a gaseous fuel meets the specifications of another gas 1 fuel as defined in 40 CFR 63.7575, you must conduct an initial fuel specification analysis according to 40 CFR 63.7521(f) through (i) and according to the frequency listed in 40 CFR 63.7540(c) and maintain records of the results of the testing as outlined in 40 CFR 63.7555(g). For samples where the initial mercury specification has not been exceeded, you will include a signed certification with the Notification of

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Compliance Status that the initial fuel specification test meets the gas specification outlined in the definition of other gas 1 fuels. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.7530(g)]

## **RECORDKEEPING AND REPORTING**

**F.19.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Compliance Reports	Annual - no later than January 31	<b>F.23</b> and <b>F.24</b>
Notifications	As required by Administrator	<b>F.17, F.21</b> and <b>F.22</b>

[Rule 62-213.440(1)(b), F.A.C.]

- **F.20.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- F.21. <u>Notifications General</u>. The Permittee must submit to the Administrator all of the notifications in 40 CFR 63.7(b) & (c), 63.8(e), (f)(4) & (6), and 63.9(b) through (h) that apply to you by the dates specified. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7545(a)]
- **F.22.** Notification of Alternative Fuel Use. If you operate a unit designed to burn natural gas, refinery gas, or other gas 1 fuels that is subject to 40 CFR 63 Subpart DDDDD, and you intend to use a fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart of part 63, part 60, 61, or 65, or other gas 1 fuel to fire the affected unit during a period of natural gas curtailment or supply interruption, as defined in 40 CFR 63.7575, you must submit a notification of alternative fuel use within 48 hours of the declaration of each period of natural gas curtailment or supply interruption, as defined in 40 CFR 63.7575. The notification must include the information specified in paragraphs (f)(1) through (5) of 40 CFR 63.7545.
  - a. Company name and address.
  - b. Identification of the affected unit.
  - c. Reason you are unable to use natural gas or equivalent fuel, including the date when the natural gas curtailment was declared or the natural gas supply interruption began.
  - d. Type of alternative fuel that you intend to use.
  - e. Dates when the alternative fuel use is expected to begin and end.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7545(f)]

- **F.23.** <u>Compliance Report Schedule</u>. Unless the EPA Administrator has approved a different schedule for submission of reports under 40 CFR 63.10(a), you must submit each report, according to paragraph (h) of 40 CFR 63.7550, by the date in Table 9 to 40 CFR 63 Subpart DDDDD and according to the requirements in paragraphs (b)(1) through (4) of 40 CFR 63.7550. For units that are subject only to a requirement to conduct subsequent annual tune-up according to 40 CFR 63.7540(a)(10), and not subject to emission limits or Table 4 operating limits, you may submit only an annual compliance report, as applicable, as specified in paragraphs (b)(1) through (4) of 40 CFR 63.7550, instead of a semi-annual compliance report.
  - f. Annual compliance reports must cover the period from January 1 to December 31.
  - g. Annual compliance reports must be postmarked or submitted no later than January 31.
  - [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7550(b)]
- **F.24.** <u>Compliance Report Contents</u>. Permittee must submit a compliance report with the information in paragraphs (c)(5)(i) through (iii), (xiv) & (xvii) of 40 CFR 63.7550 as follows:

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- a. Company and Facility name and address.
- b. Process unit information, emissions limitations, and operating parameter limitations.
- c. Date of report and beginning and ending dates of the reporting period.
- d. Include the date of the most recent tune-up for each unit subject to only the requirement to conduct an annual tune-up according to 40 CFR 63.7540(a)(10). Include the date of the most recent burner inspection if it was not done annually and was delayed until the next scheduled or unscheduled unit shutdown.
- e. Statement by a responsible official with that official's name, title, and signature, certifying the truth, accuracy, and completeness of the content of the report.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7550(c)]

- **F.25.** <u>Records Requirements</u>. The Permittee must keep records according to paragraphs (a)(1) & (2) of 40 CFR 63.7555.
  - a. A copy of each notification and report that you submitted to comply with 40 CFR 63 Subpart DDDDD, including all documentation supporting any Initial Notification or Notification of Compliance Status or annual compliance report that you submitted, according to the requirements in 40 CFR 63.10(b)(2)(xiv).
  - b. Records of performance tests, fuel analyses, or other compliance demonstrations and performance evaluations as required in 40 CFR 63.10(b)(2)(viii).

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.7555(a)]

- **F.26.** <u>Fuel Specification Records</u>. If you elected to demonstrate that the unit meets the specification for mercury for the unit designed to burn gas 1 subcategory, you must maintain monthly records (or at the frequency required by 40 CFR 63.7540(c)) of the calculations and results of the fuel specification for mercury in Table 6. [Rule 62-204.800(11)(b)86., F.A.C.; 40 CFR 63.7555(g)]
- **F.27.** <u>Records of Alternate Fuel Usage</u>. If you operate a unit in the unit designed to burn gas 1 subcategory that is subject to this subpart, and you use an alternative fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart under this part, other gas 1 fuel, or gaseous fuel subject to another subpart of this part or part 60, 61, or 65, you must keep records of the total hours per calendar year that alternative fuel is burned and the total hours per calendar year that the unit operated during periods of gas curtailment or gas supply emergencies. [Rule 62-204.800(11)(b)86., F.A.C.; 40 CFR 63.7555(h)]
- **F.28.** <u>Records Retention</u>. Permittee shall maintain records of compliance information in accordance with 40 CFR 63.7560.
  - a. Your records must be in a form suitable and readily available for expeditious review, according to 40 CFR 63.10(b)(1).
  - b. As specified in 40 CFR 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.
  - c. The Permittee must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to 40 CFR 63.10(b)(1). You can keep the records off site for the remaining 3 years.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7560]

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## Subsection G. Emission Unit 005

## The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
005	Amines Plants Flare

The amines plants flare is a non-assisted flare with a natural gas pilot. Off-gases from the product absorbers at MA Plant Nos. 1 and 4, the Higher Amines Plants and the DIMLA Plant, as well as other process vents at the facility, are continuously released to the flare for destruction. An infra-red and a flame strength camera is utilized to continuously monitor the flame. The flame strength will alarm the control room operator if the flame goes out. The flare will not relight itself. An alarm delay is built into the computer logic to avoid false alarms during brief instances when weather conditions may disrupt the flame viewed by the camera. Natural gas is fed with process gas in a ratio of 0.3:1 for streams that do not have direct BTU measurement to ensure that the minimum net heating value of the gas being combusted is maintained, and a high flow alarm on the natural gas flow ensures that the maximum allowable flare exit velocity is not exceeded.

*Permitting Note: This emissions unit is regulated by 40 CFR 60.18, Subpart A; 40 CFR 63.11, Subpart A; 40* CFR 60 Subpart Kb - Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984 (adopted and incorporated by reference in Rule 62-204.800(8)(b)18., F.A.C.); 40 CFR 63 Subpart F – National Emission Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry (adopted and incorporated by reference in Rule 62-204.800(11)(b)1., F.A.C.); 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.); 40 CFR 63 Subpart H - National Emissions Standards for Organic Hazardous Air Pollutants for Equipment Leaks (adopted and incorporated by reference in Rule 62-204.800(11)(b)3., F.A.C.); and 40 CFR 63 Subpart FFFF - National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing (adopted and incorporated by reference in Rule 62-204.800(11)(b)63., F.A.C.). This emissions unit is subject to the flare requirements in 40 CFR 63, Subpart SS—National Emission Standards for Closed Vent Systems, Control Devices, Recovery Devices and Routing to a Fuel Gas System or a Process (adopted and incorporated by reference in Rule 62-204.800(11)(b)34., F.A.C.). Compliance with NSPS Subparts NNN (Distillation Vents) and RRR (Reactor Vents) will be met by compliance with 40 CFR 63 Subpart FFFF (MON) as per the overlap provisions specified in 40 CFR 63.2535(h).}

## **Essential Potential to Emit (PTE) Parameters**

**G.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

# **Equipment Limitations and Standards**

Unless otherwise specified, the averaging times are based on the specified averaging time of the applicable test method.

- G.2. Operating Limitations. The Amines Plants Flare, a non-assisted flare, shall:
  - a. Be operated at all times when HON or MON-regulated emissions may be vented to it and shall maintain a minimum net heating value of the gas being combusted at 7.45 MJ/scm (200 Btu/scf) (calculated using the net heating value) when emission units subject to 40 CFR 63 Subparts G, H or FFFF are venting to the flare;
  - b. Be operated with a flame present at all times. The presence of a flare pilot flame shall be monitored, *at least once each hour*, using a thermocouple or any other equivalent device to detect the presence of a flame; and

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c. Maintain the exit velocity of gas from the flare at less than or equal to 60 ft/sec (18.3 m/sec).

[Rules 62-204.800(8) & (11), F.A.C., 40 CFR 63.11(b)(3), (5), (6) & (7); 40 CFR 60.18(c)(2), (c)(3), (c)(4), (e), (f)(2) & (f)(4); and 40 CFR 63.998(a)(1)(ii) referenced by 63.987(b)]

- **G.3.** <u>Visible Emissions</u>. The Amines Plants Flare shall be operated with no visible emissions, except for periods not to exceed a total of five minutes in any two consecutive hours. [Rules 62-204.800(8) & (11), F.A.C.; 40 CFR 63.11(b)(4), and 40 CFR 60.18(c)(1) & (f)(1)]
- **G.4.** <u>Alternative Control Device</u>. During periods of flare startup, shutdown, malfunction, and maintenance, or other such periods that the Permittee may choose, the Permittee may divert emissions from the flare to the Boilers (See Emissions Units 001 and 003). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.6(e)(3)]
- **G.5.** <u>DIMLA Process Vent Provisions</u>. Continuous process vent streams from the DIMLA plant will be vented either directly or routed through process recovery devices to the flare at all times when the DIMLA plant is operating. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.2455; and Permit No. 1130004-019-AC]
- **G.6.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the emission limitations and standards contained in Section IV, Common Conditions:

C.C.1. Startup, Shutdown, and Malfunction Plan

C.C.4. Excess Emissions and Data Obtained During Startups, Shutdowns, and Malfunctions

## **Monitoring of Operations**

- **G.7.** <u>Bypass monitoring</u>. Except for equipment needed for safety purposes such as pressure relief devices, low leg drains, high point bleeds, analyzer vents, and open-ended valves or lines, Permittee shall comply with one of the following for each closed vent system that contains bypass lines that could divert a vent stream to the atmosphere:
  - a. Properly install, maintain, and operate a flow indicator that is capable of taking readings at least once every 15 minutes. The flow indicator shall be installed at the entrance to any bypass line. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.983(a)(3)(i) & (b)(4)(i), referenced by 40 CFR 63.2450(e) via 63.982(b)]
  - b. Secure the bypass line valve in the non-diverting position with a car-seal or a lock-and-key type configuration and visually inspect the seal or closure mechanism at least monthly to verify that the valve is maintained in the non-diverting position, and the vent stream is not diverted through the bypass line.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.983(a)(3)(ii) & (b)(4)(ii), referenced by 40 CFR 63.2450(e) via 63.982(b)]

- **G.8.** <u>Leak Monitoring</u>. Each closed vent system used to route vent streams to the flare shall be inspected in accordance with Method 21 of 40 CFR part 60, Appendix A, initially, and then annually using sensory means as specified in 40 CFR 63.983(b) & (c). If there are visible, audible, or olfactory indications of leaks at the time of the annual visual inspections, the leaks will be repaired and monitored as specified in 40 CFR 63.983(d). [Rules 62-204.800(11), F.A.C.; 40 CFR 63.982(b), referenced by 40 CFR 63.2450(e)]
- G.9. <u>Flare Monitoring Requirements</u>. Permittee shall:
  - a. Demonstrate compliance with the minimum net heating value requirement by maintaining a vent gas to natural gas fuel input ratio sufficient to maintain a minimum net heating value of 7.45 MJ/scm (200 Btu/scf) (calculated using the net heating value). Approved alternate monitoring allows use of the Honeywell control system that continuously monitors the natural gas and process gas flow rate at the flare in lieu of collecting samples of gas ducted to the flare tip for heating value analysis and testing to measure the velocity at the flare tip;

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- b. Continuously monitor for the presence of a flare pilot flame using a thermocouple or any other equivalent device to detect the presence of a flame; and
- c. Utilize a high velocity alarm to ensure the maximum allowable velocity of 60 ft/sec (18.3 (m/sec) will not be exceeded.

[Rules 62-204.800(8) & (11), F.A.C., 40 CFR 63.11(b)(3), (5), (6) & (7), and 40 CFR 60.18(c)(2), (c)(3), (c)(4), (e), (f)(2), (f)(3) & (f)(4)]

## **Test Methods and Procedures**

**G.10.** <u>Test Methods</u>. When required, tests shall be performed in accordance with the following reference methods:

Method	Description of Method and Comments
22	Visual determination of fugitive emissions from material sources

The above methods are described in 40 CFR 60, Appendix A, and adopted by reference in Rule 62-204.800, F.A.C. No other methods may be used unless prior written approval is received from the Department. [Rule 62-204.800, F.A.C., and Permit No. 1130004-019-AC]

**G.11.** <u>Common Testing Requirements</u>. Unless otherwise specified, tests shall be conducted in accordance with the requirements and procedures specified in Appendix TR, Facility-Wide Testing Requirements, of this permit. [Rule 62-297.310, F.A.C.]

{Permitting Note: Air compliance test notifications can now be completed online in the Department's Business Portal. To access this online process, go to <u>http://www.fldepportal.com/go/home</u> and sign in (or register if you're a new user) from the link in the upper right corner of the page. On the Welcome page select the Submit option, then select Registration/Notification, and then click on Air Compliance Test Notifications. Once in the process, just carefully read the instructions on each screen (and under the Help tabs) to complete the notification.}

**G.12.** <u>Compliance Tests Prior to Renewal</u>. Permittee shall conduct a flare compliance assessment using EPA Method 22 during operations at a time when either the MA Plant No. 1 or 4 <u>and</u> the DIMLA Plant are operating. The test shall be conducted within the 12 months prior to the submittal of and included with the Title V Permit Renewal Application. The observation period shall be at least two hours. [Rules 62-204.800(8) & (11), F.A.C.; 40 CFR 63.11(b)(4), 40 CFR 60.18(c)(1) & (f)(1); and Permit No. 1130004-019-AC]

*{Permitting Note. Taminco does not have any measurable parameters in existing permits to show the plants are operating at maximum capacity, but they do have measurable parameters for the flare.}* 

- **G.13.** <u>Startup, Shutdown, Malfunction</u>. Permittee shall maintain compliance with 40 CFR 63 requirements pertaining to startup, shutdown and malfunction in accordance with other permit conditions set forth in this permit that pertain to emission units that emit organic hazardous air pollutants to the Amines Flare and that are regulated under 40 CFR 63 Subparts F, G, and H. [Rules 62-204.800(11), F.A.C.; and 40 CFR 63.10(d)(5)]
- **G.14.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the test methods and procedures contained in Section IV, Common Condition: **C.C.9.** Closed Vent System Inspections.

## Subsection G. Emission Unit 005

#### **Recordkeeping and Reporting Requirements**

**G.15.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Periodic/Semiannual Compliance Reports (Includes Flare Compliance Reports	Semi-Annual	G.18. and G.21.
Annual Calibration Report	Annual	G.18.
Other Reporting Requirements	As required by Administrator	G.22.

[Rule 62-213.440(1)(b), F.A.C.]

- **G.16.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- G.17. Flare Compliance Records. Permittee shall maintain records of the following information:
  - a. Identification of the dates and durations of periods during which the minimum heating value, pilot flame, and exit velocity requirements were not maintained and the reasons why these requirements were not met; and
  - b. Identification of the dates and durations during which flare control and monitoring systems were inoperative.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.118(a)(1), 40 CFR 63.130(a)(1) and 40 CFR 63.130(a)(2)(i)]

- G.18. <u>Flare Compliance Reports</u>. Permittee shall submit periodic reports that identify each occurrence during which heating value, pilot flame, and exit velocity requirements were not maintained. Periodic reports shall also specify periods during which the control and monitoring systems were inoperative. The lack of monitoring data shall not constitute an excursion if other process data is available that adequately demonstrates that the flare was operating normally. Permittee shall submit an annual calibration report for calibration of the orifice plates that measure the flow rate of natural gas and process gas sent to the flare. [Rules 62-204.800(8) and (11), F.A.C.; 40 CFR 63.122(g)(3), 40 CFR 63.152(c)(4)(E)(iii), and 40 CFR 60.115b]
- **G.19.** <u>Maintenance Records and Reporting</u>. Permittee shall maintain compliance with 40 CFR 63 requirements pertaining to reporting of maintenance activities in accordance with other permit conditions set forth in this permit for emission units that emit organic hazardous air pollutants to the Amines Flare and that are regulated under 40 CFR 63 Subparts F, G, H and FFFF. [Rules 62-204.800(11), F.A.C., and 40 CFR 63.10(d)(5)]</u>
- **G.20.** <u>Bypass Monitoring Records</u>. For each closed vent system that contains bypass lines that could divert a vent stream away from the control device and to the atmosphere, the permittee shall keep a record of the information specified in either paragraph (d)(1)(ii)(A) or (B) of 40 CFR 63.998, as applicable.
  - a. Hourly records of whether the flow indicator specified under 40 CFR 63.983(a)(3)(i) was operating and whether a diversion was detected at any time during the hour, as well as records of the times of all periods when the vent stream is diverted from the control device or the flow indicator is not operating.
  - b. Where a seal mechanism is used to comply with 40 CFR 63.983(a)(3)(ii), hourly records of flow are not required. In such cases, the permittee shall record that the monthly visual inspection of the seals or closure mechanisms has been done, and shall record the occurrence of all periods when the seal mechanism is broken, the bypass line valve position has changed, or the key for a lock-and-key type lock has been checked out, and records of any car-seal that has been broken.

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[Rules 62-204.800(11), F.A.C.; 40 CFR 63.983(a)(3), referenced by 40 CFR 63.2450(e) via 63.982(b); and Permit No. 1130004-019-AC]

- **G.21.** <u>Periodic/Semiannual Compliance Reports</u>. Permittee shall maintain continuous records of flare operation and shall submit periodic reports on flare operation as required by 40 CFR 63.152(c)(4). The Periodic Reports shall include the information in paragraphs (c)(4)(i) through (c)(4)(iv) of 40 CFR 63.152, as applicable:
  - a. For process vents, reports of process changes as required under 40 CFR 63.118 (g), (h), (i), and (j),
  - b. Any supplements required under 40 CFR 63.151(i) & (j),
  - c. Notification if any Group 2 emission point becomes a Group 1 emission point, including a compliance schedule as required in 40 CFR 63.100, and
  - d. For gas streams sent for disposal pursuant to 40 CFR 63.113(i) or for process wastewater streams sent for treatment pursuant to 40 CFR 63.132(g), reports of changes in the identity of the transferee.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.118 and 40 CFR 63.152(c)(4)]

- **G.22.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:
  - **C.C.1.** Compliance Monitoring
  - C.C.2. Startup, Shutdown, and Malfunction Plan
  - C.C.3. Recordkeeping and Reporting of Startups, Shutdowns, and Malfunctions
  - C.C.5. General Recordkeeping Requirements
  - C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G
  - C.C.7. Additional Reporting Requirements for Sources with Continuous Monitoring Systems
  - C.C.8. Schedule of Reporting for Specific Sources Subject to 40 CFR 63 Subparts F, G and H

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## Subsection H. Emission Unit 006

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
006	Methylamines Plant No. 1 Gas-Fired Heater

At MA Plant No. 1, a natural gas-fired preheater is used to heat the reaction of methyl alcohol, ammonia and recycled methylamines from the process to yield methylamine.

{*Permitting Note: This emissions unit is subject to 40 CFR 63, Subpart DDDDD – National Emissions Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters (Boiler MACT) (adopted and incorporated by reference in Rule 62-204.800(11)(b)86., F.A.C.).*}

## **Essential Potential to Emit (PTE) Parameters**

- **H.1.** <u>Capacity</u>. The maximum allowable operating rate of the Methylamines Gas-Fired Heater is 10.0 MMBtu per hour heat input. The actual gas-fired heater heat input will be calculated on a semi-annual basis as the sum of the previous 12 months total measured flow of natural gas to the heater and the average higher heating value of the natural gas. [Rule 62-4.070(3), 62-210.200(PTE) and 62-213.440(1), F.A.C.]
- **H.2.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

## **Emission Limitations and Compliance Requirements**

**H.3.** <u>Annual Tune-ups</u>. Permittee shall conduct an annual tune-up of the boiler. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7540(a)(10); and Table 3 (Item 3) to Subpart DDDDD of Part 63]

*{Permitting Note: The one-time energy assessment for this emissions unit was completed in January 2016.}* 

- **H.4.** <u>Tune-up Requirements</u>. Permittee shall perform tune-ups according to the criteria specified in 40 CFR 63.7540(a)(10)(i) through (vi). The Permittee must conduct the tune-up while burning the type of fuel (or fuels in case of units that routinely burn a mixture) that provided the majority of the heat input to the boiler or process heater over the 12 months prior to the tune-up.
  - a. As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;
  - b. Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;
  - c. Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;
  - d. Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any NOx requirement to which the unit is subject;
  - e. Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and

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- f. Maintain on-site and submit, if requested by the Administrator, a report containing the following information:
  - (1) The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
  - (2) A description of any corrective actions taken as a part of the tune-up; and
  - (3) The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7540(a)(10)]

#### **Recordkeeping and Reporting Requirements**

**H.5.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	<b>Related Condition(s)</b>
Tune-Up Reports	if requested by Administrator	H.7. and H.4.f

[Rule 62-213.440(1)(b), F.A.C.]

- **H.6.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **H.7.** <u>Tune-Up records and Reports</u>. Permittee shall maintain and submit, if requested by the Administrator, a report containing the following information:
  - a. The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
  - b. A description of any corrective actions taken as a part of the tune-up; and
  - c. The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7540(a)(10)(vi)]

- **H.8.** <u>Records Retention</u>. Permittee shall maintain records of compliance information in accordance with 40 CFR 63.7560.
  - a. Your records must be in a form suitable and readily available for expeditious review, according to 40 CFR 63.10(b)(1).
  - b. As specified in 40 CFR 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.
  - c. The Permittee must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to 40 CFR 63.10(b)(1). You can keep the records off site for the remaining 3 years.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7560]

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## Subsection I. Emission Unit 049

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
049	Methylamines Plant No. 1 Process Vents

Emissions from several process vents at MA Plant No. 1 are collected using a vapor collection system and routed to the Amines Flare (EU 005) or boilers during normal operation. MA Plant No. 1 process vents used intermittently include, but are not limited to, the Low-Pressure Absorber vent and the High Pressure Absorber vent. The absorbers are used for product recovery and are not considered pollution control devices.

{Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.). As stated in 40 CFR 63 Subpart G, "After the compliance dates specified in 40 CFR 63.100 (40 CFR 63 Subpart F), a Group 1 process vent that is also subject to the provisions of 40 CFR 60 Subpart NNN is required to comply only with the provisions of 40 CFR 63 Subpart F." [40 CFR 63.110(d)(4)]; and, "After the compliance dates specified in 40 CFR 63.100, a Group 1 process vent that is also subject to the provisions of 40 CFR 63 Subpart F." [40 CFR 63.110(d)(7)]}

## **Essential Potential to Emit (PTE) Parameters**

**I.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

#### **Equipment Limitations and Standards**

**I.2.** <u>Organic HAP Control Device</u>. Permittee shall reduce emissions of organic hazardous air pollutants (i.e., chemicals listed in Table 2 of 40 CFR 63 Subpart F) using a vapor collection system and flare meeting the criteria of 40 CFR 63.11(b). [Rules 62-204.800(11), F.A.C., and 40 CFR 63.113(a)(1)]

#### **Test Methods and Procedures**

I.3. <u>Flare Requirements</u>. Organic hazardous air pollutant emissions from MA Plant No. 1 Process Vents shall be vented to the Amines Plants Flare, which shall meet the general control device requirements of 40 CFR 63.11(b). Specific permit conditions applicable to the Amines Plants Flare are specified elsewhere in this permit (See EU 005, Specific Condition G.2. Operating Limitations). [Rules 62-204.800(11), F.A.C., and 40 CFR 63.113(a)(1)]

#### Recordkeeping and Reporting Requirements

I.4. <u>Reporting Schedule</u>. The following reports shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Other Recordkeeping and Reporting Requirements	As required by Administrator	I.6

[Rule 62-213.440(1)(b), F.A.C.]

- **I.5.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **I.6.** <u>Other Recordkeeping and Reporting Requirements</u>. emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:

C.C.2. Startup, Shutdown, and Malfunction Plan

C.C.3. Recordkeeping and Reporting of Startups, Shutdowns, and Malfunctions

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- C.C.4. Excess Emissions and Data Obtained During Startups, Shutdowns, and Malfunctions
- C.C.5. General Recordkeeping Requirements
- C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G
- C.C.8. Schedule of Reporting for Specific Sources Subject to 40 CFR 63 Subparts F, G and H
- C.C.9. Closed Vent System Inspections

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## Subsection J. Emission Unit 050

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
050	Methylamines Plant No. 1 Wastewater

MA Plant No. 1 Wastewater is the bottoms stream from various MA Plant No. 1 distillation columns. The stream, consisting of water and negligible quantities of product and methanol, is directed to the plant sewer system, which goes to the Wastewater Treatment Plant, after processing in the dehydration column and/or the environmental column.

EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.).}

## **Essential Potential to Emit (PTE) Parameters**

**J.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

## **Equipment Limitations and Standards**

J.2. Group 1 or Group 2 Determination. Permittee shall comply with the requirements in 40 CFR 63.132 (a)(1) through (a)(3), which requires a determination of a wastewater emissions source being a Group 1 or Group 2 stream. For Group 2 streams, the Permittee shall comply with the recordkeeping requirements of 40 CFR 63.147 (See Specific Condition J.3. Reporting Schedule). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.132(a) and 63.147]

## **Recordkeeping and Reporting Requirements**

**J.3.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	<b>Reporting Deadline</b>	Related Condition(s)
Other Reporting Requirements	As required by Administrator	J.6

[Rule 62-213.440(1)(b), F.A.C.]

- **J.4.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **J.5.** <u>Process Knowledge</u>. If Permittee has used process knowledge to determine the annual average concentration of a wastewater stream and/or the annual average flow rate and thereby concluded that a wastewater stream is not a Group 1 stream, Permittee shall keep in a readily accessible location the documentation of how process knowledge was used. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.147(f)]
- **J.6.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:

C.C.5. General Recordkeeping Requirements

C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G

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## Subsection K. Emission Unit 051

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
051	Methylamines Plant No. 1 HON Maintenance Wastewater

Wastewater removed during maintenance activities at the MA Plant No. 1 is disposed of in the plant wastewater system.

EUs for individual plant wastewater are for regulatory purposes only and emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.).}

## The following specific conditions apply to the emissions unit listed above:

## **Essential Potential to Emit (PTE) Parameters**

**K.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate on an as-needed basis. [Rule 62-210.200(PTE), F.A.C.]

## **Operational Limitations and Standards**

- **K.2.** <u>Maintenance Procedures</u>. Permittee shall maintain, modify and update as needed a description of the maintenance procedures for management of wastewaters containing those organic HAPs listed in Table 9 of 40 CFR Subpart G which are generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdown (i.e., routine maintenance). The descriptions shall:
  - a. Specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities,
  - b. Specify procedures that will be followed to properly manage the wastewater and control organic HAP emissions to the atmosphere, and
  - c. Specify the procedures to be followed when clearing materials from process equipment.

[Rule 62-204.800(11), F.A.C., and 40 CFR 63.105(b) & (c)]

#### **Recordkeeping and Reporting Requirements**

- **K.3.** <u>Startup, Shutdown, Malfunction Plan</u>. Permittee shall maintain a record of the required information as part of the startup, shutdown, and malfunction plan required under 40 CFR 63.6(e)(3). Plans shall be maintained and kept readily available for inspection for the life of the source, or until 40 CFR 63 standards no longer apply to the source. Previous versions of Plans shall also be maintained for a period of five years following revision. No notification or periodic reporting of maintenance wastewater activities is required. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.105(d)]
- **K.4.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:
  - C.C.5. General Recordkeeping Requirements
  - C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G
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## Subsection L. Emission Unit 053

## The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
053	Methylamines Plant Nos. 1 and 4 HON Group 2 Storage Tanks

Storage tanks D-68127, D-68146, D-67116O and D-67134B are used in the common service of both MA Plant Nos. 1 and 4. These storage tanks are vented through scrubbers and/or knock out pots and vented to the Amines Plants Flare (EU 005). The scrubbers are used to maximize product recovery with air emissions being controlled by the flare or boilers. These tanks are all Group 2 tanks because they have a capacity less than 10,000 gallons per 40 CFR 63 Subpart FFFF (Definitions).

{Permitting Note: These tanks are subject to the HON requirements of 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2, F.A.C.).}

## The following specific conditions apply to the emissions unit listed above:

## **Essential Potential to Emit (PTE) Parameters**

L.1. <u>Hours of Operation</u>. This emissions unit is allowed to operate on an as-needed basis. [Rule 62-210.200(PTE), F.A.C.]

## **Recordkeeping and Reporting Requirements**

- L.2. <u>Dimension and Capacity Records</u>. Permittee shall keep records showing the dimensions of the Group 2 storage vessel and an analysis showing its capacity. Permittee is not required to comply with any other provisions of 40 CFR 63.119 through 40 CFR 63.123. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.123(a)]
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## Subsection M. Emission Unit 054

## The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
054	Methylamines Plant Nos. 1 and 4 NSPS Storage Tanks

Storage tanks D-67204E, D-67216A and D-67216B are used in common service of both MA Plant Nos. 1 and 4.

All product storage tanks are vented through absorbers and/or knock out pots and vented to the flare or boilers. The absorbers are used to maximize product recovery, with air emissions being controlled by the flare.

{Permitting Note: These tanks are exempt from the NESHAP regulations but remain subject to the NSPS requirements of 40 CFR 60 Subpart Kb, Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction or Modification Commenced After July 23, 1984 (adopted and incorporated by reference in Rule 62-204.800(8)(b)18., F.A.C.).}

## The following specific conditions apply to the emissions unit listed above:

## **Essential Potential to Emit (PTE) Parameters**

**M.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

## **Equipment Limitations and Standards**

- **M.2.** <u>VOC Reduction</u>. The Methylamines NSPS Storage Tanks shall vent through a closed vent system followed by a control device designed and operated to reduce inlet emissions of VOC by 95 percent. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.112b(a)(3)(i)]
- M.3. <u>Flare Requirements</u>. Emissions from the storage tanks shall be vented to the Amines Plants Flare (EU 005), which shall meet the general control device requirements of 40 CFR 60.18. Specific permit conditions applicable to the Amines Plants Flare are specified elsewhere in this permit (See EU 005, Specific Condition G.2. Operating Limitations). [Rule 62-204.800(8)., F.A.C., and 40 CFR 60.112b(a)(3)(ii)]
- **M.4.** <u>Closed Vent System Limits</u>. The closed vent system shall be designed to collect all VOC vapors and gases discharged from the storage vessel and operated with no detectable emissions as indicated by an instrument reading of less than 500 ppm above background and visual inspections, as determined in 40 CFR 60.485a(b). [Rule 62-204.800(8), F.A.C., and 40 CFR 60.112b(a)(3)(i)]

## **Excess Emissions**

- Rule 62-210.700 (Excess Emissions), F.A.C. cannot vary any requirement of an NSPS, NESHAP or Acid Rain program provision.
- **M.5.** Excess Emissions. Excess emissions resulting from startup, shutdown or malfunction of any emissions unit shall be permitted provided (1) best practices to minimize emissions are adhered to and (2) the duration of excess emissions shall be minimized but in no case exceed two hours in any 24-hour period unless specifically authorized by the Department for longer duration. Excess emissions that are caused entirely or in part by poor maintenance, poor operation, or any other equipment or process failure that may reasonably be prevented during startup, shutdown or malfunction shall be prohibitedExcess emissions which are caused entirely or in part by poor maintenance, poor operation, or any other equipment or process failure which may reasonably be prevented during startup, shutdown, or malfunction shall be prohibited. [Rule 62-210.700(1), F.A.C.]
- **M.6.** <u>Notification and Reporting</u>. In case of excess emissions resulting from malfunctions, the permittee shall notify the Department or the appropriate Local Program in accordance with Rule 62-4.130, F.A.C. A full written report on the malfunctions shall be submitted in a quarterly report, if requested by the Department. [Rule 62-210.700(5), F.A.C.]

## Subsection M. Emission Unit 054

## **Monitoring of Operations**

- M.7. <u>Storage Vessel Monitoring</u>. Permittee of each storage vessel with a design capacity greater than or equal to 75 m3 but less than 151 m3 storing a liquid with a maximum true vapor pressure greater than or equal to 15.0 kPa shall maintain a record of the VOL stored, the period of storage, and the maximum true vapor pressure of that VOL during the respective storage period. These records shall be kept for at least two years. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.116b(c)]
- **M.8.** <u>Vapor Pressure Monitoring</u>. Permittee of each storage vessel with a design capacity greater than or equal to 75 m3 but less than 151 m3 storing a liquid with a maximum true vapor pressure that is normally less than 27.6 kPa shall notify the Administrator within 30 days when the maximum true vapor pressure of the liquid exceeds the respective maximum true vapor pressure values for each volume range. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.116b(d)]

#### **Recordkeeping and Reporting Requirements**

**M.9.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	<b>Reporting Deadline</b>	Related Condition(s)
Notifications – Excess Vapor Pressure	Within 30 days of event	M.8.

[Rule 62-213.440(1)(b), F.A.C.]

- **M.10.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- M.11. <u>Storage Vessel Records</u>. Permittee of each storage vessel as specified in 40 CFR 60.110b(a) shall keep readily accessible records showing the dimension of the storage vessel and an analysis showing the capacity of the storage vessel. The records required by paragraph (b) of 40 CFR 60.116b shall be kept for the life of the source. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.116b(b)]

## Additional Recordkeeping and Reporting Requirements

- **M.12.** <u>Storage Vessel Recordkeeping</u>. The permittee shall maintain a readily accessible record of the volatile organic liquid (VOL) stored, the period of storage, and the maximum true vapor pressure of that VOL for at least two years, and available for Department inspection. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.116b(c)]
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## Subsection N. Emission Unit 007

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
007	Higher Amines Plant No. 2 Gas-Fired Heater

At the Higher Amines Plant No. 2, a natural gas-fired preheater is used to heat the reaction of alcohols, ethers, aldehydes, ketones and other amines to yield various alkylamines.

{*Permitting Note: This emissions unit is subject to 40 CFR 63, Subpart DDDDD – National Emissions Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters (Boiler MACT) (adopted and incorporated by reference in Rule 62-204.800(11)(b)86., F.A.C.).*}

## **Essential Potential to Emit (PTE) Parameters**

- **N.1.** <u>Capacity</u>. The maximum allowed operating rate of the Higher Amines Gas-Fired Heater is 8.4 MMBtu/hr. The gas-fired heater heat capacity will be calculated on a semi-annual basis as the sum of the previous 12 months total measured flow of natural gas to the heater and the average higher heating value of the natural gas. [Rules 62-4.070(3), 62-210.200(PTE) and 62-213.440(1), F.A.C.]
- N.2. <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

## **Emission Limitations and Compliance Requirements**

- N.3. <u>Tune-Up</u>. Permittee shall conduct a biennial tune-up of the boiler. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7540(a)(11); and Table 3 (Item 2) to Subpart DDDDD of Part 63] {*Permitting Note: The one-time energy assessment for this emissions unit was completed in January 2016.*}
- **N.4.** <u>Tune-Up Procedures</u>. Permittee shall perform tune-ups according to the criteria specified in 40 CFR 63.7540(a)(10)(i) through (vi). The Permittee must conduct the tune-up while burning the type of fuel (or fuels in case of units that routinely burn a mixture) that provided the majority of the heat input to the boiler or process heater over the 12 months prior to the tune-up.
  - a. As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;
  - b. Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;
  - c. Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;
  - d. Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any NOx requirement to which the unit is subject;
  - e. Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and

Subsection N. Emission Unit 007

- f. Maintain on-site and submit, if requested by the Administrator, a report containing the following information:
  - (1) The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
  - (2) A description of any corrective actions taken as a part of the tune-up; and
  - (3) The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7540(a)(10)]

## **RECORDKEEPING AND REPORTING**

**N.5.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	<b>Related Condition(s)</b>
Tune-Up Reports	Annual – if requested by Administrator	N.7.

[Rule 62-213.440(1)(b), F.A.C.]

- **N.6.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **N.7.** <u>Tune-Up Reports</u>. Permittee shall maintain and submit, if requested by the Administrator, a report containing the following information:
  - a. The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
  - b. A description of any corrective actions taken as a part of the tune-up; and
  - c. The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7540(a)(10)(vi)]

- N.8. <u>Records Retention</u>. Permittee shall maintain records in accordance with 40 CFR 63.7560 as follows:
  - a. Your records must be in a form suitable and readily available for expeditious review, according to 40 CFR 63.10(b)(1).
  - b. As specified in 40 CFR 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.
  - c. The Permittee must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to 40 CFR 63.10(b)(1). You can keep the records off site for the remaining 3 years.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7560]

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## Subsection O. Emission Unit 055

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description	
055	72-inch Batch Column Process Vent	

A 72-inch batch distillation column is physically located within the Higher Amines Plant area but is a detached stand-alone processing unit. The process vent from the column exhausts to the Amines Plants Flare (EU 005) or boilers (EU 001 and EU 003) when not under vacuum operation.

As the column is a flexible process (i.e., not used for the same process all year), the actual operation of the column is continuous operation when in use. This column does not process, use, or generate any organic HAPs listed in section 112(b) of the Clean Air Act or hydrogen halide and halogen HAP. This column does not manufacture as a primary product the chemicals listed in 40 CFR 63.100(b)(1)(i) or (ii).

{Permitting Note: This column does not process, use, or generate any organic HAPs listed in section 112(b) of the Clean Air Act or hydrogen halide and halogen HAP; therefore, this column is not subject to 40 CFR 63 Subpart FFFF. This column does not manufacture as a primary product the chemicals listed in 40 CFR 63.100(b)(1)(i) or (ii); therefore, this column is not subject to 40 CFR 63 Subpart G.}

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## Subsection P. Emission Unit 056

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
056	72-inch Batch Column Maintenance Wastewater

Wastewater removed during maintenance activities on the 72-inch batch distillation column and associated equipment is disposed of in the plant sewer system, which goes to the Wastewater Treatment Plant. The 72-inch Batch Column is physically located within the Higher Amines Plant area but is a detached, stand-alone activity. EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{Permitting Note: This column does not process, use, or generate any organic HAPs listed in section 112(b) of the Clean Air Act or hydrogen halide and halogen HAP; therefore, this column is not subject to 40 CFR 63 Subpart FFFF. This column does not manufacture as a primary product the chemicals listed in 40 CFR 63.100(b)(1)(i) or (ii); therefore, this column is not subject to 40 CFR 63 Subpart G.}

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## Subsection Q. Emission Unit 058

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
058	DIMLA MON Group 2 Storage Tank

The Formalin storage tank (TK-62141), installed for the DIMLA unit, also meets the MON definition of a Group 2 storage tank because it has a capacity less than 10,000 gallons. The DIMLA Formalin tank (TK-62141) is stainless steel and vents to the atmosphere.

{Permitting Note: This emissions unit is subject to 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.) and 40 CFR 63 Subpart FFFF - National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing (adopted and incorporated by reference in Rule 62-204.800(11)(b)63., F.A.C.).}

## **Essential Potential to Emit (PTE) Parameters**

**Q.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate on an as-needed basis. [Rule 62-210.200(PTE), F.A.C.]

## **Recordkeeping and Reporting Requirements**

- **Q.2.** <u>Operational Records</u>. Permittee shall keep records showing the dimensions of each storage vessel and an analysis showing the capacity of each vessel. Permittee is not required to comply with any other provisions of 40 CFR 63.119 through 40 CFR 63.123, per 40 CFR 63.119(a)(3). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.123(a)]
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## Subsection R. Emission Unit 059

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
059	72" Batch Column Wastewater

Wastewater is comprised of the column bottoms stream from the 72-inch batch distillation column. This wastewater is disposed in the plant sewer system, which goes to the Wastewater Treatment Plant. The 72-inch Batch Column is physically located within the Higher Amines Plant area but is a detached stand-alone activity.

EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{Permitting Note: This column does not process, use, or generate any organic HAPs listed in section 112(b) of the Clean Air Act or hydrogen halide and halogen HAP; therefore, this column is not subject to 40 CFR 63 Subpart FFFF. This column does not manufacture as a primary product the chemicals listed in 40 CFR 63.100(b)(1)(i) or (ii); therefore, this column is not subject to 40 CFR 63 Subpart G.}

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## Subsection S. Emission Unit 060

## The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
060	Methylamines Plant No. 4 Gas Fired Heater

At MA Plant No. 4, a natural gas-fired preheater is used to heat the reaction of methyl alcohol, ammonia and recycled methylamine to yield methylamine. The feed streams to the MA process are preheated using reactor effluents in a series of heat exchangers to maximize energy efficiency. A secondary steam reboiler is provided for start-up and is used as needed to maintain proper temperature of the streams.

{*Permitting Note: This emissions unit is subject to 40 CFR 63, Subpart DDDDD – National Emissions Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters (Boiler MACT) (adopted and incorporated by reference in Rule 62-204.800(11)(b)86, F.A.C.).*}

## **Essential Potential to Emit (PTE) Parameters**

**S.1.** <u>Permitted Capacity</u>. The maximum allowable heat input rate is as follows:

	EU No.	Unit Description	MMBtu/hr Heat Input	Fuel Type
	060	MA Plant No. 4 Gas-Fired Heater	10	Natural Gas
[]	Rules 62-4.070(3), 62	-210.200(PTE), 62-296.406, 62-213.440(	1), F.A.C., and Permit No. 11	30004-020-AC]

- **S.2.** <u>Methods of Operation (fuel)</u>. The fuel that is allowed to be burned in this unit is natural gas. The heat input rate for this unit will be calculated on a semi-annual basis as the sum of the previous 12 months total measured flow of natural gas to the heater and the average higher heating value of the natural gas. [Rules 62-4.070(3), F.A.C., and Permit No. 1130004-020-AC]
- **S.3.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year. [Rule 62-210.200(PTE), F.A.C.]

## **Emission Limitations and Compliance Requirements**

**S.4.** <u>Tune-Up</u>. Permittee shall conduct an annual tune-up of the boiler. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7540(a)(10); and Table 3 (Item 3) to Subpart DDDDD of Part 63]

*{Permitting Note: The one-time energy assessment for this emissions unit was completed in January 2016.}* <u>Monitoring of Operations</u>

- S.5. <u>Tune-Up Procedures</u>. The Permittee shall conduct an annual tune-up of the boiler or process heater to demonstrate continuous compliance as specified in paragraphs (a)(10)(i) through (vi) of 40 CFR 63.7540. You must conduct the tune-up while burning the type of fuel (or fuels in case of units that routinely burn a mixture) that provided the majority of the heat input to the boiler or process heater over the 12 months prior to the tune-up. This frequency does not apply to limited-use boilers and process heaters, as defined in 40 CFR 63.7575, or units with continuous oxygen trim systems that maintain an optimum air to fuel ratio.
  - a. As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;
  - b. Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;
  - c. Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units

## Subsection S. Emission Unit 060

that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;

- d. Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any NOx requirement to which the unit is subject;
- e. Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and
- f. Maintain on-site and submit, if requested by the Administrator, a report containing the following information:
  - (1) The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
  - (2) A description of any corrective actions taken as a part of the tune-up; and
  - (3) The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7540(a)(10)(vi)]

## **Recordkeeping and Reporting Requirements**

**S.6.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	<b>Related Condition(s)</b>
Tune-Up Reports	if requested by Administrator	S.5.f.

[Rule 62-213.440(1)(b), F.A.C.]

- **S.7.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- S.8. <u>Tune-Up Records and Reports</u>. Permittee shall maintain records of information specified in the Specific Condition S.5.f. Tune-Up Procedures. Such records shall be kept in accordance with 40 CFR 63.7560 as follows:
  - a. Your records must be in a form suitable and readily available for expeditious review, according to 40 CFR 63.10(b)(1).
  - b. As specified in 40 CFR 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.
  - c. The Permittee must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to 40 CFR 63.10(b)(1). You can keep the records off site for the remaining 3 years.

[Rule 62-204.800(11), F.A.C.; and 40 CFR 63.7560]

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## Subsection T. Emission Unit 033

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description	
033	Methylamines Plant No. 4 Process Vents	

Emissions from several process vents at MA Plant No. 4 are collected using a vapor collection system and routed to the amines plants flare or boilers during normal operation. These process vents are used intermittently, and include, but are not limited to, the Low-Pressure Absorber vent and the High-Pressure Absorber vent. (The absorber is used for product recovery and is not considered a pollution control device.)

{Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.). As stated in 40 CFR 63 Subpart G "After the compliance dates specified in 40 CFR 63 Subpart F, a Group 1 process vent that is also subject to the provisions of 40 CFR 60 Subpart NNN is required to comply only with the provisions of 40 CFR 63 Subpart F, a Group 1 process vent that is also subject to the provisions of 10 CFR 63.110(d)(4)]; and "After the compliance dates specified in 40 CFR 63.100 of 40 CFR 63 Subpart F, a Group 1 process vent that is also subject to the provisions of 40 CFR 60 CFR 63 Subpart G." [40 CFR 63.110(d)(4)]; CFR 63 Subpart G." [40 CFR 63.110(d)(7).]}

## **Essential Potential to Emit (PTE) Parameters**

T.1. <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.

[Rule 62-210.200(PTE), F.A.C.]

## **Equipment Limitations and Standards**

- **T.2.** <u>Organic HAP Control Device</u>. Permittee shall reduce emissions of organic hazardous air pollutants (i.e., chemicals listed in Table 2 of 40 CFR 60 Subpart F) using a vapor collection system and flare meeting the criteria of 40 CFR 63.11(b). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.11(b) and 40 CFR 63.113(a)(1)]
- **T.3.** <u>Flare Requirements</u>. Organic hazardous air pollutant emissions from MA Plant No. 4 Process Vents shall be vented to the Amines Plants Flare (EU 005) which shall meet the general control device requirements of 40 CFR 63.11(b). Specific permit conditions applicable to the Amines Plants Flare are specified in this permit under Emissions Unit 005, <u>Subsection G</u>. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.11(b) and 40 CFR 63.113(a)(1)]
- **T.4.** <u>Other Limitations and Standards</u>. This emissions unit is subject to the emission limitations and standards contained in Section IV, Common Conditions:

C.C.2. Startup, Shutdown, and Malfunction Plan

C.C.4. Excess Emissions and Data Obtained During Startups, Shutdowns, and Malfunctions

#### **Test Methods and Procedures**

**T.5.** <u>Other Methods and Procedures</u>. This emissions unit is subject to the test methods and procedures contained in Section IV, Common Condition. **C.C.9.** Closed Vent System Inspections.

#### **Recordkeeping and Reporting Requirements**

**T.6.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Other Recordkeeping and Reporting Requirements	As required by Administrator	Т.8.

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[Rule 62-213.440(1)(b), F.A.C.]

- **T.7.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **T.8.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:
  - C.C.2. Startup, Shutdown, and Malfunction Plan
  - C.C.3. Recordkeeping and Reporting of Startups, Shutdowns, and Malfunctions
  - C.C.5. General Recordkeeping Requirements
  - C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G
  - C.C.8. Schedule of Reporting for Specific Sources Subject to 40 CFR 63 Subparts F, G and H

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## Subsection U. Emission Unit 034

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
034	Methylamines Plant No. 4 Wastewater

The MA Plant No. 4 wastewater is the stream from the MA Plant No. 4 distillation process. The stream, consisting of water and negligible quantities of product, is directed to the plant sewer system, which goes to the Wastewater Treatment Plant. Wastewater streams covered under HON includes the No. 4 Dehydration Column bottoms.

EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.).}

## **Essential Potential to Emit (PTE) Parameters**

U.1. <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year. [Rule 62-210.200(PTE), F.A.C.]

## **Equipment Limitations and Standards**

**U.2.** <u>Group 1 or Group 2 Determination</u>. Permittee shall comply with the requirements in 40 CFR 63.132(a)(1) through (a)(3), which requires that Permittee determine whether a wastewater emission source is a Group 1 or Group 2 stream. For Group 2 streams, Permittee shall comply with the recordkeeping requirements of 40 CFR 63.146. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.132(a)]

#### **Recordkeeping and Reporting Requirements**

**U.3.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Other Recordkeeping and Reporting Requirements	As required by Administrator	U.6.

[Rule 62-213.440(1)(b), F.A.C.]

- **U.4.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **U.5.** <u>Recordkeeping</u>. If Permittee uses process knowledge to determine the annual average concentration of a wastewater stream and/or the annual average flow rate used to determine that a wastewater stream is not a Group 1 stream, Permittee shall keep in a readily accessible location the documentation of how process knowledge was used. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.147]
- **U.6.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:

C.C.5. General Recordkeeping Requirements

C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G

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## Subsection V. Emission Unit 035

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description	
035	Methylamines Plant No. 4 HON Maintenance Wastewater	

Wastewater removed during maintenance activities at the MA Plant No. 4 is disposed of in the plant sewer system, which goes to the Wastewater Treatment Plant.

EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.).}`

## **Essential Potential to Emit (PTE) Parameters**

1. <u>Hours of Operation</u>. This emissions unit is allowed to operate on an as-needed basis. [Rule 62-210.200(PTE), F.A.C.]

## **Operational Limitations and Standards**

- 2. <u>Maintenance Procedures</u>. Permittee shall maintain, modify and update as needed a description of maintenance procedures for management of wastewaters containing those organic HAPs listed in Table 9 of 40 CFR 63 Subpart G which are generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdown (i.e., routine maintenance). The descriptions shall:
  - a. Specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities,
  - b. Specify procedures that will be followed to properly manage the wastewater and control organic HAP emissions to the atmosphere, and
  - c. Specify the procedures to be followed when clearing materials from process equipment.

[Rules 62-204.800(11), F.A.C.; 40 CFR 63.105(b) & (c), and 40 CFR 63 Subpart G - Table 9]

## **Recordkeeping and Reporting Requirements**

- 3. <u>Startup, Shutdown, Malfunction Plan</u>. Permittee shall maintain a record of the required information as part of the startup, shutdown, and malfunction plan required under 40 CFR 63.6(e)(3). Plans shall be maintained and kept readily available for inspection for the life of the source, or until 40 CFR 63 standards no longer apply to the source. Previous versions of Plans shall also be maintained for a period of five years following revision. No notification or periodic reporting of maintenance wastewater activities is required. [Rules 62-204.800(11), F.A.C., and 40 CFR 63.105(d)]
- 4. <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Conditions:

C.C.5. General Recordkeeping Requirements

C.C.6. General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G

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## Subsection W. Emission Unit 036

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
036	Methylamines Plant Nos. 1 and 4 HON Equipment Leaks

HON Equipment Leaks (Methanol Storage leaks) from MA Plant No. 1 and MA Plant No. 4 are comprised of fugitive emissions from the pump seals, pressure relief valves, open-ended valves or lines, valves, connectors, and sampling points in organic hazardous air pollutant service.

EUs for equipment leaks are for regulatory purposes only and emissions are reported under EU 062, Facility-wide Equipment Leak Fugitives.

{*Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart H - National Emissions Standards for Organic Hazardous Air Pollutants for Equipment Leaks (adopted and incorporated by reference in Rule 62-204.800(11)(b)3., F.A.C.).*}

## **Essential Potential to Emit (PTE) Parameters**

W.1. <u>Hours of Operation</u>. This emissions unit is allowed to operate on an as-needed basis. [Rule 62-210.200(PTE), F.A.C.]

## **Equipment Limitations and Standards**

- W.2. <u>Pumps</u>. Permittee shall meet the criteria set forth in 40 CFR 63.163 for pumps in light liquid service that have been designated by Permittee to be in organic hazardous air pollutant light liquid service for 300 or more hours per year. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.163]
- W.3. <u>Pressure Relief Devices</u>. Permittee shall comply with the requirements set forth in 40 CFR 63.165 for pressure relief devices in gas/vapor service that have been designated by Permittee to be in organic hazardous air pollutant gas/vapor service for 300 or more hours per year. Pressure relief devices that are routed to a process or fuel gas system are exempt. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.165]
- W.4. <u>Open-ended Valves or Lines</u>. Permittee shall comply with requirements set forth in 40 CFR 63.167 for open-ended lines that have been designated by Permittee to be in organic hazardous air pollutant service for 300 or more hours per year. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.167]
- W.5. <u>Valves</u>. Permittee shall comply with Phase III leak detection and repair criteria set forth in 40 CFR 63.168 for valves in light liquid and gas service that have been designated by Permittee to be in organic hazardous air pollutant light liquid/gas service for 300 or more hours per year. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.168]
- **W.6.** <u>Connectors</u>. Permittee shall comply with Phase III leak detection and repair criteria set forth in 40 CFR 63.174 for connectors in light liquid and gas service that have been designated by Permittee to be in organic hazardous air pollutant light liquid/gas service for 300 or more hours per year. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.174]
- W.7. <u>Sampling Points</u>. Permittee shall meet the criteria set forth in 40 CFR 63.166 for sampling points in organic hazardous service that have been designated by Permittee to be in organic hazardous air pollutant service for 300 or more hours per year. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.166]

#### **Compliance Methods and Procedures**

- W.8. <u>Pumps</u>. In order to comply with the requirements of 40 CFR 63.163, Permittee shall either comply with the Phase III leak detection and repair requirements specified in 40 CFR 63.163 or comply by using methods specified in 40 CFR 63.163(e), (f), or (g). [Rule 62-204.800(11), F.A.C., 40 CFR 63.163]
- **W.9.** <u>Pressure Relief Devices</u>. After pressure releases from pressure relief valves that are not equipped with upstream rupture disks, the pressure relief device shall be returned to less than 500 ppmv above background,

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as confirmed by the method specified in 40 CFR 63.180(c), as soon as practicable, but no later than five days after the release. Any pressure relief device with an upstream rupture disk is exempt from monitoring, provided that in the event that a release ruptures the disk, the disk is replaced as soon as practicable, but no later than five days after the release. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.165, and 40 CFR 63.180]

- W.10. <u>Open-ended Valves or Lines</u>. Each open-ended valve or line shall be equipped with a cap, blind flange, plug, or a second valve, except for open-ended valves specified in 40 CFR 63.167(d) & (e), which are exempt. Permittee shall also comply with work and operating practices specified in 40 CFR 63.167(a)(2), (b), and (c). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.167]
- W.11. <u>Valves</u>. Permittee shall inspect and repair valves according to the criteria specified in 40 CFR 63.168. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.168 and 40 CFR 63.180]
- W.12. <u>Connectors</u>. Permittee shall inspect and repair connectors according to the criteria specified in 40 CFR 63.174. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.174]
- **W.13.** <u>Sampling Points</u>. Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent system. Gases displaced during filling of the sample container are not required to be collected or captured. Each sampling system shall meet one of the specifications specified in 40 CFR 63.166(b). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.166]

## **Recordkeeping and Reporting Requirements**

**W.14.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Periodic Reports	submitted with Semiannual Progress Reports	W.16., W.17., W.18., W.19., W.20.
Other Reporting Requirements	As required by Administrator	W.22.

[Rule 62-213.440(1)(b), F.A.C.]

- W.15. <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- W.16. <u>Pumps</u>. If Permittee elects to demonstrate compliance with the requirements of 40 CFR 63.163 by implementing a leak detection and repair program, records shall be maintained in accordance with 40 CFR 63.181 (b)(1)(i), (b)(7), (c), (d), and if a quality improvement plan is implemented, records required under paragraph (h) shall also be maintained. If the Permittee elects to demonstrate compliance using methods specified in 40 CFR 63.163(e), (f), or (g), other relevant records specified in 40 CFR 63.163 shall be maintained. Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.181 and 63.182]
- W.17. <u>Pressure relief devices</u>. Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i), (b)(3), and (f). Periodic reports meeting the specifications of 40 CFR 63.182(d)(xiv) shall be submitted to the Department. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.181 and 63.182]
- W.18. <u>Open-ended valves or lines</u>. Permittee shall maintain records specified in 40 CFR 63.181 (b)(1)(i) and no periodic reporting shall be required under 40 CFR 63.182. Notwithstanding, Title V semi-annual progress reports shall be submitted that identify any instances of non-compliance and annual Title V compliance certification reports must certify whether or not compliance with applicable requirements has been achieved. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.181 and 63.182]

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- W.19. <u>Valves</u>. Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i) & (ii), (b)(7), (d), and if a quality improvement plan is implemented, records required under paragraph (i) shall also be required. Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.181 and 63.182]
- W.20. <u>Connectors</u>. Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i) & (ii), (b)(5), (b)(7), and (d). Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.181 and 63.182]
- W.21. <u>Sampling Points</u>. Permittee shall maintain records specified in 40 CFR 63.181(b)(1)(i) and no periodic reporting shall be required. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.181]

## Additional Recordkeeping and Reporting Requirements

**W.22.** <u>Other Recordkeeping and Reporting Requirements</u>. This emissions unit is subject to the recordkeeping and reporting requirements contained in Section IV, Common Condition:</u>

C.C.8. Schedule of Reporting for Specific Sources Subject to 40 CFR 63 Subparts F, G and H.

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## Subsection X. Emission Unit 037

#### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
037	Methylamines Plant No. 4 VOC Equipment Leaks

MA Plant No. 4 VOC Equipment Leaks is comprised of fugitive emissions from the pressure relief valves, openended valves or lines, valves, connectors, and sampling points in VOC service. Components are considered in VOC service when the piece of equipment contains or contacts a process fluid that is at least 10 percent VOC by weight.

EUs for equipment leaks are for regulatory purposes only and emissions are reported under EU 062, Facility-wide Equipment Leak Fugitives.

{Permitting Note: This emissions unit is subject to 40 CFR 60 Subpart VVa - Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006 (adopted and incorporated by reference in Rule 62-204.800(8)(b)55., F.A.C.). As an alternative means of compliance in accordance with 40 CFR 60.480a(e)(2), Taminco chooses to comply with 40 CFR Part 63 Subpart H - National Emissions Standards for Organic Hazardous Air Pollutants for Equipment Leaks (adopted and incorporated by reference in Rule 62-204.800(11)(b)3., F.A.C.). When choosing to comply with 40 CFR part 63 Subpart H, the requirements of 40 CFR 60.485a(d), (e), and (f), and 40 CFR 60.486a(i) & (j) still apply.}

#### Essential Potential to Emit (PTE) Parameters

**X.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate on an as-needed basis. [Rule 62-210.200(PTE), F.A.C.]

## **Equipment Limitations and Standards**

- **X.2.** <u>Pumps</u>. This emissions unit is equipped with seal less pumps and is therefore exempt from the requirements of 40 CFR 63.163. [Rules 62-204.800(11), F.A.C., and 40 CFR 63.162(d)]
- X.3. <u>Pressure relief devices</u>. Permittee shall comply with the requirements set forth in 40 CFR 63.165 for pressure relief devices in gas/vapor service. Permittee shall comply with the requirements set forth in 40 CFR 63.169 for pressure relief devices in light liquid service. Pressure relief devices that are routed to a process or fuel gas system are exempt. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.165 and 63.169]
- **X.4.** <u>Open-ended valves or lines</u>. Permittee shall comply with requirements set forth in 40 CFR 63.167 for open-ended lines that have been designated by Permittee to be in organic hazardous air pollutant service for 300 or more hours per year. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.167]
- **X.5.** <u>Valves</u>. Permittee shall comply with the requirements set forth in 40 CFR 63.168 for valves in light liquid or gas/vapor service. [62-204.800(11), F.A.C., and 40 CFR 63.168]
- **X.6.** <u>Flanges and Connectors</u>. Permittee shall comply with the requirements set forth in 40 CFR 63.174 for flanges and connectors. [62-204.800(11), F.A.C., and 40 CFR 63.174]
- X.7. <u>Sampling Points</u>. Permittee shall meet the criteria set forth in 40 CFR 63.166 for sampling points. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.166]

#### **Test Methods and Procedures**

- **X.8.** <u>Test Methods</u>. Permittee shall determine compliance with the standards using the methods specified in 40 CFR 63.180, except permittee shall also comply with 40 CFR 60.485a(d). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.180]
- **X.9.** <u>Pumps</u>. This emissions unit is equipped with seal less pumps and is therefore exempt from the requirements of 40 CFR 63.163. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.162(d)]

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- X.10. Pressure relief devices. After pressure releases from pressure relief valves, the pressure relief device shall be returned to less than 500 ppmv above background, as confirmed by the method specified in 40 CFR 63.180(c), as soon as practicable, but no later than five days after the release. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.165 and 63.180(c)]
- **X.11.** <u>Open-ended valves or lines</u>. Each open-ended valve or line shall be equipped with a cap, blind flange, plug, or a second valve. Permittee shall also comply with work and operating practices specified in 40 CFR 63.167(a)(2), (b) & (c). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.167(a)(2), (b) & (c)]
- **X.12.** <u>Valves</u>. Permittee shall inspect and repair valves in light liquid or gas/vapor service according to the criteria specified in 40 CFR 63.168. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.168]
- **X.13.** <u>Connectors</u>. Permittee shall inspect and repair connectors according to the criteria specified in 40 CFR 63.174. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.174]
- X.14. <u>Sampling Points</u>. Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent system. Each sampling system shall meet one of the specifications specified in 40 CFR 63.166(b). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.166(b)]

## **Recordkeeping and Reporting Requirements**

**X.15.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Periodic Reports	submitted with Semiannual Progress Reports	X.18., X.19., X.20.
Other Reporting Requirements	As required by Administrator	X.25.

[Rule 62-213.440(1)(b), F.A.C.]

- **X.16.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **X.17.** <u>Pumps</u>. This emissions unit is equipped with seal less pumps and is therefore exempt from the requirements of 40 CFR 63.163. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.163]
- **X.18.** <u>Pressure Relief Devices</u>. Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i), 63.181(b)(3), and 63.181(d). Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.181(b)(1)(i), 63.181(b)(3), and 63.181(d)]
- X.19. <u>Valves</u>. Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i and ii), and 63.181(d). Records shall also be maintained in accordance with 40 CFR 63.181(7 and 8) for every valve subject to the requirements of 40 CFR 63.168(g and h). Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.168, 63.181, and 63.182(d)]
- **X.20.** <u>Connectors</u>. Records shall be maintained in accordance with 40 CFR 60.486a(b)(1) & (c). Periodic reports containing relevant information specified in 40 CFR 60.487a(c) shall be submitted to the Department. [Rule 62-204.800(8) F.A.C., and 40 CFR 60.486a]
- **X.21.** <u>Recordkeeping Requirements for All Equipment in VOC Service</u>. Records shall be maintained for all equipment subject to 40 CFR 60.482-1a to 482-10a in accordance with the requirements of 40 CFR 63.181(b) & (d), as applicable. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.181]
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- **X.22.** <u>Components Not in VOC Service</u>. Permittee shall maintain records specified in 40 CFR 60.486a(j) for any equipment considered not in VOC service. [62-204.800(8), F.A.C., and 40 CFR 60.486a]
- **X.23.** <u>Semiannual Reporting</u>. Permittee shall submit reports on a semi-annual basis to the Department in accordance with the requirements of 40 CFR 63.182. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.182]
- **X.24.** <u>Performance Test Reporting</u>. Permittee shall report the results of all performance tests in accordance with 40 CFR 63.182(c). [Rule 62-204.800(11), F.A.C., and 40 CFR 63.182(c)]

# Additional Recordkeeping and Reporting Requirements

- **X.25.** <u>Other Recordkeeping and Reporting Requirements</u>. In addition to the recordkeeping and reporting requirements contained above, the permittee shall comply with the requirements of 40 CFR 60.485a(d), (e) & (f) and 60.486a(i) & (j) as follows:
  - a. Permittee shall test each piece of equipment unless it is demonstrated that a process unit is not in VOC service, i.e., that the VOC content would never be reasonably expected to exceed 10 percent by weight. For purposes of this demonstration, the following methods and procedures shall be used:
    - (1) Procedures that conform to the general methods in ASTM E260–73, 91, or 96, E168–67, 77, or 92, E169–63, 77, or 93 (incorporated by reference—see 40 CFR 60.17) shall be used to determine the percent VOC content in the process fluid that is contained in or contacts a piece of equipment.
    - (2) Organic compounds that are considered by the Administrator to have negligible photochemical reactivity may be excluded from the total quantity of organic compounds in determining the VOC content of the process fluid.
    - (3) Engineering judgment may be used to estimate the VOC content, if a piece of equipment had not been shown previously to be in service. If the Administrator disagrees with the judgment, paragraphs
       (d)(1) & (2) of 40 CFR 60.486a shall be used to resolve the disagreement.

[Rule 62-204.800(8), F.A.C.; 40 CFR 60.485a(d)(1), (2), and (3)]

- b. Permittee shall demonstrate that a piece of equipment is in light liquid service by showing that all the following conditions apply:
  - The vapor pressure of one or more of the organic components is greater than 0.3 kPa at 20°C (1.2 in. H2O at 68°F). Standard reference texts or ASTM D2879–83, 96, or 97 (incorporated by reference—see 40 CFR 60.17) shall be used to determine the vapor pressures.
  - (2) The total concentration of the pure organic components having a vapor pressure greater than 0.3 kPa at 20°C (1.2 in. H2O at 68°F) is equal to or greater than 20 percent by weight.
  - (3) The fluid is a liquid at operating conditions.

[Rule 62-204.800(8), F.A.C.; 40 CFR 60.485a(e)(1), (2), and (3)]

- c. Samples used in conjunction with **Specific Conditions X.25a and X.25b Other Recordkeeping and Reporting Requirements** above (paragraphs (d) & (e) of 40 CFR 60.485a) shall be representative of the process fluid that is contained in or contacts the equipment or the gas being combusted in the flare. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.485a(f)]
- d. The following information shall be recorded in a log that is kept in a readily accessible location for use in determining exemptions as provided in 40 CFR 60.480a(d):
  - (1) An analysis demonstrating the design capacity of the affected facility,
  - (2) A statement listing the feed or raw materials and products from the affected facilities and an analysis demonstrating whether these chemicals are heavy liquids or beverage alcohol, and

### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection X. Emission Unit 037

(3) An analysis demonstrating that equipment is not in VOC service.

[Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(i) (1), (2), and (3)]

e. Information and data used to demonstrate that a piece of equipment is not in VOC service shall be recorded in a log that is kept in a readily accessible location available for Department inspection.

[Rules 62-4.070 and 62-204.800(8), F.A.C.; and 40 CFR 60.486a(j)]

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# Subsection Y. Emission Unit 070

### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
070	Higher Amines Plant Process Vents

At the Higher Amines Plant, alcohols, ammonia, ethers, aldehydes, ketones, and other amines are reacted to yield various diamylamines and amylamines. A natural gas-fired preheater is used to bring the mixture to reaction temperature. Process vents include Plant No. 2 Low Pressure Absorber Vent and Plant No. 2 High Pressure Absorber Vent. The ammonia column is sent to a high-pressure absorber. All other columns are sent to a low-pressure absorber. Vents from the high-pressure absorber and the low-pressure absorber are routed to the Amines Plants Flare (EU 005) or boilers (EU 001 and EU 003) for control. The process vents operate intermittently (open during startup, shutdown, and malfunction only). The 42" Column Jet Condensate vents to the atmosphere following a water scrub with 99% removal efficiency.

{Permitting Note: The Higher Amines Plant does not process, use, or generate any organic HAPs listed in section 112(b) of the Clean Air Act or hydrogen halide and halogen HAP; therefore, this plant is not subject to 40 CFR 63 Subpart FFFF. This plant does not manufacture as a primary product the chemicals listed in 40 CFR 63.100(b)(1)(i) or (ii); therefore, this plant is not subject to 40 CFR 63 Subpart G.}

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# Subsection Z. Emission Unit 071

### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
071	DIMLA MON Maintenance Wastewater

Maintenance wastewater from this emission unit is sent to the plant sewer system, which goes to the Wastewater Treatment Plant. The Operation and Maintenance Plan includes procedures for minimizing emissions to the air while clearing equipment for maintenance work. EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{*Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart FFFF - National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing (adopted and incorporated by reference in Rule 62-204.800(11)(b)63., F.A.C.).*}

# **Essential Potential to Emit (PTE) Parameters**

**Z.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year. [Rule 62-210.200(PTE), F.A.C.]

# **Equipment Limitations and Standards**

- **Z.2.** <u>Maintenance Procedures</u>. For each maintenance wastewater stream containing organic HAP listed in Table 8 or Table 9 of 40 CFR Part 63 Subpart FFFF, the Permittee shall prepare a description of maintenance procedures for management of wastewaters generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdowns (i.e., routine maintenance). The descriptions shall:
  - a. Specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities.
  - b. Specify the procedures to be followed to properly manage the wastewater and control organic HAP emissions to the atmosphere; and
  - c. Specify the procedures to be followed when clearing materials from process equipment. [Rule 62-204.800(11), F.A.C; 40 CFR 63.105(b) referenced by 40 CFR 63.2485(a) & (b); and Permit No. 1130004-019-AC]

# **Test Methods and Procedures**

Z.3. <u>Maintenance Wastewater Procedures</u>. Permittee shall modify and update the information required by Specific Condition Z.2. Maintenance Procedures of this subsection as needed following each maintenance procedure based on the actions taken and the wastewater generated. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.105(c) referenced by 40 CFR 63.2485(a) & (b); and Permit No. 1130004-019-AC]

### **Recordkeeping and Reporting Requirements**

- Z.4. <u>Startup, Shutdown and Malfunction Plan</u>. For historical compliance purposes, a copy of the plan must be retained and available on-site for five years after August 12, 2023. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.105(d) referenced by 40 CFR 63.2485(a) & (b); 40 CFR 63.2520€(4); and Permit No. 1130004-019-AC]
- Z.5. Other Recordkeeping and Reporting Requirements. In the event that an affected unit does not meet an applicable standard, record the number of deviations. For each deviation record the date, time, and duration of each deviation. For each deviation from an applicable standard, record and retain a list of the affected sources or equipment, an estimate of the quantity of each regulated pollutant emitted over any emission limit and a description of the method used to estimate the emissions. Record actions taken to minimize emissions in accordance with 40 CFR 63.2450(u) and any corrective actions taken to return the affected unit to its normal or usual manner of operation. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.105€ referenced by 40 CFR 63.2485; 40 CFR 63.2525(l)] Back to Table of Contents

# Subsection AA. Emission Unit 071

### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
072	DIMLA MON Wastewater

This emission unit is a Group 2 wastewater stream subject to MON. EUs for individual plant wastewater are for regulatory purposes only. Emissions from all wastewater have been included under EU 075, Wastewater Treatment Plant Fugitives.

{Permitting Notes: This emissions unit is regulated by 40 CFR 63 Subpart FFFF - National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing (adopted and incorporated by reference in Rule 62-204.800(11)(b)63., F.A.C.) and 40 CFR 63 Subpart G – National Emissions Standards for Organic Hazardous Air Pollutants from the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater (adopted and incorporated by reference in Rule 62-204.800(11)(b)2., F.A.C.).

<u>Group 2 wastewater stream</u> means any process wastewater stream that does not meet the definition of a Group 1 wastewater stream.

<u>Group 1 wastewater stream</u> means a wastewater stream consisting of process wastewater at an existing or new source that meets the criteria for Group 1 status in 40 CFR 63.2485(c) for compounds in Tables 8 and 9 to 40 CFR 63 Subpart FFFF and/or a wastewater stream consisting of process wastewater at a new source that meets the criteria for Group 1 status in 40 CFR 63.132(d) for compounds in Table 8 to 40 CFR 63 subpart G.}

### **Essential Potential to Emit (PTE) Parameters**

AA.1. <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year. [Rule 62-210.200(PTE), F.A.C.]

# Equipment Limitations and Standards

- **AA.2.** <u>Group Status Determination</u>. The Permittee shall comply with the requirements in 63.132 through 63.148 and the requirements referenced therein, except as specified in 63.2485. The compounds in table 8 and 9 to 40 CFR 63 Subpart FFFF apply. Permittee shall comply with the requirements in 40 CFR 63.132(a)(1) through (a)(3), except as specified in 63.2485(c), which requires that Permittee determine whether each wastewater stream is Group 1 or Group 2 stream. For Group 2 streams, Permittee shall comply with recordkeeping requirements of 40 CFR 63.147(b)(8)(i) through (iv).
  - a. A wastewater stream is a Group 1 wastewater stream for compounds in Tables 8 and 9 to 40 CFR 63 Subpart FFFF if:
    - (1) The total annual average concentration of compounds in Table 8 is greater than or equal to 10,000 parts per million by weight at any flow rate, and the total annual load of compounds in Table 8 to 40 CFR 63 Subpart FFFF is greater than or equal to 200 lb/yr; or
    - (2) The total annual average concentration of compounds in Table 8 is greater than or equal to 1,000 parts per million by weight and the annual average flow rate is greater than or equal to 1 liter per minute.
    - (3) The combined total annual average concentration of compounds in Tables 8 and 9 is greater than or equal to 30,000 part per million by weight, and the combined total annual load of compounds in Tables 8 and 9 to 40 CFR 63 Subpart FFFF is greater than or equal to 1 ton per year.
  - b. A wastewater stream is a Group 2 wastewater stream if the process wastewater stream does not meet the definition of a Group 1 wastewater stream.
  - c. Re-determine group status for each Group 2 stream, as necessary, to determine whether the stream is Group 1 or Group 2 whenever process changes are made that could reasonably be expected to change the stream to a Group 1 stream.

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[Rule 62-204.800(11), F.A.C., 40 CFR 63.2485]

{Permitting Note: Examples of process changes include, but are not limited to, changes in production capacity, production rate, feedstock type, or catalyst type, or whenever there is replacement, removal, or addition of recovery equipment. Process changes do not include: process upsets; unintentional, temporary process changes; and changes that are within the range on which the original TRE calculation was based.}

### **Recordkeeping and Reporting Requirements**

AA.3. <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	<b>Related Condition(s)</b>
Periodic/Semiannual Compliance Reports	Semi-Annual	AA.7.
Other Reporting Requirements	As required by Administrator	AA.8.
Notifications	As required by Administrator	AA.5.

[Rule 62-213.440(1)(b), F.A.C.]

- AA.4. <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- AA.5. Notification of Compliance Status Reporting. Permittee shall submit the information specified in 40 CFR 63.146(b)(1) through (b)(9) as part of the Notification of Compliance Status required by 40 CFR 63.152(b). [Rules 62-204.800(11), F.A.C.; 40 CFR 63.146(b), 40 CFR 63.152(b), 40 CFR 63.2520(d), 40 CFR 63.1039(b) referenced by 40 CFR 63.2520(d), and 40 CFR 63.2485]
- **AA.6.** Notification of Compliance Status Recordkeeping. Permittee shall maintain records of all Group 1/Group 2 determinations, and the Notification of Compliance Status available for Department inspection. If Permittee uses process knowledge to determine the annual average concentration of a wastewater stream as specified in 40 CFR 63.144(b)(3) and/or uses process knowledge to determine the annual average flow rate as specified in 40 CFR 63.144(c)(1), and determines that the wastewater stream is not a Group 1 wastewater stream, Permittee shall keep in a readily accessible location the documentation of how process knowledge was used to determine the annual average concentration and/or the annual average flow rate of the wastewater stream. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.152(f) and 40 CFR 63.2485]
- AA.7. <u>Periodic/Semiannual Compliance Reports</u>. Periodic compliance reports required by 40 CFR 63.2520(d) shall be submitted semiannually according to the schedule specified in 40 CFR 63.2520(b) as follows:
  - a. Each subsequent compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31.
  - b. Each subsequent compliance report must be postmarked or delivered no later than August 31 or February 28, whichever date is the first date following the end of the semiannual reporting period.
    [Rule 62-204.800(11), F.A.C.; 40 CFR 63.2520(b) & (e)]
- **AA.8.** <u>Other Recordkeeping and Reporting Requirements</u>. In the event that an affected unit does not meet an applicable standard, record the number of deviations. For each deviation record the date, time, and duration of each deviation. For each deviation from an applicable standard, record and retain a list of the affected sources or equipment, an estimate of the quantity of each regulated pollutant emitted over any emission limit and a description of the method used to estimate the emissions. Record actions taken to minimize emissions in accordance with 40 CFR 63.2450(u) and any corrective actions taken to return the affected unit to its normal or usual manner of operation. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.105(e) referenced by 40 CFR 63.2485; 40 CFR 63.2525(l)]
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### Subsection BB. Emission Unit 077

### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
077	DIMLA MON Equipment Leaks

This emissions unit consists of fugitive emissions from fugitive equipment leaks from pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors and instrumentation systems associated with the DIMLA process in organic HAP service greater than 300 hours per year; and any control devices or systems used to comply with control standards under 40 CFR 63.2480 and located within the unit boundaries of the DIMLA process.

EUs for equipment leaks are for regulatory purposes only and emissions are reported under EU 062, Facility-wide Equipment Leak Fugitives.

{*Permitting Note: This emissions unit is regulated by 40 CFR 63, Subpart FFFF - National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing (adopted and incorporated by reference in Rule 62-204.800(11)(b)63., F.A.C.).*}

# **Essential Potential to Emit (PTE) Parameters**

**BB.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

# **Equipment Limitations and Standards**

- **BB.2.** Equipment Identification. Equipment contained within this emissions unit shall be identified as specified in 40 CFR 63.1022, Equipment Identification Standards, referenced by 40 CFR 63.2480. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.1022 referenced by 40 CFR 63.2480]
- **BB.3.** <u>Standards for Equipment Leak Detection</u>. The permittee shall comply with the following equipment leak standards as applicable:
  - a. Standards for Valves in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1025 referenced by 40 CFR 63.2480]
  - b. Standards for Pumps in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1026 and 63.1035 referenced by 40 CFR 63.2480]
  - c. Standards for Connectors in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1027 referenced by 40 CFR 63.2480]
  - d. Standards for Agitators in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1028 referenced by 40 CFR 63.2480]
  - e. Standards for Pumps, Valves, Connectors, and Agitators in heavy liquid service; pressure relief devices in liquid service; and instrumentation systems. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1029 and 63.1035 referenced by 40 CFR 63.2480]
  - f. Standards for Pressure relief devices in gas and vapor service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1030 referenced by 40 CFR 63.2480]
  - g. Standard for Compressors standards. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1031 referenced by 40 CFR 63.2480]
  - h. Standards for Sampling connection systems. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1032 referenced by 40 CFR 63.2480]
  - i. Open-ended valves or lines standards. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1033 referenced by 40 CFR 63.2480]

# Subsection BB. Emission Unit 077

- j. Closed vent systems and control devices; or emissions routed to a fuel gas system or process standards. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1034 referenced by 40 CFR 63.2480]
- **BB.4.** <u>Leak Repair</u>. When a leak is detected, the leaking component shall be identified and repaired as soon as possible, but not later than allowed under the standard. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1024 referenced by 40 CFR 63.2480]

# **Compliance Methods and Procedures**

**BB.5.** <u>Compliance Tests</u>. Compliance tests shall be conducted using instruments or sensory methods as specified in the standards for instrument and sensory monitoring for leaks specified in 40 CFR 63.1023. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1023 referenced by 40 CFR 63.2480]

**BB.6.** <u>Test Methods</u>. Required tests shall be performed in accordance with the following reference methods.

Method	Description of Method and Comments
21	Determination of Volatile Organic Compound Leaks
Sensory	Determination of Volatile Organic Compound Leaks

Monitoring shall comply with Method 21 of 40 CFR part 60, Appendix A, as specified by, and, except as otherwise provided in 40 CFR 63.1023. The above methods are described in 40 CFR 60, Appendix A, and adopted by reference in Rule 62-204.800, F.A.C. No other methods may be used unless prior written approval is received from the Department. [Rule 62-204.800, F.A.C.]

### **Monitoring of Operations**

- **BB.7.** Equipment to be Monitored. The permittee shall monitor the equipment comprising this emissions unit routinely as follows:
  - a. Valves in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1025(b) and (c) referenced by 40 CFR 63.2480]
  - b. Pumps in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1026(b)-(e) referenced by 40 CFR 63.2480]
  - c. Connectors in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1027(b) and (c) referenced by 40 CFR 63.2480]
  - d. Agitators in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1028(c) referenced by 40 CFR 63.2480]
  - e. Pumps, valves, connectors, and agitators in heavy liquid service; pressure relief devices in liquid service; and instrumentation systems. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1029(b) and (c) referenced by 40 CFR 63.2480]
  - f. Pressure relief devices in gas and vapor service standards. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1030(b) referenced by 40 CFR 63.2480]
  - g. Compressors. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1031(f) referenced by 40 CFR 63.2480]

# **Recordkeeping and Reporting Requirements**

**BB.8.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	<b>Reporting Deadline</b>	<b>Related Condition(s)</b>
Periodic/Semiannual Compliance Reports	Semi-Annual	<b>BB.10. and BB.11.</b>

[Rule 62-213.440(1)(b), F.A.C.]

### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection BB. Emission Unit 077

- **BB.9.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **BB.10.** <u>Reporting Requirements</u>. For the equipment specified in **Specific Condition BB.7. Equipment to be Monitored**, the permittee shall report in a summary format by equipment type, the number of components for which leaks were detected and for valves, pumps and connectors show the percent leakers, and the total number of components monitored. Also include the number of leaking components that were not repaired as required by 40 CFR 63.1024, and for valves and connectors, identify the number of components that are determined by 40 CFR 63.1025(c)(3) to be nonrepairable. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1039(b) referenced by 40 CFR 63.2480]
- **BB.11.** <u>Periodic/Semiannual Compliance Reports</u>. Periodic compliance reports required by 40 CFR 63.2520(d) shall be submitted semiannually according to the schedule specified in 40 CFR 63.2520(b) as follows:
  - a. Each subsequent compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31.
  - b. Each subsequent compliance report must be postmarked or delivered no later than August 31 or February 28, whichever date is the first date following the end of the semiannual reporting period.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.2520(b) & (e)]

- **BB.12.** <u>Operational Records</u>. The permittee shall maintain the following operational records:
  - a. Equipment identification and documentation of unsafe-to-monitor or repair and special equipment designations. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1022, 63.1023(e) and 63.1038(b) referenced by 40 CFR 63.2480]
  - b. Leak Monitoring Records. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1024(d), (f); 63.1038(c) referenced by 40 CFR 63.2480]
  - c. Valves Subject to Subgrouping (If applicable). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1025(b)(4)(iv) referenced by 40 CFR 63.2480]
  - d. Dual mechanical seal design criteria for exempt pumps (If applicable). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1026(e)(1)(i) referenced by 40 CFR 63.2480]
  - e. Monitoring Periods for Connectors. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1027(b)(3)(v) referenced by 40 CFR 63.2480]
  - f. Dual mechanical seal design criteria for exempt agitators (If applicable). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1028(e)(1)(vi)(B) referenced by 40 CFR 63.2480]
  - g. Pressure Relief Device Demands. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1030(c)(3) referenced by 40 CFR 63.2480]
  - h. Compressor seal design criteria (If applicable). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1031(d)(2) referenced by 40 CFR 63.2480]
  - i. Pumps Subject to a Quality Improvement Program (If applicable). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1035(d)(2), (6)(iii), 6(iv), (7) & (e)(1)-(6) referenced by 40 CFR 63.2480]
  - j. Alternative Means of Compliance (If applicable). [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1036(d) referenced by 40 CFR 63.2480]
  - k. General Recordkeeping Requirements. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1038 referenced by 40 CFR 63.2480]

[Rule 62-4.070(3), F.A.C.] <sup>L</sup> Back to Table of Contents

# Subsection CC. Emission Unit 078

### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
078	DIMLA VOC Equipment Leaks

DIMLA VOC Equipment Leaks comprise fugitive emissions from pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves and connectors in VOC service but not also in HAP service (which are regulated as EU 077) and located within the unit boundaries of the DIMLA process.

EUs for equipment leaks are for regulatory purposes only and emissions are reported under EU 062, Facility-wide Equipment Leak Fugitives.

{Permitting Note: This emissions unit is regulated under 40 CFR 60 Subpart VVa - Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006 (adopted and incorporated by reference in Rule 62-204.800(8)(b)55., F.A.C.).}

# **Essential Potential to Emit (PTE) Parameters**

**CC.1.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

# **Equipment Limitations and Standards**

- **CC.2.** Equipment Identification. Equipment shall be identified as either subject to monitoring or exempt from monitoring. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(e)(1)-(6) & (f), (i) & (j)]
- CC.3. Emission Standards. The permittee shall comply with the following emission standards, as applicable:
  - a. Standards for Pumps in light liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-2a]
  - b. Standards for Compressors. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-3a]
  - c. Standards for Pressure relief devices in gas/vapor service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-4a]
  - d. Standards for Sampling connection systems. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-5a]
  - e. Standards for Open-ended valves or lines. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-6a]
  - f. Standards for Valves in gas/vapor service and in light liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-7a]
  - g. Standards for Pumps, valves, and connectors in heavy liquid service and pressure relief devices in light liquid or heavy liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-8a]
  - h. Standards for Delay of repair. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-9a]
  - i. Standards for Closed vent systems and control devices. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-10a]
  - j. Standards for Connectors in gas/vapor service and in light liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-11a (Currently stayed at 73 FR 31376)]

When a leak is detected, it shall be flagged in the field and recorded in a log which shall be kept for two years in a readily accessible location. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(b) and (c)]

### **Compliance Methods and Procedures**

**CC.4.** <u>Test Methods</u>. Required tests shall be performed in accordance with the following reference methods.

### Subsection CC. Emission Unit 078

Method	Description of Method and Comments
21	Determination of Volatile Organic Compound Leaks

Monitoring shall comply with Method 21 of 40 CFR part 60, Appendix A, except as otherwise provided in 40 CFR 60.485a. The above method is described in Appendix A of 40 CFR 60 and adopted by reference in Rule 62-204.800, F.A.C. No other methods may be used unless prior written approval is received from the Department. [Rule 62-204.800, F.A.C.]

### **Monitoring of Operations**

- **CC.5.** <u>Leak Monitoring</u>. Except where equipment has been designated exempt from monitoring under **Specific Condition CC.2 Equipment Identification.**, the permittee shall comply with the routine monitoring requirements in the following standards:
  - a. Standards for Pumps in light liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-2a(a), (b)(2)]
  - b. Standards for Compressors. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-3a(e)(1)]
  - c. Standards for Pressure relief devices in gas/vapor service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-4a(b)]
  - d. Standards for Valves in gas/vapor service and in light liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-7a(a) & (c)]
  - e. Standards for Connectors in gas/vapor service and in light liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-11a(a) & (b)(3) (Currently stayed)]

[Rule 62-4.070(3), F.A.C. and Rule 62-204.800(8), F.A.C.; 40 CFR 60.482-2a, 3a, 4a, 7a and 11a]

### **Recordkeeping and Reporting Requirements**

**CC.6.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	<b>Reporting Deadline</b>	Related Condition(s)
Semiannual Equipment Leak Reports	Semi-Annual	CC.8.

[Rule 62-213.440(1)(b), F.A.C.]

- **CC.7.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- CC.8. Equipment Leak Reports. The permittee shall submit the following reports:
  - a. Semiannual Equipment Leak Reports required by 40 CFR 60.487(a). [Rule 62-204.800(8), F.A.C.; 40 CFR 60.487a(a)-(c)]
  - b. Notification of compliance with alternative standards, if applicable. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.487a(d)]
  - c. Performance test reports required by 40 CFR 60.487(e), if applicable. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.487a(e)]
- **CC.9.** <u>Operational Records</u>. The following records shall be kept to demonstrate compliance with the leak detection and repair standards.

### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection CC. Emission Unit 078

- a. For each monitoring event the following information shall be recorded: (1) monitoring instrument identification, (2) operator identification, (3) equipment identification, (4) date of monitoring, and (5) instrument reading. Rule 62-204.800(8), F.A.C.; [40 CFR 60.486a(a)(3)]
- b. When each leak is detected, the following information shall be recorded in a log and shall be kept for two years in a readily accessible location:
  - (1) The instrument and operator identification numbers and the equipment identification number, except when indications of liquids dripping from a pump are designated as a leak,
  - (2) The date the leak was detected and the dates of each attempt to repair the leak,
  - (3) Repair methods applied in each attempt to repair the leak,
  - (4) Maximum instrument reading measured by Method 21 of Appendix A to 40 CFR part 60 at the time the leak is successfully repaired or determined to be no repairable (except when a pump is repaired by eliminating indications of liquids dripping),
  - (5) "Repair delayed" and the reason for the delay if a leak is not repaired within 15 calendar days after discovery,
  - (6) The signature of Permittee (or designee) whose decision it was that repair could not be effected without a process shutdown,
  - (7) The expected date of successful repair of the leak if a leak is not repaired within 15 days,
  - (8) Dates of process unit shutdowns that occur while the equipment is unrepaired,
  - (9) The date of successful repair of the leak.

[Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(b)]

- c. If applicable, information pertaining to the design of closed vent systems and control devices used to control equipment leaks. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(d)]
- d. Documentation for each compliance test performed to designate equipment operating with no detectable emissions in 40 CFR 60.482-2a(e), 60.482-3a(i), 60.482-4a, and 60.482-7a(f). [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(e)(4)]
- e. The date and results of the weekly visual inspection for indications of liquids dripping from pumps in light liquid service. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(e)(7)]
- f. Calibration records for monitoring instruments. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(e)(8)]
- g. The connector monitoring schedule (if applicable). [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(e)(9)]
- h. Records of each release from a pressure relief device subject to monitoring. [Rule 62-204.800(8), F.A.C.; 40CFR 60.486a(e)(10)]
- i. Documentation required for compliance with the alternative monitoring frequency for valves described in 40 CFR 60.483-2a, if applicable. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(g)]
- j. Design criteria for pump or compressor seal systems equipped with leak detectors as described in 40 CFR 60.482-2a(d)(5) and/or 60.482-3a(e)(2), if applicable. [Rule 62-204.800(8), F.A.C.; 40 CFR 60.486a(h)]

[Rule 62-4.070(3), F.A.C.]

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### Subsection DD. Emission Unit 079

### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
079	DIMLA Scrubber

The DIMLA scrubber, T-62028, recovers methanol (which is a HAP) and methylamines from the DIMLA Purification Tower overhead vacuum system. The recovered amines are fed to the MA Plant No. 4 via the DIMLA Absorption and Desorption Columns with the methanol going through tank TK-62099 to the wastewater treatment system.

{Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart FFFF - National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing (adopted and incorporated by reference in Rule 62-204.800(11)(b)63., F.A.C.). Compliance with 40 CFR 63 Subpart FFFF constitutes compliance with 40 CFR 60 Subpart NNN.}

# **Essential Potential to Emit (PTE) Parameters**

- **DD.1.** <u>Methods of Operation</u>. The DIMLA Scrubber shall be operated with a minimum water flow of 1 gpm, based on a 24-hr block average (midnight to midnight) at all times when emissions are vented to it, excluding periods of non-operation of the source. [Rules 62-210.200(PTE), 62-4.070(3), F.A.C.; Permit No. 1130004-019-AC, and Permit No. 1130004-026-AC]
- **DD.2.** <u>Hours of Operation</u>. This emissions unit is allowed to operate continuously, i.e., 8,760 hour/year. [Rule 62-210.200(PTE), F.A.C.]

### **Monitoring of Operations**

- **DD.3.** <u>Bypass monitoring</u>. Except for equipment needed for safety purposes such as pressure relief devices, low leg drains, high point bleeds, analyzer vents, and open-ended valves or lines, Permittee shall comply with one of the following for each closed vent system that contains bypass lines that could divert a vent stream to the atmosphere:
  - a. Properly install, maintain, and operate a flow indicator that is capable of taking readings at least once every 15 minutes. The flow indicator shall be installed at the entrance to any bypass line.
  - b. Secure the bypass line valve in the non-diverting position with a car-seal or a lock-and-key type configuration and visually inspect the seal or closure mechanism at least monthly to verify that the valve is maintained in the non-diverting position, and the vent stream is not diverted through the bypass line.

[Rule 62-204.800(11), F.A.C., and 40 CFR 63.983(a)(3)(i) & (ii)]

**DD.4.** <u>Process Monitoring.</u> The permittee shall install a flow meter capable of providing a continuous record (block average values recorded at least every 15 minutes) of the absorber influent water flow. For absorbers that control organic compounds and use water as the scrubbing fluid, the permittee must conduct monitoring and recordkeeping as specified in 40 CFR 63.2450(k)(5). [Rule 62-204.800(11), F.A.C. and 40 CFR 63.2450(k)(5)]

### **Recordkeeping and Reporting Requirements**

**DD.5.** <u>Reporting Schedule</u>. The following reports and notifications shall be submitted to the Compliance Authority:

Report	Reporting Deadline	Related Condition(s)
Periodic/Semiannual Report	Semi-Annual	DD.9.

[Rule 62-213.440(1)(b), F.A.C.]

### SECTION III. EMISSIONS UNITS AND SPECIFIC CONDITIONS. Subsection DD. Emission Unit 079

- **DD.6.** <u>Other Reporting Requirements</u>. See Appendix RR, Facility-Wide Reporting Requirements, for additional reporting requirements. [Rule 62-213.440(1)(b), F.A.C.]
- **DD.7.** <u>Bypass Monitoring Records</u>. The permittee shall maintain the records specified in 40 CFR 63.998(d)(1)(ii)(A) or (B), as appropriate to document that the DIMLA scrubber is not bypassed.
  - a. Hourly records of whether the flow indicator specified under 40 CFR 63.983(a)(3)(i) was operating and whether a diversion was detected at any time during the hour, as well as records of the times of all periods when the vent stream is diverted from the control device or the flow indicator is not operating.
     [63.998(d)(1)(ii)(A)]
  - b. Where a seal mechanism is used to comply with 40 CFR 63.983(a)(3)(ii), hourly records of flow are not required. In such cases, Permittee shall record that the monthly visual inspection of the seals or closure mechanisms has been done and shall record the occurrence of all periods when the seal mechanism is broken, the bypass line valve position has changed, or the key for a lock-and-key type lock has been checked out, and records of any car-seal that has been broken. [63.998(d)(1)(ii)(B)]

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.983(a)(3) and 63.998(d)(1)(ii)(A) & (B)]

- **DD.8.** <u>Leak Repair Records</u>. The permittee shall maintain leak detection and repair records for the piping connecting the DIMLA Purification Tower overhead vacuum system discharge to the DIMLA Scrubber as specified in 40 CFR 63.998(d)(1)(iii)(A)-(F). These records shall be maintained for five years.
  - a. The instrument and the equipment identification number and the operator name, initials, or identification number.
  - b. The date the leak was detected and the date of the first attempt to repair the leak.
  - c. The date of successful repair of the leak.
  - d. The maximum instrument reading measured by the procedures in 40 CFR 63.983(c) after the leak is successfully repaired or determined to be nonrepairable.
  - e. "Repair delayed" and the reason for the delay if a leak is not repaired within 15 days after discovery of the leak. Permittee may develop a written procedure that identifies the conditions that justify a delay of repair. In such cases, reasons for delay of repair may be documented by citing the relevant sections of the written procedure.
  - f. Copies of the Periodic Reports as specified in 40 CFR 63.999(c), if records are not maintained on a computerized database capable of generating summary reports from the records.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.983(a)(3) and 63.998(d)(1)(iii)(A)-(F)]

- **DD.9.** <u>Periodic/Semiannual Report</u>. Information required by 40 CFR 63.999(c)(2) pertaining to the monitoring of closed vent systems shall be included in the Periodic Report.
  - a. The information recorded in 40 CFR 63.998(d)(1)(iii)(B) through (E) (Specific Condition DD.8. Leak Repair Records).
  - b. Reports of the times of all periods recorded under 40 CFR 63.998(d)(1)(ii)(A) (Specific Condition DD.7.a. Bypass Monitoring Records) when the vent stream is diverted from the control device through a bypass line; and
  - c. Reports of all times recorded under 40 CFR 63.998(d)(1)(ii)(B) (Specific Condition DD.7.b. Bypass Monitoring Records) when maintenance is performed in car-sealed valves, when the seal is broken, when the bypass line valve position is changed, or the key for a lock-and-key type configuration has been checked out.

[Rule 62-204.800(11), F.A.C.; 40 CFR 63.982(c); 40 CFR 63.999(c)(2)(i)-(iii); and Permit 1130004-019-AC]

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### Subsection EE. Emission Unit 080

### The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
080	Existing Emergency Reciprocating Internal Combustion Engines (RICE) (Before 2006)

This emission unit consists of four stationary, emergency, diesel fueled, compression ignition, reciprocating internal combustion engines (CI RICE). These stationary RICE each have a rating of less than 500 brake hp; they are located at a major source of hazardous air pollutants (HAP) emissions and were constructed before June 12, 2006. Therefore, in accordance with 40 CFR 63.6590(a)(1)(ii) they are existing emergency stationary CI RICE and must comply with the emission limitations in Table 2c to 40 CFR 63 Subpart ZZZZ which apply to Emergency Stationary CI RICE. The following table provides important details for this emissions unit.

Equip. I.D.	Area/Location	Existing or New	Construction Commenced Date	Brake hp	Fuel Type
PG24101C	B-Area well water pump	Existing	04/19/1994	234	Diesel
PG24101B	No. 2 well water pump	Existing	04/06/1994	234	Diesel
D24018	Plant emergency generator	Existing	06/07/1991	330	Diesel
PG24121	South Foxtrot fire water pump	Existing	04/15/1994	340	Diesel

{*Permitting Note: This emissions unit is regulated by 40 CFR 63 Subpart ZZZ – National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (adopted and incorporated by reference in Rule 62-204.800(11)(b)82., F.A.C.).*}

# **Essential Potential to Emit (PTE) Parameters**

**EE.1.** <u>Hours of Operation</u>. Emergency stationary RICE may be operated for the purpose of maintenance checks and readiness testing, provided that the tests are recommended by Federal, State or local government, the manufacturer, the vendor, or the insurance company associated with the engine. Maintenance checks and readiness testing of such units is limited to 100 hours per year. There is no time limit on the use of emergency stationary RICE in emergency situations. Permittee may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if Permittee maintains records indicating that Federal, State, or local standards require maintenance and testing of emergency situations, but those 50 hours are counted towards the 100 hours per year provided for maintenance and testing. The 50 hours per year for non- emergency situations cannot be used for peak shaving or to generate income for a facility to supply power to an electric grid or otherwise supply power as part of a financial arrangement with another entity. For owners and operation in non-emergency situations for 50 hours per year, as permitted in 40 CFR 63.6640, is prohibited. [Rules 62-210.200(PTE), 62-204.800(11), F.A.C.; and 40 CFR 63.6640(f)]

### **Emission Limitations and Standards**

- **EE.2.** <u>Work or Management Practice Standards</u>. Permittee of an existing stationary CI RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions must comply with the applicable emission limitations and operating limitations in Table 2c to 40 CFR 63 Subpart ZZZZ which apply to Emergency Stationary CI RICE.
  - a. The Permittee must meet the following requirements, except during periods of startup:
    - (1) Change oil and filter every 500 hours of operation or annually, whichever comes first;
    - (2) Inspect air cleaner every 1,000 hours of operation or annually, whichever comes first, and replace as necessary; and;

- (3) Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary.
- b. During periods of startup you must minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply.

[Rule 62-204.800(11), F.A.C.; 40 CFR63.6602 and Table 2c to 40 CFR63 Subpart ZZZZ]

- **EE.3.** <u>Monitoring of Operations</u>. The Permittee must comply with the following monitoring, installation, collection, operation, and maintenance requirements:
  - a. The Permittee must operate and maintain the stationary RICE and after-treatment control device (if any) according to the manufacturer's emission-related written instructions or develop your own maintenance plan which must provide to the extent practicable for the maintenance and operation of the engine in a manner consistent with good air pollution control practice for minimizing emissions. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.6625(e)]
  - b. The Permittee must install a non-resettable hour meter if one is not already installed. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.6625(f)]
  - c. The Permittee must minimize the engine's time spent at idle during startup and minimize the engine's startup time to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the emission standards applicable to all times other than startup in Tables 1a, 2a, 2c, and 2d to 40 CFR63 Subpart ZZZZ apply. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.6625(h)]
  - d. You have the option of utilizing an oil analysis program in order to extend the specified oil change requirement in Tables 2c and 2d to 40 CFR63 Subpart ZZZZ. The oil analysis must be performed at the same frequency specified for changing the oil in Table 2c or 2d to 40 CFR63 Subpart ZZZZ. The analysis program must at a minimum analyze the following three parameters: Total Base Number, viscosity, and percent water content. The condemning limits for these parameters are as follows: Total Base Number is less than 30 percent of the Total Base Number of the oil when new; viscosity of the oil has changed by more than 20 percent from the viscosity of the oil when new; or percent water content (by volume) is greater than 0.5. If all of these condemning limits are not exceeded, the engine owner or operator is not required to change the oil. If any of the limits are exceeded, the engine owner or operator must change the oil within 2 days of receiving the results of the analysis; if the engine is not in operation when the results of the analysis are received, the engine owner or operator must change the oil within 2 days of receiving the results of the analysis; if the engine is not in operation when the results of the program, the results of the analysis, and the oil changes for the engine. The analyzed as part of the program, the results of the analysis, and the oil changes for the engine. The analyzed as part of the program, the results of the analysis, and the oil changes for the engine. The analyzed as part of the program, the results of the engine. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.6625(i)]

# **Recordkeeping and Reporting Requirements**

**EE.4.** <u>Maintenance Records</u>. The Permittee must keep records of the maintenance conducted on the existing stationary emergency RICE in order to demonstrate that you operated and maintained the stationary RICE and after-treatment control device (if any) according to your own maintenance plan. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.6655(e) & (f)]

### **Applicable Federal Regulations**

EE.5. <u>NESHAP Subpart ZZZZ</u>. The existing emergency stationary CI RICE are subject to applicable requirements in NESHAP 40 CFR 63 Subpart ZZZZ and must comply with the emission limitations in Table 2c to 40 CFR 63 Subpart ZZZZ which apply to Emergency Stationary CI RICE. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.6585, 63.6590(a)(1)(ii) and 63.6602]

# Subsection FF. Emission Unit 081

# The specific conditions in this section apply to the following emissions unit:

EU No.	Brief Description
081	New Emergency Reciprocating Internal Combustion Engine (Fire Pump) (After 2007)

This emission unit consists of one "new" stationary, emergency, 268 bhp, diesel-fueled, manufacturer-certified, compression ignition, CI RICE, manufactured after 2007, with a displacement of less than 30 liters per cylinder.

Equip. I.D.	Area/Location	Existing or New	Construction Commenced Date	Brake hp	Fuel Type
PG24114	Main fire water pump	New	06/2016	268	Diesel

{Permitting Note: This new CI RICE is regulated by 40 CFR 60, Subpart IIII - Standards of Performance for Stationary Compression Ignition Internal Combustion Engines (adopted and incorporated by reference in Rule 62-204.800(8)(b)82., F.A.C.). The fire pump engine is a "new" stationary emergency CI RICE with a displacement of less than 30 liters per cylinder, located at a major source of HAP, commenced construction on or after 6/12/2006, and has a post-2007 model year.}

# **PERFORMANCE RESTRICTIONS**

- FF.1. Hours of Operation. The stationary compression ignition reciprocating internal combustion engine (emergency ire pump) is allowed to operate in accordance with the definition of emergency stationary internal combustion engines in 40 CFR 60.4219. The engine may be operated 100 hours per year for maintenance and testing, and up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing. There is no time limit on the use of emergency stationary RICE in emergency situations. Records of hours of operation for this stationary RICE shall be maintained and available for Department inspection. [Rules 62-4.070(3) 62.210.200(PTE), and 62-204.800(8), F.A.C.; and 40 CFR 60.4211(f)]
- **FF.2.** <u>Fuel requirements for stationary CI RICE subject to 40 CFR 60, Subpart IIII</u>. Owners and operators of stationary CI RICE subject to 40 CFR 60, Subpart IIII with a displacement of less than 30 liters per cylinder that use diesel fuel must use diesel fuel that has a maximum sulfur content of 15 ppm, a cetane index of 40 and a maximum aromatic content of 35 volume percent. [Rule 62-204.800(8), F.A.C., 40 CFR 80.510(b) and 40 CFR 60.4207(b)]</u>

# **EMISSION STANDARDS**

- **FF.3.** <u>Emission Limits</u>. Owners and operators of fire pump engines with a displacement of less than 30 liters per cylinder must comply with the emission standards in table 4 to 40 CFR 60, Subpart IIII, for all pollutants. The maximum NMHC + NO<sub>X</sub> is 3.0 g/HP-hr, the maximum CO is 2.6 g/HP-hr, and the maximum PM is 0.15 g/HP-hr. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.4205(c)]
- **FF.4.** <u>Continuous Compliance</u>. Owners and operators of stationary CI ICE must operate and maintain stationary CI RICE that achieve the emission standards as required in 40 CFR 60.4205 over the entire life of the engine. [Rule 62-204.800(8), F.A.C. and 40 CFR 60.4206]

# MONITORING OF OPERATIONS

**FF.5.** <u>Monitoring requirements for stationary CI internal combustion engines</u>. Owners and operators must install a non-resettable hour meter prior to startup of the engine, if such a meter is not already installed. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.4209(a)]

# Subsection FF. Emission Unit 081

# **COMPLIANCE REQUIREMENTS**

- **FF.6.** <u>Work or Management Practice Standards</u>. Compliance requirements for stationary CI internal combustion engines are as follows:
  - a. The Permittee must do all of the following:
    - (1) Operate and maintain the stationary CI internal combustion engine and control device according to the manufacturer's emission-related written instructions;
    - (2) Change only those emission-related settings that are permitted by the manufacturer; and
    - (3) Meet the requirements of 40 CFR 89, 94 and/or 1068, as they apply to you.
  - b. The Permittee must operate the emergency stationary RICE according to the requirements in paragraphs (f)(1) through (3) of section 40 CFR 60.4211. In order for the engine to be considered an emergency stationary RICE under 40 CFR 63 Subpart IIII, any operation other than emergency operation, maintenance and testing, and operation in non-emergency situations for 50 hours per year, as described in paragraphs (f)(1) through (3) of 40 CFR 60.4211, is prohibited. If you do not operate the engine according to the requirements in paragraphs (f)(1) through (3) of 40 CFR 63 Subpart IIII and must meet all requirements for non-emergency engines.
    - (1) There is no time limit on the use of emergency stationary RICE in emergency situations.
    - (2) You may operate your emergency stationary RICE for any combination of the purposes specified in paragraphs (f)(2)(i) through (iii) of 40 CFR 60.4211 for a maximum of 100 hours per calendar year. Any operation for non-emergency situations as allowed by paragraph (f)(3) of 40 CFR 60.4211 counts as part of the 100 hours per calendar year allowed by paragraph (f)(2).
      - (a) Emergency stationary RICE may be operated for maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor, or the insurance company associated with the engine.
      - (b) Permittee may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if Permittee maintains records indicating that federal, state, or local standards require maintenance and testing of emergency RICE beyond 100 hours per calendar year.
    - (3) Emergency stationary RICE may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing provided in paragraph (f)(2) of 40 CFR 60.4211.
  - c. If you do not install, configure, operate and maintain your engine and control device according to the manufacturer's emission-related written instructions, or you change emission-related settings in a way that is not permitted by the manufacturer, you must demonstrate compliance as follows:
    - (1) The Permittee must keep a maintenance plan and records of conducted maintenance to demonstrate compliance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions.
    - (2) In addition, you must conduct an initial performance test to demonstrate compliance with the applicable emission standards within 1 year of such action.

# Subsection FF. Emission Unit 081

[Rule 62-204.800(8), F.A.C., and 40 CFR 60.4211]

# **Recordkeeping and reporting Requirements**

- **FF.7.** Notification, reporting, and recordkeeping requirements for stationary CI RICE. Permittee of an emergency stationary CI RICE is not required to submit an initial notification. The Permittee must keep records of the operation of the engine in emergency and non-emergency service that are recorded through the non-resettable hour meter. The owner must record the time of operation of the engine and the reason the engine was in operation during that time. [Rule 62-204.800(8), F.A.C., and 40 CFR 60.4214(b)]
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### SECTION IV. COMMON CONDITIONS.

# These Common Conditions Apply to Specific Emission Units as Referenced in this Permit.

### The following conditions apply to specific emission units and activities as referenced in this Permit:

**C.C.1.** <u>Compliance Monitoring</u>. In addition to specific control device parameter monitoring requirements previously specified, Permittee must maintain minimum daily monitoring data availability in accordance with criteria specified in 40 CFR 63.152(c)(2)(A). Each day in which the average daily value of a control device parameter is not maintained within its required ranges or minimum data availability is not achieved is considered a single excursion. The maximum number of allowable excursions during any semiannual reporting period is specified in 40 CFR 63.152(c)(4)(B). If a monitored parameter is outside its established range or monitoring data are not collected during periods of start-up, shutdown, or malfunction (and the source is operated during such periods in accordance with the source's start-up, shutdown, and malfunction plan as required by 40 CFR 63.6(e)(3) or 40 CFR 63 Subpart A) or during periods of nonoperation of the chemical manufacturing process unit or portion thereof (resulting in cessation of the emissions to which the monitoring applies), then the excursion is not a violation and, in cases where continuous monitoring is required, the excursion does not count toward the number of excused excursions for determining compliance. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.152(c)]

# C.C.2. Startup, Shutdown, and Malfunction Plan (SSMP). Permittee shall prepare a

startup/shutdown/malfunction plan that describes, in detail, procedures for operating and maintaining the source during periods of startup, shutdown, and malfunction and a program of corrective action for malfunctioning process and air pollution control equipment used to comply with the relevant standard. The plan shall identify all routine or otherwise predictable continuous monitoring system malfunctions. The plan shall be developed by the compliance date for that relevant standard. Each plan prepared is incorporated by reference into this Title V permit. Actions taken that are consistent with the startup/shutdown/malfunction plan must be reported on a semi-annual basis within 30 days after each calendar half year (January 31 and July 31). [Rules 62-204.800(11), F.A.C., 40 CFR 63.6(e)(3)(i) & (ii), and 40 CFR 63.103(c)(2)(i)(ii)]

**C.C.3.** <u>Recordkeeping and Reporting of Startups, Shutdowns, and Malfunctions</u>. When actions during startup/shutdown/malfunction with excess emissions (startup/shutdown/malfunction that causes the source to exceed any applicable emission limitation in the relevant emission standards) are taken consistent with the SSMP, records shall be maintained indicating that recommended procedures were followed. A Periodic Startup, Shutdown, and Malfunction Report shall be submitted semiannually for actions that were taken that were consistent with the Plans in accordance with the requirements of 40 CFR 63.10(d)(5)(i). Actions taken that are inconsistent with a startup/shutdown/malfunction plan must be reported within 2 working days with written follow-up provided within 7 working days. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.10(d)(5)]</u>

### C.C.4. Excess Emissions and Data Obtained During Startups, Shutdowns, and Malfunctions.

- a. Excess emissions resulting from startup, shutdown or malfunction of any emissions unit shall be permitted provided (1) best practices to minimize emissions are adhered to and (2) the duration of excess emissions shall be minimized but in no case exceed two hours in any 24-hour period unless specifically authorized by the Department for longer duration. Excess emissions that are caused entirely or in part by poor maintenance, poor operation, or any other equipment or process failure that may reasonably be prevented during startup, shutdown or malfunction shall be prohibited. [Rule 62-210.700(1), F.A.C.]
- b. Malfunctions must be corrected as soon as practicable after their occurrence. To the extent that an unexpected event arises during a startup, shutdown, or malfunction, an owner or operator must comply by minimizing emissions during such a startup, shutdown, and malfunction event consistent with safety and good air pollution control practices. [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.6(e)(ii)]
- c. Monitoring data recorded during monitoring system breakdowns, repairs, calibration checks, and zero (low-level) and high-level adjustments; Start-ups; Shutdowns; Malfunctions; Periods of non-operation of the chemical manufacturing process unit (or portion thereof), resulting in cessation of the emissions to which the monitoring applies, shall not be included in any average computed under 40 CFR 63, Subpart

G. Records shall be kept of the times and durations of all such periods and any other periods during process or control device operation when monitors are not operating. [Rule 62-204.800(11), F.A.C.; and 40CFR 152(f)(7)]

- d. The provisions set forth in 40 CFR 63 Subparts F and G shall apply at all times except during periods of start-up or shutdown, malfunction, or non-operation of the chemical manufacturing process unit (or specific portion thereof) resulting in cessation of the emissions to which 40 CFR 63Subparts F and G apply. However, if a start-up, shutdown, malfunction or period of non-operation of one portion of a chemical manufacturing process unit does not affect the ability of a particular emission point to comply with the specific provisions to which it is subject, then that emission point shall still be required to comply with the applicable provisions of 40 CFR 63 Subparts F and G during the start-up, shutdown, malfunction or period of non-operation. [Rules 62-204.800(11) and 2., F.A.C.; and 40 CFR 63.102(a)(1)]
- **C.C.5.** <u>General Recordkeeping Requirements</u>. In addition to recordkeeping requirements specified in Specific Conditions, Permittee shall maintain files of information (including performance reports and initial notifications) required under 40 CFR 63. Required information includes information specified in the following sections:
  - a. 40 CFR 63.10(b) & (c) ("general provisions");
  - b. 40 CFR 63.117 and/or 63.118 ("process vents")
  - c. 40 CFR 63.123 ("storage vessels")
  - d. 40 CFR 63.130 ("transfer operations")
  - e. 40 CFR 63.147 ("process wastewater")
  - f. 40 CFR 63.152 ("general reporting and continuous records")

[Rules 62-204.800(11), and (11)(d), F.A.C.]

- **C.C.6.** <u>General Reporting Requirements for Specific Emission Units Subject to 40 CFR 63 Subpart G</u>. Periodic reports shall be submitted to the Department semiannually no later than 60 calendar days after the end of each 6-month period. In addition to any reporting required under Specific Conditions of this permit, Periodic Reports shall include information specified in the following sections:
  - a. 40 CFR 63.10(d) ("general provisions");
  - b. 40 CFR 63.117 and/or 63.118 ("process vents")
  - c. 40 CFR 63.122 ("storage vessels")
  - d. 40 CFR 63.129 and/or 63.130 ("transfer operations")
  - e. 40 CFR 63.146 ("process wastewater")
  - f. 40 CFR 63.152(c)(2), (c)(3), (c)(4) ("general reporting and continuous records")

[Rules 62-204.800(11), and (11)(d), F.A.C.]

- **C.C.7.** <u>Additional Reporting Requirements for Sources with Continuous Monitoring Systems (CMS)</u>. Sources required by a relevant standard under 40 CFR 63 to install a CMS shall submit semiannual reports summarizing information specified in 40 CFR 63.10(e)(3). [Rule 62-204.800(11), F.A.C.; and 40 CFR 63.10(e)(3)]</u>
- **C.C.8.** <u>Schedule of Reporting for Specific Sources Subject to 40 CFR 63 Subparts F, G and H</u>. Periodic reporting required under Common Conditions **C.C.3**, **C.C.6** and **C.C.7** shall be submitted with Title V semiannual Progress Reports unless a mutual agreement to change the schedule of reporting is reached between Permittee and the Department. Notwithstanding, the Department may reduce the frequency of periodic reporting at the request of

Permittee provided that the conditions specified in 40 CFR 63.10(e)(3)(ii) are met. [Rule 62-204.800(11(d), F.A.C., and 40 CFR 63.10(e)(3)(ii)]

**C.C.9.** <u>Closed Vent System Inspections</u>. Each closed vent system shall be inspected and maintained on an annual basis according to the criteria specified in 40 CFR 63.148. [Rule 62-204.800(11), F.A.C., and 40 CFR 63.120(d)(6)]

C.C.10. Compliance reports. Compliance reports must contain the following information per 40 CFR 63.2520(e):

- a. Company name and address.
- b. Statement by a responsible official with that official's name, title, and signature, certifying the accuracy of the content of the report. If your report is submitted via CEDRI, the certifier's electronic signature during the submission process replaces the requirement in this paragraph.
- c. Date of report and beginning and ending dates of the reporting period. You are no longer required to provide the date of the report when the report is submitted via CEDRI.
- d. For each SSM during which excess emissions occur, the compliance report must include records that the procedures specified in your startup, shutdown, and malfunction plan (SSMP) were followed or documentation of actions taken that are not consistent with the SSMP and include a brief description of each malfunction. On or after August 12, 2023, this paragraph no longer applies; however, for historical compliance purposes, a copy of the plan must be retained and available on-site for five years after August 12, 2023.
- e. The compliance report must contain the information on deviations, as defined in 40 CFR 63.2550, according to paragraphs (e)(5)(i), (ii), (iii), and (iv) of 40 CFR 63.2520.
  - (1) If there are no deviations from any emission limit, operating limit or work practice standard specified in 40 CFR 63 Subpart FFFF, include a statement that there were no deviations from the emission limits, operating limits, or work practice standards during the reporting period.
  - (2) For each deviation from an emission limit, operating limit, and work practice standard that occurs at an affected source where you are not using a continuous monitoring system (CMS) to comply with the emission limit or work practice standard in 40 CFR 63 Subpart FFFF, you must include the information in paragraphs (e)(5)(ii)(A) through (D) of 40 CFR 63.2520. This includes periods of SSM.
    - (i) The total operating time in hours of the affected source during the reporting period.
    - (ii) Operating logs of processes with batch vents from batch operations for the day(s) during which the deviation occurred, except operating logs are not required for deviations of the work practice standards for equipment leaks.
    - (iii) Report information for each deviation to meet an applicable standard. For each instance, report the start date, start time, and duration in hours of each deviation. For each deviation, the report must include a list of the affected sources or equipment, an estimate of the quantity in pounds of each regulated pollutant emitted over any emission limit, a description of the method used to estimate the emissions, the cause of the deviation (including unknown cause, if applicable), as applicable, and the corrective action taken.
  - (3) For each deviation from an emission limit or operating limit occurring at an affected source where you are using a CMS to comply with an emission limit in 40 CFR 63 Subpart FFFF, you must include the information in paragraphs (e)(5)(iii)(A) through (N) of 40 CFR 63.2520. This includes periods of SSM.
    - (i) The start date, start time, and duration in hours that each CMS was inoperative, except for zero (low-level) and high-level checks.

- (ii) The start date, start time, and duration in hours that each CMS was out-of-control and a description of the corrective actions taken.
- (iii) A summary of the total duration in hours of all deviations for each CMS during the reporting period, the total operating time in hours of the affected source during the reporting period, and the total duration as a percent of the total operating time of the affected source during that reporting period.
- (iv) A summary of the total duration in hours of CMS downtime for each CMS during the reporting period, and the total duration of CMS downtime as a percent of the total operating time of the affected source during that reporting period.
- (v) An identification of each HAP that is known to be in the emission stream.
- (vi) A brief description of the process units.
- (vii) A brief description of the CMS. The monitoring equipment manufacturer(s) and model number(s) and the pollutant or parameter monitored.
- (viii)The date of the latest CMS certification or audit.
- (ix) Operating logs of processes with batch vents from batch operations for each day(s) during which the deviation occurred.
- (x) The operating day or operating block average values of monitored parameters for each day(s) during which the deviation occurred.
- (xi) Report the number of deviations to meet an applicable standard. For each instance, report the start date, start time and duration in hours of each deviation. For each deviation, the report must include a list of the affected sources or equipment, an estimate of the quantity in pounds of each regulated pollutant emitted over any emission limit, a description of the method used to estimate the emissions, and the cause of the deviation (including unknown cause, if applicable), as applicable, and the corrective action taken.
- (xii) Report a breakdown of the total duration in hours of the deviations during the reporting period into those that are due control equipment problems, process problems, other known causes, and other unknown causes.
- (4) If you documented in your notification of compliance status report that an MCPU has Group 2 batch process vents because the non-reactive HAP is the only HAP and usage is less than 10,000 lb/yr, the total uncontrolled organic HAP emissions from the batch process vents in an MCPU will be less than 1,000 lb/yr for the anticipated number of standard batches, or total uncontrolled hydrogen halide and halogen HAP emissions from all batch process vents and continuous process vents in a process are less than 1,000 lb/yr, include the records associated with each calculation required by 40 CFR 63.2525(e) that exceeds an applicable HAP usage or emissions threshold.
- f. If you use a CEMS, and there were no periods during which it was out-of-control as specified in 40 CFR 63.8(c)(7), include a statement that there were no periods during which the CEMS was out-of-control during the reporting period.
- g. Include each new operating scenario which has been operated since the time period covered by the last compliance report and has not been submitted in the notification of compliance status report or a previous compliance report. For each new operating scenario, you must report the information specified in 40 CFR 63.2525(b) and provide verification that the operating conditions for any associated control or treatment device have not been exceeded and that any required calculations and engineering analyses have been

performed. For the purposes of this paragraph, a revised operating scenario for an existing process is considered to be a new operating scenario.

- h. Records of process units added to a process unit group (PUG) as specified in 40 CFR 63.2525(i)(4) and records of primary product redeterminations as specified in 40 CFR 63.2525(i)(5).
- i. Applicable records and information for periodic reports as specified in referenced subparts F, G, H, SS, UU, WW, and GGG of Part 63 and 40 CFR 65 subpart F (Equipment Leaks); except as specified in 40 CFR 63.2450(e)(4), 40 CFR 63.2480(f), and 40 CFR 63.2485(p) and (q) and paragraph (t) of 40 CFR 63.2520.
- j. Notification of process change:
  - (1) Except as specified in paragraph (e)(10)(ii) of 40 CFR 63.2520, whenever you make a process change, or change any of the information submitted in the notification of compliance status report or a previous compliance report, that is not within the scope of an existing operating scenario, you must document the change in your compliance report. A process change does not include moving within a range of conditions identified in the standard batch, and a nonstandard batch does not constitute a process change. The notification must include all of the information in paragraphs (e)(10)(i)(A) through (C) of 40 CFR 63.2520.
    - (i) A description of the process change.
    - (ii) Revisions to any of the information reported in the original notification of compliance status report under paragraph (d) of 40 CFR 63.2520.
    - (iii) Information required by the notification of compliance status report under paragraph (d) of 40 CFR 63.2520 for changes involving the addition of processes or equipment at the affected source.
  - (2) You must submit a report 60 days before the scheduled implementation date of any of the changes identified in paragraph (e)(10)(ii)(A), (B), or (C) of 40 CFR 63.2520.
    - (i) Any change to the information contained in the pre-compliance report.
    - (ii) A change in the status of a control device from small to large.
    - (iii) A change from Group 2 to Group 1 for any emission point except for batch process vents that meet the conditions specified in 40 CFR 63.2460(b)(6)(i).

[Rule 62-204.800(11), F.A.C., and 40 CFR 63.2520(e)]

- k. For each flare subject to the requirements in 40 CFR 63.2450(e)(5), the compliance report must include the items specified in paragraphs (e)(11)(i) through (vi) of 40 CFR 63.2520(e)(11) in lieu of the information required in 40 CFR 63.999(c)(3) of subpart SS.
  - (1) Records as specified in 40 CFR 63.2525(m)(1) for each 15-minute block during which there was at least one minute when regulated material is routed to a flare and no pilot flame or flare flame is present. Include the start and stop time and date of each 15-minute block.
  - (2) Visible emission records as specified in 40 CFR 63.2525(m)(2)(iv) for each period of 2 consecutive hours during which visible emissions exceeded a total of 5 minutes.
  - (3) The periods specified in 40 CFR 63.2525(m)(6). Indicate the date and start and end times for each period, and the net heating value operating parameter(s) determined following the methods in 40 CFR 63.670(k) through (n) of subpart CC as applicable.
  - (4) For flaring events meeting the criteria in 40 CFR 63.670(o)(3) of subpart CC and 40 CFR 63.2450(e)(5)(v):

### SECTION IV. COMMON CONDITIONS.

# These Common Conditions Apply to Specific Emission Units as Referenced in this Permit.

- i. The start and stop time and date of the flaring event.
- ii. The length of time in minutes for which emissions were visible from the flare during the event.
- iii. For steam-assisted, air-assisted, and non-assisted flares, the start date, start time, and duration in minutes for periods of time that the flare tip velocity exceeds the maximum flare tip velocity determined using the methods in 40 CFR 63.670(d)(2) of subpart CC and the maximum 15-minute block average flare tip velocity in ft/sec recorded during the event.
- iv. Results of the root cause and corrective actions analysis completed during the reporting period, including the corrective actions implemented during the reporting period and, if applicable, the implementation schedule for planned corrective actions to be implemented subsequent to the reporting period.
- For bypass lines subject to the requirements 40 CFR 63.2450(e)(6), the compliance report must include the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours.
- m. For any maintenance vent release exceeding the applicable limits in 40 CFR 63.2450(v)(1), the compliance report must include the information specified in paragraphs (e)(14)(i) through (iv) of 40 CFR 63.2520(e)(14). For the purposes of this reporting requirement, if you comply with 40 CFR 63.2450(v)(1)(iv) then you must report each venting event conducted under those provisions and include an explanation for each event as to why utilization of this alternative was required.
  - (1) Identification of the maintenance vent and the equipment served by the maintenance vent.
  - (2) The date and time the maintenance vent was opened to the atmosphere.
  - (3) The lower explosive limit in percent, vessel pressure in psig, or mass in pounds of VOC in the equipment, as applicable, at the start of atmospheric venting. If the 5 psig vessel pressure option in 40 CFR 63.2450(v)(1)(ii) was used and active purging was initiated while the concentration of the vapor was 10 percent or greater of its LEL, also include the concentration of the vapors at the time active purging was initiated.
  - (4) An estimate of the mass in pounds of organic HAP released during the entire atmospheric venting event.
- n. Compliance reports for pressure relief devices subject to the requirements 40 CFR 63.2480(e) must include the information specified in paragraphs (e)(15)(i) through (iii) of 40 CFR 63.2520(e)(15).
  - (1) For pressure relief devices in organic HAP gas or vapor service, pursuant to 40 CFR 63.2480(e)(1), report the instrument readings and dates for all readings of 500 ppmv or greater.
  - (2) For pressure relief devices in organic HAP gas or vapor service subject to 40 CFR 63.2480(e)(2), report the instrument readings and dates of instrument monitoring conducted.
  - (3) For pressure relief devices in organic HAP service subject to 40 CFR 63.2480(e)(3), report each pressure release to the atmosphere, including the start date, start time, and duration in minutes of the pressure release and an estimate of the mass quantity in pounds of each organic HAP released; the results of any root cause analysis and corrective action analysis completed during the reporting period, including the corrective actions implemented during the reporting period; and, if applicable, the implementation schedule for planned corrective actions to be implemented subsequent to the reporting period.

[Rule 62-204.800(11), F.A.C., and 40 CFR 63.2520(e)] <sup>1</sup> Back to Table of Contents

#### SECTION V. APPENDICES.

### The Following Appendices Are Enforceable Parts of This Permit:

Appendix A, Abbreviations, Acronyms, Citations, and Identification Numbers. Appendix I, List of Insignificant Emissions Units and/or Activities. Appendix NESHAP, Subpart A - NESHAP General Provisions. Appendix NESHAP, Subpart DDDDD - NESHAP for Boilers and Process Heaters. Appendix NESHAP, Subpart F - NESHAP for the Synthetic Organic Chemical Manufacturing Industry. Appendix NESHAP, Subpart FFFF - NESHAP for Miscellaneous Organic Chemical Manufacturing. Appendix NESHAP, Subpart G - NESHAP for Process Vents-Stg Vessels-Transfer Ops-Wastewater. Appendix NESHAP, Subpart H - NESHAP for Equipment Leaks. Appendix NESHAP, Subpart ZZZZ - NESHAP for Stationary Reciprocating Internal Combustion Engines. Appendix NSPS, Subpart A - General Provisions. Appendix NSPS, Subpart Kb - NSPS for Volatile Organic Liquid Storage Vessels After July 23, 1984. Appendix NSPS, Subpart IIII - Standards of Performance for Stationary CI RICE. Appendix NSPS, Subpart VVa - NSPS for Equipment Leaks of VOC After November 7, 2006. Appendix RR, Facility-wide Reporting Requirements. Appendix TR, Facility-wide Testing Requirements. Appendix TV, Title V General Conditions. Appendix U, List of Unregulated Emissions Units and/or Activities.

Referenced Attachments (Not Enforceable - Included for Convenience and Informational Purposes Only):

 Figure 1 - Summary Report-Gaseous and Opacity Excess Emission and Monitoring System Performance (40 CFR 60, July, 1996).

 Table H - Permit History.

 Time Sensitive Action Chart.

 Table 1 - Summary of Applicable Requirements and Compliance Procedures.

 Figure 2 - Project Emissions Increase Report - Example Format.

### ABBREVIATIONS, ACRONYMS, CITATIONS AND IDENTIFICATION NUMBERS

**Abbreviations and Acronyms:** °F: degrees Fahrenheit acfm: actual cubic feet per minute AOR: Annual Operating Report **ARMS**: Air Resource Management System (Department's database) **BACT**: best available control technology **BHP**: brake horsepower **Btu:** British thermal units CAA: Clean Air Act CAAA: Clean Air Act Amendments of 1990 CAM: compliance assurance monitoring **CEMS**: continuous emissions monitoring system cfm: cubic feet per minute CFR: Code of Federal Regulations **CI**: compression ignition CO: carbon monoxide COMS: continuous opacity monitoring system **DARM**: Division of Air Resource Management **DCA**: Department of Community Affairs **DEP**: Department of Environmental Protection Department: Department of Environmental Protection dscfm: dry standard cubic feet per minute **EPA:** Environmental Protection Agency ESP: electrostatic precipitator (control system for reducing particulate matter) EU: emissions unit F.A.C.: Florida Administrative Code F.D.: forced draft **F.S.**: Florida Statutes FGR: flue gas recirculation Fl: fluoride ft<sup>2</sup>: square feet ft<sup>3</sup>: cubic feet g: grams gpm: gallons per minute gr: grains HAP: hazardous air pollutant **HP**: horsepower Hg: mercury ICE: internal combustion engine **I.D.**: induced draft **ID**: identification **ISO:** International Standards Organization (refers to those conditions at 288 Kelvin, 60% relative humidity and 101.3 kilopascals pressure.) **kPa**: kilopascals **kW**: kilowatts LAT: Latitude **lb**: pound **lbs/hr**: pounds per hour LONG: Longitude MACT: maximum achievable technology **mm**: millimeter MMBtu: million British thermal units MSDS: material safety data sheets MW: megawatt

NESHAP: National Emissions Standards for Hazardous Air Pollutants NOx: nitrogen oxides NSPS: New Source Performance Standards **O&M**: operation and maintenance O<sub>2</sub>: oxygen **ORIS:** Office of Regulatory Information Systems **OS**: Organic Solvent **Pb**: lead **PM**: particulate matter PM<sub>10</sub>: particulate matter with a mean aerodynamic diameter of 10 microns or less **PSD**: prevention of significant deterioration **psi**: pounds per square inch PTE: potential to emit RACT: reasonably available control technology RATA: relative accuracy test audit **RICE**: reciprocating internal combustion engine **RMP**: Risk Management Plan **RO**: Responsible Official SAM: sulfuric acid mist **scf**: standard cubic feet scfm: standard cubic feet per minute SI: spark ignition SIC: standard industrial classification code SNCR: selective non-catalytic reduction (control system used for reducing emissions of nitrogen oxides) **SOA:** Specific Operating Agreement SO<sub>2</sub>: sulfur dioxide TPH: tons per hour TPY: tons per year UTM: Universal Transverse Mercator coordinate system **VE**: visible emissions **VOC:** volatile organic compounds **x**: By or times

### APPENDIX A

# ABBREVIATIONS, ACRONYMS, CITATIONS AND IDENTIFICATION NUMBERS

# **<u>Citations</u>:**

The following exc	imples illustrate the method	ds used in this permit to abbreviate and cite the references of rules, regulations,		
guidance memore	andums, permit numbers ar	nd ID numbers.		
Code of Federal I	<u>Regulations</u> :			
<i>Example</i> : Whe	[40 CFR 60.334]			
whe	40 refers to	Title 40		
	CFR refers to	Code of Federal Regulations		
	60 refers to	Part 60		
	60 334 refers to	Regulation 60 334		
Florida Administ	rative Code ( $\mathbf{F} \wedge \mathbf{C}$ ) Rules			
Example:	IRule 62-213 205 F A C			
Whe	[Kult 02-215.205, F.A.C.	1		
vv ne	62	rafare to Title 62		
	62 213	refers to Chapter 62 212		
	62 213 205	refers to Chapter 02-215		
	02-213.203	Teleis to Rule 02-213.203, F.A.C.		
Identification N	umhers			
Eacility Identifica	ation (ID) Number:			
<u>Frampla</u>	Eacility ID No $\cdot$ 1050221			
Whe	re.			
vv ne	105 = 3 digit num	her code identifying the facility is located in Polk County		
	0221 = 4-digit num	nber assigned by state database		
Permit Numbers	0221 - 4-digit liu	noer assigned by state database.		
Frampla:	1050221 002 AV or			
Example.	1050221-002-AV, 01			
When	1050221-001-AC			
W IIC.		Air Construction Dormit		
	AC -	Air Construction Permit		
	AV = 105	All Operation Ferning (The V Source)		
	103 -	4 digit number code identifying the facility is located in Fork County		
	0221 - 001  or  002 - 002 - 0000  or  0000  or  0000  or  00000  or  0000000000000000000000000000000000	4-digit number assigned by permit tracking database		
Example	001 01 002 -	5-digit sequential project number assigned by permit tracking database		
Example.	PA05 01			
	PA95-01			
33.71	AC53-208321			
when		Descention of Simificant Details action Demuit		
	PSD =	Prevention of Significant Deterioration Permit		
	PA =	Power Plant Siting Act Permit		
	AC53 =	old Air Construction Permit numbering identifying the facility is located in Polk		
		County		
A Back to Table	of Contents	•		
	<u>or contents</u>			
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#### APPENDIX I

### LIST OF INSIGNIFICANT EMISSIONS UNITS AND/OR ACTIVITIES

The facilities, emissions units, or pollutant-emitting activities listed in Rule 62-210.300(3)(a), F.A.C., <u>Categorical Exemptions</u>, or that meet the criteria specified in Rule 62-210.300(3)(b)1., F.A.C., <u>Generic Emissions Unit Exemption</u>, are exempt from the permitting requirements of Chapters 62-210, 62-212 and 62-4, F.A.C.; provided, however, that exempt emissions units shall be subject to any applicable emission limiting standards and the emissions from exempt emissions units or activities shall be considered in determining the potential emissions of the facility containing such emissions units. Emissions units and pollutant-emitting activities exempt from permitting under Rules 62-210.300(3)(a) and (b)1., F.A.C., shall not be exempt from the permitting requirements of Chapter 62-213, F.A.C., if they are contained within a Title V source; however, such emissions units and activities shall be considered insignificant for Title V purposes provided they also meet the criteria of Rule 62-213.430(6)(b), F.A.C. No emissions unit shall be entitled to an exemption from permitting under Rules 62-210.300(3)(a) and (b)1., F.A.C., if its emissions, in combination with the emissions of other units and activities at the facility, would cause the facility to emit or have the potential to emit any pollutant in such amount as to make the facility a Title V source.

The below listed emissions units and/or activities are considered insignificant pursuant to Rule 62-213.430(6), F.A.C.

Brief Description of Emissions Units and/or Activities

Activity	Description	Justification of Status		
Boilers Area				
Fugitives	Emissions from equipment leaks in the boilers area	No regulated pollutants		
Non-Product Tanks	TK-24018; D-24003; TK-24012; D-24009; D-24015A/B; TK-24001; TK-24020; D-24023; D-24020	Low emissions and no applicable requirements.		
Soot blowing	Emissions from boiler soot blowing 116j	NA—Covered by facility requirement FAC62- 210.700(3)		
	Methylamines #1 and Methanol Storage and Methylami	ines #4		
Vent Scrubber	Vent from T-67123 to flare	Product recovery device, no applicable requirements		
Methylamines #1 and #4 Unregulated Process equipment	Process equipment used to produce methylamines not regulated under HON (such as distillation, separation columns)	Product recovery device, no applicable requirements		
Acetic Acid Scrubber	Vent from T-67125 used to control odors during preparation of equipment for safe maintenance or when purging sample lines of residual material following manual sample collection	Emissions below threshold and no applicable requirements		
Methylamines #1 and #4 Non HON Maintenance Wastewater	Fluids drained from non-methanol containing process equipment during preparation for mechanical work.	Covered by FAC 62-210.700.		
Methylamines #1 and #4 Non- Regulated Storage Tanks	D-67001; D-67101; D-67103; D-67105A,B; D-67106A,B; D- 67107A,B; D-67110A,B; D-67112A,B; D- 67116A,B,C,D,O,R,S; D-67117; D67134A,B,C; D- 67137A,B; D-67203A,B,C,D; D-67204A,B,C,D,E; D-67205; D-67207; D-67215; D-67216A,B; D-67019B; D-67204A; D- 67025A,B	Low emissions and no applicable requirements, all tanks vent to the flare.		
Non-Product Tanks	D-67102; D-67130; TK-67004; D-24101B; D-67136; D- 68136; D-68139; D-67034; D-67014; GN-8004; D-67044; D- 67045; D-67043; D-67047; D-67140; D-67147; D-67142; D-	Low emissions and no applicable requirements. D-67102 and D-67130 vent to an absorber then flare.		

# APPENDIX I LIST OF INSIGNIFICANT EMISSIONS UNITS AND/OR ACTIVITIES

Activity	Description	Justification of Status			
	67141; D-67139; D-67127; D-67159				
Non-HON Shutdown Losses	Emissions from clearing non-MeOH containing equipment	NA—Covered by facility requirement FAC62-			
	for Inspection/repair downtime	210.700.			
Methylamines #1 and #4 Loading	Methylamines loading is closed dome	Very low emissions and no regulations.			
		Emissions are vented to the flare for odor control.			
#4 Plant Steam Eductor	Used to evacuate lines, condensate flows to Low Pressure Absorber	Low emissions, no regulations			
Railcar Cleaning	-	Low emissions and no regulations, routed to flare			
	Higher Amines and Batch Still				
Gas Chromatograph	-	Low emissions, no regulations			
Higher Amines Non-HON	Fluids drained from equipment which is not in HAP service	Covered by FAC 62-210.700			
Maintenance Wastewater	during preparation for mechanical work				
Drum Cleaning	Emissions from rinsing or steaming RCRA empty drums	Low emissions, no regulations			
	formerly containing amines, oil, water treatment chemicals,				
	MEK, MeOH, or dielectron blue solvent				
	DIMLA Plant				
DIMLA Plant Non-Regulated Storage	TK-62101, TK-62102, TK-62103, TK-62190, TK-62191,	Low emissions and no applicable requirements.			
Tanks	TK-62192, TK-62193, TK-62194, TK-62168, TK-62090,	Will be listed as an insignificant source of			
	TK-62091, TK-62092, TK-62099, TK-62025	emissions.			
DIMLA Purification	DIMLA purification absorber (T-62028)	The DIMLA Plant Absorber is considered a			
		product recovery device under MON, so there are			
		no applicable requirements. Very small emissions			
		(<<0.1 tpy VOC) and will be listed as an			
		insignificant source of emissions.			
DIMLA Non-regulated Process	DIMLA non-MON and non-NSPS fugitive leaks.	No regulated pollutants			
Equipment					
	General Plant	$E^{-1} = \frac{1}{2} + \frac{1}{$			
Wastewater Treatment Methanol	Use of methanol in Echo Pond of Equalization Basin to	Emission below threshold (200 lb/yr)			
Audition System	D (8127 uses soft a side issues flades into furiture	Deserved west the definition of CMDU as listed in			
Amines waste Treatment Tanks	D-68127 – uses acetic acid to increase flashpoint of mixture	Does not meet the definition of CMPU as listed in			
	of water, animolia, and various amines; D-08140	40 CFR 05, vents to hare with low emissions,			
		requirements.			
Non-Product Tanks	D-67116E,I,M,Q,U; D-68140; D-30206A,B; D-30210; D-	Low emissions, no applicable requirements. D-			
	30202; D-30327; D-30204; D-30218; D-24018; D-24108;	30206A,B are pressurized and vapors during			
	TK-11201; TK-24109; TK-24014; TK-24019; TK-24017; D-	loading/unloading are vented back to tanks.			
	24021; D-11207; TK-53406; D-67160; TK-32008; 30.21				
Plant Grounds Maintenance	Includes lawn mowing, hedge trimming, weed eating, leaf	Trivial list			

### APPENDIX I LIST OF INSIGNIFICANT EMISSIONS UNITS AND/OR ACTIVITIES

Activity	Description	Justification of Status
	blowing, tree trimming, etc., plus application of fertilizers, pesticides, herbicides, and fungicides.	
Degreasing	Soaking parts in low vapor pressure, non-halogenated solvent for degreasing.	Covered by 62-213.420(3)(c)3.b.
Sandblasting	Abrasive blasting performed on equipment in the field using sand or grit; may be tarped but not totally enclosed	No applicable requirements, emissions below threshold
Emergency Generators (5)	Diesel powered generators used to supply emergency electrical power	Less than 32,000 gal of fuel used as per FAC 62- 210.300(3)(a)20.b
Construction Activities	Construction of buildings and structures using equipment ranging from hand tools to heavy equipment such as bulldozers and large cranes	Trivial emissions
Cook Outs	Emissions from cooking out for recreational purposes; includes bar-b-q, fish fry and crawfish boils	Trivial emissions
Unloading Sandblast Grit	Particulate emissions from sand/grit during unloading of new deliveries	Low emissions and no regulations
Motor Vehicle Fuel Tanks (4)	Emissions from fuel tanks used to store motor vehicle fuel (gasoline and diesel)	Low emissions and no regulations
Emergency Generator Fuel Tanks (5)	Emissions from tanks used to store diesel emergency generator fuel	Low emissions and no regulations
Water Treatment Chemicals Storage and Use	Storage and use of water treatment chemicals (Note: some containers may contain small amounts of VOC)	No regulated pollutants or very low emissions
Bead Blasting	Totally enclosed shop sand blasting using equipment with filter	No unconfined emissions
Steam Vents	Various vents used for venting excess steam	No regulated pollutants
Indoor Fugitives	Use of cleaning supplies, office supplies, and storage of such materials in closed containers; copy machines	Trivial
Fire Training and Emergency Response	Emergency response and training using dry chemical extinguishers, CO2, water and simulated fires using propane as fuel.	Covered by FAC62-256.700(4)
Sulfuric Acid Tanks	Tanks used for storage of sulfuric acid for water treatment	No regulated pollutants
Vehicle Maintenance	Maintenance on vehicles including oil changes, radiator flushing and parts cleaning	Materials handled in closed containers
Laboratories	Fume hoods and other activities associated with quality control, environmental, and unit analytical labs located at control rooms	62-210-300(3) exempts analytical laboratories
Portable Scrubber	Used as needed.	Emissions below threshold. No applicable requirements
Road Maintenance	Paving or patching with asphalt, concrete, or grading dirt/clay	Trivial list

# APPENDIX I LIST OF INSIGNIFICANT EMISSIONS UNITS AND/OR ACTIVITIES

Activity	Description	Justification of Status
Materials Storage	Storage of VOC or HAP containing materials in closed	Trivial list
	containers	
Solvent Recycling Equipment	Totally enclosed equipment used for the small scale	Negligible emissions and no regulations
	recycling/recovering of spent solvents	
Fuel Loading/Unloading	Emissions from unloading fuel from trucks and from fueling	Low emissions and no regulations
	vehicles	
Oil Tank Vents	Vents from oil storage tanks	Low emissions and no regulations
Leak Check with SO2 gas	Using a cylinder of SO2 to spray on mechanical components	Negligible emissions and no regulations
	to check for leaks	
Oil Decanter	Decanter used to remove water from used oil	Low emissions and no regulations
Laboratory Vent Scrubber	Acetic acid scrubber used to control odors form the QC lab	Low emissions and no regulations

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### Subpart A—General Provisions

Source:

59 FR 12430, Mar. 16, 1994, unless otherwise noted.

# § 63.1 Applicability.

### (a) General.

(1) Terms used throughout this part are defined in  $\S 63.2$  or in the Clean Air Act (Act) as amended in 1990, except that individual subparts of this part may include specific definitions in addition to or that supersede definitions in  $\S 63.2$ .

(2) This part contains national emission standards for hazardous air pollutants (NESHAP) established pursuant to section 112 of the Act as amended November 15, 1990. These standards regulate specific categories of stationary sources that emit (or have the potential to emit) one or more hazardous air pollutants listed in this part pursuant to section 112(b) of the Act. This section explains the applicability of such standards to sources affected by them. The standards in this part are independent of NESHAP contained in <u>40 CFR part 61</u>. The NESHAP in part 61 promulgated by signature of the Administrator before November 15, 1990 (i.e., the date of enactment of the Clean Air Act Amendments of 1990) remain in effect until they are amended, if appropriate, and added to this part.

(3) No emission standard or other requirement established under this part shall be interpreted, construed, or applied to diminish or replace the requirements of a more stringent emission limitation or other applicable requirement established by the Administrator pursuant to other authority of the Act (section 111, part C or D or any other authority of this Act), or a standard issued under State authority. The Administrator may specify in a specific standard under this part that facilities subject to other provisions under the Act need only comply with the provisions of that standard.

(4)

(i) Each relevant standard in this part 63 must identify explicitly whether each provision in this subpart A is or is not included in such relevant standard.

(ii) If a relevant part 63 standard incorporates the requirements of <u>40 CFR part 60</u>, part 61 or other part 63 standards, the relevant part 63 standard must identify explicitly the applicability of each corresponding part 60, part 61, or other part 63 subpart A (General) provision.

(iii) The General Provisions in this subpart A do not apply to regulations developed pursuant to section 112(r) of the amended Act, unless otherwise specified in those regulations.

(5) [Reserved]

(6) To obtain the most current list of categories of sources to be regulated under section 112 of the Act, or to obtain the most recent regulation promulgation schedule established pursuant to section 112(e) of the Act, contact the Office of the Director, Emission Standards Division, Office of Air Quality Planning and Standards, U.S. EPA (MD-13), Research Triangle Park, North Carolina 27711.

# (7)-(9) [Reserved]

(10) For the purposes of this part, time periods specified in days shall be measured in calendar days, even if the word "calendar" is absent, unless otherwise specified in an applicable requirement.

(11) For the purposes of this part, if an explicit postmark deadline is not specified in an applicable requirement for the submittal of a notification, application, test plan, report, or other written communication to the Administrator, the owner or operator shall postmark the submittal on or before the number of days specified in the applicable requirement. For example, if a notification must be submitted 15 days before a particular event is scheduled to take place, the notification shall be postmarked on or before 15 days preceding the event; likewise, if a notification must be submitted 15 days after a particular event takes place, the notification shall be postmarked on or before 15 days following the end of the event. The use of reliable non-Government mail carriers that provide indications of verifiable delivery of information required to be submitted to the Administrator, similar to the postmark provided by the U.S. Postal Service, or alternative means of delivery agreed to by the permitting authority, is acceptable.

(12) Notwithstanding time periods or postmark deadlines specified in this part for the submittal of information to the Administrator by an owner or operator, or the review of such information by the Administrator, such time periods or

deadlines may be changed by mutual agreement between the owner or operator and the Administrator. Procedures governing the implementation of this provision are specified in  $\S 63.9(i)$ .

(b) Initial applicability determination for this part.

(1) The provisions of this part apply to the owner or operator of any stationary source that-

(i) Emits or has the potential to emit any hazardous air pollutant listed in or pursuant to section 112(b) of the Act; and

(ii) Is subject to any standard, limitation, prohibition, or other federally enforceable requirement established pursuant to this part.

### (2) [Reserved]

(3) An owner or operator of a stationary source who is in the relevant source category and who determines that the source is not subject to a relevant standard or other requirement established under this part must keep a record as specified in  $\S$  <u>63.10(b)(3)</u>.

(c) *Applicability of this part after a relevant standard has been set under this part.* 

(1) If a relevant standard has been established under this part, the owner or operator of an affected source must comply with the provisions of that standard and of this subpart as provided in <u>paragraph (a)(4)</u> of this section.

(2) Except as provided in  $\S$  <u>63.10(b)(3)</u>, if a relevant standard has been established under this part, the owner or operator of an affected source may be required to obtain a title V permit from a permitting authority in the State in which the source is located. Emission standards promulgated in this part for area sources pursuant to section 112(c)(3) of the Act will specify whether—

(i) States will have the option to exclude area sources affected by that standard from the requirement to obtain a title V permit (i.e., the standard will exempt the category of area sources altogether from the permitting requirement);

(ii) States will have the option to defer permitting of area sources in that category until the Administrator takes rulemaking action to determine applicability of the permitting requirements; or

(iii) If a standard fails to specify what the permitting requirements will be for area sources affected by such a standard, then area sources that are subject to the standard will be subject to the requirement to obtain a title V permit without any deferral.

# (3)-(4) [Reserved]

(5) If an area source that otherwise would be subject to an emission standard or other requirement established under this part if it were a major source subsequently increases its emissions of hazardous air pollutants (or its potential to emit hazardous air pollutants) such that the source is a major source that is subject to the emission standard or other requirement, such source also shall be subject to the notification requirements of this subpart.

(6) A major source may become an area source at any time upon reducing its emissions of and potential to emit hazardous air pollutants, as defined in this subpart, to below the major source thresholds established in  $\S$  63.2, subject to the provisions in paragraphs (c)(6)(i) and (ii) of this section.

(i) A major source reclassifying to area source status is subject to the applicability of standards, compliance dates and notification requirements specified in (c)(6)(i)(A) of this section. An area source that previously was a major source and becomes a major source again is subject to the applicability of standards, compliance dates, and notification requirements specified in (c)(6)(i)(B) of this section:

(B) An area source that previously was a major source under this part and that becomes a major source again is subject to the applicable major source requirements established under this part immediately upon becoming a major source again, provided the compliance date for the major source requirements has passed, notwithstanding any provision within the applicable subparts. The owner or operator of an area source that becomes a major source again must comply with the initial notification

pursuant to  $\S$  <u>63.9(b)</u>. The owner or operator must also provide to the Administrator any change in the information already provided under  $\S$  <u>63.9(b)</u> per  $\S$  <u>63.9(j)</u>.

(ii) Becoming an area source does not absolve a source subject to an enforcement action or investigation for major source violations or infractions from the consequences of any actions occurring when the source was major. Becoming a major source does not absolve a source subject to an enforcement action or investigation for area source violations or infractions from the consequences of any actions occurring when the source was an area source.

(iii) After September 10, 2024, affected sources subject to the following <u>40 CFR part 63 subparts on</u> September 10, 2024, must remain subject to those subparts, and any modifications thereafter, even if the source becomes an area source by reducing both its actual emissions and potential to emit hazardous air pollutants to below major source thresholds: F, G, H, I, L, R, X, CC, GG, II, JJ, KK, LL, MM, EEE, JJJ, LLL, MMM, RRR, UUU, FFFF, JJJJ, MMMM, PPPP, ZZZZ, CCCCC, DDDDD, FFFFF, IIIII, LLLLL, YYYYY, JJJJJJ, EEEEEEE.

(d) [Reserved]

(e) If the Administrator promulgates an emission standard under section 112(d) or (h) of the Act that is applicable to a source subject to an emission limitation by permit established under section 112(j) of the Act, and the requirements under the section 112(j) emission limitation are substantially as effective as the promulgated emission standard, the owner or operator may request the permitting authority to revise the source's title V permit to reflect that the emission limitation in the permit satisfies the requirements of the promulgated emission standard. The process by which the permitting authority determines whether the section 112(j) emission limitation is substantially as effective as the promulgated emission standard must include, consistent with part 70 or 71 of this chapter, the opportunity for full public, EPA, and affected State review (including the opportunity for EPA's objection) prior to the permit revision being finalized. A negative determination by the permitting authority constitutes final action for purposes of review and appeal under the applicable title V operating permit program.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>67 FR 16595</u>, Apr. 5, 2002; <u>85 FR 73885</u>, Nov. 19, 2020; <u>89 FR 73307</u>, Sept. 10, 2024; <u>90 FR 1041</u>, Jan. 7, 2025]

### § 63.2 Definitions.

The terms used in this part are defined in the Act or in this section as follows:

Act means the Clean Air Act (42 U.S.C. 7401 et seq., as amended by Pub. L. 101-549, 104 Stat. 2399).

Actual emissions is defined in <u>subpart D of this part</u> for the purpose of granting a compliance extension for an early reduction of hazardous air pollutants.

*Administrator* means the Administrator of the United States Environmental Protection Agency or his or her authorized representative (e.g., a State that has been delegated the authority to implement the provisions of this part).

*Affected source,* for the purposes of this part, means the collection of equipment, activities, or both within a single contiguous area and under common control that is included in a section 112(c) source category or subcategory for which a section 112(d) standard or other relevant standard is established pursuant to section 112 of the Act. Each relevant standard will define the "affected source," as defined in this paragraph unless a different definition is warranted based on a published justification as to why this definition would result in significant administrative, practical, or implementation problems and why the different definition would resolve those problems. The term "affected source," as used in this part, is separate and distinct from any other use of that term in EPA regulations such as those implementing title IV of the Act. Affected source may be defined differently for part 63 than affected facility and stationary source in parts 60 and 61, respectively. This definition of "affected source," and the procedures for adopting an alternative definition of "affected source," shall apply to each section 112(d) standard for which the initial proposed rule is signed by the Administrator after June 30, 2002.

Alternative emission limitation means conditions established pursuant to sections 112(i)(5) or 112(i)(6) of the Act by the Administrator or by a State with an approved permit program.

*Alternative emission standard* means an alternative means of emission limitation that, after notice and opportunity for public comment, has been demonstrated by an owner or operator to the Administrator's satisfaction to achieve a reduction in emissions of any air pollutant at least equivalent to the reduction in emissions of such pollutant achieved under a relevant design, equipment, work practice, or operational emission standard, or combination thereof, established under this part pursuant to section 112(h) of the Act.

*Alternative test method* means any method of sampling and analyzing for an air pollutant that has been demonstrated to the Administrator's satisfaction, using Method 301 in <u>appendix A of this part</u>, to produce results adequate for the Administrator's determination that it may be used in place of a test method specified in this part.

*Approved permit program* means a State permit program approved by the Administrator as meeting the requirements of <u>part</u> <u>70 of this chapter</u> or a Federal permit program established in this chapter pursuant to title V of the Act (<u>42 U.S.C. 7661</u>).

Area source means any stationary source of hazardous air pollutants that is not a major source as defined in this part.

*Commenced* means, with respect to construction or reconstruction of an affected source, that an owner or operator has undertaken a continuous program of construction or reconstruction or that an owner or operator has entered into a contractual obligation to undertake and complete, within a reasonable time, a continuous program of construction or reconstruction.

*Compliance date* means the date by which an affected source is required to be in compliance with a relevant standard, limitation, prohibition, or any federally enforceable requirement established by the Administrator (or a State with an approved permit program) pursuant to section 112 of the Act.

### *Compliance schedule* means:

(1) In the case of an affected source that is in compliance with all applicable requirements established under this part, a statement that the source will continue to comply with such requirements; or

(2) In the case of an affected source that is required to comply with applicable requirements by a future date, a statement that the source will meet such requirements on a timely basis and, if required by an applicable requirement, a detailed schedule of the dates by which each step toward compliance will be reached; or

(3) In the case of an affected source not in compliance with all applicable requirements established under this part, a schedule of remedial measures, including an enforceable sequence of actions or operations with milestones and a schedule for the submission of certified progress reports, where applicable, leading to compliance with a relevant standard, limitation, prohibition, or any federally enforceable requirement established pursuant to section 112 of the Act for which the affected source is not in compliance. This compliance schedule shall resemble and be at least as stringent as that contained in any judicial consent decree or administrative order to which the source is subject. Any such schedule of compliance shall be supplemental to, and shall not sanction noncompliance with, the applicable requirements on which it is based.

*Construction* means the on-site fabrication, erection, or installation of an affected source. Construction does not include the removal of all equipment comprising an affected source from an existing location and reinstallation of such equipment at a new location. The owner or operator of an existing affected source that is relocated may elect not to reinstall minor ancillary equipment including, but not limited to, piping, ductwork, and valves. However, removal and reinstallation of an affected source will be construed as reconstruction if it satisfies the criteria for reconstruction as defined in this section. The costs of replacing minor ancillary equipment must be considered in determining whether the existing affected source is reconstructed.

*Continuous emission monitoring system* (CEMS) means the total equipment that may be required to meet the data acquisition and availability requirements of this part, used to sample, condition (if applicable), analyze, and provide a record of emissions.

*Continuous monitoring system* (CMS) is a comprehensive term that may include, but is not limited to, continuous emission monitoring systems, continuous opacity monitoring systems, continuous parameter monitoring systems, or other manual or automatic monitoring that is used for demonstrating compliance with an applicable regulation on a continuous basis as defined by the regulation.

*Continuous opacity monitoring system* (COMS) means a continuous monitoring system that measures the opacity of emissions.

*Continuous parameter monitoring system* means the total equipment that may be required to meet the data acquisition and availability requirements of this part, used to sample, condition (if applicable), analyze, and provide a record of process or control system parameters.

### *Effective date* means:

(1) With regard to an emission standard established under this part, the date of promulgation in the Federal Register of such standard; or
(2) With regard to an alternative emission limitation or equivalent emission limitation determined by the Administrator (or a State with an approved permit program), the date that the alternative emission limitation or equivalent emission limitation becomes effective according to the provisions of this part.

*Emission standard* means a national standard, limitation, prohibition, or other regulation promulgated in a subpart of this part pursuant to sections 112(d), 112(h), or 112(f) of the Act.

*Emissions averaging* is a way to comply with the emission limitations specified in a relevant standard, whereby an affected source, if allowed under a subpart of this part, may create emission credits by reducing emissions from specific points to a level below that required by the relevant standard, and those credits are used to offset emissions from points that are not controlled to the level required by the relevant standard.

EPA means the United States Environmental Protection Agency.

Equivalent emission limitation means any maximum achievable control technology emission limitation or requirements which are applicable to a major source of hazardous air pollutants and are adopted by the Administrator (or a State with an approved permit program) on a case-by-case basis, pursuant to section 112(g) or (j) of the Act.

Excess emissions and continuous monitoring system performance report is a report that must be submitted periodically by an affected source in order to provide data on its compliance with relevant emission limits, operating parameters, and the performance of its continuous parameter monitoring systems.

Existing source means any affected source that is not a new source.

Federally enforceable means all limitations and conditions that are enforceable by the Administrator and citizens under the Act or that are enforceable under other statutes administered by the Administrator. Examples of federally enforceable limitations and conditions include, but are not limited to:

(1) Emission standards, alternative emission standards, alternative emission limitations, and equivalent emission limitations established pursuant to section 112 of the Act as amended in 1990;

(2) New source performance standards established pursuant to section 111 of the Act, and emission standards established pursuant to section 112 of the Act before it was amended in 1990;

(3) All terms and conditions in a title V permit, including any provisions that limit a source's potential to emit, unless expressly designated as not federally enforceable;

(4) Limitations and conditions that are part of an approved State Implementation Plan (SIP) or a Federal Implementation Plan (FIP);

(5) Limitations and conditions that are part of a Federal construction permit issued under 40 CFR 52.21 or any construction permit issued under regulations approved by the EPA in accordance with 40 CFR part 51;

(6) Limitations and conditions that are part of an operating permit where the permit and the permitting program pursuant to which it was issued meet all of the following criteria:

(i) The operating permit program has been submitted to and approved by EPA into a State implementation plan (SIP) under section 110 of the CAA:

(ii) The SIP imposes a legal obligation that operating permit holders adhere to the terms and limitations of such permits and provides that permits which do not conform to the operating permit program requirements and the requirements of EPA's underlying regulations may be deemed not "federally enforceable" by EPA;

(iii) The operating permit program requires that all emission limitations, controls, and other requirements imposed by such permits will be at least as stringent as any other applicable limitations and requirements contained in the SIP or enforceable under the SIP, and that the program may not issue permits that waive, or make less stringent, any limitations or requirements contained in or issued pursuant to the SIP, or that are otherwise "federally enforceable";

(iv) The limitations, controls, and requirements in the permit in question are permanent, quantifiable, and otherwise enforceable as a practical matter; and

(v) The permit in question was issued only after adequate and timely notice and opportunity for comment for EPA and the public.

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(7) Limitations and conditions in a State rule or program that has been approved by the EPA under <u>subpart E of this part</u> for the purposes of implementing and enforcing section 112; and

(8) Individual consent agreements that the EPA has legal authority to create.

Fixed capital cost means the capital needed to provide all the depreciable components of an existing source.

*Force majeure* means, for purposes of  $\S$  <u>63.7</u>, an event that will be or has been caused by circumstances beyond the control of the affected facility, its contractors, or any entity controlled by the affected facility that prevents the owner or operator from complying with the regulatory requirement to conduct performance tests within the specified timeframe despite the affected facility's best efforts to fulfill the obligation. Examples of such events are acts of nature, acts of war or terrorism, or equipment failure or safety hazard beyond the control of the affected facility.

*Fugitive emissions* means those emissions from a stationary source that could not reasonably pass through a stack, chimney, vent, or other functionally equivalent opening. Under section 112 of the Act, all fugitive emissions are to be considered in determining whether a stationary source is a major source.

Hazardous air pollutant means any air pollutant listed in or pursuant to section 112(b) of the Act.

*Issuance* of a part 70 permit will occur, if the State is the permitting authority, in accordance with the requirements of <u>part 70</u> <u>of this chapter</u> and the applicable, approved State permit program. When the EPA is the permitting authority, issuance of a title V permit occurs immediately after the EPA takes final action on the final permit.

*Major source* means any stationary source or group of stationary sources located within a contiguous area and under common control that emits or has the potential to emit considering controls, in the aggregate, 10 tons per year or more of any hazardous air pollutant or 25 tons per year or more of any combination of hazardous air pollutants, unless the Administrator establishes a lesser quantity, or in the case of radionuclides, different criteria from those specified in this sentence.

*Malfunction* means any sudden, infrequent, and not reasonably preventable failure of air pollution control and monitoring equipment, process equipment, or a process to operate in a normal or usual manner which causes, or has the potential to cause, the emission limitations in an applicable standard to be exceeded. Failures that are caused in part by poor maintenance or careless operation are not malfunctions.

*Monitoring* means the collection and use of measurement data or other information to control the operation of a process or pollution control device or to verify a work practice standard relative to assuring compliance with applicable requirements. Monitoring is composed of four elements:

(1) Indicator(s) of performance—the parameter or parameters you measure or observe for demonstrating proper operation of the pollution control measures or compliance with the applicable emissions limitation or standard. Indicators of performance may include direct or predicted emissions measurements (including opacity), operational parametric values that correspond to process or control device (and capture system) efficiencies or emissions rates, and recorded findings of inspection of work practice activities, materials tracking, or design characteristics. Indicators may be expressed as a single maximum or minimum value, a function of process variables (for example, within a range of pressure drops), a particular operational or work practice status (for example, a damper position, completion of a waste recovery task, materials tracking), or an interdependency between two or among more than two variables.

(2) Measurement techniques—the means by which you gather and record information of or about the indicators of performance. The components of the measurement technique include the detector type, location and installation specifications, inspection procedures, and quality assurance and quality control measures. Examples of measurement techniques include continuous emission monitoring systems, continuous opacity monitoring systems, continuous parametric monitoring systems, and manual inspections that include making records of process conditions or work practices.

(3) Monitoring frequency—the number of times you obtain and record monitoring data over a specified time interval. Examples of monitoring frequencies include at least four points equally spaced for each hour for continuous emissions or parametric monitoring systems, at least every 10 seconds for continuous opacity monitoring systems, and at least once per operating day (or week, month, etc.) for work practice or design inspections.

(4) Averaging time—the period over which you average and use data to verify proper operation of the pollution control approach or compliance with the emissions limitation or standard. Examples of averaging time include a 3-hour average in units of the emissions limitation, a 30-day rolling average emissions value, a daily average of a control device operational parametric range, and an instantaneous alarm.

*New affected source* means the collection of equipment, activities, or both within a single contiguous area and under common control that is included in a section 112(c) source category or subcategory that is subject to a section 112(d) or other relevant standard for new sources. This definition of "new affected source," and the criteria to be utilized in implementing it, shall apply to each section 112(d) standard for which the initial proposed rule is signed by the Administrator after June 30, 2002. Each relevant standard will define the term "new affected source," which will be the same as the "affected source" unless a different collection is warranted based on consideration of factors including:

- (1) Emission reduction impacts of controlling individual sources versus groups of sources;
- (2) Cost effectiveness of controlling individual equipment;
- (3) Flexibility to accommodate common control strategies;
- (4) Cost/benefits of emissions averaging;
- (5) Incentives for pollution prevention;
- (6) Feasibility and cost of controlling processes that share common equipment (e.g., product recovery devices);
- (7) Feasibility and cost of monitoring; and
- (8) Other relevant factors.

*New source* means any affected source the construction or reconstruction of which is commenced after the Administrator first proposes a relevant emission standard under this part establishing an emission standard applicable to such source.

One-hour period, unless otherwise defined in an applicable subpart, means any 60-minute period commencing on the hour.

*Opacity* means the degree to which emissions reduce the transmission of light and obscure the view of an object in the background. For continuous opacity monitoring systems, opacity means the fraction of incident light that is attenuated by an optical medium.

Owner or operator means any person who owns, leases, operates, controls, or supervises a stationary source.

*Performance audit* means a procedure to analyze blind samples, the content of which is known by the Administrator, simultaneously with the analysis of performance test samples in order to provide a measure of test data quality.

*Performance evaluation* means the conduct of relative accuracy testing, calibration error testing, and other measurements used in validating the continuous monitoring system data.

*Performance test* means the collection of data resulting from the execution of a test method (usually three emission test runs) used to demonstrate compliance with a relevant emission standard as specified in the performance test section of the relevant standard.

*Permit modification* means a change to a title V permit as defined in regulations codified in this chapter to implement title V of the Act (<u>42 U.S.C. 7661</u>).

*Permit program* means a comprehensive State operating permit system established pursuant to title V of the Act (<u>42 U.S.C.</u>) and regulations codified in <u>part 70 of this chapter</u> and applicable State regulations, or a comprehensive Federal operating permit system established pursuant to title V of the Act and regulations codified in this chapter.

*Permit revision* means any permit modification or administrative permit amendment to a title V permit as defined in regulations codified in this chapter to implement title V of the Act (<u>42 U.S.C. 7661</u>).

*Permitting authority* means:

(1) The State air pollution control agency, local agency, other State agency, or other agency authorized by the Administrator to carry out a permit program under <u>part 70 of this chapter</u>; or

(2) The Administrator, in the case of EPA-implemented permit programs under title V of the Act (42 U.S.C. 7661).

*Pollution Prevention* means *source reduction* as defined under the Pollution Prevention Act (<u>42 U.S.C. 13101-13109</u>). The definition is as follows:

(1) *Source reduction* is any practice that:

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(i) Reduces the amount of any hazardous substance, pollutant, or contaminant entering any waste stream or otherwise released into the environment (including fugitive emissions) prior to recycling, treatment, or disposal; and

(ii) Reduces the hazards to public health and the environment associated with the release of such substances, pollutants, or contaminants.

(2) The term *source reduction* includes equipment or technology modifications, process or procedure modifications, reformulation or redesign of products, substitution of raw materials, and improvements in housekeeping, maintenance, training, or inventory control.

(3) The term *source reduction* does not include any practice that alters the physical, chemical, or biological characteristics or the volume of a hazardous substance, pollutant, or contaminant through a process or activity which itself is not integral to and necessary for the production of a product or the providing of a service.

*Potential to emit* means the maximum capacity of a stationary source to emit a pollutant under its physical and operational design. Any physical or operational limitation on the capacity of the stationary source to emit a pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored, or processed, shall be treated as part of its design if the limitation or the effect it would have on emissions is enforceable.

*Reconstruction*, unless otherwise defined in a relevant standard, means the replacement of components of an affected or a previously nonaffected source to such an extent that:

(1) The fixed capital cost of the new components exceeds 50 percent of the fixed capital cost that would be required to construct a comparable new source; and

(2) It is technologically and economically feasible for the reconstructed source to meet the relevant standard(s) established by the Administrator (or a State) pursuant to section 112 of the Act. Upon reconstruction, an affected source, or a stationary source that becomes an affected source, is subject to relevant standards for new sources, including compliance dates, irrespective of any change in emissions of hazardous air pollutants from that source.

*Regulation promulgation schedule* means the schedule for the promulgation of emission standards under this part, established by the Administrator pursuant to section 112(e) of the Act and published in the Federal Register.

#### Relevant standard means:

(1) An emission standard;

- (2) An alternative emission standard;
- (3) An alternative emission limitation; or

(4) An equivalent emission limitation established pursuant to section 112 of the Act that applies to the collection of equipment, activities, or both regulated by such standard or limitation. A relevant standard may include or consist of a design, equipment, work practice, or operational requirement, or other measure, process, method, system, or technique (including prohibition of emissions) that the Administrator (or a State) establishes for new or existing sources to which such standard or limitation applies. Every relevant standard established pursuant to section 112 of the Act includes <u>subpart A of this part</u>, as provided by <u>§ 63.1(a)(4)</u>, and all applicable appendices of this part or of other parts of this chapter that are referenced in that standard.

#### Responsible official means one of the following:

(1) For a corporation: A president, secretary, treasurer, or vice president of the corporation in charge of a principal business function, or any other person who performs similar policy or decision-making functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities and either:

(i) The facilities employ more than 250 persons or have gross annual sales or expenditures exceeding \$25 million (in second quarter 1980 dollars); or

(ii) The delegation of authority to such representative is approved in advance by the Administrator.

(2) For a partnership or sole proprietorship: a general partner or the proprietor, respectively.

(3) For a municipality, State, Federal, or other public agency: either a principal executive officer or ranking elected official. For the purposes of this part, a principal executive officer of a Federal agency includes the chief executive officer having

responsibility for the overall operations of a principal geographic unit of the agency (e.g., a Regional Administrator of the EPA).

(4) For affected sources (as defined in this part) applying for or subject to a title V permit: "responsible official" shall have the same meaning as defined in part 70 or Federal title V regulations in this chapter (<u>42 U.S.C. 7661</u>), whichever is applicable.

*Run* means one of a series of emission or other measurements needed to determine emissions for a representative operating period or cycle as specified in this part.

Shutdown means the cessation of operation of an affected source or portion of an affected source for any purpose.

Six-minute period means, with respect to opacity determinations, any one of the 10 equal parts of a 1-hour period.

*Source at a Performance Track member facility* means a major or area source located at a facility which has been accepted by EPA for membership in the Performance Track Program (as described at <u>www.epa.gov/PerformanceTrack</u>) and is still a member of the Program. The Performance Track Program is a voluntary program that encourages continuous environmental improvement through the use of environmental management systems, local community outreach, and measurable results.

Standard conditions means a temperature of 293 K (68 °F) and a pressure of 101.3 kilopascals (29.92 in. Hg).

Startup means the setting in operation of an affected source or portion of an affected source for any purpose.

*State* means all non-Federal authorities, including local agencies, interstate associations, and State-wide programs, that have delegated authority to implement:

(1) The provisions of this part and/or

(2) the permit program established under part 70 of this chapter. The term State shall have its conventional meaning where clear from the context.

Stationary source means any building, structure, facility, or installation which emits or may emit any air pollutant.

*Test method* means the validated procedure for sampling, preparing, and analyzing for an air pollutant specified in a relevant standard as the performance test procedure. The test method may include methods described in an appendix of this chapter, test methods incorporated by reference in this part, or methods validated for an application through procedures in Method 301 of appendix A of this part.

*Title V permit* means any permit issued, renewed, or revised pursuant to Federal or State regulations established to implement title V of the Act (<u>42 U.S.C. 7661</u>). A title V permit issued by a State permitting authority is called a part 70 permit in this part.

Visible emission means the observation of an emission of opacity or optical density above the threshold of vision.

*Working day* means any day on which Federal Government offices (or State government offices for a State that has obtained delegation under section 112(l)) are open for normal business. Saturdays, Sundays, and official Federal (or where delegated, State) holidays are not working days.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>67 FR 16596</u>, Apr. 5, 2002; <u>68 FR 32600</u>, May 30, 2003; <u>69 FR 21752</u>, Apr. 22, 2004; <u>72 FR 27443</u>, May 16, 2007; <u>85 FR 63418</u>, Oct. 7, 2020; <u>85 FR 73885</u>, Nov. 19, 2020]

## § 63.3 Units and abbreviations.

Used in this part are abbreviations and symbols of units of measure. These are defined as follows:

(a) System International (SI) units of measure:

A = ampere

- g = gram
- Hz = hertz
- J = joule

°K = degree Kelvin

kg = kilogram

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l = liter
m = meter
m^3 = cubic meter
mg = milligram = 10^{-3} gram
ml = milliliter = 10^{-3} liter
mm = millimeter = 10^{-3} meter
Mg = megagram = 10^6 gram = metric ton
MJ = megajoule
mol = mole
N = newton
ng = nanogram = 10^{-9} gram
nm = nanometer = 10^{-9} meter
Pa = pascal
s = second
V = volt
W = watt
\Omega = ohm
\mu g = microgram = 10^{-6} gram
\mul = microliter = 10<sup>-6</sup> liter
(b) Other units of measure:
Btu = British thermal unit
°C = degree Celsius (centigrade)
cal = calorie
cfm = cubic feet per minute
cc = cubic centimeter
cu ft = cubic feet
d = day
dcf = dry cubic feet
dcm = dry cubic meter
dscf = dry cubic feet at standard conditions
dscm = dry cubic meter at standard conditions
eq = equivalent
°F degree Fahrenheit
ft = feet
ft^2 = square feet
ft^3 = cubic feet
gal = gallon
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gr = grain g-eq = gram equivalent g-mole = gram mole hr = hourin. = inchin.  $H_2 O =$  inches of water K = 1,000kcal = kilocalorie lb = poundlpm = liter per minute meq = milliequivalent min = minuteMW = molecular weight oz = ounces ppb = parts per billion ppbw = parts per billion by weight ppbv = parts per billion by volume ppm = parts per million ppmw = parts per million by weight ppmv = parts per million by volume psia = pounds per square inch absolute psig = pounds per square inch gage  $^{\circ}R = degree Rankine$ scf = cubic feet at standard conditions scfh = cubic feet at standard conditions per hour scm = cubic meter at standard conditions scmm = cubic meter at standard conditions per minute sec = secondsq ft = square feet std = at standard conditions v/v = volume per volume $yd^2 = square yards$ yr = year (c) Miscellaneous: act = actualavg = average I.D. = inside diameter

M = molar

N = normal

O.D. = outside diameter

% = percent

[59 FR 12430, Mar. 16, 1994, as amended at 67 FR 16598, Apr. 5, 2002]

# § 63.4 Prohibited activities and circumvention.

(a) Prohibited activities.

(1) No owner or operator subject to the provisions of this part must operate any affected source in violation of the requirements of this part. Affected sources subject to and in compliance with either an extension of compliance or an exemption from compliance are not in violation of the requirements of this part. An extension of compliance can be granted by the Administrator under this part; by a State with an approved permit program; or by the President under section 112(i)(4) of the Act.

(2) No owner or operator subject to the provisions of this part shall fail to keep records, notify, report, or revise reports as required under this part.

(3)-(5) [Reserved]

(b) *Circumvention*. No owner or operator subject to the provisions of this part shall build, erect, install, or use any article, machine, equipment, or process to conceal an emission that would otherwise constitute noncompliance with a relevant standard. Such concealment includes, but is not limited to—

(1) The use of diluents to achieve compliance with a relevant standard based on the concentration of a pollutant in the effluent discharged to the atmosphere;

(2) The use of gaseous diluents to achieve compliance with a relevant standard for visible emissions; and

(c) *Fragmentation*. Fragmentation after November 15, 1990 which divides ownership of an operation, within the same facility among various owners where there is no real change in control, will not affect applicability. The owner and operator must not use fragmentation or phasing of reconstruction activities (i.e., intentionally dividing reconstruction into multiple parts for purposes of avoiding new source requirements) to avoid becoming subject to new source requirements.

[59 FR 12430, Mar. 16, 1994, as amended at 67 FR 16598, Apr. 5, 2002]

# § 63.5 Preconstruction review and notification requirements.

## (a) *Applicability*.

(1) This section implements the preconstruction review requirements of section 112(i)(1). After the effective date of a relevant standard, promulgated pursuant to section 112(d), (f), or (h) of the Act, under this part, the preconstruction review requirements in this section apply to the owner or operator of new affected sources and reconstructed affected sources that are major-emitting as specified in this section. New and reconstructed affected sources that commence construction or reconstruction before the effective date of a relevant standard are not subject to the preconstruction review requirements specified in paragraphs (b)(3), (d), and (e) of this section.

(2) This section includes notification requirements for new affected sources and reconstructed affected sources that are not major-emitting affected sources and that are or become subject to a relevant promulgated emission standard after the effective date of a relevant standard promulgated under this part.

(b) Requirements for existing, newly constructed, and reconstructed sources.

(1) A new affected source for which construction commences after proposal of a relevant standard is subject to relevant standards for new affected sources, including compliance dates. An affected source for which reconstruction commences after proposal of a relevant standard is subject to relevant standards for new sources, including compliance dates, irrespective of any change in emissions of hazardous air pollutants from that source.

(2) [Reserved]

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(3) After the effective date of any relevant standard promulgated by the Administrator under this part, no person may, without obtaining written approval in advance from the Administrator in accordance with the procedures specified in <u>paragraphs (d)</u> and (e) of this section, do any of the following:

(i) Construct a new affected source that is major-emitting and subject to such standard;

(ii) Reconstruct an affected source that is major-emitting and subject to such standard; or

(iii) Reconstruct a major source such that the source becomes an affected source that is major-emitting and subject to the standard.

(4) After the effective date of any relevant standard promulgated by the Administrator under this part, an owner or operator who constructs a new affected source that is not major-emitting or reconstructs an affected source that is not major-emitting that is subject to such standard, or reconstructs a source such that the source becomes an affected source subject to the standard, must notify the Administrator of the intended construction or reconstruction. The notification must be submitted in accordance with the procedures in  $\frac{§ 63.9(b)}{5}$ .

### (5) [Reserved]

(6) After the effective date of any relevant standard promulgated by the Administrator under this part, equipment added (or a process change) to an affected source that is within the scope of the definition of affected source under the relevant standard must be considered part of the affected source and subject to all provisions of the relevant standard established for that affected source.

### (c) [Reserved]

(d) Application for approval of construction or reconstruction. The provisions of this paragraph implement section 112(i)(1) of the Act.

(1) General application requirements.

(i) An owner or operator who is subject to the requirements of <u>paragraph (b)(3)</u> of this section must submit to the Administrator an application for approval of the construction or reconstruction. The application must be submitted as soon as practicable before actual construction or reconstruction begins. The application for approval of construction or reconstruction may be used to fulfill the initial notification requirements of § 63.9(b)(5). The owner or operator may submit the application for approval well in advance of the date actual construction or reconstruction begins in order to ensure a timely review by the Administrator and that the planned date to begin will not be delayed.

(ii) A separate application shall be submitted for each construction or reconstruction. Each application for approval of construction or reconstruction shall include at a minimum:

(A) The applicant's name and address;

(B) A notification of intention to construct a new major affected source or make any physical or operational change to a major affected source that may meet or has been determined to meet the criteria for a reconstruction, as defined in  $\S$  63.2 or in the relevant standard;

(C) The address (i.e., physical location) or proposed address of the source;

(D) An identification of the relevant standard that is the basis of the application;

(E) The expected date of the beginning of actual construction or reconstruction;

(F) The expected completion date of the construction or reconstruction;

(G) [Reserved]

(H) The type and quantity of hazardous air pollutants emitted by the source, reported in units and averaging times and in accordance with the test methods specified in the relevant standard, or if actual emissions data are not yet available, an estimate of the type and quantity of hazardous air pollutants expected to be emitted by the source reported in units and averaging times specified in the relevant standard. The owner or operator may submit percent reduction information if a relevant standard is established in terms of percent reduction. However, operating parameters, such as flow rate, shall be included in the submission to the extent that they demonstrate performance and compliance; and

(I) [Reserved]

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(J) Other information as specified in <u>paragraphs (d)(2)</u> and (d)(3) of this section.

(iii) An owner or operator who submits estimates or preliminary information in place of the actual emissions data and analysis required in <u>paragraphs (d)(1)(ii)(H)</u> and (d)(2) of this section shall submit the actual, measured emissions data and other correct information as soon as available but no later than with the notification of compliance status required in  $\S$  <u>63.9(h)(5)</u>).

(2) Application for approval of construction. Each application for approval of construction must include, in addition to the information required in <u>paragraph (d)(1)(ii)</u> of this section, technical information describing the proposed nature, size, design, operating design capacity, and method of operation of the source, including an identification of each type of emission point for each type of hazardous air pollutant that is emitted (or could reasonably be anticipated to be emitted) and a description of the planned air pollution control system (equipment or method) for each emission point. The description of the equipment to be used for the control of emissions must include each control device for each hazardous air pollutant and the estimated control efficiency (percent) for each control device. The description of the method to be used for the control of emissions must include an estimated control efficiency (percent) for that method. Such technical information must include calculations of emission estimates in sufficient detail to permit assessment of the validity of the calculations.

(3) Application for approval of reconstruction. Each application for approval of reconstruction shall include, in addition to the information required in paragraph (d)(1)(ii) of this section—

(i) A brief description of the affected source and the components that are to be replaced;

(ii) A description of present and proposed emission control systems (i.e., equipment or methods). The description of the equipment to be used for the control of emissions shall include each control device for each hazardous air pollutant and the estimated control efficiency (percent) for each control device. The description of the method to be used for the control of emissions shall include an estimated control efficiency (percent) for that method. Such technical information shall include calculations of emission estimates in sufficient detail to permit assessment of the validity of the calculations;

(iii) An estimate of the fixed capital cost of the replacements and of constructing a comparable entirely new source;

(iv) The estimated life of the affected source after the replacements; and

(v) A discussion of any economic or technical limitations the source may have in complying with relevant standards or other requirements after the proposed replacements. The discussion shall be sufficiently detailed to demonstrate to the Administrator's satisfaction that the technical or economic limitations affect the source's ability to comply with the relevant standard and how they do so.

(vi) If in the application for approval of reconstruction the owner or operator designates the affected source as a reconstructed source and declares that there are no economic or technical limitations to prevent the source from complying with all relevant standards or other requirements, the owner or operator need not submit the information required in <u>paragraphs</u> (d)(3)(ii) through (d)(3)(v) of this section.

(4) *Additional information*. The Administrator may request additional relevant information after the submittal of an application for approval of construction or reconstruction.

(e) Approval of construction or reconstruction.

(1)

(i) If the Administrator determines that, if properly constructed, or reconstructed, and operated, a new or existing source for which an application under <u>paragraph (d)</u> of this section was submitted will not cause emissions in violation of the relevant standard(s) and any other federally enforceable requirements, the Administrator will approve the construction or reconstruction.

(ii) In addition, in the case of reconstruction, the Administrator's determination under this paragraph will be based on:

(A) The fixed capital cost of the replacements in comparison to the fixed capital cost that would be required to construct a comparable entirely new source;

(B) The estimated life of the source after the replacements compared to the life of a comparable entirely new source;

(C) The extent to which the components being replaced cause or contribute to the emissions from the source; and

(D) Any economic or technical limitations on compliance with relevant standards that are inherent in the proposed replacements.

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(2)

(i) The Administrator will notify the owner or operator in writing of approval or intention to deny approval of construction or reconstruction within 60 calendar days after receipt of sufficient information to evaluate an application submitted under <u>paragraph (d)</u> of this section. The 60-day approval or denial period will begin after the owner or operator has been notified in writing that his/her application is complete. The Administrator will notify the owner or operator in writing of the status of his/her application, that is, whether the application contains sufficient information to make a determination, within 30 calendar days after receipt of the original application and within 30 calendar days after receipt of any supplementary information that is submitted.

(ii) When notifying the owner or operator that his/her application is not complete, the Administrator will specify the information needed to complete the application and provide notice of opportunity for the applicant to present, in writing, within 30 calendar days after he/she is notified of the incomplete application, additional information or arguments to the Administrator to enable further action on the application.

(3) Before denying any application for approval of construction or reconstruction, the Administrator will notify the applicant of the Administrator's intention to issue the denial together with—

(i) Notice of the information and findings on which the intended denial is based; and

(ii) Notice of opportunity for the applicant to present, in writing, within 30 calendar days after he/she is notified of the intended denial, additional information or arguments to the Administrator to enable further action on the application.

(4) A final determination to deny any application for approval will be in writing and will specify the grounds on which the denial is based. The final determination will be made within 60 calendar days of presentation of additional information or arguments (if the application is complete), or within 60 calendar days after the final date specified for presentation if no presentation is made.

(5) Neither the submission of an application for approval nor the Administrator's approval of construction or reconstruction shall—

(i) Relieve an owner or operator of legal responsibility for compliance with any applicable provisions of this part or with any other applicable Federal, State, or local requirement; or

(ii) Prevent the Administrator from implementing or enforcing this part or taking any other action under the Act.

(f) Approval of construction or reconstruction based on prior State preconstruction review.

(1) Preconstruction review procedures that a State utilizes for other purposes may also be utilized for purposes of this section if the procedures are substantially equivalent to those specified in this section. The Administrator will approve an application for construction or reconstruction specified in <u>paragraphs (b)(3)</u> and (d) of this section if the owner or operator of a new affected source or reconstructed affected source, who is subject to such requirement meets the following conditions:

(i) The owner or operator of the new affected source or reconstructed affected source has undergone a preconstruction review and approval process in the State in which the source is (or would be) located and has received a federally enforceable construction permit that contains a finding that the source will meet the relevant promulgated emission standard, if the source is properly built and operated.

(ii) Provide a statement from the State or other evidence (such as State regulations) that it considered the factors specified in paragraph (e)(1) of this section.

(2) The owner or operator must submit to the Administrator the request for approval of construction or reconstruction under this <u>paragraph (f)(2)</u> no later than the application deadline specified in <u>paragraph (d)(1)</u> of this section (see also § 63.9(b)(2)). The owner or operator must include in the request information sufficient for the Administrator's determination. The Administrator will evaluate the owner or operator's request in accordance with the procedures specified in <u>paragraph (e)</u> of this section. The Administrator may request additional relevant information after the submittal of a request for approval of construction under this <u>paragraph (f)(2)</u>.

[59 FR 12430, Mar. 16, 1994, as amended at 67 FR 16598, Apr. 5, 2002]

## § 63.6 Compliance with standards and maintenance requirements.

(a) Applicability.

(1) The requirements in this section apply to the owner or operator of affected sources for which any relevant standard has been established pursuant to section 112 of the Act and the applicability of such requirements is set out in accordance with  $\frac{5}{63.1(a)(4)}$  unless—

(i) The Administrator (or a State with an approved permit program) has granted an extension of compliance consistent with <u>paragraph (i)</u> of this section; or

(ii) The President has granted an exemption from compliance with any relevant standard in accordance with section 112(i)(4) of the Act.

(2) If an area source that otherwise would be subject to an emission standard or other requirement established under this part if it were a major source subsequently increases its emissions of hazardous air pollutants (or its potential to emit hazardous air pollutants) such that the source is a major source, such source shall be subject to the relevant emission standard or other requirement.

### (b) Compliance dates for new and reconstructed sources.

(1) Except as specified in <u>paragraphs (b)(3)</u> and (4) of this section, the owner or operator of a new or reconstructed affected source for which construction or reconstruction commences after proposal of a relevant standard that has an initial startup before the effective date of a relevant standard established under this part pursuant to section 112(d), (f), or (h) of the Act must comply with such standard not later than the standard's effective date.

(2) Except as specified in <u>paragraphs (b)(3)</u> and (4) of this section, the owner or operator of a new or reconstructed affected source that has an initial startup after the effective date of a relevant standard established under this part pursuant to section 112(d), (f), or (h) of the Act must comply with such standard upon startup of the source.

(3) The owner or operator of an affected source for which construction or reconstruction is commenced after the proposal date of a relevant standard established under this part pursuant to section 112(d), 112(f), or 112(h) of the Act but before the effective date (that is, promulgation) of such standard shall comply with the relevant emission standard not later than the date 3 years after the effective date if:

(i) The promulgated standard (that is, the relevant standard) is more stringent than the proposed standard; for purposes of this paragraph, a finding that controls or compliance methods are "more stringent" must include control technologies or performance criteria and compliance or compliance assurance methods that are different but are substantially equivalent to those required by the promulgated rule, as determined by the Administrator (or his or her authorized representative); and

(ii) The owner or operator complies with the standard as proposed during the 3-year period immediately after the effective date.

(4) The owner or operator of an affected source for which construction or reconstruction is commenced after the proposal date of a relevant standard established pursuant to section 112(d) of the Act but before the proposal date of a relevant standard established pursuant to section 112(f) shall not be required to comply with the section 112(f) emission standard until the date 10 years after the date construction or reconstruction is commenced, except that, if the section 112(f) standard is promulgated more than 10 years after construction or reconstruction is commenced, the owner or operator must comply with the standard as provided in paragraphs (b)(1) and (2) of this section.

(5) The owner or operator of a new source that is subject to the compliance requirements of <u>paragraph (b)(3)</u> or (4) of this section must notify the Administrator in accordance with  $\S 63.9(d)$ 

(6) [Reserved]

(7) When an area source increases its emissions of (or its potential to emit) hazardous air pollutants such that the source becomes a major source, the portion of the facility that meets the definition of a new affected source must comply with all requirements of that standard applicable to new sources. The source owner or operator must comply with the relevant standard upon startup.

#### (c) Compliance dates for existing sources.

(1) After the effective date of a relevant standard established under this part pursuant to section 112(d) or 112(h) of the Act, the owner or operator of an existing source shall comply with such standard by the compliance date established by the Administrator in the applicable subpart(s) of this part, except as provided in  $\S 63.1(c)(6)(i)$ . Except as otherwise provided for in section 112 of the Act, in no case will the compliance date established for an existing source in an applicable subpart of this part exceed 3 years after the effective date of such standard.

(2) If an existing source is subject to a standard established under this part pursuant to section 112(f) of the Act, the owner or operator must comply with the standard by the date 90 days after the standard's effective date, or by the date specified in an extension granted to the source by the Administrator under paragraph (i)(4)(ii) of this section, whichever is later.

(3)-(4) [Reserved]

(5) Except as provided in paragraph (b)(7) of this section, the owner or operator of an area source that increases its emissions of (or its potential to emit) hazardous air pollutants such that the source becomes a major source and meets the definition of an existing source in the applicable major source standard shall be subject to relevant standards for existing sources. Except as provided in paragraph § 63.1(c)(6)(i)(B), such sources must comply by the date specified in the standards for existing area sources that become major sources. If no such compliance date is specified in the standards, the source shall have a period of time to comply with the relevant emission standard that is equivalent to the compliance period specified in the relevant standard for existing sources at the time the standard becomes effective.

## (d) [Reserved]

(e) Operation and maintenance requirements.

(1)

(i) At all times, including periods of startup, shutdown, and malfunction, the owner or operator must operate and maintain any affected source, including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. During a period of startup, shutdown, or malfunction, this general duty to minimize emissions requires that the owner or operator reduce emissions from the affected source to the greatest extent which is consistent with safety and good air pollution control practices. The general duty to minimize emissions during a period of startup, shutdown, or malfunction does not require the owner or operator to achieve emission levels that would be required by the applicable standard at other times if this is not consistent with safety and good air pollution control practices, nor does it require the owner or operator to make any further efforts to reduce emissions if levels required by the applicable standard have been achieved. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator which may include, but is not limited to, monitoring results, review of operation and maintenance procedures (including the startup, shutdown, and malfunction plan required in <u>paragraph (e)(3)</u> of this section), review of operation and maintenance records, and inspection of the source.

(ii) Malfunctions must be corrected as soon as practicable after their occurrence. To the extent that an unexpected event arises during a startup, shutdown, or malfunction, an owner or operator must comply by minimizing emissions during such a startup, shutdown, and malfunction event consistent with safety and good air pollution control practices.

(iii) Operation and maintenance requirements established pursuant to section 112 of the Act are enforceable independent of emissions limitations or other requirements in relevant standards.

# (2) [Reserved]

# (3) Startup, shutdown, and malfunction plan.

(i) The owner or operator of an affected source must develop a written startup, shutdown, and malfunction plan that describes, in detail, procedures for operating and maintaining the source during periods of startup, shutdown, and malfunction; and a program of corrective action for malfunctioning process, air pollution control, and monitoring equipment used to comply with the relevant standard. The startup, shutdown, and malfunction plan does not need to address any scenario that would not cause the source to exceed an applicable emission limitation in the relevant standard. This plan must be developed by the owner or operator by the source's compliance date for that relevant standard. The purpose of the startup, shutdown, and malfunction plan is to—

(A) Ensure that, at all times, the owner or operator operates and maintains each affected source, including associated air pollution control and monitoring equipment, in a manner which satisfies the general duty to minimize emissions established by paragraph (e)(1)(i) of this section;

(B) Ensure that owners or operators are prepared to correct malfunctions as soon as practicable after their occurrence in order to minimize excess emissions of hazardous air pollutants; and

(C) Reduce the reporting burden associated with periods of startup, shutdown, and malfunction (including corrective action taken to restore malfunctioning process and air pollution control equipment to its normal or usual manner of operation).

(ii) [Reserved]

(iii) When actions taken by the owner or operator during a startup or shutdown (and the startup or shutdown causes the source to exceed any applicable emission limitation in the relevant emission standards), or malfunction (including actions taken to correct a malfunction) are consistent with the procedures specified in the affected source's startup, shutdown, and malfunction plan, the owner or operator must keep records for that event which demonstrate that the procedures specified in the plan were followed. These records may take the form of a "checklist," or other effective form of recordkeeping that confirms conformance with the startup, shutdown, and malfunction plan and describes the actions taken for that event. In addition, the owner or operator must keep records of these events as specified in paragraph 63.10(b), including records of the occurrence and duration of each startup or shutdown (if the startup or shutdown causes the source to exceed any applicable emission limitation in the relevant emission standards), or malfunction of operation and each malfunction of the air pollution control and monitoring equipment. Furthermore, the owner or operator shall confirm that actions taken during the relevant reporting period during periods of startup, shutdown, and malfunction were consistent with the affected source's startup, shutdown and malfunction plan in the semiannual (or more frequent) startup, shutdown, and malfunction report required in § 63.10(d)(5).

(iv) If an action taken by the owner or operator during a startup, shutdown, or malfunction (including an action taken to correct a malfunction) is not consistent with the procedures specified in the affected source's startup, shutdown, and malfunction plan, and the source exceeds any applicable emission limitation in the relevant emission standard, then the owner or operator must record the actions taken for that event and must report such actions within 2 working days after commencing actions inconsistent with the plan, followed by a letter within 7 working days after the end of the event, in accordance with  $\frac{63.10(d)(5)}{10}$  (unless the owner or operator makes alternative reporting arrangements, in advance, with the Administrator).

(v) The owner or operator must maintain at the affected source a current startup, shutdown, and malfunction plan and must make the plan available upon request for inspection and copying by the Administrator. In addition, if the startup, shutdown, and malfunction plan is subsequently revised as provided in paragraph (e)(3)(viii) of this section, the owner or operator must maintain at the affected source each previous (i.e., superseded) version of the startup, shutdown, and malfunction plan, and must make each such previous version available for inspection and copying by the Administrator for a period of 5 years after revision of the plan. If at any time after adoption of a startup, shutdown, and malfunction plan the affected source ceases operation or is otherwise no longer subject to the provisions of this part, the owner or operator must retain a copy of the most recent plan for 5 years from the date the source ceases operation or is no longer subject to this part and must make the plan available upon request for inspection and copying by the Administrator. The Administrator may at any time request in writing that the owner or operator submit a copy of any startup, shutdown, and malfunction plan (or a portion thereof) which is maintained at the affected source or in the possession of the owner or operator. Upon receipt of such a request, the owner or operator must promptly submit a copy of the requested plan (or a portion thereof) to the Administrator. The owner or operator may elect to submit the required copy of any startup, shutdown, and malfunction plan to the Administrator in an electronic format. If the owner or operator claims that any portion of such a startup, shutdown, and malfunction plan is confidential business information entitled to protection from disclosure under section 114(c) of the Act or 40 CFR 2.301, the material which is claimed as confidential must be clearly designated in the submission.

(vi) To satisfy the requirements of this section to develop a startup, shutdown, and malfunction plan, the owner or operator may use the affected source's standard operating procedures (SOP) manual, or an Occupational Safety and Health Administration (OSHA) or other plan, provided the alternative plans meet all the requirements of this section and are made available for inspection or submitted when requested by the Administrator.

(vii) Based on the results of a determination made under <u>paragraph (e)(1)(i)</u> of this section, the Administrator may require that an owner or operator of an affected source make changes to the startup, shutdown, and malfunction plan for that source. The Administrator must require appropriate revisions to a startup, shutdown, and malfunction plan, if the Administrator finds that the plan:

(A) Does not address a startup, shutdown, or malfunction event that has occurred;

(B) Fails to provide for the operation of the source (including associated air pollution control and monitoring equipment) during a startup, shutdown, or malfunction event in a manner consistent with the general duty to minimize emissions established by <u>paragraph (e)(1)(i)</u> of this section;

(C) Does not provide adequate procedures for correcting malfunctioning process and/or air pollution control and monitoring equipment as quickly as practicable; or

(D) Includes an event that does not meet the definition of startup, shutdown, or malfunction listed in  $\S$  63.2.

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(viii) The owner or operator may periodically revise the startup, shutdown, and malfunction plan for the affected source as necessary to satisfy the requirements of this part or to reflect changes in equipment or procedures at the affected source. Unless the permitting authority provides otherwise, the owner or operator may make such revisions to the startup, shutdown, and malfunction plan without prior approval by the Administrator or the permitting authority. However, each such revision to a startup, shutdown, and malfunction plan must be reported in the semiannual report required by  $\S$  <u>63.10(d)(5)</u>. If the startup, shutdown, and malfunction plan fails to address or inadequately addresses an event that meets the characteristics of a malfunction but was not included in the startup, shutdown, and malfunction plan at the time the owner or operator developed the plan, the owner or operator must revise the startup, shutdown, and malfunction plan within 45 days after the event to include detailed procedures for operating and maintaining the source during similar malfunction events and a program of corrective action for similar malfunctions of process or air pollution control and monitoring equipment. In the event that the owner or operator makes any revision to the startup, shutdown, and malfunction plan which alters the scope of the activities at the source which are deemed to be a startup, shutdown, or malfunction, or otherwise modifies the applicability of any emission limit, work practice requirement, or operator has provided a written notice describing the revision to the permitting authority of any emission limit, work practice requirement or operator has provided a written notice describing the revision to the permitting authority.

(ix) The title V permit for an affected source must require that the owner or operator develop a startup, shutdown, and malfunction plan which conforms to the provisions of this part, but may do so by citing to the relevant subpart or subparagraphs of <u>paragraph (e)</u> of this section. However, any revisions made to the startup, shutdown, and malfunction plan in accordance with the procedures established by this part shall not be deemed to constitute permit revisions under <u>part 70</u> or <u>part 71 of this chapter</u> and the elements of the startup, shutdown, and malfunction plan shall not be considered an applicable requirement as defined in § 70.2 and § 71.2 of this chapter. Moreover, none of the procedures specified by the startup, shutdown, and malfunction plan for an affected source shall be deemed to fall within the permit shield provision in section 504(f) of the Act.

## (f) Compliance with nonopacity emission standards —

(1) *Applicability*. The non-opacity emission standards set forth in this part shall apply at all times except as otherwise specified in an applicable subpart. If a startup, shutdown, or malfunction of one portion of an affected source does not affect the ability of particular emission points within other portions of the affected source to comply with the non-opacity emission standards set forth in this part, then that emission point must still be required to comply with the non-opacity emission standards and other applicable requirements.

## (2) Methods for determining compliance.

(i) The Administrator will determine compliance with nonopacity emission standards in this part based on the results of performance tests conducted according to the procedures in  $\S$  63.7, unless otherwise specified in an applicable subpart of this part.

(ii) The Administrator will determine compliance with nonopacity emission standards in this part by evaluation of an owner or operator's conformance with operation and maintenance requirements, including the evaluation of monitoring data, as specified in  $\S$  63.6(e) and applicable subparts of this part.

(iii) If an affected source conducts performance testing at startup to obtain an operating permit in the State in which the source is located, the results of such testing may be used to demonstrate compliance with a relevant standard if—

(A) The performance test was conducted within a reasonable amount of time before an initial performance test is required to be conducted under the relevant standard;

(B) The performance test was conducted under representative operating conditions for the source;

(C) The performance test was conducted and the resulting data were reduced using EPA-approved test methods and procedures, as specified in  $\S$  63.7(e) of this subpart; and

(D) The performance test was appropriately quality-assured, as specified in  $\S$  63.7(c).

(iv) The Administrator will determine compliance with design, equipment, work practice, or operational emission standards in this part by review of records, inspection of the source, and other procedures specified in applicable <u>subparts of this part</u>.

(v) The Administrator will determine compliance with design, equipment, work practice, or operational emission standards in this part by evaluation of an owner or operator's conformance with operation and maintenance requirements, as specified in <u>paragraph (e)</u> of this section and applicable <u>subparts of this part</u>.

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(3) *Finding of compliance.* The Administrator will make a finding concerning an affected source's compliance with a nonopacity emission standard, as specified in <u>paragraphs (f)(1)</u> and (2) of this section, upon obtaining all the compliance information required by the relevant standard (including the written reports of performance test results, monitoring results, and other information, if applicable), and information available to the Administrator pursuant to <u>paragraph (e)(1)(i)</u> of this section.

## (g) Use of an alternative nonopacity emission standard.

(1) If, in the Administrator's judgment, an owner or operator of an affected source has established that an alternative means of emission limitation will achieve a reduction in emissions of a hazardous air pollutant from an affected source at least equivalent to the reduction in emissions of that pollutant from that source achieved under any design, equipment, work practice, or operational emission standard, or combination thereof, established under this part pursuant to section 112(h) of the Act, the Administrator will publish in the Federal Register a notice permitting the use of the alternative emission standard for purposes of compliance with the promulgated standard. Any Federal Register notice under this paragraph shall be published only after the public is notified and given the opportunity to comment. Such notice will restrict the permission to the stationary source(s) or category(ies) of sources from which the alternative emission standard will achieve equivalent emission reductions. The Administrator will condition permission in such notice on requirements to assure the proper operation and maintenance of equipment and practices required for compliance with the alternative emission standard and other requirements, including appropriate quality assurance and quality control requirements, that are deemed necessary.

(2) An owner or operator requesting permission under this paragraph shall, unless otherwise specified in an applicable subpart, submit a proposed test plan or the results of testing and monitoring in accordance with  $\S$  63.7 and  $\S$  63.8, a description of the procedures followed in testing or monitoring, and a description of pertinent conditions during testing or monitoring. Any testing or monitoring conducted to request permission to use an alternative nonopacity emission standard shall be appropriately quality assured and quality controlled, as specified in  $\S$  63.7 and  $\S$  63.8.

(3) The Administrator may establish general procedures in an applicable subpart that accomplish the requirements of paragraphs (g)(1) and (g)(2) of this section.

(h) Compliance with opacity and visible emission standards —

(1) *Applicability*. The opacity and visible emission standards set forth in this part must apply at all times except as otherwise specified in an applicable subpart. If a startup, shutdown, or malfunction of one portion of an affected source does not affect the ability of particular emission points within other portions of the affected source to comply with the opacity and visible emission standards set forth in this part, then that emission point shall still be required to comply with the opacity and visible emission standards and other applicable requirements.

## (2) Methods for determining compliance.

(i) The Administrator will determine compliance with opacity and visible emission standards in this part based on the results of the test method specified in an applicable subpart. Whenever a continuous opacity monitoring system (COMS) is required to be installed to determine compliance with numerical opacity emission standards in this part, compliance with opacity emission standards in this part, compliance with opacity emission standards in this part shall be determined by using the results from the COMS. Whenever an opacity emission test method is not specified, compliance with opacity emission standards in this part shall be determined by in appendix A of part 60 of this chapter or the method specified in paragraph (h)(7)(ii) of this section. Whenever a visible emission test method is not specified, compliance with visible emission standards in this part shall be determined by conducting observations in accordance with visible emission test method is not specified, appendix A of part 60 of this chapter or the method 22 in appendix A of part 60 of this chapter.

## (ii) [Reserved]

(iii) If an affected source undergoes opacity or visible emission testing at startup to obtain an operating permit in the State in which the source is located, the results of such testing may be used to demonstrate compliance with a relevant standard if—

(A) The opacity or visible emission test was conducted within a reasonable amount of time before a performance test is required to be conducted under the relevant standard;

(B) The opacity or visible emission test was conducted under representative operating conditions for the source;

(C) The opacity or visible emission test was conducted and the resulting data were reduced using EPA-approved test methods and procedures, as specified in  $\S$  63.7(e); and

(D) The opacity or visible emission test was appropriately quality-assured, as specified in  $\frac{63.7(c)}{2}$  of this section.

(3) [Reserved]

(4) Notification of opacity or visible emission observations. The owner or operator of an affected source shall notify the Administrator in writing of the anticipated date for conducting opacity or visible emission observations in accordance with  $\S$  <u>63.9(f)</u>, if such observations are required for the source by a relevant standard.

(5) *Conduct of opacity or visible emission observations*. When a relevant standard under this part includes an opacity or visible emission standard, the owner or operator of an affected source shall comply with the following:

(i) For the purpose of demonstrating initial compliance, opacity or visible emission observations shall be conducted concurrently with the initial performance test required in  $\S$  63.7 unless one of the following conditions applies:

(A) If no performance test under § 63.7 is required, opacity or visible emission observations shall be conducted within 60 days after achieving the maximum production rate at which a new or reconstructed source will be operated, but not later than 120 days after initial startup of the source, or within 120 days after the effective date of the relevant standard in the case of new sources that start up before the standard's effective date. If no performance test under § 63.7 is required, opacity or visible emission observations shall be conducted within 120 days after the compliance date for an existing or modified source; or

(B) If visibility or other conditions prevent the opacity or visible emission observations from being conducted concurrently with the initial performance test required under § 63.7, or within the time period specified in paragraph (h)(5)(i)(A) of this section, the source's owner or operator shall reschedule the opacity or visible emission observations as soon after the initial performance test, or time period, as possible, but not later than 30 days thereafter, and shall advise the Administrator of the rescheduled date. The rescheduled opacity or visible emission observations shall be conducted (to the extent possible) under the same operating conditions that existed during the initial performance test conducted under § 63.7. The visible emissions observer shall determine whether visibility or other conditions prevent the opacity or visible emission observations from being made concurrently with the initial performance test in accordance with procedures contained in Test Method 9 or Test Method 22 in appendix A of part 60 of this chapter.

(ii) For the purpose of demonstrating initial compliance, the minimum total time of opacity observations shall be 3 hours (30 6-minute averages) for the performance test or other required set of observations (e.g., for fugitive-type emission sources subject only to an opacity emission standard).

(iii) The owner or operator of an affected source to which an opacity or visible emission standard in this part applies shall conduct opacity or visible emission observations in accordance with the provisions of this section, record the results of the evaluation of emissions, and report to the Administrator the opacity or visible emission results in accordance with the provisions of  $\frac{63.10(d)}{10}$ .

# (iv) [Reserved]

(v) Opacity readings of portions of plumes that contain condensed, uncombined water vapor shall not be used for purposes of determining compliance with opacity emission standards.

(6) *Availability of records*. The owner or operator of an affected source shall make available, upon request by the Administrator, such records that the Administrator deems necessary to determine the conditions under which the visual observations were made and shall provide evidence indicating proof of current visible observer emission certification.

## (7) Use of a continuous opacity monitoring system.

(i) The owner or operator of an affected source required to use a continuous opacity monitoring system (COMS) shall record the monitoring data produced during a performance test required under  $\frac{63.7}{3}$  and shall furnish the Administrator a written report of the monitoring results in accordance with the provisions of  $\frac{63.10(e)(4)}{2}$ .

(ii) Whenever an opacity emission test method has not been specified in an applicable subpart, or an owner or operator of an affected source is required to conduct Test Method 9 observations (see appendix A of <u>part 60 of this chapter</u>), the owner or operator may submit, for compliance purposes, COMS data results produced during any performance test required under § 63.7 in lieu of Method 9 data. If the owner or operator elects to submit COMS data for compliance with the opacity emission standard, he or she shall notify the Administrator of that decision, in writing, simultaneously with the notification under § 63.7(b) of the date the performance test is scheduled to begin. Once the owner or operator of an affected source has notified the Administrator to that effect, the COMS data results will be used to determine opacity compliance during subsequent performance tests required under § 63.7(b) of the date the notification under § 63.7(b) of the date the notification under § 63.7(b) of the date the subsequent performance tests required under § 63.7(b) of the date the subsequent performance test is scheduled to begin.

(iii) For the purposes of determining compliance with the opacity emission standard during a performance test required under <u>§ 63.7</u> using COMS data, the COMS data shall be reduced to 6-minute averages over the duration of the mass emission performance test.

(iv) The owner or operator of an affected source using a COMS for compliance purposes is responsible for demonstrating that he/she has complied with the performance evaluation requirements of  $\S$  63.8(e), that the COMS has been properly maintained, operated, and data quality-assured, as specified in  $\S$  63.8(c) and  $\S$  63.8(d), and that the resulting data have not been altered in any way.

(v) Except as provided in <u>paragraph (h)(7)(ii)</u> of this section, the results of continuous monitoring by a COMS that indicate that the opacity at the time visual observations were made was not in excess of the emission standard are probative but not conclusive evidence of the actual opacity of an emission, provided that the affected source proves that, at the time of the alleged violation, the instrument used was properly maintained, as specified in  $\S$  <u>63.8(c)</u>, and met Performance Specification 1 in appendix B of <u>part 60 of this chapter</u>, and that the resulting data have not been altered in any way.

(8) *Finding of compliance.* The Administrator will make a finding concerning an affected source's compliance with an opacity or visible emission standard upon obtaining all the compliance information required by the relevant standard (including the written reports of the results of the performance tests required by § 63.7, the results of Test Method 9 or another required opacity or visible emission test method, the observer certification required by <u>paragraph (h)(6)</u> of this section, and the continuous opacity monitoring system results, whichever is/are applicable) and any information available to the Administrator needed to determine whether proper operation and maintenance practices are being used.

## (9) Adjustment to an opacity emission standard.

(i) If the Administrator finds under paragraph (h)(8) of this section that an affected source is in compliance with all relevant standards for which initial performance tests were conducted under § 63.7, but during the time such performance tests were conducted fails to meet any relevant opacity emission standard, the owner or operator of such source may petition the Administrator to make appropriate adjustment to the opacity emission standard for the affected source. Until the Administrator notifies the owner or operator of the appropriate adjustment, the relevant opacity emission standard remains applicable.

(ii) The Administrator may grant such a petition upon a demonstration by the owner or operator that-

(A) The affected source and its associated air pollution control equipment were operated and maintained in a manner to minimize the opacity of emissions during the performance tests;

(B) The performance tests were performed under the conditions established by the Administrator; and

(C) The affected source and its associated air pollution control equipment were incapable of being adjusted or operated to meet the relevant opacity emission standard.

(iii) The Administrator will establish an adjusted opacity emission standard for the affected source meeting the above requirements at a level at which the source will be able, as indicated by the performance and opacity tests, to meet the opacity emission standard at all times during which the source is meeting the mass or concentration emission standard. The Administrator will promulgate the new opacity emission standard in the Federal Register.

(iv) After the Administrator promulgates an adjusted opacity emission standard for an affected source, the owner or operator of such source shall be subject to the new opacity emission standard, and the new opacity emission standard shall apply to such source during any subsequent performance tests.

## (i) Extension of compliance with emission standards.

(1) Until an extension of compliance has been granted by the Administrator (or a State with an approved permit program) under this paragraph, the owner or operator of an affected source subject to the requirements of this section shall comply with all applicable requirements of this part.

(2) Extension of compliance for early reductions and other reductions —

(i) *Early reductions*. Pursuant to section 112(i)(5) of the Act, if the owner or operator of an existing source demonstrates that the source has achieved a reduction in emissions of hazardous air pollutants in accordance with the provisions of <u>subpart D of</u> this part, the Administrator (or the State with an approved permit program) will grant the owner or operator an extension of compliance with specific requirements of this part, as specified in subpart D.

(ii) Other reductions. Pursuant to section 112(i)(6) of the Act, if the owner or operator of an existing source has installed best available control technology (BACT) (as defined in section 169(3) of the Act) or technology required to meet a lowest achievable emission rate (LAER) (as defined in section 171 of the Act) prior to the promulgation of an emission standard in this part applicable to such source and the same pollutant (or stream of pollutants) controlled pursuant to the BACT or LAER installation, the Administrator will grant the owner or operator an extension of compliance with such emission standard that will apply until the date 5 years after the date on which such installation was achieved, as determined by the Administrator.

(3) Request for extension of compliance. Paragraphs (i)(4) through (i)(7) of this section concern requests for an extension of compliance with a relevant standard under this part (except requests for an extension of compliance under paragraph (i)(2)(i) of this section will be handled through procedures specified in subpart D of this part).

(4)

(i)

(A) The owner or operator of an existing source who is unable to comply with a relevant standard established under this part pursuant to section 112(d) of the Act may request that the Administrator (or a State, when the State has an approved part 70 permit program and the source is required to obtain a part 70 permit under that program, or a State, when the State has been delegated the authority to implement and enforce the emission standard for that source) grant an extension allowing the source up to 1 additional year to comply with the standard, if such additional period is necessary for the installation of controls. An additional extension of up to 3 years may be added for mining waste operations, if the 1-year extension of compliance is insufficient to dry and cover mining waste in order to reduce emissions of any hazardous air pollutant. The owner or operator of an affected source who has requested an extension of compliance under this paragraph and who is otherwise required to obtain a title V permit shall apply for such permit or apply to have the source's title V permit revised to incorporate the conditions of the extension of compliance. The conditions of an extension of compliance granted under this paragraph will be incorporated into the affected source's title V permit according to the provisions of part 70 or Federal title V regulations in this chapter (<u>42 U.S.C. 7661</u>), whichever are applicable.

(B) Any request under this paragraph for an extension of compliance with a relevant standard must be submitted in writing to the appropriate authority no later than 120 days prior to the affected source's compliance date (as specified in <u>paragraphs</u> (b) and (c) of this section), except as provided for in <u>paragraph (i)(4)(i)(C)</u> of this section. Nonfrivolous requests submitted under this paragraph will stay the applicability of the rule as to the emission points in question until such time as the request is granted or denied. A denial will be effective as of the date of denial. Emission standards established under this part may specify alternative dates for the submittal of requests for an extension of compliance if alternatives are appropriate for the source categories affected by those standards.

(C) An owner or operator may submit a compliance extension request after the date specified in paragraph (i)(4)(i)(B) of this section provided the need for the compliance extension arose after that date, and before the otherwise applicable compliance date and the need arose due to circumstances beyond reasonable control of the owner or operator. This request must include, in addition to the information required in paragraph (i)(6)(i) of this section, a statement of the reasons additional time is needed and the date when the owner or operator first learned of the problems. Nonfrivolous requests submitted under this paragraph will stay the applicability of the rule as to the emission points in question until such time as the request is granted or denied. A denial will be effective as of the original compliance date.

(ii) The owner or operator of an existing source unable to comply with a relevant standard established under this part pursuant to section 112(f) of the Act may request that the Administrator grant an extension allowing the source up to 2 years after the standard's effective date to comply with the standard. The Administrator may grant such an extension if he/she finds that such additional period is necessary for the installation of controls and that steps will be taken during the period of the extension to assure that the health of persons will be protected from imminent endangerment. Any request for an extension of compliance with a relevant standard under this paragraph must be submitted in writing to the Administrator not later than 90 calendar days after the effective date of the relevant standard.

(5) The owner or operator of an existing source that has installed BACT or technology required to meet LAER [as specified in <u>paragraph (i)(2)(ii)</u> of this section] prior to the promulgation of a relevant emission standard in this part may request that the Administrator grant an extension allowing the source 5 years from the date on which such installation was achieved, as determined by the Administrator, to comply with the standard. Any request for an extension of compliance with a relevant standard under this paragraph shall be submitted in writing to the Administrator not later than 120 days after the promulgation date of the standard. The Administrator may grant such an extension if he or she finds that the installation of BACT or technology to meet LAER controls the same pollutant (or stream of pollutants) that would be controlled at that source by the relevant emission standard.

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(6)

(i) The request for a compliance extension under <u>paragraph (i)(4)</u> of this section shall include the following information:

(A) A description of the controls to be installed to comply with the standard;

(B) A compliance schedule, including the date by which each step toward compliance will be reached. At a minimum, the list of dates shall include:

(1) The date by which on-site construction, installation of emission control equipment, or a process change is planned to be initiated; and

(2) The date by which final compliance is to be achieved.

(3) The date by which on-site construction, installation of emission control equipment, or a process change is to be completed; and

(4) The date by which final compliance is to be achieved;

(C)-(D)

(ii) The request for a compliance extension under <u>paragraph (i)(5)</u> of this section shall include all information needed to demonstrate to the Administrator's satisfaction that the installation of BACT or technology to meet LAER controls the same pollutant (or stream of pollutants) that would be controlled at that source by the relevant emission standard.

(7) Advice on requesting an extension of compliance may be obtained from the Administrator (or the State with an approved permit program).

(8) Approval of request for extension of compliance. Paragraphs (i)(9) through (i)(14) of this section concern approval of an extension of compliance requested under paragraphs (i)(4) through (i)(6) of this section.

(9) Based on the information provided in any request made under <u>paragraphs (i)(4)</u> through <u>(i)(6)</u> of this section, or other information, the Administrator (or the State with an approved permit program) may grant an extension of compliance with an emission standard, as specified in <u>paragraphs (i)(4)</u> and <u>(i)(5)</u> of this section.

(10) The extension will be in writing and will-

(i) Identify each affected source covered by the extension;

(ii) Specify the termination date of the extension;

(iii) Specify the dates by which steps toward compliance are to be taken, if appropriate;

(iv) Specify other applicable requirements to which the compliance extension applies (e.g., performance tests); and

(v)

(A) Under paragraph (i)(4), specify any additional conditions that the Administrator (or the State) deems necessary to assure installation of the necessary controls and protection of the health of persons during the extension period; or

(B) Under paragraph (i)(5), specify any additional conditions that the Administrator deems necessary to assure the proper operation and maintenance of the installed controls during the extension period.

(11) The owner or operator of an existing source that has been granted an extension of compliance under paragraph (i)(10) of this section may be required to submit to the Administrator (or the State with an approved permit program) progress reports indicating whether the steps toward compliance outlined in the compliance schedule have been reached. The contents of the progress reports and the dates by which they shall be submitted will be specified in the written extension of compliance granted under paragraph (i)(10) of this section.

(12)

(i) The Administrator (or the State with an approved permit program) will notify the owner or operator in writing of approval or intention to deny approval of a request for an extension of compliance within 30 calendar days after receipt of sufficient information to evaluate a request submitted under paragraph (i)(4)(i) or (i)(5) of this section. The Administrator (or the State) will notify the owner or operator in writing of the status of his/her application, that is, whether the application contains sufficient information to make a determination, within 30 calendar days after receipt of the original application and within 30

calendar days after receipt of any supplementary information that is submitted. The 30-day approval or denial period will begin after the owner or operator has been notified in writing that his/her application is complete.

(ii) When notifying the owner or operator that his/her application is not complete, the Administrator will specify the information needed to complete the application and provide notice of opportunity for the applicant to present, in writing, within 30 calendar days after he/she is notified of the incomplete application, additional information or arguments to the Administrator to enable further action on the application.

(iii) Before denying any request for an extension of compliance, the Administrator (or the State with an approved permit program) will notify the owner or operator in writing of the Administrator's (or the State's) intention to issue the denial, together with—

(A) Notice of the information and findings on which the intended denial is based; and

(B) Notice of opportunity for the owner or operator to present in writing, within 15 calendar days after he/she is notified of the intended denial, additional information or arguments to the Administrator (or the State) before further action on the request.

(iv) The Administrator's final determination to deny any request for an extension will be in writing and will set forth the specific grounds on which the denial is based. The final determination will be made within 30 calendar days after presentation of additional information or argument (if the application is complete), or within 30 calendar days after the final date specified for the presentation if no presentation is made.

(13)

(i) The Administrator will notify the owner or operator in writing of approval or intention to deny approval of a request for an extension of compliance within 30 calendar days after receipt of sufficient information to evaluate a request submitted under <u>paragraph (i)(4)(ii)</u> of this section. The 30-day approval or denial period will begin after the owner or operator has been notified in writing that his/her application is complete. The Administrator (or the State) will notify the owner or operator in writing of the status of his/her application, that is, whether the application contains sufficient information to make a determination, within 15 calendar days after receipt of the original application and within 15 calendar days after receipt of any supplementary information that is submitted.

(ii) When notifying the owner or operator that his/her application is not complete, the Administrator will specify the information needed to complete the application and provide notice of opportunity for the applicant to present, in writing, within 15 calendar days after he/she is notified of the incomplete application, additional information or arguments to the Administrator to enable further action on the application.

(iii) Before denying any request for an extension of compliance, the Administrator will notify the owner or operator in writing of the Administrator's intention to issue the denial, together with—

(A) Notice of the information and findings on which the intended denial is based; and

(B) Notice of opportunity for the owner or operator to present in writing, within 15 calendar days after he/she is notified of the intended denial, additional information or arguments to the Administrator before further action on the request.

(iv) A final determination to deny any request for an extension will be in writing and will set forth the specific grounds on which the denial is based. The final determination will be made within 30 calendar days after presentation of additional information or argument (if the application is complete), or within 30 calendar days after the final date specified for the presentation if no presentation is made.

(14) The Administrator (or the State with an approved permit program) may terminate an extension of compliance at an earlier date than specified if any specification under <u>paragraph (i)(10)(iii)</u> or <u>(iv)</u> of this section is not met. Upon a determination to terminate, the Administrator will notify, in writing, the owner or operator of the Administrator's determination to terminate, together with:

(i) Notice of the reason for termination; and

(ii) Notice of opportunity for the owner or operator to present in writing, within 15 calendar days after he/she is notified of the determination to terminate, additional information or arguments to the Administrator before further action on the termination.

(iii) A final determination to terminate an extension of compliance will be in writing and will set forth the specific grounds on which the termination is based. The final determination will be made within 30 calendar days after presentation of

additional information or arguments, or within 30 calendar days after the final date specified for the presentation if no presentation is made.

(15) [Reserved]

(16) The granting of an extension under this section shall not abrogate the Administrator's authority under section 114 of the Act.

(j) *Exemption from compliance with emission standards.* The President may exempt any stationary source from compliance with any relevant standard established pursuant to section 112 of the Act for a period of not more than 2 years if the President determines that the technology to implement such standard is not available and that it is in the national security interests of the United States to do so. An exemption under this paragraph may be extended for 1 or more additional periods, each period not to exceed 2 years.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>67 FR 16599</u>, Apr. 5, 2002; <u>68 FR 32600</u>, May 30, 2003; <u>71 FR 20454</u>, Apr. 20, 2006; <u>85 FR 73885</u>, Nov. 19, 2020; <u>86 FR 13821</u>, Mar. 11, 2021]

# § 63.7 Performance testing requirements.

(a) Applicability and performance test dates.

(1) The applicability of this section is set out in  $\S 63.1(a)(4)$ .

(2) Except as provided in <u>paragraph (a)(4)</u> of this section, if required to do performance testing by a relevant standard, and unless a waiver of performance testing is obtained under this section or the conditions of <u>paragraph (c)(3)(ii)(B)</u> of this section apply, the owner or operator of the affected source must perform such tests within 180 days of the compliance date for such source.

(i)-(viii) [Reserved]

(ix) Except as provided in <u>paragraph (a)(4)</u> of this section, when an emission standard promulgated under this part is more stringent than the standard proposed (see  $\frac{63.6(b)(3)}{1000}$ ), the owner or operator of a new or reconstructed source subject to that standard for which construction or reconstruction is commenced between the proposal and promulgation dates of the standard shall comply with performance testing requirements within 180 days after the standard's effective date, or within 180 days after startup of the source, whichever is later. If the promulgated standard is more stringent than the proposed standard, the owner or operator chooses to demonstrate compliance with either the proposed or the promulgated standard. If the owner or operator shall conduct a second performance test within 3 years and 180 days after the effective date of the standard, or after startup of the source, whichever is later, to demonstrate compliance with the promulgated standard.

(3) The Administrator may require an owner or operator to conduct performance tests at the affected source at any other time when the action is authorized by section 114 of the Act.

(4) If a force majeure is about to occur, occurs, or has occurred for which the affected owner or operator intends to assert a claim of force majeure:

(i) The owner or operator shall notify the Administrator, in writing as soon as practicable following the date the owner or operator first knew, or through due diligence should have known that the event may cause or caused a delay in testing beyond the regulatory deadline specified in paragraph (a)(2) or (a)(3) of this section, or elsewhere in this part, but the notification must occur before the performance test deadline unless the initial force majeure or a subsequent force majeure event delays the notice, and in such cases, the notification shall occur as soon as practicable.

(ii) The owner or operator shall provide to the Administrator a written description of the force majeure event and a rationale for attributing the delay in testing beyond the regulatory deadline to the force majeure; describe the measures taken or to be taken to minimize the delay; and identify a date by which the owner or operator proposes to conduct the performance test. The performance test shall be conducted as soon as practicable after the force majeure occurs.

(iii) The decision as to whether or not to grant an extension to the performance test deadline is solely within the discretion of the Administrator. The Administrator will notify the owner or operator in writing of approval or disapproval of the request for an extension as soon as practicable.

(iv) Until an extension of the performance test deadline has been approved by the Administrator under <u>paragraphs</u> (a)(4)(i), (a)(4)(ii), and (a)(4)(iii) of this section, the owner or operator of the affected facility remains strictly subject to the requirements of this part.

### (b) Notification of performance test.

(1) The owner or operator of an affected source must notify the Administrator in writing of his or her intention to conduct a performance test at least 60 calendar days before the performance test is initially scheduled to begin to allow the Administrator, upon request, to review an approve the site-specific test plan required under <u>paragraph (c)</u> of this section and to have an observer present during the test.

(2) In the event the owner or operator is unable to conduct the performance test on the date specified in the notification requirement specified in <u>paragraph (b)(1)</u> of this section due to unforeseeable circumstances beyond his or her control, the owner or operator must notify the Administrator as soon as practicable and without delay prior to the scheduled performance test date and specify the date when the performance test is rescheduled. This notification of delay in conducting the performance test shall not relieve the owner or operator of legal responsibility for compliance with any other applicable provisions of this part or with any other applicable Federal, State, or local requirement, nor will it prevent the Administrator from implementing or enforcing this part or taking any other action under the Act.

## (c) *Quality assurance program.*

(1) The results of the quality assurance program required in this paragraph will be considered by the Administrator when he/she determines the validity of a performance test.

(2)

(i) *Submission of site-specific test plan*. Before conducting a required performance test, the owner or operator of an affected source shall develop and, if requested by the Administrator, shall submit a site-specific test plan to the Administrator for approval. The test plan shall include a test program summary, the test schedule, data quality objectives, and both an internal and external quality assurance (QA) program. Data quality objectives are the pretest expectations of precision, accuracy, and completeness of data.

(ii) The internal QA program shall include, at a minimum, the activities planned by routine operators and analysts to provide an assessment of test data precision; an example of internal QA is the sampling and analysis of replicate samples.

(iii) The performance testing shall include a test method performance audit (PA) during the performance test. The PAs consist of blind audit samples supplied by an accredited audit sample provider and analyzed during the performance test in order to provide a measure of test data bias. Gaseous audit samples are designed to audit the performance of the sampling system as well as the analytical system and must be collected by the sampling system during the compliance test just as the compliance samples are collected. If a liquid or solid audit sample is designed to audit the sampling system, it must also be collected by the sampling system during the compliance test. If multiple sampling systems or sampling trains are used during the compliance test for any of the test methods, the tester is only required to use one of the sampling systems per method to collect the audit sample. The audit sample must be analyzed by the same analyst using the same analytical reagents and analytical system and at the same time as the compliance samples. Retests are required when there is a failure to produce acceptable results for an audit sample. However, if the audit results do not affect the compliance or noncompliance status of the affected facility, the compliance authority may waive the reanalysis requirement, further audits, or retests and accept the results of the compliance test. Acceptance of the test results shall constitute a waiver of the reanalysis requirement, further audits, or retests. The compliance authority may also use the audit sample failure and the compliance test results as evidence to determine the compliance or noncompliance status of the affected facility. A blind audit sample is a sample whose value is known only to the sample provider and is not revealed to the tested facility until after they report the measured value of the audit sample. For pollutants that exist in the gas phase at ambient temperature, the audit sample shall consist of an appropriate concentration of the pollutant in air or nitrogen that can be introduced into the sampling system of the test method at or near the same entry point as a sample from the emission source. If no gas phase audit samples are available, an acceptable alternative is a sample of the pollutant in the same matrix that would be produced when the sample is recovered from the sampling system as required by the test method. For samples that exist only in a liquid or solid form at ambient temperature, the audit sample shall consist of an appropriate concentration of the pollutant in the same matrix that would be produced when the sample is recovered from the sampling system as required by the test method. An accredited audit sample provider (AASP) is an organization that has been accredited to prepare audit samples by an independent, third party accrediting body.

(A) The source owner, operator, or representative of the tested facility shall obtain an audit sample, if commercially available, from an AASP for each test method used for regulatory compliance purposes. No audit samples are required for the following test methods: Methods 3A and 3C of appendix A-3 of part 60 of this chapter; Methods 6C, 7E, 9, and 10 of appendix A-4 of part 60; Methods 18 and 19 of appendix A-6 of part 60; Methods 20, 22, and 25A of appendix A-7 of part

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60; Methods 30A and 30B of appendix A-8 of part 60; and Methods 303, 318, 320, and 321 of appendix A of this part. If multiple sources at a single facility are tested during a compliance test event, only one audit sample is required for each method used during a compliance test. The compliance authority responsible for the compliance test may waive the requirement to include an audit sample if they believe that an audit sample is not necessary. "Commercially available" means that two or more independent AASPs have blind audit samples available for purchase. If the source owner, operator, or representative cannot find an audit sample for a specific method, the owner, operator, or representative shall consult the EPA Web site at the following URL, <u>www.epa.gov/ttn/emc</u>, to confirm whether there is a source that can supply an audit sample for that method. If the EPA Web site does not list an available audit sample at least 60 days prior to the beginning of the compliance test, the source owner, operator, or representative shall not be required to include an audit sample as part of the quality assurance program for the compliance test. When ordering an audit sample, the source owner, operator, or representative shall give the sample provider an estimate for the concentration of each pollutant that is emitted by the source or the estimated concentration of each pollutant based on the permitted level and the name, address, and phone number of the compliance authority. The source owner, operator, or representative shall report the results for the audit sample along with a summary of the emission test results for the audited pollutant to the compliance authority and shall report the results of the audit sample to the AASP. The source owner, operator, or representative shall make both reports at the same time and in the same manner or shall report to the compliance authority first and then report to the AASP. If the method being audited is a method that allows the samples to be analyzed in the field and the tester plans to analyze the samples in the field, the tester may analyze the audit samples prior to collecting the emission samples provided a representative of the compliance authority is present at the testing site. The tester may request, and the compliance authority may grant, a waiver to the requirement that a representative of the compliance authority must be present at the testing site during the field analysis of an audit sample. The source owner, operator, or representative may report the results of the audit sample to the compliance authority and then report the results of the audit sample to the AASP prior to collecting any emission samples. The test protocol and final test report shall document whether an audit sample was ordered and utilized and the pass/fail results as applicable.

(B) An AASP shall have and shall prepare, analyze, and report the true value of audit samples in accordance with a written technical criteria document that describes how audit samples will be prepared and distributed in a manner that will ensure the integrity of the audit sample program. An acceptable technical criteria document shall contain standard operating procedures for all of the following operations:

(1) Preparing the sample;

(2) Confirming the true concentration of the sample;

(3) Defining the acceptance limits for the results from a well qualified tester. This procedure must use well established statistical methods to analyze historical results from well qualified testers. The acceptance limits shall be set so that there is 95 percent confidence that 90 percent of well qualified labs will produce future results that are within the acceptance limit range;

(4) Providing the opportunity for the compliance authority to comment on the selected concentration level for an audit sample;

(5) Distributing the sample to the user in a manner that guarantees that the true value of the sample is unknown to the user;

(6) Recording the measured concentration reported by the user and determining if the measured value is within acceptable limits;

(7) Reporting the results from each audit sample in a timely manner to the compliance authority and to the source owner, operator, or representative by the AASP. The AASP shall make both reports at the same time and in the same manner or shall report to the compliance authority first and then report to the source owner, operator, or representative. The results shall include the name of the facility tested, the date on which the compliance test was conducted, the name of the company performing the sample collection, the name of the company that analyzed the compliance samples including the audit sample, the measured result for the audit sample, and whether the testing company passed or failed the audit. The AASP shall report the true value of the audit sample to the compliance authority. The AASP may report the true value to the source owner, operator, or representative if the AASP's operating plan ensures that no laboratory will receive the same audit sample twice.

(8) Evaluating the acceptance limits of samples at least once every two years to determine in consultation with the voluntary consensus standard body if they should be changed.

(9) Maintaining a database, accessible to the compliance authorities, of results from the audit that shall include the name of the facility tested, the date on which the compliance test was conducted, the name of the company performing the sample collection, the name of the company that analyzed the compliance samples including the audit sample, the measured result

for the audit sample, the true value of the audit sample, the acceptance range for the measured value, and whether the testing company passed or failed the audit.

(C) The accrediting body shall have a written technical criteria document that describes how it will ensure that the AASP is operating in accordance with the AASP technical criteria document that describes how audit samples are to be prepared and distributed. This document shall contain standard operating procedures for all of the following operations:

(1) Checking audit samples to confirm their true value as reported by the AASP.

(2) Performing technical systems audits of the AASP's facilities and operating procedures at least once every two years.

(3) Providing standards for use by the voluntary consensus standard body to approve the accrediting body that will accredit the audit sample providers.

(D) The technical criteria documents for the accredited sample providers and the accrediting body shall be developed through a public process guided by a voluntary consensus standards body (VCSB). The VCSB shall operate in accordance with the procedures and requirements in the Office of Management and Budget *Circular A-119*. A copy of Circular A-119 is available upon request by writing the Office of Information and Regulatory Affairs, Office of Management and Budget, 725 17th Street, NW., Washington, DC 20503, by calling (202) 395-6880 or downloading online

at <u>http://standards.gov/standards\_gov/a119.cfm</u>. The VCSB shall approve all accrediting bodies. The Administrator will review all technical criteria documents. If the technical criteria documents do not meet the minimum technical requirements in <u>paragraphs (c)(2)(iii)(B)</u> through (C) of this section, the technical criteria documents are not acceptable and the proposed audit sample program is not capable of producing audit samples of sufficient quality to be used in a compliance test. All acceptable technical criteria documents shall be posted on the EPA Web site at the following URL, <u>http://www.epa.gov/ttn/emc</u>.

(iv) The owner or operator of an affected source shall submit the site-specific test plan to the Administrator upon the Administrator's request at least 60 calendar days before the performance test is scheduled to take place, that is, simultaneously with the notification of intention to conduct a performance test required under <u>paragraph (b)</u> of this section, or on a mutually agreed upon date.

(v) The Administrator may request additional relevant information after the submittal of a site-specific test plan.

(3) Approval of site-specific test plan.

(i) The Administrator will notify the owner or operator of approval or intention to deny approval of the site-specific test plan (if review of the site-specific test plan is requested) within 30 calendar days after receipt of the original plan and within 30 calendar days after receipt of any supplementary information that is submitted under <u>paragraph (c)(3)(i)(B)</u> of this section. Before disapproving any site-specific test plan, the Administrator will notify the applicant of the Administrator's intention to disapprove the plan together with—

(A) Notice of the information and findings on which the intended disapproval is based; and

(B) Notice of opportunity for the owner or operator to present, within 30 calendar days after he/she is notified of the intended disapproval, additional information to the Administrator before final action on the plan.

(ii) In the event that the Administrator fails to approve or disapprove the site-specific test plan within the time period specified in <u>paragraph (c)(3)(i)</u> of this section, the following conditions shall apply:

(A) If the owner or operator intends to demonstrate compliance using the test method(s) specified in the relevant standard or with only minor changes to those tests methods (see <u>paragraph (e)(2)(i)</u> of this section), the owner or operator must conduct the performance test within the time specified in this section using the specified method(s);

(B) If the owner or operator intends to demonstrate compliance by using an alternative to any test method specified in the relevant standard, the owner or operator is authorized to conduct the performance test using an alternative test method after the Administrator approves the use of the alternative method when the Administrator approves the site-specific test plan (if review of the site-specific test plan is requested) or after the alternative method is approved (see <u>paragraph (f)</u> of this section). However, the owner or operator is authorized to conduct the performance test using an alternative method in the absence of notification of approval 45 days after submission of the site-specific test plan or request to use an alternative method. The owner or operator is authorized to conduct the performance test within 60 calendar days after he/she is authorized to demonstrate compliance using an alternative test method. Notwithstanding the requirements in the preceding three sentences, the owner or operator may proceed to conduct the performance test as required in this section (without the Administrator's

prior approval of the site-specific test plan) if he/she subsequently chooses to use the specified testing and monitoring methods instead of an alternative.

(iii) Neither the submission of a site-specific test plan for approval, nor the Administrator's approval or disapproval of a plan, nor the Administrator's failure to approve or disapprove a plan in a timely manner shall—

(A) Relieve an owner or operator of legal responsibility for compliance with any applicable provisions of this part or with any other applicable Federal, State, or local requirement; or

(B) Prevent the Administrator from implementing or enforcing this part or taking any other action under the Act.

(d) *Performance testing facilities.* If required to do performance testing, the owner or operator of each new source and, at the request of the Administrator, the owner or operator of each existing source, shall provide performance testing facilities as follows:

(1) Sampling ports adequate for test methods applicable to such source. This includes:

(i) Constructing the air pollution control system such that volumetric flow rates and pollutant emission rates can be accurately determined by applicable test methods and procedures; and

(ii) Providing a stack or duct free of cyclonic flow during performance tests, as demonstrated by applicable test methods and procedures;

(2) Safe sampling platform(s);

- (3) Safe access to sampling platform(s);
- (4) Utilities for sampling and testing equipment; and

(5) Any other facilities that the Administrator deems necessary for safe and adequate testing of a source.

(e) Conduct of performance tests.

(1) Performance tests shall be conducted under such conditions as the Administrator specifies to the owner or operator based on representative performance (i.e., performance based on normal operating conditions) of the affected source. Operations during periods of startup, shutdown, and malfunction shall not constitute representative conditions for the purpose of a performance test, nor shall emissions in excess of the level of the relevant standard during periods of startup, shutdown, and malfunction be considered a violation of the relevant standard unless otherwise specified in the relevant standard or a determination of noncompliance is made under  $\frac{§ 63.6(e)}{2}$ . Upon request, the owner or operator shall make available to the Administrator such records as may be necessary to determine the conditions of performance tests.

(2) Performance tests shall be conducted and data shall be reduced in accordance with the test methods and procedures set forth in this section, in each relevant standard, and, if required, in applicable appendices of <u>parts 51</u>, <u>60</u>, <u>61</u>, and <u>63 of this chapter</u> unless the Administrator—

(i) Specifies or approves, in specific cases, the use of a test method with minor changes in methodology (see definition in  $\S$  <u>63.90(a)</u>). Such changes may be approved in conjunction with approval of the site-specific test plan (see <u>paragraph (c)</u> of this section); or

(ii) Approves the use of an intermediate or major change or alternative to a test method (see definitions in  $\S$  63.90(a)), the results of which the Administrator has determined to be adequate for indicating whether a specific affected source is in compliance; or

(iii) Approves shorter sampling times or smaller sample volumes when necessitated by process variables or other factors; or

(iv) Waives the requirement for performance tests because the owner or operator of an affected source has demonstrated by other means to the Administrator's satisfaction that the affected source is in compliance with the relevant standard.

(3) Unless otherwise specified in a relevant standard or test method, each performance test shall consist of three separate runs using the applicable test method. Each run shall be conducted for the time and under the conditions specified in the relevant standard. For the purpose of determining compliance with a relevant standard, the arithmetic mean of the results of the three runs shall apply. Upon receiving approval from the Administrator, results of a test run may be replaced with results of an additional test run in the event that—

(i) A sample is accidentally lost after the testing team leaves the site; or

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(ii) Conditions occur in which one of the three runs must be discontinued because of forced shutdown; or

(iii) Extreme meteorological conditions occur; or

(iv) Other circumstances occur that are beyond the owner or operator's control.

(4) Nothing in <u>paragraphs (e)(1)</u> through (e)(3) of this section shall be construed to abrogate the Administrator's authority to require testing under section 114 of the Act.

(f) Use of an alternative test method —

(1) *General*. Until authorized to use an intermediate or major change or alternative to a test method, the owner or operator of an affected source remains subject to the requirements of this section and the relevant standard.

(2) The owner or operator of an affected source required to do performance testing by a relevant standard may use an alternative test method from that specified in the standard provided that the owner or operator—

(i) Notifies the Administrator of his or her intention to use an alternative test method at least 60 days before the performance test is scheduled to begin;

(ii) Uses Method 301 in <u>appendix A of this part</u> to validate the alternative test method. This may include the use of specific procedures of Method 301 if use of such procedures are sufficient to validate the alternative test method; and

(iii) Submits the results of the Method 301 validation process along with the notification of intention and the justification for not using the specified test method. The owner or operator may submit the information required in this paragraph well in advance of the deadline specified in <u>paragraph (f)(2)(i)</u> of this section to ensure a timely review by the Administrator in order to meet the performance test date specified in this section or the relevant standard.

(3) The Administrator will determine whether the owner or operator's validation of the proposed alternative test method is adequate and issue an approval or disapproval of the alternative test method. If the owner or operator intends to demonstrate compliance by using an alternative to any test method specified in the relevant standard, the owner or operator is authorized to conduct the performance test using an alternative test method after the Administrator approves the use of the alternative method. However, the owner or operator is authorized to conduct the performance test using an alternative test method after submission of the request to use an alternative method and the absence of notification of approval/disapproval 45 days after submission of the request to use an alternative method and the request satisfies the requirements in paragraph (f)(2) of this section. The owner or operator is authorized to conduct the performance test within 60 calendar days after he/she is authorized to demonstrate compliance using an alternative test method. Notwithstanding the requirements in the preceding three sentences, the owner or operator may proceed to conduct the performance test as required in this section (without the Administrator's prior approval of the site-specific test plan) if he/she subsequently chooses to use the specified testing and monitoring methods instead of an alternative.

(4) If the Administrator finds reasonable grounds to dispute the results obtained by an alternative test method for the purposes of demonstrating compliance with a relevant standard, the Administrator may require the use of a test method specified in a relevant standard.

(5) If the owner or operator uses an alternative test method for an affected source during a required performance test, the owner or operator of such source shall continue to use the alternative test method for subsequent performance tests at that affected source until he or she receives approval from the Administrator to use another test method as allowed under  $\frac{1}{5}$  63.7(f).

(6) Neither the validation and approval process nor the failure to validate an alternative test method shall abrogate the owner or operator's responsibility to comply with the requirements of this part.

#### (g) Data analysis, recordkeeping, and reporting.

(1) Unless otherwise specified in a relevant standard or test method, or as otherwise approved by the Administrator in writing, results of a performance test shall include the analysis of samples, determination of emissions, and raw data. A performance test is "completed" when field sample collection is terminated. The owner or operator of an affected source shall report the results of the performance test to the Administrator before the close of business on the 60th day following the completion of the performance test, unless specified otherwise in a relevant standard or as approved otherwise in writing by the Administrator (see § 63.9(i)). The results of the performance test shall be submitted as part of the notification of compliance status required under § 63.9(h). Before a title V permit has been issued to the owner or operator of an affected source, the owner or operator shall send the results of the performance test to the Administrator. After a title V permit has

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been issued to the owner or operator of an affected source, the owner or operator shall send the results of the performance test to the appropriate permitting authority.

(2) Contents of a performance test, CMS performance evaluation, or CMS quality assurance test report (electronic or paper submitted copy). Unless otherwise specified in a relevant standard, test method, CMS performance specification, or quality assurance requirement for a CMS, or as otherwise approved by the Administrator in writing, the report shall include the elements identified in paragraphs (g)(2)(i) through (vi) of this section.

(i) General identification information for the facility including a mailing address, the physical address, the owner or operator or responsible official (where applicable) and his/her email address, and the appropriate Federal Registry System (FRS) number for the facility.

(ii) Purpose of the test including the applicable regulation requiring the test, the pollutant(s) and other parameters being measured, the applicable emission standard, and any process parameter component, and a brief process description.

(iii) Description of the emission unit tested including fuel burned, control devices, and vent characteristics; the appropriate source classification code (SCC); the permitted maximum process rate (where applicable); and the sampling location.

(iv) Description of sampling and analysis procedures used and any modifications to standard procedures, quality assurance procedures and results, record of process operating conditions that demonstrate the applicable test conditions are met, and values for any operating parameters for which limits were being set during the test.

(v) Where a test method, CEMS, PEMS, or COMS performance specification, or on-going quality assurance requirement for a CEMS, PEMS, or COMS requires you record or report, the following shall be included in your report: Record of preparation of standards, record of calibrations, raw data sheets for field sampling, raw data sheets for field and laboratory analyses, chain-of-custody documentation, and example calculations for reported results.

(vi) Identification of the company conducting the performance test including the primary office address, telephone number, and the contact for this test including his/her email address.

(3) For a minimum of 5 years after a performance test is conducted, the owner or operator shall retain and make available, upon request, for inspection by the Administrator the records or results of such performance test and other data needed to determine emissions from an affected source.

(h) Waiver of performance tests.

(1) Until a waiver of a performance testing requirement has been granted by the Administrator under this paragraph, the owner or operator of an affected source remains subject to the requirements of this section.

(2) Individual performance tests may be waived upon written application to the Administrator if, in the Administrator's judgment, the source is meeting the relevant standard(s) on a continuous basis, or the source is being operated under an extension of compliance, or the owner or operator has requested an extension of compliance and the Administrator is still considering that request.

## (3) Request to waive a performance test.

test shall accompany the information required for the request for an extension of compliance. If no extension of compliance is requested or if the owner or operator has requested an extension of compliance and the Administrator is still considering that request, the application for a waiver of an initial performance test shall be submitted at least 60 days before the performance test if the site-specific test plan under paragraph (c) of this section is not submitted.

(ii) If an application for a waiver of a subsequent performance test is made, the application may accompany any required compliance progress report, compliance status report, or excess emissions and continuous monitoring system performance report [such as those required under  $\S$  63.6(i),  $\S$  63.9(h), and  $\S$  63.10(e) or specified in a relevant standard or in the source's title V permit], but it shall be submitted at least 60 days before the performance test if the site-specific test plan required under paragraph (c) of this section is not submitted.

(iii) Any application for a waiver of a performance test shall include information justifying the owner or operator's request for a waiver, such as the technical or economic infeasibility, or the impracticality, of the affected source performing the required test.

(4) Approval of request to waive performance test. The Administrator will approve or deny a request for a waiver of a performance test made under paragraph (h)(3) of this section when he/she-

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(i) Approves or denies an extension of compliance under  $\S 63.6(i)(8)$ ; or

(ii) Approves or disapproves a site-specific test plan under  $\frac{63.7(c)(3)}{2}$ ; or

(iii) Makes a determination of compliance following the submission of a required compliance status report or excess emissions and continuous monitoring systems performance report; or

(iv) Makes a determination of suitable progress towards compliance following the submission of a compliance progress report, whichever is applicable.

(5) Approval of any waiver granted under this section shall not abrogate the Administrator's authority under the Act or in any way prohibit the Administrator from later canceling the waiver. The cancellation will be made only after notice is given to the owner or operator of the affected source.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>65 FR 62215</u>, Oct. 17, 2000; <u>67 FR 16602</u>, Apr. 5, 2002; <u>72 FR 27443</u>, May 16, 2007; <u>75 FR 55655</u>, Sept. 13, 2010; <u>79 FR 11277</u>, Feb. 27, 2014; <u>81 FR 59825</u>, Aug. 30, 2016; <u>83 FR 56725</u>, Nov. 14, 2018]

### § 63.8 Monitoring requirements.

(a) Applicability.

(1) The applicability of this section is set out in  $\S 63.1(a)(4)$ .

(2) For the purposes of this part, all CMS required under relevant standards shall be subject to the provisions of this section upon promulgation of performance specifications for CMS as specified in the relevant standard or otherwise by the Administrator.

(3) [Reserved]

(4) Additional monitoring requirements for control devices used to comply with provisions in relevant standards of this part are specified in  $\frac{63.11}{1}$ .

(b) Conduct of monitoring.

(1) Monitoring shall be conducted as set forth in this section and the relevant standard(s) unless the Administrator—

(i) Specifies or approves the use of minor changes in methodology for the specified monitoring requirements and procedures (see  $\S$  63.90(a) for definition); or

(ii) Approves the use of an intermediate or major change or alternative to any monitoring requirements or procedures (see  $\underline{\S}$  <u>63.90(a)</u> for definition).

(iii) Owners or operators with flares subject to  $\frac{63.11(b)}{2}$  are not subject to the requirements of this section unless otherwise specified in the relevant standard.

(2)

(i) When the emissions from two or more affected sources are combined before being released to the atmosphere, the owner or operator may install an applicable CMS for each emission stream or for the combined emissions streams, provided the monitoring is sufficient to demonstrate compliance with the relevant standard.

(ii) If the relevant standard is a mass emission standard and the emissions from one affected source are released to the atmosphere through more than one point, the owner or operator must install an applicable CMS at each emission point unless the installation of fewer systems is—

(A) Approved by the Administrator; or

(B) Provided for in a relevant standard (e.g., instead of requiring that a CMS be installed at each emission point before the effluents from those points are channeled to a common control device, the standard specifies that only one CMS is required to be installed at the vent of the control device).

(3) When more than one CMS is used to measure the emissions from one affected source (e.g., multiple breechings, multiple outlets), the owner or operator shall report the results as required for each CMS. However, when one CMS is used as a backup to another CMS, the owner or operator shall report the results from the CMS used to meet the monitoring requirements of this part. If both such CMS are used during a particular reporting period to meet the monitoring requirements of this part, then the owner or operator shall report the results from each CMS for the relevant compliance period.

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(c) Operation and maintenance of continuous monitoring systems.

(1) The owner or operator of an affected source shall maintain and operate each CMS as specified in this section, or in a relevant standard, and in a manner consistent with good air pollution control practices.

(i) The owner or operator of an affected source must maintain and operate each CMS as specified in  $\frac{63.6(e)(1)}{2}$ .

(ii) The owner or operator must keep the necessary parts for routine repairs of the affected CMS equipment readily available.

(iii) The owner or operator of an affected source must develop a written startup, shutdown, and malfunction plan for CMS as specified in  $\S 63.6(e)(3)$ .

(2)

(i) All CMS must be installed such that representative measures of emissions or process parameters from the affected source are obtained. In addition, CEMS must be located according to procedures contained in the applicable performance specification(s).

(ii) Unless the individual subpart states otherwise, the owner or operator must ensure the read out (that portion of the CMS that provides a visual display or record), or other indication of operation, from any CMS required for compliance with the emission standard is readily accessible on site for operational control or inspection by the operator of the equipment.

(3) All CMS shall be installed, operational, and the data verified as specified in the relevant standard either prior to or in conjunction with conducting performance tests under  $\S$  63.7. Verification of operational status shall, at a minimum, include completion of the manufacturer's written specifications or recommendations for installation, operation, and calibration of the system.

(4) Except for system breakdowns, out-of-control periods, repairs, maintenance periods, calibration checks, and zero (low-level) and high-level calibration drift adjustments, all CMS, including COMS and CEMS, shall be in continuous operation and shall meet minimum frequency of operation requirements as follows:

(i) All COMS shall complete a minimum of one cycle of sampling and analyzing for each successive 10-second period and one cycle of data recording for each successive 6-minute period.

(ii) All CEMS for measuring emissions other than opacity shall complete a minimum of one cycle of operation (sampling, analyzing, and data recording) for each successive 15-minute period.

(5) Unless otherwise approved by the Administrator, minimum procedures for COMS shall include a method for producing a simulated zero opacity condition and an upscale (high-level) opacity condition using a certified neutral density filter or other related technique to produce a known obscuration of the light beam. Such procedures shall provide a system check of all the analyzer's internal optical surfaces and all electronic circuitry, including the lamp and photodetector assembly normally used in the measurement of opacity.

(6) The owner or operator of a CMS that is not a CPMS, which is installed in accordance with the provisions of this part and the applicable CMS performance specification(s), must check the zero (low-level) and high-level calibration drifts at least once daily in accordance with the written procedure specified in the performance evaluation plan developed under <u>paragraphs</u> (e)(3)(i) and (ii) of this section. The zero (low-level) and high-level calibration drifts must be adjusted, at a minimum, whenever the 24-hour zero (low-level) drift exceeds two times the limits of the applicable performance specification(s) specified in the relevant standard. The system shall allow the amount of excess zero (low-level) and high-level drift measured at the 24-hour interval checks to be recorded and quantified whenever specified. For COMS, all optical and instrumental surfaces exposed to the effluent gases must be cleaned prior to performing the zero (low-level) and high-level drift adjustments; the optical surfaces and instrumental surfaces must be cleaned when the cumulative automatic zero compensation, if applicable, exceeds 4 percent opacity. The CPMS must be calibrated prior to use for the purposes of complying with this section. The CPMS must be checked daily for indication that the system is responding. If the CPMS system includes an internal system check, results must be recorded and checked daily for proper operation.

(7)

(i) A CMS is out of control if-

(A) The zero (low-level), mid-level (if applicable), or high-level calibration drift (CD) exceeds two times the applicable CD specification in the applicable performance specification or in the relevant standard; or

(B) The CMS fails a performance test audit (e.g., cylinder gas audit), relative accuracy audit, relative accuracy test audit, or linearity test audit; or

(C) The COMS CD exceeds two times the limit in the applicable performance specification in the relevant standard.

(ii) When the CMS is out of control, the owner or operator of the affected source shall take the necessary corrective action and shall repeat all necessary tests which indicate that the system is out of control. The owner or operator shall take corrective action and conduct retesting until the performance requirements are below the applicable limits. The beginning of the out-of-control period is the hour the owner or operator conducts a performance check (e.g., calibration drift) that indicates an exceedance of the performance requirements established under this part. The end of the out-of-control period is the hour following the completion of corrective action and successful demonstration that the system is within the allowable limits. During the period the CMS is out of control, recorded data shall not be used in data averages and calculations, or to meet any data availability requirement established under this part.

(8) The owner or operator of a CMS that is out of control as defined in <u>paragraph (c)(7)</u> of this section shall submit all information concerning out-of-control periods, including start and end dates and hours and descriptions of corrective actions taken, in the excess emissions and continuous monitoring system performance report required in <u>§ 63.10(e)(3)</u>.

(d) Quality control program.

(1) The results of the quality control program required in this paragraph will be considered by the Administrator when he/she determines the validity of monitoring data.

(2) The owner or operator of an affected source that is required to use a CMS and is subject to the monitoring requirements of this section and a relevant standard shall develop and implement a CMS quality control program. As part of the quality control program, the owner or operator shall develop and submit to the Administrator for approval upon request a site-specific performance evaluation test plan for the CMS performance evaluation required in paragraph (e)(3)(i) of this section, according to the procedures specified in paragraph (e). In addition, each quality control program shall include, at a minimum, a written protocol that describes procedures for each of the following operations:

(i) Initial and any subsequent calibration of the CMS;

(ii) Determination and adjustment of the calibration drift of the CMS;

(iii) Preventive maintenance of the CMS, including spare parts inventory;

(iv) Data recording, calculations, and reporting;

(v) Accuracy audit procedures, including sampling and analysis methods; and

(vi) Program of corrective action for a malfunctioning CMS.

(3) The owner or operator shall keep these written procedures on record for the life of the affected source or until the affected source is no longer subject to the provisions of this part, to be made available for inspection, upon request, by the Administrator. If the performance evaluation plan is revised, the owner or operator shall keep previous (i.e., superseded) versions of the performance evaluation plan on record to be made available for inspection, upon request, by the Administrator, for a period of 5 years after each revision to the plan. Where relevant, e.g., program of corrective action for a malfunctioning CMS, these written procedures may be incorporated as part of the affected source's startup, shutdown, and malfunction plan to avoid duplication of planning and recordkeeping efforts.

(e) Performance evaluation of continuous monitoring systems —

(1) *General.* When required by a relevant standard, and at any other time the Administrator may require under section 114 of the Act, the owner or operator of an affected source being monitored shall conduct a performance evaluation of the CMS. Such performance evaluation shall be conducted according to the applicable specifications and procedures described in this section or in the relevant standard.

(2) Notification of performance evaluation. The owner or operator shall notify the Administrator in writing of the date of the performance evaluation simultaneously with the notification of the performance test date required under  $\frac{63.7(b)}{100}$  or at least 60 days prior to the date the performance evaluation is scheduled to begin if no performance test is required.

(3)

(i) *Submission of site-specific performance evaluation test plan.* Before conducting a required CMS performance evaluation, the owner or operator of an affected source shall develop and submit a site-specific performance evaluation test plan to the

Administrator for approval upon request. The performance evaluation test plan shall include the evaluation program objectives, an evaluation program summary, the performance evaluation schedule, data quality objectives, and both an internal and external QA program. Data quality objectives are the pre-evaluation expectations of precision, accuracy, and completeness of data.

(ii) The internal QA program shall include, at a minimum, the activities planned by routine operators and analysts to provide an assessment of CMS performance. The external QA program shall include, at a minimum, systems audits that include the opportunity for on-site evaluation by the Administrator of instrument calibration, data validation, sample logging, and documentation of quality control data and field maintenance activities.

(iii) The owner or operator of an affected source shall submit the site-specific performance evaluation test plan to the Administrator (if requested) at least 60 days before the performance test or performance evaluation is scheduled to begin, or on a mutually agreed upon date, and review and approval of the performance evaluation test plan by the Administrator will occur with the review and approval of the site-specific test plan (if review of the site-specific test plan is requested).

(iv) The Administrator may request additional relevant information after the submittal of a site-specific performance evaluation test plan.

(v) In the event that the Administrator fails to approve or disapprove the site-specific performance evaluation test plan within the time period specified in  $\frac{63.7(c)(3)}{2}$ , the following conditions shall apply:

(A) If the owner or operator intends to demonstrate compliance using the monitoring method(s) specified in the relevant standard, the owner or operator shall conduct the performance evaluation within the time specified in this subpart using the specified method(s);

(B) If the owner or operator intends to demonstrate compliance by using an alternative to a monitoring method specified in the relevant standard, the owner or operator shall refrain from conducting the performance evaluation until the Administrator approves the use of the alternative method. If the Administrator does not approve the use of the alternative method within 30 days before the performance evaluation is scheduled to begin, the performance evaluation deadlines specified in <u>paragraph</u> (e)(4) of this section may be extended such that the owner or operator shall conduct the performance evaluation within 60 calendar days after the Administrator approves the use of the alternative method. Notwithstanding the requirements in the preceding two sentences, the owner or operator may proceed to conduct the performance evaluation as required in this section (without the Administrator's prior approval of the site-specific performance evaluation test plan) if he/she subsequently chooses to use the specified monitoring method(s) instead of an alternative.

(vi) Neither the submission of a site-specific performance evaluation test plan for approval, nor the Administrator's approval or disapproval of a plan, nor the Administrator's failure to approve or disapprove a plan in a timely manner shall—

(A) Relieve an owner or operator of legal responsibility for compliance with any applicable provisions of this part or with any other applicable Federal, State, or local requirement; or

(B) Prevent the Administrator from implementing or enforcing this part or taking any other action under the Act.

(4) Conduct of performance evaluation and performance evaluation dates. The owner or operator of an affected source shall conduct a performance evaluation of a required CMS during any performance test required under § 63.7 in accordance with the applicable performance specification as specified in the relevant standard. Notwithstanding the requirement in the previous sentence, if the owner or operator of an affected source elects to submit COMS data for compliance with a relevant opacity emission standard as provided under § 63.6(h)(7), he/she shall conduct a performance evaluation of the COMS as specified in the relevant standard, before the performance test required under § 63.7 is conducted in time to submit the results of the performance evaluation as specified in paragraph (e)(5)(ii) of this section. If a performance test is not required, or the requirement for a performance test has been waived under § 63.7(h), the owner or operator of an affected source, as specified in  $\frac{63.7(a)}{10}$ , or as otherwise specified in the relevant standard.

## (5) Reporting performance evaluation results.

(i) The owner or operator shall furnish the Administrator a copy of a written report of the results of the performance evaluation containing the information specified in  $\S 63.7(g)(2)(i)$  through (vi) simultaneously with the results of the performance test required under  $\S 63.7$  or within 60 days of completion of the performance evaluation, unless otherwise specified in a relevant standard.

(ii) The owner or operator of an affected source using a COMS to determine opacity compliance during any performance test required under  $\S$  <u>63.7</u> and described in  $\S$  <u>63.6(d)(6)</u> shall furnish the Administrator two or, upon request, three copies of a written report of the results of the COMS performance evaluation under this paragraph. The copies shall be provided at least 15 calendar days before the performance test required under  $\S$  <u>63.7</u> is conducted.

(f) Use of an alternative monitoring method —

(1) *General.* Until permission to use an alternative monitoring procedure (minor, intermediate, or major changes; see definition in  $\frac{63.90(a)}{1}$ ) has been granted by the Administrator under this <u>paragraph (f)(1)</u>, the owner or operator of an affected source remains subject to the requirements of this section and the relevant standard.

(2) After receipt and consideration of written application, the Administrator may approve alternatives to any monitoring methods or procedures of this part including, but not limited to, the following:

(i) Alternative monitoring requirements when installation of a CMS specified by a relevant standard would not provide accurate measurements due to liquid water or other interferences caused by substances within the effluent gases;

(ii) Alternative monitoring requirements when the affected source is infrequently operated;

(iii) Alternative monitoring requirements to accommodate CEMS that require additional measurements to correct for stack moisture conditions;

(iv) Alternative locations for installing CMS when the owner or operator can demonstrate that installation at alternate locations will enable accurate and representative measurements;

(v) Alternate methods for converting pollutant concentration measurements to units of the relevant standard;

(vi) Alternate procedures for performing daily checks of zero (low-level) and high-level drift that do not involve use of high-level gases or test cells;

(vii) Alternatives to the American Society for Testing and Materials (ASTM) test methods or sampling procedures specified by any relevant standard;

(viii) Alternative CMS that do not meet the design or performance requirements in this part, but adequately demonstrate a definite and consistent relationship between their measurements and the measurements of opacity by a system complying with the requirements as specified in the relevant standard. The Administrator may require that such demonstration be performed for each affected source; or

(ix) Alternative monitoring requirements when the effluent from a single affected source or the combined effluent from two or more affected sources is released to the atmosphere through more than one point.

(3) If the Administrator finds reasonable grounds to dispute the results obtained by an alternative monitoring method, requirement, or procedure, the Administrator may require the use of a method, requirement, or procedure specified in this section or in the relevant standard. If the results of the specified and alternative method, requirement, or procedure do not agree, the results obtained by the specified method, requirement, or procedure shall prevail.

(4)

(i) Request to use alternative monitoring procedure. An owner or operator who wishes to use an alternative monitoring procedure must submit an application to the Administrator as described in paragraph (f)(4)(ii) of this section. The application may be submitted at any time provided that the monitoring procedure is not the performance test method used to demonstrate compliance with a relevant standard or other requirement. If the alternative monitoring procedure will serve as the performance test method that is to be used to demonstrate compliance with a relevant standard, the application must be submitted at least 60 days before the performance evaluation is scheduled to begin and must meet the requirements for an alternative test method under  $\frac{5}{5}$  63.7(f).

(ii) The application must contain a description of the proposed alternative monitoring system which addresses the four elements contained in the definition of monitoring in § 63.2 and a performance evaluation test plan, if required, as specified in paragraph (e)(3) of this section. In addition, the application must include information justifying the owner or operator's request for an alternative monitoring method, such as the technical or economic infeasibility, or the impracticality, of the affected source using the required method.

(iii) The owner or operator may submit the information required in this paragraph well in advance of the submittal dates specified in paragraph (f)(4)(i) above to ensure a timely review by the Administrator in order to meet the compliance demonstration date specified in this section or the relevant standard.

(iv) Application for minor changes to monitoring procedures, as specified in <u>paragraph (b)(1)</u> of this section, may be made in the site-specific performance evaluation plan.

(5) Approval of request to use alternative monitoring procedure.

(i) The Administrator will notify the owner or operator of approval or intention to deny approval of the request to use an alternative monitoring method within 30 calendar days after receipt of the original request and within 30 calendar days after receipt of any supplementary information that is submitted. If a request for a minor change is made in conjunction with site-specific performance evaluation plan, then approval of the plan will constitute approval of the minor change. Before disapproving any request to use an alternative monitoring method, the Administrator will notify the applicant of the Administrator's intention to disapprove the request together with—

(A) Notice of the information and findings on which the intended disapproval is based; and

(B) Notice of opportunity for the owner or operator to present additional information to the Administrator before final action on the request. At the time the Administrator notifies the applicant of his or her intention to disapprove the request, the Administrator will specify how much time the owner or operator will have after being notified of the intended disapproval to submit the additional information.

(ii) The Administrator may establish general procedures and criteria in a relevant standard to accomplish the requirements of paragraph (f)(5)(i) of this section.

(iii) If the Administrator approves the use of an alternative monitoring method for an affected source under <u>paragraph</u> (f)(5)(i) of this section, the owner or operator of such source shall continue to use the alternative monitoring method until he or she receives approval from the Administrator to use another monitoring method as allowed by  $\S$  63.8(f).

(6) Alternative to the relative accuracy test. An alternative to the relative accuracy test for CEMS specified in a relevant standard may be requested as follows:

(i) Criteria for approval of alternative procedures. An alternative to the test method for determining relative accuracy is available for affected sources with emission rates demonstrated to be less than 50 percent of the relevant standard. The owner or operator of an affected source may petition the Administrator under paragraph (f)(6)(ii) of this section to substitute the relative accuracy test in section 7 of Performance Specification 2 with the procedures in section 10 if the results of a performance test conducted according to the requirements in § 63.7, or other tests performed following the criteria in § 63.7, demonstrate that the emission rate of the pollutant of interest in the units of the relevant standard is less than 50 percent of the relevant standard. For affected sources subject to emission limitations expressed as control efficiency levels, the owner or operator may petition the Administrator to substitute the relative accuracy test with the procedures in section 10 of Performance Specification 2 if the control device exhaust emission rate is less than 50 percent of the level needed to meet the control efficiency requirement. The alternative procedures do not apply if the CEMS is used continuously to determine compliance with the relevant standard.

(ii) *Petition to use alternative to relative accuracy test.* The petition to use an alternative to the relative accuracy test shall include a detailed description of the procedures to be applied, the location and the procedure for conducting the alternative, the concentration or response levels of the alternative relative accuracy materials, and the other equipment checks included in the alternative procedure(s). The Administrator will review the petition for completeness and applicability. The Administrator's determination to approve an alternative will depend on the intended use of the CEMS data and may require specifications more stringent than in Performance Specification 2.

(iii) *Rescission of approval to use alternative to relative accuracy test.* The Administrator will review the permission to use an alternative to the CEMS relative accuracy test and may rescind such permission if the CEMS data from a successful completion of the alternative relative accuracy procedure indicate that the affected source's emissions are approaching the level of the relevant standard. The criterion for reviewing the permission is that the collection of CEMS data shows that emissions have exceeded 70 percent of the relevant standard for any averaging period, as specified in the relevant standard. For affected sources subject to emission limitations expressed as control efficiency levels, the criterion for reviewing the permission is that the collection of CEMS data shows that emissions have exceeded 70 percent of the relevant standard for any averaging here exceeded 70 percent of the level needed to meet the control efficiency requirement for any averaging period, as specified in the relevant standard. The owner or operator of the affected source shall maintain records and determine the level of emissions relative to the criterion for permission to

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use an alternative for relative accuracy testing. If this criterion is exceeded, the owner or operator shall notify the Administrator within 10 days of such occurrence and include a description of the nature and cause of the increased emissions. The Administrator will review the notification and may rescind permission to use an alternative and require the owner or operator to conduct a relative accuracy test of the CEMS as specified in section 7 of Performance Specification 2. The Administrator will review the notification and may rescind permission to use an alternative and require the owner or operator to conduct a relative accuracy test of the CEMS as specified in section 7 of Performance Specification 2.

(g) Reduction of monitoring data.

(1) The owner or operator of each CMS must reduce the monitoring data as specified in <u>paragraphs (g)(1)</u> through (5) of this section.

(2) The owner or operator of each COMS shall reduce all data to 6-minute averages calculated from 36 or more data points equally spaced over each 6-minute period. Data from CEMS for measurement other than opacity, unless otherwise specified in the relevant standard, shall be reduced to 1-hour averages computed from four or more data points equally spaced over each 1-hour period, except during periods when calibration, quality assurance, or maintenance activities pursuant to provisions of this part are being performed. During these periods, a valid hourly average shall consist of at least two data points with each representing a 15-minute period. Alternatively, an arithmetic or integrated 1-hour average of CEMS data may be used. Time periods for averaging are defined in  $\frac{5 \times 63.2}{2}$ .

(3) The data may be recorded in reduced or nonreduced form (e.g., ppm pollutant and percent O<sub>2</sub> or ng/J of pollutant).

(4) All emission data shall be converted into units of the relevant standard for reporting purposes using the conversion procedures specified in that standard. After conversion into units of the relevant standard, the data may be rounded to the same number of significant digits as used in that standard to specify the emission limit (e.g., rounded to the nearest 1 percent opacity).

(5) Monitoring data recorded during periods of unavoidable CMS breakdowns, out-of-control periods, repairs, maintenance periods, calibration checks, and zero (low-level) and high-level adjustments must not be included in any data average computed under this part. For the owner or operator complying with the requirements of  $\frac{63.10(b)(2)(vii)(A)}{(A)}$  or (B), data averages must include any data recorded during periods of monitor breakdown or malfunction.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>64 FR 7468</u>, Feb. 12, 1999; <u>67 FR 16603</u>, Apr. 5, 2002; <u>71 FR 20455</u>, Apr. 20, 2006; <u>79 FR 11277</u>, Feb. 27, 2014; <u>83 FR 56725</u>, Nov. 14, 2018]

## § 63.9 Notification requirements.

(a) Applicability and general information.

(1) The applicability of this section is set out in  $\S 63.1(a)(4)$ .

(2) For affected sources that have been granted an extension of compliance under <u>subpart D of this part</u>, the requirements of this section do not apply to those sources while they are operating under such compliance extensions.

(3) If any State requires a notice that contains all the information required in a notification listed in this section, the owner or operator may send the Administrator a copy of the notice sent to the State to satisfy the requirements of this section for that notification.

(4)

(i) Before a State has been delegated the authority to implement and enforce notification requirements established under this part, the owner or operator of an affected source in such State subject to such requirements shall submit notifications to the appropriate Regional Office of the EPA (to the attention of the Director of the Division indicated in the list of the EPA Regional Offices in  $\frac{63.13}{1.13}$ ).

(ii) After a State has been delegated the authority to implement and enforce notification requirements established under this part, the owner or operator of an affected source in such State subject to such requirements shall submit notifications to the delegated State authority (which may be the same as the permitting authority). In addition, if the delegated (permitting) authority is the State, the owner or operator shall send a copy of each notification submitted to the State to the appropriate Regional Office of the EPA, as specified in paragraph (a)(4)(i) of this section. The Regional Office may waive this requirement for any notifications at its discretion.

(b) Initial notifications.

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(1)

(i) The requirements of this paragraph apply to the owner or operator of an affected source when such source becomes subject to a relevant standard.

(ii) If an area source subsequently becomes a major source that is subject to the emission standard or other requirement, such source shall be subject to the notification requirements of this section. Area sources previously subject to major source requirements that become major sources again are also subject to the notification requirements of this paragraph and must submit the notification according to the requirements of <u>paragraph (k)</u> of this section.

(iii) Affected sources that are required under this paragraph to submit an initial notification may use the application for approval of construction or reconstruction under  $\S$  63.5(d) of this subpart, if relevant, to fulfill the initial notification requirements of this paragraph.

(2) The owner or operator of an affected source that has an initial startup before the effective date of a relevant standard under this part shall notify the Administrator in writing that the source is subject to the relevant standard. The notification, which shall be submitted not later than 120 calendar days after the effective date of the relevant standard (or within 120 calendar days after the source becomes subject to the relevant standard), shall provide the following information:

(i) The name and address of the owner or operator;

(ii) The address (i.e., physical location) of the affected source;

(iii) An identification of the relevant standard, or other requirement, that is the basis of the notification and the source's compliance date;

(iv) A brief description of the nature, size, design, and method of operation of the source and an identification of the types of emission points within the affected source subject to the relevant standard and types of hazardous air pollutants emitted; and

(v) A statement of whether the affected source is a major source or an area source.

(3) [Reserved]

(4) The owner or operator of a new or reconstructed major affected source for which an application for approval of construction or reconstruction is required under  $\S 63.5(d)$  must provide the following information in writing to the Administrator:

(i) A notification of intention to construct a new major-emitting affected source, reconstruct a major-emitting affected source, or reconstruct a major source such that the source becomes a major-emitting affected source with the application for approval of construction or reconstruction as specified in  $\S$  63.5(d)(1)(i); and

(ii)-(iv) [Reserved]

(v) A notification of the actual date of startup of the source, delivered or postmarked within 15 calendar days after that date.

(5) The owner or operator of a new or reconstructed affected source for which an application for approval of construction or reconstruction is not required under  $\frac{63.5(d)}{1000}$  must provide the following information in writing to the Administrator:

(i) A notification of intention to construct a new affected source, reconstruct an affected source, or reconstruct a source such that the source becomes an affected source, and

(ii) A notification of the actual date of startup of the source, delivered or postmarked within 15 calendar days after that date.

(iii) Unless the owner or operator has requested and received prior permission from the Administrator to submit less than the information in  $\S$  63.5(d), the notification must include the information required on the application for approval of construction or reconstruction as specified in  $\S$  63.5(d)(1)(i).

(c) Request for extension of compliance. If the owner or operator of an affected source cannot comply with a relevant standard by the applicable compliance date for that source, or if the owner or operator has installed BACT or technology to meet LAER consistent with  $\S$  63.6(i)(5) of this subpart, he/she may submit to the Administrator (or the State with an approved permit program) a request for an extension of compliance as specified in  $\S$  63.6(i)(4) through  $\S$  63.6(i)(6).

(d) Notification that source is subject to special compliance requirements. An owner or operator of a new source that is subject to special compliance requirements as specified in  $\S$  63.6(b)(3) and  $\S$  63.6(b)(4) shall notify the Administrator of
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his/her compliance obligations not later than the notification dates established in <u>paragraph (b)</u> of this section for new sources that are not subject to the special provisions.

(e) Notification of performance test. The owner or operator of an affected source shall notify the Administrator in writing of his or her intention to conduct a performance test at least 60 calendar days before the performance test is scheduled to begin to allow the Administrator to review and approve the site-specific test plan required under  $\S$  63.7(c), if requested by the Administrator, and to have an observer present during the test.

(f) Notification of opacity and visible emission observations. The owner or operator of an affected source shall notify the Administrator in writing of the anticipated date for conducting the opacity or visible emission observations specified in § 63.6(h)(5), if such observations are required for the source by a relevant standard. The notification shall be submitted with the notification of the performance test date, as specified in paragraph (e) of this section, or if no performance test is required or visibility or other conditions prevent the opacity or visible emission observations from being conducted concurrently with the initial performance test required under § 63.7, the owner or operator shall deliver or postmark the notification not less than 30 days before the opacity or visible emission observations are scheduled to take place.

(g) Additional notification requirements for sources with continuous monitoring systems. The owner or operator of an affected source required to use a CMS by a relevant standard shall furnish the Administrator written notification as follows:

(1) A notification of the date the CMS performance evaluation under  $\frac{\& 63.8(e)}{\& 63.7(b)}$  is scheduled to begin, submitted simultaneously with the notification of the performance test date required under  $\frac{\& 63.7(b)}{\& 63.7(b)}$ . If no performance test is required, or if the requirement to conduct a performance test has been waived for an affected source under  $\frac{\& 63.7(b)}{\& 63.7(b)}$ , the owner or operator shall notify the Administrator in writing of the date of the performance evaluation at least 60 calendar days before the evaluation is scheduled to begin;

(2) A notification that COMS data results will be used to determine compliance with the applicable opacity emission standard during a performance test required by  $\frac{63.7}{10}$  in lieu of Method 9 or other opacity emissions test method data, as allowed by  $\frac{63.6(h)(7)(ii)}{10}$ , if compliance with an opacity emission standard is required for the source by a relevant standard. The notification shall be submitted at least 60 calendar days before the performance test is scheduled to begin; and

(3) A notification that the criterion necessary to continue use of an alternative to relative accuracy testing, as provided by  $\S$  <u>63.8(f)(6)</u>, has been exceeded. The notification shall be delivered or postmarked not later than 10 days after the occurrence of such exceedance, and it shall include a description of the nature and cause of the increased emissions.

(h) Notification of compliance status.

(1) The requirements of <u>paragraphs (h)(2)</u> through (h)(4) of this section apply when an affected source becomes subject to a relevant standard.

(2)

(i) Before a title V permit has been issued to the owner or operator of an affected source, and each time a notification of compliance status is required under this part, the owner or operator of such source shall submit to the Administrator a notification of compliance status, signed by the responsible official who shall certify its accuracy, attesting to whether the source has complied with the relevant standard. The notification shall list—

(A) The methods that were used to determine compliance;

(B) The results of any performance tests, opacity or visible emission observations, continuous monitoring system (CMS) performance evaluations, and/or other monitoring procedures or methods that were conducted;

(C) The methods that will be used for determining continuing compliance, including a description of monitoring and reporting requirements and test methods;

(D) The type and quantity of hazardous air pollutants emitted by the source (or surrogate pollutants if specified in the relevant standard), reported in units and averaging times and in accordance with the test methods specified in the relevant standard;

(E) If the relevant standard applies to both major and area sources, an analysis demonstrating whether the affected source is a major source (using the emissions data generated for this notification);

(F) A description of the air pollution control equipment (or method) for each emission point, including each control device (or method) for each hazardous air pollutant and the control efficiency (percent) for each control device (or method); and

(G) A statement by the owner or operator of the affected existing, new, or reconstructed source as to whether the source has complied with the relevant standard or other requirements.

(ii) The notification must be sent before the close of business on the 60th day following the completion of the relevant compliance demonstration activity specified in the relevant standard (unless a different reporting period is specified in the standard, in which case the letter must be sent before the close of business on the day the report of the relevant testing or monitoring results is required to be delivered or postmarked). For example, the notification shall be sent before the close of business on the 60th (or other required) day following completion of the initial performance test and again before the close of business on the 60th (or other required) day following the completion of any subsequent required performance test. If no performance test is required but opacity or visible emission observations are required to demonstrate compliance with an opacity or visible emission standard under this part, the notification of compliance status shall be sent before close of business on the 30th day following the completion of opacity or visible emission observations. Notifications may be combined as long as the due date requirement for each notification is met.

(3) After a title V permit has been issued to the owner or operator of an affected source, the owner or operator of such source shall comply with all requirements for compliance status reports contained in the source's title V permit, including reports required under this part. After a title V permit has been issued to the owner or operator of an affected source, and each time a notification of compliance status is required under this part, the owner or operator of such source shall submit the notification of compliance status to the appropriate permitting authority following completion of the relevant compliance demonstration activity specified in the relevant standard.

(4) [Reserved]

(5) If an owner or operator of an affected source submits estimates or preliminary information in the application for approval of construction or reconstruction required in  $\S$  63.5(d) in place of the actual emissions data or control efficiencies required in paragraphs (d)(1)(ii)(H) and (d)(2) of  $\S$  63.5, the owner or operator shall submit the actual emissions data and other correct information as soon as available but no later than with the initial notification of compliance status required in this section.

(6) Advice on a notification of compliance status may be obtained from the Administrator.

(i) Adjustment to time periods or postmark deadlines for submittal and review of required communications.

(1)

(i) Until an adjustment of a time period or postmark deadline has been approved by the Administrator under <u>paragraphs</u> (i)(2) and (i)(3) of this section, the owner or operator of an affected source remains strictly subject to the requirements of this part.

(ii) An owner or operator shall request the adjustment provided for in <u>paragraphs (i)(2)</u> and <u>(i)(3)</u> of this section each time he or she wishes to change an applicable time period or postmark deadline specified in this part.

(2) Notwithstanding time periods or postmark deadlines specified in this part for the submittal of information to the Administrator by an owner or operator, or the review of such information by the Administrator, such time periods or deadlines may be changed by mutual agreement between the owner or operator and the Administrator. An owner or operator who wishes to request a change in a time period or postmark deadline for a particular requirement shall request the adjustment in writing as soon as practicable before the subject activity is required to take place. The owner or operator shall include in the request whatever information he or she considers useful to convince the Administrator that an adjustment is warranted.

(3) If, in the Administrator's judgment, an owner or operator's request for an adjustment to a particular time period or postmark deadline is warranted, the Administrator will approve the adjustment. The Administrator will notify the owner or operator in writing of approval or disapproval of the request for an adjustment within 15 calendar days of receiving sufficient information to evaluate the request.

(4) If the Administrator is unable to meet a specified deadline, he or she will notify the owner or operator of any significant delay and inform the owner or operator of the amended schedule.

(j) *Change in information already provided*. Any change in the information already provided under this section shall be provided to the Administrator within 15 calendar days after the change. The owner or operator of a major source that reclassifies to area source status is also subject to the notification requirements of this paragraph. The owner or operator may submit the application for reclassification with the regulatory authority (*e.g.*, permit application) according to <u>paragraph</u> (<u>k</u>) of this section to fulfill the requirements of this paragraph, but the information required in <u>paragraphs (j)(1)</u> through (<u>4</u>) of

this section must be included. A source which reclassified after January 25, 2018, and before January 19, 2021, and has not yet provided the notification of a change in information is required to provide such notification no later than February 2, 2021, according to the requirements of <u>paragraph (k)</u> of this section. Beginning January 19, 2021, the owner or operator of a major source that reclassifies to area source status must submit the notification according to the requirements of <u>paragraph (k)</u> of this section. A notification of reclassification must contain the following information:

(1) The name and address of the owner or operator;

(2) The address (*i.e.*, physical location) of the affected source;

(3) An identification of the standard being reclassified from and to (if applicable); and

(4) Date of effectiveness of the reclassification.

(k) *Electronic submission of notifications or reports*. If you are required to submit notifications or reports following the procedure specified in this <u>paragraph (k)</u>, you must submit notifications or reports to the EPA via the EPA's Compliance and Emissions Data Reporting Interface (CEDRI), which can be accessed through the EPA's Central Data Exchange (CDX) (<u>https://cdx.epa.gov/</u>). The notification or report must be submitted by the deadline specified. The EPA will make all the information submitted through CEDRI available to the public without further notice to you. Do not use CEDRI to submit information you claim as confidential business information (CBI). Although we do not expect persons to assert a claim of CBI, if you wish to assert a CBI claim for some of the information in the report or notification, you must submit the information claimed to be CBI according to the procedures in <u>paragraph (k)(3)</u> of this section.

(1) If you are required to electronically submit a notification or report by this <u>paragraph (k)</u> through CEDRI in the EPA's CDX, you may assert a claim of EPA system outage for failure to timely comply with the electronic submittal requirement. To assert a claim of EPA system outage, you must meet the requirements outlined in <u>paragraphs (k)(1)(i)</u> through <u>(vii)</u> of this section.

(i) You must have been or will be precluded from accessing CEDRI and submitting a required notification or report within the time prescribed due to an outage of either the EPA's CEDRI or CDX systems.

(ii) The outage must have occurred within the period of time beginning 5 business days prior to the date that the notification or report is due.

(iii) The outage may be planned or unplanned.

(iv) You must submit notification to the Administrator in writing as soon as possible following the date you first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

(v) You must provide to the Administrator a written description identifying:

(A) The date(s) and time(s) when CDX or CEDRI was accessed and the system was unavailable;

(B) A rationale for attributing the delay in submitting beyond the regulatory deadline to EPA system outage;

(C) Measures taken or to be taken to minimize the delay in submitting; and

(D) The date by which you propose to submit, or if you have already met the electronic submittal requirement in this <u>paragraph (k)</u> at the time of the notification, the date you submitted the notification or report.

(vi) The decision to accept the claim of EPA system outage and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(vii) In any circumstance, the notification or report must be submitted electronically as soon as possible after the outage is resolved.

(2) If you are required to electronically submit a notification or report by this <u>paragraph (k)</u> through CEDRI in the EPA's CDX, you may assert a claim of force majeure for failure to timely comply with the electronic submittal requirement. To assert a claim of force majeure, you must meet the requirements outlined in <u>paragraphs (k)(2)(i)</u> through (v) of this section.

(i) You may submit a claim if a force majeure event is about to occur, occurs, or has occurred or there are lingering effects from such an event within the period of time beginning five business days prior to the date the submission is due. For the purposes of this section, a force majeure event is defined as an event that will be or has been caused by circumstances beyond the control of the affected facility, its contractors, or any entity controlled by the affected facility that prevents you from complying with the requirement to submit a notification or report electronically within the time period prescribed. Examples

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of such events are acts of nature (*e.g.*, hurricanes, earthquakes, or floods), acts of war or terrorism, or equipment failure or safety hazard beyond the control of the affected facility (*e.g.*, large scale power outage).

(ii) You must submit notification to the Administrator in writing as soon as possible following the date you first knew, or through due diligence should have known, that the event may cause or has caused a delay in submitting through CEDRI.

(iii) You must provide to the Administrator:

(A) A written description of the force majeure event;

(B) A rationale for attributing the delay in reporting beyond the regulatory deadline to the force majeure event;

(C) Measures taken or to be taken to minimize the delay in reporting; and

(D) The date by which you propose to submit the notification or report, or if you have already met the electronic submittal requirement in this paragraph (k) at the time of the notification, the date you submitted the notification or report.

(iv) The decision to accept the claim of force majeure and allow an extension to the submittal deadline is solely within the discretion of the Administrator.

(v) In any circumstance, the reporting must occur as soon as possible after the force majeure event occurs.

(3) If you wish to assert a CBI claim for some of the information submitted under <u>paragraph (k)</u> of this section, you must submit a complete file, including information claimed to be CBI, to the EPA following the procedures in <u>paragraphs</u> (<u>k)(3)(i)</u> through (<u>iv)</u> of this section. Where a subpart specifies a specific file format for the report or notification for which you are asserting a claim of CBI, the complete file that you submit under this <u>paragraph (k)(3)</u> must be in the same file format specified in the subpart.

(i) Clearly mark the part or all of the information that you claim to be CBI. Information not marked as CBI may be authorized for public release without prior notice. Information marked as CBI will not be disclosed except in accordance with procedures set forth in <u>40 CFR part 2</u>. All CBI claims must be asserted at the time of submission. Anything submitted using CEDRI cannot later be claimed CBI. Furthermore, under CAA section 114(c), emissions data are not entitled to confidential treatment, and the EPA is required to make emissions data available to the public. Thus, emissions data will not be protected as CBI and will be made publicly available.

(ii) You must submit the same file submitted to the CBI office with the CBI omitted to the EPA via the EPA's CDX as described in <u>paragraph (k)</u> of this section.

(iii) The preferred method to receive CBI is for it to be transmitted electronically using email attachments, File Transfer Protocol, or other online file sharing services. Electronic submissions must be transmitted directly to the OAQPS CBI Office at the email address <u>oaqpscbi@epa.gov</u>, and as described above, should include clear CBI markings. Electronic Reporting Tool (ERT) files should be flagged to the attention of the Group Leader, Measurement Policy Group; all other files should be flagged to the attention of the subpart for which you are submitting your notification or report. If assistance is needed with submitting large electronic files that exceed the file size limit for email attachments, and if you do not have your own file sharing service, please email <u>oaqpscbi@epa.gov</u> to request a file transfer link.

(iv) If you cannot transmit the file electronically, you may send CBI information through the postal service to the following address: U.S. EPA, Attn: OAQPS Document Control Officer, Mail Drop: C404-02, 109 T.W. Alexander Drive, P.O. Box 12055, RTP, NC 27711. ERT files should also be flagged to the attention of the Group Leader, Measurement Policy Group; all other files should also be flagged to the attention of the Sector Lead for the subpart for which you are submitting your notification or report. The mailed CBI material should be double wrapped and clearly marked. Any CBI markings should not show through the outer envelope.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>64 FR 7468</u>, Feb. 12, 1999; <u>67 FR 16604</u>, Apr. 5, 2002; <u>68 FR 32601</u>, May 30, 2003; <u>85 FR 73885</u>, Nov. 19, 2020; <u>89 FR 73307</u>, Sept. 10, 2024]

### § 63.10 Recordkeeping and reporting requirements.

(a) Applicability and general information.

(1) The applicability of this section is set out in  $\S 63.1(a)(4)$ .

(2) For affected sources that have been granted an extension of compliance under <u>subpart D of this part</u>, the requirements of this section do not apply to those sources while they are operating under such compliance extensions.

(3) If any State requires a report that contains all the information required in a report listed in this section, an owner or operator may send the Administrator a copy of the report sent to the State to satisfy the requirements of this section for that report.

(4)

(i) Before a State has been delegated the authority to implement and enforce recordkeeping and reporting requirements established under this part, the owner or operator of an affected source in such State subject to such requirements shall submit reports to the appropriate Regional Office of the EPA (to the attention of the Director of the Division indicated in the list of the EPA Regional Offices in  $\S$  63.13).

(ii) After a State has been delegated the authority to implement and enforce recordkeeping and reporting requirements established under this part, the owner or operator of an affected source in such State subject to such requirements shall submit reports to the delegated State authority (which may be the same as the permitting authority). In addition, if the delegated (permitting) authority is the State, the owner or operator shall send a copy of each report submitted to the State to the appropriate Regional Office of the EPA, as specified in paragraph (a)(4)(i) of this section. The Regional Office may waive this requirement for any reports at its discretion.

(5) If an owner or operator of an affected source in a State with delegated authority is required to submit periodic reports under this part to the State, and if the State has an established timeline for the submission of periodic reports that is consistent with the reporting frequency(ies) specified for such source under this part, the owner or operator may change the dates by which periodic reports under this part shall be submitted (without changing the frequency of reporting) to be consistent with the State's schedule by mutual agreement between the owner or operator and the State. For each relevant standard established pursuant to section 112 of the Act, the allowance in the previous sentence applies in each State beginning 1 year after the affected source's compliance date for that standard. Procedures governing the implementation of this provision are specified in  $\frac{\delta 63.9(i)}{i}$ .

(6) If an owner or operator supervises one or more stationary sources affected by more than one standard established pursuant to section 112 of the Act, he/she may arrange by mutual agreement between the owner or operator and the Administrator (or the State permitting authority) a common schedule on which periodic reports required for each source shall be submitted throughout the year. The allowance in the previous sentence applies in each State beginning 1 year after the latest compliance date for any relevant standard established pursuant to section 112 of the Act for any such affected source(s). Procedures governing the implementation of this provision are specified in  $\S 63.9(i)$ .

(7) If an owner or operator supervises one or more stationary sources affected by standards established pursuant to section 112 of the Act (as amended November 15, 1990) and standards set under part 60, part 61, or both such parts of this chapter, he/she may arrange by mutual agreement between the owner or operator and the Administrator (or the State permitting authority) a common schedule on which periodic reports required by each relevant (i.e., applicable) standard shall be submitted throughout the year. The allowance in the previous sentence applies in each State beginning 1 year after the stationary source is required to be in compliance with the relevant section 112 standard, or 1 year after the stationary source is required to be in compliance with the applicable part 60 or part 61 standard, whichever is latest. Procedures governing the implementation of this provision are specified in  $\frac{8}{63.9(i)}$ .

### (b) General recordkeeping requirements.

(1) The owner or operator of an affected source subject to the provisions of this part shall maintain files of all information (including all reports and notifications) required by this part recorded in a form suitable and readily available for expeditious inspection and review. The files shall be retained for at least 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record. At a minimum, the most recent 2 years of data shall be retained on site. The remaining 3 years of data may be retained off site. Such files may be maintained on microfilm, on a computer, on computer floppy disks, on magnetic tape disks, or on microfiche.

(2) The owner or operator of an affected source subject to the provisions of this part shall maintain relevant records for such source of—

(i) The occurrence and duration of each startup or shutdown when the startup or shutdown causes the source to exceed any applicable emission limitation in the relevant emission standards;

(ii) The occurrence and duration of each malfunction of operation (i.e., process equipment) or the required air pollution control and monitoring equipment;

(iii) All required maintenance performed on the air pollution control and monitoring equipment;

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(iv)

(A) Actions taken during periods of startup or shutdown when the source exceeded applicable emission limitations in a relevant standard and when the actions taken are different from the procedures specified in the affected source's startup, shutdown, and malfunction plan (see  $\frac{63.6(e)(3)}{2}$ ); or

(B) Actions taken during periods of malfunction (including corrective actions to restore malfunctioning process and air pollution control and monitoring equipment to its normal or usual manner of operation) when the actions taken are different from the procedures specified in the affected source's startup, shutdown, and malfunction plan (see  $\frac{63.6(e)(3)}{2}$ );

(v) All information necessary, including actions taken, to demonstrate conformance with the affected source's startup, shutdown, and malfunction plan (see  $\S$  <u>63.6(e)(3)</u>) when all actions taken during periods of startup or shutdown (and the startup or shutdown causes the source to exceed any applicable emission limitation in the relevant emission standards), and malfunction (including corrective actions to restore malfunctioning process and air pollution control and monitoring equipment to its normal or usual manner of operation) are consistent with the procedures specified in such plan. (The information needed to demonstrate conformance with the startup, shutdown, and malfunction plan may be recorded using a "checklist," or some other effective form of recordkeeping, in order to minimize the recordkeeping burden for conforming events);

(vi) Each period during which a CMS is malfunctioning or inoperative (including out-of-control periods);

(vii) All required measurements needed to demonstrate compliance with a relevant standard (including, but not limited to, 15minute averages of CMS data, raw performance testing measurements, and raw performance evaluation measurements, that support data that the source is required to report);

(A) This paragraph applies to owners or operators required to install a continuous emissions monitoring system (CEMS) where the CEMS installed is automated, and where the calculated data averages do not exclude periods of CEMS breakdown or malfunction. An automated CEMS records and reduces the measured data to the form of the pollutant emission standard through the use of a computerized data acquisition system. In lieu of maintaining a file of all CEMS subhourly measurements as required under <u>paragraph (b)(2)(vii)</u> of this section, the owner or operator shall retain the most recent consecutive three averaging periods of subhourly measurements and a file that contains a hard copy of the data acquisition system algorithm used to reduce the measured data into the reportable form of the standard.

(B) This paragraph applies to owners or operators required to install a CEMS where the measured data is manually reduced to obtain the reportable form of the standard, and where the calculated data averages do not exclude periods of CEMS breakdown or malfunction. In lieu of maintaining a file of all CEMS subhourly measurements as required under paragraph (b)(2)(vii) of this section, the owner or operator shall retain all subhourly measurements for the most recent reporting period. The subhourly measurements shall be retained for 120 days from the date of the most recent summary or excess emission report submitted to the Administrator.

(C) The Administrator or delegated authority, upon notification to the source, may require the owner or operator to maintain all measurements as required by paragraph (b)(2)(vii), if the administrator or the delegated authority determines these records are required to more accurately assess the compliance status of the affected source.

(viii) All results of performance tests, CMS performance evaluations, and opacity and visible emission observations;

(ix) All measurements as may be necessary to determine the conditions of performance tests and performance evaluations;

(x) All CMS calibration checks;

(xi) All adjustments and maintenance performed on CMS;

(xii) Any information demonstrating whether a source is meeting the requirements for a waiver of recordkeeping or reporting requirements under this part, if the source has been granted a waiver under <u>paragraph (f)</u> of this section;

(xiii) All emission levels relative to the criterion for obtaining permission to use an alternative to the relative accuracy test, if the source has been granted such permission under  $\frac{63.8(f)(6)}{5}$ ; and

(xiv) All documentation supporting initial notifications and notifications of compliance status under <u>§ 63.9</u>.

(3) If an owner or operator determines that his or her existing or new stationary source is in the source category regulated by a standard established pursuant to section 112 of the Act, but that source is not subject to the relevant standard (or other requirement established under this part) because of enforceable limitations on the source's potential to emit, or the source otherwise qualifies for an exclusion, the owner or operator must keep a record of the applicability determination. The

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applicability determination must be kept on site at the source for a period of 5 years after the determination, or until the source changes its operations to become an affected source subject to the relevant standard (or other requirement established under this part), whichever comes first if the determination is made prior to January 19, 2021. The applicability determination must be kept until the source changes its operations to become an affected source subject to the relevant standard (or other requirement established under this part) if the determination was made on or after January 19, 2021. The record of the applicability determination must be signed by the person making the determination and include an emissions analysis (or other information) that demonstrates the owner or operator's conclusion that the source is unaffected (*e.g.*, because the source is an area source). The analysis (or other information) must be sufficiently detailed to allow the Administrator to make an applicability finding for the source with regard to the relevant standard or other requirement. If applicable, the analysis must be performed in accordance with requirements established in relevant <u>subparts of this part</u> for this purpose for particular categories of stationary sources. If relevant, the analysis should be performed in accordance with EPA guidance materials published to assist sources in making applicability determinations under section 112 of the Act, if any. The requirements to determine applicability of a standard under <u>§ 63.1(b)(3)</u> and to record the results of that determination under this <u>paragraph</u> (<u>b)(3)</u> of this section shall not by themselves create an obligation for the owner or operator to obtain a title V permit.

(c) Additional recordkeeping requirements for sources with continuous monitoring systems. In addition to complying with the requirements specified in paragraphs (b)(1) and (b)(2) of this section, the owner or operator of an affected source required to install a CMS by a relevant standard shall maintain records for such source of—

(1) All required CMS measurements (including monitoring data recorded during unavoidable CMS breakdowns and out-ofcontrol periods);

(2)-(4) [Reserved]

(5) The date and time identifying each period during which the CMS was inoperative except for zero (low-level) and high-level checks;

(6) The date and time identifying each period during which the CMS was out of control, as defined in  $\frac{63.8(c)(7)}{5}$ ;

(7) The specific identification (i.e., the date and time of commencement and completion) of each period of excess emissions and parameter monitoring exceedances, as defined in the relevant standard(s), that occurs during startups, shutdowns, and malfunctions of the affected source;

(8) The specific identification (i.e., the date and time of commencement and completion) of each time period of excess emissions and parameter monitoring exceedances, as defined in the relevant standard(s), that occurs during periods other than startups, shutdowns, and malfunctions of the affected source;

(9) [Reserved]

- (10) The nature and cause of any malfunction (if known);
- (11) The corrective action taken or preventive measures adopted;
- (12) The nature of the repairs or adjustments to the CMS that was inoperative or out of control;
- (13) The total process operating time during the reporting period; and
- (14) All procedures that are part of a quality control program developed and implemented for CMS under <u>§ 63.8(d)</u>.

(15) In order to satisfy the requirements of <u>paragraphs (c)(10)</u> through (c)(12) of this section and to avoid duplicative recordkeeping efforts, the owner or operator may use the affected source's startup, shutdown, and malfunction plan or records kept to satisfy the recordkeeping requirements of the startup, shutdown, and malfunction plan specified in § 63.6(e), provided that such plan and records adequately address the requirements of paragraphs (c)(10) through (c)(12).

### (d) General reporting requirements.

(1) Notwithstanding the requirements in this paragraph or <u>paragraph (e)</u> of this section, and except as provided in <u>§ 63.16</u>, the owner or operator of an affected source subject to reporting requirements under this part shall submit reports to the Administrator in accordance with the reporting requirements in the relevant standard(s).

(2) Reporting results of performance tests. Before a title V permit has been issued to the owner or operator of an affected source, the owner or operator shall report the results of any performance test under  $\S$  63.7 to the Administrator. After a title V permit has been issued to the owner or operator of an affected source, the owner or operator shall report the results of a required performance test to the appropriate permitting authority. The owner or operator of an affected source shall report the

results of the performance test to the Administrator (or the State with an approved permit program) before the close of business on the 60th day following the completion of the performance test, unless specified otherwise in a relevant standard or as approved otherwise in writing by the Administrator. The results of the performance test shall be submitted as part of the notification of compliance status required under  $\S$  63.9(h).

(3) Reporting results of opacity or visible emission observations. The owner or operator of an affected source required to conduct opacity or visible emission observations by a relevant standard shall report the opacity or visible emission results (produced using Test Method 9 or Test Method 22, or an alternative to these test methods) along with the results of the performance test required under § 63.7. If no performance test is required, or if visibility or other conditions prevent the opacity or visible emission observations from being conducted concurrently with the performance test required under § 63.7, the owner or operator shall report the opacity or visible emission results before the close of business on the 30th day following the completion of the opacity or visible emission observations.

(4) *Progress reports.* The owner or operator of an affected source who is required to submit progress reports as a condition of receiving an extension of compliance under  $\S$  63.6(i) shall submit such reports to the Administrator (or the State with an approved permit program) by the dates specified in the written extension of compliance.

(5)

(i) Periodic startup, shutdown, and malfunction reports. If actions taken by an owner or operator during a startup or shutdown (and the startup or shutdown causes the source to exceed any applicable emission limitation in the relevant emission standards), or malfunction of an affected source (including actions taken to correct a malfunction) are consistent shall state such information in a startup, shutdown, and malfunction report. Actions taken to minimize emissions during such startups, shutdowns, and malfunctions shall be summarized in the report and may be done in checklist form; if actions taken are the same for each event, only one checklist is necessary. Such a report shall also include the number, duration, and a brief description for each type of malfunction which occurred during the reporting period and which caused or may have caused any applicable emission limitation to be exceeded. Reports shall only be required if a startup or shutdown caused the source to exceed any applicable emission limitation in the relevant emission standards, or if a malfunction occurred during the reporting period. The startup, shutdown, and malfunction report shall consist of a letter, containing the name, title, and signature of the owner or operator or other responsible official who is certifying its accuracy, that shall be submitted to the Administrator semiannually (or on a more frequent basis if specified otherwise in a relevant standard or as established otherwise by the permitting authority in the source's title V permit). The startup, shutdown, and malfunction report shall be delivered or postmarked by the 30th day following the end of each calendar half (or other calendar reporting period, as appropriate). If the owner or operator is required to submit excess emissions and continuous monitoring system performance (or other periodic) reports under this part, the startup, shutdown, and malfunction reports required under this paragraph may be submitted simultaneously with the excess emissions and continuous monitoring system performance (or other) reports. If startup, shutdown, and malfunction reports are submitted with excess emissions and continuous monitoring system performance (or other periodic) reports, and the owner or operator receives approval to reduce the frequency of reporting for the latter under paragraph (e) of this section, the frequency of reporting for the startup, shutdown, and malfunction reports also may be reduced if the Administrator does not object to the intended change. The procedures to implement the allowance in the preceding sentence shall be the same as the procedures specified in paragraph (e)(3) of this section.

(ii) *Immediate startup, shutdown, and malfunction reports.* Notwithstanding the allowance to reduce the frequency of reporting for periodic startup, shutdown, and malfunction reports under paragraph (d)(5)(i) of this section, any time an action taken by an owner or operator during a startup or shutdown that caused the source to exceed any applicable emission limitation in the relevant emission standards, or malfunction (including actions taken to correct a malfunction) is not consistent with the procedures specified in the affected source's startup, shutdown, and malfunction plan, the owner or operator shall report the actions taken for that event within 2 working days after commencing actions inconsistent with the plan followed by a letter within 7 working days after the end of the event. The immediate report required under this paragraph (d)(5)(ii) shall consist of a telephone call (or facsimile (FAX) transmission) to the Administrator within 2 working days after commencing actions inconsistent with the plan, and it shall be followed by a letter, delivered or postmarked within 7 working days after the end of the event, that contains the name, title, and signature of the owner or operator or other responsible official who is certifying its accuracy, explaining the circumstances of the event, the reasons for not following the startup, shutdown, and malfunction plan, describing all excess emissions and/or parameter monitoring exceedances which are believed to have occurred (or could have occurred in the case of malfunctions), and actions taken to minimize emissions in conformance with  $\frac{§ 63.6(e)(1)(i)}{(i)}$ . Notwithstanding the requirements of the owner or operator may

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make alternative reporting arrangements, in advance, with the permitting authority in that State. Procedures governing the arrangement of alternative reporting requirements under this <u>paragraph (d)(5)(ii)</u> are specified in  $\S$  <u>63.9(i)</u>.

(e) Additional reporting requirements for sources with continuous monitoring systems —

(1) *General.* When more than one CEMS is used to measure the emissions from one affected source (e.g., multiple breechings, multiple outlets), the owner or operator shall report the results as required for each CEMS.

(2) Reporting results of continuous monitoring system performance evaluations.

(i) The owner or operator of an affected source required to install a CMS by a relevant standard shall furnish the Administrator a copy of a written report of the results of the CMS performance evaluation, as required under  $\S$  63.8(e), simultaneously with the results of the performance test required under  $\S$  63.7, unless otherwise specified in the relevant standard.

(ii) The owner or operator of an affected source using a COMS to determine opacity compliance during any performance test required under § 63.7 and described in § 63.6(d)(6) shall furnish the Administrator two or, upon request, three copies of a written report of the results of the COMS performance evaluation conducted under § 63.8(e). The copies shall be furnished at least 15 calendar days before the performance test required under § 63.7 is conducted.

(3) Excess emissions and continuous monitoring system performance report and summary report.

(i) Excess emissions and parameter monitoring exceedances are defined in relevant standards. The owner or operator of an affected source required to install a CMS by a relevant standard shall submit an excess emissions and continuous monitoring system performance report and/or a summary report to the Administrator semiannually, except when—

(A) More frequent reporting is specifically required by a relevant standard;

(B) The Administrator determines on a case-by-case basis that more frequent reporting is necessary to accurately assess the compliance status of the source; or

(C) [Reserved]

(D) The affected source is complying with the Performance Track Provisions of  $\S$  63.16, which allows less frequent reporting.

#### (ii) Request to reduce frequency of excess emissions and continuous monitoring system performance

*reports.* Notwithstanding the frequency of reporting requirements specified in <u>paragraph (e)(3)(i)</u> of this section, an owner or operator who is required by a relevant standard to submit excess emissions and continuous monitoring system performance (and summary) reports on a quarterly (or more frequent) basis may reduce the frequency of reporting for that standard to semiannual if the following conditions are met:

(A) For 1 full year (e.g., 4 quarterly or 12 monthly reporting periods) the affected source's excess emissions and continuous monitoring system performance reports continually demonstrate that the source is in compliance with the relevant standard;

(B) The owner or operator continues to comply with all recordkeeping and monitoring requirements specified in this subpart and the relevant standard; and

(C) The Administrator does not object to a reduced frequency of reporting for the affected source, as provided in <u>paragraph</u>  $(\underline{e})(\underline{3})(\underline{iii})$  of this section.

(iii) The frequency of reporting of excess emissions and continuous monitoring system performance (and summary) reports required to comply with a relevant standard may be reduced only after the owner or operator notifies the Administrator in writing of his or her intention to make such a change and the Administrator does not object to the intended change. In deciding whether to approve a reduced frequency of reporting, the Administrator may review information concerning the source's entire previous performance history during the 5-year recordkeeping period prior to the intended change, including performance test results, monitoring data, and evaluations of an owner or operator's conformance with operation and maintenance requirements. Such information may be used by the Administrator to make a judgment about the source's potential for noncompliance in the future. If the Administrator disapproves the owner or operator's request to reduce the frequency of reporting, the Administrator will notify the owner or operator in writing within 45 days after receiving notice of the owner or operator's intention. The notification from the Administrator to the owner or operator will specify the grounds on which the disapproval is based. In the absence of a notice of disapproval within 45 days, approval is automatically granted.

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(iv) As soon as CMS data indicate that the source is not in compliance with any emission limitation or operating parameter specified in the relevant standard, the frequency of reporting shall revert to the frequency specified in the relevant standard, and the owner or operator shall submit an excess emissions and continuous monitoring system performance (and summary) report for the noncomplying emission points at the next appropriate reporting period following the noncomplying event. After demonstrating ongoing compliance with the relevant standard for another full year, the owner or operator may again request approval from the Administrator to reduce the frequency of reporting for that standard, as provided for in paragraphs (e)(3)(ii) and (e)(3)(iii) of this section.

(v) Content and submittal dates for excess emissions and monitoring system performance reports. All excess emissions and monitoring system performance reports and all summary reports, if required, shall be delivered or postmarked by the 30th day following the end of each calendar half or quarter, as appropriate. Written reports of excess emissions or exceedances of process or control system parameters shall include all the information required in paragraphs (c)(5) through (c)(13) of this section, in  $\frac{\$\$ 63.8(c)(7)}{1000}$  and  $\frac{63.8(c)(8)}{1000}$ , and in the relevant standard, and they shall contain the name, title, and signature of the responsible official who is certifying the accuracy of the report. When no excess emissions or exceedances of a parameter have occurred, or a CMS has not been inoperative, out of control, repaired, or adjusted, such information shall be stated in the report.

(vi) Summary report. As required under <u>paragraphs (e)(3)(vii)</u> and <u>(e)(3)(viii)</u> of this section, one summary report shall be submitted for the hazardous air pollutants monitored at each affected source (unless the relevant standard specifies that more than one summary report is required, e.g., one summary report for each hazardous air pollutant monitored). The summary report shall be entitled "Summary Report—Gaseous and Opacity Excess Emission and Continuous Monitoring System Performance" and shall contain the following information:

- (A) The company name and address of the affected source;
- (B) An identification of each hazardous air pollutant monitored at the affected source;
- (C) The beginning and ending dates of the reporting period;
- (D) A brief description of the process units;
- (E) The emission and operating parameter limitations specified in the relevant standard(s);
- (F) The monitoring equipment manufacturer(s) and model number(s);
- (G) The date of the latest CMS certification or audit;
- (H) The total operating time of the affected source during the reporting period;

(I) An emission data summary (or similar summary if the owner or operator monitors control system parameters), including the total duration of excess emissions during the reporting period (recorded in minutes for opacity and hours for gases), the total duration of excess emissions expressed as a percent of the total source operating time during that reporting period, and a breakdown of the total duration of excess emissions during the reporting the reporting period into those that are due to startup/shutdown, control equipment problems, process problems, other known causes, and other unknown causes;

(J) A CMS performance summary (or similar summary if the owner or operator monitors control system parameters), including the total CMS downtime during the reporting period (recorded in minutes for opacity and hours for gases), the total duration of CMS downtime expressed as a percent of the total source operating time during that reporting period, and a breakdown of the total CMS downtime during the reporting period into periods that are due to monitoring equipment malfunctions, nonmonitoring equipment malfunctions, quality assurance/quality control calibrations, other known causes, and other unknown causes;

(K) A description of any changes in CMS, processes, or controls since the last reporting period;

(L) The name, title, and signature of the responsible official who is certifying the accuracy of the report; and

(M) The date of the report.

(vii) If the total duration of excess emissions or process or control system parameter exceedances for the reporting period is less than 1 percent of the total operating time for the reporting period, and CMS downtime for the reporting period is less than 5 percent of the total operating time for the reporting period, only the summary report shall be submitted, and the full excess emissions and continuous monitoring system performance report need not be submitted unless required by the Administrator.

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(viii) If the total duration of excess emissions or process or control system parameter exceedances for the reporting period is 1 percent or greater of the total operating time for the reporting period, or the total CMS downtime for the reporting period is 5 percent or greater of the total operating time for the reporting period, both the summary report and the excess emissions and continuous monitoring system performance report shall be submitted.

(4) Reporting continuous opacity monitoring system data produced during a performance test. The owner or operator of an affected source required to use a COMS shall record the monitoring data produced during a performance test required under  $\frac{5}{3.7}$  and shall furnish the Administrator a written report of the monitoring results. The report of COMS data shall be submitted simultaneously with the report of the performance test reguired in <u>paragraph (d)(2)</u> of this section.

(f) Waiver of recordkeeping or reporting requirements.

(1) Until a waiver of a recordkeeping or reporting requirement has been granted by the Administrator under this paragraph, the owner or operator of an affected source remains subject to the requirements of this section.

(2) Recordkeeping or reporting requirements may be waived upon written application to the Administrator if, in the Administrator's judgment, the affected source is achieving the relevant standard(s), or the source is operating under an extension of compliance, or the owner or operator has requested an extension of compliance and the Administrator is still considering that request.

(3) If an application for a waiver of recordkeeping or reporting is made, the application shall accompany the request for an extension of compliance under  $\frac{63.6(i)}{1}$ , any required compliance progress report or compliance status report required under this part (such as under  $\frac{86.6(i)}{1}$  and  $\frac{63.9(h)}{1}$ ) or in the source's title V permit, or an excess emissions and continuous monitoring system performance report required under <u>paragraph (e)</u> of this section, whichever is applicable. The application shall include whatever information the owner or operator considers useful to convince the Administrator that a waiver of recordkeeping or reporting is warranted.

(4) The Administrator will approve or deny a request for a waiver of recordkeeping or reporting requirements under this paragraph when he/she—

(i) Approves or denies an extension of compliance; or

(ii) Makes a determination of compliance following the submission of a required compliance status report or excess emissions and continuous monitoring systems performance report; or

(iii) Makes a determination of suitable progress towards compliance following the submission of a compliance progress report, whichever is applicable.

(5) A waiver of any recordkeeping or reporting requirement granted under this paragraph may be conditioned on other recordkeeping or reporting requirements deemed necessary by the Administrator.

(6) Approval of any waiver granted under this section shall not abrogate the Administrator's authority under the Act or in any way prohibit the Administrator from later canceling the waiver. The cancellation will be made only after notice is given to the owner or operator of the affected source.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>64 FR 7468</u>, Feb. 12, 1999; <u>67 FR 16604</u>, Apr. 5, 2002; <u>68 FR 32601</u>, May 30, 2003; <u>69 FR 21752</u>, Apr. 22, 2004; <u>71 FR 20455</u>, Apr. 20, 2006; <u>85 FR 73886</u>, Nov. 19, 2020]

# § 63.11 Control device and work practice requirements.

(a) Applicability.

(1) The applicability of this section is set out in  $\S 63.1(a)(4)$ .

(2) This section contains requirements for control devices used to comply with applicable <u>subparts of this part</u>. The requirements are placed here for administrative convenience and apply only to facilities covered by subparts referring to this section.

(3) This section also contains requirements for an alternative work practice used to identify leaking equipment. This alternative work practice is placed here for administrative convenience and is available to all subparts in  $\frac{40 \text{ CFR parts}}{1000 \text{ CFR parts}}$  60, 61, 63, and 65 that require monitoring of equipment with a  $\frac{40 \text{ CFR part } 60}{1000 \text{ CFR part}}$  60, appendix A-7, Method 21 monitor.

(b) Flares.

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(1) Owners or operators using flares to comply with the provisions of this part shall monitor these control devices to assure that they are operated and maintained in conformance with their designs. Applicable subparts will provide provisions stating how owners or operators using flares shall monitor these control devices.

(2) Flares shall be steam-assisted, air-assisted, or non-assisted.

(3) Flares shall be operated at all times when emissions may be vented to them.

(4) Flares shall be designed for and operated with no visible emissions, except for periods not to exceed a total of 5 minutes during any 2 consecutive hours. Test Method 22 in appendix A of <u>part 60 of this chapter</u> shall be used to determine the compliance of flares with the visible emission provisions of this part. The observation period is 2 hours and shall be used according to Method 22.

(5) Flares shall be operated with a flame present at all times. The presence of a flare pilot flame shall be monitored using a thermocouple or any other equivalent device to detect the presence of a flame.

(6) An owner/operator has the choice of adhering to the heat content specifications in <u>paragraph (b)(6)(ii)</u> of this section, and the maximum tip velocity specifications in <u>paragraph (b)(7)</u> or (b)(8) of this section, or adhering to the requirements in <u>paragraph (b)(6)(i)</u> of this section.

(i)

(A) Flares shall be used that have a diameter of 3 inches or greater, are nonassisted, have a hydrogen content of 8.0 percent (by volume) or greater, and are designed for and operated with an exit velocity less than 37.2 m/sec (122 ft/sec) and less than the velocity  $V_{max}$ , as determined by the following equation:

 $V_{max} = (X_{H2} - K_1) * K_2$ 

Where:

 $V_{max} = Maximum permitted velocity, m/sec.$ 

 $K_1$  = Constant, 6.0 volume-percent hydrogen.

 $K_2 = Constant, 3.9(m/sec)/volume-percent hydrogen.$ 

 $X_{H2}$  = The volume-percent of hydrogen, on a wet basis, as calculated by using the American Society for Testing and Materials (ASTM) Method D1946-77. (Incorporated by reference as specified in <u>§ 63.14</u>).

(B) The actual exit velocity of a flare shall be determined by the method specified in paragraph (b)(7)(i) of this section.

(ii) Flares shall be used only with the net heating value of the gas being combusted at 11.2 MJ/scm (300 Btu/scf) or greater if the flare is steam-assisted or air-assisted; or with the net heating value of the gas being combusted at 7.45 M/scm (200 Btu/scf) or greater if the flares is non-assisted. The net heating value of the gas being combusted in a flare shall be calculated using the following equation:

$$H_{T} = K \sum_{i=1}^{n} C_{i} H_{i}$$

Where:

 $H_T$  = Net heating value of the sample, MJ/scm; where the net enthalpy per mole of offgas is based on combustion at 25 °C and 760 mm Hg, but the standard temperature for determining the volume corresponding to one mole is 20 °C.

K = Constant =

$$1.740 \times 10^{-7} \left(\frac{1}{\text{ppmv}}\right) \left(\frac{\text{g-mole}}{\text{scm}}\right) \left(\frac{\text{MJ}}{\text{kcal}}\right)$$

where the standard temperature for (g-mole/scm) is 20 °C.

 $C_i$  = Concentration of sample component i in ppmv on a wet basis, as measured for organics by Test Method 18 and measured for hydrogen and carbon monoxide by American Society for Testing and Materials (ASTM) D1946-77 or 90 (Reapproved 1994) (incorporated by reference as specified in § 63.14).

 $H_i$  = Net heat of combustion of sample component i, kcal/g-mole at 25 °C and 760 mm Hg. The heats of combustion may be determined using ASTM D2382-76 or 88 or D4809-95 (incorporated by reference as specified in § 63.14) if published values are not available or cannot be calculated.

n = Number of sample components.

(7)

(i) Steam-assisted and nonassisted flares shall be designed for and operated with an exit velocity less than 18.3 m/sec (60 ft/sec), except as provided in <u>paragraphs (b)(7)(ii)</u> and (b)(7)(iii) of this section. The actual exit velocity of a flare shall be determined by dividing by the volumetric flow rate of gas being combusted (in units of emission standard temperature and pressure), as determined by Test Method 2, 2A, 2C, or 2D in appendix A to 40 CFR part 60 of this chapter, as appropriate, by the unobstructed (free) cross-sectional area of the flare tip.

(ii) Steam-assisted and nonassisted flares designed for and operated with an exit velocity, as determined by the method specified in <u>paragraph (b)(7)(i)</u> of this section, equal to or greater than 18.3 m/sec (60 ft/sec) but less than 122 m/sec (400 ft/sec), are allowed if the net heating value of the gas being combusted is greater than 37.3 MJ/scm (1,000 Btu/scf).

(iii) Steam-assisted and nonassisted flares designed for and operated with an exit velocity, as determined by the method specified in <u>paragraph (b)(7)(i)</u> of this section, less than the velocity  $V_{max}$ , as determined by the method specified in this paragraph, but less than 122 m/sec (400 ft/sec) are allowed. The maximum permitted velocity,  $V_{max}$ , for flares complying with this paragraph shall be determined by the following equation:

 $Log_{10}(V_{max}) = (H_T + 28.8)/31.7$ 

Where:

 $V_{max} = Maximum permitted velocity, m/sec.$ 

28.8 = Constant.

31.7 = Constant.

 $H_T$  = The net heating value as determined in <u>paragraph (b)(6)</u> of this section.

(8) Air-assisted flares shall be designed and operated with an exit velocity less than the velocity  $V_{max}$ . The maximum permitted velocity,  $V_{max}$ , for air-assisted flares shall be determined by the following equation:

 $V_{max} = 8.71 + 0.708(H_T)$ 

Where:

 $V_{max}$  = Maximum permitted velocity, m/sec.

8.71 = Constant.

0.708 = Constant.

 $H_T$  = The net heating value as determined in <u>paragraph (b)(6)(ii)</u> of this section.

(c) Alternative work practice for monitoring equipment for leaks. Paragraphs (c), (d), and (e) of this section apply to all equipment for which the applicable subpart requires monitoring with a 40 CFR part 60, appendix A-7, Method 21 monitor, except for closed vent systems, equipment designated as leakless, and equipment identified in the applicable subpart as having no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background. An owner or operator may use an optical gas imaging instrument instead of a 40 CFR part 60, sppendix A-7, Method 21 monitor. Requirements in the existing subparts that are specific to the Method 21 instrument do not apply under this section. All other requirements in the applicable subpart that are not addressed in paragraphs (c), (d), and (e) of this section continue to apply. For example, equipment specification requirements, and non-Method 21 instrument recordkeeping and reporting requirements in the applicable subpart continue to apply. The terms defined in paragraphs (c), (d), and (e) of this section have meanings that are specific to the alternative work practice standard in paragraphs (c), (d), and (e) of this section.

(1) Applicable subpart means the subpart in <u>40 CFR parts 60</u>, <u>61</u>, <u>63</u>, and <u>65</u> that requires monitoring of equipment with a <u>40 CFR part 60</u>, <u>appendix A</u>-7, Method 21 monitor.

(2) *Equipment* means pumps, valves, pressure relief valves, compressors, open-ended lines, flanges, connectors, and other equipment covered by the applicable subpart that require monitoring with a <u>40 CFR part 60, appendix A</u>-7, Method 21 monitor.

(3) Imaging means making visible emissions that may otherwise be invisible to the naked eye.

(4) *Optical gas imaging instrument* means an instrument that makes visible emissions that may otherwise be invisible to the naked eye.

(5) Repair means that equipment is adjusted, or otherwise altered, in order to eliminate a leak.

(6) Leak means:

(i) Any emissions imaged by the optical gas instrument;

(ii) Indications of liquids dripping;

(iii) Indications by a sensor that a seal or barrier fluid system has failed; or

(iv) Screening results using a <u>40 CFR part 60, appendix A</u>-7, Method 21 monitor that exceed the leak definition in the applicable subpart to which the equipment is subject.

(d) The alternative work practice standard for monitoring equipment for leaks is available to all subparts in  $\frac{40 \text{ CFR parts}}{60, 61, 63}$ , and  $\frac{65}{5}$  that require monitoring of equipment with a  $\frac{40 \text{ CFR part } 60, \text{ appendix } A}{10 \text{ CFR part } 60, \text{ appendix } A}$ .

(1) An owner or operator of an affected source subject to <u>40 CFR parts 60</u>, <u>61</u>, <u>63</u>, or <u>65</u> can choose to comply with the alternative work practice requirements in <u>paragraph (e)</u> of this section instead of using the <u>40 CFR part 60</u>, <u>appendix A</u>-7, Method 21 monitor to identify leaking equipment. The owner or operator must document the equipment, process units, and facilities for which the alternative work practice will be used to identify leaks.

(2) Any leak detected when following the leak survey procedure in <u>paragraph (e)(3)</u> of this section must be identified for repair as required in the applicable subpart.

(3) If the alternative work practice is used to identify leaks, re-screening after an attempted repair of leaking equipment must be conducted using either the alternative work practice or the <u>40 CFR part 60, Appendix A</u>-7, Method 21 monitor at the leak definition required in the applicable subparts to which the equipment is subject.

(4) The schedule for repair is as required in the applicable subpart.

(5) When this alternative work practice is used for detecting leaking equipment, choose one of the monitoring frequencies listed in Table 1 to <u>subpart A of this part</u> in lieu of the monitoring frequency specified for regulated equipment in the applicable subpart. Reduced monitoring frequencies for good performance are not applicable when using the alternative work practice.

(6) When this alternative work practice is used for detecting leaking equipment, the following are not applicable for the equipment being monitored:

(i) Skip period leak detection and repair;

(ii) Quality improvement plans; or

(iii) Complying with standards for allowable percentage of valves and pumps to leak.

(7) When the alternative work practice is used to detect leaking equipment, the regulated equipment in paragraph (d)(1)(i) of this section must also be monitored annually using a <u>40 CFR part 60</u>, <u>Appendix A</u>-7, Method 21 monitor at the leak definition required in the applicable subpart. The owner or operator may choose the specific monitoring period (for example, first quarter) to conduct the annual monitoring. Subsequent monitoring must be conducted every 12 months from the initial period. Owners or operators must keep records of the annual Method 21 screening results, as specified in <u>paragraph</u> (i)(4)(vii) of this section.

(e) An owner or operator of an affected source who chooses to use the alternative work practice must comply with the requirements of <u>paragraphs (e)(1)</u> through (e)(5) of this section.

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(1) Instrument specifications. The optical gas imaging instrument must comply with the requirements specified in paragraphs  $(\underline{e})(1)(\underline{i})$  and  $(\underline{e})(1)(\underline{i})$  of this section.

(i) Provide the operator with an image of the potential leak points for each piece of equipment at both the detection sensitivity level and within the distance used in the daily instrument check described in <u>paragraph (e)(2)</u> of this section. The detection sensitivity level depends upon the frequency at which leak monitoring is to be performed.

(ii) Provide a date and time stamp for video records of every monitoring event.

(2) Daily instrument check. On a daily basis, and prior to beginning any leak monitoring work, test the optical gas imaging instrument at the mass flow rate determined in paragraph (e)(2)(i) of this section in accordance with the procedure specified in paragraphs (e)(2)(ii) through (e)(2)(iv) of this section for each camera configuration used during monitoring (for example, different lenses used), unless an alternative method to demonstrate daily instrument checks has been approved in accordance with paragraph (e)(2)(v) of this section.

(i) Calculate the mass flow rate to be used in the daily instrument check by following the procedures in <u>paragraphs</u> (e)(2)(i)(A) and (e)(2)(i)(B) of this section.

(A) For a specified population of equipment to be imaged by the instrument, determine the piece of equipment in contact with the lowest mass fraction of chemicals that are detectable, within the distance to be used in <u>paragraph (e)(2)(iv)(B)</u> of this section, at or below the standard detection sensitivity level.

(B) Multiply the standard detection sensitivity level, corresponding to the selected monitoring frequency in Table 1 of <u>subpart</u> <u>A of this part</u>, by the mass fraction of detectable chemicals from the stream identified in <u>paragraph (e)(2)(i)(A)</u> of this section to determine the mass flow rate to be used in the daily instrument check, using the following equation.

$$E_{dic} = (E_{sds}) \sum_{i=1}^{k} x_i$$

Where:

 $E_{dic}$  = Mass flow rate for the daily instrument check, grams per hour

 $x_i = Mass$  fraction of detectable chemical(s) i seen by the optical gas imaging instrument, within the distance to be used in <u>paragraph (e)(2)(iv)(B)</u> of this section, at or below the standard detection sensitivity level,  $E_{sds}$ .

 $E_{sds}$  = Standard detection sensitivity level from Table 1 to subpart A, grams per hour

k = Total number of detectable chemicals emitted from the leaking equipment and seen by the optical gas imaging instrument.

(ii) Start the optical gas imaging instrument according to the manufacturer's instructions, ensuring that all appropriate settings conform to the manufacturer's instructions.

(iii) Use any gas chosen by the user that can be viewed by the optical gas imaging instrument and that has a purity of no less than 98 percent.

(iv) Establish a mass flow rate by using the following procedures:

(A) Provide a source of gas where it will be in the field of view of the optical gas imaging instrument.

(B) Set up the optical gas imaging instrument at a recorded distance from the outlet or leak orifice of the flow meter that will not be exceeded in the actual performance of the leak survey. Do not exceed the operating parameters of the flow meter.

(C) Open the valve on the flow meter to set a flow rate that will create a mass emission rate equal to the mass rate calculated in <u>paragraph (e)(2)(i)</u> of this section while observing the gas flow through the optical gas imaging instrument viewfinder. When an image of the gas emission is seen through the viewfinder at the required emission rate, make a record of the reading on the flow meter.

(v) Repeat the procedures specified in <u>paragraphs (e)(2)(ii)</u> through (e)(2)(iv) of this section for each configuration of the optical gas imaging instrument used during the leak survey.

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(vi) To use an alternative method to demonstrate daily instrument checks, apply to the Administrator for approval of the alternative under  $\frac{63.177}{10}$  or  $\frac{63.178}{100}$ , whichever is applicable.

(3) *Leak survey procedure.* Operate the optical gas imaging instrument to image every regulated piece of equipment selected for this work practice in accordance with the instrument manufacturer's operating parameters. All emissions imaged by the optical gas imaging instrument are considered to be leaks and are subject to repair. All emissions visible to the naked eye are also considered to be leaks and are subject to repair.

(4) *Recordkeeping*. Keep the records described in <u>paragraphs (e)(4)(i)</u> through  $(\underline{e})(\underline{4})(\underline{vii})$  of this section:

(i) The equipment, processes, and facilities for which the owner or operator chooses to use the alternative work practice.

(ii) The detection sensitivity level selected from Table 1 to subpart A of this part for the optical gas imaging instrument.

(iii) The analysis to determine the piece of equipment in contact with the lowest mass fraction of chemicals that are detectable, as specified in paragraph (e)(2)(i)(A) of this section.

(iv) The technical basis for the mass fraction of detectable chemicals used in the equation in <u>paragraph (e)(2)(i)(B)</u> of this section.

(v) The daily instrument check. Record the distance, per <u>paragraph (e)(2)(iv)(B)</u> of this section, and the flow meter reading, per <u>paragraph (e)(2)(iv)(C)</u> of this section, at which the leak was imaged. Keep a video record of the daily instrument check for each configuration of the optical gas imaging instrument used during the leak survey (for example, the daily instrument check must be conducted for each lens used). The video record must include a time and date stamp for each daily instrument check. The video record must be kept for 5 years.

(vi) *Recordkeeping requirements in the applicable subpart.* A video record must be used to document the leak survey results. The video record must include a time and date stamp for each monitoring event. A video record can be used to meet the recordkeeping requirements of the applicable subparts if each piece of regulated equipment selected for this work practice can be identified in the video record. The video record must be kept for 5 years.

(vii) The results of the annual Method 21 screening required in <u>paragraph (h)(7)</u> of this section. Records must be kept for all regulated equipment specified in <u>paragraph (h)(1)</u> of this section. Records must identify the equipment screened, the screening value measured by Method 21, the time and date of the screening, and calibration information required in the existing applicable subparts.

(5) *Reporting.* Submit the reports required in the applicable subpart. Submit the records of the annual Method 21 screening required in <u>paragraph (h)(7)</u> of this section to the Administrator via e-mail to <u>CCG-AWP@EPA.GOV</u>.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>63 FR 24444</u>, May 4, 1998; <u>65 FR 62215</u>, Oct. 17, 2000; <u>67 FR 16605</u>, Apr. 5, 2002; <u>73 FR 78211</u>, Dec. 22, 2008]

# § 63.12 State authority and delegations.

(a) The provisions of this part shall not be construed in any manner to preclude any State or political subdivision thereof from—

(1) Adopting and enforcing any standard, limitation, prohibition, or other regulation applicable to an affected source subject to the requirements of this part, provided that such standard, limitation, prohibition, or regulation is not less stringent than any requirement applicable to such source established under this part;

(2) Requiring the owner or operator of an affected source to obtain permits, licenses, or approvals prior to initiating construction, reconstruction, modification, or operation of such source; or

(3) Requiring emission reductions in excess of those specified in subpart D of this part as a condition for granting the extension of compliance authorized by section 112(i)(5) of the Act.

(b)

(1) Section 112(1) of the Act directs the Administrator to delegate to each State, when appropriate, the authority to implement and enforce standards and other requirements pursuant to section 112 for stationary sources located in that State. Because of the unique nature of radioactive material, delegation of authority to implement and enforce standards that control radionuclides may require separate approval.

(2) <u>Subpart E of this part</u> establishes procedures consistent with section 112(l) for the approval of State rules or programs to implement and enforce applicable Federal rules promulgated under the authority of section 112. Subpart E also establishes procedures for the review and withdrawal of section 112 implementation and enforcement authorities granted through a section 112(l) approval.

(c) All information required to be submitted to the EPA under this part also shall be submitted to the appropriate state agency of any state to which authority has been delegated under section 112(l) of the Act, provided that each specific delegation may exempt sources from a certain federal or state reporting requirement. Any information required to be submitted electronically by this part via the EPA's CEDRI may, at the discretion of the delegated authority, satisfy the requirements of this paragraph. The Administrator may permit all or some of the information to be submitted to the appropriate state agency only, instead of to the EPA and the state agency with the exception of federal electronic reporting requirements under this part. Sources may not be exempted from federal electronic reporting requirements.

[59 FR 12430, Mar. 16, 1994, as amended at 85 FR 73887, Nov. 19, 2020]

# § 63.13 Addresses of State air pollution control agencies and EPA Regional Offices.

(a) All requests, reports, applications, submittals, and other communications to the Administrator pursuant to this part shall be submitted to the appropriate Regional Office of the U.S. Environmental Protection Agency indicated in the following table. If a request, report, application, submittal, or other communication is required by this part to be submitted electronically via the EPA's CEDRI then such submission satisfies the requirements of this <u>paragraph (a)</u>.

	Table 1 to Paragraph (a)			
Region	Address	State		
Ι	Director, Enforcement and Compliance Assurance Division, U.S. EPA Region I, 5 Post Office Square—Suite 100 (04-2), Boston, MA 02109-3912, Attn: Air Compliance Clerk	Connecticut, Maine, Massachusetts, New Hampshire, Rhode Island, Vermont.		
II	Director, Air and Waste Management Division, 26 Federal Plaza, New York, NY 10278	New Jersey, New York, Puerto Rico, Virgin Islands.		
III	Director, Air Protection Division, 1650 Arch Street, Philadelphia, PA 19103	Delaware, District of Columbia, Maryland, Pennsylvania, Virginia, West Virginia.		
IV	Director, Air and Radiation Division, 61 Forsyth Street, SW, Atlanta, Georgia 30303-8960	Alabama, Florida, Georgia, Kentucky, Mississippi, North Carolina, South Carolina, Tennessee.		
v	Director, Air and Radiation Division, 77 West Jackson Blvd., Chicago, IL 60604- 3507	Illinois, Indiana, Michigan, Minnesota, Ohio, Wisconsin.		
VI	Director; Enforcement and Compliance Assurance Division; U.S. Environmental Protection Agency, 1201 Elm Street, Suite 500, Mail Code 6ECD, Dallas, Texas 75270-2102	Arkansas, Louisiana, New Mexico, Oklahoma, Texas.		
VII	Director, Air and Waste Management Division, 11201 Renner Boulevard, Lenexa, Kansas 66219	Iowa, Kansas, Missouri, Nebraska.		
VIII	Director, Air and Toxics Technical Enforcement Program, Office of Enforcement, Compliance and Environmental Justice, Mail Code 8ENF- AT, 1595 Wynkoop Street, Denver, CO 80202-1129	Colorado, Montana, North Dakota, South Dakota, Utah, Wyoming.		
IX	Director, Air Division, 75 Hawthorne	Arizona, California, Hawaii, Nevada; the territories of American Samoa		

#### National Emission Standards for Hazardous Air Pollutants (NESHAP) – General Provisions

Table 1 to Paragraph (a)			
Region	Address	State	
	Street, San Francisco, CA 94105	and Guam; the Commonwealth of the Northern Mariana Islands; the territories of Baker Island, Howland Island, Jarvis Island, Johnston Atoll, Kingman Reef, Midway Atoll, Palmyra Atoll, and Wake Islands; and certain U.S. Government activities in the freely associated states of the Republic of the Marshall Islands, the Federated States of Micronesia, and the Republic of Palau.	
X	Director, Office of Air Quality, 1200 Sixth Avenue (OAQ-107), Seattle, WA 98101	Alaska, Idaho, Oregon, Washington.	

(b) All information required to be submitted to the Administrator under this part also shall be submitted to the appropriate State agency of any State to which authority has been delegated under section 112(l) of the Act. The owner or operator of an affected source may contact the appropriate EPA Regional Office for the mailing addresses for those States whose delegation requests have been approved.

(c) If any State requires a submittal that contains all the information required in an application, notification, request, report, statement, or other communication required in this part, an owner or operator may send the appropriate Regional Office of the EPA a copy of that submittal to satisfy the requirements of this part for that communication.

[<u>59 FR 12430</u>, Mar. 16, 1994, as amended at <u>63 FR 66061</u>, Dec. 1, 1998; <u>67 FR 4184</u>, Jan. 29, 2002; <u>68 FR 32601</u>, May 30, 2003; <u>68 FR 35792</u>, June 17, 2003; <u>73 FR 24871</u>, May 6, 2008; <u>75 FR 69532</u>, Nov. 12, 2010; <u>76 FR 49673</u>, Aug. 11, 2011; <u>78 FR 37977</u>, June 25, 2013; <u>84 FR 34069</u>, July 17, 2019; <u>84 FR 44230</u>, Aug. 23, 2019; <u>85 FR 73887</u>, Nov. 19, 2020; <u>89 FR 86748</u>, Oct. 31, 2024]

#### § 63.14 Incorporations by reference.

(a)

(1) Certain material is incorporated by reference into this part with the approval of the Director of the Federal Register under <u>5 U.S.C. 552(a)</u> and <u>1 CFR part 51</u>. To enforce any edition other than that specified in this section, the U.S. Environmental Protection Agency (EPA) must publish a document in the Federal Register and the material must be available to the public. All approved incorporation by reference (IBR) material is available for inspection at the EPA and at the National Archives and Records Administration (NARA). Contact the EPA at: EPA Docket Center, Public Reading Room, EPA WJC West, Room 3334, 1301 Constitution Ave. NW, Washington, DC; phone: (202) 566-1744. For information on the availability of this material at NARA, visit <u>www.archives.gov/federal-register/cfr/ibr-locations</u> or email <u>fr.inspection@nara.gov</u>.

(2) The IBR material may be obtained from the sources in the following paragraphs of this section or from one or more private resellers listed in this <u>paragraph (a)(2)</u>. For material that is no longer commercially available, contact: the EPA (see <u>paragraph (a)(1)</u> of this section).

(i) Accuris Standards Store, 321 Inverness Drive, South Englewood, CO, 80112; phone: (800) 332-6077; website: *https://store.accuristech.com*.

(ii) American National Standards Institute (ANSI), 25 West 43rd Street, Fourth Floor, New York, NY 10036-7417; phone: (212) 642-4980; email: *info@ansi.org*; website: *www.ansi.org*.

(iii) GlobalSpec, 257 Fuller Road, Suite NFE 1100, Albany, NY 12203-3621; phone: (800) 261-2052; website: *https://standards.globalspec.com*.

(iv) Nimonik Document Center, 401 Roland Way, Suite 224, Oakland, CA, 94624; phone (650) 591-7600; email: *info@document-center.com*; website: *www.document-center.com*.

(v) Techstreet, phone: (855) 999-9870; email: <u>store@techstreet.com</u>; website: <u>www.techstreet.com</u>.

(b) American Conference of Governmental Industrial Hygienists (ACGIH), Customer Service Department, 1330 Kemper Meadow Drive, Cincinnati, Ohio 45240, telephone number (513) 742-2020.

# National Emission Standards for Hazardous Air Pollutants (NESHAP) – General Provisions

(1) Industrial Ventilation: A Manual of Recommended Practice, 22nd Edition, 1995, Chapter 3, "Local Exhaust Hoods" and Chapter 5, "Exhaust System Design Procedure." IBR approved for  $\frac{\$\$ 63.843(b)}{\$\$ 63.843(b)}$ .

(2) Industrial Ventilation: A Manual of Recommended Practice, 23rd Edition, 1998, Chapter 3, "Local Exhaust Hoods" and Chapter 5, "Exhaust System Design Procedure." IBR approved for  $\frac{\& 63.1503}{63.1506(c)}$ ,  $\frac{63.1512(e)}{63.1512(e)}$ , Table 2 to subpart RRR, Table 3 to subpart RRR, and appendix A to subpart RRR, and  $\frac{\& 63.2984(e)}{6}$ .

(3) Industrial Ventilation: A Manual of Recommended Practice for Design, 27th Edition, 2010. IBR approved for  $\frac{63.1503}{63.1506(c)}$ ,  $\frac{63.1512(e)}{63.2984(e)}$ . Table 2 to subpart RRR, Table 3 to subpart RRR, and appendix A to subpart RRR, and  $\frac{63.2984(e)}{63.2984(e)}$ .

(c) American Petroleum Institute (API), 200 Massachusetts Ave. NW, Suite 1100, Washington, DC 20001; phone: (202) 682-8000; website: <u>www.api.org</u>.

(1) API Publication 2517, Evaporative Loss from External Floating-Roof Tanks, Third Edition, February 1989; IBR approved for <u>§§ 63.111; 63.1402; 63.2406; 63.7944</u>.

(2) API Publication 2518, Evaporative Loss from Fixed-roof Tanks, Second Edition, October 1991; IBR approved for  $\S$  <u>63.150(g)</u>.

(3) API Manual of Petroleum Measurement Specifications (MPMS) Chapter 19.2 (API MPMS 19.2), Evaporative Loss From Floating-Roof Tanks, First Edition, April 1997; IBR approved for <u>§§ 63.1251</u>; <u>63.12005</u>.

(4) API Manual of Petroleum Measurement Specifications (MPMS) Chapter 19.2 (API MPMS 19.2), Evaporative Loss From Floating-Roof Tanks, Fourth Edition, August 2020; IBR approved for <u>§ 63.101(b)</u>.

(d) American Public Health Association, 1015 18th Street NW, Washington, DC 20036; phone (844) 232-3707; email: <u>standardmethods@subscritpionoffice.com</u>; website: <u>www.standardmethods.org</u>.

(1) Standard Method 5210, Biochemical Oxygen Demand (BOD), revised December 10, 2019; IBR approved for § 63.457(c)

(2) [Reserved]

(e) American Society of Heating, Refrigerating, and Air-Conditioning Engineers at 1791 Tullie Circle, NE., Atlanta, GA 30329 <u>orders@ashrae.org</u>.

(1) American Society of Heating, Refrigerating, and Air-Conditioning Engineers Method 52.1, *Gravimetric and Dust-Spot Procedures for Testing Air-Cleaning Devices Used in General Ventilation for Removing Particulate Matter* June 4, 1992; IBR approved for <u>§ 63.11516(d)</u>.

(2) ANSI/ASHRAE Standard 52.2-2017, *Method of Testing General Ventilation Air-Cleaning Devices for Removal Efficiency by Particle Size*, copyright 2017; IBR approved for <u>§ 63.11173(e)</u>.

(f) American Society of Mechanical Engineers (ASME), Two Park Avenue, New York, NY 10016-5990; phone: (800) 843-2763; email: <u>*CustomerCare@asme.org*</u>; website: <u>www.asme.org</u>.

(1) ANSI/ASME PTC 19.10-1981, Flue and Exhaust Gas Analyses [Part 10, Instruments and Apparatus], issued August 31, 1981; <u>§§</u>

 $\frac{63.116(c)}{63.128(a)} \text{ and } (\underline{h}); \\ \frac{63.128(a)}{63.128(a)}; \\ \frac{63.145(i)}{63.309(k)}; \\ \frac{63.365(b)}{63.365(b)}; \\ \frac{63.457(k)}{63.490(g)}; \\ \frac{63.490(g)}{63.772(e)} \text{ and } (\underline{h}); \\ \frac{63.865(b)}{63.865(b)}; \\ \frac{63.997(e)}{63.1282(d)}; \\ \frac{63.1282(d)}{63.1450(a)}, \\ \frac{(b)}{(b)}, \\ \frac{(d)}{(b)}, \\ \frac{(d)}{(b)}; \\ \frac{(d)}{(b)}$ 

 $\frac{63.3166(a); 63.3360(e); 63.3545(a); 63.3555(a); 63.4166(a); 63.4362(a); 63.4766(a); 63.4965(a); 63.5160(d); table 4 to subpart UUUU; tables 5, 16, and 17 to subpart XXXX; table 3 to subpart YYYY; table 4 to subpart AAAA; § 63.7322(b); table 5 to subpart DDDDD; § 63.7822(b); 63.7824(e); 63.7825(b); 63.8000(d); table 4 to subpart JJJJJ; table 4 to subpart KKKKK; §§ 63.9307(c); 63.9323(a); 63.9621(b) and (c); table 4 to subpart SSSSS; tables 4 and 5 of subpart UUUUU; table 1 to subpart ZZZZZ; §§ 63.11148(e); 63.11155(e); 63.11162(f); 63.11163(g); table 4 to subpart JJJJJJ; §§ 63.111410(j); 63.11551(a); 63.11646(a); 63.11945.$ 

(2) [Reserved]

(g) The Association of Florida Phosphate Chemists, P.O. Box 1645, Bartow, Florida 33830.

(1) Book of Methods Used and Adopted By The Association of Florida Phosphate Chemists, Seventh Edition 1991:

(i) Section IX, Methods of Analysis for Phosphate Rock, No. 1 Preparation of Sample, IBR approved for  $\S 63.606(f)$ ,  $\S 63.626(f)$ .

(ii) Section IX, Methods of Analysis for Phosphate Rock, No. 3 Phosphorus-P2O5 or Ca3(PO4)2, Method A—Volumetric Method, IBR approved for  $\S 63.606(f)$ ,  $\S 63.626(f)$ .

(iii) Section IX, Methods of Analysis for Phosphate Rock, No. 3 Phosphorus-P2O5 or Ca3(PO4)2, Method B—Gravimetric Quimociac Method, IBR approved for  $\S 63.606(f)$ ,  $\S 63.626(f)$ .

(iv) Section IX, Methods of Analysis For Phosphate Rock, No. 3 Phosphorus-P2O5 or Ca3(PO4)2, Method C—Spectrophotometric Method, IBR approved for  $\frac{63.606(f)}{63.606(f)}$ .

(v) Section XI, Methods of Analysis for Phosphoric Acid, Superphosphate, Triple Superphosphate, and Ammonium Phosphates, No. 3 Total Phosphorus-P2O5, Method A—Volumetric Method, IBR approved for  $\S$  63.606(f),  $\S$  63.626(f), and (g).

(vi) Section XI, Methods of Analysis for Phosphoric Acid, Superphosphate, Triple Superphosphate, and Ammonium Phosphates, No. 3 Total Phosphorus-P2O5, Method B—Gravimetric Quimociac Method, IBR approved for  $\S$  63.606(f),  $\S$  63.626(f), and (g).

(vii) Section XI, Methods of Analysis for Phosphoric Acid, Superphosphate, Triple Superphosphate, and Ammonium Phosphates, No. 3 Total Phosphorus-P2O5, Method C—Spectrophotometric Method, IBR approved for  $\S$  63.606(f),  $\S$  63.626(f), and (g).

(2) [Reserved]

(h) Association of Official Analytical Chemists (AOAC) International, Customer Services, Suite 400, 2200 Wilson Boulevard, Arlington, Virginia 22201-3301, Telephone (703) 522-3032, Fax (703) 522-5468.

(1) AOAC Official Method 929.01 Sampling of Solid Fertilizers, Sixteenth edition, 1995, IBR approved for <u>§ 63.626(g)</u>.

(2) AOAC Official Method 929.02 Preparation of Fertilizer Sample, Sixteenth edition, 1995, IBR approved for <u>§ 63.626(g)</u>.

(3) AOAC Official Method 957.02 Phosphorus (Total) in Fertilizers, Preparation of Sample Solution, Sixteenth edition, 1995, IBR approved for  $\frac{\& 63.626(g)}{2}$ .

(4) AOAC Official Method 958.01 Phosphorus (Total) in Fertilizers, Spectrophotometric Molybdovanadophosphate Method, Sixteenth edition, 1995, IBR approved for  $\frac{\& 63.626(g)}{2}$ .

(5) AOAC Official Method 962.02 Phosphorus (Total) in Fertilizers, Gravimetric Quinolinium Molybdophosphate Method, Sixteenth edition, 1995, IBR approved for  $\frac{\& 63.626(g)}{2}$ .

(6) AOAC Official Method 969.02 Phosphorus (Total) in Fertilizers, Alkalimetric Quinolinium Molybdophosphate Method, Sixteenth edition, 1995, IBR approved for  $\frac{\& 63.626(g)}{2}$ .

(7) AOAC Official Method 978.01 Phosphorus (Total) in Fertilizers, Automated Method, Sixteenth edition, 1995, IBR approved for  $\frac{63.626(g)}{2}$ .

(i) ASTM International, 100 Barr Harbor Drive, P.O. Box CB700, West Conshohocken, Pennsylvania 19428-2959; phone: (800) 262-1373; website: <u>www.astm.org</u>.

(1) ASTM D95-05 (Reapproved 2010), Standard Test Method for Water in Petroleum Products and Bituminous Materials by Distillation, approved May 1, 2010, IBR approved for <u>§ 63.10005(i)</u> and table 6 to subpart DDDDD.

(2) ASTM D240-09 Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter, approved July 1, 2009, IBR approved for table 6 to subpart DDDDD.

(3) ASTM Method D388-05, Standard Classification of Coals by Rank, approved September 15, 2005, IBR approved for  $\underline{\$\$}$  <u>63.7575, 63.10042</u>, and <u>63.11237</u>.

(4) ASTM Method D396-10, Standard Specification for Fuel Oils, including Appendix X1, approved October 1, 2010, IBR approved for  $\frac{63.10042}{5}$ .

(5) ASTM D396-10, Standard Specification for Fuel Oils, approved October 1, 2010, IBR approved for <u>§§</u> <u>63.7575</u> and <u>63.11237</u>.

(6) ASTM D523-89, Standard Test Method for Specular Gloss, IBR approved for <u>§ 63.782</u>.

(7) ASTM D975-11b, Standard Specification for Diesel Fuel Oils, approved December 1, 2011, IBR approved for <u>§ 63.7575</u>.

(8) ASTM D1193-77, Standard Specification for Reagent Water, IBR approved for appendix A to part 63: Method 306, Sections 7.1.1 and 7.4.2.

(9) ASTM D1193-91, Standard Specification for Reagent Water, IBR approved for appendix A to part 63: Method 306, Sections 7.1.1 and 7.4.2.

(10) ASTM D1331-89, Standard Test Methods for Surface and Interfacial Tension of Solutions of Surface Active Agents, IBR approved for appendix A to part 63: Method 306B, Sections 6.2, 11.1, and 12.2.2.

(11) ASTM D1475-90, Standard Test Method for Density of Paint, Varnish Lacquer, and Related Products, IBR approved for appendix A to subpart II.

(12) ASTM D1475-13, Standard Test Method for Density of Liquid Coatings, Inks, and Related Products, approved November 1, 2013, IBR approved for <u>§§</u>

<u>63.3151(b)</u>, <u>63.3941(b)</u> and <u>(c)</u>, <u>63.3951(c)</u>, <u>63.4141(b)</u> and <u>(c)</u>, <u>63.4551(c)</u>, <u>63.4741(b)</u> and <u>(c)</u>, <u>63.4751(c)</u>, and <u>63.4941(b)</u> and <u>(c)</u>.

(13) ASTM Method D1835-05, Standard Specification for Liquefied Petroleum (LP) Gases, approved April 1, 2005, IBR approved for  $\frac{88}{53.7575}$  and  $\frac{63.11237}{5.7575}$ .

(14) ASTM D1945-03 (Reapproved 2010), Standard Test Method for Analysis of Natural Gas by Gas Chromatography, Approved January 1, 2010, IBR approved for  $\frac{\&\& 63.670(j)}{63.772(h)}$ , and  $\frac{63.1282(g)}{63.772(h)}$ .

(15) ASTM D1945-14, Standard Test Method for Analysis of Natural Gas by Gas Chromatography, Approved November 1, 2014, IBR approved for <u>§ 63.670(j)</u>.

(16) ASTM D1946-77, Standard Method for Analysis of Reformed Gas by Gas Chromatography, IBR approved for <u>§</u> <u>63.11(b)</u>.

(17) ASTM D1946-90 (Reapproved 1994), Standard Method for Analysis of Reformed Gas by Gas Chromatography, 1994, IBR approved for <u>§§ 63.11(b)</u>, <u>63.987(b)</u>, and <u>63.1412</u>.

(18) ASTM D1963-85 (Reapproved 1996), Standard Test Method for Specific Gravity of Drying Oils, Varnishes, Resins, and Related Materials at 25/25 °C, approved November 29, 1985, IBR approved for <u>§ 63.3360(c)</u>.

(19) ASTM D2013/D2013M-09, Standard Practice for Preparing Coal Samples for Analysis, (Approved November 1, 2009), IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(20) ASTM D2099-00, Standard Test Method for Dynamic Water Resistance of Shoe Upper Leather by the Maeser Water Penetration Tester, IBR approved for <u>§ 63.5350</u>.

(21) ASTM D2111-10 (Reapproved 2015), Standard Test Methods for Specific Gravity and Density of Halogenated Organic Solvents and Their Admixtures, approved June 1, 2015, IBR approved for <u>§§</u> <u>63.3360(c), 63.3951(c), 63.4141(b)</u> and (c), <u>63.4551(c)</u>, and <u>63.4741(a)</u>.

(22) ASTM D2216-05, Standard Test Methods for Laboratory Determination of Water (Moisture) Content of Soil and Rock by Mass, IBR approved for the definition of "Free organic liquids" in  $\frac{8}{63.10692}$ .

(23) ASTM D2234/D2234M-10, Standard Practice for Collection of a Gross Sample of Coal, approved January 1, 2010, IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(24) ASTM D2369-93, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A to subpart II.

(25) ASTM D2369-95, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A to subpart II.

(26) ASTM D2369-10 (Reapproved 2015)e1, Standard Test Method for Volatile Content of Coatings, approved June 1, 2015, IBR approved for <u>§§</u>

 $\frac{63.3151(a)}{63.3360(c)}, \frac{63.3961(j)}{63.4141(a)} \text{ and } (\underline{b}), \frac{63.4161(h)}{63.4321(e)}, \frac{63.4341(e)}{63.4341(e)}, \frac{63.4351(d)}{63.4541(a)}, \\ \text{and } \frac{63.4561(j)}{63.4961(j)}, \text{ appendix A to subpart PPPP, and } \underbrace{\$\$ 63.4741(a)}_{\$\$ 63.4941(a)}, \underbrace{63.4941(a)}_{\$\$ 63.4961(j)}, \underbrace{63.4961(j)}_{\$\$ 63.8055(b)}, \underbrace{63.4361(a)}_{\$\$ 63.4961(j)}, \underbrace{63.4961(j)}_{\$\$ 63.8055(b)}, \underbrace{63.4961(j)}_{\$\$ 63.4961(j)}, \underbrace{63.4961(j)}_{\$\$ 63.4951(j)}, \underbrace{63.4961(j)}_{\$\ast 63.4951(j)}, \underbrace{63.4961(j)}_{$\ast\ast 63.4951(j)$ 

(27) ASTM D2382-76, Heat of Combustion of Hydrocarbon Fuels by Bomb Calorimeter (High-Precision Method), IBR approved for  $\frac{63.11(b)}{2}$ .

(28) ASTM D2382-88, Heat of Combustion of Hydrocarbon Fuels by Bomb Calorimeter (High-Precision Method), IBR approved for  $\frac{63.11(b)}{2}$ .

(29) ASTM D2697-86 (Reapproved 1998), Standard Test Method for Volume Nonvolatile Matter in Clear or Pigmented Coatings, IBR approved for <u>§§ 63.3521(b)</u>, and <u>63.5160(c)</u>.

(30) ASTM D2697-03 (Reapproved 2014), Standard Test Method for Volume Nonvolatile Matter in Clear or Pigmented Coatings, approved July 1, 2014, IBR approved for  $\frac{88}{53.3161(f)}$ ,  $\frac{63.3360(c)}{63.3941(b)}$ ,  $\frac{63.4141(b)}{63.4141(b)}$ ,  $\frac{63.4741(a)}{63.4941(b)}$ , and  $\frac{63.8055(b)}{63.8055(b)}$ .

(31) ASTM D2879-83, Standard Method for Vapor Pressure-Temperature Relationship and Initial Decomposition Temperature of Liquids by Isoteniscope, Approved November 28, 1983, IBR approved for <u>§§</u> 63.111, 63.1402, 63.2406, 63.7944, and 63.12005.

(32) ASTM D2879-96, Test Method for Vapor Pressure-Temperature Relationship and Initial Decomposition Temperature of Liquids by Isoteniscope, (Approved 1996), IBR approved for  $\frac{\&\& 63.111}{\&\& 63.12005}$ .

(33) ASTM D2879-23, Standard Test Method for Vapor Pressure-Temperature Relationship and Initial Decomposition Temperature of Liquids by Isoteniscope, approved December 1, 2023; IBR approved for <u>§ 63.101(b)</u>.

(34) ASTM D2908-74, Standard Practice for Measuring Volatile Organic Matter in Water by Aqueous-Injection Gas Chromatography, Approved June 27, 1974, IBR approved for <u>§ 63.1329(c)</u>.

(35) ASTM D2908-91, Standard Practice for Measuring Volatile Organic Matter in Water by Aqueous-Injection Gas Chromatography, Approved December 15, 1991, IBR approved for  $\frac{\& 63.1329(c)}{C}$ .

(36) ASTM D2908-91(Reapproved 2001), Standard Practice for Measuring Volatile Organic Matter in Water by Aqueous-Injection Gas Chromatography, Approved December 15, 1991, IBR approved for  $\frac{\$ 63.1329(c)}{2}$ .

(37) ASTM D2908-91(Reapproved 2005), Standard Practice for Measuring Volatile Organic Matter in Water by Aqueous-Injection Gas Chromatography, Approved December 1, 2005, IBR approved for  $\frac{63.1329(c)}{c}$ .

(38) ASTM D2908-91(Reapproved 2011), Standard Practice for Measuring Volatile Organic Matter in Water by Aqueous-Injection Gas Chromatography, Approved May 1, 2011, IBR approved for  $\S$  63.1329(c).

(39) ASTM D2986-95A, "Standard Practice for Evaluation of Air Assay Media by the Monodisperse DOP (Dioctyl Phthalate) Smoke Test," approved September 10, 1995, IBR approved for <u>section 7.1.1</u> of Method 315 in appendix A to this part.

(40) ASTM D3173-03 (Reapproved 2008), Standard Test Method for Moisture in the Analysis Sample of Coal and Coke, (Approved February 1, 2008), IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(41) ASTM D3257-93, Standard Test Methods for Aromatics in Mineral Spirits by Gas Chromatography, IBR approved for <u>§</u> 63.786(b).

(42) ASTM D3370-76, Standard Practices for Sampling Water, Approved August 27, 1976, IBR approved for <u>§ 63.1329(c)</u>.

(43) ASTM D3370-95a, Standard Practices for Sampling Water from Closed Conduits, Approved September 10, 1995, IBR approved for <u>§ 63.1329(c)</u>.

(44) ASTM D3370-07, Standard Practices for Sampling Water from Closed Conduits, Approved December 1, 2007, IBR approved for <u>§ 63.1329(c)</u>.

(45) ASTM D3370-08, Standard Practices for Sampling Water from Closed Conduits, Approved October 1, 2008, IBR approved for  $\frac{63.1329(c)}{2}$ .

(46) ASTM D3370-10, Standard Practices for Sampling Water from Closed Conduits, Approved December 1, 2010, IBR approved for <u>§ 63.1329(c)</u>.

(47) ASTM D3588-98 (Reapproved 2003), Standard Practice for Calculating Heat Value, Compressibility Factor, and Relative Density of Gaseous Fuels, (Approved May 10, 2003), IBR approved for <u>§§ 63.772(h)</u> and <u>63.1282(g)</u>.

(48) ASTM D3695-88, Standard Test Method for Volatile Alcohols in Water by Direct Aqueous-Injection Gas Chromatography, IBR approved for  $\S 63.365(e)$ .

(49) ASTM D3792-91, Standard Method for Water Content of Water-Reducible Paints by Direct Injection into a Gas Chromatograph, IBR approved for appendix A to subpart II.

(50) ASTM D3912-80, Standard Test Method for Chemical Resistance of Coatings Used in Light-Water Nuclear Power Plants, IBR approved for  $\frac{63.782}{2}$ .

(51) ASTM D3960-98, Standard Practice for Determining Volatile Organic Compound (VOC) Content of Paints and Related Coatings, approved November 10, 1998, IBR approved for <u>§§ 63.3360(c)</u> and <u>63.8055(b)</u>.

(52) ASTM D4006-11, Standard Test Method for Water in Crude Oil by Distillation, including Annex A1 and Appendix X1, (Approved June 1, 2011), IBR approved for  $\S$  63.10005(i) and table 6 to subpart DDDDD.

(53) ASTM D4017-81, Standard Test Method for Water in Paints and Paint Materials by the Karl Fischer Titration Method, IBR approved for appendix A to subpart II.

(54) ASTM D4017-90, Standard Test Method for Water in Paints and Paint Materials by the Karl Fischer Titration Method, IBR approved for appendix A to subpart II.

(55) ASTM D4017-96a, Standard Test Method for Water in Paints and Paint Materials by the Karl Fischer Titration Method, IBR approved for appendix A to subpart II.

(56) ASTM D4057-06 (Reapproved 2011), Standard Practice for Manual Sampling of Petroleum and Petroleum Products, including Annex A1, (Approved June 1, 2011), IBR approved for <u>§ 63.10005(i)</u> and table 6 to subpart DDDDD.

(57) ASTM D4082-89, Standard Test Method for Effects of Gamma Radiation on Coatings for Use in Light-Water Nuclear Power Plants, IBR approved for  $\frac{\& 63.782}{\& 63.782}$ .

(58) ASTM D4084-07, Standard Test Method for Analysis of Hydrogen Sulfide in Gaseous Fuels (Lead Acetate Reaction Rate Method), (Approved June 1, 2007), IBR approved for table 6 to subpart DDDDD.

(59) ASTM D4177-95 (Reapproved 2010), Standard Practice for Automatic Sampling of Petroleum and Petroleum Products, including Annexes A1 through A6 and Appendices X1 and X2, (Approved May 1, 2010), IBR approved for § 63.10005(i) and table 6 to subpart DDDDD.

(60) ASTM D4208-02 (Reapproved 2007), Standard Test Method for Total Chlorine in Coal by the Oxygen Bomb Combustion/Ion Selective Electrode Method, approved May 1, 2007, IBR approved for table 6 to subpart DDDDD.

(61) ASTM D4239-14e1, "Standard Test Method for Sulfur in the Analysis Sample of Coal and Coke Using High-Temperature Tube Furnace Combustion," approved March 1, 2014, IBR approved for <u>§ 63.849(f)</u>.

(62) ASTM D4256-89, Standard Test Method for Determination of the Decontaminability of Coatings Used in Light-Water Nuclear Power Plants, IBR approved for  $\frac{63.782}{2}$ .

(63) ASTM D4256-89 (Reapproved 94), Standard Test Method for Determination of the Decontaminability of Coatings Used in Light-Water Nuclear Power Plants, IBR approved for  $\frac{\& 63.782}{\& 63.782}$ .

(64) ASTM D4282-15, Standard Test Method for Determination of Free Cyanide in Water and Wastewater by Microdiffusion, Approved July 15, 2015, IBR approved for  $\frac{63.1103(g)}{2}$ .

(65) ASTM D4606-03 (Reapproved 2007), Standard Test Method for Determination of Arsenic and Selenium in Coal by the Hydride Generation/Atomic Absorption Method, (Approved October 1, 2007), IBR approved for table 6 to subpart DDDDD.

(66) ASTM D4809-95, Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter (Precision Method), IBR approved for  $\underline{\S \ 63.11(b)}$ .

(67) ASTM D4840-99 (Reapproved 2018)<sup>e</sup>, Standard Guide for Sampling Chain-of-Custody Procedures, approved August 15, 2018, IBR approved for appendix A to part 63.

(68) ASTM D4891-89 (Reapproved 2006), Standard Test Method for Heating Value of Gases in Natural Gas Range by Stoichiometric Combustion, (Approved June 1, 2006), IBR approved for  $\frac{\&\& 63.772(h)}{\& 63.772(h)}$  and  $\frac{63.1282(g)}{\& 63.772(h)}$ .

(69) ASTM D5066-91 (Reapproved 2017), Standard Test Method for Determination of the Transfer Efficiency Under Production Conditions for Spray Application of Automotive Paints-Weight Basis, approved June 1, 2017, IBR approved for  $\S$  <u>63.3161(g)</u>.

(70) ASTM D5087-02, Standard Test Method for Determining Amount of Volatile Organic Compound (VOC) Released from Solventborne Automotive Coatings and Available for Removal in a VOC Control Device (Abatement), IBR approved for  $\frac{63.3165(e)}{100}$  and appendix A to subpart IIII.

(71) ASTM D5192-09, Standard Practice for Collection of Coal Samples from Core, (Approved June 1, 2009), IBR approved for table 6 to subpart DDDDD.

(72) ASTM D5198-09, Standard Practice for Nitric Acid Digestion of Solid Waste, (Approved February 1, 2009), IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(73) ASTM D5228-92, Standard Test Method for Determination of Butane Working Capacity of Activated Carbon, (Reapproved 2005), IBR approved for <u>§ 63.11092(b)</u>.

(74) ASTM D5291-02, Standard Test Methods for Instrumental Determination of Carbon, Hydrogen, and Nitrogen in Petroleum Products and Lubricants, IBR approved for appendix A to subpart MMMM.

(75) ASTM D5790-95 (Reapproved 2012), Standard Test Method for Measurement of Purgeable Organic Compounds in Water by Capillary Column Gas Chromatography/Mass Spectrometry, Approved June 15, 2012, IBR approved for <u>§</u> <u>63.2485(h)</u> and Table 4 to subpart UUUU.

(76) ASTM D5864-11, Standard Test Method for Determining Aerobic Aquatic Biodegradation of Lubricants or Their Components, (Approved March 1, 2011), IBR approved for table 6 to subpart DDDDD.

(77) ASTM D5865-10a, Standard Test Method for Gross Calorific Value of Coal and Coke, (Approved May 1, 2010), IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(78) ASTM D5954-98 (Reapproved 2006), Test Method for Mercury Sampling and Measurement in Natural Gas by Atomic Absorption Spectroscopy, (Approved December 1, 2006), IBR approved for table 6 to subpart DDDDD.

(79) ASTM D5965-02 (Reapproved 2013), Standard Test Methods for Specific Gravity of Coating Powders, approved June 1, 2013, IBR approved for  $\frac{\& 63.3151(b)}{63.3951(c)}$ .

(80) ASTM D6053-00, Standard Test Method for Determination of Volatile Organic Compound (VOC) Content of Electrical Insulating Varnishes, IBR approved for appendix A to subpart MMMM.

(81) ASTM D6093-97 (Reapproved 2003), Standard Test Method for Percent Volume Nonvolatile Matter in Clear or Pigmented Coatings Using a Helium Gas Pycnometer, IBR approved for <u>§§ 63.3521</u> and <u>63.5160(c)</u>.

(82) ASTM D6093-97 (Reapproved 2016), Standard Test Method for Percent Volume Nonvolatile Matter in Clear or Pigmented Coatings Using a Helium Gas Pycnometer, approved December 1, 2016, IBR approved for <u>§§</u> <u>63.3161(f)</u>, <u>63.3360(c)</u>, <u>63.3941(b)</u>, <u>63.4141(b)</u>, <u>63.4741(a)</u> and <u>(b)</u>, and <u>63.4941(b)</u>.

(83) ASTM D6196-03 (Reapproved 2009), Standard Practice for Selection of Sorbents, Sampling, and Thermal Desorption Analysis Procedures for Volatile Organic Compounds in Air, Approved March 1, 2009, IBR approved for appendix A to this part: Method 325A and Method 325B.

(84) ASTM D6266-00a (Reapproved 2017), Standard Test Method for Determining the Amount of Volatile Organic Compound (VOC) Released from Waterborne Automotive Coatings and Available for Removal in a VOC Control Device (Abatement), approved July 1, 2017, IBR approved for <u>§ 63.3165(e)</u>.

(85) ASTM D6323-98 (Reapproved 2003), Standard Guide for Laboratory Subsampling of Media Related to Waste Management Activities, (Approved August 10, 2003), IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(86) ASTM D6348-03, Standard Test Method for Determination of Gaseous Compounds by Extractive Direct Interface Fourier Transform Infrared (FTIR) Spectroscopy, including Annexes A1 through A8, Approved October 1, 2003, IBR approved for <u>§§ 63.457(b)</u>, <u>63.997(e)</u>, and <u>63.1349</u>, table 4 to subpart DDDD, table 5 to subpart EEEE, table 4 to subpart UUUU, table 4 subpart ZZZZ, and table 8 to subpart HHHHHHH.

(87) ASTM D6348-03 (Reapproved 2010), Standard Test Method for Determination of Gaseous Compounds by Extractive Direct Interface Fourier Transform Infrared (FTIR) Spectroscopy, including Annexes A1 through A8, Approved October 1, 2010, IBR approved for <u>§§ 63.1571(a)</u>, <u>63.4751(i)</u>, <u>63.4752(e)</u>, <u>63.4766(b)</u>, <u>63.7142(a)</u> and <u>(b)</u>, tables 4 and 5 to subpart JJJJJ, tables 4 and 6 to subpart KKKKK, tables 1, 2, and 5 to subpart UUUUU and appendix B to subpart UUUUU.

(88) ASTM D6348-12e1, Standard Test Method for Determination of Gaseous Compounds by Extractive Direct Interface Fourier Transform Infrared (FTIR) Spectroscopy, Approved February 1, 2012, IBR approved for <u>\$</u> 63.997(e), 63.1571(a), and 63.2354(b), table 5 to subpart EEEE, table 4 to subpart UUUU, <u>\$</u> 63.7142(a) and (b) and 63.8000(d), and table 4 to subpart SSSSS.

(89) ASTM D6348-12 (Reapproved 2020), Standard Test Method for Determination of Gaseous Compounds by Extractive Direct Interface Fourier Transform Infrared (FTIR) Spectroscopy, Approved February 1, 2012, IBR approved for <u>§§</u> <u>63.109(a)</u>; <u>63.365(b)</u>; <u>63.509(a)</u>; <u>63.7322(d)</u>, (e), and (g); <u>63.7825(g)</u> and (h); table 5 to subpart AAAAA.

(90) ASTM D6350-98 (Reapproved 2003), Standard Test Method for Mercury Sampling and Analysis in Natural Gas by Atomic Fluorescence Spectroscopy, (Approved May 10, 2003), IBR approved for table 6 to subpart DDDDD.

(91) ASTM D6357-11, Test Methods for Determination of Trace Elements in Coal, Coke, and Combustion Residues from Coal Utilization Processes by Inductively Coupled Plasma Atomic Emission Spectrometry, (Approved April 1, 2011), IBR approved for table 6 to subpart DDDDD.

(92) ASTM D6376-10, "Standard Test Method for Determination of Trace Metals in Petroleum Coke by Wavelength Dispersive X-Ray Fluorescence Spectroscopy," Approved July 1, 2010, IBR approved for <u>§ 63.849(f)</u>.

(93) ASTM D6420-99, Standard Test Method for Determination of Gaseous Organic Compounds by Direct Interface Gas Chromatography-Mass Spectrometry, IBR approved for  $\frac{\$\$ 63.5799}{\$\$ 63.5799}$  and  $\frac{63.5850}{\$\$ 63.5799}$ .

(94) ASTM D6420-99 (Reapproved 2004), Standard Test Method for Determination of Gaseous Organic Compounds by Direct Interface Gas Chromatography-Mass Spectrometry (Approved October 1, 2004), IBR approved for <u>§§</u> <u>63.457(b)</u>, <u>63.772(a)</u>, <u>63.1282(a)</u> and <u>(d)</u>, and table 8 to subpart HHHHHHH.

(95) ASTM D6420-99 (Reapproved 2010), Standard Test Method for Determination of Gaseous Organic Compounds by Direct Interface Gas Chromatography-Mass Spectrometry, Approved October 1, 2010, IBR approved for <u>§§ 63.670(j)</u>; table 4 to subpart UUUU; 63.1450(f); 63.7142(b); appendix A to this part.

(96) ASTM D6420-18, Standard Test Method for Determination of Gaseous Organic Compounds by Direct Interface Gas Chromatography-Mass Spectrometry, approved November 1, 2018' IBR approved for <u>§§</u> <u>63.101(b)</u>; <u>63.115(g)</u>; <u>63.116(c)</u>; <u>63.126(d)</u>; <u>63.128(a)</u>; <u>63.139(c)</u>; <u>63.145(d)</u> and <u>(i)</u>; <u>63.150(g)</u>; <u>63.180(d</u>; 63.305(c); 63.482(b); 63.485(t); 63.488(b); 63.490(c) and (e); 63.496(b); 63.500(c); 63.501(a); 63.502(j); 63.503(a) and (g); 63.525(a) and (e); 63.987(b); 63.997(e); 63.2354(b); table 5 to subpart EEEE; <u>§§</u> <u>63.2450(i)</u>; <u>63.8000(d)</u>.

(97) ASTM D6522-00, Standard Test Method for Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Concentrations in Emissions from Natural Gas Fired Reciprocating Engines, Combustion Turbines, Boilers, and Process Heaters Using Portable Analyzers, IBR approved for § 63.9307(c).

(98) ASTM D6522-00 (Reapproved 2005), Standard Test Method for Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Concentrations in Emissions from Natural Gas Fired Reciprocating Engines, Combustion Turbines, Boilers, and Process Heaters Using Portable Analyzers, (Approved October 1, 2005), IBR approved for table 4 to subpart ZZZZ, table 5 to subpart DDDDDD, table 4 to subpart JJJJJJ, and <u>§§ 63.772(e)</u> and (<u>h</u>) and 63.1282(d) and (g).

(99) ASTM D6522-11 Standard Test Method for Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Concentrations in Emissions from Natural Gas-Fired Reciprocating Engines, Combustion Turbines, Boilers, and Process Heaters Using Portable Analyzers, Approved December 1, 2011, IBR approved for <u>§ 63.1961(a)</u> and table 3 to subpart YYYY.

(100) ASTM D6721-01 (Reapproved 2006), Standard Test Method for Determination of Chlorine in Coal by Oxidative Hydrolysis Microcoulometry, (Approved April 1, 2006), IBR approved for table 6 to subpart DDDDD.

(101) ASTM D6722-01 (Reapproved 2006), Standard Test Method for Total Mercury in Coal and Coal Combustion Residues by the Direct Combustion Analysis, (Approved April 1, 2006), IBR approved for Table 6 to subpart DDDDD and Table 5 to subpart JJJJJJ.

(102) ASTM D6735-01 (Reapproved 2009), Standard Test Method for Measurement of Gaseous Chlorides and Fluorides from Mineral Calcining Exhaust Sources—Impinger Method, IBR approved for <u>§ 63.7142(b)</u>, tables 4 and 5 to subpart JJJJJ, and tables 4 and 6 to subpart KKKKK.

(103) ASTM D6751-11b, Standard Specification for Biodiesel Fuel Blend Stock (B100) for Middle Distillate Fuels, (Approved July 15, 2011), IBR approved for  $\frac{\$\$ 63.7575}{\$\$ 63.7575}$  and  $\frac{63.11237}{\$\$ 63.11237}$ .

(104) ASTM D6784-02 (Reapproved 2008), Standard Test Method for Elemental, Oxidized, Particle-Bound and Total Mercury in Flue Gas Generated from Coal-Fired Stationary Sources (Ontario Hydro Method), Approved April 1, 2008; IBR approved for <u>§§ 63.2465(d)</u>; <u>63.11646(a)</u>; <u>63.11647(a)</u> and <u>(d)</u>; tables 1, 2, 5, 11, 12t, and 13 to subpart DDDDD; tables 4 and 5 to subpart JJJJJ; tables 4 and 6 to subpart KKKKK; table 4 to subpart JJJJJJ.

(105) ASTM D6784-16, Standard Test Method for Elemental, Oxidized, Particle-Bound and Total Mercury in Flue Gas Generated from Coal-Fired Stationary Sources (Ontario Hydro Method), Approved March 1, 2016; IBR approved for <u>§§</u> <u>63.1450(d)</u>; <u>63.9621</u>; table 5 to subpart AAAAA; table 17 to subpart XXXX; table 5 to subpart UUUUU; appendix A to subpart UUUUU.

(106) ASTM D6883-04, Standard Practice for Manual Sampling of Stationary Coal from Railroad Cars, Barges, Trucks, or Stockpiles, (Approved June 1, 2004), IBR approved for table 6 to subpart DDDDD.

(107) ASTM D6886-18, Standard Test Method for Determination of the Weight Percent Individual Volatile Organic Compounds in Waterborne Air-Dry Coatings by Gas Chromatography, approved October 1, 2018, IBR approved for § 63.2354(c).

(108) ASTM D7237-18, Standard Test Method for Free Cyanide and Aquatic Free Cyanide with Flow Injection Analysis (FIA) Utilizing Gas Diffusion Separation and Amperometric Detection, Approved December 1, 2018, IBR approved for  $\S$  <u>63.1103(g)</u>.

(109) ASTM D7430-11ae1, Standard Practice for Mechanical Sampling of Coal, (Approved October 1, 2011), IBR approved for table 6 to subpart DDDDD.

(110) ASTM D7520-16, Standard Test Method for Determining the Opacity of a Plume in the Outdoor Ambient Atmosphere, approved April 1, 2016; IBR approved for <u>§§ 63.1450(c)</u>, (e), and (g); <u>63.1453(h)</u>; <u>63.1625(b)</u>; table 3 to subpart LLLLL; <u>§§ 63.7823(c)</u> through (f), <u>63.7833(g)</u>; <u>63.11423(c)</u>.

(111) [Reserved]

(112) ASTM E145-94 (Reapproved 2001), Standard Specification for Gravity-Convection and Forced-Ventilation Ovens, IBR approved for appendix A to subpart PPPP.

(113) ASTM E180-93, Standard Practice for Determining the Precision of ASTM Methods for Analysis and Testing of Industrial Chemicals, IBR approved for  $\frac{63.786(b)}{5}$ .

(114) ASTM E260-91, General Practice for Packed Column Gas Chromatography, IBR approved for <u>§§</u> <u>63.750(b)</u> and <u>63.786(b)</u>.

(115) ASTM E260-96, General Practice for Packed Column Gas Chromatography, IBR approved for <u>§§</u> <u>63.750(b)</u> and <u>63.786(b)</u>.

(116) ASTM E515-95 (Reapproved 2000), Standard Test Method for Leaks Using Bubble Emission Techniques, IBR approved for  $\frac{63.425(i)}{10}$ .

(117) ASTM E711-87 (Reapproved 2004), Standard Test Method for Gross Calorific Value of Refuse-Derived Fuel by the Bomb Calorimeter, (Approved August 28, 1987), IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(118) ASTM E776-87 (Reapproved 2009), Standard Test Method for Forms of Chlorine in Refuse-Derived Fuel, (Approved July 1, 2009), IBR approved for table 6 to subpart DDDDD.

(119) ASTM E871-82 (Reapproved 2006), Standard Test Method for Moisture Analysis of Particulate Wood Fuels, (Approved November 1, 2006), IBR approved for table 6 to subpart DDDDD and table 5 to subpart JJJJJJ.

(120) ASTM UOP539-12, Refinery Gas Analysis by GC, Copyright 2012 (to UOP), IBR approved for § 63.670(j).

Note 2 to paragraph (i):

Standards listed in this <u>paragraph (i)</u> may also be available from standards resellers including the Standards Store, <u>https://global.ihs.com</u>.

(j) Bay Area Air Quality Management District (BAAQMD), 939 Ellis Street, San Francisco, California 94109, <u>http://www.arb.ca.gov/DRDB/BA/CURHTML/ST/st30.pdf</u>.

(1) "BAAQMD Source Test Procedure ST-30—Static Pressure Integrity Test, Underground Storage Tanks," adopted November 30, 1983, and amended December 21, 1994, IBR approved for  $\frac{63.11120(a)}{2}$ .

(2) [Reserved]

(k) British Standards Institute, 389 Chiswick High Road, London W4 4AL, United Kingdom.

(1) BS EN 1593:1999, Non-destructive Testing: Leak Testing—Bubble Emission Techniques, IBR approved for <u>§ 63.425(i)</u>.

(2) BS EN 14662-4:2005, Ambient air quality standard method for the measurement of benzene concentrations—Part 4: Diffusive sampling followed by thermal desorption and gas chromatography, Published June 27, 2005, IBR approved for appendix A to this part: Method 325A and Method 325B.

(1) California Air Resources Board (CARB), 1001 I Street, P.O. Box 2815, Sacramento, CA 95812-2815, Telephone (916) 327-0900, <u>http://www.arb.ca.gov/</u>.

(1) Method 310, "Determination of Volatile Organic Compounds (VOC) in Consumer Products and Reactive Organic Compounds (ROC) in Aerosol Coating Products," amended May 25, 2018, IBR approved for <u>§ 63.8055(b)</u>.

(2) Method 428, "Determination Of Polychlorinated Dibenzo-P-Dioxin (PCDD), Polychlorinated Dibenzofuran (PCDF), and Polychlorinated Biphenyle Emissions from Stationary Sources," amended September 12, 1990, IBR approved for  $\S$  <u>63.849(a)(13)</u> and <u>(14)</u>.

(3) Method 429, Determination of Polycyclic Aromatic Hydrocarbon (PAH) Emissions from Stationary Sources, Adopted September 12, 1989, Amended July 28, 1997, IBR approved for <u>§ 63.1625(b)</u>.

(4) California Air Resources Board Vapor Recovery Test Procedure TP-201.1—"Volumetric Efficiency for Phase I Vapor Recovery Systems," adopted April 12, 1996, and amended February 1, 2001 and October 8, 2003, IBR approved for <u>§</u> <u>63.11120(b)</u>.

(5) California Air Resources Board Vapor Recovery Test Procedure TP-201.1E—"Leak Rate and Cracking Pressure of Pressure/Vacuum Vent Valves," adopted October 8, 2003, IBR approved for <u>§ 63.11120(a)</u>.

(6) California Air Resources Board Vapor Recovery Test Procedure TP-201.3—"Determination of 2-Inch WC Static Pressure Performance of Vapor Recovery Systems of Dispensing Facilities," adopted April 12, 1996 and amended March 17, 1999, IBR approved for <u>§ 63.11120(a)</u>.

(m) Composite Panel Association, 19465 Deerfield Avenue, Suite 306, Leesburg, VA 20176, Telephone (703)724-1128, and <u>www.compositepanel.org</u>.

(1) ANSI A135.4-2012, Basic Hardboard, approved June 8, 2012, IBR approved for § 63.4781.

(2) [Reserved]

(n) Environmental Protection Agency. Air and Radiation Docket and Information Center, 1200 Pennsylvania Avenue NW., Washington, DC 20460, telephone number (202) 566-1745.

(1) California Regulatory Requirements Applicable to the Air Toxics Program, November 16, 2010, IBR approved for  $\underline{\$}$  <u>63.99(a)</u>.

(2) New Jersey's Toxic Catastrophe Prevention Act Program, (July 20, 1998), IBR approved for § 63.99(a).

(3) Delaware Department of Natural Resources and Environmental Control, Division of Air and Waste Management, Accidental Release Prevention Regulation, sections 1 through 5 and sections 7 through 14, effective January 11, 1999, IBR approved for  $\frac{63.99(a)}{2}$ .

(4) State of Delaware Regulations Governing the Control of Air Pollution (October 2000), IBR approved for <u>§ 63.99(a)</u>.

(5) Massachusetts Department of Environmental Protection regulations at 310 CMR 7.26(10)-(16), Air Pollution Control, effective as of September 5, 2008, corrected March 6, 2009, and 310 CMR 70.00, Environmental Results Program Certification, effective as of December 28, 2007. IBR approved for <u>§ 63.99(a)</u>.

(6)

(i) New Hampshire Regulations at Env-Sw 2100, Management and Control of Asbestos Disposal Sites Not Operated after July 9, 1981, effective September 1, 2018, (including a letter from Robert R. Scott, Commissioner, Department of Environmental Services, State of New Hampshire, to David J. Alukonis, Director, Office of Legislative Services, dated October 23, 2018, certifying that the enclosed rule, Env-Sw 2100, is the official version of this rule), IBR approved for § 63.99(a).

(ii) New Hampshire Code of Administrative Rules: Chapter Env-A 1800, Asbestos Management and Control, effective as of May 5, 2017 (certified with June 23, 2017 letter from Clark B. Freise, Assistant Commissioner, Department of

Environmental Services, State of New Hampshire), as follows: Revision Notes #1 and #2; Part Env-A 1801-1807, excluding Env-A 1801.02(e), Env-A 1801.07, Env-A 1802.02, Env-A 1802.04, Env-A 1802.07-1802.09, Env-A 1802.13, Env-A 1802.15-1802.17, Env-A 1802.25, Env-A 1802.31, Env-A 1802.37, Env-A 1802.40, Env-A 1802.44, and Env-A 1803.05-1803.09; and Appendices B, C, and D; IBR approved for <u>§ 63.99(a)</u>.

(7) Maine Department of Environmental Protection regulations at Chapter 125, Perchloroethylene Dry Cleaner Regulation, effective as of June 2, 1991, last amended on June 24, 2009. IBR approved for  $\frac{\delta 63.99(a)}{100}$ .

(8) California South Coast Air Quality Management District's "Spray Equipment Transfer Efficiency Test Procedure for Equipment User, May 24, 1989," IBR approved for  $\frac{\$\$ 63.11173(e)}{\$\$ 63.11173(e)}$  and  $\frac{63.11516(d)}{\$\$ 63.11516(d)}$ .

(9) California South Coast Air Quality Management District's "Guidelines for Demonstrating Equivalency with District Approved Transfer Efficient Spray Guns, September 26, 2002," Revision 0, IBR approved for  $\underline{\$\$}$ <u>63.11173(e)</u> and <u>63.11516(d)</u>.

(10) Rhode Island Regulations at Title 250 Department of Environmental Management, Chapter 120 Air Resources, Subchapter 05 Air Pollution Control:

(i) 250-RICR-120-05-0. Part 0 General Definitions Regulation, effective as of January 4, 2022, excluding 0.2 "Application"; IBR approved for  $\frac{63.99(a)}{2}$ .

(ii) 250-RICR-120-05-36. Part 36 Control of Emissions from Organic Solvent Cleaning, effective as of June 13, 2022, excluding 36.2 "Application", 36.5.A.28, "Industrial solvent cleaning", 36.6.D, and 36.17 "Requirements for Industrial Cleaning Solvents"; IBR approved for § 63.99(a).

(11) [Reserved]

(12) Alaska Statute 42.45.045. Renewable energy grant fund and recommendation program, available at <u>http://www.legis.state.ak.us/basis/folio.asp</u>, IBR approved for <u>§ 63.6675</u>.

(13) Vermont Air Pollution Control Regulations, Chapter 5, Air Pollution Control, <u>section 5-253.11</u>, Perchloroethylene Dry Cleaning, effective as of December 15, 2016. Incorporation by reference approved for  $\frac{63.99(a)}{2}$ .

(o) U.S. Environmental Protection Agency (EPA), 1200 Pennsylvania Avenue NW, Washington, DC 20460; phone: (202) 272-0167; website: <u>www.epa.gov/aboutepa/forms/contact-epa</u>.

(1) EPA/100/R-10/005, Recommended Toxicity Equivalence Factors (TEFs) for Human Health Risk Assessments of 2, 3, 7, 8-Tetrachlorodibenzo-p-dioxin and Dioxin-Like Compounds, December 2010; IBR approved for <u>§§ 63.1450(f); 63.1459</u>; table 2 to subpart QQQ; table 1 to subpart AAAAA. (Available at <u>https://www.epa.gov/sites/default/files/2013-09/documents/tefs-for-dioxin-epa-00-r-10-005-final.pdf</u>.)

(2) EPA-453/R-01-005, National Emission Standards for Hazardous Air Pollutants (NESHAP) for Integrated Iron and Steel Plants—Background Information for Proposed Standards, Final Report, January 2001; IBR approved for <u>§ 63.7491(g)</u>.

(3) EPA-454/B-08-002, Quality Assurance Handbook for Air Pollution Measurement Systems; Volume IV: Meteorological Measurements, Version 2.0 (Final), Issued March 2008; IBR approved for <u>§§ 63.184(c)</u>; <u>63.7792(b)</u>.

(4) EPA-454/R-98-015, Fabric Filter Bag Leak Detection Guidance, September 1997; IBR approved for <u>§§</u> <u>63.548(e)</u>; <u>63.864(e)</u>; <u>63.6012(c)</u>; <u>63.7525(j)</u>; <u>63.8450(e)</u>; <u>63.8600(e)</u>; <u>63.9632(a)</u>; <u>63.9804(f)</u>; <u>63.11224(f)</u>; <u>63.11423(e)</u>. (Available at: <u>https://nepis.epa.gov/Exe/ZvPDF.cgi?Dockey=2000D576.pdf</u>).

(5) EPA-454/R-99-005, Office of Air Quality Planning and Standards (OAQPS), Meteorological Monitoring Guidance for Regulatory Modeling Applications, February 2000; IBR approved for appendix A to this part.

(6) EPA/600/R-12/531, EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards, May 2012; IBR approved for <u>§ 63.2163(b)</u>.

(7) EPA-625/3-89-016, Interim Procedures for Estimating Risks Associated with Exposures to Mixtures of Chlorinated Dibenzo-p-Dioxins and -Dibenzofurans (CDDs and CDFs) and 1989 Update, March 1989; IBR approved for <u>§ 63.1513(d)</u>.

(8) EPA-821-R-02-019, Method 1631 Revision E, Mercury in Water by Oxidation, Purge and Trap, and Cold Vapor Atomic Absorption Fluorescence Spectrometry, Revision E, August 2002; IBR approved for table 6 to subpart DDDDD.

(9) EPA Method 200.8, Determination of Trace Elements in Waters and Wastes by Inductively Coupled Plasma—Mass Spectrometry, Revision 5.4, 1994; IBR approved for table 6 to subpart DDDDD.

(10) In EPA Publication No. SW-846, Test Methods for Evaluating Solid Waste, Physical/Chemical Methods (Available from: <u>www.epa.gov/hw-sw846/sw-846-compendium</u>):

(i) SW-846-0011, Sampling for Selected Aldehyde and Ketone Emissions from Stationary Sources, Revision 0, December 1996; IBR approved for table 4 to subpart DDDD.

(ii) SW-846-3020A, Acid Digestion of Aqueous Samples And Extracts For Total Metals For Analysis By GFAA Spectroscopy, Revision 1, July 1992; IBR approved for table 6 to subpart DDDDD; table 5 to subpart JJJJJJ.

(iii) SW-846-3050B, Acid Digestion of Sediments, Sludges, and Soils, Revision 2, December 1996; IBR approved for table 6 to subpart DDDDD; table 5 to subpart JJJJJJ.

(iv) SW-846-5030B, Purge-And-Trap For Aqueous Samples, Revision 2, December 1996; IBR approved for  $\underline{\$\$}$  <u>63.109(b)</u>, (c), (d), and (e); <u>63.509(b)</u> and (c); <u>63.2492(b)</u> and (c).

(v) SW-846-5031, Volatile, Nonpurgeable, Water-Soluble Compounds by Azeotropic Distillation, Revision 0, December 1996; IBR approved for  $\S$  63.109(b), (c), (d), and (e); 63.509(b) and (c); 63.2492(b) and (c).

(vi) SW-846-7470A, Mercury In Liquid Waste (Manual Cold-Vapor Technique), Revision 1, September 1994; IBR approved for table 6 to subpart DDDDD; table 5 to subpart JJJJJJ.

(vii) SW-846-7471B, Mercury In Solid Or Semisolid Waste (Manual Cold-Vapor Technique), Revision 2, February 2007; IBR approved for table 6 to subpart DDDDD; table 5 to subpart JJJJJJ.

(viii) SW-846-8015C, Nonhalogenated Organics by Gas Chromatography, Revision 3, February 2007; IBR approved for <u>§§</u> <u>63.11960</u>; <u>63.11980</u>; table 10 to subpart HHHHHHH.

(ix) SW-846-8260B, Volatile Organic Compounds by Gas Chromatography/Mass Spectrometry (GC/MS), Revision 2, December 1996; IBR approved for <u>§§ 63.1107(a)</u>; <u>63.11960</u>; <u>63.11980</u>; table 10 to subpart HHHHHHH.

(x) SW-846-8260D, Volatile Organic Compounds By Gas Chromatography/Mass Spectrometry, Revision 4, June 2018; IBR approved for  $\frac{8863.109(b)}{(c)}$ , (c), (d), and (e);  $\frac{63.509(b)}{(c)}$  and (c);  $\frac{63.2492(b)}{(c)}$  and (c).

(xi) SW-846-8270D, Semivolatile Organic Compounds by Gas Chromatography/Mass Spectrometry (GC/MS), Revision 4, February 2007; IBR approved for <u>§§ 63.1107(a)</u>; <u>63.11960</u>; <u>63.11980</u>; table 10 to subpart HHHHHHH.

(xii) SW-846-8315A, Determination of Carbonyl Compounds by High Performance Liquid Chromatography (HPLC), Revision 1, December 1996; IBR approved for <u>§§ 63.11960</u>; <u>63.11980</u>; table 10 to subpart HHHHHH.

(xiii) SW-846-5050, Bomb Preparation Method for Solid Waste, Revision 0, September 1994; IBR approved for table 6 to subpart DDDDD.

(xiv) SW-846-6010C, Inductively Coupled Plasma-Atomic Emission Spectrometry, Revision 3, February 2007; IBR approved for table 6 to subpart DDDDD.

(xv) SW-846-6020A, Inductively Coupled Plasma-Mass Spectrometry, Revision 1, February 2007; IBR approved for table 6 to subpart DDDDD.

(xvi) SW-846-7060A, Arsenic (Atomic Absorption, Furnace Technique), Revision 1, September 1994; IBR approved for table 6 to subpart DDDDD.

(xvii) SW-846-7740, Selenium (Atomic Absorption, Furnace Technique), Revision 0, September 1986; IBR approved for table 6 to subpart DDDDD.

(xviii) SW-846-9056, Determination of Inorganic Anions by Ion Chromatography, Revision 1, February 2007; IBR approved for table 6 to subpart DDDDD.

(xix) SW-846-9076, Test Method for Total Chlorine in New and Used Petroleum Products by Oxidative Combustion and Microcoulometry, Revision 0, September 1994; IBR approved for table 6 to subpart DDDDD.

(xx) SW-846-9250, Chloride (Colorimetric, Automated Ferricyanide AAI), Revision 0, September 1986; IBR approved for table 6 to subpart DDDDD.

(11)-(30) [Reserved]

(31) EPA/100/R-10/005, Recommended Toxicity Equivalence Factors (TEFs) for Human Health Risk Assessments of 2, 3, 7, 8-Tetrachlorodibenzo-p-dioxin and Dioxin-Like Compounds, December 2010; IBR approved for <u>§ 63.1459</u> and table 2 to subpart QQQ. (Available at <u>https://www.epa.gov/sites/default/files/2013-09/documents/tefs-for-dioxin-epa-00-r-10-005-final.pdf</u>.)

(p) International Standards Organization (ISO), 1, ch. de la Voie-Creuse, Case postale 56, CH-1211 Geneva 20, Switzerland, + 41 22 749 01 11, <u>http://www.iso.org/iso/home.htm</u>.

(1) ISO 6978-1:2003(E), Natural Gas—Determination of Mercury—Part 1: Sampling of Mercury by Chemisorption on Iodine, First edition, October 15, 2003, IBR approved for table 6 to subpart DDDDD.

(2) ISO 6978-2:2003(E), Natural gas—Determination of Mercury—Part 2: Sampling of Mercury by Amalgamation on Gold/Platinum Alloy, First edition, October 15, 2003, IBR approved for table 6 to subpart DDDDD.

(3) ISO 16017-2:2003(E): Indoor, ambient and workplace air—sampling and analysis of volatile organic compounds by sorbent tube/thermal desorption/capillary gas chromatography—Part 2: Diffusive sampling, May 15, 2003, IBR approved for appendix A to this part: Method 325A and Method 325B.

(q) National Council of the Paper Industry for Air and Stream Improvement, Inc. (NCASI), P.O. Box 133318, Research Triangle Park, NC 27709-3318 or at <u>http://www.ncasi.org</u>.

(1) NCASI Method DI/MEOH-94.03, Methanol in Process Liquids and Wastewaters by GC/FID, Issued May 2000, IBR approved for <u>§§ 63.457</u> and <u>63.459</u>.

(2) NCASI Method CI/WP-98.01, Chilled Impinger Method For Use At Wood Products Mills to Measure Formaldehyde, Methanol, and Phenol, 1998, Methods Manual, IBR approved for table 4 to subpart DDDD.

(3) NCASI Method DI/HAPS-99.01, Selected HAPs In Condensates by GC/FID, Issued February 2000, IBR approved for § 63.459(b).

(4) NCASI Method IM/CAN/WP-99.02, Impinger/Canister Source Sampling Method for Selected HAPs and Other Compounds at Wood Products Facilities, January 2004, Methods Manual, IBR approved for table 4 to subpart DDDD.

(5) NCASI Method ISS/FP A105.01, Impinger Source Sampling Method for Selected Aldehydes, Ketones, and Polar Compounds, December 2005, Methods Manual, IBR approved for table 4 to subpart DDDD and <u>§§</u> <u>63.4751(i)</u> and <u>63.4752(e)</u>.

(r) National Technical Information Service (NTIS), 5285 Port Royal Road, Springfield, VA 22161, (703) 605-6000 or (800) 553-6847; or for purchase from the Superintendent of Documents, U.S. Government Printing Office, Washington, DC 20402, (202) 512-1800.

(1) Handbook 44, Specificiations, Tolerances, and Other Technical Requirements for Weighing and Measuring Devices 1998, IBR approved for  $\S 63.1303(e)$ .

(2) "Test Methods for Evaluating Solid Waste, Physical/Chemical Methods," EPA Publication SW-846, Third Edition. (A suffix of "A" in the method number indicates revision one (the method has been revised once). A suffix of "B" in the method number indicates revision two (the method has been revised twice).

(i) Method 0023A, "Sampling Method for Polychlorinated Dibenzo-p-Dioxins and Polychlorinated Dibenzofuran Emissions from Stationary Sources," Revision 2, dated August 2018, IBR approved for <u>§ 63.1208(b)</u>.

(ii) Method 9071B, "n-Hexane Extractable Material (HEM) for Sludge, Sediment, and Solid Samples," dated April 1998, IBR approved for <u>§ 63.7824(e)</u>.

(iii) Method 9095A, "Paint Filter Liquids Test," dated December 1996, IBR approved for <u>§§ 63.7700(b)</u> and <u>63.7765</u>.

(iv) Method 9095B, "Paint Filter Liquids Test," (revision 2), dated November 2004, IBR approved for the definition of "Free organic liquids" in § 63.10692, 63.10885(a), and the definition of "Free liquids" in § 63.10906.

(v) SW-846 74741B, Revision 2, "Mercury in Solid or Semisolid Waste (Manual Cold-Vapor Technique)," February 2007, IBR approved for <u>§ 63.11647(f)</u>.

(3) National Institute of Occupational Safety and Health (NIOSH) test method compendium, "NIOSH Manual of Analytical Methods," NIOSH publication no. 94-113, Fourth Edition, August 15, 1994.

# National Emission Standards for Hazardous Air Pollutants (NESHAP) – General Provisions

(i) NIOSH Method 2010, "Amines, Aliphatic," Issue 2, August 15, 1994, IBR approved for <u>§ 63.7732(g)</u>.

(ii) [Reserved]

(s) North American Electric Reliability Corporation, 1325 G Street, NW., Suite 600, Washington, DC 20005-3801, <u>http://www.nerc.com/files/EOP0002-3\_1.pdf</u>.

(1) North American Electric Reliability Corporation Reliability Standard EOP-002-3, Capacity and Energy Emergencies, adopted August 5, 2010, IBR approved for  $\frac{63.6640(f)}{10}$ .

(2) [Reserved]

(t) Technical Association of the Pulp and Paper Industry (TAPPI), 15 Technology Parkway South, Norcross, GA 30092, (800) 332-8686, <u>http://www.tappi.org</u>.

(1) TAPPI T 266, Determination of Sodium, Calcium, Copper, Iron, and Manganese in Pulp and Paper by Atomic Absorption Spectroscopy (Reaffirmation of T 266 om-02), Draft No. 2, July 2006, IBR approved for table 6 to subpart DDDDD.

(2) [Reserved]

(u) Texas Commission on Environmental Quality (TCEQ) Library, Post Office Box 13087, Austin, Texas 78711-3087; phone: (512) 239-0028; email: <u>info@www.tceq.texas.gov</u>; website: <u>www.tceq.texas.gov</u>.

(1) "Air Stripping Method (Modified El Paso Method) for Determination of Volatile Organic Compound Emissions from Water Sources," Revision Number One, dated January 2003, Sampling Procedures Manual, Appendix P: Cooling Tower Monitoring, January 31, 2003; IBR approved for <u>§§</u>

 $\frac{63.104(f)}{f} \text{ and } (g); \\ \frac{63.654(c)}{63.655(i)}; \\ \frac{63.655(i)}{63.1086(e)}; \\ \frac{63.1089}{63.2490(d)}; \\ \frac{63.2525(r)}{63.2525(r)}; \\ \frac{63.11920}{63.11920}. \\ (Available from: www.tceq.texas.gov/downloads/compliance/investigations/assistance/samplingappp.pdf).$ 

(2) [Reserved]

[79 FR 11277, Feb. 27, 2014]

#### **Editorial Note**

### **Editorial Note:**

For Federal Register citations affecting <u>§ 63.14</u>, see the List of CFR Sections Affected, which appears in the Finding Aids section of the printed volume and at <u>www.govinfo.gov</u>.

### § 63.15 Availability of information and confidentiality.

#### (a) Availability of information.

(1) With the exception of information protected through <u>part 2 of this chapter</u>, all reports, records, and other information collected by the Administrator under this part are available to the public. In addition, a copy of each permit application, compliance plan (including the schedule of compliance), notification of compliance status, excess emissions and continuous monitoring systems performance report, and title V permit is available to the public, consistent with protections recognized in section 503(e) of the Act.

(2) The availability to the public of information provided to or otherwise obtained by the Administrator under this part shall be governed by part 2 of this chapter.

(b) Confidentiality.

(1) If an owner or operator is required to submit information entitled to protection from disclosure under section 114(c) of the Act, the owner or operator may submit such information separately. The requirements of section 114(c) shall apply to such information.

(2) The contents of a title V permit shall not be entitled to protection under section 114(c) of the Act; however, information submitted as part of an application for a title V permit may be entitled to protection from disclosure.

### § 63.16 Performance Track Provisions.

(a) Notwithstanding any other requirements in this part, an affected source at any major source or any area source at a Performance Track member facility, which is subject to regular periodic reporting under any subpart of this part, may submit such periodic reports at an interval that is twice the length of the regular period specified in the applicable subparts; provided,

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that for sources subject to permits under <u>40 CFR part 70</u> or <u>71</u> no interval so calculated for any report of the results of any required monitoring may be less frequent than once in every six months.

(b) Notwithstanding any other requirements in this part, the modifications of reporting requirements in <u>paragraph (c)</u> of this section apply to any major source at a Performance Track member facility which is subject to requirements under any of the <u>subparts of this part</u> and which has:

(1) Reduced its total HAP emissions to less than 25 tons per year;

(2) Reduced its emissions of each individual HAP to less than 10 tons per year; and

(3) Reduced emissions of all HAPs covered by each MACT standard to at least the level required for full compliance with the applicable emission standard.

(c) For affected sources at any area source at a Performance Track member facility and which meet the requirements of <u>paragraph (b)(3)</u> of this section, or for affected sources at any major source that meet the requirements of <u>paragraph (b)</u> of this section:

(1) If the emission standard to which the affected source is subject is based on add-on control technology, and the affected source complies by using add-on control technology, then all required reporting elements in the periodic report may be met through an annual certification that the affected source is meeting the emission standard by continuing to use that control technology. The affected source must continue to meet all relevant monitoring and recordkeeping requirements. The compliance certification must meet the requirements delineated in Clean Air Act section 114(a)(3).

(2) If the emission standard to which the affected source is subject is based on add-on control technology, and the affected source complies by using pollution prevention, then all required reporting elements in the periodic report may be met through an annual certification that the affected source is continuing to use pollution prevention to reduce HAP emissions to levels at or below those required by the applicable emission standard. The affected source must maintain records of all calculations that demonstrate the level of HAP emissions required by the emission standard as well as the level of HAP emissions achieved by the affected source. The affected source must continue to meet all relevant monitoring and recordkeeping requirements. The compliance certification must meet the requirements delineated in Clean Air Act section 114(a)(3).

(3) If the emission standard to which the affected source is subject is based on pollution prevention, and the affected source complies by using pollution prevention and reduces emissions by an additional 50 percent or greater than required by the applicable emission standard, then all required reporting elements in the periodic report may be met through an annual certification that the affected source is continuing to use pollution prevention to reduce HAP emissions by an additional 50 percent or greater than required by the applicable emission standard. The affected source must maintain records of all calculations that demonstrate the level of HAP emissions required by the emission standard as well as the level of HAP emissions achieved by the affected source. The affected source must continue to meet all relevant monitoring and recordkeeping requirements. The compliance certification must meet the requirements delineated in Clean Air Act section 114(a)(3).

(4) Notwithstanding the provisions of paragraphs (c)(1) through (3), of this section, for sources subject to permits under  $\frac{40}{CFR \text{ part } 70}$  or  $\frac{71}{1}$ , the results of any required monitoring and recordkeeping must be reported not less frequently than once in every six months.

#### [69 FR 21753, Apr. 22, 2004]

Table 1 to Subpart A of Part 63—Detection Sensitivity Levels (grams per hour)

Monitoring frequency per subpart <sup>a</sup>	Detection sensitivity level
Bi-Monthly	60
Semi-Quarterly	85
Monthly	100

<sup>a</sup> When this alternative work practice is used to identify leaking equipment, the owner or operator must choose one of the monitoring frequencies listed in this table, in lieu of the monitoring frequency specified in the applicable subpart. Bi-monthly means every other month. Semi-quarterly means twice per quarter. Monthly means once per month.

[73 FR 78213, Dec. 22, 2008]

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### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

# Subpart DDDDD—National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters

Source:

76 FR 15664, Mar. 21, 2011, unless otherwise noted.

## What This Subpart Covers

# § 63.7480 What is the purpose of this subpart?

This subpart establishes national emission limitations and work practice standards for hazardous air pollutants (HAP) emitted from industrial, commercial, and institutional boilers and process heaters located at major sources of HAP. This subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limitations and work practice standards.

# § 63.7485 Am I subject to this subpart?

You are subject to this subpart if you own or operate an industrial, commercial, or institutional boiler or process heater as defined in  $\S$  <u>63.7575</u> that is located at, or is part of, a major source of HAP, except as specified in  $\S$  <u>63.7491</u>. For purposes of this subpart, a major source of HAP is as defined in  $\S$  <u>63.2</u>, except that for oil and natural gas production facilities, a major source of HAP is as defined in  $\S$  <u>63.7575</u>.

[<u>78 FR 7162</u>, Jan. 31, 2013]

# § 63.7490 What is the affected source of this subpart?

(a) This subpart applies to new, reconstructed, and existing affected sources as described in <u>paragraphs (a)(1)</u> and (2) of this section.

(1) The affected source of this subpart is the collection at a major source of all existing industrial, commercial, and institutional boilers and process heaters within a subcategory as defined in  $\S$  63.7575.

(2) The affected source of this subpart is each new or reconstructed industrial, commercial, or institutional boiler or process heater, as defined in  $\S$  63.7575, located at a major source.

(b) A boiler or process heater is new if you commence construction of the boiler or process heater after June 4, 2010, and you meet the applicability criteria at the time you commence construction.

(c) A boiler or process heater is reconstructed if you meet the reconstruction criteria as defined in  $\frac{63.2}{3}$ , you commence reconstruction after June 4, 2010, and you meet the applicability criteria at the time you commence reconstruction.

(d) A boiler or process heater is existing if it is not new or reconstructed.

(e) An existing electric utility steam generating unit (EGU) that meets the applicability requirements of this subpart after the effective date of this final rule due to a change (e.g., fuel switch) is considered to be an existing source under this subpart.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7162, Jan. 31, 2013]

# § 63.7491 Are any boilers or process heaters not subject to this subpart?

The types of boilers and process heaters listed in paragraphs (a) through (n) of this section are not subject to this subpart.

(a) An electric utility steam generating unit (EGU) covered by <u>subpart UUUUU of this part</u> or a natural gas-fired EGU as defined in <u>subpart UUUUU of this part</u> firing at least 85 percent natural gas on an annual heat input basis.

(b) A recovery boiler or furnace covered by subpart MM of this part.

(c) A boiler or process heater that is used specifically for research and development, including test steam boilers used to provide steam for testing the propulsion systems on military vessels. This does not include units that provide heat or steam to a process at a research and development facility.

(d) A hot water heater as defined in this subpart.

(e) A refining kettle covered by subpart X of this part.

(f) An ethylene cracking furnace covered by subpart YY of this part.

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## National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

(g) Blast furnace stoves as described in EPA-453/R-01-005 (incorporated by reference, see § 63.14).

(h) Any boiler or process heater that is part of the affected source subject to another subpart of this part, such as boilers and process heaters used as control devices to comply with <u>subparts JJJ</u>, <u>OOO</u>, <u>PPP</u>, and <u>U of this part</u>.

(i) Any boiler or process heater that is used as a control device to comply with another subpart of this <u>part, or part 60</u>, <u>part 61</u>, or <u>part 65 of this chapter</u> provided that at least 50 percent of the average annual heat input during any 3 consecutive calendar years to the boiler or process heater is provided by regulated gas streams that are subject to another standard.

(j) Temporary boilers and process heaters as defined in this subpart.

(k) Blast furnace gas fuel-fired boilers and process heaters as defined in this subpart.

(l) Any boiler or process heater specifically listed as an affected source in any standard(s) established under section 129 of the Clean Air Act.

(m) A unit that burns hazardous waste covered by <u>Subpart EEE of this part</u>. A unit that is exempt from Subpart EEE as specified in  $\S 63.1200(b)$  is not covered by Subpart EEE.

(n) Residential boilers as defined in this subpart.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7162, Jan. 31, 2013; 80 FR 72806, Nov. 20, 2015]

# § 63.7495 When do I have to comply with this subpart?

(a) If you have a new or reconstructed boiler or process heater, you must comply with this subpart by April 1, 2013, or upon startup of your boiler or process heater, whichever is later.

(b) If you have an existing boiler or process heater, you must comply with this subpart no later than January 31, 2016, except as provided in  $\frac{63.6(i)}{2}$ .

(c) If you have an area source that increases its emissions or its potential to emit such that it becomes a major source of HAP, <u>paragraphs (c)(1)</u> and (2) of this section apply to you.

(1) Any new or reconstructed boiler or process heater at the existing source must be in compliance with this subpart upon startup.

(2) Any existing boiler or process heater at the existing source must be in compliance with this subpart within 3 years after the source becomes a major source.

(d) You must meet the notification requirements in  $\S 63.7545$  according to the schedule in  $\S 63.7545$  and in subpart A of this part. Some of the notifications must be submitted before you are required to comply with the emission limits and work practice standards in this subpart.

(e) If you own or operate an industrial, commercial, or institutional boiler or process heater and would be subject to this subpart except for the exemption in § 63.7491(1) for commercial and industrial solid waste incineration units covered by part 60, subpart CCCC or subpart DDDD, and you cease combusting solid waste, you must be in compliance with this subpart and are no longer subject to part 60, subparts CCCC or DDDD beginning on the effective date of the switch as identified under the provisions of § 60.2145(a)(2) and (3) or § 60.2710(a)(2) and (3).

(f) If you own or operate an existing EGU that becomes subject to this subpart after January 31, 2016, you must be in compliance with the applicable existing source provisions of this subpart on the effective date such unit becomes subject to this subpart.

(g) If you own or operate an existing industrial, commercial, or institutional boiler or process heater and would be subject to this subpart except for a exemption in  $\S$  63.7491(i) that becomes subject to this subpart after January 31, 2013, you must be in compliance with the applicable existing source provisions of this subpart within 3 years after such unit becomes subject to this subpart.

(h) If you own or operate an existing industrial, commercial, or institutional boiler or process heater and have switched fuels or made a physical change to the boiler or process heater that resulted in the applicability of a different subcategory after the compliance date of this subpart, you must be in compliance with the applicable existing source provisions of this subpart on the effective date of the fuel switch or physical change.

#### 40 CFR 63 SUBPART DDDDD

## National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

(i) If you own or operate a new industrial, commercial, or institutional boiler or process heater and have switched fuels or made a physical change to the boiler or process heater that resulted in the applicability of a different subcategory, you must be in compliance with the applicable new source provisions of this subpart on the effective date of the fuel switch or physical change.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7162, Jan. 31, 2013; 80 FR 72807, Nov. 20, 2015]

### **Emission Limitations and Work Practice Standards**

## § 63.7499 What are the subcategories of boilers and process heaters?

The subcategories of boilers and process heaters, as defined in  $\S$  63.7575 are:

- (a) Pulverized coal/solid fossil fuel units.
- (b) Stokers designed to burn coal/solid fossil fuel.
- (c) Fluidized bed units designed to burn coal/solid fossil fuel.
- (d) Stokers/sloped grate/other units designed to burn kiln dried biomass/bio-based solid.
- (e) Fluidized bed units designed to burn biomass/bio-based solid.
- (f) Suspension burners designed to burn biomass/bio-based solid.
- (g) Fuel cells designed to burn biomass/bio-based solid.
- (h) Hybrid suspension/grate burners designed to burn wet biomass/bio-based solid.
- (i) Stokers/sloped grate/other units designed to burn wet biomass/bio-based solid.
- (j) Dutch ovens/pile burners designed to burn biomass/bio-based solid.
- (k) Units designed to burn liquid fuel that are non-continental units.
- (l) Units designed to burn gas 1 fuels.
- (m) Units designed to burn gas 2 (other) gases.
- (n) Metal process furnaces.
- (o) Limited-use boilers and process heaters.
- (p) Units designed to burn solid fuel.
- (q) Units designed to burn liquid fuel.
- (r) Units designed to burn coal/solid fossil fuel.
- (s) Fluidized bed units with an integrated fluidized bed heat exchanger designed to burn coal/solid fossil fuel.
- (t) Units designed to burn heavy liquid fuel.
- (u) Units designed to burn light liquid fuel.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7163, Jan. 31, 2013]

### § 63.7500 What emission limitations, work practice standards, and operating limits must I meet?

(a) You must meet the requirements in <u>paragraphs (a)(1)</u> through (3) of this section, except as provided in <u>paragraphs</u> (b) through (c) of this section. You must meet these requirements at all times the affected unit is operating, except as provided in <u>paragraph (f)</u> of this section.

(1) You must meet each emission limit and work practice standard in Tables 1 through 3 and 11 through 15 to this subpart that applies to your boiler or process heater, for each boiler or process heater at your source, except as provided under  $\S$  <u>63.7522</u>. The output-based emission limits, in units of pounds per million Btu of steam output, in Table 1 or 2 to this subpart are an alternative applicable only to boilers and process heaters that generate either steam, cogenerate steam with electricity, or both. The output-based emission limits, in units of pounds per megawatt-hour, in Table 1 or 2 to this subpart are an alternative applicable only to boilers that generate only electricity. Boilers that perform multiple functions (cogeneration and

#### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

electricity generation) or supply steam to common headers would calculate a total steam energy output using Equation 1 of § <u>63.7575</u> to demonstrate compliance with the output-based emission limits, in units of pounds per million Btu of steam output, in Table 1 or 2 to this subpart. If you operate a new boiler or process heater, you can choose to comply with alternative limits as discussed in <u>paragraphs (a)(1)(i)</u> through (iv) of this section, but on or after October 6, 2025, you must comply with the emission limits in Table 1 to this subpart. If you operate an existing boiler or process heater, you can choose to comply with alternative limits as discussed in <u>paragraphs (a)(1)(i)</u> of this section, but on or after October 6, 2025 you must comply with alternative limits as discussed in <u>paragraph (a)(1)(v)</u> of this section, but on or after October 6, 2025 you must comply with the emission limits in Table 2 to this subpart.

(i) If your boiler or process heater commenced construction or reconstruction after June 4, 2010, and before May 20, 2011, you may comply with the emission limits in Table 11 or 14 to this subpart until January 31, 2016.

(ii) If your boiler or process heater commenced construction or reconstruction on or after May 20, 2011, and before December 23, 2011, you may comply with the emission limits in Table 12 or 14 to this subpart until January 31, 2016.

(iii) If your boiler or process heater commenced construction or reconstruction on or after December 23, 2011, and before April 1, 2013, you may comply with the emission limits in Table 13 or 14 to this subpart until January 31, 2016.

(iv) If you operate a new boiler or process heater, you must comply with either the emission limits in Table 1 to this subpart or the emission limits in Table 14 to this subpart until you must comply with the emission limits in Table 1.

(v) If you operate an existing boiler or process heater, you must comply with either the emission limits in Table 2 to this subpart or the emission limits in Table 15 to this subpart until you must comply with the emission limits in Table 2.

(2) You must meet each operating limit in Table 4 to this subpart that applies to your boiler or process heater. If you use a control device or combination of control devices not covered in Table 4 to this subpart, or you wish to establish and monitor an alternative operating limit or an alternative monitoring parameter, you must apply to the EPA Administrator for approval of alternative monitoring under  $\frac{63.8(f)}{10}$ .

(3) At all times, you must operate and maintain any affected source (as defined in <u>§ 63.7490</u>), including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator that may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.

(b) As provided in § 63.6(g), EPA may approve use of an alternative to the work practice standards in this section.

(c) Limited-use boilers and process heaters must complete a tune-up every 5 years as specified in  $\S$  63.7540. They are not subject to the emission limits in Tables 1 and 2 or Tables 11 through 15 to this subpart, the annual tune-up, or the energy assessment requirements in Table 3 to this subpart, or the operating limits in Table 4 to this subpart.

(d) Boilers and process heaters with a heat input capacity of less than or equal to 5 million Btu per hour in the units designed to burn gas 2 (other) fuels subcategory or units designed to burn light liquid fuels subcategory must complete a tune-up every 5 years as specified in  $\frac{\$ 63.7540}{10}$ .

(e) Boilers and process heaters in the units designed to burn gas 1 fuels subcategory with a heat input capacity of less than or equal to 5 million Btu per hour must complete a tune-up every 5 years as specified in  $\frac{63.7540}{10}$ . Boilers and process heaters in the units designed to burn gas 1 fuels subcategory with a heat input capacity greater than 5 million Btu per hour and less than 10 million Btu per hour must complete a tune-up every 2 years as specified in  $\frac{63.7540}{10}$ . Boilers and process heaters in the units designed to burn gas 1 fuels subcategory are not subject to the emission limits in Tables 1 and 2 or Tables 11 through 15 to this subpart, or the operating limits in Table 4 to this subpart.

(f) These standards apply at all times the affected unit is operating, except during periods of startup and shutdown during which time you must comply only with items 5 and 6 of Table 3 to this subpart.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7163</u>, Jan. 31, 2013; <u>80 FR 72807</u>, Nov. 20, 2015; <u>87 FR 60840</u>, Oct. 6, 2022]

### § 63.7501 [Reserved]

**General Compliance Requirements** 

§ 63.7505 What are my general requirements for complying with this subpart?
(a) You must be in compliance with the emission limits, work practice standards, and operating limits in this subpart. These emission and operating limits apply to you at all times the affected unit is operating except for the periods noted in  $\S$  <u>63.7500(f)</u>.

(b) [Reserved]

(c) You must demonstrate compliance with all applicable emission limits using performance stack testing, fuel analysis, or continuous monitoring systems (CMS), including a continuous emission monitoring system (CEMS), continuous opacity monitoring system (COMS), continuous parameter monitoring system (CPMS), or particulate matter continuous parameter monitoring system (PM CPMS), where applicable. You may demonstrate compliance with the applicable emission limit for hydrogen chloride (HCl), mercury, or total selected metals (TSM) using fuel analysis if the emission rate calculated according to § 63.7530(c) is less than the applicable emission limit. For gaseous fuels, you may not use fuel analyses to comply with the TSM alternative standard or the HCl standard. Otherwise, you must demonstrate compliance for HCl, mercury, or TSM using performance stack testing, if subject to an applicable emission limit listed in Table 1 or 2 or Tables 11 through 15 to this subpart.

(d) If you demonstrate compliance with any applicable emission limit through performance testing and subsequent compliance with operating limits through the use of CPMS, or with a CEMS or COMS, you must develop a site-specific monitoring plan according to the requirements in <u>paragraphs (d)(1)</u> through (4) of this section for the use of any CEMS, COMS, or CPMS. This requirement also applies to you if you petition the EPA Administrator for alternative monitoring parameters under  $\frac{\& 63.8(f)}{1.5}$ .

(1) For each CMS required in this section (including CEMS, COMS, or CPMS), you must develop, and submit to the Administrator for approval upon request, a site-specific monitoring plan that addresses design, data collection, and the quality assurance and quality control elements outlined in § 63.8(d) and the elements described in paragraphs (d)(1)(i) through (iii) of this section. You must submit this site-specific monitoring plan, if requested, at least 60 days before your initial performance evaluation of your CMS. This requirement to develop and submit a site specific monitoring plan does not apply to affected sources with existing CEMS or COMS operated according to the performance specifications under appendix B to part 60 of this chapter and that meet the requirements of § 63.7525. Using the process described in § 63.8(f)(4), you may request approval of alternative monitoring system quality assurance and quality control procedures in place of those specified in this paragraph and, if approved, include the alternatives in your site-specific monitoring plan.

(i) Installation of the CMS sampling probe or other interface at a measurement location relative to each affected process unit such that the measurement is representative of control of the exhaust emissions (e.g., on or downstream of the last control device);

(ii) Performance and equipment specifications for the sample interface, the pollutant concentration or parametric signal analyzer, and the data collection and reduction systems; and

(iii) Performance evaluation procedures and acceptance criteria (e.g., calibrations, accuracy audits, analytical drift).

(2) In your site-specific monitoring plan, you must also address paragraphs (d)(2)(i) through (iii) of this section.

(i) Ongoing operation and maintenance procedures in accordance with the general requirements of  $\frac{63.8(c)(1)(ii)}{(c)(3)}$ , and  $\frac{(c)(4)(ii)}{(c)(3)}$ ;

(ii) Ongoing data quality assurance procedures in accordance with the general requirements of § 63.8(d); and

(iii) Ongoing recordkeeping and reporting procedures in accordance with the general requirements of  $\frac{63.10(c)}{c}$  (as applicable in Table 10 to this subpart), (e)(1), and (e)(2)(i).

(3) You must conduct a performance evaluation of each CMS in accordance with your site-specific monitoring plan.

(4) You must operate and maintain the CMS in continuous operation according to the site-specific monitoring plan.

(e) If you have an applicable emission limit, and you choose to comply using definition (2) of "startup" in § 63.7575, you must develop and implement a written startup and shutdown plan (SSP) according to the requirements in Table 3 to this subpart. The SSP must be maintained onsite and available upon request for public inspection.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7164</u>, Jan. 31, 2013; <u>80 FR 72807</u>, Nov. 20, 2015; <u>87 FR 60841</u>, Oct. 6, 2022]

# Testing, Fuel Analyses, and Initial Compliance Requirements

### § 63.7510 What are my initial compliance requirements and by what date must I conduct them?

(a) For each boiler or process heater that is required or that you elect to demonstrate compliance with any of the applicable emission limits in Table 1 or 2 or Tables 11 through 15 to this subpart through performance (stack) testing, your initial compliance requirements include all the following:

(1) Conduct performance tests according to  $\S 63.7520$  and Table 5 to this subpart.

(2) Conduct a fuel analysis for each type of fuel burned in your boiler or process heater according to  $\frac{63.7521}{100}$  and Table 6 to this subpart, except as specified in paragraphs (a)(2)(i) through (iii) of this section.

(i) For each boiler or process heater that burns a single type of fuel, you are not required to conduct a fuel analysis for each type of fuel burned in your boiler or process heater according to  $\S$  63.7521 and Table 6 to this subpart. For purposes of this subpart, units that use a supplemental fuel only for startup, unit shutdown, and transient flame stability purposes still qualify as units that burn a single type of fuel, and the supplemental fuel is not subject to the fuel analysis requirements under  $\S$  63.7521 and Table 6 to this subpart.

(ii) When natural gas, refinery gas, or other gas 1 fuels are co-fired with other fuels, you are not required to conduct a fuel analysis of those Gas 1 fuels according to  $\frac{63.7521}{1}$  and Table 6 to this subpart. If gaseous fuels other than natural gas, refinery gas, or other gas 1 fuels are co-fired with other fuels and those non-Gas 1 gaseous fuels are subject to another subpart of this part, part 60, part 61, or part 65, you are not required to conduct a fuel analysis of those non-Gas 1 fuels according to  $\frac{63.7521}{2}$  and Table 6 to this subpart. The subject to another subpart of this part, part 60, part 61, or part 65, you are not required to conduct a fuel analysis of those non-Gas 1 fuels according to  $\frac{63.7521}{2}$  and Table 6 to this subpart.

(iii) You are not required to conduct a chlorine fuel analysis for any gaseous fuels. You must conduct a fuel analysis for mercury on gaseous fuels unless the fuel is exempted in <u>paragraphs (a)(2)(i)</u> and <u>(ii)</u> of this section.

(3) Establish operating limits according to  $\S 63.7530$  and Table 7 to this subpart.

(4) Conduct CMS performance evaluations according to  $\frac{\& 63.7525}{\& 63.7525}$ .

(b) For each boiler or process heater that you elect to demonstrate compliance with the applicable emission limits in Table 1 or 2 or Tables 11 through 15 to this subpart for HCl, mercury, or TSM through fuel analysis, your initial compliance requirement is to conduct a fuel analysis for each type of fuel burned in your boiler or process heater according to  $\frac{5}{5}$  <u>63.7521</u> and Table 6 to this subpart and establish operating limits according to  $\frac{5}{5}$  <u>63.7530</u> and Table 8 to this subpart. The fuels described in <u>paragraphs (a)(2)(i)</u> and (ii) of this section are exempt from these fuel analysis and operating limit requirements. The fuels described in <u>paragraph (a)(2)(ii)</u> of this section are exempt from the chloride fuel analysis and operating limit requirements. Boilers and process heaters that use a CEMS for mercury or HCl are exempt from the performance testing and operating limit requirements specified in <u>paragraph (a)</u> of this section for the HAP for which CEMS are used.

(c) If your boiler or process heater is subject to a carbon monoxide (CO) limit, your initial compliance demonstration for CO is to conduct a performance test for CO according to Table 5 to this subpart or conduct a performance evaluation of your continuous CO monitor, if applicable, according to  $\frac{63.7525(a)}{2}$ . Boilers and process heaters that use a CO CEMS to comply with the applicable alternative CO CEMS emission standard listed in Table 1 or 2 or Tables 11 through 15 to this subpart, as specified in  $\frac{63.7525(a)}{2}$ , are exempt from the initial CO performance testing and oxygen concentration operating limit requirements specified in paragraph (a) of this section.

(d) If your boiler or process heater is subject to a PM limit, your initial compliance demonstration for PM is to conduct a performance test in accordance with  $\frac{63.7520}{2}$  and Table 5 to this subpart.

(e) For existing affected sources (as defined in § 63.7490), you must complete the initial compliance demonstrations, as specified in paragraphs (a) through (d) of this section, no later than 180 days after the compliance date that is specified for your source in § 63.7495 and according to the applicable provisions in § 63.7(a)(2) as cited in Table 10 to this subpart, except as specified in paragraph (j) of this section. You must complete an initial tune-up by following the procedures described in § 63.7540(a)(10)(i) through (vi) no later than the compliance date specified in § 63.7495, except as specified in paragraph (j) of this section. You must complete the one-time energy assessment specified in Table 3 to this subpart no later than the compliance date specified in Table 3 to this subpart no later than the compliance date specified in § 63.7495.

(f) For new or reconstructed affected sources (as defined in  $\frac{63.7490}{30}$ ), you must complete the initial compliance demonstration with the emission limits no later than July 30, 2013, or within 180 days after startup of the source, whichever is later.

(1) If you are demonstrating compliance with an emission limit in Tables 11 through 13 to this subpart that is less stringent than the applicable emission limit in Table 14 to this subpart, you must demonstrate compliance with the applicable emission limit in Table 14 no later than July 29, 2016.

(2) If you are demonstrating compliance with an emission limit in Table 14 to this subpart that is less stringent than the applicable emission limit in Table 1 to this subpart, you must demonstrate compliance with the applicable emission limit in Table 1 no later than October 6, 2025.

(g) For new or reconstructed affected sources (as defined in  $\S$  63.7490), you must demonstrate initial compliance with the applicable work practice standards in Table 3 to this subpart within the applicable annual, biennial, or 5-year schedule as specified in  $\S$  63.7515(d) following the initial compliance date specified in  $\S$  63.7495(a). Thereafter, you are required to complete the applicable annual, biennial, or 5-year tune-up as specified in  $\S$  63.7515(d).

(h) For affected sources (as defined in  $\S$  63.7490) that ceased burning solid waste consistent with  $\S$  63.7495(e) and for which the initial compliance date has passed, you must demonstrate compliance within 60 days of the effective date of the waste-to-fuel switch. If you have not conducted your compliance demonstration for this subpart within the previous 12 months, you must complete all compliance demonstrations for this subpart before you commence or recommence combustion of solid waste.

(i) For an existing EGU that becomes subject after January 31, 2016, you must demonstrate compliance within 180 days after becoming an affected source.

(j) For existing affected sources (as defined in  $\S$  63.7490) that have not operated between the effective date of the rule and the compliance date that is specified for your source in  $\S$  63.7495, you must complete the initial compliance demonstration, if subject to the emission limits in Table 2 or 14 to this subpart, as applicable, as specified in paragraphs (a) through (d) of this section, no later than 180 days after the re-start of the affected source and according to the applicable provisions in  $\S$  63.7(a)(2) as cited in Table 10 to this subpart. You must complete an initial tune-up by following the procedures described in  $\S$  63.7540(a)(10)(i) through (vi) no later than 30 days after the re-start of the affected source and, if applicable, complete the one-time energy assessment specified in Table 3 to this subpart, no later than the compliance date specified in  $\S$  63.7495.

(k) For affected sources, as defined in  $\S$  63.7490, that switch subcategories consistent with  $\S$  63.7545(h) after the initial compliance date, you must demonstrate compliance within 60 days of the effective date of the switch, unless you had previously conducted your compliance demonstration for this subcategory within the previous 12 months.

[78 FR 7164, Jan. 31, 2013, as amended at 80 FR 72808, Nov. 20, 2015; 87 FR 60841, Oct. 6, 2022]

#### § 63.7515 When must I conduct subsequent performance tests, fuel analyses, or tune-ups?

(a) You must conduct all applicable performance tests according to  $\S 63.7520$  on an annual basis, except as specified in <u>paragraphs (b)</u> through (c), (g), and (h) of this section. Annual performance tests must be completed no more than 13 months after the previous performance test, except as specified in <u>paragraphs (b)</u> through (c), (g), and (h) of this section.

(b) If your performance tests for a given pollutant for at least 2 consecutive years show that your emissions are at or below 75 percent of the emission limit (or, in limited instances as specified in Tables 1 and 2 or 11 through 15 to this subpart, at or below the emission limit) for the pollutant, and if there are no changes in the operation of the individual boiler or process heater or air pollution control equipment that could increase emissions, you may choose to conduct performance tests for the pollutant every third year. Each such performance test must be conducted no more than 37 months after the previous performance tests annually. The requirement to test at maximum chloride input level is waived unless the stack test is conducted for HCl. The requirement to test at maximum mercury input level is waived unless the stack test is conducted for TSM.

(c) If a performance test shows emissions exceeded the emission limit or 75 percent of the emission limit (as specified in Tables 1 and 2 or 11 through 15 to this subpart) for a pollutant, you must conduct annual performance tests for that pollutant until all performance tests over a consecutive 2-year period meet the required level (at or below 75 percent of the emission limit, as specified in Tables 1 and 2 or 11 through 15).

(d) If you are required to meet an applicable tune-up work practice standard, you must conduct an annual, biennial, or 5-year performance tune-up according to  $\frac{63.7540(a)(10)}{(11)}$ , or (12), respectively. Each annual tune-up specified in  $\frac{63.7540(a)(10)}{(11)}$  must be no more than 13 months after the previous tune-up. Each biennial tune-up specified in  $\frac{63.7540(a)(11)}{(11)}$  must be conducted no more than 25 months after the previous tune-up. Each 5-year tune-up specified in  $\frac{8}{(11)}$ 

63.7540(a)(12) must be conducted no more than 61 months after the previous tune-up. For a new or reconstructed affected source (as defined in § 63.7490), the first annual, biennial, or 5-year tune-up must be no later than 13 months, 25 months, or 61 months, respectively, after April 1, 2013 or the initial startup of the new or reconstructed affected source, whichever is later.

(e) If you demonstrate compliance with the mercury, HCl, or TSM based on fuel analysis, you must conduct a monthly fuel analysis according to  $\S$  63.7521 for each type of fuel burned that is subject to an emission limit in Table 1 or 2 or Tables 11 through 15 to this subpart. You may comply with this monthly requirement by completing the fuel analysis any time within the calendar month as long as the analysis is separated from the previous analysis by at least 14 calendar days. If you burn a new type of fuel, you must conduct a fuel analysis before burning the new type of fuel in your boiler or process heater. You must still meet all applicable continuous compliance requirements in  $\S$  63.7540. If each of 12 consecutive monthly fuel analyses demonstrates 75 percent or less of the compliance level, you may decrease the fuel analysis frequency to quarterly for that fuel. If any quarterly sample exceeds 75 percent of the compliance level or you begin burning a new type of fuel, you must return to monthly monitoring for that fuel, until 12 months of fuel analyses are again less than 75 percent of the compliance level. If sampling is conducted on 1 day per month, samples should be no less than 14 days apart, but if multiple samples are taken per month, the 14-day restriction does not apply.

(f) You must report the results of performance tests and the associated fuel analyses within 60 days after the completion of the performance tests. This report must also verify that the operating limits for each boiler or process heater have not changed or provide documentation of revised operating limits established according to  $\frac{63,7530}{50}$  and Table 7 to this subpart, as applicable. The reports for all subsequent performance tests must include all applicable information required in  $\frac{63,7550}{50}$ .

(g) For affected sources (as defined in § 63.7490) that have not operated since the previous compliance demonstration and more than 1 year has passed since the previous compliance demonstration, you must complete the subsequent compliance demonstration, if subject to the emission limits in Table 1 or 2 or Tables 11 through 15 to this subpart, no later than 180 days after the re-start of the affected source and according to the applicable provisions in § 63.7(a)(2) as cited in Table 10 to this subpart. You must complete a subsequent tune-up by following the procedures described in § 63.7540(a)(10)(i) through (vi) and the schedule described in § 63.7540(a)(13) for units that are not operating at the time of their scheduled tune-up.

(h) If your affected boiler or process heater is in the unit designed to burn light liquid subcategory and you combust ultra-low sulfur liquid fuel, you do not need to conduct further performance tests (stack tests or fuel analyses) if the pollutants measured during the initial compliance performance tests meet the emission limits in Tables 1 or 2 of this subpart providing you demonstrate ongoing compliance with the emissions limits by monitoring and recording the type of fuel combusted on a monthly basis. If you intend to use a fuel other than ultra-low sulfur liquid fuel, natural gas, refinery gas, or other gas 1 fuel, you must conduct new performance tests within 60 days of burning the new fuel type.

(i) If you operate a CO CEMS that meets the Performance Specifications outlined in  $\frac{63.7525(a)(3)}{63.7525(a)(3)}$  to demonstrate compliance with the applicable alternative CO CEMS emission standard listed in Table 1 or 2 or Tables 11 through 15 to this subpart, you are not required to conduct CO performance tests and are not subject to the oxygen concentration operating limit requirement specified in  $\frac{63.7510(a)}{2}$ .

[78 FR 7165, Jan. 31, 2013, as amended at 80 FR 72808, Nov. 20, 2015; 87 FR 60842, Oct. 6, 2022]

#### § 63.7520 What stack tests and procedures must I use?

(a) You must conduct all performance tests according to  $\S$  63.7(c), (d), (f), and (h). You must also develop a site-specific stack test plan according to the requirements in  $\S$  63.7(c). You shall conduct all performance tests under such conditions as the Administrator specifies to you based on the representative performance of each boiler or process heater for the period being tested. Upon request, you shall make available to the Administrator such records as may be necessary to determine the conditions of the performance tests.

(b) You must conduct each performance test according to the requirements in Table 5 to this subpart.

(c) You must conduct each performance test under the specific conditions listed in Tables 5 and 7 to this subpart. You must conduct performance tests at representative operating load conditions while burning the type of fuel or mixture of fuels that has the highest content of chlorine and mercury, and TSM if you are opting to comply with the TSM alternative standard and you must demonstrate initial compliance and establish your operating limits based on these performance tests. These requirements could result in the need to conduct more than one performance test. Following each performance test and until

the next performance test, you must comply with the operating limit for operating load conditions specified in Table 4 to this subpart.

(d) You must conduct a minimum of three separate test runs for each performance test required in this section, as specified in  $\frac{63.7(e)(3)}{10}$ . Each test run must comply with the minimum applicable sampling times or volumes specified in Tables 1 and 2 or 11 through 15 to this subpart.

(e) To determine compliance with the emission limits, you must use the F-Factor methodology and equations in sections 12.2 and 12.3 of EPA Method 19 at <u>40 CFR part 60, appendix A</u>-7 of this chapter to convert the measured particulate matter (PM) concentrations, the measured HCl concentrations, the measured mercury concentrations, and the measured TSM concentrations that result from the performance test to pounds per million Btu heat input emission rates.

(f) Except for a 30-day rolling average based on CEMS (or sorbent trap monitoring system) data, if measurement results for any pollutant are reported as below the method detection level (e.g., laboratory analytical results for one or more sample components are below the method defined analytical detection level), you must use the method detection level as the measured emissions level for that pollutant in calculating compliance. The measured result for a multiple component analysis (e.g., analytical values for multiple Method 29 fractions both for individual HAP metals and for total HAP metals) may include a combination of method detection level data and analytical data reported above the method detection level.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7166, Jan. 31, 2013; 87 FR 60842, Oct. 6, 2022]

#### § 63.7521 What fuel analyses, fuel specification, and procedures must I use?

(a) For solid and liquid fuels, you must conduct fuel analyses for chloride and mercury according to the procedures in <u>paragraphs (b)</u> through (c) of this section and Table 6 to this subpart, as applicable. For solid fuels and liquid fuels, you must also conduct fuel analyses for TSM if you are opting to comply with the TSM alternative standard. For gas 2 (other) fuels, you must conduct fuel analyses for mercury according to the procedures in <u>paragraphs (b)</u> through (c) of this section and Table 6 to this subpart, as applicable. For gaseous fuels, you may not use fuel analyses to comply with the TSM alternative standard or the HCl standard. For purposes of complying with this section, a fuel gas system that consists of multiple gaseous fuels collected and mixed with each other is considered a single fuel type and sampling and analysis is only required on the combined fuel gas system that will feed the boiler or process heater. Sampling and analysis of the individual gaseous streams prior to combining is not required. You are not required to conduct fuel analyses for fuels used for only startup, unit shutdown, and transient flame stability purposes. You are required to conduct fuel analyses only for fuels and units that are subject to emission limits for mercury, HCl, or TSM in Tables 1 and 2 or 11 through 15 to this subpart. Gaseous and liquid fuels are exempt from the sampling requirements in <u>paragraphs (c)</u> and (d) of this section.

(b) You must develop a site-specific fuel monitoring plan according to the following procedures and requirements in <u>paragraphs (b)(1)</u> and (2) of this section, if you are required to conduct fuel analyses as specified in  $\frac{63.7510}{5.000}$ .

(1) If you intend to use an alternative analytical method other than those required by Table 6 to this subpart, you must submit the fuel analysis plan to the Administrator for review and approval no later than 60 days before the date that you intend to conduct the initial compliance demonstration described in  $\frac{63.7510}{2}$ .

(2) You must include the information contained in paragraphs (b)(2)(i) through (vi) of this section in your fuel analysis plan.

(i) The identification of all fuel types anticipated to be burned in each boiler or process heater.

(ii) For each anticipated fuel type, the notification of whether you or a fuel supplier will be conducting the fuel analysis.

(iii) For each anticipated fuel type, a detailed description of the sample location and specific procedures to be used for collecting and preparing the composite samples if your procedures are different from <u>paragraph (c)</u> or <u>(d)</u> of this section. Samples should be collected at a location that most accurately represents the fuel type, where possible, at a point prior to mixing with other dissimilar fuel types.

(iv) For each anticipated fuel type, the analytical methods from Table 6, with the expected minimum detection levels, to be used for the measurement of chlorine or mercury.

(v) If you request to use an alternative analytical method other than those required by Table 6 to this subpart, you must also include a detailed description of the methods and procedures that you are proposing to use. Methods in Table 6 shall be used until the requested alternative is approved.

(vi) If you will be using fuel analysis from a fuel supplier in lieu of site-specific sampling and analysis, the fuel supplier must use the analytical methods required by Table 6 to this subpart.

(c) You must obtain composite fuel samples for each fuel type according to the procedures in paragraph (c)(1) or (2) of this section, or the methods listed in Table 6 to this subpart, or use an automated sampling mechanism that provides representative composite fuel samples for each fuel type that includes both coarse and fine material. At a minimum, for demonstrating initial compliance by fuel analysis, you must obtain three composite samples. For monthly fuel analyses, at a minimum, you must obtain a single composite sample. For fuel analyses as part of a performance stack test, as specified in § 63.7510(a), you must obtain a composite fuel sample during each performance test run.

(1) If sampling from a belt (or screw) feeder, collect fuel samples according to <u>paragraphs (c)(1)(i)</u> and <u>(ii)</u> of this section.

(i) Stop the belt and withdraw a 6-inch wide sample from the full cross-section of the stopped belt to obtain a minimum two pounds of sample. You must collect all the material (fines and coarse) in the full cross-section. You must transfer the sample to a clean plastic bag.

(ii) Each composite sample will consist of a minimum of three samples collected at approximately equal intervals during the testing period for sampling during performance stack testing.

(2) If sampling from a fuel pile or truck, you must collect fuel samples according to <u>paragraphs (c)(2)(i)</u> through (iii) of this section.

(i) For each composite sample, you must select a minimum of five sampling locations uniformly spaced over the surface of the pile.

(ii) At each sampling site, you must dig into the pile to a uniform depth of approximately 18 inches. You must insert a clean shovel into the hole and withdraw a sample, making sure that large pieces do not fall off during sampling; use the same shovel to collect all samples.

(iii) You must transfer all samples to a clean plastic bag for further processing.

(d) You must prepare each composite sample according to the procedures in <u>paragraphs (d)(1)</u> through (7) of this section.

(1) You must thoroughly mix and pour the entire composite sample over a clean plastic sheet.

(2) You must break large sample pieces (e.g., larger than 3 inches) into smaller sizes.

(3) You must make a pie shape with the entire composite sample and subdivide it into four equal parts.

(4) You must separate one of the quarter samples as the first subset.

(5) If this subset is too large for grinding, you must repeat the procedure in <u>paragraph (d)(3)</u> of this section with the quarter sample and obtain a one-quarter subset from this sample.

(6) You must grind the sample in a mill.

(7) You must use the procedure in <u>paragraph (d)(3)</u> of this section to obtain a one-quarter subsample for analysis. If the quarter sample is too large, subdivide it further using the same procedure.

(e) You must determine the concentration of pollutants in the fuel (mercury and/or chlorine and/or TSM) in units of pounds per million Btu of each composite sample for each fuel type according to the procedures in Table 6 to this subpart, for use in Equations 7, 8, and 9 of this subpart.

(f) To demonstrate that a gaseous fuel other than natural gas or refinery gas qualifies as an other gas 1 fuel, as defined in  $\S$  <u>63.7575</u>, you must conduct a fuel specification analyses for mercury according to the procedures in <u>paragraphs</u> (g) through (i) of this section and Table 6 to this subpart, as applicable, except as specified in <u>paragraph (f)(1)</u> through (<u>4</u>) of this section, or as an alternative where fuel specification analysis is not practical, you must measure mercury concentration in the exhaust gas when firing only the gaseous fuel to be demonstrated as an other gas 1 fuel in the boiler or process heater according to the procedures in Table 6 to this subpart.

(1) You are not required to conduct the fuel specification analyses in <u>paragraphs (g)</u> through (i) of this section for natural gas or refinery gas.

(2) You are not required to conduct the fuel specification analyses in <u>paragraphs (g)</u> through (i) of this section for gaseous fuels that are subject to another subpart of this part, part 60, part 61, or part 65.

(3) You are not required to conduct the fuel specification analyses in <u>paragraphs (g)</u> through (i) of this section on gaseous fuels for units that are complying with the limits for units designed to burn gas 2 (other) fuels.

(4) You are not required to conduct the fuel specification analyses in <u>paragraphs (g)</u> through <u>(i)</u> of this section for gas streams directly derived from natural gas at natural gas production sites or natural gas plants.

(g) You must develop a site-specific fuel analysis plan for other gas 1 fuels according to the following procedures and requirements in <u>paragraphs (g)(1)</u> and (2) of this section.

(1) If you intend to use an alternative analytical method other than those required by Table 6 to this subpart, you must submit the fuel analysis plan to the Administrator for review and approval no later than 60 days before the date that you intend to conduct the initial compliance demonstration described in  $\S$  63.7510.

(2) You must include the information contained in <u>paragraphs (g)(2)(i)</u> through <u>(vi)</u> of this section in your fuel analysis plan.

(i) The identification of all gaseous fuel types other than those exempted from fuel specification analysis under  $(\underline{f})(\underline{1})$  through  $(\underline{3})$  of this section anticipated to be burned in each boiler or process heater.

(ii) For each anticipated fuel type, the identification of whether you or a fuel supplier will be conducting the fuel specification analysis.

(iii) For each anticipated fuel type, a detailed description of the sample location and specific procedures to be used for collecting and preparing the samples if your procedures are different from the sampling methods contained in Table 6 to this subpart. Samples should be collected at a location that most accurately represents the fuel type, where possible, at a point prior to mixing with other dissimilar fuel types. If multiple boilers or process heaters are fueled by a common fuel stream it is permissible to conduct a single gas specification at the common point of gas distribution.

(iv) For each anticipated fuel type, the analytical methods from Table 6 to this subpart, with the expected minimum detection levels, to be used for the measurement of mercury.

(v) If you request to use an alternative analytical method other than those required by Table 6 to this subpart, you must also include a detailed description of the methods and procedures that you are proposing to use. Methods in Table 6 to this subpart shall be used until the requested alternative is approved.

(vi) If you will be using fuel analysis from a fuel supplier in lieu of site-specific sampling and analysis, the fuel supplier must use the analytical methods required by Table 6 to this subpart. When using a fuel supplier's fuel analysis, the owner or operator is not required to submit the information in  $\frac{63.7521(g)(2)(iii)}{100}$ .

(h) You must obtain a single fuel sample for each fuel type for fuel specification of gaseous fuels.

(i) You must determine the concentration in the fuel of mercury, in units of microgram per cubic meter, dry basis, of each sample for each other gas 1 fuel type according to the procedures in Table 6 to this subpart.

[78 FR 7167, Jan. 31, 2013, as amended at 80 FR 72808, Nov. 20, 2015; 87 FR 60842, Oct. 6, 2022]

#### § 63.7522 Can I use emissions averaging to comply with this subpart?

(a) As an alternative to meeting the requirements of <u>§ 63.7500</u> for PM (or TSM), HCl, or mercury on a boiler or process heater-specific basis, if you have more than one existing boiler or process heater in any subcategories located at your facility, you may demonstrate compliance by emissions averaging, if your averaged emissions are not more than 90 percent of the applicable emission limit, according to the procedures in this section. You may not include new boilers or process heaters in an emissions average.

(b) For a group of two or more existing boilers or process heaters in the same subcategory that each vent to a separate stack, you may average PM (or TSM), HCl, or mercury emissions among existing units to demonstrate compliance with the limits in Table 2 or 15 to this subpart as specified in <u>paragraphs (b)(1)</u> through (3) of this section, if you satisfy the requirements in <u>paragraphs (c)</u> through (g) of this section.

(1) You may average units using a CEMS or PM CPMS for demonstrating compliance.

(2) For mercury and HCl, averaging is allowed as follows:

- (i) You may average among units in any of the solid fuel subcategories.
- (ii) You may average among units in any of the liquid fuel subcategories.

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(iii) You may average among units in a subcategory of units designed to burn gas 2 (other) fuels.

(iv) You may not average across the units designed to burn liquid, units designed to burn solid fuel, and units designed to burn gas 2 (other) subcategories.

(3) For PM (or TSM), averaging is only allowed between units within each of the following subcategories and you may not average across subcategories:

(i) Units designed to burn coal/solid fossil fuel.

(ii) Stokers/sloped grate/other units designed to burn kiln dried biomass/bio-based solids.

(iii) Stokers/sloped grate/other units designed to burn wet biomass/bio-based solids.

(iv) Fluidized bed units designed to burn biomass/bio-based solid.

(v) Suspension burners designed to burn biomass/bio-based solid.

(vi) Dutch ovens/pile burners designed to burn biomass/bio-based solid.

(vii) Fuel Cells designed to burn biomass/bio-based solid.

(viii) Hybrid suspension/grate burners designed to burn wet biomass/bio-based solid.

(ix) Units designed to burn heavy liquid fuel.

(x) Units designed to burn light liquid fuel.

(xi) Units designed to burn liquid fuel that are non-continental units.

(xii) Units designed to burn gas 2 (other) gases.

(c) For each existing boiler or process heater in the averaging group, the emission rate achieved during the initial compliance test for the HAP being averaged must not exceed the emission level that was being achieved on April 1, 2013 or the control technology employed during the initial compliance test must not be less effective for the HAP being averaged than the control technology employed on April 1, 2013.

(d) The averaged emissions rate from the existing boilers and process heaters participating in the emissions averaging option must not exceed 90 percent of the limits in Table 2 or 15 to this subpart at all times the affected units are subject to numeric emission limits following the compliance date specified in  $\frac{\& 63.7495}{\& 63.7495}$ .

(e) You must demonstrate initial compliance according to <u>paragraph (e)(1)</u> or (2) of this section using the maximum rated heat input capacity or maximum steam generation capacity of each unit and the results of the initial performance tests or fuel analysis.

(1) You must use Equation 1a or 1b or 1c to this paragraph (e)(1) to demonstrate that the PM (or TSM), HCl, or mercury emissions from all existing units participating in the emissions averaging option for that pollutant do not exceed the emission limits in Table 2 or 15 to this subpart. Use Equation 1a if you are complying with the emission limits on a heat input basis, use Equation 1b if you are complying with the emission limits on a steam generation (output) basis, and use Equation 1c if you are complying with the emission limits on a electric generation (output) basis.

# Equation 1a to paragraph (e)(1)

AveWeightedEmissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times Hm) \div \sum_{i=1}^{n} Hm$$
 (Eq.1a)

Where:

AveWeightedEmissions = Average weighted emissions for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input.

Er = Emission rate (as determined during the initial compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by

performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in  $\frac{63.7530(c)}{c}$ .

Hm = Maximum rated heat input capacity of unit, i, in units of million Btu per hour.

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

Equation 1b to paragraph (e)(1)

AveWeightedEmissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times So) \div \sum_{i=1}^{n} So$$
 (Eq.1b)

Where:

*AveWeightedEmissions* = Average weighted emissions for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of steam output.

Er = Emission rate (as determined during the initial compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of steam output. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in <u>§ 63.7530(c)</u>. If you are taking credit for energy conservation measures from a unit according to <u>§ 63.7533</u>, use the adjusted emission level for that unit, Eadj, determined according to <u>§ 63.7533</u> for that unit.

So = Maximum steam output capacity of unit, i, in units of million Btu per hour, as defined in  $\S 63.7575$ .

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

Equation 1c to paragraph (e)(1)

AveWeightedEmissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times Eo) + \sum_{i=1}^{n} Eo$$
 (Eq.1c)

Where:

AveWeightedEmissions = Average weighted emissions for PM (or TSM), HCl, or mercury, in units of pounds per megawatt hour.

Er = Emission rate (as determined during the initial compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per megawatt hour. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in § 63.7530(c). If you are taking credit for energy conservation measures from a unit according to § 63.7533, use the adjusted emission level for that unit, Eadj, determined according to § 63.7533 for that unit.

Eo = Maximum electric generating output capacity of unit, i, in units of megawatt hour, as defined in <u>§ 63.7575</u>.

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

(2) If you are not capable of determining the maximum rated heat input capacity of one or more boilers that generate steam, you may use Equation 2 to this paragraph (e)(2) as an alternative to using Equation 1a of paragraph (e)(1) of this section to demonstrate that the PM (or TSM), HCl, or mercury emissions from all existing units participating in the emissions averaging option do not exceed the emission limits for that pollutant in Table 2 or 15 to this subpart that are in pounds per million Btu of heat input.

# Equation 2 to paragraph (e)(2)

Ave Weighted Emissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times Sm \times Cfi) + \sum_{i=1}^{n} (Sm \times Cfi)$$
 (Eq. 2)

Where:

*AveWeightedEmissions* = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in <u>§ 63.7530(c)</u>.

Sm = Maximum steam generation capacity by unit, i, in units of pounds per hour.

Cfi = Conversion factor, calculated from the most recent compliance test, in units of million Btu of heat input per pounds of steam generated for unit, i.

1.1 = Required discount factor.

(f) After the initial compliance demonstration described in <u>paragraph (e)</u> of this section, you must demonstrate compliance on a monthly basis determined at the end of every month (12 times per year) according to <u>paragraphs (f)(1)</u> through (3) of this section. The first monthly period begins on the compliance date specified in § 63.7495. If the affected source elects to collect monthly data for up the 11 months preceding the first monthly period, these additional data points can be used to compute the 12-month rolling average in <u>paragraph (f)(3)</u> of this section.

(1) For each calendar month, you must use Equation 3a or 3b or 3c of this section to calculate the average weighted emission rate for that month. Use Equation 3a and the actual heat input for the month for each existing unit participating in the emissions averaging option if you are complying with emission limits on a heat input basis. Use Equation 3b and the actual steam generation for the month if you are complying with the emission limits on a steam generation (output) basis. Use Equation 3c and the actual electrical generation for the month if you are complying with the emission limits on a steam generation limits on an electrical generation (output) basis.

AveWeightedEmissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times Hb) \div \sum_{i=1}^{n} Hb$$
 (Eq. 3a)

Where:

AveWeightedEmissions = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input, for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart.

Hb = The heat input for that calendar month to unit, i, in units of million Btu.

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

AveWeightedEmissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times So) \div \sum_{i=1}^{n} So$$
 (Eq. 3b)

Where:

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AveWeightedEmissions = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of steam output, for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of steam output. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart. If you are taking credit for energy conservation measures from a unit according to  $\frac{63.7533}{5.000}$ , use the adjusted emission level for that unit,  $E_{adj}$ , determined according to  $\frac{63.7533}{5.0000}$  for that unit.

So = The steam output for that calendar month from unit, i, in units of million Btu, as defined in  $\S$  63.7575.

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

AveWeightedEmissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times Eo) \div \sum_{i=1}^{n} Eo$$
 (Eq. 3c)

Where:

AveWeightedEmissions = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per megawatt hour, for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per megawatt hour. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart. If you are taking credit for energy conservation measures from a unit according to  $\frac{63.7533}{5.000}$ , use the adjusted emission level for that unit,  $E_{adj}$ , determined according to  $\frac{63.7533}{5.0000}$  for that unit.

Eo = The electric generating output for that calendar month from unit, i, in units of megawatt hour, as defined in  $\frac{63.7575}{5}$ .

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

(2) If you are not capable of monitoring heat input, you may use Equation 4 of this section as an alternative to using Equation 3a of this section to calculate the average weighted emission rate using the actual steam generation from the boilers participating in the emissions averaging option.

AveWeightedEmissions = 
$$1.1 \times \sum_{i=1}^{n} (Er \times Sa \times Cfi) \div \sum_{i=1}^{n} (Sa \times Cfi)$$
 (Eq. 4)

Where:

AveWeightedEmissions = average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart.

Sa = Actual steam generation for that calendar month by boiler, i, in units of pounds.

Cfi = Conversion factor, as calculated during the most recent compliance test, in units of million Btu of heat input per pounds of steam generated for boiler, i.

1.1 = Required discount factor.

(3) Until 12 monthly weighted average emission rates have been accumulated, calculate and report only the average weighted emission rate determined under <u>paragraph (f)(1)</u> or (2) of this section for each calendar month. After 12 monthly weighted average emission rates have been accumulated, for each subsequent calendar month, use Equation 5 of this section to

calculate the 12-month rolling average of the monthly weighted average emission rates for the current calendar month and the previous 11 calendar months.

$$Eavg = \sum_{i=1}^{n} ERi \div 12 \quad (Eq. 5)$$

Where:

Eavg = 12-month rolling average emission rate, (pounds per million Btu heat input)

ERi = Monthly weighted average, for calendar month "i" (pounds per million Btu heat input), as calculated by <u>paragraph</u> (<u>f)(1)</u> or (<u>2</u>) of this section.

(g) You must develop, and submit upon request to the applicable Administrator for review and approval, an implementation plan for emission averaging according to the following procedures and requirements in <u>paragraphs (g)(1)</u> through (4) of this section.

(1) If requested, you must submit the implementation plan no later than 180 days before the date that the facility intends to demonstrate compliance using the emission averaging option.

(2) You must include the information contained in <u>paragraphs (g)(2)(i)</u> through <u>(vii)</u> of this section in your implementation plan for all emission sources included in an emissions average:

(i) The identification of all existing boilers and process heaters in the averaging group, including for each either the applicable HAP emission level or the control technology installed as of January 31, 2013 and the date on which you are requesting emission averaging to commence;

(ii) The process parameter (heat input or steam generated) that will be monitored for each averaging group;

(iii) The specific control technology or pollution prevention measure to be used for each emission boiler or process heater in the averaging group and the date of its installation or application. If the pollution prevention measure reduces or eliminates emissions from multiple boilers or process heaters, the owner or operator must identify each boiler or process heater;

(iv) The test plan for the measurement of PM (or TSM), HCl, or mercury emissions in accordance with the requirements in  $\S$  63.7520;

(v) The operating parameters to be monitored for each control system or device consistent with  $\frac{63.7500}{100}$  and Table 4, and a description of how the operating limits will be determined;

(vi) If you request to monitor an alternative operating parameter pursuant to § 63.7525, you must also include:

(A) A description of the parameter(s) to be monitored and an explanation of the criteria used to select the parameter(s); and

(B) A description of the methods and procedures that will be used to demonstrate that the parameter indicates proper operation of the control device; the frequency and content of monitoring, reporting, and recordkeeping requirements; and a demonstration, to the satisfaction of the Administrator, that the proposed monitoring frequency is sufficient to represent control device operating conditions; and

(vii) A demonstration that compliance with each of the applicable emission limit(s) will be achieved under representative operating load conditions. Following each compliance demonstration and until the next compliance demonstration, you must comply with the operating limit for operating load conditions specified in Table 4 to this subpart.

(3) If submitted upon request, the Administrator shall review and approve or disapprove the plan according to the following criteria:

(i) Whether the content of the plan includes all of the information specified in paragraph (g)(2) of this section; and

(ii) Whether the plan presents sufficient information to determine that compliance will be achieved and maintained.

(4) The applicable Administrator shall not approve an emission averaging implementation plan containing any of the following provisions:

(i) Any averaging between emissions of differing pollutants or between differing sources; or

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(ii) The inclusion of any emission source other than an existing unit in the same subcategories.

(h) For a group of two or more existing affected units, each of which vents through a single common stack, you may average PM (or TSM), HCl, or mercury emissions to demonstrate compliance with the limits for that pollutant in Table 2 or 15 to this subpart if you satisfy the requirements in <u>paragraph (i)</u> or (j) of this section.

(i) For a group of two or more existing units in the same subcategory, each of which vents through a common emissions control system to a common stack, that does not receive emissions from units in other subcategories or categories, you may treat such averaging group as a single existing unit for purposes of this subpart and comply with the requirements of this subpart as if the group were a single unit.

(j) For all other groups of units subject to the common stack requirements of <u>paragraph (h)</u> of this section, including situations where the exhaust of affected units are each individually controlled and then sent to a common stack, the owner or operator may elect to:

(1) Conduct performance tests according to procedures specified in  $\S 63.7520$  in the common stack if affected units from other subcategories vent to the common stack. The emission limits that the group must comply with are determined by the use of Equation 6 to this paragraph (j)(1).

# Equation 6 to paragraph (j)(1)

$$En = \sum_{i=1}^{n} (ELi \times Hi) + \sum_{i=1}^{n} Hi$$
 (Eq. 6)

Where:

*En* = HAP emission limit, pounds per million British thermal units (lb/MMBtu) or parts per million (ppm).

*ELi* = Appropriate emission limit from Table 2 or 15 to this subpart for unit i, in units of lb/MMBtu or ppm.

Hi = Heat input from unit i, MMBtu.

(2) Conduct performance tests according to procedures specified in  $\S$  <u>63.7520</u> in the common stack. If affected units and non-affected units vent to the common stack, the non-affected units must be shut down or vented to a different stack during the performance test unless the facility determines to demonstrate compliance with the non-affected units venting to the stack; and

(3) Meet the applicable operating limit specified in  $\frac{63.7540}{2}$  and Table 8 to this subpart for each emissions control system (except that, if each unit venting to the common stack has an applicable opacity operating limit, then a single continuous opacity monitoring system may be located in the common stack instead of in each duct to the common stack).

(k) The common stack of a group of two or more existing boilers or process heaters in the same subcategories subject to <u>paragraph (h)</u> of this section may be treated as a separate stack for purposes of <u>paragraph (b)</u> of this section and included in an emissions averaging group subject to <u>paragraph (b)</u> of this section.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7168</u>, Jan. 31, 2013; <u>80 FR 72809</u>, Nov. 20, 2015; <u>87 FR 60843</u>, Oct. 6, 2022]

# § 63.7525 What are my monitoring, installation, operation, and maintenance requirements?

(a) If your boiler or process heater is subject to a CO emission limit in Table 1 or 2 or Tables 11 through 15 to this subpart, you must install, operate, and maintain an oxygen analyzer system, as defined in § 63.7575, or install, certify, operate and maintain continuous emission monitoring systems for CO and oxygen ( $O_2$ ) (or carbon dioxide ( $CO_2$ )) according to the procedures in paragraphs (a)(1) through (6) of this section.

(1) Install the CO CEMS including an O<sub>2</sub> (or CO<sub>2</sub>) analyzer by the compliance date specified in <u>§ 63.7495</u>. The CO and O<sub>2</sub> (or CO<sub>2</sub>) levels shall be monitored at the same location at the outlet of the boiler or process heater. An owner or operator may determine compliance with the CO emissions limit using a CO<sub>2</sub> analyzer as the diluent monitor. If a CO<sub>2</sub> analyzer is used as the diluent monitor, EPA Method 19 F-factors in <u>40 CFR part 60, appendix A</u>-7, for the fuel type(s) being burned in the unit and EPA Method 19 equations in <u>40 CFR part 60, appendix A</u>-7, must be used to calculate the emissions corrected to

3 percent  $O_2$  using the measured  $CO_2$  percentage, and must also take into account that the 3 percent oxygen correction is to be done on a dry basis. The equations used to calculate the emissions, must also account for any  $CO_2$  being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. The methodology used to calculate the CO emissions and the methodology used to account for any  $CO_2$  being added to, or removed from the emissions gas stream shall be detailed and approved in the site-specific monitoring plan developed according to § 63.7505(d).

(2) To demonstrate compliance with the applicable alternative CO CEMS emission standard listed in Table 1 or 2 or Tables 11 through 15 to this subpart, you must install, certify, operate, and maintain a CO CEMS and an oxygen analyzer according to the applicable procedures under Performance Specification 4, 4A, or 4B at <u>40 CFR part 60, appendix B; part 75 of this chapter</u> (if an CO<sub>2</sub> analyzer is used); the site-specific monitoring plan developed according to <u>§ 63.7505(d)</u>; and the requirements in <u>§ 63.7540(a)(8)</u> and this <u>paragraph (a)</u>. Any boiler or process heater that has a CO CEMS that is compliant with Performance Specification 4, 4A, or 4B at <u>40 CFR part 60, appendix B</u>, a site-specific monitoring plan developed according to <u>§ 63.7505(d)</u>, and the requirements in <u>§ 63.7505(d)</u>, and the requirements in <u>§ 63.7540(a)(8)</u> and this <u>paragraph (a)</u> must use the CO CEMS to comply with the applicable alternative CO CEMS emission standard listed in Table 1 or 2 or Tables 11 through 15 to this subpart.

(i) You must conduct a performance evaluation of each CO CEMS according to the requirements in  $\frac{63.8(e)}{2}$  and according to Performance Specification 4, 4A, or 4B at  $\frac{40 \text{ CFR part } 60, \text{ appendix B}}{2}$ .

(ii) During each relative accuracy test run of the CO CEMS, you must collect emission data for CO concurrently using both the CO CEMS and Method 10, 10A, or 10B at <u>40 CFR part 60, appendix A</u>-4. The relative accuracy testing must be conducted at representative operating conditions.

(iii) You must follow the quality assurance procedures (e.g., quarterly accuracy determinations and daily calibration drift tests) of Procedure 1 of appendix F to part 60. The measurement span value of the CO CEMS must be two times the applicable CO emission limit, expressed as a concentration.

(iv) Any CO CEMS that does not comply with this <u>paragraph (a)</u> cannot be used to meet any requirement in this subpart to demonstrate compliance with a CO emission limit listed in Table 1 or 2 or Tables 11 through 15 to this subpart.

(v) For a new unit, complete the initial performance evaluation no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, complete the initial performance evaluation no later than July 29, 2016.

(vi) When CO<sub>2</sub> is used to correct CO emissions and CO<sub>2</sub> is measured on a wet basis, if needed, correct for moisture as follows: Install, operate, maintain, and quality assure a continuous moisture monitoring system for measuring and recording the moisture content of the flue gases, in order to correct the measured hourly volumetric flow rates for moisture when calculating CO concentrations. The following continuous moisture monitoring systems are acceptable: a continuous moisture sensor; an oxygen analyzer (or analyzers) capable of measuring O<sub>2</sub> both on a wet basis and on a dry basis; or a stack temperature sensor and a moisture look-up table, *i.e.*, a psychrometric chart (for saturated gas streams following wet scrubbers or other demonstrably saturated gas streams, only). The moisture monitoring system shall include as a component the automated data acquisition and handling system (DAHS) for recording and reporting both the raw data (e.g., hourly average wet-and dry-basis O<sub>2</sub> values) and the hourly average values of the stack gas moisture content derived from those data. When a moisture look-up table is used, the moisture monitoring system shall be represented as a single component, the certified DAHS, in the monitoring plan for the unit or common stack.

(3) Complete a minimum of one cycle of CO and oxygen (or  $CO_2$ ) CEMS operation (sampling, analyzing, and data recording) for each successive 15-minute period. Collect CO and oxygen (or  $CO_2$ ) data concurrently. Collect at least four CO and oxygen (or  $CO_2$ ) CEMS data values representing the four 15-minute periods in an hour, or at least two 15-minute data values during an hour when CEMS calibration, quality assurance, or maintenance activities are being performed.

(4) Reduce the CO CEMS data as specified in  $\S$  63.8(g)(2).

(5) Calculate one-hour arithmetic averages, corrected to 3 percent oxygen (or corrected to an  $CO_2$  percentage determined to be equivalent to 3 percent oxygen) from each hour of CO CEMS data in parts per million CO concentration. The one-hour arithmetic averages required shall be used to calculate the 30-day or 10-day rolling average emissions. Use Equation 19-19 in section 12.4.1 of Method 19 of 40 CFR part 60, appendix A-7 for calculating the average CO concentration from the hourly values.

(6) For purposes of collecting CO data, operate the CO CEMS as specified in  $\S$  <u>63.7535(b)</u>. You must use all the data collected during all periods in calculating data averages and assessing compliance, except that you must exclude certain data as specified in  $\S$  <u>63.7535(c)</u>. Periods when CO data are unavailable may constitute monitoring deviations as specified in  $\S$  <u>63.7535(d)</u>.

(7) Operate an oxygen trim system with the oxygen level set no lower than the lowest hourly average oxygen concentration measured during the most recent CO performance test as the operating limit for oxygen according to Table 7 to this subpart.

(b) If your boiler or process heater is in the unit designed to burn coal/solid fossil fuel subcategory or the unit designed to burn heavy liquid subcategory and has an average annual heat input rate greater than 250 MMBtu per hour from solid fossil fuel and/or heavy liquid, and you demonstrate compliance with the PM limit instead of the alternative TSM limit, you must install, maintain, and operate a PM CPMS monitoring emissions discharged to the atmosphere and record the output of the system as specified in paragraphs (b)(1) through (4) of this section. As an alternative to use of a PM CPMS to demonstrate compliance with the PM limit instead of the alternative to demonstrate compliance with the PM limit instead of the alternative TSM limit, you may choose to use a PM CEMS. If you choose to use a PM CEMS to demonstrate compliance with the PM limit instead of the alternative TSM limit, you must install, certify, maintain, and operate a PM CEMS monitoring emissions discharged to the atmosphere and record the output of the system as specified in paragraphs (b)(5) through (8) of this section. For other boilers or process heaters, you may elect to use a PM CPMS or PM CEMS operated in accordance with this section in lieu of using other CMS for monitoring PM compliance (*e.g.*, bag leak detectors, ESP secondary power, and PM scrubber pressure). Owners of boilers and process heaters who elect to comply with the alternative TSM limit are not required to install a PM CPMS.

(1) Install, operate, and maintain your PM CPMS according to the procedures in your approved site-specific monitoring plan developed in accordance with § 63.7505(d), the requirements in § 63.7540(a)(9), and paragraphs (b)(1)(i) through (iii) of this section.

(i) The operating principle of the PM CPMS must be based on in-stack or extractive light scatter, light scintillation, beta attenuation, or mass accumulation detection of PM in the exhaust gas or representative exhaust gas sample. The reportable measurement output from the PM CPMS must be expressed as milliamps.

(ii) The PM CPMS must have a cycle time (i.e., period required to complete sampling, measurement, and reporting for each measurement) no longer than 60 minutes.

(iii) The PM CPMS must have a documented detection limit of 0.5 milligram per actual cubic meter, or less.

(2) For a new unit, complete the initial performance evaluation no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, complete the initial performance evaluation no later than July 29, 2016.

(3) Collect PM CPMS hourly average output data for all boiler or process heater operating hours except as indicated in § 63.7535(a) through (d). Express the PM CPMS output as milliamps.

(4) Calculate the arithmetic 30-day rolling average of all of the hourly average PM CPMS output data collected during all boiler or process heater operating hours (milliamps).

(5) Install, certify, operate, and maintain your PM CEMS according to the procedures in your approved site-specific monitoring plan developed in accordance with  $\S$  63.7505(d), the requirements in  $\S$  63.7540(a)(9), and paragraphs (b)(5)(i) through (iv) of this section.

(ii) During each PM correlation testing run of the CEMS required by Performance Specification 11 at  $\frac{40 \text{ CFR part 60}}{40 \text{ CFR part 60}}$ , appendix B of this chapter, you shall collect PM and oxygen (or carbon dioxide) data concurrently (or within a 30-to 60-minute period) by both the CEMS and conducting performance tests using Method 5 at  $\frac{40 \text{ CFR part 60}}{40 \text{ CFR part 60}}$ , appendix A-3 or Method 17 at  $\frac{40 \text{ CFR part 60}}{40 \text{ CFR part 60}}$ , appendix A-6 of this chapter.

(iii) You shall perform quarterly accuracy determinations and daily calibration drift tests in accordance with Procedure 2 at <u>40 CFR part 60, appendix F</u> of this chapter. You must perform Relative Response Audits annually and perform Response Correlation Audits every 3 years.

(iv) Within 60 days after the date of completing each CEMS relative accuracy test audit or performance test conducted to demonstrate compliance with this subpart, you must submit the relative accuracy test audit data and performance test data to the EPA by successfully submitting the data electronically into the EPA's Central Data Exchange by using the Electronic Reporting Tool (see <u>http://www.epa.gov/ttn/chief/ert/erttool.html/</u>).

(6) For a new unit, complete the initial performance evaluation no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, complete the initial performance evaluation no later than July 29, 2016.

(7) Collect PM CEMS hourly average output data for all boiler or process heater operating hours except as indicated in  $\S$  <u>63.7535(a)</u> through (d).

(8) Calculate the arithmetic 30-day rolling average of all of the hourly average PM CEMS output data collected during all boiler or process heater operating hours.

(c) If you have an applicable opacity operating limit in this rule, and are not otherwise required or elect to install and operate a PM CPMS, PM CEMS, or a bag leak detection system, you must install, operate, certify and maintain each COMS according to the procedures in paragraphs (c)(1) through (7) of this section by the compliance date specified in  $\frac{63.7495}{5}$ .

(1) Each COMS must be installed, operated, and maintained according to Performance Specification 1 at appendix B to <u>part</u> <u>60 of this chapter</u>.

(2) You must conduct a performance evaluation of each COMS according to the requirements in  $\frac{63.8(e)}{1}$  and according to Performance Specification 1 at appendix B to part 60 of this chapter.

(3) As specified in  $\frac{63.8(c)(4)(i)}{10}$ , each COMS must complete a minimum of one cycle of sampling and analyzing for each successive 10-second period and one cycle of data recording for each successive 6-minute period.

(4) The COMS data must be reduced as specified in  $\S 63.8(g)(2)$ .

(5) You must include in your site-specific monitoring plan procedures and acceptance criteria for operating and maintaining each COMS according to the requirements in  $\S$  63.8(d). At a minimum, the monitoring plan must include a daily calibration drift assessment, a quarterly performance audit, and an annual zero alignment audit of each COMS.

(6) You must operate and maintain each COMS according to the requirements in the monitoring plan and the requirements of  $\S$  63.8(e). You must identify periods the COMS is out of control including any periods that the COMS fails to pass a daily calibration drift assessment, a quarterly performance audit, or an annual zero alignment audit. Any 6-minute period for which the monitoring system is out of control and data are not available for a required calculation constitutes a deviation from the monitoring requirements.

(7) You must determine and record all the 6-minute averages (and daily block averages as applicable) collected for periods during which the COMS is not out of control.

(d) If you have an operating limit that requires the use of a CMS other than a PM CPMS or COMS, you must install, operate, and maintain each CMS according to the procedures in <u>paragraphs (d)(1)</u> through (5) of this section by the compliance date specified in  $\frac{8}{5}$  63.7495.

(1) The CPMS must complete a minimum of one cycle of operation every 15-minutes. You must have a minimum of four successive cycles of operation, one representing each of the four 15-minute periods in an hour, to have a valid hour of data.

(2) You must operate the monitoring system as specified in  $\S 63.7535(b)$ , and comply with the data calculation requirements specified in  $\S 63.7535(c)$ .

(3) Any 15-minute period for which the monitoring system is out-of-control and data are not available for a required calculation constitutes a deviation from the monitoring requirements. Other situations that constitute a monitoring deviation are specified in  $\frac{63.7535(d)}{10}$ .

(4) You must determine the 30-day rolling average of all recorded readings, except as provided in § 63.7535(c).

(5) You must record the results of each inspection, calibration, and validation check.

(e) If you have an operating limit that requires the use of a flow monitoring system, you must meet the requirements in <u>paragraphs (d)</u> and (e)(1) through (4) of this section.

(1) You must install the flow sensor and other necessary equipment in a position that provides a representative flow.

(2) You must use a flow sensor with a measurement sensitivity of no greater than 2 percent of the design flow rate.

(3) You must minimize, consistent with good engineering practices, the effects of swirling flow or abnormal velocity distributions due to upstream and downstream disturbances.

(4) You must conduct a flow monitoring system performance evaluation in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

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(f) If you have an operating limit that requires the use of a pressure monitoring system, you must meet the requirements in <u>paragraphs (d)</u> and (f)(1) through (6) of this section.

(1) Install the pressure sensor(s) in a position that provides a representative measurement of the pressure (*e.g.*, PM scrubber pressure drop).

(2) Minimize or eliminate pulsating pressure, vibration, and internal and external corrosion consistent with good engineering practices.

(3) Use a pressure sensor with a minimum tolerance of 1.27 centimeters of water or a minimum tolerance of 1 percent of the pressure monitoring system operating range, whichever is less.

(4) Perform checks at least once each process operating day to ensure pressure measurements are not obstructed (*e.g.*, check for pressure tap pluggage daily).

(5) Conduct a performance evaluation of the pressure monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(6) If at any time the measured pressure exceeds the manufacturer's specified maximum operating pressure range, conduct a performance evaluation of the pressure monitoring system in accordance with your monitoring plan and confirm that the pressure monitoring system continues to meet the performance requirements in you monitoring plan. Alternatively, install and verify the operation of a new pressure sensor.

(g) If you have an operating limit that requires a pH monitoring system, you must meet the requirements in <u>paragraphs</u> (d) and (g)(1) through (4) of this section.

(1) Install the pH sensor in a position that provides a representative measurement of scrubber effluent pH.

(2) Ensure the sample is properly mixed and representative of the fluid to be measured.

(3) Calibrate the pH monitoring system in accordance with your monitoring plan and according to the manufacturer's instructions. Clean the pH probe at least once each process operating day. Maintain on-site documentation that your calibration frequency is sufficient to maintain the specified accuracy of your device.

(4) Conduct a performance evaluation (including a two-point calibration with one of the two buffer solutions having a pH within 1 of the pH of the operating limit) of the pH monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(h) If you have an operating limit that requires a secondary electric power monitoring system for an electrostatic precipitator (ESP) operated with a wet scrubber, you must meet the requirements in <u>paragraphs (h)(1)</u> and (2) of this section.

(1) Install sensors to measure (secondary) voltage and current to the precipitator collection plates.

(2) Conduct a performance evaluation of the electric power monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(i) If you have an operating limit that requires the use of a monitoring system to measure sorbent injection rate (e.g., weigh belt, weigh hopper, or hopper flow measurement device), you must meet the requirements in <u>paragraphs</u> (d) and (i)(1) through (2) of this section.

(1) Install the system in a position(s) that provides a representative measurement of the total sorbent injection rate.

(2) Conduct a performance evaluation of the sorbent injection rate monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(j) If you are not required to use a PM CPMS and elect to use a fabric filter bag leak detection system to comply with the requirements of this subpart, you must install, calibrate, maintain, and continuously operate the bag leak detection system as specified in paragraphs (j)(1) through (6) of this section.

(1) You must install a bag leak detection sensor(s) in a position(s) that will be representative of the relative or absolute PM loadings for each exhaust stack, roof vent, or compartment (e.g., for a positive pressure fabric filter) of the fabric filter.

(2) Conduct a performance evaluation of the bag leak detection system in accordance with your monitoring plan and consistent with the guidance provided in EPA-454/R-98-015 (incorporated by reference, see  $\S$  63.14).

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(3) Use a bag leak detection system certified by the manufacturer to be capable of detecting PM emissions at concentrations of 10 milligrams per actual cubic meter or less.

(4) Use a bag leak detection system equipped with a device to record continuously the output signal from the sensor.

(5) Use a bag leak detection system equipped with a system that will alert plant operating personnel when an increase in relative PM emissions over a preset level is detected. The alert must easily recognizable (e.g., heard or seen) by plant operating personnel.

(6) Where multiple bag leak detectors are required, the system's instrumentation and alert may be shared among detectors.

(k) For each unit that meets the definition of limited-use boiler or process heater, you must keep fuel use records for the days the boiler or process heater was operating.

(1) For each unit for which you decide to demonstrate compliance with the mercury or HCl emissions limits in Table 1 or 2 or Tables 11 through 15 to this subpart by use of a CEMS for mercury or HCl, you must install, certify, maintain, and operate a CEMS measuring emissions discharged to the atmosphere and record the output of the system as specified in <u>paragraphs</u> (1)(1) through (8) of this section. For HCl, this option for an affected unit takes effect on the date of approval of a site-specific monitoring plan.

(1) Notify the Administrator one month before starting use of the CEMS, and notify the Administrator one month before stopping use of the CEMS.

(2) Each CEMS shall be installed, certified, operated, and maintained according to the requirements in  $\frac{63.7540(a)(14)}{63.7540(a)(15)}$  for a HCl CEMS.

(3) For a new unit, you must complete the initial performance evaluation of the CEMS by the latest of the dates specified in paragraph (1)(3)(i) through (iii) of this section.

(i) No later than July 30, 2013.

(ii) No later 180 days after the date of initial startup.

(iii) No later 180 days after notifying the Administrator before starting to use the CEMS in place of performance testing or fuel analysis to demonstrate compliance.

(4) For an existing unit, you must complete the initial performance evaluation by the latter of the two dates specified in <u>paragraph (1)(4)(i)</u> and <u>(ii)</u> of this section.

(i) No later than July 29, 2016.

(ii) No later 180 days after notifying the Administrator before starting to use the CEMS in place of performance testing or fuel analysis to demonstrate compliance.

(5) Compliance with the applicable emissions limit shall be determined based on the 30-day rolling average of the hourly arithmetic average emissions rates using the continuous monitoring system outlet data. The 30-day rolling arithmetic average emission rate (lb/MMBtu) shall be calculated using the equations in EPA Reference Method 19 at  $\frac{40 \text{ CFR part } 60, \text{ appendix}}{4.7}$ , but substituting the mercury or HCl concentration for the pollutant concentrations normally used in Method 19.

(6) Collect CEMS hourly averages for all operating hours on a 30-day rolling average basis. Collect at least four CMS data values representing the four 15-minute periods in an hour, or at least two 15-minute data values during an hour when CMS calibration, quality assurance, or maintenance activities are being performed.

(7) The one-hour arithmetic averages required shall be expressed in lb/MMBtu and shall be used to calculate the boiler 30day and 10-day rolling average emissions.

(8) You are allowed to substitute the use of the PM, mercury or HCl CEMS for the applicable fuel analysis, annual performance test, and operating limits specified in Table 4 to this subpart to demonstrate compliance with the PM, mercury or HCl emissions limit, and if you are using an acid gas wet scrubber or dry sorbent injection control technology to comply with the HCl emission limit, you are allowed to substitute the use of a sulfur dioxide (SO<sub>2</sub>) CEMS for the applicable fuel analysis, annual performance test, and operating limits specified in Table 4 to this subpart to demonstrate compliance with HCl emissions limit.

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(m) If your unit is subject to a HCl emission limit in Table 1 or 2 or Tables 11 through 15 to this subpart and you have an acid gas wet scrubber or dry sorbent injection control technology and you elect to use an SO<sub>2</sub> CEMS to demonstrate continuous compliance with the HCl emission limit, you must install the monitor at the outlet of the boiler or process heater, downstream of all emission control devices, and you must install, certify, operate, and maintain the CEMS according to either <u>part 60</u> or <u>part 75 of this chapter</u>.

(1) The SO<sub>2</sub> CEMS must be installed by the compliance date specified in  $\S$  63.7495.

(2) For on-going quality assurance (QA), the SO<sub>2</sub> CEMS must meet either the applicable daily and quarterly requirements in Procedure 1 of appendix F of part 60 or the applicable daily, quarterly, and semiannual or annual requirements in sections 2.1 through 2.3 of appendix B to <u>part 75 of this chapter</u>, with the following addition: You must perform the linearity checks required in <u>section 2.2</u> of appendix B to <u>part 75 of this chapter</u> if the SO<sub>2</sub> CEMS has a span value of 30 ppm or less.

(3) For a new unit, the initial performance evaluation shall be completed no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, the initial performance evaluation shall be completed no later than July 29, 2016.

(4) For purposes of collecting SO<sub>2</sub> data, you must operate the SO<sub>2</sub> CEMS as specified in § <u>63.7535(b)</u>. You must use all the data collected during all periods in calculating data averages and assessing compliance, except that you must exclude certain data as specified in § <u>63.7535(c)</u>. Periods when SO<sub>2</sub> data are unavailable may constitute monitoring deviations as specified in § <u>63.7535(d)</u>.

(5) Collect CEMS hourly averages for all operating hours on a 30-day rolling average basis.

(6) Use only unadjusted, quality-assured  $SO_2$  concentration values in the emissions calculations; do not apply bias adjustment factors to the part 75  $SO_2$  data and do not use part 75 substitute data values.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7171</u>, Jan. 31, 2013; <u>80 FR 72810</u>, Nov. 20, 2015; <u>87 FR 60844</u>, Oct. 6, 2022]

# § 63.7530 How do I demonstrate initial compliance with the emission limitations, fuel specifications and work practice standards?

(a) You must demonstrate initial compliance with each emission limit that applies to you by conducting initial performance tests and fuel analyses and establishing operating limits, as applicable, according to  $\S$  63.7520, paragraphs (b) and (c) of this section, and Tables 5 and 7 to this subpart. The requirement to conduct a fuel analysis is not applicable for units that burn a single type of fuel, as specified by  $\S$  63.7510(a)(2). If applicable, you must also install, operate, and maintain all applicable CMS (including CEMS, COMS, and CPMS) according to  $\S$  63.7525.

(b) If you demonstrate compliance through performance stack testing, you must establish each site-specific operating limit in Table 4 to this subpart that applies to you according to the requirements in § 63.7520, Table 7 to this subpart, and <u>paragraph</u> (b)(4) of this section, as applicable. You must also conduct fuel analyses according to § 63.7521 and establish maximum fuel pollutant input levels according to <u>paragraphs</u> (b)(1) through (3) of this section, as applicable, and as specified in § 63.7510(a)(2). (Note that § 63.7510(a)(2) exempts certain fuels from the fuel analysis requirements.) However, if you switch fuel(s) and cannot show that the new fuel(s) does (do) not increase the chlorine, mercury, or TSM input into the unit through the results of fuel analysis, then you must repeat the performance test to demonstrate compliance while burning the new fuel(s).

(1) You must establish the maximum chlorine fuel input (Clinput) during the initial fuel analysis according to the procedures in paragraphs (b)(1)(i) through (iii) of this section.

(i) You must determine the fuel type or fuel mixture that you could burn in your boiler or process heater that has the highest content of chlorine.

(ii) During the fuel analysis for hydrogen chloride, you must determine the fraction of the total heat input for each fuel type burned (Qi) based on the fuel mixture that has the highest content of chlorine, and the average chlorine concentration of each fuel type burned (Ci).

(iii) You must establish a maximum chlorine input level using Equation 7 of this section.

$$Clinput = \sum_{i=1}^{n} (Ci \times Qi) \quad (Eq. 7)$$

Where:

Clinput = Maximum amount of chlorine entering the boiler or process heater through fuels burned in units of pounds per million Btu.

Ci = Arithmetic average concentration of chlorine in fuel type, i, analyzed according to <u>§ 63.7521</u>, in units of pounds per million Btu.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest content of chlorine during the initial compliance test. If you do not burn multiple fuel types during the performance testing, it is not necessary to determine the value of this term. Insert a value of "1" for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of chlorine.

(2) You must establish the maximum mercury fuel input level (Mercuryinput) during the initial fuel analysis using the procedures in <u>paragraphs (b)(2)(i)</u> through (iii) of this section.

(i) You must determine the fuel type or fuel mixture that you could burn in your boiler or process heater that has the highest content of mercury.

(ii) During the compliance demonstration for mercury, you must determine the fraction of total heat input for each fuel burned (Qi) based on the fuel mixture that has the highest content of mercury, and the average mercury concentration of each fuel type burned (HGi).

(iii) You must establish a maximum mercury input level using Equation 8 of this section.

$$Mercuryinput = \sum_{i=1}^{n} (HGi \times Qi) \quad (Eq. 8)$$

Where:

Mercuryinput = Maximum amount of mercury entering the boiler or process heater through fuels burned in units of pounds per million Btu.

HGi = Arithmetic average concentration of mercury in fuel type, i, analyzed according to § 63.7521, in units of pounds per million Btu.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest mercury content during the initial compliance test. If you do not burn multiple fuel types during the performance test, it is not necessary to determine the value of this term. Insert a value of "1" for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of mercury.

(3) If you opt to comply with the alternative TSM limit, you must establish the maximum TSM fuel input (TSMinput) for solid or liquid fuels during the initial fuel analysis according to the procedures in <u>paragraphs (b)(3)(i)</u> through <u>(iii)</u> of this section.

(i) You must determine the fuel type or fuel mixture that you could burn in your boiler or process heater that has the highest content of TSM.

(ii) During the fuel analysis for TSM, you must determine the fraction of the total heat input for each fuel type burned (Qi) based on the fuel mixture that has the highest content of TSM, and the average TSM concentration of each fuel type burned (TSMi).

(iii) You must establish a maximum TSM input level using Equation 9 of this section.

$$TSMinput = \sum_{i=1}^{n} (TSMi \times Qi) \quad (Eq. 9)$$

Where:

TSMinput = Maximum amount of TSM entering the boiler or process heater through fuels burned in units of pounds per million Btu.

TSMi = Arithmetic average concentration of TSM in fuel type, i, analyzed according to § 63.7521, in units of pounds per million Btu.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest content of TSM during the initial compliance test. If you do not burn multiple fuel types during the performance testing, it is not necessary to determine the value of this term. Insert a value of "1" for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of TSM.

(4) You must establish parameter operating limits according to <u>paragraphs (b)(4)(i)</u> through <u>(ix)</u> of this section. As indicated in Table 4 to this subpart, you are not required to establish and comply with the operating parameter limits when you are using a CEMS to monitor and demonstrate compliance with the applicable emission limit for that control device parameter.

(i) For a wet acid gas scrubber, you must establish the minimum scrubber effluent pH and liquid flow rate as defined in § 63.7575, as your operating limits during the performance test during which you demonstrate compliance with your applicable limit. If you use a wet scrubber and you conduct separate performance tests for HCl and mercury emissions, you must establish one set of minimum scrubber effluent pH, liquid flow rate, and pressure drop operating limits. The minimum scrubber effluent pH operating limit must be established during the HCl performance test. If you conduct multiple performance tests, you must set the minimum liquid flow rate operating limit at the higher of the minimum values established during the performance tests.

(ii) For any particulate control device (e.g., ESP, particulate wet scrubber, fabric filter) for which you use a PM CPMS, you must establish your PM CPMS operating limit and determine compliance with it according to <u>paragraphs</u> (b)(4)(ii)(A) through (F) of this section.

(A) Determine your operating limit as the average PM CPMS output value recorded during the most recent performance test run demonstrating compliance with the filterable PM emission limit or at the PM CPMS output value corresponding to 75 percent of the emission limit if your PM performance test demonstrates compliance below 75 percent of the emission limit. You must verify an existing or establish a new operating limit after each repeated performance test. You must repeat the performance test annually and reassess and adjust the site-specific operating limit in accordance with the results of the performance test.

(1) Your PM CPMS must provide a 4-20 milliamp output and the establishment of its relationship to manual reference method measurements must be determined in units of milliamps.

(2) Your PM CPMS operating range must be capable of reading PM concentrations from zero to a level equivalent to at least two times your allowable emission limit. If your PM CPMS is an auto-ranging instrument capable of multiple scales, the primary range of the instrument must be capable of reading PM concentration from zero to a level equivalent to two times your allowable emission limit.

(3) During the initial performance test or any such subsequent performance test that demonstrates compliance with the PM limit, record and average all milliamp output values from the PM CPMS for the periods corresponding to the compliance test runs (e.g., average all your PM CPMS output values for three corresponding 2-hour Method 5I test runs).

(B) If the average of your three PM performance test runs are below 75 percent of your PM emission limit, you must calculate an operating limit by establishing a relationship of PM CPMS signal to PM concentration using the PM CPMS instrument zero, the average PM CPMS values corresponding to the three compliance test runs, and the average PM

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concentration from the Method 5 or performance test with the procedures in <u>paragraphs (b)(4)(ii)(B)(1)</u> through (4) of this section.

(1) Determine your instrument zero output with one of the following procedures:

(*i*) Zero point data for *in-situ* instruments should be obtained by removing the instrument from the stack and monitoring ambient air on a test bench.

(*ii*) Zero point data for *extractive* instruments should be obtained by removing the extractive probe from the stack and drawing in clean ambient air.

(*iii*) The zero point may also be established by performing manual reference method measurements when the flue gas is free of PM emissions or contains very low PM concentrations (e.g., when your process is not operating, but the fans are operating or your source is combusting only natural gas) and plotting these with the compliance data to find the zero intercept.

(*iv*) If none of the steps in <u>paragraphs (b)(4)(ii)(B)(I)(i)</u> through (*iii*) of this section are possible, you must use a zero output value provided by the manufacturer.

(2) Determine your PM CPMS instrument average in milliamps, and the average of your corresponding three PM compliance test runs, using equation 10.



Where:

 $X_1$  = the PM CPMS data points for the three runs constituting the performance test,

 $Y_1$  = the PM concentration value for the three runs constituting the performance test, and

n = the number of data points.

(3) With your instrument zero expressed in milliamps, your three run average PM CPMS milliamp value, and your three run average PM concentration from your three compliance tests, determine a relationship of lb/MMBtu per milliamp with equation 11.

$$R = \frac{Y_1}{(X_1 - z)}$$
 (Eq. 11)

Where:

R = the relative lb/MMBtu per milliamp for your PM CPMS,

 $Y_1$  = the three run average lb/MMBtu PM concentration,

 $X_1$  = the three run average milliamp output from you PM CPMS, and

z = the milliamp equivalent of your instrument zero determined from (B)(i).

(4) Determine your source specific 30-day rolling average operating limit using the lb/MMBtu per milliamp value from Equation 11 in equation 12, below. This sets your operating limit at the PM CPMS output value corresponding to 75 percent of your emission limit.



Where:

 $O_1$  = the operating limit for your PM CPMS on a 30-day rolling average, in milliamps.

L = your source emission limit expressed in lb/MMBtu,

z = your instrument zero in milliamps, determined from (B)(i), and

R = the relative lb/MMBtu per milliamp for your PM CPMS, from Equation 11.

(C) If the average of your three PM compliance test runs is at or above 75 percent of your PM emission limit you must determine your 30-day rolling average operating limit by averaging the PM CPMS milliamp output corresponding to your three PM performance test runs that demonstrate compliance with the emission limit using equation 13 and you must submit all compliance test and PM CPMS data according to the reporting requirements in <u>paragraph (b)(4)(ii)(F)</u> of this section.



Where:

 $X_1$  = the PM CPMS data points for all runs i,

n = the number of data points, and

 $O_h$  = your site specific operating limit, in milliamps.

(D) To determine continuous compliance, you must record the PM CPMS output data for all periods when the process is operating and the PM CPMS is not out-of-control. You must demonstrate continuous compliance by using all quality-assured hourly average data collected by the PM CPMS for all operating hours to calculate the arithmetic average operating parameter in units of the operating limit (milliamps) on a 30-day rolling average basis, updated at the end of each new operating hour. Use Equation 14 to determine the 30-day rolling average.

$$30 - day = \frac{\sum_{i=1}^{n} Hpw}{n}$$
 (Eq. 14)  
Where:

30-day = 30-day average.

Hpvi = is the hourly parameter value for hour i

n = is the number of valid hourly parameter values collected over the previous 30 operating days.

(E) Use EPA Method 5 of appendix A to <u>part 60 of this chapter</u> to determine PM emissions. For each performance test, conduct three separate runs under the conditions that exist when the affected source is operating at the highest load or capacity level reasonably expected to occur. Conduct each test run to collect a minimum sample volume specified in Table 1 or 2 or Tables 11 through 15 to this subpart, as applicable, for determining compliance with a new source limit or an existing source limit. Calculate the average of the results from three runs to determine compliance. You need not determine the PM collected in the impingers ("back half") of the Method 5 particulate sampling train to demonstrate compliance with the PM standards in this subpart. This shall not preclude the permitting authority from requiring a determination of the "back half" for other purposes.

(F) For PM performance test reports used to set a PM CPMS operating limit, the electronic submission of the test report must also include the make and model of the PM CPMS instrument, serial number of the instrument, analytical principle of the instrument (*e.g.* beta attenuation), span of the instruments primary analytical range, milliamp value equivalent to the instrument zero output, technique by which this zero value was determined, and the average milliamp signals corresponding to each PM compliance test run.

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(iii) For a particulate wet scrubber, you must establish the minimum pressure drop and liquid flow rate as defined in § 63.7575, as your operating limits during the three-run performance test during which you demonstrate compliance with your applicable limit. If you use a wet scrubber and you conduct separate performance tests for PM and TSM emissions, you must establish one set of minimum scrubber liquid flow rate and pressure drop operating limits. If you conduct multiple performance tests, you must set the minimum liquid flow rate and pressure drop operating limits at the higher of the minimum values established during the performance tests.

(iv) For an electrostatic precipitator (ESP) operated with a wet scrubber, you must establish the minimum total secondary electric power input, as defined in § 63.7575, as your operating limit during the three-run performance test during which you demonstrate compliance with your applicable limit. (These operating limits do not apply to ESP that are operated as dry controls without a wet scrubber.)

(v) For a dry scrubber, you must establish the minimum sorbent injection rate for each sorbent, as defined in  $\S$  63.7575, as your operating limit during the three-run performance test during which you demonstrate compliance with your applicable limit.

(vi) For activated carbon injection, you must establish the minimum activated carbon injection rate, as defined in § 63.7575, as your operating limit during the three-run performance test during which you demonstrate compliance with your applicable limit.

(vii) The operating limit for boilers or process heaters with fabric filters that demonstrate continuous compliance through bag leak detection systems is that a bag leak detection system be installed according to the requirements in  $\frac{63.7525}{5}$ , and that each fabric filter must be operated such that the bag leak detection system alert is not activated more than 5 percent of the operating time during a 6-month period.

(viii) For a minimum oxygen level, if you conduct multiple performance tests, you must set the minimum oxygen level at the lower of the minimum values established during the performance tests.

(ix) The operating limit for boilers or process heaters that demonstrate continuous compliance with the HCl emission limit using a SO<sub>2</sub> CEMS is to install and operate the SO<sub>2</sub> according to the requirements in  $\frac{\& 63.7525(m)}{\& 63.7525(m)}$  establish a maximum SO<sub>2</sub> emission rate equal to the highest hourly average SO<sub>2</sub> measurement during the most recent three-run performance test for HCl.

(c) If you elect to demonstrate compliance with an applicable emission limit through fuel analysis, you must conduct fuel analyses according to  $\frac{63.7521}{10}$  and follow the procedures in <u>paragraphs (c)(1)</u> through (5) of this section.

(1) If you burn more than one fuel type, you must determine the fuel mixture you could burn in your boiler or process heater that would result in the maximum emission rates of the pollutants that you elect to demonstrate compliance through fuel analysis.

(2) You must determine the 90th percentile confidence level fuel pollutant concentration of the composite samples analyzed for each fuel type using the one-sided t-statistic test described in Equation 15 of this section.

# $P90 = mean + (SD \times t) \quad (Eq. 15)$

Where:

P90 = 90th percentile confidence level pollutant concentration, in pounds per million Btu.

Mean = Arithmetic average of the fuel pollutant concentration in the fuel samples analyzed according to  $\frac{63.7521}{1000}$ , in units of pounds per million Btu.

SD = Standard deviation of the mean of pollutant concentration in the fuel samples analyzed according to § 63.7521, in units of pounds per million Btu. SD is calculated as the sample standard deviation divided by the square root of the number of samples.

t = t distribution critical value for 90th percentile ( $t_{0.1}$ ) probability for the appropriate degrees of freedom (number of samples minus one) as obtained from a t-Distribution Critical Value Table.

(3) To demonstrate compliance with the applicable emission limit for HCl, the HCl emission rate that you calculate for your boiler or process heater using Equation 16 of this section must not exceed the applicable emission limit for HCl.

$$HCl = \sum_{i=1}^{n} (Ci90 \times Qi \times 1.028)$$
 (Eq. 16)

Where:

HCl = HCl emission rate from the boiler or process heater in units of pounds per million Btu.

Ci90 = 90th percentile confidence level concentration of chlorine in fuel type, i, in units of pounds per million Btu as calculated according to Equation 15 of this section.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest content of chlorine. If you do not burn multiple fuel types, it is not necessary to determine the value of this term. Insert a value of "1" for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of chlorine.

1.028 = Molecular weight ratio of HCl to chlorine.

(4) To demonstrate compliance with the applicable emission limit for mercury, the mercury emission rate that you calculate for your boiler or process heater using Equation 17 of this section must not exceed the applicable emission limit for mercury.

$$Mercury = \sum_{i=1}^{n} (Hgi90 \times Qi) \quad (Eq. 17)$$

Where:

Mercury = Mercury emission rate from the boiler or process heater in units of pounds per million Btu.

Hgi90 = 90th percentile confidence level concentration of mercury in fuel, i, in units of pounds per million Btu as calculated according to Equation 15 of this section.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest mercury content. If you do not burn multiple fuel types, it is not necessary to determine the value of this term. Insert a value of "1" for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest mercury content.

(5) To demonstrate compliance with the applicable emission limit for TSM for solid or liquid fuels, the TSM emission rate that you calculate for your boiler or process heater from solid fuels using Equation 18 of this section must not exceed the applicable emission limit for TSM.

$$Metals = \sum_{i=1}^{n} (TSM90i \times Qi) \quad (Eq. 18)$$

Where:

Metals = TSM emission rate from the boiler or process heater in units of pounds per million Btu.

TSMi90 = 90th percentile confidence level concentration of TSM in fuel, i, in units of pounds per million Btu as calculated according to Equation 15 of this section.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest TSM content. If you do not burn multiple fuel types, it is not necessary to determine the value of this term. Insert a value of "1" for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest TSM content.

(d) [Reserved]

(e) You must include with the Notification of Compliance Status a signed certification that either the energy assessment was completed according to Table 3 to this subpart, and that the assessment is an accurate depiction of your facility at the time of the assessment, or that the maximum number of on-site technical hours specified in the definition of energy assessment applicable to the facility has been expended.

(f) You must submit the Notification of Compliance Status containing the results of the initial compliance demonstration according to the requirements in  $\S$  63.7545(e).

(g) If you elect to demonstrate that a gaseous fuel meets the specifications of another gas 1 fuel as defined in § 63.7575, you must conduct an initial fuel specification analyses according to § 63.7521(f) through (i) and according to the frequency listed in § 63.7540(c) and maintain records of the results of the testing as outlined in § 63.7555(g). For samples where the initial mercury specification has not been exceeded, you will include a signed certification with the Notification of Compliance Status that the initial fuel specification test meets the gas specification outlined in the definition of other gas 1 fuels.

(h) If you own or operate a unit subject to emission limits in Table 1 or 2 or Tables 11 through 15 to this subpart, you must meet the work practice standard according to Table 3 to this subpart. During startup and shutdown, you must only follow the work practice standards according to items 5 and 6 of Table 3 to this subpart.

(i) If you opt to comply with the alternative  $SO_2$  CEMS operating limit in Tables 4 and 8 to this subpart, you may do so only if your affected boiler or process heater:

(1) Has a system using wet scrubber or dry sorbent injection and SO<sub>2</sub> CEMS installed on the unit; and

(2) At all times, you operate the wet scrubber or dry sorbent injection for acid gas control on the unit consistent with  $\S$  <u>63.7500(a)(3)</u>; and

(3) You establish a unit-specific maximum  $SO_2$  operating limit by collecting the maximum hourly  $SO_2$  emission rate on the  $SO_2$  CEMS during the paired 3-run test for HCl. The maximum  $SO_2$  operating limit is equal to the highest hourly average  $SO_2$  concentration measured during the HCl performance test.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7174</u>, Jan. 31, 2013; <u>80 FR 72811</u>, Nov. 20, 2015; <u>87 FR 60845</u>, Oct. 6, 2022]

# § 63.7533 Can I use efficiency credits earned from implementation of energy conservation measures to comply with this subpart?

(a) If you elect to comply with the alternative equivalent output-based emission limits, instead of the heat input-based limits listed in Table 2 or 15 to this subpart, and you want to take credit for implementing energy conservation measures identified in an energy assessment, you may demonstrate compliance using efficiency credits according to the procedures in this section. You may use this compliance approach for an existing affected boiler for demonstrating initial compliance according to  $\S 63.7522(e)$  and for demonstrating monthly compliance according to  $\S 63.7522(f)$ . Owners or operators using this compliance approach must establish an emissions benchmark, calculate and document the efficiency credits, develop an Implementation Plan, comply with the general reporting requirements, and apply the efficiency credit according to the procedures in paragraphs (b) through (f) of this section. You cannot use this compliance approach for a new or reconstructed affected boiler. Additional guidance from the Department of Energy on efficiency credits is available at *https://www.epa.gov/ttn/atw/boiler/boilerpg.html*.

(b) For each existing affected boiler for which you intend to apply emissions credits, establish a benchmark from which emission reduction credits may be generated by determining the actual annual fuel heat input to the affected boiler before initiation of an energy conservation activity to reduce energy demand (*i.e.*, fuel usage) according to <u>paragraphs</u> (b)(1) through (4) of this section. The benchmark shall be expressed in trillion Btu per year heat input.

(1) The benchmark from which efficiency credits may be generated shall be determined by using the most representative, accurate, and reliable process available for the source. The benchmark shall be established for a one-year period before the date that an energy demand reduction occurs, unless it can be demonstrated that a different time period is more representative of historical operations.

(2) Determine the starting point from which to measure progress. Inventory all fuel purchased and generated on-site (off-gases, residues) in physical units (MMBtu, million cubic feet, etc.).

(3) Document all uses of energy from the affected boiler. Use the most recent data available.

(4) Collect non-energy related facility and operational data to normalize, if necessary, the benchmark to current operations, such as building size, operating hours, etc. If possible, use actual data that are current and timely rather than estimated data.

(c) Efficiency credits can be generated if the energy conservation measures were implemented after January 1, 2008 and if sufficient information is available to determine the appropriate value of credits.

(1) The following emission points cannot be used to generate efficiency credits:

(i) Energy conservation measures implemented on or before January 1, 2008, unless the level of energy demand reduction is increased after January 1, 2008, in which case credit will be allowed only for change in demand reduction achieved after January 1, 2008.

(ii) Efficiency credits on shut-down boilers. Boilers that are shut down cannot be used to generate credits unless the facility provides documentation linking the permanent shutdown to energy conservation measures identified in the energy assessment. In this case, the bench established for the affected boiler to which the credits from the shutdown will be applied must be revised to include the benchmark established for the shutdown boiler.

(2) For all points included in calculating emissions credits, the owner or operator shall:

(i) Calculate annual credits for all energy demand points. Use Equation 19 to calculate credits. Energy conservation measures that meet the criteria of <u>paragraph (c)(1)</u> of this section shall not be included, except as specified in <u>paragraph (c)(1)(i)</u> of this section.

(3) Credits are generated by the difference between the benchmark that is established for each affected boiler, and the actual energy demand reductions from energy conservation measures implemented after January 1, 2008. Credits shall be calculated using Equation 19 of this section as follows:

(i) The overall equation for calculating credits is:

$$ECredits = \left(\sum_{i=1}^{n} EIS_{iactual}\right) \div EI_{baseline} \quad (Eq. 19)$$

Where:

ECredits = Energy Input Savings for all energy conservation measures implemented for an affected boiler, expressed as a decimal fraction of the baseline energy input.

EIS<sub>iactual</sub> = Energy Input Savings for each energy conservation measure, i, implemented for an affected boiler, million Btu per year.

EI<sub>baseline</sub> = Energy Input baseline for the affected boiler, million Btu per year.

n = Number of energy conservation measures included in the efficiency credit for the affected boiler.

(ii) [Reserved]

(d) The owner or operator shall develop, and submit for approval upon request by the Administrator, an Implementation Plan containing all of the information required in this paragraph for all boilers to be included in an efficiency credit approach. The Implementation Plan shall identify all existing affected boilers to be included in applying the efficiency credits. The Implementation Plan shall include a description of the energy conservation measures implemented and the energy savings generated from each measure and an explanation of the criteria used for determining that savings. If requested, you must submit the implementation plan for efficiency credits to the Administrator for review and approval no later than 180 days before the date on which the facility intends to demonstrate compliance using the efficiency credit approach.

(e) The emissions rate as calculated using Equation 20 in <u>paragraph (f)</u> of this section from each existing boiler participating in the efficiency credit option must be in compliance with the limits in Table 2 or 15 to this subpart at all times the affected unit is subject to numeric emission limits, following the compliance date specified in  $\frac{63.7495}{5}$ .

(f) You must use Equation 20 of this <u>paragraph (f)</u> to demonstrate initial compliance by demonstrating that the emissions from the affected boiler participating in the efficiency credit compliance approach do not exceed the emission limits in Table 2 or 15 to this subpart.

# Equation 20 to paragraph (f)

# $E_{\alpha\beta} = E_{\alpha} \times (1 - ECredits)$ (Eq. 20)

Where:

 $E_{adj} = Emission$  level adjusted by applying the efficiency credits earned, lb per million Btu steam output (or lb per MWh) for the affected boiler.

 $E_m$  = Emissions measured during the performance test, lb per million Btu steam output (or lb per MWh) for the affected boiler.

ECredits = Efficiency credits from Equation 19 to paragraph(c)(3)(i) of this section for the affected boiler.

(g) As part of each compliance report submitted as required under  $\S$  <u>63.7550</u>, you must include documentation that the energy conservation measures implemented continue to generate the credit for use in demonstrating compliance with the emission limits.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7178</u>, Jan. 31, 2013; <u>80 FR 72812</u>, Nov. 20, 2015; <u>87 FR 60845</u>, Oct. 6, 2022]

# **Continuous Compliance Requirements**

# § 63.7535 Is there a minimum amount of monitoring data I must obtain?

(a) You must monitor and collect data according to this section and the site-specific monitoring plan required by  $\S$  <u>63.7505(d)</u>.

(b) You must operate the monitoring system and collect data at all required intervals at all times that each boiler or process heater is operating and compliance is required, except for periods of monitoring system malfunctions or out of control periods (see § 63.8(c)(7) of this part), and required monitoring system quality assurance or control activities, including, as applicable, calibration checks, required zero and span adjustments, and scheduled CMS maintenance as defined in your site-specific monitoring plan. A monitoring system malfunction is any sudden, infrequent, not reasonably preventable failure of the monitoring system to provide valid data. Monitoring system failures that are caused in part by poor maintenance or careless operation are not malfunctions. You are required to complete monitoring system repairs in response to monitoring system malfunctions or out-of-control periods and to return the monitoring system to operation as expeditiously as practicable.

(c) You may not use data recorded during periods of startup and shutdown, monitoring system malfunctions or out-of-control periods, repairs associated with monitoring system malfunctions or out-of-control periods, or required monitoring system quality assurance or control activities in data averages and calculations used to report emissions or operating levels. You must record and make available upon request results of CMS performance audits and dates and duration of periods when the CMS is out of control to completion of the corrective actions necessary to return the CMS to operation consistent with your site-specific monitoring plan. You must use all the data collected during all other periods in assessing compliance and the operation of the control device and associated control system.

(d) Except for periods of monitoring system malfunctions, repairs associated with monitoring system malfunctions, and required monitoring system quality assurance or quality control activities (including, as applicable, system accuracy audits, calibration checks, and required zero and span adjustments), failure to collect required data is a deviation of the monitoring

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requirements. In calculating monitoring results, do not use any data collected during periods of startup and shutdown, when the monitoring system is out of control as specified in your site-specific monitoring plan, while conducting repairs associated with periods when the monitoring system is out of control, or while conducting required monitoring system quality assurance or quality control activities. You must calculate monitoring results using all other monitoring data collected while the process is operating. You must report all periods when the monitoring system is out of control in your semi-annual report.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7179, Jan. 31, 2013; 80 FR 72812, Nov. 20, 2015]

# § 63.7540 How do I demonstrate continuous compliance with the emission limitations, fuel specifications and work practice standards?

(a) You must demonstrate continuous compliance with each emission limit in Tables 1 and 2 or 11 through 15 to this subpart, the work practice standards in Table 3 to this subpart, and the operating limits in Table 4 to this subpart that applies to you according to the methods specified in Table 8 to this subpart and <u>paragraphs (a)(1)</u> through (19) of this section.

(1) Following the date on which the initial compliance demonstration is completed or is required to be completed under  $\frac{\$\$}{63.7}$  and  $\frac{63.7510}{63.7510}$ , whichever date comes first, operation above the established maximum or below the established minimum operating limits shall constitute a deviation of established operating limits listed in Table 4 of this subpart except during performance tests conducted to determine compliance with the emission limits or to establish new operating limits. Operating limits must be confirmed or reestablished during performance tests.

(2) As specified in  $\S$  63.7555(d), you must keep records of the type and amount of all fuels burned in each boiler or process heater during the reporting period to demonstrate that all fuel types and mixtures of fuels burned would result in either of the following:

(i) Equal to or lower emissions of HCl, mercury, and TSM than the applicable emission limit for each pollutant, if you demonstrate compliance through fuel analysis.

(ii) Equal to or lower fuel input of chlorine, mercury, and TSM than the maximum values calculated during the last performance test, if you demonstrate compliance through performance testing.

(3) If you demonstrate compliance with an applicable HCl emission limit through fuel analysis for a solid or liquid fuel and you plan to burn a new type of solid or liquid fuel, you must recalculate the HCl emission rate using Equation 16 of § 63.7530 according to paragraphs (a)(3)(i) through (iii) of this section. You are not required to conduct fuel analyses for the fuels described in § 63.7510(a)(2)(i) through (iii). You may exclude the fuels described in § 63.7510(a)(2)(i) through (iii) when recalculating the HCl emission rate.

(i) You must determine the chlorine concentration for any new fuel type in units of pounds per million Btu, based on supplier data or your own fuel analysis, according to the provisions in your site-specific fuel analysis plan developed according to  $\frac{\$}{63.7521(b)}$ .

(ii) You must determine the new mixture of fuels that will have the highest content of chlorine.

(iii) Recalculate the HCl emission rate from your boiler or process heater under these new conditions using Equation 16 of  $\S$  <u>63.7530</u>. The recalculated HCl emission rate must be less than the applicable emission limit.

(4) If you demonstrate compliance with an applicable HCl emission limit through performance testing and you plan to burn a new type of fuel or a new mixture of fuels, you must recalculate the maximum chlorine input using Equation 7 of § 63.7530. If the results of recalculating the maximum chlorine input using Equation 7 of § 63.7530 are greater than the maximum chlorine input level established during the previous performance test, then you must conduct a new performance test within 60 days of burning the new fuel type or fuel mixture according to the procedures in § 63.7520 to demonstrate that the HCl emissions do not exceed the emission limit. You must also establish new operating limits based on this performance test according to the procedures in § 63.7530(b). In recalculating the maximum chlorine input and establishing the new operating limits, you are not required to conduct fuel analyses for and include the fuels described in § 63.7510(a)(2)(i) through (iii).

(5) If you demonstrate compliance with an applicable mercury emission limit through fuel analysis, and you plan to burn a new type of fuel, you must recalculate the mercury emission rate using Equation 17 of § 63.7530 according to the procedures specified in paragraphs (a)(5)(i) through (iii) of this section. You are not required to conduct fuel analyses for the fuels described in § 63.7510(a)(2)(i) through (iii). You may exclude the fuels described in § 63.7510(a)(2)(i) through (iii) when recalculating the mercury emission rate.

(i) You must determine the mercury concentration for any new fuel type in units of pounds per million Btu, based on supplier data or your own fuel analysis, according to the provisions in your site-specific fuel analysis plan developed according to  $\frac{63.7521(b)}{2}$ .

(ii) You must determine the new mixture of fuels that will have the highest content of mercury.

(iii) Recalculate the mercury emission rate from your boiler or process heater under these new conditions using Equation 17 of  $\S$  63.7530. The recalculated mercury emission rate must be less than the applicable emission limit.

(6) If you demonstrate compliance with an applicable mercury emission limit through performance testing, and you plan to burn a new type of fuel or a new mixture of fuels, you must recalculate the maximum mercury input using Equation 8 of § <u>63.7530</u>. If the results of recalculating the maximum mercury input using Equation 8 of § <u>63.7530</u> are higher than the maximum mercury input level established during the previous performance test, then you must conduct a new performance test within 60 days of burning the new fuel type or fuel mixture according to the procedures in § <u>63.7520</u> to demonstrate that the mercury emissions do not exceed the emission limit. You must also establish new operating limits based on this performance test according to the procedures in § <u>63.7510(a)(2)(i)</u> through (iii). You may exclude the fuels described in § <u>63.7510(a)(2)(i)</u> through (iii) when recalculating the mercury emission rate.

(7) If your unit is controlled with a fabric filter, and you demonstrate continuous compliance using a bag leak detection system, you must initiate corrective action within 1 hour of a bag leak detection system alert and complete corrective actions as soon as practical, and operate and maintain the fabric filter system such that the periods which would cause an alert are no more than 5 percent of the operating time during a 6-month period. You must also keep records of the date, time, and duration of each alert, the time corrective action was initiated and completed, and a brief description of the cause of the alert and the corrective action taken. You must also record the percent of the operating time during each 6-month period that the conditions exist for an alert. In calculating this operating time percentage, if inspection of the fabric filter demonstrates that no corrective action is required, no alert time is counted. If corrective action is required, each alert shall be counted as a minimum of 1 hour. If you take longer than 1 hour to initiate corrective action, the alert time shall be counted as the actual amount of time taken to initiate corrective action.

(8) To demonstrate compliance with the applicable alternative CO CEMS emission limit listed in Table 1 or 2 or Tables 11 through 15 to this subpart, you must meet the requirements in paragraphs (a)(8)(i) through (iv) of this section.

(i) Continuously monitor CO according to <u>§§ 63.7525(a)</u> and <u>63.7535</u>.

(ii) Maintain a CO emission level below or at your applicable alternative CO CEMS-based standard in Table 1 or 2 or Tables 11 through 15 to this subpart at all times the affected unit is subject to numeric emission limits.

(iii) Keep records of CO levels according to  $\S$  63.7555(b).

(iv) You must record and make available upon request results of CO CEMS performance audits, dates and duration of periods when the CO CEMS is out of control to completion of the corrective actions necessary to return the CO CEMS to operation consistent with your site-specific monitoring plan.

(9) The owner or operator of a boiler or process heater using a PM CPMS or a PM CEMS to meet requirements of this subpart shall install, certify (PM CEMS only), operate, and maintain the PM CPMS or PM CEMS in accordance with your site-specific monitoring plan as required in  $\frac{63.7505(d)}{2}$ .

(10) If your boiler or process heater has a heat input capacity of 10 million Btu per hour or greater, you must conduct an annual tune-up of the boiler or process heater to demonstrate continuous compliance as specified in <u>paragraphs</u> (a)(10)(i) through (vi) of this section. You must conduct the tune-up while burning the type of fuel (or fuels in case of units that routinely burn a mixture) that provided the majority of the heat input to the boiler or process heater over the 12 months prior to the tune-up. This frequency does not apply to limited-use boilers and process heaters, as defined in § 63.7575, or units with continuous oxygen trim systems that maintain an optimum air to fuel ratio.

(i) As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;

(ii) Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;

(iii) Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;

(iv) Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any  $NO_X$  requirement to which the unit is subject;

(v) Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and

(vi) Maintain on-site and submit, if requested by the Administrator, a report containing the information in <u>paragraphs</u> (a)(10)(vi)(A) through (C) of this section,

(A) The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;

(B) A description of any corrective actions taken as a part of the tune-up; and

(C) The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

(11) If your boiler or process heater has a heat input capacity of less than 10 million Btu per hour (except as specified in paragraph (a)(12) of this section), you must conduct a biennial tune-up of the boiler or process heater as specified in paragraphs (a)(10)(i) through (vi) of this section to demonstrate continuous compliance.

(12) If your boiler or process heater has a continuous oxygen trim system that maintains an optimum air to fuel ratio, or a heat input capacity of less than or equal to 5 million Btu per hour and the unit is in the units designed to burn gas 1; units designed to burn gas 2 (other); or units designed to burn light liquid subcategories, or meets the definition of limited-use boiler or process heater in § 63.7575, you must conduct a tune-up of the boiler or process heater every 5 years as specified in paragraphs (a)(10)(i) through (vi) of this section to demonstrate continuous compliance. You may delay the burner inspection specified in paragraph (a)(10)(i) of this section until the next scheduled or unscheduled unit shutdown, but you must inspect each burner at least once every 72 months. If an oxygen trim system is utilized on a unit without emission standards to reduce the tune-up frequency to once every 5 years, set the oxygen level no lower than the oxygen concentration measured during the most recent tune-up.

(13) If the unit is not operating on the required date for a tune-up, the tune-up must be conducted within 30 calendar days of startup.

(14) If you are using a CEMS measuring mercury emissions to meet requirements of this subpart you must install, certify, operate, and maintain the mercury CEMS as specified in <u>paragraphs (a)(14)(i)</u> and <u>(ii)</u> of this section.

(i) Operate the mercury CEMS in accordance with performance specification 12A of <u>40 CFR part 60</u>, <u>appendix B</u> or operate a sorbent trap based integrated monitor in accordance with performance specification 12B of <u>40 CFR part 60</u>, <u>appendix B</u>. The duration of the performance test must be 30 operating days if you specified a 30 operating day basis in § <u>63.7545(e)(2)(iii)</u> for mercury CEMS or it must be 720 hours if you specified a 720 hour basis in § <u>63.7545(e)(2)(iii)</u> for mercury CEMS. For each day in which the unit operates, you must obtain hourly mercury concentration data, and stack gas volumetric flow rate data.

(ii) If you are using a mercury CEMS, you must install, operate, calibrate, and maintain an instrument for continuously measuring and recording the mercury mass emissions rate to the atmosphere according to the requirements of performance specifications 6 and 12A of <u>40 CFR part 60</u>, appendix B, and quality assurance procedure 6 of <u>40 CFR part 60</u>, appendix F.

(15) If you are using a CEMS to measure HCl emissions to meet requirements of this subpart, you must install, certify, operate, and maintain the HCl CEMS as specified in <u>paragraphs (a)(15)(i)</u> and <u>(ii)</u> of this section. This option for an affected unit takes effect on the date of approval of a site-specific monitoring plan.

(i) Operate the continuous emissions monitoring system in accordance with the applicable performance specification in <u>40</u> <u>CFR part 60, appendix B</u>. The duration of the performance test must be 30 operating days if you specified a 30 operating day basis in § 63.7545(e)(2)(iii) for HCl CEMS or it must be 720 hours if you specified a 720 hour basis in § <u>63.7545(e)(2)(iii)</u> for HCl CEMS. For each day in which the unit operates, you must obtain hourly HCl concentration data, and stack gas volumetric flow rate data.

(ii) If you are using a HCl CEMS, you must install, operate, calibrate, and maintain an instrument for continuously measuring and recording the HCl mass emissions rate to the atmosphere according to the requirements of the applicable performance specification of  $\frac{40 \text{ CFR part } 60}{40 \text{ cFR part } 60}$ , appendix B, and the quality assurance procedures of  $\frac{40 \text{ CFR part } 60}{40 \text{ cFR part } 60}$ , appendix F.

(16) If you demonstrate compliance with an applicable TSM emission limit through performance testing, and you plan to burn a new type of fuel or a new mixture of fuels, you must recalculate the maximum TSM input using Equation 9 of § 63.7530. If the results of recalculating the maximum TSM input using Equation 9 of § 63.7530 are higher than the maximum total selected input level established during the previous performance test, then you must conduct a new performance test within 60 days of burning the new fuel type or fuel mixture according to the procedures in § 63.7520 to demonstrate that the TSM emissions do not exceed the emission limit. You must also establish new operating limits based on this performance test according to the procedures in § 63.7530(b). You are not required to conduct fuel analyses for the fuels described in § 63.7510(a)(2)(i) through (iii). You may exclude the fuels described in § 63.7510(a)(2)(i) through (iii) when recalculating the TSM emission rate.

(17) If you demonstrate compliance with an applicable TSM emission limit through fuel analysis for solid or liquid fuels, and you plan to burn a new type of fuel, you must recalculate the TSM emission rate using Equation 18 of § 63.7530 according to the procedures specified in paragraphs (a)(5)(i) through (iii) of this section. You are not required to conduct fuel analyses for the fuels described in § 63.7510(a)(2)(i) through (iii). You may exclude the fuels described in § 63.7510(a)(2)(i) through (iii) when recalculating the TSM emission rate.

(i) You must determine the TSM concentration for any new fuel type in units of pounds per million Btu, based on supplier data or your own fuel analysis, according to the provisions in your site-specific fuel analysis plan developed according to  $\frac{63.7521(b)}{2}$ .

(ii) You must determine the new mixture of fuels that will have the highest content of TSM.

(iii) Recalculate the TSM emission rate from your boiler or process heater under these new conditions using Equation 18 of  $\S$  <u>63.7530</u>. The recalculated TSM emission rate must be less than the applicable emission limit.

(18) If you demonstrate continuous PM emissions compliance with a PM CPMS you will use a PM CPMS to establish a sitespecific operating limit corresponding to the results of the performance test demonstrating compliance with the PM limit. You will conduct your performance test using the test method criteria in Table 5 of this subpart. You will use the PM CPMS to demonstrate continuous compliance with this operating limit. You must repeat the performance test annually and reassess and adjust the site-specific operating limit in accordance with the results of the performance test.

(i) To determine continuous compliance, you must record the PM CPMS output data for all periods when the process is operating and the PM CPMS is not out-of-control. You must demonstrate continuous compliance by using all quality-assured hourly average data collected by the PM CPMS for all operating hours to calculate the arithmetic average operating parameter in units of the operating limit (milliamps) on a 30-day rolling average basis.

(ii) For any deviation of the 30-day rolling PM CPMS average value from the established operating parameter limit, you must:

(A) Within 48 hours of the deviation, visually inspect the air pollution control device (APCD);

(B) If inspection of the APCD identifies the cause of the deviation, take corrective action as soon as possible and return the PM CPMS measurement to within the established value; and

(C) Within 30 days of the deviation or at the time of the annual compliance test, whichever comes first, conduct a PM emissions compliance test to determine compliance with the PM emissions limit and to verify or re-establish the CPMS operating limit. You are not required to conduct additional testing for any deviations that occur between the time of the original deviation and the PM emissions compliance test required under this paragraph.

(iii) PM CPMS deviations from the operating limit leading to more than four required performance tests in a 12-month operating period constitute a separate violation of this subpart.

(19) If you choose to comply with the PM filterable emissions limit by using PM CEMS you must install, certify, operate, and maintain a PM CEMS and record the output of the PM CEMS as specified in <u>paragraphs (a)(19)(i)</u> through (vii) of this section. The compliance limit will be expressed as a 30-day rolling average of the numerical emissions limit value applicable for your unit in Table 1 or 2 or Tables 11 through 15 to this subpart.

(i) Install and certify your PM CEMS according to the procedures and requirements in Performance Specification 11— Specifications and Test Procedures for Particulate Matter Continuous Emission Monitoring Systems at Stationary Sources in Appendix B to <u>part 60 of this chapter</u>, using test criteria outlined in Table V of this rule. The reportable measurement output from the PM CEMS must be expressed in units of the applicable emissions limit (e.g., lb/MMBtu, lb/MWh).

(ii) Operate and maintain your PM CEMS according to the procedures and requirements in Procedure 2— Quality Assurance Requirements for Particulate Matter Continuous Emission Monitoring Systems at Stationary Sources in Appendix F to <u>part</u> <u>60 of this chapter</u>.

(A) You must conduct the relative response audit (RRA) for your PM CEMS at least once annually.

(B) You must conduct the relative correlation audit (RCA) for your PM CEMS at least once every 3 years.

(iii) Collect PM CEMS hourly average output data for all boiler operating hours except as indicated in <u>paragraph (v)</u> of this section.

(iv) Calculate the arithmetic 30-day rolling average of all of the hourly average PM CEMS output data collected during all nonexempt boiler or process heater operating hours.

(v) You must collect data using the PM CEMS at all times the unit is operating and at the intervals specified this <u>paragraph</u> (a), except for periods of monitoring system malfunctions, repairs associated with monitoring system malfunctions, and required monitoring system quality assurance or quality control activities.

(vi) You must use all the data collected during all boiler or process heater operating hours in assessing the compliance with your operating limit except:

(A) Any data collected during monitoring system malfunctions, repairs associated with monitoring system malfunctions, or required monitoring system quality assurance or control activities conducted during monitoring system malfunctions in calculations and report any such periods in your annual deviation report;

(B) Any data collected during periods when the monitoring system is out of control as specified in your site-specific monitoring plan, repairs associated with periods when the monitoring system is out of control, or required monitoring system quality assurance or control activities conducted during out of control periods in calculations used to report emissions or operating levels and report any such periods in your annual deviation report;

(C) Any data recorded during periods of startup or shutdown.

(vii) You must record and make available upon request results of PM CEMS system performance audits, dates and duration of periods when the PM CEMS is out of control to completion of the corrective actions necessary to return the PM CEMS to operation consistent with your site-specific monitoring plan.

(b) You must report each instance in which you did not meet each emission limit and operating limit in Tables 1 through 4 or 11 through 15 to this subpart that apply to you. These instances are deviations from the emission limits or operating limits, respectively, in this subpart. These deviations must be reported according to the requirements in  $\frac{\& 63.7550}{\& 63.7550}$ .

(c) If you elected to demonstrate that the unit meets the specification for mercury for the unit designed to burn gas 1 subcategory, you must follow the sampling frequency specified in <u>paragraphs (c)(1)</u> through (4) of this section and conduct this sampling according to the procedures in  $\frac{\$ 63.7521(f)}{10}$  through (i).

(1) If the initial mercury constituents in the gaseous fuels are measured to be equal to or less than half of the mercury specification as defined in  $\frac{63.7575}{5}$ , you do not need to conduct further sampling.

(2) If the initial mercury constituents are greater than half but equal to or less than 75 percent of the mercury specification as defined in <u>§ 63.7575</u>, you will conduct semi-annual sampling. If 6 consecutive semi-annual fuel analyses demonstrate 50 percent or less of the mercury specification, you do not need to conduct further sampling. If any semi-annual sample exceeds 75 percent of the mercury specification, you must return to monthly sampling for that fuel, until 12 months of fuel analyses again are less than 75 percent of the compliance level.

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(3) If the initial mercury constituents are greater than 75 percent of the mercury specification as defined in <u>§ 63.7575</u>, you will conduct monthly sampling. If 12 consecutive monthly fuel analyses demonstrate 75 percent or less of the mercury specification, you may decrease the fuel analysis frequency to semi-annual for that fuel.

(4) If the initial sample exceeds the mercury specification as defined in  $\S$  63.7575, each affected boiler or process heater combusting this fuel is not part of the unit designed to burn gas 1 subcategory and must be in compliance with the emission and operating limits for the appropriate subcategory. You may elect to conduct additional monthly sampling while complying with these emissions and operating limits to demonstrate that the fuel qualifies as another gas 1 fuel. If 12 consecutive monthly fuel analyses samples are at or below the mercury specification as defined in  $\S$  63.7575, each affected boiler or process heater combusting the fuel can elect to switch back into the unit designed to burn gas 1 subcategory until the mercury specification is exceeded.

(d) For startup and shutdown, you must meet the work practice standards according to items 5 and 6 of Table 3 of this subpart.

[78 FR 7179, Jan. 31, 2013, as amended at 80 FR 72813, Nov. 20, 2015; 87 FR 60846, Oct. 6, 2022]

#### § 63.7541 How do I demonstrate continuous compliance under the emissions averaging provision?

(a) Following the compliance date, the owner or operator must demonstrate compliance with this subpart on a continuous basis by meeting the requirements of paragraphs (a)(1) through (5) of this section.

(1) For each calendar month, demonstrate compliance with the average weighted emissions limit for the existing units participating in the emissions averaging option as determined in  $\S$  63.7522(f) and (g).

(2) You must maintain the applicable opacity limit according to paragraphs (a)(2)(i) and (ii) of this section.

(i) For each existing unit participating in the emissions averaging option that is equipped with a dry control system and not vented to a common stack, maintain opacity at or below the applicable limit.

(ii) For each group of units participating in the emissions averaging option where each unit in the group is equipped with a dry control system and vented to a common stack that does not receive emissions from non-affected units, maintain opacity at or below the applicable limit at the common stack.

(3) For each existing unit participating in the emissions averaging option that is equipped with a wet scrubber, maintain the 30-day rolling average parameter values at or above the operating limits established during the most recent performance test.

(4) For each existing unit participating in the emissions averaging option that has an approved alternative operating parameter, maintain the 30-day rolling average parameter values consistent with the approved monitoring plan.

(5) For each existing unit participating in the emissions averaging option venting to a common stack configuration containing affected units from other subcategories, maintain the appropriate operating limit for each unit as specified in Table 4 to this subpart that applies.

(b) Any instance where the owner or operator fails to comply with the continuous monitoring requirements in <u>paragraphs</u> (a)(1) through (5) of this section is a deviation.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7182, Jan. 31, 2013]

#### Notification, Reports, and Records

#### § 63.7545 What notifications must I submit and when?

(a) You must submit to the Administrator all of the notifications in  $\underline{\$\$ 63.7(b)}$  and (c),  $\underline{63.8(e)}$ , (f)(4) and (6), and  $\underline{63.9(b)}$  through (h) that apply to you by the dates specified.

(b) As specified in  $\frac{63.9(b)(2)}{10}$ , if you startup your affected source before January 31, 2013, you must submit an Initial Notification not later than 120 days after January 31, 2013, or no later than 120 days after the source becomes subject to this subpart, whichever is later.

(c) As specified in  $\S 63.9(b)(4)$  and (5), if you startup your new or reconstructed affected source on or after January 31, 2013, you must submit an Initial Notification not later than 15 days after the actual date of startup of the affected source. For a new or reconstructed affected source that has reclassified to major source status, you must submit an Initial Notification not later 120 days after the source becomes subject to this subpart.

(d) If you are required to conduct a performance test you must submit a Notification of Intent to conduct a performance test at least 60 days before the performance test is scheduled to begin.

(e) If you are required to conduct an initial compliance demonstration as specified in § 63.7530, you must submit a Notification of Compliance Status according to § 63.9(h)(2)(ii). For the initial compliance demonstration for each boiler or process heater, you must submit the Notification of Compliance Status, including all performance test results and fuel analyses, before the close of business on the 60th day following the completion of all performance test and/or other initial compliance demonstrations for all boiler or process heaters at the facility according to § 63.10(d)(2). The Notification of Compliance Status report must contain all the information specified in paragraphs (e)(1) through (8) of this section, as applicable. If you are not required to conduct an initial compliance demonstration as specified in § 63.7530(a), the Notification of Compliance Status must only contain the information specified in paragraphs (e)(1) and (8) of this section and must be submitted within 60 days of the compliance date specified at § 63.7495(b).

(1) A description of the affected unit(s) including identification of which subcategories the unit is in, the design heat input capacity of the unit, a description of the add-on controls used on the unit to comply with this subpart, description of the fuel(s) burned, including whether the fuel(s) were a secondary material determined by you or the EPA through a petition process to be a non-waste under § 241.3 of this chapter, whether the fuel(s) were a secondary material processed from discarded non-hazardous secondary materials within the meaning of § 241.3 of this chapter, and justification for the selection of fuel(s) burned during the compliance demonstration.

(2) Summary of the results of all performance tests and fuel analyses, and calculations conducted to demonstrate initial compliance including all established operating limits, and including:

(i) Identification of whether you are complying with the PM emission limit or the alternative TSM emission limit.

(ii) Identification of whether you are complying with the output-based emission limits or the heat input-based (i.e., lb/MMBtu or ppm) emission limits,

(iii) Identification of whether you are complying the arithmetic mean of all valid hours of data from the previous 30 operating days or of the previous 720 hours. This identification shall be specified separately for each operating parameter.

(3) A summary of the maximum CO emission levels recorded during the performance test to show that you have met any applicable emission standard in Table 1 or 2 or Tables 11 through 15 to this subpart, if you are not using a CO CEMS to demonstrate compliance.

(4) Identification of whether you plan to demonstrate compliance with each applicable emission limit through performance testing, a CEMS, or fuel analysis.

(5) Identification of whether you plan to demonstrate compliance by emissions averaging and identification of whether you plan to demonstrate compliance by using efficiency credits through energy conservation:

(i) If you plan to demonstrate compliance by emission averaging, report the emission level that was being achieved or the control technology employed on January 31, 2013.

(ii) [Reserved]

(6) A signed certification that you have met all applicable emission limits and work practice standards.

(7) If you had a deviation from any emission limit, work practice standard, or operating limit, you must also submit a description of the deviation, the duration of the deviation, and the corrective action taken in the Notification of Compliance Status report.

(8) In addition to the information required in  $\frac{63.9(h)(2)}{100}$ , your notification of compliance status must include the following certification(s) of compliance, as applicable, and signed by a responsible official:

(i) "This facility completed the required initial tune-up for all of the boilers and process heaters covered by  $\frac{40 \text{ CFR part } 63}{\text{subpart DDDDD}}$  at this site according to the procedures in  $\frac{63.7540(a)(10)(i)}{10}$  through (vi)."

(ii) "This facility has had an energy assessment performed according to § 63.7530(e)."

(iii) Except for units that burn only natural gas, refinery gas, or other gas 1 fuel, or units that qualify for a statutory exemption as provided in section 129(g)(1) of the Clean Air Act, include the following: "No secondary materials that are solid waste were combusted in any affected unit."

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(f) If you operate a unit designed to burn natural gas, refinery gas, or other gas 1 fuels that is subject to this subpart, and you intend to use a fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart of this part, part 60, 61, or 65, or other gas 1 fuel to fire the affected unit during a period of natural gas curtailment or supply interruption, as defined in  $\frac{63.7575}{5}$ , you must submit a notification of alternative fuel use within 48 hours of the declaration of each period of natural gas curtailment or supply interruption, as defined in  $\frac{8.63.7575}{5}$ . The notification must include the information specified in paragraphs (f)(1) through (5) of this section.

(1) Company name and address.

(2) Identification of the affected unit.

(3) Reason you are unable to use natural gas or equivalent fuel, including the date when the natural gas curtailment was declared or the natural gas supply interruption began.

(4) Type of alternative fuel that you intend to use.

(5) Dates when the alternative fuel use is expected to begin and end.

(g) If you intend to commence or recommence combustion of solid waste, you must provide 30 days prior notice of the date upon which you will commence or recommence combustion of solid waste. The notification must identify:

(1) The name of the owner or operator of the affected source, as defined in  $\S$  63.7490, the location of the source, the boiler(s) or process heater(s) that will commence burning solid waste, and the date of the notice.

(2) The currently applicable subcategories under this subpart.

(3) The date on which you became subject to the currently applicable emission limits.

(4) The date upon which you will commence combusting solid waste.

(h) If you have switched fuels or made a physical change to the boiler or process heater and the fuel switch or physical change resulted in the applicability of a different subcategory, you must provide notice of the date upon which you switched fuels or made the physical change within 30 days of the switch/change. The notification must identify:

(1) The name of the owner or operator of the affected source, as defined in  $\S$  63.7490, the location of the source, the boiler(s) and process heater(s) that have switched fuels, were physically changed, and the date of the notice.

(2) The currently applicable subcategory under this subpart.

(3) The date upon which the fuel switch or physical change occurred.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7183</u>, Jan. 31, 2013; <u>80 FR 72814</u>, Nov. 20, 2015; <u>85 FR 73913</u>, Nov. 19, 2020; <u>85 FR 84262</u>, Dec. 28, 2020; <u>87 FR 60846</u>, Oct. 6, 2022]

# § 63.7550 What reports must I submit and when?

(a) You must submit each report in Table 9 to this subpart that applies to you.

(b) Unless the EPA Administrator has approved a different schedule for submission of reports under  $\frac{63.10(a)}{2}$ , you must submit each report, according to <u>paragraph (h)</u> of this section, by the date in Table 9 to this subpart and according to the requirements in <u>paragraphs (b)(1)</u> through (4) of this section. For units that are subject only to a requirement to conduct subsequent annual, biennial, or 5-year tune-up according to  $\frac{63.7540(a)(10)}{2}$ , (11), or (12), respectively, and not subject to emission limits or Table 4 operating limits, you may submit only an annual, biennial, or 5-year compliance report, as applicable, as specified in <u>paragraphs (b)(1)</u> through (4) of this section, instead of a semi-annual compliance report.

(1) The first semi-annual compliance report must cover the period beginning on the compliance date that is specified for each boiler or process heater in  $\S$  63.7495 and ending on June 30 or December 31, whichever date is the first date that occurs at least 180 days after the compliance date that is specified for your source in  $\S$  63.7495. If submitting an annual, biennial, or 5-year compliance report, the first compliance report must cover the period beginning on the compliance date that is specified for each boiler or process heater in  $\S$  63.7495 and ending on December 31 within 1, 2, or 5 years, as applicable, after the compliance date that is specified for your source in  $\S$  63.7495.

(2) The first semi-annual compliance report must be postmarked or submitted no later than July 31 or January 31, whichever date is the first date following the end of the first calendar half after the compliance date that is specified for each boiler or
process heater in § 63.7495. The first annual, biennial, or 5-year compliance report must be postmarked or submitted no later than January 31.

(3) Each subsequent semi-annual compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31. Annual, biennial, and 5-year compliance reports must cover the applicable 1-, 2-, or 5-year periods from January 1 to December 31.

(4) Each subsequent semi-annual compliance report must be postmarked or submitted no later than July 31 or January 31, whichever date is the first date following the end of the semiannual reporting period. Annual, biennial, and 5-year compliance reports must be postmarked or submitted no later than January 31.

(5) For each affected source that is subject to permitting regulations pursuant to part 70 or part 71 of this chapter, and if the permitting authority has established dates for submitting semiannual reports pursuant to 70.6(a)(3)(iii)(A) or 71.6(a)(3)(iii)(A), you may submit the first and subsequent compliance reports according to the dates the permitting authority has established in the permit instead of according to the dates in paragraphs (b)(1) through (4) of this section.

(c) A compliance report must contain the following information depending on how the facility chooses to comply with the limits set in this rule.

(1) If the facility is subject to the requirements of a tune up you must submit a compliance report with the information in <u>paragraphs (c)(5)(i)</u> through (iii) of this section, (xiv) and (xvii) of this section, and <u>paragraph (c)(5)(iv)</u> of this section for limited-use boiler or process heater.

(2) If you are complying with the fuel analysis you must submit a compliance report with the information in paragraphs (c)(5)(i) through (iii), (vi), (x), (xi), (xiii), (xv), (xviii), (xviii) and <u>paragraph (d)</u> of this section.

(3) If you are complying with the applicable emissions limit with performance testing you must submit a compliance report with the information in (c)(5)(i) through (iii), (vi), (vii), (ix), (xi), (xi), (xv), (xvii), (xviii) and paragraph (d) of this section.

(4) If you are complying with an emissions limit using a CMS the compliance report must contain the information required in paragraphs (c)(5)(i) through (iii), (v), (vi), (xi) through (xiii), (xv) through (xviii), and <u>paragraph (e)</u> of this section.

(5)

(i) Company and Facility name and address.

(ii) Process unit information, emissions limitations, and operating parameter limitations.

(iii) Date of report and beginning and ending dates of the reporting period.

(iv) The total operating time during the reporting period.

(v) If you use a CMS, including CEMS, COMS, or CPMS, you must include the monitoring equipment manufacturer(s) and model numbers and the date of the last CMS certification or audit.

(vi) The total fuel use by each individual boiler or process heater subject to an emission limit within the reporting period, including, but not limited to, a description of the fuel, whether the fuel has received a non-waste determination by the EPA or your basis for concluding that the fuel is not a waste, and the total fuel usage amount with units of measure.

(vii) If you are conducting performance tests once every 3 years consistent with  $\S$  63.7515(b) or (c), the date of the last 2 performance tests and a statement as to whether there have been any operational changes since the last performance test that could increase emissions.

(viii) A statement indicating that you burned no new types of fuel in an individual boiler or process heater subject to an emission limit. Or, if you did burn a new type of fuel and are subject to a HCl emission limit, you must submit the calculation of chlorine input, using Equation 7 of § 63.7530, that demonstrates that your source is still within its maximum chlorine input level established during the previous performance testing (for sources that demonstrate compliance through performance testing) or you must submit the calculation of HCl emission rate using Equation 16 of § 63.7530 that demonstrates that your source is still meeting the emission limit for HCl emissions (for boilers or process heaters that demonstrate compliance through fuel analysis). If you burned a new type of fuel and are subject to a mercury emission limit, you must submit the calculation 8 of § 63.7530, that demonstrates that your source is still within its maximum mercury input, using Equation 8 of § 63.7530, that demonstrates that your source is still within its maximum mercury input level established during the previous performance testing (for sources that demonstrate compliance through fuel analysis).

performance testing), or you must submit the calculation of mercury emission rate using Equation 17 of § 63.7530 that demonstrates that your source is still meeting the emission limit for mercury emissions (for boilers or process heaters that demonstrate compliance through fuel analysis). If you burned a new type of fuel and are subject to a TSM emission limit, you must submit the calculation of TSM input, using Equation 9 of § 63.7530, that demonstrates that your source is still within its maximum TSM input level established during the previous performance testing (for sources that demonstrate compliance through or you must submit the calculation of TSM emission rate, using Equation 18 of § 63.7530, that demonstrates that your source is still meeting the emission limit for TSM emissions (for boilers or process heaters that demonstrate compliance through performance testing), or you must submit the calculation of TSM emissions (for boilers or process heaters that demonstrate compliance through fuel analysis).

(ix) If you wish to burn a new type of fuel in an individual boiler or process heater subject to an emission limit and you cannot demonstrate compliance with the maximum chlorine input operating limit using Equation 7 of  $\frac{63.7530}{50.00}$  or the maximum mercury input operating limit using Equation 8 of  $\frac{63.7530}{50.000}$ , or the maximum TSM input operating limit using Equation 9 of  $\frac{63.7530}{50.0000}$  you must include in the compliance report a statement indicating the intent to conduct a new performance test within 60 days of starting to burn the new fuel.

(x) A summary of any monthly fuel analyses conducted to demonstrate compliance according to  $\frac{\&\& 63.7521}{\&\& 63.7521}$  and  $\frac{63.7530}{\&\& 63.7521}$  for individual boilers or process heaters subject to emission limits, and any fuel specification analyses conducted according to  $\frac{\&\&}{63.7521(f)}$  and  $\frac{63.7530(g)}{63.7521(f)}$ .

(xi) If there are no deviations from any emission limits or operating limits in this subpart that apply to you, a statement that there were no deviations from the emission limits or operating limits during the reporting period.

(xii) If there were no deviations from the monitoring requirements including no periods during which the CMSs, including CEMS, COMS, and CPMS, were out of control as specified in  $\S$  63.8(c)(7), a statement that there were no deviations and no periods during which the CMS were out of control during the reporting period.

(xiii) If a malfunction occurred during the reporting period, the report must include the number, duration, and a brief description for each type of malfunction which occurred during the reporting period and which caused or may have caused any applicable emission limitation to be exceeded. The report must also include a description of actions taken by you during a malfunction of a boiler, process heater, or associated air pollution control device or CMS to minimize emissions in accordance with  $\S$  63.7500(a)(3), including actions taken to correct the malfunction.

(xiv) Include the date of the most recent tune-up for each unit subject to only the requirement to conduct an annual, biennial, or 5-year tune-up according to  $\frac{63.7540(a)(10)}{(11)}$ , or  $\frac{(12)}{(12)}$  respectively. Include the date of the most recent burner inspection if it was not done annually, biennially, or on a 5-year period and was delayed until the next scheduled or unscheduled unit shutdown.

(xv) If you plan to demonstrate compliance by emission averaging, certify the emission level achieved or the control technology employed is no less stringent than the level or control technology contained in the notification of compliance status in  $\frac{63.7545(e)(5)(i)}{10}$ .

(xvi) For each reporting period, the compliance reports must include all of the calculated 30 day rolling average values for CEMS (CO, HCl, SO<sub>2</sub>, and mercury), 10 day rolling average values for CO CEMS when the limit is expressed as a 10 day instead of 30 day rolling average, and the PM CPMS data.

(xvii) Statement by a responsible official with that official's name, title, and signature, certifying the truth, accuracy, and completeness of the content of the report.

(xviii) For each instance of startup or shutdown include the information required to be monitored, collected, or recorded according to the requirements of  $\frac{8}{5}$  63.7555(d).

(d) For each deviation from an emission limit or operating limit in this subpart that occurs at an individual boiler or process heater where you are not using a CMS to comply with that emission limit or operating limit, or from the work practice standards for periods if startup and shutdown, the compliance report must additionally contain the information required in paragraphs (d)(1) through (3) of this section.

(1) A description of the deviation and which emission limit, operating limit, or work practice standard from which you deviated.

(2) Information on the number, duration, and cause of deviations (including unknown cause), as applicable, and the corrective action taken.

#### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

(3) If the deviation occurred during an annual performance test, provide the date the annual performance test was completed.

(e) For each deviation from an emission limit, operating limit, and monitoring requirement in this subpart occurring at an individual boiler or process heater where you are using a CMS to comply with that emission limit or operating limit, the compliance report must additionally contain the information required in <u>paragraphs (e)(1)</u> through (9) of this section. This includes any deviations from your site-specific monitoring plan as required in § 63.7505(d).

(1) The date and time that each deviation started and stopped and description of the nature of the deviation (i.e., what you deviated from).

(2) The date and time that each CMS was inoperative, except for zero (low-level) and high-level checks.

(3) The date, time, and duration that each CMS was out of control, including the information in  $\frac{63.8(c)(8)}{2}$ .

(4) The date and time that each deviation started and stopped.

(5) A summary of the total duration of the deviation during the reporting period and the total duration as a percent of the total source operating time during that reporting period.

(6) A characterization of the total duration of the deviations during the reporting period into those that are due to control equipment problems, process problems, other known causes, and other unknown causes.

(7) A summary of the total duration of CMS's downtime during the reporting period and the total duration of CMS downtime as a percent of the total source operating time during that reporting period.

(8) A brief description of the source for which there was a deviation.

(9) A description of any changes in CMSs, processes, or controls since the last reporting period for the source for which there was a deviation.

(f)-(g) [Reserved]

(h) You must submit the reports according to the procedures specified in <u>paragraphs (h)(1)</u> through (3) of this section.

(1) Within 60 days after the date of completing each performance test (as defined in  $\S$  <u>63.2</u>) required by this subpart, you must submit the results of the performance tests, including any fuel analyses, following the procedure specified in either <u>paragraph (h)(1)(i)</u> or <u>(ii)</u> of this section.

(i) For data collected using test methods supported by the EPA's Electronic Reporting Tool (ERT) as listed on the EPA's ERT Web site (*http://www.epa.gov/ttn/chief/ert/index.html*), you must submit the results of the performance test to the EPA via the Compliance and Emissions Data Reporting Interface (CEDRI). (CEDRI can be accessed through the EPA's Central Data Exchange (CDX) (*https://cdx.epa.gov/*).) Performance test data must be submitted in a file format generated through use of the EPA's ERT or an electronic file format consistent with the extensible markup language (XML) schema listed on the EPA's ERT Web site. If you claim that some of the performance test information being submitted is confidential business information (CBI), you must submit a complete file generated through the use of the EPA's ERT or an alternate electronic file consistent with the XML schema listed on the EPA's ERT Web site, including information claimed to be CBI, on a compact disc, flash drive, or other commonly used electronic storage media to the EPA. The electronic media must be clearly marked as CBI and mailed to U.S. EPA/OAPQS/CORE CBI Office, Attention: Group Leader, Measurement Policy Group, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same ERT or alternate file with the CBI omitted must be submitted to the EPA's CDX as described earlier in this paragraph.

(ii) For data collected using test methods that are not supported by the EPA's ERT as listed on the EPA's ERT Web site at the time of the test, you must submit the results of the performance test to the Administrator at the appropriate address listed in  $\S$  63.13.

(2) Within 60 days after the date of completing each CEMS performance evaluation (as defined in 63.2), you must submit the results of the performance evaluation following the procedure specified in either paragraph (h)(2)(i) or (ii) of this section.

(i) For performance evaluations of continuous monitoring systems measuring relative accuracy test audit (RATA) pollutants that are supported by the EPA's ERT as listed on the EPA's ERT Web site at the time of the evaluation, you must submit the results of the performance evaluation to the EPA via the CEDRI. (CEDRI can be accessed through the EPA's CDX.) Performance evaluation data must be submitted in a file format generated through the use of the EPA's ERT or an alternate file format consistent with the XML schema listed on the EPA's ERT Web site. If you claim that some of the performance

evaluation information being transmitted is CBI, you must submit a complete file generated through the use of the EPA's ERT or an alternate electronic file consistent with the XML schema listed on the EPA's ERT Web site, including information claimed to be CBI, on a compact disc, flash drive, or other commonly used electronic storage media to the EPA. The electronic media must be clearly marked as CBI and mailed to U.S. EPA/OAPQS/CORE CBI Office, Attention: Group Leader, Measurement Policy Group, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same ERT or alternate file with the CBI omitted must be submitted to the EPA via the EPA's CDX as described earlier in this paragraph.

(ii) For any performance evaluations of continuous monitoring systems measuring RATA pollutants that are not supported by the EPA's ERT as listed on the ERT Web site at the time of the evaluation, you must submit the results of the performance evaluation to the Administrator at the appropriate address listed in  $\frac{863.13}{2}$ .

(3) You must submit all reports required by Table 9 of this subpart electronically to the EPA via the CEDRI. (CEDRI can be accessed through the EPA's CDX.) You must use the appropriate electronic report in CEDRI for this subpart. Instead of using the electronic report in CEDRI for this subpart, you may submit an alternate electronic file consistent with the XML schema listed on the CEDRI Web site (<u>http://www.epa.gov/ttn/chief/cedri/index.html</u>), once the XML schema is available. If the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, you must submit the report to the Administrator at the appropriate address listed in § 63.13. You must begin submitting reports via CEDRI no later than 90 days after the form becomes available in CEDRI.

[78 FR 7183, Jan. 31, 2013, as amended at 80 FR 72814, Nov. 20, 2015]

#### § 63.7555 What records must I keep?

(a) You must keep records according to <u>paragraphs (a)(1)</u> and (2) of this section.

(1) A copy of each notification and report that you submitted to comply with this subpart, including all documentation supporting any Initial Notification or Notification of Compliance Status or semiannual compliance report that you submitted, according to the requirements in  $\S$  63.10(b)(2)(xiv).

(2) Records of performance tests, fuel analyses, or other compliance demonstrations and performance evaluations as required in  $\frac{63.10(b)(2)(viii)}{63.10(b)(2)(viii)}$ .

(3) For units in the limited use subcategory, you must keep a copy of the federally enforceable permit that limits the annual capacity factor to less than or equal to 10 percent and fuel use records for the days the boiler or process heater was operating.

(b) For each CEMS, COMS, and continuous monitoring system you must keep records according to <u>paragraphs</u> (b)(1) through (5) of this section.

(1) Records described in  $\S 63.10(b)(2)(vii)$  through (xi).

(2) Monitoring data for continuous opacity monitoring system during a performance evaluation as required in  $\S$  <u>63.6(h)(7)(i)</u> and <u>(ii)</u>.

(3) Previous (*i.e.*, superseded) versions of the performance evaluation plan as required in  $\frac{63.8(d)(3)}{2}$ .

(4) Request for alternatives to relative accuracy test for CEMS as required in  $\frac{63.8(f)(6)(i)}{5.000}$ .

(5) Records of the date and time that each deviation started and stopped.

(c) You must keep the records required in Table 8 to this subpart including records of all monitoring data and calculated averages for applicable operating limits, such as opacity, pressure drop, pH, and operating load, to show continuous compliance with each emission limit and operating limit that applies to you.

(d) For each boiler or process heater subject to an emission limit in Table 1 or 2 or Tables 11 through 15 to this subpart, you must also keep the applicable records in paragraphs (d)(1) through (11) of this section.

(1) You must keep records of monthly fuel use by each boiler or process heater, including the type(s) of fuel and amount(s) used.

(2) If you combust non-hazardous secondary materials that have been determined not to be solid waste pursuant to  $\frac{2}{241.3(b)(1)}$  and  $\frac{(2)}{(2)}$  of this chapter, you must keep a record that documents how the secondary material meets each of the legitimacy criteria under  $\frac{2}{241.3(d)(1)}$  of this chapter. If you combust a fuel that has been processed from a discarded non-hazardous secondary material pursuant to  $\frac{2}{241.3(b)(4)}$  of this chapter, you must keep records as to how the operations that produced the fuel satisfy the definition of processing in  $\frac{2}{241.2}$  of this chapter. If the fuel received a non-waste determination

pursuant to the petition process submitted under § 241.3(c) of this chapter, you must keep a record that documents how the fuel satisfies the requirements of the petition process. For operating units that combust non-hazardous secondary materials as fuel per § 241.4 of this chapter, you must keep records documenting that the material is listed as a non-waste under § 241.4(a) of this chapter. Units exempt from the incinerator standards under section 129(g)(1) of the Clean Air Act because they are qualifying facilities burning a homogeneous waste stream do not need to maintain the records described in this paragraph (d)(2).

(3) A copy of all calculations and supporting documentation of maximum chlorine fuel input, using Equation 7 of  $\frac{6}{5}$  63.7530, that were done to demonstrate continuous compliance with the HCl emission limit, for sources that demonstrate compliance through performance testing. For sources that demonstrate compliance through fuel analysis, a copy of all calculations and supporting documentation of HCl emission rates, using Equation 16 of  $\frac{6}{5}$  63.7530, that were done to demonstrate compliance with the HCl emission limit. Supporting documentation should include results of any fuel analyses and basis for the estimates of maximum chlorine fuel input or HCl emission rates. You can use the results from one fuel analysis for multiple boilers and process heaters provided they are all burning the same fuel type. However, you must calculate chlorine fuel input, or HCl emission rate, for each boiler and process heater.

(4) A copy of all calculations and supporting documentation of maximum mercury fuel input, using Equation 8 of  $\S$  63.7530, that were done to demonstrate continuous compliance with the mercury emission limit for sources that demonstrate compliance through performance testing. For sources that demonstrate compliance through fuel analysis, a copy of all calculations and supporting documentation of mercury emission rates, using Equation 17 of  $\S$  63.7530, that were done to demonstrate compliance with the mercury emission limit. Supporting documentation should include results of any fuel analyses and basis for the estimates of maximum mercury fuel input or mercury emission rates. You can use the results from one fuel analysis for multiple boilers and process heaters provided they are all burning the same fuel type. However, you must calculate mercury fuel input, or mercury emission rates, for each boiler and process heater.

(5) If, consistent with  $\S$  <u>63.7515(b)</u>, you choose to stack test less frequently than annually, you must keep a record that documents that your emissions in the previous stack test(s) were less than 75 percent of the applicable emission limit (or, in specific instances noted in Tables 1 and 2 or 11 through 15 to this subpart, less than the applicable emission limit), and document that there was no change in source operations including fuel composition and operation of air pollution control equipment that would cause emissions of the relevant pollutant to increase within the past year.

(6) Records of the occurrence and duration of each malfunction of the boiler or process heater, or of the associated air pollution control and monitoring equipment.

(7) Records of actions taken during periods of malfunction to minimize emissions in accordance with the general duty to minimize emissions in  $\frac{63.7500(a)(3)}{2}$ , including corrective actions to restore the malfunctioning boiler or process heater, air pollution control, or monitoring equipment to its normal or usual manner of operation.

(8) A copy of all calculations and supporting documentation of maximum TSM fuel input, using Equation 9 of § 63.7530, that were done to demonstrate continuous compliance with the TSM emission limit for sources that demonstrate compliance through performance testing. For sources that demonstrate compliance through fuel analysis, a copy of all calculations and supporting documentation of TSM emission rates, using Equation 18 of § 63.7530, that were done to demonstrate compliance with the TSM emission limit. Supporting documentation should include results of any fuel analyses and basis for the estimates of maximum TSM fuel input or TSM emission rates. You can use the results from one fuel analysis for multiple boilers and process heaters provided they are all burning the same fuel type. However, you must calculate TSM fuel input, or TSM emission rates, for each boiler and process heater.

(9) You must maintain records of the calendar date, time, occurrence and duration of each startup and shutdown.

(10) You must maintain records of the type(s) and amount(s) of fuels used during each startup and shutdown.

(11) For each startup period, for units selecting paragraph (2) of the definition of "startup" in § 63.7575 you must maintain records of the time that clean fuel combustion begins; the time when you start feeding fuels that are not clean fuels; the time when useful thermal energy is first supplied; and the time when the PM controls are engaged.

(12) If you choose to rely on paragraph (2) of the definition of "startup" in § <u>63.7575</u>, for each startup period, you must maintain records of the hourly steam temperature, hourly steam pressure, hourly steam flow, hourly flue gas temperature, and all hourly average CMS data (*e.g.*, CEMS, PM CPMS, COMS, ESP total secondary electric power input, scrubber pressure drop, scrubber liquid flow rate) collected during each startup period to confirm that the control devices are engaged. In

addition, if compliance with the PM emission limit is demonstrated using a PM control device, you must maintain records as specified in <u>paragraphs (d)(12)(i)</u> through (iii) of this section.

(i) For a boiler or process heater with an electrostatic precipitator, record the number of fields in service, as well as each field's secondary voltage and secondary current during each hour of startup.

(ii) For a boiler or process heater with a fabric filter, record the number of compartments in service, as well as the differential pressure across the baghouse during each hour of startup.

(iii) For a boiler or process heater with a wet scrubber needed for filterable PM control, record the scrubber's liquid flow rate and the pressure drop during each hour of startup.

(13) If you choose to use paragraph (2) of the definition of "startup" in <u>§ 63.7575</u> and you find that you are unable to safely engage and operate your PM control(s) within 1 hour of first firing of non-clean fuels, you may choose to rely on paragraph (1) of definition of "startup" in <u>§ 63.7575</u> or you may submit to the delegated permitting authority a request for a variance with the PM controls requirement, as described below.

(i) The request shall provide evidence of a documented manufacturer-identified safety issue.

(ii) The request shall provide information to document that the PM control device is adequately designed and sized to meet the applicable PM emission limit.

(iii) In addition, the request shall contain documentation that:

(A) The unit is using clean fuels to the maximum extent possible to bring the unit and PM control device up to the temperature necessary to alleviate or prevent the identified safety issues prior to the combustion of primary fuel;

(B) The unit has explicitly followed the manufacturer's procedures to alleviate or prevent the identified safety issue; and

(C) Identifies with specificity the details of the manufacturer's statement of concern.

(iv) You must comply with all other work practice requirements, including but not limited to data collection, recordkeeping, and reporting requirements.

(e) If you elect to average emissions consistent with  $\S$  <u>63.7522</u>, you must additionally keep a copy of the emission averaging implementation plan required in  $\S$  <u>63.7522(g)</u>, all calculations required under  $\S$  <u>63.7522</u>, including monthly records of heat input or steam generation, as applicable, and monitoring records consistent with  $\S$  <u>63.7541</u>.

(f) If you elect to use efficiency credits from energy conservation measures to demonstrate compliance according to § 63.7533, you must keep a copy of the Implementation Plan required in § 63.7533(d) and copies of all data and calculations used to establish credits according to § 63.7533(b), (c), and (f).

(g) If you elected to demonstrate that the unit meets the specification for mercury for the unit designed to burn gas 1 subcategory, you must maintain monthly records (or at the frequency required by  $\S 63.7540(c)$ ) of the calculations and results of the fuel specification for mercury in Table 6.

(h) If you operate a unit in the unit designed to burn gas 1 subcategory that is subject to this subpart, and you use an alternative fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart under this part, other gas 1 fuel, or gaseous fuel subject to another subpart of this part or part 60, 61, or 65, you must keep records of the total hours per calendar year that alternative fuel is burned and the total hours per calendar year that the unit operated during periods of gas curtailment or gas supply emergencies.

[<u>76 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7185</u>, Jan. 31, 2013; <u>80 FR 72816</u>, Nov. 20, 2015; <u>87 FR 60846</u>, Oct. 6, 2022]

#### § 63.7560 In what form and how long must I keep my records?

(a) Your records must be in a form suitable and readily available for expeditious review, according to  $\frac{63.10(b)(1)}{10.000}$ .

(b) As specified in  $\S$  63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.

(c) You must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to  $\frac{63.10(b)(1)}{2}$ . You can keep the records off site for the remaining 3 years.

#### Other Requirements and Information

#### § 63.7565 What parts of the General Provisions apply to me?

Table 10 to this subpart shows which parts of the General Provisions in  $\frac{\&\& 63.1}{\&\& 63.1}$  through  $\frac{63.15}{\&\& 63.1}$  apply to you.

#### § 63.7570 Who implements and enforces this subpart?

(a) This subpart can be implemented and enforced by the EPA, or an Administrator such as your state, local, or tribal agency. If the EPA Administrator has delegated authority to your state, local, or tribal agency, then that agency (as well as the EPA) has the authority to implement and enforce this subpart. You should contact your EPA Regional Office to find out if this subpart is delegated to your state, local, or tribal agency.

(1) Approval of alternatives to the emission limits and work practice standards in § 63.7500(a) and (b) under § 63.6(g), except as specified in § 63.7555(d)(13).

(2) Approval of major change to test methods in Table 5 to this subpart under  $\S 63.7(e)(2)(ii)$  and (f) and as defined in  $\S 63.90$ , and alternative analytical methods requested under  $\S 63.7521(b)(2)$ .

(3) Approval of major change to monitoring under § 63.8(f) and as defined in § 63.90, and approval of alternative operating parameters under §§ 63.7500(a)(2) and  $\underline{63.7522(g)(2)}$ .

(4) Approval of major change to recordkeeping and reporting under  $\S 63.10(e)$  and as defined in  $\S 63.90$ .

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7186, Jan. 31, 2013; 80 FR 72817, Nov. 20, 2015]

#### § 63.7575 What definitions apply to this subpart?

Terms used in this subpart are defined in the Clean Air Act, in <u>§ 63.2</u> (the General Provisions), and in this section as follows:

*10-day rolling average* means the arithmetic mean of the previous 240 hours of valid operating data. Valid data excludes hours during startup and shutdown, data collected during periods when the monitoring system is out of control as specified in your site-specific monitoring plan, while conducting repairs associated with periods when the monitoring system is out of control, or while conducting required monitoring system quality assurance or quality control activities, and periods when this unit is not operating. The 240 hours should be consecutive, but not necessarily continuous if operations were intermittent.

12-month rolling average means the arithmetic mean of the previous 12 months of valid fuel analysis data. The 12 months should be consecutive, but not necessarily continuous if operations were intermittent.

*30-day rolling average* means the arithmetic mean of the previous 720 hours of valid CO CEMS data. The 720 hours should be consecutive, but not necessarily continuous if operations were intermittent. For parameters other than CO, 30-day rolling average means either the arithmetic mean of all valid hours of data from 30 successive operating days or the arithmetic mean of the previous 720 hours of valid operating data. Valid data excludes hours during startup and shutdown, data collected during periods when the monitoring system is out of control as specified in your site-specific monitoring plan, while conducting repairs associated with periods when the monitoring system is out of control, or while conducting required monitoring system quality assurance or quality control activities, and periods when this unit is not operating.

Annual capacity factor means the ratio between the actual heat input to a boiler or process heater from the fuels burned during a calendar year and the potential heat input to the boiler or process heater had it been operated for 8,760 hours during a year at the maximum steady state design heat input capacity.

Annual heat input means the heat input for the 12 months preceding the compliance demonstration.

Average annual heat input rate means total heat input divided by the hours of operation for the 12 months preceding the compliance demonstration.

*Bag leak detection system* means a group of instruments that are capable of monitoring particulate matter loadings in the exhaust of a fabric filter (*i.e.*, baghouse) in order to detect bag failures. A bag leak detection system includes, but is not

limited to, an instrument that operates on electrodynamic, triboelectric, light scattering, light transmittance, or other principle to monitor relative particulate matter loadings.

*Benchmark* means the fuel heat input for a boiler or process heater for the one-year period before the date that an energy demand reduction occurs, unless it can be demonstrated that a different time period is more representative of historical operations.

*Biodiesel* means a mono-alkyl ester derived from biomass and conforming to ASTM D6751-11b, Standard Specification for Biodiesel Fuel Blend Stock (B100) for Middle Distillate Fuels (incorporated by reference, see  $\frac{\& 63.14}{1.00}$ ).

*Biomass or bio-based solid fuel* means any biomass-based solid fuel that is not a solid waste. This includes, but is not limited to, wood residue; wood products (*e.g.*, trees, tree stumps, tree limbs, bark, lumber, sawdust, sander dust, chips, scraps, slabs, millings, and shavings); animal manure, including litter and other bedding materials; vegetative agricultural and silvicultural materials, such as logging residues (slash), nut and grain hulls and chaff (*e.g.*, almond, walnut, peanut, rice, and wheat), bagasse, orchard prunings, corn stalks, coffee bean hulls and grounds. This definition of biomass is not intended to suggest that these materials are or are not solid waste.

Blast furnace gas fuel-fired boiler or process heater means an industrial/commercial/institutional boiler or process heater that receives 90 percent or more of its total annual gas volume from blast furnace gas.

*Boiler* means an enclosed device using controlled flame combustion and having the primary purpose of recovering thermal energy in the form of steam or hot water. Controlled flame combustion refers to a steady-state, or near steady-state, process wherein fuel and/or oxidizer feed rates are controlled. A device combusting solid waste, as defined in § 241.3 of this chapter, is not a boiler unless the device is exempt from the definition of a solid waste incineration unit as provided in section 129(g)(1) of the Clean Air Act. Waste heat boilers are excluded from this definition.

*Boiler system* means the boiler and associated components, such as, the feed water system, the combustion air system, the fuel system (including burners), blowdown system, combustion control systems, steam systems, and condensate return systems.

Calendar year means the period between January 1 and December 31, inclusive, for a given year.

*Clean dry biomass* means any biomass-based solid fuel that have not been painted, pigment-stained, or pressure treated, does not contain contaminants at concentrations not normally associated with virgin biomass materials and has a moisture content of less than 20 percent and is not a solid waste.

*Coal* means all solid fuels classifiable as anthracite, bituminous, sub-bituminous, or lignite by ASTM D388 (incorporated by reference, see  $\S$  63.14), coal refuse, and petroleum coke. For the purposes of this subpart, this definition of "coal" includes synthetic fuels derived from coal, including but not limited to, solvent-refined coal, coal-oil mixtures, and coal-water mixtures. Coal derived gases are excluded from this definition.

*Coal refuse* means any by-product of coal mining or coal cleaning operations with an ash content greater than 50 percent (by weight) and a heating value less than 13,900 kilojoules per kilogram (6,000 Btu per pound) on a dry basis.

*Commercial/institutional boiler* means a boiler used in commercial establishments or institutional establishments such as medical centers, nursing homes, research centers, institutions of higher education, elementary and secondary schools, libraries, religious establishments, governmental buildings, hotels, restaurants, and laundries to provide electricity, steam, and/or hot water.

*Common stack* means the exhaust of emissions from two or more affected units through a single flue. Affected units with a common stack may each have separate air pollution control systems located before the common stack, or may have a single air pollution control system located after the exhausts come together in a single flue.

*Cost-effective energy conservation measure* means a measure that is implemented to improve the energy efficiency of the boiler or facility that has a payback (return of investment) period of 2 years or less.

*Daily block average* means the arithmetic mean of all valid emission concentrations or parameter levels recorded when a unit is operating measured over the 24-hour period from 12 a.m. (midnight) to 12 a.m. (midnight), except for periods of startup and shutdown or downtime.

Deviation.

(1) Deviation means any instance in which an affected source subject to this subpart, or an owner or operator of such a source:

(i) Fails to meet any applicable requirement or obligation established by this subpart including, but not limited to, any emission limit, operating limit, or work practice standard; or

(ii) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart and that is included in the operating permit for any affected source required to obtain such a permit.

(2) A deviation is not always a violation.

Dioxins/furans means tetra- through octa-chlorinated dibenzo-p-dioxins and dibenzofurans.

*Distillate oil* means fuel oils that contain 0.05 weight percent nitrogen or less and comply with the specifications for fuel oil numbers 1 and 2, as defined by the American Society of Testing and Materials in ASTM D396 (incorporated by reference, see  $\S$  63.14) or diesel fuel oil numbers 1 and 2, as defined by the American Society for Testing and Materials in ASTM D975 (incorporated by reference, see  $\S$  63.14), kerosene, and biodiesel as defined by the American Society of Testing and Materials in ASTM D6751-11b (incorporated by reference, see  $\S$  60.14).

*Dry scrubber* means an add-on air pollution control system that injects dry alkaline sorbent (dry injection) or sprays an alkaline sorbent (spray dryer) to react with and neutralize acid gas in the exhaust stream forming a dry powder material. Sorbent injection systems used as control devices in fluidized bed boilers and process heaters are included in this definition. A dry scrubber is a dry control system.

*Dutch oven* means a unit having a refractory-walled cell connected to a conventional boiler setting. Fuel materials are introduced through an opening in the roof of the dutch oven and burn in a pile on its floor. Fluidized bed boilers are not part of the dutch oven design category.

*Efficiency credit* means emission reductions above those required by this subpart. Efficiency credits generated may be used to comply with the emissions limits. Credits may come from pollution prevention projects that result in reduced fuel use by affected units. Boilers that are shut down cannot be used to generate credits unless the facility provides documentation linking the permanent shutdown to implementation of the energy conservation measures identified in the energy assessment.

*Electric utility steam generating unit (EGU)* means a fossil fuel-fired combustion unit of more than 25 megawatts electric (MWe) that serves a generator that produces electricity for sale. A fossil fuel-fired unit that cogenerates steam and electricity and supplies more than one-third of its potential electric output capacity and more than 25 MWe output to any utility power distribution system for sale is considered an electric utility steam generating unit. To be "capable of combusting" fossil fuels, an EGU would need to have these fuels allowed in their operating permits and have the appropriate fuel handling facilities on-site or otherwise available (e.g., coal handling equipment, including coal storage area, belts and conveyers, pulverizers, etc.; oil storage facilities). In addition, fossil fuel-fired EGU means any EGU that fired fossil fuel for more than 10.0 percent of the average annual heat input in any 3 consecutive calendar years or for more than 15.0 percent of the annual heat input during any one calendar year after April 16, 2012.

*Electrostatic precipitator (ESP)* means an add-on air pollution control device used to capture particulate matter by charging the particles using an electrostatic field, collecting the particles using a grounded collecting surface, and transporting the particles into a hopper. An electrostatic precipitator is usually a dry control system.

*Energy assessment* means the following for the emission units covered by this subpart:

(1) The energy assessment for facilities with affected boilers and process heaters with a combined heat input capacity of less than 0.3 trillion Btu (TBtu) per year will be 8 on-site technical labor hours in length maximum, but may be longer at the discretion of the owner or operator of the affected source. The boiler system(s), process heater(s), and any on-site energy use system(s) accounting for at least 50 percent of the affected boiler(s) energy (*e.g.*, steam, hot water, process heat, or electricity) production, as applicable, will be evaluated to identify energy savings opportunities, within the limit of performing an 8-hour on-site energy assessment.

(2) The energy assessment for facilities with affected boilers and process heaters with a combined heat input capacity of 0.3 to 1.0 TBtu/year will be 24 on-site technical labor hours in length maximum, but may be longer at the discretion of the owner or operator of the affected source. The boiler system(s), process heater(s), and any on-site energy use system(s) accounting for at least 33 percent of the energy (*e.g.*, steam, hot water, process heat, or electricity) production, as applicable, will be evaluated to identify energy savings opportunities, within the limit of performing a 24-hour on-site energy assessment.

(3) The energy assessment for facilities with affected boilers and process heaters with a combined heat input capacity greater than 1.0 TBtu/year will be up to 24 on-site technical labor hours in length for the first TBtu/yr plus 8 on-site technical labor hours for every additional 1.0 TBtu/yr not to exceed 160 on-site technical hours, but may be longer at the discretion of the owner or operator of the affected source. The boiler system(s), process heater(s), and any on-site energy use system(s) accounting for at least 20 percent of the energy (*e.g.*, steam, process heat, hot water, or electricity) production, as applicable, will be evaluated to identify energy savings opportunities.

(4) The on-site energy use systems serving as the basis for the percent of affected boiler(s) and process heater(s) energy production in paragraphs (1), (2), and (3) of this definition may be segmented by production area or energy use area as most logical and applicable to the specific facility being assessed (*e.g.*, product X manufacturing area; product Y drying area; Building Z).

*Energy management practices* means the set of practices and procedures designed to manage energy use that are demonstrated by the facility's energy policies, a facility energy manager and other staffing responsibilities, energy performance measurement and tracking methods, an energy saving goal, action plans, operating procedures, internal reporting requirements, and periodic review intervals used at the facility.

*Energy management program* means a program that includes a set of practices and procedures designed to manage energy use that are demonstrated by the facility's energy policies, a facility energy manager and other staffing responsibilities, energy performance measurement and tracking methods, an energy saving goal, action plans, operating procedures, internal reporting requirements, and periodic review intervals used at the facility. Facilities may establish their program through energy management systems compatible with ISO 50001.

*Energy use system* includes the following systems located on-site that use energy (steam, hot water, or electricity) provided by the affected boiler or process heater: process heating; compressed air systems; machine drive (motors, pumps, fans); process cooling; facility heating, ventilation, and air-conditioning systems; hot water systems; building envelop; and lighting; or other systems that use steam, hot water, process heat, or electricity provided by the affected boiler or process heater. Energy use systems are only those systems using energy clearly produced by affected boilers and process heaters.

Equivalent means the following only as this term is used in Table 6 to this subpart:

(1) An equivalent sample collection procedure means a published voluntary consensus standard or practice (VCS) or EPA method that includes collection of a minimum of three composite fuel samples, with each composite consisting of a minimum of three increments collected at approximately equal intervals over the test period.

(2) An equivalent sample compositing procedure means a published VCS or EPA method to systematically mix and obtain a representative subsample (part) of the composite sample.

(3) An equivalent sample preparation procedure means a published VCS or EPA method that: Clearly states that the standard, practice or method is appropriate for the pollutant and the fuel matrix; or is cited as an appropriate sample preparation standard, practice or method for the pollutant in the chosen VCS or EPA determinative or analytical method.

(4) An equivalent procedure for determining heat content means a published VCS or EPA method to obtain gross calorific (or higher heating) value.

(5) An equivalent procedure for determining fuel moisture content means a published VCS or EPA method to obtain moisture content. If the sample analysis plan calls for determining metals (especially the mercury, selenium, or arsenic) using an aliquot of the dried sample, then the drying temperature must be modified to prevent vaporizing these metals. On the other hand, if metals analysis is done on an "as received" basis, a separate aliquot can be dried to determine moisture content and the metals concentration mathematically adjusted to a dry basis.

(6) An equivalent pollutant (mercury, HCl) determinative or analytical procedure means a published VCS or EPA method that clearly states that the standard, practice, or method is appropriate for the pollutant and the fuel matrix and has a published detection limit equal or lower than the methods listed in Table 6 to this subpart for the same purpose.

*Fabric filter* means an add-on air pollution control device used to capture particulate matter by filtering gas streams through filter media, also known as a baghouse. A fabric filter is a dry control system.

*Federally enforceable* means all limitations and conditions that are enforceable by the EPA Administrator, including, but not limited to, the requirements of  $\frac{40 \text{ CFR parts } 60, 61, 63}{40 \text{ CFR } 52.21}$  or under  $\frac{40 \text{ CFR } 51.18}{40 \text{ CFR } 51.24}$ .

#### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

Fluidized bed boiler means a boiler utilizing a fluidized bed combustion process that is not a pulverized coal boiler.

*Fluidized bed boiler with an integrated fluidized bed heat exchanger* means a boiler utilizing a fluidized bed combustion where the entire tube surface area is located outside of the furnace section at the exit of the cyclone section and exposed to the flue gas stream for conductive heat transfer. This design applies only to boilers in the unit designed to burn coal/solid fossil fuel subcategory that fire coal refuse.

*Fluidized bed combustion* means a process where a fuel is burned in a bed of granulated particles, which are maintained in a mobile suspension by the forward flow of air and combustion products.

Fossil fuel means natural gas, oil, coal, and any form of solid, liquid, or gaseous fuel derived from such material.

*Fuel cell* means a boiler type in which the fuel is dropped onto suspended fixed grates and is fired in a pile. The refractorylined fuel cell uses combustion air preheating and positioning of secondary and tertiary air injection ports to improve boiler efficiency. Fluidized bed, dutch oven, pile burner, hybrid suspension grate, and suspension burners are not part of the fuel cell subcategory.

*Fuel type* means each category of fuels that share a common name or classification. Examples include, but are not limited to, bituminous coal, sub-bituminous coal, lignite, anthracite, biomass, distillate oil, residual oil. Individual fuel types received from different suppliers are not considered new fuel types.

*Gaseous fuel* includes, but is not limited to, natural gas, process gas, landfill gas, coal derived gas, refinery gas, and biogas. Blast furnace gas and process gases that are regulated under another subpart of this <u>part, or part 60</u>, <u>part 61</u>, or <u>part 65 of this chapter</u>, are exempted from this definition.

*Heat input* means heat derived from combustion of fuel in a boiler or process heater and does not include the heat input from preheated combustion air, recirculated flue gases, returned condensate, or exhaust gases from other sources such as gas turbines, internal combustion engines, kilns, etc.

Heavy liquid includes residual oil and any other liquid fuel not classified as a light liquid.

*Hourly average* means the arithmetic average of at least four CMS data values representing the four 15-minute periods in an hour, or at least two 15-minute data values during an hour when CMS calibration, quality assurance, or maintenance activities are being performed.

*Hot water heater* means a closed vessel with a capacity of no more than 120 U.S. gallons in which water is heated by combustion of gaseous, liquid, or biomass/bio-based solid fuel and is withdrawn for use external to the vessel. Hot water boilers (i.e., not generating steam) combusting gaseous, liquid, or biomass fuel with a heat input capacity of less than 1.6 million Btu per hour are included in this definition. The 120 U.S. gallon capacity threshold to be considered a hot water heater is independent of the 1.6 MMBtu/hr heat input capacity threshold for hot water boilers. Hot water heater also means a tankless unit that provides on demand hot water.

*Hybrid suspension grate boiler* means a boiler designed with air distributors to spread the fuel material over the entire width and depth of the boiler combustion zone. The biomass fuel combusted in these units exceeds a moisture content of 40 percent on an as-fired annual heat input basis as demonstrated by monthly fuel analysis. The drying and much of the combustion of the fuel takes place in suspension, and the combustion is completed on the grate or floor of the boiler. Fluidized bed, dutch oven, and pile burner designs are not part of the hybrid suspension grate boiler design category.

*Industrial boiler* means a boiler used in manufacturing, processing, mining, and refining or any other industry to provide steam, hot water, and/or electricity.

Light liquid includes distillate oil, biodiesel, or vegetable oil.

*Limited-use boiler or process heater* means any boiler or process heater that burns any amount of solid, liquid, or gaseous fuels and has a federally enforceable annual capacity factor of no more than 10 percent.

*Liquid fuel* includes, but is not limited to, light liquid, heavy liquid, any form of liquid fuel derived from petroleum, used oil, liquid biofuels, biodiesel, and vegetable oil.

*Load fraction* means the actual heat input of a boiler or process heater divided by heat input during the performance test that established the minimum sorbent injection rate or minimum activated carbon injection rate, expressed as a fraction (*e.g.*, for 50 percent load the load fraction is 0.5). For boilers and process heaters that co-fire natural gas or refinery gas with a solid or liquid fuel, the load fraction is determined by the actual heat input of the solid or liquid fuel divided by heat input of the solid

or liquid fuel fired during the performance test (*e.g.*, if the performance test was conducted at 100 percent solid fuel firing, for 100 percent load firing 50 percent solid fuel and 50 percent natural gas the load fraction is 0.5).

*Major source for oil and natural gas production facilities,* as used in this subpart, shall have the same meaning as in <u>§ 63.2</u>, except that:

(1) Emissions from any oil or gas exploration or production well (with its associated equipment, as defined in this section), and emissions from any pipeline compressor station or pump station shall not be aggregated with emissions from other similar units to determine whether such emission points or stations are major sources, even when emission points are in a contiguous area or under common control;

(2) Emissions from processes, operations, or equipment that are not part of the same facility, as defined in this section, shall not be aggregated; and

(3) For facilities that are production field facilities, only HAP emissions from glycol dehydration units and storage vessels with the potential for flash emissions shall be aggregated for a major source determination. For facilities that are not production field facilities, HAP emissions from all HAP emission units shall be aggregated for a major source determination.

*Metal process furnaces* are a subcategory of process heaters, as defined in this subpart, which include natural gas-fired annealing furnaces, preheat furnaces, reheat furnaces, aging furnaces, heat treat furnaces, and homogenizing furnaces.

Million Btu (MMBtu) means one million British thermal units.

*Minimum activated carbon injection rate* means load fraction multiplied by the lowest hourly average activated carbon injection rate measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

*Minimum oxygen level* means the lowest hourly average oxygen level measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

*Minimum pressure drop* means the lowest hourly average pressure drop measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

*Minimum scrubber effluent pH* means the lowest hourly average sorbent liquid pH measured at the inlet to the wet scrubber according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable hydrogen chloride emission limit.

*Minimum scrubber liquid flow rate* means the lowest hourly average liquid flow rate (e.g., to the PM scrubber or to the acid gas scrubber) measured according to Table 7 to this subpart during the most recent performance stack test demonstrating compliance with the applicable emission limit.

*Minimum scrubber pressure drop* means the lowest hourly average scrubber pressure drop measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

Minimum sorbent injection rate means:

(1) The load fraction multiplied by the lowest hourly average sorbent injection rate for each sorbent measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limits; or

(2) For fluidized bed combustion not using an acid gas wet scrubber or dry sorbent injection control technology to comply with the HCl emission limit, the lowest average ratio of sorbent to sulfur measured during the most recent performance test.

*Minimum total secondary electric power* means the lowest hourly average total secondary electric power determined from the values of secondary voltage and secondary current to the electrostatic precipitator measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limits.

#### Natural gas means:

(1) A naturally occurring mixture of hydrocarbon and nonhydrocarbon gases found in geologic formations beneath the earth's surface, of which the principal constituent is methane; or

(2) Liquefied petroleum gas, as defined in ASTM D1835 (incorporated by reference, see  $\frac{63.14}{3}$ ); or

#### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

(3) A mixture of hydrocarbons that maintains a gaseous state at ISO conditions. Additionally, natural gas must either be composed of at least 70 percent methane by volume or have a gross calorific value between 35 and 41 megajoules (MJ) per dry standard cubic meter (950 and 1,100 Btu per dry standard cubic foot); or

(4) Propane or propane derived synthetic natural gas. Propane means a colorless gas derived from petroleum and natural gas, with the molecular structure  $C_3H_8$ .

*Opacity* means the degree to which emissions reduce the transmission of light and obscure the view of an object in the background.

*Operating day* means a 24-hour period between 12 midnight and the following midnight during which any fuel is combusted at any time in the boiler or process heater unit. It is not necessary for fuel to be combusted for the entire 24-hour period. For calculating rolling average emissions, an operating day does not include the hours of operation during startup or shutdown.

*Other combustor* means a unit designed to burn solid fuel that is not classified as a dutch oven, fluidized bed, fuel cell, hybrid suspension grate boiler, pulverized coal boiler, stoker, sloped grate, or suspension boiler as defined in this subpart.

Other gas 1 fuel means a gaseous fuel that is not natural gas or refinery gas and does not exceed a maximum mercury concentration of 40 micrograms/cubic meters of gas.

*Oxygen analyzer system* means all equipment required to determine the oxygen content of a gas stream and used to monitor oxygen in the boiler or process heater flue gas, boiler or process heater, firebox, or other appropriate location. This definition includes oxygen trim systems. The source owner or operator must install, calibrate, maintain, and operate the oxygen analyzer system in accordance with the manufacturer's recommendations.

*Oxygen trim system* means a system of monitors that is used to maintain excess air at the desired level in a combustion device over its operating load range. A typical system consists of a flue gas oxygen and/or CO monitor that automatically provides a feedback signal to the combustion air controller or draft controller.

*Particulate matter (PM)* means any finely divided solid or liquid material, other than uncombined water, as measured by the test methods specified under this subpart, or an approved alternative method.

*Period of gas curtailment or supply interruption* means a period of time during which the supply of gaseous fuel to an affected boiler or process heater is restricted or halted for reasons beyond the control of the facility. The act of entering into a contractual agreement with a supplier of natural gas established for curtailment purposes does not constitute a reason that is under the control of a facility for the purposes of this definition. An increase in the cost or unit price of natural gas due to normal market fluctuations not during periods of supplier delivery restriction does not constitute a period of natural gas curtailment or supply interruption. On-site gaseous fuel system emergencies or equipment failures qualify as periods of supply interruption when the emergency or failure is beyond the control of the facility.

*Pile burner* means a boiler design incorporating a design where the anticipated biomass fuel has a high relative moisture content. Grates serve to support the fuel, and underfire air flowing up through the grates provides oxygen for combustion, cools the grates, promotes turbulence in the fuel bed, and fires the fuel. The most common form of pile burning is the dutch oven.

*Process heater* means an enclosed device using controlled flame, and the unit's primary purpose is to transfer heat indirectly to a process material (liquid, gas, or solid) or to a heat transfer material (e.g., glycol or a mixture of glycol and water) for use in a process unit, instead of generating steam. Process heaters are devices in which the combustion gases do not come into direct contact with process materials. A device combusting solid waste, as defined in § 241.3 of this chapter, is not a process heater unless the device is exempt from the definition of a solid waste incineration unit as provided in section 129(g)(1) of the Clean Air Act. Process heaters do not include units used for comfort heat or space heat, food preparation for on-site consumption, or autoclaves. Waste heat process heaters are excluded from this definition.

*Pulverized coal boiler* means a boiler in which pulverized coal or other solid fossil fuel is introduced into an air stream that carries the coal to the combustion chamber of the boiler where it is fired in suspension.

Qualified energy assessor means:

(1) Someone who has demonstrated capabilities to evaluate energy savings opportunities for steam generation and major energy using systems, including, but not limited to:

(i) Boiler combustion management.

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- (ii) Boiler thermal energy recovery, including
- (A) Conventional feed water economizer,
- (B) Conventional combustion air preheater, and
- (C) Condensing economizer.
- (iii) Boiler blowdown thermal energy recovery.
- (iv) Primary energy resource selection, including
- (A) Fuel (primary energy source) switching, and
- (B) Applied steam energy versus direct-fired energy versus electricity.
- (v) Insulation issues.
- (vi) Steam trap and steam leak management.
- (vi) Condensate recovery.
- (viii) Steam end-use management.
- (2) Capabilities and knowledge includes, but is not limited to:

(i) Background, experience, and recognized abilities to perform the assessment activities, data analysis, and report preparation.

(ii) Familiarity with operating and maintenance practices for steam or process heating systems.

(iii) Additional potential steam system improvement opportunities including improving steam turbine operations and reducing steam demand.

(iv) Additional process heating system opportunities including effective utilization of waste heat and use of proper process heating methods.

(v) Boiler-steam turbine cogeneration systems.

(vi) Industry specific steam end-use systems.

*Refinery gas* means any gas that is generated at a petroleum refinery and is combusted. Refinery gas includes natural gas when the natural gas is combined and combusted in any proportion with a gas generated at a refinery. Refinery gas includes gases generated from other facilities when that gas is combined and combusted in any proportion with gas generated at a refinery.

*Regulated gas stream* means an offgas stream that is routed to a boiler or process heater for the purpose of achieving compliance with a standard under another subpart of this part or part 60, part 61, or part 65 of this chapter.

*Residential boiler* means a boiler used to provide heat and/or hot water and/or as part of a residential combined heat and power system. This definition includes boilers located at an institutional facility (e.g., university campus, military base, church grounds) or commercial/industrial facility (e.g., farm) used primarily to provide heat and/or hot water for:

(1) A dwelling containing four or fewer families; or

(2) A single unit residence dwelling that has since been converted or subdivided into condominiums or apartments.

*Residual oil* means crude oil, fuel oil that does not comply with the specifications under the definition of distillate oil, and all fuel oil numbers 4, 5, and 6, as defined by the American Society of Testing and Materials in ASTM D396-10 (incorporated by reference, see  $\frac{63.14(b)}{5}$ ).

Responsible official means responsible official as defined in § 70.2.

*Rolling average* means the average of all data collected during the applicable averaging period. For demonstration of compliance with a CO CEMS-based emission limit based on CO concentration a 30-day (10-day) rolling average is comprised of the average of all the hourly average concentrations over the previous 720 (240) operating hours calculated each operating day. To demonstrate compliance on a 30-day rolling average basis for parameters other than CO, you must indicate the basis of the 30-day rolling average period you are using for compliance, as discussed in § 63.7545(e)(2)(iii).

you indicate the 30 operating day basis, you must calculate a new average value each operating day and shall include the measured hourly values for the preceding 30 operating days. If you select the 720 operating hours basis, you must average of all the hourly average concentrations over the previous 720 operating hours calculated each operating day.

Secondary material means the material as defined in § 241.2 of this chapter.

*Shutdown* means the period in which cessation of operation of a boiler or process heater is initiated for any purpose. Shutdown begins when the boiler or process heater no longer supplies useful thermal energy (such as heat or steam) for heating, cooling, or process purposes and/or generates electricity or when no fuel is being fed to the boiler or process heater, whichever is earlier. Shutdown ends when the boiler or process heater no longer supplies useful thermal energy (such as steam or heat) for heating, cooling, or process purposes and/or generates electricity, and no fuel is being combusted in the boiler or process heater.

*Sloped grate* means a unit where the solid fuel is fed to the top of the grate from where it slides downwards; while sliding the fuel first dries and then ignites and burns. The ash is deposited at the bottom of the grate. Fluidized bed, dutch oven, pile burner, hybrid suspension grate, suspension burners, and fuel cells are not considered to be a sloped grate design.

Solid fossil fuel includes, but is not limited to, coal, coke, petroleum coke, and tire derived fuel.

Solid fuel means any solid fossil fuel or biomass or bio-based solid fuel.

#### Startup means:

(1) Either the first-ever firing of fuel in a boiler or process heater for the purpose of supplying useful thermal energy for heating and/or producing electricity, or for any other purpose, or the firing of fuel in a boiler after a shutdown event for any purpose. Startup ends when any of the useful thermal energy from the boiler or process heater is supplied for heating, and/or producing electricity, or for any other purpose, or

(2) The period in which operation of a boiler or process heater is initiated for any purpose. Startup begins with either the firstever firing of fuel in a boiler or process heater for the purpose of supplying useful thermal energy (such as steam or heat) for heating, cooling or process purposes, or producing electricity, or the firing of fuel in a boiler or process heater for any purpose after a shutdown event. Startup ends four hours after when the boiler or process heater supplies useful thermal energy (such as heat or steam) for heating, cooling, or process purposes, or generates electricity, whichever is earlier.

#### Steam output means:

(1) For a boiler that produces steam for process or heating only (no power generation), the energy content in terms of MMBtu of the boiler steam output,

(2) For a boiler that cogenerates process steam and electricity (also known as combined heat and power), the total energy output, which is the sum of the energy content of the steam exiting the turbine and sent to process in MMBtu and the energy of the electricity generated converted to MMBtu at a rate of 10,000 Btu per kilowatt-hour generated (10 MMBtu per megawatt-hour), and

(3) For a boiler that generates only electricity, the alternate output-based emission limits would be the appropriate emission limit from Table 1, 2, 14, or 15 to this subpart in units of pounds per million Btu heat input (lb per MWh).

(4) For a boiler that performs multiple functions and produces steam to be used for any combination of paragraphs (1), (2), and (3) of this definition that includes electricity generation of paragraph (3) of this definition, the total energy output, in terms of MMBtu of steam output, is the sum of the energy content of steam sent directly to the process and/or used for heating ( $S_1$ ), the energy content of turbine steam sent to process plus energy in electricity according to paragraph (2) of this definition ( $S_2$ ), and the energy content of electricity generated by a electricity only turbine as paragraph (3) of this definition ( $MW_3$ ) and would be calculated using Equation 1 to this definition. In the case of boilers supplying steam to one or more common headers,  $S_1$ ,  $S_2$ , and  $MW_{(3)}$  for each boiler would be calculated based on its (steam energy) contribution (fraction of total steam energy) to the common header.

# Equation 1 to the definition Steam Output

 $SO_M = S_1 + S_2 + (MW_{(3)} \times CFn)$  (Eq. 1)

Where:

SO<sub>M</sub> = Total steam output for multi-function boiler, MMBtu.

 $S_1$  = Energy content of steam sent directly to the process and/or used for heating, MMBtu.

 $S_2$  = Energy content of turbine steam sent to the process plus energy in electricity according to paragraph (2) of this definition, MMBtu.

 $MW_{(3)}$  = Electricity generated according to paragraph (3) of this definition, MWh.

CFn = Conversion factor for the appropriate subcategory for converting electricity generated according to paragraph (3) of this definition to equivalent steam energy, MMBtu/MWh.

CFn for emission limits for boilers in the unit designed to burn solid fuel subcategory = 10.8.

CFn PM and CO emission limits for boilers in one of the subcategories of units designed to burn coal = 11.7.

CFn PM and CO emission limits for boilers in one of the subcategories of units designed to burn biomass = 12.1.

CFn for emission limits for boilers in one of the subcategories of units designed to burn liquid fuel = 11.2.

CFn for emission limits for boilers in the unit designed to burn gas 2 (other) subcategory = 6.2.

*Stoker* means a unit consisting of a mechanically operated fuel feeding mechanism, a stationary or moving grate to support the burning of fuel and admit under-grate air to the fuel, an overfire air system to complete combustion, and an ash discharge system. This definition of stoker includes air swept stokers. There are two general types of stokers: Underfeed and overfeed. Overfeed stokers include mass feed and spreader stokers. Fluidized bed, dutch oven, pile burner, hybrid suspension grate, suspension burners, and fuel cells are not considered to be a stoker design.

Stoker/sloped grate/other unit designed to burn kiln dried biomass means the unit is in the units designed to burn biomass/bio-based solid subcategory that is either a stoker, sloped grate, or other combustor design and is not in the stoker/sloped grate/other units designed to burn wet biomass subcategory.

Stoker/sloped grate/other unit designed to burn wet biomass means the unit is in the units designed to burn biomass/biobased solid subcategory that is either a stoker, sloped grate, or other combustor design and any of the biomass/bio-based solid fuel combusted in the unit exceeds 20 percent moisture on an annual heat input basis.

*Suspension burner* means a unit designed to fire dry biomass/biobased solid particles in suspension that are conveyed in an airstream to the furnace like pulverized coal. The combustion of the fuel material is completed on a grate or floor below. The biomass/biobased fuel combusted in the unit shall not exceed 20 percent moisture on an annual heat input basis. Fluidized bed, dutch oven, pile burner, and hybrid suspension grate units are not part of the suspension burner subcategory.

*Temporary boiler* means any gaseous or liquid fuel boiler or process heater that is designed to, and is capable of, being carried or moved from one location to another by means of, for example, wheels, skids, carrying handles, dollies, trailers, or platforms. A boiler or process heater is not a temporary boiler or process heater if any one of the following conditions exists:

(1) The equipment is attached to a foundation.

(2) The boiler or process heater or a replacement remains at a location within the facility and performs the same or similar function for more than 12 consecutive months, unless the regulatory agency approves an extension. An extension may be granted by the regulating agency upon petition by the owner or operator of a unit specifying the basis for such a request. Any temporary boiler or process heater that replaces a temporary boiler or process heater at a location and performs the same or similar function will be included in calculating the consecutive time period.

(3) The equipment is located at a seasonal facility and operates during the full annual operating period of the seasonal facility, remains at the facility for at least 2 years, and operates at that facility for at least 3 months each year.

(4) The equipment is moved from one location to another within the facility but continues to perform the same or similar function and serve the same electricity, process heat, steam, and/or hot water system in an attempt to circumvent the residence time requirements of this definition.

*Total selected metals (TSM)* means the sum of the following metallic hazardous air pollutants: arsenic, beryllium, cadmium, chromium, lead, manganese, nickel and selenium.

#### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

Traditional fuel means the fuel as defined in § 241.2 of this chapter.

*Tune-up* means adjustments made to a boiler or process heater in accordance with the procedures outlined in § 63.7540(a)(10).

Ultra low sulfur liquid fuel means a distillate oil that has less than or equal to 15 ppm sulfur.

*Unit designed to burn biomass/bio-based solid subcategory* includes any boiler or process heater that burns at least 10 percent biomass or bio-based solids on an annual heat input basis in combination with solid fossil fuels, liquid fuels, or gaseous fuels.

*Unit designed to burn coal/solid fossil fuel subcategory* includes any boiler or process heater that burns any coal or other solid fossil fuel alone or at least 10 percent coal or other solid fossil fuel on an annual heat input basis in combination with liquid fuels, gaseous fuels, or less than 10 percent biomass and bio-based solids on an annual heat input basis.

*Unit designed to burn gas 1 subcategory* includes any boiler or process heater that burns only natural gas, refinery gas, and/or other gas 1 fuels. Gaseous fuel boilers and process heaters that burn liquid fuel for periodic testing of liquid fuel, maintenance, or operator training, not to exceed a combined total of 48 hours during any calendar year, are included in this definition. Gaseous fuel boilers and process heaters that burn liquid fuel during periods of gas curtailment or gas supply interruptions of any duration are also included in this definition.

Unit designed to burn gas 2 (other) subcategory includes any boiler or process heater that is not in the unit designed to burn gas 1 subcategory and burns any gaseous fuels either alone or in combination with less than 10 percent coal/solid fossil fuel, and less than 10 percent biomass/bio-based solid fuel on an annual heat input basis, and no liquid fuels. Gaseous fuel boilers and process heaters that are not in the unit designed to burn gas 1 subcategory and that burn liquid fuel for periodic testing of liquid fuel, maintenance, or operator training, not to exceed a combined total of 48 hours during any calendar year, are included in this definition. Gaseous fuel boilers and process heaters that are not in the unit designed to gas curtailment or gas supply interruption of any duration are also included in this definition.

Unit designed to burn heavy liquid subcategory means a unit in the unit designed to burn liquid subcategory where at least 10 percent of the heat input from liquid fuels on an annual heat input basis comes from heavy liquids.

Unit designed to burn light liquid subcategory means a unit in the unit designed to burn liquid subcategory that is not part of the unit designed to burn heavy liquid subcategory.

*Unit designed to burn liquid subcategory* includes any boiler or process heater that burns any liquid fuel, but less than 10 percent coal/solid fossil fuel and less than 10 percent biomass/bio-based solid fuel on an annual heat input basis, either alone or in combination with gaseous fuels. Units in the unit design to burn gas 1 or unit designed to burn gas 2 (other) subcategories that burn liquid fuel for periodic testing of liquid fuel, maintenance, or operator training, not to exceed a combined total of 48 hours during any calendar year are not included in this definition. Units in the unit design to burn gas 1 or unit designed to burn gas 2 (other) subcategories during periods of gas curtailment or gas supply interruption of any duration are also not included in this definition.

*Unit designed to burn liquid fuel that is a non-continental unit* means an industrial, commercial, or institutional boiler or process heater meeting the definition of the unit designed to burn liquid subcategory located in the State of Hawaii, the Virgin Islands, Guam, American Samoa, the Commonwealth of Puerto Rico, or the Northern Mariana Islands.

*Unit designed to burn solid fuel subcategory* means any boiler or process heater that burns only solid fuels or at least 10 percent solid fuel on an annual heat input basis in combination with liquid fuels or gaseous fuels.

*Useful thermal energy* means energy (*i.e.*, steam, hot water, or process heat) that meets the minimum operating temperature, flow, and/or pressure required by any energy use system that uses energy provided by the affected boiler or process heater.

Vegetable oil means oils extracted from vegetation.

*Voluntary Consensus Standards or VCS* mean technical standards (*e.g.*, materials specifications, test methods, sampling procedures, business practices) developed or adopted by one or more voluntary consensus bodies. EPA/Office of Air Quality Planning and Standards, by precedent, has only used VCS that are written in English. Examples of VCS bodies are: American Society of Testing and Materials (ASTM 100 Barr Harbor Drive, P.O. Box CB700, West Conshohocken, Pennsylvania 19428-B2959, (800) 262-1373, <u>http://www.astm.org</u>), American Society of Mechanical Engineers (ASME ASME, Three Park Avenue, New York, NY 10016-5990, (800) 843-2763, <u>http://www.asme.org</u>), International Standards Organization (ISO

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11, <u>http://www.iso.org/iso/home.htm</u>), Standards Australia (AS Level 10, The Exchange Centre, 20 Bridge Street, Sydney, GPO Box 476, Sydney NSW 2001, + 61 2 9237 6171 <u>http://www.stadards.org.au</u>), British Standards Institution (BSI, 389 Chiswick High Road, London, W4 4AL, United Kingdom, + 44 (0)20 8996 9001, <u>http://www.bsigroup.com</u>), Canadian Standards Association (CSA 5060 Spectrum Way, Suite 100, Mississauga, Ontario L4W 5N6, Canada, 800-463-6727, <u>http://www.csa.ca</u>), European Committee for Standardization (CEN CENELEC Management Centre Avenue Marnix 17 B-1000 Brussels, Belgium + 32 2 550 08 11, <u>http://www.cen.eu/cen</u>), and German Engineering Standards (VDI VDI Guidelines Department, P.O. Box 10 11 39 40002, Duesseldorf, Germany, + 49 211 6214-230, <u>http://www.vdi.eu</u>). The types of standards that are not considered VCS are standards developed by: The United States, *e.g.*, California (CARB) and Texas (TCEQ); industry groups, such as American Petroleum Institute (API), Gas Processors Association (GPA), and Gas Research Institute (GRI); and other branches of the U.S. government, *e.g.*, Department of Defense (DOD) and Department of Transportation (DOT). This does not preclude EPA from using standards developed by groups that are not VCS bodies within their rule. When this occurs, EPA has done searches and reviews for VCS equivalent to these non-EPA methods.

*Waste heat boiler* means a device that recovers normally unused energy (i.e., hot exhaust gas) and converts it to usable heat. Waste heat boilers are also referred to as heat recovery steam generators. Waste heat boilers are heat exchangers generating steam from incoming hot exhaust gas from an industrial (e.g., thermal oxidizer, kiln, furnace) or power (e.g., combustion turbine, engine) equipment. Duct burners are sometimes used to increase the temperature of the incoming hot exhaust gas.

*Waste heat process heater* means an enclosed device that recovers normally unused energy (i.e., hot exhaust gas) and converts it to usable heat. Waste heat process heaters are also referred to as recuperative process heaters. This definition includes both fired and unfired waste heat process heaters.

*Wet scrubber* means any add-on air pollution control device that mixes an aqueous stream or slurry with the exhaust gases from a boiler or process heater to control emissions of particulate matter or to absorb and neutralize acid gases, such as hydrogen chloride. A wet scrubber creates an aqueous stream or slurry as a byproduct of the emissions control process.

*Work practice standard* means any design, equipment, work practice, or operational standard, or combination thereof, that is promulgated pursuant to section 112(h) of the Clean Air Act.

[<u>78 FR 15664</u>, Mar. 21, 2011, as amended at <u>78 FR 7163</u>, Jan. 31, 2013; <u>80 FR 72817</u>, Nov. 20, 2015; <u>87 FR 60846</u>, Oct. 6, 2022]

#### Table 1 to Subpart DDDDD of Part 63—Emission Limits for New or Reconstructed Boilers and Process Heaters <sup>c</sup>

As stated in  $\S$  63.7500, you must comply with the following applicable emission limits:

Table 1 to Subpart DDDDD of Part 63—Emission Limits for New or Reconstructed Boilers and Process Heaters <sup>c</sup> [Units with heat input capacity of 10 million Btu per hour or greater]

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling
1. Units in all subcategories designed to burn solid fuel	a. HCl	2.1E-04 <sup>a</sup> lb per MMBtu of heat input	2.9E-04 <sup>a</sup> lb per MMBtu of steam output or 2.7E-03 <sup>a</sup> lb per MWh	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.
	b. Mercury	8.0E-07ª lb per MMBtu of heat input	8.7E-07 <sup>a</sup> lb per MMBtu of steam output or 1.1E-05 <sup>a</sup> lb per MWh	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.
2. Units designed to	a. Filterable	1.1E-03 lb per MMBtu of	1.1E-03 lb per MMBtu	Collect a minimum of 3 dscm

Table 1 to Subpart DDDDD of Part 63—Emission Limits for New or Reconstructed Boilers and Process Heaters <sup>c</sup> [Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling
burn coal/solid fossil fuel	PM (or TSM)	heat input; or (2.3E-05 lb per MMBtu of heat input)	of steam output or 1.4E-02 lb per MWh; or (2.7E-05 lb per MMBtu of steam output or 2.9E-04 lb per MWh)	per run.
3. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
4. Stokers/others designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3-percent oxygen <sup>d</sup> , 30-day rolling average)	0.12 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
5. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
6. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	1.2E-01 lb per MMBtu of steam output or 1.5 lb per MWh; 3-run average	1 hr minimum sampling time.
7. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	590 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (390 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	6.1E-01 lb per MMBtu of steam output or 6.5 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or	1.3E-02 lb per MMBtu of heat input; or (2.6E-05 lb per	1.4E-02 lb per MMBtu of steam output or	Collect a minimum of 2 dscm per run.

Table 1 to Subpar	rt DDDDD of [ [Units wi	Part 63—Emission Limits for N th heat input capacity of 10 mi	New or Reconstructed Bo llion Btu per hour or grea	ilers and Process Heaters <sup>°</sup> ter]
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling
	TSM)	MMBtu of heat input)	1.9E-01 lb per MWh; or (2.7E-05 lb per MMBtu of steam output or 3.7E-04 lb per MWh)	
8. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	460 ppm by volume on a dry basis corrected to 3-percent oxygen	4.3E-01 lb per MMBtu of steam output or 5.1 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (5.0E-03 lb per MMBtu of heat input)	3.5E-02 lb per MMBtu of steam output or 4.2E-01 lb per MWh; or (5.2E-03 lb per MMBtu of steam output or 7.0E-02 lb per MWh)	Collect a minimum of 2 dscm per run.
9. Fluidized bed units designed to burn biomass/bio-based solids	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	1.3E-01 lb per MMBtu of steam output or 1.5 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	4.1E-03 lb per MMBtu of heat input; or (8.4E-06 <sup>a</sup> lb per MMBtu of heat input)	5.0E-03 lb per MMBtu of steam output or 5.8E-02 lb per MWh; or (1.1E-05 <sup>a</sup> lb per MMBtu of steam output or 1.2E-04 <sup>a</sup> lb per MWh)	Collect a minimum of 3 dscm per run.
10. Suspension burners designed to burn biomass/bio- based solids	a. CO (or CEMS)	220 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3- percent oxygen, <sup>d</sup> 10-day rolling average)	0.18 lb per MMBtu of steam output or 2.5 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (8.0E-03 lb per MMBtu of heat input)	3.1E-02 lb per MMBtu of steam output or 4.2E-01 lb per MWh; or (8.1E-03 lb per MMBtu of steam output or 1.2E-01 lb per	Collect a minimum of 2 dscm per run.

Table 1 to Subpar	rt DDDDD of [ [Units wi	Part 63—Emission Limits for N th heat input capacity of 10 mi	New or Reconstructed Bo Ilion Btu per hour or grea	ilers and Process Heaters <sup>c</sup> ter]
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling
			MWh)	
11. Dutch Ovens/Pile burners designed to burn biomass/bio- based solids	a. CO (or CEMS)	330 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 10-day rolling average)	3.5E-01 lb per MMBtu of steam output or 3.6 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.5E-03 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input)	3.4E-03 lb per MMBtu of steam output or 3.5E-02 lb per MWh; or (5.2E-05 lb per MMBtu of steam output or 5.5E-04 lb per MWh)	Collect a minimum of 3 dscm per run.
12. Fuel cell units designed to burn biomass/bio-based solids	a. CO	910 ppm by volume on a dry basis corrected to 3-percent oxygen	1.1 lb per MMBtu of steam output or 1.0E+01 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-02 lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	2.0E-02 lb per MMBtu of steam output or 1.6E-01 lb per MWh; or (5.1E-05 lb per MMBtu of steam output or 4.1E-04 lb per MWh)	Collect a minimum of 2 dscm per run.
13. Hybrid suspension grate boiler designed to burn biomass/bio- based solids	a. CO (or CEMS)	180 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3-percent oxygen <sup>d</sup> , 30-day rolling average)	0.22 lb per MMBtu of steam output or 2.0 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.6E-02 lb per MMBtu of heat input; or (4.4E-04 lb per MMBtu of heat input)	3.3E-02 lb per MMBtu of steam output or 3.7E-01 lb per MWh; or (5.5E-04 lb per MMBtu of steam output or 6.2E-03 lb per MWh)	Collect a minimum of 3 dscm per run.
14. Units designed to burn liquid fuel	a. HCl	1.5E-04 <sup>a</sup> lb per MMBtu of heat input	1.7E-04 <sup>a</sup> lb per MMBtu of steam output or 2.1E-03 <sup>a</sup> lb per MWh	For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240

Table 1 to Subpar	rt DDDDD of I [Units wi	Part 63—Emission Limits for M th heat input capacity of 10 mi	New or Reconstructed Bo llion Btu per hour or grea	ilers and Process Heaters <sup>c</sup> ter]
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling
				liters per run.
	b. Mercury	4.8E-07ª lb per MMBtu of heat input	5.3E-07 <sup>a</sup> lb per MMBtu of steam output or 6.7E-06 <sup>a</sup> lb per MWh	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.
15. Units designed to burn heavy liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average	0.13 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.9E-03 lb per MMBtu of heat input; or (6.1E-06 <sup>a</sup> lb per MMBtu of heat input)	2.1E-03 lb per MMBtu of steam output or 2.7E-02 lb per MWh; or (6.7E-6 <sup>a</sup> lb per MMBtu of steam output or 8.5E-5 <sup>a</sup> lb per MWh)	Collect a minimum of 3 dscm per run.
16. Units designed to burn light liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen	0.13 lb per MMBtu of steam output or 1.4 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-03 <sup>a</sup> lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	1.2E-03 <sup>a</sup> lb per MMBtu of steam output or 1.6E-02 <sup>a</sup> lb per MWh; or (3.2E-05 lb per MMBtu of steam output or 4.0E-04 lb per MWh)	Collect a minimum of 3 dscm per run.
17. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average based on stack test	0.13 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)	2.5E-02 lb per MMBtu of steam output or 3.2E-01 lb per MWh; or (9.4E-04 lb per MMBtu of steam output or 1.2E-02 lb per MWh)	Collect a minimum of 4 dscm per run.
18. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen	0.16 lb per MMBtu of steam output or 1.0 lb per MWh	1 hr minimum sampling time.

Table 1 to Subpart DDDDD of Part 63—Emission Limits for New or Reconstructed Boilers and Process Heaters ° [Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling
	b. HCl	1.7E-03 lb per MMBtu of heat input	2.9E-03 lb per MMBtu of steam output or 1.8E-02 lb per MWh	For M26A, collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	1.4E-05 lb per MMBtu of steam output or 8.3E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.
	d. Filterable PM (or TSM)	7.3E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	1.3E-02 lb per MMBtu of steam output or 7.6E-02 lb per MWh; or (3.5E-04 lb per MMBtu of steam output or 2.2E-03 lb per MWh)	Collect a minimum of 3 dscm per run.

<sup>a</sup> If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to  $\frac{63.7515}{10}$  if all of the other provisions of  $\frac{63.7515}{10}$  are met. For all other pollutants that do not contain a footnote "a", your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

<sup>b</sup> Incorporated by reference, see  $\S$  <u>63.14</u>.

<sup>c</sup> If your affected source is a new or reconstructed affected source that commenced construction or reconstruction after June 4, 2010, and before April 1, 2013, you may comply with the emission limits in Table 11, 12, or 13 to this subpart until January 31, 2016. On and after January 31, 2016, but before October 6, 2025 you may comply with the emission limits in Table 14 to this subpart. On and after October 6, 2025 you must comply with the emission limits in this Table 1.

<sup>d</sup> An owner or operator may determine compliance with the carbon monoxide emissions limit using CO<sub>2</sub> as a diluent correction in place of oxygen as described in § 63.7525(a)(1). EPA Method 19 F-factors in <u>40 CFR part 60, appendix A</u>-7, and EPA Method 19 equations in <u>40 CFR part 60, appendix A</u>-7, must be used to generate the appropriate CO<sub>2</sub> correction percentage for the fuel type burned in the unit and must also take into account that the 3-percent oxygen correction is to be done on a dry basis. The methodology must account for any CO<sub>2</sub> being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. This methodology must be detailed in the site-specific monitoring plan developed according to § 63.7505(d).

[<u>87 FR 60847</u>, Oct. 6, 2022]

#### Table 2 to Subpart DDDDD of Part 63—Emission Limits for Existing Boilers and Process Heaters<sup>d</sup>

As stated in § 63.7500, you must comply with the following applicable emission limits:

[Units with heat input capacity of 10 million Btu per hour or greater]

If your boiler or	For the	The emissions must not	The emissions must not exceed the	Using this spacified sampling
process heater is in this subcategory	following pollutants . 	emission limits, except during startup and shutdown	following alternative output-based limits, except during startup and shutdown	volume or test run duration .
1. Units in all subcategories designed to burn solid fuel	a. HCl	2.0E-02 lb per MMBtu of heat input	2.3E-02 lb per MMBtu of steam output or 0.26 lb per MWh	For M26A, collect a minimum of 1 dscm per run; for M26, collect a minimum of 120 liters per run.
	b. Mercury	5.4E-06 lb per MMBtu of heat input	6.2E-06 lb per MMBtu of steam output or 6.9E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.
2. Units design to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	3.9E-02 lb per MMBtu of heat input; or (5.3E-05 lb per MMBtu of heat input)	4.1E-02 lb per MMBtu of steam output or 4.8E-01 lb per MWh; or (5.6E-05 lb per MMBtu of steam output or 6.5E-04 lb per MWh)	Collect a minimum of 2 dscm per run.
3. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>e</sup> 30-day rolling average)	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
4. Stokers/others designed to burn coal/solid fossil fuel	a. CO (or CEMS)	150 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 30-day rolling average)	0.14 lb per MMBtu of steam output or 1.6 lb per MWh; 3-run average	1 hr minimum sampling time.
5. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 30-day rolling average)	0.12 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
6. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 30-day rolling average)	1.3E-01 lb per MMBtu of steam output or 1.5 lb per MWh; 3-run average	1 hr minimum sampling time.
7. Stokers/sloped	a. CO (or	1,100 ppm by volume on a	1.1 lb per MMBtu of	1 hr minimum sampling time.

[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants .	The emissions must not exceed the following emission limits, except during startup and shutdown	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 
grate/others designed to burn wet biomass fuel	CEMS)	dry basis corrected to 3- percent oxygen, 3-run average; or (720 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 30-day rolling average)	steam output or 13 lb per MWh; 3-run average	
	b. Filterable PM (or TSM)	3.4E-02 lb per MMBtu of heat input; or (2.0E-04 lb per MMBtu of heat input)	4.0E-02 lb per MMBtu of steam output or 4.8E-01 lb per MWh; or (2.4E-04 lb per MMBtu of steam output or 2.8E-03 lb per MWh)	Collect a minimum of 2 dscm per run.
8. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	460 ppm by volume on a dry basis corrected to 3-percent oxygen	4.2E-01 lb per MMBtu of steam output or 5.1 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.2E-01 lb per MMBtu of heat input; or (5.0E-03 lb per MMBtu of heat input)	3.7E-01 lb per MMBtu of steam output or 4.5 lb per MWh; or (5.9E- 03 lb per MMBtu of steam output or 7.0E-02 lb per MWh)	Collect a minimum of 1 dscm per run.
9. Fluidized bed units designed to burn biomass/bio-based solid	a. CO (or CEMS)	210 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>e</sup> 30-day rolling average)	2.1E-01 lb per MMBtu of steam output or 2.3 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	7.4E-03 lb per MMBtu of heat input; or (6.4E-05 lb per MMBtu of heat input)	9.2E-03 lb per MMBtu of steam output or 0.11 lb per MWh; or (8.0E- 05 lb per MMBtu of steam output or 9.0E-04 lb per MWh)	Collect a minimum of 1 dscm per run.
10. Suspension burners designed to burn biomass/bio- based solid	a. CO (or CEMS)	2,400 ppm by volume on a dry basis corrected to 3- percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 10-day rolling average)	1.9 lb per MMBtu of steam output or 27 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable	4.1E-02 lb per MMBtu of	4.2E-02 lb per MMBtu	Collect a minimum of 2 dscm

	[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants . 	The emissions must not exceed the following emission limits, except during startup and shutdown	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 	
	PM (or TSM)	heat input; or (8.0E-03 lb per MMBtu of heat input)	of steam output or 5.8E-01 lb per MWh; or (8.1E-03 lb per MMBtu of steam output or 0.12 lb per MWh)	per run.	
11. Dutch Ovens/Pile burners designed to burn biomass/bio- based solid	a. CO (or CEMS)	770 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 10-day rolling average)	8.4E-01 lb per MMBtu of steam output or 8.4 lb per MWh; 3-run average	1 hr minimum sampling time.	
	b. Filterable PM (or TSM)	1.8E-01 lb per MMBtu of heat input; or (2.0E-03 lb per MMBtu of heat input)	2.5E-01 lb per MMBtu of steam output or 2.6 lb per MWh; or (2.8E- 03 lb per MMBtu of steam output or 2.8E-02 lb per MWh)	Collect a minimum of 1 dscm per run.	
12. Fuel cell units designed to burn biomass/bio-based solid	a. CO	1,100 ppm by volume on a dry basis corrected to 3- percent oxygen	2.4 lb per MMBtu of steam output or 12 lb per MWh	1 hr minimum sampling time.	
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (5.8E-03 lb per MMBtu of heat input)	5.5E-02 lb per MMBtu of steam output or 2.8E-01 lb per MWh; or (1.6E-02 lb per MMBtu of steam output or 8.1E-02 lb per MWh)	Collect a minimum of 2 dscm per run.	
13. Hybrid suspension grate units designed to burn biomass/bio- based solid	a. CO (or CEMS)	3,500 ppm by volume on a dry basis corrected to 3- percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 30-day rolling average)	3.5 lb per MMBtu of steam output or 39 lb per MWh; 3-run average	1 hr minimum sampling time.	
	b. Filterable PM (or TSM)	4.4E-01 lb per MMBtu of heat input; or (4.5E-04 lb per MMBtu of heat input)	5.5E-01 lb per MMBtu of steam output or 6.2 lb per MWh; or (5.7E- 04 lb per MMBtu of steam output or 6.3E-03 lb per MWh)	Collect a minimum of 1 dscm per run.	
14. Units designed to burn liquid fuel	a. HCl	1.1E-03 lb per MMBtu of heat input	1.4E-03 lb per MMBtu of steam output or 1.6E-02 lb per MWh	For M26A, collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters	

#### [Units with heat input capacity of 10 million Btu per hour or greater] The emissions must The emissions must not If your boiler or For the not exceed the Using this specified sampling exceed the following process heater is in following following alternative emission limits, except volume or test run duration. this pollutants. output-based limits, during startup and subcategory ... except during startup . . shutdown . . . and shutdown . . . per run. For M29, collect a minimum of 3 dscm per run; for M30A or 8.8E-07 lb per MMBtu M30B collect a minimum 7.3E-07 lb per MMBtu of sample as specified in the b. Mercury of steam output or heat input 1.1E-05 lb per MWh method, for ASTM D6784<sup>b</sup> collect a minimum of 2 dscm. 0.13 lb per MMBtu of 130 ppm by volume on a dry steam output or 1.4 lb 15. Units designed to a. CO basis corrected to 3-percent 1 hr minimum sampling time. burn heavy liquid fuel per MWh; 3-run oxygen, 3-run average average 7.2E-02 lb per MMBtu of steam output or b. Filterable 5.9E-02 lb per MMBtu of 8.2E-01 lb per MWh; or Collect a minimum of 1 dscm PM (or heat input; or (2.0E-04 lb per (2.5E-04 lb per MMBtu per run. TSM) MMBtu of heat input) of steam output or 2.8E-03 lb per MWh) 0.13 lb per MMBtu of 130 ppm by volume on a dry 16. Units designed to a. CO basis corrected to 3-percent steam output or 1.4 lb 1 hr minimum sampling time. burn light liquid fuel per MWh oxygen 9.6E-03 lb per MMBtu of steam output or b. Filterable 7.9E-03 lb per MMBtu of 1.1E-01 lb per MWh; or Collect a minimum of 3 dscm PM (or heat input; or (6.2E-05 lb per (7.5E-05 lb per MMBtu per run. TSM) MMBtu of heat input) of steam output or 8.6E-04 lb per MWh) 17. Units designed to 130 ppm by volume on a dry 0.13 lb per MMBtu of burn liquid fuel that steam output or 1.4 lb basis corrected to 3-percent a. CO 1 hr minimum sampling time. per MWh; 3-run are non-continental oxygen, 3-run average based units on stack test average 2.7E-01 lb per MMBtu of steam output or 3.1 b. Filterable 2.2E-01 lb per MMBtu of lb per MWh; or (1.1E-Collect a minimum of 2 dscm heat input; or (8.6E-04 lb per PM (or 03 lb per MMBtu of per run. TSM) MMBtu of heat input) steam output or 1.2E-02 lb per MWh) 0.16 lb per MMBtu of 18. Units designed to 130 ppm by volume on a dry burn gas 2 (other) a. CO basis corrected to 3-percent steam output or 1.0 lb 1 hr minimum sampling time. per MWh gases oxygen For M26A, collect a minimum 2.9E-03 lb per MMBtu 1.7E-03 lb per MMBtu of of 2 dscm per run; for M26, b. HCl of steam output or collect a minimum of 240 liters heat input 1.8E-02 lb per MWh per run.

[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants . 	The emissions must not exceed the following emission limits, except during startup and shutdown	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 
	c. Mercury	7.9E-06 lb per MMBtu of heat input	1.4E-05 lb per MMBtu of steam output or 8.3E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 2 dscm.
	d. Filterable PM (or TSM)	7.3E-03 lb per MMBtu of heat input or (2.1E-04 lb per MMBtu of heat input)	1.3E-02 lb per MMBtu of steam output or 7.6E-02 lb per MWh; or (3.5E-04 lb per MMBtu of steam output or 2.2E-03 lb per MWh)	Collect a minimum of 3 dscm per run.

<sup>a</sup> If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to  $\frac{63.7515}{10}$  if all of the other provisions of  $\frac{63.7515}{10}$  are met. For all other pollutants that do not contain a footnote a, your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

<sup>b</sup> Incorporated by reference, see  $\S$  <u>63.14</u>.

<sup>c</sup> An owner or operator may determine compliance with the carbon monoxide emissions limit be determined using CO<sub>2</sub> as a diluent correction in place of oxygen as described in § 63.7525(a)(1). EPA Method 19 F-factors in 40 CFR part 60, appendix A-7, and EPA Method 19 equations in 40 CFR part 60, appendix A-7, must be used to generate the appropriate CO<sub>2</sub> correction percentage for the fuel type burned in the unit and must also take into account that the 3-percent oxygen correction is to be done on a dry basis. The methodology must account for any CO<sub>2</sub> being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. This methodology must be detailed in the site-specific monitoring plan developed according to § 63.7505(d).

<sup>d</sup> Before October 6, 2025 you may comply with the emission limits in Table 15 to this subpart. On and after October 6, 2025], you must comply with the emission limits in this Table 2.

[87 FR 60849, Oct. 6, 2022]

#### Table 3 to Subpart DDDDD of Part 63—Work Practice Standards

As stated in  $\S$  63.7500, you must comply with the following applicable work practice standards:

If your unit is	You must meet the following
1. A new or existing boiler or process heater with a continuous oxygen trim system that maintains an optimum air to fuel ratio, or a heat input capacity of less than or equal to 5 million Btu per hour in any of the following subcategories: unit designed to burn gas 1; unit designed to burn gas 2 (other); or unit designed to burn light liquid, or a limited use boiler or process heater	Conduct a tune-up of the boiler or process heater every 5 years as specified in $\frac{63.7540}{2}$ .
2. A new or existing boiler or process heater without a continuous oxygen trim system and with heat input capacity of less than 10 million Btu per hour in the unit designed to	Conduct a tune-up of the boiler or process heater biennially as specified in $\frac{63.7540}{2}$ .

If your unit is	You must meet the following
burn heavy liquid or unit designed to burn solid fuel subcategories; or a new or existing boiler or process heater with heat input capacity of less than 10 million Btu per hour, but greater than 5 million Btu per hour, in any of the following subcategories: unit designed to burn gas 1; unit designed to burn gas 2 (other); or unit designed to burn light liquid	
3. A new or existing boiler or process heater without a continuous oxygen trim system and with heat input capacity of 10 million Btu per hour or greater	Conduct a tune-up of the boiler or process heater annually as specified in <u>§ 63.7540</u> . Units in either the Gas 1 or Metal Process Furnace subcategories will conduct this tune-up as a work practice for all regulated emissions under this subpart. Units in all other subcategories will conduct this tune-up as a work practice for dioxins/furans.
4. An existing boiler or process heater located at a major source facility, not including limited use units	Must have a one-time energy assessment performed by a qualified energy assessor. An energy assessment completed on or after January 1, 2008, that meets or is amended to meet the energy assessment requirements in this table, satisfies the energy assessment requirement. A facility that operated under an energy management program developed according to the ENERGY STAR guidelines for energy management or compatible with ISO 50001 for at least one year between January 1, 2008 and the compliance date specified in § $63.7495$ that includes the affected units also satisfies the energy assessment requirement. The energy assessment must include the following with extent of the evaluation for items a. to e. appropriate for the on-site technical hours listed in § $63.7575$ :
	a. A visual inspection of the boiler or process heater system.
	b. An evaluation of operating characteristics of the boiler or process heater systems, specifications of energy using systems, operating and maintenance procedures, and unusual operating constraints.
	c. An inventory of major energy use systems consuming energy from affected boilers and process heaters and which are under the control of the boiler/process heater owner/operator.
	d. A review of available architectural and engineering plans, facility operation and maintenance procedures and logs, and fuel usage.
	e. A review of the facility's energy management program and provide recommendations for improvements consistent with the definition of energy management program, if identified.
	f. A list of cost-effective energy conservation measures that are within the facility's control.
	g. A list of the energy savings potential of the energy conservation measures identified.
	h. A comprehensive report detailing the ways to improve efficiency, the cost of specific improvements, benefits, and the time frame for recouping those investments.
5. An existing or new boiler or process heater subject to emission limits in Table 1 or 2 or 11 through 15 to this subpart during startup	<ul><li>a. You must operate all CMS during startup.</li><li>b. For startup of a boiler or process heater, you must use one or a combination of the following clean fuels: natural gas,</li></ul>

You must meet the following
synthetic natural gas, propane, other Gas 1 fuels, distillate oil, syngas, ultra-low sulfur diesel, fuel oil-soaked rags, kerosene, hydrogen, paper, cardboard, refinery gas, liquefied petroleum gas, clean dry biomass, and any fuels meeting the appropriate HCl, mercury and TSM emission standards by fuel analysis.
c. You have the option of complying using either of the following work practice standards. (1) If you choose to comply using paragraph (1) of the definition of "startup" in § 63.7575, once you start firing fuels that are not clean fuels you must vent emissions to the main stack(s) and engage all of the applicable control devices except limestone injection in fluidized bed combustion (FBC) boilers, dry scrubber, fabric filter, and selective catalytic reduction (SCR). You must start your limestone injection in FBC boilers, dry scrubber, fabric filter, and SCR systems as expeditiously as possible. Startup ends when steam or heat is supplied for any purpose, OR (2) If you choose to comply using paragraph (2) of the definition of "startup" in § 63.7575, once you start to feed fuels that are not clean fuels, you must vent emissions to the main stack(s) and engage all of the applicable control devices so as to comply with the emission limits within 4 hours of start of supplying useful thermal energy. You must engage and operate PM control within one hour of first feeding fuels that are not clean fuels <sup>a</sup> . You must start all applicable to the source by a permit limit or a rule other than this subpart that require operation of the control devices. You must develop and implement a written startup and shutdown plan, as specified in § 63.7505(e).
d. You must comply with all applicable emission limits at all times except during startup and shutdown periods at which time you must meet this work practice. You must collect monitoring data during periods of startup, as specified in § $63.7535$ (b). You must keep records during periods of startup. You must provide reports concerning activities and periods of startup, as specified in § $63.7555$ .
You must operate all CMS during shutdown. While firing fuels that are not clean fuels during shutdown, you must vent emissions to the main stack(s) and operate all applicable control devices, except limestone injection in FBC boilers, dry scrubber, fabric filter, and SCR but, in any case, when necessary to comply with other standards applicable to the source that require operation of the control device.
If, in addition to the fuel used prior to initiation of shutdown, another fuel must be used to support the shutdown process, that additional fuel must be one or a combination of the following clean fuels: Natural gas, synthetic natural gas, propane, other Gas 1 fuels, distillate oil, syngas, ultra-low sulfur diesel, refinery gas, and liquefied petroleum gas.

If your unit is	You must meet the following
	times except for startup or shutdown periods conforming with this work practice. You must collect monitoring data during periods of shutdown, as specified in § $63.7535(b)$ . You must keep records during periods of shutdown. You must provide reports concerning activities and periods of shutdown, as
	specified in <u>§ 63.7555</u> .

<sup>a</sup> As specified in § 63.7555(d)(13), the source may request an alternative timeframe with the PM controls requirement to the permitting authority (state, local, or tribal agency) that has been delegated authority for this subpart by EPA. The source must provide evidence that (1) it is unable to safely engage and operate the PM control(s) to meet the "fuel firing + 1 hour" requirement and (2) the PM control device is appropriately designed and sized to meet the filterable PM emission limit. It is acknowledged that there may be another control device that has been installed other than ESP that provides additional PM control (e.g., scrubber).

[<u>87 FR 60852</u>, Oct. 6, 2022]

#### Table 4 to Subpart DDDDD of Part 63—Operating Limits for Boilers and Process Heaters

As stated in <u>§ 63.7500</u>, you must comply with the applicable operating limits:

Table 4 to Subpart DDDDD of Part 63—Operating Limits for Boilers and Process Heaters			
When complying with a numerical emission limit under Table 1, 2, 11, 12, 13, 14, or 15 of this subpart using	You must meet these operating limits		
1. Wet PM scrubber control on a boiler or process heater not using a PM CPMS	Maintain the 30-day rolling average pressure drop and the 30-day rolling average liquid flow rate at or above the lowest one-hour average pressure drop and the lowest one-hour average liquid flow rate, respectively, measured during the performance test demonstrating compliance with the PM emission limitation according to $\underline{\$}$ <u>63.7530(b)</u> and Table 7 to this subpart.		
2. Wet acid gas (HCl) scrubber <sup>a</sup> control on a boiler or process heater not using a HCl CEMS	Maintain the 30-day rolling average effluent pH at or above the lowest one-hour average pH and the 30-day rolling average liquid flow rate at or above the lowest one-hour average liquid flow rate measured during the performance test demonstrating compliance with the HCl emission limitation according to $\frac{63.7530(b)}{53.7530(b)}$ and Table 7 to this subpart.		
3. Fabric filter control on a boiler or process heater not using a PM CPMS	a. Maintain opacity to less than or equal to 10 percent opacity or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation (daily block average); or		
	b. Install and operate a bag leak detection system according to $\S 63.7525$ and operate the fabric filter such that the bag leak detection system alert is not activated more than 5 percent of the operating time during each 6-month period.		
4. Electrostatic precipitator control on a boiler or process heater not using a PM CPMS	a. This option is for boilers and process heaters that operate dry control systems ( <i>i.e.</i> , an ESP without a wet scrubber). Existing and new boilers and process heaters must maintain opacity to less than or equal to 10 percent opacity or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation (daily block average).		
	b. This option is only for boilers and process heaters not subject to PM CPMS or continuous compliance with an opacity limit ( <i>i.e.</i> , dry ESP). Maintain the 30-day rolling average total secondary electric power input of the electrostatic precipitator at or above the operating limits established during the performance test according to $\S$ <u>63.7530(b)</u> and Table 7 to this subpart.		
5. Dry scrubber or carbon injection control on a boiler or process heater	Maintain the minimum sorbent or carbon injection rate as defined in <u>§ 63.7575 of this</u> subpart.		

Table 4 to Subpart DDDDD of Part 63—Operating Limits for Boilers and Process Heaters			
When complying with a numerical emission limit under Table 1, 2, 11, 12, 13, 14, or 15 of this subpart using	You must meet these operating limits		
not using a mercury CEMS			
6. Any other add-on air pollution control type on a boiler or process heater not using a PM CPMS	This option is for boilers and process heaters that operate dry control systems. Existing and new boilers and process heaters must maintain opacity to less than or equal to 10 percent opacity or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation (daily block average).		
7. Performance testing	For boilers and process heaters that demonstrate compliance with a performance test, maintain the 30-day rolling average operating load of each unit such that it does not exceed 110 percent of the highest hourly average operating load recorded during the performance test.		
8. Oxygen analyzer system	For boilers and process heaters subject to a CO emission limit that demonstrate compliance with an O <sub>2</sub> analyzer system as specified in § 63.7525(a), maintain the 30-day rolling average oxygen content at or above the lowest hourly average oxygen concentration measured during the CO performance test, as specified in Table 8. This requirement does not apply to units that install an oxygen trim system since these units will set the trim system to the level specified in § 63.7525(a).		
9. SO <sub>2</sub> CEMS	For boilers or process heaters subject to an HCl emission limit that demonstrate compliance with an SO <sub>2</sub> CEMS, maintain the 30-day rolling average SO <sub>2</sub> emission rate at or below the highest hourly average SO <sub>2</sub> concentration measured during the HCl performance test, as specified in Table 8.		
<sup>a</sup> A wet acid gas scrubber is a control device that removes acid gases by contacting the combustion gas with an alkaline			

slurry or solution. Alkaline reagents include, but not limited to, lime, limestone and sodium.

[80 FR 72874, Nov. 20, 2015, as amended at 87 FR 60853, Oct. 6, 2022]

#### Table 5 to Subpart DDDDD of Part 63—Performance Testing Requirements

As stated in <u>§ 63.7520</u>, you must comply with the following requirements for performance testing for existing, new or reconstructed affected sources:

To conduct a performance test for the following pollutant	You must	Using, as appropriate	
1. Filterable PM	a. Select sampling ports location and the number of traverse points	Method 1 at <u>40 CFR part 60, appendix A</u> -1 of this chapter.	
	b. Determine velocity and volumetric flow-rate of the stack gas	Method 2, 2F, or 2G at <u>40 CFR part 60, appendix A</u> -1 or A-2 to <u>part 60 of this chapter</u> .	
	c. Determine oxygen or carbon dioxide concentration of the stack gas	Method 3A or 3B at <u>40 CFR part 60, appendix A</u> -2 to <u>part 60 of</u> <u>this chapter</u> , or ANSI/ASME PTC 19.10-1981. <sup>a</sup>	
	d. Measure the moisture content of the stack gas	Method 4 at <u>40 CFR part 60, appendix A</u> -3 of this chapter.	
	e. Measure the PM emission concentration	Method 5 or 17 (positive pressure fabric filters must use Method 5D) at <u>40 CFR part 60, appendix A</u> -3 or A-6 of this chapter.	
f. Convert emissions Method 19 F-factor methodology at <u>40 Cl</u>		Method 19 F-factor methodology at <u>40 CFR part 60, appendix</u>	

To conduct a performance test for the following pollutant	You must	Using, as appropriate	
	concentration to lb per MMBtu emission rates	$\underline{\mathbf{A}}$ -7 of this chapter.	
2. TSM	a. Select sampling ports location and the number of traverse points	Method 1 at <u>40 CFR part 60, appendix A</u> -1 of this chapter.	
	b. Determine velocity and volumetric flow-rate of the stack gas	Method 2, 2F, or 2G at <u>40 CFR part 60, appendix A</u> -1 or A-2 of this chapter.	
	c. Determine oxygen or carbon dioxide concentration of the stack gas	Method 3A or 3B at <u>40 CFR part 60, appendix A</u> -1 of this chapter, or ANSI/ASME PTC 19.10-1981. <sup>a</sup>	
	d. Measure the moisture content of the stack gas	Method 4 at <u>40 CFR part 60, appendix A</u> -3 of this chapter.	
	e. Measure the TSM emission concentration	Method 29 at 40 CFR part 60, appendix A-8 of this chapter	
	f. Convert emissions concentration to lb per MMBtu emission rates	Method 19 F-factor methodology at <u>40 CFR part 60, appendix</u> <u>A</u> -7 of this chapter.	
3. Hydrogen chloridea. Select sampling ports location and the number of traverse points		Method 1 at <u>40 CFR part 60, appendix A</u> -1 of this chapter.	
	b. Determine velocity and volumetric flow-rate of the stack gas	Method 2, 2F, or 2G at <u>40 CFR part 60, appendix A</u> -2 of this chapter.	
	c. Determine oxygen or carbon dioxide concentration of the stack gas	Method 3A or 3B at <u>40 CFR part 60, appendix A</u> -2 of this chapter, or ANSI/ASME PTC 19.10-1981. <sup>a</sup>	
	d. Measure the moisture content of the stack gas	Method 4 at <u>40 CFR part 60, appendix A</u> -3 of this chapter.	
	e. Measure the hydrogen chloride emission concentration	Method 26 or 26A (M26 or M26A) at $40$ CFR part 60, apper <u>A</u> -8 of this chapter.	
	f. Convert emissions concentration to lb per MMBtu emission rates	Method 19 F-factor methodology at <u>40 CFR part 60, appendix</u> <u>A</u> -7 of this chapter.	
4. Mercury	a. Select sampling ports location and the number of traverse points	Method 1 at <u>40 CFR part 60, appendix A</u> -1 of this chapter.	
	b. Determine velocity and volumetric flow-rate of the stack gas	Method 2, 2F, or 2G at <u>40 CFR part 60, appendix A</u> -1 or A-2 of this chapter.	
	c. Determine oxygen or carbon dioxide concentration of the stack gas	Method 3A or 3B at <u>40 CFR part 60, appendix A</u> -1 of this chapter, or ANSI/ASME PTC 19.10-1981. <sup>a</sup>	
	d. Measure the moisture content of the stack gas	Method 4 at <u>40 CFR part 60, appendix A</u> -3 of this chapter.	

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To conduct a performance test for the following pollutant	You must	Using, as appropriate	
	e. Measure the mercury emission concentration	Method 29, 30A, or 30B (M29, M30A, or M30B) at <u>40 CFR part</u> <u>60, appendix A</u> -8 of this chapter or Method 101A at <u>40 CFR part</u> <u>61, appendix B</u> of this chapter, or ASTM Method D6784. <sup>a</sup>	
	f. Convert emissions concentration to lb per MMBtu emission rates	Method 19 F-factor methodology at $40 \text{ CFR part } 60$ , appendices $\underline{A}$ -7 of this chapter.	
5. CO	a. Select the sampling ports location and the number of traverse points	Method 1 at <u>40 CFR part 60, appendix A</u> -1 of this chapter.	
b. Determine oxygen concentration of the stack gas Method 3A or 3B at 40 C chapter, or ASTM D6522 ANSI/ASME PTC 19.10-		Method 3A or 3B at <u>40 CFR part 60, appendix A</u> -3 of this chapter, or ASTM D6522-00 (Reapproved 2005), or ANSI/ASME PTC 19.10-1981. <sup>a</sup>	
	c. Measure the moisture content of the stack gas	Method 4 at <u>40 CFR part 60, appendix A</u> -3 of this chapter.	
	d. Measure the CO emission concentration	Method 10 at <u>40 CFR part 60, appendix A</u> -4 of this chapter. Use a measurement span value of 2 times the concentration of the applicable emission limit.	
<sup>a</sup> Incorporated by reference, s	see § 63.14.		

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7200, Jan. 31, 2013; 80 FR 72825, Nov. 20, 2015]

#### Table 6 to Subpart DDDDD of Part 63—Fuel Analysis Requirements

As stated in  $\S$  <u>63.7521</u>, you must comply with the following requirements for fuel analysis testing for existing, new or reconstructed affected sources. However, equivalent methods (as defined in  $\S$  <u>63.7575</u>) may be used in lieu of the prescribed methods at the discretion of the source owner or operator:

To conduct a fuel analysis for the following pollutant 	You must	Using
1. Mercury a. Collect fuel samples		Procedure in <u>§ 63.7521(c)</u> or ASTM D5192 <sup>a</sup> , or ASTM D7430 <sup>a</sup> , or ASTM D6883 <sup>a</sup> , or ASTM D2234/D2234M <sup>a</sup> (for coal) or EPA 1631 or EPA 1631E or ASTM D6323 <sup>a</sup> (for solid), or EPA 821-R-01-013 (for liquid or solid), or ASTM D4177 <sup>a</sup> (for liquid), or ASTM D4057 <sup>a</sup> (for liquid), or equivalent.
	b. Composite fuel samples	Procedure in § 63.7521(d) or equivalent.
	c. Prepare composited fuel samples	EPA SW-846-3050B <sup>a</sup> (for solid samples), ASTM D2013/D2013M <sup>a</sup> (for coal), ASTM D5198 <sup>a</sup> (for biomass), or EPA 3050 <sup>a</sup> (for solid fuel), or EPA 821-R-01-013 <sup>a</sup> (for liquid or solid), or equivalent.
d. Determine heat content of the fuel type		ASTM D5865 <sup>a</sup> (for coal) or ASTM E711 <sup>a</sup> (for biomass), or ASTM D5864 <sup>a</sup> for liquids and other solids, or ASTM D240 <sup>a</sup> or equivalent.
	e. Determine moisture content of the fuel type	ASTM D3173 <sup>a</sup> , ASTM E871 <sup>a</sup> , or ASTM D5864 <sup>a</sup> , or ASTM D240 <sup>a</sup> , or ASTM D95 <sup>a</sup> (for liquid fuels), or ASTM D4006 <sup>a</sup> (for liquid fuels), or equivalent.
	f. Measure mercury concentration in fuel sample	ASTM D6722 <sup>a</sup> (for coal), EPA SW-846-7471B <sup>a</sup> or EPA 1631 or EPA 1631E <sup>a</sup> (for solid samples), or EPA SW-846-7470A <sup>a</sup> or EPA SW-846-7471B <sup>a</sup> (for liquid samples), or EPA 821-R-01-013 <sup>a</sup> (for

To conduct a fuel analysis for the following pollutant	You must	Using		
		liquid or solid), or equivalent.		
	g. Convert concentration into units of pounds of mercury per MMBtu of heat content	For fuel mixtures use Equation 8 in <u>§ 63.7530</u> .		
2. HCl	a. Collect fuel samples	Procedure in § 63.7521(c) or ASTM D5192 <sup>a</sup> , or ASTM D7430 <sup>a</sup> , or ASTM D6883 <sup>a</sup> , or ASTM D2234/D2234M <sup>a</sup> (for coal) or ASTM D6323 <sup>a</sup> (for coal or biomass), ASTM D4177 <sup>a</sup> (for liquid fuels) or ASTM D4057 <sup>a</sup> (for liquid fuels), or equivalent.		
	b. Composite fuel samples	Procedure in <u>§ 63.7521(d)</u> or equivalent.		
	c. Prepare composited fuel samples	EPA SW-846-3050B <sup>a</sup> (for solid samples), ASTM D2013/D2013M <sup>a</sup> (for coal), or ASTM D5198 <sup>a</sup> (for biomass), or EPA 3050 <sup>a</sup> or equivalent.		
	d. Determine heat content of the fuel type	ASTM D5865 <sup>a</sup> (for coal) or ASTM E711 <sup>a</sup> (for biomass), ASTM D5864 <sup>a</sup> , ASTM D240 <sup>a</sup> or equivalent.		
e. Determine moisture content of the fuel type		ASTM D3173 <sup>a</sup> or ASTM E871 <sup>a</sup> , or D5864 <sup>a</sup> , or ASTM D240 <sup>a</sup> , or ASTM D95 <sup>a</sup> (for liquid fuels), or ASTM D4006 <sup>a</sup> (for liquid fuels), or equivalent.		
	f. Measure chlorine concentration in fuel sample	EPA SW-846-9250 <sup>a</sup> , ASTM D6721 <sup>a</sup> , ASTM D4208 <sup>a</sup> (for coal), or EPA SW-846-5050 <sup>a</sup> or ASTM E776 <sup>a</sup> (for solid fuel), or EPA SW- 846-9056 <sup>a</sup> or SW-846-9076 <sup>a</sup> (for solids or liquids) or equivalent.		
	g. Convert concentrations into units of pounds of HCl per MMBtu of heat content	For fuel mixtures use Equation 7 in $\S$ <u>63.7530</u> and convert from chlorine to HCl by multiplying by 1.028.		
3. Mercury Fuel Specification for other gas 1 fuels	a. Measure mercury concentration in the fuel sample and convert to units of micrograms per cubic meter, or	Method 30B (M30B) at <u>40 CFR part 60, appendix A</u> -8 of this chapter or ASTM D5954 <sup>a</sup> , ASTM D6350 <sup>a</sup> , ISO 6978-1:2003(E) <sup>a</sup> , or ISO 6978-2:2003(E) <sup>a</sup> , or EPA-1631 <sup>a</sup> or equivalent.		
	b. Measure mercury concentration in the exhaust gas when firing only the other gas 1 fuel is fired in the boiler or process heater	Method 29, 30A, or 30B (M29, M30A, or M30B) at <u>40 CFR part 60,</u> <u>appendix A-8</u> of this chapter or Method 101A or Method 102 at <u>40</u> <u>CFR part 61, appendix B</u> of this chapter, or ASTM Method D6784 <sup>a</sup> or equivalent.		
4. TSM a. Collect fuel samples Procedure in <u>§ 63.752</u> ASTM D6883 <sup>a</sup> , or AS <sup>b</sup> D6323 <sup>a</sup> (for coal or bio or ASTM D4057 <sup>a</sup> (for		Procedure in § 63.7521(c) or ASTM D5192 <sup>a</sup> , or ASTM D7430 <sup>a</sup> , or ASTM D6883 <sup>a</sup> , or ASTM D2234/D2234M <sup>a</sup> (for coal) or ASTM D6323 <sup>a</sup> (for coal or biomass), or ASTM D4177 <sup>a</sup> , (for liquid fuels), or ASTM D4057 <sup>a</sup> (for liquid fuels), or equivalent.		
	b. Composite fuel samples	Procedure in <u>§ 63.7521(d)</u> or equivalent.		
	c. Prepare composited fuel samples	EPA SW-846-3050B <sup>a</sup> (for solid samples), ASTM D2013/D2013M <sup>a</sup> (for coal), ASTM D5198 <sup>a</sup> or TAPPI T266 <sup>a</sup> (for biomass), or EPA 3050 <sup>a</sup> or equivalent.		
	d. Determine heat content of the fuel type	ASTM D5865 <sup>a</sup> (for coal) or ASTM E711 <sup>a</sup> (for biomass), or ASTM D5864 <sup>a</sup> for liquids and other solids, or ASTM D240 <sup>a</sup> or equivalent.		
	e. Determine moisture content of the fuel type	ASTM D3173 <sup>a</sup> or ASTM E871 <sup>a</sup> , or D5864 <sup>a</sup> , or ASTM D240 <sup>a</sup> , or ASTM D95 <sup>a</sup> (for liquid fuels), or ASTM D4006 <sup>a</sup> (for liquid fuels), or ASTM D4177 <sup>a</sup> (for liquid fuels) or ASTM D4057 <sup>a</sup> (for liquid fuels), or equivalent.		

#### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

To conduct a fuel analysis for the following pollutant 	You must	Using
	f. Measure TSM concentration in fuel sample	ASTM D3683 <sup>a</sup> , or ASTM D4606 <sup>a</sup> , or ASTM D6357 <sup>a</sup> or EPA 200.8 <sup>a</sup> or EPA SW-846-6020 <sup>a</sup> , or EPA SW-846-6020A <sup>a</sup> , or EPA SW-846-6010C <sup>a</sup> , EPA 7060 <sup>a</sup> or EPA 7060A <sup>a</sup> (for arsenic only), or EPA SW-846-7740 <sup>a</sup> (for selenium only).
	g. Convert concentrations into units of pounds of TSM per MMBtu of heat content	For fuel mixtures use Equation 9 in <u>§ 63.7530</u> .
<sup>a</sup> Incorporated by refe	rence see 8 63 14	

[<u>83 FR 56725</u>, Nov. 14, 2018]

#### Table 7 to Subpart DDDDD of Part 63—Establishing Operating Limits ab

As stated in <u>§ 63.7520</u>, you must comply with the following requirements for establishing operating limits:

Table 7 to Subpart DDDDD of Part 63—Establishing Operating Limits <sup>ab</sup>					
If you have an applicable emission limit for	And your operating limits are based on	You must	Using	According to the following requirements	
1. PM, TSM, or mercury	a. Wet scrubber operating parameters	i. Establish a site-specific minimum scrubber pressure drop and minimum flow rate operating limit according to $\frac{63.7530(b)}{5}$	(1) Data from the scrubber pressure drop and liquid flow rate monitors and the PM, TSM, or mercury performance test	(a) You must collect scrubber pressure drop and liquid flow rate data every 15 minutes during the entire period of the performance tests.	
				(b) Determine the lowest hourly average scrubber pressure drop and liquid flow rate by computing the hourly averages using all of the 15- minute readings taken during each performance test.	
	b. Electrostatic precipitator operating parameters (option only for units that operate wet scrubbers)	i. Establish a site-specific minimum total secondary electric power input according to <u>§ 63.7530(b)</u>	(1) Data from the voltage and secondary amperage monitors during the PM or mercury performance test	(a) You must collect secondary voltage and secondary amperage for each ESP cell and calculate total secondary electric power input data every 15 minutes during the entire period of the performance tests.	
				(b) Determine the average total secondary electric power input by computing the hourly averages using all of the 15-minute readings taken during each performance test.	
	c. Opacity	i. Establish a site-specific maximum opacity level	(1) Data from the opacity monitoring system during the PM performance	(a) You must collect opacity readings every 15 minutes during the entire period of the performance tests.	
Table 7 to Subpart DDDDD of Part 63—Establishing Operating Limits <sup>ab</sup>					
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If you have an applicable emission limit for	And your operating limits are based on	You must	Using	According to the following requirements	
			test		
				(b) Determine the average hourly opacity reading by computing the hourly averages using all of the 15- minute readings taken during each performance test.	
				(c) Determine the highest hourly average opacity reading measured during the test run demonstrating compliance with the PM (or TSM) emission limitation.	
2. HCl	a. Wet scrubber operating parameters	i. Establish site-specific minimum effluent pH and flow rate operating limits according to <u>§ 63.7530(b)</u>	(1) Data from the pH and liquid flow-rate monitors and the HCl performance test	(a) You must collect pH and liquid flow-rate data every 15 minutes during the entire period of the performance tests.	
				(b) Determine the hourly average pH and liquid flow rate by computing the hourly averages using all of the 15-minute readings taken during each performance test.	
	b. Dry scrubber operating parameters	i. Establish a site-specific minimum sorbent injection rate operating limit according to $\S$ 63.7530(b). If different acid gas sorbents are used during the HC1 performance test, the average value for each sorbent becomes the site- specific operating limit for that sorbent	(1) Data from the sorbent injection rate monitors and HCl or mercury performance test	(a) You must collect sorbent injection rate data every 15 minutes during the entire period of the performance tests.	
				(b) Determine the hourly average sorbent injection rate by computing the hourly averages using all of the 15-minute readings taken during each performance test.	
				(c) Determine the lowest hourly average of the three test run averages established during the performance test as your operating limit. When your unit operates at lower loads, multiply your sorbent injection rate by the load fraction, as defined in § 63.7575, to determine the required injection rate.	

Table 7 to Subpart DDDDD of Part 63—Establishing Operating Limits <sup>ab</sup>					
If you have an applicable emission limit for	And your operating limits are based on	You must	Using	According to the following requirements	
	c. Alternative Maximum SO <sub>2</sub> emission rate	i. Establish a site-specific maximum SO <sub>2</sub> emission rate operating limit according to $\frac{63.7530(b)}{2}$	(1) Data from SO <sub>2</sub> CEMS and the HCl performance test	(a) You must collect the SO <sub>2</sub> emissions data according to $\S$ 63.7525(m) during the most recent HCl performance tests.	
				(b) The maximum SO <sub>2</sub> emission rate is equal to the highest hourly average SO <sub>2</sub> emission rate measured during the most recent HCl performance tests.	
3. Mercury	a. Activated carbon injection	i. Establish a site-specific minimum activated carbon injection rate operating limit according to <u>§ 63.7530(b)</u>	(1) Data from the activated carbon rate monitors and mercury performance test	(a) You must collect activated carbon injection rate data every 15 minutes during the entire period of the performance tests.	
				(b) Determine the hourly average activated carbon injection rate by computing the hourly averages using all of the 15-minute readings taken during each performance test.	
				(c) Determine the lowest hourly average established during the performance test as your operating limit. When your unit operates at lower loads, multiply your activated carbon injection rate by the load fraction, as defined in § 63.7575, to determine the required injection rate.	
4. Carbon monoxide for which compliance is demonstrated by a performance test	a. Oxygen	i. Establish a unit-specific limit for minimum oxygen level according to $\S$ <u>63.7530(b)</u>	(1) Data from the oxygen analyzer system specified in <u>§ 63.7525(a)</u>	(a) You must collect oxygen data every 15 minutes during the entire period of the performance tests.	
				(b) Determine the hourly average oxygen concentration by computing the hourly averages using all of the 15-minute readings taken during each performance test.	
				(c) Determine the lowest hourly average established during the performance test as your minimum operating limit.	
5. Any pollutant for which compliance is	a. Boiler or process heater operating load	i. Establish a unit specific limit for maximum operating load according to $\S$	(1) Data from the operating load monitors or from	(a) You must collect operating load or steam generation data every 15 minutes during the entire period of	

Table 7 to Subpart DDDDD of Part 63—Establishing Operating Limits <sup>ab</sup>					
If you have an applicable emission limit for	And your operating limits are based on	You must	Using	According to the following requirements	
demonstrated by a performance test		<u>63.7520(c)</u>	steam generation monitors	the performance test.	
				(b) Determine the average operating load by computing the hourly averages using all of the 15-minute readings taken during each performance test.	
				(c) Determine the highest hourly average of the three test run averages during the performance test, and multiply this by 1.1 (110 percent) as your operating limit.	

<sup>a</sup> Operating limits must be confirmed or reestablished during performance tests.

<sup>b</sup> If you conduct multiple performance tests, you must set the minimum liquid flow rate and pressure drop operating limits at the higher of the minimum values established during the performance tests. For a minimum oxygen level, if you conduct multiple performance tests, you must set the minimum oxygen level at the lower of the minimum values established during the performance tests. For maximum operating load, if you conduct multiple performance tests, you must set the maximum operating load at the lower of the maximum values established during the performance tests.

#### [<u>87 FR 60853</u>, Oct. 6, 2022]

#### Table 8 to Subpart DDDDD of Part 63—Demonstrating Continuous Compliance

As stated in  $\S$  63.7540, you must show continuous compliance with the emission limitations for each boiler or process heater according to the following:

If you must meet the following operating limits or work practice standards	You must demonstrate continuous compliance by
1. Opacity	a. Collecting the opacity monitoring system data according to $\S 63.7525(c)$ and $\S 63.7535$ ; and
	b. Reducing the opacity monitoring data to 6-minute averages; and
	c. Maintaining daily block average opacity to less than or equal to 10 percent or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation.
2. PM CPMS	a. Collecting the PM CPMS output data according to <u>§ 63.7525</u> ;
	b. Reducing the data to 30-day rolling averages; and
	c. Maintaining the 30-day rolling average PM CPMS output data to less than the operating limit established during the performance test according to $\frac{63.7530(b)(4)}{2}$ .
3. Fabric Filter Bag Leak Detection Operation	Installing and operating a bag leak detection system according to $\frac{63.7525}{3}$ and operating the fabric filter such that the requirements in $\frac{63.7540(a)(7)}{3}$ are met.
4. Wet Scrubber Pressure Drop and Liquid Flow-rate	a. Collecting the pressure drop and liquid flow rate monitoring system data according to $\frac{8863.7525}{3}$ and $\frac{63.7535}{3}$ ; and
	b. Reducing the data to 30-day rolling averages; and
	c. Maintaining the 30-day rolling average pressure drop and liquid flow-rate at or above

If you must meet the following operating limits or work practice standards	You must demonstrate continuous compliance by	
	the operating limits established during the performance test according to $\frac{63.7530(b)}{2}$ .	
5. Wet Scrubber pH	a. Collecting the pH monitoring system data according to $\frac{8863.7525}{2}$ and $\frac{63.7535}{2}$ ; and	
	b. Reducing the data to 30-day rolling averages; and	
	c. Maintaining the 30-day rolling average pH at or above the operating limit established during the performance test according to $\frac{63.7530(b)}{2}$ .	
6. Dry Scrubber Sorbent or Carbon Injection Rate	a. Collecting the sorbent or carbon injection rate monitoring system data for the dry scrubber according to $\frac{\&\& 63.7525}{\&\& 63.7525}$ and $\frac{63.7535}{\&\& 63.7525}$ ; and	
	b. Reducing the data to 30-day rolling averages; and	
	c. Maintaining the 30-day rolling average sorbent or carbon injection rate at or above the minimum sorbent or carbon injection rate as defined in $\S 63.7575$ .	
7. Electrostatic Precipitator Total Secondary Electric Power Input	a. Collecting the total secondary electric power input monitoring system data for the electrostatic precipitator according to $\frac{\$\$ 63.7525}{\$}$ and $\frac{63.7535}{\$}$ ; and	
	b. Reducing the data to 30-day rolling averages; and	
	c. Maintaining the 30-day rolling average total secondary electric power input at or above the operating limits established during the performance test according to $\frac{63.7530(b)}{5.000}$ .	
8. Emission limits using fuel analysis	a. Conduct monthly fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart; and	
	b. Reduce the data to 12-month rolling averages; and	
	c. Maintain the 12-month rolling average at or below the applicable emission limit for HCl or mercury or TSM in Tables 1 and 2 or 11 through 15 to this subpart.	
	d. Calculate the HCI, mercury, and/or TSM emission rate from the boiler or process heater in units of lb/MMBtu using Equation 15 and Equations 16, 17, and/or 18 in $\S$ 63.7530.	
9. Oxygen content	a. Continuously monitor the oxygen content using an oxygen analyzer system according to $\frac{63.7525(a)}{2}$ . This requirement does not apply to units that install an oxygen trim system since these units will set the trim system to the level specified in $\frac{63.7525(a)}{7}$ .	
	b. Reducing the data to 30-day rolling averages; and	
	c. Maintain the 30-day rolling average oxygen content at or above the lowest hourly average oxygen level measured during the CO performance test.	
10. Boiler or process heater operating load	<ul><li>a. Collecting operating load data or steam generation data every 15 minutes.</li><li>b. Reducing the data to 30-day rolling averages; and</li></ul>	
	c. Maintaining the 30-day rolling average operating load such that it does not exceed 110 percent of the highest hourly average operating load recorded during the performance test according to $\frac{63.7520(c)}{c}$ .	
11. SO <sub>2</sub> emissions using SO <sub>2</sub> CEMS	a. Collecting the SO <sub>2</sub> CEMS output data according to $\S$ 63.7525;	
	b. Reducing the data to 30-day rolling averages; and	
	c. Maintaining the 30-day rolling average SO <sub>2</sub> CEMS emission rate to a level at or below the highest hourly SO <sub>2</sub> rate measured during the HCl performance test according to $\frac{\$}{53.7530}$ .	

[78 FR 7204, Jan. 31, 2013, as amended at 80 FR 72829, Nov. 20, 2015; 87 FR 60855, Oct. 6, 2022]

### Table 9 to Subpart DDDDD of Part 63—Reporting Requirements

As stated in <u>§ 63.7550</u>, you must comply with the following requirements for reports:

You must submit a(n)	The report must contain	You must submit the report
1. Compliance report	a. Information required in <u>§ 63.7550(c)(1)</u> through <u>(5)</u> ; and	Semiannually, annually, biennially, or every 5 years according to the requirements in $\S$ 63.7550(b).
	b. If there are no deviations from any emission limitation (emission limit and operating limit) that applies to you and there are no deviations from the requirements for work practice standards for periods of startup and shutdown in Table 3 to this subpart that apply to you, a statement that there were no deviations from the emission limitations and work practice standards during the reporting period. If there were no periods during which the CMSs, including continuous emissions monitoring system, continuous opacity monitoring system, and operating parameter monitoring systems, were out-of-control as specified in § $63.8(c)(7)$ , a statement that there were no period; and	
	c. If you have a deviation from any emission limitation (emission limit and operating limit) where you are not using a CMS to comply with that emission limit or operating limit, or a deviation from a work practice standard for periods of startup and shutdown, during the reporting period, the report must contain the information in $\frac{8}{63.7550(d)}$ ; and	
	d. If there were periods during which the CMSs, including continuous emissions monitoring system, continuous opacity monitoring system, and operating parameter monitoring systems, were out-of-control as specified in $\frac{\& 63.8(c)(7)}{50(c)}$ , or otherwise not operating, the report must contain the information in $\frac{\& 63.7550(c)}{50(c)}$	

### National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7205, Jan. 31, 2013; 80 FR 72830, Nov. 20, 2015]

## Table 10 to Subpart DDDDD of Part 63—Applicability of General Provisions to Subpart DDDDD

As stated in <u>§ 63.7565</u>, you must comply with the applicable General Provisions according to the following:

Citation	Subject	Applies to subpart DDDDD
§ 63.1	Applicability	Yes.
§ 63.2	Definitions	Yes. Additional terms defined in § 63.7575
§ 63.3	Units and Abbreviations	Yes.
§ 63.4	Prohibited Activities and Circumvention	Yes.
§ 63.5	Preconstruction Review and Notification Requirements	Yes.
§ 63.6(a), (b)(1)-(b)(5), (b)(7), (c)	Compliance with Standards and Maintenance Requirements	Yes.
§ 63.6(e)(1)(i)	General duty to minimize emissions.	No. See $\S$ 63.7500(a)(3) for the general duty requirement.
§ 63.6(e)(1)(ii)	Requirement to correct malfunctions as soon as practicable.	No.
§ 63.6(e)(3)	Startup, shutdown, and malfunction plan requirements.	No.

Citation	Subject	Applies to subpart DDDDD	
§ 63.6(f)(1) Startup, shutdown, and malfunction exemption compliance with non- opacity emission stand		No.	
§ 63.6(f)(2) and (3)	Compliance with non- opacity emission standards.	Yes.	
§ 63.6(g) Use of alternative standards		Yes, except § <u>63.7555(d)(13)</u> specifies the procedure for application and approval of an alternative timeframe with the PM controls requirement in the startup work practice (2).	
§ 63.6(h)(1)	Startup, shutdown, and malfunction exemptions to opacity standards.	No. See <u>§ 63.7500(a)</u> .	
§ 63.6(h)(2) to (h)(9)	Determining compliance with opacity emission standards	No. Subpart DDDDD specifies opacity as an operating limit not an emission standard.	
§ 63.6(i) Extension of compliance		Yes. Note: Facilities may also request extensions of compliance for the installation of combined heat and power, waste heat recovery, or gas pipeline or fuel feeding infrastructure as a means of complying with this subpart.	
§ 63.6(j)	Presidential exemption.	Yes.	
§ 63.7(a), (b), (c), and (d)	Performance Testing Requirements	Yes.	
§ 63.7(e)(1)	Conditions for conducting performance tests	No. Subpart DDDDD specifies conditions for conducting performance tests at $\S 63.7520(a)$ to (c).	
§ 63.7(e)(2)-(e)(9), (f), (g), and (h)	Performance Testing Requirements	Yes.	
§ 63.8(a) and (b)	Applicability and Conduct of Monitoring	Yes.	
§ 63.8(c)(1)	Operation and maintenance of CMS	Yes.	
§ 63.8(c)(1)(i)	General duty to minimize emissions and CMS operation	No. See <u>§ 63.7500(a)(3)</u> .	
§ 63.8(c)(1)(ii)	Operation and maintenance of CMS	Yes.	
§ 63.8(c)(1)(iii)	Startup, shutdown, and malfunction plans for CMS	No.	
§ 63.8(c)(2) to (c)(9)	Operation and maintenance of CMS	Yes.	
§ 63.8(d)(1) and (2)	Monitoring Requirements, Quality Control Program	Yes.	
§ 63.8(d)(3)	Written procedures for CMS	Yes, except for the last sentence, which refers to a startup, shutdown, and malfunction plan. Startup, shutdown, and malfunction plans are not required.	
§ 63.8(e)	Performance evaluation of a CMS	Yes.	

Citation	Subject	Applies to subpart DDDDD	
§ 63.8(f)	Use of an alternative monitoring method.	Yes.	
§ 63.8(g)	Reduction of monitoring data	Yes.	
§ 63.9	Notification Requirements	Yes.	
§ 63.10(a), (b)(1)	Recordkeeping and Reporting Requirements	Yes.	
§ 63.10(b)(2)(i)	Recordkeeping of occurrence and duration of startups or shutdowns	Yes.	
§ 63.10(b)(2)(ii)	Recordkeeping of malfunctions	No. See $\S$ <u>63.7555(d)(7)</u> for recordkeeping of occurrence and duration and $\S$ <u>63.7555(d)(8)</u> for actions taken during malfunctions.	
§ 63.10(b)(2)(iii)	Maintenance records	Yes.	
§ 63.10(b)(2)(iv) and (v)	Actions taken to minimize emissions during startup, shutdown, or malfunction	No.	
§ 63.10(b)(2)(vi)	Recordkeeping for CMS malfunctions	Yes.	
§ 63.10(b)(2)(vii) to (xiv)	Other CMS requirements	Yes.	
§ 63.10(b)(3)	Recordkeeping requirements for applicability determinations	No.	
§ 63.10(c)(1) to (9)	Recordkeeping for sources with CMS	Yes.	
§ 63.10(c)(10) and (11)	Recording nature and cause of malfunctions, and corrective actions	No. See $\S$ <u>63.7555(d)(7)</u> for recordkeeping of occurrence and duration and $\S$ <u>63.7555(d)(8)</u> for actions taken during malfunctions.	
§ 63.10(c)(12) and (13)	Recordkeeping for sources with CMS	Yes.	
§ 63.10(c)(15)	Use of startup, shutdown, and malfunction plan	No.	
§ 63.10(d)(1) and (2)	General reporting requirements	Yes.	
§ 63.10(d)(3)	Reporting opacity or visible emission observation results	No.	
§ 63.10(d)(4)	Progress reports under an extension of compliance	Yes.	
§ 63.10(d)(5)	Startup, shutdown, and malfunction reports	No. See $\S$ 63.7550(c)(11) for malfunction reporting requirements.	
§ 63.10(e)	Additional reporting requirements for sources with CMS	Yes.	
§ 63.10(f)	Waiver of recordkeeping or reporting requirements	Yes.	
§ 63.11	Control Device Requirements	No.	

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Citation	Subject	Applies to subpart DDDDD
§ 63.12	State Authority and Delegation	Yes.
§ 63.13-63.16	Addresses, Incorporation by Reference, Availability of Information, Performance Track Provisions	Yes.
$ \begin{cases} 63.1(a)(5),(a)(7)-(a)(9), (b)(2), (c)(3)-(4), (d), 63.6(b)(6), (c)(3), (c)(4), (d), (e)(2), (e)(3)(ii), (h)(3), (h)(5)(iv), \\ 63.8(a)(3), 63.9(b)(3), (h)(4), \\ 63.10(c)(2)-(4), (c)(9). \end{cases} $	Reserved	No.

[76 FR 15664, Mar. 21, 2011, as amended at 78 FR 7205, Jan. 31, 2013; 80 FR 72830, Nov. 20, 2015]

Table 11 to Subpart DDDDD of Part 63—Alternative Emission Limits for New or Reconstructed Boilers and ProcessHeaters That Commenced Construction or Reconstruction After June 4, 2010, and Before May 20, 2011

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
1. Units in all subcategories designed to burn solid fuel	a. HCl	0.022 lb per MMBtu of heat input	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.
2. Units in all subcategories designed to burn solid fuel that combust at least 10 percent biomass/bio-based solids on an annual heat input basis and less than 10 percent coal/solid fossil fuels on an annual heat input basis	a. Mercury	8.0E-07 <sup>a</sup> lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.
3. Units in all subcategories designed to burn solid fuel that combust at least 10 percent coal/solid fossil fuels on an annual heat input basis and less than 10 percent biomass/bio-based solids on an annual heat input basis	a. Mercury	2.0E-06 lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.
4. Units design to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
5. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
6. Stokers designed to burn coal/solid fossil fuel	a. CO (or CEMS).	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3 percent oxygen , <sup>c</sup> 10-day rolling average)	1 hr minimum sampling time.
7. Fluidized bed units designed to burn	a. CO (or	130 ppm by volume on a dry	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
coal/solid fossil fuel	CEMS)	basis corrected to 3 percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	
8. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
9. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	620 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (390 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (2.6E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
10. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	560 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run
11. Fluidized bed units designed to burn biomass/bio-based solids	a. CO (or CEMS)	230 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	9.8E-03 lb per MMBtu of heat input; or (8.3E-05 <sup>a</sup> lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run
12. Suspension burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	2,400 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3 percent oxygen <sup>c</sup> 10-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
13. Dutch Ovens/Pile burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	1,010 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (520	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
		ppm by volume on a dry basis corrected to 3 percent oxygen <sup>c</sup> 10-day rolling average)	
	b. Filterable PM (or TSM)	8.0E-03 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
14. Fuel cell units designed to burn biomass/bio-based solids	a. CO	910 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
15. Hybrid suspension grate boiler designed to burn biomass/bio-based solids	a. CO (or CEMS)	1,100 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.6E-02 lb per MMBtu of heat input; or (4.4E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run
16. Units designed to burn liquid fuel	a. HCl	4.4E-04 lb per MMBtu of heat input	For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run
	b. Mercury.	4.8E-07 <sup>a</sup> lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.
17. Units designed to burn heavy liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.3E-02 lb per MMBtu of heat input; or (7.5E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
18. Units designed to burn light liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-03 <sup>a</sup> lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run
19. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average based on stack test	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory	For the followingThe emissions must not exceed the following emission limits, except during periods of 		Using this specified sampling volume or test run duration
	b. Filterable PM (or TSM)	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)	Collect a minimum of 4 dscm per run
20. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. HCl	1.7E-03 lb per MMBtu of heat input	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.
	d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.

<sup>a</sup> If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to  $\frac{63.7515}{10}$  if all of the other provision of  $\frac{63.7515}{10}$  are met. For all other pollutants that do not contain a footnote "a", your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

<sup>b</sup> Incorporated by reference, see <u>§ 63.14</u>.

<sup>c</sup> An owner or operator may determine compliance with the carbon monoxide emissions limit using carbon dioxide as a diluent correction in place of oxygen as described in § 63.7525(a)(1). EPA Method 19 F-factors in 40 CFR part 60, appendix A-7, and EPA Method 19 equations in 40 CFR part 60, appendix A-7, must be used to generate the appropriate CO<sub>2</sub> correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The methodology must account for any CO<sub>2</sub> being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. This methodology must be detailed in the site-specific monitoring plan developed according to § 63.7505(d).

[<u>87 FR 60855</u>, Oct. 6, 2022]

 Table 12 to Subpart DDDDD of Part 63—Alternative Emission Limits for New or Reconstructed Boilers and Process

 Heaters That Commenced Construction or Reconstruction After May 20, 2011, and Before December 23, 2011

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
1. Units in all subcategories designed to burn solid fuel	a. HCl	0.022 lb per MMBtu of heat input	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.
	b. Mercury	3.5E-06 <sup>a</sup> lb per MMBtu of heat input	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.

#### The emissions must not For the If your boiler or exceed the following Using this specified sampling volume process heater is in this following emission limits, except during or test run duration . . . subcategory . . . pollutants.. periods of startup and shutdown . . . 2. Units design to burn 1.1E-03 lb per MMBtu of heat input; or a. Filterable Collect a minimum of 3 dscm per run. coal/solid fossil fuel (2.3E-05 lb per MMBtu of heat input) PM (or TSM) 130 ppm by volume on a dry basis a. Carbon 3. Pulverized coal boilers corrected to 3 percent oxygen, 3-run monoxide average; or (320 ppm by volume on a designed to burn coal/solid 1 hr minimum sampling time. (CO) (or fossil fuel dry basis corrected to 3 percent CEMS) oxygen,<sup>c</sup> 30-day rolling average) 130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run 4. Stokers designed to burn a. CO (or average; or (340 ppm by volume on a 1 hr minimum sampling time. coal/solid fossil fuel CEMS) dry basis corrected to 3 percent oxygen,<sup>c</sup> 10-day rolling average) 130 ppm by volume on a dry basis 5. Fluidized bed units corrected to 3 percent oxygen, 3-run a. CO (or designed to burn coal/solid average; or (230 ppm by volume on a 1 hr minimum sampling time. CEMS) fossil fuel dry basis corrected to 3 percent oxygen,<sup>c</sup> 30-day rolling average) 140 ppm by volume on a dry basis 6. Fluidized bed units with corrected to 3 percent oxygen, 3-run an integrated heat a. CO (or average; or (150 ppm by volume on a 1 hr minimum sampling time. exchanger designed to burn CEMS) dry basis corrected to 3 percent coal/solid fossil fuel oxygen,<sup>c</sup> 30-day rolling average) 620 ppm by volume on a dry basis 7. Stokers/sloped corrected to 3 percent oxygen, 3-run a. CO (or grate/others designed to average; or (390 ppm by volume on a 1 hr minimum sampling time. CEMS) dry basis corrected to 3 percent burn wet biomass fuel oxygen,<sup>c</sup> 30-day rolling average) 3.0E-02 lb per MMBtu of heat input; or b. Filterable Collect a minimum of 2 dscm per run. PM (or TSM) (2.6E-05 lb per MMBtu of heat input) 8. Stokers/sloped grate/others designed to 460 ppm by volume on a dry basis a. CO 1 hr minimum sampling time. burn kiln-dried biomass corrected to 3 percent oxygen fuel b. Filterable 3.0E-02 lb per MMBtu of heat input; or Collect a minimum of 2 dscm per run. (4.0E-03 lb per MMBtu of heat input) PM (or TSM) 260 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run 9. Fluidized bed units a. CO (or average; or (310 ppm by volume on a designed to burn 1 hr minimum sampling time. CEMS) dry basis corrected to 3 percent biomass/bio-based solids oxygen,<sup>c</sup> 30-day rolling average) 9.8E-03 lb per MMBtu of heat input; or b. Filterable Collect a minimum of 3 dscm per run. PM (or TSM) (8.3E-05<sup>a</sup> lb per MMBtu of heat input) 2,400 ppm by volume on a dry basis 10. Suspension burners corrected to 3 percent oxygen, 3-run a. CO (or designed to burn average; or (2,000 ppm by volume on a 1 hr minimum sampling time. CEMS) biomass/bio-based solids dry basis corrected to 3 percent oxygen,<sup>c</sup> 10-day rolling average)

#### The emissions must not For the If your boiler or exceed the following Using this specified sampling volume process heater is in this following emission limits, except during or test run duration . . . subcategory ... pollutants.. periods of startup and shutdown ... b. Filterable 3.0E-02 lb per MMBtu of heat input; or Collect a minimum of 2 dscm per run. (6.5E-03 lb per MMBtu of heat input) PM (or TSM) 470 ppm by volume on a dry basis 11. Dutch Ovens/Pile corrected to 3 percent oxygen, 3-run a. CO (or average; or (520 ppm by volume on a burners designed to burn 1 hr minimum sampling time. CEMS) biomass/bio-based solids dry basis corrected to 3 percent oxygen,<sup>c</sup> 10-day rolling average) 3.2E-03 lb per MMBtu of heat input; or b. Filterable Collect a minimum of 3 dscm per run. (3.9E-05 lb per MMBtu of heat input) PM (or TSM) 12. Fuel cell units designed 910 ppm by volume on a dry basis to burn biomass/bio-based a. CO 1 hr minimum sampling time. corrected to 3 percent oxygen solids b. Filterable 2.0E-02 lb per MMBtu of heat input; or Collect a minimum of 2 dscm per run. PM (or TSM) (2.9E-05 lb per MMBtu of heat input) 1,500 ppm by volume on a dry basis 13. Hybrid suspension corrected to 3 percent oxygen, 3-run grate boiler designed to a. CO (or average; or (900 ppm by volume on a 1 hr minimum sampling time. burn biomass/bio-based CEMS) dry basis corrected to 3 percent solids oxygen,<sup>c</sup> 30-day rolling average) 2.6E-02 lb per MMBtu of heat input; or b. Filterable Collect a minimum of 3 dscm per run. PM (or TSM) (4.4E-04 lb per MMBtu of heat input) For M26A: Collect a minimum of 2 14. Units designed to burn a. HCl 4.4E-04 lb per MMBtu of heat input dscm per run; for M26, collect a liquid fuel minimum of 240 liters per run. For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a b. Mercury 4.8E-07<sup>a</sup> lb per MMBtu of heat input minimum sample as specified in the method; for ASTM D6784<sup>b</sup> collect a minimum of 4 dscm. 130 ppm by volume on a dry basis 15. Units designed to burn a. CO corrected to 3 percent oxygen, 3-run 1 hr minimum sampling time. heavy liquid fuel average b. Filterable 1.3E-02 lb per MMBtu of heat input; or Collect a minimum of 2 dscm per run. (7.5E-05 lb per MMBtu of heat input) PM (or TSM) 16. Units designed to burn 130 ppm by volume on a dry basis a. CO 1 hr minimum sampling time. light liquid fuel corrected to 3 percent oxygen 1.3E-03<sup>a</sup> lb per MMBtu of heat input; b. Filterable or (2.9E-05 lb per MMBtu of heat Collect a minimum of 3 dscm per run. PM (or TSM) input) 130 ppm by volume on a dry basis 17. Units designed to burn liquid fuel that are nona. CO corrected to 3 percent oxygen, 3-run 1 hr minimum sampling time. continental units average based on stack test b. Filterable 2.3E-02 lb per MMBtu of heat input; or Collect a minimum of 4 dscm per run. PM (or TSM) (8.6E-04 lb per MMBtu of heat input) 18. Units designed to burn 130 ppm by volume on a dry basis a. CO 1 hr minimum sampling time. gas 2 (other) gases corrected to 3 percent oxygen

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
	b. HCl	1.7E-03 lb per MMBtu of heat input	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.
	d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.

<sup>a</sup> If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to  $\frac{63.7515}{10}$  if all of the other provision of  $\frac{63.7515}{10}$  are met. For all other pollutants that do not contain a footnote "a", your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

### <sup>b</sup> Incorporated by reference, see $\S$ <u>63.14</u>.

<sup>c</sup> An owner or operator may determine compliance with the carbon monoxide emissions limit using carbon dioxide as a diluent correction in place of oxygen as described in § 63.7525(a)(1). EPA Method 19 F-factors in <u>40 CFR part 60, appendix A</u>-7, and EPA Method 19 equations in <u>40 CFR part 60, appendix A</u>-7, must be used to generate the appropriate CO<sub>2</sub> correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The methodology must account for any CO<sub>2</sub> being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. This methodology must be detailed in the site-specific monitoring plan developed according to § 63.7505(d).

### [<u>87 FR 60857</u>, Oct. 6, 2022]

 Table 13 to Subpart DDDDD of Part 63—Alternative Emission Limits for New or Reconstructed Boilers and Process

 Heaters That Commenced Construction or Reconstruction After December 23, 2011, and Before April 1, 2013

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
1. Units in all subcategories designed to burn solid fuel	a. HCl	0.022 lb per MMBtu of heat input	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.
	b. Mercury	8.6E-07 <sup>a</sup> lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.
2. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.8E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
3. Stokers designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 10-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.8E-02 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
4. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
5. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
6. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	620 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (410 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 10-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (2.6E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
7. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	460 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.2E-01 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
8. Fluidized bed units designed to burn biomass/bio-based solids	a. CO (or CEMS)	230 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	9.8E-03 lb per MMBtu of heat input; or (8.3E-05 <sup>a</sup> lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
9. Suspension burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	2,400 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 10-day rolling average)	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
	b. Filterable PM (or TSM)	5.1E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
10. Dutch Ovens/Pile burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	810 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 10-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.6E-02 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
11. Fuel cell units designed to burn biomass/bio-based solids	a. CO	910 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
12. Hybrid suspension grate boiler designed to burn biomass/bio-based solids	a. CO (or CEMS)	1,500 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.6E-02 lb per MMBtu of heat input; or (4.4E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
13. Units designed to burn liquid fuel	a. HCl	1.2E-03 lb per MMBtu of heat input	For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	b. Mercury	4.9E-07 <sup>a</sup> lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.
14. Units designed to burn heavy liquid fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (18 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 10- day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.3E-03 lb per MMBtu of heat input; or (7.5E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
15. Units designed to burn light liquid fuel	a. CO (or CEMS)	130 <sup>a</sup> ppm by volume on a dry basis corrected to 3 percent oxygen; or (60 ppm by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 1-day block average).	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-03 <sup>a</sup> lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
16. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average based on stack test; or (91 ppm	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during periods of startup and shutdown	Using this specified sampling volume or test run duration
		by volume on a dry basis corrected to 3 percent oxygen, <sup>c</sup> 3-hour rolling average)	
	b. Filterable PM (or TSM)	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
17. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. HCl	1.7E-03 lb per MMBtu of heat input	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.
	d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.

<sup>a</sup> If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit and you are not required to conduct testing for CEMS or CPMS monitor certification, you can skip testing according to  $\frac{63.7515}{10}$  if all of the other provision of  $\frac{63.7515}{10}$  are met. For all other pollutants that do not contain a footnote "a", your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

<sup>b</sup> Incorporated by reference, see § 63.14.

<sup>c</sup> An owner or operator may determine compliance with the carbon monoxide emissions limit using carbon dioxide as a diluent correction in place of oxygen as described in § 63.7525(a)(1). EPA Method 19 F-factors in 40 CFR part 60, appendix A-7, and EPA Method 19 equations in 40 CFR part 60, appendix A-7, must be used to generate the appropriate CO<sub>2</sub> correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The methodology must account for any CO<sub>2</sub> being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. This methodology must be detailed in the site-specific monitoring plan developed according to § 63.7505(d).

### [<u>87 FR 60859</u>, Oct. 6, 2022]

# Table 14 to Subpart DDDDD of Part 63—Alternative Emission Limits for New or Reconstructed Boilers and Process Heaters <sup>c</sup>

As stated in <u>§ 63.7500</u>, you may continue to comply with the following applicable emission limits until October 6, 2025:

	[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 	
1. Units in all subcategories designed to burn solid fuel.	a. HCl	2.2E-02 lb per MMBtu of heat input	2.5E-02 lb per MMBtu of steam output or 0.28 lb per MWh	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.	

[Units with heat input capacity of 10 million Btu per hour or greater]					
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 	
	b. Mercury	8.0E-07ª lb per MMBtu of heat input	8.7E-07ª lb per MMBtu of steam output or 1.1E-05ª lb per MWh	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.	
2. Units designed to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	1.1E-03 lb per MMBtu of steam output or 1.4E-02 lb per MWh; or (2.7E-05 lb per MMBtu of steam output or 2.9E-04 lb per MWh)	Collect a minimum of 3 dscm per run.	
3. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.	
4. Stokers/others designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	0.12 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.	
5. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.	
6. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3- percent oxygen, <sup>d</sup> 30-day rolling average)	1.2E-01 lb per MMBtu of steam output or 1.5 lb per MWh; 3-run average	1 hr minimum sampling time.	
7. Stokers/sloped grate/others designed	a. CO (or CEMS)	620 ppm by volume on a dry basis corrected to 3-percent	5.8E-01 lb per MMBtu of steam output or 6.8	1 hr minimum sampling time.	

#### [Units with heat input capacity of 10 million Btu per hour or greater] Or the emissions must The emissions must not not If your boiler or For the exceed the following exceed the following Using this specified sampling process heater is in following emission limits, except alternative outputvolume or test run duration . this pollutants.. during startup and based limits, except . . subcategory ... shutdown . . . during startup and shutdown . . . to burn wet biomass oxygen, 3-run average; or lb per MWh; 3-run (390 ppm by volume on a dry fuel average basis corrected to 3-percent oxygen,<sup>d</sup> 30-day rolling average) 3.5E-02 lb per MMBtu of steam output or b. Filterable 3.0E-02 lb per MMBtu of 4.2E-01 lb per MWh; Collect a minimum of 2 dscm PM (or heat input; or (2.6E-05 lb per or (2.7E-05 lb per per run. TSM) MMBtu of heat input) MMBtu of steam output or 3.7E-04 lb per MWh) 8. Stokers/sloped 460 ppm by volume on a dry 4.2E-01 lb per MMBtu grate/others designed a. CO basis corrected to 3-percent of steam output or 5.1 1 hr minimum sampling time. to burn kiln-dried lb per MWh oxygen biomass fuel 3.5E-02 lb per MMBtu of steam output or 4.2E-01 lb per MWh; b. Filterable 3.0E-02 lb per MMBtu of Collect a minimum of 2 dscm PM (or heat input; or (4.0E-03 lb per or (4.2E-03 lb per per run. MMBtu of heat input) MMBtu of steam TSM) output or 5.6E-02 lb per MWh) 230 ppm by volume on a dry basis corrected to 3-percent 9. Fluidized bed units 2.2E-01 lb per MMBtu oxygen, 3-run average; or designed to burn a. CO (or of steam output or 2.6 (310 ppm by volume on a dry 1 hr minimum sampling time. biomass/bio-based CEMS) lb per MWh; 3-run basis corrected to 3-percent solids average oxygen,<sup>d</sup> 30-day rolling average) 1.2E-02 lb per MMBtu of steam output or 0.14 b. Filterable 9.8E-03 lb per MMBtu of lb per MWh; or (1.1E-Collect a minimum of 3 dscm heat input; or (8.3E-05<sup>a</sup> lb per PM (or 04<sup>a</sup> lb per MMBtu of per run. TSM) MMBtu of heat input) steam output or 1.2E-03<sup>a</sup> lb per MWh) 2,400 ppm by volume on a dry basis corrected to 3-10. Suspension percent oxygen, 3-run 1.9 lb per MMBtu of burners designed to a. CO (or average; or (2,000 ppm by steam output or 27 lb 1 hr minimum sampling time. burn biomass/biovolume on a dry basis per MWh; 3-run CEMS) based solids corrected to 3-percent average oxygen,<sup>d</sup> 10-day rolling average)

	[Units with heat input capacity of 10 million Btu per hour or greater]					
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 		
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input)	3.1E-02 lb per MMBtu of steam output or 4.2E-01 lb per MWh; or (6.6E-03 lb per MMBtu of steam output or 9.1E-02 lb per MWh)	Collect a minimum of 2 dscm per run.		
11. Dutch Ovens/Pile burners designed to burn biomass/bio- based solids	a. CO (or CEMS)	330 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 10-day rolling average)	3.5E-01 lb per MMBtu of steam output or 3.6 lb per MWh; 3-run average	1 hr minimum sampling time.		
	b. Filterable PM (or TSM)	3.2E-03 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input)	4.3E-03 lb per MMBtu of steam output or 4.5E-02 lb per MWh; or (5.2E-05 lb per MMBtu of steam output or 5.5E-04 lb per MWh)	Collect a minimum of 3 dscm per run.		
12. Fuel cell units designed to burn biomass/bio-based solids	a. CO	910 ppm by volume on a dry basis corrected to 3-percent oxygen	1.1 lb per MMBtu of steam output or 1.0E+01 lb per MWh	1 hr minimum sampling time.		
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	3.0E-02 lb per MMBtu of steam output or 2.8E-01 lb per MWh; or (5.1E-05 lb per MMBtu of steam output or 4.1E-04 lb per MWh)	Collect a minimum of 2 dscm per run.		
13. Hybrid suspension grate boiler designed to burn biomass/bio- based solids	a. CO (or CEMS)	1,100 ppm by volume on a dry basis corrected to 3- percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>d</sup> 30-day rolling average)	1.4 lb per MMBtu of steam output or 12 lb per MWh; 3-run average	1 hr minimum sampling time.		
	b. Filterable PM (or TSM)	2.6E-02 lb per MMBtu of heat input; or (4.4E-04 lb per MMBtu of heat input)	3.3E-02 lb per MMBtu of steam output or 3.7E-01 lb per MWh; or (5.5E-04 lb per	Collect a minimum of 3 dscm per run.		

	[Units with heat input capacity of 10 million Btu per hour or greater]					
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 		
			MMBtu of steam output or 6.2E-03 lb per MWh)			
14. Units designed to burn liquid fuel	a. HCl	4.4E-04 lb per MMBtu of heat input	4.8E-04 lb per MMBtu of steam output or 6.1E-03 lb per MWh	For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.		
	b. Mercury	4.8E-07ª lb per MMBtu of heat input	5.3E-07 <sup>a</sup> lb per MMBtu of steam output or 6.7E-06 <sup>a</sup> lb per MWh	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 4 dscm.		
15. Units designed to burn heavy liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average	0.13 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.		
	b. Filterable PM (or TSM)	1.3E-02 lb per MMBtu of heat input; or (7.5E-05 <sup>a</sup> lb per MMBtu of heat input)	1.5E-02 lb per MMBtu of steam output or 1.8E-01 lb per MWh; or (8.2E-05 <sup>a</sup> lb per MMBtu of steam output or 1.1E-03 <sup>a</sup> lb per MWh)	Collect a minimum of 3 dscm per run.		
16. Units designed to burn light liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen	0.13 lb per MMBtu of steam output or 1.4 lb per MWh	1 hr minimum sampling time.		
	b. Filterable PM (or TSM)	1.1E-03 <sup>a</sup> lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	1.2E-03 <sup>a</sup> lb per MMBtu of steam output or 1.6E-02 <sup>a</sup> lb per MWh; or (3.2E-05 lb per MMBtu of steam output or 4.0E-04 lb per MWh)	Collect a minimum of 3 dscm per run.		
17. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average based on stack test	0.13 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.		
	b. Filterable PM (or TSM)	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)	2.5E-02 lb per MMBtu of steam output or 3.2E-01 lb per MWh; or (9.4E-04 lb per MMBtu of steam	Collect a minimum of 4 dscm per run.		

[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants	The emissions must not exceed the following emission limits, except during startup and shutdown	Or the emissions must not exceed the following alternative output- based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 
			output or 1.2E-02 lb per MWh)	
18. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3-percent oxygen	0.16 lb per MMBtu of steam output or 1.0 lb per MWh	1 hr minimum sampling time.
	b. HCl	1.7E-03 lb per MMBtu of heat input	2.9E-03 lb per MMBtu of steam output or 1.8E-02 lb per MWh	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	1.4E-05 lb per MMBtu of steam output or 8.3E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.
	d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	1.2E-02 lb per MMBtu of steam output or 7.0E-02 lb per MWh; or (3.5E-04 lb per MMBtu of steam output or 2.2E-03 lb per MWh)	Collect a minimum of 3 dscm per run.

<sup>a</sup> If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to  $\frac{63.7515}{10}$  if all of the other provisions of  $\frac{63.7515}{10}$  are met. For all other pollutants that do not contain a footnote "a", your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

<sup>b</sup> Incorporated by reference, see <u>§ 63.14</u>.

<sup>c</sup> If your affected source is a new or reconstructed affected source that commenced construction or reconstruction after June 4, 2010, and before April 1, 2013, you may comply with the emission limits in Table 11, 12, or 13 to this subpart until January 31, 2016. On and after January 31, 2016, but before October 6, 2025 you may comply with the emission limits in this Table 14. On and after October 6, 2025, you must comply with the emission limits in Table 1 to this subpart.

<sup>d</sup> An owner or operator may determine compliance with the carbon monoxide emissions limit using carbon dioxide as a diluent correction in place of oxygen as described in § 63.7525(a)(1). EPA Method 19 F-factors in <u>40 CFR part 60, appendix</u> <u>A</u>-7, and EPA Method 19 equations in <u>40 CFR part 60, appendix A</u>-7, must be used to generate the appropriate CO<sub>2</sub> correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The methodology must account for any CO<sub>2</sub> being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. This methodology must be detailed in the site-specific monitoring plan developed according to § 63.7505(d).

[87 FR 60860, Oct. 6, 2022]

Table 15 to Subpart DDDDD of Part 63—Alternative Emission Limits for Existing Boilers and Process Heaters<sup>d</sup>

# National Emission Standards for Hazardous Air Pollutants for Boilers and Process Heaters

As stated in <u>§ 63.7500</u>, you may continue to comply with following emission limits until October 6, 2025:

[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants . 	The emissions must not exceed the following emission limits, except during startup and shutdown	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 
1. Units in all subcategories designed to burn solid fuel	a. HCl	2.2E-02 lb per MMBtu of heat input	2.5E-02 lb per MMBtu of steam output or 0.27 lb per MWh	For M26A, Collect a minimum of 1 dscm per run; for M26, collect a minimum of 120 liters per run.
	b. Mercury	5.7E-06 lb per MMBtu of heat input	6.4E-06 lb per MMBtu of steam output or 7.3E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 3 dscm.
2. Units design to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	4.0E-02 lb per MMBtu of heat input; or (5.3E-05 lb per MMBtu of heat input)	4.2E-02 lb per MMBtu of steam output or 4.9E-01 lb per MWh; or (5.6E-05 lb per MMBtu of steam output or 6.5E-04 lb per MWh)	Collect a minimum of 2 dscm per run.
3. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3-percent oxygen, ° 30-day rolling average)	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
4. Stokers/others designed to burn coal/solid fossil fuel	a. CO (or CEMS)	160 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3- percent oxygen, <sup>c</sup> 30-day rolling average)	0.14 lb per MMBtu of steam output or 1.7 lb per MWh; 3-run average	1 hr minimum sampling time.
5. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3- percent oxygen, <sup>c</sup> 30-day rolling average)	0.12 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
6. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 30-day rolling	1.3E-01 lb per MMBtu of steam output or 1.5 lb per MWh; 3-run average	1 hr minimum sampling time.

[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants . 	The emissions must not exceed the following emission limits, except during startup and shutdown	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 
		average)		
7. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	1,500 ppm by volume on a dry basis corrected to 3- percent oxygen, 3-run average; or (720 ppm by volume on a dry basis corrected to 3-percent oxygen, <sup>c</sup> 30-day rolling average)	1.4 lb per MMBtu of steam output or 17 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.7E-02 lb per MMBtu of heat input; or (2.4E-04 lb per MMBtu of heat input)	4.3E-02 lb per MMBtu of steam output or 5.2E-01 lb per MWh; or (2.8E-04 lb per MMBtu of steam output or 3.4E-04 lb per MWh)	Collect a minimum of 2 dscm per run.
8. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	460 ppm by volume on a dry basis corrected to 3-percent oxygen	4.2E-01 lb per MMBtu of steam output or 5.1 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.2E-01 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat input)	3.7E-01 lb per MMBtu of steam output or 4.5 lb per MWh; or (4.6E- 03 lb per MMBtu of steam output or 5.6E-02 lb per MWh)	Collect a minimum of 1 dscm per run.
9. Fluidized bed units designed to burn biomass/bio-based solid	a. CO (or CEMS)	470 ppm by volume on a dry basis corrected to 3-percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3- percent oxygen, <sup>c</sup> 30-day rolling average)	4.6E-01 lb per MMBtu of steam output or 5.2 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-01 lb per MMBtu of heat input; or (1.2E-03 lb per MMBtu of heat input)	1.4E-01 lb per MMBtu of steam output or 1.6 lb per MWh; or (1.5E- 03 lb per MMBtu of steam output or 1.7E-02 lb per MWh)	Collect a minimum of 1 dscm per run.
10. Suspension burners designed to burn biomass/bio- based solid	a. CO (or CEMS)	2,400 ppm by volume on a dry basis corrected to 3- percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3-percent oxygen. <sup>c</sup> 10-day rolling	1.9 lb per MMBtu of steam output or 27 lb per MWh; 3-run average	1 hr minimum sampling time.

#### [Units with heat input capacity of 10 million Btu per hour or greater] The emissions must The emissions must not If your boiler or For the not exceed the exceed the following Using this specified sampling process heater is in following following alternative volume or test run duration. emission limits, except this pollutants. output-based limits, during startup and subcategory ... except during startup •• shutdown . . . and shutdown . . . average) 5.2E-02 lb per MMBtu of steam output or b. Filterable 5.1E-02 lb per MMBtu of 7.1E-01 lb per MWh; or Collect a minimum of 2 dscm PM (or heat input; or (6.5E-03 lb per (6.6E-03 lb per MMBtu per run. TSM) MMBtu of heat input) of steam output or 9.1E-02 lb per MWh) 770 ppm by volume on a dry basis corrected to 3-percent 11. Dutch Ovens/Pile 8.4E-01 lb per MMBtu oxygen, 3-run average; or burners designed to a. CO (or of steam output or 8.4 (520 ppm by volume on a dry 1 hr minimum sampling time. burn biomass/bio-CEMS) lb per MWh; 3-run basis corrected to 3-percent based solid average oxygen,<sup>c</sup> 10-day rolling average) 3.9E-01 lb per MMBtu of steam output or 3.9 b. Filterable 2.8E-01 lb per MMBtu of lb per MWh; or (2.8E-Collect a minimum of 1 dscm heat input; or (2.0E-03 lb per PM (or 03 lb per MMBtu of per run. MMBtu of heat input) TSM) steam output or 2.8E-02 lb per MWh) 12. Fuel cell units 2.4 lb per MMBtu of 1,100 ppm by volume on a designed to burn a. CO dry basis corrected to 3steam output or 12 lb 1 hr minimum sampling time. biomass/bio-based percent oxygen per MWh solid 5.5E-02 lb per MMBtu of steam output or b. Filterable 2.0E-02 lb per MMBtu of 2.8E-01 lb per MWh; or Collect a minimum of 2 dscm PM (or heat input; or (5.8E-03 lb per (1.6E-02 lb per MMBtu per run. TSM) MMBtu of heat input) of steam output or 8.1E-02 lb per MWh) 3,500 ppm by volume on a dry basis corrected to 3-13. Hybrid suspension percent oxygen, 3-run 3.5 lb per MMBtu of grate units designed to average; or (900 ppm by steam output or 39 lb a. CO (or 1 hr minimum sampling time. burn biomass/bio-CEMS) volume on a dry basis per MWh; 3-run based solid corrected to 3- percent average oxygen,<sup>c</sup> 30-day rolling average) 5.5E-01 lb per MMBtu of steam output or 6.2 b. Filterable 4.4E-01 lb per MMBtu of lb per MWh; or (5.7E-Collect a minimum of 1 dscm PM (or heat input; or (4.5E-04 lb per 04 lb per MMBtu of per run. TSM) MMBtu of heat input) steam output or 6.3E-03 lb per MWh) 1.4E-03 lb per MMBtu For M26A, collect a minimum a. HCl 1.1E-03 lb per MMBtu of 14. Units designed to

#### [Units with heat input capacity of 10 million Btu per hour or greater] The emissions must The emissions must not If your boiler or For the not exceed the Using this specified sampling exceed the following process heater is in following following alternative volume or test run duration. emission limits, except this pollutants. output-based limits, during startup and subcategory .... except during startup . . shutdown . . . and shutdown . . . burn liquid fuel of steam output or heat input of 2 dscm per run; for M26, 1.6E-02 lb per MWh collect a minimum of 240 liters per run. For M29, collect a minimum of 3 dscm per run; for M30A or 2.5E-06 lb per MMBtu M30B collect a minimum 2.0E-06 lb per MMBtu of of steam output or sample as specified in the b. Mercury heat input method, for ASTM 2.8E-05 lb per MWh D6784<sup>b</sup> collect a minimum of 2 dscm. 0.13 lb per MMBtu of 130 ppm by volume on a dry steam output or 1.4 lb 15. Units designed to a. CO 1 hr minimum sampling time. basis corrected to 3-percent burn heavy liquid fuel per MWh; 3-run oxygen, 3-run average average 7.5E-02 lb per MMBtu of steam output or b. Filterable 6.2E-02 lb per MMBtu of 8.6E-01 lb per MWh; or Collect a minimum of 1 dscm PM (or heat input; or (2.0E-04 lb per (2.5E-04 lb per MMBtu per run. TSM) MMBtu of heat input) of steam output or 2.8E-03 lb per MWh) 0.13 lb per MMBtu of 130 ppm by volume on a dry 16. Units designed to a. CO basis corrected to 3-percent steam output or 1.4 lb 1 hr minimum sampling time. burn light liquid fuel oxygen per MWh 9.6E-03 lb per MMBtu of steam output or b. Filterable 7.9E-03 lb per MMBtu of 1.1E-01 lb per MWh; or Collect a minimum of 3 dscm heat input; or (6.2E-05 lb per PM (or (7.5E-05 lb per MMBtu per run. TSM) MMBtu of heat input) of steam output or 8.6E-04 lb per MWh) 0.13 lb per MMBtu of 17. Units designed to 130 ppm by volume on a dry burn liquid fuel that basis corrected to 3-percent steam output or 1.4 lb a. CO 1 hr minimum sampling time. are non-continental oxygen, 3-run average based per MWh; 3-run units on stack test average 3.3E-01 lb per MMBtu of steam output or 3.8 b. Filterable 2.7E-01 lb per MMBtu of lb per MWh; or (1.1E-Collect a minimum of 2 dscm heat input; or (8.6E-04 lb per PM (or 03 lb per MMBtu of per run. TSM) MMBtu of heat input) steam output or 1.2E-02 lb per MWh) 0.16 lb per MMBtu of 18. Units designed to 130 ppm by volume on a dry burn gas 2 (other) a. CO basis corrected to 3-percent steam output or 1.0 lb 1 hr minimum sampling time. gases oxygen per MWh 1.7E-03 lb per MMBtu of 2.9E-03 lb per MMBtu For M26A, collect a minimum b. HCl heat input of steam output or of 2 dscm per run; for M26,

[Units with heat input capacity of 10 million Btu per hour or greater]				
If your boiler or process heater is in this subcategory	For the following pollutants . 	The emissions must not exceed the following emission limits, except during startup and shutdown	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown	Using this specified sampling volume or test run duration . 
			1.8E-02 lb per MWh	collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	1.4E-05 lb per MMBtu of steam output or 8.3E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 <sup>b</sup> collect a minimum of 2 dscm.
	d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input or (2.1E-04 lb per MMBtu of heat input)	1.2E-02 lb per MMBtu of steam output or 7.0E-02 lb per MWh; or (3.5E-04 lb per MMBtu of steam output or 2.2E-03 lb per MWh)	Collect a minimum of three dscm per run.

<sup>a</sup> If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to  $\frac{63.7515}{10}$  if all of the other provisions of  $\frac{63.7515}{10}$  are met. For all other pollutants that do not contain a footnote a, your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

<sup>b</sup> Incorporated by reference, see  $\S$  <u>63.14</u>.

<sup>c</sup> An owner or operator may determine compliance with the carbon monoxide emissions limit using carbon dioxide as a diluent correction in place of oxygen as described in § 63.7525(a)(1). EPA Method 19 F-factors in <u>40 CFR part 60, appendix</u> <u>A</u>-7, and EPA Method 19 equations in <u>40 CFR part 60, appendix A</u>-7, must be used to generate the appropriate CO<sub>2</sub> correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The methodology must account for any CO<sub>2</sub> being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc. This methodology must be detailed in the site-specific monitoring plan developed according to § 63.7505(d).

<sup>d</sup> Before October 6, 2025 you may comply with the emission limits in this Table 15. On and after October 6, 2025, you must comply with the emission limits in Table 2 to this subpart.

[<u>87 FR 60863</u>, Oct. 6, 2022]

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### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

# Subpart F—National Emission Standards for Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

Source:

59 FR 19454, Apr. 22, 1994, unless otherwise noted.

### § 63.100 Applicability and designation of source.

(a) This subpart provides applicability provisions, definitions, and other general provisions that are applicable to <u>subparts</u> <u>G</u> and <u>H of this part</u>. This subpart also provides requirements for certain heat exchange systems, maintenance wastewater, and flares.

(b) Except as provided in <u>paragraphs (b)(4)</u> and (c) of this section, the provisions of <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> apply to chemical manufacturing process units that meet all the criteria specified in <u>paragraphs (b)(1)</u>, (b)(2), and (b)(3) of this section:

(1) Manufacture as a primary product one or more of the chemicals listed in <u>paragraphs (b)(1)(i)</u> or (b)(1)(i) of this section.

(i) One or more of the chemicals listed in table 1 of this subpart; or

(ii) One or more of the chemicals listed in paragraphs (b)(1)(ii)(A) or (b)(1)(ii)(B) of this section:

(A) Tetrahydrobenzaldehyde (CAS Number 100-50-5); or

(B) Crotonaldehyde (CAS Number 123-73-9).

(2) Use as a reactant or manufacture as a product, or co-product, one or more of the organic hazardous air pollutants listed in table 2 of this subpart;

(3) Are located at a plant site that is a major source as defined in section 112(a) of the Act.

(4) The owner or operator of a chemical manufacturing processing unit is exempt from all requirements of <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> until not later than April 22, 1997 if the owner or operator certifies, in a notification to the appropriate EPA Regional Office, not later than May 14, 1996, that the plant site at which the chemical manufacturing processing unit is located emits, and will continue to emit, during any 12-month period, less than 10 tons per year of any individual hazardous air pollutants (HAP), and less than 25 tons per year of any combination of HAP.

(i) If such a determination is based on limitations and conditions that are not federally enforceable (as defined in subpart A of this part), the owner or operator shall document the basis for the determination as specified in paragraphs (b)(4)(i)(A) through (b)(4)(i)(C) and comply with the recordkeeping requirement in 63.103(f).

(A) The owner or operator shall identify all HAP emission points at the plant site, including those emission points subject to and emission points not subject to subparts F, G, and H;

(B) The owner or operator shall calculate the amount of annual HAP emissions released from each emission point at the plant site, using acceptable measurement or estimating techniques for maximum expected operating conditions at the plant site. Examples of estimating procedures that are considered acceptable include the calculation procedures in  $\S$  63.150 of subpart G, the early reduction demonstration procedures specified in  $\S$  63.74 (c)(2), (c)(3), (d)(2), (d)(3), and (g), or accepted engineering practices. If the total annual HAP emissions for the plant site are annually reported under Emergency Planning and Community Right-to-Know Act (EPCRA) section 313, then such reported annual emissions may be used to satisfy the requirements of  $\S$  63.100(b)(4)(i)(B).

(C) The owner or operator shall sum the amount of annual HAP emissions from all emission points on the plant site. If the total emissions of any one HAP are less than 10 tons per year and the total emissions of any combination of HAP are less than 25 tons per year, the plant site qualifies for the exemption described in <u>paragraph (b)(4)</u> of this section, provided that emissions are kept below these thresholds.

(ii) If such a determination is based on limitations and conditions that are federally enforceable (as defined in subpart A of this part), the owner or operator is not subject to the provisions of paragraph (b)(4) of this section.

(c) The owner or operator of a chemical manufacturing process unit that meets the criteria specified in <u>paragraphs</u> (b)(1) and (b)(3) of this section but does not use as a reactant or manufacture as a product or co-product, any organic

### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

hazardous air pollutant listed in table 2 of this subpart shall comply only with the requirements of  $\frac{63.103(e)}{100}$  of this subpart. To comply with this subpart, such chemical manufacturing process units shall not be required to comply with the provisions of subpart A of this part.

(d) The primary product of a chemical manufacturing process unit shall be determined according to the procedures specified in paragraphs (d)(1), (d)(2), (d)(3), and (d)(4) of this section.

(1) If a chemical manufacturing process unit produces more than one intended chemical product, the product with the greatest annual design capacity on a mass basis determines the primary product of the process.

(2) If a chemical manufacturing process unit has two or more products that have the same maximum annual design capacity on a mass basis and if one of those chemicals is listed in table 1 of this subpart, then the listed chemical is considered the primary product and the chemical manufacturing process unit is subject to this subpart. If more than one of the products is listed in table 1 of this subpart, then the owner or operator may designate as the primary product any of the listed chemicals and the chemical manufacturing process unit is subject to this subpart.

(3) For chemical manufacturing process units that are designed and operated as flexible operation units producing one or more chemicals listed in table 1 of this subpart, the primary product shall be determined for existing sources based on the expected utilization for the five years following April 22, 1994 and for new sources based on the expected utilization for the first five years after initial start-up.

(i) If the predominant use of the flexible operation unit, as described in <u>paragraphs (d)(3)(i)(A)</u> and  $(\underline{d})(\underline{3})(\underline{i})(\underline{B})$  of this section, is to produce one or more chemicals listed in table 1 of this subpart, then the flexible operation unit shall be subject to the provisions of <u>subparts F, G</u>, and <u>H of this part</u>.

(A) If the flexible operation unit produces one product for the greatest annual operating time, then that product shall represent the primary product of the flexible operation unit.

(B) If the flexible operation unit produces multiple chemicals equally based on operating time, then the product with the greatest annual production on a mass basis shall represent the primary product of the flexible operation unit.

(ii) The determination of applicability of this subpart to chemical manufacturing process units that are designed and operated as flexible operation units shall be reported as part of an operating permit application or as otherwise specified by the permitting authority.

(4) Notwithstanding the provisions of <u>paragraph (d)(3)</u> of this section, for chemical manufacturing process units that are designed and operated as flexible operation units producing a chemical listed in <u>paragraph (b)(1)(ii)</u> of this section, the primary product shall be determined for existing sources based on the expected utilization for the five years following May 12, 1998 and for new sources based on the expected utilization for the first five years after initial start-up.

(i) The predominant use of the flexible operation unit shall be determined according to <u>paragraphs</u> (d)(3)(i)(A) and (d)(3)(i)(B) of this section. If the predominant use is to produce one of the chemicals listed in <u>paragraph</u> (b)(1)(ii) of this section, then the flexible operation unit shall be subject to the provisions of this subpart and <u>subparts</u> <u>G</u> and <u>H of this part</u>.

(ii) The determination of applicability of this subpart to chemical manufacturing process units that are designed and operated as flexible operation units shall be reported as part of an operating permit application or as otherwise specified by the permitting authority.

(e) The source to which this subpart applies is the collection of all chemical manufacturing process units and the associated equipment at a major source that meet the criteria specified in <u>paragraphs (b)(1)</u> through (3) of this section. The source includes the process vents; storage vessels; transfer racks; waste management units; maintenance wastewater; heat exchange systems; equipment identified in § 63.149; and pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, instrumentation systems, surge control vessels, and bottoms receivers that are associated with that collection of chemical manufacturing process units. The source also includes equipment required by, or utilized as a method of compliance with, <u>subparts F, G</u>, or <u>H of this part</u> which may include control devices and recovery devices.

(1) This subpart applies to maintenance wastewater and heat exchange systems within a source that is subject to this subpart; and also applies to flares used to reduce organic HAP emissions from a source.

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(2) This subpart F and subpart G of this part apply to process vents, storage vessels, transfer racks, equipment identified in § 63.149 of subpart G of this part, and wastewater streams and associated treatment residuals within a source that is subject to this subpart.

(3) This subpart and subpart H of this part apply to pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, instrumentation systems, surge control vessels, and bottoms receivers within a source that is subject to this subpart. Subpart H also contains fenceline monitoring requirements that apply to all emission sources (*i.e.*, maintenance wastewater, heat exchange systems, process vents, storage vessels, transfer racks, equipment identified in § 63.149, wastewater streams and associated treatment residuals within a source, and pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, instrumentation systems, surge control vessels, and bottoms receivers within a source). If specific items of equipment, comprising part of a chemical manufacturing process unit subject to this subpart, are managed by different administrative organizations (*e.g.*, different companies, affiliates, departments, divisions, etc.), those items of equipment may be aggregated with any chemical manufacturing process unit within the source for all purposes under subpart H, providing there is no delay in the applicable compliance date in § 63.100(k).

(f) The source includes the emission points listed in <u>paragraphs (f)(1)</u> through (f)(11) of this section, but those emission points are not subject to the requirements of this subpart F and <u>subparts G</u> and <u>H of this part</u>. This subpart does not require emission points that are listed in <u>paragraphs (f)(1)</u> through (f)(11) of this section to comply with the provisions of <u>subpart A</u> of this part.

(1) Equipment that is located within a chemical manufacturing process unit that is subject to this subpart but the equipment does not contain organic hazardous air pollutants.

(2) Stormwater from segregated sewers;

- (3) Water from fire-fighting and deluge systems in segregated sewers;
- (4) Spills;
- (5) Water from safety showers;
- (6) Water from testing of deluge systems;
- (7) Water from testing of firefighting systems;

(8) Except for storage vessels in ethylene oxide service, vessels storing organic liquids that contain organic hazardous air pollutants only as impurities;

(9) Loading racks, loading arms, or loading hoses that only transfer liquids containing organic hazardous air pollutants as impurities;

(10) Loading racks, loading arms, or loading hoses that vapor balance during all loading operations; and

(11) Equipment that is intended to operate in organic hazardous air pollutant service, as defined in  $\S$  63.101, for less than 300 hours during the calendar year.

(g) The owner or operator shall follow the procedures specified in <u>paragraphs (g)(1)</u> through (g)(4) of this section to determine whether a storage vessel is part of the source to which this subpart applies.

(1) Where a storage vessel is dedicated to a chemical manufacturing process unit, the storage vessel shall be considered part of that chemical manufacturing process unit.

(i) If the chemical manufacturing process unit is subject to this subpart according to the criteria specified in <u>paragraph (b)</u> of this section, then the storage vessel is part of the source to which this subpart applies.

(ii) If the chemical manufacturing process unit is not subject to this subpart according to the criteria specified in <u>paragraph</u> (b) of this section, then the storage vessel is not part of the source to which this subpart applies.

(2) If a storage vessel is not dedicated to a single chemical manufacturing process unit, then the applicability of this subpart F and subpart G of this part shall be determined according to the provisions in paragraphs (g)(2)(i) through (g)(2)(ii) of this section.

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(i) If a storage vessel is shared among chemical manufacturing process units and one of the process units has the predominant use, as determined by paragraph(g)(2)(i)(A) and (g)(2)(i)(B) of this section, then the storage vessel is part of that chemical manufacturing process unit.

(A) If the greatest input into the storage vessel is from a chemical manufacturing process unit that is located on the same plant site, then that chemical manufacturing process unit has the predominant use.

(B) If the greatest input into the storage vessel is provided from a chemical manufacturing process unit that is not located on the same plant site, then the predominant use is the chemical manufacturing process unit on the same plant site that receives the greatest amount of material from the storage vessel.

(ii) If a storage vessel is shared among chemical manufacturing process units so that there is no single predominant use, and at least one of those chemical manufacturing process units is subject to this subpart, the storage vessel shall be considered to be part of the chemical manufacturing process unit that is subject to this subpart. If more than one chemical manufacturing process unit is subject to this subject to any of the chemical manufacturing manufacturing process units is subject to this subject.

(iii) If the predominant use of a storage vessel varies from year to year, then the applicability of this subpart shall be determined according to the criteria in paragraphs (g)(2)(iii)(A) and (g)(2)(iii)(B) of this section, as applicable. This determination shall be reported as part of an operating permit application or as otherwise specified by the permitting authority.

(A) For chemical manufacturing process units that produce one or more of the chemicals listed in table 1 of this subpart and meet the criteria in <u>paragraphs (b)(2)</u> and (b)(3) of this section, the applicability shall be based on the utilization that occurred during the 12-month period preceding April 22, 1994.

(B) For chemical manufacturing process units that produce one or more of the chemicals listed in <u>paragraph (b)(1)(ii)</u> of this section and meet the criteria in <u>paragraphs (b)(2)</u> and (b)(3) of this section, the applicability shall be based on the utilization that occurred during the 12-month period preceding May 12, 1998.

(iv) If there is a change in the material stored in the storage vessel, the owner or operator shall reevaluate the applicability of this subpart to the vessel.

(3) Where a storage vessel is located at a major source that includes one or more chemical manufacturing process units which place material into, or receive materials from the storage vessel, but the storage vessel is located in a tank farm (including a marine tank farm), the applicability of this subpart F and subpart G of this part shall be determined according to the provisions in paragraphs (g)(3)(i) through (g)(3)(iv) of this section.

(i) The storage vessel may only be assigned to a chemical manufacturing process unit that utilizes the storage vessel and does not have an intervening storage vessel for that product (or raw material, as appropriate). With respect to any chemical manufacturing process unit, an intervening storage vessel means a storage vessel connected by hard-piping to the chemical manufacturing process unit and to the storage vessel in the tank farm so that product or raw material entering or leaving the chemical manufacturing process unit flows into (or from) the intervening storage vessel and does not flow directly into (or from) the storage vessel in the tank farm.

(ii) If there is no chemical manufacturing process unit at the major source that meets the criteria of <u>paragraph (g)(3)(i)</u> of this section with respect to a storage vessel, this subpart F and <u>subpart G of this part</u> do not apply to the storage vessel.

(iii) If there is only one chemical manufacturing process unit at the major source that meets the criteria of <u>paragraph</u> (g)(3)(i) of this section with respect to a storage vessel, the storage vessel shall be assigned to that chemical manufacturing process unit. Applicability of this subpart F and subpart G to this part to the storage vessel shall then be determined according to the provisions of <u>paragraph</u> (b) of this section.

(iv) If there are two or more chemical manufacturing process units at the major source that meet the criteria of <u>paragraph</u> (g)(3)(i) of this section with respect to a storage vessel, the storage vessel shall be assigned to one of those chemical manufacturing process units according to the provisions of <u>paragraph</u> (g)(2) of this section. The predominant use shall be determined among only those chemical manufacturing process units that meet the criteria of <u>paragraph</u> (g)(3)(i) of this section. Applicability of this subpart F and <u>subpart G of this part</u> to the storage vessel shall then be determined according to the provisions of <u>paragraph</u> (g)(3)(i) of this section.

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(4) If the storage vessel begins receiving material from (or sending material to) another chemical manufacturing process unit, or ceases to receive material from (or send material to) a chemical manufacturing process unit, or if the applicability of this subpart F and subpart G of this part to a storage vessel has been determined according to the provisions of paragraphs (g)(2)(i) and (g)(2)(ii) of this section and there is a change so that the predominant use may reasonably have changed, the owner or operator shall reevaluate the applicability of this subpart to the storage vessel.

(h) The owner or operator shall follow the procedures specified in <u>paragraphs (h)(1)</u> and (h)(2) of this section to determine whether the arms and hoses in a loading rack are part of the source to which this subpart applies.

(1) Where a loading rack is dedicated to a chemical manufacturing process unit, the loading rack shall be considered part of that specific chemical manufacturing process unit.

(i) If the chemical manufacturing process unit is subject to this subpart according to the criteria specified in <u>paragraph (b)</u> of this section and the loading rack does not meet the criteria specified in <u>paragraphs (f)(9)</u> and <u>(f)(10)</u> of this section, then the loading rack is considered a transfer rack (as defined in <u>§ 63.101 of this subpart</u>) and is part of the source to which this subpart applies.

(ii) If the chemical manufacturing process unit is not subject to this subpart according to the criteria specified in <u>paragraph</u> (b) of this section, then the loading rack is not considered a transfer rack (as defined in  $\S$  63.101 of this subpart) and is not a part of the source to which this subpart applies.

(2) If a loading rack is shared among chemical manufacturing process units, then the applicability of this subpart F and subpart G of this part shall be determined at each loading arm or loading hose according to the provisions in paragraphs (h)(2)(i) through (h)(2)(iv) of this section.

(i) Each loading arm or loading hose that is dedicated to the transfer of liquid organic hazardous air pollutants listed in table 2 of this subpart from a chemical manufacturing process unit to which this subpart applies is part of that chemical manufacturing process unit and is part of the source to which this subpart applies unless the loading arm or loading hose meets the criteria specified in paragraphs (f)(9) or (f)(10) of this section.

(ii) If a loading arm or loading hose is shared among chemical manufacturing process units, and one of the chemical manufacturing process units provides the greatest amount of the material that is loaded by the loading arm or loading hose, then the loading arm or loading hose is part of that chemical manufacturing process unit.

(A) If the chemical manufacturing process unit is subject to this subpart according to the criteria specified in <u>paragraph (b)</u> of this section, then the loading arm or loading hose is part of the source to which this subpart applies unless the loading arm or loading hose meets the criteria specified in <u>paragraphs (f)(9)</u> or <u>(f)(10)</u> of this section.

(B) If the chemical manufacturing process unit is not subject to this subpart according to the criteria specified in <u>paragraph</u> (b) of this section, then the loading arm or loading hose is not part of the source to which this subpart applies.

(iii) If a loading arm or loading hose is shared among chemical manufacturing process units so that there is no single predominant use as described in paragraph (h)(2)(ii) of this section and at least one of those chemical manufacturing process units is subject to this subpart, then the loading arm or hose is part of the chemical manufacturing process unit that is subject to this subpart. If more than one of the chemical manufacturing process units is subject to this subpart, the owner or operator may assign the loading arm or loading hose to any of the chemical manufacturing process units subject to this subpart.

(iv) If the predominant use of a loading arm or loading hose varies from year to year, then the applicability of this subpart shall be determined according to the criteria in paragraphs (h)(2)(iv)(A) and (h)(2)(iv)(B) of this section, as applicable. This determination shall be reported as part of an operating permit application or as otherwise specified by the permitting authority.

(A) For chemical manufacturing process units that produce one or more of the chemicals listed in table 1 of this subpart and meet the criteria in <u>paragraphs (b)(2)</u> and (b)(3) of this section, the applicability shall be based on the utilization that occurred during the 12-month period preceding April 22, 1994.

(B) For chemical manufacturing process units that produce one or more of the chemicals listed in <u>paragraph (b)(1)(ii)</u> of this section and meet the criteria in <u>paragraphs (b)(2)</u> and (b)(3) of this section, the applicability shall be based on the utilization that occurred during the year preceding May 12, 1998.

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(3) If a loading rack that was dedicated to a single chemical manufacturing process unit begins to serve another chemical manufacturing process unit, or if applicability was determined under the provisions of <u>paragraphs</u> (h)(2)(i) through (h)(2)(iii) of this section and there is a change so that the predominant use may reasonably have changed, the owner or operator shall reevaluate the applicability of this subpart to the loading rack, loading arm, or loading hose.

(i) Except as provided in paragraph (i)(4) of this section, the owner or operator shall follow the procedures specified in paragraphs (i)(1) through (i)(3) and (i)(5) of this section to determine whether the vent(s) from a distillation unit is part of the source to which this subpart applies.

(1) Where a distillation unit is dedicated to a chemical manufacturing process unit, the distillation column shall be considered part of that chemical manufacturing process unit.

(i) If the chemical manufacturing process unit is subject to this subpart according to the criteria specified in <u>paragraph (b)</u> of this section, then the distillation unit is part of the source to which this subpart applies.

(ii) If the chemical manufacturing process unit is not subject to this subpart according to the criteria specified in <u>paragraph</u> (b) of this section, then the distillation unit is not part of the source to which this subpart applies.

(2) If a distillation unit is not dedicated to a single chemical manufacturing process unit, then the applicability of this subpart and subpart G of this part shall be determined according to the provisions in paragraphs (i)(2)(i) through (i)(2)(iv) of this section.

(i) If the greatest input to the distillation unit is from a chemical manufacturing process unit located on the same plant site, then the distillation unit shall be assigned to that chemical manufacturing process unit.

(ii) If the greatest input to the distillation unit is provided from a chemical manufacturing process unit that is not located on the same plant site, then the distillation unit shall be assigned to the chemical manufacturing process unit located at the same plant site that receives the greatest amount of material from the distillation unit.

(iii) If a distillation unit is shared among chemical manufacturing process units so that there is no single predominant use as described in <u>paragraphs (i)(2)(i)</u> and <u>(i)(2)(ii)</u> of this section, and at least one of those chemical manufacturing process units is subject to this subpart, the distillation unit shall be assigned to the chemical manufacturing process unit that is subject to this subpart. If more than one chemical manufacturing process unit is subject to this subpart, the owner or operator may assign the distillation unit to any of the chemical manufacturing process units subject to this subpart.

(iv) If the predominant use of a distillation unit varies from year to year, then the applicability of this subpart shall be determined according to the criteria in paragraphs (i)(2)(iv)(A) and (i)(2)(iv)(B), as applicable. This determination shall be included as part of an operating permit application or as otherwise specified by the permitting authority.

(A) For chemical manufacturing process units that produce one or more of the chemicals listed in table 1 of this subpart and meet the criteria in paragraphs (b)(2) and (b)(3) of this section, the applicability shall be based on the utilization that occurred during the year preceding April 22, 1994.

(B) For chemical manufacturing process units that produce one or more of the chemicals listed in <u>paragraph (b)(1)(ii)</u> of this section and meet the criteria in <u>paragraphs (b)(2)</u> and (b)(3) of this section, the applicability shall be based on the utilization that occurred during the year preceding May 12, 1998.

(3) If the chemical manufacturing process unit to which the distillation unit is assigned is subject to this subpart, then each vent from the individual distillation unit shall be considered separately to determine whether it is a process vent (as defined in  $\S$  63.101 of this subpart). Each vent that is a process vent is part of the source to which this subpart applies.

(4) If the distillation unit is part of one of the chemical manufacturing process units listed in <u>paragraphs</u> (i)(4)(i) through (i)(4)(iii) of this section, then each vent from the individual distillation unit shall be considered separately to determine whether it is a process vent (as defined in § 63.101 of this subpart). Each vent that is a process vent is part of the source to which this subpart applies:

(i) The Aromex unit that produces benzene, toluene, and xylene;

- (ii) The unit that produces hexane; or
- (iii) The unit that produces cyclohexane.

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(5) If a distillation unit that was dedicated to a single chemical manufacturing process unit, or that was part of a chemical manufacturing unit identified in <u>paragraphs (i)(4)(i)</u> through <u>(i)(4)(iii)</u> of this section, begins to serve another chemical manufacturing process unit, or if applicability was determined under the provisions of <u>paragraphs</u> (i)(2)(ii) through (i)(2)(iii) of this section and there is a change so that the predominant use may reasonably have changed, the owner or operator shall reevaluate the applicability of this subpart to the distillation unit.

(j) The provisions of subparts F, G, and H of this part do not apply to the processes specified in paragraphs (j)(1) through (j)(6) of this section. Subparts F, G, and H do not require processes specified in paragraphs (j)(1) through (j)(6) to comply with the provisions of subpart A of this part.

(1) Research and development facilities, regardless of whether the facilities are located at the same plant site as a chemical manufacturing process unit that is subject to the provisions of subparts F, G, or H of this part.

(2) Petroleum refining process units, regardless of whether the units supply feedstocks that include chemicals listed in table 1 of this subpart to chemical manufacturing process units that are subject to the provisions of subparts F, G, or H of this part.

(3) Ethylene production units, regardless of whether the units supply feedstocks that include chemicals listed in table 1 of this subpart to chemical manufacturing process units that are subject to the provisions of subpart F, G, or H of this part.

(4) Batch process vents within a chemical manufacturing process unit.

(5) Chemical manufacturing process units that are located in coke by-product recovery plants.

(6) Solvent reclamation, recovery, or recycling operations at hazardous waste TSDF facilities requiring a permit under <u>40</u> <u>CFR part 270</u> that are separate entities and not part of a SOCMI chemical manufacturing process unit.

(k) Except as provided in <u>paragraphs (1)</u>, (<u>m</u>), and (<u>p</u>) of this section, sources subject to <u>subpart F</u>, <u>G</u>, or <u>H of this part</u> are required to achieve compliance on or before the dates specified in <u>paragraphs (k)(1)</u> through (<u>8</u>) and (<u>10</u>) and (<u>11</u>) of this section.

(1)

(i) New sources that commence construction or reconstruction after December 31, 1992, but before August 27, 1996 shall be in compliance with this subpart F, <u>subparts G</u> and <u>H of this part</u> upon initial start-up or by April 22, 1994, whichever is later, as provided in § 63.6(b) of <u>subpart A of this part</u>, and further, where start-up occurs before January 17, 1997 shall also be in compliance with this subpart F and <u>subparts G</u> and <u>H of this part</u> (as amended on January 17, 1997) by January 17, 1997, except that, with respect to all new sources that commenced construction or reconstruction after December 31, 1992, and before August 27, 1996:

(A) Heat exchange systems and maintenance wastewater, that are part of a new source on which construction or reconstruction commenced after December 31, 1992, but before August 27, 1996, shall be in compliance with this subpart F no later than initial start-up or 180 days after January 17, 1997, whichever is later;

(B) Process wastewater streams and equipment subject to  $\S$  63.149, that are part of a new source on which construction or reconstruction commenced after December 31, 1992, but before August 27, 1996, shall be in compliance with this subpart F and subpart G of this part no later than initial start-up or 180 days after January 17, 1997, whichever is later; and

(ii) New sources that commence construction after August 26, 1996 shall be in compliance with this subpart F, <u>subparts</u> <u>G</u> and <u>H of this part</u> upon initial start-up or by January 17, 1997, whichever is later.

(2) Existing sources shall be in compliance with this subpart F and subpart G of this part no later than the dates specified in paragraphs (k)(2)(i) and (k)(2)(ii) of this section, unless an extension has been granted by the Administrator as provided in § 63.151(a)(6) of subpart G of this part or granted by the permitting authority as provided in § 63.6(i) of subpart A of this part.

(i) Process vents, storage vessels, and transfer racks at an existing source shall be in compliance with the applicable sections of this subpart and <u>subpart G of this part</u> no later than April 22, 1997.

(ii) Heat exchange systems and maintenance wastewater shall be in compliance with the applicable sections of this subpart, and equipment subject to  $\frac{63.149}{10}$  and process wastewater streams shall be in compliance with the applicable sections of this subpart and subpart G of this part no later than April 22, 1999, except as provided in paragraphs (k)(2)(ii)(A) and (k)(2)(ii)(B) of this section.

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(A) If a process wastewater stream or equipment subject to  $\S 63.149$  is subject to the control requirements of subpart G of this part due to the contribution of nitrobenzene to the total annual average concentration (as determined according to the procedures in  $\S 63.144$ (b) of subpart G of this part), the wastewater stream shall be in compliance no later than January 18, 2000.

(B) If a process wastewater stream is used to generate credits in an emissions average in accordance with  $\frac{\& 63.150}{G of this part}$ , the process wastewater stream shall be in compliance with the applicable sections of subpart G of this part no later than April 22, 1997.

(3) Existing sources shall be in compliance with <u>subpart H of this part</u> no later than the dates specified in <u>paragraphs</u> (k)(3)(i) through (k)(3)(v) of this section, except as provided for in <u>paragraphs</u> (k)(4) through (k)(8) of this section, unless an extension has been granted by the Administrator as provided in § 63.182(a)(6) of this part or granted by the permitting authority as provided in § 63.6(i) of <u>subpart A of this part</u>. The group designation for each process unit is indicated in table 1 of this subpart.

(i) Group I: October 24, 1994.

(ii) Group II: January 23, 1995.

(iii) Group III: April 24, 1995.

(iv) Group IV: July 24, 1995.

(v) Group V: October 23, 1995.

(4) Existing chemical manufacturing process units in Groups I and II as identified in table 1 of this subpart shall be in compliance with the requirements of § 63.164 no later than May 10, 1995, for any compressor meeting one or more of the criteria in paragraphs (k)(4)(i) through (iv) of this section, if the work can be accomplished without a process unit shutdown, as defined in § 63.101.

(i) The seal system will be replaced;

(ii) A barrier fluid system will be installed;

(iii) A new barrier fluid will be utilized which requires changes to the existing barrier fluid system; or

(iv) The compressor must be modified to permit connecting the compressor to a closed vent system.

(5) Existing chemical manufacturing process units shall be in compliance with the requirements of  $\frac{63.164}{100}$  in subpart H no later than 1 year after the applicable compliance date specified in <u>paragraph (k)(3)</u> of this section, for any compressor meeting the criteria in <u>paragraphs (k)(5)(i)</u> through (k)(5)(iv) of this section.

(i) The compressor meets one or more of the criteria specified in paragraphs (k)(4) (i) through (iv) of this section;

(ii) The work can be accomplished without a process unit shutdown as defined in  $\S$  63.101;

(iii) The additional time is actually necessary due to the unavailability of parts beyond the control of the owner or operator; and

(iv) The owner or operator submits a request to the appropriate EPA Regional Office at the addresses listed in  $\S$  <u>63.13</u> of <u>subpart A of this part</u> no later than 45 days before the applicable compliance date in <u>paragraph (k)(3)</u> of this section, but in no event earlier than May 10, 1995. The request shall include the information specified in <u>paragraphs</u> (k)(5)(iv)(A) through (k)(5)(iv)(E) of this section. Unless the EPA Regional Office objects to the request within 30 days after receipt, the request shall be deemed approved.

(A) The name and address of the owner or operator and the address of the existing source if it differs from the address of the owner or operator;

(B) The name, address, and telephone number of a contact person for further information;

(C) An identification of the chemical manufacturing process unit, and of the specific equipment for which additional compliance time is required;

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(D) The reason compliance can not reasonably be achieved by the applicable date specified in <u>paragraphs</u>  $(\underline{k})(3)(\underline{i})$  through  $(\underline{k})(3)(\underline{v})$  of this section; and

(E) The date by which the owner or operator expects to achieve compliance.

(6)

(i) If compliance with the compressor provisions of  $\S$  63.164 cannot reasonably be achieved without a process unit shutdown, as defined in  $\S$  63.101, the owner or operator shall achieve compliance no later than April 22, 1996, except as provided for in paragraph (k)(6)(ii) of this section. The owner or operator who elects to use this provision shall comply with the requirements of  $\S$  63.103(g).

(ii) If compliance with the compressor provisions of  $\S 63.164$  of subpart H of this part can not be achieved without replacing the compressor or recasting the distance piece, the owner or operator shall achieve compliance no later than April 22, 1997. The owner or operator who elects to use this provision shall also comply with the requirements of  $\S 63.103(g)$  of this subpart.

(7) Existing sources shall be in compliance with the provisions of  $\frac{63.170}{2}$  of subpart H no later than April 22, 1997.

(8) If an owner or operator of a chemical manufacturing process unit subject to the provisions of subparts F, G, and H of part 63 plans to implement pollution prevention measures to eliminate the use or production of HAP listed in table 2 of this subpart by October 23, 1995, the provisions of subpart H do not apply regardless of the compliance dates specified in paragraph (k)(3) of this section. The owner or operator who elects to use this provision shall comply with the requirements of  $\S$  63.103(h) of this subpart.

(9) All terms in this subpart F or <u>subpart G of this part</u> that define a period of time for completion of required tasks (e.g., weekly, monthly, quarterly, annual), unless specified otherwise in the section or subsection that imposes the requirement, refer to the standard calendar periods.

(i) Notwithstanding time periods specified in this subpart F or <u>subpart G of this part</u> for completion of required tasks, such time periods may be changed by mutual agreement between the owner or operator and the Administrator, as specified in <u>subpart A of this part</u> (e.g., a period could begin on the compliance date or another date, rather than on the first day of the standard calendar period). For each time period that is changed by agreement, the revised period shall remain in effect until it is changed. A new request is not necessary for each recurring period.

(ii) Where the period specified for compliance is a standard calendar period, if the initial compliance date occurs after the beginning of the period, compliance shall be required according to the schedule specified in <u>paragraphs</u> ( $\underline{k}$ )(9)(ii)(A) or ( $\underline{k}$ )(9)(ii)(B) of this section, as appropriate.

(A) Compliance shall be required before the end of the standard calendar period within which the compliance deadline occurs, if there remain at least 3 days for tasks that must be performed weekly, at least 2 weeks for tasks that must be performed monthly, at least 1 month for tasks that must be performed each quarter, or at least 3 months for tasks that must be performed annually; or

(B) In all other cases, compliance shall be required before the end of the first full standard calendar period after the period within which the initial compliance deadline occurs.

(iii) In all instances where a provision of this subpart F or <u>subpart G of this part</u> requires completion of a task during each of multiple successive periods, an owner or operator may perform the required task at any time during the specified period, provided the task is conducted at a reasonable interval after completion of the task during the previous period.

(10) All affected sources that commenced construction or reconstruction on or before April 25, 2023, must be in compliance with the requirements listed in <u>paragraphs (k)(10)(i)</u> through (viii) of this section upon initial startup or on July 15, 2027, whichever is later. All affected sources that commenced construction or reconstruction after April 25, 2023, must be in compliance with the requirements listed in <u>paragraphs (k)(10)(i)</u> through (viii) of this section upon initial startup, or on July 15, 2024, whichever is later.

(i) The general requirements specified in <u>paragraph (q)(4)(iii)</u> of this section,  $\frac{\&\& 63.102(e)}{(2)(iv)}$ ,  $\frac{63.103(b)(1)}{(2)(iv)}$ ,  $\frac{63.103(b)(1)}{(2)(iv)}$ ,  $\frac{63.107(j)}{(2)(iv)}$ ,  $\frac{63.107(j)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)(b)(2)(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)(b)(2)(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)(b)(2)(b)(2)}{(2)(iv)}$ ,  $\frac{63.100(b)(2)(b)(2)(b)(2)(b)$ 

(ii) For heat exchange systems, the requirements specified in  $\S 63.104(a)(3)$  and (a)(4)(v)(g), (h), (i), (j), and (l).
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(iii) For process vents, the requirements specified in  $\frac{\$\$ 63.113(a)(4)}{63.114(a)(5)(v)}$  and  $\frac{(1)}{(d)(3)}$ ,  $\frac{63.115(g)}{63.116(g)}$ ,  $\frac{63.117(g)}{63.117(g)}$ , and  $\frac{63.118(f)(7)}{63.118(f)(7)}$  and  $\frac{(n)}{63.118(f)(7)}$ .

(iv) For storage vessels, the requirements specified in  $\underline{\$\$}$ 

 $\frac{63.119(a)(6)}{63.119(b)(5)(ix)}$  through (xii),  $\frac{63.119(b)(7)}{63.119(b)(7)}$ ,  $\frac{63.119(f)(3)(iv)}{63.120(d)(1)(iii)}$ , and footnotes b and c of tables 5 and 6 to subpart G of this part. For pressure vessels, the requirements specified in <u>§§ 63.119(a)(7)</u>, <u>63.122(j)</u>, and <u>63.123(b)</u>.

(v) For transfer operations, the requirements specified in  $\S$  63.126(h)(1), 63.127(b)(4) and (d)(3), and 63.130(a)(2)(iv), (b)(3), and (d)(7).

(vi) For process wastewater, the requirements specified in  $\frac{\$\$ 63.132(a)(2)(i)(C)}{and (b)(3)(i)(C)}$ ,  $\frac{63.135(b)(4)}{63.139(d)(5)}$ , and  $\frac{63.145(a)(10)}{63.145(a)(10)}$ .

(vii) For equipment leaks and pressure relief devices, the requirements specified in  $\underline{\$\$}$ <u>63.165(a)</u> and (e), <u>63.170(b)</u>, <u>63.172(j)(4)</u>, <u>63.181(g)(3)(iii)</u>, and <u>63.182(d)(2)(xix)</u>.

(viii) The other notification, reports, and records requirements specified in  $\frac{63.152(c)(2)(ii)(F)}{F}$ , table 3 to <u>subpart G of this</u> part, item 3 in column 3 for presence of flow and monthly inspections of sealed valves for all control devices, table 7 to <u>subpart G of this part</u>, item 3 in column 3 for presence of flow and monthly inspections of sealed valves for all control devices and vapor balancing systems, and table 20 to <u>subpart G of this part</u>, item (8)(iii).

(11) All affected sources that commenced construction or reconstruction on or before April 25, 2023, must be in compliance with the ethylene oxide requirements in  $\underline{\$\$}$ 

 $\frac{63.104(k)}{63.109}, \frac{63.113(j)}{63.119(a)(5)}, \frac{63.120(d)(9)}{63.120(d)(9)}, \frac{63.124}{63.163(a)(1)(iii)}, \frac{(b)(2)(iv)}{(b)(5)}, \frac{(c)(4)}{63.168(b)(2)(iv)}, \frac{(d)(5)}{63.171(f)}, \frac{63.174(a)(3)}{63.174(a)(3)}, \frac{(b)(3)(vi)}{(b)(5)}, \frac{(b)(3)(vi)}{63.100}, \frac{(b)(3)(vi)}{63.100}, \frac{(c)(4)}{63.100}, \frac{(c)(4)}{6$ 

 $\frac{63.104(k)}{(63.109, 63.113(j), 63.119(a)(5), 63.120(d)(9), § 63.124, 63.163(a)(1)(iii), (b)(2)(iv), (c)(4), and (e)(7), 63.168(b)(2)(iv) and (d)(5), § 63.171(f), and 63.174(a)(3), (b)(3)(vi), (b)(5), and (g)(3), upon initial startup or on July 15, 2024, whichever is later.$ 

(12) All affected sources that commenced construction or reconstruction on or before April 25, 2023, must commence fenceline monitoring according to the requirements in § 63.184 by no later than July 15, 2026, however requirements for corrective actions are not required until on or after July 15, 2027. All affected sources that commenced construction or reconstruction after April 25, 2023, must be in compliance with the fenceline monitoring requirements listed in § 63.184 upon initial startup, or on July 15, 2024, whichever is later.

(1)

(1) If an additional chemical manufacturing process unit meeting the criteria specified in <u>paragraph (b)</u> of this section is added to a plant site that is a major source as defined in section 112(a) of the Act, the addition shall be subject to the requirements for a new source in <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> if:

(i) It is an addition that meets the definition of construction in  $\S$  63.2 of subpart A of this part;

(ii)

(A) Such construction commenced after December 31, 1992 for chemical manufacturing process units that produce as a primary product one or more of the chemicals listed in table 1 of this subpart;

(B) Such construction commenced after August 22, 1997 for chemical manufacturing process units that produce as a primary product one or more of the chemicals listed in paragraph (b)(1)(ii) of this section; and

(iii) The addition has the potential to emit 10 tons per year or more of any HAP or 25 tons per year or more of any combination of HAP's, unless the Administrator establishes a lesser quantity.

(2) If any change is made to a chemical manufacturing process unit subject to this subpart, the change shall be subject to the requirements of a new source in subparts F, G, and H of this part if:

(i) It is a change that meets the definition of reconstruction in <u>§ 63.2</u> of <u>subpart A of this part</u>; and

(ii)

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(A) Such reconstruction commenced after December 31, 1992 for chemical manufacturing process units that produce as a primary product one or more of the chemicals listed in table 1 of this subpart; and

(B) Such construction commenced after August 22, 1997 for chemical manufacturing process units that produce as a primary product one or more of the chemicals listed in paragraph (b)(1)(ii) of this section.

(3) If an additional chemical manufacturing process unit is added to a plant site or a change is made to a chemical manufacturing process unit and the addition or change is determined to be subject to the new source requirements according to paragraph (1)(1) or (1)(2) of this section:

(i) The new or reconstructed source shall be in compliance with the new source requirements of <u>subparts F</u>, <u>G</u>, and <u>H of this</u> <u>part</u> upon initial start-up of the new or reconstructed source or by April 22, 1994, whichever is later; and

(ii) The owner or operator of the new or reconstructed source shall comply with the reporting and recordkeeping requirements in <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> that are applicable to new sources. The applicable reports include, but are not limited to:

(A) The application for approval of construction or reconstruction which shall be submitted by the date specified in  $\S$ <u>63.151(b)(2)(ii)</u> of subpart G of this part, or an Initial Notification as specified in  $\S$  63.151(b)(2)(iii) of subpart G of this part;

(B) Changes that meet the criteria in  $\S$  63.151(j) of subpart G of this part, unless the information has been submitted in an operating permit application or amendment;

(C) The Notification of Compliance Status as required by  $\S 63.152(b)$  of subpart G of this part for the new or reconstructed source;

(D) Periodic Reports and Other Reports as required by § 63.152(c) and (d) of subpart G of this part;

(E) Reports required by <u>§ 63.182</u> of <u>subpart H of this part;</u> and

(F) Reports and notifications required by sections of <u>subpart A of this part</u> that are applicable to <u>subparts F</u>, <u>G</u>, and <u>H of this part</u>, as identified in table 3 of this subpart.

(4) If an additional chemical manufacturing process unit is added to a plant site, or if an emission point is added to an existing chemical manufacturing process unit, or if another deliberate operational process change creating an additional Group 1 emission point(s) is made to an existing chemical manufacturing process unit, or if a surge control vessel or bottoms receiver becomes subject to  $\frac{63.170}{5}$  of subpart H, or if a compressor becomes subject to  $\frac{63.164}{5}$  of subpart H, and if the addition or change is not subject to the new source requirements as determined according to paragraph (1)(1) or (1)(2) of this section, the requirements in paragraphs (1)(4)(i) through (1)(4)(iii) of this section shall apply. Examples of process changes include, but are not limited to, changes in production capacity, feedstock type, or catalyst type, or whenever there is replacement, removal, or addition of recovery equipment. For purposes of this paragraph and paragraph (m) of this section, process changes do not include: Process upsets, unintentional temporary process changes, and changes that are within the equipment configuration and operating conditions documented in the Notification of Compliance Status required by  $\frac{5}{2}$  (63.152(b) of subpart G of this part.

(i) The added emission point(s) and any emission point(s) within the added or changed chemical manufacturing process unit are subject to the requirements of subparts F, G, and H of this part for an existing source;

(ii) The added emission point(s) and any emission point(s) within the added or changed chemical manufacturing process unit shall be in compliance with <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> by the dates specified in <u>paragraph (1)(4)(ii) (A)</u> or <u>(B)</u> of this section, as applicable.

(A) If a chemical manufacturing process unit is added to a plant site or an emission point(s) is added to an existing chemical manufacturing process unit, the added emission point(s) shall be in compliance upon initial start-up of the added chemical manufacturing process unit or emission point(s) or by 3 years after April 22, 1994, whichever is later.

(B) If a deliberate operational process change to an existing chemical manufacturing process unit causes a Group 2 emission point to become a Group 1 emission point, if a surge control vessel or bottoms receiver becomes subject to  $\frac{63.170}{5}$ , or if a compressor becomes subject to  $\frac{63.164}{5}$ , the owner or operator shall be in compliance upon initial start-up or by 3 years after April 22, 1994, whichever is later, unless the owner or operator demonstrates to the Administrator that achieving compliance

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will take longer than making the change. If this demonstration is made to the Administrator's satisfaction, the owner or operator shall follow the procedures in paragraphs (m)(1) through (3) of this section to establish a compliance date.

(iii) The owner or operator of a chemical manufacturing process unit or emission point that is added to a plant site and is subject to the requirements for existing sources shall comply with the reporting and recordkeeping requirements of <u>subparts</u> <u>F</u>, <u>G</u>, and <u>H of this part</u> that are applicable to existing sources, including, but not limited to, the reports listed in <u>paragraphs</u> (<u>1)(4)(iii)(A)</u> through (<u>E)</u> of this section. A change to an existing chemical manufacturing process unit shall be subject to the reporting requirements for existing sources, including but not limited to, the reports listed in <u>paragraphs</u> (<u>1)(4)(iii)(A)</u> through (<u>E)</u> of this section if the change meets the criteria specified in <u>§ 63.118(g)</u>, (<u>h</u>), (<u>i</u>), or (<u>j</u>) of <u>subpart G of</u> this part for process vents or the criteria in <u>§ 63.155(i)</u> or (<u>j</u>) of <u>subpart G of this part</u>. The applicable reports include, but are not limited to:

(A) Reports specified in  $\S$  63.151(i) and (j) of subpart G of this part, unless the information has been submitted in an operating permit application or amendment;

(B) The Notification of Compliance Status as required by  $\S 63.152(b)$  of subpart G of this part for the emission points that were added or changed;

(C) Periodic Reports and other reports as required by § 63.152 (c) and (d) of subpart G of this part;

(D) Reports required by § 63.182 of subpart H of this part; and

(E) Reports and notifications required by sections of subpart A of this part that are applicable to subparts F, G, and H of this part, as identified in table 3 of this subpart.

(m) If a change that does not meet the criteria in <u>paragraph (1)(4)</u> of this section is made to a chemical manufacturing process unit subject to <u>subparts F</u> and <u>G of this part</u>, and the change causes a Group 2 emission point to become a Group 1 emission point (as defined in § 63.101), then the owner or operator shall comply with the requirements of <u>subpart G of this part</u> for the Group 1 emission point as expeditiously as practicable, but in no event later than 3 years after the emission point becomes Group 1.

(1) The owner or operator shall submit to the Administrator for approval a compliance schedule, along with a justification for the schedule.

(2) The compliance schedule shall be submitted with the report required in  $\S 63.151(i)(2)$  of subpart G of this part for emission points included in an emissions average or  $\S 63.151(j)(1)$  or subpart G of this part for emission points not in an emissions average, unless the compliance schedule has been submitted in an operating permit application or amendment.

(3) The Administrator shall approve the compliance schedule or request changes within 120 calendar days of receipt of the compliance schedule and justification.

(n) *Rules stayed for reconsideration*. Notwithstanding any other provision of this subpart, the effectiveness of subpart F is stayed from October 24, 1994, to April 24, 1995, only as applied to those sources for which the owner or operator makes a representation in writing to the Administrator that the resolution of the area source definition issues could have an effect on the compliance status of the source with respect to subpart F.

(o) Sections stayed for reconsideration. Notwithstanding any other provision of this subpart, the effectiveness of  $\frac{88}{63.164}$  and  $\frac{63.170}{63.100}$  of subpart H is stayed from October 28, 1994, to April 24, 1995, only as applied to those sources subject to  $\frac{863.100(k)(3)}{(1)}$  and  $\frac{(11)}{(1)}$ .

(p) Compliance dates for chemical manufacturing process units that produce crotonaldehyde or

*tetrahydrobenzaldehyde*. Notwithstanding the provisions of <u>paragraph (k)</u> of this section, chemical manufacturing process units that meet the criteria in <u>paragraphs (b)(1)(ii)</u>, (b)(2), and (b)(3) of this section shall be in compliance with this subpart and <u>subparts G</u> and <u>H of this part</u> by the dates specified in <u>paragraphs (p)(1)</u> and (<u>p)(2)</u> of this section, as applicable.

(1) If the source consists only of chemical manufacturing process units that produce as a primary product one or more of the chemicals listed in <u>paragraph (b)(1)(ii)</u> of this section, new sources shall comply by the date specified in <u>paragraph</u> (<u>p)(1)(i)</u> of this section and existing sources shall comply by the dates specified in <u>paragraphs (p)(1)(ii)</u> and (<u>p)(1)(iii)</u> of this section.

(i) Upon initial start-up or May 12, 1998, whichever is later.

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(ii) This subpart and <u>subpart G of this part</u> by May 14, 2001, unless an extension has been granted by the Administrator as provided in § 63.151(a)(6) or granted by the permitting authority as provided in § 63.6(i) of <u>subpart A of this part</u>. When April 22, 1994 is referred to in this subpart and <u>subpart G of this part</u>, May 12, 1998 shall be used as the applicable date for that provision. When December 31, 1992 is referred to in this subpart and <u>subpart G of this part</u>, August 22, 1997 shall be used as the applicable date for that provision.

(iii) <u>Subpart H of this part</u> by May 12, 1999, unless an extension has been granted by the Administrator as provided in § <u>63.151(a)(6)</u> or granted by the permitting authority as provided in § <u>63.6(i)</u> of <u>subpart A of this part</u>. When April 22, 1994 is referred to in <u>subpart H of this part</u>, May 12, 1998 shall be used as the applicable date for that provision. When December 31, 1992 is referred to in <u>subpart H of this part</u>, August 22, 1997 shall be used as the applicable date for that provision.

(2) If the source consists of a combination of chemical manufacturing process units that produce as a primary product one or more of the chemicals listed in <u>paragraphs (b)(1)(i)</u> and (b)(1)(ii) of this section, new chemical manufacturing process units that meet the criteria in <u>paragraph (b)(1)(ii)</u> of this section shall comply by the date specified in <u>paragraph (p)(1)(i)</u> of this section and existing chemical manufacturing process units producing crotonaldehyde and/or tetrahydrobenzaldehyde shall comply by the dates specified in <u>paragraphs (p)(1)(ii)</u> and (p)(1)(iii) of this section.

(q) If the owner or operator of a process vent, or of a gas stream transferred subject to  $\frac{63.113(i)}{10}$ , is unable to comply with the provisions of  $\frac{863.113}{10}$  through  $\frac{63.118}{63.118}$  by the applicable compliance date specified in <u>paragraph (k)</u>, (l), or (m) of this section for the reasons stated in <u>paragraph (q)(1)</u>, (3), or (5) of this section, the owner or operator shall comply with the applicable provisions in  $\frac{8663.113}{10}$  through  $\frac{63.118}{63.118}$  as expeditiously as practicable, but in no event later than the date approved by the Administrator pursuant to <u>paragraph (q)(2)</u>, (4), or (6) of this section, respectively. For requests under <u>paragraph (q)(1)</u> or (3) of this section, the date approved by the Administrator may be earlier than, and shall not be later than, the later of January 22, 2004, or 3 years after the transferee's refusal to accept the stream for disposal. For requests submitted under <u>paragraph (q)(5)</u> of this section, the date approved by the Administrator may be earlier than, and shall not be later than, 3 years after the date of publication of the amendments to this subpart or to <u>subpart G of this part</u> which created the need for an extension of the compliance.

(1) If the owner or operator has been sending a gas stream for disposal as described in  $\frac{63.113(i)}{2}$  prior to January 22, 2001, and the transferee does not submit a written certification as described in  $\frac{63.113(i)}{2}$  and ceases to accept the gas stream for disposal, the owner or operator shall comply with paragraph (q)(2) of this section.

(2)

(i) An owner or operator directed to comply with <u>paragraph (q)(2)</u> of this section shall submit to the Administrator for approval a compliance schedule, along with a justification for the schedule.

(ii) The compliance schedule and justification shall be submitted no later than 90 days after the transferee ceases to accept the gas stream for disposal.

(iii) The Administrator shall approve the compliance schedule or request changes within 120 days of receipt of the compliance schedule and justification.

(3) Except as specified in paragraph (q)(4)(iii) of this section, if the owner or operator has been sending the gas stream for disposal as described in  $\S$  63.113(i) to a transferee who had submitted a written certification as described in  $\S$  63.113(i)(2), and the transferee revokes its written certification, the owner or operator shall comply with paragraphs (q)(4)(i) and (ii) of this section. During the period between the date when the owner or operator receives notice of revocation of the transferee's written certification and the compliance date established under paragraph (q)(4) of this section, the owner or operator shall implement, to the extent reasonably available, measures to prevent or minimize excess emissions to the extent practical. For purposes of this paragraph (q)(3), the term "excess emissions" means emissions in excess of those that would have occurred if the transferee had continued managing the gas stream in compliance with the requirements in  $\S$  63.113 through 63.118. The measures to be taken shall be identified in the applicable startup, shutdown, and malfunction plan. If the measures that can be reasonably taken will change over time, so that a more effective measure which could not reasonably be taken initially would be reasonable at a later date, the Administrator may require the more effective measure by a specified date (in addition to or instead of any other measures taken sooner or later than that date) as a condition of approval of the compliance schedule.

(4)

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(i) An owner or operator directed to comply with this <u>paragraph (q)(4)</u> shall submit to the Administrator for approval the documents specified in <u>paragraphs (q)(4)(i)(A)</u> through (E) of this section no later than 90 days after the owner or operator receives notice of revocation of the transferee's written certification.

- (A) A request for determination of a compliance date.
- (B) A justification for the request for determination of a compliance date.
- (C) A compliance schedule.
- (D) A justification for the compliance schedule.

(E) A description of the measures that will be taken to minimize excess emissions until the new compliance date, and the date when each measure will first be implemented. The owner or operator shall describe how, and to what extent, each measure will minimize excess emissions, and shall justify any period of time when measures are not in place.

(ii) The Administrator shall approve or disapprove the request for determination of a compliance date and the compliance schedule, or request changes, within 120 days after receipt of the documents specified in <u>paragraphs</u> (q)(4)(i)(A) through (E) of this section. Upon approving the request for determination and compliance schedule, the Administrator shall specify a reasonable compliance date consistent with the introductory text in <u>paragraph (q)</u> of this section.

(iii) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$  63.100(k)(10), paragraph (q)(3) of this section no longer applies.

(5) If the owner's or operator's inability to meet otherwise applicable compliance deadlines is due to amendments of this subpart or of subpart G of this part published on or after January 22, 2001, and neither condition specified in paragraph (q)(1) or (3) of this section is applicable, the owner or operator shall comply with paragraph (q)(6) of this section.

(6)

(i) An owner or operator directed to comply with this <u>paragraph (6)(i)</u> shall submit to the Administrator for approval, a request for determination of a compliance date, a compliance schedule, a justification for the determination of a compliance date, and a justification for the compliance schedule.

(ii) The documents required to be submitted under <u>paragraph (q)(6)(i)</u> of this section shall be submitted no later than 120 days after publication of the amendments of this subpart or of <u>subpart G of this part</u> which necessitate the request for an extension.

(iii) The Administrator shall approve or disapprove the request for a determination of a compliance date, or request changes, within 120 days after receipt of the request for determination of a compliance date, the compliance schedule, and the two justifications. If the request for determination of a compliance date is disapproved, the compliance schedule is disapproved and the owner or operator shall comply by the applicable date specified in <u>paragraph (k),(l)</u>, or (<u>m</u>) of this section. If the request for the determination of a compliance date is approved, the Administrator shall specify, at the time of approval, a reasonable compliance date consistent with the introductory text in <u>paragraph (q)</u> of this section.

[<u>59 FR 19454</u>, Apr. 22, 1994, as amended at <u>59 FR 53360</u>, Oct. 24, 1994; <u>59 FR 54132</u>, Oct. 28, 1994; <u>60 FR 5321</u>, Jan. 27, 1995; <u>60 FR 18023</u>, <u>18028</u>, Apr. 10, 1995; <u>60 FR 63626</u>, Dec. 12, 1995; <u>61 FR 7718</u>, Feb. 29, 1996; <u>61 FR 64574</u>, Dec. 5, 1996; <u>62 FR 2729</u>, Jan. 17, 1997; <u>63 FR 26081</u>, May 12, 1998; <u>64 FR 20191</u>, Apr. 26, 1999; <u>66 FR 6927</u>, Jan. 22, 2001; <u>89 FR 43153</u>, May 16, 2024]

# § 63.101 Definitions.

(a) The following terms as used in <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> shall have the meaning given them in <u>subpart A of this part</u>: Act, actual emissions, Administrator, affected source, approved permit program, commenced, compliance date, construction, continuous monitoring system, continuous parameter monitoring system, effective date, emission standard, emissions averaging, EPA, equivalent emission limitation, existing source, Federally enforceable, fixed capital cost, hazardous air pollutant, lesser quantity, major source, malfunction, new source, owner or operator, performance evaluation, performance test, permit program, permitting authority, reconstruction, relevant standard, responsible official, run, standard conditions, State, and stationary source.

(b) All other terms used in this subpart and subparts G and <u>H of this part</u> shall have the meaning given them in the Act and in this section. If the same term is defined in subpart A of this part and in this section, it shall have the meaning given in this section for purposes of subparts F, G, and <u>H of this part</u>.

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

*Air oxidation reactor* means a device or vessel in which air, or a combination of air and oxygen, is used as an oxygen source in combination with one or more organic reactants to produce one or more organic compounds. Air oxidation reactor includes the product separator and any associated vacuum pump or steam jet.

*Ancillary activities* means boilers and incinerators (not used to comply with the emission limits of <u>subparts F</u>, <u>G</u>, and <u>H of</u> <u>this part</u>), chillers and refrigeration systems, and other equipment and activities that are not directly involved (*i.e.*, they operate within a closed system and materials are not combined with process fluids) in the processing of raw materials or the manufacturing of a product or isolated intermediate.

Annual average concentration, as used in the wastewater provisions, means the flow-weighted annual average concentration, as determined according to the procedures specified in  $\frac{63.144(b)}{2}$ .

Annual average flow rate, as used in the wastewater provisions, means the annual average flow rate, as determined according to the procedures specified in  $\S$  63.144(c).

Automated monitoring and recording system means any means of measuring values of monitored parameters and creating a hard copy or computer record of the measured values that does not require manual reading of monitoring instruments and manual transcription of data values. Automated monitoring and recording systems include, but are not limited to, computerized systems and strip charts.

*Batch operation* means a noncontinuous operation in which a discrete quantity or batch of feed is charged into a unit operation within a chemical manufacturing process unit and processed at one time. Batch operation includes noncontinuous operations in which the equipment is fed intermittently or discontinuously. Addition of raw material and withdrawal of product do not occur simultaneously in a batch operation. After each batch operation, the equipment is generally emptied before a fresh batch is started.

*Batch process* means a process in which the equipment is fed intermittently or discontinuously. Processing then occurs in this equipment after which the equipment is generally emptied. Examples of industries that use batch processes include pharmaceutical production and pesticide production.

Batch process vent means gaseous venting to the atmosphere from a batch operation.

*Batch product-process equipment train* means the collection of equipment (e.g., connectors, reactors, valves, pumps, etc.) configured to produce a specific product or intermediate by a batch process.

*Bench-scale batch process* means a batch process (other than a research and development facility) that is operated on a small scale, such as one capable of being located on a laboratory bench top. This bench-scale equipment will typically include reagent feed vessels, a small reactor and associated product separator, recovery and holding equipment. These processes are only capable of producing small quantities of product.

*Boiler* means any enclosed combustion device that extracts useful energy in the form of steam and is not an incinerator. Boiler also means any industrial furnace as defined in <u>40 CFR 260.10</u>.

*Bottoms receiver* means a tank that collects distillation bottoms before the stream is sent for storage or for further downstream processing.

*Breakthrough* means the time when the level of HAP or TOC, measured at the outlet of the first bed, has been detected is at the highest concentration allowed to be discharged from the adsorber system and indicates that the adsorber bed should be replaced.

By compound means by individual stream components, not carbon equivalents.

By-product means a chemical that is produced coincidentally during the production of another chemical.

*Car-seal* means a seal that is placed on a device that is used to change the position of a valve (*e.g.*, from opened to closed) in such a way that the position of the valve cannot be changed without breaking the seal.

*Chemical manufacturing process unit or CMPU* means the equipment assembled and connected by pipes or ducts to process raw materials and to manufacture an intended product. A chemical manufacturing process unit consists of more than one unit operation. For the purpose of this subpart, chemical manufacturing process unit includes air oxidation reactors and their associated product separators and recovery devices; reactors and their associated product separators and recovery devices; distillation units and their associated distillate receivers and recovery devices; associated unit operations; associated associ

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

devices; and any feed, intermediate and product storage vessels and pressure vessels, product transfer racks, and connected ducts and piping. A chemical manufacturing process unit includes pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, instrumentation systems, and control devices or systems. A chemical manufacturing process unit is identified by its primary product. Ancillary activities are not considered a process or part of any process. Quality assurance/quality control laboratories are not considered part of any process.

*Closed biological treatment process* means a tank or surface impoundment where biological treatment occurs and air emissions from the treatment process are routed to either a control device by means of a closed vent system or to a fuel gas system by means of hard-piping. The tank or surface impoundment has a fixed roof, as defined in this section, or a floating flexible membrane cover that meets the requirements specified in  $\S$  63.134.

*Closed-loop system* means an enclosed system that returns process fluid to the process and is not vented to the atmosphere except through a closed-vent system.

*Closed-purge system* means a system or combination of system and portable containers, to capture purged liquids. Containers must be covered or closed when not being filled or emptied.

*Closed vent system* means a system that is not open to the atmosphere and is composed of piping, ductwork, connections, and, if necessary, flow inducing devices that transport gas or vapor from an emission point to a control device.

*Combustion device* means an individual unit of equipment, such as a flare, incinerator, process heater, or boiler, used for the combustion of organic hazardous air pollutant emissions.

*Compliance date* means the dates specified in  $\S 63.100(k)$  or (1)(3) for process units subject to subpart F of this part; the dates specified in  $\S 63.190(e)$  for process units subject to subpart I of this part. For sources subject to other subparts in this part that reference this subpart, compliance date will be defined in those subparts. However, the compliance date for  $\S 63.170$  shall be no later than 3 years after the effective date of those subparts unless otherwise specified in such other subparts.

*Connector* means flanged, screwed, or other joined fittings used to connect two pipe lines or a pipe line and a piece of equipment. A common connector is a flange. Joined fittings welded completely around the circumference of the interface are not considered connectors for the purpose of this regulation. For the purpose of reporting and recordkeeping, connector means joined fittings that are not inaccessible, glass, or glass-lined as described in  $\frac{\& 63.174(h)}{\& 63.174(h)}$ .

*Container*, as used in the wastewater provisions, means any portable waste management unit that has a capacity greater than or equal to 0.1 m<sup>3</sup> in which a material is stored, transported, treated, or otherwise handled. Examples of containers are drums, barrels, tank trucks, barges, dumpsters, tank cars, dump trucks, and ships.

*Continuous record* means documentation, either in hard copy or computer readable form, of data values measured at least once every 15 minutes and recorded at the frequency specified in  $\frac{63.152(f)}{g}$  or (g).

*Continuous recorder* means a data recording device that either records an instantaneous data value at least once every 15 minutes or records 15-minute or more frequent block average values.

*Continuous seal* means a seal that forms a continuous closure that completely covers the space between the wall of the storage vessel and the edge of the floating roof. A continuous seal may be a vapor-mounted, liquid-mounted, or metallic shoe seal. A continuous seal may be constructed of fastened segments so as to form a continuous seal.

*Continuous vapor processing system* means a vapor processing system that treats total organic compound vapors collected from tank trucks or railcars on a demand basis without intermediate accumulation in a vapor holder.

*Control device* means any combustion device, recovery device, or recapture device. Such equipment includes, but is not limited to, absorbers, carbon adsorbers, condensers, incinerators, flares, boilers, and process heaters. For process vents, recapture devices are considered control devices but recovery devices are not considered control devices, and for a steam stripper, a primary condenser is not considered a control device.

Co-product means a chemical that is produced during the production of another chemical.

*Cover*, as used in the wastewater provisions, means a device or system which is placed on or over a waste management unit containing wastewater or residuals so that the entire surface area is enclosed to minimize air emissions. A cover may have openings necessary for operation, inspection, and maintenance of the waste management unit such as access hatches, sampling ports, and gauge wells provided that each opening is closed when not in use. Examples of covers include a fixed

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roof installed on a wastewater tank, a lid installed on a container, and an air-supported enclosure installed over a waste management unit.

Dioxins and furans means total tetra-through octachlorinated dibenzo-p-dioxins and dibenzofurans.

*Distillate receiver* means overhead receivers, overhead accumulators, reflux drums, and condenser(s) including ejectorcondenser(s) associated with a distillation unit.

*Distillation unit* means a device or vessel in which one or more feed streams are separated into two or more exit streams, each exit stream having component concentrations different from those in the feed stream(s). The separation is achieved by the redistribution of the components between the liquid and the vapor phases by vaporization and condensation as they approach equilibrium within the distillation unit. Distillation unit includes the distillate receiver, reboiler, and any associated vacuum pump or steam jet.

*Double block and bleed system* means two block valves connected in series with a bleed valve or line that can vent the line between the two block valves.

*Duct work* means a conveyance system such as those commonly used for heating and ventilation systems. It is often made of sheet metal and often has sections connected by screws or crimping. Hard-piping is not ductwork.

Emission point means an individual process vent, storage vessel, transfer rack, wastewater stream, or equipment leak.

*Empty or emptying* means the removal of the stored liquid from a storage vessel. Storage vessels where stored liquid is left on the walls, as bottom clingage, or in pools due to bottom irregularities are considered empty. Lowering of the stored liquid level, so that the floating roof is resting on its legs, as necessitated by normal vessel operation (for example, when changing stored material or when transferring material out of the vessel for shipment) is not considered emptying.

*Enhanced biological treatment system or enhanced biological treatment process* means an aerated, thoroughly mixed treatment unit(s) that contains biomass suspended in water followed by a clarifier that removes biomass from the treated water and recycles recovered biomass to the aeration unit. The mixed liquor volatile suspended solids (biomass) is greater than 1 kilogram per cubic meter throughout each aeration unit. The biomass is suspended and aerated in the water of the aeration unit(s) by either submerged air flow or mechanical agitation. A thoroughly mixed treatment unit is a unit that is designed and operated to approach or achieve uniform biomass distribution and organic compound concentration throughout the aeration unit by quickly dispersing the recycled biomass and the wastewater entering the unit.

*Equipment leak* means emissions of organic hazardous air pollutants from a connector, pump, compressor, agitator, pressure relief device, sampling connection system, open-ended valve or line, valve, surge control vessel, bottoms receiver, or instrumentation system in organic hazardous air pollutant service as defined in this section.

*Equipment* means each pump, compressor, agitator, pressure relief device, sampling connection system, open-ended valve or line, valve, connector, surge control vessel, bottoms receiver, and instrumentation system in organic hazardous air pollutant service; and any control devices or systems required by this subpart.

*Ethylene production unit* means a chemical manufacturing process unit in which ethylene and/or propylene are produced by separation from petroleum refining process streams or by subjecting hydrocarbons to high temperatures in the presence of steam. The ethylene process unit includes the separation of ethylene and/or propylene from associated streams such as a  $C_4$  product, pyrolysis gasoline, and pyrolysis fuel oil. The ethylene process does not include the manufacture of SOCMI chemicals such as the production of butadiene from the  $C_4$  stream and aromatics from pyrolysis gasoline.

*External floating roof* means a pontoon-type or double-deck-type cover that rests on the liquid surface in a storage vessel or waste management unit with no fixed roof.

*Fill* or *filling* means the introduction of organic hazardous air pollutant into a storage vessel or the introduction of a wastewater stream or residual into a waste management unit, but not necessarily to complete capacity.

*First attempt at repair* means to take action for the purpose of stopping or reducing leakage of organic material to the atmosphere, followed by monitoring as specified in  $\S$  63.180(b) and (c), as appropriate, to verify whether the leak is repaired, unless the owner or operator determines by other means that the leak is not repaired.

*Fixed roof* means a cover that is mounted on a waste management unit or storage vessel in a stationary manner and that does not move with fluctuations in liquid level.

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Flame zone means the portion of the combustion chamber in a boiler or process heater occupied by the flame envelope.

*Flexible operation unit* means a chemical manufacturing process unit that manufactures different chemical products periodically by alternating raw materials or operating conditions. These units are also referred to as campaign plants or blocked operations.

*Floating roof* means a cover consisting of a double deck, pontoon single deck, internal floating cover or covered floating roof, which rests upon and is supported by the liquid being contained, and is equipped with a closure seal or seals to close the space between the roof edge and waste management unit or storage vessel wall.

*Flow indicator* means a device which indicates whether gas flow is, or whether the valve position would allow gas flow to be, present in a line.

Fuel gas means gases that are combusted to derive useful work or heat.

*Fuel gas system* means the offsite and onsite piping and flow and pressure control system that gathers gaseous stream(s) generated by onsite operations, may blend them with other sources of gas, and transports the gaseous stream for use as fuel gas in combustion devices or in in-process combustion equipment such as furnaces and gas turbines either singly or in combination.

*Group 1 process vent* means, before July 15, 2027, a process vent for which the vent stream flow rate is greater than or equal to 0.005 standard cubic meter per minute, the total organic HAP concentration is greater than or equal to 50 parts per million by volume, and the total resource effectiveness index value, calculated according to  $\frac{63.115}{10}$ , is less than or equal to 1.0. On and after July 15, 2027, Group 1 process vent means a process vent that emits greater than or equal to 1.0 pound per hour of total organic HAP.

*Group 1 storage vessel* means a storage vessel that meets the criteria for design storage capacity and stored-liquid maximum true vapor pressure specified in table 5 to <u>subpart G of this part</u> for storage vessels at existing sources, and in table 6 to <u>subpart G of this part</u> for storage vessels at new sources.

*Group 1 transfer rack* means a transfer rack that annually loads greater than or equal to 0.65 million liter of liquid products that contain organic hazardous air pollutants with a rack weighted average vapor pressure greater than or equal to 10.3 kilopascals.

*Group 1 wastewater stream* means a wastewater stream consisting of process wastewater as defined in this section at an existing or new source that meets the criteria for Group 1 status in  $\frac{63.132(c)}{1.000}$  for table 9 compounds and/or a wastewater stream consisting of process wastewater at a new source that meets the criteria for Group 1 status in  $\frac{63.132(c)}{1.0000}$  for table 8 compounds.

*Group 2 process vent* means, before July 15, 2027, a process vent for which the vent stream flow rate is less than 0.005 standard cubic meter per minute, the total organic HAP concentration is less than 50 parts per million by volume or the total resource effectiveness index value, calculated according to  $\S$  63.115, is greater than 1.0. On and after July 15, 2027, Group 2 process vent means a process vent that emits less than 1.0 pound per hour of total organic HAP.

Group 2 storage vessel means a storage vessel that does not meet the definition of a Group 1 storage vessel.

Group 2 transfer rack means a transfer rack that does not meet the definition of Group 1 transfer rack.

Group 2 wastewater stream means any process wastewater stream that does not meet the definition of a Group 1 wastewater stream.

*Halogenated vent stream* or *halogenated stream* means a vent stream from a process vent or transfer operation determined to have a mass emission rate of halogen atoms contained in organic compounds of 0.45 kilograms per hour or greater determined by the procedures presented in  $\frac{63.115(d)(2)(v)}{2}$ .

*Halogens* and *hydrogen halides* means hydrogen chloride (HCl), chlorine (Cl<sub>2</sub>), hydrogen bromide (HBr), bromine (Br<sub>2</sub>), and hydrogen fluoride (HF).

*Hard-piping* means pipe or tubing that is manufactured and properly installed using good engineering judgment and standards such as American National Standards Institute (ANSI) B31-3 (see § 63.14 for ANSI contact information).

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

*Heat exchange system* means a device or collection of devices used to transfer heat from process fluids to water without intentional direct contact of the process fluid with the water (*i.e.*, non-contact heat exchanger) and to transport and/or cool the water in a closed-loop recirculation system (cooling tower system) or a once-through system (*e.g.*, river or pond water). For closed-loop recirculation systems, the heat exchange system consists of a cooling tower, all CMPU heat exchangers that are in organic HAP service, as defined in this subpart, serviced by that cooling tower, and all water lines to and from these process unit heat exchangers. For once-through systems, the heat exchange system consists of all heat exchangers that are in organic HAP service, as defined in this subpart, servicing an individual CMPU and all water lines to and from these heat exchangers. Sample coolers or pump seal coolers are not considered heat exchangers for the purpose of this definition and are not part of the heat exchange system. Intentional direct contact with process fluids results in the formation of a wastewater.

*Impurity* means a substance that is produced coincidentally with the primary product or is present in a raw material. An impurity does not serve a useful purpose in the production or use of the primary product and is not isolated.

*In ethylene oxide service* means the following:

(i) For equipment leaks, any equipment that contains or contacts a fluid (liquid or gas) that is at least 0.1 percent by weight of ethylene oxide. If information exists that suggests ethylene oxide could be present in equipment, the equipment is considered to be "in ethylene oxide service" unless the procedures specified in  $\S$  63.109 are performed to demonstrate that the equipment does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in equipment, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(ii) For heat exchange systems, any heat exchange system in a process that cools process fluids (liquid or gas) that are 0.1 percent or greater by weight of ethylene oxide. If knowledge exists that suggests ethylene oxide could be present in a heat exchange system, then the heat exchange system is considered to be "in ethylene oxide service" unless the procedures specified in  $\frac{63.109}{3}$  are performed to demonstrate that the heat exchange system does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in a heat exchange system, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(iii) For process vents, each Group 1 and Group 2 process vent in a process that, when uncontrolled, contains a concentration of greater than or equal to 1 ppmv undiluted ethylene oxide, and when combined, the sum of all these process vents within the process would emit uncontrolled, ethylene oxide emissions greater than or equal to 5 lb/yr (2.27 kg/yr). If information exists that suggests ethylene oxide could be present in a Group 1 or Group 2 process vent, then the Group 1 or Group 2 process vent is considered to be "in ethylene oxide service" unless an analysis is performed as specified in § 63.109 to demonstrate that the Group 1 or Group 2 process vent does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in a Group 1 or Group 2 process vent, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(iv) For storage vessels, storage vessels of any capacity and vapor pressure storing a liquid that is at least 0.1 percent by weight of ethylene oxide. If knowledge exists that suggests ethylene oxide could be present in a storage vessel, then the storage vessel is considered to be "in ethylene oxide service" unless the procedures specified in § 63.109 are performed to demonstrate that the storage vessel does not meet the definition of being "in ethylene oxide service". The exemption for "vessels storing organic liquids that contain organic hazardous air pollutants only as impurities" listed in the definition of "storage vessel" in this section does not apply for storage vessels that may be in ethylene oxide service. Examples of information that could suggest ethylene oxide could be present in a storage vessel, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(v) For wastewater streams, any wastewater stream that contains total annual average concentration of ethylene oxide greater than or equal to 1 parts per million by weight at any flow rate. If knowledge exists that suggests ethylene oxide could be present in a wastewater stream, then the wastewater stream is considered to be "in ethylene oxide service" unless sampling and analysis is performed as specified in  $\S 63.109$  to demonstrate that the wastewater stream does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in a wastewater stream, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

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*In food/medical service* means that a piece of equipment in organic hazardous air pollutant service contacts a process stream used to manufacture a Food and Drug Administration regulated product where leakage of a barrier fluid into the process stream would cause any of the following:

(i) A dilution of product quality so that the product would not meet written specifications,

(ii) An exothermic reaction which is a safety hazard,

(iii) The intended reaction to be slowed down or stopped, or

(iv) An undesired side reaction to occur.

In gas/vapor service means that a piece of equipment in organic hazardous air pollutant service contains a gas or vapor at operating conditions.

In heavy liquid service means that a piece of equipment in organic hazardous air pollutant service is not in gas/vapor service or in light liquid service.

*In light liquid service* means that a piece of equipment in organic hazardous air pollutant service contains a liquid that meets the following conditions:

(i) The vapor pressure of one or more of the organic compounds is greater than 0.3 kilopascals at 20 °C,

(ii) The total concentration of the pure organic compounds constituents having a vapor pressure greater than 0.3 kilopascals at 20 °C is equal to or greater than 20 percent by weight of the total process stream, and

(iii) The fluid is a liquid at operating conditions.

Note 1 to *In light liquid service*: Vapor pressures may be determined by the methods described in  $\frac{60.485(e)(1)}{0.000}$  of this <u>chapter</u>.

In liquid service means that a piece of equipment in organic hazardous air pollutant service is not in gas/vapor service.

In organic hazardous air pollutant or in organic HAP service means that a piece of equipment or heat exchange system either contains or contacts a fluid (liquid or gas) that is at least 5 percent by weight of total organic HAP's as determined according to the provisions of  $\S$  63.180(d). The provisions of  $\S$  63.180(d) also specify how to determine that a piece of equipment is not in organic HAP service. For purposes of the definition of "heat exchange system", the term "equipment" in  $\S$  63.180(d) includes heat exchange systems.

In vacuum service means that equipment is operating at an internal pressure which is at least 5 kilopascals below ambient pressure.

In volatile organic compound or in VOC service means, for the purposes of subpart H of this part, that:

(i) The piece of equipment contains or contacts a process fluid that is at least 10 percent VOC by weight (see  $\S$  60.2 of this chapter for the definition of VOC, and  $\S$  60.485(d) of this chapter to determine whether a piece of equipment is not in VOC service); and

(ii) The piece of equipment is not in heavy liquid service as defined in § 60.481 of this chapter.

*Incinerator* means an enclosed combustion device that is used for destroying organic compounds. Auxiliary fuel may be used to heat waste gas to combustion temperatures. Any energy recovery section present is not physically formed into one manufactured or assembled unit with the combustion section; rather, the energy recovery section is a separate section following the combustion section and the two are joined by ducts or connections carrying flue gas. The above energy recovery section limitation does not apply to an energy recovery section used solely to preheat the incoming vent stream or combustion air.

*Individual drain system* means the stationary system used to convey wastewater streams or residuals to a waste management unit or to discharge or disposal. The term includes hard-piping, all process drains and junction boxes, together with their associated sewer lines and other junction boxes, manholes, sumps, and lift stations, conveying wastewater streams or residuals. A segregated stormwater sewer system, which is a drain and collection system designed and operated for the sole purpose of collecting rainfall runoff at a facility, and which is segregated from all other individual drain systems, is excluded from this definition.

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*Initial start-up* means the first time a new or reconstructed source begins production, or, for equipment added or changed as described in <u>§ 63.100(1)</u> or (<u>m</u>), the first time the equipment is put into operation. Initial start-up does not include operation solely for testing equipment. For purposes of <u>subpart G of this part</u>, initial start-up does not include subsequent start-ups (as defined in this section) of chemical manufacturing process units following malfunctions or shutdowns or following changes in product for flexible operation units or following recharging of equipment in batch operation. For purposes of <u>subpart H of this part</u>, initial start-up does not include subsequent start-ups (as defined in this section) of process units (as defined in § this section) following malfunctions or process unit shutdowns.

In-situ sampling systems means nonextractive samplers or in-line samplers.

*Instrumentation system* means a group of equipment components used to condition and convey a sample of the process fluid to analyzers and instruments for the purpose of determining process operating conditions (*e.g.*, composition, pressure, flow, etc.). Valves and connectors are the predominant type of equipment used in instrumentation systems; however, other types of equipment may also be included in these systems. Only valves nominally 0.5 inches and smaller, and connectors nominally 0.75 inches and smaller in diameter are considered instrumentation systems for the purposes of <u>subpart H of this part</u>. Valves greater than nominally 0.75 inches and connectors greater than nominally 0.75 inches associated with instrumentation systems are not considered part of instrumentation systems and must be monitored individually.

*Intermittent vapor processing system* means a vapor processing system that employs an intermediate vapor holder to accumulate total organic compound vapors collected from tank trucks or railcars, and treats the accumulated vapors only during automatically controlled cycles.

*Internal floating roof* means a cover that rests or floats on the liquid surface (but not necessarily in complete contact with it) inside a storage vessel or waste management unit that has a permanently affixed roof.

Junction box means a manhole or access point to a wastewater sewer line or a lift station.

*Liquid-mounted seal* means a foam- or liquid-filled seal mounted in contact with the liquid between the wall of the storage vessel or waste management unit and the floating roof. The seal is mounted continuously around the circumference of the vessel or unit.

*Liquids dripping* means any visible leakage from the seal including dripping, spraying, misting, clouding, and ice formation. Indications of liquid dripping include puddling or new stains that are indicative of an existing evaporated drip.

*Loading cycle* means the time period from the beginning of filling a tank truck or railcar until flow to the control device ceases, as measured by the flow indicator.

*Loading rack* means a single system used to fill tank trucks and railcars at a single geographic site. Loading equipment and operations that are physically separate (i.e., do not share common piping, valves, and other equipment) are considered to be separate loading racks.

*Maintenance wastewater* means wastewater generated by the draining of process fluid from components in the chemical manufacturing process unit into an individual drain system prior to or during maintenance activities. Maintenance wastewater can be generated during planned and unplanned shutdowns and during periods not associated with a shutdown. Examples of activities that can generate maintenance wastewaters include descaling of heat exchanger tubing bundles, cleaning of distillation column traps, draining of low legs and high point bleeds, draining of pumps into an individual drain system, and draining of portions of the chemical manufacturing process unit for repair.

*Maximum true vapor pressure* means the equilibrium partial pressure exerted by the total organic HAP's in the stored or transferred liquid at the temperature equal to the highest calendar-month average of the liquid storage or transfer temperature for liquids stored or transferred above or below the ambient temperature or at the local maximum monthly average temperature as reported by the National Weather Service for liquids stored or transferred at the ambient temperature, as determined:

(i) In accordance with methods described in API MPMS 19.2 (incorporated by reference as specified in § 63.14); or

(ii) As obtained from standard reference texts; or

(iii) As determined by the ASTM D2879-23 (incorporated by reference as specified in § 63.14); or

(iv) Any other method approved by the Administrator.

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

*Metallic shoe seal* or *mechanical shoe seal* means metal sheets that are held vertically against the wall of the storage vessel by springs, weighted levers, or other mechanisms and connected to the floating roof by braces or other means. A flexible coated fabric (envelope) spans the annular space between the metal sheet and the floating roof.

*Non-automated monitoring and recording system* means manual reading of values measured by monitoring instruments and manual transcription of those values to create a record. Non-automated systems do not include strip charts.

*Nonrepairable* means that it is technically infeasible to repair a piece of equipment from which a leak has been detected without a process unit shutdown.

*Oil-water separator* or *organic-water separator* means a waste management unit, generally a tank used to separate oil or organics from water. An oil-water or organic-water separator consists of not only the separation unit but also the forebay and other separator basins, skimmers, weirs, grit chambers, sludge hoppers, and bar screens that are located directly after the individual drain system and prior to additional treatment units such as an air flotation unit, clarifier, or biological treatment unit. Examples of an oil-water or organic-water separator include, but are not limited to, an American Petroleum Institute separator, parallel-plate interceptor, and corrugated-plate interceptor with the associated ancillary equipment.

*On-site* or *On site* means, with respect to records required to be maintained by this subpart, that the records are stored at a location within a major source which encompasses the affected source. On-site includes, but is not limited to, storage at the chemical manufacturing process unit to which the records pertain, or storage in central files elsewhere at the major source.

*Open biological treatment process* means a biological treatment process that is not a closed biological treatment process as defined in this section.

*Open-ended valve or line* means any valve, except pressure relief valves, having one side of the valve seat in contact with process fluid and one side open to atmosphere, either directly or through open piping.

Operating permit means a permit required by <u>40 CFR part 70</u> or <u>71</u>.

Organic hazardous air pollutant or organic HAP means one of the chemicals listed in table 2 of this subpart.

*Organic monitoring device* means a unit of equipment used to indicate the concentration level of organic compounds exiting a recovery device based on a detection principle such as infra-red, photoionization, or thermal conductivity.

*Petroleum refining process*, also referred to as a *petroleum refining process unit*, means a process that for the purpose of producing transportation fuels (such as gasoline and diesel fuels), heating fuels (such as fuel gas, distillate, and residual fuel oils), or lubricants separates petroleum or separates, cracks, or reforms unfinished derivatives. Examples of such units include, but are not limited to, alkylation units, catalytic hydrotreating, catalytic hydrorefining, catalytic hydrocracking, catalytic reforming, catalytic cracking, crude distillation, and thermal processes.

*Plant site* means all contiguous or adjoining property that is under common control, including properties that are separated only by a road or other public right-of-way. Common control includes properties that are owned, leased, or operated by the same entity, parent entity, subsidiary, or any combination thereof.

*Point of determination* means each point where process wastewater exits the chemical manufacturing process unit. This subpart and <u>subpart G of this part</u> allows point of determination of the characteristics of a wastewater stream:

# (i) At the point of determination or

(ii) Downstream of the point of determination if corrections are made for changes in flow rate and annual average concentration of table 8 or table 9 compounds as determined in § 63.144. Such changes include losses by air emissions; reduction of annual average concentration or changes in flow rate by mixing with other water or wastewater streams; and reduction in flow rate or annual average concentration by treating or otherwise handling the wastewater stream to remove or destroy hazardous air pollutants.

# *Point of transfer* means:

(i) If the transfer is to an off-site location for control, the point where the conveyance crosses the property line; or

(ii) If the transfer is to an on-site location not owned or operated by the owner or operator of the source, the point where the conveyance enters the operation or equipment of the transferee.

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

*Polymerizing monomer* means a molecule or compound usually containing carbon and of relatively low molecular weight and simple structure (*e.g.*, hydrogen cyanide, acrylonitrile, styrene), which is capable of conversion to polymers, synthetic resins, or elastomers by combination with itself due to heat generation caused by a pump mechanical seal surface, contamination by a seal fluid (*e.g.*, organic peroxides or chemicals that will form organic peroxides), or a combination of both with the resultant polymer buildup causing rapid mechanical seal failure.

*Pressure release* means the emission of materials resulting from the system pressure being greater than the set pressure of the pressure relief device. This release can be one release or a series of releases over a short time period.

*Pressure relief device or valve* means a valve, rupture disk, or similar device used only to release an unplanned, nonroutine discharge of gas from process equipment in order to avoid safety hazards or equipment damage. A pressure relief device discharge can result from an operator error, a malfunction such as a power failure or equipment failure, or other unexpected cause. Such devices include conventional, spring-actuated relief valves, balanced bellows relief valves, pilot-operated relief valves, rupture disks, and breaking, buckling, or shearing pin devices. Devices that are actuated either by a pressure of less than or equal to 2.5 pounds per square inch gauge or by a vacuum are not pressure relief devices.

*Pressure-assisted multi-point flare* means a flare system consisting of multiple flare burners in staged arrays whereby the vent stream pressure is used to promote mixing and smokeless operation at the flare burner tips. Pressure-assisted multi-point flares are designed for smokeless operation at velocities up to Mach = 1 conditions (*i.e.*, sonic conditions), can be elevated or at ground level, and typically use cross-lighting for flame propagation to combust any flare vent gases sent to a particular stage of flare burners.

*Pressure vessel* means a storage vessel that is used to store liquids or gases and is designed not to vent to the atmosphere as a result of compression of the vapor headspace in the pressure vessel during filling of the pressure vessel to its design capacity.

*Primary fuel* means the fuel that provides the principal heat input to the device. To be considered primary, the fuel must be able to sustain operation without the addition of other fuels.

*Process heater* means a device that transfers heat liberated by burning fuel directly to process streams or to heat transfer liquids other than water.

*Process unit* means a chemical manufacturing process unit as defined in <u>subpart F of this part</u>, a process subject to the provisions of <u>subpart I of this part</u>, or a process subject to another subpart in this part that references this subpart.

*Process unit shutdown* means a work practice or operational procedure that stops production from a process unit or part of a process unit during which it is technically feasible to clear process material from a process unit or part of a process unit consistent with safety constraints and during which repairs can be effected. An unscheduled work practice or operational procedure that stops production from a process unit or part of a process unit shutdown. An unscheduled work practice or operational procedure that would stop production from a process unit or part of a process unit for a shorter period of time than would be required to clear the process unit or part of the process unit of materials and start up the unit, and would result in greater emissions than delay of repair of leaking components until the next scheduled process unit shutdown, is not a process unit shutdown. The use of spare equipment and technically feasible bypassing of equipment without stopping production are not process unit shutdowns.

*Process vent* means the point of discharge to the atmosphere (or the point of entry into a control device, if any) of a gas stream if the gas stream has the characteristics specified in  $\S$  <u>63.107(b)</u> through (h), or meets the criteria specified in  $\S$  <u>63.107(i)</u>. For purposes of  $\S$  <u>63.113</u> through <u>63.118</u>, all references to the characteristics of a process vent (e.g., flow rate, total HAP concentration, or TRE index value) shall mean the characteristics of the gas stream.

*Process wastewater* means wastewater which, during manufacturing or processing, comes into direct contact with or results from the production or use of any raw material, intermediate product, finished product, by-product, or waste product. Examples are product tank drawdown or feed tank drawdown; water formed during a chemical reaction or used as a reactant; water used to wash impurities from organic products or reactants; water used to cool or quench organic vapor streams through direct contact; and condensed steam from jet ejector systems pulling vacuum on vessels containing organics.

Process wastewater stream means a stream that contains process wastewater.

*Product* means a compound or chemical which is manufactured as the intended product of the chemical manufacturing process unit. By-products, isolated intermediates, impurities, wastes, and trace contaminants are not considered products.

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

*Product separator* means phase separators, flash drums, knock-out drums, decanters, degassers, and condenser(s) including ejector-condenser(s) associated with a reactor or an air oxidation reactor.

*Product tank drawdown* means any material or mixture of materials discharged from a product tank for the purpose of removing water or other contaminants from the product tank.

*Product tank,* as used in the wastewater provisions, means a stationary unit that is designed to contain an accumulation of materials that are fed to or produced by a process unit, and is constructed primarily of non-earthen materials (*e.g.*, wood, concrete, steel, plastic) which provide structural support. This term has the same meaning as a product storage vessel.

*Rack-weighted average partial pressure* means the throughput weighted average of the average maximum true vapor pressure of liquids containing organic HAP transferred at a transfer rack. The rack-weighted average partial pressure shall be calculated using the equation below:

Equation 1 to Paragraph (b) Rack-Weighted Average Partial Pressure



Where:

P = Rack-weighted average partial pressure, kilopascals.

 $P_i$  = Individual HAP maximum true vapor pressure, kilopascals, =  $X_i$ \*P, where  $X_i$  is the mole fraction of compound i in the liquid.

G<sub>i</sub> = Yearly volume of each liquid that contains organic HAP that is transferred at the rack, liters.

I = Each liquid that contains HAP that is transferred at the rack.

*Reactor* means a device or vessel in which one or more chemicals or reactants, other than air, are combined or decomposed in such a way that their molecular structures are altered and one or more new organic compounds are formed. Reactor includes the product separator and any associated vacuum pump or steam jet.

*Recapture device* means an individual unit of equipment capable of and used for the purpose of recovering chemicals, but not normally for use, reuse, or sale. For example, a recapture device may recover chemicals primarily for disposal. Recapture devices include, but are not limited to, absorbers, carbon adsorbers, and condensers.

*Recovery device* means an individual unit of equipment capable of and normally used for the purpose of recovering chemicals for fuel value (*i.e.*, net positive heating value), use, reuse or for sale for fuel value, use, or reuse. Examples of equipment that may be recovery devices include absorbers, carbon adsorbers, condensers, oil-water separators or organic-water separators, or organic removal devices such as decanters, strippers, or thin-film evaporation units. For purposes of the monitoring, recordkeeping, and reporting requirements of <u>subparts G</u> and <u>H of this part</u>, recapture devices are considered recovery devices.

*Reference control technology for process vents* means a combustion device or recapture device used to reduce organic hazardous air pollutant emissions by 98 percent, or to an outlet concentration of 20 parts per million by volume.

*Reference control technology for storage vessels* means an internal floating roof meeting the specifications of § <u>63.119(b)</u>, an external floating roof meeting the specifications of § <u>63.119(c)</u>, an external floating roof converted to an internal floating roof meeting the specifications of § <u>63.119(d)</u>, or a closed-vent system to a control device achieving 95-percent reduction in organic HAP emissions. For purposes of emissions averaging, these four technologies are considered equivalent.

*Reference control technology for transfer racks* means a combustion device, recapture device, or recovery device used to reduce organic hazardous air pollutants emissions by 98 percent, or to an outlet concentration of 20 parts per million by volume; or a vapor balancing system.

*Reference control technology for wastewater* means the use of:

(i) Controls specified in  $\underline{\$\$ 63.133}$  through  $\underline{63.137}$ ;

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

(ii) A steam stripper meeting the specifications of  $\S$  <u>63.138(d)</u> or any of the other alternative control measures specified in  $\S$  <u>63.138(b)</u>, (c), (e), (f), (g), or (h); and

(iii) A control device to reduce by 95 percent (or to an outlet concentration of 20 parts per million by volume for combustion devices or for noncombustion devices controlling air emissions from waste management units other than surface impoundments or containers) the organic hazardous air pollutants emissions in the vapor streams vented from wastewater tanks, oil-water separators, containers, surface impoundments, individual drain systems, and treatment processes (including the design steam stripper) managing wastewater.

Relief valve means a type of pressure relief device that is designed to re-close after the pressure relief.

Repaired means that equipment:

(i) Is adjusted, or otherwise altered, to eliminate a leak as defined in the applicable sections of subpart H of this part, and

(ii) Unless otherwise specified in applicable provisions of <u>subpart H of this part</u>, is monitored as specified in  $\S$  <u>63.180(b)</u> and <u>(c)</u>, as appropriate, to verify that emissions from the equipment are below the applicable leak definition.

*Research and development facility* means laboratory and pilot plant operations whose primary purpose is to conduct research and development into new processes and products, where the operations are under the close supervision of technically trained personnel, and is not engaged in the manufacture of products for commercial sale, except in a *de minimis* manner.

*Residual* means any liquid or solid material containing table 9 compounds that is removed from a wastewater stream by a waste management unit or treatment process that does not destroy organics (nondestructive unit). Examples of residuals from nondestructive wastewater management units are: the organic layer and bottom residue removed by a decanter or organic-water separator and the overheads from a steam stripper or air stripper. Examples of materials which are not residuals are: silt; mud; leaves; bottoms from a steam stripper or air stripper; and sludges, ash, or other materials removed from wastewater being treated by destructive devices such as biological treatment units and incinerators.

*Routed to a process or route to a process* means the emissions are conveyed to any enclosed portion of a process unit where the emissions are predominately recycled and/or consumed in the same manner as a material that fulfills the same function in the process; and/or transformed by chemical reaction into materials that are not organic hazardous air pollutants; and/or incorporated into a product; and/or recovered.

*Sampling connection system* means an assembly of equipment within a process unit used during periods of representative operation to take samples of the process fluid. Equipment used to take non-routine grab samples is not considered a sampling connection system.

*Screwed connector* means a threaded pipe fitting where the threads are cut on the pipe wall and the fitting requires only two pieces to make the connection (*i.e.*, the pipe and the fitting).

Secondary fuel means a fuel fired through a burner other than the primary fuel burner that provides supplementary heat in addition to the heat provided by the primary fuel.

*Sensor* means a device that measures a physical quantity or the change in a physical quantity, such as temperature, pressure, flow rate, pH, or liquid level.

Set pressure means the pressure at which a properly operating pressure relief device begins to open to relieve atypical process system operating pressure.

Sewer line means a lateral, trunk line, branch line, or other conduit including, but not limited to, grates, trenches, etc., used to convey wastewater streams or residuals to a downstream waste management unit.

*Shutdown* means for purposes including, but not limited to, periodic maintenance, replacement of equipment, or repair, the cessation of operation of a chemical manufacturing process unit or a reactor, air oxidation reactor, distillation unit, waste management unit, equipment required or used to comply with this subpart, <u>subpart G</u> or <u>H of this part</u>, or the emptying and degassing of a storage vessel. Shutdown does not include the routine rinsing or washing of equipment in batch operation between batches.

*Simultaneous loading* means, for a shared control device, loading of organic HAP materials from more than one transfer arm at the same time such that the beginning and ending times of loading cycles coincide or overlap and there is no interruption in vapor flow to the shared control device.

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*Single-seal system* means a floating roof having one continuous seal that completely covers the space between the wall of the storage vessel and the edge of the floating roof. This seal may be a vapor-mounted, liquid-mounted, or metallic shoe seal.

*Source* means the collection of emission points to which this subpart applies as determined by the criteria in  $\frac{63.100}{100}$ . For purposes of <u>subparts F</u>, <u>G</u>, and <u>H of this part</u>, the term *affected source* as used in <u>subpart A of this part</u> has the same meaning as the term *source* defined here.

Specific gravity monitoring device means a unit of equipment used to monitor specific gravity and having a minimum accuracy of  $\pm 0.02$  specific gravity units.

*Start-up* means the setting into operation of a chemical manufacturing process unit or a reactor, air oxidation reactor, distillation unit, waste management unit, or equipment required or used to comply with this subpart, <u>subpart G</u> or <u>H of this</u> <u>part</u>, or a storage vessel after emptying and degassing. Start-up includes initial start-up, operation solely for testing equipment, the recharging of equipment in batch operation, and transitional conditions due to changes in product for flexible operation units.

*Start-up, shutdown, and malfunction plan* means the plan required under  $\frac{63.6(e)(3)}{2}$ . This plan details the procedures for operation and maintenance of the source during periods of start-up, shutdown, and malfunction. For each source as defined in this section, this definition no longer applies on and after July 15, 2027.

Steam jet ejector means a steam nozzle which discharges a high-velocity jet across a suction chamber that is connected to the equipment to be evacuated.

*Storage vessel* means a tank or other vessel that is used to store organic liquids that contain one or more of the organic HAP's listed in table 2 to this subpart and that has been assigned, according to the procedures in  $\S$  <u>63.100(g)</u>, to a chemical manufacturing process unit that is subject to this subpart. Storage vessel does not include:

(i) Vessels permanently attached to motor vehicles such as trucks, railcars, barges, or ships;

(ii) Vessels with capacities smaller than 38 cubic meters;

(iii) Except for storage vessels in ethylene oxide service, vessels storing organic liquids that contain organic hazardous air pollutants only as impurities;

(iv) Bottoms receiver tanks;

(v) Surge control vessels; or

(vi) Wastewater storage tanks. Wastewater storage tanks are covered under the wastewater provisions.

*Surface impoundment* means a waste management unit which is a natural topographic depression, manmade excavation, or diked area formed primarily of earthen materials (although it may be lined with manmade materials), which is designed to hold an accumulation of liquid wastes or waste containing free liquids. A surface impoundment is used for the purpose of treating, storing, or disposing of wastewater or residuals, and is not an injection well. Examples of surface impoundments are equalization, settling, and aeration pits, ponds, and lagoons.

*Surge control vessel* means feed drums, recycle drums, and intermediate vessels. Surge control vessels are used within a chemical manufacturing process unit when in-process storage, mixing, or management of flow rates or volumes is needed to assist in production of a product.

Table 8 compound means a compound listed in table 8 to subpart G of this part.

Table 9 compound means a compound listed in table 9 to subpart G of this part.

Temperature monitoring device means a unit of equipment used to monitor temperature and having a minimum accuracy of

(a) ±1 percent of the temperature being monitored expressed in degrees Celsius (( °C) or

(b)  $\pm 0.5$  degrees ( °C), whichever is greater.

*The 33/50 program* means a voluntary pollution prevention initiative established and administered by the EPA to encourage emissions reductions of 17 chemicals emitted in large volumes by industrial facilities. The EPA Document Number 741-K-92-001 provides more information about the 33/50 program.

### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

*Total organic compounds (TOC)*, as used in the process vents provisions, means those compounds measured according to the procedures of Method 18 of appendix A-6 to <u>40 CFR part 60</u>, ASTM D6420-18 (incorporated by reference, see § 63.14) may be used in lieu of Method 18, if the target compounds are all known and are all listed in <u>Section 1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method.

*Total resource effectiveness index value* or *TRE index value* means a measure of the supplemental total resource requirement per unit reduction of organic HAP associated with a process vent stream, based on vent stream flow rate, emission rate of organic HAP, net heating value, and corrosion properties (whether or not the vent stream contains halogenated compounds), as quantified by the equations given under  $\frac{§ 63.115}{5}$ .

*Transfer operation* means the loading, into a tank truck or railcar, of organic liquids that contain one or more of the organic hazardous air pollutants listed in table 2 of this subpart from a transfer rack (as defined in this section). Transfer operations do not include loading at an operating pressure greater than 204.9 kilopascals. For each source as defined in this section, the greater than 204.9 kilopascals exemption in this definition no longer applies on and after July 15, 2027.

*Transfer rack* means the collection of loading arms and loading hoses, at a single loading rack, that are assigned to a chemical manufacturing process unit subject to this subpart according to the procedures specified in § 63.100(h) and are used to fill tank trucks and/or railcars with organic liquids that contain one or more of the organic hazardous air pollutants listed in table 2 to this subpart. Transfer rack includes the associated pumps, meters, shutoff valves, relief valves, and other piping and valves. Transfer rack does not include:

(i) Racks, arms, or hoses that only transfer liquids containing organic hazardous air pollutants as impurities; or

(ii) Racks, arms, or hoses that vapor balance during all loading operations.

*Treatment process* means a specific technique that removes or destroys the organics in a wastewater or residual stream such as a steam stripping unit, thin-film evaporation unit, waste incinerator, biological treatment unit, or any other process applied to wastewater streams or residuals to comply with  $\S$  63.138. Most treatment processes are conducted in tanks. Treatment processes are a subset of waste management units.

*Unit operation* means one or more pieces of process equipment used to make a single change to the physical or chemical characteristics of one or more process streams. Unit operations include, but are not limited to, reactors, distillation units, extraction columns, absorbers, decanters, dryers, condensers, and filtration equipment.

*Vapor balancing system* means a piping system that is designed to collect organic hazardous air pollutants vapors displaced from tank trucks or railcars during loading; and to route the collected organic hazardous air pollutants vapors to the storage vessel from which the liquid being loaded originated, or to another storage vessel connected by a common header or to compress and route to a process or a fuel gas system the collected organic hazardous air pollutants vapors.

*Vapor collection system*, as used in the transfer provisions, means the equipment used to collect and transport organic HAP vapors displaced during the loading of tank trucks or railcars. This does not include the vapor collection system that is part of any tank truck or railcar vapor collection manifold system.

*Vapor-mounted seal* means a continuous seal that completely covers the annular space between the wall of the storage vessel or waste management unit and the edge of the floating roof and is mounted such that there is a vapor space between the stored liquid and the bottom of the seal.

Vent stream, as used in the process vent provisions, means the gas stream flowing through the process vent.

*Waste management unit* means the equipment, structure(s), and/or device(s) used to convey, store, treat, or dispose of wastewater streams or residuals. Examples of waste management units include: Wastewater tanks, surface impoundments, individual drain systems, and biological wastewater treatment units. Examples of equipment that may be waste management units include containers, air flotation units, oil-water separators or organic-water separators, or organic removal devices such as decanters, strippers, or thin-film evaporation units. If such equipment is used for recovery then it is part of a chemical manufacturing process unit and is not a waste management unit.

*Wastewater* means water that:

(i) Contains either:

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(A) An annual average concentration of table 9 compounds of at least 5 parts per million by weight and has an annual average flow rate of 0.02 liter per minute or greater, or

(B) An annual average concentration of table 9 compounds of at least 10,000 parts per million by weight at any flow rate, and that

(ii) Is discarded from a chemical manufacturing process unit that meets all of the criteria specified in  $\S$  63.100 (b)(1) through (3). Wastewater is process wastewater or maintenance wastewater.

Wastewater stream means a stream that contains only wastewater.

*Wastewater tank* means a stationary waste management unit that is designed to contain an accumulation of wastewater or residuals and is constructed primarily of non-earthen materials (*e.g.*, wood, concrete, steel, plastic) which provide structural support. Wastewater tanks used for flow equalization are included in this definition.

*Water seal controls* means a seal pot, p-leg trap, or other type of trap filled with water (*e.g.*, flooded sewers that maintain water levels adequate to prevent air flow through the system) that creates a water barrier between the sewer line and the atmosphere. The water level of the seal must be maintained in the vertical leg of a drain in order to be considered a water seal.

[<u>59 FR 19454</u>, Apr. 22, 1994, as amended at <u>60 FR 18024</u>, Apr. 10, 1995; <u>60 FR 63626</u>, Dec. 12, 1995; <u>62 FR 2731</u>, Jan. 17, 1997; <u>65 FR 26497</u>, May 8, 2000; <u>66 FR 6928</u>, Jan. 22, 2001; <u>89 FR 43155</u>, May 16, 2024]

# § 63.102 General standards.

(a) Except as specified in <u>paragraph (e)</u> of this section, owners and operators of sources subject to this subpart shall comply with the requirements of <u>subparts G</u> and <u>H of this part</u> as specified in <u>paragraphs (a)(1)</u> through (4) of this section.

(1) The provisions set forth in this subpart and <u>subpart G of this part</u> shall apply at all times except during periods of start-up or shutdown (as defined in § 63.101 of this subpart), malfunction, or non-operation of the chemical manufacturing process unit (or specific portion thereof) resulting in cessation of the emissions to which this subpart and <u>subpart G of this part</u> apply. However, if a start-up, shutdown, malfunction or period of non-operation of one portion of a chemical manufacturing process unit does not affect the ability of a particular emission point to comply with the specific provisions to which it is subpart G of this part that emission point shall still be required to comply with the applicable provisions of this subpart and <u>subpart G of this</u> part during the start-up, shutdown, malfunction or period of non-operation. For example, if there is an overpressure in the reactor area, a storage vessel in the chemical manufacturing process unit would still be required to be controlled in accordance with § 63.119. Similarly, the degassing of a storage vessel would not affect the ability of a process vent to meet the requirements of § 63.113.

(2) The provisions set forth in <u>subpart H of this part</u> shall apply at all times except during periods of start-up or shutdown, malfunction, or process unit shutdown (as defined in § 63.101(b)), or non-operation of the chemical manufacturing process unit (or specific portion thereof) in which the lines are drained and depressurized resulting in cessation of the emissions to which <u>subpart H of this part</u> applies.

(3) The owner or operator shall not shut down items of equipment that are required or utilized for compliance with the provisions of this subpart or <u>subpart G</u> or <u>H of this part</u> during times when emissions (or, where applicable, wastewater streams or residuals) are being routed to such items of equipment, if the shutdown would contravene requirements of this subpart or <u>subpart G</u> or <u>H of this part</u> applicable to such items of equipment. This paragraph does not apply if the item of equipment is malfunctioning, or if the owner or operator must shut down the equipment to avoid damage due to a contemporaneous start-up, shutdown, or malfunction of the chemical manufacturing process unit or portion thereof.

(4) During start-ups, shutdowns, and malfunctions when the requirements of this subpart and subparts G and/or H of this part do not apply pursuant to <u>paragraphs (a)(1)</u> through (3) of this section, the owner or operator shall implement, to the extent reasonably available, measures to prevent or minimize excess emissions to the extent practical. The general duty to minimize emissions during a period of startup, shutdown, or malfunction does not require the owner or operator to achieve emission levels that would be required by the applicable standard at other times if this is not consistent with safety and good air pollution control practices, nor does it require the owner or operator to make any further efforts to reduce emissions if levels required by the applicable standard have been achieved. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator which may include, but is not limited to, monitoring results, review of operation and maintenance procedures (including the startup, shutdown, and malfunction

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plan required in  $\frac{63.6(e)(3)}{2}$ , review of operation and maintenance records, and inspection of the source. The measures to be taken may include, but are not limited to, air pollution control technologies, recovery technologies, work practices, pollution prevention, monitoring, and/or changes in the manner of operation of the source. Back-up control devices are not required but may be used if available.

(b) If, in the judgment of the Administrator, an alternative means of emission limitation will achieve a reduction in organic HAP emissions at least equivalent to the reduction in organic HAP emissions from that source achieved under any design, equipment, work practice, or operational standards in <u>subpart G</u> or <u>H of this part</u>, the Administrator will publish in the Federal Register a notice permitting the use of the alternative means for purposes of compliance with that requirement.

(1) The notice may condition the permission on requirements related to the operation and maintenance of the alternative means.

(2) Any notice under this <u>paragraph (b)</u> shall be published only after public notice and an opportunity for a hearing.

(3) Any person seeking permission to use an alternative means of compliance under this section shall collect, verify, and submit to the Administrator information showing that the alternative means achieves equivalent emission reductions.

(1) If the EPA has approved a State operating permit program under <u>40 CFR part 70</u>, the permit shall be obtained from the State authority. If the State operating permit program has not been approved, the source shall apply to the EPA Regional Office.

(2) [Reserved]

(d) The requirements in this subpart and subparts G and <u>H of this part</u> are federally enforceable under section 112 of the Act on and after the dates specified in  $\S 63.100(k)$  of this subpart.

(e) For each source as defined in § <u>63.101</u>, beginning no later than the compliance dates specified in § <u>63.100(k)(10)</u>, <u>paragraph (a)</u> of this section does not apply. Instead, owners and operators of sources as defined in § <u>63.101</u> shall comply with the requirements in this subpart and <u>subparts G</u> and <u>H of this part</u> at all times, except during periods of nonoperation of the source (or specific portion thereof) resulting in cessation of the emissions to which this subpart or <u>subpart G</u> or <u>H of this part</u> applies.

(f) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), at all times, owners and operators must operate and maintain any source, including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. The general duty to minimize emissions does not require owners and operators to make any further efforts to reduce emissions if levels required by the applicable standard have been achieved. Determination of whether a source is operating in compliance with operation and maintenance requirements will be based on information available to the Administrator which may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.

[89 FR 43163, May 16, 2024]

# § 63.103 General compliance, reporting, and recordkeeping provisions.

(a) Table 3 of this subpart specifies the provisions of subpart A that apply and those that do not apply to owners and operators of sources subject to subparts F, G, and H of this part.

(b) Performance tests and initial compliance determinations shall be required only as specified in <u>subparts G</u> and <u>H of this</u> <u>part</u>.

(1) Initial performance tests and compliance determinations shall be conducted according to the schedule and procedures in § 63.7(a) and the applicable sections of subparts G and H of this part. Beginning no later than the compliance dates specified in § 63.100(k)(10), except as outlined in subpart H of this part, conduct subsequent performance tests no later than 60 calendar months after the previous performance test.

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(2) The owner or operator shall notify the Administrator of the intention to conduct a performance test at least 30 calendar days before the performance test is scheduled to allow the Administrator the opportunity to have an observer present during the test.

(3) Performance tests shall be conducted as specified in <u>paragraph (b)(3)(i)</u> or (ii) of this section.

(i) Except as specified in <u>paragraph (b)(3)(ii)</u> of this section, performance tests shall be conducted according to the provisions of  $\S$  63.7(e), except that performance tests shall be conducted at maximum representative operating conditions for the process. During the performance test, an owner or operator may operate the control or recovery device at maximum or minimum representative operating conditions for monitored control or recovery device parameters, whichever results in lower emission reduction.

(ii) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$ 

63.100(k)(10), paragraph (b)(3)(i) of this section no longer applies and instead the owner or operator may not conduct performance tests during periods of malfunction. Owners and operators must record the process information that is necessary to document operating conditions during the test and include in such record an explanation to support that such conditions represent normal operation. Upon request, owners and operators must make available to the Administrator such records as may be necessary to determine the conditions of performance tests.

(4) Data shall be reduced in accordance with the EPA-approved methods specified in the applicable subpart or, if other test methods are used, the data and methods shall be validated according to the protocol in Method 301 of <u>appendix A of this part</u>.

(5) Performance tests may be waived with approval of the Administrator as specified in § 63.7(h)(2) of subpart A of this part. Owners or operators of sources subject to subparts F, G, and <u>H of this part</u> who apply for a waiver of a performance test shall submit the application by the dates specified in <u>paragraph (b)(5)(i)</u> of this section rather than the dates specified in § 63.7(h)(3) of subpart A of this part.

(i) If a request is made for an extension of compliance under  $\S$  <u>63.151(a)(6)</u> of subpart G or  $\S$  <u>63.6(i)</u> of <u>subpart A of this part</u>, the application for a waiver of an initial performance test shall accompany the information required for the request for an extension of compliance. If no extension of compliance is requested, the application for a waiver of an initial performance test shall be submitted no later than 90 calendar days before the Notification of Compliance Status required in  $\S$  <u>63.152(b)</u> of <u>subpart G of this part</u> is due to be submitted.

(ii) Any application for a waiver of a performance test shall include information justifying the owner or operator's request for a waiver, such as the technical or economic infeasibility, or the impracticality, of the source performing the required test.

(6) The owner or operator of a flexible operation unit shall conduct all required compliance demonstrations during production of the primary product. The owner or operator is not required to conduct compliance demonstrations for operating conditions during production of a product other than the primary product. Except as otherwise provided in this subpart or in subpart G or <u>subpart H of this part</u>, as applicable, the owner or operator shall operate each control device, recovery device, and/or recapture device that is required or used for compliance, and associated monitoring systems, without regard for whether the product that is being produced is the primary product or a different product. Except as otherwise provided in this subpart, subpart G and/or <u>subpart H of this part</u>, as applicable, operation of a control device, recapture device and/or recovery device required or used for compliance such that the daily average of monitored parameter values is outside the parameter range established pursuant to  $\frac{63.152(b)(2)}{63.120(d)(2)}$  or  $\frac{63.181(g)(1)(iv)}{50.181(g)(1)(iv)}$ , shall constitute a violation of the required operating conditions.

(c) Each owner or operator of a source subject to <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> shall keep copies of all applicable reports and records required by <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> for at least 5 years; except that, if subparts G or H require records to be maintained for a time period different than 5 years, those records shall be maintained for the time specified in <u>subpart</u> <u>G</u> or <u>H of this part</u>. If an owner or operator submits copies of reports to the applicable EPA Regional Office, the owner or operator is not required to maintain copies of reports. If the EPA Regional Office has waived the requirement of § <u>63.10(a)(4)(ii)</u> for submittal of copies of reports, the owner or operator is not required to maintain copies of reports.

(1) All applicable records shall be maintained in such a manner that they can be readily accessed. The most recent 6 months of records shall be retained on site or shall be accessible from a central location by computer or other means that provides access within 2 hours after a request. The remaining four and one-half years of records may be retained offsite. Records may be maintained in hard copy or computer-readable form including, but not limited to, on paper, microfilm, computer, floppy disk, magnetic tape, or microfiche.

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(2) The owner or operator subject to subparts  $\underline{F}$ ,  $\underline{G}$ , and  $\underline{H}$  of this part shall keep the records specified in this paragraph, as well as records specified in subparts G and H.

(i) Records of the occurrence and duration of each start-up, shutdown, and malfunction of operation of process equipment or of air pollution control equipment or continuous monitoring systems used to comply with this subpart or <u>subpart G</u> or <u>H of</u> this part during which excess emissions (as defined in § 63.102(a)(4)) occur. For each source as defined in § 63.101, on and after July 15, 2027, this <u>paragraph (c)(2)(i)</u> no longer applies; however, for historical compliance purposes, a copy of these records must be retained and available on-site for at least five years after the date of occurrence.

(ii) For each start-up, shutdown, and malfunction during which excess emissions (as defined in  $\S$  63.102(a)(4)) occur, records that the procedures specified in the source's start-up, shutdown, and malfunction plan were followed, and documentation of actions taken that are not consistent with the plan. For example, if a start-up, shutdown, and malfunction plan includes procedures for routing a control device to a backup control device (*e.g.*, the incinerator for a halogenated stream could be routed to a flare during periods when the primary control device is out of service), records must be kept of whether the plan was followed. These records may take the form of a "checklist," or other form of recordkeeping that confirms conformance with the start-up, shutdown, and malfunction plan for the event. For each source as defined in  $\S$  63.101, on and after July 15, 2027, this paragraph (c)(2)(ii) no longer applies; however, for historical compliance purposes, a copy of the plan and these records must be retained and available on-site for 5 years after July 15, 2027.

(iii) For continuous monitoring systems used to comply with <u>subpart G of this part</u>, records documenting the completion of calibration checks and maintenance of continuous monitoring systems that are specified in the manufacturer's instructions or other written procedures that provide adequate assurance that the equipment would reasonably be expected to monitor accurately.inning no later than the compliance dates specified in  $\frac{63.100(k)(10)}{10}$ , the manufacturer's specifications specified in <u>paragraph (c)(2)(iii)</u> of this section must include a schedule for calibrations, preventative maintenance procedures, a schedule for preventative maintenance, and corrective actions to be taken if a calibration fails. If a continuous monitoring system is considered to be inoperative until the owner or operator takes corrective action and the system passes calibration. The owner or operator must record the nature and cause of instances when the continuous monitoring system is inoperative action taken.

(3) Records of start-up, shutdown and malfunction and continuous monitoring system calibration and maintenance are not required if they pertain solely to Group 2 emission points, as defined in § 63.101, that are not included in an emissions average. For each source as defined in § 63.101, on and after July 15, 2027, the phrase "start-up, shutdown and malfunction and" in this paragraph (c)(3) no longer applies.

(d) Unless required to be submitted electronically via the EPA's CEDRI, all reports required under this subpart and <u>subparts</u> <u>G</u> and <u>H of this part</u> must be sent to the Administrator at the addresses listed in § 63.13, except that requests for permission to use an alternative means of compliance as provided for in § 63.102(b) of this subpart and application for approval of a nominal efficiency as provided for in § 63.150 (i)(1) through (6) must be submitted to the Director of the EPA Office of Air Quality Planning and Standards rather than to the Administrator or delegated authority.

(1) Wherever subpart A of this part specifies "postmark" dates, submittals may be sent by methods other than the U.S. Mail (*e.g.*, by fax or courier). Submittals shall be sent on or before the specified date.

(2) If acceptable to both the Administrator and the owner or operator of a source, reports may be submitted on electronic media.

(e) The owner or operator of a chemical manufacturing process unit which meets the criteria of  $\frac{63.100(b)(1)}{2}$ , but not the criteria of  $\frac{63.100(b)(2)}{2}$ , shall comply with the requirements of either <u>paragraph (e)(1)</u> or (2) of this section.

(1) Retain information, data, and analysis used to determine that the chemical manufacturing process unit does not use as a reactant or manufacture as a product or co-product any organic hazardous air pollutant. Examples of information that could document this include, but are not limited to, records of chemicals purchased for the process, analyses of process stream composition, engineering calculations, or process knowledge.

(2) When requested by the Administrator, demonstrate that the chemical manufacturing process unit does not use as a reactant or manufacture as a product or co-product any organic hazardous air pollutant.

(f) To qualify for the exemption specified in  $\S 63.100(b)(4)$ , the owner or operator shall maintain the documentation of the information required pursuant to  $\S 63.100(b)(4)(i)$ , and documentation of any update of this information requested by the EPA Regional Office, and shall provide the documentation to the EPA Regional Office upon request. The EPA Regional

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Office will notify the owner or operator, after reviewing such documentation, if the source does not qualify for the exemption specified in § 63.100(b)(4). In such cases, compliance with subpart H shall be required no later than 90 days after expiration of the applicable compliance date in § 63.100(k)(3), but in no event earlier than 90 days after the date of such notification by the EPA Regional Office. Compliance with this subpart and subpart G of this part shall be no later than April 22, 1997, or as otherwise specified in § 63.100(k)(2)(ii), unless an extension has been granted by the EPA Regional Office or permitting authority as provided in § 63.60(i).

(g) An owner or operator who elects to use the compliance extension provisions of  $\frac{63.100(k)(6)(i)}{60}$  or (ii) shall submit a compliance extension request to the appropriate EPA Regional Office no later than 45 days before the applicable compliance date in  $\frac{63.100(k)(3)}{63.100(k)(3)}$ , but in no event is submittal required earlier than May 10, 1995. The request shall contain the information specified in  $\frac{63.100(k)(5)(iv)}{40.000}$  and the reason compliance cannot reasonably be achieved without a process unit shutdown, as defined in  $\frac{40.0000}{40.0000}$  or without replacement of the compressor or recasting of the distance piece.

(h) An owner or operator who elects to use the compliance extension provisions of  $\frac{63.100(k)(8)}{63.100(k)(8)}$  shall submit to the appropriate EPA Regional Office a brief description of the process change, identify the HAP eliminated, and the expected date of cessation of use or production of HAP. The description shall be submitted no later than May 10, 1995, or with the Notice of Compliance Status as required in  $\frac{63.182(c)}{53.182(c)}$ , whichever is later.

[<u>59 FR 19454</u>, Apr. 22, 1994, as amended at <u>59 FR 48176</u>, Sept. 20, 1994; <u>60 FR 18024</u>, Apr. 10, 1995; <u>62 FR 2733</u>, Jan. 17, 1997; <u>63 FR 26082</u>, May 12, 1998; <u>89 FR 43164</u>, May 16, 2024]

# § 63.104 Heat exchange system requirements.

(a) Unless one or more of the conditions specified in paragraphs (a)(1) through (6) or <u>paragraph (1)</u> of this section are met, owners and operators of sources subject to this subpart shall monitor each heat exchange system used to cool process equipment in a chemical manufacturing process unit meeting the conditions of § 63.100(b)(1) through (3), except for chemical manufacturing process units meeting the condition specified in § 63.100(c), according to the provisions in either <u>paragraph (b)</u> or (c) of this section, and if applicable, <u>paragraph (g)</u> of this section. Whenever a leak is detected, the owner or operator shall comply with the requirements in <u>paragraph (d)</u> of this section, and if applicable, <u>paragraphs (h)</u> through (j) of this section. Owners and operators of heat exchange systems in a chemical manufacturing process unit meeting the conditions of § 63.100(b)(1) through (3) must also comply with <u>paragraph (k)</u> of this section.

(1) The heat exchange system is operated with the minimum pressure on the cooling water side at least 35 kilopascals greater than the maximum pressure on the process side.

(2) There is an intervening cooling fluid, containing less than 5 percent by weight of total hazardous air pollutants listed in table 4 of this subpart, between the process and the cooling water. This intervening fluid serves to isolate the cooling water from the process fluid and the intervening fluid is not sent through a cooling tower or discharged. For purposes of this section, discharge does not include emptying for maintenance purposes.

(3) The once-through heat exchange system is subject to a National Pollution Discharge Elimination System (NPDES) permit with an allowable discharge limit of 1 part per million or less above influent concentration or 10 percent or less above influent concentration, whichever is greater. For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), this paragraph (a)(3) no longer applies.

(4) Except as specified in <u>paragraph (a)(4)(v)</u> of this section, the once-through heat exchange system is subject to an NPDES permit that:

(i) Requires monitoring of a parameter(s) or condition(s) to detect a leak of process fluids into cooling water;

(ii) Specifies or includes the normal range of the parameter or condition;

(iii) Requires monitoring for the parameters selected as leak indicators no less frequently than monthly for the first six months and quarterly thereafter; and

(iv) Requires the owner or operator to report and correct leaks to the cooling water when the parameter or condition exceeds the normal range.

(v) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), this paragraph (a)(4) no longer applies.

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(b) The owner or operator who elects to comply with the requirements of paragraph(a) of this section by monitoring the cooling water for the presence of one or more organic hazardous air pollutants or other representative substances whose presence in cooling water indicates a leak shall comply with the requirements specified in paragraphs(b)(1) through (b)(6) of this section. The cooling water shall be monitored for total hazardous air pollutants, total volatile organic compounds, total organic carbon, one or more speciated HAP compounds, or other representative substances that would indicate the presence of a leak in the heat exchange system.

(1) The cooling water shall be monitored monthly for the first 6 months and quarterly thereafter to detect leaks.

(2)

(i) For recirculating heat exchange systems (cooling tower systems), the monitoring of speciated hazardous air pollutants or total hazardous air pollutants refers to the hazardous air pollutants listed in table 4 of this subpart.

(ii) For once-through heat exchange systems, the monitoring of speciated hazardous air pollutants or total hazardous air pollutants refers to the hazardous air pollutants listed in table 9 of <u>subpart G of this part</u>.

(3) The concentration of the monitored substance(s) in the cooling water shall be determined using any EPA-approved method listed in <u>part 136 of this chapter</u> as long as the method is sensitive to concentrations as low as 10 parts per million and the same method is used for both entrance and exit samples. Alternative methods may be used upon approval by the Administrator.

(4) The samples shall be collected either at the entrance and exit of each heat exchange system or at locations where the cooling water enters and exits each heat exchanger or any combination of heat exchangers.

(i) For samples taken at the entrance and exit of recirculating heat exchange systems, the entrance is the point at which the cooling water leaves the cooling tower prior to being returned to the process equipment and the exit is the point at which the cooling water is introduced to the cooling tower after being used to cool the process fluid.

(ii) For samples taken at the entrance and exit of once-through heat exchange systems, the entrance is the point at which the cooling water exits the plant site or chemical manufacturing process units.

(iii) For samples taken at the entrance and exit of each heat exchanger or any combination of heat exchangers in chemical manufacturing process units, the entrance is the point at which the cooling water enters the individual heat exchanger or group of heat exchangers and the exit is the point at which the cooling water exits the heat exchanger or group of heat exchangers.

(5) A minimum of three sets of samples shall be taken at each entrance and exit as defined in <u>paragraph (b)(4)</u> of this section. The average entrance and exit concentrations shall then be calculated. The concentration shall be corrected for the addition of any makeup water or for any evaporative losses, as applicable.

(6) A leak is detected if the exit mean concentration is found to be greater than the entrance mean using a one-sided statistical procedure at the 0.05 level of significance and the amount by which it is greater is at least 1 part per million or 10 percent of the entrance mean, whichever is greater.

(c) The owner or operator who elects to comply with the requirement of <u>paragraph (a)</u> of this section by monitoring using a surrogate indicator of heat exchange system leaks shall comply with the requirements specified in <u>paragraphs</u> (c)(1) through (c)(3) of this section. Surrogate indicators that could be used to develop an acceptable monitoring program are ion specific electrode monitoring, pH, conductivity or other representative indicators.

(1) The owner or operator shall prepare and implement a monitoring plan that documents the procedures that will be used to detect leaks of process fluids into cooling water. The plan shall require monitoring of one or more surrogate indicators or monitoring of one or more process parameters or other conditions that indicate a leak. Monitoring that is already being conducted for other purposes may be used to satisfy the requirements of this section. The plan shall include the information specified in paragraphs (c)(1)(i) and (c)(1)(ii) of this section.

(i) A description of the parameter or condition to be monitored and an explanation of how the selected parameter or condition will reliably indicate the presence of a leak.

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(ii) The parameter level(s) or conditions(s) that shall constitute a leak. This shall be documented by data or calculations showing that the selected levels or conditions will reliably identify leaks. The monitoring must be sufficiently sensitive to determine the range of parameter levels or conditions when the system is not leaking. When the selected parameter level or condition is outside that range, a leak is indicated.

(iii) The monitoring frequency which shall be no less frequent than monthly for the first 6 months and quarterly thereafter to detect leaks.

(iv) The records that will be maintained to document compliance with the requirements of this section.

(2) If a substantial leak is identified by methods other than those described in the monitoring plan and the method(s) specified in the plan could not detect the leak, the owner or operator shall revise the plan and document the basis for the changes. The owner or operator shall complete the revisions to the plan no later than 180 days after discovery of the leak.

(3) The owner or operator shall maintain, at all times, the monitoring plan that is currently in use. The current plan shall be maintained on-site, or shall be accessible from a central location by computer or other means that provides access within 2 hours after a request. If the monitoring plan is superseded, the owner or operator shall retain the most recent superseded plan at least until 5 years from the date of its creation. The superseded plan shall be retained on-site (or accessible from a central location by computer or other means that provides access within two hours after a request) for at least 6 months after its creation.

(d) If a leak is detected according to the criteria of <u>paragraph (b)</u> or (c) of this section, the owner or operator shall comply with the requirements in <u>paragraphs (d)(1)</u> and (d)(2) of this section, except as provided in <u>paragraph (e)</u> of this section.

(1) The leak shall be repaired as soon as practical but not later than 45 calendar days after the owner or operator receives results of monitoring tests indicating a leak. The leak shall be repaired unless the owner or operator demonstrates that the results are due to a condition other than a leak.

(2) Once the leak has been repaired, the owner or operator shall confirm that the heat exchange system has been repaired within 7 calendar days of the repair or startup, whichever is later.

(e) Delay of repair of heat exchange systems for which leaks have been detected is allowed if the equipment is isolated from the process. Delay of repair is also allowed if repair is technically infeasible without a shutdown and any one of the conditions in <u>paragraph (e)(1)</u> or (e)(2) of this section is met. All time periods in <u>paragraphs (e)(1)</u> and (e)(2) of this section shall be determined from the date when the owner or operator determines that delay of repair is necessary.

(1) If a shutdown is expected within the next 2 months, a special shutdown before that planned shutdown is not required.

(2) If a shutdown is not expected within the next 2 months, the owner or operator may delay repair as provided in <u>paragraph</u>  $(\underline{e})(2)(\underline{i})$  or  $(\underline{e})(2)(\underline{i})$  of this section. Documentation of a decision to delay repair shall state the reasons repair was delayed and shall specify a schedule for completing the repair as soon as practical.

(i) If a shutdown for repair would cause greater emissions than the potential emissions from delaying repair, the owner or operator may delay repair until the next shutdown of the process equipment associated with the leaking heat exchanger. The owner or operator shall document the basis for the determination that a shutdown for repair would cause greater emissions than the emissions likely to result from delaying repair as specified in <u>paragraphs (e)(2)(i)(A)</u> and (e)(2)(i)(B) of this section.

(A) The owner or operator shall calculate the potential emissions from the leaking heat exchanger by multiplying the concentration of total hazardous air pollutants listed in table 4 of this subpart in the cooling water from the leaking heat exchanger by the flowrate of the cooling water from the leaking heat exchanger by the expected duration of the delay. The owner or operator may calculate potential emissions using total organic carbon concentration instead of total hazardous air pollutants listed in table 4 of this subpart.

(B) The owner or operator shall determine emissions from purging and depressurizing the equipment that will result from the unscheduled shutdown for the repair.

(ii) If repair is delayed for reasons other than those specified in <u>paragraph (e)(2)(i)</u> of this section, the owner or operator may delay repair up to a maximum of 120 calendar days. The owner shall demonstrate that the necessary parts or personnel were not available.

(f)

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(1) *Required records*. The owner or operator shall retain the records identified in <u>paragraphs (f)(1)(i)</u> through (iv) of this section, and if applicable, <u>paragraph (f)(3)</u> of this section, as specified in  $\frac{\& 63.103(c)(1)}{\& 63.103(c)(1)}$ .

(i) Monitoring data required by this section indicating a leak and the date when the leak was detected, and if demonstrated not to be a leak, the basis for that determination;

(ii) Records of any leaks detected by procedures subject to <u>paragraph (c)(2)</u> of this section and the date the leak was discovered;

(iii) The dates of efforts to repair leaks; and

(iv) The method or procedure used to confirm repair of a leak and the date repair was confirmed.

(2) *Reports.* If an owner or operator invokes the delay of repair provisions for a heat exchange system, the following information shall be submitted in the next semi-annual periodic report required by § 63.152(c). If the leak remains unrepaired, the information shall also be submitted in each subsequent periodic report, until repair of the leak is reported. In addition, if an owner or operator is complying with <u>paragraph (g)</u> or (<u>1</u>) of this section, then the semi-annual periodic report must include the information specified in <u>paragraph (f)(2)(vi)</u> of this section.

(i) The owner or operator shall report the presence of the leak by identifying the heat exchange system and the date that the leak was detected.

(ii) The owner or operator shall report whether or not the leak has been repaired.

(iii) The owner or operator shall report the reason(s) for delay of repair. If delay of repair is invoked due to the reasons described in <u>paragraph (e)(2)</u> of this section, documentation of emissions estimates must also be submitted.

(iv) If the leak remains unrepaired, the owner or operator shall report the expected date of repair.

(v) If the leak is repaired, the owner or operator shall report the date the leak was successfully repaired.

(vi) For each heat exchange system subject to <u>paragraph (g)</u> or (<u>1</u>) of this section, the following information must be submitted in each semi-annual periodic report required by  $\S 63.152(c)$ .

(A) The number of heat exchange systems at the plant site subject to the monitoring requirements in <u>paragraph (g)</u> or (<u>l)</u> of this section during the reporting period.

(B) The number of heat exchange systems subject to the monitoring requirements in <u>paragraph (g)</u> or <u>(1)</u> of this section at the plant site found to be leaking during the reporting period.

(C) For each monitoring location where a leak was identified during the reporting period, identification of the monitoring location (*e.g.*, unique monitoring location or heat exchange system ID number), the measured total strippable hydrocarbon concentration (in ppmv as methane) or total hydrocarbon mass emissions rate (in kg/hr as methane) (if complying with paragraph (g) of this section) or the measured concentration of the monitored substance(s) (in ppmv) (if complying with paragraph (l) of this section), the date the leak was first identified, and, if applicable, the date the source of the leak was identified;

(D) For leaks that were repaired during the reporting period (including delayed repairs), identification of the monitoring location associated with the repaired leak, the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with <u>paragraph (g)</u> of this section) or the measured concentration of the monitored substance(s) (if complying with <u>paragraph (l)</u> of this section) measured during re-monitoring to verify repair, and the re-monitoring date (*i.e.*, the effective date of repair); and

(E) For each delayed repair, identification of the monitoring location associated with the leak for which repair is delayed, the date when the delay of repair began, the date the repair was completed or is expected to be completed (if the leak is not repaired during the reporting period), the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with <u>paragraph (g)</u> of this section) or the measured concentration of the monitored substance(s) (if complying with <u>paragraph (l)</u> of this section) and date of each monitoring event conducted on the delayed repair during the reporting period, and an estimate in pounds of the potential total hydrocarbon emissions or monitored substance(s) emissions over the reporting period associated with the delayed repair.

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(3) Additional records. For each heat exchange system subject to paragraph (g) or (l) of this section, owners and operators must also keep records in paragraphs ( $f_{(3)(1)}$  through (iv) of this section.

(i) Monitoring data required by <u>paragraph (g)</u> or <u>(1)</u> of this section that indicate a leak, the date the leak was detected, or, if applicable, the basis for determining there is no leak.

(ii) The dates of efforts to repair leaks.

(iii) The method or procedures used to confirm repair of a leak and the date the repair was confirmed.

(iv) Documentation of delay of repair as specified in <u>paragraphs (f)(3)(iv)(A)</u> through (f)(3)(iv)(D) of this section.

(A) The reason(s) for delaying repair.

(B) A schedule for completing the repair as soon as practical.

(C) The date and concentration or mass emissions rate of the leak as first identified and the results of all subsequent monitoring events during the delay of repair.

(D) An estimate of the potential total hydrocarbon emissions (if monitoring the cooling water for leaks according to paragraph (g)(1) of this section) or monitored substance(s) emissions (if monitoring the cooling water for leaks according to paragraph (l) of this section) from the leaking heat exchange system or heat exchanger for each required delay of repair monitoring interval following the procedures in paragraphs (f)(3)(iv)(D)(1) through (4) of this section.

(1) If an owner or operator complies with the total strippable hydrocarbon concentration leak action level, as specified in paragraph (g)(4) of this section, then the owner or operator must calculate the mass emissions rate by complying with the requirements of paragraph (g)(3)(ii) of this section or by determining the mass flow rate of the cooling water at the monitoring location where the leak was detected. If the monitoring location is an individual cooling tower riser, determine the total cooling water mass flow rate to the cooling tower. Cooling water mass flow rates may be determined using direct measurement, pump curves, heat balance calculations, or other engineering methods. If an owner or operator determines the mass flow rate of the cooling water, calculate the mass emissions rate by converting the stripping gas leak concentration (in ppmv as methane) to an equivalent liquid concentration, in parts per million by weight (ppmw), using equation 7-1 from "Air Stripping Method (Modified El Paso Method) for Determination of Volatile Organic Compound Emissions from Water Sources" (incorporated by reference—see § 63.14) and multiply the equivalent liquid concentration by the mass flow rate of the cooling water.

(2) For delay of repair monitoring intervals prior to repair of the leak, calculate the potential total hydrocarbon emissions or monitored substance(s) emissions for the leaking heat exchange system or heat exchanger for the monitoring interval by multiplying the mass emissions rate, determined in paragraph (g)(3)(ii) or (f)(3)(iv)(D)(1) or (4) of this section, by the duration of the delay of repair monitoring interval. The duration of the delay of repair monitoring interval is the time period starting at midnight on the day of the previous monitoring event or at midnight on the day the repair would have had to be completed if the repair had not been delayed, whichever is later, and ending at midnight of the day the of the current monitoring event.

(3) For delay of repair monitoring intervals ending with a repaired leak, calculate the potential total hydrocarbon emissions or monitored substance(s) emissions for the leaking heat exchange system or heat exchanger for the final delay of repair monitoring interval by multiplying the duration of the final delay of repair monitoring interval by the mass emissions rate determined for the last monitoring event prior to the re-monitoring event used to verify the leak was repaired. The duration of the final delay of repair monitoring event prior to re-monitoring to verify the leak was repaired and ending at the time of the re-monitoring event that verified that the leak was repaired.

(4) If an owner or operator monitors the cooling water for leaks according to <u>paragraph (1)</u> of this section, then the owner or operator must calculate the mass emissions rate by determining the mass flow rate of the cooling water at the monitoring location where the leak was detected. Cooling water mass flow rates may be determined using direct measurement, pump curves, heat balance calculations, or other engineering methods. Once determined, multiply the mass flow rate of the cooling water by the concentration of the measured substance(s).

(g) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), owners and operators must monitor the cooling water for the presence of total strippable hydrocarbons that indicate a leak according to paragraph (g)(1) of this section, and if an owner or operator detects a leak pursuant to the procedures in this paragraph,

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then the owner or operator must repair it according to <u>paragraphs (h)</u> and <u>(i)</u> of this section, unless repair is delayed according to <u>paragraph (j)</u> of this section. The requirements in this paragraph do not apply to heat exchange systems that have a maximum cooling water flow rate of 10 gallons per minute or less.

(1) For each recirculating heat exchange system subject to the requirements of <u>paragraph (g)</u> of this section, owners and operators must collect and analyze a sample from the location(s) described in either <u>paragraph (g)(1)(i)</u> or <u>(ii)</u> of this section.

(i) Each cooling tower return line or any representative riser within the cooling tower prior to exposure to air for each heat exchange system.

(ii) Selected heat exchanger exit line(s), so that each heat exchanger or group of heat exchangers within a heat exchange system is covered by the selected monitoring location(s).

(2) For each once-through heat exchange system, owners and operators must collect and analyze a sample from the location(s) described in <u>paragraph (g)(2)(i)</u> of this section. The owner or operator may also elect to collect and analyze an additional sample from the location(s) described in <u>paragraph (g)(2)(ii)</u> of this section.

(i) Selected heat exchanger exit line(s), so that each heat exchanger or group of heat exchangers within a heat exchange system is covered by the selected monitoring location(s). The selected monitoring location may be at a point where discharges from multiple heat exchange systems are combined provided that the combined cooling water flow rate at the monitoring location does not exceed 40,000 gallons per minute.

(ii) The inlet water feed line for a once-through heat exchange system prior to any heat exchanger. If multiple heat exchange systems use the same water feed (*i.e.*, inlet water from the same primary water source), the owner or operator may monitor at one representative location and use the monitoring results for that sampling location for all heat exchange systems that use that same water feed.

(3) If an owner or operator complies with the total strippable hydrocarbon concentration leak action level as specified in paragraph (g)(4) of this section, then the owner or operator must comply with the requirements in paragraph (g)(3)(i) of this section. If an owner or operator complies with the total hydrocarbon mass emissions rate leak action level as specified in paragraph (g)(4) of this section, then the owner or operator must comply with the requirements in paragraph (g)(3)(i) of (g)(3)(i) and (ii) of this section.

(i) Owners and operators must determine the total strippable hydrocarbon concentration (in parts per million by volume (ppmv) as methane) at each monitoring location using the "Air Stripping Method (Modified El Paso Method) for Determination of Volatile Organic Compound Emissions from Water Sources" (incorporated by reference—see § 63.14) using a flame ionization detector (FID) analyzer for on-site determination as described in Section 6.1 of the Modified El Paso Method.

(ii) Owners and operators must convert the total strippable hydrocarbon concentration (in ppmv as methane) to a total hydrocarbon mass emissions rate (as methane) using the calculations in Section 7.0 of "Air Stripping Method (Modified El Paso Method) for Determination of Volatile Organic Compound Emissions from Water Sources" (incorporated by reference—see § 63.14).

(4) Except as specified in paragraph (g)(6) of this section, for each heat exchange system, owners and operators must initially monitor monthly for 6-months beginning upon startup and monitor quarterly thereafter using a leak action level defined as a total strippable hydrocarbon concentration (as methane) in the stripping gas of 6.2 ppmv or, for heat exchange systems with a recirculation rate of 10,000 gallons per minute or less, the owner or operator may monitor quarterly using a leak action level defined as a total hydrocarbon mass emissions rate from the heat exchange system (as methane) of 0.18 kg/hr. If a leak is detected as specified in paragraph (g)(5) of this section, then owners and operators must monitor monthly until the leak has been repaired according to the requirements in paragraph (h) or (i) of this section. Once the leak has been repaired according to the requirements in paragraph also apply to the inlet water feed line for a once-through heat exchange system, if monitoring of the inlet water feed is elected as provided in paragraph (g)(2)(ii) of this section.

(5) A leak is defined as described in <u>paragraph (g)(5)(i)</u> or <u>(ii)</u> of this section, as applicable.

(i) For once-through heat exchange systems for which the inlet water feed is monitored as described in paragraph (g)(2)(ii) of this section, a leak is detected if the difference in the measurement value of the sample taken from a location specified

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in <u>paragraph (g)(2)(i)</u> of this section and the measurement value of the corresponding sample taken from the location specified in <u>paragraph (g)(2)(ii)</u> of this section equals or exceeds the leak action level.

(ii) For all other heat exchange systems, a leak is detected if a measurement value of the sample taken from a location specified in <u>paragraph (g)(1)(i)</u> or <u>(ii)</u> or <u>(g)(2)(i)</u> of this section equals or exceeds the leak action level.

(6) For heat exchange systems in ethylene oxide service, as defined in  $\S$  63.101, the monitoring frequency is weekly.

(h) If a leak is detected using the methods described in <u>paragraph (g)</u> of this section, owners and operators must repair the leak to reduce the concentration or mass emissions rate to below the applicable leak action level as soon as practicable, but no later than 45 days after identifying the leak, except as specified in <u>paragraph (h)(6)</u> or (j) of this section. Repair must include re-monitoring at the monitoring location where the leak was identified according to the method specified in <u>paragraph</u> (g)(3) of this section to verify that the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is below the applicable leak action level. Repair may also include performing the additional monitoring in <u>paragraph (i)</u> of this section to verify that the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is below the applicable leak action level. Actions that can be taken to achieve repair include but are not limited to:

(1) Physical modifications to the leaking heat exchanger, such as welding the leak or replacing a tube;

(2) Blocking the leaking tube within the heat exchanger;

(3) Changing the pressure so that water flows into the process fluid;

(4) Replacing the heat exchanger or heat exchanger bundle; or

(5) Isolating, bypassing, or otherwise removing the leaking heat exchanger from service until it is otherwise repaired.

(6) For heat exchange systems in ethylene oxide service, as defined in  $\frac{63.101}{100}$ , paragraph (j) of this section does not apply, and owners and operators must repair the leak to reduce the concentration or mass emissions rate to below the applicable leak action level as soon as practicable, but no later than 15 days after the sample was collected. Delay of repair of heat exchange systems in ethylene oxide service for which leaks have been detected is allowed if the equipment is isolated from the process such that it is no longer in ethylene oxide service.

(i) If an owner or operator detects a leak when monitoring a cooling tower return line under <u>paragraph (g)(1)(i)</u> of this section, then the owner or operator may conduct additional monitoring of each heat exchanger or group of heat exchangers associated with the heat exchange system for which the leak was detected, as provided in <u>paragraph (g)(1)(ii)</u> of this section. If no leaks are detected when monitoring according to the requirements of <u>paragraph (g)(1)(ii)</u> of this section, the heat exchange system is considered to have met the repair requirements through re-monitoring of the heat exchange system, as provided in <u>paragraph (h)</u> of this section.

(j) Owners and operators may delay repair when one of the conditions in <u>paragraph (j)(1)</u> or (2) of this section is met and the leak is less than the delay of repair action level specified in <u>paragraph (j)(3)</u> of this section. Owners and operators must determine if a delay of repair is necessary as soon as practicable, but no later than 45 days after first identifying the leak.

(1) If the repair is technically infeasible without a shutdown and the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is initially and remains less than the delay of repair action level for all monitoring periods during the delay of repair, then the owner or operator may delay repair until the next scheduled shutdown of the heat exchange system. If, during subsequent monitoring, the delay of repair action level is exceeded, then owners and operators must repair the leak within 30 days of the monitoring event in which the leak was equal to or exceeded the delay of repair action level.

(2) If the necessary equipment, parts, or personnel are not available and the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is initially and remains less than the delay of repair action level for all monitoring periods during the delay of repair, then the owner or operator may delay the repair for a maximum of 120 calendar days. Owners and operators must demonstrate that the necessary equipment, parts, or personnel were not available. If, during subsequent monitoring, the delay of repair action level is exceeded, then owners and operators must repair the leak within 30 days of the monitoring event in which the leak was equal to or exceeded the delay of repair action level.

(3) The delay of repair action level is a total strippable hydrocarbon concentration (as methane) in the stripping gas of 62 ppmv or, for heat exchange systems with a recirculation rate of 10,000 gallons per minute or less, the delay of repair action

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level is a total hydrocarbon mass emissions rate (as methane) of 1.8 kg/hr. The delay of repair action level is assessed as described in paragraph (j)(3)(i) or (ii) of this section, as applicable.

(i) For once-through heat exchange systems for which the inlet water feed is monitored as described in <u>paragraph (g)(2)(ii)</u> of this section, the delay of repair action level is exceeded if the difference in the measurement value of the sample taken from a location specified in <u>paragraph (g)(2)(i)</u> of this section and the measurement value of the corresponding sample taken from the location specified in <u>paragraph (g)(2)(ii)</u> of this section equals or exceeds the delay of repair action level.

(ii) For all other heat exchange systems, the delay of repair action level is exceeded if a measurement value of the sample taken from a location specified in paragraph (g)(1)(i), (1)(ii), or (2)(i) of this section equals or exceeds the delay of repair action level.

(k) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(11), owners and operators must not inject water into or dispose of water through any heat exchange system in a chemical manufacturing process unit meeting the conditions of § 63.100(b)(1) through (3) if the water contains any amount of ethylene oxide, has been in contact with any process stream containing ethylene oxide, or the water is considered wastewater as defined in § 63.101.

(1) If 99 percent by weight or more of the organic compounds that could leak into the heat exchange system are water soluble and have a Henry's Law Constant less than 5.0E-6 atmospheres-cubic meters/mol at 25 degrees Celsius, beginning no later than the compliance dates specified in  $\S$  63.100(k)(10), owners and operators may monitor the cooling water for leaks according to the requirements in paragraph (b) of this section in lieu of using the Modified El Paso Method. If an owner or operator detects a leak according to paragraph (b) of this section, then the owner or operator must repair it according to paragraph (l)(1) of this section, unless repair is delayed according to paragraph (l)(2) of this section.

(1) If a leak is detected using the methods described in <u>paragraph (1)</u> of this section, the owner or operator must repair the leak as soon as practicable, but no later than 45 days after identifying the leak, except as specified in <u>paragraph (1)(2)</u> of this section. Repair must include re-monitoring at the monitoring location where the leak was identified to verify that the criteria in <u>paragraph (b)(6)</u> of this section is no longer met. Actions that can be taken to achieve repair include but are not limited to:

(i) Physical modifications to the leaking heat exchanger, such as welding the leak or replacing a tube;

- (ii) Blocking the leaking tube within the heat exchanger;
- (iii) Changing the pressure so that water flows into the process fluid;
- (iv) Replacing the heat exchanger or heat exchanger bundle; or
- (v) Isolating, bypassing, or otherwise removing the leaking heat exchanger from service until it is otherwise repaired.
- (2) The owner or operator may delay repair when the conditions in <u>paragraph (e)</u> of this section are met.

[62 FR 2733, Jan. 17, 1997, as amended at 89 FR 43166, May 16, 2024]

# § 63.105 Maintenance wastewater requirements.

(a) Each owner or operator of a source subject to this subpart shall comply with the requirements of <u>paragraphs</u>
(b) through (c) of this section for maintenance wastewaters containing those organic HAP's listed in table 9 of <u>subpart G of this part</u>.

(b) The owner or operator shall prepare a description of maintenance procedures for management of wastewaters generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdowns (i.e., routine maintenance). The descriptions shall:

(1) Specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities.

(2) Specify the procedures that will be followed to properly manage the wastewater and control organic HAP emissions to the atmosphere; and

(3) Specify the procedures to be followed when clearing materials from process equipment.

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(c) The owner or operator shall modify and update the information required by <u>paragraph (b)</u> of this section as needed following each maintenance procedure based on the actions taken and the wastewaters generated in the preceding maintenance procedure.

(d) The owner or operator shall incorporate the procedures described in <u>paragraphs (b)</u> and (c) of this section as part of the startup, shutdown, and malfunction plan required under  $\frac{63.6(e)(3)}{2}$ . For each source as defined in  $\frac{63.101}{2}$ , on and after July 15, 2027, this paragraph no longer applies.

(e) The owner or operator shall maintain a record of the information required by <u>paragraphs (b)</u> and (c) of this section as part of the start-up, shutdown, and malfunction plan required under  $\S 63.6(e)(3)$ . For each source as defined in  $\S 63.101$ , on and after July 15, 2027, the phrase "as part of the start-up, shutdown, and malfunction plan required under  $\S 63.6(e)(3)$ " in this paragraph no longer applies.

[<u>59 FR 19454</u>, Apr. 22, 1994, as amended at <u>60 FR 63626</u>, Dec. 12, 1995; <u>71 FR 20456</u>, Apr. 20, 2006; <u>89 FR 43169</u>, May 16, 2024]

# § 63.106 Implementation and enforcement.

(a) This subpart can be implemented and enforced by the U.S. EPA, or a delegated authority such as the applicable State, local, or Tribal agency. If the U.S. EPA Administrator has delegated authority to a State, local, or Tribal agency, then that agency, in addition to the U.S. EPA, has the authority to implement and enforce this subpart. Contact the applicable U.S. EPA Regional Office to find out if implementation and enforcement of this subpart is delegated to a State, local, or Tribal agency.

(b) In delegating implementation and enforcement authority of this subpart to a State, local, or Tribal agency under <u>subpart E</u> <u>of this part</u>, the authorities contained in <u>paragraph (c)</u> of this section are retained by the Administrator of U.S. EPA and cannot be transferred to the State, local, or Tribal agency.

(c) The authorities that cannot be delegated to State, local, or Tribal agencies are as specified in <u>paragraphs</u> (c)(1) through (4) of this section.

(1) Approval of alternatives to requirements in  $\frac{8863.100}{63.102}$ , and  $\frac{63.104}{63.104}$ . Where these standards reference another subpart, the cited provisions will be delegated according to the delegation provisions of the referenced subpart.

(2) Approval of major alternatives to test methods under  $\S 63.7(e)(2)(ii)$  and (f), as defined in  $\S 63.90$ , and as required in this subpart.

(3) Approval of major alternatives to monitoring under  $\frac{63.8(f)}{1000}$ , as defined in  $\frac{63.90}{1000}$ , and as required in this subpart.

(4) Approval of major alternatives to recordkeeping and reporting under  $\frac{63.10(f)}{10}$ , as defined in  $\frac{63.90}{10}$ , and as required in this subpart.

# [<u>68 FR 37344</u>, June 23, 2003]

# § 63.107 Identification of process vents subject to this subpart.

(a) The owner or operator shall use the criteria specified in this  $\frac{63.107}{100}$  to determine whether there are any process vents associated with an air oxidation reactor, distillation unit, or reactor that is in a source subject to this subpart. A process vent is the point of discharge to the atmosphere (or the point of entry into a control device, if any) of a gas stream if the gas stream has the characteristics specified in <u>paragraphs (b)</u> through (h) of this section, or meets the criteria specified in <u>paragraph (i)</u> of this section.

(b) Some, or all, of the gas stream originates as a continuous flow from an air oxidation reactor, distillation unit, or reactor during operation of the chemical manufacturing process unit.

(c) The discharge to the atmosphere (with or without passing through a control device) meets at least one of the conditions specified in paragraphs (c)(1) through (3) of this section.

(1) Is directly from an air oxidation reactor, distillation unit, or reactor; or

(2) Is from an air oxidation reactor, distillation unit, or reactor after passing solely (i.e., without passing through any other unit operation for a process purpose) through one or more recovery devices within the chemical manufacturing process unit; or

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(3) Is from a device recovering only mechanical energy from a gas stream that comes either directly from an air oxidation reactor, distillation unit, or reactor, or from an air oxidation reactor, distillation unit, or reactor after passing solely (i.e., without passing through any other unit operation for a process purpose) through one or more recovery devices within the chemical manufacturing process unit.

(d) The gas stream contains greater than 0.005 weight percent total organic HAP at the point of discharge to the atmosphere (or at the point of entry into a control device, if any).

(e) The air oxidation reactor, distillation unit, or reactor is part of a chemical manufacturing process unit that meets the criteria of  $\frac{63.100(b)}{2}$ .

(f) The gas stream is in the gas phase from the point of origin at the air oxidation reactor, distillation unit, or reactor to the point of discharge to the atmosphere (or to the point of entry into a control device, if any).

(g) The gas stream is discharged to the atmosphere either on-site, off-site, or both.

(h) The gas stream is not any of the items identified in <u>paragraphs (h)(1)</u> through (9) of this section.

(1) A relief valve discharge.

(2) A leak from equipment subject to subpart H of this part.

(3) A gas stream going to a fuel gas system as defined in  $\S$  63.101.

(4) A gas stream exiting a control device used to comply with  $\S$  63.113.

(5) A gas stream transferred to other processes (on-site or off-site) for reaction or other use in another process (i.e., for chemical value as a product, isolated intermediate, byproduct, or coproduct, or for heat value).

(6) A gas stream transferred for fuel value (i.e., net positive heating value), use, reuse, or for sale for fuel value, use, or reuse.

(7) A storage vessel vent or transfer operation vent subject to  $\frac{63.119}{5.000}$  or  $\frac{63.126}{5.0000}$ .

(8) A vent from a waste management unit subject to  $\frac{8863.132}{5}$  through  $\frac{63.137}{5}$ .

(9) A gas stream exiting an analyzer.

(i) Except as specified in paragraph (j) of this section, the gas stream would meet the characteristics specified in paragraphs (b) through (g) of this section, but, for purposes of avoiding applicability, has been deliberately interrupted, temporarily liquefied, routed through any item of equipment for no process purpose, or disposed of in a flare that does not meet the criteria in  $\frac{63.11(b)}{20}$ , or an incinerator that does not reduce emissions of organic HAP by 98 percent or to a concentration of 20 parts per million by volume, whichever is less stringent.

(j) For each source as defined in  $\S$  <u>63.101</u>, beginning no later than the compliance dates specified in  $\S$  <u>63.100(k)(10)</u>, the phrase "disposed of in a flare that does not meet the criteria in  $\S$  <u>63.11(b)</u>" in <u>paragraph (i)</u> of this section is replaced with "disposed of in a flare that does not meet the criteria in  $\S$  <u>63.108</u>".

[66 FR 6928, Jan. 22, 2001, as amended at 89 FR 43169, May 16, 2024]

# § 63.108 Flare requirements.

(a) For any flare that is used to reduce organic HAP emissions from a chemical manufacturing process unit, the owner or operator may elect to comply with the requirements in this section in lieu of the requirements of § 63.11(b) and the requirements referenced therein. The owner or operator may also elect to comply with the requirements in this section pursuant to the overlap provisions provided in § 63.110(j). However, for each source as defined in § 63.101 and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(10), the provisions specified in paragraphs (a)(1) through (22) of this section no longer apply. Instead, if an owner or operator reduces organic HAP emissions from a chemical manufacturing process unit by venting emissions through a closed-vent system to a steam-assisted, air-assisted, non-assisted, or pressure-assisted multi-point flare, then the owner or operator must meet the applicable requirements for flares as specified in § 63.670 and 63.671, including the provisions in tables 12 and 13 to subpart CC of this part, except as specified in paragraphs (b) through (o) of this section. This requirement also applies to any flare using fuel gas from a fuel gas system, of which 50 percent or more of the fuel gas is derived from a chemical manufacturing process unit, as determined on an annual average basis. For purposes of compliance with this paragraph, the following terms are

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defined in <u>§ 63.641</u>: Assist air, assist steam, center steam, combustion zone, combustion zone gas, flare, flare purge gas, flare supplemental gas, flare sweep gas, flare vent gas, lower steam, net heating value, perimeter assist air, pilot gas, premix assist air, total steam, and upper steam.

- (1) Section 63.107(i) related to criteria in  $\S 63.11(b)$ ;
- (2) Section 63.113(a)(1);
- (3) Section 63.114(a)(2);
- (4) Section 63.116(a)(1) through (3);
- (5) Section 63.117(a)(5)(i) through (iii);
- (6) Section 63.118(f)(5);
- (7) The last sentence in  $\S 63.119(e)(1)$  related to flares;
- (8) Section 63.120(e)(1) through (6);
- (9) Section 63.122(c)(2) and (g)(3);
- (10) Section 63.126(b)(2)(i);
- (11) Section 63.127(a)(2);
- (12) Section 63.128(b)(1) through (3);
- (13) Section 63.129(a)(5)(i) through (iii);
- (14) Section 63.130(a)(2)(i), (c), and (d)(5);
- (15) Section 63.139(c)(3) and (d)(3);
- (16) Section 63.145(j)(1) through (3);
- (17) Section 63.146(b)(7)(i)(A) through (C);
- (18) V63.147(d)(1);
- (19) Section 63.172(d);
- (20) Section 63.180(e)(1) through (3);
- (21) Section 63.181(g)(1)(iii); and

(22) The phrase "including periods when a flare pilot light system does not have a flame" in  $\frac{63.181(g)(2)(i)}{10}$  of subpart H of this part.

(b) When determining compliance with the pilot flame requirements specified in  $\S$  <u>63.670(b)</u> and <u>(g)</u>, substitute "pilot flame or flare flame" for each occurrence of "pilot flame."

(c) When determining compliance with the flare tip velocity and combustion zone operating limits specified in  $\S$  <u>63.670(d)</u> and <u>(e)</u>, the requirement effectively applies starting with the 15-minute block that includes a full 15 minutes of the flaring event. The owner or operator is required to demonstrate compliance with the velocity and NHVcz requirements starting with the block that contains the fifteenth minute of a flaring event. The owner or operator is not required to demonstrate compliance for the previous 15-minute block in which the event started and contained only a fraction of flow.

(d) Instead of complying with  $\S$  63.670(o)(2)(i), owners and operators must develop and implement the flare management plan no later than the compliance dates specified in  $\S$  63.100(k)(10).

(e) Instead of complying with  $\frac{63.670(0)(2)(iii)}{63.670(0)(2)(iii)}$ , if required to develop a flare management plan and submit it to the Administrator, then owners and operators must also submit all versions of the plan in portable document format (PDF) to the EPA following the procedure specified in  $\frac{63.9(k)}{63.9(k)}$ , except any medium submitted through mail must be sent to the attention of the Hazardous Organic Chemical Manufacturing Sector Lead.

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(f) Section 63.670(o)(3)(ii) and all references to it do not apply. Instead, the owner or operator must comply with the maximum flare tip velocity operating limit at all times.

(g) Substitute "chemical manufacturing process unit" for each occurrence of "petroleum refinery."

(h) Each occurrence of "refinery" does not apply.

(i) If a pressure-assisted multi-point flare is used as a control device, then owners and operators must meet the following conditions:

(1) The owner or operator is not required to comply with the flare tip velocity requirements in  $\S$  63.670(d) and (k);

(2) The NHVcz for pressure-assisted mulit-point flares is 800 Btu/scf;

(3) Owners and operators must determine the 15-minute block average NHVvg using only the direct calculation method specified in <u>§ 63.670(1)(5)(ii);</u>

(4) Instead of complying with § 63.670(b) and (g), if a pressure-assisted multi-point flare uses cross-lighting on a stage of burners rather than having an individual pilot flame on each burner, then owners and operators must operate each stage of the pressure-assisted multi-point flare with a flame present at all times when regulated material is routed to that stage of burners. Each stage of burners that cross-lights in the pressure-assisted multi-point flare must have at least two pilots with at least one continuously lit and capable of igniting all regulated material that is routed to that stage of burners. Each 15-minute block during which there is at least one minute where no pilot flame is present on a stage of burners when regulated material is routed to the flare is a violation of the standard. Violations in different 15-minute blocks from the same event are considered separate violations. The pilot flame(s) on each stage of burners that use cross-lighting must be continuously monitored by a thermocouple or any other equivalent device used to detect the presence of a flame;

(5) Unless the owner or operator chooses to conduct a cross-light performance demonstration as specified in this paragraph, owners and operators must ensure that if a stage of burners on the flare uses cross-lighting, that the distance between any two burners in series on that stage is no more than 6 feet when measured from the center of one burner to the next burner. A distance greater than 6 feet between any two burners in series may be used provided the owner or operator conducts a performance demonstration that confirms the pressure-assisted multi-point flare will cross-light a minimum of three burners and the spacing between the burners and location of the pilot flame must be representative of the projected installation. The compliance demonstration must be approved by the permitting authority and a copy of this approval must be maintained onsite. The compliance demonstration report must include: a protocol describing the test methodology used, associated test method QA/QC parameters, the waste gas composition and NHVcz of the gas tested, the velocity of the waste gas tested, the pressure-assisted multi-point flare burner tip pressure, the time, length, and duration of the test, records of whether a successful cross-light was observed over all of the burners and the length of time it took for the burners to cross-light, records of maintaining a stable flame after a successful cross-light and the duration for which this was observed, records of any smoking events during the cross-light, waste gas temperature, meteorological conditions (e.g., ambient temperature, barometric pressure, wind speed and direction, and relative humidity), and whether there were any observed flare flameouts; and

(6) Owners and operators must install and operate pressure monitor(s) on the main flare header, as well as a valve position indicator monitoring system for each staging valve to ensure that the flare operates within the proper range of conditions as specified by the manufacturer. The pressure monitor must meet the requirements in table 13 to subpart CC of this part.

(7) If a pressure-assisted multi-point flare is operating under the requirements of an approved alternative means of emission limitations, owners and operators must either continue to comply with the terms of the alternative means of emission limitations or comply with the provisions in paragraphs (i)(1) through (6) of this section.

(j) If an owner or operator chooses to determine compositional analysis for net heating value with a continuous process mass spectrometer, then the owner or operator must comply with the requirements specified in paragraphs (i)(1) through (7) of this section.

(1) Owners and operators must meet the requirements in  $\S$  63.671(e)(2). The owner or operator may augment the minimum list of calibration gas components found in (63.671(e))(2) with compounds found during a pre-survey or known to be in the gas through process knowledge.

(2) Calibration gas cylinders must be certified to an accuracy of 2 percent and traceable to National Institute of Standards and Technology (NIST) standards.

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(3) For unknown gas components that have similar analytical mass fragments to calibration compounds, the owner or operator may report the unknowns as an increase in the overlapped calibration gas compound. For unknown compounds that produce mass fragments that do not overlap calibration compounds, the owner or operator may use the response factor for the nearest molecular weight hydrocarbon in the calibration mix to quantify the unknown component's NHVvg.

(4) The owner or operator may use the response factor for n-pentane to quantify any unknown components detected with a higher molecular weight than n-pentane.

(5) Owners and operators must perform an initial calibration to identify mass fragment overlap and response factors for the target compounds.

(6) Owners and operators must meet applicable requirements in Performance Specification 9 in appendix B to <u>part 60 of this</u> <u>chapter</u> for continuous monitoring system acceptance including, but not limited to, performing an initial multi-point calibration check at three concentrations following the procedure in <u>section 10.1</u> and performing the periodic calibration requirements listed for gas chromatographs in table 13 to <u>subpart CC of this part</u>, for the process mass spectrometer. The owner or operator may use the alternative sampling line temperature allowed under Net Heating Value by Gas Chromatograph in table 13 to <u>subpart CC of this part</u>.

(7) The average instrument calibration error (CE) for each calibration compound at any calibration concentration must not differ by more than 10 percent from the certified cylinder gas value. The CE for each component in the calibration blend must be calculated using equation 1 to this paragraph.

Equation 1 to Paragraph (j)(7)

$$CE = \frac{C_m - C_a}{C_a} \times 100 \text{ (Eq. 1)}$$

Where:

C<sub>m</sub> = Average instrument response (ppm)

C<sub>a</sub> = Certified cylinder gas value (ppm)

(k) If an owner or operator use a gas chromatograph or mass spectrometer for compositional analysis for net heating value, then the owner or operator may choose to use the CE of  $NHV_{measured}$  versus the cylinder tag value NHV as the measure of agreement for daily calibration and quarterly audits in lieu of determining the compound-specific CE. The CE for NHV at any calibration level must not differ by more than 10 percent from the certified cylinder gas value. The CE for must be calculated using equation 2 to this paragraph.

Equation 2 to Paragraph (k)

$$CE = \frac{NHV_{measured} - NHV_a}{NHV_a} \times 100 \text{ (Eq. 2)}$$

Where:

NHV<sub>measured</sub> = Average instrument response (Btu/scf)

NHV<sub>a</sub> = Certified cylinder gas value (Btu/scf)

(1) Instead of complying with  $\frac{63.670(q)}{1}$ , owners and operators must comply with the reporting requirements specified in paragraphs (1)(1) and (2) of this section.

(1) The initial notification requirements specified in  $\S 63.152(b)(7)$ .

(2) The Periodic Report required by  $\S$  63.152(c) must include the items specified in paragraphs (l)(2)(i) through (vi) of this section.

(i) Records as specified in <u>paragraph (m)(1)</u> of this section for each 15-minute block during which there was at least one minute when regulated material is routed to a flare and no pilot flame or flare flame is present. Include the start and stop time and date of each 15-minute block.

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(ii) Visible emission records as specified in paragraph (m)(2)(iv) of this section for each period of 2 consecutive hours during which visible emissions exceeded a total of 5 minutes. Indicate the date and start and end times for each period.

(iii) The periods specified in <u>paragraph (m)(6)</u> of this section. Indicate the date and start and end times for each period, and the net heating value operating parameter(s) determined following the methods in  $\S 63.670(k)$  through (n) as applicable.

(iv) For flaring events meeting the criteria in  $\frac{63.670(0)(3)}{3}$  and <u>paragraph (f)</u> of this section:

(A) The start and stop time and date of the flaring event.

(B) The length of time in minutes for which emissions were visible from the flare during the event.

(C) For steam-assisted, air-assisted, and non-assisted flares, the start date, start time, and duration in minutes for periods of time that the flare tip velocity exceeds the maximum flare tip velocity determined using the methods in  $\S$  63.670(d)(2) and the maximum 15-minute block average flare tip velocity in ft/sec recorded during the event.

(D) Results of the root cause and corrective actions analysis completed during the reporting period, including the corrective actions implemented during the reporting period and, if applicable, the implementation schedule for planned corrective actions to be implemented subsequent to the reporting period.

(v) For pressure-assisted multi-point flares, the periods of time when the pressure monitor(s) on the main flare header show the burners operating outside the range of the manufacturer's specifications. Indicate the date and start and end times for each period.

(vi) For pressure-assisted multi-point flares, the periods of time when the staging valve position indicator monitoring system indicates a stage should not be in operation and is or when a stage should be in operation and is not. Indicate the date and start and end times for each period.

(m) Instead of complying with § 63.670(p), owners and operators must keep the flare monitoring records specified in paragraphs (m)(1) through (14) of this section.

(1) Retain records of the output of the monitoring device used to detect the presence of a pilot flame or flare flame as required in  $\frac{63.670(b)}{2}$  and the presence of a pilot flame as required in <u>paragraph (i)(4)</u> of this section for a minimum of 2 years. Retain records of each 15-minute block during which there was at least one minute that no pilot flame or flare flame is present when regulated material is routed to a flare for a minimum of 5 years. For a pressure-assisted multi-point flare that uses cross-lighting, retain records of each 15-minute block during which there was at least one minute that no pilot flame is present on each stage when regulated material is routed to a flare for a minimum of 5 years. The owner or operator may reduce the collected minute-by-minute data to a 15-minute block basis with an indication of whether there was at least one minute where no pilot flame or flare flame was present.

(2) Retain records of daily visible emissions observations as specified in <u>paragraphs (m)(2)(i)</u> through <u>(iv)</u> of this section, as applicable, for a minimum of 3 years.

(i) To determine when visible emissions observations are required, the record must identify all periods when regulated material is vented to the flare.

(ii) If visible emissions observations are performed using Method 22 in appendix A-7 to <u>part 60 of this chapter</u>, then the record must identify whether the visible emissions observation was performed, the results of each observation, total duration in minutes of observed visible emissions, and whether it was a 5-minute or 2-hour observation. Record the date and start time of each visible emissions observation.

(iii) If a video surveillance camera is used pursuant to  $\frac{63.670(h)(2)}{5.670(h)(2)}$ , then the record must include all video surveillance images recorded, with time and date stamps.

(iv) For each 2-hour period for which visible emissions are observed for more than 5 minutes in 2 consecutive hours, then the record must include the date and start and end time of the 2-hour period and an estimate of the cumulative number of minutes in the 2-hour period for which emissions were visible.

(3) The 15-minute block average cumulative flows for flare vent gas and, if applicable, total steam, perimeter assist air, and premix assist air specified to be monitored under  $\S$  63.670(i), along with the date and time interval for the 15-minute block. If multiple monitoring locations are used to determine cumulative vent gas flow, total steam, perimeter assist air, and premix assist air, then retain records of the 15-minute block average flows for each monitoring location for a minimum of 2 years
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and retain the 15-minute block average cumulative flows that are used in subsequent calculations for a minimum of 5 years. If pressure and temperature monitoring is used, then retain records of the 15-minute block average temperature, pressure, and molecular weight of the flare vent gas or assist gas stream for each measurement location used to determine the 15-minute block average cumulative flows for a minimum of 2 years, and retain the 15-minute block average cumulative flows that are used in subsequent calculations for a minimum of 5 years.

(4) The flare vent gas compositions specified to be monitored under  $\S 63.670(j)$ . Retain records of individual component concentrations from each compositional analysis for a minimum of 2 years. If an NHVvg analyzer is used, retain records of the 15-minute block average values for a minimum of 5 years.

(5) Each 15-minute block average operating parameter calculated following the methods specified in  $\S$  <u>63.670(k)</u> through (<u>n</u>) as applicable.

(6) All periods during which operating values are outside of the applicable operating limits specified in  $\S$  <u>63.670(d)</u> through (f) and paragraph (i) of this section when regulated material is being routed to the flare.

(7) All periods during which the owner or operator does not perform flare monitoring according to the procedures in  $\S$  <u>63.670(g)</u> through (j).

(8) For pressure-assisted multi-point flares, if a stage of burners on the flare uses cross-lighting, then a record of any changes made to the distance between burners.

(9) For pressure-assisted multi-point flares, all periods when the pressure monitor(s) on the main flare header show burners are operating outside the range of the manufacturer's specifications. Indicate the date and time for each period, the pressure measurement, the stage(s) and number of burners affected, and the range of manufacturer's specifications.

(10) For pressure-assisted multi-point flares, all periods when the staging valve position indicator monitoring system indicates a stage of the pressure-assisted multi-point flare should not be in operation and when a stage of the pressure-assisted multi-point flare should be in operation and is not. Indicate the date and time for each period, whether the stage was supposed to be open, but was closed or vice versa, and the stage(s) and number of burners affected.

(11) Records of periods when there is flow of vent gas to the flare, but when there is no flow of regulated material to the flare, including the start and stop time and dates of periods of no regulated material flow.

(12) Records when the flow of vent gas exceeds the smokeless capacity of the flare, including start and stop time and dates of the flaring event.

(13) Records of the root cause analysis and corrective action analysis conducted as required in  $\frac{\$ 63.670(0)(3)}{\$ 63.670(0)(3)}$  and paragraph (f) of this section, including an identification of the affected flare, the date and duration of the event, a statement noting whether the event resulted from the same root cause(s) identified in a previous analysis and either a description of the recommended corrective action(s) or an explanation of why corrective action is not necessary under  $\frac{\$ 63.670(0)(3)}{\$ 63.670(0)(5)(i)}$ .

(14) For any corrective action analysis for which implementation of corrective actions are required in  $\frac{63.670(0)(5)}{5}$ , a description of the corrective action(s) completed within the first 45 days following the discharge and, for action(s) not already completed, a schedule for implementation, including proposed commencement and completion dates.

(n) The owner or operator may elect to comply with the alternative means of emissions limitation requirements specified in § 63.670(r) in lieu of the requirements in § 63.670(d) through (f), as applicable. However, instead of complying with § 63.670(r)(3)(iii), owners and operators must also submit the alternative means of emissions limitation request to the following address: U.S. Environmental Protection Agency, Office of Air Quality Planning and Standards, Sector Policies and Programs Division, U.S. EPA Mailroom (C404-02), Attention: Hazardous Organic Chemical Manufacturing Sector Lead, 4930 Old Page Rd., Durham, NC 27703.

(o) The referenced provisions specified in <u>paragraphs (o)(1)</u> through (4) of this section do not apply when demonstrating compliance with this section.

- (1) Section 63.670(o)(4)(iv) of subpart CC of this part.
- (2) The last sentence of  $\S 63.670(o)(6)$ .
- (3) The phrase "that were not caused by a *force majeure* event" in § 63.670(0)(7)(ii).

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(4) The phrase "that were not caused by a *force majeure* event" in  $\S 63.670(o)(7)(iv)$ .

# [<u>89 FR 43169</u>, May 16, 2024]

# § 63.109 Procedures for determining whether process vents, storage vessels, equipment, wastewater, and heat exchange systems are in ethylene oxide service.

This section applies beginning no later than the compliance dates specified in  $\S 63.100(k)(11)$ . To determine if process vents, storage vessels, equipment leaks, wastewater, and heat exchange systems are in ethylene oxide service, as defined in  $\S 63.101$ , owners and operators must comply with the requirements in paragraphs (a) through (c) of this section, as applicable.

(a) Except as specified in <u>paragraph (a)(7)</u> of this section, for each Group 1 and Group 2 process vent stream, owners and operators must measure the flow rate and concentration of ethylene oxide of each process vent as specified in <u>paragraphs</u> (a)(1) through (6) of this section.

(1) Measurements must be made prior to any dilution of the vent streams.

(2) Measurements may be made on the combined vent streams at a chemical manufacturing process unit or for each separate vent stream.

(3) The sampling site shall be after the last recovery device (if any recovery devices are present) but prior to the inlet of any control device that is present and prior to release to the atmosphere. Method 1 or 1A of appendix A-1 to <u>part 60 of this</u> <u>chapter</u>, as appropriate, must be used for the selection of the sampling sites. For vents smaller than 0.10 meter in diameter, sample at one point at the center of the duct.

(4) The gas volumetric flow rate must be determined using Method 2, 2A, 2C, 2D, 2F, or 2G of appendices A-1 and A-2 to <u>part 60 of this chapter</u> (respectively), as appropriate.

(5) Except as specified in <u>paragraph (a)(6)</u> of this section, the concentration of ethylene oxide must be determined using Method 18 of appendix A-6 to <u>part 60 of this chapter</u>, or Method 320 of appendix A to this part.

(6) You may elect to use ASTM D6348-12 (Reapproved 2020) (incorporated by reference, § 63.14) in lieu of Method 320 of appendix A to this part as specified in paragraph (a)(5) of this section. To comply with this paragraph, annexes Al through A8 to ASTM D6348-12 (Reapproved 2020) are mandatory; the percent (%) R must be determined for each target analyte using Equation A5.5 of ASTM D6348-12 (Reapproved 2020) Annex A5 (Analyte Spiking Technique); and in order for the test data to be acceptable for a compound, the %R must be 70%  $\ge$  R  $\le$  130%. If the %R value does not meet this criterion for a target compound, then the test data is not acceptable for that compound and the test must be repeated for that analyte (*i.e.*, the sampling and/or analytical procedure should be adjusted before a retest). The %R value for each compound must be reported in the test report, and all field measurements must be corrected with the calculated %R value for that compound by using the following equation:

Equation 1 to Paragraph (a)(6)

Reported Results = (Measured Concentration in the Stack  $\times$  100)/%R.

(7) The requirements specified in <u>paragraphs (a)(1)</u> through (6) of this section for an initial measurement or initial performance test do not apply if the conditions specified in <u>paragraphs (a)(7)(i)</u> through (iv) of this section are met for a previously conducted measurement or performance test.

(i) No changes have been made to the process since the time of the measurement or performance test;

(ii) The operating conditions and test methods used during measurement or performance test conform to the ethylene oxide related requirements of this subpart;

(iii) The control device and process parameter values established during the previously conducted measurement or performance test are used to demonstrate continuous compliance with the ethylene oxide related requirements of this subpart; and

(iv) The previously conducted measurement or performance test was completed within the last 60 months.

(b) For storage vessels, owners and operators must determine the concentration of ethylene oxide of the fluid stored in the storage vessels by complying with the requirements in paragraph (b)(1) or (2) of this section.

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(1) The owner or operator must measure concentration of ethylene oxide of the fluid stored in the storage vessel using Method 624.1 of appendix A to 40 CFR part 136, or preparation by Method SW-846-5031 or SW-846-5030B and analysis by Method SW-846-8260D (incorporated by reference, see  $\S$  63.14). The owner or operator may not use a preservative in the collected sample; the owner or operator must store the sample with minimal headspace as cold as possible and at least below 4 degrees C; and the owner or operator must analyze the sample as soon as possible, but in no case longer than 7 days from the time the sample was collected. If owners and operators collect a sample from a pressure vessel, then the owner or operator must maintain the sample under pressure both during and following sampling.

(2) Unless specified by the Administrator, the owner or operator may calculate the concentration of ethylene oxide of the fluid stored in the storage vessels if information specific to the fluid stored is available. Information specific to the fluid stored includes concentration data from safety data sheets.

(c) For equipment leaks, owners and operators must comply with the requirements in <u>paragraphs (c)(1)</u> through (4) of this section.

(1) Each piece of equipment within a chemical manufacturing process unit that can reasonably be expected to contain equipment in ethylene oxide service is presumed to be in ethylene oxide service unless the owner or operator demonstrates that the piece of equipment is not in ethylene oxide service. For a piece of equipment to be considered not in ethylene oxide service, it must be determined that the percent ethylene oxide content of the process fluid that is contained in or contacts equipment can be reasonably expected to not exceed 0.1 percent by weight on an annual average basis. For purposes of determining the percent ethylene oxide content of the process fluid, owners and operators must use Method 18 of appendix A-6 to part 60 of this chapter, for gaseous process fluid, and Method 624.1 of appendix A to part 136 of this chapter, or preparation by Method SW-846-5031 and analysis by Method SW-846-8260D (both incorporated by reference, see  $\frac{63.14}{5030B}$  (incorporated by reference, see  $\frac{63.14}{5030B}$ ), as long as: the owner or operator does not use a preservative in the collected sample; the owner or operator stores the sample with minimal headspace as cold as possible and at least below 4 degrees C; and the owner or operator analyzes the sample as soon as possible, but in no case longer than 7 days from the time the sample was collected.

(2) Unless specified by the Administrator, owners and operators may use good engineering judgment rather than the procedures specified in paragraph (c)(1) of this section to determine that the percent ethylene oxide content of the process fluid that is contained in or contacts equipment does not exceed 0.1 percent by weight.

(3) Owners and operators may revise a determination for whether a piece of equipment is in ethylene oxide service by following the procedures in <u>paragraph (c)(1)</u> of this section, or by documenting that a change in the process or raw materials no longer causes the equipment to be in ethylene oxide service.

(4) Samples used in determining the ethylene oxide content must be representative of the process fluid that is contained in or contacts the equipment.

(d) For wastewater, owners and operators must determine the concentration of ethylene oxide of each wastewater stream using Method 624.1 of appendix A to part 136 of this chapter, or preparation by either Method SW-846-5031 or SW-846-5030B and analysis by Method SW-846-8260D (incorporated by reference, see § 63.14). The owner or operator may not use a preservative in the collected sample; the owner or operator must store the sample with minimal headspace as cold as possible and at least below 4 degrees C; and the owner or operator must analyze the sample as soon as possible, but in no case longer than 7 days from the time the sample was collected.

(e) For heat exchange systems, owners and operators must comply with the requirements in <u>paragraph (e)(1)</u> or (2) of this section.

(1) Determine the concentration of ethylene oxide of the process fluid cooled by the heat exchange system using Method 624.1 of appendix A to part 136 of this chapter, or preparation by either Method SW-846-5031 or SW-846-5030B and analysis by Method SW-846-8260D (incorporated by reference, see § 63.14). The owner or operator may not use a preservative in the collected sample; the owner or operator must store the sample with minimal headspace as cold as possible and at least below 4 degrees C; and the owner or operator must analyze the sample as soon as possible, but in no case longer than 7 days from the time the sample was collected.

## National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

(2) Unless specified by the Administrator, owners and operators may use good engineering judgment rather than the procedures specified in paragraph (e)(1) of this section to determine that the percent ethylene oxide content of the process fluid cooled by the heat exchange system does not exceed 0.1 percent by weight.

## [89 FR 43173, May 16, 2024]

## Table 1 to Subpart F of Part 63—Synthetic Organic Chemical Manufacturing Industry Chemicals

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Acenaphthene	83329	V
Acetal	105577	V
Acetaldehyde	75070	II
Acetamide	60355	II
Acetanilide	103844	II
Acetic acid	64197	II
Acetic anhydride	108247	II
Acetoacetanilide	102012	III
Acetone	67641	Ι
Acetone cyanohydrin	75865	V
Acetonitrile	75058	Ι
Acetophenone	98862	Ι
Acrolein	107028	IV
Acrylamide	79061	Ι
Acrylic acid	79107	IV
Acrylonitrile	107131	Ι
Adiponitrile	111693	Ι
Alizarin	72480	V
Alkyl anthraquinones	008	V
Allyl alcohol	107186	Ι
Allyl chloride	107051	IV
Allyl cyanide	109751	IV
Aminophenol sulfonic acid	0010	V
Aminophenol (p-)	123308	Ι
Aniline	62533	Ι
Aniline hydrochloride	142041	III
Anisidine (o-)	90040	II
Anthracene	120127	V
Anthraquinone	84651	III
Azobenzene	103333	Ι
Benzaldehyde	100527	III
Benzene	71432	Ι
Benzenedisulfonic acid	98486	Ι
Benzenesulfonic acid	98113	Ι
Benzil	134816	III

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Benzilic acid	76937	III
Benzoic acid	65850	III
Benzoin	119539	III
Benzonitrile	100470	III
Benzophenone	119619	Ι
Benzotrichloride	98077	III
Benzoyl chloride	98884	III
Benzyl acetate	140114	III
Benzyl alcohol	100516	III
Benzyl benzoate	120514	III
Benzyl chloride	100447	III
Benzyl dichloride	98873	III
Biphenyl	92524	Ι
Bisphenol A	80057	III
Bis(Chloromethyl) Ether	542881	Ι
Bromobenzene	108861	Ι
Bromoform	75252	V
Bromonaphthalene	27497514	IV
Butadiene (1,3-)	106990	II
Butanediol (1,4-)	110634	Ι
Butyl acrylate (n-)	141322	V
Butylene glycol (1,3-)	107880	II
Butyrolactone	96480	Ι
Caprolactam	105602	II
Carbaryl	63252	V
Carbazole	86748	V
Carbon disulfide	75150	IV
Carbon tetrabromide	558134	II
Carbon tetrachloride	56235	Ι
Carbon tetrafluoride	75730	II
Chloral	75876	II
Chloroacetic acid	79118	II
Chloroacetophenone (2-)	532274	Ι
Chloroaniline (p-)	106478	II
Chlorobenzene	108907	Ι
2-Chloro-1,3-butadiene (Chloroprene)	126998	II
Chlorodifluoroethane	25497294	V
Chlorodifluoromethane	75456	Ι
Chloroform	67663	Ι
Chloronaphthalene	25586430	IV

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Chloronitrobenzene	121733	Ι
(m-).		
Chloronitrobenzene	88733	Ι
(0-).		
Chloronitrobenzene	100005	Ι
(p-).		
Chlorophenol (m-)	108430	II
Chlorophenol (o-)	95578	II
Chlorophenol (p-)	106489	II
Chlorotoluene (m-)	108418	III
Chlorotoluene (o-)	95498	III
Chlorotoluene (p-)	106434	III
Chlorotrifluoromethane	75729	II
Chrysene	218019	V
Cresol and cresylic acid (m-)	108394	III
Cresol and cresylic acid (o-)	95487	III
Cresol and cresylic acid (p-)	106445	III
Cresols and cresylic acids (mixed)	1319773	III
Cumene	98828	Ι
Cumene hydroperoxide	80159	Ι
Cyanoacetic acid	372098	II
Cyclohexane	110827	Ι
Cyclohexanol	108930	Ι
Cyclohexanone	108941	Ι
Cyclohexylamine	108918	III
Cyclooctadienes	29965977	II
Decahydronaphthalene	91178	IV
Diacetoxy-2-Butene (1,4-)	0012	V
Diaminophenol hydrochloride	137097	V
Dibromomethane	74953	V
Dichloroaniline (mixed isomers)	27134276	Ι
Dichlorobenzene (p-)	106467	Ι
Dichlorobenzene (m-)	541731	Ι
Dichlorobenzene (o-)	95501	Ι
Dichlorobenzidine	91941	Ι
(3,3'-).		
Dichlorodifluoromethane	75718	Ι
Dichloroethane (1,2-) (Ethylenedichloride) (EDC)	107062	Ι
Dichloroethyl ether (bis(2-chloroethyl)ether)	111444	Ι
Dichloroethylene (1,2-)	540590	II

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Dichlorophenol (2,4-)	120832	III
Dichloropropene (1,3-)	542756	II
Dichlorotetrafluoro-	1320372	V
ethane.		
Dichloro-1-butene (3,4-)	760236	II
Dichloro-2-butene (1,4-)	764410	V
Diethanolamine (2,2'-Iminodiethanol)	111422	Ι
Diethyl sulfate	64675	II
Diethylamine	109897	IV
Diethylaniline (2,6-)	579668	V
Diethylene glycol	111466	Ι
Diethylene glycol dibutyl ether	112732	Ι
Diethylene glycol diethyl ether	112367	I
Diethylene glycol dimethyl ether	111966	Ι
Diethylene glycol monobutyl ether acetate	124174	Ι
Diethylene glycol monobutyl ether	112345	Ι
Diethylene glycol monoethyl ether acetate	112152	Ι
Diethylene glycol monoethyl ether	111900	Ι
Diethylene glycol monohexyl ether	112594	V
Diethylene glycol monomethyl ether acetate	629389	V
Diethylene glycol monomethyl ether	111773	Ι
Dihydroxybenzoic acid (Resorcylic acid)	27138574	V
Dimethylbenzidine	119937	II
(3,3'-).		
Dimethyl ether	115106	IV
Dimethylformamide (N,N-)	68122	II
Dimethylhydrazine	57147	II
(1,1-).		
Dimethyl sulfate	77781	Ι
Dimethyl terephthalate	120616	II
Dimethylamine	124403	IV
Dimethylaminoethanol (2-)	108010	Ι
Dimethylaniline (N,N')	121697	III
Dinitrobenzenes (NOS) <sup>c</sup>	25154545	Ι
Dinitrophenol (2,4-)	51285	III
Dinitrotoluene (2,4-)	121142	III
Dioxane (1,4-) (1,4-Diethyleneoxide)	1239	11I
Dioxolane (1,3-)	646060	Ι
Diphenyl methane	101815	Ι
Diphenyl oxide	101848	Ι

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Diphenyl thiourea	102089	III
Diphenylamine	122394	III
Dipropylene glycol	110985	Ι
Di-o-tolyguanidine	97392	III
Dodecanedioic acid	693232	Ι
Dodecyl benzene (branched)	123013	V
Dodecyl phenol (branched)	121158585	V
Dodecylaniline	28675174	V
Dodecylbenzene (n-)	121013	Ι
Dodecylphenol	27193868	III
Epichlorohydrin (1-chloro-2,3-epoxypropane)	106898	Ι
Ethanolamine	141435	Ι
Ethyl acrylate	140885	II
Ethylbenzene	100414	Ι
Ethyl chloride (Chloroethane)	75003	IV
Ethyl chloroacetate	105395	II
Ethylamine	75047	V
Ethylaniline (N-)	103695	III
Ethylaniline (o-)	578541	III
Ethylcellulose	9004573	V
Ethylcyanoacetate	105566	V
Ethylene carbonate	96491	Ι
Ethylene dibromide (Dibromoethane)	106934	Ι
Ethylene glycol	107211	Ι
Ethylene glycol diacetate	111557	Ι
Ethylene glycol dibutyl ether	112481	V
Ethylene glycol diethyl ether	629141	Ι
(1,2-diethoxyethane).		
Ethylene glycol	110714	Ι
dimethyl ether		
Ethylene glycol monoacetate	542596	V
Ethylene glycol monobutyl ether	112072	Ι
acetate.		
Ethylene glycol monobutyl ether	111762	Ι
Ethylene glycol monoethyl ether	111159	Ι
acetate.		
Ethylene glycol monoethyl ether	110805	Ι
Ethylene glycol monohexyl ether	112254	V
Ethylene glycol monomethyl ether acetate	110496	Ι
Ethylene glycol monomethyl ether	109864	I

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Ethylene glycol monooctyl ether	002	V
Ethylene glycol monophenyl ether	122996	Ι
Ethylene glycol monopropyl ether	2807309	Ι
Ethylene oxide	75218	Ι
Ethylenediamine	107153	II
Ethylenediamine tetraacetic acid	60004	V
Ethylenimine (Aziridine)	151564	II
Ethylhexyl acrylate (2-isomer)	103117	II
Fluoranthene	206440	V
Formaldehyde	50000	Ι
Formamide	75127	II
Formic acid	64186	II
Fumaric acid	110178	Ι
Glutaraldehyde	111308	IV
Glyceraldehyde	367475	V
Glycerol	56815	II
Glycine	56406	II
Glyoxal	107222	II
Hexachlorobenzene	118741	II
Hexachlorobutadiene	87683	II
Hexachloroethane	67721	II
Hexadiene (1,4-)	592450	II
Hexamethylene-	100970	Ι
tetramine.		
Hexane	110543	V
Hexanetriol (1,2,6-)	106694	IV
Hydroquinone	123319	Ι
Hydroxyadipaldehyde	141311	V
Isobutyl acrylate	106638	V
Isobutylene	115117	V
Isophorone	78591	IV
Isophorone nitrile	0017	V
Isophthalic acid	121915	III
Isopropylphenol	25168063	III
Linear alkylbenzene	d	Ι
Maleic anhydride	108316	Ι
Maleic hydrazide	123331	Ι
Malic acid	6915157	Ι
Metanilic acid	121471	Ι
Methacrylic acid	79414	V

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Methanol	67561	IV
Methionine	63683	Ι
Methyl acetate	79209	IV
Methyl acrylate	96333	V
Methyl bromide (Bromomethane)	74839	IV
Methyl chloride (Chloromethane)	74873	IV
Methyl ethyl ketone (2-butanone)	78933	V
Methyl formate	107313	II
Methyl hydrazine	60344	IV
Methyl isobutyl carbinol	108112	IV
Methyl isobutyl ketone (Hexone)	108101	IV
Methyl isocyanate	624839	IV
Methyl mercaptan	74931	IV
Methyl methacrylate	80626	IV
Methyl phenyl carbinol	98851	II
Methyl tert-butyl ether	1634044	V
Methylamine	74895	IV
Methylaniline (N-)	100618	III
Methylcyclohexane	108872	III
Methylcyclohexanol	25639423	V
Methylcyclohexanone	1331222	III
Methylene chloride (Dichloromethane)	75092	Ι
Methylene dianiline (4,4'-isomer)	101779	Ι
Methylene diphenyl diisocyanate (4,4'-) (MDI)	101688	III
Methylionones (a-)	79696	V
Methylpentynol	77758	V
Methylstyrene (a-)	98839	Ι
Naphthalene	91203	IV
Naphthalene sulfonic acid (a-)	85472	IV
Naphthalene sulfonic acid (b-)	120183	IV
Naphthol (a-)	90153	IV
Naphthol (b-)	135193	IV
Naphtholsulfonic acid (1-)	567180	V
Naphthylamine sulfonic acid (1,4-)	84866	V
Naphthylamine sulfonic acid (2,1-)	81163	V
Naphthylamine (1-)	134327	V
Naphthylamine (2-)	91598	V
Nitroaniline (m-)	99092	II
Nitroaniline (o-)	88744	I
Nitroanisole (o-)	91236	III

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Nitroanisole (p-)	100174	III
Nitrobenzene	98953	Ι
Nitronaphthalene (1-)	86577	IV
Nitrophenol (p-)	100027	III
Nitrophenol (o-)	88755	III
Nitropropane (2-)	79469	II
Nitrotoluene (all isomers)	1321126	III
Nitrotoluene (o-)	88722	III
Nitrotoluene (m-)	99081	III
Nitrotoluene (p-)	99990	III
Nitroxylene	25168041	V
Nonylbenzene (branched)	1081772	V
Nonylphenol	25154523	V
Octene-1	111660	Ι
Octylphenol	27193288	III
Paraformaldehyde	30525894	Ι
Paraldehyde	123637	II
Pentachlorophenol	87865	III
Pentaerythritol	115775	Ι
Peracetic acid	79210	II
Perchloromethyl mercaptan	594423	IV
Phenanthrene	85018	V
Phenetidine (p-)	156434	III
Phenol	108952	III
Phenolphthalein	77098	III
Phenolsulfonic acids (all isomers)	1333397	III
Phenyl anthranilic acid (all isomers)	91407	III
Phenylenediamine (p-)	106503	Ι
Phloroglucinol	108736	III
Phosgene	75445	IV
Phthalic acid	88993	III
Phthalic anhydride	85449	III
Phthalimide	85416	III
Phthalonitrile	91156	III
Picoline (b-)	108996	II
Piperazine	110850	Ι
Propiolactone (beta-)	57578	Ι
Propionaldehyde	123386	IV
Propionic acid	79094	Ι
Propylene carbonate	108327	V

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Propylene dichloride (1,2-dichloropropane)	78875	IV
Propylene glycol	57556	Ι
Propylene glycol monomethyl ether	107982	Ι
Propylene oxide	75569	Ι
Pyrene	129000	V
Pyridine	110861	II
p-tert-Butyl toluene	98511	III
Quinone	106514	III
Resorcinol	108463	Ι
Salicylic acid	69727	III
Sodium methoxide	124414	IV
Sodium phenate	139026	III
Stilbene	588590	III
Styrene	100425	Ι
Succinic acid	110156	Ι
Succinonitrile	110612	Ι
Sulfanilic acid	121573	III
Sulfolane	126330	II
Tartaric acid	526830	Ι
Terephthalic acid	100210	II
Tetrabromophthalic anhydride	632791	III
Tetrachlorobenzene (1,2,4,5-)	95943	Ι
Tetrachloroethane (1,1,2,2-)	79345	II
Tetrachloroethylene (Perchloroethylene)	127184	Ι
Tetrachlorophthalic-	117088	III
anhydride.		
Tetraethyl lead	78002	IV
Tetraethylene glycol	112607	Ι
Tetraethylene-	112572	V
pentamine.		
Tetrahydrofuran	109999	Ι
Tetrahydronapthalene	119642	IV
Tetrahydrophthalic anhydride	85438	II
Tetramethylene-	110601	II
diamine.		
Tetramethylethylenediamine	110189	V
Tetramethyllead	75741	V
Toluene	108883	Ι
Toluene 2,4 diamine	95807	II
Toluene 2,4 diisocyanate	584849	II

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Toluene diisocyanates (mixture)	26471625	II
Toluene sulfonic acids	104154	III
Toluenesulfonyl chloride	98599	III
Toluidine (o-)	95534	II
Trichloroaniline-	634935	III
(2,4,6-).		
Trichlorobenzene (1,2,3-)	87616	V
Trichlorobenzene (1,2,4-)	120821	Ι
Trichloroethane	71556	II
(1,1,1-)		
Trichloroethane (1,1,2-) (Vinyl trichloride)	79005	II
Trichloroethylene	79016	Ι
Trichlorofluoromethane	75694	I
Trichlorophenol	95954	Ι
(2,4,5-).		
(1,1,2-) Trichloro	76131	Ι
(1,2,2-) trifluoroethane.		
Triethanolamine	102716	Ι
Triethylamine	121448	IV
Triethylene glycol	112276	Ι
Triethylene glycol	112492	Ι
dimethyl ether.		
Triethylene glycol monoethyl ether	112505	V
Triethylene glycol monomethyl ether	112356	Ι
Trimethylamine	75503	IV
Trimethylcyclohexanol	933482	IV
Trimethylcyclo-	2408379	IV
hexanone.		
Trimethylcyclo-	34216347	V
hexylamine.		
Trimethylolpropane	77996	Ι
Trimethylpentane (2,2,4-)	540841	V
Tripropylene glycol	24800440	V
Vinyl acetate	108054	Π
Vinyl chloride (Chloroethylene)	75014	Ι
Vinyl toluene	25013154	III
Vinylcyclohexene (4-)	100403	II
Vinylidene chloride	75354	II
(1,1-dichloroethylene).		
Vinyl(N-)-pyrrolidone(2-)	88120	V

## National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

Chemical name <sup>a</sup>	CAS No. <sup>b</sup>	Group
Xanthates	140896	V
Xylene sulfonic acid	25321419	III
Xylenes (NOS) <sup>c</sup>	1330207	Ι
Xylene (m-)	108383	Ι
Xylene (o-)	95476	Ι
Xylene (p-)	106423	Ι
Xylenols (Mixed)	1300716	V
Xylidene	1300738	III
a Learner means all structured among comparts for the same much an of stars	of each element and door not mean	colta octara or

<sup>a</sup> Isomer means all structural arrangements for the same number of atoms of each element and does not mean salts, esters, or derivatives.

<sup>b</sup> CAS Number = Chemical Abstract Service number.

<sup>c</sup> NOS = not otherwise specified.

<sup>d</sup> No CAS number assigned.

[<u>59 FR 19454</u>, Apr. 22, 1994, as amended at <u>59 FR 48176</u>, Sept. 20, 1994; <u>61 FR 31439</u>, June 20, 1996; <u>63 FR 26082</u>, May 12, 1998]

## Table 2 to Subpart F of Part 63—Organic Hazardous Air Pollutants

Chemical name <sup>a b</sup>	CAS No. <sup>c</sup>
Acenaphthene	83329
Acetaldehyde	75070
Acetamide	60355
Acetonitrile	75058
Acetophenone	98862
Acrolein	107028
Acrylamide	79061
Acrylic acid	79107
Acrylonitrile	107131
Alizarin	72480
Allyl chloride	107051
Aniline	62533
Anisidine (o-)	90040
Anthracene	120127
Anthraquinone	84651
Benzene	71432
Benzotrichloride	98077
Benzyl chloride	100447
Biphenyl	92524
Bis(chloromethyl)ether	542881
Bromoform	75252
Bromonaphthalene	27497514

Chemical name <sup>a b</sup>	CAS No. <sup>c</sup>
Butadiene (1,3-)	106990
Carbon disulfide	75150
Carbon tetrachloride	56235
Chloroacetic acid	79118
Chloroacetophenone (2-)	532274
Chlorobenzene	108907
2-Chloro-,1,3-butadiene (Chloroprene)	126998
Chloroform	67663
Chloronaphthalene	25586430
Chrysene	218019
Cresols and cresylic acids (mixed)	1319773
Cresol and cresylic acid (o-)	95487
Cresol and cresylic acid (m-)	108394
Cresol and cresylic acid (p-)	106445
Cumene	98828
Dichlorobenzene (p-)	106467
Dichlorobenzidine (3,3'-)	91941
Dichloroethane (1,2-) (Ethylene dichloride) (EDC)	107062
Dichloroethylether (Bis(2-chloroethyl)ether)	111444
Dichloropropene (1,3-)	542756
Diethanolamine (2,2'-Iminodiethanol)	111422
Dimethylaniline (N,N-)	121697
Diethyl sulfate	64675
Dimethylbenzidine (3,3'-)	119937
Dimethylformamide (N,N-)	68122
Dimethylhydrazine (1,1-)	58147
Dimethylphthalate	131113
Dimethylsulfate	77781
Dinitrophenol (2,4-)	51285
Dinitrotoluene (2,4-)	121142
Dioxane (1,4-) (1,4-Diethyleneoxide)	123911
1,2-Diphenylhydrazine	122667
Epichlorohydrin (1-Chloro-2,3-epoxypropane)	106898
Ethyl acrylate	140885
Ethylbenzene	100414
Ethyl chloride (Chloroethane)	75003
Ethylene dibromide (Dibromoethane)	106934
Ethylene glycol	107211
Ethylene oxide	75218
Ethylidene dichloride (1,1-Dichloroethane)	75343

Chemical name <sup>a b</sup>	CAS No. <sup>c</sup>
Fluoranthene	206440
Formaldehyde	50000
Glycol ethers <sup>d</sup>	
Hexachlorobenzene	118741
Hexachlorobutadiene	87683
Hexachloroethane	67721
Hexane	110543
Hydroquinone	123319
Isophorone	78591
Maleic anhydride	108316
Methanol	67561
Methylbromide (Bromomethane)	74839
Methylchloride (Chloromethane)	74873
Methyl hydrazine	60344
Methyl isobutyl ketone (Hexone)	108101
Methyl isocyanate	624839
Methyl methacrylate	80626
Methyl tert-butyl ether	1634044
Methylene chloride (Dichloromethane)	75092
Methylene diphenyl diisocyanate (4,4'-) (MDI)	101688
Methylenedianiline (4,4'-)	101779
Naphthalene	91203
Naphthalene sulfonic acid (α)	85472
Naphthalene sulfonic acid (β)	120183
Naphthol (a)	90153
Naphthol (β)	135193
Naphtholsulfonic acid (1-)	567180
Naphthylamine sulfonic acid (1,4-)	84866
Naphthylamine sulfonic acid (2,1-)	81163
Naphthylamine (1-)	134327
Naphthylamine (2-)	91598
Nitronaphthalene (1-)	86577
Nitrobenzene	98953
Nitrophenol (p-)	100027
Nitropropane (2-)	79469
Phenanthrene	85018
Phenol	108952
Phenylenediamine (p-)	106503
Phosgene	75445
Phthalic anhydride	85449

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Chemical name <sup>a b</sup>	CAS No. <sup>c</sup>	
Propiolactone (beta-)	57578	
Propionaldehyde	123386	
Propylene dichloride (1,2-Dichloropropane)	78875	
Propylene oxide	75569	
Pyrene	129000	
Quinone	106514	
Styrene	100425	
Tetrachloroethane (1,1,2,2-)	79345	
Tetrachloroethylene (Perchloroethylene)	127184	
Tetrahydronaphthalene	119642	
Toluene	108883	
Toluene diamine (2,4-)	95807	
Toluene diisocyanate (2,4-)	584849	
Toluidine (o-)	95534	
Trichlorobenzene (1,2,4-)	120821	
Trichloroethane (1,1,1-) (Methyl chloroform)	71556	
Trichloroethane (1,1,2-) (Vinyl trichloride)	79005	
Trichloroethylene	79016	
Trichlorophenol (2,4,5-)	95954	
Triethylamine	121448	
Trimethylpentane (2,2,4-)	540841	
Vinyl acetate	108054	
Vinyl chloride (Chloroethylene)	75014	
Vinylidene chloride (1,1-Dichloroethylene)	75354	
Xylenes (NOS)	1330207	
Xylene (m-)	108383	
Xylene (o-)	95476	
Xylene (p-)	106423	
<sup>a</sup> For all Listings above containing the word "Compounds," the following applies: Unless otherwise specified, these listings are defined as including any unique chemical substance that contains the named chemical (i.e., antimony, arsenic) as part of that chemical's infrastructure.		
<sup>b</sup> Isomer means all structural arrangements for the same number of atoms of each element and does not mean salts, esters, or derivatives.		
° CAS No. = Chemical Abstract Service number.		
<sup>d</sup> Includes mono- and di- ethers of ethylene glycol, diethylene glycol, and triethylene glycol R-(OCH	I <sub>2</sub> CH <sub>2n</sub> -OR where:	
n = 1, 2,  or  3;		
R = alkyl or aryl groups; and		
R'' = R, H or groups which, when removed, yield glycol ethers with the structure:		
R-(OCH <sub>2</sub> CH <sub>2n</sub> -OH		

Polymers are excluded from the glycol category.

## National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

## [62 FR 2735, Jan. 17, 1997, as amended at 71 FR 76614, Dec. 21, 2006]

# Table 3 to Subpart F of Part 63—General Provisions Applicability to Subparts F, G, and H<sup>a</sup> to Subpart F

Reference	Applies to subparts F, G, and H	Comment
63.1(a)(1)	Yes	Overlap clarified in <u>§ 63.101, § 63.111, § 63.161</u> .
63.1(a)(2)	Yes	
63.1(a)(3)	Yes	§ 63.110 and § 63.160(b) of subparts G and H identify which standards are overridden.
63.1(a)(4)	No	Subpart F specifies applicability of each paragraph in subpart A to subparts F, G, and H.
63.1 (a)(5)-(a)(9)	No	
63.1(a)(10)	No	Subparts F, G, and H specify calendar or operating day.
63.1(a)(11)	No	Subpart F § 63.103(d) specifies acceptable methods for submitting reports. <sup>a</sup>
63.1 (a)(12)-(a)(14)	Yes	
63.1(b)(1)	No	Subpart F specifies applicability.
63.1(b)(2)	Yes	
63.1(b)(3)	No	
63.1(c)(1)	No	Subpart F specifies applicability.
63.1(c)(2)	No	Area sources are not subject to subparts F, G, and H.
63.1(c)(3)	No	
63.1(c)(4)	Yes	
63.1(c)(5)	No	Subparts G and H specify applicable notification requirements.
63.1(c)(6)	Yes	
63.1(d)	No	
63.1(e)	No	Subparts F, G, and H established before permit program.
63.2	Yes	Subpart F § 63.101(a) specifies those subpart A definitions that apply to the HON. Subpart F definition of "source" is equivalent to subpart A definition of "affected source."
63.3	No	Units of measure are spelled out in subparts F, G, and H.
63.4 (a)(1)-(a)(3)	Yes	
63.4(a)(4)	No	This is a reserved paragraph in subpart A of part 63.
63.4(a)(5)	Yes	
63.4(b)	Yes	
63.4(c)	Yes	
63.5(a)(1)	Yes	Except the terms "source" and "stationary source" in § $63.5(a)(1)$ should be interpreted as having the same meaning as "affected source."
63.5(a)(2)	Yes	
63.5(b)(1)	Yes	Except § $63.100(1)$ defines when construction or reconstruction is subject to standards for new sources.
63.5(b)(2)	No	This is a reserved paragraph in subpart A of part 63.
63.5(b)(3)	Yes	
63.5(b)(4)	Yes	Except the cross reference to $\S 63.9(b)$ is limited to $\S 63.9(b) (4)$ and $(5)$ .

Reference	Applies to subparts F, G, and H	Comment
		Subpart F overrides $\S$ 63.9 (b)(1) through (b)(3).
63.5(b)(5)	Yes	
63.5(b)(6)	Yes	Except $\S$ 63.100(1) defines when construction or reconstruction is subject to standards for new sources.
63.5(c)	No	This is a reserved paragraph in subpart A of part 63.
63.5(d)(1)(i)	No	For subpart G, see § 63.151(b) (2)(ii) and (2)(iii) for the applicability and timing of this submittal; for subpart H, see § 63.182(b) (2)(ii) and (b)(2)(iii) for applicability and timing of this submittal.
63.5(d)(1)(ii)	Yes	Except $\S 63.5(d)(1)(ii)(H)$ does not apply.
63.5(d)(1)(iii)	No	Subpart G requires submittal of the Notification of Compliance Status in § <u>63.152(b)</u> ; subpart H specifies requirements in § <u>63.182(c)</u> .
63.5(d)(2)	No	
63.5(d)(3)	Yes—subpart G No— subpart H	Except $\S$ 63.5(d)(3)(ii) does not apply to subpart G.
63.5(d)(4)	Yes	
63.5(e)	Yes	
63.5(f)(1)	Yes	
63.5(f)(2)	Yes	Except the cross-reference to $\S 63.5(d)(1)$ is changed to $\S 63.151(b)(2)(ii)$ of subpart G and to $\S 63.182(b)(2)(ii)$ of subpart H. The cross-reference to $\S 63.5(b)(2)$ does not apply.
63.6(a)	Yes	
63.6(b)(1)	No	Subparts F and H specify compliance dates for sources subject to subparts F, G, and H.
63.6(b)(2)	No	
63.6(b)(3)	Yes	
63.6(b)(4)	No	May apply when standards are proposed under Section 112(f) of the Clean Air Act.
63.6(b)(5)	No	Subparts G and H include notification requirements.
63.6(b)(6)	No	
63.6(b)(7)	No	
63.6(c)(1)	No	Subpart F specifies the compliance dates for subparts G and H.
63.6(c)(2)	No	
63.6(c)(3)	No	
63.6(c)(4)	No	
63.6(c)(5)	Yes	
63.6(d)	[Reserved]	
63.6(e)	Yes <sup>c</sup>	Except as otherwise specified for individual paragraphs. Does not apply to Group 2 emission points unless they are included in an emissions average. <sup>bc</sup>
63.6(e)(1)(i)	No	This is addressed by $\S 63.102(a)(4)$ and (f) of subpart F.
63.6(e)(1)(ii)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	

Reference	Applies to subparts F, G, and H	Comment
63.6(e)(1)(iii)	Yes	
63.6(e)(2)	[Reserved]	
63.6(e)(3)(i)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.6(e)(3)(i)(A)	No	This is addressed by $\S 63.102(a)(4)$ .
63.6(e)(3)(i)(B)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.6(e)(3)(i)(C)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.6(e)(3)(ii)	[Reserved]	
63.6(e)(3)(iii)	No	Recordkeeping and reporting are specified in $\S 63.103(c)(2)$ of subpart F and $\S 63.152(d)(1)$ of subpart G.
63.6(e)(3)(iv)	No	Recordkeeping and reporting are specified in $\S 63.103(c)(2)$ of subpart F and $\S 63.152(d)(1)$ of subpart G.
63.6(e)(3)(v)	No	Records retention requirements are specified in $\S$ <u>63.103(c)</u> .
63.6(e)(3)(vi)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.6(e)(3)(vii)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.6(e)(3)(viii)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.6(e)(3)(ix)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.6(f)(1)	No	§ 63.102(a) and (e) of subpart F specifies when the standards apply.
63.6(f)(2)(i)	Yes	
63.6(f)(2)(ii)	Yes—subpart G No— subpart H	§ 63.152(c)(2) of subpart G specifies the use of monitoring data in determining compliance with subpart G.
63.6(f)(2)(iii) (A), (B), and (C)	Yes	
63.6(f)(2)(iii)(D)	No	
63.6(f)(2)(iv)	Yes	
63.6(f)(2)(v)	Yes	
63.6(f)(3)	Yes	
63.6(g)	No	Procedures specified in $\S$ 63.102(b) of subpart F.
63.6(h)	No	
63.6(i)(1)	Yes	

Reference	Applies to subparts F, G, and H	Comment
63.6(i)(2)	Yes	
63.6(i)(3)	No	For subpart G, $\S 63.151(a)(6)$ specifies procedures; for subpart H, $\S 63.182(a)(6)$ specifies procedures.
63.6(i)(4)(i)(A)	Yes	
63.6(i)(4)(i)(B)	No	Dates are specified in $\S 63.151(a)(6)(i)$ of subpart G and $\S 63.182(a)(6)(i)$ of subpart H.
63.6(i)(4)(ii)	No	
63.6(i) (5)-(14)	Yes	
63.6(i)(15)	No	
63.6(i)(16)	Yes	
63.6(j)	Yes	
63.7(a)(1)	No	Subparts F, G, and H specify required testing and compliance demonstration procedures.
63.7(a)(2)	No	For subpart G, test results must be submitted in the Notification of Compliance Status due 150 days after compliance date, as specified in $\S$ <u>63.152(b)</u> ; for subpart H, all test results subject to reporting are reported in periodic reports.
63.7(a)(3)	Yes	
63.7(a)(4)	Yes	
63.7(b)	No	
63.7(c)	No	
63.7(d)	Yes	
63.7(e)(1)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	See <u>§ 63.103(b)(3)</u> .
63.7(e)(2)	Yes	
63.7(e)(3)	No	Subparts F, G, and H specify test methods and procedures.
63.7(e)(4)	Yes	
63.7(f)	Yes	
63.7(g)	No	Performance test reporting specified in <u>§ 63.152(b)</u> of subpart G: Not applicable to subpart H because no performance test required by subpart H.
63.7(h)(1)	Yes	
63.7(h)(2)	Yes	
63.7(h)(3)	No	§ 63.103(b)(5) of subpart F specifies provisions for requests to waive performance tests.
63.7(h)(4)	No	
63.7(h)(5)	Yes	
63.8(a)(1)	Yes	
63.8(a)(2)	No	
63.8(a)(3)	[Reserved]	
63.8(a)(4)	Yes, except for flares subject to $\frac{\& 63.108}{\& 63.108}$	

Reference	Applies to subparts F, G, and H	Comment
63.8(b)(1)	Yes	
63.8(b)(2)	No	Subparts G and H specify locations to conduct monitoring.
63.8(b)(3)	Yes	
63.8(c)(1)(i)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.8(c)(1)(ii)	No	For subpart G, submit as part of periodic report required by $\S 63.152(c)$ ; for subpart H, retain as required by $\S 63.181(g)(2)(ii)$ .
63.8(c)(1)(iii)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	
63.8(c)(2)	Yes	
63.8(c)(3)	Yes	
63.8(c)(4)	No	Subpart G specifies monitoring frequency by kind of emission point and control technology used (e.g., $\S$ 63.111, $\S$ 63.120(d)(2), $\S$ 63.143, and $\S$ 63.152(f)); subpart H does not require use of continuous monitoring systems.
63.8 (c)(5)-(c)(8)	No	
63.8(d)	No	
63.8(e)	No	
63.8 (f)(1)-(f)(3)	Yes	
63.8(f)(4)(i)	No	Timeframe for submitting request specified in $\S 63.151(f)$ or (g) of subpart G; not applicable to subpart H because subpart H specifies acceptable alternative methods.
63.8(f)(4)(ii)	Yes	
63.8(f)(4)(iii)	No	
63.8(f)(5)(i)	Yes	
63.8(f)(5)(ii)	No	
63.8(f)(5)(iii)	Yes	
63.8(f)(6)	No	Subparts G and H do not require continuous emission monitoring.
63.8(g)	No	Data reduction procedures specified in $\S 63.152(f)$ and (g) of subpart G; not applicable to subpart H.
63.9(a)	Yes	
63.9(b)(1)	No	Specified in § 63.151(b)(2) of subpart G; specified in § 63.182(b) of subpart H.
63.9(b)(2)	No	Initial Notification provisions are specified in $\S 63.151(b)$ of subpart G; in $\S 63.182(b)$ of subpart H.
63.9(b)(3)	No	
63.9(b)(4)	Yes	Except that the notification in $\S 63.9(b)(4)(i)$ shall be submitted at the time specified in $\S 63.151(b)(2)(ii)$ of subpart G; in $\S 63.182(b)(2)$ of subpart H.
63.9(b)(5)	Yes	Except that the notification in § $63.9(b)(5)$ shall be submitted at the time specified in § $63.151(b)(2)(ii)$ of subpart G; in § $63.182(b)(2)$ of subpart H.
63.9(c)	Yes	

## National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

Reference	Applies to subparts F, G, and H	Comment
63.9(d)	Yes	
63.9(e)	No	
63.9(f)	No	
63.9(g)	No	
63.9(h)	No	§ 63.152(b) of subpart G and <u>§ 63.182 (c)</u> of subpart H specify Notification of Compliance Status requirements.
63.9(i)	Yes	
63.9(j)	Yes	Only as related to change to major source status.
63.9(k)	Yes	
63.10(a)	Yes	
63.10(b)(1)	No	§ 63.103(c) of subpart F specifies record retention requirements.
63.10(b)(2)	No	§ 63.103(c) of subpart F specifies required records.
63.10(b)(3)	No	
63.10(c)	No	
63.10(d)(1)	No	
63.10(d)(2)	No	§ 63.152(b) of subpart G specifies performance test reporting; not applicable to subpart H.
63.10(d)(3)	No	
63.10(d)(4)	Yes	
63.10(d)(5)	Yes, before July 15, 2027. No, beginning on and after July 15, 2027	Except that, before July 15, 2027, reports required by $\S 63.10(d)(5)$ shall be submitted at the time specified in $\S 63.152(d)$ of subpart G and in $\S 63.182(d)$ of subpart H.
63.10(e)	No	
63.10(f)	Yes	
63.11-63.15	Yes, except $63.11(b)$ does not apply to flares subject to $\S 63.108$	
<sup>a</sup> Wherever subpar courier). Submitta	t A specifies "postmark" dat ls shall be sent by the specifi	es, submittals may be sent by methods other than the U.S. Mail ( <i>e.g.</i> , by fax or ed dates, but a postmark is not necessarily required.

<sup>b</sup> Except as specified in footnote c of this table, the plan, and any records or reports of start-up, shutdown, and malfunction do not apply to Group 2 emission points unless they are included in an emissions average.

<sup>c</sup> On and after July 15, 2027, footnote b of this table does not apply and the row for the "63.6(e)" entry of this table is no longer applicable.

[<u>62 FR 2737</u>, Jan. 17, 1997, as amended at <u>71 FR 20456</u>, Apr. 20, 2006; <u>85 FR 73887</u>, Nov. 19, 2020; <u>89 FR 43174</u>, May 16, 2024]

 Table 4 to Subpart F of Part 63—Organic Hazardous Air Pollutants Subject to Cooling Tower Monitoring Requirements in § 63.104

Chemical name	CAS Number <sup>a</sup>
Acetaldehyde	75070
Acetonitrile	75058

Chemical name	CAS Number <sup>a</sup>
Acetophenone	98862
Acrolein	107028
Acrylonitrile	107131
Allyl chloride	107051
Aniline	62533
Anisidine (o-)	90040
Benzene	71432
Benzyl chloride	100447
Biphenyl	92524
Bromoform	75252
Butadiene (1,3-)	106990
Carbon disulfide	75150
Carbon tetrachloride	56235
Chloroacetophenone (2-)	532274
Chlorobenzene	108907
2-Chloro-1,3-butadiene (Chloroprene)	126998
Chloroform	67663
Cresol and cresylic acid (o-)	95487
Cresol and cresylic acid (m-)	108394
Cresol and cresylic acid (p-)	106445
Cumene	98828
Dichlorobenzene (p-)	106467
Dichlorobenzidine (3,3"-)	91941
Dichloroethane (1,2-) (Ethylene dichloride) (EDC)	107062
Dichloroethyl ether (Bis(2-chloroethyl)ether)	111444
Dichloropropene (1,3-)	542756
Diethylene glycol diethyl ether	112367
Diethylene glycol dimethyl ether	111966
Diethyl sulfate	64675
Dimethylaniline (N,N-)	121697
Dimethylhydrazine (1,1-)	57147
Dimethyl phthalate	131113
Dimethyl sulfate	77781
Dinitrophenol (2,4-)	51285
Dinitrotoluene (2,4-)	121142
Dioxane (1,4-) (1,4-Diethyleneoxide)	123911
Epichlorohydrin (1-Chloro-2,3-epoxypropane)	106898
Ethyl acrylate	140885
Ethylbenzene	100414

Chemical name	CAS Number <sup>a</sup>
Ethyl chloride (Chloroethane)	75003
Ethylene dibromide (Dibromoethane)	106934
Ethylene glycol dimethyl ether	110714
Ethylene glycol monobutyl ether acetate	112072
Ethylene glycol monoethyl ether acetate	111159
Ethylene glycol monoethyl ether	110805
Ethylene glycol monomethyl ether	109864
Ethylene glycol monomethyl ether acetate	110496
Ethylene glycol monopropyl ether	2807309
Ethylene oxide	75218
Ethylidene dichloride (1,1-Dichloroethane)	75343
Formaldehyde	50000
Hexachlorobenzene	118741
Hexachlorobutadiene	87683
Hexachloroethane	67721
Hexane	110543
Isophorone	78591
Methanol	67561
Methyl bromide (Bromomethane)	74839
Methyl chloride (Chloromethane)	74873
Methyl hydrazine	60344
Methyl isobutyl ketone (Hexone)	108101
Methyl methacrylate	80626
Methyl tert-butyl ether	1634044
Methylene chloride (Dichloromethane)	75092
Methylenedianiline (4,4"-)	101779
Naphthalene	91203
Nitrobenzene	98953
Nitropropane (2-)	79469
Phenol	108952
Phenylenediamine (p-)	106503
Phosgene	75445
Propionaldehyde	123386
Propylene dichloride (1,2-Dichloropropane)	78875
Propylene oxide	75569
Quinone	106514
Styrene	100425
Tetrachloroethane (1,1,2,2-)	79345
Tetrachloroethylene (Perchloroethylene)	127184

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry

Chemical name	CAS Number <sup>a</sup>
Toluene	108883
Toluidine (o-)	95534
Trichlorobenzene (1,2,4-)	120821
Trichloroethane (1,1,1-) (Methyl chloroform)	71556
Trichloroethane (1,1,2-) (Vinyl trichloride)	79005
Trichloroethylene	79016
Trichlorophenol (2,4,5-)	95954
Triethylamine	121448
Trimethylpentane (2,2,4-)	540841
Vinyl acetate	108054
Vinyl chloride (chloroethylene)	75014
Vinylidene chloride (1,1-Dichloroethylene)	75354
Xylene (m-)	108383
Xylene (o-)	95476
Xylene (p-)	106423
<sup>a</sup> CAS Number = Chemical Abstract Service number	

[62 FR 2740, Jan. 17, 1997, as amended at 71 FR 76614, Dec. 21, 2006; 89 FR 43175, May 16, 2024]

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# Subpart FFFF—National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing

## Source:

68 FR 63888, Nov. 10, 2003, unless otherwise noted.

## What This Subpart Covers

## § 63.2430 What is the purpose of this subpart?

This subpart establishes national emission standards for hazardous air pollutants (NESHAP) for miscellaneous organic chemical manufacturing. This subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limits, operating limits, and work practice standards.

### § 63.2435 Am I subject to the requirements in this subpart?

(a) You are subject to the requirements in this subpart if you own or operate miscellaneous organic chemical manufacturing process units (MCPU) that are located at, or are part of, a major source of hazardous air pollutants (HAP) emissions as defined in section 112(a) of the Clean Air Act (CAA).

(b) An MCPU includes equipment necessary to operate a miscellaneous organic chemical manufacturing process, as defined in  $\S$  63.2550, that satisfies all of the conditions specified in <u>paragraphs (b)(1)</u> through (3) of this section. An MCPU also includes any assigned storage tanks and transfer racks; equipment in open systems that is used to convey or store water having the same concentration and flow characteristics as wastewater; and components such as pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, and instrumentation systems that are used to manufacture any material or family of materials described in <u>paragraphs</u> (b)(1)(i) through (v) of this section.

(1) The MCPU produces material or family of materials that is described in <u>paragraph (b)(1)(i)</u>, (ii), (iii), (iv), or (v) of this section.

(i) An organic chemical(s) classified using the 1987 version of SIC code 282, 283, 284, 285, 286, 287, 289, or 386, except as provided in <u>paragraph (c)(5)</u> of this section.

(ii) An organic chemical(s) classified using the 1997 version of NAICS code 325, except as provided in <u>paragraph (c)(5)</u> of this section.

(iii) Quaternary ammonium compounds and ammonium sulfate produced with caprolactam.

(iv) Hydrazine.

(v) Organic solvents classified in any of the SIC or NAICS codes listed in <u>paragraph (b)(1)(i)</u> or <u>(ii)</u> of this section that are recovered using nondedicated solvent recovery operations.

(2) The MCPU processes, uses, or generates any of the organic HAP listed in section 112(b) of the CAA or hydrogen halide and halogen HAP, as defined in  $\frac{63.2550}{25.0}$ .

(3) The MCPU is not an affected source or part of an affected source under another subpart of this part 63, except for process vents from batch operations within a chemical manufacturing process unit (CMPU), as identified in  $\S$  63.100(j)(4). For this situation, the MCPU is the same as the CMPU as defined in  $\S$  63.100, and you are subject only to the requirements for batch process vents in this subpart.

(c) The requirements in this subpart do not apply to the operations specified in <u>paragraphs (c)(1)</u> through (7) of this section.

(1) Research and development facilities, as defined in section 112(c)(7) of the CAA.

(2) The manufacture of ammonium sulfate as a by-product, if the slurry entering the by-product manufacturing process contains 50 parts per million by weight (ppmw) HAP or less or 10 ppmw benzene or less. You must retain information, data, and analysis to document the HAP concentration in the entering slurry in order to claim this exemption.

(3) The affiliated operations located at an affected source under subparts GG (National Emission Standards for Aerospace Manufacturing and Rework Facilities), KK (National Emission Standards for the Printing and Publishing Industry), JJJJ (NESHAP: Paper and Other Web Coating), MMMM (NESHAP: Surface Coating of Miscellaneous Metal Parts and Products), and SSSS (NESHAP: Surface Coating of Metal Coil) of this part. Affiliated operations include, but are not limited

to, mixing or dissolving of coating ingredients; coating mixing for viscosity adjustment, color tint or additive blending, or pH adjustment; cleaning of coating lines and coating line parts; handling and storage of coatings and solvent; and conveyance and treatment of wastewater.

(4) Fabricating operations (such as spinning or compressing a solid polymer into its end use); compounding operations (in which blending, melting, and resolidification of a solid polymer product occur for the purpose of incorporating additives, colorants, or stabilizers); and extrusion and drawing operations (converting an already produced solid polymer into a different shape by melting or mixing the polymer and then forcing it or pulling it through an orifice to create an extruded product). An operation is not exempt if it involves processing with HAP solvent or if an intended purpose of the operation is to remove residual HAP monomer.

(5) Production activities described using the 1997 version of NAICS codes 325131, 325181, 325188 (except the requirements do apply to hydrazine), 325314, 325991 (except the requirements do apply to reformulating plastics resins from recycled plastics products), and 325992 (except the requirements do apply to photographic chemicals).

(6) Tall oil recovery systems.

(7) Carbon monoxide production.

(d) If the predominant use of a transfer rack loading arm or storage tank (including storage tanks in series) is associated with a miscellaneous organic chemical manufacturing process, and the loading arm or storage tank is not part of an affected source under a subpart of this part 63, then you must assign the loading arm or storage tank to the MCPU for that miscellaneous organic chemical manufacturing process. If the predominant use cannot be determined, then you may assign the loading arm or storage tank to any MCPU that shares it and is subject to this subpart. If the use varies from year to year, then you must base the determination on the utilization that occurred during the year preceding November 10, 2003 or, if the loading arm or storage tank was not in operation during that year, you must base the use on the expected use for the first 5-year period after startup. You must include the determination in the notification of compliance status report specified in § 63.2520(d). You must redetermine the primary use at least once every 5 years, or any time you implement emissions averaging or pollution prevention after the compliance date.

(e) For nondedicated equipment used to create at least one MCPU, you may elect to develop process unit groups (PUG), determine the primary product of each PUG, and comply with the requirements of the subpart in 40 CFR part 63 that applies to that primary product as specified in § 63.2535(1).

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40331, July 14, 2006; 85 FR 49132, Aug. 12, 2020]

## § 63.2440 What parts of my plant does this subpart cover?

(a) This subpart applies to each miscellaneous organic chemical manufacturing affected source.

(b) The miscellaneous organic chemical manufacturing affected source is the facilitywide collection of MCPU and heat exchange systems, wastewater, and waste management units that are associated with manufacturing materials described in  $\frac{5}{63.2435(b)(1)}$ .

(c) A new affected source is described by either <u>paragraph (c)(1)</u> or (2) of this section.

(1) Each affected source defined in <u>paragraph (b)</u> of this section for which you commenced construction or reconstruction after April 4, 2002, and you meet the applicability criteria at the time you commenced construction or reconstruction.

(2) Each dedicated MCPU that has the potential to emit 10 tons per year (tpy) of any one HAP or 25 tpy of combined HAP, and you commenced construction or reconstruction of the MCPU after April 4, 2002. For the purposes of this paragraph, an MCPU is an affected source in the definition of the term "reconstruction" in  $\frac{63.2}{2}$ .

(d) An MCPU that is also a CMPU under  $\frac{63.100}{563.100}$  is reconstructed for the purposes of this subpart if, and only if, the CMPU meets the requirements for reconstruction in  $\frac{63.100(1)(2)}{563.100(1)(2)}$ .

## **Compliance Dates**

## § 63.2445 When do I have to comply with this subpart?

(a) Except as specified in <u>paragraphs (g)</u> through (i) of this section, if you have a new affected source, you must comply with this subpart according to the requirements in <u>paragraphs (a)(1)</u> and (2) of this section.

(1) If you startup your new affected source before November 10, 2003, then you must comply with the requirements for new sources in this subpart no later than November 10, 2003.

(2) If you startup your new affected source after November 10, 2003, then you must comply with the requirements for new sources in this subpart upon startup of your affected source.

(b) Except as specified in <u>paragraphs (g)</u> through (i) of this section, if you have an existing source on November 10, 2003, you must comply with the requirements for existing sources in this subpart no later than May 10, 2008.

(c) You must meet the notification requirements in  $\frac{63.2515}{2}$  according to the dates specified in that section and in <u>subpart A</u> of this part 63. Some of the notifications must be submitted before you are required to comply with the emission limits, operating limits, and work practice standards in this subpart.

(d) If you have a Group 2 emission point that becomes a Group 1 emission point after the compliance date for your affected source, you must comply with the Group 1 requirements beginning on the date the switch occurs. An initial compliance demonstration as specified in this subpart must be conducted within 150 days after the switch occurs.

(e) If, after the compliance date for your affected source, hydrogen halide and halogen HAP emissions from process vents in a process increase to more than 1,000 lb/yr, or HAP metals emissions from a process at a new affected source increase to more than 150 lb/yr, you must comply with the applicable emission limits specified in Table 3 to this subpart and the associated compliance requirements beginning on the date the emissions exceed the applicable threshold. An initial compliance demonstration as specified in this subpart must be conducted within 150 days after the switch occurs.

(f) If you have a small control device for process vent or transfer rack emissions that becomes a large control device, as defined in  $\S$  63.2550(i), you must comply with monitoring and associated recordkeeping and reporting requirements for large control devices beginning on the date the switch occurs. An initial compliance demonstration as specified in this subpart must be conducted within 150 days after the switch occurs.

(g) All affected sources that commenced construction or reconstruction on or before December 17, 2019, must be in compliance with the requirements listed in <u>paragraphs (g)(1)</u> through (7) of this section upon initial startup or on August 12, 2023, whichever is later. All affected sources that commenced construction or reconstruction after December 17, 2019, must be in compliance with the requirements listed in <u>paragraphs (g)(1)</u> through (7) of this section upon initial startup, or on August 12, 2020 whichever is later.

(1) The general requirements specified in  $\underline{\$\$}$ <u>63.2450(a)(2), (e)(4)</u> through (7), (g)(6) and (7), (i)(3), (j)(5)(ii), (j)(6), (k)(1)(ii), (k)(7) and (8), (t), and (u), 63.2520(d)(3) and (e)(11) through (13), 63.2525(m) through (0), and 63.2535(m).

(2) For process vents, the requirements specified in  $\S$  63.2450(v), 63.2520(e)(14), and 63.2525(p).

(3) For storage tank degassing, the requirements specified in § 63.2470(f).

(4) For equipment leaks and pressure relief devices, the requirements specified in <u>§§</u> <u>63.2480(e)</u> and <u>(f)</u>, <u>63.2520(d)(4)</u> and <u>(e)(14)</u>, and <u>63.2525(q)</u>.

(5) For wastewater streams and liquid streams in open systems within an MCPU, the requirements specified in § 63.2485(i)(2)(iii), (n)(2)(vii), (p), and (q).

(6) For heat exchange systems, the requirements specified in <u>§§ 63.2490(d)</u>, <u>63.2520(e)(16)</u>, and <u>63.2525(r)</u>.

(7) The other notification, reports, and records requirements specified in  $\underline{\$\$}$ <u>63.2500(g)</u>, <u>63.2520(e)(5)(ii)(D)</u> and <u>(e)(5)(iii)(M)</u> and <u>(N)</u>, and <u>63.2525(1)</u> and <u>(u)</u>.

(h) All affected sources that commenced construction or reconstruction on or before December 17, 2019, must be in compliance with the requirements for pumps in light liquid service in § 63.2480(b)(6) and (c)(10) upon initial startup or on August 12, 2021, whichever is later. All affected sources that commenced construction or reconstruction after December 17, 2019, must be in compliance with the requirements for pumps in light liquid service in § 63.2480(b)(6) and (c)(10) upon initial startup, or on August 12, 2020, whichever is later.

(i) All affected sources that commenced construction or reconstruction on or before December 17, 2019, must be in compliance with the ethylene oxide requirements in  $\underline{\$\$}$ 

 $\underline{63.2450(h)}$  and  $\underline{(r)}$ ,  $\underline{63.2470(b)}$  and  $\underline{(c)(4)}$ ,  $\underline{63.2492}$ ,  $\underline{63.2493}$ ,  $\underline{63.2520(d)(5)}$  and  $\underline{(e)(17)}$ , and  $\underline{63.2525(s)}$  and Table 1 to this subpart, item 5, Table 2 to this subpart, item 3, Table 4 to this subpart, item 3, and Table 6 to this subpart, item 3, upon initial

startup or on August 12, 2022, whichever is later. All affected sources that commenced construction or reconstruction after December 17, 2019, must be in compliance with the ethylene oxide requirements listed in §§ <u>63.2450(h)</u> and (r), <u>63.2470(b)</u> and (c)(4), <u>63.2492</u>, <u>63.2493</u>, <u>63.2520(d)(5)</u> and (e)(17), and <u>63.2525(s)</u> and Table 1 to this subpart, item 5, Table 2 to this subpart, item 3, Table 4 to this subpart, item 3, and Table 6 to this subpart, item 3, upon initial startup, or on August 12, 2020, whichever is later.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>71 FR 10442</u>, Mar. 1, 2006; <u>71 FR 40332</u>, July 14, 2006; <u>85 FR 49132</u>, Aug. 12, 2020]

## Emission Limits, Work Practice Standards, and Compliance Requirements

## § 63.2450 What are my general requirements for complying with this subpart?

(a) General. You must comply with paragraphs (a)(1) and (2) of this section.

(1) Except as specified in paragraph (a)(2) of this section, you must be in compliance with the emission limits and work practice standards in Tables 1 through 7 to this subpart at all times, except during periods of startup, shutdown, and malfunction (SSM), and you must meet the requirements specified in  $\frac{\&\& 63.2455}{63.2495}$  through  $\frac{63.2490}{63.2495}$  (or the alternative means of compliance in & 63.2495, & 63.2505), except as specified in paragraphs (b) through (s) of this section. You must meet the notification, reporting, and recordkeeping requirements specified in && 63.2515, & 63.2515, & 63.2520, and & 63.2525.

(2) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , paragraph (a)(1) of this section no longer applies. Instead, you must be in compliance with the emission limits and work practice standards in Tables 1 through 7 to this subpart at all times, and you must meet the requirements specified in  $\S 83.2455$  through 63.2490 (or the alternative means of compliance in  $\S 63.2495$ ,  $\S 63.2500$ , or  $\S 63.2505$ ), except as specified in paragraphs (b) through (v) of this section. You must meet the notification, reporting, and recordkeeping requirements specified in  $\S 8 63.2515$ , 63.2515, 63.2520, and 63.2525.

(b) Determine halogenated vent streams. You must determine if an emission stream is a halogenated vent stream, as defined in  $\S$  63.2550, by calculating the mass emission rate of halogen atoms in accordance with  $\S$  63.115(d)(2)(v). Alternatively, you may elect to designate the emission stream as halogenated.

(c) Requirements for combined emission streams. When organic HAP emissions from different emission types (e.g., continuous process vents, batch process vents, storage tanks, transfer operations, and waste management units) are combined, you must comply with the requirements of either paragraph (c)(1) or (2) of this section.

(1) Comply with the applicable requirements of this subpart for each kind of organic HAP emissions in the stream (e.g., the requirements of table 1 to this subpart for continuous process vents and the requirements of table 4 to this subpart for emissions from storage tanks).

(2) Determine the applicable requirements based on the hierarchy presented in <u>paragraphs (c)(2)(i)</u> through (vi) of this section. For a combined stream, the applicable requirements are specified in the highest-listed paragraph in the hierarchy that applies to any of the individual streams that make up the combined stream. For example, if a combined stream consists of emissions from Group 1 batch process vents and any other type of emission stream, then you must comply with the requirements in <u>paragraph (c)(2)(i)</u> of this section for the combined stream; compliance with the requirements in <u>paragraph (c)(2)(i)</u> of this section for the other emission streams in the combined stream. Two exceptions are that you must comply with the requirements in Table 3 to this subpart and § 63.2465 for all process vents with hydrogen halide and halogen HAP emissions, and recordkeeping requirements for Group 2 applicability or compliance are still required (*e.g.*, the requirement in § 63.2525(e)(3) and (4) to track the number of batches produced and calculate rolling annual emissions for processes with Group 2 batch process vents).

(i) The requirements of table 2 to this subpart and <u>§ 63.2460</u> for Group 1 batch process vents, including applicable monitoring, recordkeeping, and reporting.

(ii) The requirements of table 1 to this subpart and  $\frac{63.2455}{5}$  for continuous process vents that are routed to a control device, as defined in  $\frac{63.981}{5}$ , including applicable monitoring, recordkeeping, and reporting.

(iii) The requirements of table 5 to this subpart and <u>§ 63.2475</u> for transfer operations, including applicable monitoring, recordkeeping, and reporting.

(iv) The requirements of table 7 to this subpart and  $\S 63.2485$  for emissions from waste management units that are used to manage and treat Group 1 wastewater streams and residuals from Group 1 wastewater streams, including applicable monitoring, recordkeeping, and reporting.

(v) The requirements of table 4 to this subpart and  $\S 63.2470$  for control of emissions from storage tanks, including applicable monitoring, recordkeeping, and reporting.

(vi) The requirements of table 1 to this subpart and <u>§ 63.2455</u> for continuous process vents after a recovery device including applicable monitoring, recordkeeping, and reporting.

(d) [Reserved]

(e) Requirements for control devices.

(1) Except when complying with § 63.2485 or paragraph (e)(7) of this section, if you reduce organic HAP emissions by venting emissions through a closed-vent system to any combination of control devices (except a flare) or recovery devices, you must meet the requirements of paragraph (e)(4) of this section, and the requirements of § 63.982(c) and the requirements referenced therein.

(2) Except as specified in <u>paragraph (e)(5)</u> of this section or except when complying with  $\S$  <u>63.2485</u>, if you reduce organic HAP emissions by venting emissions through a closed-vent system to a flare, you must meet the requirements of <u>paragraph</u> (e)(4) of this section, and the requirements of  $\S$  <u>63.982(b)</u> and the requirements referenced therein.

(3) Except as specified in <u>paragraphs (e)(3)(i)</u> and (ii) of this section, if you use a halogen reduction device to reduce hydrogen halide and halogen HAP emissions from halogenated vent streams, you must meet the requirements of <u>paragraph</u> (e)(4) of this section, and the requirements of <u>§ 63.994</u> and the requirements referenced therein. If you use a halogen reduction device before a combustion device, you must determine the halogen atom emission rate prior to the combustion device according to the procedures in <u>§ 63.115(d)(2)(v)</u>.

(i) Beginning on and after October 13, 2020, performance test reports must be submitted according to the procedures in  $\S$  <u>63.2520(f)</u>.

(ii) If you use a halogen reduction device other than a scrubber, then you must submit procedures for establishing monitoring parameters to the Administrator as part of your precompliance report as specified in  $\frac{63.2520(c)(8)}{2}$ .

(4) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , the referenced provisions specified in paragraphs (e)(4)(i) through (xvi) of this section do not apply when demonstrating compliance with subpart SS of this part.

(i) The phrase "Except for equipment needed for safety purposes such as pressure relief devices, low leg drains, high point bleeds, analyzer vents, and open-ended valves or lines" in  $\frac{63.983(a)(3)}{2}$  of subpart SS.

(ii) The second sentence of  $\S 63.983(a)(5)$  of subpart SS.

(iii) The phrase "except during periods of start-up, shutdown and malfunction as specified in the referencing subpart" in  $\S$  <u>63.984(a)</u> of subpart SS.

(iv) The phrase "except during periods of start-up, shutdown, and malfunction as specified in the referencing subpart" in  $\S$  <u>63.985(a)</u> of subpart SS.

(v) The phrase "other than start-ups, shutdowns, or malfunctions" in  $\frac{63.994(c)(1)(ii)(D)}{1000}$  of subpart SS.

(vi) Section 63.996(c)(2)(ii) of subpart SS.

(vii) The last sentence of  $\S 63.997(e)(1)(i)$  of subpart SS.

- (viii) Section 63.998(b)(2)(iii) of subpart SS.
- (ix) The phrase "other than start-ups, shutdowns or malfunctions" in  $\frac{63.998(b)(5)(i)(A)}{5}$  of subpart SS.
- (x) The phrase "other than a start-up, shutdown, or malfunction" from  $\frac{63.998(b)(5)(i)(B)(3)}{5}$  of subpart SS.
- (xi) The phrase "other than start-ups, shutdowns or malfunctions" in  $\frac{63.998(b)(5)(i)(C)}{5}$  of subpart SS.
- (xii) The phrase "other than a start-up, shutdown, or malfunction" from § 63.998(b)(5)(ii)(C) of subpart SS.
- (xiii) The phrase "except as provided in <u>paragraphs (b)(6)(i)(A)</u> and (B) of this section" in  $\S$  63.998(b)(6)(i) of subpart SS.
- (xiv) The second sentence of  $\S$  63.998(b)(6)(ii) of subpart SS.
- (xv) Section 63.998(c)(1)(ii)(D), (E), (F), and (G) of subpart SS.

(xvi) Section 63.998(d)(3) of subpart SS.

(5) For any flare that is used to reduce organic HAP emissions from an MCPU, you may elect to comply with the requirements in this paragraph in lieu of the requirements of § 63.982(b) and the requirements referenced therein. However, beginning no later than the compliance dates specified in  $\S$  63.2445(g), paragraphs (e)(2) and (f) of this section no longer apply to flares that control ethylene oxide emissions from affected sources in ethylene oxide service as defined in § 63.2550 and flares used to control emissions from MCPUs that produce olefins or polyolefins. Instead, if you reduce organic HAP emissions by venting emissions through a closed-vent system to a steam-assisted, air-assisted, non-assisted, or pressureassisted multi-point flare that controls ethylene oxide emissions from affected sources in ethylene oxide service as defined in § 63.2550 or is used to control emissions from an MCPU that produces olefins or polyolefins, then you must meet the applicable requirements for flares as specified in §§ 63.670 and 63.671 of subpart CC, including the provisions in Tables 12 and 13 to subpart CC of this part, except as specified in paragraphs (e)(5)(i) through (xiii) of this section. This requirement in this paragraph (e)(5) also applies to any flare using fuel gas from a fuel gas system, of which 50 percent or more of the fuel gas is derived from an MCPU that has processes and/or equipment in ethylene oxide service or that produces olefins or polyolefins, as determined on an annual average basis. For purposes of compliance with this paragraph (e)(5), the following terms are defined in § 63.641 of subpart CC: Assist air, assist steam, center steam, combustion zone, combustion zone gas, flare, flare purge gas, flare supplemental gas, flare sweep gas, flare vent gas, lower steam, net heating value, perimeter assist air, pilot gas, premix assist air, total steam, and upper steam. Also, for purposes of compliance with this paragraph (e)(5), "MCPUs that produces olefins or polyolefins" includes only those MCPUs that manufacture ethylene, propylene, polyethylene, and/or polypropylene as a product. By-products and impurities as defined in § 63.101, as well as wastes and trace contaminants, are not considered products.

(i) When determining compliance with the pilot flame requirements specified in  $\S$  63.670(b) and (g), substitute "pilot flame or flare flame" for each occurrence of "pilot flame."

(ii) When determining compliance with the flare tip velocity and combustion zone operating limits specified in § <u>63.670(d)</u> and (e), the requirement effectively applies starting with the 15-minute block that includes a full 15 minutes of the flaring event. You are required to demonstrate compliance with the velocity and NHVcz requirements starting with the block that contains the fifteenth minute of a flaring event. You are not required to demonstrate compliance for the previous 15-minute block in which the event started and contained only a fraction of flow.

(iii) Instead of complying with <u>paragraph (0)(2)(i) of § 63.670</u> of subpart CC, you must develop and implement the flare management plan no later than the compliance dates specified in § 63.2445(g).

(iv) Instead of complying with paragraph ( $_{0}(2)(iii)$  of § 63.670 of subpart CC, if required to develop a flare management plan and submit it to the Administrator, then you must also submit all versions of the plan in portable document format (PDF) to the EPA following the procedure specified in § 63.9(k), except any medium submitted through mail must be sent to the attention of the Miscellaneous Organic Chemical Manufacturing Sector Lead.

(v) Section 63.670(o)(3)(ii) of subpart CC and all references to  $\frac{63.670(o)(3)(ii)}{63.670(o)(3)(ii)}$  of subpart CC do not apply. Instead, the owner or operator must comply with the maximum flare tip velocity operating limit at all times.

(vi) Substitute "MCPU" for each occurrence of "petroleum refinery."

(vii) Each occurrence of "refinery" does not apply.

(viii) If a pressure-assisted multi-point flare is used as a control device, then you must meet the following conditions:

(A) You are not required to comply with the flare tip velocity requirements in <u>paragraph (d)</u> and <u>(k) of § 63.670</u> of subpart CC;

(B) You must comply with the NHVcz requirements in paragraph (e)(2) of § 63.670 of subpart CC;

(C) You must determine the 15-minute block average NHVvg using only the direct calculation method specified in in paragraph (1)(5)(ii) of § 63.670 of subpart CC;

(D) Instead of complying with <u>paragraph (b)</u> and (g) of § 63.670 of subpart CC, if a pressure-assisted multi-point flare uses cross-lighting on a stage of burners rather than having an individual pilot flame on each burner, then you must operate each stage of the pressure-assisted multi-point flare with a flame present at all times when regulated material is routed to that stage of burners. Each stage of burners that cross-lights in the pressure-assisted multi-point flare must have at least two pilots with at least one continuously lit and capable of igniting all regulated material that is routed to that stage of burners. Each 15-minute block during which there is at least one minute where no pilot flame is present on a stage of burners when regulated

material is routed to the flare is a deviation of the standard. Deviations in different 15-minute blocks from the same event are considered separate deviations. The pilot flame(s) on each stage of burners that use cross-lighting must be continuously monitored by a thermocouple or any other equivalent device used to detect the presence of a flame;

(E) Unless you choose to conduct a cross-light performance demonstration as specified in this paragraph (e)(5)(viii)(E), you must ensure that if a stage of burners on the flare uses cross-lighting, that the distance between any two burners in series on that stage is no more than 6 feet when measured from the center of one burner to the next burner. A distance greater than 6 feet between any two burners in series may be used provided you conduct a performance demonstration that confirms the pressure-assisted multi-point flare will cross-light a minimum of three burners and the spacing between the burners and location of the pilot flame must be representative of the projected installation. The compliance demonstration must be approved by the permitting authority and a copy of this approval must be maintained onsite. The compliance demonstration report must include: A protocol describing the test methodology used, associated test method QA/QC parameters, the waste gas composition and NHVcz of the gas tested, the velocity of the waste gas tested, the pressure-assisted multi-point flare burners to cross-light, records of maintaining a stable flame after a successful cross-light and the duration for which this was observed, records of any smoking events during the cross-light, waste gas temperature, meteorological conditions (*e.g.*, ambient temperature, barometric pressure, wind speed and direction, and relative humidity), and whether there were any observed flare flameouts; and

(F) You must install and operate pressure monitor(s) on the main flare header, as well as a valve position indicator monitoring system for each staging valve to ensure that the flare operates within the proper range of conditions as specified by the manufacturer. The pressure monitor must meet the requirements in Table 13 to <u>subpart CC of this part</u>.

(G) If a pressure-assisted multi-point flare is operating under the requirements of an approved alternative means of emission limitations, you must either continue to comply with the terms of the alternative means of emission limitations or comply with the provisions in paragraphs (e)(5)(viii)(A) through (F) of this section.

(ix) If you choose to determine compositional analysis for net heating value with a continuous process mass spectrometer, then you must comply with the requirements specified in paragraphs (e)(5)(ix)(A) through (G) of this section.

(A) You must meet the requirements in  $\frac{63.671(e)(2)}{2}$ . You may augment the minimum list of calibration gas components found in  $\frac{63.671(e)(2)}{2}$  with compounds found during a pre-survey or known to be in the gas through process knowledge.

(B) Calibration gas cylinders must be certified to an accuracy of 2 percent and traceable to National Institute of Standards and Technology (NIST) standards.

(C) For unknown gas components that have similar analytical mass fragments to calibration compounds, you may report the unknowns as an increase in the overlapped calibration gas compound. For unknown compounds that produce mass fragments that do not overlap calibration compounds, you may use the response factor for the nearest molecular weight hydrocarbon in the calibration mix to quantify the unknown component's NHVvg.

(D) You may use the response factor for n-pentane to quantify any unknown components detected with a higher molecular weight than n-pentane.

(E) You must perform an initial calibration to identify mass fragment overlap and response factors for the target compounds.

(F) You must meet applicable requirements in Performance Specification 9 of <u>40 CFR part 60, appendix B</u>, for continuous monitoring system acceptance including, but not limited to, performing an initial multi-point calibration check at three concentrations following the procedure in <u>Section 10.1</u> and performing the periodic calibration requirements listed for gas chromatographs in Table 13 to <u>subpart CC of this part</u>, for the process mass spectrometer. You may use the alternative sampling line temperature allowed under Net Heating Value by Gas Chromatograph in Table 13 to <u>subpart CC of this part</u>.

(G) The average instrument calibration error (CE) for each calibration compound at any calibration concentration must not differ by more than 10 percent from the certified cylinder gas value. The CE for each component in the calibration blend must be calculated using Equation 1 to this paragraph (e)(5)(ix)(G).

$$CE = \frac{C_m - C_a}{C_a} \times 100 \text{ (Eq. 1)}$$

Where:

Cm = Average instrument response (ppm).

Ca = Certified cylinder gas value (ppm).

(x) If you use a gas chromatograph or mass spectrometer for compositional analysis for net heating value, then you may choose to use the CE of  $NHV_{measured}$  versus the cylinder tag value NHV as the measure of agreement for daily calibration and quarterly audits in lieu of determining the compound-specific CE. The CE for NHV at any calibration level must not differ by more than 10 percent from the certified cylinder gas value. The CE for must be calculated using Equation 2 to this <u>paragraph</u> (e)(5)(x).

$$CE = \frac{NHV_{measured} - NHV_a}{NHV_a} \times 100 \text{ (Eq. 2)}$$

Where:

 $NHV_{measured} = Average instrument response (Btu/scf).$ 

 $NHV_a = Certified$  cylinder gas value (Btu/scf).

(xi) Instead of complying with <u>paragraph (q) of § 63.670</u> of subpart CC, you must comply with the reporting requirements specified in § 63.2520(d)(3) and (e)(11).

(xii) Instead of complying with <u>paragraph (p) of § 63.670</u> of subpart CC, you must keep the flare monitoring records specified in § 63.2525(m).

(xiii) You may elect to comply with the alternative means of emissions limitation requirements specified in paragraph (r) of § 63.670 of subpart CC in lieu of the requirements in paragraphs (d) through (f) of § 63.670 of subpart CC, as applicable. However, instead of complying with paragraph (r)(3)(iii) of § 63.670 of subpart CC, you must also submit the alternative means of emissions limitation request to the following address: U.S. Environmental Protection Agency, Office of Air Quality Planning and Standards, Sector Policies and Programs Division, U.S. EPA Mailroom (C404-02), Attention: Miscellaneous Organic Chemical Manufacturing Sector Lead, 4930 Old Page Rd., Durham, NC 27703.

(6) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , the use of a bypass line at any time on a closed vent system to divert emissions subject to the requirements in Tables 1 through 7 to this subpart to the atmosphere or to a control device not meeting the requirements specified in Tables 1 through 7 to this subpart is an emissions standards deviation. You must also comply with the requirements specified in paragraphs (e)(6)(i) through (v) of this section, as applicable:

(i) If you are subject to the bypass monitoring requirements of  $\S 63.148(f)$  of subpart G, then you must continue to comply with the requirements in  $\S 63.148(f)$  of subpart G and the recordkeeping and reporting requirements in  $\S \S 63.148(f)$  of subpart G, and  $\S 63.148(i)(3)$  of subpart G, in addition to the applicable requirements specified in  $\S 63.2485(q)$ , the recordkeeping requirements specified in  $\S 63.2525(n)$ , and the reporting requirements specified in  $\S 63.2520(e)(12)$ .

(ii) If you are subject to the bypass monitoring requirements of  $\S 63.172(j)$  of subpart H, then you must continue to comply with the requirements in  $\S 63.172(j)$  of subpart H and the recordkeeping and reporting requirements in  $\S 63.118(a)(3)$  and (4), and (f)(3) and (4) of subpart G, in addition to the applicable requirements specified in  $\S 83.2480(f)$  and 63.2485(q), the recordkeeping requirements specified in  $\S 63.2525(n)$ , and the reporting requirements specified in  $\S 63.2520(e)(12)$ .

(iii) If you are subject to the bypass monitoring requirements of  $\frac{63.983(a)(3)}{63.983(a)(3)}$  of subpart SS, then you must continue to comply with the requirements in  $\frac{63.983(a)(3)}{63.998(d)(1)(ii)}$  and  $\frac{63.999(c)(2)}{63.2520(c)(2)}$  of subpart SS, in addition to the requirements specified in  $\frac{63.2450(c)(4)}{63.2520(c)(12)}$ .

(iv) If you are subject to the bypass monitoring requirements of  $\frac{65.143(a)(3)}{65.143(a)(3)}$  of this chapter, then you must continue to comply with the requirements in  $\frac{65.143(a)(3)}{65.163(a)(1)}$  and the recordkeeping and reporting requirements in  $\frac{86}{53.2480(f)}$ , the recordkeeping requirements specified in  $\frac{63.2480(f)}{63.2520(e)(12)}$ .

(v) For purposes of compliance with this <u>paragraph (e)(6)</u>, <u>§§ 63.148(f)(3)</u> of subpart G, and 63.172(j)(3) of subpart H, the phrase "Except for equipment needed for safety purposes such as pressure relief devices, low leg drains, high point bleeds,

analyzer vents, and open-ended valves or lines" in  $\S 63.983(a)(3)$  of subpart SS, and the phrase "Except for pressure relief devices needed for safety purposes, low leg drains, high point bleeds, analyzer vents, and open-ended valves or lines" in  $\S 65.143(a)(3)$  of this chapter do not apply; instead, the exemptions specified in paragraphs (e)(6)(v)(A) and (B) of this section apply.

(A) Except for pressure relief devices subject to  $\frac{63.2480(e)(4)}{63.2480(e)(4)}$ , equipment such as low leg drains and equipment subject to the requirements specified in  $\frac{63.2480}{63.2480}$  are not subject to this paragraph (e)(6).

(B) Open-ended valves or lines that use a cap, blind flange, plug, or second valve and follow the requirements specified in  $\frac{40}{CFR}$  <u>60.482-6(a)(2)</u>, (b), and (c) or follow requirements codified in another regulation that are the same as  $\frac{40 \ CFR \ 60.482-6(a)(2)}{6(a)(2)}$ , (b), and (c) are not subject to this <u>paragraph (e)(6)</u>.

(7) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , if you reduce organic HAP emissions by venting emissions through a closed-vent system to an adsorber(s) that cannot be regenerated or a regenerative adsorber(s) that is regenerated offsite, then you must comply with paragraphs (e)(4) and (6) of this section,  $\S 63.2470(c)(3)$ ,  $\S \S 63.2520(d)(6)$  and (e)(13),  $\S 63.2525(o)$ , the requirements in  $\S 63.983$  including the requirements referenced therein, and you must install a system of two or more adsorber units in series and comply with the requirements specified in paragraphs (e)(7)(i) through (iii) of this section.

(i) Conduct an initial performance test or design evaluation of the adsorber and establish the breakthrough limit and adsorber bed life.

(ii) Monitor the HAP or total organic compound (TOC) concentration through a sample port at the outlet of the first adsorber bed in series according to the schedule in <u>paragraph (e)(7)(iii)(B)</u> of this section. You must measure the concentration of HAP or TOC using either a portable analyzer, in accordance with Method 21 of <u>40 CFR part 60</u>, <u>appendix A</u>-7, using methane, propane, isobutylene, or the primary HAP being controlled as the calibration gas or Method 25A of <u>40 CFR part 60</u>, <u>appendix A</u>-7, using methane, propane, or the primary HAP being controlled as the calibration gas.

(iii) Comply with <u>paragraph (e)(7)(iii)(A)</u> of this section, and comply with the monitoring frequency according to <u>paragraph</u> (e)(7)(iii)(B) of this section.

(A) The first adsorber in series must be replaced immediately when breakthrough, as defined in § 63.2550(i), is detected between the first and second adsorber. The original second adsorber (or a fresh canister) will become the new first adsorber and a fresh adsorber will become the second adsorber. For purposes of this paragraph (e)(7)(iii)(A), "immediately" means within 8 hours of the detection of a breakthrough for adsorbers of 55 gallons or less, and within 24 hours of the detection of a breakthrough for adsorber at the outlet of the first adsorber within 3 days of replacement to confirm it is performing properly.

(B) Based on the adsorber bed life established according to <u>paragraph (e)(7)(i)</u> of this section and the date the adsorbent was last replaced, conduct monitoring to detect breakthrough at least monthly if the adsorbent has more than 2 months of life remaining, at least weekly if the adsorbent has between 2 months and 2 weeks of life remaining, and at least daily if the adsorbent has 2 weeks or less of life remaining.

(f) Requirements for flare compliance assessments. Except as specified in paragraph (e)(5) of this section, you must comply with paragraphs (f)(1) and (2) of this section.

(1) As part of a flare compliance assessment required in  $\S$  63.987(b), you have the option of demonstrating compliance with the requirements of  $\S$  63.11(b) by complying with the requirements in either  $\S$  63.11(b)(6)(i) or  $\S$  63.987(b)(3)(ii).

(2) If you elect to meet the requirements in  $\S 63.11(b)(6)(i)$ , you must keep flare compliance assessment records as specified in paragraphs (f)(2)(i) and (ii) of this section.

(i) Keep records as specified in  $\frac{63.998(a)(1)(i)}{2}$ , except that a record of the heat content determination is not required.

(ii) Keep records of the flare diameter, hydrogen content, exit velocity, and maximum permitted velocity. Include these records in the flare compliance report required in  $\frac{63.999(a)(2)}{2}$ .

(g) Requirements for performance tests. The requirements specified in paragraphs (g)(1) through (7) of this section apply instead of or in addition to the requirements specified in subpart SS of this part.

(1) Conduct gas molecular weight analysis using Method 3, 3A, or 3B in appendix A to part 60 of this chapter.

(2) Measure moisture content of the stack gas using Method 4 in appendix A to part 60 of this chapter.

(3) If the uncontrolled or inlet gas stream to the control device contains carbon disulfide, you must conduct emissions testing according to  $\frac{\text{paragraph } (g)(3)(i)}{\text{or } (ii)}$  of this section.

(i) If you elect to comply with the percent reduction emission limits in tables 1 through 7 to this subpart, and carbon disulfide is the principal organic HAP component (*i.e.*, greater than 50 percent of the HAP in the stream by volume), then you must use Method 18, or Method 15 (40 CFR part 60, appendix A) to measure carbon disulfide at the inlet and outlet of the control device. Use the percent reduction in carbon disulfide as a surrogate for the percent reduction in total organic HAP emissions.

(ii) If you elect to comply with the outlet TOC concentration emission limits in Tables 1 through 7 to this subpart, and the uncontrolled or inlet gas stream to the control device contains greater than 10 percent (volume concentration) carbon disulfide, you must use Method 18 or Method 15 of <u>40 CFR part 60</u>, appendix A, to separately determine the carbon disulfide concentration. Calculate the total HAP or TOC emissions by totaling the carbon disulfide emissions measured using Method 18 or 15 of <u>40 CFR part 60</u>, appendix A, and the other HAP emissions measured using Method 18 or 25A of <u>40 CFR part 60</u>, appendix A.

(4) As an alternative to using Method 18, Method 25/25A, or Method 26/26A of <u>40 CFR part 60</u>, <u>appendix A</u>, to comply with any of the emission limits specified in tables 1 through 7 to this subpart, you may use Method 320 of <u>40 CFR part 60</u>, <u>appendix A</u>. When using Method 320, you must follow the analyte spiking procedures of section 13 of Method 320, unless you demonstrate that the complete spiking procedure has been conducted at a similar source.

(5) Section 63.997(c)(1) does not apply. For the purposes of this subpart, results of all initial compliance demonstrations must be included in the notification of compliance status report, which is due 150 days after the compliance date, as specified in § 63.2520(d)(1). If the initial compliance demonstration includes a performance test and the results are submitted electronically via CEDRI in accordance with § 63.2520(f), the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the notification of compliance status report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(6) Beginning no later than the compliance dates specified in § 63.2445(g), in lieu of the requirements specified in § 63.7(e)(1) of subpart A you must conduct performance tests under such conditions as the Administrator specifies based on representative performance of the affected source for the period being tested. Representative conditions exclude periods of startup and shutdown. You may not conduct performance tests during periods of malfunction. You must record the process information that is necessary to document operating conditions during the test and include in such record an explanation to support that such conditions represent normal operation. Upon request, you must make available to the Administrator such records as may be necessary to determine the conditions of performance tests.

(7) Comply with the requirements in  $\S 63.2450(e)(4)$ , as applicable.

(h) Design evaluation. To determine the percent reduction of a small control device that is used to comply with an emission limit specified in Table 1, 2, 3, or 5 to this subpart, you may elect to conduct a design evaluation as specified in  $\S$  <u>63.1257(a)(1)</u> instead of a performance test as specified in <u>subpart SS of this part</u>. You must establish the value(s) and basis for the operating limits as part of the design evaluation. For continuous process vents, the design evaluation must be conducted at maximum representative operating conditions for the process, unless the Administrator specifies or approves alternate operating conditions. For transfer racks, the design evaluation must demonstrate that the control device achieves the required control efficiency during the reasonably expected maximum transfer loading rate. Beginning no later than the compliance dates specified in  $\S$  <u>63.2445(i)</u>, this <u>paragraph (h)</u> does not apply to process vents in ethylene oxide service as defined in  $\S$  <u>63.2550</u>.

(i) Outlet concentration correction for combustion devices. Except as specified in paragraph (i)(3) of this section, when  $\S$  <u>63.997(e)(2)(iii)(C)</u> requires you to correct the measured concentration at the outlet of a combustion device to 3-percent oxygen if you add supplemental combustion air, the requirements in either paragraph (i)(1) or (2) of this section apply for the purposes of this subpart.

(1) You must correct the concentration in the gas stream at the outlet of the combustion device to 3 percent oxygen if you add supplemental gases, as defined in  $\S$  63.2550, to the vent stream, or;

(2) You must correct the measured concentration for supplemental gases using Equation 1 in  $\S$  63.2460(c)(6); you may use process knowledge and representative operating data to determine the fraction of the total flow due to supplemental gas.

(3) Beginning no later than the compliance dates specified in  $\S$  63.2445(g), paragraphs (i)(1) and (2) of this section no longer apply. Instead, when  $\S$  63.997(e)(2)(iii)(C) requires you to correct the measured concentration at the outlet of a combustion
device to 3-percent oxygen if you add supplemental combustion air, you must follow the procedures in § <u>63.997(e)(2)(iii)(C)</u> to perform the concentration correction, except you may also use Method 3A of <u>40 CFR part 60</u>, <u>appendix A</u>-2, to determine the oxygen concentration.

(j) Continuous emissions monitoring systems. Each continuous emissions monitoring system (CEMS) must be installed, operated, and maintained according to the requirements in  $\S$  63.8 of subpart A and paragraphs (j)(1) through (6) of this section.

(1) Each CEMS must be installed, operated, and maintained according to the applicable Performance Specification of <u>40</u> <u>CFR part 60, appendix B</u>, and the applicable Quality Assurance Procedures of <u>40 CFR part 60, appendix F</u>, and according to <u>paragraph (j)(2)</u> of this section, except as specified in <u>paragraph (j)(1)(i)</u> of this section. For any CEMS meeting Performance Specification 8 of <u>40 CFR part 60, appendix B</u>, you must also comply with procedure 1 of <u>40 CFR part 60, appendix F</u>. Locate the sampling probe or other interface at a measurement location such that you obtain representative measurements of emissions from the regulated source. For CEMS installed after August 12, 2020, conduct a performance evaluation of each CEMS within 180 days of installation of the monitoring system.

(i) If you wish to use a CEMS other than a Fourier Transform Infrared Spectroscopy (FTIR) meeting the requirements of Performance Specification 15 of <u>40 CFR part 60</u>, <u>appendix B</u>, to measure hydrogen halide, other than hydrogen chloride, and halogen HAP or CEMS meeting the requirements of Performance Specification 18 of <u>40 CFR part 60</u>, <u>appendix B</u>, to measure hydrogen chloride before we promulgate a Performance Specification for such CEMS, you must prepare a monitoring plan and submit it for approval in accordance with the procedures specified in <u>§ 63.8</u> of subpart A.

(ii) [Reserved]

(2) You must determine the calibration gases and reporting units for TOC CEMS in accordance with <u>paragraph (j)(2)(i)</u>, (ii), or (iii) of this section.

(i) For CEMS meeting Performance Specification 9 or 15 requirements, determine the target analyte(s) for calibration using either process knowledge of the control device inlet stream or the screening procedures of Method 18 on the control device inlet stream.

(ii) For CEMS meeting Performance Specification 8 used to monitor performance of a combustion device, calibrate the instrument on the predominant organic HAP and report the results as carbon (C1), and use Method 25A or any approved alternative as the reference method for the relative accuracy tests.

(iii) For CEMS meeting Performance Specification 8 of <u>40 CFR part 60</u>, <u>appendix B</u>, used to monitor performance of a noncombustion device, determine the predominant organic HAP using either process knowledge or the screening procedures of Method 18 of <u>40 CFR part 60</u>, <u>appendix A-6</u>, on the control device inlet stream, calibrate the monitor on the predominant organic HAP, and report the results as  $C_1$ . Use Method 18 of <u>40 CFR part 60</u>, <u>appendix A-6</u>, Method 320 of appendix A to this part, ASTM D6420-18 (incorporated by reference, see § 63.14), or any approved alternative as the reference method for the relative accuracy tests, and report the results as  $C_1$ .

(3) You must conduct a performance evaluation of each CEMS according to the requirements in § 63.8 of subpart A and according to the applicable Performance Specification of  $\frac{40 \text{ CFR part } 60, \text{ appendix B}}{13, 2020}$ , except that the schedule in § 63.8(e)(4) of subpart A does not apply, and before October 13, 2020, the results of the performance evaluation must be included in the notification of compliance status report. Unless otherwise specified in this subpart, beginning on and after October 13, 2020, the results of the performance evaluation must be submitted in accordance with § 63.2520(g).

(4) The CEMS data must be reduced to operating day or operating block averages computed using valid data consistent with the data availability requirements specified in  $\S 63.999(c)(6)(i)(B)$  through (D), except monitoring data also are sufficient to constitute a valid hour of data if measured values are available for at least two of the 15-minute periods during an hour when calibration, quality assurance, or maintenance activities are being performed. An operating block is a period of time from the beginning to end of batch operating within a process. Operating block averages may be used only for batch process vent data. In computing operating day or operating block averages to determine compliance with this subpart, you must exclude monitoring data recorded during CEMS breakdowns, out-of-control periods, repairs, maintenance periods, calibration checks, or other quality assurance activities. Out-of-control periods are as specified in  $\S 63.8(c)(7)$  of subpart A.

(5) If you add supplemental gases, you must comply with <u>paragraphs (j)(5)(i)</u> and <u>(ii)</u> of this section.

(i) Except as specified in <u>paragraph (j)(5)(ii)</u> of this section, correct the measured concentrations in accordance with <u>paragraph (i)</u> of this section and  $\frac{63.2460(c)(6)}{6}$ .

(ii) Beginning no later than the compliance dates specified in § 63.2445(g), you must use Performance Specification 3 of <u>40</u> <u>CFR part 60, appendix B</u>, to certify your oxygen CEMS, and you must comply with procedure 1 of <u>40 CFR part 60, appendix</u> <u>F</u>. Use Method 3A of <u>40 CFR part 60, appendix A</u>-2, as the reference method when conducting a relative accuracy test audit.

(6) Beginning no later than the compliance dates specified in § 63.2445(g), in lieu of the requirements specified in § 63.8(d)(3) of subpart A you must keep the written procedures required by § 63.8(d)(2) of subpart A on record for the life of the affected source or until the affected source is no longer subject to the provisions of this part, to be made available for inspection, upon request, by the Administrator. If the performance evaluation plan is revised, you must keep previous (*i.e.*, superseded) versions of the performance evaluation plan on record to be made available for inspection, upon request, by the Administrator to the plan. The program of corrective action should be included in the plan required under § 63.8(d)(2) of subpart A. In addition to the information required in § 63.8(d)(2) of subpart A, your written procedures for CEMS must include the information in paragraphs (j)(6)(i) through (vi) of this section:

(i) Description of CEMS installation location.

(ii) Description of the monitoring equipment, including the manufacturer and model number for all monitoring equipment components and the span of the analyzer.

(iii) Routine quality control and assurance procedures.

(iv) Conditions that would trigger a CEMS performance evaluation, which must include, at a minimum, a newly installed CEMS; a process change that is expected to affect the performance of the CEMS; and the Administrator's request for a performance evaluation under section 114 of the Clean Air Act.

(v) Ongoing operation and maintenance procedures in accordance with the general requirements of § <u>63.8(c)(1)</u> and (3), (c)(4)(ii), and (c)(7) and (8) of subpart A;

(vi) Ongoing recordkeeping and reporting procedures in accordance with the general requirements of  $\frac{63.10(c)}{2}$  and  $\frac{(e)(1)}{2}$  of subpart A.

(k) Continuous parameter monitoring. The provisions in paragraphs (k)(1) through (8) of this section apply in addition to the requirements for continuous parameter monitoring system (CPMS) in subpart SS of this part.

(1) You must comply with <u>paragraphs (k)(1)(i)</u> and <u>(ii)</u> of this section.

(i) Except as specified in <u>paragraph (k)(1)(ii)</u> of this section, record the results of each calibration check and all maintenance performed on the CPMS as specified in  $\frac{63.998(c)(1)(ii)(A)}{2}$ .

(ii) Beginning no later than the compliance dates specified in  $\S$  63.2445(g), paragraph (k)(1)(i) of this section no longer applies. Instead, you must record the results of each calibration check and all maintenance performed on the CPMS as specified in  $\S$  63.998(c)(1)(ii)(A), except you must record all maintenance, not just preventative maintenance.

(2) When <u>subpart SS of this part 63</u> uses the term "a range" or "operating range" of a monitored parameter, it means an "operating limit" for a monitored parameter for the purposes of this subpart.

(3) As an alternative to continuously measuring and recording pH as specified in  $\frac{\$\$ 63.994(c)(1)(i)}{\$}$  and  $\frac{63.998(a)(2)(ii)(D)}{\$}$ , you may elect to continuously monitor and record the caustic strength of the effluent. For halogen scrubbers used to control only batch process vents you may elect to monitor and record either the pH or the caustic strength of the scrubber effluent at least once per day.

(4) As an alternative to the inlet and outlet temperature monitoring requirements for catalytic incinerators as specified in  $\S$  <u>63.988(c)(2)</u> and the related recordkeeping requirements specified in  $\S$  <u>63.998(a)(2)(ii)(B)(2)</u> and <u>(c)(2)(ii)</u>, you may elect to comply with the requirements specified in <u>paragraphs (k)(4)(i)</u> through <u>(iv)</u> of this section.

(i) Monitor and record the inlet temperature as specified in <u>subpart SS of this part</u> 63.

(ii) Check the activity level of the catalyst at least every 12 months and take any necessary corrective action, such as replacing the catalyst to ensure that the catalyst is performing as designed.

(iii) Maintain records of the annual checks of catalyst activity levels and the subsequent corrective actions.

(iv) Recording the downstream temperature and temperature difference across the catalyst bed as specified in § 63.998(a)(2)(ii)(B)(2) and (c)(2)(ii) is not required.

(5) For absorbers that control organic compounds and use water as the scrubbing fluid, you must conduct monitoring and recordkeeping as specified in <u>paragraphs (k)(5)(i)</u> through (iii) of this section instead of the monitoring and recordkeeping requirements specified in <u> $\frac{88}{63.990(c)(1)}$ </u>, <u> $\frac{63.993(c)(1)}{63.993(c)(1)}$ </u>, and <u> $\frac{63.998(a)(2)(ii)(C)}{63.998(a)(2)(ii)(C)}$ </u>.

(i) You must use a flow meter capable of providing a continuous record of the absorber influent liquid flow.

(ii) You must determine gas stream flow using one of the procedures specified in  $\frac{63.994(c)(1)(ii)(A)}{(D)}$  through (D).

(iii) You must record the absorber liquid-to-gas ratio averaged over the time period of any performance test.

(6) For a control device with total inlet HAP emissions less than 1 tpy, you must establish an operating limit(s) for a parameter(s) that you will measure and record at least once per averaging period (i.e., daily or block) to verify that the control device is operating properly. You may elect to measure the same parameter(s) that is required for control devices that control inlet HAP emissions equal to or greater than 1 tpy. If the parameter will not be measured continuously, you must request approval of your proposed procedure in the precompliance report. You must identify the operating limit(s) and the measurement frequency, and you must provide rationale to support how these measurements demonstrate the control device is operating properly.

(7) Beginning no later than the compliance dates specified in  $\S$  63.2445(g), the manufacturer's specifications or your written procedures must include a schedule for calibrations, preventative maintenance procedures, a schedule for preventative maintenance, and corrective actions to be taken if a calibration fails. If a CPMS calibration fails, the CPMS is considered to be inoperative until you take corrective action and the system passes calibration. You must record the nature and cause of instances when the CPMS is inoperative and the corrective action taken.

(8) You must comply with the requirements in <u>paragraph (e)(4)</u> of this section, as applicable.

(1) *Startup, shutdown, and malfunction*. Sections 63.152(f)(7)(ii) through (iv) and 63.998(b)(2)(iii) and (b)(6)(i)(A), which apply to the exclusion of monitoring data collected during periods of SSM from daily averages, do not apply for the purposes of this subpart.

(m) Reporting.

(1) When  $\frac{\$\$ 63.2455}{63.2455}$  through  $\underline{63.2490}$  reference other subparts in this part 63 that use the term "periodic report," it means "compliance report" for the purposes of this subpart. The compliance report must include the information specified in  $\frac{\$}{63.2520(e)}$ , as well as the information specified in referenced subparts.

(2) When there are conflicts between this subpart and referenced subparts for the due dates of reports required by this subpart, reports must be submitted according to the due dates presented in this subpart.

(3) Excused excursions, as defined in subparts G and SS of this part 63, are not allowed.

(n) [Reserved]

(o) You may not use a flare to control halogenated vent streams or hydrogen halide and halogen HAP emissions.

(p) Original safety device requirements. Except as specified in paragraph (t) of this section, opening a safety device, as defined in  $\frac{63.2550}{50}$ , is allowed at any time conditions require it to avoid unsafe conditions.

(q) If an emission stream contains energetics or organic peroxides that, for safety reasons, cannot meet an applicable emission limit specified in Tables 1 through 7 to this subpart, then you must submit documentation in your precompliance report explaining why an undue safety hazard would be created if the air emission controls were installed, and you must describe the procedures that you will implement to minimize HAP emissions from these vent streams.

(r) Surge control vessels and bottoms receivers. For each surge control vessel or bottoms receiver that meets the capacity and vapor pressure thresholds for a Group 1 storage tank, you must meet emission limits and work practice standards specified in Table 4 to this subpart. Beginning no later than the compliance dates specified in § 63.2445(i), for each surge control vessel and bottoms receiver in ethylene oxide service as defined in § 63.2550, you must also meet the applicable process vent requirements specified in §§ 63.2492 and 63.2493(a) through (c).

(s) For the purposes of determining Group status for continuous process vents, batch process vents, and storage tanks in  $\underline{\$\$}$  <u>63.2455</u>, <u>63.2460</u>, and <u>63.2470</u>, hydrazine is to be considered an organic HAP.

(t) New safety device requirements. Beginning no later than the compliance dates specified in  $\S$  63.2445(g), paragraph (p) of this section no longer applies. Instead, you must comply with the requirements specified in  $\S$  63.2480(e).

(u) *General duty*. Beginning no later than the compliance dates specified in § <u>63.2445(g)</u>, at all times, you must operate and maintain any affected source, including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. The general duty to minimize emissions does not require you to make any further efforts to reduce emissions if levels required by the applicable standard have been achieved. Determination of whether a source is operating in compliance with operation and maintenance requirements will be based on information available to the Administrator which may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.

(v) *Maintenance vents*. Beginning no later than the compliance dates specified in  $\S$  63.2445(g), you may designate a process vent as a maintenance vent if the vent is only used as a result of startup, shutdown, maintenance, or inspection of equipment where equipment is emptied, depressurized, degassed, or placed into service. You must comply with the applicable requirements in paragraphs (v)(1) through (3) of this section for each maintenance vent. Any vent designated as a maintenance vent is only subject to the maintenance vent provisions in this paragraph (v) and the associated recordkeeping and reporting requirements in  $\S$  63.2525(p) and 63.2520(e)(14), respectively. You do not need to designate a maintenance vent as a Group 1 or Group 2 process vent nor identify maintenance vents in a Notification of Compliance Status report.

(1) Prior to venting to the atmosphere, remove process liquids from the equipment as much as practical and depressurize the equipment to either: A flare meeting the requirements of paragraph (e)(2) or (5) of this section, as applicable, or a non-flare control device meeting the requirements in paragraph (e)(4) of this section and the requirements specified in § 63.982(c)(2) of subpart SS until one of the following conditions, as applicable, is met.

(i) The vapor in the equipment served by the maintenance vent has a concentration less than 10 percent of its lower explosive limit (LEL) and has an outlet concentration less than or equal to 20 ppmv hydrogen halide and halogen HAP.

(ii) If there is no ability to measure the concentration of the vapor in the equipment based on the design of the equipment, the pressure in the equipment served by the maintenance vent is reduced to 5 pounds per square inch gauge (psig) or less. Upon opening the maintenance vent, active purging of the equipment cannot be used until the concentration of the vapors in the maintenance vent (or inside the equipment if the maintenance is a hatch or similar type of opening) is less than 10 percent of its LEL.

(iii) The equipment served by the maintenance vent contains less than 50 pounds of total volatile organic compounds (VOC).

(iv) If, after applying best practices to isolate and purge equipment served by a maintenance vent, none of the applicable criterion in <u>paragraphs (v)(1)(i)</u> through (iii) of this section can be met prior to installing or removing a blind flange or similar equipment blind, then the pressure in the equipment served by the maintenance vent must be reduced to 2 psig or less before installing or removing the equipment blind. During installation or removal of the equipment blind, active purging of the equipment may be used provided the equipment pressure at the location where purge gas is introduced remains at 2 psig or less.

(2) Except for maintenance vents complying with the alternative in <u>paragraph (v)(1)(iii)</u> of this section, you must determine the concentration of the vapor or, if applicable, equipment pressure using process instrumentation or portable measurement devices and follow procedures for calibration and maintenance according to manufacturer's specifications.

(3) For maintenance vents complying with the alternative in paragraph (v)(1)(iii) of this section, you must determine mass of VOC in the equipment served by the maintenance vent based on the equipment size and contents after considering any contents drained or purged from the equipment. Equipment size may be determined from equipment design specifications. Equipment contents may be determined using process knowledge.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>70 FR 38559</u>, July 1, 2005; <u>71 FR 40332</u>, July 14, 2006; <u>85 FR 49133</u>, Aug. 12, 2020; <u>89 FR 23868</u>, Apr. 4, 2024]

# § 63.2455 What requirements must I meet for continuous process vents?

(a) You must meet each emission limit in Table 1 to this subpart that applies to your continuous process vents, and you must meet each applicable requirement specified in <u>paragraphs (b)</u> through (c) of this section and  $\frac{\$\$}{63.2492}$  and  $\frac{63.2493(a)}{63.2493(a)}$  through (c).

(b) For each continuous process vent, you must either designate the vent as a Group 1 continuous process vent or determine the total resource effectiveness (TRE) index value as specified in  $\S$  63.115(d), except as specified in paragraphs (b)(1) through (3) of this section.

(1) You are not required to determine the Group status or the TRE index value for any continuous process vent that is combined with Group 1 batch process vents before a control device or recovery device because the requirements of  $\S$  <u>63.2450(c)(2)(i)</u> apply to the combined stream.

(2) When a TRE index value of 4.0 is referred to in  $\S$  63.115(d), TRE index values of 5.0 for existing affected sources and 8.0 for new and reconstructed affected sources apply for the purposes of this subpart.

(3) When  $\S 63.115(d)$  refers to "emission reductions specified in  $\S 63.113(a)$ ," the reductions specified in Table 1 to this subpart apply for the purposes of this subpart.

(c) If you use a recovery device to maintain the TRE above a specified threshold, you must meet the requirements of  $\S$  <u>63.982(e)</u> and the requirements referenced therein, except as specified in  $\S$  <u>63.2450</u> and <u>paragraph (c)(1)</u> of this section.

(1) When  $\frac{63.993}{2}$  uses the phrase "the TRE index value is between the level specified in a referencing subpart and 4.0," the phrase "the TRE index value is >1.9 but  $\leq$ 5.0" applies for an existing affected source, and the phrase "the TRE index value is >5.0 but  $\leq$ 8.0" applies for a new and reconstructed affected source, for the purposes of this subpart.

(2) [Reserved]

[68 FR 63888, Nov. 10, 2003, as amended at 85 FR 49139, Aug. 12, 2020]

#### § 63.2460 What requirements must I meet for batch process vents?

(a) *General.* You must meet each emission limit in Table 2 to this subpart that applies to you, and you must meet each applicable requirement specified in <u>paragraphs (b)</u> and (c) of this section and <u>§§ 63.2492</u> and <u>63.2493(a)</u> through (c).

(b) *Group status*. If a process has batch process vents, as defined in  $\S 63.2550$ , you must determine the group status of the batch process vents by determining and summing the uncontrolled organic HAP emissions from each of the batch process vents within the process using the procedures specified in  $\S 63.1257(d)(2)(i)$  and (ii), except as specified in paragraphs (b)(1) through (7) of this section.

(1) To calculate emissions caused by the heating of a vessel without a process condenser to a temperature lower than the boiling point, you must use the procedures in  $\frac{63.1257(d)(2)(i)(C)(3)}{2}$ .

(2) To calculate emissions from depressurization of a vessel without a process condenser, you must use the procedures in  $\S$  <u>63.1257(d)(2)(i)(D)(10)</u>.

(3) To calculate emissions from vacuum systems for the purposes of this subpart, the receiving vessel is part of the vacuum system, and terms used in Equation 33 to <u>40 CFR part 63</u>, subpart <u>GGG</u>, are defined as follows:

P<sub>system</sub> = absolute pressure of the receiving vessel;

 $P_i$  = partial pressure of the HAP determined at the exit temperature and exit pressure conditions of the condenser or at the conditions of the dedicated receiver;

 $P_j$  = partial pressure of condensables (including HAP) determined at the exit temperature and exit pressure conditions of the condenser or at the conditions of the dedicated receiver;

 $MW_{HAP}$  = molecular weight of the HAP determined at the exit temperature and exit pressure conditions of the condenser or at the conditions of the dedicated receiver.

(4) To calculate uncontrolled emissions when a vessel is equipped with a process condenser, you must use the procedures in  $\frac{63.1257(d)(3)(i)(B)}{(2000)}$ , except as specified in paragraphs (b)(4)(i) through (vii) of this section.

(i) You must determine the flowrate of gas (or volume of gas), partial pressures of condensables, temperature (T), and HAP molecular weight ( $MW_{HAP}$ ) at the exit temperature and exit pressure conditions of the condenser or at the conditions of the dedicated receiver.

(ii) You must assume that all of the components contained in the condenser exit vent stream are in equilibrium with the same components in the exit condensate stream (except for noncondensables).

(iii) You must perform a material balance for each component.

(iv) For the emissions from gas evolution, the term for time, t, must be used in Equation 12 to <u>40 CFR part 63, subpart GGG</u>.

(v) Emissions from empty vessel purging shall be calculated using Equation 36 to <u>40 CFR part 63</u>, <u>subpart GGG</u> and <u>the</u> exit temperature and exit pressure conditions of the condenser or the conditions of the dedicated receiver.

(vi) You must conduct an engineering assessment as specified in  $\S$  63.1257(d)(2)(ii) for each emission episode that is not due to vapor displacement, purging, heating, depressurization, vacuum operations, gas evolution, air drying, or empty vessel purging. The requirements of paragraphs (b)(3) through (4) of this section shall apply.

(vii) You may elect to conduct an engineering assessment if you can demonstrate to the Administrator that the methods in  $\S$  <u>63.1257(d)(3)(i)(B)</u> are not appropriate.

(5) You may elect to designate the batch process vents within a process as Group 1 and not calculate uncontrolled emissions if you comply with one of the situations in paragraph (b)(5)(i), (ii), or (iii) of this section.

(i) If you comply with the alternative standard specified in  $\underline{\$ 63.2505}$ .

(ii) If all Group 1 batch process vents within a process are controlled; you conduct the performance test under hypothetical worst case conditions, as defined in § 63.1257(b)(8)(i)(B); and the emission profile is based on capture and control system limitations as specified in § 63.1257(b)(8)(i)(C).

(iii) If you comply with an emission limit using a flare that meets the requirements specified in  $\S$  63.987 or  $\S$  63.2450(e)(5), as applicable.

(6) You may change from Group 2 to Group 1 in accordance with either <u>paragraph (b)(6)(i)</u> or <u>(ii)</u> of this section. Before October 13, 2020, you must comply with the requirements of this section and submit the test report. Beginning on and after October 13, 2020, you must comply with the requirements of this section and submit the performance test report for the demonstration required in § 63.1257(b)(8) in accordance with § 63.2520(f).

(i) You may switch at any time after operating as Group 2 for at least 1 year so that you can show compliance with the 10,000 pounds per year (lb/yr) threshold for Group 2 batch process vents for at least 365 days before the switch. You may elect to start keeping records of emissions from Group 2 batch process vents before the compliance date. Report a switch based on this provision in your next compliance report in accordance with  $\S$  63.2520(e)(10)(i).

(ii) If the conditions in <u>paragraph (b)(6)(i)</u> of this section are not applicable, you must provide a 60-day advance notice in accordance with  $\frac{63.2520(e)(10)(ii)}{10}$  before switching.

(7) As an alternative to determining the uncontrolled organic HAP emissions as specified in § 63.1257(d)(2)(i) and (ii), you may elect to demonstrate that non-reactive organic HAP are the only HAP used in the process and non-reactive HAP usage in the process is less than 10,000 lb/yr. You must provide data and supporting rationale in your notification of compliance status report explaining why the non-reactive organic HAP usage will be less than 10,000 lb/yr. You must keep records of the non-reactive organic HAP usage as specified in § 63.2525(e)(2) and include information in compliance reports as specified in § 63.2520(e)(5)(iv).

(c) Exceptions to the requirements in subparts SS and <u>WW of this part</u> 63 are specified in <u>paragraphs (c)(1)</u> through (9) of this section.

(1) *Process condensers.* Process condensers, as defined in  $\S$  <u>63.2550(i)</u>, are not considered to be control devices for batch process vents. You must determine whether a condenser is a control device for a batch process vent or a process condenser from which the uncontrolled HAP emissions are evaluated as part of the initial compliance demonstration for each MCPU and report the results with supporting rationale in your notification of compliance status report.

(2) Initial compliance.

(i) To demonstrate initial compliance with a percent reduction emission limit in Table 2 to this subpart, you must compare the sums of the controlled and uncontrolled emissions for the applicable Group 1 batch process vents within the process, and show that the specified reduction is met. This requirement does not apply if you comply with the emission limits of Table 2 to this subpart by using a flare that meets the requirements of  $\frac{8}{53.987}$  or  $\frac{63.2450(e)(5)}{5}$ , as applicable.

(ii) When you conduct a performance test or design evaluation for a non-flare control device used to control emissions from batch process vents, you must establish emission profiles and conduct the test under worst-case conditions according to  $\frac{63.1257(b)(8)}{53.2450(g)(6)}$  instead of under normal operating conditions as specified in  $\frac{63.7(e)(1)}{5}$  of subpart A or the conditions as specified in  $\frac{63.2450(g)(6)}{50.2450(g)(6)}$ . The requirements in  $\frac{63.997(e)(1)(i)}{50.997(e)(1)(i)}$  and (iii) also do not apply for performance tests

conducted to determine compliance with the emission limits for batch process vents. For purposes of this subpart, references in  $\frac{63.997(b)(1)}{5}$  to "methods specified in  $\frac{63.997(c)}{5}$ " include the methods specified in  $\frac{63.1257(b)(8)}{5}$ .

(iii) As an alternative to conducting a performance test or design evaluation to demonstrate initial compliance with a percent reduction requirement for a condenser, you may determine controlled emissions using the procedures specified in  $\S$  <u>63.1257(d)(3)(i)(B)</u> and <u>paragraphs (b)(3)</u> through (4) of this section.

(iv) When  $\frac{63.1257(d)(3)(i)(B)(7)}{60}$  specifies that condenser-controlled emissions from an air dryer must be calculated using Equation 11 of  $\frac{40 \text{ CFR part } 63, \text{ subpart } GGG}{60}$ , with "V equal to the air flow rate," it means "V equal to the dryer outlet gas flow rate," for the purposes of this subpart. Alternatively, you may use Equation 12 of  $\frac{40 \text{ CFR part } 63, \text{ subpart } GGG}{12}$ , with V equal to the dryer inlet air flow rate. Account for time as appropriate in either equation.

(v) If a process condenser is used for boiling operations in which HAP (not as an impurity) is heated to the boiling point, you must demonstrate that it is properly operated according to the procedures specified in  $\underline{\$}$ 

63.1257(d)(2)(i)(C)(4)(ii) and (d)(3)(iii)(B), and the demonstration must occur only during the boiling operation. The reference in § 63.1257(d)(3)(iii)(B) to the alternative standard in § 63.1254(c) means § 63.2505 for the purposes of this subpart. As an alternative to measuring the exhaust gas temperature, as required by § 63.1257(d)(3)(iii)(B), you may elect to measure the liquid temperature in the receiver.

(vi) You must conduct a subsequent performance test or compliance demonstration equivalent to an initial compliance demonstration within 180 days of a change in the worst-case conditions.

(3) *Establishing operating limits*. You must establish operating limits under the conditions required for your initial compliance demonstration, except you may elect to establish operating limit(s) for conditions other than those under which a performance test was conducted as specified in paragraph (c)(3)(i) of this section and, if applicable, paragraph (c)(3)(ii) of this section.

(i) The operating limits may be based on the results of the performance test and supplementary information such as engineering assessments and manufacturer's recommendations. These limits may be established for conditions as unique as individual emission episodes for a batch process. You must provide rationale in the precompliance report for the specific level for each operating limit, including any data and calculations used to develop the limit and a description of why the limit indicates proper operation of the control device. The procedures provided in this paragraph (c)(3)(i) have not been approved by the Administrator and determination of the operating limit using these procedures is subject to review and approval by the Administrator.

(ii) If you elect to establish separate monitoring levels for different emission episodes within a batch process, you must maintain records in your daily schedule or log of processes indicating each point at which you change from one operating limit to another, even if the duration of the monitoring for an operating limit is less than 15 minutes. You must maintain a daily schedule or log of processes according to  $\frac{§ 63.2525(c)}{2}$ .

(4) Averaging periods. As an alternative to the requirement for daily averages in  $\frac{63.998(b)(3)}{5}$ , you may determine averages for operating blocks. An operating block is a period of time that is equal to the time from the beginning to end of batch process operations within a process.

(5) [Reserved]

(6) Outlet concentration correction for supplemental gases. If you use a control device other than a combustion device to comply with a TOC, organic HAP, or hydrogen halide and halogen HAP outlet concentration emission limit for batch process vents, you must correct the actual concentration for supplemental gases using Equation 1 to this paragraph (e)(6); you may use process knowledge and representative operating data to determine the fraction of the total flow due to supplemental gas.

$$C_{a} = C_{m} \left( \frac{Q_{a} + Q_{a}}{Q_{a}} \right) \quad (Eq. 1)$$

Where:

C<sub>a</sub> = corrected outlet TOC, organic HAP, or hydrogen halide and halogen HAP concentration, dry basis, ppmv;

 $C_m$  = actual TOC, organic HAP, or hydrogen halide and halogen HAP concentration measured at control device outlet, dry basis, ppmv;

Q<sub>a</sub> = total volumetric flowrate of all gas streams vented to the control device, except supplemental gases;

 $Q_s$  = total volumetric flowrate of supplemental gases.

(7) If flow to a control device could be intermittent, you must install, calibrate, and operate a flow indicator at the inlet or outlet of the control device to identify periods of no flow. Periods of no flow may not be used in daily or block averages, and it may not be used in fulfilling a minimum data availability requirement.

(8) *Terminology*. When the term "storage vessel" is used in <u>subpart WW of this part</u> 63, the term "process tank," as defined in <u>§ 63.2550(i)</u>, applies for the purposes of this section.

(9) Requirements for a biofilter. If you use a biofilter to meet either the 95-percent reduction requirement or outlet concentration requirement specified in Table 2 to this subpart, you must meet the requirements specified in paragraphs (c)(9)(i) through (iv) of this section.

(i) Operational requirements. The biofilter must be operated at all times when emissions are vented to it.

(A) Keep up-to-date, readily accessible continuous records of either the biofilter bed temperature averaged over the full period of the performance test or the outlet total organic HAP or TOC concentration averaged over the full period of the performance test. Include these data in your notification of compliance status report as required by  $\frac{63.999(b)(3)(ii)}{50.999(b)(3)(ii)}$ .

(B) Record either the percent reduction of total organic HAP achieved by the biofilter determined as specified in § 63.997(e)(2)(iv) or the concentration of TOC or total organic HAP determined as specified in § 63.997(e)(2)(iii) at the outlet of the biofilter, as applicable.

(C) If you monitor the biofilter bed temperature, you may elect to use multiple thermocouples in representative locations throughout the biofilter bed and calculate the average biofilter bed temperature across these thermocouples prior to reducing the temperature data to 15 minute (or shorter) averages for purposes of establishing operating limits for the biofilter. If you use multiple thermocouples, include your rationale for their site selection in your notification of compliance status report.

(D) Before October 13, 2020, submit a performance test report as specified in  $\S$  <u>63.999(a)(2)(i)</u> and <u>(ii)</u> and include the records from <u>paragraph (c)(9)(ii)(B)</u> of this section. Beginning on and after October 13, 2020, you must submit a performance test report as specified in  $\S$  <u>63.2520(f)</u>.

(iii) Monitoring requirements. Use either a biofilter bed temperature monitoring device (or multiple devices) capable of providing a continuous record or an organic monitoring device capable of providing a continuous record. Comply with the requirements in  $\S$  63.2450(e)(4), the general requirements for monitoring in  $\S$  63.996, and keep records of temperature or other parameter monitoring results as specified in  $\S$  63.998(b) and (c), as applicable. If you monitor temperature, the operating temperature range must be based on only the temperatures measured during the performance test; these data may not be supplemented by engineering assessments or manufacturer's recommendations as otherwise allowed in  $\S$  63.999(b)(3)(ii)(A). If you establish the operating range (minimum and maximum temperatures) using data from previous performance tests in accordance with  $\S$  63.996(c)(6), replacement of the biofilter media with the same type of media is not considered a process change under  $\S$  63.997(b)(1). You may expand your biofilter bed temperature operating range by conducting a repeat performance test that demonstrates compliance with the 95-percent reduction requirement or outlet concentration limit, as applicable.

(iv) *Repeat performance tests*. You must conduct a repeat performance test using the applicable methods specified in  $\frac{\$\$}{63.2450(g)}$  and  $\frac{63.997}{63.2450(g)}$  within 2 years following the previous performance test and within 150 days after each replacement of any portion of the biofilter bed media with a different type of media or each replacement of more than 50 percent (by volume) of the biofilter bed media with the same type of media.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>70 FR 38559</u>, July 1, 2005; <u>71 FR 40333</u>, July 14, 2006; <u>85 FR 49139</u>, Aug. 12, 2020; <u>89 FR 23868</u>, Apr. 4, 2024]

# § 63.2465 What requirements must I meet for process vents that emit hydrogen halide and halogen HAP or HAP metals?

(a) You must meet each emission limit in Table 3 to this subpart that applies to you, and you must meet each applicable requirement in <u>paragraphs (b)</u> through (d) of this section.

(b) If any process vents within a process emit hydrogen halide and halogen HAP, you must determine and sum the uncontrolled hydrogen halide and halogen HAP emissions from each of the process vents within the process using the procedures specified in  $\S 63.1257(d)(2)(i)$  and/or (ii), as appropriate. When  $\S 63.1257(d)(2)(i)(E)$  requires documentation to be submitted in the precompliance report, it means the notification of compliance status report for the purposes of this paragraph.

(c) If collective uncontrolled hydrogen halide and halogen HAP emissions from the process vents within a process are greater than or equal to 1,000 pounds per year (lb/yr), you must comply with the requirements in  $\frac{63.2450(e)(4)}{63.994}$  and the requirements referenced therein, except as specified in <u>paragraphs (c)(1)</u> through (3) of this section.

(1) When  $\S 63.994(b)(1)$  requires a performance test, you may elect to conduct a design evaluation in accordance with  $\S 63.1257(a)(1)$ .

(2) When  $\frac{63.994(b)(1)}{10}$  refers to "a combustion device followed by a halogen scrubber or other halogen reduction device," it means any combination of control devices used to meet the emission limits specified in Table 3 to this subpart.

(3) Section 63.994(b)(2) does not apply for the purposes of this section.

(d) To demonstrate compliance with the emission limit in Table 3 to this subpart for HAP metals at a new source, you must comply with <u>paragraphs (d)(1)</u> through (3) of this section.

(1) Determine the mass emission rate of HAP metals based on process knowledge, engineering assessment, or test data.

(2) Conduct an initial performance test of each control device that is used to comply with the emission limit for HAP metals specified in Table 3 to this subpart. Conduct the performance test according to the procedures in  $\frac{§§}{63.2450(g)}$  and  $\frac{63.997}{63.997}$ . Use Method 29 of  $\frac{40 \text{ CFR part } 60}{40 \text{ CFR part } 60}$ , appendix A, to determine the HAP metals at the inlet and outlet of each control device, or use Method 5 of  $\frac{40 \text{ CFR part } 60}{40 \text{ cFR part } 60}$ , appendix A, to determine the total particulate matter (PM) at the inlet and outlet of each control device. You may use ASTM D6784-02 (Reapproved 2008) (incorporated by reference, see  $\frac{§}{63.14}$ ) as an alternative to Method 29 (portion for mercury only) as a method for measuring mercury concentrations of 0.5 to 100 micrograms per standard cubic meter. You have demonstrated initial compliance if the overall reduction of either HAP metals or total PM from the process is greater than or equal to 97 percent by weight.

(3) Comply with the monitoring requirements specified in  $\frac{63.1366(b)(1)(xi)}{63.1366(b)(1)(xi)}$  for each fabric filter used to control HAP metals.

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40334, July 14, 2006; 85 FR 49140, Aug. 12, 2020]

#### § 63.2470 What requirements must I meet for storage tanks?

(a) *General.* You must meet each emission limit in Table 4 to this subpart that applies to your storage tanks, and except as specified in <u>paragraph (b)</u> of this section, you must also meet each applicable requirement specified in <u>paragraphs</u> (c) through (f) of this section and  $\frac{88}{63.2492}$  and  $\frac{63.2493(a)}{63.2493(a)}$  through (c).

(b) General for storage tanks in ethylene oxide service. On and after the compliance dates specified in § 63.2445(i), paragraphs (d) and (e) of this section do not apply to storage tanks in ethylene oxide service as defined in § 63.2550.

(c) Exceptions to subparts SS and WW of this part.

(1) Except as specified in paragraph (c)(4)(ii) of this section, if you conduct a performance test or design evaluation for a control device used to control emissions only from storage tanks, you must establish operating limits, conduct monitoring, and keep records using the same procedures as required in <u>subpart SS of this part</u> for control devices used to reduce emissions from process vents instead of the procedures specified in <u>§§ 63.985(c)</u>, <u>63.998(d)(2)(i)</u>, and <u>63.999(b)(2)</u>. You must also comply with the requirements in § <u>63.2450(e)(4)</u>, as applicable.

(2) Except as specified in <u>paragraph (c)(4)</u> of this section, when the term "storage vessel" is used in <u>subparts SS</u> and <u>WW of</u> this part, the term "storage tank," as defined in <u>§ 63.2550</u> applies for the purposes of this subpart.

(3) For adsorbers that cannot be regenerated or regenerative adsorbers that are regenerated offsite, you must comply with the monitoring requirements in  $\frac{63.2450(e)(7)}{10}$  in lieu of  $\frac{63.995(c)}{10}$ .

(4) Beginning no later than the compliance dates specified in § 63.2445(i), you must comply with paragraphs (c)(4)(i) and (ii) of this section.

(i) The exemptions for "vessels storing organic liquids that contain HAP only as impurities" and "pressure vessels designed to operate in excess of 204.9 kilopascals and without emissions to the atmosphere" listed in the definition of "storage tank" in  $\frac{63.2550}{100}$  do not apply for storage tanks in ethylene oxide service.

(ii) For storage tanks in ethylene oxide service as defined in  $\S$  <u>63.2550</u>, you may not use a design evaluation to determine the percent reduction of any control device that is used to comply with an emission limit specified in Table 4 to this subpart.

(d) *Planned routine maintenance*. The emission limits in Table 4 to this subpart for control devices used to control emissions from storage tanks do not apply during periods of planned routine maintenance. Periods of planned routine maintenance of each control device, during which the control device does not meet the emission limit specified in Table 4 to this subpart, must not exceed 240 hours per year (hr/yr). You may submit an application to the Administrator requesting an extension of this time limit to a total of 360 hr/yr. The application must explain why the extension is needed, it must indicate that no material will be added to the storage tank between the time the 240-hr limit is exceeded and the control device is again operational, and it must be submitted at least 60 days before the 240-hr limit will be exceeded.

(e) *Vapor balancing alternative*. As an alternative to the emission limits specified in Table 4 to this subpart, you may elect to implement vapor balancing in accordance with  $\S$  63.1253(f), except as specified in paragraphs (e)(1) through (3) of this section.

(1) When <u>§ 63.1253(f)(6)(i)</u> refers to a 90 percent reduction, 95 percent applies for the purposes of this subpart.

(2) To comply with  $\S 63.1253(f)(6)(i)$ , the owner or operator of an offsite cleaning or reloading facility must comply with  $\S 63.2445$  through 63.2550 instead of complying with  $\S 63.1253(f)(7)(ii)$ , except as specified in paragraph (e)(2)(i) or (ii) of this section.

(i) The reporting requirements in  $\frac{63.2520}{2}$  do not apply to the owner or operator of the offsite cleaning or reloading facility.

(ii) As an alternative to complying with the monitoring, recordkeeping, and reporting provisions in  $\frac{\$\$}{63.2445}$  through  $\frac{63.2550}{63.2535(a)(2)}$ , the owner or operator of an offsite cleaning or reloading facility may comply as specified in  $\frac{\$}{63.2535(a)(2)}$  with any other subpart of this part 63 which has monitoring, recordkeeping, and reporting provisions as specified in  $\frac{\$}{63.2535(a)(2)}$ .

(3) You may elect to set a pressure relief device to a value less than the 2.5 psig required in § 63.1253(f)(5) if you provide rationale in your notification of compliance status report explaining why the alternative value is sufficient to prevent breathing losses at all times.

(4) You may comply with the vapor balancing alternative in  $\S 63.1253(f)$  when your storage tank is filled from a barge. All requirements for tank trucks and railcars specified in  $\S 63.1253(f)$  also apply to barges, except as specified in  $\S 63.2470(e)(4)(i)$ .

(i) When  $\frac{63.1253(f)(2)}{2}$  refers to pressure testing certifications, the requirements in  $\frac{40 \text{ CFR } 61.304(f)}{2}$  apply for barges.

(ii) [Reserved]

(f) Storage tank degassing. Beginning no later than the compliance dates specified in  $\S$  63.2445(g), for each storage tank subject to item 1 of Table 4 to this subpart, you must comply with paragraphs (f)(1) through (4) of this section during storage tank shutdown operations (*i.e.*, emptying and degassing of a storage tank) until the vapor space concentration in the storage tank is less than 10 percent of the LEL. You must determine the concentration using process instrumentation or portable measurement devices and follow procedures for calibration and maintenance according to manufacturer's specifications.

(1) Remove liquids from the storage tank as much as practicable.

(2) Comply with one of the following:

(i) Reduce emissions of total organic HAP by venting emissions through a closed vent system to a flare.

(ii) Reduce emissions of total organic HAP by 95 weight-percent by venting emissions through a closed vent system to any combination of non-flare control devices.

(iii) Reduce emissions of total organic HAP by routing emissions to a fuel gas system or process and meet the requirements specified in  $\frac{63.982(d)}{10}$  and the applicable requirements in  $\frac{63.2450(e)(4)}{10}$ .

(3) Maintain records necessary to demonstrate compliance with the requirements in  $\S$  <u>63.2450(u)</u> including, if appropriate, records of existing standard site procedures used to empty and degas (deinventory) equipment for safety purposes.

(4) For floating roof storage tanks, the storage tank may be opened to set up equipment (e.g., making connections to a temporary control device) for the shutdown operations but must not be actively degassed during this time period.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>70 FR 38559</u>, July 1, 2005; <u>71 FR 40335</u>, July 14, 2006; <u>85 FR 49140</u>, Aug. 12, 2020; <u>89 FR 23868</u>, Apr. 4, 2024]

#### § 63.2475 What requirements must I meet for transfer racks?

(a) You must comply with each emission limit and work practice standard in Table 5 to this subpart that applies to your transfer racks, and you must meet each applicable requirement in <u>paragraph (b)</u> of this section.

(b) When the term "high throughput transfer rack" is used in <u>subpart SS of this part</u> 63, the term "Group 1 transfer rack," as defined in  $\S$  63.2550, applies for the purposes of this subpart.

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40335, July 14, 2006; 85 FR 49141, Aug. 12, 2020]

#### § 63.2480 What requirements must I meet for equipment leaks?

(a) You must meet each requirement in table 6 to this subpart that applies to your equipment leaks, except as specified in <u>paragraphs (b)</u> through (f) of this section. For each light liquid pump, pressure relief device, and connector in ethylene oxide service as defined in § 63.2550(i), you must also meet the applicable requirements specified in §§ 63.2492 and 63.2493(d) and (e).

(b) Except as specified in <u>paragraphs (b)(6)</u> and (7) of this section, if you comply with either <u>subpart H</u> or <u>UU of this part</u>, you may elect to comply with the provisions in <u>paragraphs (b)(1)</u> through (5) of this section as an alternative to the referenced provisions in <u>subpart H</u> or <u>UU of this part</u>.

(1) The requirements for pressure testing in  $\S 63.178(b)$  or  $\S 63.1036(b)$  may be applied to all processes, not just batch processes.

(2) For the purposes of this subpart, pressure testing for leaks in accordance with  $\frac{63.178(b)}{5.178(b)}$  or  $\frac{63.1036(b)}{5.100}$  is not required after reconfiguration of an equipment train if flexible hose connections are the only disturbed equipment.

(3) For an existing source, you are not required to develop an initial list of identification numbers for connectors as would otherwise be required under  $\frac{63.1022(b)(1)}{5.000}$  or  $\frac{63.181(b)(1)(i)}{5.0000}$ .

(4) For connectors in gas/vapor and light liquid service at an existing source, you may elect to comply with the requirements in  $\frac{63.169}{63.1029}$  for connectors in heavy liquid service, including all associated recordkeeping and reporting requirements, rather than the requirements of  $\frac{63.174}{63.1027}$  or  $\frac{63.1027}{63.1027}$ .

(5) Except as specified in <u>paragraph (b)(6)</u> of this section, for pumps in light liquid service in an MCPU that has no continuous process vents and is part of an existing source, you may elect to consider the leak definition that defines a leak to be 10,000 parts per million (ppm) or greater as an alternative to the values specified in  $\frac{63.1026(b)(2)(i)}{63.163(b)(2)}$ .

(6) Beginning no later than the compliance dates specified in § 63.2445(h), paragraph (b)(5) of this section no longer applies.

(7) For each piece of equipment that is subject to Table 6 to this subpart and is also subject to periodic monitoring with EPA Method 21 of  $\frac{40 \text{ CFR part 60, appendix A}}{12, 2020}$ , and is added to an affected source after December 17, 2019, or replaces equipment at an affected source after December 17, 2019, you must initially monitor for leaks within 30 days after August 12, 2020, or initial startup of the equipment, whichever is later. Equipment that is designated as unsafe- or difficult-to-monitor is not subject to this paragraph (b)(7).

(c) Except as specified in <u>paragraphs (c)(10)</u> and <u>(11)</u> of this section, if you comply with <u>40 CFR part 65</u>, <u>subpart F</u>, you may elect to comply with the provisions in <u>paragraphs (c)(1)</u> through <u>(9)</u> of this section as an alternative to the referenced provisions in <u>40 CFR part 65</u>, <u>subpart F</u>.

(1) The requirements for pressure testing in  $\S 65.117(b)$  may be applied to all processes, not just batch processes.

(2) For the purposes of this subpart, pressure testing for leaks in accordance with  $\frac{65.117(b)}{5.117(b)}$  is not required after reconfiguration of an equipment train if flexible hose connections are the only disturbed equipment.

(3) For an existing source, you are not required to develop an initial list of identification numbers for connectors as would otherwise be required under  $\frac{65.103(b)(1)}{2}$ .

(4) You may elect to comply with the monitoring and repair requirements specified in § 65.108(e)(3) as an alternative to the requirements specified in § 65.108(a) through (d) for any connectors at your affected source.

(5) Except as specified in <u>paragraph (c)(10)</u> of this section, for pumps in light liquid service in an MCPU that has no continuous process vents and is part of an existing source, you may elect to consider the leak definition that defines a leak to be 10,000 ppm or greater as an alternative to the values specified in  $\S$  65.107(b)(2)(i) through (iii) of this chapter.

(6) When  $\frac{40 \text{ CFR part 65, subpart F}}{63.2445}$  refers to the implementation date specified in §  $\frac{65.1(f)}{63.2445}$ .

(7) When <u>§§ 65.105(f)</u> and <u>65.117(d)(3)</u> refer to <u>§ 65.4</u>, it means <u>§ 63.2525</u>.

(8) When  $\S 65.120(a)$  refers to  $\S 65.5(d)$ , it means  $\S 63.2515$ .

(9) When  $\S 65.120(b)$  refers to  $\S 65.5(e)$ , it means  $\S 63.2520$ .

(10) Beginning no later than the compliance dates specified in  $\S$  63.2445(h), paragraph (c)(5) of this section no longer applies.

(11) For each piece of equipment that is subject to Table 6 to this subpart and is also subject to periodic monitoring with EPA Method 21 of <u>40 CFR part 60, appendix A</u>-7, and is added to an affected source after December 17, 2019, or replaces equipment at an affected source after December 17, 2019, you must initially monitor for leaks within 30 days after August 12, 2020, or initial startup of the equipment, whichever is later. Equipment that is designated as unsafe- or difficult-to-monitor is not subject to this <u>paragraph (c)(11)</u>.

(d) The provisions of this section do not apply to bench-scale processes, regardless of whether the processes are located at the same plant site as a process subject to the provisions of this subpart.

(e) Beginning no later than the compliance dates specified in § 63.2445(g), except as specified in paragraph (e)(4) of this section, you must comply with the requirements specified in paragraphs (e)(1) and (2) of this section for pressure relief devices, such as relief valves or rupture disks, in organic HAP gas or vapor service instead of the pressure relief device requirements of § 63.1030 of subpart UU, § 63.165 of subpart H, or § 65.111 of this chapter. Except as specified in paragraphs (e)(4) and (5) of this section, you must also comply with the requirements specified in paragraphs (e)(3), (6), (7), and (8) of this section for all pressure relief devices in organic HAP service.

(1) Operating requirements. Except during a pressure release, operate each pressure relief device in organic HAP gas or vapor service with an instrument reading of less than 500 ppm above background as measured by the method in § 63.1023(b) of subpart UU, § 63.180(c) of subpart H, or § 65.104(b) of this chapter.

(2) Pressure release requirements. For pressure relief devices in organic HAP gas or vapor service, you must comply with the applicable requirements paragraphs (e)(2)(i) through (iii) of this section following a pressure release.

(i) If the pressure relief device does not consist of or include a rupture disk, conduct instrument monitoring, as specified in  $\S$  <u>63.1023(b)</u> of subpart UU,  $\S$  <u>63.180(c)</u> of subpart H, or  $\S$  <u>65.104(b)</u> of this chapter, no later than 5 calendar days after the pressure relief device returns to organic HAP gas or vapor service following a pressure release to verify that the pressure relief device is operating with an instrument reading of less than 500 ppm.

(ii) If the pressure relief device includes a rupture disk, either comply with the requirements in <u>paragraph (e)(2)(i)</u> of this section (and do not replace the rupture disk) or install a replacement disk as soon as practicable after a pressure release, but no later than 5 calendar days after the pressure release.

(iii) If the pressure relief device consists only of a rupture disk, install a replacement disk as soon as practicable after a pressure release, but no later than 5 calendar days after the pressure release. You must not initiate startup of the equipment served by the rupture disk until the rupture disc is replaced.

(3) *Pressure release management*. Except as specified in <u>paragraphs (e)(4)</u> and (5) of this section, you must comply with the requirements specified in <u>paragraphs (e)(3)(i)</u> through (v) of this section for all pressure relief devices in organic HAP service.

(i) You must equip each affected pressure relief device with a device(s) or use a monitoring system that is capable of:

(A) Identifying the pressure release;

(B) Recording the time and duration of each pressure release; and

(C) Notifying operators immediately that a pressure release is occurring. The device or monitoring system must be either specific to the pressure relief device itself or must be associated with the process system or piping, sufficient to indicate a pressure release to the atmosphere. Examples of these types of devices and systems include, but are not limited to, a rupture disk indicator, magnetic sensor, motion detector on the pressure relief valve stem, flow monitor, or pressure monitor.

(ii) You must apply at least three redundant prevention measures to each affected pressure relief device and document these measures. Examples of prevention measures include:

(A) Flow, temperature, liquid level and pressure indicators with deadman switches, monitors, or automatic actuators. Independent, non-duplicative systems within this category count as separate redundant prevention measures.

(B) Documented routine inspection and maintenance programs and/or operator training (maintenance programs and operator training may count as only one redundant prevention measure).

(C) Inherently safer designs or safety instrumentation systems.

(D) Deluge systems.

(E) Staged relief system where the initial pressure relief device (with lower set release pressure) discharges to a flare or other closed vent system and control device.

(iii) If any affected pressure relief device releases to atmosphere as a result of a pressure release event, you must perform root cause analysis and corrective action analysis according to the requirement in <u>paragraph (e)(6)</u> of this section and implement corrective actions according to the requirements in <u>paragraph (e)(7)</u> of this section. You must also calculate the quantity of organic HAP released during each pressure release event and report this quantity as required in § 63.2520(e)(15). Calculations may be based on data from the pressure relief device monitoring alone or in combination with process parameter monitoring data and process knowledge.

(iv) You must determine the total number of release events that occurred during the calendar year for each affected pressure relief device separately. Prior to June 3, 2024, you must also determine the total number of release events for each pressure relief device for which the root cause analysis concluded that the root cause was a *force majeure* event, as defined in § 63.2550.

(v) Except for pressure relief devices described in <u>paragraphs (e)(4)</u> and (5) of this section, the following release events from an affected pressure relief device are a deviation of the pressure release management work practice standards.

(A) Any release event for which the root cause of the event was determined to be operator error or poor maintenance.

(B) Prior to June 3, 2024, a second release event not including force majeure events from a single pressure relief device in a 3 calendar year period for the same root cause for the same equipment. On and after June 3, 2024, a second release event from a single pressure relief device in a 3 calendar year period for the same root cause for the same root cause for the same equipment.

(C) Prior to June 3, 2024, a third release event not including force majeure events from a single pressure relief device in a 3 calendar year period for any reason. On and after June 3, 2024, a third release event from a single pressure relief device in a 3 calendar year period for any reason.

(4) Pressure relief devices routed to a control device, process, fuel gas system, or drain system.

(i) If all releases and potential leaks from a pressure relief device are routed through a closed vent system to a control device, back into the process, to the fuel gas system, or to a drain system, then you are not required to comply with <u>paragraph</u> (e)(1), (2), or (3) of this section.

(ii) Before the compliance dates specified in  $\frac{63.2445(g)}{63.2445(g)}$ , both the closed vent system and control device (if applicable) referenced in <u>paragraph (e)(4)(i)</u> of this section must meet the applicable requirements specified in  $\frac{63.982(b)}{63.982(c)}$  and  $\frac{(c)(2)}{2}$  of subpart SS. Beginning no later than the compliance dates specified in  $\frac{63.2445(g)}{63.982(c)(2)}$ , both the closed vent system and control device (if applicable) referenced in <u>paragraph (e)(4)(i)</u> of this section must meet the applicable requirements specified in  $\frac{863.982(b)}{63.982(c)(2)}$ ,  $\frac{63.983}{63.2450(e)(4)}$  through (<u>6</u>).

(iii) The drain system (if applicable) referenced in paragraph (e)(4)(i) must meet the applicable requirements specified in  $\S$  <u>63.2485(e)</u>.

(5) *Pressure relief devices exempted from pressure release management requirements.* The following types of pressure relief devices are not subject to the pressure release management requirements in <u>paragraph (e)(3)</u> of this section.

(i) Pressure relief devices in heavy liquid service, as defined in § 63.1020 of subpart UU or § 65.103(f) of this chapter.

(ii) Thermal expansion relief valves.

(iii) Pressure relief devices on mobile equipment.

(iv) Pilot-operated pressure relief devices where the primary release valve is routed through a closed vent system to a control device or back into the process, to the fuel gas system, or to a drain system.

(v) Balanced bellows pressure relief devices where the primary release valve is routed through a closed vent system to a control device or back into the process, to the fuel gas system, or to a drain system.

(6) Root cause analysis and corrective action analysis. A root cause analysis and corrective action analysis must be completed as soon as possible, but no later than 45 days after a release event. Special circumstances affecting the number of root cause analyses and/or corrective action analyses are provided in paragraphs (e)(6)(i) through (iii) of this section.

(i) You may conduct a single root cause analysis and corrective action analysis for a single emergency event that causes two or more pressure relief devices installed on the same equipment to release.

(ii) Prior to June 3, 2024, you may conduct a single root cause analysis and corrective action analysis for a single emergency event that causes two or more pressure relief devices to release, regardless of the equipment served, if the root cause is reasonably expected to be a *force majeure* event, as defined in  $\frac{\& 63.2550}{\& 1.2550}$ .

(iii) Except as provided in <u>paragraphs (e)(6)(i)</u> and <u>(ii)</u> of this section, if more than one pressure relief device has a release during the same time period, an initial root cause analysis must be conducted separately for each pressure relief device that had a release. If the initial root cause analysis indicates that the release events have the same root cause(s), the initially separate root cause analyses may be recorded as a single root cause analysis and a single corrective action analysis may be conducted.

(7) Corrective action implementation. You must conduct a root cause analysis and corrective action analysis as specified in paragraphs (e)(3)(iii) and (e)(6) of this section, and you must implement the corrective action(s) identified in the corrective action analysis in accordance with the applicable requirements in paragraphs (e)(7)(i) through (iii) of this section.

(i) All corrective action(s) must be implemented within 45 days of the event for which the root cause and corrective action analyses were required or as soon thereafter as practicable. If you conclude that no corrective action should be implemented, you must record and explain the basis for that conclusion no later than 45 days following the event.

(ii) For corrective actions that cannot be fully implemented within 45 days following the event for which the root cause and corrective action analyses were required, you must develop an implementation schedule to complete the corrective action(s) as soon as practicable.

(iii) No later than 45 days following the event for which a root cause and corrective action analyses were required, you must record the corrective action(s) completed to date, and, for action(s) not already completed, a schedule for implementation, including proposed commencement and completion dates.

(8) Flowing pilot-operated pressure relief devices. For affected sources that commenced construction or reconstruction on or before December 17, 2019, you are prohibited from installing a flowing pilot-operated pressure relief device or replacing any

pressure relief device with a flowing pilot-operated pressure relief device after August 12, 2023. For affected sources that commenced construction or reconstruction after December 17, 2019, you are prohibited from installing and operating flowing pilot-operated pressure relief devices. For purpose of compliance with this <u>paragraph (e)(8)</u>, a flowing pilot-operated pressure relief device where the pilot discharge vent continuously releases emissions to the atmosphere when the pressure relief device is actuated.

(f) Beginning no later than the compliance dates specified in  $\frac{63.2445(g)}{10}$ , the referenced provisions specified in <u>paragraphs</u> (f)(1) through (18) of this section do not apply when demonstrating compliance with this section.

- (1) Section 63.163(c)(3) of subpart H.
- (2) Section 63.172(j)(3) of subpart H.
- (3) The second sentence of  $\S 63.181(d)(5)(i)$  of subpart H.

(4) The phrase "may be included as part of the startup, shutdown, and malfunction plan, as required by the referencing subpart for the source, or" from  $\frac{63.1024(f)(4)(i)}{1000}$  of subpart UU.

- (5) Section 63.1026(b)(3) of subpart UU.
- (6) The phrase "(except periods of startup, shutdown, or malfunction)" from  $\frac{63.1026(e)(1)(ii)(A)}{63.1026(e)(1)(ii)(A)}$  of subpart UU.
- (7) The phrase "(except during periods of startup, shutdown, or malfunction)" from  $\frac{63.1028(e)(1)(i)(A)}{100}$  of subpart UU.
- (8) The phrase "(except during periods of startup, shutdown, or malfunction)" from § 63.1031(b)(1) of subpart UU.
- (9) The second sentence of  $\S 65.105(f)(4)(i)$  of this chapter.
- (10) Section 65.107(b)(3) of this chapter.
- (11) The phrase "(except periods of start-up, shutdown, or malfunction)" from § 65.107(e)(1)(ii)(A) of this chapter.
- (12) The phrase "(except during periods of start-up, shutdown, or malfunction)" from <u>§ 65.109(e)(1)(i)(A) of this chapter</u>.
- (13) The phrase "(except during periods of start-up, shutdown, or malfunction)" from  $\S 65.112(b)(1)$  of this chapter.
- (14) The last sentence of  $\S 65.115(b)(1)$  of this chapter.
- (15) The last sentence of § 65.115(b)(2) of this chapter.

(16) The phrase "Except for pressure relief devices needed for safety purposes, low leg drains, high point bleeds, analyzer vents, and open-ended valves or lines" in  $\frac{65.143(a)(3)}{65.143(a)(3)}$  of this chapter.

- (17) For flares complying with  $\S$  63.2450(e)(5), the following provisions do not apply:
- (i) Section 63.172(d) of subpart H;
- (ii) Section 63.180(e) of subpart H;
- (iii) Section 63.181(g)(1)(iii) of subpart H;
- (iv) The phrase "including periods when a flare pilot light system does not have a flame" from  $\frac{63.181(g)(2)(i)}{10}$  of subpart H;
- (v) Section 63.1034(b)(2)(iii) of subpart UU; and
- (vi) Section 65.115(b)(2) of this chapter.
- (18) For pressure relief devices complying with  $\frac{63.2480(e)}{2}$ , the following provisions are modified as follows:
- (i) In the introductory text of  $\S 63.180(c)$ , replace the reference to  $\S 63.165(a)$  with  $\S 63.2480(e)(1)$ .
- (ii) In (63.181(b)(2)(i)), replace the reference to (63.165(c)) with (63.2480(c)(4)).
- (iii) In  $\S 63.181(b)(3)(i)$ , replace the reference to  $\S 63.165(a)$  with  $\S 63.2480(e)(1)$ .
- (iv) In  $\S 63.181(b)(3)(ii)$ , replace the reference to  $\S 63.165(d)$  with  $\S 63.2480(e)(2)(ii)$  and (iii).
- (v) In § 63.181(f), replace the reference to § 63.165(a) and (b) with § 63.2480(e)(1) and (2).

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(vi) The information in § 63.165(a) required to be reported under § 63.182(d)(2)(xiv) is now required to be reported under § 63.2520(e)(15)(i) through (iii).

(vii) The reference to  $\S 63.1030(b)$  in  $\S 63.1021(a)$  no longer applies.

(viii) In  $\S 63.1022(b)(2)$ , replace the reference to  $\S 63.1030(d)$  with  $\S 63.2480(e)(4)$ .

(ix) In § 63.1022(b)(3), replace the reference to § 63.1030(e) with § 63.2480(e)(2)(ii).

(x) The reference to  $\frac{63.1030(c)}{100}$  in  $\frac{63.1023(a)(1)(v)}{100}$  no longer applies. Instead comply with the  $\frac{63.2480(e)(1)}{100}$  and  $\frac{(2)}{100}$ .

(xi) In § 63.1023(c) introductory text and (c)(4), replace the reference to § 63.1030(b) with § 63.2480(e)(1).

(xii) In § 63.1038(c) replace the reference to § 63.1030(c)(3) with § 63.2480(e)(2).

(xiii) The information in  $\S 63.1030(b)$  required to be reported under  $\S 63.1039(b)(4)$  is now required to be reported under  $\S 63.2520(e)(15)(i)$  and (ii).

(xiv) The reference to § 65.111(b) of this chapter in § 65.102(a) of this chapter no longer applies.

(xv) In § 65.103(b)(3) of this chapter, replace the reference to § 65.111(d) with § 63.2480(e)(4).

(xvi) In  $\S 65.103(b)(4)$  of this chapter, replace the reference to  $\S 63.111(e)$  with  $\S 63.2480(e)(2)(ii)$ .

(xvii) The reference to  $\S 65.111(b)$  and (c) of this chapter in  $\S 65.104(a)(1)(iv)$  of this chapter no longer applies. Instead comply with  $\S 63.2480(e)(1)$  and (2).

(xviii) In  $\S 65.104(c)$  introductory text and (c)(4) of this chapter, replace the reference to  $\S 63.111(b)$  with  $\S 63.2480(e)(1)$ .

(xix) In § 65.119(c)(5) of this chapter, replace the reference to § 65.111(c)(3) with § 63.2480(e)(2) and replace the reference to § 65.111(e) with § 63.2480(e)(2)(ii) and (iii).

(xx) The information required to be reported under  $\S 65.120(b)(4)$  of this chapter is now required to be reported under  $\S 63.2520(e)(15)(i)$  and (ii).

[71 FR 40335, July 14, 2006, as amended at 85 FR 49141, Aug. 12, 2020; 89 FR 23869, Apr. 4, 2024]

# § 63.2485 What requirements must I meet for wastewater streams and liquid streams in open systems within an MCPU?

(a) *General.* You must meet each requirement in Table 7 to this subpart that applies to your wastewater streams and liquid streams in open systems within an MCPU, except as specified in <u>paragraphs (b)</u> through  $(\underline{q})$  of this section.

(b) *Wastewater HAP*. Where  $\S 63.105$  and  $\S \S 63.132$  through 63.148 refer to compounds in table 9 of subpart G of this part 63, the compounds in tables 8 and 9 to this subpart apply for the purposes of this subpart.

(c) Group 1 wastewater. Section 63.132(c)(1) (i) and (ii) do not apply. For the purposes of this subpart, a process wastewater stream is Group 1 for compounds in tables 8 and 9 to this subpart if any of the conditions specified in paragraphs (c) (1) through (3) of this section are met.

(1) The total annual average concentration of compounds in table 8 to this subpart is greater than or equal to 10,000 ppmw at any flowrate, and the total annual load of compounds in table 8 to this subpart is greater than or equal to 200 lb/yr.

(2) The total annual average concentration of compounds in table 8 to this subpart is greater than or equal to 1,000 ppmw, and the annual average flowrate is greater than or equal to 1 l/min.

(3) The combined total annual average concentration of compounds in tables 8 and 9 to this subpart is greater than or equal to 30,000 ppmw, and the combined total annual load of compounds in tables 8 and 9 to this subpart is greater than or equal to 1 tpy.

(d) Wastewater tank requirements.

(1) When  $\frac{\&\& 63.133}{\&B}$  and  $\frac{63.147}{B}$  reference floating roof requirements in  $\frac{\&\& 63.119}{\&B}$  and  $\frac{63.120}{B}$ , the corresponding requirements in  $\frac{\&B}{B}$  for the purposes of this subpart.

(2) When  $\S 63.133(a)$  refers to table 10 of subpart G of this part 63, the maximum true vapor pressure in the table shall be limited to the HAP listed in tables 8 and 9 of this subpart FFFF.

(3) For the purposes of this subpart, the requirements of  $\frac{63.133(a)(2)}{50.133(a)(2)}$  are satisfied by operating and maintaining a fixed roof if you demonstrate that the total soluble and partially soluble HAP emissions from the wastewater tank are no more than 5 percent higher than the emissions would be if the contents of the wastewater tank were not heated, treated by an exothermic reaction, or sparged.

(4) The emission limits specified in  $\frac{\$\$ 63.133(b)(2)}{\$}$  and  $\frac{63.139}{\$}$  for control devices used to control emissions from wastewater tanks do not apply during periods of planned routine maintenance of the control device(s) of no more than 240 hr/yr. You may request an extension to a total of 360 hr/yr in accordance with the procedures specified in  $\frac{\$ 63.2470(d)}{\$}$ .

(e) Individual drain systems. The provisions of  $\S$  63.136(e)(3) apply except as specified in paragraph (e)(1) of this section.

(1) A sewer line connected to drains that are in compliance with  $\frac{63.136(e)(1)}{10}$  may be vented to the atmosphere, provided that the sewer line entrance to the first downstream junction box is water sealed and the sewer line vent pipe is designed as specified in  $\frac{63.136(e)(2)(ii)(A)}{10}$ .

# (2) [Reserved]

(f) *Closed-vent system requirements*. Except as specified in  $\S 63.2450(e)(6)$ , when  $\S 63.148(k)$  refers to closed vent systems that are subject to the requirements of  $\S 63.172$ , the requirements of either  $\S 63.172$  or  $\S 63.1034$  apply for the purposes of this subpart.

(g) *Halogenated vent stream requirements*. For each halogenated vent stream from a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream that is vented through a closed-vent system to a combustion device to reduce organic HAP emissions, you must meet the same emission limits as specified for batch process vents in item 2 of table 2 to this subpart.

# (h) Alternative test methods.

(1) As an alternative to the test methods specified in  $\S$  <u>63.144(b)(5)(i)</u>, you may use Method 8260 or 8270 as specified in  $\S$  <u>63.1257(b)(10)(iii)</u>.

(2) As an alternative to using the methods specified in  $\S 63.144(b)(5)(i)$ , you may conduct wastewater analyses using Method 1666 or 1671 of <u>40 CFR part 136</u> and comply with the sampling protocol requirements specified in  $\S 63.144(b)(5)(ii)$ . The validation requirements specified in  $\S 63.144(b)(5)(ii)$  do not apply if you use Method 1666 or 1671 of <u>40 CFR part 136</u>.

(3) As an alternative to using Method 18 of <u>40 CFR part 60</u>, as specified in <u>§§ 63.139(c)(1)(ii)</u> and <u>63.145(i)(2)</u>, you may elect to use Method 25A of <u>40 CFR part 60</u> as specified in <u>§ 63.997</u>.

(4) As an alternative to using EPA Method 624 of <u>40 CFR part 136</u>, <u>appendix A</u>, as specified in <u>§ 63.144(b)(5)(i)(C)</u>, you may use ASTM D5790-95 (Reapproved 2012) (incorporated by reference, see <u>§ 63.14</u>) for the analysis of total organic HAP in wastewater samples. If you choose to use ASTM D5790-95 (Reapproved 2012), then you must also use the sampling procedures of EPA Method 25D <u>40 CFR part 60</u>, <u>appendix A</u>-7, or an equivalent method.

#### (i) Offsite management and treatment option.

(1) If you ship wastewater to an offsite treatment facility that meets the requirements of  $\S$  <u>63.138(h)</u>, you may elect to document in your notification of compliance status report that the wastewater will be treated as hazardous waste at a facility that meets the requirements of  $\S$  <u>63.138(h)</u> as an alternative to having the offsite facility submit the certification specified in  $\S$  <u>63.132(g)(2)</u>.

(2) As an alternative to the management and treatment options specified in  $\S$  <u>63.132(g)(2)</u>, any affected wastewater stream (or residual removed from an affected wastewater stream) with a total annual average concentration of compounds in Table 8 to this subpart less than 50 ppmw may be transferred offsite in accordance with <u>paragraphs (i)(2) (i)</u> and <u>(ii)</u> of this section.

(i) The transferee (or you) must demonstrate that less than 5 percent of the HAP in Table 9 to this subpart is emitted from the waste management units up to the activated sludge unit.

(ii) The transferee must treat the wastewater stream or residual in a biological treatment unit in accordance with the requirement in <u>paragraph (i)(2)(iii)</u> of this section and the requirements of <u>§§ 63.138</u> and <u>63.145</u> and the requirements referenced therein.

(iii) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , the requirement of  $\S 63.145(a)(3)$  no longer applies. Instead, the transferee must comply with the conditions specified in  $\S 63.2450(g)(6)$ .

(j) You must determine the annual average concentration and annual average flowrate for wastewater streams for each MCPU. The procedures for flexible operation units specified in § 63.144 (b) and (c) do not apply for the purposes of this subpart.

(k) *Outlet concentration correction for supplemental gases.* The requirement to correct outlet concentrations from combustion devices to 3-percent oxygen in  $\frac{\&\& 63.139(c)(1)(ii)}{1000}$  and  $\frac{63.145(i)(6)}{1000}$  applies only if supplemental gases are combined with a vent stream from a Group 1 wastewater stream. If emissions are controlled with a vapor recovery system as specified in  $\frac{\& 63.139(c)(2)}{10000}$ , you must correct for supplemental gases as specified in  $\frac{\& 63.2460(c)(6)}{100000000}$ .

(1) Requirements for liquid streams in open systems.

(1) References in § 63.149 to § 63.100(b) mean § 63.2435(b) for the purposes of this subpart.

(2) When <u>§ 63.149(e)</u> refers to <u>40 CFR 63.100(1) (1)</u> or <u>(2)</u>, <u>§ 63.2445(a)</u> applies for the purposes of this subpart.

(3) When  $\S 63.149$  uses the term "chemical manufacturing process unit," the term "MCPU" applies for the purposes of this subpart.

(4) When  $\S 63.149(e)(1)$  refers to characteristics of water that contain compounds in Table 9 to 40 CFR part 63, subpart <u>G</u>, the characteristics specified in paragraphs (c) (1) through (3) of this section apply for the purposes of this subpart.

(5) When  $\S 63.149(e)(2)$  refers to characteristics of water that contain compounds in Table 9 to 40 CFR part 63, subpart G, the characteristics specified in paragraph (c)(2) of this section apply for the purposes of this subpart.

(m) When  $\S$  <u>63.132(f)</u> refers to "a concentration of greater than 10,000 ppmw of table 9 compounds," the phrase "a concentration of greater than 30,000 ppmw of total partially soluble HAP (PSHAP) and soluble HAP (SHAP) or greater than 10,000 ppmw of PSHAP" shall apply for the purposes of this subpart.

(n) Alternative requirements for wastewater that is Group 1 for soluble HAP only. The option specified in this paragraph (n) applies to wastewater that is Group 1 for soluble HAP in accordance with paragraph (c)(3) of this section and is discharged to biological treatment. Except as provided in paragraph (n)(4) of this section, this option does not apply to wastewater that is Group 1 for partially soluble HAP in accordance with paragraph (c)(1), (c)(2), or (c)(4) of this section. For wastewater that is Group 1 for SHAP, you need not comply with  $\frac{8}{6} \frac{63.133}{6}$  through  $\frac{63.137}{6}$  for any equalization unit, neutralization unit, and/or clarifier prior to the activated sludge unit, and you need not comply with the venting requirements in  $\frac{63.136(e)(2)(ii)(A)}{6}$  for lift stations with a volume larger than 10,000 gal, provided you comply with the requirements specified in table 7 to this subpart. For this option, the treatment requirements in  $\frac{63.138}{63.138}$  and the performance testing requirements in  $\frac{63.145}{6}$  do not apply to the biological treatment unit, except as specified in paragraphs (n)(2)(i) through (iv) of this section.

(1) Wastewater must be hard-piped between the equalization unit, clarifier, and activated sludge unit. This requirement does not apply to the transfer between any of these types of units that are part of the same structure and one unit overflows into the next.

(2) Calculate the destruction efficiency of the biological treatment unit using Equation 1 to this paragraph (n)(2) in accordance with the procedures described in paragraphs (n)(2)(i) through (viii) of this section. You have demonstrated initial compliance if E is greater than or equal to 90 percent.

$$E = \frac{\left[QMW_{s} - QMG_{s} - QMG_{s} - QMG_{s}\right]\left(F_{bw}\right)}{QMW_{s}} \times 100 \quad (Eq. 1)$$

Where:

E = destruction efficiency of total PSHAP and SHAP for the biological treatment unit including the equalization unit, neutralization unit, and/or clarifier, percent;

 $QMW_a = mass$  flow rate of total PSHAP and SHAP compounds entering the equalization unit (or whichever of the three types of units is first), kilograms per hour (kg/hr);

QMG<sub>e</sub> = mass flow rate of total PSHAP and SHAP compounds emitted from the equalization unit, kg/hr;

QMG<sub>n</sub> = mass flow rate of total PSHAP and SHAP compounds emitted from the neutralization unit, kg/hr;

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QMG<sub>c</sub> = mass flow rate of total PSHAP and SHAP compounds emitted from the clarifier, kg/hr

 $F_{bio}$  = site-specific fraction of PSHAP and SHAP compounds biodegraded in the biological treatment unit.

(i) Include all PSHAP and SHAP compounds in both Group 1 and Group 2 wastewater streams from all MCPU, except you may exclude any compounds that meet the criteria specified in  $\frac{63.145(a)(6)(ii)}{63.145(a)(6)(ii)}$  or (iii).

(ii) Except as specified in <u>paragraph (n)(2)(vii)</u> of this section, conduct the demonstration under representative process unit and treatment unit operating conditions in accordance with  $\S 63.145(a)(3)$  and (4).

(iii) Determine PSHAP and SHAP concentrations and the total wastewater flow rate at the inlet to the equalization unit in accordance with  $\S 63.145(f)(1)$  and (2). References in  $\S 63.145(f)(1)$  and (2) to required mass removal and actual mass removal do not apply for the purposes of this section.

(iv) Determine  $F_{bio}$  for the activated sludge unit as specified in § 63.145(h), except as specified in paragraph (n)(2)(iv)(A) or paragraph (n)(2)(iv)(B) of this section.

(A) If the biological treatment process meets both of the requirements specified in  $\S$  63.145(h)(1)(i) and (ii), you may elect to replace the F<sub>bio</sub> term in Equation 1 to paragraph (n)(2) of this section with the numeral "1."

(B) You may elect to assume f<sub>bio</sub> is zero for any compounds on List 2 of table 36 in subpart G.

(v) Determine QMG<sub>e</sub>, QMG<sub>n</sub>, and QMG<sub>e</sub> using EPA's WATER9 model or the most recent update to this model, and conduct testing or use other procedures to validate the modeling results.

(vi) Submit the data and results of your demonstration, including both a description of and the results of your WATER9 modeling validation procedures, in your notification of compliance status report as specified in  $\frac{63.2520(d)(2)(ii)}{2}$ .

(vii) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , the requirement of  $\S 63.145(a)(3)$  no longer applies. Instead, you must comply with the conditions specified in  $\S 63.2450(g)(6)$ .

(3) As an alternative to the venting requirements in  $\frac{63.136(e)(2)(ii)(A)}{A}$ , a lift station with a volume larger than 10,000 gal may have openings necessary for proper venting of the lift station. The size and other design characteristics of these openings may be established based on manufacturer recommendations or engineering judgment for venting under normal operating conditions. You must describe the design of such openings and your supporting calculations and other rationale in your notification of compliance status report.

(4) For any wastewater streams that are Group 1 for both PSHAP and SHAP, you may elect to meet the requirements specified in Table 7 to this subpart for the PSHAP and then comply with <u>paragraphs (n)(1)</u> through (3) of this section for the SHAP in the wastewater system. You may determine the SHAP mass removal rate, in kg/hr, in treatment units that are used to meet the requirements for PSHAP and add this amount to both the numerator and denominator in Equation 1 to <u>paragraph</u> (n)(2) of this section.

(o) Compliance records. Except as specified in paragraph (p) of this section, for each CPMS used to monitor a nonflare control device for wastewater emissions, you must keep records as specified in  $\frac{63.998(c)(1)}{10}$  in addition to the records required in  $\frac{63.147(d)}{10}$ .

(p) Compliance records after date of compliance. Beginning no later than the compliance dates specified in § 63.2445(g), paragraph (o) of this section no longer applies. Instead, for each CPMS used to monitor a nonflare control device for wastewater emissions, you must keep records as specified in § 63.998(c)(1) in addition to the records required in § 63.147(d), except that the provisions of § 63.998(c)(1)(ii)(D), (E), (F), and (G) do not apply.

(q) Startup, shutdown, and malfunction referenced provisions. Beginning no later than the compliance dates specified in  $\S$  <u>63.2445(g)</u>, the referenced provisions specified in <u>paragraphs (q)(1)</u> through (5) of this section do not apply when demonstrating compliance with this section.

(1) Section 63.105(d) of subpart F and the phrase "as part of the start-up, shutdown, and malfunction plan required under  $\S$  <u>63.6(e)(3)</u> of <u>subpart A of this part</u>" from  $\S$  <u>63.105(e)</u> of subpart F.

(2) Section 63.132(b)(3)(i)(B) of subpart G.

(3) The phrase "or startup/shutdown/malfunction" in  $\S 63.132(f)(2)$  of subpart G.

(4) Section 63.148(f)(3) of subpart G.

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(5) For flares complying with  $\S 63.2450(e)(5)$ , the following provisions do not apply:

(i) Section 63.139(c)(3) of subpart G;

(ii) Section 63.139(d)(3) of subpart G;

(iii) Section 63.145(j) of subpart G;

(iv) Section 63.146(b)(7)(i) of subpart G; and

(v) Section 63.147(d)(1) of subpart G.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>70 FR 38559</u>, July 1, 2005; <u>71 FR 40335</u>, July 14, 2006; <u>85 FR 49144</u>, Aug. 12, 2020]

# § 63.2490 What requirements must I meet for heat exchange systems?

(a) You must comply with each requirement in Table 10 to this subpart that applies to your heat exchange systems, except as specified in <u>paragraphs (b)</u> through (c) of this section.

(b) Except as specified in <u>paragraph (d)</u> of this section, if you comply with the requirements of  $\S 63.104$  as specified in Table 10 to this subpart, then the phrase "a chemical manufacturing process unit meeting the conditions of  $\S 63.100$  (b)(1) through (b)(3) of this subpart" in  $\S 63.104(a)$  means "an MCPU meeting the conditions of  $\S 63.2435$ " for the purposes of this subpart.

(c) Except as specified in paragraph (d) of this section, if you comply with the requirements of  $\frac{63.104}{2}$  as specified in Table 10 to this subpart, then the reference to " $\frac{63.100(c)}{2}$ " in  $\frac{63.104(a)}{2}$  does not apply for the purposes of this subpart.

(d) Unless one or more of the conditions specified in § 63.104(a)(1), (2), (5), and (6) or paragraph (e) of this section are met, beginning no later than the compliance dates specified in § 63.2445(g), the requirements of § 63.104 as specified in Table 10 to this subpart and paragraphs (b) and (c) of this section no longer apply. Instead, you must monitor the cooling water for the presence of total strippable hydrocarbons that indicate a leak according to paragraph (d)(1) of this section, and if you detect a leak, then you must repair it according to paragraphs (d)(2) and (3) of this section, unless repair is delayed according to paragraph (d)(4) of this section. At any time before the compliance dates specified in § 63.2445(g), you may choose to comply with the requirements in this paragraph (d) in lieu of the requirements of § 63.104 as specified in Table 10 to this subpart and paragraphs (b) and (c) of this section. The requirements in this paragraph (d) do not apply to heat exchange systems that have a maximum cooling water flow rate of 10 gallons per minute or less.

(1) You must perform monitoring to identify leaks of total strippable hydrocarbons from each heat exchange system subject to the requirements of this subpart according to the procedures in <u>paragraphs (d)(1)(i)</u> through (v) of this section.

(i) Monitoring locations for closed-loop recirculation heat exchange systems. For each closed loop recirculating heat exchange system, you must collect and analyze a sample from the location(s) described in either paragraph  $(\underline{d})(1)(\underline{i})(\underline{A})$  or  $(\underline{B})$  of this section.

(A) Each cooling tower return line or any representative riser within the cooling tower prior to exposure to air for each heat exchange system.

(B) Selected heat exchanger exit line(s), so that each heat exchanger or group of heat exchangers within a heat exchange system is covered by the selected monitoring location(s).

(ii) Monitoring locations for once-through heat exchange systems. For each once-through heat exchange system, you must collect and analyze a sample from the location(s) described in paragraph(d)(1)(ii)(A) of this section. You may also elect to collect and analyze an additional sample from the location(s) described in paragraph(d)(1)(ii)(B) of this section.

(A) Selected heat exchanger exit line(s), so that each heat exchanger or group of heat exchangers within a heat exchange system is covered by the selected monitoring location(s). The selected monitoring location may be at a point where discharges from multiple heat exchange systems are combined provided that the combined cooling water flow rate at the monitoring location does not exceed 40,000 gallons per minute.

(B) The inlet water feed line for a once-through heat exchange system prior to any heat exchanger. If multiple heat exchange systems use the same water feed (*i.e.*, inlet water from the same primary water source), you may monitor at one representative location and use the monitoring results for that sampling location for all heat exchange systems that use that same water feed.

(iii) Monitoring method. If you comply with the total strippable hydrocarbon concentration leak action level as specified in paragraph (d)(1)(iv) of this section, you must comply with the requirements in paragraph (d)(1)(iii)(A) of this section. If you comply with the total hydrocarbon mass emissions rate leak action level as specified in paragraph (d)(1)(iv) of this section. If section, you must comply with the requirements in paragraph (d)(1)(iv) of this section.

(A) You must determine the total strippable hydrocarbon concentration (in parts per million by volume (ppmv) as methane) at each monitoring location using the "Air Stripping Method (Modified El Paso Method) for Determination of Volatile Organic Compound Emissions from Water Sources" (incorporated by reference—see § 63.14) using a flame ionization detector (FID) analyzer for on-site determination as described in Section 6.1 of the Modified El Paso Method.

(B) You must convert the total strippable hydrocarbon concentration (in ppmv as methane) to a total hydrocarbon mass emissions rate (as methane) using the calculations in Section 7.0 of "Air Stripping Method (Modified El Paso Method) for Determination of Volatile Organic Compound Emissions from Water Sources" (incorporated by reference—see § 63.14).

(iv) Monitoring frequency and leak action level. For each heat exchange system, you must initially monitor monthly for 6months beginning upon startup and monitor quarterly thereafter using a leak action level defined as a total strippable hydrocarbon concentration (as methane) in the stripping gas of 6.2 ppmv or, for heat exchange systems with a recirculation rate of 10,000 gallons per minute or less, you may monitor quarterly using a leak action level defined as a total hydrocarbon mass emissions rate from the heat exchange system (as methane) of 0.18 kg/hr. If a leak is detected as specified in paragraph (d)(1)(v) of this section, then you must monitor monthly until the leak has been repaired according to the requirements in paragraph (d)(2) or (3) of this section. Once the leak has been repaired according to the requirements in paragraph (d)(2) or (3) of this section, quarterly monitoring for the heat exchange system may resume. The monitoring frequencies specified in this paragraph (d)(1)(iv) also apply to the inlet water feed line for a once-through heat exchange system, if monitoring of the inlet water feed is elected as provided in paragraph (d)(1)(ii)(B) of this section.

(v) Leak definition. A leak is defined as described in paragraph (d)(1)(v)(A) or (B) of this section, as applicable.

(A) For once-through heat exchange systems for which the inlet water feed is monitored as described in <u>paragraph</u> (d)(1)(ii)(B) of this section, a leak is detected if the difference in the measurement value of the sample taken from a location specified in <u>paragraph (d)(1)(ii)(A)</u> of this section and the measurement value of the corresponding sample taken from the location specified in <u>paragraph (d)(1)(ii)(B)</u> of this section equals or exceeds the leak action level.

(B) For all other heat exchange systems, a leak is detected if a measurement value of the sample taken from a location specified in paragraph (d)(1)(i)(A) or (B) or (d)(1)(i)(A) of this section equals or exceeds the leak action level.

(2) If a leak is detected using the methods described in <u>paragraph (d)(1)</u> of this section, you must repair the leak to reduce the concentration or mass emissions rate to below the applicable leak action level as soon as practicable, but no later than 45 days after identifying the leak, except as specified in <u>paragraph (d)(4)</u> of this section. Repair must include re-monitoring at the monitoring location where the leak was identified according to the method specified in <u>paragraph (d)(1)(iii)</u> of this section to verify that the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is below the applicable leak action level. Repair may also include performing the additional monitoring in <u>paragraph (d)(3)</u> of this section to verify that the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is below the applicable leak action level. Actions that can be taken to achieve repair include but are not limited to:

(i) Physical modifications to the leaking heat exchanger, such as welding the leak or replacing a tube;

- (ii) Blocking the leaking tube within the heat exchanger;
- (iii) Changing the pressure so that water flows into the process fluid;
- (iv) Replacing the heat exchanger or heat exchanger bundle; or

(v) Isolating, bypassing, or otherwise removing the leaking heat exchanger from service until it is otherwise repaired.

(3) If you detect a leak when monitoring a cooling tower return line under paragraph (d)(1)(i)(A) of this section, you may conduct additional monitoring of each heat exchanger or group of heat exchangers associated with the heat exchange system for which the leak was detected, as provided in paragraph (d)(1)(i)(B) of this section. If no leaks are detected when monitoring according to the requirements of paragraph (d)(1)(i)(B) of this section, the heat exchange system is considered to have met the repair requirements through re-monitoring of the heat exchange system, as provided in paragraph (d)(2) of this section.

(4) You may delay repair when one of the conditions in paragraph (d)(4)(i) or (ii) of this section is met and the leak is less than the delay of repair action level specified in paragraph (d)(4)(iii) of this section. You must determine if a delay of repair is necessary as soon as practicable, but no later than 45 days after first identifying the leak.

(i) If the repair is technically infeasible without a shutdown and the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is initially and remains less than the delay of repair action level for all monitoring periods during the delay of repair, then you may delay repair until the next scheduled shutdown of the heat exchange system. If, during subsequent monitoring, the delay of repair action level is exceeded, then you must repair the leak within 30 days of the monitoring event in which the leak was equal to or exceeded the delay of repair action level.

(ii) If the necessary equipment, parts, or personnel are not available and the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate is initially and remains less than the delay of repair action level for all monitoring periods during the delay of repair, then you may delay the repair for a maximum of 120 calendar days. You must demonstrate that the necessary equipment, parts, or personnel were not available. If, during subsequent monitoring, the delay of repair action level is exceeded, then you must repair the leak within 30 days of the monitoring event in which the leak was equal to or exceeded the delay of repair action level.

(iii) The delay of repair action level is a total strippable hydrocarbon concentration (as methane) in the stripping gas of 62 ppmv or, for heat exchange systems with a recirculation rate of 10,000 gallons per minute or less, the delay of repair action level is a total hydrocarbon mass emissions rate (as methane) of 1.8 kg/hr. The delay of repair action level is assessed as described in paragraph (d)(4)(iii)(A) or (B) of this section, as applicable.

(A) For once-through heat exchange systems for which the inlet water feed is monitored as described in <u>paragraph</u>  $(\underline{d})(1)(\underline{ii})(\underline{B})$  of this section, the delay of repair action level is exceeded if the difference in the measurement value of the sample taken from a location specified in <u>paragraph</u>  $(\underline{d})(1)(\underline{ii})(\underline{A})$  of this section and the measurement value of the corresponding sample taken from the location specified in <u>paragraph</u>  $(\underline{d})(1)(\underline{ii})(\underline{A})$  of this section equals or exceeds the delay of repair action level.

(B) For all other heat exchange systems, the delay of repair action level is exceeded if a measurement value of the sample taken from a location specified in paragraph (d)(1)(i)(A) or (B) or (d)(1)(i)(A) of this section equals or exceeds the delay of repair action level.

(e) If 99 percent by weight or more of the organic compounds that could leak into the heat exchange system are water soluble and have a Henry's Law Constant less than 5.0E-6 at 25 degrees Celsius (atmospheres-cubic meters/mol) and none of the conditions specified in § 63.104(a)(1), (2), (5), and (6) are met, beginning no later than the compliance dates specified in § 63.2445(g), you may monitor the cooling water for leaks according to the requirements in § 63.104(b) in lieu of using the Modified El Paso Method. If you detect a leak according to § 63.104(b), then you must repair it according to paragraph (e)(1) of this section, unless repair is delayed according to paragraph (e)(2) of this section.

(1) If a leak is detected using the methods described in <u>paragraph (e)</u> of this section, you must repair the leak as soon as practicable, but no later than 45 days after identifying the leak, except as specified in <u>paragraph (e)(2)</u> of this section. Repair must include re-monitoring at the monitoring location where the leak was identified to verify that the criteria in  $\frac{8}{63.104(b)(6)}$  is no longer met. Actions that can be taken to achieve repair include but are not limited to:

(i) Physical modifications to the leaking heat exchanger, such as welding the leak or replacing a tube;

- (ii) Blocking the leaking tube within the heat exchanger;
- (iii) Changing the pressure so that water flows into the process fluid;
- (iv) Replacing the heat exchanger or heat exchanger bundle; or

(v) Isolating, bypassing, or otherwise removing the leaking heat exchanger from service until it is otherwise repaired.

(2) You may delay repair when the conditions in  $\frac{63.104(e)}{2}$  are met.

[85 FR 49145, Aug. 12, 2020, as amended at 89 FR 23869, Apr. 4, 2024]

#### § 63.2492 How do I determine whether my process vent, storage tank, or equipment is in ethylene oxide service?

To determine if process vents, storage tanks, and equipment leaks are in ethylene oxide service as defined in  $\S$  <u>63.2550(i)</u>, you must comply with the requirements in <u>paragraphs (a)</u> through <u>(c)</u> of this section, as applicable.

(a) For each batch process vent or continuous process vent stream, you must measure the flow rate and concentration of ethylene oxide of each process vent as specified in <u>paragraphs (a)(1)</u> through (5) of this section.

(1) Measurements must be made prior to any dilution of the vent streams.

(2) Measurements may be made on the combined vent streams at an MCPU or for each separate vent stream.

(3) Method 1 or 1A of <u>40 CFR part 60</u>, appendix A-1, as appropriate, must be used for the selection of the sampling sites. For vents smaller than 0.10 meter in diameter, sample at one point at the center of the duct.

(4) The gas volumetric flow rate must be determined using Method 2, 2A, 2C, 2D, 2F, or 2G of <u>40 CFR part 60</u>, appendices A-1 and A-2, as appropriate.

(5) The concentration of ethylene oxide must be determined using Method 18 of <u>40 CFR part 60, appendix A</u>-6, or Method 320 of appendix A to this part.

(b) For storage tanks, you must determine the concentration of ethylene oxide of the fluid stored in the storage tanks by complying with the requirements in paragraph (b)(1) or (2) of this section.

(1) You must measure the concentration of ethylene oxide of the fluid stored in the storage tanks using Method 624.1 of  $\frac{40}{CFR}$  part 136, appendix A, or preparation by Method 5031 and analysis by Method 8260D (both incorporated by reference, see § 63.14) in the SW-846 Compendium. In lieu of preparation by SW-846 Method 5031, you may use SW-846 Method 5030B (incorporated by reference, see § 63.14), as long as: You do not use a preservative in the collected sample; you store the sample with minimal headspace as cold as possible and at least below 4 degrees C; and you analyze the sample as soon as possible, but in no case longer than 7 days from the time the sample was collected. If you are collecting a sample from a pressure vessel, you must maintain the sample under pressure both during and following sampling.

(2) Unless specified by the Administrator, you may calculate the concentration of ethylene oxide of the fluid stored in the storage tanks if information specific to the fluid stored is available. Information specific to the fluid stored includes concentration data from safety data sheets.

(c) For equipment leaks, you must comply with the requirements in <u>paragraphs (c)(1)</u> through (4) of this section.

(1) Each piece of equipment within an MCPU that can reasonably be expected to contain equipment in ethylene oxide service is presumed to be in ethylene oxide service unless you demonstrate that the piece of equipment is not in ethylene oxide service. For a piece of equipment to be considered not in ethylene oxide service, it must be determined that the percent ethylene oxide content of the process fluid that is contained in or contacts equipment can be reasonably expected to not exceed 0.1 percent by weight on an annual average basis. For purposes of determining the percent ethylene oxide content of the process fluid that is 640 CFR part 60, appendix A-6, for gaseous process fluid, and Method 624.1 of 40 CFR part 136, appendix A, or preparation by Method 5031 and analysis by Method 8260D (both incorporated by reference, see § 63.14) in the SW-846 Compendium for liquid process fluid. In lieu of preparation by SW-846 Method 5031, you may use SW-846 Method 5030B (incorporated by reference, see § 63.14), as long as: You do not use a preservative in the collected sample; you store the sample with minimal headspace as cold as possible and at least below 4 degrees C; and you analyze the sample as soon as possible, but in no case longer than 7 days from the time the sample was collected.

(2) Unless specified by the Administrator, you may use good engineering judgment rather than the procedures specified in paragraph (c)(1) of this section to determine that the percent ethylene oxide content of the process fluid that is contained in or contacts equipment does not exceed 0.1 percent by weight.

(3) You may revise your determination for whether a piece of equipment is in ethylene oxide service by following the procedures in paragraph (c)(1) of this section, or by documenting that a change in the process or raw materials no longer causes the equipment to be in ethylene oxide service.

(4) Samples used in determining the ethylene oxide content must be representative of the process fluid that is contained in or contacts the equipment.

[85 FR 49146, Aug. 12, 2020, as amended at 89 FR 23870, Apr. 3, 2024]

# § 63.2493 What requirements must I meet for process vents, storage tanks, or equipment that are in ethylene oxide service?

This section applies beginning no later than the compliance dates specified in  $\frac{63.2445(i)}{10}$ . In order to demonstrate compliance with the emission limits and work practice standards specified in Tables 1, 2, and 4 to this subpart for process

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vents and storage tanks in ethylene oxide service, you must meet the requirements specified in <u>paragraphs (a)</u> through (c) of this section. In order to demonstrate compliance with the requirements specified in Table 6 to this subpart for equipment in ethylene oxide service, you must meet the requirements specified in <u>paragraphs (d)</u> and (e) of this section.

(a) *Initial compliance*. For initial compliance, you must comply with <u>paragraphs (a)(1)</u> through (4) of this section, as applicable.

(1) If you choose to reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a flare as specified in Table 1, 2, or 4 to this subpart, then you must comply with  $\S 63.2450(e)(4)$  and (6) and the requirements in  $\S 63.983$ , and you must conduct the initial visible emissions demonstration required by  $\S 63.670(h)$  of subpart CC as specified in  $\S 63.2450(e)(5)$ .

(2) If you choose to reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a non-flare control device that reduces ethylene oxide by greater than or equal to 99.9 percent by weight as specified in Table 1, 2, or 4 to this subpart, then you must comply with  $\S$  63.2450(e)(4) and (6) and the requirements in  $\S$  63.983, and you must comply with paragraphs (a)(2)(i) through (viii) of this section.

(i) Conduct an initial performance test of the control device that is used to comply with the percent reduction requirement at the inlet and outlet of the control device. For purposes of compliance with this <u>paragraph (a)(2)</u>, you may not use a design evaluation.

(ii) Conduct the performance test according to the procedures in §§ 63.997 and 63.2450(g). Use Method 18 of 40 CFR part 60, appendix A-6, or Method 320 of appendix A to this part to determine the ethylene oxide concentration. Use Method 1 or 1A of 40 CFR part 60, appendix A-1, to select the sampling sites at each sampling location. Determine the gas volumetric flowrate using Method 2, 2A, 2C, or 2D of 40 CFR part 60, appendix A-2. Use Method 4 of 40 CFR part 60, appendix A-3, to convert the volumetric flowrate to a dry basis.

(iii) Calculate the mass emission rate of ethylene oxide entering the control device and exiting the control device using Equations 1 and 2 to this paragraph (a)(2)(iii).

 $E_{EtO,inlet} = K \ C_{EtO,inlet} \ M_{EtO} \ Q_{inlet} \ (Eq. \ 1)$ 

 $E_{EtO,outlet} = K C_{EtO,outlet} M_{EtO} Q_{outlet} (Eq. 2)$ 

Where:

 $E_{EtO,inlet}$ ,  $E_{EtO,outlet}$  = Mass rate of ethylene oxide at the inlet and outlet of the control device, respectively, kilogram per hour.

 $C_{EtO,inlet}$ ,  $C_{EtO,outlet}$  = Concentration of ethylene oxide in the gas stream at the inlet and outlet of the control device, respectively, dry basis, parts per million by volume.

 $M_{EtO}$  = Molecular weight of ethylene oxide, 44.05 grams per gram-mole.

 $Q_{\text{inlet}}$ ,  $Q_{\text{outlet}}$  = Flow rate of the gas stream at the inlet and outlet of the control device, respectively, dry standard cubic meter per minute.

K = Constant, 2.494 × 10–6 (parts per million)–1 (gram-mole per standard cubic meter) (kilogram per gram) (minutes per hour), where standard temperature (gram-mole per standard cubic meter) is 20 °C.

(iv) Calculate the percent reduction from the control device using Equation 3 to this <u>paragraph (a)(2)(iv)</u>. You have demonstrated initial compliance if the overall reduction of ethylene oxide is greater than or equal to 99.9 percent by weight.

Percent reduction =  $(E_{EtO,inlet} - E_{EtO,outlet})/E_{EtO,inlet} * 100$  (Eq. 3)

Where:

 $E_{EtO,inlet}$ ,  $E_{EtO,outlet}$  = Mass rate of ethylene oxide at the inlet and outlet of the control device, respectively, kilogram per hour, calculated using Equations 1 and 2 to paragraph (a)(2)(iii) of this section.

(v) If a new control device is installed, then conduct a performance test of the new device following the procedures in paragraphs (a)(2)(i) through (iv) of this section.

(vi) If you vent emissions through a closed-vent system to a scrubber with a reactant tank, then you must establish operating parameter limits by monitoring the operating parameters specified in <u>paragraphs (a)(2)(vi)(A)</u> through (C) of this section during the performance test.

(vi) If you vent emissions through a closed-vent system to a scrubber with a reactant tank, then you must establish operating parameter limits by monitoring the operating parameters specified in <u>paragraphs (a)(2)(vi)(A)</u> through (C) of this section during the performance test.

(A) Scrubber liquid-to-gas ratio (L/G), determined from the total scrubber liquid inlet flow rate and the exit gas flow rate. Determine the average L/G during the performance test as the average of the test run averages.

(B) Scrubber liquid pH of the liquid in the reactant tank. The pH may be measured at any point between the discharge from the scrubber column and the inlet to the reactant tank. Determine the average pH during the performance test as the average of the test run averages.

(C) Temperature of the scrubber liquid entering the scrubber column. The temperature may be measured at any point after the heat exchanger and prior to entering the top of the scrubber column. Determine the average inlet scrubber liquid temperature as the average of the test run averages.

(vii) If you vent emissions through a closed-vent system to a thermal oxidizer, then you must establish operating parameter limits by monitoring the operating parameters specified in <u>paragraphs (a)(2)(vii)(A)</u> and <u>(B)</u> of this section during the performance test.

(A) Combustion chamber temperature. Determine the average combustion chamber temperature during the performance test as the average of the test run averages.

(B) Flue gas flow rate. Determine the average flue gas flow rate during the performance test as the average of the test run averages.

(viii) If you vent emissions through a closed-vent system to a control device other than a flare, scrubber with a reactant tank, or thermal oxidizer, then you must notify the Administrator of the operating parameters that you plan to monitor during the performance test prior to establishing operating parameter limits for the control device.

(viii) If you vent emissions through a closed-vent system to a control device other than a flare, scrubber with a reactant tank, or thermal oxidizer, then you must notify the Administrator of the operating parameters that you plan to monitor during the performance test prior to establishing operating parameter limits for the control device.

(3) If you choose to reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a non-flare control device that reduces ethylene oxide to less than 1 ppmv as specified in Table 1, 2, or 4 to this subpart, then you must comply with  $\frac{63.2450(e)(4)}{(a)}$  and  $\frac{(6)}{(b)}$  and the requirements in  $\frac{63.983}{(b)}$ , and you must comply with either paragraph  $\frac{(a)(3)(i)}{(a)}$  or (ii) of this section.

(i) Install an FTIR CEMS meeting the requirements of Performance Specification 15 of <u>40 CFR part 60</u>, appendix B, to continuously monitor the ethylene oxide concentration at the exit of the control device. Comply with the requirements specified in <u>§ 63.2450(j)</u> for your CEMS.

(ii) If you do not install a CEMS under <u>paragraph (a)(3)(i)</u> of this section, you must comply with <u>paragraphs</u> (a)(3)(ii)(A) through (C) of this section.

(A) Conduct an initial performance test of the control device that is used to comply with the concentration requirement at the outlet of the control device.

(B) Conduct the performance test according to the procedures in  $\frac{\&\& 63.997}{B}$  and  $\frac{63.2450(g)}{B}$ . Use Method 18 of  $\frac{40 \text{ CFR part}}{40 \text{ CFR part}}$  60, appendix A-6, or Method 320 of appendix A to this part to determine the ethylene oxide concentration. You have demonstrated initial compliance if the ethylene oxide concentration is less than 1 ppmv.

(C) Comply with the requirements specified in paragraphs (a)(2)(v) through (viii) of this section, as applicable.

(4) If you choose to reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a non-flare control device that reduces ethylene oxide to less than 5 pounds per year for all combined process vents as specified in Table 1 or 2 to this subpart, then you must comply with  $\frac{63.2450(e)(4)}{2}$  and  $\frac{60}{2}$  and the requirements in  $\frac{8}{2}$  63.983, and you must comply with paragraphs (a)(4)(i) through (iv) of this section.

(i) Conduct an initial performance test of the control device that is used to comply with the mass emission limit requirement at the outlet of the control device.

(ii) Conduct the performance test according to the procedures in §§ 63.997 and 63.2450(g). Use Method 18 of 40 CFR part 60, appendix A-6, or Method 320 of appendix A to this part to determine the ethylene oxide concentration. Use Method 1 or 1A of 40 CFR part 60, appendix A-1, to select the sampling site. Determine the gas volumetric flowrate using Method 2, 2A, 2C, or 2D of 40 CFR part 60, appendix A-2. Use Method 4 of 40 CFR part 60, appendix A-3, to convert the volumetric flowrate to a dry basis.

(iii) Calculate the mass emission rate of ethylene oxide exiting the control device using Equation 2 to <u>paragraph (a)(2)(iii)</u> of this section. You have demonstrated initial compliance if the ethylene oxide from all process vents (controlled and uncontrolled) is less than 5 pounds per year when combined.

(iv) Comply with the requirements specified in <u>paragraphs (a)(2)(v)</u> through (viii) of this section, as applicable.

(b) *Continuous compliance*. For continuous compliance, you must comply with <u>paragraphs (b)(1)</u> through (6) of this section, as applicable.

(1) If you choose to reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a flare as specified in Table 1, 2, or 4 to this subpart, then you must comply with the requirements in  $\underline{\$\$}$ <u>63.983</u> and <u>63.2450(e)(4)</u> through (6).

(2) If you choose to reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a non-flare control device that reduces ethylene oxide to less than 1 ppmv as specified in Table 1, 2, or 4 to this subpart, and you choose to comply with paragraph (a)(3)(i) of this section, then continuously monitor the ethylene oxide concentration at the exit of the control device using an FTIR CEMS meeting the requirements of Performance Specification 15 of  $\frac{40 \text{ CFR part 60}}{40 \text{ CFR part 60}}$ , appendix B, and § 63.2450(j). If you use an FTIR CEMS, you do not need to conduct the performance testing required in paragraph (b)(3) of this section or the operating parameter monitoring required in paragraphs (b)(4) through (6) of this section.

(3) Conduct a performance test no later than 60 months after the previous performance test and reestablish operating parameter limits following the procedures in paragraph (a)(2) through (4) of this section. The Administrator may request a repeat performance test at any time. For purposes of compliance with this paragraph (b)(3), you may not use a design evaluation.

(4) If you vent emissions through a closed-vent system to a scrubber with a reactant tank, then you must comply with  $\frac{63.2450(e)(4)}{10}$  and  $\frac{6}{10}$  and the requirements in  $\frac{63.983}{10}$ , and you must meet the operating parameter limits specified in paragraphs (b)(4)(i) through (v) of this section.

(i) Minimum scrubber liquid-to-gas ratio (L/G), equal to the average L/G measured during the most recent performance test. Determine total scrubber liquid inlet flow rate with a flow sensor with a minimum accuracy of at least  $\pm 5$  percent over the normal range of flow measured, or 1.9 liters per minute (0.5 gallons per minute), whichever is greater. Determine exit gas flow rate with a flow sensor with a minimum accuracy of at least  $\pm 5$  percent over the normal range of flow measured, or 280 liters per minute (10 cubic feet per minute), whichever is greater. Compliance with the minimum L/G operating limit must be determined continuously on a 1-hour block basis.

(ii) Maximum scrubber liquid pH of the liquid in the reactant tank, equal to the average pH measured during the most recent performance test. Compliance with the pH operating limit must be determined continuously on a 1-hour block basis. Use a pH sensor with a minimum accuracy of  $\pm 0.2$  pH units.

(iii) Pressure drop across the scrubber column, within the pressure drop range specified by the manufacturer or established based on engineering analysis. Compliance with the pressure drop operating limit must be determined continuously on a 1-hour block basis. Use pressure sensors with a minimum accuracy of  $\pm 5$  percent over the normal operating range or 0.12 kilopascals, whichever is greater.

(iv) Maximum temperature of the scrubber liquid entering the scrubber column, equal to the average temperature measured during the most recent performance test. Compliance with the inlet scrubber liquid temperature operating limit must be determined continuously on a 1-hour block basis. Use a temperature sensor with a minimum accuracy of  $\pm 1$  percent over the normal range of the temperature measured, expressed in degrees Celsius, or 2.8 degrees Celsius, whichever is greater.

(v) Liquid feed pressure to the scrubber column within the feed pressure range specified by the manufacturer or established based on engineering analysis. Compliance with the liquid feed pressure operating limit must be determined continuously on a 1-hour block basis. Use a pressure sensor with a minimum accuracy of  $\pm 5$  percent over the normal operating range or 0.12 kilopascals, whichever is greater.

(5) If you vent emissions through a closed-vent system to a thermal oxidizer, then you must comply with  $\S$  <u>63.2450(e)(4)</u> and <u>(6)</u> and the requirements in  $\S$  <u>63.983</u>, and you must meet the operating parameter limits specified in paragraphs (b)(5)(i) and <u>(ii)</u> of this section and the requirements in paragraph (b)(5)(iii) of this section.

(i) Minimum combustion chamber temperature, equal to the average combustion chamber temperature measured during the most recent performance test. Determine combustion chamber temperature with a temperature sensor with a minimum accuracy of at least  $\pm 1$  percent over the normal range of temperature measured, expressed in degrees Celsius, or 2.8 degrees Celsius, whichever is greater. Compliance with the minimum combustion chamber temperature operating limit must be determined continuously on a 1-hour block basis.

(ii) Maximum flue gas flow rate, equal to the average flue gas flow rate measured during the most recent performance test. Determine flue gas flow rate with a flow sensor with a minimum accuracy of at least  $\pm 5$  percent over the normal range of flow measured, or 280 liters per minute (10 cubic feet per minute), whichever is greater. Compliance with the maximum flue gas flow rate operating limit must be determined continuously on a 1-hour block basis.

(iii) You must maintain the thermal oxidizer in accordance with good combustion practices that ensure proper combustion. Good combustion practices include, but are not limited to, proper burner maintenance, proper burner alignment, proper fuel to air distribution and mixing, routine inspection, and preventative maintenance.

(6) If you vent emissions through a closed-vent system to a control device other than a flare, scrubber with a reactant tank, or thermal oxidizer, then you must comply with § 63.2450(e)(4) and (6) and the requirements in § 63.983, and you must monitor the operating parameters identified in <u>paragraph (a)(2)(viii)</u> of this section and meet the established operating parameter limits to ensure continuous compliance. The frequency of monitoring and averaging time will be determined based upon the information provided to the Administrator.

(c) *Pressure vessels*. If you have a storage tank in ethylene oxide service that is considered a pressure vessel as defined in as defined in  $\frac{63.2550(i)}{10}$ , then you must operate and maintain the pressure vessel, as specified in <u>paragraphs</u> (c)(1) through (5) of this section.

(1) The pressure vessel must be designed to operate with no detectable emissions at all times.

(2) Monitor each point on the pressure vessel through which ethylene oxide could potentially be emitted by conducting initial and annual performance tests using Method 21 of  $\frac{40 \text{ CFR part } 60, \text{ appendix A}}{1000 \text{ CFR part } 60, \text{ appendix A}}$ .

(3) Each instrument reading greater than 500 ppmv is a deviation.

(4) Estimate the flow rate and total regulated material emissions from the defect. Assume the pressure vessel has been emitting for half of the time since the last performance test, unless other information supports a different assumption.

(5) Whenever ethylene oxide is in the pressure vessel, you must operate the pressure vessel as a closed system that vents through a closed vent system to a control device as specified in <u>paragraphs (c)(5)(i)</u> through (iii) of this section, as applicable.

(i) For closed vent systems, comply with  $\S 63.2450(e)(4)$  and (6) and the requirements in  $\S 63.983$ .

(ii) For a non-flare control device, comply with requirements as specified in paragraph (b) of this section.

(iii) For a flare, comply with the requirements of  $\frac{63.2450(e)(5)}{2}$ .

(d) Equipment in ethylene oxide service. Except as specified in <u>paragraphs (d)(1)</u> through (4) and (e) of this section, for equipment in ethylene oxide service as defined in § 63.2550(i), you must comply with the requirements of <u>subpart UU</u> or <u>H</u> of this part, or <u>40 CFR part 65</u>, <u>subpart F</u>.

(1) For pumps in ethylene oxide service, you must comply with the requirements in <u>paragraphs (d)(1)(i)</u> through (iii) of this section.

(i) The instrument reading that defines a leak for pumps is 1,000 parts per million or greater.

(ii) The monitoring period for pumps is monthly.

(iii) When a leak is detected, it must be repaired as soon as practicable, but not later than 15 calendar days after it is detected. Delay of repair of pumps for which leaks have been detected is allowed for pumps that are isolated from the process and that do not remain in ethylene oxide service.

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(2) For connectors in ethylene oxide service, you must comply with the requirements in <u>paragraphs (d)(2)(i)</u> through (iii) of this section.

(i) The instrument reading that defines a leak for connectors is 500 parts per million or greater.

(ii) The monitoring period for connectors is once every 12 months.

(iii) When a leak is detected, it must be repaired as soon as practicable, but not later than 15 calendar days after it is detected. Delay of repair of connectors for which leaks have been detected is allowed for connectors that are isolated from the process and that do not remain in ethylene oxide service.

(3) For each light liquid pump or connector in ethylene oxide service that is added to an MCPU, and for each light liquid pump or connector in ethylene oxide service that replaces a light liquid pump or connector in ethylene oxide service, you must initially monitor for leaks within 5 days after initial startup of the equipment.

(4) Pressure relief devices in ethylene oxide service must comply with the requirements in  $\S$  63.2480(e) and (f), except as specified in paragraphs (d)(4)(i) through (v) of this section.

- (i) The second sentence in  $\S 63.2480(e)(3)(iv)$  does not apply.
- (ii) Section 63.2480(e)(3)(v) does not apply.
- (iii) Section 63.2480(e)(6)(ii) does not apply.

(iv) Any release event from an affected pressure relief device is a deviation of the pressure release management work practice standards.

(v) Replace all references to  $\S 63.2445(g)$  with  $\S 63.2445(i)$ .

(e) *Non-applicable referenced provisions*. The referenced provisions specified in <u>paragraphs (e)(1)</u> through (<u>16</u>) of this section do not apply when demonstrating compliance with this section.

- (1) Section 63.163(c)(3) of subpart H.
- (2) Section 63.163(e) of subpart H.
- (3) The second sentence of  $\S 63.181(d)(5)(i)$  of subpart H.
- (4) Section 63.1026(b)(3) of subpart UU.
- (5) Section 63.1026(e) of subpart UU.
- (6) The phrase "(except during periods of startup, shutdown, or malfunction)" from  $\frac{63.1028(e)(1)(i)(A)}{2}$  of subpart UU.
- (7) The phrase "(except during periods of startup, shutdown, or malfunction)" from § 63.1031(b)(1) of subpart UU.
- (8) The second sentence of  $\S 65.105(f)(4)(i)$  of this chapter.
- (9) Section 65.107(b)(3) of this chapter.
- (10) Section 65.107(e) of this chapter.
- (11) The phrase "(except during periods of start-up, shutdown, or malfunction)" from  $\frac{65.109(e)(1)(i)(A)}{100}$  of this chapter.
- (12) The phrase "(except during periods of start-up, shutdown, or malfunction)" from § 65.112(b)(1) of this chapter.
- (13) The last sentence of  $\S$  65.115(b)(1) of this chapter.
- (14) The last sentence of § 65.115(b)(2) of this chapter.
- (15) For flares complying with  $\S$  63.2450(e)(5), the following provisions do not apply:
- (i) Section 63.172(d) of subpart H;
- (ii) Section 63.180(e) of subpart H;
- (iii) Section 63.181(g)(1)(iii) of subpart H;
- (iv) The phrase "including periods when a flare pilot light system does not have a flame" from  $\frac{63.181(g)(2)(i)}{2}$  of subpart H;

(v) Section 63.1034(b)(2)(iii) of subpart H; and

(vi) Section 65.115(b)(2) of this chapter.

(16) Requirements for maintenance vents in  $\S 63.2450(v)$ .

[85 FR 49147, Aug. 12, 2020, as amended at 89 FR 23870, Apr. 4, 2024]

# Alternative Means of Compliance

# § 63.2495 How do I comply with the pollution prevention standard?

(a) You may elect to comply with the pollution prevention alternative requirements specified in <u>paragraphs (a) (1)</u> and (2) of this section in lieu of the emission limitations and work practice standards contained in Tables 1 through 7 to this subpart for any MCPU for which initial startup occurred before April 4, 2002.

(1) You must reduce the production-indexed HAP consumption factor (HAP factor) by at least 65 percent from a 3-year average baseline beginning no earlier than the 1994 through 1996 calendar years. For any reduction in the HAP factor that you achieve by reducing HAP that are also volatile organic compounds (VOC), you must demonstrate an equivalent reduction in the production-indexed VOC consumption factor (VOC factor) on a mass basis. For any reduction in the HAP factor that you achieve by reducing a HAP that is not a VOC, you may not increase the VOC factor.

(2) Any MCPU for which you seek to comply by using the pollution prevention alternative must begin with the same starting material(s) and end with the same product(s). You may not comply by eliminating any steps of a process by transferring the step offsite (to another manufacturing location). You may also not merge a solvent recovery step conducted offsite to onsite and as part of an existing process as a method of reducing consumption.

(3) You may comply with the requirements of <u>paragraph (a)(1)</u> of this section for a series of processes, including situations where multiple processes are merged, if you demonstrate to the satisfaction of the Administrator that the multiple processes were merged after the baseline period into an existing process or processes.

(b) Exclusions.

(1) You must comply with the emission limitations and work practice standards contained in Tables 1 through 7 to this subpart for all HAP that are generated in the MCPU and that are not included in consumption, as defined in  $\S$  63.2550. If any vent stream routed to the combustion control is a halogenated vent stream, as defined in  $\S$  63.2550, then hydrogen halides that are generated as a result of combustion control must be controlled according to the requirements in  $\S$  63.2450(e)(4) and the requirements of  $\S$  63.994 and the requirements referenced therein.

(2) You may not merge nondedicated formulation or nondedicated solvent recovery processes with any other processes.

(c) *Initial compliance procedures*. To demonstrate initial compliance with <u>paragraph (a)</u> of this section, you must prepare a demonstration summary in accordance with <u>paragraph (c) (1)</u> of this section and calculate baseline and target annual HAP and VOC factors in accordance with <u>paragraphs (c) (2)</u> and (3) of this section.

(1) Demonstration plan. You must prepare a pollution prevention demonstration plan that contains, at a minimum, the information in <u>paragraphs (c)(1) (i)</u> through <u>(iii)</u> of this section for each MCPU for which you comply with <u>paragraph (a)</u> of this section.

(i) Descriptions of the methodologies and forms used to measure and record consumption of HAP and VOC compounds.

(ii) Descriptions of the methodologies and forms used to measure and record production of the product(s).

(iii) Supporting documentation for the descriptions provided in accordance with <u>paragraphs (c)(1) (i)</u> and <u>(ii)</u> of this section including, but not limited to, samples of operator log sheets and daily, monthly, and/or annual inventories of materials and products. You must describe how this documentation will be used to calculate the annual factors required in <u>paragraph (d)</u> of this section.

(2) *Baseline factors.* You must calculate baseline HAP and VOC factors by dividing the consumption of total HAP and total VOC by the production rate, per process, for the first 3-year period in which the process was operational, beginning no earlier than the period consisting of the 1994 through 1996 calendar years.

(3) *Target annual factors*. You must calculate target annual HAP and VOC factors. The target annual HAP factor must be equal to 35 percent of the baseline HAP factor. The target annual VOC factor must be lower than the baseline VOC factor by

an amount equivalent to the reduction in any HAP that is also a VOC, on a mass basis. The target annual VOC factor may be the same as the baseline VOC factor if the only HAP you reduce is not a VOC.

(d) Continuous compliance requirements. You must calculate annual rolling average values of the HAP and VOC factors (annual factors) in accordance with the procedures specified in paragraphs (d) (1) through (3) of this section. To show continuous compliance, the annual factors must be equal to or less than the target annual factors calculated according to paragraph (c)(3) of this section.

(1) To calculate the annual factors, you must divide the consumption of both total HAP and total VOC by the production rate, per process, for 12-month periods at the frequency specified in either <u>paragraph (d) (2)</u> or (3) of this section, as applicable.

(2) For continuous processes, you must calculate the annual factors every 30 days for the 12-month period preceding the 30th day (i.e., annual rolling average calculated every 30 days). A process with both batch and continuous operations is considered a continuous process for the purposes of this section.

(3) For batch processes, you must calculate the annual factors every 10 batches for the 12-month period preceding the 10th batch (*i.e.*, annual rolling average calculated every 10 batches), except as specified in <u>paragraphs (d)(3) (i)</u> and <u>(ii)</u> of this section.

(i) If you produce more than 10 batches during a month, you must calculate the annual factors at least once during that month.

(ii) If you produce less than 10 batches in a 12-month period, you must calculate the annual factors for the number of batches in the 12-month period since the previous calculations.

(e) *Records*. You must keep records of HAP and VOC consumption, production, and the rolling annual HAP and VOC factors for each MCPU for which you are complying with <u>paragraph (a)</u> of this section.

#### (f) Reporting.

(1) You must include the pollution prevention demonstration plan in the precompliance report required by <u>§ 63.2520(c)</u>.

(2) You must identify all days when the annual factors were above the target factors in the compliance reports.

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40336, July 14, 2006; 85 FR 49150, Aug. 12, 2020]

#### § 63.2500 How do I comply with emissions averaging?

(a) For an existing source, you may elect to comply with the percent reduction emission limitations in Tables 1, 2, 4, 5, and 7 to this subpart by complying with the emissions averaging provisions specified in  $\S$  63.150, except as specified in paragraphs (b) through (g) of this section.

(b) The batch process vents in an MCPU collectively are considered one individual emission point for the purposes of emissions averaging, except that only individual batch process vents must be excluded to meet the requirements of  $\S$  <u>63.150(d)(5)</u>.

(c) References in  $\S 63.150$  to  $\S 8 63.112$  through 63.130 mean the corresponding requirements in  $\S 8 63.2450$  through 63.2490, including applicable monitoring, recordkeeping, and reporting.

(d) References to "periodic reports" in § 63.150 mean "compliance report" for the purposes of this subpart.

(e) For batch process vents, estimate uncontrolled emissions for a standard batch using the procedures in § 63.1257(d)(2)(i) and (ii) instead of the procedures in § 63.150(g)(2). Multiply the calculated emissions per batch by the number of batches per month when calculating the monthly emissions for use in calculating debits and credits.

(f) References to "storage vessels" in  $\S$  63.150 mean "storage tank" as defined in  $\S$  63.2550 for the purposes of this subpart.

(g) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ ,  $\S 63.150(f)(2)$  does not apply when demonstrating compliance with this section.

[68 FR 63888, Nov. 10, 2003, as amended at 85 FR 49150, Aug. 12, 2020]

#### § 63.2505 How do I comply with the alternative standard?

As an alternative to complying with the emission limits and work practice standards for process vents and storage tanks in Tables 1 through 4 to this subpart and the requirements in  $\frac{88}{63.2455}$  through  $\frac{63.2470}{70}$ , you may comply with the emission

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limits in <u>paragraph (a)</u> of this section and demonstrate compliance in accordance with the requirements in <u>paragraph (b)</u> of this section.

(a) Emission limits and work practice standards.

(1) You must route vent streams through a closed-vent system to a control device that reduces HAP emissions as specified in either paragraph (a)(1)(i) or (ii) of this section.

(i) If you use a combustion control device, it must reduce HAP emissions as specified in <u>paragraphs (a)(1)(i)(A)</u>, (B), and (C) of this section.

(A) To an outlet TOC concentration of 20 parts per million by volume (ppmv) or less.

(B) To an outlet concentration of hydrogen halide and halogen HAP of 20 ppmv or less.

(C) As an alternative to <u>paragraph (a)(1)(i)(B)</u> of this section, if you control halogenated vent streams emitted from a combustion device followed by a scrubber, reduce the hydrogen halide and halogen HAP generated in the combustion device by greater than or equal to 95 percent by weight in the scrubber.

(ii) If you use a noncombustion control device(s), it must reduce HAP emissions to an outlet total organic HAP concentration of 50 ppmv or less, and an outlet concentration of hydrogen halide and halogen HAP of 50 ppmv or less.

(2) Any Group 1 process vents within a process that are not controlled according to this alternative standard must be controlled according to the emission limits in tables 1 through 3 to this subpart.

(b) Compliance requirements. To demonstrate compliance with <u>paragraph (a)</u> of this section, you must meet the requirements of  $\S$  63.1258(b)(5) beginning no later than the initial compliance date specified in  $\S$  63.2445, except as specified in <u>paragraphs (b)(1)</u> through (9) of this section.

(1) You must comply with the requirements in  $\frac{63.2450(e)(4)}{6}$  and  $\frac{6}{6}$ , and the requirements in  $\frac{63.983}{63.983}$  and the requirements referenced therein for closed-vent systems, except if you are not reducing organic HAP emissions by venting emissions through a closed-vent system to any combination of control devices, including a flare or recovery device, you are not required to comply with the requirements in  $\frac{63.983(b)(1)(i)(A)}{(b)(1)(i)(A)}$ ,  $\frac{(b)(1)(ii)}{(b)(1)(ii)}$ , and  $\frac{(d)(2)}{(d)}$  and  $\frac{(3)}{(3)}$ .

(2) When  $\S 63.1258(b)(5)(i)$  refers to  $\S\S 63.1253(d)$  and 63.1254(c), the requirements in paragraph (a) of this section apply for the purposes of this subpart FFFF.

(3) When  $\frac{63.1258(b)(5)(i)(B)}{(5)(i)(B)}$  refers to "HCl," it means "total hydrogen halide and halogen HAP" for the purposes of this subpart FFFF.

(4) When  $\S 63.1258(b)(5)(ii)$  refers to  $\S 63.1257(a)(3)$ , it means  $\S 63.2450(j)(5)$  for the purposes of this subpart FFFF.

(5) You must submit the results of any determination of the target analytes of predominant HAP in the notification of compliance status report.

(6) If you elect to comply with the requirement to reduce hydrogen halide and halogen HAP by greater than or equal to 95 percent by weight in <u>paragraph (a)(1)(i)(C)</u> of this section, you must meet the requirements in <u>paragraphs (b)(6)(i)</u> and <u>(ii)</u> of this section.

(i) Demonstrate initial compliance with the 95-percent reduction by conducting a performance test and setting a site-specific operating limit(s) for the scrubber in accordance with the requirements in  $\S 63.2450(e)(4)$  and the requirements of  $\S 63.994$  and the requirements referenced therein. You must submit the results of the initial compliance demonstration in the notification of compliance status report. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with  $\S 63.2520(f)$ , the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the notification of compliance status report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(ii) Install, operate, and maintain CPMS for the scrubber as specified in  $\frac{\&\& 63.994(c)}{(b)}$  and  $\frac{63.2450(k)}{(b)(c)}$ , instead of as specified in  $\frac{\& 63.1258(b)(5)(i)(C)}{(c)}$ . You must also comply with the requirements in  $\frac{\& 63.2450(e)(4)}{(c)}$ , as applicable.

(7) If flow to the scrubber could be intermittent, you must install, calibrate, and operate a flow indicator as specified in  $\frac{5}{63.2460(c)(7)}$ .

(8) Use the operating day as the averaging period for CEMS data and scrubber parameter monitoring data.

(9) The requirements in <u>paragraph (a)</u> of this section do not apply to emissions from storage tanks during periods of planned routine maintenance of the control device that do not exceed 240 hr/yr. You may submit an application to the Administrator requesting an extension of this time limit to a total of 360 hr/yr in accordance with the procedures specified in § 63.2470(d). You must comply with the recordkeeping and reporting specified in §§ 63.998(d)(2)(ii) and 63.999(c)(4) for periods of planned routine maintenance.

[68 FR 63888, Nov. 10, 2003, as amended at 70 FR 38559, July 1, 2005; 85 FR 49150, Aug. 12, 2020]

# Notification, Reports, and Records

# § 63.2515 What notifications must I submit and when?

(a) *General.* Except as specified in <u>paragraph (d)</u> of this section, you must submit all of the notifications in  $\underline{\$\$}$ <u>63.6(h)(4)</u> and (<u>5)</u>, <u>63.7(b)</u> and (<u>c)</u>, <u>63.8(e)</u> and (<u>f)(4)</u> and (<u>6)</u>, and <u>63.9(b)</u> through (<u>h)</u> of subpart A that apply to you by the dates specified.

#### (b) Initial notification.

(1) As specified in  $\frac{63.9(b)(2)}{10}$ , if you startup your affected source before November 10, 2003, you must submit an initial notification not later than 120 calendar days after November 10, 2003, or no later than 120 days after the source becomes subject to this subpart, whichever is later.

(2) As specified in  $\frac{63.9(b)(3)}{100}$ , if you startup your new affected source on or after November 10, 2003, you must submit an initial notification not later than 120 calendar days after you become subject to this subpart.

(c) *Notification of performance test.* If you are required to conduct a performance test, you must submit a notification of intent to conduct a performance test at least 60 calendar days before the performance test is scheduled to begin as required in  $\frac{63.7(b)(1)}{10}$ . For any performance test required as part of the initial compliance procedures for batch process vents in table 2 to this subpart, you must also submit the test plan required by  $\frac{63.7(c)}{10}$  and the emission profile with the notification of the performance test.

(d) Supplement to Notification of Compliance Status. You must also submit supplements to the Notification of Compliance Status as specified in  $\frac{63.2520(d)(3)}{6}$  through (6).

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>85 FR 49150</u>, Aug. 12, 2020; <u>85 FR 73903</u>, Nov. 19, 2020; <u>89 FR 23870</u>, Apr. 4, 2024]

# § 63.2520 What reports must I submit and when?

(a) You must submit each report in Table 11 to this subpart that applies to you.

(b) Unless the Administrator has approved a different schedule for submission of reports under  $\frac{63.10(a)}{(5)}$ , you must submit each report by the date in table 11 to this subpart and according to paragraphs (b)(1) through (5) of this section.

(1) The first compliance report must cover the period beginning on the compliance date that is specified for your affected source in  $\S 63.2445$  and ending on June 30 or December 31, whichever date is the first date following the end of the first 6 months after the compliance date that is specified for your affected source in  $\S 63.2445$ .

(2) The first compliance report must be postmarked or delivered no later than August 31 or February 28, whichever date is the first date following the end of the first reporting period specified in <u>paragraph (b)(1)</u> of this section.

(3) Each subsequent compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31.

(4) Each subsequent compliance report must be postmarked or delivered no later than August 31 or February 28, whichever date is the first date following the end of the semiannual reporting period.

(5) For each affected source that is subject to permitting regulations pursuant to  $\frac{40 \text{ CFR part 70}}{40 \text{ CFR part 71}}$ , and if the permitting authority has established dates for submitting semiannual reports pursuant to  $\frac{40 \text{ CFR part 70}}{40 \text{ CFR 70.6(a)(3)(iii)(A)}}$ , or  $\frac{40 \text{ CFR part 71}}{40 \text{ CFR 70.6(a)(3)(iii)(A)}}$ , or  $\frac{40 \text{ CFR 70.6(a)(3)(iii)(A)}}{40 \text{ CFR 70.6(a)(3)(iii)(A)}}$ , or  $\frac{40 \text{ CFR 70.6(a)(3)(iii)(A)}}{40 \text{ CFR 70.6(a)(3)(iii)(A)}}$ , or  $\frac{40 \text{ CFR 70.6(a)(3)(iii)(A)}}{40 \text{ CFR 70.6(a)(3)(iii)(A)}}$ , and if the first and subsequent compliance reports according to the dates the permitting authority has established instead of according to the dates in paragraphs (b)(1) through (4) of this section.

(c) *Precompliance report.* You must submit a precompliance report to request approval for any of the items in <u>paragraphs</u> (c)(1) through (8) of this section. We will either approve or disapprove the report within 90 days after we receive it. If we

disapprove the report, you must still be in compliance with the emission limitations and work practice standards in this subpart by the compliance date. To change any of the information submitted in the report, you must notify us 60 days before the planned change is to be implemented.

(1) Requests for approval to set operating limits for parameters other than those specified in  $\frac{\$\$ 63.2455}{\$!}$  through  $\frac{63.2485}{\$!}$  and referenced therein. Alternatively, you may make these requests according to  $\frac{\$!63.8(f)}{\$!}$ .

(2) Descriptions of daily or per batch demonstrations to verify that control devices subject to  $\frac{63.2450(k)(6)}{2}$  are operating as designed.

(3) A description of the test conditions, data, calculations, and other information used to establish operating limits according to  $\frac{63.2460(c)(3)}{2}$ .

(4) Data and rationale used to support an engineering assessment to calculate uncontrolled emissions in accordance with  $\S$  <u>63.1257(d)(2)(ii)</u>. This requirement does not apply to calculations of hydrogen halide and halogen HAP emissions as specified in  $\S$  <u>63.2465(b)</u>, to determinations that the total HAP concentration is less than 50 ppmv, or if you use previous test data to establish the uncontrolled emissions.

(5) The pollution prevention demonstration plan required in  $\S$  <u>63.2495(c)(1)</u>, if you are complying with the pollution prevention alternative.

(6) Documentation of the practices that you will implement to minimize HAP emissions from streams that contain energetics and organic peroxides, and rationale for why meeting the emission limit specified in tables 1 through 7 to this subpart would create an undue safety hazard.

(7) For fabric filters that are monitored with bag leak detectors, an operation and maintenance plan that describes proper operation and maintenance procedures, and a corrective action plan that describes corrective actions to be taken, and the timing of those actions, when the PM concentration exceeds the set point and activates the alarm.

(8) For halogen reduction device other than a scrubber, procedures for establishing monitoring parameters as required by  $\underline{\$}$  <u>63.2450(e)(3)(ii)</u>.

(d) Notification of compliance status report. You must submit a notification of compliance status report according to the schedule in paragraph (d)(1) of this section, and the notification of compliance status report must contain the information specified in paragraphs (d)(2) through ( $\underline{6}$ ) of this section.

(1) You must submit the notification of compliance status report no later than 150 days after the applicable compliance date specified in § 63.2445.

(2) The notification of compliance status report must include the information in <u>paragraphs (d)(2)(i)</u> through (ix) of this section.

(i) The results of any applicability determinations, emission calculations, or analyses used to identify and quantify HAP usage or HAP emissions from the affected source.

(ii) The results of emissions profiles, performance tests, engineering analyses, design evaluations, flare compliance assessments, inspections and repairs, and calculations used to demonstrate initial compliance according to  $\underline{\$\$}$  <u>63.2455</u> through <u>63.2485</u>. For performance tests, results must include descriptions of sampling and analysis procedures and quality assurance procedures. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with <u>paragraph (f)</u> of this section, the process unit(s) tested, the pollutant(s) tested, and the date that such performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(iii) Descriptions of monitoring devices, monitoring frequencies, and the operating limits established during the initial compliance demonstrations, including data and calculations to support the levels you establish.

(iv) All operating scenarios.

(v) Descriptions of worst-case operating and/or testing conditions for control devices.

(vi) Identification of parts of the affected source subject to overlapping requirements described in  $\frac{63.2535}{3}$  and the authority under which you will comply.

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(vii) The information specified in  $\S$  63.1039(a)(1) through (3) for each process subject to the work practice standards for equipment leaks in Table 6 to this subpart.

(viii) Identify storage tanks for which you are complying with the vapor balancing alternative in § 63.2470(e).

(ix) Records as specified in  $\frac{63.2535(1)(1)}{10}$  through (3) of process units used to create a PUG and calculations of the initial primary product of the PUG.

(3) For flares subject to the requirements of  $\S$  63.2450(e)(5), you must also submit the information in this paragraph (d)(3) in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date for flare monitoring. In lieu of the information required in  $\S$  63.987(b) of subpart SS, the supplement to the Notification of Compliance Status must include flare design (*e.g.*, steam-assisted, air-assisted, non-assisted, or pressure-assisted multi-point); all visible emission readings, heat content determinations, flow rate measurements, and exit velocity determinations made during the initial visible emissions demonstration required by  $\S$  63.670(h) of subpart CC, as applicable; and all periods during the compliance determination when the pilot flame or flare flame is absent.

(4) For pressure relief devices subject to the pressure release management work practice standards in  $\frac{63.2480(e)(3)}{63.2480(e)(3)}$ , you must also submit the information listed in <u>paragraphs (d)(4)(i)</u> and <u>(ii)</u> of this section in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date for pressure relief device monitoring.

(i) A description of the monitoring system to be implemented, including the relief devices and process parameters to be monitored, and a description of the alarms or other methods by which operators will be notified of a pressure release.

(ii) A description of the prevention measures to be implemented for each affected pressure relief device.

(5) For process vents, storage tanks, and equipment leaks subject to the requirements of § 63.2493, you must also submit the information in this paragraph (d)(5) in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date. The supplement to the Notification of Compliance Status must identify all process vents, storage tanks, and equipment that are in ethylene oxide service as defined in § 63.2550, the method(s) used to control ethylene oxide emissions from each process vent and storage tank (*i.e.*, use of a flare, scrubber, or other control device), the method(s) used to control ethylene oxide emissions from equipment (*i.e.*, subpart UU or H of this part, or 40 CFR part 65, subpart F), and the information specified in paragraphs (d)(5)(i) through (iii) of this section.

(i) For process vents, include all uncontrolled, undiluted ethylene oxide concentration measurements, and the calculations you used to determine the total uncontrolled ethylene oxide mass emission rate for the sum of all vent gas streams.

(ii) For storage tanks, include the concentration of ethylene oxide of the fluid stored in each storage tank.

(iii) For equipment, include the percent ethylene oxide content of the process fluid and the method used to determine it.

(6) For adsorbers subject to the requirements of  $\S$  <u>63.2450(e)(7)</u>, you must also submit the information listed in <u>paragraphs</u> (<u>d)(6)(i)</u> and (<u>ii)</u> of this section in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date.

(i) Whether the adsorber cannot be regenerated or is a regenerative adsorber(s) that is regenerated off site.

(ii) The breakthrough limit and adsorber bed life established during the initial performance test or design evaluation of the adsorber.

(e) Compliance report. The compliance report must contain the information specified in paragraphs (e)(1) through (17) of this section. On and after August 12, 2023 or once the reporting template for this subpart has been available on the CEDRI website for 1 year, whichever date is later, you must submit all subsequent reports following the procedure specified in § 63.9(k), except any medium submitted through mail must be sent to the attention of the Miscellaneous Organic Chemical Manufacturing Sector Lead. You must use the appropriate electronic report template on the CEDRI website (https://www.epa.gov/electronic-reporting-air-emissions/cedri) for this subpart. The date report templates become available will be listed on the CEDRI website. Unless the Administrator or delegated state agency or other authority has approved a different schedule for submission of reports under §§ 63.9(i) and 63.10(a) of subpart A, the report must be submitted by the deadline specified in this subpart, regardless of the method in which the report is submitted.

(1) Company name and address.

(2) Statement by a responsible official with that official's name, title, and signature, certifying the accuracy of the content of the report. If your report is submitted via CEDRI, the certifier's electronic signature during the submission process replaces the requirement in this paragraph (e)(2).

(3) Date of report and beginning and ending dates of the reporting period. You are no longer required to provide the date of report when the report is submitted via CEDRI.

(4) For each SSM during which excess emissions occur, the compliance report must include records that the procedures specified in your startup, shutdown, and malfunction plan (SSMP) were followed or documentation of actions taken that are not consistent with the SSMP, and include a brief description of each malfunction. On and after August 12, 2023, this <u>paragraph (e)(4)</u> no longer applies; however, for historical compliance purposes, a copy of the plan must be retained and available on-site for five years after August 12, 2023.

(5) The compliance report must contain the information on deviations, as defined in § 63.2550, according to paragraphs (e)(5)(i), (ii), (iii), and (iv) of this section.

(i) If there are no deviations from any emission limit, operating limit or work practice standard specified in this subpart, include a statement that there were no deviations from the emission limits, operating limits, or work practice standards during the reporting period.

(ii) For each deviation from an emission limit, operating limit, and work practice standard that occurs at an affected source where you are not using a continuous monitoring system (CMS) to comply with the emission limit or work practice standard in this subpart, you must include the information in paragraphs (e)(5)(ii)(A) through (D) of this section. This includes periods of SSM.

(A) The total operating time in hours of the affected source during the reporting period.

(B) Except as specified in <u>paragraph (e)(5)(ii)(D)</u> of this section, information on the number, duration, and cause of deviations (including unknown cause, if applicable), as applicable, and the corrective action taken.

(C) Operating logs of processes with batch vents from batch operations for the day(s) during which the deviation occurred, except operating logs are not required for deviations of the work practice standards for equipment leaks.

(D) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , paragraph (e)(5)(ii)(B) of this section no longer applies. Instead, report information for each deviation to meet an applicable standard. For each instance, report the start date, start time, and duration in hours of each deviation. For each deviation, the report must include a list of the affected sources or equipment, an estimate of the quantity in pounds of each regulated pollutant emitted over any emission limit, a description of the method used to estimate the emissions, the cause of the deviation (including unknown cause, if applicable), as applicable, and the corrective action taken.

(iii) For each deviation from an emission limit or operating limit occurring at an affected source where you are using a CMS to comply with an emission limit in this subpart, you must include the information in <u>paragraphs (e)(5)(iii)(A)</u> through (N) of this section. This includes periods of SSM.

(A) The start date, start time, and duration in hours that each CMS was inoperative, except for zero (low-level) and high-level checks.

(B) The start date, start time, and duration in hours that each CEMS was out-of-control and a description of the corrective actions taken.

(C) Except as specified in <u>paragraph (e)(5)(iii)(M)</u> of this section, the date and time that each deviation started and stopped, and whether each deviation occurred during a period of startup, shutdown, or malfunction or during another period.

(D) The total duration in hours of all deviations for each CMS during the reporting period, the total operating time in hours of the affected source during the reporting period, and the total duration as a percent of the total operating time of the affected source during that reporting period.

(E) Except as specified in <u>paragraph (e)(5)(iii)(N)</u> of this section, a breakdown of the total duration of the deviations during the reporting period into those that are due to startup, shutdown, control equipment problems, process problems, other known causes, and other unknown causes.

(F) The total duration in hours of CMS downtime for each CMS during the reporting period, and the total duration of CMS downtime as a percent of the total operating time of the affected source during that reporting period.

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(G) An identification of each HAP that is known to be in the emission stream.

(H) A brief description of the process units.

(I) The monitoring equipment manufacturer(s) and model number(s) and the pollutant or parameter monitored.

(J) The date of the latest CMS certification or audit.

(K) Operating logs of processes with batch vents from batch operations for each day(s) during which the deviation occurred.

(L) The operating day or operating block average values of monitored parameters for each day(s) during which the deviation occurred.

(M) Beginning no later than the compliance dates specified in  $\S$  <u>63.2445(g)</u>, <u>paragraph (e)(5)(iii)(C)</u> of this section no longer applies. Instead, report the number of deviation to meet an applicable standard. For each instance, report the start date, start time and duration in hours of each deviation. For each deviation, the report must include a list of the affected sources or equipment, an estimate of the quantity in pounds of each regulated pollutant emitted over any emission limit, a description of the method used to estimate the emissions, and the cause of the deviation (including unknown cause, if applicable), as applicable, and the corrective action taken.

(N) Beginning no later than the compliance dates specified in  $\S$  63.2445(g), paragraph (e)(5)(iii)(E) of this section no longer applies. Instead, report a breakdown of the total duration in hours of the deviations during the reporting period into those that are due control equipment problems, process problems, other known causes, and other unknown causes.

(iv) If you documented in your notification of compliance status report that an MCPU has Group 2 batch process vents because the non-reactive HAP is the only HAP and usage is less than 10,000 lb/yr, the total uncontrolled organic HAP emissions from the batch process vents in an MCPU will be less than 1,000 lb/yr for the anticipated number of standard batches, or total uncontrolled hydrogen halide and halogen HAP emissions from all batch process vents and continuous process vents in a process are less than 1,000 lb/yr, include the records associated with each calculation required by  $\underline{\$}$  <u>63.2525(e)</u> that exceeds an applicable HAP usage or emissions threshold.

(6) If you use a CEMS, and there were no periods during which it was out-of-control as specified in  $\frac{63.8(c)(7)}{1000}$ , include a statement that there were no periods during which the CEMS was out-of-control during the reporting period.

(7) Include each new operating scenario which has been operated since the time period covered by the last compliance report and has not been submitted in the notification of compliance status report or a previous compliance report. For each new operating scenario, you must report the information specified in § 63.2525(b) and provide verification that the operating conditions for any associated control or treatment device have not been exceeded and that any required calculations and engineering analyses have been performed. For the purposes of this <u>paragraph (e)(7)</u>, a revised operating scenario for an existing process is considered to be a new operating scenario.

(8) For process units added to a PUG, you must report the description and rationale specified in  $\frac{63.2525(i)(4)}{50.2525(i)(5)}$ . You must report your primary product redeterminations specified in  $\frac{63.2525(i)(5)}{50.2525(i)(5)}$ .

(9) Except as specified in  $\S$  63.2450(e)(4), 63.2480(f), and 63.2485(p) and (q) and paragraph (t) of this section, applicable records and information for periodic reports as specified in referenced subparts F, G, H, SS, UU, WW, and GGG of this part and subpart F of 40 CFR part 65.

(10) Except as specified in paragraph (e)(10)(ii) of this section, whenever you make a process change, or change any of the information submitted in the notification of compliance status report or a previous compliance report, that is not within the scope of an existing operating scenario, you must document the change in your compliance report. A process change does not include moving within a range of conditions identified in the standard batch, and a nonstandard batch does not constitute a process change.

(i) The notification must include all of the information in <u>paragraphs (e)(10)(i)(A)</u> through (C) of this section.

(A) A description of the process change.

(B) Revisions to any of the information reported in the original notification of compliance status report under <u>paragraph</u> (d) of this section.

(C) Information required by the notification of compliance status report under <u>paragraph (d)</u> of this section for changes involving the addition of processes or equipment at the affected source.
(ii) You must submit a report 60 days before the scheduled implementation date of any of the changes identified in <u>paragraph</u> (e)(10)(ii)(A), (B), or (C) of this section.

(A) Any change to the information contained in the precompliance report.

(B) A change in the status of a control device from small to large.

(C) A change from Group 2 to Group 1 for any emission point except for batch process vents that meet the conditions specified in  $\frac{63.2460(b)(6)(i)}{6}$ .

(11) For each flare subject to the requirements in  $\S 63.2450(e)(5)$ , the compliance report must include the items specified in paragraphs (e)(11)(i) through (vi) of this section in lieu of the information required in  $\S 63.999(c)(3)$  of subpart SS.

(i) Records as specified in  $\S$  63.2525(m)(1) for each 15-minute block during which there was at least one minute when regulated material is routed to a flare and no pilot flame or flare flame is present. Include the start and stop time and date of each 15-minute block.

(ii) Visible emission records as specified in  $\frac{63.2525(m)(2)(iv)}{5}$  for each period of 2 consecutive hours during which visible emissions exceeded a total of 5 minutes.

(iii) The periods specified in  $\frac{63.2525(m)}{6}$ . Indicate the date and start and end times for each period, and the net heating value operating parameter(s) determined following the methods in  $\frac{63.670(k)}{10}$  through (n) of subpart CC as applicable.

(iv) For flaring events meeting the criteria in  $\frac{\$\$ 63.670(0)(3)}{\$}$  of subpart CC and 63.2450(e)(5)(v):

(A) The start and stop time and date of the flaring event.

(B) The length of time in minutes for which emissions were visible from the flare during the event.

(C) For steam-assisted, air-assisted, and non-assisted flares, the start date, start time, and duration in minutes for periods of time that the flare tip velocity exceeds the maximum flare tip velocity determined using the methods in  $\frac{63.670(d)(2)}{2}$  of subpart CC and the maximum 15-minute block average flare tip velocity in ft/sec recorded during the event.

(D) Results of the root cause and corrective actions analysis completed during the reporting period, including the corrective actions implemented during the reporting period and, if applicable, the implementation schedule for planned corrective actions to be implemented subsequent to the reporting period.

(v) For pressure-assisted multi-point flares, the periods of time when the pressure monitor(s) on the main flare header show the burners operating outside the range of the manufacturer's specifications. Indicate the date and start and end times for each period.

(vi) For pressure-assisted multi-point flares, the periods of time when the staging valve position indicator monitoring system indicates a stage should not be in operation and is or when a stage should be in operation and is not. Indicate the date and start and end times for each period.

(12) For bypass lines subject to the requirements  $\frac{63.2450(e)(6)}{6}$ , the compliance report must include the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours.

(13) For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in § 63.2450(e)(7), you must report the date of each instance when breakthrough, as defined in § 63.2550(i), is detected between the first and second adsorber and the adsorber is not replaced according to § 63.2450(e)(7)(iii)(A).

(14) For any maintenance vent release exceeding the applicable limits in  $\frac{63.2450(v)(1)}{50.2450(v)(1)}$ , the compliance report must include the information specified in paragraphs (e)(14)(i) through (iv) of this section. For the purposes of this reporting requirement, if you comply with  $\frac{63.2450(v)(1)(iv)}{50.2450(v)(1)(iv)}$  then you must report each venting event conducted under those provisions and include an explanation for each event as to why utilization of this alternative was required.

(i) Identification of the maintenance vent and the equipment served by the maintenance vent.

(ii) The date and time the maintenance vent was opened to the atmosphere.

(iii) The lower explosive limit in percent, vessel pressure in psig, or mass in pounds of VOC in the equipment, as applicable, at the start of atmospheric venting. If the 5 psig vessel pressure option in  $\frac{63.2450(v)(1)(ii)}{100}$  was used and active purging was

initiated while the concentration of the vapor was 10 percent or greater of its LEL, also include the concentration of the vapors at the time active purging was initiated.

(iv) An estimate of the mass in pounds of organic HAP released during the entire atmospheric venting event.

(15) Compliance reports for pressure relief devices subject to the requirements  $\frac{63.2480(e)}{15}$  must include the information specified in paragraphs (e)(15)(i) through (iii) of this section.

(i) For pressure relief devices in organic HAP gas or vapor service, pursuant to  $\frac{63.2480(e)(1)}{1000}$ , report the instrument readings and dates for all readings of 500 ppmv or greater.

(ii) For pressure relief devices in organic HAP gas or vapor service subject to  $\frac{63.2480(e)(2)}{2}$ , report the instrument readings and dates of instrument monitoring conducted.

(iii) For pressure relief devices in organic HAP service subject to  $\frac{63.2480(e)(3)}{2}$ , report each pressure release to the atmosphere, including the start date, start time, and duration in minutes of the pressure release and an estimate of the mass quantity in pounds of each organic HAP released; the results of any root cause analysis and corrective action analysis completed during the reporting period, including the corrective actions implemented during the reporting period; and, if applicable, the implementation schedule for planned corrective actions to be implemented subsequent to the reporting period.

(16) For each heat exchange system subject to  $\S 63.2490(d)$  or (e), beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , the reporting requirements of  $\S 63.104(f)(2)$  no longer apply; instead, the compliance report must include the information specified in paragraphs (e)(16)(i) through (v) of this section.

(i) The number of heat exchange systems at the plant site subject to the monitoring requirements in  $\frac{63.2490(d)}{2}$  or (e) during the reporting period;

(ii) The number of heat exchange systems subject to the monitoring requirements in  $\S 63.2490(d)$  or (e) at the plant site found to be leaking during the reporting period;

(iii) For each monitoring location where a leak was identified during the reporting period, identification of the monitoring location (e.g., unique monitoring location or heat exchange system ID number), the measured total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with  $\S$  63.2490(d)) or the measured concentration of the monitored substance(s) (if complying with  $\S$  63.2490(e)), the date the leak was first identified, and, if applicable, the date the source of the leak was identified;

(iv) For leaks that were repaired during the reporting period (including delayed repairs), identification of the monitoring location associated with the repaired leak, the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with  $\S$  63.2490(d)) or the measured concentration of the monitored substance(s) (if complying with  $\S$  63.2490(c)) measured during re-monitoring to verify repair, and the re-monitoring date (*i.e.*, the effective date of repair); and

(v) For each delayed repair, identification of the monitoring location associated with the leak for which repair is delayed, the date when the delay of repair began, the date the repair is expected to be completed (if the leak is not repaired during the reporting period), the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with  $\frac{63.2490(d)}{10}$ ) or the measured concentration of the monitored substance(s) (if complying with  $\frac{63.2490(e)}{10}$ ) and date of each monitoring event conducted on the delayed repair during the reporting period, and an estimate in pounds of the potential total hydrocarbon emissions or monitored substance(s) emissions over the reporting period associated with the delayed repair.

(16) For each heat exchange system subject to  $\S 63.2490(d)$  or (e), beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , the reporting requirements of  $\S 63.104(f)(2)$  no longer apply; instead, the compliance report must include the information specified in paragraphs (e)(16)(i) through (v) of this section.

(i) The number of heat exchange systems at the plant site subject to the monitoring requirements in  $\frac{63.2490(d)}{2}$  or (e) during the reporting period;

(ii) The number of heat exchange systems subject to the monitoring requirements in  $\S 63.2490(d)$  or (e) at the plant site found to be leaking during the reporting period;

(iii) For each monitoring location where a leak was identified during the reporting period, identification of the monitoring location (e.g., unique monitoring location or heat exchange system ID number), the measured total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with  $\S$  63.2490(d)) or the measured concentration of

the monitored substance(s) (if complying with  $\S$  63.2490(e)), the date the leak was first identified, and, if applicable, the date the source of the leak was identified;

(iv) For leaks that were repaired during the reporting period (including delayed repairs), identification of the monitoring location associated with the repaired leak, the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with  $\S$  63.2490(d)) or the measured concentration of the monitored substance(s) (if complying with  $\S$  63.2490(e)) measured during re-monitoring to verify repair, and the re-monitoring date (*i.e.*, the effective date of repair); and

(v) For each delayed repair, identification of the monitoring location associated with the leak for which repair is delayed, the date when the delay of repair began, the date the repair is expected to be completed (if the leak is not repaired during the reporting period), the total strippable hydrocarbon concentration or total hydrocarbon mass emissions rate (if complying with  $\S 63.2490(d)$ ) or the measured concentration of the monitored substance(s) (if complying with  $\S 63.2490(e)$ ) and date of each monitoring event conducted on the delayed repair during the reporting period, and an estimate in pounds of the potential total hydrocarbon emissions or monitored substance(s) emissions over the reporting period associated with the delayed repair.

(17) For process vents and storage tanks in ethylene oxide service subject to the requirements of  $\S$  63.2493, the compliance report must include:

(i) The periods specified in  $\S 63.2525(s)(4)$ . Indicate the date and start and end times for each period.

(ii) If you obtain an instrument reading greater than 500 ppmv of a leak when monitoring a pressure vessel in accordance with  $\frac{63.2493(c)(2)}{5}$ , submit a copy of the records specified in  $\frac{63.2525(s)(5)(ii)}{5}$ .

(iii) Reports for equipment subject to the requirements of  $\frac{63.2493}{2}$  as specified in <u>paragraph (e)(9)</u> of this section.

(f) *Performance test reports*. Beginning no later than October 13, 2020, you must submit performance test reports in accordance with this <u>paragraph (f)</u>. Unless otherwise specified in this subpart, within 60 days after the date of completing each performance test required by this subpart, you must submit the results of the performance test following the procedures specified in § 63.9(k). Data collected using test methods supported by the EPA's Electronic Reporting Tool (ERT) as listed on the EPA's ERT website (*https://www.epa.gov/electronic-reporting-air-emissions/electronic-reporting-tool-ert*) at the time of the test must be submitted in a file format generated through the use of the EPA's ERT. Alternatively, you may submit an electronic file consistent with the extensible markup language (XML) schema listed on the EPA's ERT website. Data collected using test methods that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the test must be included as an attachment in the ERT or alternate electronic file.

(g) *CEMS relative accuracy test audit (RATA) Performance evaluation reports.* Beginning no later than October 13, 2020, you must start submitting CEMS RATA performance evaluation reports in accordance with this <u>paragraph (g)</u>. Unless otherwise specified in this subpart, within 60 days after the date of completing each continuous monitoring system performance evaluation (as defined in § 63.2) that includes a RATA, you must submit the results of the performance evaluation following the procedures specified in § 63.9(k). The results of performance evaluations of CEMS measuring RATA pollutants that are supported by the EPA's ERT as listed on the EPA's ERT website at the time of the evaluation must be submitted in a file format generated through the use of the EPA's ERT. Alternatively, you may submit an electronic file consistent with the XML schema listed on the EPA's ERT as listed on the EPA's ERT website at the time of CEMS measuring RATA pollutants that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the evaluations of CEMS measuring RATA pollutants that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the evaluations of CEMS measuring RATA pollutants that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the evaluation for the evaluation must be included as an attachment in the ERT or alternate electronic file.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>70 FR 38560</u>, July 1, 2005; <u>71 FR 40336</u>, July 14, 2006; <u>85 FR 49150</u>, Aug. 12, 2020; <u>89 FR 23871</u>, Apr. 4, 2024]

#### § 63.2525 What records must I keep?

You must keep the records specified in paragraphs (a) through (t) of this section.

(a) Except as specified in  $\frac{\$\$}{63.2450(e)(4)}$ ,  $\frac{63.2480(f)}{63.2480(f)}$ , and  $\frac{63.2485(p)}{63.2485(p)}$  and  $\frac{(q)}{(q)}$  and  $\frac{$ 

(b) Records of each operating scenario as specified in <u>paragraphs (b)(1)</u> through (8) of this section.

(1) A description of the process and the type of process equipment used.

(2) An identification of related process vents, including their associated emissions episodes if not complying with the alternative standard in  $\S$  63.2505; wastewater point of determination (POD); storage tanks; and transfer racks.

(3) The applicable control requirements of this subpart, including the level of required control, and for vents, the level of control for each vent.

(4) The control device or treatment process used, as applicable, including a description of operating and/or testing conditions for any associated control device.

(5) The process vents, wastewater POD, transfer racks, and storage tanks (including those from other processes) that are simultaneously routed to the control device or treatment process(s).

(6) The applicable monitoring requirements of this subpart and any parametric level that assures compliance for all emissions routed to the control device or treatment process.

(7) Calculations and engineering analyses required to demonstrate compliance.

(8) For reporting purposes, a change to any of these elements not previously reported, except for <u>paragraph (b)(5)</u> of this section, constitutes a new operating scenario.

(c) A schedule or log of operating scenarios for processes with batch vents from batch operations updated each time a different operating scenario is put into effect.

(d) The information specified in <u>paragraphs (d)(1)</u> and (2) of this section for Group 1 batch process vents in compliance with a percent reduction emission limit in Table 2 to this subpart if some of the vents are controlled to less the percent reduction requirement.

(1) Records of whether each batch operated was considered a standard batch.

(2) The estimated uncontrolled and controlled emissions for each batch that is considered to be a nonstandard batch.

(e) The information specified in <u>paragraph (e)(2)</u>, (3), or (4) of this section, as applicable, for each process with Group 2 batch process vents or uncontrolled hydrogen halide and halogen HAP emissions from the sum of all batch and continuous process vents less than 1,000 lb/yr. No records are required for situations described in <u>paragraph (e)(1)</u> of this section.

(1) No records are required if you documented in your notification of compliance status report that the MCPU meets any of the situations described in <u>paragraph (e)(1)(i)</u>, (ii), or (iii) of this section.

(i) The MCPU does not process, use, or generate HAP.

(ii) You control the Group 2 batch process vents using a flare that meets the requirements of  $\S 63.987$  or  $\S 63.2450(e)(5)$ , as applicable.

(iii) You control the Group 2 batch process vents using a control device for which your determination of worst case for initial compliance includes the contribution of all Group 2 batch process vents.

(2) If you documented in your notification of compliance status report that an MCPU has Group 2 batch process vents because the non-reactive organic HAP is the only HAP and usage is less than 10,000 lb/yr, as specified in  $\frac{63.2460(b)(7)}{1000}$ , you must keep records of the amount of HAP material used, and calculate the daily rolling annual sum of the amount used no less frequently than monthly. If a record indicates usage exceeds 10,000 lb/yr, you must estimate emissions for the preceding 12 months based on the number of batches operated and the estimated emissions for a standard batch, and you must begin recordkeeping as specified in paragraph (e)(4) of this section. After 1 year, you may revert to recording only usage if the usage during the year is less than 10,000 lb.

(3) If you documented in your notification of compliance status report that total uncontrolled organic HAP emissions from the batch process vents in an MCPU will be less than 1,000 lb/yr for the anticipated number of standard batches, then you must keep records of the number of batches operated and calculate a daily rolling annual sum of batches operated no less frequently than monthly. If the number of batches operated results in organic HAP emissions that exceed 1,000 lb/yr, you must estimate emissions for the preceding 12 months based on the number of batches operated and the estimated emissions for a standard batch, and you must begin recordkeeping as specified in paragraph (e)(4) of this section. After 1 year, you may revert to recording only the number of batches if the number of batches operated during the year results in less than 1,000 lb of organic HAP emissions.

(4) If you meet none of the conditions specified in <u>paragraphs (e)(1)</u> through (3) of this section, you must keep records of the information specified in <u>paragraphs (e)(4)(i)</u> through (iv) of this section.

(i) A record of the day each batch was completed and/or the operating hours per day for continuous operations with hydrogen halide and halogen emissions.

(ii) A record of whether each batch operated was considered a standard batch.

(iii) The estimated uncontrolled and controlled emissions for each batch that is considered to be a nonstandard batch.

(iv) Records of the daily 365-day rolling summations of emissions, or alternative records that correlate to the emissions (e.g., number of batches), calculated no less frequently than monthly.

(f) A record of each time a safety device is opened to avoid unsafe conditions in accordance with <u>§ 63.2450(p)</u>.

(g) Records of the results of each CPMS calibration check and the maintenance performed, as specified in § 63.2450(k)(1).

(h) Except as specified in <u>paragraph (l)</u> of this section, for each CEMS, you must keep records of the date and time that each deviation started and stopped, and whether the deviation occurred during a period of startup, shutdown, or malfunction or during another period.

(i) For each PUG, you must keep records specified in <u>paragraphs (i)(1)</u> through (5) of this section.

(1) Descriptions of the MCPU and other process units in the initial PUG required by  $\frac{63.2535(1)(1)(v)}{2}$ .

(2) Rationale for including each MCPU and other process unit in the initial PUG (*i.e.*, identify the overlapping equipment between process units) required by  $\frac{63.2535(1)(1)(v)}{2}$ .

(3) Calculations used to determine the primary product for the initial PUG required by § 63.2535(1)(2)(iv).

(4) Descriptions of process units added to the PUG after the creation date and rationale for including the additional process units in the PUG as required by  $\frac{63.2535(1)(1)(v)}{2}$ .

(5) The calculation of each primary product redetermination required by  $\S$  63.2535(1)(2)(iv).

(j) In the SSMP required by  $\frac{63.6(e)(3)}{10}$  of subpart A, you are not required to include Group 2 emission points, unless those emission points are used in an emissions average. For equipment leaks, the SSMP requirement is limited to control devices and is optional for other equipment. On and after August 12, 2023, this <u>paragraph (j)</u> no longer applies.

(k) For each bag leak detector used to monitor PM HAP emissions from a fabric filter, maintain records of any bag leak detection alarm, including the date and time, with a brief explanation of the cause of the alarm and the corrective action taken.

(1) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , paragraph (h) of this section no longer applies. Instead, for each deviation from an emission limit, operating limit, or work practice standard, you must keep a record of the information specified in paragraph (1)(1) through (3) of this section. The records shall be maintained as specified in  $\S 63.10(b)(1)$  of subpart A.

(1) In the event that an affected unit does not meet an applicable standard, record the number of deviations. For each deviation record the date, time, and duration of each deviation.

(2) For each deviation from an applicable standard, record and retain a list of the affected sources or equipment, an estimate of the quantity of each regulated pollutant emitted over any emission limit and a description of the method used to estimate the emissions.

(3) Record actions taken to minimize emissions in accordance with  $\frac{63.2450(u)}{2}$  and any corrective actions taken to return the affected unit to its normal or usual manner of operation.

(m) For each flare subject to the requirements in  $\frac{63.2450(e)(5)}{63.2450(e)(5)}$ , you must keep records specified in <u>paragraphs</u> (m)(1) through (14) of this section in lieu of the information required in  $\frac{63.998(a)(1)}{63.998(a)(1)}$  of subpart SS.

(1) Retain records of the output of the monitoring device used to detect the presence of a pilot flame or flare flame as required in  $\frac{63.670(b)}{50}$  of subpart CC and the presence of a pilot flame as required in  $\frac{63.2450(c)(5)(viii)(D)}{50}$  for a minimum of 2 years. Retain records of each 15-minute block during which there was at least one minute that no pilot flame or flare flame is present when regulated material is routed to a flare for a minimum of 5 years. For a pressure-assisted multi-point flare that

uses cross-lighting, retain records of each 15-minute block during which there was at least one minute that no pilot flame is present on each stage when regulated material is routed to a flare for a minimum of 5 years. You may reduce the collected minute-by-minute data to a 15-minute block basis with an indication of whether there was at least one minute where no pilot flame or flare flame was present.

(2) Retain records of daily visible emissions observations as specified in <u>paragraphs (m)(2)(i)</u> through (iv) of this section, as applicable, for a minimum of 3 years.

(i) To determine when visible emissions observations are required, the record must identify all periods when regulated material is vented to the flare.

(ii) If visible emissions observations are performed using Method 22 of <u>40 CFR part 60, appendix A</u>-7, then the record must identify whether the visible emissions observation was performed, the results of each observation, total duration of observed visible emissions, and whether it was a 5-minute or 2-hour observation. Record the date and start time of each visible emissions observation.

(iii) If a video surveillance camera is used pursuant to  $\S 63.670(h)(2)$  of subpart CC, then the record must include all video surveillance images recorded, with time and date stamps.

(iv) For each 2 hour period for which visible emissions are observed for more than 5 minutes in 2 consecutive hours, then the record must include the date and start and end time of the 2 hour period and an estimate of the cumulative number of minutes in the 2 hour period for which emissions were visible.

(3) The 15-minute block average cumulative flows for flare vent gas and, if applicable, total steam, perimeter assist air, and premix assist air specified to be monitored under  $\S$  63.670(i) of subpart CC, along with the date and time interval for the 15-minute block. If multiple monitoring locations are used to determine cumulative vent gas flow, total steam, perimeter assist air, and premix assist air, then retain records of the 15-minute block average flows for each monitoring location for a minimum of 2 years, and retain the 15-minute block average cumulative flows that are used in subsequent calculations for a minimum of 5 years. If pressure and temperature monitoring is used, then retain records of the 15-minute block average temperature, pressure, and molecular weight of the flare vent gas or assist gas stream for each measurement location used to determine the 15-minute block average cumulative flows for a minimum of 2 years, and retain the 15-minute flows for a minimum of 2 years, and molecular weight of the flare vent gas or assist gas stream for each measurement location used to determine the 15-minute block average cumulative flows for a minimum of 2 years, and retain the 15-minute block average cumulative flows for a minimum of 2 years.

(4) The flare vent gas compositions specified to be monitored under  $\frac{63.670(j)}{10}$  of subpart CC. Retain records of individual component concentrations from each compositional analysis for a minimum of 2 years. If an NHVvg analyzer is used, retain records of the 15-minute block average values for a minimum of 5 years.

(5) Each 15-minute block average operating parameter calculated following the methods specified in § 63.670(k) through (n) of subpart CC, as applicable.

(6) All periods during which operating values are outside of the applicable operating limits specified in  $\underline{\$\$}$ <u>63.670(d)</u> through (<u>f</u>) of subpart CC and 63.2450(e)(5)(viii) when regulated material is being routed to the flare.

(7) All periods during which you do not perform flare monitoring according to the procedures in  $\S$  63.670(g) through (j) of subpart CC.

(8) For pressure-assisted multi-point flares, if a stage of burners on the flare uses cross-lighting, then a record of any changes made to the distance between burners.

(9) For pressure-assisted multi-point flares, all periods when the pressure monitor(s) on the main flare header show burners are operating outside the range of the manufacturer's specifications. Indicate the date and time for each period, the pressure measurement, the stage(s) and number of burners affected, and the range of manufacturer's specifications.

(10) For pressure-assisted multi-point flares, all periods when the staging valve position indicator monitoring system indicates a stage of the pressure-assisted multi-point flare should not be in operation and when a stage of the pressure-assisted multi-point flare should be in operation and is not. Indicate the date and time for each period, whether the stage was supposed to be open, but was closed or vice versa, and the stage(s) and number of burners affected.

(11) Records of periods when there is flow of vent gas to the flare, but when there is no flow of regulated material to the flare, including the start and stop time and dates of periods of no regulated material flow.

(12) Records when the flow of vent gas exceeds the smokeless capacity of the flare, including start and stop time and dates of the flaring event.

(13) Records of the root cause analysis and corrective action analysis conducted as required in  $\frac{\$\$ 63.670(0)(3)}{\$}$  of subpart CC and 63.2450(e)(5)(v), including an identification of the affected flare, the date and duration of the event, a statement noting whether the event resulted from the same root cause(s) identified in a previous analysis and either a description of the recommended corrective action(s) or an explanation of why corrective action is not necessary under  $\frac{\$ 63.670(0)(5)(i)}{\$}$  of subpart CC.

(14) For any corrective action analysis for which implementation of corrective actions are required in § 63.670(o)(5) of subpart CC, a description of the corrective action(s) completed within the first 45 days following the discharge and, for action(s) not already completed, a schedule for implementation, including proposed commencement and completion dates.

(n) For each flow event from a bypass line subject to the requirements in § 63.2450(e)(6), you must maintain records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requiring control that is released either directly to the atmosphere or to a control device not meeting the requirements specified in Tables 1 through 7 to this subpart, you must include an estimate of the volume of gas, the concentration of organic HAP in the gas and the resulting emissions of organic HAP that bypassed the control device using process knowledge and engineering estimates.

(o) For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in § 63.2450(e)(7), you must keep the applicable records specified in <u>paragraphs (o)(1)</u> through (3) of this section.

(1) Breakthrough limit and bed life established according to § 63.2450(e)(7)(i).

(2) Each outlet HAP or TOC concentration measured according to §§ 63.2450(e)(7)(ii) and (e)(7)(iii).

(3) Date and time you last replaced the adsorbent.

(p) For each maintenance vent opening subject to the requirements in § 63.2450(v), you must keep the applicable records specified in <u>paragraphs (p)(1)</u> through (5) of this section.

(1) You must maintain standard site procedures used to deinventory equipment for safety purposes (*e.g.*, hot work or vessel entry procedures) to document the procedures used to meet the requirements in § 63.2450(v). The current copy of the procedures must be retained and available on-site at all times. Previous versions of the standard site procedures, as applicable, must be retained for five years.

(2) If complying with the requirements of § 63.2450(v)(1)(i) and the concentration of the vapor at the time of the vessel opening exceeds 10 percent of its LEL, identification of the maintenance vent, the process units or equipment associated with the maintenance vent, the date of maintenance vent opening, and the concentration of the vapor at the time of the vessel opening.

(3) If complying with the requirements of § 63.2450(v)(1)(ii) and either the vessel pressure at the time of the vessel opening exceeds 5 psig or the concentration of the vapor at the time of the active purging was initiated exceeds 10 percent of its LEL, identification of the maintenance vent, the process units or equipment associated with the maintenance vent, the date of maintenance vent opening, the pressure of the vessel or equipment at the time of discharge to the atmosphere and, if applicable, the concentration of the vapors in the equipment when active purging was initiated.

(4) If complying with the requirements of § 63.2450(v)(1)(iii), records of the estimating procedures used to determine the total quantity of VOC in the equipment and the type and size limits of equipment that contain less than 50 pounds of VOC at the time of maintenance vent opening. For each maintenance vent opening that contains greater than 50 pounds of VOC for which the deinventory procedures specified in paragraph (p)(1) of this section are not followed or for which the equipment opened exceeds the type and size limits established in the records specified in this paragraph (p)(4), records that identify the maintenance vent, the process units or equipment associated with the maintenance vent, the date of maintenance vent opening, and records used to estimate the total quantity of VOC in the equipment at the time the maintenance vent was opened to the atmosphere.

(5) If complying with the requirements of § 63.2450(v)(1)(iv), identification of the maintenance vent, the process units or equipment associated with the maintenance vent, records documenting actions taken to comply with other applicable alternatives and why utilization of this alternative was required, the date of maintenance vent opening, the equipment pressure and concentration of the vapors in the equipment at the time of discharge, an indication of whether active purging was performed and the pressure of the equipment during the installation or removal of the blind if active purging was used,

the duration the maintenance vent was open during the blind installation or removal process, and records used to estimate the total quantity of VOC in the equipment at the time the maintenance vent was opened to the atmosphere for each applicable maintenance vent opening.

(q) For each pressure relief device subject to the pressure release management work practice standards in § 63.2480(e), you must keep the records specified in <u>paragraphs (q)(1)</u> through (3) of this section.

(1) Records of the prevention measures implemented as required in § 63.2480(e)(3)(ii).

(2) Records of the number of releases during each calendar year and, prior to June 3, 2024, the number of those releases for which the root cause was determined to be a *force majeure* event. Keep these records for the current calendar year and the past 5 calendar years.

(3) For each release to the atmosphere, you must keep the records specified in <u>paragraphs (q)(3)(i)</u> through (iv) of this section.

(i) The start and end time and date of each pressure release to the atmosphere.

(ii) Records of any data, assumptions, and calculations used to estimate of the mass quantity of each organic HAP released during the event.

(iii) Records of the root cause analysis and corrective action analysis conducted as required in § 63.2480(e)(3)(iii), including an identification of the affected facility, a statement noting whether the event resulted from the same root cause(s) identified in a previous analysis and either a description of the recommended corrective action(s) or an explanation of why corrective action is not necessary under § 63.2480(e)(7)(i).

(iv) For any corrective action analysis for which implementation of corrective actions are required in § 63.2480(e)(7), a description of the corrective action(s) completed within the first 45 days following the discharge and, for action(s) not already completed, a schedule for implementation, including proposed commencement and completion dates.

(r) For each heat exchange system, beginning no later than the compliance dates specified in § 63.2445(g), the recordkeeping requirements of § 63.104(f)(1) no longer apply; instead, you must keep records in <u>paragraphs (r)(1)</u> through (4) of this section.

(1) Monitoring data required by § 63.2490(d) and (e) that indicate a leak, the date the leak was detected, or, if applicable, the basis for determining there is no leak.

(2) The dates of efforts to repair leaks.

(3) The method or procedures used to confirm repair of a leak and the date the repair was confirmed.

(4) Documentation of delay of repair as specified in <u>paragraphs (r)(4)(i)</u> through <u>(iv)</u> of this section.

(i) The reason(s) for delaying repair.

(ii) A schedule for completing the repair as soon as practical.

(iii) The date and concentration or mass emissions rate of the leak as first identified and the results of all subsequent monitoring events during the delay of repair.

(iv) An estimate of the potential total hydrocarbon emissions (if you monitor the cooling water for leaks according to § 63.2490(d)(1)) or monitored substance(s) emissions (if you monitor the cooling water for leaks according to § 63.2490(e)) from the leaking heat exchange system or heat exchanger for each required delay of repair monitoring interval following the procedures in paragraphs (r)(4)(iv)(A) through (D) of this section.

(A) If you comply with the total strippable hydrocarbon concentration leak action level, as specified in § 63.2490(d)(1)(iv), you must calculate the mass emissions rate by complying with the requirements of § 63.2490(d)(1)(iii)(B) or by determining the mass flow rate of the cooling water at the monitoring location where the leak was detected. If the monitoring location is an individual cooling tower riser, determine the total cooling water mass flow rate to the cooling tower. Cooling water mass flow rates may be determined using direct measurement, pump curves, heat balance calculations, or other engineering methods. If you determine the mass flow rate of the cooling water, calculate the mass emissions rate by converting the stripping gas leak concentration (in ppmv as methane) to an equivalent liquid concentration, in parts per million by weight (ppmw), using equation 7-1 from "Air Stripping Method (Modified El Paso Method) for Determination of Volatile Organic

Compound Emissions from Water Sources" (incorporated by reference—see § 63.14) and multiply the equivalent liquid concentration by the mass flow rate of the cooling water.

(B) For delay of repair monitoring intervals prior to repair of the leak, calculate the potential total hydrocarbon emissions or monitored substance(s) emissions for the leaking heat exchange system or heat exchanger for the monitoring interval by multiplying the mass emissions rate, determined in § 63.2490(d)(1)(iii)(B) or paragraph (r)(4)(iv)(A) or (D) of this section, by the duration of the delay of repair monitoring interval. The duration of the delay of repair monitoring interval is the time period starting at midnight on the day of the previous monitoring event or at midnight on the day the repair would have had to be completed if the repair had not been delayed, whichever is later, and ending at midnight of the day the of the current monitoring event.

(C) For delay of repair monitoring intervals ending with a repaired leak, calculate the potential total hydrocarbon emissions or monitored substance(s) emissions for the leaking heat exchange system or heat exchanger for the final delay of repair monitoring interval by multiplying the duration of the final delay of repair monitoring interval by the mass emissions rate determined for the last monitoring event prior to the re-monitoring event used to verify the leak was repaired. The duration of the final delay of repair monitoring event prior to re-monitoring to verify the leak was repaired and ending at the time of the re-monitoring event that verified that the leak was repaired.

(D) If you monitor the cooling water for leaks according to § 63.2490(e), you must calculate the mass emissions rate by determining the mass flow rate of the cooling water at the monitoring location where the leak was detected. Cooling water mass flow rates may be determined using direct measurement, pump curves, heat balance calculations, or other engineering methods. Once determined, multiply the mass flow rate of the cooling water by the concentration of the measured substance(s).

(s) For process vents and storage tanks in ethylene oxide service subject to the requirements of § 63.2493, you must keep the records specified in <u>paragraphs (s)(1)</u> through (5) of this section in addition to those records specified in <u>paragraph (a)</u> of this section. Records for equipment in ethylene oxide service subject to the requirements of § 63.2493 are specified in <u>paragraph (a)</u> of this section.

(1) For process vents, include all uncontrolled, undiluted ethylene oxide concentration measurements, and the calculations you used to determine the total uncontrolled ethylene oxide mass emission rate for the sum of all vent gas streams.

(2) For storage tanks, records of the concentration of ethylene oxide of the fluid stored in each storage tank.

(3) For equipment, records of the percent ethylene oxide content of the process fluid and the method used to determine it.

(4) If you vent emissions through a closed-vent system to a non-flare control device, then you must keep records of all periods during which operating values are outside of the applicable operating limits specified in § 63.2493(b)(4) through (6) when regulated material is being routed to the non-flare control device. The record must specify the operating parameter, the applicable limit, and the highest (for maximum operating limits) or lowest (for minimum operating limits) value recorded during the period.

(5) For pressure vessels subject to § 63.2493(c), records as specified in paragraphs (s)(5)(i) through (iv) of this section.

(i) The date of each performance test conducted according to (3.2493)(c)(2).

(ii) The instrument reading of each performance test conducted according to § 63.2493(c)(2), including the following:

(A) Date each defect was detected.

(B) Date of the next performance test that shows the instrument reading is less than 500 ppmv.

(C) Start and end dates of each period after the date in <u>paragraph (s)(5)(ii)(A)</u> of this section when the pressure vessel was completely empty.

(D) Estimated emissions from each defect.

(t) Any records required to be maintained by this part that are submitted electronically via the EPA's CEDRI may be maintained in electronic format. This ability to maintain electronic copies does not affect the requirement for facilities to make records, data, and reports available upon request to a delegated air agency or the EPA as part of an on-site compliance evaluation.

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(u) Beginning no later than the compliance dates specified in § 63.2445(g), the referenced provisions specified in <u>paragraphs</u> (u)(1) through (8) of this section do not apply when demonstrating compliance with <u>paragraph (a)</u> of this section.

(1) Section 63.103(c)(2)(i) of subpart F.

(2) Section 63.103(c)(2)(ii) of subpart F.

(3) The phrase "start-up, shutdown and malfunction and" from § 63.103(c)(3) of subpart F.

(4) The phrase "other than startups, shutdowns, or malfunctions (*e.g.*, a temperature reading of -200 °C on a boiler)," from § 63.152(g)(1)(i) of subpart G.

(5) The phrase "other than a startup, shutdown, or malfunction" from 63.152(g)(1)(ii)(C) of subpart G.

(6) The phrase "other than startups, shutdowns, or malfunctions" from § 63.152(g)(1)(iii) of subpart G.

(7) The phrase "other than a startup, shutdown, or malfunction" from 63.152(g)(2)(iii) of subpart G.

(8) Section 63.152(g)(2)(iv)(A) of subpart G.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>70 FR 38560</u>, July 1, 2005; <u>71 FR 40337</u>, July 14, 2006; <u>85 FR 49155</u>, Aug. 12, 2020; <u>89 FR 23872</u>, Apr. 4, 2024]

#### **Other Requirements and Information**

#### § 63.2535 What compliance options do I have if part of my plant is subject to both this subpart and another subpart?

For any equipment, emission stream, or wastewater stream not subject to  $\S$  <u>63.2493</u> but subject to other provisions of both this subpart and another subpart, you may elect to comply only with the provisions as specified in <u>paragraphs</u> (a) through (1) of this section. You also must identify the subject equipment, emission stream, or wastewater stream, and the provisions with which you will comply, in your notification of compliance status report required by  $\S$  <u>63.2520(d)</u>.

(a) Compliance with other <u>subparts of this part</u> 63.

(1) If you have an MCPU that includes a batch process vent that also is part of a CMPU as defined in <u>subparts F</u> and <u>G of this</u> <u>part</u> 63, you must comply with the emission limits; operating limits; work practice standards; and the compliance, monitoring, reporting, and recordkeeping requirements for batch process vents in this subpart, and you must continue to comply with the requirements in <u>subparts F</u>, <u>G</u>, and <u>H of this part</u> 63 that are applicable to the CMPU and associated equipment.

(2) After the compliance dates specified in § 63.2445, at an offsite reloading or cleaning facility subject to § 63.1253(f), as referenced from § 63.2470(e), compliance with the monitoring, recordkeeping, and reporting provisions of any other subpart of this part 63 constitutes compliance with the monitoring, recordkeeping, and reporting provisions of § 63.1253(f)(7)(ii) or § 63.1253(f)(7)(iii). You must identify in your notification of compliance status report required by § 63.2520(d) the subpart of this part 63 with which the owner or operator of the offsite reloading or cleaning facility complies.

(b) Compliance with <u>40 CFR parts 264</u> and 265, subparts AA, BB, and/or CC.

(1) After the compliance dates specified in § 63.2445, if a control device that you use to comply with this subpart is also subject to monitoring, recordkeeping, and reporting requirements in 40 CFR part 264, subpart AA, BB, or CC; or the monitoring and recordkeeping requirements in 40 CFR part 265, subpart AA, BB, or CC; and you comply with the periodic reporting requirements under 40 CFR part 264, subpart AA, BB, or CC that would apply to the device if your facility had final-permitted status, you may elect to comply either with the monitoring, recordkeeping, and reporting requirements of this subpart; or with the monitoring and recordkeeping requirements in 40 CFR part 264 or 265 and the reporting requirements in 40 CFR part 264, as described in this paragraph (b)(1), which constitute compliance with the monitoring, recordkeeping, and reporting requirements in 40 CFR part 264, and/or 265, you must report the information described in § 63.2520(e).

(2) After the compliance dates specified in § 63.2445, if you have an affected source with equipment that is also subject to <u>40</u> <u>CFR part 264</u>, <u>subpart BB</u>, or to <u>40 CFR part 265</u>, <u>subpart BB</u>, <u>then</u> compliance with the recordkeeping and reporting requirements of <u>40 CFR parts 264</u> and/or 265 may be used to comply with the recordkeeping and reporting requirements of this subpart, to the extent that the requirements of <u>40 CFR parts 264</u> and/or 265 duplicate the requirements of this subpart.

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(c) Compliance with <u>40 CFR part 60</u>, <u>subpart Kb</u> and <u>40</u> CFR part 61, <u>subpart Y</u>. After the compliance dates specified in § <u>63.2445</u>, you are in compliance with the provisions of this subpart FFFF for any storage tank that is assigned to an MCPU and that is both controlled with a floating roof and in compliance with the provisions of either <u>40 CFR part 60</u>, <u>subpart Kb</u>, or <u>40 CFR part 61</u>, <u>subpart Y</u>. You are in compliance with this subpart FFFF if you have a storage tank with a fixed roof, closed-vent system, and control device in compliance with the provisions of either <u>40 CFR part 60</u>, <u>subpart Kb</u>, or <u>40 CFR part 61</u>, <u>subpart Y</u>, except that you must comply with the monitoring, recordkeeping, and reporting requirements in this subpart FFFF. Alternatively, if a storage tank assigned to an MCPU is subject to control under <u>40 CFR part 60</u>, <u>subpart Kb</u>, or <u>40 CFR part 61</u>, <u>subpart Y</u>, you may elect to comply only with the requirements for Group 1 storage tanks in this subpart FFFF.

(d) Compliance with <u>subpart I</u>, <u>GGG</u>, or <u>MMM of this part</u>. After the compliance dates specified in § <u>63.2445</u>, if you have an affected source with equipment subject to <u>subpart I</u>, <u>GGG</u>, or <u>MMM of this part</u>, you may elect to comply with the provisions of <u>subpart H</u>, <u>GGG</u>, or <u>MMM of this part</u>, respectively, for all such equipment, except the affirmative defense requirements in subparts GGG and MMM no longer apply.

(e) Compliance with <u>subpart GGG of this part</u> 63 for wastewater. After the compliance dates specified in § 63.2445, if you have an affected source subject to this subpart and you have an affected source that generates wastewater streams that meet the applicability thresholds specified in § 63.1256, you may elect to comply with the provisions of this subpart FFFF for all such wastewater streams.

(f) Compliance with <u>subpart MMM of this part</u> 63 for wastewater. After the compliance dates specified in § 63.2445, if you have an affected source subject to this subpart, and you have an affected source that generates wastewater streams that meet the applicability thresholds specified in § 63.1362(d), you may elect to comply with the provisions of this subpart FFFF for all such wastewater streams (except that the 99 percent reduction requirement for streams subject to § 63.1362(d)(10) still applies).

(g) Compliance with other regulations for wastewater. After the compliance dates specified in § 63.2445, if you have a Group 1 wastewater stream that is also subject to provisions in 40 CFR parts 260 through 272, you may elect to determine whether this subpart or 40 CFR parts 260 through 272 contain the more stringent control requirements (*e.g.*, design, operation, and inspection requirements for waste management units; numerical treatment standards; etc.) and the more stringent testing, monitoring, recordkeeping, and reporting requirements. Compliance with provisions of 40 CFR parts 260 through 272 that are determined to be more stringent than the requirements of this subpart constitute compliance with this subpart. For example, provisions of 40 CFR parts 260 through 272 for treatment units that meet the conditions specified in § 63.138(h) constitute compliance with this subpart. You must identify in the notification of compliance status report required by § 63.2520(d) the information and procedures that you used to make any stringency determinations.

(h) Compliance with <u>40 CFR part 60</u>, subpart DDD, III, NNN, or RRR. After the compliance dates specified in § <u>63.2445</u>, if you have an MCPU that contains equipment subject to the provisions of this subpart that are also subject to the provisions of <u>40 CFR part 60</u>, subpart DDD, III, NNN, or RRR, you may elect to apply this subpart to all such equipment in the MCPU. If an MCPU subject to the provisions of this subpart has equipment to which this subpart does not apply but which is subject to a standard in <u>40 CFR part 60</u>, subpart DDD, III, NNN, or RRR, you may elect to comply with the requirements for Group 1 process vents in this subpart for such equipment. If you elect any of these methods of compliance, you must consider all total organic compounds, minus methane and ethane, in such equipment for purposes of compliance with this subpart, as if they were organic HAP. Compliance with the provisions of this subpart, in the manner described in this <u>paragraph (h)</u>, will constitute compliance with <u>40 CFR part 60</u>, <u>subpart DDD</u>, III, <u>NNN</u>, or RRR, as applicable.

(i) Compliance with <u>40 CFR part 61, subpart BB</u>.

(1) After the compliance dates specified in  $\S$  63.2445, a Group 1 transfer rack, as defined in  $\S$  63.2550, that is also subject to the provisions of 40 CFR part 61, subpart BB, you are required to comply only with the provisions of this subpart.

(2) After the compliance dates specified in § 63.2445, a Group 2 transfer rack, as defined in § 63.2550, that is also subject to the provisions of  $\frac{40 \text{ CFR part } 61, \text{ subpart BB}}{1000 \text{ cm}}$ , is required to comply with the provisions of either paragraph (1)(2)(i) or (ii) of this section.

(i) If the transfer rack is subject to the control requirements specified in  $\S 61.302$  of 40 CFR part 61, subpart BB, then you may elect to comply with either the requirements of 40 CFR part 61, subpart BB, or the requirements for Group 1 transfer racks under this subpart FFFF.

(ii) If the transfer rack is subject only to reporting and recordkeeping requirements under <u>40 CFR part 61, subpart</u> <u>BB</u>, then you are required to comply only with the reporting and recordkeeping requirements specified in this subpart for Group 2 transfer racks, and you are exempt from the reporting and recordkeeping requirements in <u>40 CFR part 61, subpart</u> <u>BB</u>.

(j) Compliance with <u>40 CFR part 61</u>, subpart FF. After the compliance date specified in § 63.2445, for a Group 1 or Group 2 wastewater stream that is also subject to the provisions of <u>40 CFR 61.342(c)</u> through (<u>h</u>), and is not exempt under <u>40 CFR 61.342(c)(2)</u> or (<u>3</u>), you may elect to comply only with the requirements for Group 1 wastewater streams in this subpart FFFF. If a Group 2 wastewater stream is exempted from <u>40 CFR 61.342(c)(1)</u> under <u>40 CFR 61.342(c)(2)</u> or (<u>3</u>), then you are required to comply only with the reporting and recordkeeping requirements specified in this subpart for Group 2 wastewater streams, and you are exempt from the requirements in <u>40 CFR part 61</u>, subpart FF.

(k) Compliance with <u>40 CFR part 60</u>, <u>subpart VV</u> or <u>VVa</u>, and <u>40</u> CFR part 61, <u>subpart V</u>. Except as specified in <u>paragraphs</u> (k)(1) and (2) of this section, after the compliance date specified in § <u>63.2445</u>, if you have an affected source with equipment that is also subject to the requirements of <u>40 CFR part 60</u>, <u>subpart VV</u> or <u>VVa</u>, or <u>40 CFR part 61</u>, <u>subpart V</u>, you may elect to apply this subpart to all such equipment. After the compliance date specified in § <u>63.2445</u>, if you have an affected source with equipment to which this subpart does not apply, but which is subject to the requirements of <u>40 CFR part 60</u>, <u>subpart</u> <u>VV</u> or <u>VVa</u>, or <u>40 CFR part 60</u>, <u>subpart</u> <u>VV</u> or <u>VVa</u>, or <u>40 CFR part 61</u>, <u>subpart V</u>, you may elect to apply this subpart to all such equipment <u>V</u>, you may elect to apply this subpart to all such equipment. If you elect either of the methods of compliance in this <u>paragraph (k)</u>, you must consider all total organic compounds, minus methane and ethane, in such equipment for purposes of compliance with this subpart, as if they were organic HAP. Compliance with the provisions of this subpart, in the manner described in this <u>paragraph (k)</u>, will constitute compliance with <u>40 CFR part 60</u>, <u>subpart</u> <u>VV</u> or <u>VVa</u>, and <u>40</u> CFR part 61, subpart V, as applicable.

(1) The provision in  $\S 63.2480(b)(4)$  does not apply to connectors in gas/vapor and light liquid service that are subject to monitoring under <u>40 CFR 60.482-11a</u> if complying with the compliance option in this <u>paragraph (k)</u>.

(2) Beginning no later than the compliance dates specified in § 63.2445(g), equipment that must be controlled according to this subpart and subpart VVa of <u>40 CFR part 60</u> is required only to comply with the equipment leak requirements of this subpart, except you must also comply with the calibration drift assessment requirements specified at <u>40 CFR 60.485a(b)(2)</u> if they are required to do so in subpart VVa of <u>40 CFR part 60</u>. When complying with the calibration drift assessment requirements at <u>40 CFR 60.485a(b)(2)</u>, the requirement at <u>40 CFR 60.486a(e)(8)(v)</u> to record the instrument reading for each scale used applies.

(1) Applicability of process units included in a process unit group. You may elect to develop and comply with the requirements for PUG in accordance with paragraphs (1)(1) through (3) of this section.

(1) Procedures to create process unit groups. Develop and document changes in a PUG in accordance with the procedures specified in paragraphs (1)(1)(i) through (v) of this section.

(i) Initially, identify an MCPU that is created from nondedicated equipment that will operate on or after November 10, 2003 and identify all processing equipment that is part of this MCPU, based on descriptions in operating scenarios.

(ii) Add to the group any other nondedicated MCPU and other nondedicated process units expected to be operated in the 5 years after the date specified in paragraph (1)(1)(i) of this section, provided they satisfy the criteria specified in paragraphs (1)(1)(i)(A) through (C) of this section. Also identify all of the processing equipment used for each process unit based on information from operating scenarios and other applicable documentation.

(A) Each process unit that is added to a group must have some processing equipment that is also part of one or more process units in the group.

(B) No process unit may be part of more than one PUG.

(C) The processing equipment used to satisfy the requirement of  $\frac{\text{paragraph } (1)(1)(ii)(A)}{\text{of this section may not be a storage tank or control device.}}$ 

(iii) The initial PUG consists of all of the processing equipment for the process units identified in <u>paragraphs</u> (<u>1)(1)(i)</u> and (<u>ii)</u> of this section. As an alternative to the procedures specified in <u>paragraphs (1)(1)(i)</u> and (<u>ii)</u> of this section, you may use a PUG that was developed in accordance with § 63.1360(h) as your initial PUG.

(iv) Add process units developed in the future in accordance with the conditions specified in <u>paragraphs</u> (1)(1)(i)(A) and (B) of this section.

(v) Maintain records that describe the process units in the initial PUG, the procedure used to create the PUG, and subsequent changes to each PUG as specified in  $\frac{63.2525(i)}{2.525(i)}$ . Submit the records in reports as specified in  $\frac{63.2520(d)(2)(ix)}{2.520(d)(2)(ix)}$  and  $\frac{(e)(8)}{2.525(i)}$ .

(2) Determine primary product. You must determine the primary product of each PUG created in <u>paragraph (1)(1)</u> of this section according to the procedures specified in <u>paragraphs (1)(2)(i)</u> through (iv) of this section.

(i) The primary product is the type of product (*e.g.*, organic chemicals subject to  $\frac{63.2435(b)(1)}{50.2435(b)(1)}$ , pharmaceutical products subject to  $\frac{63.1250}{50.2435(b)(1)}$ , or pesticide active ingredients subject to  $\frac{63.1360}{50.2435(b)(1)}$  expected to be produced for the greatest operating time in the 5-year period specified in paragraph (1)(1)(ii) of this section.

(ii) If the PUG produces multiple types of products equally based on operating time, then the primary product is the type of product with the greatest production on a mass basis over the 5-year period specified in paragraph(l)(1)(ii) of this section.

(iii) At a minimum, you must redetermine the primary product of the PUG following the procedure specified in <u>paragraphs</u> ( $\underline{1})(\underline{2})(\underline{i})$  and ( $\underline{ii}$ ) of this section every 5 years.

(iv) You must record the calculation of the initial primary product determination as specified in  $\S$  63.2525(i)(3) and report the results in the notification of compliance status report as specified in  $\S$  63.2520(d)(8)(ix). You must record the calculation of each redetermination of the primary product as specified in  $\S$  63.2525(i)(5) and report the calculation in a compliance report submitted no later than the report covering the period for the end of the 5th year after cessation of production of the previous primary product, as specified in  $\S$  63.2520(e)(8).

#### (3) Compliance requirements.

(i) If the primary product of the PUG is determined according to paragraph (1)(2) of this section to be material described in § 63.2435(b)(1), then you must comply with this subpart for each MCPU in the PUG. You may also elect to comply with this subpart for all other process units in the PUG, which constitutes compliance with other part 63 rules.

(ii) If the primary product of the PUG is determined according to <u>paragraph (1)(2)</u> of this section to be material not described in  $\S 63.2435(b)(1)$ , then you must comply with <u>paragraph (1)(3)(ii)(A)</u>, (B), or (C) of this section, as applicable.

(A) If the primary product is subject to <u>subpart GGG of this part</u> 63, then comply with the requirements of subpart GGG for each MCPU in the PUG.

(B) If the primary product is subject to <u>subpart MMM of this part</u> 63, then comply with the requirements of subpart MMM for each MCPU in the PUG.

(C) If the primary product is subject to any subpart in this part 63 other than subpart GGG or subpart MMM, then comply with the requirements of this subpart for each MCPU in the PUG.

(iii) The requirements for new and reconstructed sources in the alternative subpart apply to all MCPU in the PUG if and only if the affected source under the alternative subpart meets the requirements for construction or reconstruction.

#### (m) Overlap of this subpart with other regulations for flares.

(1) Beginning no later than the compliance dates specified in § 63.2445(g), flares that control ethylene oxide emissions from affected sources in ethylene oxide service as defined in § 63.2450(g), flares that control emissions from MCPUs that produce olefins and polyolefins, subject to the provisions of 40 CFR 60.18 or 63.11, and used as a control device for an emission point subject to the emission limits and work practice standards in Tables 1, 2, 4 or 5 to this subpart are required to comply only with the provisions specified in § 63.2450(e)(5). At any time before the compliance dates specified in § 63.2445(g), flares that are subject to the provisions of 40 CFR 60.18 or 63.11 and elect to comply with the requirements in § 63.2450(e)(5) are required to comply only with the provisions specified in provisions specified in this subpart. For purposes of compliance with this paragraph (m), "MCPUs that produces olefins or polyolefins" includes only those MCPUs that manufacture ethylene, propylene, polyethylene, and/or polypropylene as a product. By-products and impurities as defined in § 63.101, as well as wastes and trace contaminants, are not considered products.

(2) Beginning no later than the compliance dates specified in  $\S 63.2445(g)$ , flares subject to  $\S 63.987$  and used as a control device for an emission point subject to the emission limits and work practice standards in Tables 1, 2, 4 or 5 to this subpart are only required to comply with  $\S 63.2450(g)(5)$ .

(3) Beginning no later than the compliance dates specified in  $\frac{63.2445(g)}{100}$ , flares subject to the requirements in subpart CC of this part and used as a control device for an emission point subject to the emission limits and work practice standards in

Tables 1, 2, 4 or 5 to this subpart are only required to comply with the flare requirements in <u>subpart CC of this part</u>. This <u>paragraph (m)(3)</u> does not apply to multi-point pressure assisted flares.

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40337, July 14, 2006; 85 FR 49158, Aug. 12, 2020]

#### § 63.2540 What parts of the General Provisions apply to me?

Table 12 to this subpart shows which parts of the General Provisions in  $\frac{863.1}{10}$  through  $\frac{63.15}{10}$  apply to you.

#### § 63.2545 Who implements and enforces this subpart?

(a) This subpart can be implemented and enforced by us, the U.S. Environmental Protection Agency (U.S. EPA), or a delegated authority such as your State, local, or tribal agency. If the U.S. EPA Administrator has delegated authority to your State, local, or tribal agency, then that agency also has the authority to implement and enforce this subpart. You should contact your U.S. EPA Regional Office to find out if this subpart is delegated to your State, local, or tribal agency.

(b) In delegating implementation and enforcement authority of this subpart to a state, local, or tribal agency under subpart E of this part, the authorities contained in paragraphs (b)(1) through (5) of this section are retained by the Administrator of U.S. EPA and are not delegated to the state, local, or tribal agency.

(1) Approval of alternatives to the non-opacity emission limits and work practice standards in  $\frac{63.2450(a)}{2}$  under  $\frac{63.6(g)}{2}$ .

(2) Approval of major alternatives to test methods under  $\frac{63.7(e)(2)(ii)}{2}$  and  $\frac{(f)}{2}$  and as defined in  $\frac{63.90}{2}$ .

(3) Approval of major alternatives to monitoring under  $\frac{63.8(f)}{100}$  and as defined in  $\frac{63.90}{100}$ .

(4) Approval of major alternatives to recordkeeping and reporting under  $\S$  <u>63.10(f)</u> and as defined in  $\S$  <u>63.90</u>.

(5) Approval of an alternative to any electronic reporting to the EPA required by this subpart.

[68 FR 63888, Nov. 10, 2003, as amended at 85 FR 49159, Aug. 12, 2020]

#### § 63.2550 What definitions apply to this subpart?

(a) For an affected source complying with the requirements in <u>subpart SS of this part</u> 63, the terms used in this subpart and in <u>subpart SS of this part</u> 63 have the meaning given them in  $\S$  63.981, except as specified in  $\S$  63.2450(k)(2) and (m), 63.2470(c)(2), 63.2475(b), and paragraph (i) of this section.

(b) For an affected source complying with the requirements in  $\frac{40 \text{ CFR part 65, subpart F}}{1000 \text{ cFR part 65, subpart F}}$ , the terms used in this subpart and in  $\frac{40 \text{ CFR part 65, subpart F}}{1000 \text{ cFR part 65, subpart F}}$  have the meaning given to them in  $\frac{60 \text{ cFR part 65, subpart F}}{1000 \text{ cFR part 65, subpart F}}$ .

(c) For an affected source complying with the requirements in <u>subpart UU of this part</u> 63, the terms used in this subpart and in <u>subpart UU of this part</u> 63 have the meaning given them in  $\S$  63.1020.

(d) For an affected source complying with the requirements in <u>subpart WW of this part</u> 63, the terms used in this subpart and <u>subpart WW of this part</u> 63 have the meaning given them in <u>§ 63.1061</u>, except as specified in <u>§§</u> <u>63.2450(m)</u>, <u>63.2470(c)(2)</u>, and <u>paragraph (i)</u> of this section.

(e) For an affected source complying with the requirements in  $\frac{\$\$ 63.132}{\$\$ 63.132}$  through  $\frac{63.149}{\$\$ 63.132}$  through  $\frac{63.149}{\$\$ 63.132}$  have the meaning given them in  $\frac{\$\$ 63.101}{\$\$ 63.101}$  and  $\frac{63.111}{\$\$ 800}$ , the terms used in this subpart  $\frac{63.2450(m)}{\$}$  and  $\frac{10}{\$}$  of this section.

(f) For an affected source complying with the requirements in  $\frac{\$\$}{63.104}$  and  $\frac{63.105}{63.104}$ , the terms used in this subpart and in  $\frac{\$\$}{63.2450}$  and  $\frac{63.105}{63.2450(m)}$ ,  $\frac{63.2490(b)}{63.2490(b)}$ , and  $\frac{10}{100}$  of this section.

(g) For an affected source complying with requirements in §§ 63.1253, 63.1257, and 63.1258, the terms used in this subpart and in §§ 63.1253, 63.1257, and 63.1258 have the meaning given them in § 63.1251, except as specified in § 63.2450(m) and paragraph (i) of this section.

(h) For an affected source complying with the requirements in  $\frac{40 \text{ CFR part 65, subpart F}}{40 \text{ CFR part 65, subpart F}}$ , the terms used in this subpart and in  $\frac{40 \text{ CFR part 65, subpart F}}{40 \text{ CFR 65.2}}$ .

(i) All other terms used in this subpart are defined in the Clean Air Act (CAA), in <u>40 CFR 63.2</u>, and in this <u>paragraph (i)</u>. If a term is defined in § 63.2, § 63.101, § 63.111, § 63.981, § 63.1020, § 63.1061, § 63.1251, or § 65.2 and in this <u>paragraph (i)</u>, the definition in this <u>paragraph (i)</u> applies for the purposes of this subpart.

Ancillary activities means boilers and incinerators (not used to comply with the emission limits in Tables 1 through 7 to this subpart), chillers and refrigeration systems, and other equipment and activities that are not directly involved (*i.e.*, they operate within a closed system and materials are not combined with process fluids) in the processing of raw materials or the manufacturing of a product or isolated intermediate.

*Batch operation* means a noncontinuous operation involving intermittent or discontinuous feed into equipment, and, in general, involves the emptying of the equipment after the operation ceases and prior to beginning a new operation. Addition of raw material and withdrawal of product do not occur simultaneously in a batch operation.

*Batch process vent* means a vent from a unit operation or vents from multiple unit operations within a process that are manifolded together into a common header, through which a HAP-containing gas stream is, or has the potential to be, released to the atmosphere. Examples of batch process vents include, but are not limited to, vents on condensers used for product recovery, reactors, filters, centrifuges, and process tanks. The following are not batch process vents for the purposes of this subpart:

(1) Continuous process vents;

- (2) Bottoms receivers;
- (3) Surge control vessels;

(4) Gaseous streams routed to a fuel gas system(s) unless on and after August 12, 2023, the fuel gas system(s) supplies a flare of which 50 percent or more of the fuel gas burned in the flare is derived from an MCPU that has processes and/or equipment in ethylene oxide service, or produces olefins or polyolefins;

(5) Vents on storage tanks, wastewater emission sources, or pieces of equipment subject to the emission limits and work practice standards in Tables 4, 6, and 7 to this subpart;

(6) Drums, pails, and totes;

(7) Flexible elephant trunk systems that draw ambient air (*i.e.*, the system is not ducted, piped, or otherwise connected to the unit operations) away from operators when vessels are opened; and

(8) Except for batch process vents in ethylene oxide service, emission streams from emission episodes that are undiluted and uncontrolled containing less than 50 ppmv HAP are not part of any batch process vent. A vent from a unit operation, or a vent from multiple unit operations that are manifolded together, from which total uncontrolled HAP emissions are less than 200 lb/yr is not a batch process vent; emissions for all emission episodes associated with the unit operation(s) must be included in the determination of the total mass emitted. The HAP concentration or mass emission rate may be determined using any of the following: Process knowledge that no HAP are present in the emission stream; an engineering assessment as discussed in  $\frac{63.1257(d)(2)(ii)}{2}$ , except that you do not need to demonstrate that the equations in  $\frac{63.1257(d)(2)(i)}{2}$  do not apply for the purposes of this demonstration; equations specified in  $\frac{63.1257(d)(2)(i)}{2}$ , as applicable; test data using Method 18 of <u>40 CFR part 60</u>, appendix A; or any other test method that has been validated according to the procedures in EPA Method 301 of appendix A to this part.

*Bench-scale process* means a process (other than a research and development facility) that is operated on a small scale, such as one capable of being located on a laboratory bench top. This bench-scale equipment will typically include reagent feed vessels, a small reactor and associated product separator, recovery and holding equipment. These processes are only capable of producing small quantities of product.

*Biofilter* means an enclosed control system such as a tank or series of tanks with a fixed roof that contact emissions with a solid media (such as bark) and use microbiological activity to transform organic pollutants in a process vent stream to innocuous compounds such as carbon dioxide, water, and inorganic salts. Wastewater treatment processes such as aeration lagoons or activated sludge systems are not considered to be biofilters.

*Bottoms receiver* means a tank that collects bottoms from continuous distillation before the stream is sent for storage or for further downstream processing.

*Breakthrough* means the time when the level of HAP or TOC, measured at the outlet of the first bed, has been detected is at the highest concentration allowed to be discharged from the adsorber system and indicates that the adsorber bed should be replaced.

#### National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing

*Construction* means the onsite fabrication, erection, or installation of an affected source or MCPU. Addition of new equipment to an MCPU subject to existing source standards does not constitute construction, but it may constitute reconstruction of the affected source or MCPU if it satisfies the definition of reconstruction in  $\frac{§ 63.2}{2}$ .

*Consumption* means the quantity of all HAP raw materials entering a process in excess of the theoretical amount used as reactant, assuming 100 percent stoichiometric conversion. The raw materials include reactants, solvents, and any other additives. If a HAP is generated in the process as well as added as a raw material, consumption includes the quantity generated in the process.

Continuous operation means any operation that is not a batch operation.

*Continuous process vent* means the point of discharge to the atmosphere (or the point of entry into a control device, if any) of a gas stream if the gas stream has the characteristics specified in  $\S$  63.107(b) through (h), or meets the criteria specified in  $\S$  63.107(i), except:

(1) The reference in  $\S 63.107(e)$  to a chemical manufacturing process unit that meets the criteria of  $\S 63.100(b)$  means an MCPU that meets the criteria of  $\S 63.2435(b)$ ;

(2) The reference in  $\S 63.107(h)(4)$  to  $\S 63.113$  means Table 1 to this subpart;

(3) The references in  $\S 63.107(h)(7)$  to  $\S 863.119$  and 63.126 mean tables 4 and 5 to this subpart; and

(4) For the purposes of  $\S$  63.2455, all references to the characteristics of a process vent (*e.g.*, flowrate, total HAP concentration, or TRE index value) mean the characteristics of the gas stream.

(5) The reference to "total organic HAP" in § 63.107(d) means "total HAP" for the purposes of this subpart FFFF.

(6) The references to an "air oxidation reactor, distillation unit, or reactor" in  $\S$  63.107 mean any continuous operation for the purposes of this subpart.

(7) A separate determination is required for the emissions from each MCPU, even if emission streams from two or more MCPU are combined prior to discharge to the atmosphere or to a control device.

(8) On and after August 12, 2023, § 63.107(h)(3) applies unless the fuel gas system supplies a flare of which 50 percent or more of the fuel gas burned in the flare is derived from an MCPU that has processes and/or equipment in ethylene oxide service, or produces olefins or polyolefins.

(9) On and after August 12, 2023, <u>§ 63.107(h)(9)</u> no longer applies.

(10) On and after August 12, 2023, § <u>63.107(i)</u> no longer applies. Instead, a process vent is the point of discharge to the atmosphere (or the point of entry into a control device, if any) of a gas stream if the gas stream meets the criteria specified in this paragraph. The gas stream would meet the characteristics specified in § <u>63.107(b)</u> through (g) of subpart F, but, for purposes of avoiding applicability, has been deliberately interrupted, temporarily liquefied, routed through any item of equipment for no process purpose, or disposed of in a flare that does not meet the criteria in § <u>63.11(b)</u> of subpart A or § <u>63.2450(e)(5)</u> as applicable, or an incinerator that does not reduce emissions of organic HAP by 98 percent or to a concentration of 20 parts per million by volume, whichever is less stringent.

(11) Section 63.107(d) does not apply to continuous process vents in ethylene oxide service.

*Dedicated MCPU* means an MCPU that consists of equipment that is used exclusively for one process, except that storage tanks assigned to the process according to the procedures in  $\frac{63.2435(d)}{2}$  also may be shared by other processes.

Deviation means any instance in which an affected source subject to this subpart, or an owner or operator of such a source:

(1) Fails to meet any requirement or obligation established by this subpart including, but not limited to, any emission limit, operating limit, or work practice standard; or

(2) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart and that is included in the operating permit for any affected source required to obtain such a permit; or

(3) Before August 12, 2023, fails to meet any emission limit, operating limit, or work practice standard in this subpart during startup, shutdown, or malfunction, regardless of whether or not such failure is permitted by this subpart. On and after August 12, 2023, this <u>paragraph (3)</u> no longer applies.

Emission point means each continuous process vent, batch process vent, storage tank, transfer rack, and wastewater stream.

*Energetics* means propellants, explosives, and pyrotechnics and include materials listed at <u>49 CFR 172.101</u> as Hazard Class I Hazardous Materials, Divisions 1.1 through 1.6.

*Equipment* means each pump, compressor, agitator, pressure relief device, sampling connection system, open-ended valve or line, valve, connector, and instrumentation system in organic HAP service; and any control devices or systems used to comply with Table 6 to this subpart.

Excess emissions means emissions greater than those allowed by the emission limit.

*Family of materials* means a grouping of materials with the same basic composition or the same basic end use or functionality produced using the same basic feedstocks with essentially identical HAP emission profiles (primary constituent and relative magnitude on a pound per product basis) and manufacturing equipment configuration. Examples of families of materials include multiple grades of the same product or different variations of a product (*e.g.*, blue, black, and red resins).

*Force majeure* event means a release of HAP, either directly to the atmosphere from a pressure relief device or discharged via a flare, that is demonstrated to the satisfaction of the Administrator to result from an event beyond the owner or operator's control, such as natural disasters; acts of war or terrorism; loss of a utility external to the MCPU (*e.g.*, external power curtailment), excluding power curtailment due to an interruptible service agreement; and fire or explosion originating at a near or adjoining facility outside of the miscellaneous organic chemical manufacturing process unit that impacts the miscellaneous organic chemical manufacturing process unit that impacts the

*Group 1 batch process vent* means each of the batch process vents in a process for which the collective uncontrolled organic HAP emissions from all of the batch process vents are greater than or equal to 10,000 lb/yr at an existing source or greater than or equal to 3,000 lb/yr at a new source.

Group 2 batch process vent means each batch process vent that does not meet the definition of Group 1 batch process vent.

*Group 1 continuous process vent* means a continuous process vent for which the flow rate is greater than or equal to 0.005 standard cubic meter per minute, and the total resource effectiveness index value, calculated according to  $\frac{63.2455(b)}{5.0}$ , is less than or equal to 1.9 at an existing source and less than or equal to 5.0 at a new source.

*Group 2 continuous process vent* means a continuous process vent that does not meet the definition of a Group 1 continuous process vent.

*Group 1 storage tank* means a storage tank with a capacity greater than or equal to 10,000 gal storing material that has a maximum true vapor pressure of total HAP greater than or equal to 6.9 kilopascals at an existing source or greater than or equal to 0.69 kilopascals at a new source.

Group 2 storage tank means a storage tank that does not meet the definition of a Group 1 storage tank.

*Group 1 transfer rack* means a transfer rack that loads more than 0.65 million liters/year of liquids that contain organic HAP with a rack-weighted average partial pressure, as defined in  $\S$  63.111, greater than or equal to 1.5 pound per square inch absolute.

Group 2 transfer rack means a transfer rack that does not meet the definition of a Group 1 transfer rack.

*Group 1 wastewater stream* means a wastewater stream consisting of process wastewater at an existing or new source that meets the criteria for Group 1 status in § 63.2485(c) for compounds in Tables 8 and 9 to this subpart and/or a wastewater stream consisting of process wastewater at a new source that meets the criteria for Group 1 status in § 63.132(d) for compounds in Table 8 to subpart G of this part 63.

Group 2 wastewater stream means any process wastewater stream that does not meet the definition of a Group 1 wastewater stream.

Halogen atoms mean chlorine and fluorine.

*Halogenated vent stream* means a vent stream determined to have a mass emission rate of halogen atoms contained in organic compounds of 0.45 kilograms per hour or greater determined by the procedures presented in  $\frac{63.115(d)(2)(v)}{2}$ .

*HAP metals* means the metal portion of antimony compounds, arsenic compounds, beryllium compounds, cadmium compounds, chromium compounds, cobalt compounds, lead compounds, manganese compounds, mercury compounds, nickel compounds, and selenium compounds.

*Heat exchange system* means a device or collection of devices used to transfer heat from process fluids to water without intentional direct contact of the process fluid with the water (*i.e.*, non-contact heat exchanger) and to transport and/or cool the water in a closed-loop recirculation system (cooling tower system) or a once-through system (*e.g.*, river or pond water). For closed-loop recirculation systems, the heat exchange system consists of a cooling tower, all miscellaneous organic chemical manufacturing process unit heat exchangers that are in organic HAP service, as defined in this subpart, serviced by that cooling tower, and all water lines to and from these miscellaneous organic chemical manufacturing process unit heat exchange system consists of all heat exchangers that are in organic HAP service, as defined in this subpart, servicing an individual miscellaneous organic chemical manufacturing process unit and all water lines to and from these heat exchange system consists of all heat exchangers that are in organic HAP service, as defined in this subpart, servicing an individual miscellaneous organic chemical manufacturing process unit and all water lines to and from these heat exchangers or pump seal coolers are not considered heat exchangers for the purpose of this definition and are not part of the heat exchange system. Intentional direct contact with process fluids results in the formation of a wastewater.

Hydrogen halide and halogen HAP means hydrogen chloride, hydrogen fluoride, and chlorine.

#### In ethylene oxide service means the following:

(1) For equipment leaks, any equipment that contains or contacts a fluid (liquid or gas) that is at least 0.1 percent by weight of ethylene oxide. If information exists that suggests ethylene oxide could be present in equipment, the equipment is considered to be "in ethylene oxide service" unless sampling and analysis is performed as specified in  $\S$  63.2492 to demonstrate that the equipment does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in equipment, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(2) For process vents, each batch and continuous process vent in a process that, when uncontrolled, contains a concentration of greater than or equal to 1 ppmv undiluted ethylene oxide, and when combined, the sum of all these process vents would emit uncontrolled ethylene oxide emissions greater than or equal to 5 lb/yr (2.27 kg/yr). If information exists that suggests ethylene oxide could be present in a batch or continuous process vent, then the batch or continuous process vent is considered to be "in ethylene oxide service" unless an analysis is performed as specified in § 63.2492 to demonstrate that the batch or continuous process vent does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in a batch or continuous process vent, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(3) For storage tanks, storage tanks of any capacity and vapor pressure storing a liquid that is at least 0.1 percent by weight of ethylene oxide. If knowledge exists that suggests ethylene oxide could be present in a storage tank, then the storage tank is considered to be "in ethylene oxide service" unless the procedures specified in § 63.2492 are performed to demonstrate that the storage tank does not meet the definition of being "in ethylene oxide service". The exemptions for "vessels storing organic liquids that contain HAP only as impurities" and "pressure vessels designed to operate in excess of 204.9 kilopascals and without emissions to the atmosphere" listed in the definition of "storage tank" in this section do not apply for storage tanks that may be in ethylene oxide service. Examples of information that could suggest ethylene oxide could be present in a storage tank, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

#### In ethylene oxide service means the following:

(1) For equipment leaks, any equipment that contains or contacts a fluid (liquid or gas) that is at least 0.1 percent by weight of ethylene oxide. If information exists that suggests ethylene oxide could be present in equipment, the equipment is considered to be "in ethylene oxide service" unless sampling and analysis is performed as specified in  $\S$  63.2492 to demonstrate that the equipment does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in equipment, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(2) For process vents, each batch and continuous process vent in a process that, when uncontrolled, contains a concentration of greater than or equal to 1 ppmv undiluted ethylene oxide, and when combined, the sum of all these process vents would emit uncontrolled ethylene oxide emissions greater than or equal to 5 lb/yr (2.27 kg/yr). If information exists that suggests ethylene oxide could be present in a batch or continuous process vent, then the batch or continuous process vent is considered to be "in ethylene oxide service" unless an analysis is performed as specified in  $\frac{8 63.2492}{5 63.2492}$  to demonstrate that the batch or

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continuous process vent does not meet the definition of being "in ethylene oxide service". Examples of information that could suggest ethylene oxide could be present in a batch or continuous process vent, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

(3) For storage tanks, storage tanks of any capacity and vapor pressure storing a liquid that is at least 0.1 percent by weight of ethylene oxide. If knowledge exists that suggests ethylene oxide could be present in a storage tank, then the storage tank is considered to be "in ethylene oxide service" unless the procedures specified in  $\S 63.2492$  are performed to demonstrate that the storage tank does not meet the definition of being "in ethylene oxide service". The exemptions for "vessels storing organic liquids that contain HAP only as impurities" and "pressure vessels designed to operate in excess of 204.9 kilopascals and without emissions to the atmosphere" listed in the definition of "storage tank" in this section do not apply for storage tanks that may be in ethylene oxide service. Examples of information that could suggest ethylene oxide could be present in a storage tank, include calculations based on safety data sheets, material balances, process stoichiometry, or previous test results provided the results are still relevant to the current operating conditions.

*In organic HAP service* means that a piece of equipment either contains or contacts a fluid (liquid or gas) that is at least 5 percent by weight of total organic HAP as determined according to the provisions of  $\frac{5}{63.180(d)}$ . The provisions of  $\frac{5}{63.180(d)}$  also specify how to determine that a piece of equipment is not in organic HAP service.

*Isolated intermediate* means a product of a process that is stored before subsequent processing. An isolated intermediate is usually a product of a chemical synthesis, fermentation, or biological extraction process. Storage of an isolated intermediate marks the end of a process. Storage occurs at any time the intermediate is placed in equipment used solely for storage. The storage equipment is part of the MCPU that produces the isolated intermediate and is not assigned as specified in § 63.2435(d).

*Large control device* means a control device that controls total HAP emissions of greater than or equal to 10 tpy, before control.

*Loading rack* means a single system used to fill tank trucks and railcars at a single geographic site. Loading equipment and operations that are physically separate (*i.e.*, do not share common piping, valves, and other equipment) are considered to be separate loading racks.

*Maintenance wastewater* means wastewater generated by the draining of process fluid from components in the MCPU into an individual drain system in preparation for or during maintenance activities. Maintenance wastewater can be generated during planned and unplanned shutdowns and during periods not associated with a shutdown. Examples of activities that can generate maintenance wastewater include descaling of heat exchanger tubing bundles, cleaning of distillation column traps, draining of pumps into an individual drain system, and draining of portions of the MCPU for repair. Wastewater from routine cleaning operations occurring as part of batch operations is not considered maintenance wastewater.

*Maximum true vapor pressure* has the meaning given in  $\S 63.111$ , except that it applies to all HAP rather than only organic HAP.

*Miscellaneous organic chemical manufacturing process* means all equipment which collectively function to produce a product or isolated intermediate that are materials described in § 63.2435(b). For the purposes of this subpart, process includes any, all or a combination of reaction, recovery, separation, purification, or other activity, operation, manufacture, or treatment which are used to produce a product or isolated intermediate. A process is also defined by the following:

(1) Routine cleaning operations conducted as part of batch operations are considered part of the process;

(2) Each nondedicated solvent recovery operation is considered a single process;

(3) Each nondedicated formulation operation is considered a single process that is used to formulate numerous materials and/or products;

(4) Quality assurance/quality control laboratories are not considered part of any process; and

(5) Ancillary activities are not considered a process or part of any process.

(6) The end of a process that produces a solid material is either up to and including the dryer or extruder, or for a polymer production process without a dryer or extruder, it is up to and including the die plate or solid-state reactor, except in two cases. If the dryer, extruder, die plate, or solid-state reactor is followed by an operation that is designed and operated to remove HAP solvent or residual HAP monomer from the solid, then the solvent removal operation is the last step in the

process. If the dried solid is diluted or mixed with a HAP-based solvent, then the solvent removal operation is the last step in the process.

*Nondedicated solvent recovery operation* means a distillation unit or other purification equipment that receives used solvent from more than one MCPU.

*Nonstandard batch* means a batch process that is operated outside of the range of operating conditions that are documented in an existing operating scenario but is still a reasonably anticipated event. For example, a nonstandard batch occurs when additional processing or processing at different operating conditions must be conducted to produce a product that is normally produced under the conditions described by the standard batch. A nonstandard batch may be necessary as a result of a malfunction, but it is not itself a malfunction.

*On-site or on site* means, with respect to records required to be maintained by this subpart or required by another subpart referenced by this subpart, that records are stored at a location within a major source which encompasses the affected source. On-site includes, but is not limited to, storage at the affected source or MCPU to which the records pertain, or storage in central files elsewhere at the major source.

*Operating scenario* means, for the purposes of reporting and recordkeeping, any specific operation of an MCPU as described by records specified in  $\S$  63.2525(b).

Organic group means structures that contain primarily carbon, hydrogen, and oxygen atoms.

*Organic peroxides* means organic compounds containing the bivalent -o-o-structure which may be considered to be a structural derivative of hydrogen peroxide where one or both of the hydrogen atoms has been replaced by an organic radical.

Point of determination means each point where process wastewater exits the MCPU or control device.

Note to definition for point of determination:

The regulation allows determination of the characteristics of a wastewater stream: At the point of determination; or downstream of the point of determination if corrections are made for changes in flow rate and annual average concentration of soluble HAP and partially soluble HAP compounds as determined according to procedures in  $\S$  63.144 of subpart G in this part 63. Such changes include losses by air emissions; reduction of annual average concentration or changes in flow rate by mixing with other water or wastewater streams; and reduction in flow rate or annual average concentration by treating or otherwise handling the wastewater stream to remove or destroy HAP.

*Predominant HAP* means as used in calibrating an analyzer, the single organic HAP that constitutes the largest percentage of the total organic HAP in the analyzed gas stream, by volume.

*Pressure release* means the emission of materials resulting from the system pressure being greater than the set pressure of the pressure relief device. This release can be one release or a series of releases over a short time period.

*Pressure relief device* means a valve, rupture disk, or similar device used only to release an unplanned, nonroutine discharge of gas from process equipment in order to avoid safety hazards or equipment damage. A pressure relief device discharge can result from an operator error, a malfunction such as a power failure or equipment failure, or other unexpected cause. Such devices include conventional, spring-actuated relief valves, balanced bellows relief valves, pilot-operated relief valves, rupture disks, and breaking, buckling, or shearing pin devices. Devices that are actuated either by a pressure of less than or equal to 2.5 pounds per square inch gauge or by a vacuum are not pressure relief devices.

*Pressure vessel* means a storage vessel that is used to store liquids or gases and is designed not to vent to the atmosphere as a result of compression of the vapor headspace in the pressure vessel during filling of the pressure vessel to its design capacity.

*Process condenser* means a condenser whose primary purpose is to recover material as an integral part of an MCPU. All condensers recovering condensate from an MCPU at or above the boiling point or all condensers in line prior to a vacuum source are considered process condensers. Typically, a primary condenser or condensers in series are considered to be integral to the MCPU if they are capable of and normally used for the purpose of recovering chemicals for fuel value (i.e., net positive heating value), use, reuse or for sale for fuel value, use, or reuse. This definition does not apply to a condenser that is used to remove materials that would hinder performance of a downstream recovery device as follows:

(1) To remove water vapor that would cause icing in a downstream condenser, or

(2) To remove water vapor that would negatively affect the adsorption capacity of carbon in a downstream carbon adsorber, or

(3) To remove high molecular weight organic compounds or other organic compounds that would be difficult to remove during regeneration of a downstream carbon adsorber.

*Process tank* means a tank or vessel that is used within a process to collect material discharged from a feedstock storage tank or equipment within the process before the material is transferred to other equipment within the process or a product storage tank. A process tank has emissions that are related to the characteristics of the batch cycle, and it does not accumulate product over multiple batches. Surge control vessels and bottoms receivers are not process tanks.

*Production-indexed HAP consumption factor (HAP factor)* means the result of dividing the annual consumption of total HAP by the annual production rate, per process.

*Production-indexed VOC consumption factor (VOC factor)* means the result of dividing the annual consumption of total VOC by the annual production rate, per process.

*Quaternary ammonium compounds* means a type of organic nitrogen compound in which the molecular structure includes a central nitrogen atom joined to four organic groups as well as an acid radical of some sort.

*Recovery device* means an individual unit of equipment used for the purpose of recovering chemicals from process vent streams and from wastewater streams for fuel value (i.e., net positive heating value), use, reuse, or for sale for fuel value, use, or reuse. For the purposes of meeting requirements in table 2 to this subpart, the recovery device must not be a process condenser and must recover chemicals to be reused in a process on site. Examples of equipment that may be recovery devices include absorbers, carbon adsorbers, condensers, oil-water separators or organic-water separators, or organic removal devices such as decanters, strippers, or thin-film evaporation units. To be a recovery device for a wastewater stream, a decanter and any other equipment based on the operating principle of gravity separation must receive only multi-phase liquid streams.

Relief valve means a type of pressure relief device that is designed to re-close after the pressure relief.

Responsible official means responsible official as defined in 40 CFR 70.2.

*Safety device* means a closure device such as a pressure relief valve, frangible disc, fusible plug, or any other type of device which functions exclusively to prevent physical damage or permanent deformation to a unit or its air emission control equipment by venting gases or vapors directly to the atmosphere during unsafe conditions resulting from an unplanned, accidental, or emergency event. For the purposes of this subpart, a safety device is not used for routine venting of gases or vapors from the vapor headspace underneath a cover such as during filling of the unit or to adjust the pressure in response to normal daily diurnal ambient temperature fluctuations. A safety device is designed to remain in a closed position during normal operations and open only when the internal pressure, or another relevant parameter, exceeds the device threshold setting applicable to the air emission control equipment as determined by the owner or operator based on manufacturer recommendations, applicable regulations, fire protection and prevention codes and practices, or other requirements for the safe handling of flammable, combustible, explosive, reactive, or hazardous materials.

*Shutdown* means the cessation of operation of a continuous operation for any purpose. Shutdown also means the cessation of a batch operation, or any related individual piece of equipment required or used to comply with this subpart, if the steps taken to cease operation differ from those described in a standard batch or nonstandard batch. Shutdown also applies to emptying and degassing storage vessels. Shutdown does not apply to cessation of batch operations at the end of a campaign or between batches within a campaign when the steps taken are routine operations.

Small control device means a control device that controls total HAP emissions of less than 10 tpy, before control.

*Standard batch* means a batch process operated within a range of operating conditions that are documented in an operating scenario. Emissions from a standard batch are based on the operating conditions that result in highest emissions. The standard batch defines the uncontrolled and controlled emissions for each emission episode defined under the operating scenario.

*Startup* means the setting in operation of a continuous operation for any purpose; the first time a new or reconstructed batch operation begins production; for new equipment added, including equipment required or used to comply with this subpart, the first time the equipment is put into operation; or for the introduction of a new product/process, the first time the product or process is run in equipment. For batch operations, startup applies to the first time the equipment is put into operation at the start of a campaign to produce a product that has been produced in the past if the steps taken to begin production differ from those specified in a standard batch or nonstandard batch. Startup does not apply when the equipment is put into operation as part of a batch within a campaign when the steps taken are routine operations.

*Storage tank* means a tank or other vessel that is used to store liquids that contain organic HAP and/or hydrogen halide and halogen HAP and that has been assigned to an MCPU according to the procedures in  $\S$  63.2435(d). The following are not considered storage tanks for the purposes of this subpart:

(1) Vessels permanently attached to motor vehicles such as trucks, railcars, barges, or ships;

- (2) Pressure vessels designed to operate in excess of 204.9 kilopascals and without emissions to the atmosphere;
- (3) Vessels storing organic liquids that contain HAP only as impurities;

(4) Wastewater storage tanks;

(5) Bottoms receivers;

- (6) Surge control vessels; and
- (7) Process tanks.

*Supplemental gases* means the air that is added to a vent stream after the vent stream leaves the unit operation. Air that is part of the vent stream as a result of the nature of the unit operation is not considered supplemental gases. Air required to operate combustion device burner(s) is not considered supplemental gases.

*Surge control vessel* means feed drums, recycle drums, and intermediate vessels as part of any continuous operation. Surge control vessels are used within an MCPU when in-process storage, mixing, or management of flowrates or volumes is needed to introduce material into continuous operations.

*Thermal expansion relief valve* means a pressure relief valve designed to protect equipment from excess pressure due to thermal expansion of blocked liquid-filled equipment or piping due to ambient heating or heat from a heat tracing system. Pressure relief valves designed to protect equipment from excess pressure due to blockage against a pump or compressor or due to fire contingency are not thermal expansion relief valves.

*Total organic compounds or (TOC)* means the total gaseous organic compounds (minus methane and ethane) in a vent stream.

*Transfer rack* means the collection of loading arms and loading hoses, at a single loading rack, that are assigned to an MCPU according to the procedures specified in  $\frac{63.2435(d)}{12}$  and are used to fill tank trucks and/or rail cars with organic liquids that contain one or more of the organic HAP listed in section 112(b) of the CAA of this subpart. Transfer rack includes the associated pumps, meters, shutoff valves, relief valves, and other piping and valves.

*Unit operation* means those processing steps that occur within distinct equipment that are used, among other things, to prepare reactants, facilitate reactions, separate and purify products, and recycle materials. Equipment used for these purposes includes, but is not limited to, reactors, distillation columns, extraction columns, absorbers, decanters, dryers, condensers, and filtration equipment.

*Waste management* unit means the equipment, structure(s), and/or device(s) used to convey, store, treat, or dispose of wastewater streams or residuals. Examples of waste management units include wastewater tanks, air flotation units, surface impoundments, containers, oil-water or organic-water separators, individual drain systems, biological wastewater treatment units, waste incinerators, and organic removal devices such as steam and air stripper units, and thin film evaporation units. If such equipment is being operated as a recovery device, then it is part of a miscellaneous organic chemical manufacturing process and is not a waste management unit.

*Wastewater* means water that is discarded from an MCPU or control device through a POD and that contains either: an annual average concentration of compounds in tables 8 and 9 to this subpart of at least 5 ppmw and has an annual average flowrate of 0.02 liters per minute or greater; or an annual average concentration of compounds in tables 8 and 9 to this subpart of at least 10,000 ppmw at any flowrate. Wastewater means process wastewater or maintenance wastewater. The following are not considered wastewater for the purposes of this subpart:

- (1) Stormwater from segregated sewers;
- (2) Water from fire-fighting and deluge systems, including testing of such systems;
- (3) Spills;
- (4) Water from safety showers;

(5) Samples of a size not greater than reasonably necessary for the method of analysis that is used;

(6) Equipment leaks;

(7) Wastewater drips from procedures such as disconnecting hoses after cleaning lines; and

(8) Noncontact cooling water.

Wastewater stream means a stream that contains only wastewater as defined in this paragraph (i).

*Work practice standard* means any design, equipment, work practice, or operational standard, or combination thereof, that is promulgated pursuant to section 112(h) of the CAA.

[<u>68 FR 63888</u>, Nov. 10, 2003, as amended at <u>70 FR 38560</u>, July 1, 2005; <u>71 FR 40338</u>, July 14, 2006; <u>85 FR 49159</u>, Aug. 12, 2020; <u>89 FR 23872</u>, Apr. 4, 2024]

#### Table 1 to Subpart FFFF of Part 63—Emission Limits and Work Practice Standards for Continuous Process Vents

As required in <u>§ 63.2455</u>, you must meet each emission limit and work practice standard in the following table that applies to your continuous process vents:

For each	For which	Then you must
1. Group 1 continuous process vent	a. Not applicable	i. Reduce emissions of total organic HAP by $\ge 98$ percent by weight or to an outlet process concentration $\le 20$ ppmv as organic HAP or TOC by venting emissions through a closed-vent system to any combination of control devices (except a flare); or
		ii. Reduce emissions of total organic HAP by venting emissions through a closed vent system to a flare; or
		iii. Use a recovery device to maintain the TRE above 1.9 for an existing source or above 5.0 for a new source.
2. Halogenated Group 1 continuous process vent stream	a. You use a combustion control device to control organic HAP emissions	i. Use a halogen reduction device after the combustion device to reduce emissions of hydrogen halide and halogen HAP by $\geq$ 99 percent by weight, or to $\leq$ 0.45 kg/hr, or to $\leq$ 20 ppmv; or
		ii. Use a halogen reduction device before the combustion device to reduce the halogen atom mass emission rate to $\leq 0.45$ kg/hr or to a concentration $\leq 20$ ppmv.
3. Group 2 continuous process vent at an existing source	You use a recovery device to maintain the TRE level >1.9 but $\leq$ 5.0	Comply with the requirements in $\S 63.2450(e)(4)$ and the requirements in $\S 63.993$ and the requirements referenced therein.
4. Group 2 continuous process vent at a new source	You use a recovery device to maintain the TRE level $>5.0$ but $\le 8.0$	Comply with the requirements in $\S 63.2450(e)(4)$ and the requirements in $\S 63.993$ and the requirements referenced therein.
5. Continuous process vent	Beginning no later than the compliance dates specified in § $63.2445(i)$ , the continuous process vent contains ethylene oxide such that it is considered to be in ethylene oxide service as defined in § $63.2550$	Comply with the applicable emission limits specified in items 1 through 4 of this Table, and also: i. Reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a flare; or ii. Reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a control device that reduces ethylene oxide by $\geq$ 99.9 percent by weight, or to a concentration <1 ppmv for each process vent or to <5 pounds per year for all combined process vents.

[85 FR 49161, Aug. 12, 2020]

#### Table 2 to Subpart FFFF of Part 63—Emission Limits and Work Practice Standards for Batch Process Vents

As required in <u>§ 63.2460</u>, you must meet each emission limit and work practice standard in the following table that applies to your batch process vents:

For each	Then you must	And you must
1. Process with Group 1 batch process vents	a. Reduce collective uncontrolled organic HAP emissions from the sum of all batch process vents within the process by $\ge 98$ percent by weight by venting emissions from a sufficient number of the vents through one or more closed-vent systems to any combination of control devices (except a flare); or	Not applicable.
	b. Reduce collective uncontrolled organic HAP emissions from the sum of all batch process vents within the process by $\geq$ 95 percent by weight by venting emissions from a sufficient number of the vents through one or more closed-vent systems to any combination of recovery devices or a biofilter, except you may elect to comply with the requirements of <u>subpart WW of</u> <u>this part</u> for any process tank; or	Not applicable.
	c. Reduce uncontrolled organic HAP emissions from one or more batch process vents within the process by venting through a closed-vent system to a flare or by venting through one or more closed-vent systems to any combination of control devices (excluding a flare) that reduce organic HAP to an outlet concentration $\leq 20$ ppmv as TOC or total organic HAP	For all other batch process vents within the process, reduce collective organic HAP emissions as specified in item 1.a and/or item 1.b of this Table.
2. Halogenated Group 1 batch process vent for which you use a combustion device to control organic HAP emissions	a. Use a halogen reduction device after the combustion control device; or	i. Reduce overall emissions of hydrogen halide and halogen HAP by $\geq$ 99 percent; or ii. Reduce overall emissions of hydrogen halide and halogen HAP to $\leq$ 0.45 kg/hr; or iii. Reduce overall emissions of hydrogen halide and halogen HAP to a concentration $\leq$ 20 ppmv.
	b. Use a halogen reduction device before the combustion control device	Reduce the halogen atom mass emission rate to $\leq 0.45$ kg/hr or to a concentration $\leq 20$ ppmv.
3. Batch process vent that contains ethylene oxide such that it is considered to be in ethylene oxide service as defined in $\frac{63.2550}{50}$	Beginning no later than the compliance dates specified in § 63.2445(i), comply with the applicable emission limits specified in items 1 and 2 of this Table, and also: i. Reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a flare; or ii. Reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a control device that reduces ethylene oxide by $\geq$ 99.9 percent by weight, or to a concentration <1 ppmv for each process vent or to <5 pounds per year for all combined process vents.	Not applicable.

#### [<u>85 FR 49161</u>, Aug. 12, 2020]

# Table 3 to Subpart FFFF of Part 63—Emission Limits for Hydrogen Halide and Halogen HAP Emissions or HAP Metals Emissions From Process Vents

As required in <u>§ 63.2465</u>, you must meet each emission limit in the following table that applies to your process vents that contain hydrogen halide and halogen HAP emissions or PM HAP emissions:

For each	You must
1. Process with uncontrolled hydrogen halide and halogen HAP emissions from process vents ≥1,000 lb/yr	a. Reduce collective hydrogen halide and halogen HAP emissions by $\geq$ 99 percent by weight or to an outlet concentration $\leq$ 20 ppmv by venting through one or more closed-vent systems to any combination of control devices, or
	b. Reduce the halogen atom mass emission rate from the sum of all batch process vents and each individual continuous process vent to $\leq 0.45$ kg/hr by venting through one or more closed-vent systems to a halogen reduction device.
2. Process at a new source with uncontrolled emissions from process vents ≥150 lb/yr of HAP metals	Reduce overall emissions of HAP metals by $\geq$ 97 percent by weight.

[68 FR 63888, Nov. 10, 2003, as amended at 71 FR 40340, July 14, 2006]

#### Table 4 to Subpart FFFF of Part 63—Emission Limits for Storage Tanks

As required in <u>§ 63.2470</u>, you must meet each emission limit in the following table that applies to your storage tanks:

For each	For which	Then you must
1. Group 1 storage tank	a. The maximum true vapor pressure of total HAP at the storage temperature is ≥76.6 kilopascals	i. Reduce total HAP emissions by $\geq$ 95 percent by weight or to $\leq$ 20 ppmv of TOC or organic HAP and $\leq$ 20 ppmv of hydrogen halide and halogen HAP by venting emissions through a closed vent system to any combination of control devices (excluding a flare); or
		ii. Reduce total organic HAP emissions by venting emissions through a closed vent system to a flare; or
		iii. Comply with the requirements in § $63.2450(e)(4)$ , as applicable; and reduce total HAP emissions by venting emissions to a fuel gas system or process in accordance with § $63.982(d)$ and the requirements referenced therein. <sup>1</sup>
	b. The maximum true vapor pressure of total HAP at the storage temperature is <76.6 kilopascals	i. Comply with the requirements of <u>subpart WW of this</u> <u>part</u> , except as specified in <u>§ 63.2470</u> ; or
		ii. Reduce total HAP emissions by $\geq$ 95 percent by weight or to $\leq$ 20 ppmv of TOC or organic HAP and $\leq$ 20 ppmv of hydrogen halide and halogen HAP by venting emissions through a closed vent system to any combination of control devices (excluding a flare); or
		iii. Reduce total organic HAP emissions by venting emissions through a closed vent system to a flare; or
		iv. Comply with the requirements in $\S 63.2450(e)(4)$ , as applicable; and reduce total HAP emissions by venting emissions to a fuel gas system or process in accordance with $\S 63.982(d)$ and the requirements referenced therein. <sup>1</sup>
2. Halogenated vent stream from a Group 1 storage tank	You use a combustion control device to control organic HAP emissions	Meet one of the emission limit options specified in Item 2.a.i or ii. in Table 1 to this subpart.
3. Storage tank of any capacity and vapor pressure	Beginning no later than the compliance dates specified in $\S$ 63.2445(i), the stored liquid contains ethylene oxide such that the storage	Comply with the applicable emission limits specified in items 1 and 2 of this Table, and also: i. Reduce emissions of ethylene oxide by venting

For each	For which	Then you must
	tank is considered to be in ethylene oxide service as defined in <u>§ 63.2550</u>	emissions through a closed-vent system to a flare; or ii. Reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a control device that reduces ethylene oxide by $\geq$ 99.9 percent by weight, or to a concentration <1 ppmv for each storage tank vent.

<sup>1</sup> Beginning no later than the compliance dates specified in § <u>63.2445(g)</u>, any flare using fuel gas from a fuel gas system, of which 50 percent or more of the fuel gas is derived from an MCPU that has processes and/or equipment in ethylene oxide service or that produces olefins or polyolefins, as determined on an annual average basis, must be in compliance with § <u>63.2450(e)(5)</u>. For purposes of compliance, an MCPU that "produces olefins or polyolefins" includes only those MCPUs that manufacture ethylene, propylene, polyethylene, and/or polypropylene as a product. By-products and impurities as defined in § <u>63.101</u>, as well as wastes and trace contaminants, are not considered products.

#### [<u>85 FR 49162</u>, Aug. 12, 2020]

#### Table 5 to Subpart FFFF of Part 63-Emission Limits and Work Practice Standards for Transfer Racks

As required in  $\S$  63.2475, you must meet each emission limit and work practice standard in the following table that applies to your transfer racks:

For each	You must
1. Group 1 transfer rack	a. Reduce emissions of total organic HAP by $\geq$ 98 percent by weight or to an outlet concentration $\leq$ 20 ppmv as organic HAP or TOC by venting emissions through a closed-vent system to any combination of control devices (except a flare); or
	b. Reduce emissions of total organic HAP by venting emissions through a closed- vent system to a flare; or
	c. Comply with the requirements in $\S 63.2450(e)(4)$ , as applicable; and reduce emissions of total organic HAP by venting emissions to a fuel gas system or process in accordance with $\S 63.982(d)$ and the requirements referenced therein; <sup>1</sup> or
	d. Use a vapor balancing system designed and operated to collect organic HAP vapors displaced from tank trucks and railcars during loading and route the collected HAP vapors to the storage tank from which the liquid being loaded originated or to another storage tank connected by a common header.
2. Halogenated Group 1 transfer rack vent stream for which you use a combustion device to control organic HAP emissions	a. Use a halogen reduction device after the combustion device to reduce emissions of hydrogen halide and halogen HAP by $\geq$ 99 percent by weight, to $\leq$ 0.45 kg/hr, or to $\leq$ 20 ppmv; or b. Use a halogen reduction device before the combustion device to reduce the halogen atom mass emission rate to $\leq$ 0.45 kg/hr or to a concentration $\leq$ 20 ppmv.

<sup>1</sup> Beginning no later than the compliance dates specified in § <u>63.2445(g)</u>, any flare using fuel gas from a fuel gas system, of which 50 percent or more of the fuel gas is derived from an MCPU that has processes and/or equipment in ethylene oxide service or that produces olefins or polyolefins, as determined on an annual average basis, must be in compliance with § <u>63.2450(e)(5)</u>. For purposes of compliance, an MCPU that "produces olefins or polyolefins" includes only those MCPUs that manufacture ethylene, propylene, polyethylene, and/or polypropylene as a product. By-products and impurities as defined in § <u>63.101</u>, as well as wastes and trace contaminants, are not considered products.

#### [85 FR 49163, Aug. 12, 2020]

#### Table 6 to Subpart FFFF of Part 63—Requirements for Equipment Leaks

As required in <u>§ 63.2480</u>, you must meet each requirement in the following table that applies to your equipment leaks:

For all	And that is part of .	You must
	••	

For all	And that is part of . 	You must
1. Equipment that is in organic HAP service	a. Any MCPU	i. Comply with the requirements of <u>subpart UU of this part</u> and the requirements referenced therein, except as specified in $\S$ 63.2480(b) and (d) through (f); or
		ii. Comply with the requirements of subpart H of this part and the requirements referenced therein, except as specified in $\S$ 63.2480(b) and (d) through (f); or
		iii. Comply with the requirements of <u>40 CFR part 65</u> , subpart F, and <u>the</u> requirements referenced therein, except as specified in § <u>63.2480(c)</u> , and <u>(d)</u> through <u>(f)</u> .
2. Equipment that is in organic HAP service at a new source	a. Any MCPU	i. Comply with the requirements of <u>subpart UU of this part</u> and the requirements referenced therein, except as specified in <u>§ 63.2480(b)(6)</u> and <u>(7)</u> , <u>(e)</u> , and <u>(f)</u> ; or
		ii. Comply with the requirements of $\frac{40 \text{ CFR part 65, subpart F}}{63.2480(c)(10)}$ and $\frac{(11)}{(e)}$ , and $\frac{(f)}{(f)}$ .
3. Equipment that is in ethylene oxide service as defined in $\frac{63.2550}{50}$	a. Any MCPU	i. Beginning no later than the compliance dates specified in $\S$ 63.2445(i), comply with the requirements of subpart UU of this part and the requirements referenced therein, except as specified in $\S$ 63.2493(d) and (e); or
		ii. Beginning no later than the compliance dates specified in $\S$ 63.2445(i), comply with the requirements of subpart H of this part and the requirements referenced therein, except as specified in $\S$ 63.2493(d) and (e);
		iii. Beginning no later than the compliance dates specified in $\S$ 63.2445(i), comply with the requirements of 40 CFR part 65, subpart F, and the requirements referenced therein, except as specified in $\S$ 63.2493(d) and (e).

#### [85 FR 49163, Aug. 12, 2020]

## Table 7 to Subpart FFFF of Part 63—Requirements for Wastewater Streams and Liquid Streams in Open Systems Within an MCPU

As required in <u>§ 63.2485</u>, you must meet each requirement in the following table that applies to your wastewater streams and liquid streams in open systems within an MCPU:

For each	You must
1. Process wastewater stream	Comply with the requirements in $\frac{\$\$ 63.132}{\$63.2485}$ through $\frac{63.148}{\$63.2485}$ and the requirements referenced therein, except as specified in $\frac{\$ 63.2485}{\$63.2485}$ .
2. Maintenance wastewater stream	Comply with the requirements in $\S 63.105$ and the requirements referenced therein, except as specified in $\S 63.2485$ .
3. Liquid streams in an open system within an MCPU	Comply with the requirements in $\frac{63.149}{2}$ and the requirements referenced therein, except as specified in $\frac{63.2485}{2}$ .

#### Table 8 to Subpart FFFF of Part 63—Partially Soluble Hazardous Air Pollutants

As specified in § 63.2485, the partially soluble HAP in wastewater that are subject to management and treatment requirements in this subpart FFFF are listed in the following table:

Chemical name	CAS No.
1. 1,1,1-Trichloroethane (methyl chloroform)	71556
2. 1,1,2,2-Tetrachloroethane	79345
3. 1,1,2-Trichloroethane	79005
4. 1,1-Dichloroethylene (vinylidene chloride)	75354
5. 1,2-Dibromoethane	106934

Chemical name	CAS No.
6. 1,2-Dichloroethane (ethylene dichloride)	107062
7. 1,2-Dichloropropane	78875
8. 1,3-Dichloropropene	542756
9. 2,4,5-Trichlorophenol	95954
10. 1,4-Dichlorobenzene	106467
11. 2-Nitropropane	79469
12. 4-Methyl-2-pentanone (MIBK)	108101
13. Acetaldehyde	75070
14. Acrolein	107028
15. Acrylonitrile	107131
16. Allyl chloride	107051
17. Benzene	71432
18. Benzyl chloride	100447
19. Biphenyl	92524
20. Bromoform (tribromomethane)	75252
21. Bromomethane	74839
22. Butadiene	106990
23. Carbon disulfide	75150
24. Chlorobenzene	108907
25. Chloroethane (ethyl chloride)	75003
26. Chloroform	67663
27. Chloromethane	74873
28. Chloroprene	126998
29. Cumene	98828
30. Dichloroethyl ether	111444
31. Dinitrophenol	51285
32. Epichlorohydrin	106898
33. Ethyl acrylate	140885
34. Ethylbenzene	100414
35. Ethylene oxide	75218
36. Ethylidene dichloride	75343
37. Hexachlorobenzene	118741
38. Hexachlorobutadiene	87683
39. Hexachloroethane	67721
40. Methyl methacrylate	80626
41. Methyl-t-butyl ether	1634044
42. Methylene chloride	75092
43. N-hexane	110543
44. N,N-dimethylaniline	121697
45. Naphthalene	91203
46. Phosgene	75445

Chemical name	CAS No.
47. Propionaldehyde	123386
48. Propylene oxide	75569
49. Styrene	100425
50. Tetrachloroethylene (perchloroethylene)	127184
51. Tetrachloromethane (carbon tetrachloride)	56235
52. Toluene	108883
53. Trichlorobenzene (1,2,4-)	120821
54. Trichloroethylene	79016
55. Trimethylpentane	540841
56. Vinyl acetate	108054
57. Vinyl chloride	75014
58. Xylene (m)	108383
59. Xylene (o)	95476
60. Xylene (p)	106423

[68 FR 63888, Nov. 10, 2003, as amended at 70 FR 38560, July 1, 2005; 71 FR 40341, July 14, 2006]

## Table 9 to Subpart FFFF of Part 63—Soluble Hazardous Air Pollutants

As specified in <u>§ 63.2485</u>, the soluble HAP in wastewater that are subject to management and treatment requirements of this subpart FFFF are listed in the following table:

Chemical name	CAS No.
1. Acetonitrile	75058
2. Acetophenone	98862
3. Diethyl sulfate	64675
4. Dimethyl hydrazine (1,1)	57147
5. Dimethyl sulfate	77781
6. Dinitrotoluene (2,4)	121142
7. Dioxane (1,4)	123911
8. Ethylene glycol dimethyl ether	110714
9. Ethylene glycol monobutyl ether acetate	112072
10. Ethylene glycol monomethyl ether acetate	110496
11. Isophorone	78591
12. Methanol	67561
13. Nitrobenzene	98953
14. Toluidine (o-)	95534
15. Triethylamine	121448

[68 FR 63888, Nov. 10, 2003, as amended at 70 FR 38561, July 1, 2005]

## Table 10 to Subpart FFFF of Part 63—Work Practice Standards for Heat Exchange Systems

As required in <u>§ 63.2490</u>, you must meet each requirement in the following table that applies to your heat exchange systems:

For each	You must
Heat exchange system, as	a. Comply with the requirements of $\S$ 63.104 and the requirements referenced therein,

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For each	You must	
defined in <u>§ 63.101</u>	except as specified in § 63.2490(b) and (c); or	
	b. Comply with the requirements in § 63.2490(d); or	
	c. Comply with the requirements in $\S 63.2490(e)$ .	

#### [<u>89 FR 23873</u>,, Apr. 4, 2024]

#### Table 11 to Subpart FFFF of Part 63—Requirements for Reports

As required in (63.2520(a)) and (b), you must submit each report that applies to you on the schedule shown in the following table:

You must submit a(n)	The report must contain	You must submit the report
1. Precompliance report	The information specified in $\S$ 63.2520(c)	At least 6 months prior to the compliance date; or for new sources, with the application for approval of construction or reconstruction.
2. Notification of compliance status report	The information specified in § 63.2520(d)	No later than 150 days after the compliance date specified in $\S$ <u>63.2445</u> .
3. Compliance report	The information specified in $\S$ 63.2520(e)	Semiannually according to the requirements in $\S 63.2520(b)$ .

#### Table 12 to Subpart FFFF of Part 63—Applicability of General Provisions to Subpart FFFF

As specified in <u>§ 63.2540</u>, the parts of the General Provisions that apply to you are shown in the following table:

Citation	Subject	Explanation
§ 63.1	Applicability	Yes.
§ 63.2	Definitions	Yes.
§ 63.3	Units and Abbreviations	Yes.
§ 63.4	Prohibited Activities	Yes.
§ 63.5	Construction/Reconstruction	Yes.
§ 63.6(a)	Applicability	Yes.
§ 63.6(b)(1)-(4)	Compliance Dates for New and Reconstructed sources	Yes.
§ 63.6(b)(5)	Notification	Yes.
§ 63.6(b)(6)	[Reserved]	
§ 63.6(b)(7)	Compliance Dates for New and Reconstructed Area Sources That Become Major	Yes.
§ 63.6(c)(1)-(2)	Compliance Dates for Existing Sources	Yes.
§ 63.6(c)(3)-(4)	[Reserved]	
§ 63.6(c)(5)	Compliance Dates for Existing Area Sources That Become Major	Yes.
§ 63.6(d)	[Reserved]	
§ 63.6(e)(1)(i)	Operation & Maintenance	Yes, before August 12, 2023.

Citation	Subject	Explanation
		No, beginning on and after August 12, 2023. See <u>§ 63.2450(u)</u> for general duty requirement.
§ 63.6(e)(1)(ii)	Operation & Maintenance	Yes, before August 12, 2023. No, beginning on and after August 12, 2023.
§ 63.6(e)(1)(iii)	Operation & Maintenance	Yes.
§ 63.6(e)(2)	[Reserved]	
§ 63.6(e)(3)(i), (iii), and (v) through (viii)	Startup, Shutdown, Malfunction Plan (SSMP)	Yes, before August 12, 2023, except information regarding Group 2 emission points and equipment leaks is not required in the SSMP, as specified in $\S$ 63.2525(j). No, beginning on and after August 12, 2023.
§ 63.6(e)(3)(iii) and (iv)	Recordkeeping and Reporting During SSM	No, see § 63.2525 for recordkeeping requirements and § $63.2520(e)(4)$ for reporting requirements.
§ 63.6(e)(3)(ix)	SSMP incorporation into title V permit	Yes, before August 12, 2023. No beginning on and after August 12, 2023.
§ 63.6(f)(1)	Compliance With Non-Opacity Standards Except During SSM	No. See <u>§ 63.2445(g)</u> through <u>(i)</u> .
§ 63.6(f)(2)-(3)	Methods for Determining Compliance	Yes.
§ 63.6(g)(1)-(3)	Alternative Standard	Yes.
§ 63.6(h)(1)	Compliance with Opacity Standards Except During SSM	No. See $\S 63.2445(g)$ through (i).
§ 63.6(h)(2)-(9)	Opacity/Visible Emission (VE) Standards	Only for flares for which Method 22 of <u>40 CFR part 60, appendix A</u> -7, observations are required as part of a flare compliance assessment.
§ 63.6(i)(1)-(14), and (16)	Compliance Extension	Yes.
§ 63.6(j)	Presidential Compliance Exemption	Yes.
§ 63.7(a)(1)-(2)	Performance Test Dates	Yes, except substitute 150 days for 180 days.
§ 63.7(a)(3)	Section 114 Authority	Yes, and this paragraph also applies to flare compliance assessments as specified under $\frac{63.997(b)(2)}{2}$ .
§ 63.7(a)(4)	Force Majeure	Yes.
§ 63.7(b)(1)	Notification of Performance Test	Yes.
§ 63.7(b)(2)	Notification of Rescheduling	Yes.
§ 63.7(c)	Quality Assurance/Test Plan	Yes, except the test plan must be submitted with the notification of the performance test if the control device controls batch process vents.
§ 63.7(d)	Testing Facilities	Yes.
§ 63.7(e)(1)	Conditions for Conducting Performance Tests	Yes, before August 12, 2023 except that performance tests for batch process vents must be conducted under worst-case conditions as specified in $\S$ 63.2460. No, beginning on and after August 12, 2023. See $\S$ 63.2450(g)(6).
§ 63.7(e)(2)	Conditions for Conducting Performance Tests	Yes.
§ 63.7(e)(3)	Test Run Duration	Yes.
§ 63.7(e)(4)	Administrator's Authority to Require Testing	Yes.

Citation	Subject	Explanation
§ 63.7(f)	Alternative Test Method	Yes.
§ 63.7(g)	Performance Test Data Analysis	Yes, except this subpart specifies how and when the performance test and performance evaluation results are reported.
§ 63.7(h)	Waiver of Tests	Yes.
§ 63.8(a)(1)	Applicability of Monitoring Requirements	Yes.
§ 63.8(a)(2)	Performance Specifications	Yes.
§ 63.8(a)(3)	[Reserved]	
§ 63.8(a)(4)	Monitoring with Flares	Yes, except for flares subject to $\S 63.2450(e)(5)$ .
§ 63.8(b)(1)	Monitoring	Yes.
§ 63.8(b)(2)-(3)	Multiple Effluents and Multiple Monitoring Systems	Yes.
§ 63.8(c)(1)	Monitoring System Operation and Maintenance	Yes.
§ 63.8(c)(1)(i)	Routine and Predictable SSM	Yes, before August 12, 2023. No, beginning on and after August 12, 2023.
§ 63.8(c)(1)(ii)	CMS malfunction not in SSM plan	Yes.
§ 63.8(c)(1)(iii)	Compliance with Operation and Maintenance Requirements	Yes, before August 12, 2023. No, beginning on and after August 12, 2023.
§ 63.8(c)(2)-(3)	Monitoring System Installation	Yes.
§ 63.8(c)(4)	CMS Requirements	Only for CEMS. Requirements for CPMS are specified in referenced <u>subparts G</u> and <u>SS of this part</u> . Requirements for COMS do not apply because this subpart does not require continuous opacity monitoring systems (COMS).
§ 63.8(c)(4)(i)	COMS Measurement and Recording Frequency	No; this subpart does not require COMS.
§ 63.8(c)(4)(ii)	CEMS Measurement and Recording Frequency	Yes.
§ 63.8(c)(5)	COMS Minimum Procedures	No. This subpart does not contain opacity or VE limits.
§ 63.8(c)(6)	CMS Requirements	Only for CEMS; requirements for CPMS are specified in referenced subparts G and SS of this part. Requirements for COMS do not apply because this subpart does not require COMS.
§ 63.8(c)(7)-(8)	CMS Requirements	Only for CEMS. Requirements for CPMS are specified in referenced <u>subparts G</u> and <u>SS of this part</u> . Requirements for COMS do not apply because this subpart does not require COMS.
§ 63.8(d)(1)	CMS Quality Control	Only for CEMS.
§ 63.8(d)(2)	CMS Quality Control	Only for CEMS.
§ 63.8(d)(3)	CMS Quality Control	Yes, only for CEMS before August 12, 2023. No, beginning on and after August 12, 2023. See $\S$ <u>63.2450(j)(6)</u> .
§ 63.8(e)	CMS Performance Evaluation	Only for CEMS, except this subpart specifies how and when the performance evaluation results are reported. Section 63.8(e)(5)(ii) does not apply because this subpart does not require COMS.
§ 63.8(f)(1)-(5)	Alternative Monitoring Method	Yes, except you may also request approval using the precompliance report.
§ 63.8(f)(6)	Alternative to Relative Accuracy	Only applicable when using CEMS to demonstrate compliance,

Citation	Subject	Explanation
	Test	including the alternative standard in $\S 63.2505$ .
§ 63.8(g)(1)-(4)	Data Reduction	Only when using CEMS, including for the alternative standard in § 63.2505, except that the requirements for COMS do not apply because this subpart has no opacity or VE limits, and § 63.8(g)(2) does not apply because data reduction requirements for CEMS are specified in § 63.2450(j).
§ 63.8(g)(5)	Data Reduction	No. Requirements for CEMS are specified in $\S$ 63.2450(j). Requirements for CPMS are specified in referenced subparts <u>G</u> and <u>SS of this part</u> .
§ 63.9(a)	Notification Requirements	Yes.
§ 63.9(b)(1)-(5)	Initial Notifications	Yes.
§ 63.9(c)	Request for Compliance Extension	Yes.
§ 63.9(d)	Notification of Special Compliance Requirements for New Source	Yes.
§ 63.9(e)	Notification of Performance Test	Yes.
§ 63.9(f)	Notification of VE/Opacity Test	No.
§ 63.9(g)	Additional Notifications When Using CMS	Only for CEMS. Section 63.9(g)(2) does not apply because this subpart does not require COMS.
63.9(h)(1)-(6)	Notification of Compliance Status	Yes, except § $63.9(h)(2)(i)(A)$ through (G) and (h)(2)(ii) do not apply because § $63.2520(d)$ specifies the required contents and due date of the notification of compliance status report.
§ 63.9(i)	Adjustment of Submittal Deadlines	Yes.
§ 63.9(j)	Change in previous information	Yes, for change in major source status, otherwise $\S$ <u>63.2520(e)</u> specifies reporting requirements for process changes.
§ 63.9(k)	Electronic reporting procedures	Yes.
§ 63.10(a)	Recordkeeping/Reporting	Yes.
§ 63.10(b)(1)	Recordkeeping/Reporting	Yes.
§ 63.10(b)(2)(i)	Records related to startup and shutdown	No, see <u>§§ 63.2450(e)</u> and <u>63.2525</u> for recordkeeping requirements.
§ 63.10(b)(2)(ii)	Recordkeeping relevant to SSM periods and CMS	Yes, before August 12, 2023. No, beginning on and after August 12, 2023. See $\S$ 63.2525(h) and (l).
§ 63.10(b)(2)(iii)	Records related to maintenance of air pollution control equipment	Yes.
§ 63.10(b)(2)(iv) and (v)	Recordkeeping relevant to SSM period	Yes, before August 12, 2023. No, beginning on and after August 12, 2023.
§ 63.10(b)(2)(vi)	CMS Records	Before August 12, 2023, yes but only for CEMS; requirements for CPMS are specified in referenced <u>subparts G</u> and <u>SS of this part</u> . Beginning on and after August 12, 2023, yes for CEMS and CPMS for flares subject to $\S 63.2450(e)(5)$ .
§ 63.10(b)(2)(x) and (xi)	CMS Records	Only for CEMS; requirements for CPMS are specified in referenced subparts G and SS of this part.
§ 63.10(b)(2)(vii)- (ix)	Records	Yes.
§ 63.10(b)(2)(xii)	Records	Yes.

Citation	Subject	Explanation
§ 63.10(b)(2)(xiii)	Records	Only for CEMS.
§ 63.10(b)(2)(xiv)	Records	Yes.
§ 63.10(b)(3)	Records	Yes.
§ 63.10(c)(1)- (6),(9)-(14)	Records	Only for CEMS. Recordkeeping requirements for CPMS are specified in referenced subparts G and SS of this part.
§ 63.10(c)(7)-(8)	Records	No. Recordkeeping requirements are specified in <u>§ 63.2525</u> .
§ 63.10(c)(15)	Records	Yes, before August 12, 2023, but only for CEMS. No, beginning on and after August 12, 2023.
§ 63.10(d)(1)	General Reporting Requirements	Yes.
§ 63.10(d)(2)	Report of Performance Test Results	Yes, before October 13, 2020. No, beginning on and after October 13, 2020.
§ 63.10(d)(3)	Reporting Opacity or VE Observations	No.
§ 63.10(d)(4)	Progress Reports	Yes.
§ 63.10(d)(5)(i)	Periodic Startup, Shutdown, and Malfunction Reports	No, $\S 63.2520(e)(4)$ and $(5)$ specify the SSM reporting requirements.
§ 63.10(d)(5)(ii)	Immediate SSM Reports	No.
§ 63.10(e)(1)	Additional CEMS Reports	Yes.
§ 63.10(e)(2)(i)	Additional CMS Reports	Only for CEMS, except this subpart specifies how and when the performance evaluation results are reported.
§ 63.10(e)(2)(ii)	Additional COMS Reports	No. This subpart does not require COMS.
§ 63.10(e)(3)	Reports	No. Reporting requirements are specified in § 63.2520.
§ 63.10(e)(3)(i)- (iii)	Reports	No. Reporting requirements are specified in <u>§ 63.2520</u> .
§ 63.10(e)(3)(iv)- (v)	Excess Emissions Reports	No. Reporting requirements are specified in <u>§ 63.2520</u> .
§ 63.10(e)(3)(iv)- (v)	Excess Emissions Reports	No. Reporting requirements are specified in <u>§ 63.2520</u> .
§ 63.10(e)(3)(vi)- (viii)	Excess Emissions Report and Summary Report	No. Reporting requirements are specified in <u>§ 63.2520</u> .
§ 63.10(e)(4)	Reporting COMS data	No.
§ 63.10(f)	Waiver for Recordkeeping/Reporting	Yes.
§ 63.11	Control device requirements for flares and work practice requirements for equipment leaks	Yes, except for flares subject to $\frac{63.2450(e)(5)}{2}$ .
§ 63.12	Delegation	Yes.
§ 63.13	Addresses	Yes.
§ 63.14	Incorporation by Reference	Yes.
§ 63.15	Availability of Information	Yes.

[85 FR 49164, Aug. 12, 2020, as amended at 85 FR 73903, Nov. 19, 2020; 89 FR 23873, Apr. 4, 2024]

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#### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

# Subpart G—National Emission Standards for Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Source:

59 FR 19468, Apr. 22, 1994, unless otherwise noted.

### § 63.110 Applicability.

(a) This subpart applies to all process vents, storage vessels, transfer racks, wastewater streams, and in-process equipment subject to  $\frac{63.149}{10}$  within a source subject to subpart F of this part.

(b) Overlap with other regulations for storage vessels.

(1) After the compliance dates specified in  $\S$  63.100 of subpart F of this part, a Group 1 or Group 2 storage vessel that is also subject to the provisions of 40 CFR part 60, subpart Kb is required to comply only with the provisions of this subpart.

(2) After the compliance dates specified in  $\S$  63.100 of subpart F of this part, a Group 1 storage vessel that is also subject to the provisions of <u>40 CFR part 61</u>, subpart <u>Y</u> is required to comply only with the provisions of this subpart.

(3) Except as specified in <u>paragraph (j)</u> of this section, after the compliance dates specified in <u>§ 63.100</u>, a Group 2 storage vessel that is also subject to the provisions of <u>40 CFR part 61</u>, <u>subpart Y</u> is required to comply only with the provisions of part 61, subpart Y, of this chapter. The recordkeeping and reporting requirements of part 61, subpart Y, will be accepted as compliance with the recordkeeping and reporting requirements of this subpart.

(c) Overlap with other regulations for transfer racks.

(1) After the compliance dates specified in  $\S$  63.100 of subpart F of this part, a Group 1 transfer rack that is also subject to the provisions of <u>40 CFR part 61</u>, subpart BB is required to comply only with the provisions of this subpart.

(2) After the compliance dates specified in § 63.100 of subpart F of this part, a Group 2 transfer rack that is also subject to the provisions of  $\frac{40 \text{ CFR part } 61, \text{ subpart BB}}{1000 \text{ cm}}$  is required to comply with the provisions of either paragraph (c)(2)(i) or (c)(2)(ii) of this subpart.

(i) Except as provided in paragraph (j) of this section, if the transfer rack is subject to the control requirements specified in  $\S$  <u>61.302 of this chapter</u>, then the transfer rack is required to comply with the control requirements of  $\S$  <u>61.302</u>. The owner or operator may elect to comply with either the associated testing, monitoring, reporting, and recordkeeping requirements of part 61, subpart BB, of this chapter or with the testing, monitoring, recordkeeping, and reporting requirements specified in this subpart for Group 1 transfer racks. The owner or operator shall indicate this decision in either the Notification of Compliance Status specified in  $\S$  <u>63.152(b)</u> or in an operating permit application or amendment.

(ii) If the transfer rack is subject only to reporting and recordkeeping requirements under <u>40 CFR part 61</u>, <u>subpart</u> <u>BB</u>, then the transfer rack is required to comply only with the reporting and recordkeeping requirements specified in this subpart for Group 2 transfer racks and is exempt from the reporting and recordkeeping requirements in <u>40 CFR part 61</u>, <u>subpart BB</u>.

(d) Overlap with other regulations for process vents.

(1) After the compliance dates specified in  $\S$  63.100 of subpart F of this part, a Group 1 process vent that is also subject to the provisions of <u>40 CFR part 60</u>, subpart III is required to comply only with the provisions of this subpart.

(2) After the compliance dates specified in  $\S$  <u>63.100</u>, the owner or operator of a Group 2 process vent that is also subject to the provisions of part 60, subpart III, of this chapter shall determine requirements according to <u>paragraphs (d)(2)(i)</u> and <u>(ii)</u> of this section. For each source as defined in  $\S$  <u>63.101</u>, on and after July 15, 2027, this paragraph no longer applies.

(i) If the Group 2 process vent has a TRE value less than 1 as determined by the procedures in  $\frac{40 \text{ CFR part } 60, \text{ subpart}}{\text{III}, \text{ the process vent is required to comply with the provisions in paragraphs (d)(2)(i)(A) through (d)(2)(i)(C) of this section.$ 

(A) The provisions in both this subpart and in <u>40 CFR part 60, subpart III</u> for applicability determination and the associated recordkeeping and reporting;

(B) The provisions in both this subpart and in <u>40 CFR part 60, subpart III</u> for process changes and recalculation of the TRE index value and the associated recordkeeping and reporting; and

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(C) The control requirements in  $\S$  60.612 of 40 CFR part 60, subpart III. The owner or operator may elect to comply with either the associated testing, monitoring, reporting, and recordkeeping requirements of 40 CFR part 60, subpart III or with the testing, monitoring, reporting, and recordkeeping requirements specified in this subpart for Group 1 process vents. The owner or operator shall indicate this decision in either the Notification of Compliance Status specified in  $\S$  63.152(b) of this subpart or in an operating permit application or amendment.

(ii) If the Group 2 process vent has a TRE value greater than or equal to 1 as determined by the procedures in  $\frac{40 \text{ CFR part}}{40 \text{ CFR part}}$ <u>60, subpart III, the</u> process vent is required to comply only with the provisions specified in <u>paragraphs</u> (d)(2)(ii)(A) through (d)(2)(ii)(D) of this section.

(A) The provisions in both this subpart and in <u>40 CFR part 60, subpart III</u> for applicability determination and the associated recordkeeping and reporting;

(B) The provisions in both this subpart and in <u>40 CFR part 60, subpart III</u> for process changes and recalculation of the TRE index value and the associated recordkeeping and reporting;

(C) If the provisions of both this subpart and <u>40 CFR part 60, subpart III</u> require continuous monitoring of recovery device operating parameters, the process vent is required to comply only with the provisions that are specified in this subpart for continuous monitoring of recovery device operating parameters and the associated testing, reporting, and recordkeeping.

(D) If only the provisions of <u>40 CFR part 60, subpart III</u> require continuous monitoring of recovery device operating parameters, the process vent is required to comply only with the provisions that are specified in <u>40 CFR part 60, subpart</u> <u>III</u> for continuous monitoring of recovery device operating parameters and the associated testing, reporting, and recordkeeping.

(3) After the compliance dates specified in 63.100, if an owner or operator of a process vent subject to this subpart that is also subject to the provisions of part 60, subpart III, of this chapter elects to control the process vent to the levels required in § 63.113(a)(1) or (2) without calculating the TRE index value for the vent according to the procedures specified in § 63.115(d), then the owner or operator shall comply with the testing, monitoring, reporting, and recordkeeping provisions of this subpart III. For each source as defined in § 63.101, on and after July 15, 2027, this paragraph no longer applies.

(4) After the compliance dates specified in § 63.100 of subpart F of this part, a Group 1 process vent that is also subject to the provisions of 40 CFR part 60, subpart NNN is required to comply only with the provisions of this subpart.

(5) After the compliance dates specified in § 63.100, the owner or operator of a Group 2 process vent that is also subject to the provisions of <u>40 CFR part 60</u>, subpart NNN shall determine requirements according to <u>paragraphs (d)(5)(i)</u> and <u>(ii)</u> of this section. For each source as defined in § 63.101, on and after July 15, 2027, this paragraph no longer applies.

(i) If the Group 2 process vent has a TRE value less than 1 as determined by the procedures in  $\frac{40 \text{ CFR part } 60, \text{ subpart }}{\text{NNN}}$ , the process vent is required to comply with the provisions in paragraphs (d)(5)(i)(A) through (d)(5)(i)(C) of this section.

(A) The provisions in both this subpart and in <u>40 CFR part 60, subpart NNN</u> for applicability determination and the associated recordkeeping and reporting;

(B) The provisions in both this subpart and in <u>40 CFR part 60, subpart NNN</u> for process changes and recalculation of the TRE index value and the associated recordkeeping and reporting; and

(C) The control requirements in § 60.662 of 40 CFR part 60, subpart NNN. The owner or operator may elect to comply with either the associated testing, monitoring, reporting, and recordkeeping requirements of  $\frac{40 \text{ CFR part } 60}{40 \text{ CFR part } 60}$ , subpart NNN or with the testing, monitoring, reporting, and recordkeeping requirements specified in this subpart for Group 1 process vents. The owner or operator shall indicate this decision in either the Notification of Compliance Status specified in § 63.152(b) of this subpart or in an operating permit application or amendment.

(ii) If the Group 2 process vent has a TRE value greater than or equal to 1 as determined by the procedures in  $\frac{40 \text{ CFR part}}{60, \text{ subpart NNN}}$ , the process vent is required to comply only with the provisions specified in paragraphs (d)(5)(ii)(A) through (d)(5)(ii)(D) of this section.

(A) The provisions in both this subpart and in <u>40 CFR part 60, subpart NNN</u> for applicability determination and the associated recordkeeping and reporting;
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(B) The provisions in both this subpart and in <u>40 CFR part 60, subpart NNN</u> for process changes and recalculation of the TRE index value and the associated recordkeeping and reporting;

(C) If the provisions of both this subpart and <u>40 CFR part 60</u>, <u>subpart NNN</u> require continuous monitoring of recovery device operating parameters, the process vent is required to comply only with the provisions that are specified in this subpart for continuous monitoring of recovery device operating parameters and the associated testing, reporting, and recordkeeping.

(D) If only the provisions of <u>40 CFR part 60, subpart NNN</u> require continuous monitoring of recovery device operating parameters, the process vent is required to comply only with the provisions that are specified in <u>40 CFR part 60, subpart NNN</u> for continuous monitoring of recovery device operating parameters and the associated testing, reporting, and recordkeeping.

(6) After the compliance dates specified in § 63.100, if an owner or operator of a process vent subject to this subpart that is also subject to the provisions of part 60, subpart NNN, of this chapter elects to control the process vent to the levels required in § 63.113(a)(1) or (2) without calculating the TRE index value for the vent according to the procedures specified in § 63.115(d), then the owner or operator shall comply with the testing, monitoring, reporting, and recordkeeping provisions of this subpart and shall be exempt from the testing, monitoring, reporting, and recordkeeping provisions of part 60, subpart NNN. For each source as defined in § 63.101, on and after July 15, 2027, this paragraph no longer applies.

(7) After the compliance dates specified in § 63.100 of subpart F of this part, a Group 1 process vent that is also subject to the provisions of 40 CFR part 60, subpart RRR is required to comply only with the provisions of this subpart.

(8) After the compliance dates specified in § 63.100, the owner or operator of a Group 2 process vent that is also subject to the provisions of part 60, subpart RRR, of this chapter shall determine requirements according to paragraphs (d)(8)(i) and (ii) of this section. For each source as defined in § 63.101, on and after July 15, 2027, this paragraph no longer applies.

(i) If the Group 2 process vent has a TRE value less than 1 as determined by the procedures in  $\frac{40 \text{ CFR part } 60, \text{ subpart}}{\text{RRR}}$ , the process vent is required to comply with the provisions in paragraphs (d)(8)(i)(A) through (d)(8)(i)(C) of this section.

(A) The provisions in both this subpart and in <u>40 CFR part 60, subpart RRR</u> for applicability determination and the associated recordkeeping and reporting;

(B) The provisions in both this subpart and in <u>40 CFR part 60, subpart RRR</u> for process changes and recalculation of the TRE index value and the associated recordkeeping and reporting; and

(C) The control requirements in § 60.702 of 40 CFR part 60, subpart RRR. The owner or operator may elect to comply with either the associated testing, monitoring, reporting, and recordkeeping requirements of 40 CFR part 60, subpart RRR or with the testing, monitoring, reporting, and recordkeeping requirements specified in this subpart for Group 1 process vents. The owner or operator shall indicate this decision in either the Notification of Compliance Status specified in § 63.152(b) of this subpart or in an operating permit application or amendment.

(ii) If the Group 2 process vent has a TRE value greater than or equal to 1 as determined by the procedures in  $\frac{40 \text{ CFR part}}{60, \text{ subpart RRR}}$ , the process vent is required to comply only with the provisions specified in paragraphs (d)(8)(ii)(A) through (d)(8)(ii)(D) of this section.

(A) The provisions in both this subpart and in <u>40 CFR part 60, subpart RRR</u> for applicability determination and the associated recordkeeping and reporting;

(B) The provisions in both this subpart and in <u>40 CFR part 60, subpart RRR</u> for process changes and recalculation of the TRE index value and the associated recordkeeping and reporting;

(C) If the provisions of both this subpart and <u>40 CFR part 60</u>, <u>subpart RRR</u> require continuous monitoring of recovery device operating parameters, the process vent is required to comply only with the provisions that are specified in this subpart for continuous monitoring of recovery device operating parameters and the associated testing, reporting, and recordkeeping.

(D) If only the provisions of  $\frac{40 \text{ CFR part 60, subpart RRR}}{40 \text{ CFR part 60, subpart RRR}}$  require continuous monitoring of recovery device operating parameters, the process vent is required to comply only with the provisions that are specified in  $\frac{40 \text{ CFR part 60, subpart}}{40 \text{ CFR part 60, subpart}}$  for continuous monitoring of recovery device operating parameters and the associated testing, reporting, and recordkeeping.

(9) After the compliance dates specified in § 63.100, if an owner or operator of a process vent subject to this subpart that is also subject to the provisions of part 60, subpart RRR, of this chapter elects to control the process vent to the levels required in § 63.113(a)(1) or (2) without calculating the TRE index value for the vent according to the procedures specified in § 63.115(d), then the owner or operator shall comply with the testing, monitoring, reporting, and recordkeeping provisions of this subpart and shall be exempt from the testing, monitoring, reporting, and recordkeeping provisions of part 60, subpart RRR. For each source as defined in § 63.101, on and after July 15, 2027, this paragraph no longer applies.

(10) As an alternative to the requirements of paragraphs (d)(2), (d)(3), (d)(5), (d)(6), (d)(8), and/or (d)(9) of this section as applicable, if a chemical manufacturing process unit has equipment subject to the provisions of this subpart and equipment subject to the provisions of  $\frac{40 \text{ CFR part } 60}{40 \text{ cFR part } 60}$ , subpart III, NNN, or RRR, the owner or operator may elect to apply this subpart to all such equipment in the chemical manufacturing process unit. If the owner or operator elects this method of compliance, all total organic compounds minus methane and ethane, in such equipment shall be considered for purposes of applicability and compliance with this subpart, as if they were organic hazardous air pollutants. Compliance with the provisions of this subpart, in the manner described in this paragraph, shall be deemed to constitute compliance with  $\frac{40 \text{ CFR part } 60}{40 \text{ cFR part } 60}$ , subpart III, NNN, or RRR, as applicable.

(e) Overlap with other regulations for wastewater.

(1) Except as specified in <u>paragraph (j)</u> of this section, after the compliance dates specified in <u>§ 63.100</u>, the owner or operator of a Group 1 or Group 2 wastewater stream that is also subject to the provisions of part 61, subpart FF, of this chapter is required to comply with the provisions of both this subpart and part 61, subpart FF. Alternatively, the owner or operator may elect to comply with the provisions of <u>paragraphs (e)(1)(i)</u> and <u>(ii)</u> of this section, which shall constitute compliance with the provisions of part 61, subpart FF.

(i) Comply with the provisions of this subpart; and

(ii) For any Group 2 wastewater stream or organic stream whose benzene emissions are subject to control through the use of one or more treatment processes or waste management units under the provisions of <u>40 CFR part 61</u>, <u>subpart FF</u> on or after December 31, 1992, comply with the requirements of this subpart for Group 1 wastewater streams.

(2) After the compliance dates specified in § 63.100 of subpart F of this part, the owner or operator of any Group 1 or Group 2 wastewater stream that is also subject to provisions in <u>40 CFR parts 260</u> through <u>272</u> shall comply with the requirements of either paragraph (e)(2)(i) or (e)(2)(ii) of this section.

(i) For each Group 1 or Group 2 wastewater stream, the owner or operator shall comply with the more stringent control requirements (e.g., waste management units, numerical treatment standards, etc.) and the more stringent testing, monitoring, recordkeeping, and reporting requirements that overlap between the provisions of this subpart and the provisions of <u>40 CFR</u> parts 260 through <u>272</u>. The owner or operator shall keep a record of the information used to determine which requirements were the most stringent and shall submit this information if requested by the Administrator; or

(ii) The owner or operator shall submit, no later than four months before the applicable compliance date specified in  $\S$  <u>63.100</u> of <u>subpart F of this part</u>, a request for a case-by-case determination of requirements. The request shall include the information specified in <u>paragraphs (e)(2)(ii)(A)</u> and <u>(e)(2)(ii)(B)</u> of this section.

(A) Identification of the wastewater streams that are subject to this subpart and to provisions in  $\frac{40 \text{ CFR parts}}{260}$  through  $\frac{272}{272}$ , determination of the Group 1/Group 2 status of those streams, determination of whether or not those streams are listed or exhibit a characteristic as specified in  $\frac{40 \text{ CFR part } 261}{40 \text{ CFR part } 261}$ , and determination of whether the waste management unit is subject to permitting under  $\frac{40 \text{ CFR part } 270}{270}$ .

(B) Identification of the specific control requirements (e.g., waste management units, numerical treatment standards, etc.) and testing, monitoring, recordkeeping, and reporting requirements that overlap between the provisions of this subpart and the provisions of <u>40 CFR parts 260</u> through <u>272</u>.

# (f) Overlap with the Vinyl Chloride NESHAP.

(1) After the compliance dates specified in § 63.100 of subpart F of this part, the owner or operator of any Group 1 process vent that is also subject to the provisions of 40 CFR part 61, subpart F shall comply only with the provisions of this subpart.

(2) Except as specified in <u>paragraph (j)</u> of this section, after the compliance dates specified in <u>§ 63.100</u>, the owner or operator of any Group 2 process vent that is also subject to the provisions of part 61, subpart F, of this chapter shall comply with the provisions specified in either <u>paragraph (f)(2)(i)</u> or <u>(ii)</u> of this section.

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(i) If the process vent is already controlled by a combustion device meeting the requirements of <u>40 CFR part 61</u>, <u>subpart</u> <u>F</u>, <u>then</u> the owner or operator shall comply with either the associated testing, monitoring, reporting, and recordkeeping provisions for Group 1 process vents in this subpart or the testing, monitoring, reporting, and recordkeeping provisions of <u>40</u> <u>CFR part 61</u>, <u>subpart F</u>. The owner or operator shall indicate this decision in either the Notification of Compliance Status specified in § 63.152(b) of this subpart or in an operating permit application or amendment.

(ii) If the process vent is not already controlled by a combustion device, then the owner or operator shall comply with the provisions of both this subpart and 40 CFR part 61, subpart F.

(3) After the compliance dates specified in § 63.100, if an owner or operator of a process vent subject to this subpart that is also subject to the provisions of part 61, subpart F, of this chapter elects to control the process vent to the levels required in § 63.113(a)(1) or (2) without calculating the TRE index value for the vent according to the procedures specified in § 63.115(d), then the owner or operator shall comply with the testing, monitoring, reporting, and recordkeeping provisions of this subpart F. For each source as defined in § 63.101, on and after July 15, 2027, this paragraph no longer applies.

(4) Except as specified in <u>paragraph (j)</u> of this section, after the compliance dates specified in <u>§ 63.100</u>, the owner or operator of a Group 1 or Group 2 wastewater stream that is also subject to the provisions of <u>40 CFR part 61</u>, <u>subpart F</u> shall comply with the provisions of either <u>paragraph (f)(4)(i)</u> or <u>(ii)</u> of this section.

(i) The owner or operator shall comply with the provisions of both this subpart and <u>40 CFR part 61, subpart F</u> or

(ii) The owner or operator may submit, no later than four months before the applicable compliance date specified in § <u>63.100</u> of <u>subpart F of this part</u>, information demonstrating how compliance with <u>40 CFR Part 61</u>, <u>subpart F</u>, will also ensure compliance with this subpart. The information shall include a description of the testing, monitoring, reporting, and recordkeeping that will be performed.

(g) *Rules stayed for reconsideration*. Notwithstanding any other provision of this subpart, the effectiveness of subpart G is stayed from October 24, 1994, to April 24, 1995, only as applied to those sources for which the owner or operator makes a representation in writing to the Administrator that the resolution of the area source definition issues could have an effect on the compliance status of the source with respect to subpart G.

(h) Overlap with other regulations for monitoring, recordkeeping, or reporting with respect to combustion devices, recovery devices, or recapture devices.

(1) Except as specified in paragraph (h)(2) of this section, after the compliance dates specified in § 63.100, if any combustion device, recovery device, or recapture device subject to this subpart is also subject to monitoring, recordkeeping, and reporting requirements in part 264, subpart AA or CC, of this chapter or is subject to monitoring and recordkeeping requirements in part 265, subpart AA or CC, of this chapter and the owner or operator complies with the periodic reporting requirements under 40 CFR part 264, subpart AA or CC that would apply to the device if the facility had final-permitted status, the owner or operator may elect to comply either with the monitoring, recordkeeping, and reporting requirements of this subpart, or with the monitoring, recordkeeping, and reporting requirements in parts 264 and/or 265, as described in this paragraph, which shall constitute compliance with the monitoring, recordkeeping, and reporting requirements of this subpart. The owner or operator shall identify which option has been selected in the Notification of Compliance Status required by § 63.152(b).

(2) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10) of subpart F of this part, paragraph (h)(1) of this section no longer applies.

(i) Alternative means of compliance — For each source as defined in  $\S$  63.101, on and after July 15, 2027, this paragraph (i) no longer applies.

(i) For Group 1 and Group 2 process vents, <u>40 CFR part 65</u>, <u>subpart D</u>, satisfies the requirements of <u>§§</u> <u>63.102</u>, <u>63.103</u>, <u>63.112</u> through <u>63.118</u>, <u>63.148</u>, <u>63.151</u>, and <u>63.152</u>.

(ii) For Group 1 storage vessels, <u>40 CFR part 65, subpart C</u>, satisfies the requirements of <u>§§</u> <u>63.102</u>, <u>63.103</u>, <u>63.112</u>, <u>63.119</u> through <u>63.123</u>, <u>63.148</u>, <u>63.151</u>, and <u>63.152</u>.

(iii) For Group 1 transfer racks, <u>40 CFR part 65, subpart E</u>, satisfies the requirements of <u>§§</u> <u>63.102</u>, <u>63.103</u>, <u>63.112</u>, <u>63.126</u> through <u>63.130</u>, <u>63.148</u>, <u>63.151</u>, and <u>63.152</u>.

(iv) For equipment, comply with  $\S 63.160(g)$ .

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(2) *Part 63, subpart A.* Owners or operators who choose to comply with <u>40 CFR part 65</u> must also comply with the applicable general provisions of this part 63 listed in table 1A of this subpart. All sections and paragraphs of <u>subpart A of this</u> <u>part</u> that are not mentioned in table 1A of this subpart do not apply to owners or operators who choose to comply with <u>40</u> <u>CFR part 65</u>, except that provisions required to be met prior to implementing <u>40 CFR part 65</u> still apply. Owners and operators who choose to comply with a subpart of <u>40 CFR part 65</u> must comply with <u>40 CFR part 65</u>, subpart <u>A</u>.

# (j) Overlap with other regulations for flares.

(1) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), flares used as a control device to comply with the overlap provisions in either paragraph (b)(3), (c)(2)(i), (e)(1), (f)(2)(i), (f)(2)(ii), or (f)(4)(i) or (ii) of this section must comply with the provisions specified in § 63.108 and are no longer subject to any flare related provisions of part 61, subparts F, Y, BB, and FF, of this chapter or § 60.18 of this chapter.

(2) Owners and operators of flares that are subject to the flare related requirements of this subpart and flare related requirements of any other regulation in <u>part 60, 61</u>, or <u>63 of this chapter</u>, may elect to comply with the requirements in § <u>63.108</u> in lieu of all flare related requirements in any other regulation in part 60, 61, or 63.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>59 FR 53360</u>, Oct. 24, 1994; <u>60 FR 5321</u>, Jan. 27, 1995; <u>61 FR 64575</u>, Dec. 5, 1996; <u>62 FR 2742</u>, Jan. 17, 1997; <u>65 FR 78284</u>, Dec. 14, 2000; <u>66 FR 6929</u>, Jan. 22, 2001; <u>89 FR 43175</u>, May 16, 2024]

# § 63.111 Definitions.

All terms used in this subpart shall have the meaning given them in the Act and in subpart F of this part.

# [<u>89 FR 43177</u>, May 16, 2024]

# § 63.112 Emission standard.

(a) The owner or operator of an existing source subject to the requirements of this subpart shall control emissions of organic HAP's to the level represented by the following equation:

 $E_A = 0.02\Sigma \ EPV_1 + \Sigma \ EPV_2 + 0.05\Sigma \ ES_1 + \Sigma \ ES_2 + 0.02\Sigma \ ETR_1 + \Sigma \ ETR_2 + \Sigma \ EWW_{1C} + \Sigma \ EWW_2$ 

where:

 $E_A$  = Emission rate, megagrams per year, allowed for the source.

 $0.02\Sigma$  EPV<sub>1</sub> = Sum of the residual emissions, megagrams per year, from all Group 1 process vents, as defined in § 63.111 of this subpart.

 $\Sigma$  EPV<sub>2</sub> = Sum of the emissions, megagrams per year, from all Group 2 process vents as defined in <u>§ 63.111 of this subpart</u>.

 $0.05\Sigma \text{ ES}_1 = \text{Sum of the residual emissions, megagrams per year, from all Group 1 storage vessels, as defined in § 63.111 of this subpart.$ 

 $\Sigma ES_2$  = Sum of the emissions, megagrams per year, from all Group 2 storage vessels, as defined in § 63.111 of this subpart.

 $0.02\Sigma$  ETR<sub>1</sub> = Sum of the residual emissions, megagrams per year, from all Group 1 transfer racks, as defined in <u>§ 63.111 of this subpart</u>.

 $\Sigma$  ETR<sub>2</sub> = Sum of the emissions, megagrams per year, from all Group 2 transfer racks, as defined in <u>§ 63.111 of this subpart</u>.

 $\Sigma \text{ EWW}_{1\text{C}}$  = Sum of the residual emissions from all Group 1 wastewater streams, as defined in <u>§ 63.111 of this subpart</u>. This term is calculated for each Group 1 stream according to the equation for EWW<sub>1C</sub> in <u>§ 63.150(g)(5)(i) of this subpart</u>.

 $\Sigma$  EWW<sub>2</sub> = Sum of emissions from all Group 2 wastewater streams, as defined in § 63.111 of this subpart.

The emissions level represented by this equation is dependent on the collection of emission points in the source. The level is not fixed and can change as the emissions from each emission point change or as the number of emission points in the source changes.

(b) The owner or operator of a new source subject to the requirements of this subpart shall control emissions of organic HAP's to the level represented by the equation in <u>paragraph (a)</u> of this section.

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(c) The owner or operator of an existing source shall demonstrate compliance with the emission standard in <u>paragraph (a)</u> of this section by following the procedures specified in <u>paragraph (e)</u> of this section for all emission points, or by following the emissions averaging compliance approach specified in <u>paragraph (f)</u> of this section for some emission points and the procedures specified in <u>paragraph (e)</u> of this section for all other emission points within the source.

(d) The owner or operator of a new source shall demonstrate compliance with the emission standard in <u>paragraph (b)</u> of this section only by following the procedures in <u>paragraph (e)</u> of this section. The owner or operator of a new source may not use the emissions averaging compliance approach.

(e) The owner or operator of an existing or new source may comply with the process vent provisions in  $\S$ <u>63.113</u> through <u>63.118 of this subpart</u>, the storage vessel provisions in <u>§§ 63.129</u> through <u>63.123 of this subpart</u>, the transfer operation provisions in <u>§§ 63.126</u> through <u>63.130 of this subpart</u>, the wastewater provisions in <u>§§ 63.131</u> through <u>63.147 of</u> <u>this subpart</u>, the leak inspection provisions in <u>§ 63.148</u>, and the provisions in <u>§ 63.149 of this subpart</u>.

(1) The owner or operator using this compliance approach shall also comply with the requirements of  $\S$  63.151 and  $\S$  63.152 of this subpart, as applicable.

(2) The owner or operator using this compliance approach is not required to calculate the annual emission rate specified in <u>paragraph (a)</u> of this section.

(3) When emissions of different kinds (e.g., emissions from process vents, transfer operations, storage vessels, process wastewater, and/or in-process equipment subject to  $\frac{63.149}{5}$  of this subpart) are combined, and at least one of the emission streams would be classified as Group 1 in the absence of combination with other emission streams, the owner or operator shall comply with the requirements of either paragraph (e)(3)(i) or paragraph (e)(3)(ii) of this section.

(i) Comply with the applicable requirements of this subpart for each kind of emissions in the stream (e.g., the requirements in <u>§§ 63.113</u> through <u>63.118 of this subpart</u> G for process vents, and the requirements of <u>§§ 63.126</u> through <u>63.130</u> for transfer operations); or

(ii) Comply with the first set of requirements identified in <u>paragraphs (e)(3)(ii)(A)</u> through (<u>e)(3)(ii)(E)</u> of this section which applies to any individual emission stream that is included in the combined stream, where either that emission stream would be classified as Group 1 in the absence of combination with other emission streams, or the owner chooses to consider that emission stream to be Group 1 for purposes of this paragraph. Compliance with the first applicable set of requirements identified in <u>paragraphs (e)(3)(ii)(A)</u> through (<u>e)(3)(ii)(E)</u> of this section constitutes compliance with all other requirements in <u>paragraphs (e)(3)(ii)(A)</u> through (<u>e)(3)(ii)(E)</u> of this section applicable to other types of emissions in the combined stream.

(A) The requirements of this subpart for Group 1 process vents, including applicable monitoring, recordkeeping, and reporting;

(B) The requirements of this subpart for Group 1 transfer racks, including applicable monitoring, recordkeeping, and reporting;

(C) The requirements of  $\S$  <u>63.119(e)</u> for control of emissions from Group 1 storage vessels, including monitoring, recordkeeping, and reporting;

(D) The requirements of  $\S$  63.139 for control devices used to control emissions from waste management units, including applicable monitoring, recordkeeping, and reporting; or

(E) The requirements of  $\S$  <u>63.139</u> for closed vent systems for control of emissions from in-process equipment subject to  $\S$  <u>63.149</u>, including applicable monitoring, recordkeeping, and reporting.

(f) The owner or operator of an existing source may elect to control some of the emission points within the source to different levels than specified under <u>§§ 63.113</u> through <u>63.148 of this subpart</u> by using an emissions averaging compliance approach as long as the overall emissions for the source do not exceed the emission level specified in <u>paragraph (a)</u> of this section. The owner or operator using emissions averaging must meet the requirements in <u>paragraphs (f)(1)</u> and <u>(f)(2)</u> of this section.

(1) Calculate emission debits and credits for those emission points involved in the emissions average as specified in  $\S$  63.150 of this subpart; and

(2) Comply with the requirements of  $\S 63.151$  and  $\S 63.152$  of this subpart, as applicable.

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(g) A State may restrict the owner or operator of an existing source to using only the procedures in <u>paragraph (e)</u> of this section to comply with the emission standard in <u>paragraph (a)</u> of this section.

(h) Where the provisions of this subpart require a performance test, waiver of that requirement shall be addressed only as provided in  $\S 63.103(b)(5)$  of subpart F of this part.

[59 FR 19468, Apr. 22, 1994, as amended at 62 FR 2744, Jan. 17, 1997]

# § 63.113 Process vent provisions—reference control technology.

(a) The owner or operator of a Group 1 process vent as defined in this subpart shall comply with the requirements of paragraph (a)(1), (2), (3), or (4) of this section, and paragraph (a)(5) of this section. The owner or operator who transfers a gas stream that has the characteristics specified in § 63.107(b) through (h) or meets the criteria specified in § 63.107(i) to an off-site location or an on-site location not owned or operated by the owner or operator of the source for disposal shall comply with the requirements of paragraph (i) of this section.

(1) Reduce emissions of organic HAP using a flare.

(i) Except as specified in  $\S 63.108(a)$ , the flare shall comply with the requirements of  $\S 63.11(b)$ .

(ii) Halogenated vent streams, as defined in <u>§ 63.111</u>, shall not be vented to a flare.

(2) Reduce emissions of total organic hazardous air pollutants by 98 weight-percent or to a concentration of 20 parts per million by volume. For combustion devices, the emission reduction or concentration shall be calculated on a dry basis, corrected to 3-percent oxygen, and compliance can be determined by measuring either organic hazardous air pollutants or total organic carbon using the procedures in  $\S$  63.116.

(i) Compliance with <u>paragraph (a)(2)</u> of this section may be achieved by using any combination of combustion, recovery, and/or recapture devices, except that a recovery device may not be used to comply with <u>paragraph (a)(2)</u> of this section by reducing emissions of total organic hazardous air pollutants by 98 weight-percent, except as provided in <u>paragraph (a)(2)(ii)</u> of this section.

(ii) An owner or operator may use a recovery device, alone or in combination with one or more combustion or recapture devices, to reduce emissions of total organic hazardous air pollutants by 98 weight-percent if all the conditions of <u>paragraphs</u> (a)(2)(ii)(A) through (a)(2)(ii)(D) of this section are met.

(A) The recovery device (and any combustion device or recapture device which operates in combination with the recovery device to reduce emissions of total organic hazardous air pollutants by 98 weight-percent) was installed before the date of proposal of the subpart of this part 63 that makes this subpart G applicable to process vents in the chemical manufacturing process unit.

(B) The recovery device that will be used to reduce emissions of total organic hazardous air pollutants by 98 weight-percent is the last recovery device before emission to the atmosphere.

(C) The recovery device, alone or in combination with one or more combustion or recapture devices, is capable of reducing emissions of total organic hazardous air pollutants by 98 weight-percent, but is not capable of reliably reducing emissions of total organic hazardous air pollutants to a concentration of 20 parts per million by volume.

(D) If the owner or operator disposed of the recovered material, the recovery device would comply with the requirements of this subpart for recapture devices.

(3) Except as specified in <u>paragraph (a)(4)</u> of this section, achieve and maintain a TRE index value greater than 1.0 at the outlet of the final recovery device, or prior to release of the vent stream to the atmosphere if no recovery device is present. If the TRE index value is greater than 1.0, the process vent shall comply with the provisions for a Group 2 process vent specified in either <u>paragraph (d)</u> or (e) of this section, whichever is applicable.

(4) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the provisions specified in paragraphs (a)(4)(i) through (xv) of this section no longer apply. Instead, an owner or operator of a Group 1 process vent as defined in § 63.101 must comply with the requirements of paragraph (a)(1) or (2) of this section; and an owner or operator of a Group 2 process vent as defined in § 63.101 must comply with the requirements of paragraph (a)(1) or (2) of this section; and an owner or operator of a Group 2 process vent as defined in § 63.101 must comply with the requirements of paragraph (a)(1) or (2) of this section; and (f) or (g) of this section.

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- (i) <u>Paragraphs (a)(3)</u>, (d), and (e) of this section;
- (ii) Section 63.114(b) and (c)(2);
- (iii) Section 63.115(d), except (d)(2)(v);

(iv) The following phrases in  $\S$  63.115(e): "TRE index value", "changes that are within the range on which the original TRE calculation was based", and "the recalculated TRE index value is less than or equal to 1.0, or less than or equal to 4.0 but greater than 1.0";

(v) The following phrases in  $\S$  63.115(f): "TRE index value", and "regardless of the TRE index value determined at the location specified in  $\S$  63.115(a)";

(vi) The last two sentences in  $\S$  <u>63.115(f)(2)</u>: "If the combined vent stream is a Group 2 process vent as determined by the previous sentence, but one or more of the HON streams, or combinations of HON streams, has a TRE index value greater than 1 but less than or equal to 4, the combined vent stream is a process vent with a TRE index value greater than 1 but less than or equal to 4. In this case, the owner or operator shall monitor the combined vent stream as required by  $\S$  <u>63.114(b)</u>.";

(vii) The phrase in § 63.117(a): "or the provisions for Group 2 process vents with a TRE index value greater than 1.0 but less than or equal to 4.0 in § 63.113(d)";

(viii) The phrase in <u>§ 63.117(a)(3)</u>: "TRE determinations or";

- (ix) Section 63.117(a)(7) and (b);
- (x) Section 63.118(b), (c), (d)(3), (e)(3), (h), (i), (j), and (k)(4);
- (xi) The following phrase in  $\S 63.118(g)(2)$ : "and TRE index value";
- (xii) The last sentence in  $\S 63.150(g)(2)(iii)(B)(2)$ ;
- (xiii) The phrase in <u>§ 63.150(m)(2)(i)</u>: "and TRE index value";
- (xiv) The last sentence in  $\S 63.151(d)(6)(i)$ ; and
- (xv) Table 4 to subpart G of this part.

(5) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), an owner or operator of a Group 1 process vent as defined in § 63.101 that contains chlorine, hydrogen chloride, or any other chlorinated compound must reduce emissions of dioxins and furans (toxic equivalency basis) to a concentration of 0.054 nanograms per standard cubic meter on a dry basis corrected to 3 percent oxygen.

(b) If a boiler or process heater is used to comply with the percent reduction requirement or concentration limit specified in paragraph (a)(2) of this section, then the vent stream shall be introduced into the flame zone of such a device.

(c) Halogenated vent streams from Group 1 process vents that are combusted shall be controlled according to <u>paragraph</u> (c)(1) or (2) of this section.

(1) If a combustion device is used to comply with <u>paragraph (a)(2)</u> of this section for a halogenated vent stream, then the gas stream exiting the combustion device shall be conveyed to a halogen reduction device, such as a scrubber, before it is discharged to the atmosphere.

(i) Except as provided in <u>paragraph (c)(1)(ii)</u> of this section, the halogen reduction device shall reduce overall emissions of hydrogen halides and halogens, as defined in  $\S$  63.111 of this subpart, by 99 percent or shall reduce the outlet mass of total hydrogen halides and halogens to less than 0.45 kilogram per hour.

(ii) If a scrubber or other halogen reduction device was installed prior to December 31, 1992, the device shall reduce overall emissions of hydrogen halides and halogens, as defined in § 63.111, by 95 percent or shall reduce the outlet mass of total hydrogen halides and halogens to less than 0.45 kilograms per hour.

(2) A halogen reduction device, such as a scrubber or other technique, may be used to reduce the vent stream halogen atom mass emission rate to less than 0.45 kilogram per hour prior to any combustion control device, and thus make the vent stream nonhalogenated; the vent stream must comply with the requirements of <u>paragraph (a)(1)</u> or (2) of this section.

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(d) Except as specified in paragraph (a)(4) of this section, the owner or operator of a Group 2 process vent having a flow rate greater than or equal to 0.005 standard cubic meter per minute, a HAP concentration greater than or equal to 50 parts per million by volume, and a TRE index value greater than 1.0 but less than or equal to 4.0 shall maintain a TRE index value greater than 1.0 and shall comply with the monitoring of recovery device parameters in § 63.114(b) or (c), the TRE index calculations of § 63.115 of this subpart, and the applicable reporting and recordscepting provisions of §§ 63.117 and 63.118. Such owner or operator is not subject to any other provisions of §§ 63.114 through 63.118.

(e) Except as specified in paragraph (a)(4) of this section, the owner or operator of a Group 2 process vent with a TRE index value greater than 4.0 shall maintain a TRE index value greater than 4.0, comply with the provisions for calculation of a TRE index value in  $\frac{63.115}{2}$  and the reporting and recordkeeping provisions in  $\frac{8}{5}$  63.117(b) and 63.118(c) and (h), and is not subject to monitoring or any other provisions of  $\frac{8}{5}$  63.114 through 63.118.

(f) Except as specified in paragraph (1) of this section, the owner or operator of a Group 2 process vent with a flow rate less than 0.005 standard cubic meter per minute shall maintain a flow rate less than 0.005 standard cubic meter per minute; comply with the Group determination procedures in § 63.115 (a), (b), and (c); and the reporting and recordkeeping requirements in §§ 63.117(c), 63.118(d), and 63.118(i); and is not subject to monitoring or any other provisions of §§ 63.114 through 63.118.

(g) Except as specified in <u>paragraph (1)</u> of this section, the owner or operator of a Group 2 process vent with a total organic HAP concentration less than 50 parts per million by volume shall maintain a total organic HAP concentration less than 50 parts per million by volume; comply with the Group determination procedures in  $\frac{63.115(a)}{(c)}$ , and (c); the reporting and recordkeeping requirements in  $\frac{88}{63.117(d)}$  and  $\frac{63.118(e)}{63.118(e)}$  and (j); and is not subject to monitoring or any other provisions of  $\frac{88}{63.118}$ .

(h) The owner or operator of a process vent complying with <u>paragraph (a)(1)</u> or (2) of this section is not required to perform the group determination described in  $\S$  63.115.

(i) Off-site control or on-site control not owned or operated by the source. This paragraph (i) applies to gas streams that have the characteristics specified in § 63.107(b) through (h) or meet the criteria specified in § 63.107(i); that are transferred for disposal to an on-site control device (or other compliance equipment) not owned or operated by the owner or operator of the source generating the gas stream, or to an off-site control device or other compliance equipment; and that have the characteristics (*e.g.*, flow rate, total organic HAP concentration, or TRE index value as applicable) of a Group 1 process vent, determined at the point of transfer.

(i) Comply with the provisions specified in  $\S$  63.114(d) for each gas stream prior to transfer.

(ii) Notify the transferee that the gas stream contains organic hazardous air pollutants that are to be treated in accordance with the provisions of this subpart. The notice shall be submitted to the transferee initially and whenever there is a change in the required control.

(2) The owner or operator may not transfer the gas stream unless the transferee has submitted to the EPA a written certification that the transferee will manage and treat any gas stream transferred under this paragraph (i) and received from a source subject to the requirements of this subpart in accordance with the requirements of either  $\frac{\&\& 63.113}{\&\& 63.102(b)}$ , or subpart D of this part if alternative emission limitations have been granted the transferor in accordance with those provisions. The certifying entity may revoke the written certification by sending a written statement to EPA and the owner or operator giving at least 90 days notice that the certifying entity is rescinding acceptance of responsibility for compliance with the regulatory provisions listed in this paragraph (i). Upon expiration of the notice period, the owner or operator may not transfer the gas stream to the transferee. Records retained by the transferee shall be retained in accordance with & 63.103(c).

(3) By providing this written certification to EPA, the certifying entity accepts responsibility for compliance with the regulatory provisions listed in <u>paragraph (i)(2)</u> of this section with respect to any transfer covered by the written certification. Failure to abide by any of those provisions with respect to such transfers may result in enforcement action by EPA against the certifying entity in accordance with the enforcement provisions applicable to violations of these provisions by owners or operators of sources.

(4) Written certifications and revocation statements to EPA from the transferees of such gas streams shall be signed by a responsible official of the certifying entity, provide the name and address of the certifying entity, and be sent to the

appropriate EPA Regional Office at the addresses listed in  $\S$  63.13. Such written certifications are not transferable by the transferee.

(j) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(11), if the Group 1 or Group 2 process vent contains ethylene oxide such that it is considered to be in ethylene oxide service, as defined in § 63.101, then the owner or operator must comply with the requirements of paragraphs (j)(1) or (2) of this section in addition to all other applicable requirements specified elsewhere in this section.

(1) Reduce emissions of ethylene oxide by venting emissions through a closed vent system to a flare; or

(2) Reduce emissions of ethylene oxide by venting emissions through a closed vent system to a control device that reduces ethylene oxide by greater than or equal to 99.9 percent by weight, or to a concentration less than 1 ppmv for each process vent or to less than 5 pounds per year for all combined process vents within the process. If a combustion device is used, the ethylene oxide concentration of 1 ppmv must be corrected to 3 percent oxygen.

(k) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), an owner or operator may designate a process vent as a maintenance vent if the vent is only used as a result of startup, shutdown, maintenance, or inspection of equipment where equipment is emptied, depressurized, degassed, or placed into service. The owner or operator must comply with the applicable requirements in <u>paragraphs (k)(1)</u> through (4) of this section for each maintenance vent. Any vent designated as a maintenance vent is only subject to the maintenance vent provisions in this <u>paragraph (k)</u> and the associated reporting and recordkeeping requirements in § 63.118(f)(9) and (m), respectively. The owner or operator does not need to designate a maintenance vent as a Group 1 or Group 2 process vent nor identify maintenance vents in a Notification of Compliance Status report.

(1) Prior to venting to the atmosphere, remove process liquids from the equipment as much as practical and depressurize the equipment to either: A flare meeting the requirements of  $\frac{63.108}{2}$ , as applicable, or using any combination of a non-flare combustion, recovery, and/or recapture device meeting the requirements in <u>paragraph (a)(2)</u> of this section until one of the following conditions, as applicable, is met.

(i) The concentration of the vapor in the equipment served by the maintenance vent is less than 10 percent of its lower explosive limit (LEL) and has an outlet concentration less than or equal to 20 ppmv hydrogen halide and halogen HAP.

(ii) If there is no ability to measure the concentration of the vapor in the equipment based on the design of the equipment, the pressure in the equipment served by the maintenance vent is reduced to 5 pounds per square inch gauge (psig) or less. Upon opening the maintenance vent, active purging of the equipment cannot be used until the concentration of the vapors in the maintenance vent (or inside the equipment if the maintenance is a hatch or similar type of opening) is less than 10 percent of its LEL.

(iii) The equipment served by the maintenance vent contains less than 50 pounds of total volatile organic compounds (VOC).

(iv) If, after applying best practices to isolate and purge equipment served by a maintenance vent, none of the applicable criterion in <u>paragraphs (k)(1)(i)</u> through (iii) of this section can be met prior to installing or removing a blind flange or similar equipment blind, then the pressure in the equipment served by the maintenance vent must be reduced to 2 psig or less before installing or removing the equipment blind. During installation or removal of the equipment blind, active purging of the equipment may be used provided the equipment pressure at the location where purge gas is introduced remains at 2 psig or less.

(2) Except for maintenance vents complying with the alternative in <u>paragraph (k)(1)(iii)</u> of this section, the owner or operator must determine the concentration or, if applicable, equipment pressure using process instrumentation or portable measurement devices and follow procedures for calibration and maintenance according to manufacturer's specifications.

(3) For maintenance vents complying with the alternative in <u>paragraph (k)(1)(iii)</u> of this section, the owner or operator must determine mass of VOC in the equipment served by the maintenance vent based on the equipment size and contents after considering any contents drained or purged from the equipment. Equipment size may be determined from equipment design specifications. Equipment contents may be determined using process knowledge.

(4) In addition to complying with the requirements in paragraphs (k)(1) through (3) of this section, for process vents in ethylene oxide service, subject to the requirements of  $\S$  63.124 that are designated as maintenance vents, owners and operators may not release more than 1.0 tons of ethylene oxide from all maintenance vents combined per any consecutive 12-

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month period. The owner or operator must keep monthly records of the quantity in tons of ethylene oxide released from each maintenance vent and include a description of the method used to estimate this quantity.

(1) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraphs (f) and (g) of this section no longer apply. Instead, the owner or operator of a Group 2 process vent with a total organic HAP mass flow rate less than 1.0 pound per hour shall maintain a total organic HAP mass flow rate less than 1.0 pound per hour; comply with the Group determination procedures in § 63.115(g); and the reporting and recordkeeping requirements in §§ 63.117(g) and 63.118(n); and is not subject to monitoring or any other provisions of §§ 63.114 through 63.118.

# [<u>89 FR 43177</u>, May 16, 2024]

# § 63.114 Process vent provisions—monitoring requirements.

(a) Each owner or operator of a process vent that uses a combustion device to comply with the requirements in  $\S$  <u>63.113(a)(1)</u>, (2), or (5), or that uses a recovery device or recapture device to comply with the requirements in  $\S$  <u>63.113(a)(2)</u>, shall install monitoring equipment specified in <u>paragraph (a)(1), (2), (3), (4), (5)</u>, or (6) of this section, depending on the type of device used. All monitoring equipment shall be installed, calibrated, maintained, and operated according to manufacturer's specifications or other written procedures that provide adequate assurance that the equipment would reasonably be expected to monitor accurately.

(1) Where an incinerator is used, a temperature monitoring device equipped with a continuous recorder is required.

(i) Where an incinerator other than a catalytic incinerator is used, a temperature monitoring device shall be installed in the firebox or in the ductwork immediately downstream of the firebox in a position before any substantial heat exchange occurs.

(ii) Where a catalytic incinerator is used, temperature monitoring devices shall be installed in the gas stream immediately before and after the catalyst bed.

(2) Where a flare is used, except as specified in  $\S$  <u>63.108(a)</u>, the following monitoring equipment is required: A device (including but not limited to a thermocouple, ultra-violet beam sensor, or infrared sensor) capable of continuously detecting the presence of a pilot flame.

(3) Where a boiler or process heater of less than 44 megawatts design heat input capacity is used, the following monitoring equipment is required: a temperature monitoring device in the firebox equipped with a continuous recorder. This requirement does not apply to gas streams that are introduced with primary fuel or are used as the primary fuel.

(4) Where a scrubber is used with an incinerator, boiler, or process heater in the case of halogenated vent streams, the following monitoring equipment is required for the scrubber.

(i) A pH monitoring device equipped with a continuous recorder shall be installed to monitor the pH of the scrubber effluent.

(ii) A flow meter equipped with a continuous recorder shall be located at the scrubber influent for liquid flow. Gas flow rate shall be determined using one of the procedures specified in <u>paragraphs (a)(4)(ii)(A)</u> through (C) of this section.

(A) The owner or operator may determine gas flow rate using the design blower capacity, with appropriate adjustments for pressure drop.

(B) If the scrubber is subject to rules in 40 CFR parts 264 through 266 that have required a determination of the liquid to gas (L/G) ratio prior to the applicable compliance date for this subpart specified in § 63.100(k), the owner or operator may determine gas flow rate by the method that had been utilized to comply with those rules. A determination that was conducted prior to the compliance date for this subpart may be utilized to comply with this subpart if it is still representative.

(C) The owner or operator may prepare and implement a gas flow rate determination plan that documents an appropriate method which will be used to determine the gas flow rate. The plan shall require determination of gas flow rate by a method which will at least provide a value for either a representative or the highest gas flow rate anticipated in the scrubber during representative operating conditions other than startups, shutdowns, or malfunctions. The plan shall include a description of the methodology to be followed and an explanation of how the selected methodology will reliably determine the gas flow rate, and a description of the records that will be maintained to document the determination of gas flow rate. The owner or operator shall maintain the plan as specified in  $\S 63.103(c)$ . For each source as defined in  $\S 63.101$ , on and after July 15, 2027, the phrase "other than startups, shutdowns, or malfunctions" in this paragraph no longer applies.

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(5) Where a recovery device or recapture device is used to comply with the requirements of  $\frac{63.113(a)(2)}{(ii)}$ , or  $\frac{(5)}{(ii)}$ , the owner or operator shall utilize the appropriate monitoring device identified in <u>paragraph (a)(5)(i)</u>, (ii), (iii), (iv), or (v) of this section. All monitoring equipment shall be installed, calibrated, and maintained according to the manufacturer's specifications or other written procedures that provide adequate assurance that the equipment would reasonably be expected to monitor accurately.

(i) Install either an organic monitoring device equipped with a continuous recorder;

(ii) Where an absorber is the final recovery device in the recovery system, a scrubbing liquid temperature monitoring device and a specific gravity monitoring device, each equipped with a continuous recorder shall be used;

(iii) Where a condenser is the final recovery device in the recovery system, a condenser exit (product side) temperature monitoring device equipped with a continuous recorder shall be used;

(iv) Except as specified in <u>paragraph (a)(5)(v)</u> of this section, where a carbon adsorber is the final recovery device in the recovery system, an integrating regeneration stream flow monitoring device having an accuracy of  $\pm 10$  percent or better, capable of recording the total regeneration stream mass or volumetric flow for each regeneration cycle; and a carbon bed temperature monitoring device, capable of recording the carbon bed temperature after each regeneration and within 15 minutes of completing any cooling cycle shall be used.

(v) Beginning no later than the compliance dates specified in  $\S$  <u>63.100(k)(10)</u>, if the owner or operator vents emissions through a closed vent system to an adsorber(s) that cannot be regenerated or a regenerative adsorber(s) that is regenerated offsite, then the owner or operator must install a system of two or more adsorber units in series and comply with the requirements specified in paragraphs (a)(5)(v)(A) through (C) of this section.

(A) Conduct an initial performance test or design evaluation of the adsorber and establish the breakthrough limit and adsorber bed life.

(B) Monitor the HAP or total organic compound (TOC) concentration through a sample port at the outlet of the first adsorber bed in series according to the schedule in paragraph (a)(5)(v)(C)(2) of this section. The owner or operator must measure the concentration of HAP or TOC using either a portable analyzer, in accordance with Method 21 of appendix A-7 to part 60 of this chapter using methane, propane, isobutylene, or the primary HAP being controlled as the calibration gas.

(C) Comply with <u>paragraph (a)(5)(v)(C)(1)</u> of this section and comply with the monitoring frequency according to <u>paragraph (a)(5)(v)(C)(2)</u> of this section.

(1) The first adsorber in series must be replaced immediately when breakthrough, as defined in  $\frac{63.101}{100}$ , is detected between the first and second adsorber. The original second adsorber (or a fresh canister) will become the new first adsorber and a fresh adsorber will become the second adsorber. For purposes of this paragraph, "immediately" means within 8 hours of the detection of a breakthrough for adsorbers of 55 gallons or less, and within 24 hours of the detection of a breakthrough for adsorber or operator must monitor at the outlet of the first adsorber within 3 days of replacement to confirm it is performing properly.

(2) Based on the adsorber bed life established according to paragraph (a)(5)(v)(A) of this section and the date the adsorbent was last replaced, conduct monitoring to detect breakthrough at least monthly if the adsorbent has more than 2 months of life remaining, at least weekly if the adsorbent has between 2 months and 2 weeks of life remaining, and at least daily if the adsorbent has 2 weeks or less of life remaining.

(6) Where sorbent injection is used, the following monitoring equipment is required for the sorbent injection system:

(i) A sorbent injection rate monitoring device (*e.g.*, weigh belt, weigh hopper, hopper flow measurement device) installed in a position that provides a representative measurement equipped with a continuous recorder to monitor the sorbent injection rate; and

(ii) A flow measurement device equipped with a continuous recorder to monitor the carrier gas flow rate.

(b) Except as specified in  $\S$  63.113(a)(4), each owner or operator of a process vent with a TRE index value greater than 1.0 as specified under  $\S$  63.113(a)(3) or (d) that uses one or more recovery devices shall install either an organic monitoring device equipped with a continuous recorder or the monitoring equipment specified in paragraph (b)(1), (2), or (3) of this section, depending on the type of recovery device used. All monitoring equipment shall be installed, calibrated, and maintained

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according to the manufacturer's specifications or other written procedures that provide adequate assurance that the equipment would reasonably be expected to monitor accurately. Monitoring is not required for process vents with TRE index values greater than 4.0 as specified in  $\S$  63.113(e).

(1) Where an absorber is the final recovery device in the recovery system, a scrubbing liquid temperature monitoring device and a specific gravity monitoring device, each equipped with a continuous recorder shall be used;

(2) Where a condenser is the final recovery device in the recovery system, a condenser exit (product side) temperature monitoring device equipped with a continuous recorder shall be used;

(3) Where a carbon adsorber is the final recovery device in the recovery system, an integrating regeneration stream flow monitoring device having an accuracy of  $\pm 10$  percent or better, capable of recording the total regeneration stream mass or volumetric flow for each regeneration cycle; and a carbon bed temperature monitoring device, capable of recording the carbon bed temperature after each regeneration and within 15 minutes of completing any cooling cycle shall be used.

(c) An owner or operator of a process vent may request approval to monitor parameters other than those listed in <u>paragraph</u> (a) or (b) of this section. The request shall be submitted according to the procedures specified in § 63.151(f) or § 63.152(e) of this subpart. Approval shall be requested if the owner or operator:

(1) Uses a combustion device other than an incinerator, boiler, process heater, or flare; or

(2) Except as specified in  $\frac{63.113(a)(4)}{b}$ , maintains a TRE greater than 1.0 but less than or equal to 4.0 without a recovery device or with a recovery device other than the recovery devices listed in <u>paragraphs (a)</u> and <u>(b)</u> of this section; or

(3) Uses one of the combustion or recovery or recapture devices listed in <u>paragraphs (a)</u> and (b) of this section, but seeks to monitor a parameter other than those specified in <u>paragraphs (a)</u> and (b) of this section.

(d) The owner or operator of a process vent shall comply with <u>paragraphs</u> (d)(1) or (2) and (d)(3) of this section for any bypass line between the origin of the gas stream (*i.e.*, at an air oxidation reactor, distillation unit, or reactor as identified in § 63.107(b)) and the point where the gas stream reaches the process vent, as described in § 63.107, that could divert the gas stream directly to the atmosphere. Except as specified in <u>paragraph</u> (d)(3)(ii) of this section, equipment such as low leg drains, high point bleeds, analyzer vents, open-ended valves or lines, and pressure relief valves needed for safety purposes are not subject to this <u>paragraph</u> (d).

(1) Properly install, maintain, and operate a flow indicator that takes a reading at least once every 15 minutes. Records shall be generated as specified in  $\S$  63.118(a)(3). The flow indicator shall be installed at the entrance to any bypass line that could divert the gas stream to the atmosphere; or

(2) Secure the bypass line valve in the non-diverting position with a car-seal or a lock-and-key type configuration. A visual inspection of the seal or closure mechanism shall be performed at least once every month to ensure that the valve is maintained in the non-diverting position and the gas stream is not diverted through the bypass line

(3) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10):

(i) The use of a bypass line at any time on a closed vent system to divert emissions (subject to the emission standards in  $\frac{5}{63.112}$ ) to the atmosphere or to a control device not meeting the requirements specified in this subpart is an emissions standards violation.

(ii) The last sentence in <u>paragraph (d)</u> of this section no longer applies. Instead, the exemptions specified in <u>paragraphs</u>  $(\underline{d})(\underline{3})(\underline{i})(\underline{A})$  and  $(\underline{B})$  of this section apply.

(A) Except for pressure relief devices subject to  $\S 63.165(e)(4)$  of subpart H of this part, equipment such as low leg drains and equipment subject to the requirements of subpart H of this part are not subject to this paragraph (d) of this section.

(B) Open-ended values or lines that use a cap, blind flange, plug, or second value and follow the requirements specified in  $\S$  <u>60.482-6(a)(2)</u>, (b), and (c) of this chapter or follow requirements codified in another regulation that are the same as  $\S$  <u>60.482-6(a)(2)</u>, (b), and (c) are not subject to this paragraph (d).

(e) The owner or operator shall establish a range that indicates proper operation of the control or recovery device for each parameter monitored under <u>paragraphs (a)</u>, (b), and (c) of this section based on the results of the most recent performance test. In order to establish the range, the information required in  $\S 63.152(b)$  shall be submitted in the Notification of Compliance Status or the operating permit application or amendment. The range may be based upon a prior performance test

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conducted for determining compliance with a regulation promulgated by the EPA, and the owner or operator is not required to conduct an initial performance test under § 63.116, if the prior performance test was conducted using the same methods specified in § 63.116 and either no process changes have been made since the test, or the owner or operator can demonstrate that the results of the performance test, with or without adjustments, reliably demonstrate compliance despite process changes. Subsequent performance tests must be conducted according to § 63.103(b)(1).

[<u>89 FR 43179</u>, May 16, 2024]

# § 63.115 Process vent provisions—methods and procedures for process vent group determination.

(a) For purposes of determining vent stream flow rate, total organic HAP or total organic carbon concentration or TRE index value as applicable, as specified under <u>paragraph (b)</u>, (c), or (d) of this section, the sampling site shall be after the last recovery device (if any recovery devices are present) but prior to the inlet of any control device that is present and prior to release to the atmosphere.

(1) Method 1 or 1A of <u>40 CFR part 60, appendix A</u>, as appropriate, shall be used for selection of the sampling site.

(2) No traverse site selection method is needed for vents smaller than 0.10 meter in diameter.

(b) Except as specified in <u>paragraph (g)</u> of this section, to demonstrate that a vent stream flow rate is less than 0.005 standard cubic meter per minute in accordance with the Group 2 process vent definition of this subpart, the owner or operator shall measure flow rate by the following procedures:

(1) The sampling site shall be selected as specified in <u>paragraph (a)</u> of this section.

(2) The gas volumetric flow rate shall be determined using Method 2, 2A, 2C, or 2D of <u>40 CFR part 60, appendix A</u>, as appropriate.

(c) Except as specified in <u>paragraph (g)</u> of this section, each owner or operator seeking to demonstrate that a vent stream has an organic HAP concentration below 50 parts per million by volume in accordance with the Group 2 process vent definition of this subpart shall measure either total organic HAP or TOC concentration using the following procedures:

(1) The sampling site shall be selected as specified in <u>paragraph (a)</u> of this section.

(2) Method 18 or Method 25A of <u>40 CFR part 60, appendix A</u> shall be used to measure concentration; alternatively, any other method or data that has been validated according to the protocol in Method 301 of <u>appendix A of this part</u> may be used.

(3) Where Method 18 of <u>40 CFR part 60, appendix A</u> is used, the following procedures shall be used to calculate parts per million by volume concentration:

(i) The minimum sampling time for each run shall be 1 hour in which either an integrated sample or four grab samples shall be taken. If grab sampling is used, then the samples shall be taken at approximately equal intervals in time, such as 15 minute intervals during the run.

(ii) The concentration of either TOC (minus methane and ethane) or organic HAP shall be calculated according to <u>paragraph</u> (c)(3)(ii)(A) or (c)(3)(ii)(B) of this section as applicable.

(A) The TOC concentration ( $C_{TOC}$ ) is the sum of the concentrations of the individual components and shall be computed for each run using the following equation:

$$C_{TOC} = \frac{\sum_{i=1}^{x} \left( \sum_{j=1}^{n} C_{ji} \right)}{x}$$

where:

C<sub>TOC</sub> = Concentration of TOC (minus methane and ethane), dry basis, parts per million by volume.

 $C_{ji}$  = Concentration of sample component j of the sample i, dry basis, parts per million by volume.

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n = Number of components in the sample.

x = Number of samples in the sample run.

(B) The total organic HAP concentration ( $C_{HAP}$ ) shall be computed according to the equation in <u>paragraph (c)(3)(ii)(A)</u> of this section except that only the organic HAP species shall be summed. The list of organic HAP's is provided in table 2 of <u>subpart</u> <u>F of this part</u>.

(4) Where Method 25A of <u>40 CFR part 60, appendix A</u> is used, the following procedures shall be used to calculate parts per million by volume TOC concentration:

(i) Method 25A of <u>40 CFR part 60</u>, appendix A, shall be used only if a single organic HAP compound is greater than 50 percent of total organic HAP, by volume, in the vent stream.

(ii) The vent stream composition may be determined by either process knowledge, test data collected using an appropriate EPA method, or a method or data validated according to the protocol in Method 301 of <u>appendix A of this part</u>. Examples of information that could constitute process knowledge include calculations based on material balances, process stoichiometry, or previous test results provided the results are still relevant to the current vent stream conditions.

(iii) The organic HAP used as the calibration gas for Method 25A of <u>40 CFR part 60, appendix A</u> shall be the single organic HAP compound present at greater than 50 percent of the total organic HAP by volume.

(iv) The span value for Method 25A of <u>40 CFR part 60, appendix A</u> shall be 50 parts per million by volume.

(v) Use of Method 25A of  $\frac{40 \text{ CFR part 60, appendix A}}{1000 \text{ appendix A}}$  is acceptable if the response from the high-level calibration gas is at least 20 times the standard deviation of the response from the zero calibration gas when the instrument is zeroed on the most sensitive scale.

(vi) The owner or operator shall demonstrate that the concentration of TOC including methane and ethane measured by Method 25A of  $\frac{40 \text{ CFR part } 60, \text{ appendix A}}{10 \text{ cFR part } 60, \text{ appendix A}}$  is below 25 parts per million by volume to be considered a Group 2 vent with an organic HAP concentration below 50 parts per million by volume and to qualify for the low concentration exclusion in  $\frac{63.113(g)}{100}$  of this subpart.

(d) Except as specified in § 63.113(a)(4), to determine the TRE index value, the owner or operator shall conduct a TRE determination and calculate the TRE index value according to the procedures in paragraph (d)(1) or (2) of this section and the TRE equation in paragraph (d)(3) of this section.

(1) Engineering assessment may be used to determine vent stream flow rate, net heating value, TOC emission rate, and total organic HAP emission rate for the representative operating condition expected to yield the lowest TRE index value.

(i) If the TRE value calculated using such engineering assessment and the TRE equation in <u>paragraph (d)(3)</u> of this section is greater than 4.0, then the owner or operator is not required to perform the measurements specified in <u>paragraph (d)(2)</u> of this section.

(ii) If the TRE value calculated using such engineering assessment and the TRE equation in <u>paragraph (d)(3)</u> of this section is less than or equal to 4.0, then the owner or operator is required to perform the measurements specified in <u>paragraph (d)(2)</u> of this section for group determination or consider the process vent a Group 1 vent and comply with the emission reduction specified in <u>§ 63.113(a) of this subpart</u>.

(iii) Engineering assessment includes, but is not limited to, the following:

(A) Previous test results provided the tests are representative of current operating practices at the process unit.

(B) Bench-scale or pilot-scale test data representative of the process under representative operating conditions.

(C) Maximum flow rate, TOC emission rate, organic HAP emission rate, or net heating value limit specified or implied within a permit limit applicable to the process vent.

(D) Design analysis based on accepted chemical engineering principles, measurable process parameters, or physical or chemical laws or properties. Examples of analytical methods include, but are not limited to:

(1) Use of material balances based on process stoichiometry to estimate maximum organic HAP concentrations,

(2) Estimation of maximum flow rate based on physical equipment design such as pump or blower capacities,

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(3) Estimation of TOC or organic HAP concentrations based on saturation conditions,

(4) Estimation of maximum expected net heating value based on the vent stream concentration of each organic compound or, alternatively, as if all TOC in the vent stream were the compound with the highest heating value.

(E) All data, assumptions, and procedures used in the engineering assessment shall be documented.

(2) Except as provided in <u>paragraph (d)(1)</u> of this section, vent stream flow rate, net heating value, TOC emission rate, and total organic HAP emission rate shall be measured and calculated according to the procedures in <u>paragraphs</u> (d)(2)(i) through (v) of this section and used as input to the TRE index value calculation in <u>paragraph (d)(3)</u> of this section.

(i) The vent stream volumetric flow rate ( $Q_s$ ), in standard cubic meters per minute at 20 degrees Celcius, shall be determined using Method 2, 2A, 2C, or 2D of <u>40 CFR part 60, appendix A</u>, as appropriate. If the vent stream tested passes through a final steam jet ejector and is not condensed, the vent stream volumetric flow shall be corrected to 2.3 percent moisture.

(ii) The molar composition of the vent stream, which is used to calculate net heating value, shall be determined using the following methods:

(A) Method 18 of 40 CFR part 60, appendix A to measure the concentration of each organic compound.

(B) American Society for Testing and Materials D1946-77 to measure the concentration of carbon monoxide and hydrogen.

(C) Method 4 of <u>40 CFR part 60, appendix A</u>, to measure the moisture content of the vent stream.

(iii) The net heating value of the vent stream shall be calculated using the following equation:

$$\mathbf{H}_{\mathrm{T}} = \mathbf{K}_{1} \left( \sum_{j=1}^{n} \mathbf{C}_{j} \mathbf{H}_{j} \right) \left( 1 - \mathbf{B}_{\mathrm{ws}} \right)$$

where:

 $H_T$  = Net heating value of the sample, megaJoule per standard cubic meter, where the net enthalpy per mole of vent stream is based on combustion at 25 °C and 760 millimeters of mercury, but the standard temperature for determining the volume corresponding to one mole is 20 °C, as in the definition of Q<sub>s</sub> (vent stream flow rate).

 $K_1 = \text{Constant}, 1.740 \times 10^{-7} \text{ (parts per million)}^{-1} \text{ (gram-mole per standard cubic meter) (megaJoule per kilocalorie), where standard temperature for (gram-mole per standard cubic meter) is 20 °C.$ 

 $B_{ws}$  = Water vapor content of the vent stream, proportion by volume; except that if the vent stream passes through a final steam jet and is not condensed, it shall be assumed that  $B_{ws}$  = 0.023 in order to correct to 2.3 percent moisture.

 $C_j$  = Concentration on a dry basis of compound j in parts per million, as measured for all organic compounds by Method 18 of <u>40 CFR part 60, appendix A</u> and measured for hydrogen and carbon monoxide by American Society for Testing and Materials D1946-77 as indicated in <u>paragraph (d)(2)(ii)</u> of this section.

 $H_j$  = Net heat of combustion of compound j, kilocalorie per gram-mole, based on combustion at 25 °C and 760 millimeters mercury. The heats of combustion of vent stream components shall be determined using American Society for Testing and Materials D2382-76 if published values are not available or cannot be calculated.

(iv) The emission rate of TOC (minus methane and ethane) ( $E_{TOC}$ ) and the emission rate of total organic HAP ( $E_{HAP}$ ) in the vent stream shall both be calculated using the following equation:



where:

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E = Emission rate of TOC (minus methane and ethane) or emission rate of total organic HAP in the sample, kilograms per hour.

 $K_2 = Constant$ , 2.494 × 10<sup>-6</sup> (parts per million)<sup>-1</sup> (gram-mole per standard cubic meter) (kilogram/gram) (minutes/hour), where standard temperature for (gram-mole per standard cubic meter) is 20 °C.

 $C_j$  = Concentration on a dry basis of organic compound j in parts per million as measured by Method 18 of <u>40 CFR part 60</u>, <u>appendix A</u> as indicated in <u>paragraph (d)(2)(ii)</u> of this section. If the TOC emission rate is being calculated,  $C_j$  includes all organic compounds measured minus methane and ethane; if the total organic HAP emission rate is being calculated, only organic HAP compounds listed in table 2 in <u>subpart F of this part</u> are included.

M<sub>j</sub> = Molecular weight of organic compound j, gram/gram-mole.

 $Q_s$  = Vent stream flow rate, dry standard cubic meter per minute, at a temperature of 20 °C.

(v) In order to determine whether a vent stream is halogenated, the mass emission rate of halogen atoms contained in organic compounds shall be calculated.

(A) The vent stream concentration of each organic compound containing halogen atoms (parts per million by volume, by compound) shall be determined based on the following procedures:

(1) Process knowledge that no halogen or hydrogen halides are present in the process, or

(2) Applicable engineering assessment as discussed in paragraph (d)(1)(iii) of this section, or

(3) Concentration of organic compounds containing halogens measured by Method 18 of <u>40 CFR part 60, appendix A</u>, or

(4) Any other method or data that has been validated according to the applicable procedures in Method 301 of <u>appendix A of</u> this part.

(B) The following equation shall be used to calculate the mass emission rate of halogen atoms:

$$E = K_2 Q \left( \sum_{j=1}^{n} \sum_{i=1}^{m} C_j * L_{j,i} * M_{j,i} \right)$$

where:

E = mass of halogen atoms, dry basis, kilogram per hour.

 $K_2 = Constant$ , 2.494 × 10<sup>-6</sup> (parts per million)<sup>-1</sup> (kilogram-mole per standard cubic meter) (minute/hour), where standard temperature is 20 °C.

C<sub>j</sub> = Concentration of halogenated compound j in the gas stream, dry basis, parts per million by volume.

 $M_{ji}$  = Molecular weight of halogen atom i in compound j of the gas stream, kilogram per kilogram-mole.

 $L_{ji}$  = Number of atoms of halogen i in compound j of the gas stream.

Q = Flow rate of gas stream, dry standard cubic meters per minute, determined according to <u>paragraph (d)(1)</u> or <u>(d)(2)(i)</u> of this section.

j = Halogenated compound j in the gas stream.

- i = Halogen atom i in compound j of the gas stream.
- n = Number of halogenated compounds j in the gas stream.

m = Number of different halogens i in each compound j of the gas stream.

(3) The owner or operator shall calculate the TRE index value of the vent stream using the equations and procedures in this paragraph.

(i) The equation for calculating the TRE index for a vent stream controlled by a flare or incinerator is as follows:

$$TRE = \frac{1}{E_{HAP}} \left[ a + b(Q_{a}) + c(H_{T}) + d(E_{TOC}) \right]$$

where:

TRE = TRE index value.

 $E_{HAP}$  = Hourly emission rate of total organic HAP, kilograms per hour, as calculated in <u>paragraph (d)(1)</u> or <u>(d)(2)(iv)</u> of this section.

 $Q_s$  = Vent stream flow rate, standard cubic meters per minute, at a standard temperature of 20 °C, as calculated in <u>paragraph</u> (d)(1) or (d)(2)(i) of this section.

 $H_T$  = Vent stream net heating value, megaJoules per standard cubic meter, as calculated in <u>paragraph (d)(1)</u> or <u>(d)(2)(iii)</u> of this section.

 $E_{TOC} = E_{mission}$  rate of TOC (minus methane and ethane), kilograms per hour, as calculated in <u>paragraph</u> (d)(1) or (d)(2)(iv) of this section.

a,b,c,d = Coefficients presented in table 1 of this subpart, selected in accordance with <u>paragraphs (d)(3)(ii)</u> and <u>(iii)</u> of this section.

(ii) The owner or operator of a nonhalogenated vent stream shall calculate the TRE index value based on the use of a flare, a thermal incinerator with 0 percent heat recovery, and a thermal incinerator with 70 percent heat recovery and shall select the lowest TRE index value. The owner or operator shall use the applicable coefficients in table 1 of this subpart for nonhalogenated vent streams located within existing sources and the applicable coefficients in table 2 of this subpart for nonhalogenated vent streams located within new sources.

(iii) The owner or operator of a halogenated vent stream shall calculate the TRE index value based on the use of a thermal incinerator with 0 percent heat recovery, and a scrubber. The owner or operator shall use the applicable coefficients in table 1 of this subpart for halogenated vent streams located within existing sources and the applicable coefficients in table 2 of this subpart for halogenated vent streams located within new sources.

(e) Except as specified in § 63.113(a)(4), the owner or operator of a Group 2 process vent shall recalculate the TRE index value, flow, or organic hazardous air pollutants concentration for each process vent, as necessary to determine whether the vent is Group 1 or Group 2, whenever process changes are made that could reasonably be expected to change the vent to a Group 1 vent. Examples of process changes include, but are not limited to, changes in production capacity, production rate, feedstock type, or catalyst type, or whenever there is replacement, removal, or addition of recovery equipment. For purposes of this paragraph, process changes do not include: Process upsets; unintentional, temporary process changes; and changes that are within the range on which the original TRE calculation was based.

(1) The TRE index value, flow rate, or organic HAP concentration shall be recalculated based on measurements of vent stream flow rate, TOC, and organic HAP concentrations, and heating values as specified in § 63.115 (a), (b), (c), and (d) of this subpart, as applicable, or on best engineering assessment of the effects of the change. Engineering assessments shall meet the specifications in paragraph (d)(1) of this section.

(2) Where the recalculated TRE index value is less than or equal to 1.0, or less than or equal to 4.0 but greater than 1.0, the recalculated flow rate is greater than or equal to 0.005 standard cubic meter per minute, or the recalculated concentration is greater than or equal to 50 parts per million by volume, the owner or operator shall submit a report as specified in § 63.118 (g), (h), (i), or (j) of this subpart and shall comply with the appropriate provisions in § 63.113 of this subpart by the dates specified in § 63.100 of subpart F of this part.

(f) Except as specified in § 63.113(a)(4), notwithstanding any other provisions of this subpart, in any case where a process vent includes one or more gas streams that are not from a source subject to this subpart (hereafter called "non-HON streams" for purposes of this paragraph), and one or more gas streams that meet the criteria in § 63.107(b) through (h) or the criteria in § 63.107(i) (hereafter called "HON streams" for purposes of this paragraph), the owner or operator may elect to comply with paragraphs (f)(1) through (3) of this section.

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(1) The owner or operator may determine the characteristics (flow rate, total organic HAP concentration, and TRE index value) for each HON stream, or combination of HON streams, at a representative point as near as practical to, but before, the point at which it is combined with one or more non-HON streams.

(2) If one or more of the HON streams, or combinations of HON streams, has the characteristics (determined at the location specified in paragraph (f)(1) of this section) associated with a Group 1 process vent, the combined vent stream is a Group 1 process vent. Except as specified in paragraph (f)(3) of this section, if none of the HON streams, or combinations of HON streams, when determined at the location specified in paragraph (f)(1) of this section, has the characteristics associated with a Group 1 process vent, the combined vent stream is a Group 2 process vent regardless of the TRE index value determined at the location specified in  $\frac{63.115(a)}{10}$ . If the combined vent stream is a Group 2 process vent as determined by the previous sentence, but one or more of the HON streams, or combinations of HON streams, has a TRE index value greater than 1 but less than or equal to 4, the combined vent stream is a process vent with a TRE index value greater than 1 but less than or equal to 4. In this case, the owner or operator shall monitor the combined vent stream as required by  $\frac{63.114(b)}{2}$ .

(3) <u>Paragraphs (f)(1)</u> and (2) of this section are not intended to apply instead of any other subpart of this part. If another subpart of this part applies to one or more of the non-HON streams contributing to the combined vent stream, that subpart may impose emission control requirements such as, but not limited to, requiring the combined vent stream to be classified and controlled as a Group 1 process vent.

(g) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraphs (b) and (c) of this section no longer apply. Instead, to demonstrate that a vent stream total organic HAP mass flow rate is less than 1.0 pound per hour in accordance with the Group 2 process vent definition of this subpart, the owner or operator must use the following procedures:

(1) The sampling site must be selected as specified in <u>paragraph (a)</u> of this section.

(2) Method 18 or Method 25A of appendices A-6 and A-7 to <u>40 CFR part 60</u> of this chapter, respectively, or Method 320 of appendix A to this part must be used to measure concentration. ASTM D6420-18 (incorporated by reference, see § 63.14) may also be used in lieu of Method 18 or Method 320, if the target compounds are all known and are all listed in <u>section</u> <u>1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method.

(3) Where Method 18 of appendix A-6 to part 60 of this chapter, Method 320 of appendix A to this part, or ASTM D6420-18 is used, the following procedures must be used to calculate the total organic HAP mass flow rate:

(i) The minimum sampling time for each run must be 1 hour in which either an integrated sample or four grab samples must be taken. If grab sampling is used, then the samples must be taken at approximately equal intervals in time, such as 15 minute intervals during the run.

(ii) The mass rate of total organic HAP for each run must be computed using the following equation:

Equation 6 to Paragraph (g)(3)(ii)



Where:

 $E_{HAP}$  = Emission rate of total organic HAP, lb/hr.

 $K = 1.675 \times 10^{-7}$  (parts per million)<sup>-1</sup> (lb-mole per standard cubic feet) (minutes per hour), where standard temperature is 68 °F (20 °C).

Q = Flowrate of gas stream, dry standard cubic feet per minute), where standard temperature is 68 °F (20 °C), determined using Method 2, 2A, 2C, or 2D of 40 CFR part 60, appendix A, as appropriate. The flowrate may be based solely on an engineering assessment if measurements cannot be made with EPA reference methods.

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 $C_j$  = Concentration of organic compound j in the gas stream as measured by Method 18 of appendix A-6 to <u>40 CFR part 60</u>, Method 320 of appendix A to this part, or ASTM D6420-18 (incorporated by reference, see § 63.14), ppmv dry basis. The concentration may be based solely on an engineering assessment if measurements cannot be made with EPA reference methods.

 $M_i$  = Molecular weight of organic compound j, lb/lb-mole.

j = Individual organic HAP compound in the gas stream. The list of organic HAPs is provided in table 2 of subpart F of this part.

n = Number of organic HAP compounds j in the gas stream.

(iii) The owner or operator must demonstrate that the emission rate of total organic HAP is less than 1.0 pound per hour for the vent stream to be considered a Group 2 process vent.

(4) Where Method 25A of appendix A-7 to <u>part 60 of this chapter</u> is used, the following procedures must be used to calculate parts per million by volume TOC concentration:

(i) Method 25A of appendix A-7 to <u>part 60 of this chapter</u> must be used only if a single organic HAP compound is greater than 50 percent of total organic HAP, by volume, in the vent stream.

(A) This organic HAP must be used as the calibration gas for Method 25A of appendix A-7 to part 60 of this chapter.

(B) Use of Method 25A of appendix A-7 to <u>part 60 of this chapter</u> is acceptable if the response from the high-level calibration gas is at least 20 times the standard deviation of the response from the zero calibration gas when the instrument is zeroed on the most sensitive scale.

(ii) The span value for Method 25A of appendix A-7 to <u>part 60 of this chapter</u> must be equal to approximately twice the expected concentration of TOC in the gas stream.

(iii) The minimum sampling time for each run must be 1 hour. The results must be corrected to a dry basis. You must use Method 4 of appendix A-3 to <u>part 60 of this chapter</u> to convert the Method 25A results to a dry basis.

(iv) The mass rate of TOC for each run must be computed using the following equation:

Equation 7 to Paragraph (g)(4)(iv)

 $E_{TOC} = KCMQ$ 

Where:

 $E_{TOC}$  = Emission rate of TOC, lb/hr.

 $K = 1.675 \times 10^{-7}$  (parts per million)<sup>-1</sup> (lb-mole per standard cubic feet) (minutes per hour), where standard temperature is 68 °F (20 °C).

C = Concentration of TOC in the gas stream as measured by Method 25A of appendix A to <u>part 60 of this chapter</u> ppmv dry basis. The concentration may be based solely on an engineering assessment if measurements cannot be made with EPA reference methods.

M = Molecular weight of the organic HAP used as the calibration gas, lb/lb-mole.

Q = Flowrate of gas stream, dry standard cubic feet per minute), where standard temperature is 68 °F (20 °C), determined using Method 2, 2A, 2C, or 2D of appendix A-1 to <u>part 60 of this chapter</u>, as appropriate. The flowrate may be based solely on an engineering assessment if measurements cannot be made with EPA reference methods.

(v) The owner or operator must demonstrate that the emission rate of TOC is less than 1.0 pound per hour for the vent stream to be considered a Group 2 process vent.

(5) The requirements specified in <u>paragraphs (g)(1)</u> through (4) of this section for an initial measurement or initial performance test do not apply if the conditions specified in <u>paragraphs (g)(5)(i)</u> through (iv) of this section are met for a previously conducted measurement or performance test.

(i) No changes have been made to the process since the time of the measurement or performance test;

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(ii) The operating conditions and test methods used during measurement or performance test conform to the requirements in paragraphs (g)(1) through (4) of this section;

(iii) The control device and process parameter values established during the previously conducted measurement or performance test are used to demonstrate continuous compliance with the related requirements of this subpart, if applicable; and

(iv) The previously conducted measurement or performance test was completed within the last 60 months.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>62 FR 2746</u>, Jan. 17, 1997; <u>66 FR 6931</u>, Jan. 22, 2001; <u>89 FR 43181</u>, May 16, 2024]

# § 63.116 Process vent provisions—performance test methods and procedures to determine compliance.

(a) When a flare is used to comply with  $\S 63.113(a)(1)$ , the owner or operator shall comply with <u>paragraphs</u> (a)(1) through (3) of this section except as specified in  $\S 63.108(a)$ . The owner or operator is not required to conduct a performance test to determine percent emission reduction or outlet organic HAP or TOC concentration.

(1) Conduct a visible emission test using the techniques specified in  $\S 63.11(b)(4)$ .

(2) Determine the net heating value of the gas being combusted using the techniques specified in  $\frac{63.11(b)(6)}{63.11(b)(6)}$ .

(3) Determine the exit velocity using the techniques specified in either  $\S 63.11(b)(7)(i)$  (and  $\S 63.11(b)(7)(ii)$ , where applicable) or  $\S 63.11(b)(8)$ , as appropriate.

(b) An owner or operator is not required to conduct a performance test when any control device specified in <u>paragraphs</u> (b)(1) through (b)(5) of this section is used.

(1) A boiler or process heater with a design heat input capacity of 44 megawatts or greater.

(2) A boiler or process heater into which the gas stream is introduced with the primary fuel or is used as the primary fuel.

(3) A control device for which a performance test was conducted for determining compliance with a regulation promulgated by the EPA and the test was conducted using the same methods specified in this section and either no process changes have been made since the test, or the owner or operator can demonstrate that the results of the performance test, with or without adjustments, reliably demonstrate compliance despite process changes is not required to conduct an initial performance test. Subsequent performance tests must be conducted according to  $\frac{63.103(b)(1)}{2}$ .

(4) A boiler or process heater burning hazardous waste for which the owner or operator:

(i) Has been issued a final permit under <u>part 270 of this chapter</u> and complies with the requirements of part 266, subpart H, of this chapter;

(ii) Has certified compliance with the interim status requirements of part 266, subpart H, of this chapter;

(iii) Meets the requirement specified in <u>paragraph (b)(4)(v)</u> of this section, and has submitted a Notification of Compliance under  $\frac{63.1207(j)}{10}$  and complies with the requirements of <u>subpart EEE of this part</u>; or

(iv) Meets the requirement specified in <u>paragraph (b)(4)(v)</u> of this section, complies with <u>subpart EEE of this part</u>, and will submit a Notification of Compliance under § 63.1207(j) by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(v) The owner and operator may not waive performance testing pursuant to  $\frac{63.1207(d)(4)}{63.1207(d)}$  and each performance test required by  $\frac{63.1207(d)}{63.1207(d)}$  must show compliance with the dioxins and furans emission limit specified in  $\frac{63.113(a)(5)}{63.1207(d)}$ .

(5) A hazardous waste incinerator for which the owner or operator:

(i) Has been issued a final permit under <u>40 CFR part 270</u> and complies with the requirements of part 264, subpart O, of this chapter;

(ii) Has certified compliance with the interim status requirements of part 265, subpart O, of this chapter.

(iii) Meets the requirement specified in <u>paragraph (b)(5)(v)</u> of this section, and has submitted a Notification of Compliance under  $\S 63.1207(j)$  and complies with the requirements <u>subpart EEE of this part</u>; or

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(iv) Meets the requirement specified in <u>paragraph (b)(5)(v)</u> of this section, complies with the requirements <u>subpart EEE of</u> <u>this part</u>, and will submit a Notification of Compliance under  $\S 63.1207(j)$  by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(v) The owner and operator may not waive performance testing pursuant to  $\frac{63.1207(d)(4)}{63.1207(d)}$  and each performance test required by  $\frac{63.1207(d)}{63.1207(d)}$  must show compliance with the dioxins and furans emission limit specified in  $\frac{63.113(a)(5)}{63.1207(d)}$ .

(c) Except as provided in <u>paragraphs (a)</u> and (b) of this section, an owner or operator using a control device to comply with the organic HAP concentration limit or percent reduction efficiency requirements in § 63.113(a)(2) of this subpart shall conduct performance tests using the procedures in <u>paragraphs (c)(1)</u> through (4) of this section according to the schedule in § 63.103(b)(1) of <u>subpart F of this part</u>. The organic HAP concentration and percent reduction may be measured as either total organic HAP or as TOC minus methane and ethane according to the procedures specified.

(1) Method 1 or 1A of <u>40 CFR part 60, appendix A</u>, as appropriate, shall be used for selection of the sampling sites.

(i) For determination of compliance with the 98 percent reduction of total organic HAP requirement of § 63.113(a)(2) of this subpart, sampling sites shall be located at the inlet of the control device as specified in paragraphs (c)(1)(i)(A) and (c)(1)(i)(B) of this section, and at the outlet of the control device.

(A) The control device inlet sampling site shall be located after the final product recovery device.

(B) If a vent stream is introduced with the combustion air or as a secondary fuel into a boiler or process heater with a design capacity less than 44 megawatts, selection of the location of the inlet sampling sites shall ensure the measurement of total organic HAP or TOC (minus methane and ethane) concentrations in all vent streams and primary and secondary fuels introduced into the boiler or process heater.

(ii) For determination of compliance with the 20 parts per million by volume total organic HAP limit in  $\frac{63.113(a)(2)}{20}$  of this subpart, the sampling site shall be located at the outlet of the control device.

(2) The gas volumetric flow rate shall be determined using Method 2, 2A, 2C, or 2D of <u>40 CFR part 60, appendix A</u>, as appropriate.

(3) To determine compliance with the 20 parts per million by volume total organic HAP limit in  $\frac{63.113(a)(2)}{63.113(a)(2)}$  of this subpart, the owner or operator shall use Method 18 of appendix A-6 to part 60 of this chapter to measure either TOC minus methane and ethane or total organic HAP. ASTM D6420-18 (incorporated by reference, see  $\frac{63.14}{60.11}$ ) may also be used in lieu of Method 18, if the target compounds are all known and are all listed in Section 1.1 of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method. Alternatively, any other method or data that has been validated according to the applicable procedures in Method 301 of appendix A of this part, may be used. The following procedures shall be used to calculate parts per million by volume concentration, corrected to 3 percent oxygen:

(i) The minimum sampling time for each run shall be 1 hour in which either an integrated sample or a minimum of four grab samples shall be taken. If grab sampling is used, then the samples shall be taken at approximately equal intervals in time, such as 15 minute intervals during the run.

(ii) The concentration of either TOC (minus methane or ethane) or total organic HAP shall be calculated according to  $\frac{\text{paragraph}(c)(3)(ii)(A)}{\text{or }(c)(3)(ii)(B)}$  of this section.

(A) The TOC concentration ( $C_{TOC}$ ) is the sum of the concentrations of the individual components and shall be computed for each run using the following equation:



where:

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C<sub>TOC</sub> = Concentration of TOC (minus methane and ethane), dry basis, parts per million by volume.

 $C_{ji}$  = Concentration of sample components j of sample i, dry basis, parts per million by volume.

n = Number of components in the sample.

x = Number of samples in the sample run.

(B) The total organic HAP concentration ( $C_{HAP}$ ) shall be computed according to the equation in <u>paragraph (c)(3)(ii)(A)</u> of this section except that only the organic HAP species shall be summed. The list of organic HAP's is provided in table 2 of <u>subpart</u> <u>F of this part</u>.

(iii) The concentration of TOC or total organic HAP shall be corrected to 3 percent oxygen if a combustion device is the control device.

(A) Method 3A of appendix A-2 to <u>part 60 of this chapter</u> or the manual method in ANSI/ASME PTC 19.10-1981 (incorporated by reference, see § 63.14) shall be used to determine the oxygen concentration (%O2d). The samples shall be taken during the same time that the TOC (minus methane or ethane) or total organic HAP samples are taken.

(B) The concentration corrected to 3 percent oxygen (C<sub>c</sub>) shall be computed using the following equation:

$$C_{c} = C_{m} \left( \frac{17.9}{20.9 - \% O_{2d}} \right)$$

Where:

C<sub>c</sub> = Concentration of TOC or organic HAP corrected to 3 percent oxygen, dry basis, parts per million by volume.

C<sub>m</sub> = Concentration of TOC (minus methane and ethane) or organic HAP, dry basis, parts per million by volume.

 $%0_{2d}$  = Concentration of oxygen, dry basis, percent by volume.

(4) To determine compliance with the 98 percent reduction requirement of  $\S$  63.113(a)(2), the owner or operator shall use Method 18 of appendix A-6 to <u>part 60 of this chapter</u>; alternatively, any other method or data that has been validated according to the applicable procedures in Method 301 of appendix A to this part may be used. ASTM D6420-18 (incorporated by reference, see  $\S$  63.14) may also be used in lieu of Method 18, if the target compounds are all known and are all listed in <u>section 1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method. The following procedures shall be used to calculate percent reduction efficiency:

(i) The minimum sampling time for each run shall be 1 hour in which either an integrated sample or a minimum of four grab samples shall be taken. If grab sampling is used, then the samples shall be taken at approximately equal intervals in time such as 15 minute intervals during the run.

(ii) The mass rate of either TOC (minus methane and ethane) or total organic HAP (E<sub>i</sub>, E<sub>o</sub>) shall be computed.

(A) The following equations shall be used:

$$\mathbf{E}_{i} = \mathbf{K}_{2} \left( \sum_{j=1}^{n} \mathbf{C}_{ij} \mathbf{M}_{ij} \right) \mathbf{Q}_{i} \ \mathbf{E}_{o} = \mathbf{K}_{2} \left( \sum_{j=1}^{n} \mathbf{C}_{oj} \mathbf{M}_{oj} \right) \mathbf{Q}_{o}$$

where:

 $C_{ij}$ ,  $C_{oj}$  = Concentration of sample component j of the gas stream at the inlet and outlet of the control device, respectively, dry basis, parts per million by volume.

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 $E_i$ ,  $E_o$  = Mass rate of TOC (minus methane and ethane) or total organic HAP at the inlet and outlet of the control device, respectively, dry basis, kilogram per hour.

 $M_{ij}$ ,  $M_{oj}$  = Molecular weight of sample component j of the gas stream at the inlet and outlet of the control device, respectively, gram/gram-mole.

 $Q_i$ ,  $Q_o$  = Flow rate of gas stream at the inlet and outlet of the control device, respectively, dry standard cubic meter per minute.

 $K_2 = Constant$ , 2.494 × 10<sup>-6</sup> (parts per million)<sup>-1</sup> (gram-mole per standard cubic meter) (kilogram/gram) (minute/hour), where standard temperature (gram-mole per standard cubic meter) is 20 °C.

(B) Where the mass rate of TOC is being calculated, all organic compounds (minus methane and ethane) measured by Method 18 of appendix A-6 to <u>part 60 of this chapter</u> or ASTM D6420-18 (incorporated by reference, see § 63.14) are summed using the equation in <u>paragraph (c)(4)(ii)(A)</u> of this section.

(C) Where the mass rate of total organic HAP is being calculated, only the organic HAP species shall be summed using the equation in paragraph (c)(4)(ii)(A) of this section. The list of organic HAP's is provided in table 2 of subpart F of this part.

(iii) The percent reduction in TOC (minus methane and ethane) or total organic HAP shall be calculated as follows:

$$\mathbf{R} = \frac{\mathbf{E}_i - \mathbf{E}_s}{\mathbf{E}_i} (100)$$

where:

R = Control efficiency of control device, percent.

 $E_i = Mass rate of TOC$  (minus methane and ethane) or total organic HAP at the inlet to the control device as calculated under <u>paragraph (c)(4)(ii)</u> of this section, kilograms TOC per hour or kilograms organic HAP per hour.

 $E_o =$  Mass rate of TOC (minus methane and ethane) or total organic HAP at the outlet of the control device, as calculated under <u>paragraph (c)(4)(ii)</u> of this section, kilograms TOC per hour or kilograms organic HAP per hour.

(iv) If the vent stream entering a boiler or process heater with a design capacity less than 44 megawatts is introduced with the combustion air or as a secondary fuel, the weight-percent reduction of total organic HAP or TOC (minus methane and ethane) across the device shall be determined by comparing the TOC (minus methane and ethane) or total organic HAP in all combusted vent streams and primary and secondary fuels with the TOC (minus methane and ethane) or total organic HAP exiting the combustion device, respectively.

(d) An owner or operator using a combustion device followed by a scrubber or other halogen reduction device to control halogenated vent streams in compliance with  $\frac{63.113(c)(1)}{5}$  shall conduct performance tests to determine compliance with the control efficiency or emission limits for hydrogen halides and halogens according to the schedule in  $\frac{63.103(b)(1)}{5}$ .

(1) For an owner or operator determining compliance with the percent reduction of total hydrogen halides and halogens, sampling sites shall be located at the inlet and outlet of the scrubber or other halogen reduction device used to reduce halogen emissions. For an owner or operator determining compliance with the less than 0.45 kilogram per hour outlet emission limit for total hydrogen halides and halogens, the sampling site shall be located at the outlet of the scrubber or other halogen reduction device and prior to any releases to the atmosphere.

(2) Except as provided in paragraph (d)(5) of this section, Method 26 or Method 26A of 40 CFR part 60, appendix A, shall be used to determine the concentration, in milligrams per dry standard cubic meter, of total hydrogen halides and halogens that may be present in the vent stream. The mass emissions of each hydrogen halide and halogen compound shall be calculated from the measured concentrations and the gas stream flow rate.

(3) To determine compliance with the percent removal efficiency, the mass emissions for any hydrogen halides and halogens present at the inlet of the scrubber or other halogen reduction device shall be summed together. The mass emissions of the compounds present at the outlet of the scrubber or other halogen reduction device shall be summed together. Percent reduction shall be determined by comparison of the summed inlet and outlet measurements.

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(4) To demonstrate compliance with the less than 0.45 kilogram per hour outlet emission limit, the test results must show that the mass emission rate of total hydrogen halides and halogens measured at the outlet of the scrubber or other halogen reduction device is below 0.45 kilogram per hour.

(5) The owner or operator may use any other method to demonstrate compliance if the method or data has been validated according to the applicable procedures of Method 301 of <u>appendix A of this part</u>.

(e) An owner or operator using a scrubber or other halogen reduction device to reduce the vent stream halogen atom mass emission rate to less than 0.45 kilogram per hour prior to a combustion control device in compliance with  $\frac{63.113(c)(2)}{50.000}$  of this subpart shall determine the halogen atom mass emission rate prior to the combustor according to the procedures in  $\frac{63.115(d)(2)(v)}{50.000}$  of this subpart.

(f) To demonstrate compliance with the emission limits and work practice standards specified in  $\frac{63.113(j)}{5}$  for process vents in ethylene oxide service, owners and operators must meet the requirements specified in  $\frac{63.124}{5}$ .

(g) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), an owner or operator using a recapture device to comply with the organic HAP concentration limit or percent reduction efficiency requirements in § 63.113(a)(2) shall conduct a performance test using the same procedures specified in paragraph (c) of this section, except the term "recapture device" is substituted for "control device."

(h) To demonstrate compliance with the dioxins and furans emission limit specified in  $\frac{63.113(a)(5)}{63.103(b)(1)}$ , owners and operators must conduct performance tests using the procedures in <u>paragraphs (h)(1)</u> through (6) of this section according to the schedule in  $\frac{63.103(b)(1)}{63.103(b)(1)}$ .

(1) The performance test must consist of three test runs. Collect at least 3 dry standard cubic meters of gas per test run.

(2) Use Method 1 or 1A of appendix A-1 to <u>40 CFR part 60</u> to select the sampling sites at the sampling location. The sampling location must be at the outlet of the final control device.

(3) Determine the gas volumetric flowrate using Method 2, 2A, 2C, or 2D of appendix A-1 to part 60 of this chapter.

(4) Use Method 4 of appendix A-3 to part 60 of this chapter to convert the volumetric flowrate to a dry basis.

(5) Measure the concentration of each tetra- through octa-chlorinated dioxin and furan congener emitted using Method 23 of appendix A-7 to <u>part 60 of this chapter</u>.

(i) For each dioxin and furan congener, multiply the congener concentration by its corresponding toxic equivalency factor specified in table 38 to this subpart. For determination of toxic equivalency, zero may be used for congeners with a concentration less than the estimated detection limit (EDL). For congeners with estimated maximum pollutant concentration (EMPC) results, if the value is less than the EDL, zero may be used. Otherwise, the EMPC value must be used in the calculation of toxic equivalency.

(ii) Sum the products calculated in accordance with <u>paragraph (h)(5)(i)</u> of this section to obtain the total concentration of dioxins and furans emitted in terms of toxic equivalency.

(6) The concentration of dioxins and furans shall be corrected to 3 percent oxygen. Use Method 3A of <u>40 CFR part 60</u>, <u>appendix A</u>, or the manual method in ANSI/ASME PTC 19.10-1981 (incorporated by reference, see § 63.14) to determine the oxygen concentration (%O2d). The oxygen concentration must be determined concurrently with Method 23 of appendix A-7 to <u>part 60 of this chapter</u>. The concentration corrected to 3 percent oxygen (Cc) shall be computed using the following equation:

$$C_{c} = C_{m} \left( \frac{17.9}{20.9 - \% O_{2d}} \right)$$

Where:

C<sub>c</sub> = Concentration of dioxins and furans corrected to 3 percent oxygen, dry basis, nanograms per standard cubic meter.

 $C_m$  = Concentration of dioxins and furans, dry basis, nanograms per standard cubic meter.

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%O2d = Concentration of oxygen, dry basis, percent by volume.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>62 FR 2746</u>, Jan. 17, 1997; <u>64 FR 20191</u>, Apr. 26, 1999; <u>66 FR 6931</u>, Jan. 22, 2001; <u>89 FR 43183</u>, May 16, 2024]

# § 63.117 Process vent provisions—reporting and recordkeeping requirements for group and TRE determinations and performance tests.

(a) Except as specified in  $\frac{63.113(a)(4)}{63.113(a)}$ , each owner or operator subject to the control provisions for Group 1 process vents in  $\frac{63.113(a)}{63.113(a)}$  or the provisions for Group 2 process vents with a TRE index value greater than 1.0 but less than or equal to 4.0 in  $\frac{63.113(a)}{63.113(a)}$  shall:

(1) Keep an up-to-date, readily accessible record of the data specified in <u>paragraphs (a)(4)</u> through (10) of this section, as applicable, and

(2) Include the data in <u>paragraphs (a)(4)</u> through (10) of this section in the Notification of Compliance Status report as specified in § 63.152(b) of this subpart.

(3) Except as specified in  $\S 63.113(a)(4)$ , if any subsequent TRE determinations or performance tests are conducted after the Notification of Compliance Status has been submitted, report the data in <u>paragraphs (a)(4)</u> through (a)(10) of this section in the next Periodic Report as specified in  $\S 63.152(c)$ .

(4) Record and report the following when using a combustion device to achieve a 98 weight percent reduction in organic HAP or an organic HAP concentration of 20 parts per million by volume, as specified in  $\frac{63.113(a)(2)}{2}$ :

(i) The parameter monitoring results for incinerators, catalytic incinerators, boilers or process heaters specified in table 3 of this subpart, and averaged over the same time period of the performance testing.

(ii) For an incinerator, the percent reduction of organic HAP or TOC achieved by the incinerator determined as specified in  $\frac{63.116(c)}{c}$ , or the concentration of organic HAP or TOC (parts per million by volume, by compound) determined as specified in  $\frac{63.116(c)}{c}$  at the outlet of the incinerator on a dry basis corrected to 3 percent oxygen.

(iii) For a boiler or process heater, a description of the location at which the vent stream is introduced into the boiler or process heater.

(iv) For a boiler or process heater with a design heat input capacity of less than 44 megawatts and where the vent stream is introduced with combustion air or used as a secondary fuel and is not mixed with the primary fuel, the percent reduction of organic HAP or TOC, or the concentration of organic HAP or TOC (parts per million by volume, by compound) determined as specified in  $\frac{63.116(c)}{2}$  at the outlet of the combustion device on a dry basis corrected to 3 percent oxygen.

(5) Except as specified in  $\S$  63.108)(a), record and report the following when using a flare to comply with  $\S$  63.113(a)(1):

(i) Flare design (*i.e.*, steam-assisted, air-assisted, or non-assisted);

(ii) All visible emission readings, heat content determinations, flow rate measurements, and exit velocity determinations made during the compliance determination required by  $\S$  63.116(a); and

(iii) All periods during the compliance determination when the pilot flame is absent.

(6) Record and report the following when using a scrubber following a combustion device to control a halogenated vent stream:

(i) The percent reduction or scrubber outlet mass emission rate of total hydrogen halides and halogens as specified in § 63.116(d);

(ii) The pH of the scrubber effluent; and

(iii) The scrubber liquid to gas ratio.

(7) Except as specified in  $\S$  <u>63.113(a)(4)</u>, record and report the following when achieving and maintaining a TRE index value greater than 1.0 but less than 4.0 as specified in  $\S$  <u>63.113(a)(3)</u> or <u>(d)</u>:

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(i) The parameter monitoring results for absorbers, condensers, or carbon adsorbers, as specified in table 4 to this subpart, and averaged over the same time period of the measurements of vent stream flow rate and concentration used in the TRE determination (both measured while the vent stream is normally routed and constituted), and

(ii) The measurements and calculations performed to determine the TRE index value of the vent stream.

(8) Record and report the halogen concentration in the vent stream determined according to the procedures specified in  $\S$  <u>63.115(d)(2)(v)</u>.

(9) When using a recapture device to achieve a 98 weight percent reduction in organic HAP or an organic HAP concentration of 20 parts per million by volume, as specified in  $\frac{63.113(a)(2)}{2}$ , record and report the parameter monitoring results for absorbers, condensers, or carbon adsorbers, as specified in table 3 of this subpart, and averaged over the same time period of the performance testing.

(10) Record and report the following when using a control device, recapture device, or recovery device to meet the dioxins and furans emissions limit.

(i) The parameter monitoring results, as specified in table 3 of this subpart, for the applicable device and averaged over the same time period of the performance testing.

(ii) The dioxins and furans concentration on a toxic equivalency basis (nanograms per standard cubic meter on a dry basis corrected to 3 percent oxygen) determined as specified in  $\frac{63.116}{10}$ .

(b) Except as specified in § 63.113(a)(4), the owner or operator of a Group 2 process vent with a TRE index greater than 4.0 as specified in § 63.113(e), shall maintain records and submit as part of the Notification of Compliance Status specified in § 63.152, measurements, engineering assessments, and calculations performed to determine the TRE index value of the vent stream. Documentation of engineering assessments shall include all data, assumptions, and procedures used for the engineering assessments, as specified in § 63.115(d)(1).

(c) Except as specified in <u>paragraph (g)</u> of this section, each owner or operator who elects to demonstrate that a process vent is a Group 2 process vent based on a flow rate less than 0.005 standard cubic meter per minute must submit to the Administrator the flow rate measurement using methods and procedures specified in § 63.115(a) and (b) with the Notification of Compliance Status specified in § 63.152.

(d) Except as specified in <u>paragraph (g)</u> of this section, each owner or operator who elects to demonstrate that a process vent is a Group 2 process vent based on organic HAP or TOC concentration less than 50 parts per million by volume must submit to the Administrator an organic HAP or TOC concentration measurement using the methods and procedures specified in  $\S$  <u>63.115(a)</u> and (c) with the Notification of Compliance Status specified in  $\S$  <u>63.152</u>.

(e) If an owner or operator uses a control or recovery device other than those listed in tables 3 and 4 to this subpart or requests approval to monitor a parameter other than those specified in tables 3 and 4 to this subpart, the owner or operator shall submit a description of planned reporting and recordkeeping procedures as required under  $\frac{63.151(f)}{10}$  or  $\frac{63.152(e)}{10}$ . The Administrator will specify appropriate reporting and recordkeeping requirements as part of the review of the permit application or by other appropriate means.

(f) For each parameter monitored according to tables 3 or 4 to this subpart or <u>paragraph (e)</u> of this section, the owner or operator shall establish a range for the parameter that indicates proper operation of the control or recovery device. In order to establish the range, the information required in  $\S$  63.152(b) shall be submitted in the Notification of Compliance Status or the operating permit application or amendment.

(g) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraphs (c) and (d) of this section no longer apply. Instead, each owner or operator demonstrating that a process vent is a Group 2 process vent based on total organic HAP mass flow rate less than 1.0 pound per hour must submit to the Administrator a total organic HAP measurement using the methods and procedures specified in § 63.115(g) with the Notification of Compliance Status specified in § 63.152.

[89 FR 43184, May 16, 2024]

# § 63.118 Process vent provisions—periodic reporting and recordkeeping requirements.

(a) Each owner or operator using a control device to comply with  $\S$  63.113(a)(1), (2), or (5) shall keep the following records up-to-date and readily accessible:

(1) Continuous records of the equipment operating parameters specified to be monitored under  $\frac{63.114(a)}{10}$  to this subpart and listed in table 3 to this subpart or specified by the Administrator in accordance with  $\frac{63.114(c)}{10}$  and  $\frac{63.117(c)}{10}$ . For flares, the hourly records and records of pilot flame outages specified in table 3 to this subpart shall be maintained in place of continuous records.

(2) Records of the daily average value of each continuously monitored parameter for each operating day determined according to the procedures specified in § 63.152(f). For flares complying with § 63.11(b), records of the times and duration of all periods during which all pilot flames are absent shall be kept rather than daily averages. For flares complying with § 63.108, the owner or operator must comply with the recordkeeping requirements specified therein.

(3) Hourly records of whether the flow indicator specified under  $\frac{663.114(d)(1)}{10}$  was operating and whether a diversion was detected at any time during the hour, as well as records of the times and durations of all periods when the gas stream is diverted to the atmosphere or the monitor is not operating.

(4) Where a seal mechanism is used to comply with  $\frac{63.114(d)(2)}{2}$ , hourly records of flow are not required. In such cases, the owner or operator shall record that the monthly visual inspection of the seals or closure mechanism has been done, and shall record the duration of all periods when the seal mechanism is broken, the bypass line valve position has changed, or the key for a lock-and-key type lock has been checked out, and records of any car-seal that has broken.

(5) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in <u>paragraphs (a)(1)</u> through (4) of this section. For each flow event from a bypass line subject to the requirements in § 63.114(d), the owner or operator must maintain records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requirements in records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requirements in the requirements in this subpart, the owner or operator must include an estimate of the volume of gas, the concentration of organic HAP in the gas and the resulting emissions of organic HAP that bypassed the control device using process knowledge and engineering estimates.

(b) Except as specified in  $\frac{63.113(a)(4)}{(4)}$ , each owner or operator using a recovery device or other means to achieve and maintain a TRE index value greater than 1.0 but less than 4.0 as specified in  $\frac{63.113(a)(3)}{(4)}$  or  $\frac{(d)}{(4)}$  shall keep the following records up-to-date and readily accessible:

(1) Continuous records of the equipment operating parameters specified to be monitored under  $\frac{63.114(b)}{63.114(c)}$  to this subpart and listed in table 4 to this subpart or specified by the Administrator in accordance with  $\frac{63.114(c)}{63.114(c)}$  and  $\frac{63.114(c)}{63.114(c)}$  and

(2) Records of the daily average value of each continuously monitored parameter for each operating day determined according to the procedures specified in  $\S$  63.152(f). If carbon adsorber regeneration stream flow and carbon bed regeneration temperature are monitored, the records specified in table 4 to this subpart shall be kept instead of the daily averages.

(c) Except as specified in  $\S 63.113(a)(4)$ , each owner or operator subject to the provisions of this subpart and who elects to demonstrate compliance with the TRE index value greater than 4.0 under  $\S 63.113(e)$  or greater than 1.0 under  $\S 63.113(a)(3)$  or (d) shall keep up-to-date, readily accessible records of:

(1) Any process changes as defined in  $\S 63.115(e)$ ; and

(2) Any recalculation of the TRE index value pursuant to  $\S 63.115(e)$ .

(d) Except as specified in <u>paragraph (n)</u> of this section, each owner or operator who elects to comply by maintaining a flow rate less than 0.005 standard cubic meter per minute under  $\frac{63.113(f)}{5}$ , shall keep up-to-date, readily accessible records of:

(1) Any process changes as defined in  $\S$  63.115(e) that increase the vent stream flow rate,

(2) Any recalculation or measurement of the flow rate pursuant to  $\frac{63.115(e)}{100}$ , and

(3) Except as specified in  $\S$  63.113(a)(4), if the flow rate increases to 0.005 standard cubic meter per minute or greater as a result of the process change, the TRE determination performed according to the procedures of  $\S$  63.115(d).

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(e) Except as specified in <u>paragraph (n)</u> of this section, each owner or operator who elects to comply by maintaining an organic HAP concentration less than 50 parts per million by volume organic HAP concentration under  $\frac{63.113(g)}{2}$  shall keep up-to-date, readily accessible records of:

(1) Any process changes as defined in § 63.115(e) that increase the organic HAP concentration of the vent stream,

(2) Any recalculation or measurement of the concentration pursuant to  $\S$  63.115(e), and

(3) Except as specified in  $\S 63.113(a)(4)$ , if the organic HAP concentration increases to 50 parts per million by volume or greater as a result of the process change, the TRE determination performed according to the procedures of  $\S 63.115(d)$ .

(f) Each owner or operator who elects to comply with the requirements of  $\frac{63.113}{5}$  of this subpart shall submit to the Administrator Periodic Reports of the following recorded information according to the schedule in  $\frac{63.152}{5}$ .

(1) Reports of daily average values of monitored parameters for all operating days when the daily average values recorded under <u>paragraphs (a)</u> and <u>(b)</u> of this section were outside the ranges established in the Notification of Compliance Status or operating permit, including the date that the parameter was outside the range.

(2) For Group 1 points, reports of the duration (in hours) of periods when monitoring data is not collected for each excursion caused by insufficient monitoring data as defined in  $\S$  63.152(c)(2)(ii)(A), including the start date of such periods.

(3) Reports of the times and durations of all periods recorded under <u>paragraph (a)(3)</u> of this section when the gas stream is diverted to the atmosphere through a bypass line and if applicable, the information in <u>paragraph (f)(7)</u> of this section. Include the start date, start time and duration in hours of each period.

(4) Reports of all periods recorded under <u>paragraph (a)(4)</u> of this section in which the seal mechanism is broken, the bypass line valve position has changed, or the key to unlock the bypass line valve was checked out and if applicable, the information in <u>paragraph (f)(7)</u> of this section. Include the start date, start time and duration in hours of each period.

(5) Except as specified in paragraph (a) of § 63.108, reports of the times and durations of all periods recorded under paragraph (a)(2) of this section in which all pilot flames of a flare were absent.

(6) Reports of all carbon bed regeneration cycles during which the parameters recorded under <u>paragraph (b)(2)(v)</u> of this section were outside the ranges established in the Notification of Compliance Status or operating permit. Include the identification of the carbon bed, the monitored parameter that was outside the established range, and the start date, start time and duration in hours of the regeneration cycle.

(7) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in <u>paragraphs</u> (f)(3) and (4) of this section. For bypass lines subject to the requirements in § 63.114(d), the Periodic Report must include the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours.

(8) For process vents in ethylene oxide service subject to the requirements of  $\S$  63.124, the Periodic Report must include the records for periods specified in paragraph (1)(2) of this section. Indicate the start date and time and end date and time for each period.

(9) For any maintenance vent release exceeding the applicable limits in  $\S 63.113(k)(1)$ , the compliance report must include the information specified in paragraphs (f)(9)(i) through (iv) of this section. For the purposes of this reporting requirement, if an owner or operator complies with  $\S 63.113(k)(1)(iv)$  then the owner or operator must report each venting event conducted under those provisions and include an explanation for each event as to why utilization of this alternative was required.

(i) Identification of the maintenance vent and the equipment served by the maintenance vent.

(ii) The date and time the maintenance vent was opened to the atmosphere.

(iii) The LEL in percent, vessel pressure in psig, or mass in pounds of VOC in the equipment, as applicable, at the start of atmospheric venting. If the 5 psig vessel pressure option in  $\frac{663.113(k)(1)(ii)}{1000}$  was used and active purging was initiated while the concentration of the vapor was 10 percent or greater of its LEL, also include the concentration of the vapors at the time active purging was initiated.

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(iv) An estimate of the mass in pounds of organic HAP released during the entire atmospheric venting event.

(g) Whenever a process change, as defined in  $\S$  63.115(e), is made that causes a Group 2 process vent to become a Group 1 process vent, the owner or operator shall submit a report within 180 calendar days after the process change as specified in  $\S$  63.151(j). The report shall include:

(1) A description of the process change;

(2) Except as specified in  $\S 63.113(a)(4)$ , the results of the recalculation of the flow rate, organic HAP concentration, and TRE index value required under  $\S 63.115(e)$  and recorded under paragraph (c), (d), or (e) of this section; and

(3) A statement that the owner or operator will comply with the provisions of  $\frac{63.113}{5}$  for Group 1 process vents by the dates specified in subpart F of this part.

(h) Except as specified in  $\S$  <u>63.113(a)(4)</u>, whenever a process change, as defined in  $\S$  <u>63.115(e)</u>, is made that causes a Group 2 process vent with a TRE greater than 4.0 to become a Group 2 process vent with a TRE less than 4.0, the owner or operator shall submit a report within 180 calendar days after the process change. The report may be submitted as part of the next periodic report. The report shall include:

(1) A description of the process change,

(2) The results of the recalculation of the TRE index value required under  $\frac{63.115(e)}{2}$  and recorded under paragraph (c) of this section, and

(3) A statement that the owner or operator will comply with the requirements specified in  $\S 63.113(d)$ .

(i) Except as specified in  $\S$  63.113(a)(4), whenever a process change, as defined in  $\S$  63.115(e), is made that causes a Group 2 process vent with a flow rate less than 0.005 standard cubic meter per minute to become a Group 2 process vent with a flow rate of 0.005 standard cubic meter per minute or greater and a TRE index value less than or equal to 4.0, the owner or operator shall submit a report within 180 calendar days after the process change. The report may be submitted as part of the next periodic report. The report shall include:

(1) A description of the process change,

(2) The results of the recalculation of the flow rate and the TRE determination required under  $\frac{63.115(e)}{100}$  and recorded under paragraph (d) of this section, and

(3) A statement that the owner or operator will comply with the requirements specified in  $\S 63.113(d)$ .

(j) Except as specified in  $\S$  63.113(a)(4), whenever a process change, as defined in  $\S$  63.115(e), is made that causes a Group 2 process vent with an organic HAP concentration less than 50 parts per million by volume to become a Group 2 process vent with an organic HAP concentration of 50 parts per million by volume or greater and a TRE index value less than or equal to 4.0, the owner or operator shall submit a report within 180 calendar days after the process change. The report may be submitted as part of the next periodic report. The report shall include:

(1) A description of the process change,

(2) The results of the recalculation of the organic HAP concentration and the TRE determination required under  $\underline{\$}$  <u>63.115(e)</u> and recorded under <u>paragraph (e)</u> of this section, and

(3) A statement that the owner or operator will comply with the requirements specified in  $\frac{63.113(d)}{2}$ .

(k) The owner or operator is not required to submit a report of a process change if one of the conditions listed in <u>paragraph</u> (k)(1), (2), (3), or (4) of this section is met.

(1) The process change does not meet the definition of a process change in  $\S 63.115(e)$ , or

(2) The vent stream flow rate is recalculated according to  $\frac{63.115(e)}{100}$  and the recalculated value is less than 0.005 standard cubic meter per minute, or

(3) The organic HAP concentration of the vent stream is recalculated according to  $\frac{63.115(e)}{2}$  and the recalculated value is less than 50 parts per million by volume, or

(4) Except as specified in  $\S$  63.113(a)(4), the TRE index value is recalculated according to  $\S$  63.115(e) and the recalculated value is greater than 4.0.

(1) For process vents in ethylene oxide service subject to the requirements of  $\frac{63.124}{2}$ , owners and operators must keep the records specified in <u>paragraphs (1)(1)</u> and (2) of this section in addition to those records specified elsewhere in this section.

(1) For process vents, include all uncontrolled, undiluted ethylene oxide concentration measurements, and the calculations used to determine the total uncontrolled ethylene oxide mass emission rate for the sum of all vent gas streams.

(2) If emissions are vented through a closed-vent system to a non-flare control device, then the owner or operator must keep records of all periods during which operating values are outside of the applicable operating limits specified in § <u>63.124(b)(4)</u> through (<u>6)</u> when regulated material is being routed to the non-flare control device. The record must specify the identification of the control device, the operating parameter, the applicable limit, and the highest (for maximum operating limits) or lowest (for minimum operating limits) value recorded during the period.(m) For each maintenance vent opening subject to the requirements of § <u>63.113(k)</u>, owners and operators must keep the applicable records specified in <u>paragraphs</u> (m)(1) through (<u>5</u>) of this section.

(1) Owners and operators must maintain standard site procedures used to deinventory equipment for safety purposes (*e.g.*, hot work or vessel entry procedures) to document the procedures used to meet the requirements in  $\frac{63.113(k)}{1000}$ . The current copy of the procedures must be retained and available on-site at all times. Previous versions of the standard site procedures, as applicable, must be retained for 5 years.

(2) If complying with the requirements of  $\frac{63.113(k)(1)(i)}{63.113(k)(1)(i)}$ , and the concentration of the vapor at the time of the vessel opening exceeds 10 percent of its LEL, identification of the maintenance vent, the process units or equipment associated with the maintenance vent, the date of maintenance vent opening, and the concentration of the vapor at the time of the vessel opening.

(3) If complying with the requirements of  $\frac{63.113(k)(1)(ii)}{(1)}$ , and either the vessel pressure at the time of the vessel opening exceeds 5 psig or the concentration of the vapor at the time of the active purging was initiated exceeds 10 percent of its LEL, identification of the maintenance vent, the process units or equipment associated with the maintenance vent, the date of maintenance vent opening, the pressure of the vessel or equipment at the time of discharge to the atmosphere and, if applicable, the concentration of the vapors in the equipment when active purging was initiated.

(4) If complying with the requirements of  $\frac{6}{5}$  63.113(k)(1)(iii), records of the estimating procedures used to determine the total quantity of VOC in the equipment and the type and size limits of equipment that contain less than 50 pounds of VOC at the time of maintenance vent opening. For each maintenance vent opening that contains greater than 50 pounds of VOC for which the deinventory procedures specified in paragraph (m)(1) of this section are not followed or for which the equipment opened exceeds the type and size limits established in the records specified in this paragraph (m)(4), records that identify the maintenance vent, the process units or equipment associated with the maintenance vent, the date of maintenance vent opening, and records used to estimate the total quantity of VOC in the equipment at the time the maintenance vent was opened to the atmosphere.

(5) If complying with the requirements of  $\frac{6.3.113(k)(1)(iv)}{(iv)}$ , identification of the maintenance vent, the process units or equipment associated with the maintenance vent, records documenting actions taken to comply with other applicable alternatives and why utilization of this alternative was required, the date of maintenance vent opening, the equipment pressure and concentration of the vapors in the equipment at the time of discharge, an indication of whether active purging was performed and the pressure of the equipment during the installation or removal of the blind if active purging was used, the duration the maintenance vent was open during the blind installation or removal process, and records used to estimate the total quantity of VOC in the equipment at the time the maintenance vent was opened to the atmosphere for each applicable maintenance vent opening.

(n) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraphs (d) and (e) of this section no longer apply. Instead, each owner or operator demonstrating that a process vent is a Group 2 process vent based on total organic HAP mass flow rate less than 1.0 pound per hour under § 63.113(1), shall keep up-to-date, readily accessible records of:

(1) Any process changes that increase the vent stream mass flow rate, and

(2) Any recalculation or measurement of the mass flow rate pursuant to  $\frac{63.115(g)}{2}$ .

[<u>89 FR 43185</u>, May 16, 2024]

# § 63.119 Storage vessel provisions—reference control technology.

(a) For each storage vessel to which this subpart applies, the owner or operator shall comply with the requirements of <u>paragraphs (a)(1)</u> through (6) of this section according to the schedule provisions of § 63.100. For each pressure vessel to which this subpart applies, the owner or operator must comply with the requirements of <u>paragraph (a)(7)</u> of this section.

(1) For each Group 1 storage vessel (as defined in table 5 of this subpart for existing sources and table 6 of the subpart for new sources) storing a liquid for which the maximum true vapor pressure of the total organic hazardous air pollutants in the liquid is less than 76.6 kilopascals, the owner or operator shall reduce hazardous air pollutants emissions to the atmosphere either by operating and maintaining a fixed roof and internal floating roof, an external floating roof, an external floating roof converted to an internal floating roof, a closed vent system and control device, routing the emissions to a process or a fuel gas system, or vapor balancing in accordance with the requirements in paragraph (b), (c), (d), (e), (f), or (g) of this section, or equivalent as provided in  $\S$  63.121 of this subpart.

(2) For each Group 1 storage vessel (as defined in table 5 of this subpart for existing sources and table 6 of this subpart for new sources) storing a liquid for which the maximum true vapor pressure of the total organic hazardous air pollutants in the liquid is greater than or equal to 76.6 kilopascals, the owner or operator shall operate and maintain a closed vent system and control device meeting the requirements specified in <u>paragraph (e)</u> of this section, route the emissions to a process or a fuel gas system as specified in <u>paragraph (f)</u> of this section, vapor balance as specified in <u>paragraph (g)</u> of this section, or equivalent as provided in § 63.121 of this subpart.

(3) For each Group 2 storage vessel that is not part of an emissions average as described in § 63.150 of this subpart, the owner or operator shall comply with the recordkeeping requirement in § 63.123(a) of this subpart and is not required to comply with any other provisions in §§ 63.119 through 63.123 of this subpart.

(4) For each Group 2 storage vessel that is part of an emissions average, the owner or operator shall comply with the emissions averaging provisions in  $\frac{63.150 \text{ of this subpart}}{1000 \text{ of this subpart}}$ .

(5) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(11), if the storage vessel (of any capacity and vapor pressure) stores liquid containing ethylene oxide such that the storage vessel is considered to be in ethylene oxide service, as defined in § 63.101, then the owner or operator must comply with the requirements of paragraph (a)(5)(i) or (ii) of this section in addition to all other applicable requirements specified elsewhere in this section.

(i) Reduce emissions of ethylene oxide by venting emissions through a closed vent system to a flare; or

(ii) Reduce emissions of ethylene oxide by venting emissions through a closed vent system to a control device that reduces ethylene oxide by greater than or equal to 99.9 percent by weight, or to a concentration less than 1 ppmv for each storage vessel vent.

(6) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), for each storage vessel subject to paragraph (a)(1), (2), or (5) of this section, the owner or operator must comply with paragraphs (a)(6)(i) through (iv) of this section during storage vessel shutdown operations (*i.e.*, emptying and degassing of a storage vessel) until the vapor space concentration in the storage vessel is less than 10 percent of the LEL, or the organic HAP concentration in the vapor space is equal to or less than of 5,000 ppmv as methane. The owner or operator must determine the concentration using process instrumentation or portable measurement devices and follow procedures for calibration and maintenance according to manufacturer's specifications. The owner or operator must determine the organic HAP concentration using Method 18 or Method 25A of appendix A to part 60 of this chapter; or alternatively, any other method or data that has been validated according to the protocol in Method 301 of appendix A of this part.

(i) Remove liquids from the storage vessel as much as practicable.

(ii) Comply with one of the following:

(A) Reduce emissions of total organic HAP by venting emissions through a closed vent system to a flare.

(B) Reduce emissions of total organic HAP by 95 weight-percent by venting emissions through a closed vent system to any combination of non-flare control devices.

(C) Reduce emissions of total organic HAP by routing emissions to a fuel gas system or process and meet the requirements specified in <u>paragraph (f)</u> of this section.

(iii) Maintain records necessary to demonstrate compliance with the requirements in  $\S$  63.102(f) of subpart F of this part including, if appropriate, records of existing standard site procedures used to empty and degas (deinventory) equipment for safety purposes.

(iv) For floating roof storage vessels, the storage vessel may be opened to set up equipment (*e.g.*, making connections to a temporary control device) for the shutdown operations but must not be actively degassed during this time period.

(7) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), for each pressure vessel as defined in § 63.101 that is considered a Group 1 storage vessel (as defined in table 5 of this subpart for existing sources and table 6 of the subpart for new sources), you must operate and maintain the pressure vessel, as specified in paragraphs (a)(7)(i) through (v) of this section.

(i) The pressure vessel must be designed to operate with no detectable emissions at all times.

(ii) Except for connectors in ethylene oxide service, gas/vapor or light liquid valves in ethylene oxide service, light liquid pumps in ethylene oxide service, and PRDs in ethylene oxide service, and except for equipment that meet the criteria specified in  $\S$  63.168(h) and (i) (for valves in gas/vapor service and in light liquid service) and in  $\S$  63.174(f) and (h) (for connectors in gas/vapor service and in light liquid service), you must monitor each point on the pressure vessel through which total organic hazardous air pollutants could potentially be emitted by conducting initial and annual performance tests using Method 21 of appendix A-7 to part 60 of this chapter

(iii) Each instrument reading greater than 500 ppmv is a violation.

(iv) Estimate the flow rate and total regulated material emissions from the defect. Assume the pressure vessel has been emitting for half of the time since the last performance test, unless other information supports a different assumption.

(v) Whenever total organic hazardous air pollutants are in the pressure vessel, you must operate the pressure vessel as a closed system that vents through a closed vent system to a control device as specified in <u>paragraph (e)</u> of this section, as applicable. For purposes of compliance with this paragraph, a release of total organic hazardous air pollutants through a pressure vessel's pressure relief device to the atmosphere is a violation.

(b) The owner or operator who elects to use a fixed roof and an internal floating roof, as defined in § 63.111, to comply with the requirements of paragraph (a)(1) of this section shall comply with the requirements specified in paragraphs (b)(1) through (7) of this section.

Note:

The intent of <u>paragraphs (b)(1)</u> and (2) of this section is to avoid having a vapor space between the floating roof and the stored liquid for extended periods. Storage vessels may be emptied for purposes such as routine storage vessel maintenance, inspections, petroleum liquid deliveries, or transfer operations. Storage vessels where liquid is left on walls, as bottom clingage, or in pools due to floor irregularity are considered completely empty.

(1) The internal floating roof shall be floating on the liquid surface at all times except when the floating roof must be supported by the leg supports during the periods specified in <u>paragraphs (b)(1)(i)</u> through  $(\underline{b})(1)(\underline{ii})$  of this section.

(i) During the initial fill.

(ii) After the vessel has been completely emptied and degassed.

(iii) When the vessel is completely emptied before being subsequently refilled.

(2) When the floating roof is resting on the leg supports, the process of filling, emptying, or refilling shall be continuous and shall be accomplished as soon as practical.

(3) Each internal floating roof shall be equipped with a closure device between the wall of the storage vessel and the roof edge. Except as provided in paragraph (b)(3)(iv) of this section, the closure device shall consist of one of the devices listed in paragraph (b)(3)(i), (b)(3)(ii), or (b)(3)(iii) of this section.

(i) A liquid-mounted seal as defined in  $\S$  63.111 of this subpart.

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(ii) A metallic shoe seal as defined in § 63.111 of this subpart.

(iii) Two seals mounted one above the other so that each forms a continuous closure that completely covers the space between the wall of the storage vessel and the edge of the internal floating roof. The lower seal may be vapor- mounted, but both must be continuous seals.

(iv) If the internal floating roof is equipped with a vapor-mounted seal as of December 31, 1992, the requirement for one of the seal options specified in <u>paragraphs (b)(3)(i)</u>, (b)(3)(ii), and (b)(3)(iii) of this section does not apply until the earlier of the dates specified in <u>paragraphs (b)(3)(iv)(A)</u> and (b)(3)(iv)(B) of this section.

(A) The next time the storage vessel is emptied and degassed.

(B) No later than 10 years after April 22, 1994.

(4) Automatic bleeder vents are to be closed at all times when the roof is floating, except when the roof is being floated off or is being landed on the roof leg supports.

(5) Except as provided in <u>paragraph (b)(5)(viii)</u> of this section, each internal floating roof shall meet the specifications listed in <u>paragraphs (b)(5)(i)</u> through (vii) of this section, and (b)(5)(ix) through (xii) of this section.

(i) Each opening in a noncontact internal floating roof except for automatic bleeder vents (vacuum breaker vents) and rim space vents is to provide a projection below the liquid surface.

(ii) Except as specified in <u>paragraph (b)(5)(ix)</u> of this section, each opening in the internal floating roof except for leg sleeves, automatic bleeder vents, rim space vents, column wells, ladder wells, sample wells, and stub drains shall be equipped with a cover or lid. The cover or lid shall be equipped with a gasket.

(iii) Each penetration of the internal floating roof for the purposes of sampling shall be a sample well. Each sample well shall have a slit fabric cover that covers at least 90 percent of the opening.

(iv) Each automatic bleeder vent shall be gasketed.

(v) Each rim space vent shall be gasketed.

(vi) Each penetration of the internal floating roof that allows for passage of a ladder shall have a gasketed sliding cover.

(vii) Each penetration of the internal floating roof that allows for passage of a column supporting the fixed roof shall have a flexible fabric sleeve seal or a gasketed sliding cover.

(viii) If the internal floating roof does not meet any one of the specifications listed in <u>paragraphs</u> (b)(5)(i) through (b)(5)(vii) of this section as of December 31, 1992, the requirement for meeting those specifications does not apply until the earlier of the dates specified in <u>paragraphs</u> (b)(5)(viii)(A) and (b)(5)(viii)(B) of this section.

(A) The next time the storage vessel is emptied and degassed.

(B) No later than 10 years after April 22, 1994.

(ix) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraph (b)(5)(i) of this section no longer applies. Instead, each opening in the internal floating roof except those for automatic bleeder vents (vacuum breaker vents), rim space vents, leg sleeves, and deck drains shall be equipped with a deck cover. The deck cover shall be equipped with a gasket between the cover and the deck.

(x) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$  63.100(k)(10), each opening for an unslotted guidepole shall be equipped with a pole wiper, and each unslotted guidepole shall be equipped with a gasketed cap on the top of the guidepole.

(xi) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), each opening for a slotted guidepole shall be equipped with one of the control device configurations specified in <u>paragraphs</u> (b)(5)(xi)(A) and (B) of this section.

(A) A pole wiper and a pole float. The wiper or seal of the pole float shall be at or above the height of the pole wiper.

(B) A pole wiper and a pole sleeve.

(xii) Each unslotted guidepole cap shall be closed at all times except when gauging the liquid level or taking liquid samples.

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(6) Each cover or lid on any opening in the internal floating roof shall be closed (i.e., no visible gaps), except when the cover or lid must be open for access. Covers on each access hatch and each gauge float well shall be bolted or fastened so as to be air-tight when they are closed. Rim space vents are to be set to open only when the internal floating roof is not floating or when the pressure beneath the rim seal exceeds the manufacturer's recommended setting.

(7) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), owners and operators that use a continuous sweep, purge, or inert blanket between the internal floating roof and fixed roof that causes a pressure/vacuum vent to remain continuously open to the atmosphere where uncontrolled emissions are greater than or equal to 1.0 pound per hour of total organic HAP must route emissions through a closed vent system and control device and comply with paragraph (e) of this section.

(c) The owner or operator who elects to use an external floating roof, as defined in § 63.111 of this subpart, to comply with the requirements of paragraph (a)(1) of this section shall comply with the requirements specified in paragraphs (c)(1) through (c)(4) of this section.

(1) Each external floating roof shall be equipped with a closure device between the wall of the storage vessel and the roof edge.

(i) Except as provided in <u>paragraph (c)(1)(iv)</u> of this section, the closure device is to consist of two seals, one above the other. The lower seal is referred to as the primary seal and the upper seal is referred to as the secondary seal.

(ii) Except as provided in <u>paragraph (c)(1)(v)</u> of this section, the primary seal shall be either a metallic shoe seal or a liquid-mounted seal.

(iii) Except during the inspections required by  $\S$  63.120(b) of this subpart, both the primary seal and the secondary seal shall completely cover the annular space between the external floating roof and the wall of the storage vessel in a continuous fashion.

(iv) If the external floating roof is equipped with a liquid-mounted or metallic shoe primary seal as of December 31, 1992, the requirement for a secondary seal in <u>paragraph (c)(1)(i)</u> of this section does not apply until the earlier of the dates specified in <u>paragraphs (c)(1)(iv)(A)</u> and (c)(1)(iv)(B) of this section.

(A) The next time the storage vessel is emptied and degassed.

(B) No later than 10 years after April 22, 1994.

(v) If the external floating roof is equipped with a vapor-mounted primary seal and a secondary seal as of December 31, 1992, the requirement for a liquid-mounted or metallic shoe primary seal in <u>paragraph (c)(1)(ii)</u> of this section does not apply until the earlier of the dates specified in <u>paragraphs (c)(1)(v)(A)</u> and (c)(1)(v)(B) of this section.

(A) The next time the storage vessel is emptied and degassed.

(B) No later than 10 years after April 22, 1994.

(2) Each external floating roof shall meet the specifications listed in <u>paragraphs (c)(2)(i)</u> through (c)(2)(xii) of this section.

(i) Except for automatic bleeder vents (vacuum breaker vents) and rim space vents, each opening in the noncontact external floating roof shall provide a projection below the liquid surface except as provided in paragraph (c)(2)(xii) of this section.

(ii) Except for automatic bleeder vents, rim space vents, roof drains, and leg sleeves, each opening in the roof is to be equipped with a gasketed cover, seal or lid which is to be maintained in a closed position (i.e., no visible gap) at all times except when the cover or lid must be open for access. Covers on each access hatch and each gauge float well shall be bolted or fastened so as to be air-tight when they are closed.

(iii) Automatic bleeder vents are to be closed at all times when the roof is floating, except when the roof is being floated off or is being landed on the roof leg supports.

(iv) Rim space vents are to be set to open only when the roof is being floated off the roof leg supports or when the pressure beneath the rim seal exceeds the manufacturer's recommended setting.

(v) Automatic bleeder vents and rim space vents are to be gasketed.

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(vi) Each roof drain that empties into the stored liquid is to be provided with a slotted membrane fabric cover that covers at least 90 percent of the area of the opening.

(vii) Each unslotted guide pole well shall have a gasketed sliding cover or a flexible fabric sleeve seal.

(viii) Each unslotted guide pole shall have on the end of the pole a gasketed cap which is closed at all times except when gauging the liquid level or taking liquid samples.

(ix) Each slotted guide pole well shall have a gasketed sliding cover or a flexible fabric sleeve seal.

(x) Each slotted guide pole shall have a gasketed float or other device which closes off the liquid surface from the atmosphere.

(xi) Each gauge hatch/sample well shall have a gasketed cover which is closed at all times except when the hatch or well must be open for access.

(xii) If each opening in a noncontact external floating roof except for automatic bleeder vents (vacuum breaker vents) and rim space vents does not provide a projection below the liquid surface as of December 31, 1992, the requirement for providing these projections below the liquid surface does not apply until the earlier of the dates specified in <u>paragraphs</u> (c)(2)(xii)(A) and (c)(2)(xii)(B) of this section.

(A) The next time the storage vessel is emptied and degassed.

(B) No later than 10 years after April 22, 1994.

Note:

The intent of <u>paragraphs (c)(3)</u> and (c)(4) of this section is to avoid having a vapor space between the floating roof and the stored liquid for extended periods. Storage vessels may be emptied for purposes such as routine storage vessel maintenance, inspections, petroleum liquid deliveries, or transfer operations. Storage vessels where liquid is left on walls, as bottom clingage, or in pools due to floor irregularity are considered completely empty.

(3) The external floating roof shall be floating on the liquid surface at all times except when the floating roof must be supported by the leg supports during the periods specified in <u>paragraphs (c)(3)(i)</u> through (c)(3)(iii) of this section.

(i) During the initial fill.

(ii) After the vessel has been completely emptied and degassed.

(iii) When the vessel is completely emptied before being subsequently refilled.

(4) When the floating roof is resting on the leg supports, the process of filling, emptying, or refilling shall be continuous and shall be accomplished as soon as practical.

(d) The owner or operator who elects to use an external floating roof converted to an internal floating roof (i.e., fixed roof installed above external floating roof) to comply with <u>paragraph (a)(1)</u> of this section shall comply with <u>paragraphs</u> (d)(1) and (d)(2) of this section.

(1) Comply with the requirements for internal floating roof vessels specified in <u>paragraphs (b)(1)</u>, (2), and (3) of this section; and

(2) Comply with the requirements for deck fittings that are specified for external floating roof vessels in <u>paragraphs</u> (c)(2)(i) through (c)(2)(xii) of this section.

(e) The owner or operator who elects to use a closed vent system and control device, as defined in § 63.111, to comply with the requirements of paragraph (a)(1) or (2) of this section, or the owner or operator who meets the requirements specified in paragraph (b)(7) of this section, shall comply with the requirements specified in paragraphs (e)(1) through (7) of this section.

(1) Except as provided in <u>paragraph (e)(2)</u> of this section, the control device shall be designed and operated to reduce inlet emissions of total organic HAP by 95 percent or greater. Except as specified in  $\S$  63.108(a), if a flare is used as the control device, it shall meet the specifications described in the general control device requirements of  $\S$  63.11(b).

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(2) If the owner or operator can demonstrate that a control device installed on a storage vessel on or before December 31, 1992 is designed to reduce inlet emissions of total organic HAP by greater than or equal to 90 percent but less than 95 percent, then the control device is required to be operated to reduce inlet emissions of total organic HAP by 90 percent or greater.

(3) Except as specified in (e)(7) of this section, periods of planned routine maintenance of the control device, during which the control device does not meet the specifications of paragraph (e)(1) or (2) of this section, as applicable, shall not exceed 240 hours per year.

(4) Except as specified in (e)(7) of this section, the specifications and requirements in <u>paragraphs (e)(1)</u> and (2) of this section for control devices do not apply during periods of planned routine maintenance.

(5) Except as specified in (e)(7) of this section, the specifications and requirements in <u>paragraphs (e)(1)</u> and (2) of this section for control devices do not apply during a control system malfunction.

(6) An owner or operator may use a combination of control devices to achieve the required reduction of total organic hazardous air pollutants specified in paragraph (e)(1) of this section. An owner or operator may use a combination of control devices installed on a storage vessel on or before December 31, 1992 to achieve the required reduction of total organic hazardous air pollutants specified in paragraph (e)(2) of this section.

(7) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$ 

63.100(k)(10), paragraphs (e)(3) through (5) of this section no longer apply. Instead, whenever gases or vapors containing total organic HAP are routed from a storage vessel through a closed vent system connected to a control device used to comply with the requirements of paragraph (e)(1) or (2) of this section, the control device must be operating, except the control device may only be bypassed for the purpose of performing planned routine maintenance of the control device. When the control device is bypassed, the owner or operator must comply with paragraphs (e)(7)(i) through (iii) of this section.

(i) The control device may only be bypassed when the planned routine maintenance cannot be performed during periods that storage vessel emissions are vented to the control device.

(ii) On an annual basis, the total time that the closed-vent system or control device is bypassed to perform planned routine maintenance shall not exceed 240 hours per each calendar year.

(iii) The level of material in the storage vessel shall not be increased during periods that the closed vent system or control device is bypassed to perform planned routine maintenance.

(f) The owner or operator who elects to route emissions to a fuel gas system or to a process, as defined in § 63.111 of this subpart, to comply with the requirements of paragraph (a)(1) or (a)(2) of this section shall comply with the requirements in paragraphs (f)(1) through (f)(3) of this section, as applicable.

(1) If emissions are routed to a fuel gas system, there is no requirement to conduct a performance test or design evaluation. If emissions are routed to a process, the organic hazardous air pollutants in the emissions shall predominantly meet one of, or a combination of, the ends specified in paragraphs (f)(1)(i) through (f)(1)(iv) of this section. The owner or operator shall comply with the compliance demonstration requirements in § 63.120(f).

(i) Recycled and/or consumed in the same manner as a material that fulfills the same function in that process;

(ii) Transformed by chemical reaction into materials that are not organic hazardous air pollutants;

(iii) Incorporated into a product; and/or

(iv) Recovered.

(2) If the emissions are conveyed by a system other than hard-piping, any conveyance system operated under positive pressure shall be subject to the requirements of  $\frac{63.148}{5}$  of this subpart.

(3) The fuel gas system or process shall be operating at all times when organic hazardous air pollutants emissions are routed to it except as provided in  $\S$  63.102(a)(1) and in paragraphs (f)(3)(i) through (iv) of this section. Whenever the owner or operator bypasses the fuel gas system or process, the owner or operator shall comply with the recordkeeping requirement in  $\S$  63.123(h). Bypassing is permitted if the owner or operator complies with one or more of the conditions specified in paragraphs (f)(3)(i) through (iv) of this section.
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(i) The liquid level in the storage vessel is not increased;

(ii) The emissions are routed through a closed vent system to a control device complying with § 63.119(e); or

(iii) Except as specified in <u>paragraph (f)(3)(iv)</u> of this section, the total aggregate amount of time during which the emissions bypass the fuel gas system or process during the calendar year without being routed to a control device, for all reasons (except start-ups/shutdowns/malfunctions or product changeovers of flexible operation units and periods when the storage vessel has been emptied and degassed), does not exceed 240 hours.

(iv) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$ 

63.100(k)(10), paragraph (f)(3)(iii) of this section no longer applies. Instead, if you elect to route emissions from storage vessels to a fuel gas system or to a process to comply with the requirements of paragraph (a)(1), (2), or (5) of this section, the fuel gas system or process may only be bypassed when the planned routine maintenance cannot be performed during periods that storage vessel emissions are vented to the fuel gas system or process, and the total aggregate amount of time during which the breathing loss emissions bypass the fuel gas system or process during the calendar year without being routed to a control device must not exceed 240 hours. The level of material in the storage vessel shall not be increased during periods that the fuel gas system or process is bypassed to perform routine maintenance.

(g) The owner or operator who elects to vapor balance to comply with the requirements of <u>paragraphs (a)(1)</u> and (2) of this section shall comply with <u>paragraphs (g)(1)</u> through (7) of this section and the recordkeeping requirements of § 63.123(i).

(1) The vapor balancing system must be designed and operated to route organic HAP vapors displaced from loading of the storage vessel to the railcar, tank truck, or barge from which the storage vessel is filled.

(2) Tank trucks and railcars must have a current certification in accordance with the U.S. Department of Transportation pressure test requirements of  $\underline{49 \text{ CFR part } 180}$  for tank trucks and  $\underline{49 \text{ CFR } 173.31}$  for railcars. Barges must have a current certification of vapor-tightness through testing in accordance with  $\underline{40 \text{ CFR } 63.565}$ .

(3) Hazardous air pollutants must only be unloaded from tank trucks or railcars when vapor collection systems are connected to the storage vessel's vapor collection system.

(4) No pressure relief device on the storage vessel, or on the railcar or tank truck, shall open during loading or as a result of diurnal temperature changes (breathing losses).

(5) Pressure relief devices must be set to no less than 2.5 psig at all times to prevent breathing losses. Pressure relief devices may be set at values less than 2.5 psig if the owner or operator provides rationale in the notification of compliance status report explaining why the alternative value is sufficient to prevent breathing losses at all times. The owner or operator shall comply with paragraphs (g)(5)(i) through (iii) of this section for each pressure relief valve.

(i) The pressure relief valve shall be monitored quarterly using the method described in  $\frac{63.180(b)}{5.180(b)}$ .

(ii) An instrument reading of 500 ppmv or greater defines a leak.

(iii) When a leak is detected, it shall be repaired as soon as practicable, but no later than 5 days after it is detected, and the owner or operator shall comply with the recordkeeping requirements of  $\frac{63.181(d)(1)}{10}$  through (4).

(6) Railcars, tank trucks, or barges that deliver HAP to a storage vessel must be reloaded or cleaned at a facility that utilizes the control techniques specified in paragraph (g)(6)(i) or (ii) of this section.

(i) The railcar, tank truck, or barge must be connected to a closed vent system with a control device that reduces inlet emissions of HAP by 95 percent by weight or greater.

(ii) A vapor balancing system designed and operated to collect organic HAP vapor displaced from the tank truck, railcar, or barge during reloading must be used to route the collected HAP vapor to the storage vessel from which the liquid being transferred originated.

(7) The owner or operator of the facility where the railcar, tank truck, or barge is reloaded or cleaned must comply with <u>paragraphs (g)(7)(i)</u> through <u>(iii)</u> of this section.

(i) Submit to the owner or operator of the storage vessel and to the Administrator a written certification that the reloading or cleaning facility will meet the requirements of this section. The certifying entity may revoke the written certification by

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sending a written statement to the owner or operator of the storage vessel giving at least 90 days notice that the certifying entity is rescinding acceptance of responsibility for compliance with the requirements of this paragraph (g)(7).

(ii) If complying with paragraph (g)(6)(i) of this section, comply with the requirements for closed vent system and control device specified in §§ 63.129 through 63.123. The notification and reporting requirements in § 63.122 do not apply to the owner or operator of the offsite cleaning or reloading facility.

(iii) If complying with <u>paragraph (g)(6)(ii)</u> of this section, keep the records specified in  $\S$  63.123(i)(3).

(iv) After the compliance dates specified in § 63.100(k) at an offsite reloading or cleaning facility subject to <u>paragraph (g)</u> of this section, compliance with the monitoring, recordkeeping, and reporting provisions of any other subpart of this part 63 constitutes compliance with the monitoring, recordkeeping, and reporting provisions of <u>paragraph (g)(7)(ii)</u> or <u>(iii)</u> of this section. You must identify in your Notification of Compliance Status report required by § 63.152(b), the subpart to the part 63 with which the owner or operator of the reloading or cleaning facility complies.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>62 FR 2747</u>, Jan. 17, 1997; <u>69 FR 76863</u>, Dec. 23, 2004; <u>71 FR 76614</u>, Dec. 21, 2006; <u>89 FR 43188</u>, May 16, 2024]

#### § 63.120 Storage vessel provisions—procedures to determine compliance.

(a) To demonstrate compliance with § 63.119(b) of this subpart (storage vessel equipped with a fixed roof and internal floating roof) or with § 63.119(d) of this subpart (storage vessel equipped with an external floating roof converted to an internal floating roof), the owner or operator shall comply with the requirements in paragraphs (a)(1) through (a)(7) of this section.

(1) The owner or operator shall visually inspect the internal floating roof, the primary seal, and the secondary seal (if one is in service), according to the schedule specified in paragraphs (a)(2) and (a)(3) of this section.

(2) For vessels equipped with a single-seal system, the owner or operator shall perform the inspections specified in paragraphs (a)(2)(i) and (a)(2)(ii) of this section.

(i) Visually inspect the internal floating roof and the seal through manholes and roof hatches on the fixed roof at least once every 12 months after initial fill, or at least once every 12 months after the compliance date specified in § 63.100 of subpart F of this part.

(ii) Visually inspect the internal floating roof, the seal, gaskets, slotted membranes, and sleeve seals (if any) each time the storage vessel is emptied and degassed, and at least once every 10 years after the compliance date specified in  $\S$  <u>63.100</u> of <u>subpart F of this part</u>.

(3) For vessels equipped with a double-seal system as specified in  $\S 63.119(b)(3)(iii)$  of this subpart, the owner or operator shall perform either the inspection required in paragraph (a)(3)(i) of this section or the inspections required in both paragraphs (a)(3)(ii) and (a)(3)(iii) of this section.

(i) The owner or operator shall visually inspect the internal floating roof, the primary seal, the secondary seal, gaskets, slotted membranes, and sleeve seals (if any) each time the storage vessel is emptied and degassed and at least once every 5 years after the compliance date specified in  $\S$  63.100 of subpart F of this part; or

(ii) The owner or operator shall visually inspect the internal floating roof and the secondary seal through manholes and roof hatches on the fixed roof at least once every 12 months after initial fill, or at least once every 12 months after the compliance date specified in  $\S$  63.100 of subpart F of this part, and

(iii) Visually inspect the internal floating roof, the primary seal, the secondary seal, gaskets, slotted membranes, and sleeve seals (if any) each time the vessel is emptied and degassed and at least once every 10 years after the compliance date specified in  $\frac{8}{50.100}$  of subpart F of this part.

(4) If during the inspections required by paragraph (a)(2)(i) or (a)(3)(ii) of this section, the internal floating roof is not resting on the surface of the liquid inside the storage vessel and is not resting on the leg supports; or there is liquid on the floating roof; or the seal is detached; or there are holes or tears in the seal fabric; or there are visible gaps between the seal and the wall of the storage vessel, the owner or operator shall repair the items or empty and remove the storage vessel from service within 45 calendar days. If a failure that is detected during inspections required by paragraph (a)(2)(i) or (a)(3)(ii) of this section cannot be repaired within 45 calendar days and if the vessel cannot be emptied within 45 calendar days, the owner or

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operator may utilize up to 2 extensions of up to 30 additional calendar days each. Documentation of a decision to utilize an extension shall include a description of the failure, shall document that alternate storage capacity is unavailable, and shall specify a schedule of actions that will ensure that the control equipment will be repaired or the vessel will be emptied as soon as practical.

(5) Except as provided in <u>paragraph (a)(6)</u> of this section, for all the inspections required by <u>paragraphs (a)(2)(ii)</u>, (a)(3)(i), and (a)(3)(iii) of this section, the owner or operator shall notify the Administrator in writing at least 30 calendar days prior to the refilling of each storage vessel to afford the Administrator the opportunity to have an observer present.

(6) If the inspection required by paragraph (a)(2)(ii), (a)(3)(i), or (a)(3)(iii) of this section is not planned and the owner or operator could not have known about the inspection 30 calendar days in advance of refilling the vessel, the owner or operator shall notify the Administrator at least 7 calendar days prior to the refilling of the storage vessel. Notification may be made by telephone and immediately followed by written documentation demonstrating why the inspection was unplanned. Alternatively, the notification including the written documentation may be made in writing and sent so that it is received by the Administrator at least 7 calendar days prior to refilling.

(7) If during the inspections required by <u>paragraph (a)(2)(ii)</u>, (a)(3)(i), or (a)(3)(ii) of this section, the internal floating roof has defects; or the primary seal has holes, tears, or other openings in the seal or the seal fabric; or the secondary seal has holes, tears, or other openings in the seal or the seal fabric; or the secondary seal has holes, tears, or other openings in the seal or the seal fabric; or the secondary seal has holes, tears, or other openings in the seal or the seal fabric; or the secondary seal has holes, tears, or other openings in the seal or the seal fabric; or the gaskets no longer close off the liquid surface from the atmosphere; or the slotted membrane has more than 10 percent open area, the owner or operator shall repair the items as necessary so that none of the conditions specified in this paragraph exist before refilling the storage vessel with organic HAP.

(b) To demonstrate compliance with  $\S$  63.119(c) of this subpart (storage vessel equipped with an external floating roof), the owner or operator shall comply with the requirements specified in paragraphs (b)(1) through (b)(10) of this section.

(1) Except as provided in <u>paragraph (b)(7)</u> of this section, the owner or operator shall determine the gap areas and maximum gap widths between the primary seal and the wall of the storage vessel, and the secondary seal and the wall of the storage vessel according to the frequency specified in <u>paragraphs (b)(1)(i)</u> through (b)(1)(ii) of this section.

(i) For an external floating roof vessel equipped with primary and secondary seals, measurements of gaps between the vessel wall and the primary seal shall be performed during the hydrostatic testing of the vessel or by the compliance date specified in  $\S$  63.100 of subpart F of this part, whichever occurs last, and at least once every 5 years thereafter.

(ii) For an external floating roof vessel equipped with a liquid-mounted or metallic shoe primary seal and without a secondary seal as provided for in § 63.119(c)(1)(iv) of this subpart, measurements of gaps between the vessel wall and the primary seal shall be performed by the compliance date specified in § 63.100 of subpart F of this part and at least once per year thereafter, until a secondary seal is installed. When a secondary seal is installed above the primary seal, measurements of gaps between the vessel wall and both the primary and secondary seals shall be performed within 90 calendar days of installation of the secondary seal, and according to the frequency specified in paragraphs (b)(1)(i) and (b)(1)(iii) of this section thereafter.

(iii) For an external floating roof vessel equipped with primary and secondary seals, measurements of gaps between the vessel wall and the secondary seal shall be performed by the compliance date specified in  $\S$  63.100 of subpart F of this part and at least once per year thereafter.

(iv) If any storage vessel ceases to store organic HAP for a period of 1 year or more, or if the maximum true vapor pressure of the total organic HAP's in the stored liquid falls below the values defining Group 1 storage vessels specified in table 5 or table 6 of this subpart for a period of 1 year or more, measurements of gaps between the vessel wall and the primary seal, and gaps between the vessel wall and the secondary seal shall be performed within 90 calendar days of the vessel being refilled with organic HAP.

(2) Except as provided in <u>paragraph (b)(7)</u> of this section, the owner or operator shall determine gap widths and gap areas in the primary and secondary seals (seal gaps) individually by the procedures described in <u>paragraphs</u> (b)(2)(i) through (b)(2)(iii) of this section.

(i) Seal gaps, if any, shall be measured at one or more floating roof levels when the roof is not resting on the roof leg supports.

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(ii) Seal gaps, if any, shall be measured around the entire circumference of the vessel in each place where an 0.32 centimeter (1/8 inch) diameter uniform probe passes freely (without forcing or binding against the seal) between the seal and the wall of the storage vessel. The circumferential distance of each such location shall also be measured.

(iii) The total surface area of each gap described in <u>paragraph (b)(2)(ii)</u> of this section shall be determined by using probes of various widths to measure accurately the actual distance from the vessel wall to the seal and multiplying each such width by its respective circumferential distance.

(3) The owner or operator shall add the gap surface area of each gap location for the primary seal and divide the sum by the nominal diameter of the vessel. The accumulated area of gaps between the vessel wall and the primary seal shall not exceed 212 square centimeters per meter of vessel diameter and the width of any portion of any gap shall not exceed 3.81 centimeters.

(4) The owner or operator shall add the gap surface area of each gap location for the secondary seal and divide the sum by the nominal diameter of the vessel. The accumulated area of gaps between the vessel wall and the secondary seal shall not exceed 21.2 square centimeters per meter of vessel diameter and the width of any portion of any gap shall not exceed 1.27 centimeters. These seal gap requirements may be exceeded during the measurement of primary seal gaps as required by paragraph (b)(1)(i) and (b)(1)(ii) of this section.

(5) The primary seal shall meet the additional requirements specified in <u>paragraphs (b)(5)(i)</u> and <u>(b)(5)(ii)</u> of this section.

(i) Where a metallic shoe seal is in use, one end of the metallic shoe shall extend into the stored liquid and the other end shall extend a minimum vertical distance of 61 centimeters above the stored liquid surface.

(ii) There shall be no holes, tears, or other openings in the shoe, seal fabric, or seal envelope.

(6) The secondary seal shall meet the additional requirements specified in <u>paragraphs (b)(6)(i)</u> and <u>(b)(6)(ii)</u> of this section.

(i) The secondary seal shall be installed above the primary seal so that it completely covers the space between the roof edge and the vessel wall except as provided in paragraph (b)(4) of this section.

(ii) There shall be no holes, tears, or other openings in the seal or seal fabric.

(7) If the owner or operator determines that it is unsafe to perform the seal gap measurements required in <u>paragraphs</u> (b)(1) and (b)(2) of this section or to inspect the vessel to determine compliance with <u>paragraphs</u> (b)(5) and (b)(6) of this section because the floating roof appears to be structurally unsound and poses an imminent or potential danger to inspecting personnel, the owner or operator shall comply with the requirements in either <u>paragraph</u> (b)(7)(i) or (b)(7)(ii) of this section.

(i) The owner or operator shall measure the seal gaps or inspect the storage vessel no later than 30 calendar days after the determination that the roof is unsafe, or

(ii) The owner or operator shall empty and remove the storage vessel from service no later than 45 calendar days after determining that the roof is unsafe. If the vessel cannot be emptied within 45 calendar days, the owner or operator may utilize up to 2 extensions of up to 30 additional calendar days each. Documentation of a decision to utilize an extension shall include an explanation of why it was unsafe to perform the inspection or seal gap measurement, shall document that alternate storage capacity is unavailable, and shall specify a schedule of actions that will ensure that the vessel will be emptied as soon as practical.

(8) The owner or operator shall repair conditions that do not meet requirements listed in <u>paragraphs (b)(3)</u>, (b)(4), (b)(5), and (b)(6) of this section (i.e., failures) no later than 45 calendar days after identification, or shall empty and remove the storage vessel from service no later than 45 calendar days after identification. If during seal gap measurements required in <u>paragraph (b)(1)</u> and (b)(2) of this section or during inspections necessary to determine compliance with <u>paragraphs</u> (b)(5) and (b)(6) of this section a failure is detected that cannot be repaired within 45 calendar days and if the vessel cannot be emptied within 45 calendar days, the owner or operator may utilize up to 2 extensions of up to 30 additional calendar days each. Documentation of a decision to utilize an extension shall include a description of the failure, shall document that alternate storage capacity is unavailable, and shall specify a schedule of actions that will ensure that the control equipment will be repaired or the vessel will be emptied as soon as practical.

(9) The owner or operator shall notify the Administrator in writing at least 30 calendar days in advance of any gap measurements required by <u>paragraph (b)(1)</u> or (2) of this section to afford the Administrator the opportunity to have an observer present.

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(10) The owner or operator shall visually inspect the external floating roof, the primary seal, secondary seal, and fittings each time the vessel is emptied and degassed.

(i) If the external floating roof has defects; the primary seal has holes, tears, or other openings in the seal or the seal fabric; or the secondary seal has holes, tears, or other openings in the seal or the seal fabric; or the gaskets no longer close off the liquid surface from the atmosphere; or the slotted membrane has more than 10 percent open area, the owner or operator shall repair the items as necessary so that none of the conditions specified in this paragraph exist before filling or refilling the storage vessel with organic HAP.

(ii) Except as provided in <u>paragraph (b)(10)(iii)</u> of this section, for all the inspections required by <u>paragraph (b)(10)</u> of this section, the owner or operator shall notify the Administrator in writing at least 30 calendar days prior to filling or refilling of each storage vessel with organic HAP to afford the Administrator the opportunity to inspect the storage vessel prior to refilling.

(iii) If the inspection required by <u>paragraph (b)(10)</u> of this section is not planned and the owner or operator could not have known about the inspection 30 calendar days in advance of refilling the vessel with organic HAP, the owner or operator shall notify the Administrator at least 7 calendar days prior to refilling of the storage vessel. Notification may be made by telephone and immediately followed by written documentation demonstrating why the inspection was unplanned. Alternatively, this notification including the written documentation may be made in writing and sent so that it is received by the Administrator at least 7 calendar days prior to the refilling.

(c) To demonstrate compliance with  $\S$  63.119(d) of this subpart (storage vessel equipped with an external floating roof converted to an internal floating roof), the owner or operator shall comply with the requirements of paragraph (a) of this section.

(d) To demonstrate compliance with § 63.119(e) (storage vessel equipped with a closed vent system and control device) using a control device other than a flare, the owner or operator shall comply with the requirements in <u>paragraphs</u> (d)(1) through (7) of this section, except as provided in <u>paragraphs</u> (d)(8) and (9) of this section.

(1) Except as provided in <u>paragraph (d)(1)(iii)</u> of this section, the owner or operator shall either prepare a design evaluation, which includes the information specified in <u>paragraph (d)(1)(i)</u> of this section or submit the results of a performance test as described in <u>paragraph (d)(1)(ii)</u> of this section.

(i) The design evaluation shall include documentation demonstrating that the control device being used achieves the required control efficiency during reasonably expected maximum filling rate. This documentation is to include a description of the gas stream which enters the control device, including flow and organic HAP content under varying liquid level conditions, and the information specified in paragraphs (d)(1)(i)(A) through (E) of this section, as applicable.

(A) If the control device receives vapors, gases or liquids, other than fuels, from emission points other than storage vessels subject to this subpart, the efficiency demonstration is to include consideration of all vapors, gases, and liquids, other than fuels, received by the control device.

(B) If an enclosed combustion device with a minimum residence time of 0.5 seconds and a minimum temperature of 760 °C is used to meet the emission reduction requirement specified in § 63.119 (e)(1) or (2), as applicable, documentation that those conditions exist is sufficient to meet the requirements of paragraph (d)(1)(i) of this section.

(C) Except as provided in <u>paragraph (d)(1)(i)(B)</u> of this section, for thermal incinerators, the design evaluation shall include the autoignition temperature of the organic HAP, the flow rate of the organic HAP emission stream, the combustion temperature, and the residence time at the combustion temperature.

(D) For carbon adsorbers, the design evaluation shall include the affinity of the organic HAP vapors for carbon, the amount of carbon in each bed, the number of beds, the humidity of the feed gases, the temperature of the feed gases, the flow rate of the organic HAP emission stream, the desorption schedule, the regeneration stream pressure or temperature, and the flow rate of the regeneration stream. For vacuum desorption, pressure drop shall be included.

(E) For condensers, the design evaluation shall include the final temperature of the organic HAP vapors, the type of condenser, and the design flow rate of the organic HAP emission stream.

(ii) If the control device used to comply with  $\S 63.119(e)$  is also used to comply with  $\S 63.113(a)(2)$ ,  $\S 63.126(b)(1)$ , or  $\S 63.139(c)$ , the performance test required by  $\S 63.116(c)$ ,  $\S 63.128(a)$ , or  $\S 63.139(d)(1)$  is acceptable to demonstrate compliance with  $\S 63.119(e)$ . The owner or operator is not required to prepare a design evaluation for the control device as

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described in <u>paragraph (d)(1)(i)</u> of this section, if the performance tests meets the criteria specified in <u>paragraphs</u> (d)(1)(ii)(A) and (B) of this section.

(A) The performance test demonstrates that the control device achieves greater than or equal to the required control efficiency specified in  $\frac{63.119}{(e)(1)}$  or (2), as applicable; and

(B) The performance test is submitted as part of the Notification of Compliance Status required by § 63.151(b). If the performance test report is submitted electronically through the EPA's CEDRI in accordance with § 63.152(h), the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the notification of compliance status report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(iii) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), if the owner or operator vents emissions through a closed vent system to an adsorber(s) that cannot be regenerated or a regenerative adsorber(s) that is regenerated offsite, then the owner or operator must install a system of two or more adsorber units in series and comply with the requirements specified in paragraphs (d)(1)(iii)(A) through (C) of this section.

(A) Conduct an initial performance test or design evaluation of the adsorber and establish the breakthrough limit and adsorber bed life.

(B) Monitor the HAP or total organic compound (TOC) concentration through a sample port at the outlet of the first adsorber bed in series according to the schedule in <u>paragraph (d)(1)(iii)(C)(2)</u> of this section. The owner or operator must measure the concentration of HAP or TOC using either a portable analyzer, in accordance with Method 21 of appendix A-7 to <u>part 60 of this chapter</u> using methane, propane, isobutylene, or the primary HAP being controlled as the calibration gas or Method 25A of appendix A-7 to part 60 using methane, propane, or the primary HAP being controlled as the calibration gas.

(C) Comply with <u>paragraph (d)(1)(iii)(C)(1)</u> of this section and comply with the monitoring frequency according to <u>paragraph (d)(1)(iii)(C)(2)</u> of this section.

(1) The first adsorber in series must be replaced immediately when breakthrough, as defined in § 63.101, is detected between the first and second adsorber. The original second adsorber (or a fresh canister) will become the new first adsorber and a fresh adsorber will become the second adsorber. For purposes of this paragraph, "immediately" means within 8 hours of the detection of a breakthrough for adsorbers of 55 gallons or less, and within 24 hours of the detection of a breakthrough for adsorber or operator must monitor at the outlet of the first adsorber within 3 days of replacement to confirm it is performing properly.

(2) Based on the adsorber bed life established according to paragraph (d)(1)(iii)(A) of this section and the date the adsorbent was last replaced, conduct monitoring to detect breakthrough at least monthly if the adsorbent has more than 2 months of life remaining, at least weekly if the adsorbent has between 2 months and 2 weeks of life remaining, and at least daily if the adsorbent has 2 weeks or less of life remaining.

(2) The owner or operator shall submit, as part of the Notification of Compliance Status required by <u>§ 63.151 (b)</u>, a monitoring plan containing the information specified in <u>paragraph (d)(2)(i)</u> of this section and in either <u>paragraph (d)(1)(ii)</u> of (<u>iii)</u> of this section. This paragraph does not apply if the owner or operator complies with <u>paragraph (d)(1)(iii)</u> of this section.

(i) A description of the parameter or parameters to be monitored to ensure that the control device is being properly operated and maintained, an explanation of the criteria used for selection of that parameter (or parameters), and the frequency with which monitoring will be performed (*e.g.*, when the liquid level in the storage vessel is being raised); and either

(ii) The documentation specified in <u>paragraph (d)(1)(i)</u> of this section, if the owner or operator elects to prepare a design evaluation; or

(iii) The information specified in <u>paragraph (d)(2)(iii) (A)</u> and (B) of this section if the owner or operator elects to submit the results of a performance test.

(A) Identification of the storage vessel and control device for which the performance test will be submitted, and

(B) Identification of the emission point(s) that share the control device with the storage vessel and for which the performance test will be conducted.

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(3) The owner or operator shall submit, as part of the Notification of Compliance Status required by § 63.152(b) of this subpart, the information specified in paragraphs (d)(3)(i) and, if applicable, (d)(3)(ii) of this section. This paragraph does not apply if the owner or operator complies with paragraph (d)(1)(iii) of this section.

(i) The operating range for each monitoring parameter identified in the monitoring plan. The specified operating range shall represent the conditions for which the control device is being properly operated and maintained.

(ii) Results of the performance test described in paragraph (d)(1)(ii) of this section. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with  $\S$  63.152(h), the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the notification of compliance status report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(4) The owner or operator shall demonstrate compliance with the requirements of  $\frac{8}{63.119(e)(3)}$  and (7) (planned routine maintenance of a control device, during which the control device does not meet the specifications of  $\frac{63.119(e)(1)}{63.152(c)}$  or (2), as applicable, shall not exceed 240 hours per year) by including in each Periodic Report required by  $\frac{63.152(c)}{63.122(g)(1)}$ .

(5) The owner or operator shall monitor the parameters specified in the Notification of Compliance Status required in  $\S$  <u>63.152(b)</u> or in the operating permit and shall operate and maintain the control device such that the monitored parameters remain within the ranges specified in the Notification of Compliance Status.

(6) Except as provided in <u>paragraph (d)(7)</u> of this section, each closed vent system shall be inspected as specified in  $\frac{63.148}{63.148}$ . The initial and annual inspections required by  $\frac{63.148(b)}{63.148(b)}$  shall be done during filling of the storage vessel.

(7) For any fixed roof tank and closed vent system that are operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements specified in  $\frac{\& 63.148}{\&}$ .

(8) A design evaluation or performance test is not required, if the owner or operator uses a combustion device meeting the criteria in paragraph (d)(8)(i), (ii), (iii), or (iv) of this section.

(i) A boiler or process heater with a design heat input capacity of 44 megawatts or greater.

(ii) A boiler or process heater burning hazardous waste for which the owner or operator:

(A) Has been issued a final permit under <u>part 270 of this chapter</u> and complies with the requirements of part 266, subpart H, of this chapter;

(B) Has certified compliance with the interim status requirements of part 266, subpart H, of this chapter;

(C) Has submitted a Notification of Compliance under  $\S 63.1207(j)$  and complies with the requirements of subpart EEE of this part; or

(D) Complies with subpart EEE of this part and will submit a Notification of Compliance under  $\S$  63.1207(j) by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(iii) A hazardous waste incinerator for which the owner or operator:

(A) Has been issued a final permit under <u>part 270 of this chapter</u> and complies with the requirements of part 264, subpart O, of this chapter;

(B) Has certified compliance with the interim status requirements of part 265, subpart O, of this chapter;

(C) Has submitted a Notification of Compliance under  $\S$  <u>63.1207(j)</u> and complies with the requirements <u>subpart EEE of this</u> <u>part</u>; or

(D) Complies with the requirements subpart EEE of this part and will submit a Notification of Compliance under  $\S$  <u>63.1207(j)</u> by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(iv) A boiler or process heater into which the vent stream is introduced with the primary fuel.

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(9) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(11), paragraph (d)(1)(i) of this section no longer applies to storage vessels in ethylene oxide service, as defined in § 63.101.

(e) Except as specified in <u>paragraph (a) of § 63.108</u>, to demonstrate compliance with § <u>63.119(e)</u> (storage vessel equipped with a closed vent system and control device) using a flare, the owner or operator shall comply with the requirements in <u>paragraphs (e)(1)</u> through (<u>6</u>) of this section.

(1) The owner or operator shall perform the compliance determination specified in  $\S$  63.11(b) of subpart A of this part.

(2) The owner or operator shall submit, as part of the Notification of Compliance Status required by  $\S 63.152(b)$  of this subpart, the information specified in paragraphs (e)(2)(i) through (e)(2)(iii) of this section.

(i) Flare design (i.e., steam-assisted, air-assisted, or non-assisted);

(ii) All visible emission readings, heat content determinations, flow rate measurements, and exit velocity determinations made during the compliance determination required by <u>paragraph (e)(1)</u> of this section; and

(iii) All periods during the compliance determination when the pilot flame is absent.

(3) The owner or operator shall demonstrate compliance with the requirements of  $\frac{88}{63.119(e)(3)}$  and (7) (planned routine maintenance of a flare, during which the flare does not meet the specifications of  $\frac{863.119(e)(1)}{63.120(e)(1)}$ , shall not exceed 240 hours per year) by including in each Periodic Report required by  $\frac{863.152(c)}{63.152(c)}$  the information specified in  $\frac{863.122(g)(1)}{63.122(g)(1)}$ .

(4) The owner or operator shall continue to meet the general control device requirements specified in  $\frac{63.11(b)}{5}$  of subpart A of this part.

(5) Except as provided in <u>paragraph (e)(6)</u> of this section, each closed vent system shall be inspected as specified in  $\frac{63.148}{63.148}$  of this subpart. The inspections required to be performed in accordance with  $\frac{63.148}{63.148}$  of this subpart shall be done during filling of the storage vessel.

(6) For any fixed roof tank and closed vent system that is operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements specified in  $\S$  63.148 of this subpart.

(f) To demonstrate compliance with  $\S$  63.119(f) of this subpart (storage vessel routed to a process), the owner or operator shall prepare a design evaluation (or engineering assessment) that demonstrates the extent to which one or more of the ends specified in  $\S$  63.119(f)(1)(i) through (f)(1)(iv) are being met. The owner or operator shall submit the design evaluation as part of the Notification of Compliance Status required by  $\S$  63.152(b) of this subpart.

(g) To demonstrate compliance with the emission limits and work practice standards specified in  $\S$  63.119(a)(5) for storage vessels in ethylene oxide service, owners and operators must meet the requirements specified in  $\S$  63.124.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>61 FR 64576</u>, Dec. 5, 1996; <u>62 FR 2748</u>, Jan. 17, 1997; <u>89 FR 43190</u>, May 16, 2024]

## § 63.121 Storage vessel provisions—alternative means of emission limitation.

(a) Determination of equivalence to the reduction in emissions achieved by the requirements of § 63.119 (b), (c), or (d) of this subpart will be evaluated according to § 63.102(b) of subpart F of this part.

(b) The determination of equivalence referred to in <u>paragraph (a)</u> of this section will be based on the application to the Administrator which shall include the information specified in either <u>paragraph (b)(1)</u> or (b)(2) of this section.

(1) Actual emissions tests that use full-size or scale-model storage vessels that accurately collect and measure all organic HAP emissions from a given control technique, and that accurately simulate wind and account for other emission variables such as temperature and barometric pressure, or

(2) An engineering analysis that the Administrator determines is an accurate method of determining equivalence.

## § 63.122 Storage vessel provisions—reporting.

(a) For each Group 1 storage vessel, the owner or operator shall comply with the requirements of <u>paragraphs</u> (a)(1) through (a)(5) of this section.

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(1) The owner or operator shall submit an Initial Notification as required by  $\S$  63.151(b) of this subpart.

(2) [Reserved]

(3) The owner or operator shall submit a Notification of Compliance Status as required by  $\frac{63.152(b)}{2}$  of this subpart and shall submit as part of the Notification of Compliance Status the information specified in <u>paragraph (c)</u> of this section.

(4) The owner or operator shall submit Periodic Reports as required by  $\S$  63.152(c) of this subpart and shall submit as part of the Periodic Reports the information specified in paragraphs (d), (e), (f), (g), and (i) of this section.

(5) The owner or operator shall submit, as applicable, other reports as required by  $\frac{63.152(d)}{63.152(d)}$  of this subpart, containing the information specified in paragraph (h) of this section.

(b) An owner or operator who elects to comply with  $\S 63.119(e)$  of this subpart by using a closed vent system and a control device other than a flare shall submit, as part of the Monitoring Plan, the information specified in  $\S 63.120(d)(2)(i)$  of this subpart and the information specified in either  $\S 63.120(d)(2)(i)$  of this subpart or  $\S 63.120(d)(2)(ii)$  of this subpart.

(c) An owner or operator who elects to comply with  $\S$  63.119(e) of this subpart by using a closed vent system and a control device shall submit, as part of the Notification of Compliance Status required by  $\S$  63.152(b) of this subpart, the information specified in either paragraph (c)(1) or (c)(2) of this section. An owner or operator who elects to comply with  $\S$  63.119(f) of this subpart by routing emissions to a process or to a fuel gas system shall submit, as part of the Notification of Compliance Status required by  $\S$  63.152(b) of this subpart, the information specified in paragraph (c)(1) or (c)(2) of this subpart, the information specified in paragraph (c)(3) of this section.

(1) If a control device other than a flare is used, the owner or operator shall submit the information specified in  $\S$  <u>63.120(d)(3)(i)</u> and, if applicable, (d)(3)(ii) of this subpart.

(2) Except as specified in <u>paragraph (a) of § 63.108</u>, if a flare is used, the owner or operator shall submit the information specified in § 63.120(e)(2)(i), (e)(2)(i) through (iii).

(3) If emissions are routed to a process, the owner or operator shall submit the information specified in § 63.120(f). If emissions are routed to a fuel gas system, the owner or operator shall submit a statement that the emission stream is connected to the fuel gas system and whether the conveyance system is subject to the requirements of § 63.148.

(d) An owner or operator who elects to comply with  $\S$  63.119(b) of this subpart by using a fixed roof and an internal floating roof or with  $\S$  63.119(d) of this subpart by using an external floating roof converted to an internal floating roof shall submit, as part of the Periodic Report required under  $\S$  63.152(c) of this subpart, the results of each inspection conducted in accordance with  $\S$  63.120(a) of this subpart in which a failure is detected in the control equipment.

(1) For vessels for which annual inspections are required under § 63.120 (a)(2)(i) or (a)(3)(ii) of this subpart, the specifications and requirements listed in paragraphs (d)(1)(i) through (d)(1)(iii) of this section apply.

(i) A failure is defined as any time in which the internal floating roof is not resting on the surface of the liquid inside the storage vessel and is not resting on the leg supports; or there is liquid on the floating roof; or the seal is detached from the internal floating roof; or there are holes, tears, or other openings in the seal or seal fabric; or there are visible gaps between the seal and the wall of the storage vessel.

(ii) Except as provided in <u>paragraph (d)(1)(iii)</u> of this section, each Periodic Report shall include the date of the inspection, identification of each storage vessel in which a failure was detected, and a description of the failure. The Periodic Report shall also describe the nature of and date the repair was made or the date the storage vessel was emptied.

(iii) If an extension is utilized in accordance with  $\S$  63.120(a)(4) of this subpart, the owner or operator shall, in the next Periodic Report, identify the vessel; include the documentation specified in  $\S$  63.120(a)(4) of this subpart; and describe the date the storage vessel was emptied and the nature of and date the repair was made.

(2) For vessels for which inspections are required under  $\S$  63.120 (a)(2)(ii), (a)(3)(i), or (a)(3)(iii) of this subpart, the specifications and requirements listed in paragraphs (d)(2)(i) and (d)(2)(ii) of this section apply.

(i) A failure is defined as any time in which the internal floating roof has defects; or the primary seal has holes, tears, or other openings in the seal or the seal fabric; or the secondary seal (if one has been installed) has holes, tears, or other openings in the seal or the seal fabric; or the gaskets no longer close off the liquid surface from the atmosphere; or the slotted membrane has more than 10 percent open area.

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(ii) Each Periodic Report required under <u>§ 63.152(c) of this subpart</u> shall include the date of the inspection, identification of each storage vessel in which a failure was detected, and a description of the failure. The Periodic Report shall also describe the nature of and date the repair was made.

(e) An owner or operator who elects to comply with  $\S$  63.119(c) of this subpart by using an external floating roof shall meet the periodic reporting requirements specified in paragraphs (e)(1), (e)(2), and (e)(3) of this section.

(1) The owner or operator shall submit, as part of the Periodic Report required under  $\frac{63.152(c)}{63.120(b)}$  of this subpart, documentation of the results of each seal gap measurement made in accordance with  $\frac{63.120(b)}{63.120(b)}$  of this subpart in which the requirements of  $\frac{63.120(b)}{63.120(b)}$ ,  $\frac{(b)(4)}{(b)(5)}$ , or  $\frac{(b)(6)}{(b)(6)}$  of this subpart are not met. This documentation shall include the information specified in paragraphs (e)(1)(i) through (e)(1)(iv) of this section.

(i) The date of the seal gap measurement.

(ii) The raw data obtained in the seal gap measurement and the calculations described in  $\S$  63.120 (b)(3) and (b)(4) of this subpart.

(iii) A description of any condition specified in  $\frac{63.120 (b)(5)}{5}$  or  $\frac{(b)(6)}{5}$  of this subpart that is not met.

(iv) A description of the nature of and date the repair was made, or the date the storage vessel was emptied.

(2) If an extension is utilized in accordance with  $\S 63.120(b)(7)(ii)$  or (b)(8) of this subpart, the owner or operator shall, in the next Periodic Report, identify the vessel; include the documentation specified in  $\S 63.120(b)(7)(ii)$  or (b)(8) of this subpart, as applicable; and describe the date the vessel was emptied and the nature of and date the repair was made.

(3) The owner or operator shall submit, as part of the Periodic Report required under  $\frac{63.152(c)}{63.120(b)(10)}$  of this subpart, documentation of any failures that are identified during visual inspections required by  $\frac{63.120(b)(10)}{63.120(b)(10)}$  of this subpart. This documentation shall meet the specifications and requirements in paragraphs (e)(3)(i) and (e)(3)(ii) of this section.

(i) A failure is defined as any time in which the external floating roof has defects; or the primary seal has holes, or other openings in the seal or the seal fabric; or the secondary seal has holes, tears, or other openings in the seal or the seal fabric; or the gaskets no longer close off the liquid surface from the atmosphere; or the slotted membrane has more than 10 percent open area.

(ii) Each Periodic Report required under <u>§ 63.152(c) of this subpart</u> shall include the date of the inspection, identification of each storage vessel in which a failure was detected, and a description of the failure. The periodic report shall also describe the nature of and date the repair was made.

(f) An owner or operator who elects to comply with  $\S$  63.119(d) of this subpart by using an external floating roof converted to an internal floating roof shall comply with the periodic reporting requirements of paragraph (d) of this section.

(g) An owner or operator who elects to comply with  $\S \underline{63.119(e)}$  by installing a closed vent system and control device shall submit, as part of the next Periodic Report required by  $\S \underline{63.152(c)}$ , the information specified in <u>paragraphs</u> (g)(1) through (4) of this section.

(1) As required by  $\S 63.120(d)(4)$  and (e)(3), the Periodic Report shall include the information specified in <u>paragraphs</u> (g)(1)(i) through (iii) of this section for those planned routine maintenance operations that would require the control device not to meet the requirements of  $\S 63.119$  (e)(1) or (2), as applicable.

(i) A description of the planned routine maintenance that is anticipated to be performed for the control device during the next 6 months. This description shall include the type of maintenance necessary, planned frequency of maintenance, and lengths of maintenance periods.

(ii) A description of the planned routine maintenance that was performed for the control device during the previous 6 months. This description shall include the type of maintenance performed and the total number of hours during those 6 months that the control device did not meet the requirements of  $\S$  63.119 (e)(1) or (2), as applicable, due to planned routine maintenance.

(iii) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), for each storage vessel for which planned routine maintenance was performed during the previous 6 months, report the identification of the storage vessel and the height of the liquid in the storage vessel at the time the control device is bypassed to conduct the planned routine maintenance and at the time the control device is placed back in service after completing the routine maintenance. These reports shall include the date and time the liquid height was measured.

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(2) If a control device other than a flare is used, the Periodic Report shall describe each occurrence when the monitored parameters were outside of the parameter ranges documented in the Notification of Compliance Status in accordance with  $\S$  <u>63.120(d)(3)(i)</u>. The description shall include the information specified in <u>paragraphs (g)(2)(i)</u> and <u>(ii)</u> of this section.

(i) Identification of the control device for which the measured parameters were outside of the established ranges, the date, and the parameter that was outside of the established ranges, and

(ii) Cause for the measured parameters to be outside of the established ranges.

(3) Except as specified in <u>paragraph (a) of § 63.108</u>, if a flare is used, the Periodic Report shall describe each occurrence when the flare does not meet the general control device requirements specified in § 63.11(b) and shall include the information specified in <u>paragraphs (g)(3)(i)</u> and <u>(ii)</u> of this section.

(i) Identification of the flare which does not meet the general requirements specified in  $\S$  63.11(b), and

(ii) Reason the flare did not meet the general requirements specified in  $\S 63.11(b)$ .

(4) For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in § <u>63.120(d)(1)(iii)</u>, the owner or operator must report the date of each instance when breakthrough, as defined in § <u>63.101</u>, is detected between the first and second adsorber and the adsorber is not replaced according to § <u>63.120(d)(1)(iii)(C)(1)</u> and an identification of the adsorber for which breakthrough was detected.

(h) An owner or operator who elects to comply with § 63.119 (b), (c), or (d) of this subpart shall submit, as applicable, the reports specified in paragraphs (h)(1) and (h)(2) of this section.

(1) In order to afford the Administrator the opportunity to have an observer present, the owner or operator shall notify the Administrator of the refilling of a storage vessel that has been emptied and degassed.

(i) If the storage vessel is equipped with an internal floating roof as specified in § 63.119(b) of this subpart, the notification shall meet the requirements of either § 63.120 (a)(5) or (a)(6) of this subpart, as applicable.

(ii) If the storage vessel is equipped with an external floating roof as specified in § 63.119(c) of this subpart, the notification shall meet the requirements of either § 63.120 (b)(10)(ii) or (b)(10)(iii) of this subpart, as applicable.

(iii) If the storage vessel is equipped with an external floating roof converted into an internal floating roof as specified in § <u>63.119(d) of this subpart</u>, the notification shall meet the requirements of either § <u>63.120 (a)(5)</u> or (a)(6) of this subpart, as applicable.

(2) In order to afford the Administrator the opportunity to have an observer present, the owner or operator of a storage vessel equipped with an external floating roof as specified in  $\S$  63.119(c) of this subpart shall notify the Administrator of any seal gap measurements. This notification shall meet the requirements of  $\S$  63.120(b)(9) of this subpart.

(i) For pressure vessels subject to the requirements of  $\S 63.119(a)(7)$ , if you obtain an instrument reading greater than 500 ppmv of a leak when monitoring a pressure vessel in accordance with  $\S 63.119(a)(7)(ii)$ , then the Periodic Report must include an identification of the pressure vessel and a copy of the records specified in  $\S 63.123(b)(2)$ .

[<u>59 FR 19468</u>, Apr. 22, 1996, as amended at <u>61 FR 64576</u>, Dec. 5, 1996; <u>62 FR 2748</u>, Jan. 17, 1997; <u>89 FR 43192</u>, May 16, 2024]

# § 63.123 Storage vessel provisions—recordkeeping.

(a) Each owner or operator of a Group 1 or Group 2 storage vessel shall keep readily accessible records showing the dimensions of the storage vessel and an analysis showing the capacity of the storage vessel. This record shall be kept as long as the storage vessel retains Group 1 or Group 2 status and is in operation. For each Group 2 storage vessel, the owner or operator is not required to comply with any other provisions of  $\frac{863.119}{1000}$  through  $\frac{63.123}{1000}$  of this subpart other than those required by this paragraph unless such vessel is part of an emissions average as described in  $\frac{863.150}{1000}$  of this subpart.

(b) Each owner or operator of a pressure vessel subject to the requirements of  $\frac{63.119(a)(7)}{2}$  shall keep readily accessible records as specified in <u>paragraphs (b)(1)</u> and (2) of this section.

(1) The date of each performance test conducted according to  $\frac{63.119(a)(7)(ii)}{63.119(a)(7)(ii)}$ .

(2) The record of each performance test conducted according to  $\frac{63.119(a)(7)(ii)}{63.119(a)(7)(ii)}$ , including the following:

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(i) Date each defect was detected and the instrument reading (in ppmv) during the performance test.

(ii) Date of the next performance test that shows the instrument reading is less than 500 ppmv and the instrument reading (in ppmv) during the performance test.

(iii) Start and end dates of each period after the date in <u>paragraph (b)(2)(i)</u> of this section when the pressure vessel was completely empty.

(iv) Estimated emissions from each defect.

(c) An owner or operator who elects to comply with  $\S$  63.119(b) of this subpart shall keep a record that each inspection required by  $\S$  63.120(a) of this subpart was performed.

(d) An owner or operator who elects to comply with  $\S 63.119(c)$  of this subpart shall keep records describing the results of each seal gap measurement made in accordance with  $\S 63.120(b)$  of this subpart. The records shall include the date of the measurement, the raw data obtained in the measurement, and the calculations described in  $\S 63.120(b)$  (3) and (4) of this subpart.

(e) An owner or operator who elects to comply with  $\S$  63.119(d) of this subpart shall keep a record that each inspection required by  $\S$  63.120 (a) and (c) of this subpart was performed.

(f) An owner or operator who elects to comply with  $\S 63.119(e)$  of this subpart shall keep in a readily accessible location the records specified in paragraphs (f)(1) and (f)(2) of this section.

(1) A record of the measured values of the parameters monitored in accordance with § 63.120(d)(5) of this subpart.

(2) A record of the planned routine maintenance performed on the control device including the duration of each time the control device does not meet the specifications of § 63.119 (e)(1) or (e)(2) of this subpart, as applicable, due to the planned routine maintenance. Such a record shall include the information specified in paragraphs (f)(2)(i) and (f)(2)(ii) of this section.

(i) The first time of day and date the requirements of  $\S$  63.119 (e)(1) or (e)(2) of this subpart, as applicable, were not met at the beginning of the planned routine maintenance, and

(ii) The first time of day and date the requirements of  $\S$  63.119 (e)(1) or (e)(2) of this subpart, as applicable, were met at the conclusion of the planned routine maintenance.

(g) An owner or operator who elects to utilize an extension in emptying a storage vessel in accordance with  $\frac{63.120}{(a)(4)}$ , (b)(7)(ii), or (b)(8) of this subpart shall keep in a readily accessible location, the documentation specified in  $\frac{63.120}{(a)(4)}$ , (b)(7)(ii), or (b)(8), as applicable.

(h) An owner or operator who uses the bypass provisions of  $\S 63.119(f)(3)$  shall keep in a readily accessible location the records specified in paragraphs (h)(1) through (3) of this section.

(1) The reason it was necessary to bypass the process equipment or fuel gas system;

(2) The duration of the period when the process equipment or fuel gas system was bypassed;

(3) Documentation or certification of compliance with the applicable provisions of  $\frac{63.119(f)(3)(i)}{1000}$  through (iv).

(i) An owner or operator who elects to comply with  $\S 63.119(g)$  shall keep the records specified in <u>paragraphs</u> (i)(1) through (3) of this section.

(1) A record of the U.S. Department of Transportation certification required by  $\frac{63.119(g)(2)}{2}$ .

(2) A record of the pressure relief vent setting specified in  $\S 63.119(g)(5)$ .

(3) If complying with  $\S 63.119(g)(6)(ii)$ , keep the records specified in <u>paragraphs (i)(3)(i)</u> and (ii) of this section.

(i) A record of the equipment to be used and the procedures to be followed when reloading the railcar, tank truck, or barge and displacing vapors to the storage vessel from which the liquid originates.

(ii) A record of each time the vapor balancing system is used to comply with  $\frac{63.119(g)(6)(ii)}{63.119(g)(6)(ii)}$ .

(j) For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in  $\S$  <u>63.120(d)(1)(iii)</u>, the owner or operator must keep the applicable records specified in (j)(1) through (3) of this section.

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(1) Breakthrough limit and bed life established according to  $\S 63.120(d)(1)(iii)(A)$ .

(2) Each outlet HAP or TOC concentration measured according to  $\frac{63.120(d)(1)(iii)(B)}{63.120(d)(1)(iii)(B)}$  and (C).

(3) Date and time you last replaced the adsorbent.

(k) For storage vessels in ethylene oxide service, subject to the requirements of  $\S$  63.124, owners and operators must keep the records specified in <u>paragraphs (k)(1)</u> and (2) of this section in addition to those records specified elsewhere in this section.

(1) For storage vessels in ethylene oxide service, records of the concentration of ethylene oxide of the fluid stored in each storage vessel.

(2) If emissions are vented through a closed-vent system to a non-flare control device, then the owner or operator must keep records of all periods during which operating values are outside of the applicable operating limits specified in  $\S$  <u>63.124(b)(4)</u> through (<u>6)</u> when regulated material is being routed to the non-flare control device. The record must specify the operating parameter, the applicable limit, and the highest (for maximum operating limits) or lowest (for minimum operating limits) value recorded during the period.

[<u>59 FR 19468</u>, Apr. 22, 1996, as amended at <u>61 FR 64576</u>, Dec. 5, 1996; <u>62 FR 2748</u>, Jan. 17, 1997; <u>69 FR 76863</u>, Dec. 23, 2004; <u>89 FR 43193</u>, May 16, 2024]

## § 63.124 Process vents and storage vessels that are in ethylene oxide service—procedures to determine compliance.

This section applies beginning no later than the compliance dates specified in  $\S$  <u>63.100(k)(11)</u>. In order to demonstrate compliance with the emission limits and work practice standards specified in  $\S$  <u>63.113(i)</u> (for process vents in ethylene oxide service) and  $\S$  <u>63.119(a)(5)</u> (for storage vessels in ethylene oxide service), owners and operators must meet the requirements specified in paragraphs (a) and (b) of this section.

(a) For initial compliance, owners and operators must comply with <u>paragraphs (a)(1)</u> through (4) of this section, as applicable.

(1) If an owner or operator chooses to reduce emissions of ethylene oxide by venting emissions through a closed vent system to a flare as specified in  $\S 63.113(j)(1)$  or  $\S 63.119(a)(5)(i)$ , then the owner or operator must comply with  $\S 63.148$  and conduct the initial visible emissions demonstration required by  $\S 63.670(h)$  as specified in  $\S 63.108$ .

(2) If an owner or operator chooses to reduce emissions of ethylene oxide by venting emissions through a closed vent system to a non-flare control device that reduces ethylene oxide by greater than or equal to 99.9 percent by weight as specified in  $\S$  <u>63.113(j)(2)</u> or  $\S$  <u>63.119(a)(5)(ii)</u>, then the owner or operator must comply with  $\S$  <u>63.148</u> and <u>paragraphs</u> (a)(2)(i) through (viii) of this section.

(i) Conduct an initial performance test of the control device that is used to comply with the percent reduction requirement at the inlet and outlet of the control device. For purposes of compliance with this paragraph, owners and operators may not use a design evaluation. This paragraph does not apply if the conditions specified in <u>paragraphs (a)(2)(i)(A)</u> through (<u>D</u>) of this section are met for a previously conducted measurement or performance test.

(A) No changes have been made to the process since the time of the measurement or performance test;

(B) The operating conditions and test methods used during measurement or performance test conform to the ethylene oxide related requirements of this subpart;

(C) The control device and process parameter values established during the previously conducted measurement or performance test are used to demonstrate continuous compliance with the ethylene oxide related requirements of this subpart; and

(D) The previously conducted measurement or performance test was completed within the last 60 months.

(ii) Conduct the performance test according to the procedures in § 63.116(c). Except as specified in § 63.109(a)(6), use Method 18 of appendix A-6 to part 60 of this chapter or Method 320 of appendix A to this part to determine the ethylene oxide concentration. Use Method 1 or 1A of appendix A-1 to part 60 of this chapter to select the sampling sites at each sampling location. Determine the gas volumetric flowrate using Method 2, 2A, 2C, or 2D of appendix A-2 to part 60 of this chapter. Use Method 4 of appendix A-3 to part 60 of this chapter convert the volumetric flowrate to a dry basis.

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(iii) Calculate the mass emission rate of ethylene oxide entering the control device and exiting the control device using equations 1 and 2 to this paragraph.

Equations 1 and 2 to Paragraph (a)(2)(iii)

 $E_{\text{,inlet}} = K C_{\text{,inlet}} M Q_{\text{inlet}} (Eq. 1)$ 

 $E_{outlet} = K C_{outlet} M Q_{outlet} (Eq. 2)$ 

Where:

E,inlet, E,outlet = Mass rate of ethylene oxide at the inlet and outlet of the control device, respectively, kilogram per hour.

 $C_{inlet}$ ,  $C_{outlet}$  = Concentration of ethylene oxide in the gas stream at the inlet and outlet of the control device, respectively, dry basis, parts per million by volume.

M = Molecular weight of ethylene oxide, 44.05 grams per gram-mole.

 $Q_{\text{inlet}}$ ,  $Q_{\text{outlet}}$  = Flow rate of the gas stream at the inlet and outlet of the control device, respectively, dry standard cubic meter per minute.

K = Constant, 2.494 × 10–6 (parts per million)–1 (gram-mole per standard cubic meter) (kilogram per gram) (minutes per hour), where standard temperature (gram-mole per standard cubic meter) is 20 °C.

(iv) Calculate the percent reduction from the control device using equation 3 to this paragraph. An owner or operator has demonstrated initial compliance with  $\frac{63.113(j)(2)}{2}$  or  $\frac{63.119(a)(5)(ii)}{2}$  if the overall reduction of ethylene oxide is greater than or equal to 99.9 percent by weight.

Equation 3 to Paragraph (a)(2)(iv)

Percent reduction =  $(E_{,inlet}-E_{,outlet})/E_{,inlet} * 100 (Eq.3)$ 

Where:

 $E_{inlet}$ ,  $E_{outlet}$  = Mass rate of ethylene oxide at the inlet and outlet of the control device, respectively, kilogram per hour, calculated using Equations 1 and 2 to <u>paragraph (a)(2)(iii)</u> of this section.

(v) If a new control device is installed, then conduct a performance test of the new device following the procedures in paragraphs (a)(2)(i) through (iv) of this section.

(vi) If an owner or operator vents emissions through a closed vent system to a scrubber with a reactant tank, then the owner or operator must establish operating parameter limits by monitoring the operating parameters specified in <u>paragraphs</u> (a)(2)(vi)(A) through (C) of this section during the performance test.

(A) Scrubber liquid-to-gas ratio (L/G), determined from the total scrubber liquid inlet flow rate and the inlet or exit gas flow rate. Determine the average L/G during the performance test as the average of the test run averages. Alternatively, separately monitor the total scrubber liquid flow rate and gas flow rate through the scrubber. Determine the average total scrubber liquid flow rate and gas flow through the scrubber as the average of the test run averages.

(B) Scrubber liquid pH of the liquid in the reactant tank. The pH may be measured at any point between the discharge from the scrubber column and the inlet to the reactant tank. Determine the average pH during the performance test as the average of the test run averages.

(C) Temperature of the scrubber liquid entering the scrubber column. The temperature may be measured at any point after the heat exchanger and prior to entering the top of the scrubber column. Determine the average inlet scrubber liquid temperature as the average of the test run averages.

(vii) If an owner or operator vents emissions through a closed vent system to a thermal oxidizer, then the owner or operator must establish operating parameter limits by monitoring the operating parameters specified in <u>paragraphs</u> (a)(2)(vii)(A) and (B) of this section during the performance test.

(A) Combustion chamber temperature. Determine the average combustion chamber temperature during the performance test as the average of the test run averages.

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(B) Flue gas flow rate. Determine the average flue gas flow rate during the performance test as the average of the test run averages.

(viii) If an owner or operator vents emissions through a closed vent system to a control device other than a flare, scrubber with a reactant tank, or thermal oxidizer, then the owner or operator must notify the Administrator of the operating parameters that are planned to be monitored during the performance test prior to establishing operating parameter limits for the control device.

(3) If an owner or operator chooses to reduce emissions of ethylene oxide by venting emissions through a closed vent system to a non-flare control device that reduces ethylene oxide to less than 1 ppmv as specified in  $\frac{63.113(j)(2)}{5}$  or  $\frac{63.119(a)(5)(ii)}{5}$ , then the owner or operator must comply with  $\frac{63.148}{5}$  and either paragraph (a)(3)(i) or (ii) of this section.

(i) Install a continuous emissions monitoring system (CEMS) to continuously monitor the ethylene oxide concentration at the exit of the control device. The CEMS must meet the requirements of either paragraph (a)(3)(i)(A) or (B) of this section. Comply with the requirements specified in  $\frac{863.2450(j)}{5}$  for CEMS.

(A) An FTIR CEMS meeting the requirements of Performance Specification 15 of appendix B to part 60 of this chapter.

(B) A gas chromatographic CEMS meeting the requirements of Performance Specification 9 of appendix B to <u>part 60 of this</u> <u>chapter</u>.

(ii) If the owner or operator does not install a CEMS under <u>paragraph (a)(3)(i)</u> of this section, then the owner or operator must comply with <u>paragraphs (a)(3)(ii)(A)</u> through (C) of this section.

(A) Conduct an initial performance test at the outlet of the control device that is used to comply with the concentration requirement.

(B) Conduct the performance test according to the procedures in  $\S$  63.116(c). Except as specified in  $\S$  63.109(a)(6), use Method 18 of appendix A-6 to part 60 of this chapter or Method 320 of appendix A to this part to determine the ethylene oxide concentration. If the non-flare control device is a combustion device, correct the ethylene oxide concentration to 3 percent oxygen according to  $\S$  63.116(c)(iii)(B), except "TOC or organic HAP" and "TOC (minus methane and ethane) or organic HAP" in the Variables C<sub>c</sub> and C<sub>m</sub> must be replaced with "ethylene oxide". An owner or operator has demonstrated initial compliance with  $\S$  63.113(j)(2) or  $\S$  63.119(a)(5)(ii), if the ethylene oxide concentration is less than 1 ppmv.

(C) Comply with the requirements specified in paragraphs (a)(2)(v) through (viii) of this section, as applicable.

(4) If owners and operators choose to reduce emissions of ethylene oxide by venting emissions through a closed vent system to a non-flare control device that reduces ethylene oxide to less than 5 pounds per year for all combined process vents within the process as specified in  $\frac{63.113(j)(2)}{(j)}$ , then the owner or operator must comply with  $\frac{63.148}{(j)}$  and <u>paragraphs</u> (a)(4)(i) through (iv) of this section.

(i) Conduct an initial performance test of the control device that is used to comply with the mass emission limit requirement at the outlet of the control device.

(ii) Conduct the performance test according to the procedures in § 63.116(c). Except as specified in § 63.109(a)(6), use Method 18 of appendix A-6 to <u>part 60 of this chapter</u> or Method 320 of appendix A to this part to determine the ethylene oxide concentration. Use Method 1 or 1A of appendix A-1 to <u>part 60 of this chapter</u> to select the sampling site. Determine the gas volumetric flowrate using Method 2, 2A, 2C, or 2D of <u>40 CFR part 60, appendix A</u>-2. Use Method 4 of appendix A-3 to <u>part 60 of this chapter</u> to convert the volumetric flowrate to a dry basis.

(iii) Calculate the mass emission rate of ethylene oxide exiting the control device using Equation 2 to paragraph (a)(2)(iii) of this section. An owner or operator has demonstrated initial compliance with  $\S$  63.113(j)(2) if the ethylene oxide from all process vents (controlled and uncontrolled) within the process is less than 5 pounds per year when combined.

(iv) Comply with the requirements specified in <u>paragraphs (a)(2)(v)</u> through (viii) of this section, as applicable.

(b) For continuous compliance, owners and operators must comply with <u>paragraphs (b)(1)</u> through <u>(6)</u> of this section, as applicable.

(1) If an owner or operator chooses to reduce emissions of ethylene oxide by venting emissions through a closed vent system to a flare as specified in  $\frac{63.113(j)(1)}{50}$  or  $\frac{63.119(a)(5)(i)}{50}$ , then the owner or operator must comply with  $\frac{88}{50}$  and  $\frac{63.108}{50}$ .

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(2) If you choose to reduce emissions of ethylene oxide by venting emissions through a closed-vent system to a non-flare control device that reduces ethylene oxide to less than 1 ppmv as specified in  $\S$  63.113(j)(2) or  $\S$  63.119(a)(5)(ii), and you choose to comply with paragraph (a)(3)(i) of this section, then continuously monitor the ethylene oxide concentration at the exit of the control device using an FTIR CEMS meeting the requirements of Performance Specification 15 of appendix B to part 60 of this chapter and  $\S$  63.2450(j). If an owner or operator uses an FTIR CEMS, then the owner or operator does not need to conduct the performance testing required in paragraph (b)(3) of this section.

(3) Conduct a performance test no later than 60 months after the previous performance test and reestablish operating parameter limits following the procedures in paragraph (a)(2) through (4) of this section. The Administrator may request a repeat performance test at any time. For purposes of compliance with this paragraph, owners and operators may not use a design evaluation.

(4) If an owner or operator vents emissions through a closed vent system to a scrubber with a reactant tank, then the owner or operator must comply with  $\S$  63.148 and meet the operating parameter limits specified in paragraphs (b)(4)(i) through (v) of this section.

(i) Minimum scrubber liquid-to-gas ratio (L/G), equal to the average L/G measured during the most recent performance test. Determine total scrubber liquid inlet flow rate with a flow sensor with a minimum accuracy of at least  $\pm 5$  percent over the normal range of flow measured, or 1.9 liters per minute (0.5 gallons per minute), whichever is greater. Determine gas flow rate at either the inlet or the exit of the scrubber with a flow sensor with a minimum accuracy of at least  $\pm 5$  percent over the normal range of flow measured, or 280 liters per minute (10 cubic feet per minute), whichever is greater. If gas flow rate is determined at the inlet of the scrubber, ensure that all gas flow through the scrubber is accounted for at the measurement location. Compliance with the minimum L/G operating limit must be determined continuously on a 1-hour block basis. Alternatively, minimum total scrubber liquid flow rate, equal to the average total scrubber, equal to the average gas flow rate through the scrubber during the most recent performance test. Compliance with the total scrubber liquid flow rate and gas flow rate through the scrubber liquid flow rate and gas flow rate through the scrubber liquid flow rate and gas flow rate through the scrubber liquid flow rate and gas flow rate through the scrubber liquid flow rate and gas flow rate through the scrubber must be determined continuously on a 1-hour block basis.

(ii) Maximum scrubber liquid pH of the liquid in the reactant tank, equal to the average pH measured during the most recent performance test. Compliance with the pH operating limit must be determined continuously on a 1-hour block basis. Use a pH sensor with a minimum accuracy of  $\pm 0.2$  pH units.

(iii) Pressure drop across the scrubber column, within the pressure drop range specified by the manufacturer or established based on engineering analysis. Compliance with the pressure drop operating limit must be determined continuously on a 1-hour block basis. Use pressure sensors with a minimum accuracy of  $\pm 5$  percent over the normal operating range or 0.12 kilopascals, whichever is greater.

(iv) Maximum temperature of the scrubber liquid entering the scrubber column, equal to the average temperature measured during the most recent performance test. Compliance with the inlet scrubber liquid temperature operating limit must be determined continuously on a 1-hour block basis. Use a temperature sensor with a minimum accuracy of  $\pm 1$  percent over the normal range of the temperature measured, expressed in degrees Celsius, or 2.8 degrees Celsius, whichever is greater.

(v) Liquid feed pressure to the scrubber column within the feed pressure range specified by the manufacturer or established based on engineering analysis. Compliance with the liquid feed pressure operating limit must be determined continuously on a 1-hour block basis. Use a pressure sensor with a minimum accuracy of  $\pm 5$  percent over the normal operating range or 0.12 kilopascals, whichever is greater.

(5) If an owner or operator vents emissions through a closed vent system to a thermal oxidizer, then the owner or operator must comply with  $\S$  63.148, and the owner or operator must meet the operating parameter limits specified in <u>paragraphs</u> (b)(5)(i) and (ii) of this section and the requirements in <u>paragraph (b)(5)(iii)</u> of this section.

(i) Minimum combustion chamber temperature, equal to the average combustion chamber temperature measured during the most recent performance test. Determine combustion chamber temperature with a temperature sensor with a minimum accuracy of at least  $\pm 1$  percent over the normal range of temperature measured, expressed in degrees Celsius, or 2.8 degrees Celsius, whichever is greater. Compliance with the minimum combustion chamber temperature operating limit must be determined continuously on a 1-hour block basis.

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(ii) Maximum flue gas flow rate, equal to the average flue gas flow rate measured during the most recent performance test. Determine flue gas flow rate with a flow sensor with a minimum accuracy of at least  $\pm 5$  percent over the normal range of flow measured, or 280 liters per minute (10 cubic feet per minute), whichever is greater. Compliance with the maximum flue gas flow rate operating limit must be determined continuously on a 1-hour block basis.

(iii) The owner or operator must maintain the thermal oxidizer in accordance with good combustion practices that ensure proper combustion. Good combustion practices include, but are not limited to, proper burner maintenance, proper burner alignment, proper fuel to air distribution and mixing, routine inspection, and preventative maintenance.

(6) If an owner or operator vents emissions through a closed vent system to a control device other than a flare, scrubber with a reactant tank, or thermal oxidizer, then the owner or operator must comply with § 63.148, and the owner or operator must monitor the operating parameters identified in paragraph (a)(2)(viii) of this section and meet the established operating parameter limits to ensure continuous compliance. The frequency of monitoring and averaging time will be determined based upon the information provided to the Administrator.

[89 FR 43193, May 16, 2024]

## § 63.125 [Reserved]

#### § 63.126 Transfer operations provisions—reference control technology.

(a) For each Group 1 transfer rack the owner or operator shall equip each transfer rack with a vapor collection system and control device.

(1) Each vapor collection system shall be designed and operated to collect the organic hazardous air pollutants vapors displaced from tank trucks or railcars during loading, and to route the collected hazardous air pollutants vapors to a process, or to a fuel gas system, or to a control device as provided in <u>paragraph (b)</u> of this section.

(2) Each vapor collection system shall be designed and operated such that organic HAP vapors collected at one loading arm will not pass through another loading arm in the rack to the atmosphere.

(3) Whenever organic hazardous air pollutants emissions are vented to a process, fuel gas system, or control device used to comply with the provisions of this subpart, the process, fuel gas system, or control device shall be operating.

(b) For each Group 1 transfer rack the owner or operator shall comply with <u>paragraph (b)(1)</u>, (b)(2), (b)(3), or (b)(4) of this section.

(1) Use a control device to reduce emissions of total organic hazardous air pollutants by 98 weight-percent or to an exit concentration of 20 parts per million by volume. For combustion devices, the emission reduction or concentration shall be calculated on a dry basis, corrected to 3-percent oxygen. If a boiler or process heater is used to comply with the percent reduction requirement, then the vent stream shall be introduced into the flame zone of such a device. Compliance may be achieved by using any combination of combustion, recovery, and/or recapture devices.

(2) Reduce emissions of organic HAP's using a flare.

(i) Except as specified in  $\S 63.108(a)$ , the flare shall comply with the requirements of  $\S 63.11(b)$ .

(ii) Halogenated vent streams, as defined in <u>§ 63.111 of this subpart</u>, shall not be vented to a flare.

(3) Reduce emissions of organic hazardous air pollutants using a vapor balancing system designed and operated to collect organic hazardous air pollutants vapors displaced from tank trucks or railcars during loading; and to route the collected hazardous air pollutants vapors to the storage vessel from which the liquid being loaded originated, or to another storage vessel connected to a common header, or to compress and route to a process collected hazardous air pollutants vapors.

(4) Route emissions of organic hazardous air pollutants to a fuel gas system or to a process where the organic hazardous air pollutants in the emissions shall predominantly meet one of, or a combination of, the ends specified in <u>paragraphs</u> (b)(4)(i) through (b)(4)(iv) of this section.

(i) Recycled and/or consumed in the same manner as a material that fulfills the same function in that process;

(ii) Transformed by chemical reaction into materials that are not organic hazardous air pollutants;

(iii) Incorporated into a product; and/or

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(iv) Recovered.

(c) For each Group 2 transfer rack, the owner or operator shall maintain records as required in  $\frac{63.130(f)}{10}$ . No other provisions for transfer racks apply to the Group 2 transfer rack.

(d) Halogenated emission streams from Group 1 transfer racks that are combusted shall be controlled according to <u>paragraph</u> (d)(1) or (d)(2) of this section. Determination of whether a vent stream is halogenated shall be made using procedures in (d)(3).

(1) If a combustion device is used to comply with <u>paragraph (b)(1)</u> of this section for a halogenated vent stream, then the vent stream exiting the combustion device shall be ducted to a halogen reduction device, including, but not limited to, a scrubber before it is discharged to the atmosphere.

(i) Except as provided in <u>paragraph (d)(1)(ii)</u> of this section, the halogen reduction device shall reduce overall emissions of hydrogen halides and halogens, as defined in  $\S$  63.111, by 99 percent or shall reduce the outlet mass emission rate of total hydrogen halides and halogens to 0.45 kilograms per hour or less.

(ii) If a scrubber or other halogen reduction device was installed prior to December 31, 1992, the halogen reduction device shall reduce overall emissions of hydrogen halides and halogens, as defined in  $\S$  63.111, by 95 percent or shall reduce the outlet mass of total hydrogen halides and halogens to less than 0.45 kilograms per hour.

(2) A halogen reduction device, such as a scrubber, or other technique may be used to make the vent stream non-halogenated by reducing the vent stream halogen atom mass emission rate to less than 0.45 kilograms per hour prior to any combustion control device used to comply with the requirements of <u>paragraphs (b)(1)</u> or <u>(b)(2)</u> of this section.

(3) In order to determine whether a vent stream is halogenated, the mass emission rate of halogen atoms contained in organic compounds shall be calculated.

(i) The vent stream concentration of each organic compound containing halogen atoms (parts per million by volume by compound) shall be determined based on the following procedures:

(A) Process knowledge that no halogen or hydrogen halides are present in the process, or

(B) Applicable engineering assessment as specified in  $\S 63.115(d)(1)(iii)$ , or

(C) Concentration of organic compounds containing halogens measured by Method 18 of appendix A to <u>part 60 of this</u> <u>chapter</u>,

(D) Any other method or data that has been validated according to the applicable procedures in Method 301 of <u>appendix A of</u> <u>this part</u>, or

(E) ASTM D6420-18 (incorporated by reference, see  $\frac{63.14}{10}$  may also be used in lieu of Method 18 of appendix A-6 to part <u>60 of this chapter</u>, if the target compounds are all known and are all listed in <u>section 1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method.

(ii) The following equation shall be used to calculate the mass emission rate of halogen atoms:

$$\mathbf{E} = \mathbf{K}_{2} \mathbf{V}_{s} \left( \sum_{j=1}^{n} \sum_{i=1}^{m} \mathbf{C}_{j} * \mathbf{L}_{ji} * \mathbf{M}_{ji} \right)$$

where:

E = Mass of halogen atoms, dry basis, kilograms per hour.

 $K_2 = Constant$ , 2.494 × 10<sup>-6</sup> (parts per million)<sup>-1</sup> (kilogram-mole per standard cubic meter) (minute/hour), where standard temperature is 20 °C.

 $C_j$  = Concentration of halogenated compound j in the gas stream, dry basis, parts per million by volume.

 $M_{ji}$  = Molecular weight of halogen atom i in compound j of the gas stream, kilogram per kilogram-mole.

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 $L_{ji}$  = Number of atoms of halogen i in compound j of the gas stream.

 $V_s =$  Flow rate of gas stream, dry standard cubic meters per minute, determined according to  $\frac{63.128(a)(8)}{63.128(a)(8)}$  of this subpart.

j = Halogenated compound j in the gas stream.

i = Halogen atom i in compound j of the gas stream.

n = Number of halogenated compounds j in the gas stream.

m = Number of different halogens i in each compound j of the gas stream.

(e) For each Group 1 transfer rack the owner or operator shall load organic HAP's into only tank trucks and railcars which:

(1) Have a current certification in accordance with the U. S. Department of Transportation pressure test requirements of <u>49</u> <u>CFR part 180</u> for tank trucks and <u>49 CFR 173.31</u> for railcars; or

(2) Have been demonstrated to be vapor-tight within the preceding 12 months, as determined by the procedures in  $\frac{63.128(f)}{50.128(f)}$  of this subpart. Vapor-tight means that the truck or railcar tank will sustain a pressure change of not more than 750 pascals within 5 minutes after it is pressurized to a minimum of 4,500 pascals.

(f) The owner or operator of a transfer rack subject to the provisions of this subpart shall load organic HAP's to only tank trucks or railcars equipped with vapor collection equipment that is compatible with the transfer rack's vapor collection system.

(g) The owner or operator of a transfer rack subject to this subpart shall load organic HAP's to only tank trucks or railcars whose collection systems are connected to the transfer rack's vapor collection systems.

(h) Except as specified in <u>paragraph (h)(1)</u> of this section, the owner or operator of a transfer rack subject to the provisions of this subpart shall ensure that no pressure-relief device in the transfer rack's vapor collection system or in the organic hazardous air pollutants loading equipment of each tank truck or railcar shall begin to open during loading. Pressure relief devices needed for safety purposes are not subject to this <u>paragraph (h)</u>.

(1) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), this paragraph (h) does not apply. Instead, pressure relief devices are subject to the requirements specified in § 63.165(e).

(2) [Reserved]

(i) Each valve in the vent system that would divert the vent stream to the atmosphere, either directly or indirectly, shall be secured in a non-diverting position using a carseal or a lock-and-key type configuration, or shall be equipped with a flow indicator. Except as specified in <u>paragraph (i)(1)</u> of this section, equipment such as low leg drains, high point bleeds, analyzer vents, open-ended valves or lines, and pressure relief devices needed for safety purposes is not subject to this <u>paragraph (i)</u>.

(1) For each source as defined in § 63.101, on and after July 15, 2027, the last sentence in <u>paragraph (i)</u> of this section no longer applies. Instead, the exemptions specified in <u>paragraphs (i)(1)(i)</u> and <u>(ii)</u> of this section apply.

(i) Except for pressure relief devices subject to  $\frac{63.165(e)(4)}{63.165(e)(4)}$  of subpart H of this part, equipment such as low leg drains and equipment subject to the requirements of subpart H of this part are not subject to this paragraph (i).

(ii) Open-ended valves or lines that use a cap, blind flange, plug, or second valve and follow the requirements specified in § 60.482-6(a)(2), (b), and (c) or follow requirements codified in another regulation that are the same as § 60.482-6(a)(2), (b), and (c) are not subject to this paragraph (i).

(2) [Reserved]

[59 FR 19468, Apr. 22, 1994, as amended at 62 FR 2749, Jan. 17, 1997; 89 FR 43196, May 16, 2024]

## § 63.127 Transfer operations provisions—monitoring requirements.

(a) Each owner or operator of a Group 1 transfer rack equipped with a combustion device used to comply with the 98 percent total organic hazardous air pollutants reduction or 20 parts per million by volume outlet concentration requirements in § 63.126(b)(1) of this subpart shall install, calibrate, maintain, and operate according to the manufacturers' specifications (or other written procedures that provide adequate assurance that the equipment would reasonably be expected to monitor accurately) the monitoring equipment specified in paragraph (a)(1), (a)(2), (a)(3), or (a)(4) of this section, as appropriate.

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(1) Where an incinerator is used, a temperature monitoring device equipped with a continuous recorder is required.

(i) Where an incinerator other than a catalytic incinerator is used, a temperature monitoring device shall be installed in the firebox or in the ductwork immediately downstream of the firebox in a position before any substantial heat exchange occurs.

(ii) Where a catalytic incinerator is used, temperature monitoring devices shall be installed in the gas stream immediately before and after the catalyst bed.

(2) Where a flare is used, except as specified in  $\S$  <u>63.108(a)</u>, a device (including but not limited to a thermocouple, infrared sensor, or an ultra-violet beam sensor) capable of continuously detecting the presence of a pilot flame is required.

(3) Where a boiler or process heater with a design heat input capacity less than 44 megawatts is used, a temperature monitoring device in the firebox equipped with a continuous recorder is required. Any boiler or process heater in which all vent streams are introduced with the primary fuel or are used as the primary fuel is exempt from this requirement.

(4) Where a scrubber is used with an incinerator, boiler, or process heater in the case of halogenated vent streams, the following monitoring equipment is required for the scrubber:

(i) A pH monitoring device equipped with a continuous recorder shall be installed to monitor the pH of the scrubber effluent.

(ii) A flow meter equipped with a continuous recorder shall be located at the scrubber influent for liquid flow. Gas stream flow shall be determined using one of the procedures specified in paragraphs (a)(4)(ii)(A) through (a)(4)(ii)(C) of this section.

(A) The owner or operator may determine gas stream flow using the design blower capacity, with appropriate adjustments for pressure drop.

(B) If the scrubber is subject to regulations in <u>40 CFR parts 264</u> through <u>266</u> that have required a determination of the liquid to gas (L/G) ratio prior to the applicable compliance date for this subpart specified in <u>§ 63.100(k)</u> of <u>subpart F of this part</u>, the owner or operator may determine gas stream flow by the method that had been utilized to comply with those regulations. A determination that was conducted prior to the compliance date for this subpart may be utilized to comply with this subpart if it is still representative.

(C) The owner or operator may prepare and implement a gas stream flow determination plan that documents an appropriate method which will be used to determine the gas stream flow. The plan shall require determination of gas stream flow by a method which will at least provide a value for either a representative or the highest gas stream flow anticipated in the scrubber during representative operating conditions other than start-ups, shutdowns, or malfunctions. The plan shall include a description of the methodology to be followed and an explanation of how the selected methodology will reliably determine the gas stream flow, and a description of the records that will be maintained to document the determination of gas stream flow. The owner or operator shall maintain the plan as specified in  $\S 63.103(c)$ . For each source as defined in  $\S 63.101$ , on and after July 15, 2027, the phrase "other than start-ups, shutdowns, or malfunctions" in this paragraph no longer applies.

(b) Each owner or operator of a Group 1 transfer rack that uses a recovery device or recapture device to comply with the 98percent organic hazardous air pollutants reduction or 20 parts per million by volume hazardous air pollutants concentration requirements in § 63.126(b)(1) of this subpart shall install either an organic monitoring device equipped with a continuous recorder, or the monitoring equipment specified in paragraph (b)(1), (b)(2), or (b)(3) of this section, depending on the type of recovery device or recapture device used. All monitoring equipment shall be installed, calibrated, and maintained according to the manufacturer's specifications or other written procedures that provide adequate assurance that the equipment would reasonably be expected to monitor accurately.

(1) Where an absorber is used, a scrubbing liquid temperature monitoring device equipped with a continuous recorder shall be used; and a specific gravity monitoring device equipped with a continuous recorder shall be used.

(2) Where a condenser is used, a condenser exit (product side) temperature monitoring device equipped with a continuous recorder shall be used.

(3) Except as specified in paragraph (b)(4) of this section, where a carbon adsorber is used, an integrating regeneration stream flow monitoring device having an accuracy of  $\pm 10$  percent or better, capable of recording the total regeneration stream mass flow for each regeneration cycle; and a carbon bed temperature monitoring device, capable of recording the temperature of the carbon bed after regeneration and within 15 minutes of completing any cooling cycle shall be used.

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(4) Beginning no later than the compliance dates specified in  $\S 63.100(k)(10)$ , if the owner or operator vents emissions through a closed vent system to an adsorber(s) that cannot be regenerated or a regenerative adsorber(s) that is regenerated offsite, then the owner or operator must install a system of two or more adsorber units in series and comply with the requirements specified in paragraphs (b)(4)(i) through (iii) of this section.

(i) Conduct an initial performance test or design evaluation of the adsorber and establish the breakthrough limit and adsorber bed life.

(ii) Monitor the HAP or total organic compound (TOC) concentration through a sample port at the outlet of the first adsorber bed in series according to the schedule in <u>paragraph (b)(4)(iii)(B)</u> of this section. The owner or operator must measure the concentration of HAP or TOC using either a portable analyzer, in accordance with Method 21 of appendix A-7 to <u>part 60 of this chapter</u> using methane, propane, isobutylene, or the primary HAP being controlled as the calibration gas.

(iii) Comply with <u>paragraph (b)(4)(iii)(A)</u> of this section and comply with the monitoring frequency according to <u>paragraph</u> (b)(4)(iii)(B) of this section.

(A) The first adsorber in series must be replaced immediately when breakthrough, as defined in § 63.101, is detected between the first and second adsorber. The original second adsorber (or a fresh canister) will become the new first adsorber and a fresh adsorber will become the second adsorber. For purposes of this paragraph, "immediately" means within 8 hours of the detection of a breakthrough for adsorbers of 55 gallons or less, and within 24 hours of the detection of a breakthrough for adsorber or operator must monitor at the outlet of the first adsorber within 3 days of replacement to confirm it is performing properly.

(B) Based on the adsorber bed life established according to <u>paragraph (b)(4)(i)</u> of this section and the date the adsorbent was last replaced, conduct monitoring to detect breakthrough at least monthly if the adsorbent has more than 2 months of life remaining, at least weekly if the adsorbent has between 2 months and 2 weeks of life remaining, and at least daily if the adsorbent has 2 weeks or less of life remaining.

(c) An owner or operator of a Group 1 transfer rack may request approval to monitor parameters other than those listed in paragraph (a) or (b) of this section. The request shall be submitted according to the procedures specified in  $\S$  63.151(f) or  $\S$  63.152(e) of this subpart. Approval shall be requested if the owner or operator:

(1) Seeks to demonstrate compliance with the standards specified in  $\S$  63.126(b) of this subpart with a control device other than an incinerator, boiler, process heater, flare, absorber, condenser, or carbon adsorber; or

(2) Uses one of the control devices listed in <u>paragraphs (a)</u> and <u>(b)</u> of this section, but seeks to monitor a parameter other than those specified in paragraphs (a) and (b) of this subpart.

(d) The owner or operator of a Group 1 transfer rack using a closed vent system that contains bypass lines that could divert a vent stream flow away from the control device used to comply with § 63.126(b) shall comply with paragraph (d)(1) or (2) and (d)(3) of this section. Except as specified in paragraph (d)(3) of this section, equipment such as low leg drains, high point bleeds, analyzer vents, open-ended valves or lines, and pressure relief valves needed for safety purposes are not subject to this paragraph.

(1) Properly install, maintain, and operate a flow indicator that takes a reading at least once every 15 minutes. Records shall be generated as specified in  $\frac{63.130(b)}{2}$ . The flow indicator shall be installed at the entrance to any bypass line that could divert the vent stream away from the control device to the atmosphere; or

(2) Secure the bypass line valve in the closed position with a car-seal or a lock-and-key type configuration.

(i) A visual inspection of the seal or closure mechanism shall be performed at least once every month to ensure that the valve is maintained in the closed position and the vent stream is not diverted through the bypass line.

(ii) If a car-seal has been broken or a valve position changed, the owner or operator shall record that the vent stream has been diverted. The car-seal or lock-and-key combination shall be returned to the secured position as soon as practicable but not later than 15 calendar days after the change in position is detected.

(3) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$  63.100(k)(10):

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(i) The use of a bypass line at any time on a closed vent system to divert emissions (subject to the emission standards in  $\S$  <u>63.112</u>) to the atmosphere or to a control device not meeting the requirements specified in this subpart is an emissions standards violation.

(ii) The last sentence in <u>paragraph (d)</u> of this section no longer applies. Instead, the exemptions specified in <u>paragraph (d)(3)(ii)(A)</u> and (B) of this section apply.

(A) Except for pressure relief devices subject to  $\frac{63.165(e)(4)}{63.165(e)(4)}$ , equipment such as low leg drains and equipment subject to the requirements of subpart H of this part are not subject to this paragraph (d).

(B) Open-ended values or lines that use a cap, blind flange, plug, or second value and follow the requirements specified in § 60.482-6(a)(2), (b), and (c) or follow requirements codified in another regulation that are the same as § 60.482-6(a)(2), (b), and (c) are not subject to this paragraph (d).

(e) The owner or operator shall establish a range that indicates proper operation of the control device for each parameter monitored under <u>paragraphs (a), (b)</u>, and (c) of this section. In order to establish the range, the information required in § 63.152(b)(2) of this subpart shall be submitted in the Notification of Compliance Status or the operating permit application or amendment.

[59 FR 19468, Apr. 22, 1994, as amended at <u>62 FR 2749</u>, Jan. 17, 1997; <u>89 FR 43197</u>, May 16, 2024]

#### § 63.128 Transfer operations provisions—test methods and procedures.

(a) A performance test is required for determining compliance with the reduction of total organic HAP emissions in  $\S$  <u>63.126(b) of this subpart</u> for all control devices except as specified in <u>paragraph (c)</u> of this section. Performance test procedures are as follows:

(1) For control devices shared between transfer racks and process vents, the performance test procedures in  $\S$  63.116(c) of this subpart shall be followed.

(2) A performance test shall consist of three runs.

(3) All testing equipment shall be prepared and installed as specified in the appropriate test methods.

(4) For control devices shared between multiple arms that load simultaneously, the minimum sampling time for each run shall be 1 hour in which either an integrated sample or a minimum of four grab samples shall be taken. If grab sampling is used, then the samples shall be taken at approximately equal intervals in time, such as 15-minute intervals during the run.

(5) For control devices that are capable of continuous vapor processing but do not meet the conditions in (a)(7)(i)(B) of this section.

(A) Sampling sites shall be located at the inlet and outlet of the control device, except as provided in <u>paragraph (a)(7)(i)(B)</u> of this section.

(B) If a vent stream is introduced with the combustion air or as a secondary fuel into a boiler or process heater with a design capacity less than 44 megawatts, selection of paragraph (a)(1) or (a)(4) of this section, each run shall represent at least one complete filling period, during which liquid organic HAP's are loaded, and samples shall be collected using integrated sampling or grab samples taken at least four times per hour at approximately equal intervals of time, such as 15-minute intervals.

(6) For intermittent vapor processing systems that do not meet the conditions in <u>paragraph (a)(1)</u> or <u>(a)(4)</u> of this section, each run shall represent at least one complete control device cycle, and samples shall be collected using integrated sampling or grab samples taken at least four times per hour at approximately equal intervals of time, such as 15-minute intervals.

(7) Method 1 or 1A of 40 CFR part 60, appendix A, as appropriate, shall be used for selection of sampling sites.

(i) For an owner or operator complying with the 98-percent total organic HAP reduction requirements in § 63.126(b)(1) of this subpart, sampling sites shall be located as specified in paragraph (a)(7)(i)(A) or (a)(7)(i)(B) of this section.

(A) Sampling sites shall be located at the inlet and outlet of the control device, except as provided in <u>paragraph (a)(7)(i)(B)</u> of this section.

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(B) If a vent stream is introduced with the combustion air or as a secondary fuel into a boiler or process heater with a design capacity less than 44 megawatts, selection of the location of the inlet sampling sites shall ensure the measurement of total organic HAP or TOC (minus methane and ethane) concentrations in all vent streams and primary and secondary fuels introduced into the boiler or process heater. A sampling site shall also be located at the outlet of the boiler or process heater.

(ii) For an owner or operator complying with the 20 parts per million by volume limit in  $\S$  63.126(b)(1) of this subpart, the sampling site shall be located at the outlet of the control device.

(8) The volumetric flow rate, in standard cubic meters per minute at 20 °C, shall be determined using Method 2, 2A, 2C, or 2D of <u>40 CFR part 60, appendix A</u> as appropriate.

(9) For the purpose of determining compliance with the 20 parts per million by volume limit in § 63.126(b)(1), Method 18 or Method 25A of appendices A-6 and A-7 to part 60 of this chapter, respectively, shall be used to measure either organic compound concentration or organic HAP concentration, except as provided in paragraphs (a)(11) and (12) of this sec

(i) If Method 25A of appendix A-7 to <u>part 60 of this chapter</u> is used, the following procedures shall be used to calculate the concentration of organic compounds ( $C_T$ ):

(A) The principal organic HAP in the vent stream shall be used as the calibration gas.

(B) The span value for Method 25A of appendix A-7 to <u>part 60 of this chapter</u> shall be between 1.5 and 2.5 times the concentration being measured.

(C) Use of Method 25A of appendix A-7 to <u>part 60 of this chapter</u> is acceptable if the response from the high-level calibration gas is at least 20 times the standard deviation of the response from the zero calibration gas when the instrument is zeroed on the most sensitive scale.

(D) The concentration of TOC shall be corrected to 3 percent oxygen using the procedures and equation in <u>paragraph</u> (a)(9)(v) of this section.

(ii) If Method 18 of appendix A-6 to  $\frac{40 \text{ CFR part } 60}{63.14}$  is used to measure the concentration of organic compounds or ASTM D6420-18 (incorporated by reference, see § 63.14), the organic compound concentration (CT) is the sum of the individual components and shall be computed for each run using the following equation:

Equation 1 to Paragraph (a)(9)(ii)

Where:

C<sub>T</sub> = Total concentration of organic compounds (minus methane and ethane), dry basis, parts per million by volume.

C<sub>j</sub> = Concentration of sample components j, dry basis, parts per million by volume.

n = Number of components in the sample.

(iii) If an owner or operator uses Method 18 of appendix A-6 to  $\frac{40 \text{ CFR part 60}}{40 \text{ cFR part 60}}$  or ASTM D6420-18 (incorporated by reference, see § 63.14) to compute total organic HAP concentration rather than organic compounds concentration, the equation in paragraph (a)(9)(ii) of this section shall be used except that only organic HAP species shall be summed. The list of organic HAP's is provided in table 2 to subpart F of this part.

(v) The organic compound concentration corrected to 3 percent oxygen (Cc) shall be calculated using the following equation:

Equation 2 to Paragraph (a)(9)(v)

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$$C_{c} = C_{T} \left( \frac{17.9}{20.9 - \% O_{2d}} \right)$$

Where:

Cc = Concentration of organic compounds corrected to 3 percent oxygen, dry basis, parts per million by volume.

 $C_T$  = Total concentration of organic compounds, dry basis, parts per million by volume.

%O2d = Concentration of oxygen, dry basis, percent by volume.

(10) For the purpose of determining compliance with the 98-percent reduction requirement in  $\S$  63.126(b)(1), Method 18 or Method 25A of appendices A-6 and A-7 to part 60 of this chapter, respectively, shall be used, except as provided in paragraphs (a)(11) and (12) of this section.

(i) For the purpose of determining compliance with the reduction efficiency requirement, organic compound concentration may be measured in lieu of organic HAP concentration.

(ii) If Method 25A of appendix A-7 to <u>part 60 of this chapter</u> is used to measure the concentration of organic compounds  $(C_T)$ , the principal organic HAP in the vent stream shall be used as the calibration gas.

(A) An emission testing interval shall consist of each 15-minute period during the performance test. For each interval, a reading from each measurement shall be recorded.

(B) The average organic compound concentration and the volume measurement shall correspond to the same emissions testing interval.

(C) The mass at the inlet and outlet of the control device during each testing interval shall be calculated as follows:

Equation 3 to Paragraph (a)(10)(ii)(C)

 $Mj = FKVs C_T$ 

Where:

Mj = Mass of organic compounds emitted during testing interval j, kilograms.

Vs = Volume of air-vapor mixture exhausted at standard conditions, 20 °C and 760 millimeters mercury, standard cubic meters.

 $C_T$  = Total concentration of organic compounds (as measured) at the exhaust vent, parts per million by volume, dry basis.

K = Density, kilograms per standard cubic meter organic HAP. 659 kilograms per standard cubic meter organic HAP. (Note: The density term cancels out when the percent reduction is calculated. Therefore, the density used has no effect. The density of hexane is given so that it can be used to maintain the units of Mj.)

 $F = 10^{-6} = Conversion factor, (cubic meters organic HAP per cubic meters air) * (parts per million by volume)^{-1}$ .

(D) The organic compound mass emission rates at the inlet and outlet of the control device shall be calculated as follows:

Equations 4 and 5 to Paragraph (a)(10)(ii)(D)

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$$E_o = \frac{\sum_{j=1}^{n} M_{oj}}{T}$$

Where:

 $E_i$ ,  $E_o$  = Mass flow rate of organic compounds at the inlet (i) and outlet (o) of the combustion or recovery device, kilograms per hour.

M<sub>ij</sub>, M<sub>oj</sub> = Mass of organic compounds at the inlet (i) or outlet (o) during testing interval j, kilograms.

T = Total time of all testing intervals, hours.

n = Number of testing intervals.

(iii) If Method 18 of appendix A-6 to  $\frac{40 \text{ CFR part 60}}{18 \text{ or ASTM D6420-18}}$  (incorporated by reference, see  $\frac{63.14}{18}$ ) is used to measure organic compounds, the mass rates of organic compounds (Ei, Eo) shall be computed using the following equations:

Equations 6 and 7 to Paragraph (a)(10)(iii)

$$E_i = K_2 \left( \sum_{j=1}^n C_{ij} M W_{ij} \right) Q_i$$

$$E_o = K_2 \left( \sum_{j=1}^n C_{oj} M W_{oj} \right) Q_o$$

Where:

 $C_{ij}$ ,  $C_{oj}$  = Concentration of sample component j of the gas stream at the inlet and outlet of the control device, respectively, dry basis, parts per million by volume.

 $MW_{ij}$ ,  $MW_{oj}$  = Molecular weight of sample component j of the gas stream at the inlet and outlet of the control device, respectively, gram/gram-mole.

 $Q_i$ ,  $Q_o$  = Flow rate of gas stream at the inlet and outlet of the control device, respectively, dry standard cubic meter per minute.

 $K_2 = Constant$ , 2.494 × 10<sup>-6</sup> (parts per million)<sup>-1</sup> (gram-mole per standard cubic meter) (kilogram/gram) (minute/hour), where standard temperature for (gram-mole per standard cubic meter) is 20 °C.

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(iv) Where Method 18 or 25A of appendices A-6 and A-7 to <u>part 60 of this chapter</u>, respectively, or ASTM D6420-18 (incorporated by reference, see  $\S$  63.14) is used to measure the percent reduction in organic compounds, the percent reduction across the control device shall be calculated as follows:

Equation 8 to Paragraph (a)(10)(iv)

$$R = \frac{E_i - E_o}{E_i} (100)$$

Where:

R = Control efficiency of control device, percent.

 $E_i = Mass$  emitted or mass flow rate of organic compounds at the inlet to the combustion or recovery device as calculated under <u>paragraph (a)(10)(ii)(D)</u> or <u>(a)(10)(iii)</u> of this section, kilogram per hour.

 $E_o =$  Mass emitted or mass flow rate of organic compounds at the outlet of the combustion or recovery device, as calculated under <u>paragraph (a)(10)(ii)(D)</u> or <u>(a)(10)(iii)</u> of this section, kilogram per hour.

(11) The owner or operator may use any methods or data other than Method 18 or Method 25A of <u>40 CFR part 60, appendix</u> <u>A</u>, if the method or data has been validated according to Method 301 of <u>appendix A of this part</u>.

(12) ASTM D6420-18 (incorporated by reference, see  $\frac{63.14}{10}$ ) may also be used in lieu of Method 18 of appendix A-6 to <u>part 60 of this chapter</u>, if the target compounds are all known and are all listed in <u>section 1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method.

(b) Except as specified in  $\S$  63.108(a), when a flare is used to comply with  $\S$  63.126(b)(2), the owner or operator shall comply with paragraphs (b)(1) through (3) of this section. The owner or operator is not required to conduct a performance test to determine percent emission reduction or outlet organic HAP or TOC concentration.

(1) Conduct a visible emission test using the techniques specified in  $\S 63.11(b)(4)$ . The observation period shall be as specified in <u>paragraph (b)(1)(i)</u> or (ii) of this section instead of the 2-hour period specified in  $\S 63.11(b)(4)$ .

(i) If the loading cycle is less than 2 hours, then the observation period for that run shall be for the entire loading cycle.

(ii) If additional loading cycles are initiated within the 2-hour period, then visible emission observations shall be conducted for the additional cycles.

(2) Determine the net heating value of the gas being combusted, using the techniques specified in  $\frac{63.11(b)(6)}{6}$ .

(3) Determine the exit velocity using the techniques specified in either  $\S 63.11(b)(7)(i)$  (and  $\S 63.11(b)(7)(ii)$ , where applicable) or  $\S 63.11(b)(8)$ , as appropriate.

(c) An owner or operator is not required to conduct a performance test when any of the conditions specified in <u>paragraphs</u> (c)(1) through (c)(7) of this section are met.

(1) When a boiler or process heater with a design heat input capacity of 44 megawatts or greater is used.

(2) When a boiler or process heater burning hazardous waste is used for which the owner or operator:

(i) Has been issued a final permit under <u>part 270 of this chapter</u> and complies with the requirements of part 266, subpart H, of this chapter;

(ii) Has certified compliance with the interim status requirements of part 266, subpart H, of this chapter;

(iii) Has submitted a Notification of Compliance under <u>§ 63.1207(j)</u> and complies with the requirements of <u>subpart EEE of</u> this part; or

(iv) Complies with <u>subpart EEE of this part</u> and will submit a Notification of Compliance under <u>§ 63.1207(j)</u> by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

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(3) When emissions are routed to a fuel gas system or when a boiler or process heater is used and the vent stream is introduced with the primary fuel.

(4) When a vapor balancing system is used.

(5) When emissions are recycled to a chemical manufacturing process unit.

(6) When a transfer rack transfers less than 11.8 million liters per year and the owner or operator complies with the requirements in <u>paragraph (h)</u> of this section or uses a flare to comply with  $\frac{63.126(b)(2)}{5.126(b)(2)}$  of this subpart.

(7) When a hazardous waste incinerator is used for which the owner or operator:

(i) Has been issued a final permit under <u>part 270 of this chapter</u> and complies with the requirements of part 264, subpart O, of this chapter;

(ii) Has certified compliance with the interim status requirements of part 265, subpart O, of this chapter;

(iii) Has submitted a Notification of Compliance under  $\frac{63.1207(j)}{2}$  and complies with the requirements <u>subpart EEE of this</u> part; or

(iv) Complies with the requirements subpart EEE of this part and will submit a Notification of Compliance under  $\S$  <u>63.1207(j)</u> by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(d) An owner or operator using a combustion device followed by a scrubber or other halogen reduction device to control a halogenated transfer vent stream in compliance with § 63.126(d) of this subpart shall conduct a performance test to determine compliance with the control efficiency or emission limits for hydrogen halides and halogens.

(1) For an owner or operator determining compliance with the percent reduction of total hydrogen halides and halogens, sampling sites shall be located at the inlet and outlet of the scrubber or other halogen reduction device used to reduce halogen emissions. For an owner or operator complying with the 0.45 kilogram per hour outlet mass emission rate limit for total hydrogen halides and halogens, the sampling site shall be located at the outlet of the scrubber or other halogen reduction device and prior to release to the atmosphere.

(2) Except as provided in <u>paragraph (d)(5)</u> of this section, Method 26 or 26A of  $\frac{40 \text{ CFR part 60, appendix A}}{40 \text{ cFR part 60, appendix A}}$ , shall be used to determine the concentration in milligrams per dry standard cubic meter of the hydrogen halides and halogens that may be present in the stream. The mass emission rate of each hydrogen halide and halogen compound shall be calculated from the concentrations and the gas stream flow rate.

(3) To determine compliance with the percent emissions reduction limit, the mass emission rate for any hydrogen halides and halogens present at the scrubber inlet shall be summed together. The mass emission rate of the compounds present at the scrubber outlet shall be summed together. Percent reduction shall be determined by comparison of the summed inlet and outlet measurements.

(4) To demonstrate compliance with the 0.45 kilograms per hour mass emission rate limit, the test results must show that the mass emission rate of the total hydrogen halides and halogens measured at the scrubber outlet is below 0.45 kilograms per hour.

(5) The owner or operator may use any other method or data to demonstrate compliance if the method or data has been validated according to the protocol of Method 301 of <u>appendix A of this part</u>.

(e) The owner or operator shall inspect the vapor collection system and vapor balancing system, according to the requirements for vapor collection systems in  $\S$  63.148 of this subpart.

(1) Inspections shall be performed only while a tank truck or railcar is being loaded.

(2) For vapor collection systems only, an inspection shall be performed prior to each performance test required to demonstrate compliance with  $\S$  63.126(b)(1) of this subpart.

(3) For each vapor collection system that is operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements specified in  $\frac{63.148}{5}$  of this subpart.

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(f) For the purposes of demonstrating vapor tightness to determine compliance with  $\S$  63.126(e)(2) of this subpart, the following procedures and equipment shall be used:

(1) The pressure test procedures specified in Method 27 of 40 CFR part 60, appendix A; and

(2) A pressure measurement device which has a precision of  $\pm 2.5$  millimeters of mercury or better and which is capable of measuring above the pressure at which the tank truck or railcar is to be tested for vapor tightness.

(g) An owner or operator using a scrubber or other halogen reduction device to reduce the vent stream halogen atom mass emission rate to less than 0.45 kilograms per hour prior to a combustion device used to comply with § 63.126(d)(2) shall determine the halogen atom mass emission rate prior to the combustor according to the procedures in paragraph (d)(3) of this section.

(h) For transfer racks that transfer less than 11.8 million liters per year of liquid organic HAP's, the owner or operator may comply with the requirements in <u>paragraphs (h)(1)</u> through (h)(3) of this section instead of the requirements in <u>paragraph</u> (a) or (b) of this section.

(1) The owner or operator shall prepare, as part of the Notification of Compliance Status required by  $\frac{63.152(b)}{5.000}$  of this subpart, a design evaluation that shall document that the control device being used achieves the required control efficiency during reasonably expected maximum loading conditions. This documentation is to include a description of the gas stream which enters the control device, including flow and organic HAP content, and the information specified in <u>paragraphs</u> (h)(1)(i) through (h)(1)(v) of this section, as applicable.

(i) If the control device receives vapors, gases, or liquids, other than fuels, from emission points other than transfer racks subject to this subpart, the efficiency demonstration is to include consideration of all vapors, gases, and liquids, other than fuels, received by the control device.

(ii) If an enclosed combustion device with a minimum residence time of 0.5 seconds and a minimum temperature of 760 degrees Celsius is used to meet the 98-percent emission reduction requirement, documentation that those conditions exist is sufficient to meet the requirements of paragraph (h)(1) of this section.

(iii) Except as provided in <u>paragraph (h)(1)(ii)</u> of this section, for thermal incinerators, the design evaluation shall include the autoignition temperature of the organic HAP, the flow rate of the organic HAP emission stream, the combustion temperature, and the residence time at the combustion temperature.

(iv) Except as provided in  $\frac{63.127(b)(4)}{10}$ , for carbon adsorbers, the design evaluation shall include the affinity of the organic HAP vapors for carbon, the amount of carbon in each bed, the number of beds, the humidity of the feed gases, the temperature of the feed gases, the flow rate of the organic HAP emission stream, the desorption schedule, the regeneration stream pressure or temperature, and the flow rate of the regeneration stream. For vacuum desorption, pressure drop shall be included.

(v) For condensers, the design evaluation shall include the final temperature of the organic HAP vapors, the type of condenser, and the design flow rate of the organic HAP emission stream.

(2) The owner or operator shall submit, as part of the Notification of Compliance Status required by  $\frac{63.152(b)}{50.152(b)}$  of this subpart, the operating range for each monitoring parameter identified for each control device. The specified operating range shall represent the conditions for which the control device can achieve the 98-percent-or-greater emission reduction required by  $\frac{63.126(b)}{50.126(b)}$  of this subpart.

(3) The owner or operator shall monitor the parameters specified in the Notification of Compliance Status required in § 63.152(b) of this subpart or operating permit and shall operate and maintain the control device such that the monitored parameters remain within the ranges specified in the Notification of Compliance Status, except as provided in §§ 63.152(c) and 63.152(f) of this subpart.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>61 FR 64576</u>, Dec. 5, 1996; <u>62 FR 2750</u>, Jan. 17, 1997; <u>66 FR 6932</u>, Jan. 22, 2001; <u>89 FR 43198</u>, May 16, 2024]

# § 63.129 Transfer operations provisions—reporting and recordkeeping for performance tests and notification of compliance status.

(a) Each owner or operator of a Group 1 transfer rack shall:

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(1) Keep an up-to-date, readily accessible record of the data specified in <u>paragraphs (a)(4)</u> through  $(\underline{a})(\underline{8})$  of this section, as applicable.

(2) Include the data specified in <u>paragraphs (a)(4)</u> through (a)(7) of this section in the Notification of Compliance Status report as specified in § 63.152(b) of this subpart. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with § 63.152(h), the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the notification of compliance status report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(3) If any subsequent performance tests are conducted after the Notification of Compliance Status has been submitted, report the data in <u>paragraphs (a)(4)</u> through (a)(7) of this section in the next Periodic Report as specified in § 63.152(c) of this subpart.

(4) Record and report the following when using a control device other than a flare to achieve a 98 weight percent reduction in total organic HAP or a total organic HAP concentration of 20 parts per million by volume, as specified in  $\frac{63.126(b)(1)}{100}$  this subpart:

(i) The parameter monitoring results for thermal incinerators, catalytic incinerators, boilers or process heaters, absorbers, condensers, or carbon adsorbers specified in table 7 of this subpart, recorded during the performance test, and averaged over the time period of the performance testing.

(ii) The percent reduction of total organic HAP or TOC achieved by the control device determined as specified in § 63.128(a) of this subpart, or the concentration of total organic HAP or TOC (parts per million by volume, by compound) determined as specified in § 63.128(a) of this subpart at the outlet of the control device. For combustion devices, the concentration shall be reported on a dry basis corrected to 3 percent oxygen.

(iii) The parameters shall be recorded at least every 15 minutes.

(iv) For a boiler or process heater, a description of the location at which the vent stream is introduced into the boiler or process heater.

(5) Except as specified in <u>paragraph (a) of § 63.108</u>, record and report the following when using a flare to comply with § 63.126(b)(2):

(i) Flare design (i.e., steam-assisted, air-assisted, or non-assisted);

(ii) All visible emission readings, heat content determinations, flow rate measurements, and exit velocity determinations made during the compliance determination required by  $\S$  63.128(b) of this subpart; and

(iii) All periods during the compliance determination when the pilot flame is absent.

(6) Record and report the following when using a scrubber following a combustion device to control a halogenated vent stream, as specified in  $\S$  63.126(d) of this subpart:

(i) The percent reduction or scrubber outlet mass emission rate of total hydrogen halides and halogens determined according to the procedures in  $\S$  63.128(d) of this subpart;

(ii) The parameter monitoring results for scrubbers specified in table 7 of this subpart, and averaged over the time period of the performance test; and

(iii) The parameters shall be recorded at least every 15 minutes.

(7) Record and report the halogen concentration in the vent stream determined according to the procedures as specified in  $\S$  <u>63.128(d) of this subpart</u>.

(8) Report that the emission stream is being routed to a fuel gas system or a process, when complying using  $\frac{63.126(b)(4)}{2}$ .

(b) If an owner or operator requests approval to use a control device other than those listed in table 7 of this subpart or to monitor a parameter other than those specified in table 7 of this subpart, the owner or operator shall submit a description of planned reporting and recordkeeping procedures as required under  $\S 63.151(f)$  or  $\S 63.152(e)$  of this subpart. The Administrator will specify appropriate reporting and recordkeeping requirements as part of the review of the permit application or by other appropriate means.

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(c) For each parameter monitored according to table 7 of this subpart or <u>paragraph (b)</u> of this section, the owner or operator shall establish a range for the parameter that indicates proper operation of the control device. In order to establish the range, the information required in § 63.152(b)(2) of this subpart shall be submitted in the Notification of Compliance Status or the operating permit application or amendment.

(d) Each owner or operator shall maintain a record describing in detail the vent system used to vent each affected transfer vent stream to a control device. This document shall list all valves and vent pipes that could vent the stream to the atmosphere, thereby bypassing the control device; identify which valves are secured by car-seals or lock-and-key type configurations; and indicate the position (open or closed) of those valves which have car-seals. Except as specified in paragraph (d)(1) of this section, equipment leaks such as low leg drains, high point bleeds, analyzer vents, open-ended valves or lines, and pressure relief valves needed for safety purposes are not subject to this paragraph.

(1) For each source as defined in § 63.101, on and after July 15, 2027, the last sentence in paragraph (d) of this section no longer applies. Instead, the exemptions specified in paragraph (d)(1)(i) and (d)(1)(ii) of this section apply.

(i) Except for pressure relief devices subject to  $\S 63.165(e)(4)$  of subpart H of this part, equipment such as low leg drains and equipment subject to the requirements of subpart H of this part are not subject to this paragraph (d) of this section.

(ii) Open-ended valves or lines that use a cap, blind flange, plug, or second valve and follow the requirements specified in  $\underline{40}$  <u>CFR 60.482-6(a)(2)</u>, (b), and (c) or follow requirements codified in another regulation that are the same as  $\underline{40}$  <u>CFR 60.482-6(a)(2)</u>, (b), and (c) are not subject to this <u>paragraph (d)</u> of this section.

#### (2) [Reserved]

(e) An owner or operator meeting the requirements of  $\S 63.128(h)$  of this subpart shall submit, as part of the Notification of Compliance Status required by  $\S 63.152(b)$  of this subpart, the information specified in  $\S 63.128(h)(1)$  of this subpart.

(f) An owner or operator meeting the requirements of  $\S$  63.128(h) of this subpart shall submit, as part of the Notification of Compliance Status required by  $\S$  63.152(b) of this subpart, the operating range for each monitoring parameter identified for each control device.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>61 FR 64576</u>, Dec. 5, 1996; <u>62 FR 2750</u>, Jan. 17, 1997; <u>64 FR 20191</u>, Apr. 26, 1999; <u>89 FR 43199</u>, May 16, 2024]

## § 63.130 Transfer operations provisions—periodic recordkeeping and reporting.

(a) Each owner or operator using a control device to comply with  $\frac{63.126(b)(1)}{5}$  or  $\frac{(b)(2)}{5}$  of this subpart shall keep the following up-to-date, readily accessible records:

(1) While the transfer vent stream is being vented to the control device, continuous records of the equipment operating parameters specified to be monitored under § 63.127, and listed in table 7 of this subpart or specified by the Administrator in accordance with §§ 63.127(c) and 63.129(b). For flares complying with § 63.11(b), the hourly records and records of pilot flame outages specified in table 7 shall be maintained in place of continuous records. For flares complying with § 63.108, the owner or operator must comply with the recordkeeping requirements specified therein.

(2) Records of the daily average value of each monitored parameter for each operating day determined according to the procedures specified in  $\S 63.152(f)$ , except as provided in paragraphs (a)(2)(i) through (a)(2)(iv) of this section.

(i) For flares, except as specified in <u>paragraph (a) of § 63.108</u>, records of the times and duration of all periods during which the pilot flame is absent shall be kept rather than daily averages.

(ii) If carbon adsorber regeneration stream flow and carbon bed regeneration temperature are monitored, the records specified in table 7 to this subpart shall be kept instead of the daily averages.

(iii) Except as specified in paragraph (a)(2)(iv) of this section, records of the duration of all periods when the vent stream is diverted through bypass lines shall be kept rather than daily averages.

(iv) For each flow event from a bypass line subject to the requirements in  $\S$  63.127(d) for each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$  63.100(k)(10), the owner or operator must also maintain records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requiring control that is released either directly to the atmosphere or to a control device not meeting the requirements in this subpart, the owner or operator must include an estimate of the volume of gas, the concentration of organic HAP in the

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gas and the resulting emissions of organic HAP that bypassed the control device using process knowledge and engineering estimates.

(3) For boilers or process heaters, records of any changes in the location at which the vent stream is introduced into the flame zone as required under the reduction of total organic HAP emissions in  $\frac{63.126(b)(1)}{5.000}$  of this subpart.

(b) If a vapor collection system containing values that could divert the emission stream away from the control device is used, each owner or operator of a Group 1 transfer rack subject to the provisions of  $\frac{63.127(d)}{10}$  shall keep up-to-date, readily accessible records of:

(1) Hourly records of whether the flow indicator specified under  $\frac{63.127(d)(1)}{10}$  was operating and whether a diversion was detected at any time during the hour, as well as records of the times of all periods when the vent stream is diverted from the control device or the flow indicator is not operating.

(2) Where a seal mechanism is used to comply with  $\frac{63.127(d)(2)}{2}$ , hourly records of flow are not required. In such cases, the owner or operator shall record that the monthly visual inspection of the seals or closure mechanisms has been done, and shall record the occurrence of all periods when the seal mechanism is broken, the bypass line valve position has changed, or the key for a lock-and-key type lock has been checked out, and records of any car-seal that has broken, as listed in table 7 of this subpart.

(3) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in <u>paragraphs (b)(1)</u> and (b)(2) of this section. For each flow event from a bypass line subject to the requirements in § 63.127(d), the owner or operator must maintain records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requirements in records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requirements in the requirements in this subpart, the owner or operator must include an estimate of the volume of gas, the concentration of organic HAP in the gas and the resulting emissions of organic HAP that bypassed the control device using process knowledge and engineering estimates.

(c) Except as specified in <u>paragraph (a) of § 63.108</u>, each owner or operator of a Group 1 transfer rack who uses a flare to comply with § 63.126(b)(2) shall keep up-to-date, readily accessible records of the flare pilot flame monitoring specified under § 63.127(a)(2).

(d) Each owner or operator of a transfer rack subject to the requirements of  $\frac{63.126}{5.126}$  shall submit to the Administrator Periodic Reports of the following information according to the schedule in  $\frac{63.152(c)}{5.152(c)}$ :

(1) Reports of daily average values of monitored parameters for all operating days when the daily average values were outside the range established in the Notification of Compliance Status or operating permit. Additionally, report the identification of the transfer rack, the monitored parameter out of range, and the date of such occurrences.

(2) Reports of the start date and duration (in hours) of periods when monitoring data are not collected for each excursion caused by insufficient monitoring data as defined in  $\frac{63.152(c)(2)(ii)(A)}{2}$ .

(3) Reports of the start date and time and duration (in hours) of all periods recorded under <u>paragraph (b)(1)</u> of this section when the vent stream was diverted from the control device, and if applicable, the information in <u>paragraph (d)(7)</u> of this section.

(4) Reports of the start date and time and duration (in hours) recorded under <u>paragraph (b)(2)</u> of this section when maintenance is performed on car-sealed valves, when the car seal is broken, when the bypass line valve position is changed, or the key for a lock-and-key type configuration has been checked out, and if applicable, the information in <u>paragraph</u> (d)(7) of this section.

(5) Except as specified in <u>paragraph (a) of § 63.108</u>, reports of the times and durations of all periods recorded under <u>paragraph (a)(2)(i)</u> of this section in which all pilot flames of a flare were absent.

(6) Reports of all carbon bed regeneration cycles during which the parameters recorded under <u>paragraph (a)(2)(ii)</u> of this section were outside the ranges established in the Notification of Compliance Status or operating permit. Include the identification of the carbon bed, the monitored parameter that was outside the established range, and the start date, start time, and duration (in hours) for the regeneration cycle in the report.

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(7) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in paragraphs (d)(3) and (d)(4) of this section. For bypass lines subject to the requirements in § 63.127(d), the Periodic Report must include the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours.

(e) The owner or operator of a Group 1 transfer rack shall record that the verification of DOT tank certification or Method 27 testing, required in  $\S$  63.126(e) of this subpart, has been performed. Various methods for the record of verification can be used, such as: A check off on a log sheet; a list of DOT serial numbers or Method 27 data; or a position description for gate security, showing that the security guard will not allow any trucks on site that do not have the appropriate documentation.

(f) Each owner or operator of a Group 1 or Group 2 transfer rack shall record, update annually, and maintain the information specified in <u>paragraphs (f)(1)</u> through (f)(3) of this section in a readily accessible location on site:

(1) An analysis demonstrating the design and actual annual throughput of the transfer rack;

(2) An analysis documenting the weight-percent organic HAP's in the liquid loaded. Examples of acceptable documentation include but are not limited to analyses of the material and engineering calculations.

(3) An analysis documenting the annual rack weighted average HAP partial pressure of the transfer rack.

(i) For Group 2 transfer racks that are limited to transfer of organic HAP's with partial pressures less than 10.3 kilopascals, documentation is required of the organic HAP's (by compound) that are transferred. The rack weighted average partial pressure does not need to be calculated.

(ii) For racks transferring one or more organic HAP's with partial pressures greater than 10.3 kilopascals, as well as one or more organic HAP's with partial pressures less than 10.3 kilopascals, a rack weighted partial pressure shall be documented. The rack weighted average HAP partial pressure shall be weighted by the annual throughput of each chemical transferred.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>62 FR 2750</u>, Jan. 17, 1997; <u>66 FR 6932</u>, Jan. 22, 2001; <u>89 FR 43200</u>, May 16, 2024]

## § 63.131 [Reserved]

## § 63.132 Process wastewater provisions—general.

(a) *Existing sources.* This paragraph specifies the requirements applicable to process wastewater streams located at existing sources. The owner or operator shall comply with the requirements in <u>paragraphs (a)(1)</u> through (a)(3) of this section, no later than the applicable dates specified in § 63.100 of subpart F of this part.

(1) Determine wastewater streams to be controlled for Table 9 compounds. Determine whether each wastewater stream requires control for Table 9 compounds by complying with the requirements in either paragraph (a)(1)(i) or (a)(1)(ii) of this section, and comply with the requirements in paragraph (a)(1)(iii) of this section.

(i) Comply with <u>paragraph (c)</u> of this section, determining whether the wastewater stream is Group 1 or Group 2 for Table 9 compounds; or

(ii) Comply with <u>paragraph (e)</u> of this section, designating the wastewater stream as a Group 1 wastewater stream.

(iii) Comply with <u>paragraph (f)</u> of this section.

(2) Requirements for Group 1 wastewater streams. For wastewater streams that are Group 1 for Table 9 compounds, comply with paragraphs (a)(2)(i) through (a)(2)(iv) of this section.

(i) Comply with the applicable requirements for wastewater tanks, surface impoundments, containers, individual drain systems, and oil/water separators as specified in § 63.133 through § 63.137 of this subpart, except as provided in paragraphs (a)(2)(i)(A) through (a)(2)(i)(C) of this section and § 63.138(a)(3).

(A) Except as specified in <u>paragraph (a)(2)(i)(C)</u> of this section, the waste management units may be equipped with pressure relief devices that vent directly to the atmosphere provided the pressure relief device is not used for planned or routine venting of emissions.

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(B) Except as specified in <u>paragraph (a)(2)(i)(C)</u> of this section, the pressure relief device remains in a closed position at all times except when it is necessary for the pressure relief device to open for the purpose of preventing physical damage or permanent deformation of the waste management unit in accordance with good engineering and safety practices.

(C) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraphs (a)(2)(i)(A) and (a)(2)(i)(B) of this section do not apply. Instead, pressure relief devices are subject to the requirements specified in § 63.165(e) of subpart H of this part.

(ii) Comply with the applicable requirements for control of Table 9 compounds as specified in § 63.138 of this subpart. Alternatively, the owner or operator may elect to comply with the treatment provisions specified in § 63.132(g) of this subpart.

(iii) Comply with the applicable monitoring and inspection requirements specified in § 63.143 of this subpart.

(iv) Comply with the applicable recordkeeping and reporting requirements specified in <u>§§ 63.146</u> and <u>63.147 of this subpart</u>.

(3) Requirements for Group 2 wastewater streams. For wastewater streams that are Group 2 for table 9 compounds, comply with the applicable recordkeeping and reporting requirements specified in  $\frac{\$\$ 63.146(b)(1)}{\$\$ 63.146(b)(1)}$  and  $\frac{63.147(b)(8)}{\$}$ .

(b) *New sources.* This paragraph specifies the requirements applicable to process wastewater streams located at new sources. The owner or operator shall comply with the requirements in <u>paragraphs (b)(1)</u> through (b)(4) of this section, no later than the applicable dates specified in § 63.100 of subpart F of this part.

(1) Determine wastewater streams to be controlled for Table 8 compounds. Determine whether each wastewater stream requires control for Table 8 compounds by complying with the requirements in either paragraph (b)(1)(i) or (b)(1)(ii) of this section, and comply with the requirements in paragraph (b)(1)(iii) of this section.

(i) Comply with <u>paragraph (d)</u> of this section, determining whether the wastewater stream is Group 1 or Group 2 for Table 8 compounds; or

(ii) Comply with <u>paragraph (e)</u> of this section, designating the wastewater stream as a Group 1 wastewater stream for Table 8 compounds.

(iii) Comply with <u>paragraph (f)</u> of this section.

(2) Determine wastewater streams to be controlled for Table 9 compounds. Determine whether each wastewater stream requires control for Table 9 compounds by complying with the requirements in either paragraph (b)(2)(i) or (b)(2)(ii) of this section, and comply with the requirements in paragraph (b)(2)(iii) of this section.

(i) Comply with <u>paragraph (c)</u> of this section, determining whether the wastewater stream is Group 1 or Group 2 for Table 9 compounds; or

(ii) Comply with <u>paragraph (e)</u> of this section, designating the wastewater stream as a Group 1 wastewater stream.

(iii) Comply with <u>paragraph (f)</u> of this section.

(3) Requirements for Group 1 wastewater streams. For wastewater streams that are Group 1 for Table 8 compounds and/or Table 9 compounds, comply with paragraphs (b)(3)(i) through (b)(3)(iv) of this section.

(i) Comply with the applicable requirements for wastewater tanks, surface impoundments, containers, individual drain systems, and oil/water separators specified in the requirements of § 63.133 through § 63.137 of this subpart, except as provided in paragraphs (b)(3)(i)(A) through (b)(3)(i)(C) of this section and § 63.138(a)(3) of this subpart.

(A) Except as specified in <u>paragraph (b)(3)(i)(C)</u> of this section, the waste management units may be equipped with pressure relief devices that vent directly to the atmosphere provided the pressure relief device is not used for planned or routine venting of emissions.

(B) Except as specified in <u>paragraph (b)(3)(i)(C)</u> of this section, the pressure relief device remains in a closed position at all times except when it is necessary for the pressure relief device to open for the purpose of preventing physical damage or permanent deformation of the waste management unit in accordance with good engineering and safety practices.

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(C) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraphs (b)(3)(i)(A) and (b)(3)(i)(B) of this section do not apply. Instead, pressure relief devices are subject to the requirements specified in § 63.165(e).

(ii) Comply with the applicable requirements for control of Table 8 compounds specified in § 63.138 of this subpart. Alternatively, the owner or operator may elect to comply with the provisions specified in § 63.132(g) of this subpart.

(iii) Comply with the applicable monitoring and inspection requirements specified in § 63.143 of this subpart.

(iv) Comply with the applicable recordkeeping and reporting requirements specified in <u>§§ 63.146</u> and <u>63.147 of this subpart</u>.

(4) Requirements for Group 2 wastewater streams. For wastewater streams that are Group 2 for both table 8 and table 9 compounds, comply with the applicable recordkeeping and reporting requirements specified in  $\underline{\$\$}$ <u>63.146(b)(1)</u> and <u>63.147(b)(8)</u>.

(c) How to determine Group 1 or Group 2 status for Table 9 compounds. This paragraph provides instructions for determining whether a wastewater stream is Group 1 or Group 2 for Table 9 compounds. Total annual average concentration shall be determined according to the procedures specified in  $\S$  63.144(b) of this subpart. Annual average flow rate shall be determined according to the procedures specified in  $\S$  63.144(c) of this subpart.

(1) A wastewater stream is a Group 1 wastewater stream for Table 9 compounds if:

(i) The total annual average concentration of Table 9 compounds is greater than or equal to 10,000 parts per million by weight at any flow rate;

(ii) The total annual average concentration of Table 9 compounds is greater than or equal to 1,000 parts per million by weight and the annual average flow rate is greater than or equal to 10 liters per minute; or

(iii) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$  63.100(k)(11), the process wastewater stream contains ethylene oxide such that it is considered to be in ethylene oxide service, as defined in  $\S$  63.101.

(2) A wastewater stream is a Group 2 wastewater stream for Table 9 compounds if it is not a Group 1 wastewater stream for Table 9 compounds by the criteria in paragraph (c)(1) of this section.

(3) The owner or operator of a Group 2 wastewater shall re-determine group status for each Group 2 stream, as necessary, to determine whether the stream is Group 1 or Group 2 whenever process changes are made that could reasonably be expected to change the stream to a Group 1 stream. Examples of process changes include, but are not limited to, changes in production capacity, production rate, feedstock type, or whenever there is a replacement, removal, or addition of recovery or control equipment. For purposes of this paragraph (c)(3), process changes do not include: Process upsets; unintentional, temporary process changes; and changes that are within the range on which the original determination was based.

(d) *How to determine Group 1 or Group 2 status for Table 8 compounds.* This paragraph provides instructions for determining whether a wastewater stream is Group 1 or Group 2 for Table 8 compounds. Annual average concentration for each Table 8 compound shall be determined according to the procedures specified in  $\S$  63.144(b). Annual average flow rate shall be determined according to the procedures specified in  $\S$  63.144(b).

(1) A wastewater stream is a Group 1 wastewater stream for Table 8 compounds if:

(i) The annual average flow rate is 0.02 liter per minute or greater and the annual average concentration of any individual table 8 compound is 10 parts per million by weight or greater; or

(ii) For each source as defined in  $\frac{63.101}{100}$ , beginning no later than the compliance dates specified in  $\frac{63.100(k)(11)}{1000}$ , the process wastewater stream contains ethylene oxide such that it is considered to be in ethylene oxide service, as defined in  $\frac{63.101}{1000}$ .

(2) A wastewater stream is a Group 2 wastewater stream for Table 8 compounds if it does not meet the criteria specified in paragraph (d)(1)(ii) of this section, and the annual average flow rate is less than 0.02 liter per minute or the annual average concentration for each individual Table 8 compound is less than 10 parts per million by weight.

(3) The owner or operator of a Group 2 wastewater shall re-determine group status for each Group 2 stream, as necessary, to determine whether the stream is Group 1 or Group 2 whenever process changes are made that could reasonably be expected

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to change the stream to a Group 1 stream. Examples of process changes include, but are not limited to, changes in production capacity, production rate, feedstock type, or whenever there is a replacement, removal, or addition of recovery or control equipment. For purposes of this <u>paragraph (d)(3)</u>, process changes do not include: Process upsets; unintentional, temporary process changes; and changes that are within the range on which the original determination was based.

(e) How to designate a Group 1 wastewater stream. The owner or operator may elect to designate a wastewater stream a Group 1 wastewater stream in order to comply with <u>paragraph (a)(1)</u> or (b)(1) of this section. To designate a wastewater stream or a mixture of wastewater streams a Group 1 wastewater stream, the procedures specified in <u>paragraphs</u> (e)(1) and (e)(2) of this section and § 63.144(a)(2) of this subpart shall be followed.

(1) From the point of determination for each wastewater stream that is included in the Group 1 designation to the location where the owner or operator elects to designate such wastewater stream(s) as a Group 1 wastewater stream, the owner or operator shall comply with all applicable emission suppression requirements specified in <u>§§ 63.133</u> through <u>63.137</u>.

(2) From the location where the owner or operator designates a wastewater stream or mixture of wastewater streams to be a Group 1 wastewater stream, such Group 1 wastewater stream shall be managed in accordance with all applicable emission suppression requirements specified in <u>§§ 63.133</u> through <u>63.137</u> and with the treatment requirements in <u>§ 63.138 of this part</u>.

(f) Owners or operators of sources subject to this subpart shall not discard liquid or solid organic materials with a concentration of greater than 10,000 parts per million of Table 9 compounds (as determined by analysis of the stream composition, engineering calculations, or process knowledge, according to the provisions of § 63.144(b) of this subpart) from a chemical manufacturing process unit to water or wastewater, unless the receiving stream is managed and treated as a Group 1 wastewater stream. This prohibition does not apply to materials from the activities listed in paragraphs (f)(1) through (f)(4) of this section.

(1) Equipment leaks;

(2) Except as specified in <u>paragraph (f)(5)</u> of this sections, activities included in maintenance or startup/shutdown/malfunction plans;

(3) Spills; or

(4) Samples of a size not greater than reasonably necessary for the method of analysis that is used.

(5) For each source as defined in § 63.101, on and after July 15, 2027, the phrase "or startup/shutdown/malfunction" in paragraph (f)(2) of this section does not apply.

(g) Off-site treatment or on-site treatment not owned or operated by the source. The owner or operator may elect to transfer a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream to an on-site treatment operation not owned or operated by the owner or operator of the source generating the wastewater stream or residual, or to an off-site treatment operation.

(1) The owner or operator transferring the wastewater stream or residual shall:

(i) Comply with the provisions specified in  $\frac{\$\$ 63.133}{\$}$  through  $\underline{63.137}$  of this subpart for each waste management unit that receives or manages a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream prior to shipment or transport.

(ii) Include a notice with the shipment or transport of each Group 1 wastewater stream or residual removed from a Group 1 wastewater stream. The notice shall state that the wastewater stream or residual contains organic hazardous air pollutants that are to be treated in accordance with the provisions of this subpart. When the transport is continuous or ongoing (for example, discharge to a publicly-owned treatment works), the notice shall be submitted to the treatment operator initially and whenever there is a change in the required treatment.

(2) The owner or operator may not transfer the wastewater stream or residual unless the transferee has submitted to the EPA a written certification that the transferee will manage and treat any Group 1 wastewater stream or residual removed from a Group 1 wastewater stream received from a source subject to the requirements of this subpart in accordance with the requirements of either <u>§§ 63.133</u> through <u>63.147</u>, or <u>§ 63.102(b)</u> of subpart F, or <u>subpart D of this part</u> if alternative emission limitations have been granted the transferor in accordance with those provisions. The certifying entity may revoke the written certification by sending a written statement to the EPA and the owner or operator giving at least 90 days notice that the certifying entity is rescinding acceptance of responsibility for compliance with the regulatory provisions listed in this

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paragraph. Upon expiration of the notice period, the owner or operator may not transfer the wastewater stream or residual to the treatment operation.

(3) By providing this written certification to the EPA, the certifying entity accepts responsibility for compliance with the regulatory provisions listed in <u>paragraph (g)(2)</u> of this section with respect to any shipment of wastewater or residual covered by the written certification. Failure to abide by any of those provisions with respect to such shipments may result in enforcement action by the EPA against the certifying entity in accordance with the enforcement provisions applicable to violations of these provisions by owners or operators of sources.

(4) Written certifications and revocation statements, to the EPA from the transferees of wastewater or residuals shall be signed by the responsible official of the certifying entity, provide the name and address of the certifying entity, and be sent to the appropriate EPA Regional Office at the addresses listed in 40 CFR 63.13. Such written certifications are not transferable by the treater.

[<u>62 FR 2751</u>, Jan. 17, 1997, as amended at <u>66 FR 6933</u>, Jan. 22, 2001; <u>71 FR 76614</u>, Dec. 21, 2006; <u>89 FR 43201</u>, May 16, 2024]

#### § 63.133 Process wastewater provisions—wastewater tanks.

(a) For each wastewater tank that receives, manages, or treats a Group 1 wastewater stream or a residual removed from a Group 1 wastewater stream, the owner or operator shall comply with the requirements of either paragraph (a)(1) or (a)(2) of this section as specified in table 10 of this subpart.

(1) The owner or operator shall operate and maintain a fixed roof except that if the wastewater tank is used for heating wastewater, or treating by means of an exothermic reaction or the contents of the tank is sparged, the owner or operator shall comply with the requirements specified in <u>paragraph (a)(2)</u> of this section.

(2) The owner or operator shall comply with the requirements in <u>paragraphs (b)</u> through (h) of this section and shall operate and maintain one of the emission control techniques listed in <u>paragraphs (a)(2)(i)</u> through (a)(2)(iv) of this section.

(i) A fixed roof and a closed vent system that routes the organic hazardous air pollutants vapors vented from the wastewater tank to a control device.

(ii) A fixed roof and an internal floating roof that meets the requirements specified in § 63.119(b) of this subpart;

(iii) An external floating roof that meets the requirements specified in  $\underline{\$\$ 63.119(c)}, \underline{63.120(b)(5)}$ , and  $\underline{63.120(b)(6)}$  of this subpart; or

(iv) An equivalent means of emission limitation. Determination of equivalence to the reduction in emissions achieved by the requirements of <u>paragraphs (a)(2)(i)</u> through <u>(a)(2)(iii)</u> of this section will be evaluated according to § 63.102(b) of <u>subpart F</u> of this part. The determination will be based on the application to the Administrator which shall include the information specified in either <u>paragraph (a)(2)(iv)(A)</u> or <u>(a)(2)(iv)(B)</u> of this section.

(A) Actual emissions tests that use full-size or scale-model wastewater tanks that accurately collect and measure all organic hazardous air pollutants emissions from a given control technique, and that accurately simulate wind and account for other emission variables such as temperature and barometric pressure, or

(B) An engineering evaluation that the Administrator determines is an accurate method of determining equivalence.

(b) If the owner or operator elects to comply with the requirements of <u>paragraph (a)(2)(i)</u> of this section, the fixed roof shall meet the requirements of <u>paragraph (b)(1)</u> of this section, the control device shall meet the requirements of <u>paragraph (b)(2)</u> of this section, and the closed vent system shall meet the requirements of <u>paragraph (b)(3)</u> of this section.

(1) The fixed-roof shall meet the following requirements:

(i) Except as provided in <u>paragraph (b)(4)</u> of this section, the fixed roof and all openings (e.g., access hatches, sampling ports, and gauge wells) shall be maintained in accordance with the requirements specified in  $\frac{63.148}{5}$  of this subpart.

(ii) Each opening shall be maintained in a closed position (e.g., covered by a lid) at all times that the wastewater tank contains a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream except when it is necessary to use the opening for wastewater sampling, removal, or for equipment inspection, maintenance, or repair.
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(2) The control device shall be designed, operated, and inspected in accordance with the requirements of  $\frac{63.139 \text{ of this}}{\text{subpart}}$ .

(3) Except as provided in <u>paragraph (b)(4)</u> of this section, the closed vent system shall be inspected in accordance with the requirements of  $\frac{63.148}{5}$ .

(4) For any fixed roof tank and closed vent system that is operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements specified in  $\frac{863.148}{2}$ .

(c) If the owner or operator elects to comply with the requirements of <u>paragraph (a)(2)(ii)</u> of this section, the floating roof shall be inspected according to the procedures specified in  $\S 63.120(a)(2)$  and (a)(3) of this subpart.

(d) Except as provided in <u>paragraph (e)</u> of this section, if the owner or operator elects to comply with the requirements of <u>paragraph (a)(2)(iii)</u> of this section, seal gaps shall be measured according to the procedures specified in § <u>63.120(b)(2)(i)</u> through (b)(4) of this subpart and the wastewater tank shall be inspected to determine compliance with § <u>63.120(b)(5)</u> and (b)(6) of this subpart.

(e) If the owner or operator determines that it is unsafe to perform the seal gap measurements specified in § <u>63.120(b)(2)(i)</u> through (b)(4) of this subpart or to inspect the wastewater tank to determine compliance with § <u>63.120(b)(5)</u> and (b)(6) of this subpart because the floating roof appears to be structurally unsound and poses an imminent or potential danger to inspecting personnel, the owner or operator shall comply with the requirements in either paragraph (e)(1) or (e)(2) of this section.

(1) The owner or operator shall measure the seal gaps or inspect the wastewater tank within 30 calendar days of the determination that the floating roof is unsafe, or

(2) The owner or operator shall empty and remove the wastewater tank from service within 45 calendar days of determining that the roof is unsafe. If the wastewater tank cannot be emptied within 45 calendar days, the owner or operator may utilize up to two extensions of up to 30 additional calendar days each. Documentation of a decision to utilize an extension shall include an explanation of why it was unsafe to perform the inspection or seal gap measurement, shall document that alternate storage capacity is unavailable, and shall specify a schedule of actions that will ensure that the wastewater tank will be emptied as soon as practical.

(f) Except as provided in <u>paragraph (e)</u> of this section, each wastewater tank shall be inspected initially, and semi-annually thereafter, for improper work practices in accordance with <u>§ 63.143 of this subpart</u>. For wastewater tanks, improper work practice includes, but is not limited to, leaving open any access door or other opening when such door or opening is not in use.

(g) Except as provided in <u>paragraph (e)</u> of this section, each wastewater tank shall be inspected for control equipment failures as defined in <u>paragraph (g)(1)</u> of this section according to the schedule in <u>paragraphs (g)(2)</u> and <u>(g)(3)</u> of this section.

(1) Control equipment failures for wastewater tanks include, but are not limited to, the conditions specified in <u>paragraphs</u> (g)(1)(i) through (g)(1)(ix) of this section.

(i) The floating roof is not resting on either the surface of the liquid or on the leg supports.

- (ii) There is stored liquid on the floating roof.
- (iii) A rim seal is detached from the floating roof.
- (iv) There are holes, tears, cracks or gaps in the rim seal or seal fabric of the floating roof.
- (v) There are visible gaps between the seal of an internal floating roof and the wall of the wastewater tank.

(vi) There are gaps between the metallic shoe seal or the liquid mounted primary seal of an external floating roof and the wall of the wastewater tank that exceed 212 square centimeters per meter of tank diameter or the width of any portion of any gap between the primary seal and the tank wall exceeds 3.81 centimeters.

(vii) There are gaps between the secondary seal of an external floating roof and the wall of the wastewater tank that exceed 21.2 square centimeters per meter of tank diameter or the width of any portion of any gap between the secondary seal and the tank wall exceeds 1.27 centimeters.

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(viii) Where a metallic shoe seal is used on an external floating roof, one end of the metallic shoe does not extend into the stored liquid or one end of the metallic shoe does not extend a minimum vertical distance of 61 centimeters above the surface of the stored liquid.

(ix) A gasket, joint, lid, cover, or door has a crack or gap, or is broken.

(2) The owner or operator shall inspect for the control equipment failures in <u>paragraphs (g)(1)(i)</u> through (g)(1)(viii) of this section according to the schedule specified in <u>paragraphs (c)</u> and (d) of this section.

(3) The owner or operator shall inspect for the control equipment failures in  $\underline{\text{paragraph } (g)(1)(ix)}$  of this section initially, and semi-annually thereafter.

(h) Except as provided in § 63.140 of this subpart, when an improper work practice or a control equipment failure is identified, first efforts at repair shall be made no later than 5 calendar days after identification and repair shall be completed within 45 calendar days after identification. If a failure that is detected during inspections required by this section cannot be repaired within 45 calendar days and if the vessel cannot be emptied within 45 calendar days, the owner or operator may utilize up to 2 extensions of up to 30 additional calendar days each. Documentation of a decision to utilize an extension shall include a description of the failure, shall document that alternate storage capacity is unavailable, and shall specify a schedule of actions that will ensure that the control equipment will be repaired or the vessel will be emptied as soon as practical.

[62 FR 2753, Jan. 17, 1997, as amended at 64 FR 20191, Apr. 26, 1999; 89 FR 43202, May 16, 2024]

# § 63.134 Process wastewater provisions—surface impoundments.

(a) For each surface impoundment that receives, manages, or treats a Group 1 wastewater stream or a residual removed from a Group 1 wastewater stream, the owner or operator shall comply with the requirements of <u>paragraphs (b)</u>, (c), and (d) of this section.

(b) The owner or operator shall operate and maintain on each surface impoundment either a cover (*e.g.*, air-supported structure or rigid cover) and a closed vent system that routes the organic hazardous air pollutants vapors vented from the surface impoundment to a control device in accordance with <u>paragraph (b)(1)</u> of this section, or a floating flexible membrane cover as specified in <u>paragraph (b)(2)</u> of this section.

(1) The cover and all openings shall meet the following requirements:

(i) Except as provided in <u>paragraph (b)(4)</u> of this section, the cover and all openings (e.g., access hatches, sampling ports, and gauge wells) shall be maintained in accordance with the requirements specified in  $\S$  63.148 of this subpart.

(ii) Each opening shall be maintained in a closed position (e.g., covered by a lid) at all times that a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream is in the surface impoundment except when it is necessary to use the opening for sampling, removal, or for equipment inspection, maintenance, or repair.

(iii) The cover shall be used at all times that a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream is in the surface impoundment except during removal of treatment residuals in accordance with 40 CFR 268.4 or closure of the surface impoundment in accordance with 40 CFR 264.228.

(2) Floating flexible membrane covers shall meet the requirements specified in <u>paragraphs (b)(2)(i)</u> through (b)(2)(vii) of this section.

(i) The floating flexible cover shall be designed to float on the liquid surface during normal operations, and to form a continuous barrier over the entire surface area of the liquid.

(ii) The cover shall be fabricated from a synthetic membrane material that is either:

(A) High density polyethylene (HDPE) with a thickness no less than 2.5 millimeters (100 mils); or

(B) A material or a composite of different materials determined to have both organic permeability properties that are equivalent to those of the material listed in paragraph (b)(2)(ii)(A) of this section, and chemical and physical properties that maintain the material integrity for the intended service life of the material.

(iii) The cover shall be installed in a manner such that there are no visible cracks, holes, gaps, or other open spaces between cover section seams or between the interface of the cover edge and its foundation mountings.

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(iv) Except as provided for in <u>paragraph (b)(2)(v)</u> of this section, each opening in the floating membrane cover shall be equipped with a closure device designed to operate such that when the closure device is secured in the closed position there are no visible cracks, holes, gaps, or other open spaces in the closure device or between the perimeter of the cover opening and the closure device.

(v) The floating membrane cover may be equipped with one or more emergency cover drains for removal of stormwater. Each emergency cover drain shall be equipped with a slotted membrane fabric cover that covers at least 90 percent of the area of the opening or a flexible fabric sleeve seal.

(vi) The closure devices shall be made of suitable materials that will minimize exposure of organic hazardous air pollutants to the atmosphere, to the extent practical, and will maintain the integrity of the equipment throughout its intended service life. Factors to be considered in designing the closure devices shall include: The effects of any contact with the liquid and its vapor managed in the surface impoundment; the effects of outdoor exposure to wind, moisture, and sunlight; and the operating practices used for the surface impoundment on which the floating membrane cover is installed.

(vii) Whenever a Group 1 wastewater stream or residual from a Group 1 wastewater stream is in the surface impoundment, the floating membrane cover shall float on the liquid and each closure device shall be secured in the closed position. Opening of closure devices or removal of the cover is allowed to provide access to the surface impoundment for performing routine inspection, maintenance, or other activities needed for normal operations and/or to remove accumulated sludge or other residues from the bottom of surface impoundment. Openings shall be maintained in accordance with § 63.148 of this subpart.

(3) The control device shall be designed, operated, and inspected in accordance with  $\frac{63.139 \text{ of this subpart.}}{563.139 \text{ of this subpart.}}$ 

(4) Except as provided in <u>paragraph (b)(5)</u> of this section, the closed vent system shall be inspected in accordance with  $\S$  <u>63.148</u>.

(5) For any cover and closed vent system that is operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements specified in  $\frac{663.148}{5}$ .

(c) Each surface impoundment shall be inspected initially, and semi-annually thereafter, for improper work practices and control equipment failures in accordance with  $\S$  63.143 of this subpart.

(1) For surface impoundments, improper work practice includes, but is not limited to, leaving open any access hatch or other opening when such hatch or opening is not in use.

(2) For surface impoundments, control equipment failure includes, but is not limited to, any time a joint, lid, cover, or door has a crack or gap, or is broken.

(d) Except as provided in <u>§ 63.140 of this subpart</u>, when an improper work practice or a control equipment failure is identified, first efforts at repair shall be made no later than 5 calendar days after identification and repair shall be completed within 45 calendar days after identification.

[62 FR 2754, Jan. 17, 1997, as amended at 64 FR 20191, Apr. 26, 1999; 89 FR 43202, May 16, 2024]

# § 63.135 Process wastewater provisions—containers.

(a) For each container that receives, manages, or treats a Group 1 wastewater stream or a residual removed from a Group 1 wastewater stream, the owner or operator shall comply with the requirements of <u>paragraphs (b)</u> through (f) of this section.

(b) The owner or operator shall operate and maintain a cover on each container used to handle, transfer, or store a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream in accordance with the following requirements:

(1) Except as provided in <u>paragraph (d)(4)</u> of this section, if the capacity of the container is greater than 0.42 m<sup>3</sup>, the cover and all openings (e.g., bungs, hatches, sampling ports, and pressure relief devices) shall be maintained in accordance with the requirements specified in  $\S$  63.148 of this subpart.

(2) If the capacity of the container is less than or equal to  $0.42 \text{ m}^3$ , the owner or operator shall comply with either <u>paragraph</u> (b)(2)(i) or (b)(2)(ii) of this section.

(i) The container must meet existing Department of Transportation specifications and testing requirements under <u>49 CFR part</u> <u>178</u>; or

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(ii) Except as provided in <u>paragraph (d)(4)</u> of this section, the cover and all openings shall be maintained without leaks as specified in  $\S$  63.148 of this subpart.

(3) Except as specified in <u>paragraph (b)(4)</u> of this section, the cover and all openings shall be maintained in a closed position (e.g., covered by a lid) at all times that a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream is in the container except when it is necessary to use the opening for filling, removal, inspection, sampling, or pressure relief events related to safety considerations.

(4) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), pressure relief devices are subject to the requirements specified in § 63.165(e) of subpart H of this part.

(c) For containers with a capacity greater than or equal to 0.42 m<sup>3</sup>, a submerged fill pipe shall be used when a container is being filled by pumping with a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream.

(1) The submerged fill pipe outlet shall extend to no more than 6 inches or within two fill pipe diameters of the bottom of the container while the container is being filled.

(2) The cover shall remain in place and all openings shall be maintained in a closed position except for those openings required for the submerged fill pipe and for venting of the container to prevent physical damage or permanent deformation of the container or cover.

(d) During treatment of a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream, including aeration, thermal or other treatment, in a container, whenever it is necessary for the container to be open, the container shall be located within an enclosure with a closed vent system that routes the organic hazardous air pollutants vapors vented from the container to a control device.

(1) Except as provided in <u>paragraph (d)(4)</u> of this section, the enclosure and all openings (e.g., doors, hatches) shall be maintained in accordance with the requirements specified in  $\frac{63.148}{5}$  of this subpart.

(2) The control device shall be designed, operated, and inspected in accordance with § 63.139 of this subpart.

(3) Except as provided in <u>paragraph (d)(4)</u> of this section, the closed vent system shall be inspected in accordance with  $\S$  <u>63.148 of this subpart</u>.

(4) For any enclosure and closed vent system that is operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements specified in  $\S$  63.148 of this subpart.

(e) Each container shall be inspected initially, and semi-annually thereafter, for improper work practices and control equipment failures in accordance with <u>§ 63.143 of this subpart</u>.

(1) For containers, improper work practice includes, but is not limited to, leaving open any access hatch or other opening when such hatch or opening is not in use.

(2) For containers, control equipment failure includes, but is not limited to, any time a cover or door has a gap or crack, or is broken.

(f) Except as provided in <u>§ 63.140 of this subpart</u>, when an improper work practice or a control equipment failure is identified, first efforts at repair shall be made no later than 5 calendar days after identification and repair shall be completed within 15 calendar days after identification.

[62 FR 2755, Jan. 17, 1997, as amended at 89 FR 43202, May 16, 2024]

#### § 63.136 Process wastewater provisions—individual drain systems.

(a) For each individual drain system that receives or manages a Group 1 wastewater stream or a residual removed from a Group 1 wastewater stream, the owner or operator shall comply with the requirements of paragraphs (b), (c), and (d) or with <u>paragraphs (e)</u>, (f), and (g) of this section.

(b) If the owner or operator elects to comply with this paragraph, the owner or operator shall operate and maintain on each opening in the individual drain system a cover and if vented, route the vapors to a process or through a closed vent system to a control device. The owner or operator shall comply with the requirements of <u>paragraphs (b)(1)</u> through (b)(5) of this section.

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(1) The cover and all openings shall meet the following requirements:

(i) Except as provided in <u>paragraph (b)(4)</u> of this section, the cover and all openings (e.g., access hatches, sampling ports) shall be maintained in accordance with the requirements specified in  $\S$  63.148 of this subpart.

(ii) The cover and all openings shall be maintained in a closed position at all times that a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream is in the drain system except when it is necessary to use the opening for sampling or removal, or for equipment inspection, maintenance, or repair.

(2) The control device shall be designed, operated, and inspected in accordance with § 63.139 of this subpart.

(3) Except as provided in <u>paragraph (b)(4)</u> of this section, the closed vent system shall be inspected in accordance with  $\underline{\$}$  <u>63.148</u>.

(4) For any cover and closed vent system that is operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements specified in  $\frac{\& 63.148}{\& 63.148}$ .

(5) The individual drain system shall be designed and operated to segregate the vapors within the system from other drain systems and the atmosphere.

(c) Each individual drain system shall be inspected initially, and semi- annually thereafter, for improper work practices and control equipment failures, in accordance with the inspection requirements specified in table 11 of this subpart.

(1) For individual drain systems, improper work practice includes, but is not limited to, leaving open any access hatch or other opening when such hatch or opening is not in use for sampling or removal, or for equipment inspection, maintenance, or repair.

(2) For individual drain systems, control equipment failure includes, but is not limited to, any time a joint, lid, cover, or door has a gap or crack, or is broken.

(d) Except as provided in <u>§ 63.140 of this subpart</u>, when an improper work practice or a control equipment failure is identified, first efforts at repair shall be made no later than 5 calendar days after identification and repair shall be completed within 15 calendar days after identification.

(e) If the owner or operator elects to comply with this paragraph, the owner or operator shall comply with the requirements in paragraphs (e)(1) through (e)(3) of this section:

(1) Each drain shall be equipped with water seal controls or a tightly fitting cap or plug. The owner or operator shall comply with <u>paragraphs (e)(1)(i)</u> and <u>(e)(1)(ii)</u> of this section.

(i) For each drain equipped with a water seal, the owner or operator shall ensure that the water seal is maintained. For example, a flow-monitoring device indicating positive flow from a main to a branch water line supplying a trap or water being continuously dripped into the trap by a hose could be used to verify flow of water to the trap. Visual observation is also an acceptable alternative.

(ii) If a water seal is used on a drain receiving a Group 1 wastewater, the owner or operator shall either extend the pipe discharging the wastewater below the liquid surface in the water seal of the receiving drain, or install a flexible shield (or other enclosure which restricts wind motion across the open area between the pipe and the drain) that encloses the space between the pipe discharging the wastewater to the drain receiving the wastewater. (Water seals which are used on hubs receiving Group 2 wastewater for the purpose of eliminating cross ventilation to drains carrying Group 1 wastewater are not required to have a flexible cap or extended subsurface discharging pipe.)

(2) Each junction box shall be equipped with a tightly fitting solid cover (i.e., no visible gaps, cracks, or holes) which shall be kept in place at all times except during inspection and maintenance. If the junction box is vented, the owner or operator shall comply with the requirements in paragraph (e)(2)(i) or (e)(2)(ii) of this section.

(i) The junction box shall be vented to a process or through a closed vent system to a control device. The closed vent system shall be inspected in accordance with the requirements of  $\frac{63.148}{63.139}$  and the control device shall be designed, operated, and inspected in accordance with the requirements of  $\frac{63.139}{63.139}$ .

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(ii) If the junction box is filled and emptied by gravity flow (i.e., there is no pump) or is operated with no more than slight fluctuations in the liquid level, the owner or operator may vent the junction box to the atmosphere provided that the junction box complies with the requirements in paragraphs (e)(2)(ii)(A) and (e)(2)(ii)(B) of this section.

(A) The vent pipe shall be at least 90 centimeters in length and no greater than 10.2 centimeters in nominal inside diameter.

(B) Water seals shall be installed and maintained at the wastewater entrance(s) to or exit from the junction box restricting ventilation in the individual drain system and between components in the individual drain system. The owner or operator shall demonstrate (e.g., by visual inspection or smoke test) upon request by the Administrator that the junction box water seal is properly designed and restricts ventilation.

(3) Each sewer line shall not be open to the atmosphere and shall be covered or enclosed in a manner so as to have no visible gaps or cracks in joints, seals, or other emission interfaces.

(f) Equipment used to comply with <u>paragraphs (e)(1), (e)(2)</u>, or (e)(3) of this section shall be inspected as follows:

(1) Each drain using a tightly fitting cap or plug shall be visually inspected initially, and semi-annually thereafter, to ensure caps or plugs are in place and that there are no gaps, cracks, or other holes in the cap or plug.

(2) Each junction box shall be visually inspected initially, and semi-annually thereafter, to ensure that there are no gaps, cracks, or other holes in the cover.

(3) The unburied portion of each sewer line shall be visually inspected initially, and semi-annually thereafter, for indication of cracks or gaps that could result in air emissions.

(g) Except as provided in <u>§ 63.140 of this subpart</u>, when a gap, hole, or crack is identified in a joint or cover, first efforts at repair shall be made no later than 5 calendar days after identification, and repair shall be completed within 15 calendar days after identification.

[62 FR 2755, Jan. 17, 1997, as amended at 89 FR 43202, May 16, 2024]

# § 63.137 Process wastewater provisions—oil-water separators.

(a) For each oil-water separator that receives, manages, or treats a Group 1 wastewater stream or a residual removed from a Group 1 wastewater stream, the owner or operator shall comply with the requirements of <u>paragraphs (c)</u> and <u>(d)</u> of this section and shall operate and maintain one of the following:

(1) A fixed roof and a closed vent system that routes the organic hazardous air pollutants vapors vented from the oil-water separator to a control device. The fixed roof, closed vent system, and control device shall meet the requirements specified in paragraph (b) of this section;

(2) A floating roof meeting the requirements in <u>40 CFR part 60</u>, subpart QQQ § 60.693-2 (a)(1)(i), (a)(1)(ii), (a)(2), (a)(3), and (a)(4). For portions of the oil-water separator where it is infeasible to construct and operate a floating roof, such as over the weir mechanism, the owner or operator shall operate and maintain a fixed roof, closed vent system, and control device that meet the requirements specified in paragraph (b) of this section.

(3) An equivalent means of emission limitation. Determination of equivalence to the reduction in emissions achieved by the requirements of paragraphs (a)(1) and (a)(2) of this section will be evaluated according to  $\frac{6}{5}$  63.102(b) of subpart F of this part. The determination will be based on the application to the Administrator which shall include the information specified in either paragraph (a)(3)(i) or (a)(3)(ii) of this section.

(i) Actual emissions tests that use full-size or scale-model oil-water separators that accurately collect and measure all organic hazardous air pollutants emissions from a given control technique, and that accurately simulate wind and account for other emission variables such as temperature and barometric pressure, or

(ii) An engineering evaluation that the Administrator determines is an accurate method of determining equivalence.

(b) If the owner or operator elects to comply with the requirements of <u>paragraphs (a)(1)</u> or (a)(2) of this section, the fixed roof shall meet the requirements of <u>paragraph (b)(1)</u> of this section, the control device shall meet the requirements of <u>paragraph (b)(2)</u> of this section, and the closed vent system shall meet the requirements of <u>paragraph (b)(3)</u> of this section.

(1) The fixed-roof shall meet the following requirements:

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(i) Except as provided in <u>paragraph (b)(4)</u> of this section, the fixed roof and all openings (e.g., access hatches, sampling ports, and gauge wells) shall be maintained in accordance with the requirements specified in  $\frac{63.148}{5}$  of this subpart.

(ii) Each opening shall be maintained in a closed, sealed position (e.g., covered by a lid that is gasketed and latched) at all times that the oil-water separator contains a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream except when it is necessary to use the opening for sampling or removal, or for equipment inspection, maintenance, or repair.

(2) The control device shall be designed, operated, and inspected in accordance with the requirements of  $\S$  63.139 of this subpart.

(3) Except as provided in <u>paragraph (b)(4)</u> of this section, the closed vent system shall be inspected in accordance with the requirements of  $\frac{63.148}{5}$ .

(4) For any fixed roof and closed vent system that is operated and maintained under negative pressure, the owner or operator is not required to comply with the requirements of  $\frac{63.148}{5}$ .

(c) If the owner or operator elects to comply with the requirements of <u>paragraph (a)(2)</u> of this section, seal gaps shall be measured according to the procedures specified in <u>40 CFR part 60</u>, <u>subpart QQQ § 60.696(d)(1)</u> and the schedule specified in <u>paragraphs (c)(1)</u> and (c)(2) of this section.

(1) Measurement of primary seal gaps shall be performed within 60 calendar days after installation of the floating roof and introduction of a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream and once every 5 years thereafter.

(2) Measurement of secondary seal gaps shall be performed within 60 calendar days after installation of the floating roof and introduction of a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream and once every year thereafter.

(d) Each oil-water separator shall be inspected initially, and semi-annually thereafter, for improper work practices in accordance with  $\S$  63.143 of this subpart. For oil-water separators, improper work practice includes, but is not limited to, leaving open or ungasketed any access door or other opening when such door or opening is not in use.

(e) Each oil-water separator shall be inspected for control equipment failures as defined in <u>paragraph (e)(1)</u> of this section according to the schedule specified in <u>paragraphs (e)(2)</u> and (e)(3) of this section.

(1) For oil-water separators, control equipment failure includes, but is not limited to, the conditions specified in <u>paragraphs</u> (e)(1)(i) through (e)(1)(vii) of this section.

(i) The floating roof is not resting on either the surface of the liquid or on the leg supports.

(ii) There is stored liquid on the floating roof.

(iii) A rim seal is detached from the floating roof.

(iv) There are holes, tears, or other open spaces in the rim seal or seal fabric of the floating roof.

(v) There are gaps between the primary seal and the separator wall that exceed 67 square centimeters per meter of separator wall perimeter or the width of any portion of any gap between the primary seal and the separator wall exceeds 3.8 centimeters.

(vi) There are gaps between the secondary seal and the separator wall that exceed 6.7 square centimeters per meter of separator wall perimeter or the width of any portion of any gap between the secondary seal and the separator wall exceeds 1.3 centimeters.

(vii) A gasket, joint, lid, cover, or door has a gap or crack, or is broken.

(2) The owner or operator shall inspect for the control equipment failures in <u>paragraphs (e)(1)(i)</u> through  $(\underline{e})(1)(\underline{v})$  of this section according to the schedule specified in <u>paragraph (c)</u> of this section.

(3) The owner or operator shall inspect for control equipment failures in <u>paragraph (e)(1)(vii)</u> of this section initially, and semi-annually thereafter.

(f) Except as provided in <u>§ 63.140 of this subpart</u>, when an improper work practice or a control equipment failure is identified, first efforts at repair shall be made no later than 5 calendar days after identification and repair shall be completed within 45 calendar days after identification.

[62 FR 2756, Jan. 17, 1997, as amended at 89 FR 43202, May 16, 2024]

# § 63.138 Process wastewater provisions—performance standards for treatment processes managing Group 1 wastewater streams and/or residuals removed from Group 1 wastewater streams.

(a) General requirements. This section specifies the performance standards for treating Group 1 wastewater streams. The owner or operator shall comply with the requirements as specified in <u>paragraphs (a)(1)</u> through (a)(6) of this section. Where multiple compliance options are provided, the options may be used in combination for different wastewater streams and/or for different compounds (e.g., Table 8 versus Table 9 compounds) in the same wastewater streams, except where otherwise provided in this section. Once a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream has been treated in accordance with this subpart, it is no longer subject to the requirements of this subpart.

(1) *Existing source*. If the wastewater stream, at an existing source, is Group 1 for Table 9 compounds, comply with  $\S$  <u>63.138(b)</u>.

(2) *New source*. If the wastewater stream, at a new source, is Group 1 for Table 8 compounds, comply with  $\S$  <u>63.138(c)</u>. If the wastewater stream, at a new source, is Group 1 for Table 9 compounds, comply with  $\S$  <u>63.138(b)</u>. If the wastewater stream, at a new source, is Group 1 for Table 9 compounds, comply with <u>§ 63.138(b)</u>. If the wastewater stream, at a new source, is Group 1 for Table 9 compounds, comply with <u>§ 63.138(b)</u>. If the wastewater stream, at a new source, is Group 1 for Table 9 compounds, comply with <u>§ 63.138(b)</u>.

Note to paragraph (a)(2):

The requirements for Table 8 and/or Table 9 compounds are similar and often identical.

(3) *Biological treatment processes*. Biological treatment processes in compliance with this section may be either open or closed biological treatment processes as defined in § 63.111. An open biological treatment process in compliance with this section need not be covered and vented to a control device as required in § 63.133 through § 63.137 of this subpart. An open or a closed biological treatment process in compliance with this section and using § 63.145(f) or § 63.145(g) of this subpart to demonstrate compliance is not subject to the requirements of § 63.133 through § 63.137 of this subpart. A closed biological treatment process in compliance with this section and using § 63.145(e) of this subpart. A closed biological treatment process in compliance with this section and using § 63.145(e) of this subpart to demonstrate compliance with this section and using § 63.145(e) of this subpart to demonstrate compliance shall comply with the requirements of § 63.133 through § 63.137 of this subpart. A closed biological treatment process shall meet the requirements of § 63.133 through § 63.137 of this subpart, as applicable.

(4) *Performance tests and design evaluations.* If design steam stripper option ( $\S$  63.138(d)) or Resource Conservation and Recovery Act (RCRA) option ( $\S$  63.138(h)) is selected to comply with this section, neither a design evaluation nor a performance test is required. For any other non-biological treatment process, and for closed biological treatment processes as defined in  $\S$  63.111 of this subpart, the owner or operator shall conduct either a design evaluation as specified in  $\S$  63.138(j), or a performance test as specified in  $\S$  63.145, of this subpart. For each open biological treatment process as defined in  $\S$  63.111 of this subpart, the owner or operator shall conduct a performance test as specified in  $\S$  63.145 of this subpart.

Note to paragraph (a)(4):

Some open biological treatment processes may not require a performance test. Refer to  $\frac{63.145(h)}{100}$  and table 36 of this subpart to determine whether the biological treatment process meets the criteria that exempt the owner or operator from conducting a performance test.

(5) Control device requirements. When gases are vented from the treatment process, the owner or operator shall comply with the applicable control device requirements specified in  $\S$  63.139 and  $\S$  63.145 (i) and (j), and the applicable leak inspection provisions specified in  $\S$  63.148, of this subpart. This requirement does not apply to any open biological treatment process that meets the mass removal requirements. Vents from anaerobic biological treatment processes may be routed through hard-piping to a fuel gas system.

(6) *Residuals: general.* When residuals result from treating Group 1 wastewater streams, the owner or operator shall comply with the requirements for residuals specified in  $\frac{63.138(k)}{5.138(k)}$  of this subpart.

(7) *Treatment using a series of treatment processes.* In all cases where the wastewater provisions in this subpart allow or require the use of a treatment process or control device to comply with emissions limitations, the owner or operator may use

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multiple treatment processes or control devices, respectively. For combinations of treatment processes where the wastewater stream is conveyed by hard-piping, the owner or operator shall comply with either the requirements of <u>paragraph</u> (a)(7)(i) or (a)(7)(ii) of this section. For combinations of treatment processes where the wastewater stream is not conveyed by hard-piping, the owner or operator shall comply with the requirements of <u>paragraph (a)(7)(ii)</u> of this section. For combinations of control devices, the owner or operator shall comply with the requirements of <u>paragraph (a)(7)(ii)</u> of this section. For combinations of control devices, the owner or operator shall comply with the requirements of <u>paragraph (a)(7)(i)</u> of this section.

(i)

(A) For combinations of treatment processes, the wastewater stream shall be conveyed by hard-piping between the treatment processes. For combinations of control devices, the vented gas stream shall be conveyed by hard-piping between the control devices.

(B) For combinations of treatment processes, each treatment process shall meet the applicable requirements of § 63.133 through § 63.137 of this subpart except as provided in paragraph (a)(3) of this section.

(C) The owner or operator shall identify, and keep a record of, the combination of treatment processes or of control devices, including identification of the first and last treatment process or control device. The owner or operator shall include this information as part of the treatment process description reported in the Notification of Compliance Status.

(D) The performance test or design evaluation shall determine compliance across the combination of treatment processes or control devices. If a performance test is conducted, the "inlet" shall be the point at which the wastewater stream or residual enters the first treatment process, or the vented gas stream enters the first control device. The "outlet" shall be the point at which the treated wastewater stream exits the last treatment process, or the vented gas stream exits the last control device.

(ii)

(A) For combinations of treatment processes, each treatment process shall meet the applicable requirements of § 63.133 through § 63.137 of this subpart except as provided in paragraph (a)(3) of this section.

(B) The owner or operator shall identify, and keep a record of, the combination of treatment processes, including identification of the first and last treatment process. The owner or operator shall include this information as part of the treatment process description reported in the Notification of Compliance Status.

(C) The owner or operator shall determine the mass removed or destroyed by each treatment process. The performance test or design evaluation shall determine compliance for the combination of treatment processes by adding together the mass removed or destroyed by each treatment process.

(b) Control options: Group 1 wastewater streams for Table 9 compounds. The owner or operator shall comply with either paragraph (b)(1) or (b)(2) of this section, and paragraph (b)(3) of this section, if applicable, for the control of Table 9 compounds at new or existing sources.

(1) 50 ppmw concentration option. The owner or operator shall comply with paragraphs (b)(1)(i) and (b)(1)(ii) of this section.

(i) Reduce, by removal or destruction, the total concentration of Table 9 compounds to a level less than 50 parts per million by weight as determined by the procedures specified in  $\S$  63.145(b) of this subpart.

(ii) This option shall not be used when the treatment process is a biological treatment process. This option shall not be used when the wastewater stream is designated as a Group 1 wastewater stream as specified in  $\S$  63.132(e). Dilution shall not be used to achieve compliance with this option.

(2) Other compliance options. Comply with the requirements specified in any one of paragraphs (d), (e), (f), (g), (h), or (i) of this section.

(3) *I ppmw ethylene oxide concentration*. Reduce, by removal or destruction, the concentration of ethylene oxide to a level less than 1 parts per million by weight as determined in the procedures specified in  $\frac{63.145(b)}{5.000}$  of this subpart.

(c) Control options: Group 1 wastewater streams for Table 8 compounds. The owner or operator shall comply with either paragraph (c)(1) or (c)(2) of this section, and paragraph (c)(3) of this section, if applicable, for the control of Table 8 compounds at new sources.

(1) 10 ppmw concentration option. The owner or operator shall comply with <u>paragraphs (c)(1)(i)</u> and <u>(c)(1)(ii)</u> of this section.

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(i) Reduce, by removal or destruction, the concentration of the individual Table 8 compounds to a level less than 10 parts per million by weight as determined in the procedures specified in  $\frac{63.145(b)}{5.000}$  of this subpart.

(ii) This option shall not be used when the treatment process is a biological treatment process. This option shall not be used when the wastewater stream is designated as a Group 1 wastewater stream as specified in  $\S$  63.132(e). Dilution shall not be used to achieve compliance with this option.

(2) Other compliance options. Comply with the requirements specified in any one of paragraphs (d), (e), (f), (g), (h), or (i) of this section.

(3) *I ppmw ethylene oxide concentration*. Reduce, by removal or destruction, the concentration of ethylene oxide to a level less than 1 parts per million by weight as determined in the procedures specified in  $\frac{\$ 63.145(b)}{100}$ .

(d) Design steam stripper option. The owner or operator shall operate and maintain a steam stripper that meets the requirements of paragraphs (d)(1) through (d)(6) of this section.

(1) Minimum active column height of 5 meters,

(2) Countercurrent flow configuration with a minimum of 10 actual trays,

(3) Minimum steam flow rate of 0.04 kilograms of steam per liter of wastewater feed within the column,

(4) Minimum wastewater feed temperature to the steam stripper of 95 °C, or minimum column operating temperature of 95 °C,

(5) Maximum liquid loading of 67,100 liters per hour per square meter, and

(6) Operate at nominal atmospheric pressure.

(e) Percent mass removal/destruction option. The owner or operator of a new or existing source shall comply with <u>paragraph</u> (e)(1) or (e)(2) of this section for control of Table 8 and/or Table 9 compounds for Group 1 wastewater streams. This option shall not be used for biological treatment processes.

(1) Reduce mass flow rate of Table 8 and/or Table 9 compounds by 99 percent. For wastewater streams that are Group 1, the owner or operator shall reduce, by removal or destruction, the mass flow rate of Table 8 and/or Table 9 compounds by 99 percent or more. The removal/destruction efficiency shall be determined by the procedures specified in § 63.145(c), for noncombustion processes, or § 63.145(d), for combustion processes.

(2) Reduce mass flow rate of Table 8 and/or Table 9 compounds by Fr value. For wastewater streams that are Group 1 for Table 8 and/or Table 9 compounds, the owner or operator shall reduce, by removal or destruction, the mass flow rate by at least the fraction removal (Fr) values specified in Table 9 of this subpart. (The Fr values for Table 8 compounds are all 0.99.) The removal/destruction efficiency shall be determined by the procedures specified in  $\S$  63.145(c), for noncombustion treatment processes, or  $\S$  63.145(d), for combustion treatment processes.

(f) Required mass removal (RMR) option. The owner or operator shall achieve the required mass removal (RMR) of Table 8 compounds at a new source for a wastewater stream that is Group 1 for Table 8 compounds and/or of Table 9 compounds at a new or existing source for a wastewater stream that is Group 1 for Table 9 compounds. For nonbiological treatment processes compliance shall be determined using the procedures specified in  $\S$  63.145(e) of this subpart. For aerobic biological treatment processes compliance shall be determined using the procedures specified in  $\S$  63.145(e) or (f) of this subpart. For closed anaerobic biological treatment processes compliance shall be determined using the procedures specified in  $\S$  63.145(e) or (f) of this subpart. For closed anaerobic biological treatment processes compliance shall be determined using the procedures specified in  $\S$  63.145(f) of this subpart. For open biological treatment processes compliance shall be determined using the procedures specified in  $\S$  63.145(f) of this subpart.

(g) 95-percent RMR option, for biological treatment processes. The owner or operator of a new or existing source using biological treatment for at least one wastewater stream that is Group 1 for Table 9 compounds shall achieve a RMR of at least 95 percent for all Table 9 compounds. The owner or operator of a new source using biological treatment for at least one wastewater stream that is Group 1 for Table 8 compounds shall achieve a RMR of at least 95 percent for all Table 8 compounds. All Group 1 and Group 2 wastewater streams entering a biological treatment unit that are from chemical manufacturing process units subject to subpart F shall be included in the demonstration of the 95-percent mass removal. The owner or operator shall comply with paragraphs (g)(1) through (g)(4) of this section.

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(1) Except as provided in <u>paragraph (g)(4)</u> of this section, the owner or operator shall ensure that all Group 1 and Group 2 wastewater streams from chemical manufacturing process units subject to this rule entering a biological treatment unit are treated to destroy at least 95-percent total mass of all Table 8 and/or Table 9 compounds.

(2) For open biological treatment processes compliance shall be determined using the procedures specified in  $\S$  <u>63.145(g) of</u> <u>this subpart</u>. For closed aerobic biological treatment processes compliance shall be determined using the procedures specified in  $\S$  <u>63.145(e)</u> or <u>(g) of this subpart</u>. For closed anaerobic biological treatment processes compliance shall be determined using the procedures specified in  $\S$  <u>63.145(e)</u> or <u>(g) of this subpart</u>. For closed anaerobic biological treatment processes compliance shall be determined using the procedures specified in  $\S$  <u>63.145(e) of this subpart</u>.

(3) For each treatment process or waste management unit that receives, manages, or treats wastewater streams subject to this paragraph, from the point of determination of each Group 1 or Group 2 wastewater stream to the biological treatment unit, the owner or operator shall comply with  $\frac{\&\& 63.133}{\&\& 63.133}$  through  $\frac{\& 63.137}{\&\& 63.137}$  of this subpart for control of air emissions. When complying with this paragraph, the term Group 1, whether used alone or in combination with other terms, in  $\frac{\& 63.137}{\&\& 63.137}$  through  $\frac{\& 63.137}{\&\& 63.137}$ 

(4) If a wastewater stream is in compliance with the requirements in <u>paragraph (b)(1)</u>, (c)(1), (d), (e), (f), or (h) of this section before entering the biological treatment unit, the hazardous air pollutants mass of that wastewater is not required to be included in the total mass flow rate entering the biological treatment unit for the purpose of demonstrating compliance.

(h) *Treatment in a RCRA unit option*. The owner or operator shall treat the wastewater stream or residual in a unit identified in, and complying with, <u>paragraph (h)(1)</u>, (h)(2), or (h)(3) of this section. These units are exempt from the design evaluation or performance tests requirements specified in § 63.138(a)(3) and § 63.138(j) of this subpart, and from the monitoring requirements specified in § 63.132(a)(2)(iii) and § 63.132(b)(3)(iii) of this subpart, as well as recordkeeping and reporting requirements associated with monitoring and performance tests.

(1) The wastewater stream or residual is discharged to a hazardous waste incinerator for which the owner or operator:

(i) Has been issued a final permit under <u>40 CFR part 270</u> and complies with the requirements of <u>40 CFR part 264, subpart O</u>;

(ii) Has certified compliance with the interim status requirements of <u>40 CFR part 265</u>, subpart O;

(iii) Has submitted a Notification of Compliance under  $\S$  63.1207(j) and complies with the requirements subpart EEE of this part; or

(iv) Complies with the requirements subpart EEE of this part and will submit a Notification of Compliance under  $\underline{\$}$  <u>63.1207(j)</u> by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(2) The wastewater stream or residual is discharged to a process heater or boiler burning hazardous waste for which the owner or operator:

(i) Has been issued a final permit under <u>40 CFR part 270</u> and complies with the requirements of <u>40 CFR part 266, subpart H;</u>

(ii) Has certified compliance with the interim status requirements of <u>40 CFR part 266, subpart H</u>;

(iii) Has submitted a Notification of Compliance under  $\S$  63.1207(j) and complies with the requirements of subpart EEE of this part; or

(iv) Complies with <u>subpart EEE of this part</u> and will submit a Notification of Compliance under <u>§ 63.1207(j)</u> by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(3) The wastewater stream or residual is discharged to an underground injection well for which the owner or operator has been issued a final permit under <u>40 CFR part 270</u> or <u>40 CFR part 144</u> and complies with the requirements of <u>40 CFR part 122</u>. The owner or operator shall comply with all applicable requirements of this subpart prior to the point where the wastewater enters the underground portion of the injection well.

(i) One megagram total source mass flow rate option. A wastewater stream is exempt from the requirements of <u>paragraphs</u> (b) and (c) of this section if the owner or operator elects to comply with either <u>paragraph (i)(1)</u> or (2) of this section, and complies with <u>paragraph (i)(3)</u> of this section.

(1) All Group 1 wastewater streams at the source. The owner or operator shall demonstrate that the total source mass flow rate for Table 8 and/or Table 9 compounds is less than 1 megagram per year using the procedures in paragraphs

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(i)(1)(i) and (i)(1)(ii) of this section. The owner or operator shall include all Group 1 wastewater streams at the source in the total source mass flow rate. The total source mass flow rate shall be based on the mass as calculated before the wastewater stream is treated. The owner or operator who meets the requirements of this paragraph (i)(1) is exempt from the requirements of  $\frac{\xi\xi}{63.133}$  through  $\frac{63.137}{5.133}$ .

(i) Calculate the annual average mass flow rate for each Group 1 wastewater stream by multiplying the annual average flow rate of the wastewater stream, as determined by procedures specified in § 63.144(c), times the total annual average concentration of Table 8 and/or Table 9 compounds, as determined by procedures specified in § 63.144(b) of this subpart. (The mass flow rate of compounds in a wastewater stream that is Group 1 for both Table 8 and Table 9 compounds should be included in the annual average mass flow rate only once.)

(ii) Calculate the total source mass flow rate from all Group 1 wastewater streams by adding together the annual average mass flow rate calculated for each Group 1 wastewater stream.

(2) Untreated and partially treated Group 1 wastewater streams. The owner or operator shall demonstrate that the total source mass flow rate for untreated Group 1 wastewater streams and Group 1 wastewater streams treated to levels less stringent than required in paragraph (b) or (c) of this section is less than 1 megagram per year using the procedures in paragraphs (i)(2)(i) and (i)(2)(ii) of this section. The owner or operator shall manage these wastewater streams in accordance with paragraph (i)(2)(iii) of this section, and shall comply with paragraph (i)(3) of this section.

(i) Calculate the annual average mass flow rate in each wastewater stream by multiplying the annual average flow rate of the wastewater stream, as determined by procedures specified in § 63.144(c), times the total annual average concentration of Table 8 and/or Table 9 compounds, as determined by procedures specified in § 63.144(b). (The mass flow rate of compounds in a wastewater stream that are Group 1 for both Table 8 and Table 9 compounds should be included in the annual average mass flow rate only once.) When determining the total source mass flow rate for the purposes of paragraph (i)(2)(i)(B) of this section, the concentration and flow rate shall be determined at the location specified in paragraph (i)(2)(i)(B) of this section and not at the location specified in § 63.144(b) and (c).

(A) For each untreated Group 1 wastewater stream, the annual average flow rate and the total annual average concentration shall be determined for that stream's point of determination.

(B) For each Group 1 wastewater stream that is treated to levels less stringent than those required by <u>paragraph (b)</u> or (c) of this section, the annual average flow rate and total annual average concentration shall be determined at the discharge from the treatment process or series of treatment processes.

(C) The annual average mass flow rate for Group 1 wastewater streams treated to the levels required by <u>paragraph</u> (b) or (c) of this section is not included in the calculation of the total source mass flow rate.

(ii) The total source mass flow rate shall be calculated by summing the annual average mass flow rates from all Group 1 wastewater streams, except those excluded by <u>paragraph (i)(2)(i)(C)</u> of this section.

(iii) The owner or operator of each waste management unit that receives, manages, or treats a partially treated wastewater stream prior to or during treatment shall comply with the requirements of  $\frac{\$\$}{63.133}$  through  $\frac{63.137}{63.137}$ , as applicable. For a partially treated wastewater stream that is stored, conveyed, treated, or managed in a waste management unit meeting the requirements of  $\frac{\$\$}{63.133}$  through  $\frac{63.137}{(2)(i)(B)}$  of this section to calculate mass flow rate. A wastewater stream, either untreated or partially treated, where the mass flow rate has been calculated following the procedures in paragraph (i)(2)(i)(A) of this section, is exempt from the requirements of  $\frac{\$\$}{63.137}$  through  $\frac{63.137}{63.133}$  through  $\frac{63.137}{63.137}$ .

(3) Wastewater streams included in this option shall be identified in the Notification of Compliance Status required by  $\S$  <u>63.152(b)</u>.

(j) Design evaluations or performance tests for treatment processes. Except as provided in paragraph (j)(3) or (h) of this section, the owner or operator shall demonstrate by the procedures in either paragraph (j)(1) or (j)(2) of this section that each nonbiological treatment process used to comply with paragraphs (b)(1), (c)(1), (e), and/or (f) of this section achieves the conditions specified for compliance. The owner or operator shall demonstrate by the procedures in either paragraph (j)(1) or (j)(2) of this section achieves the conditions specified for compliance. The owner or operator shall demonstrate by the procedures in either paragraph (j)(1) or (j)(2) of this section that each closed biological treatment process used to comply with paragraphs (f) or (g) of this section achieves the conditions specified for compliance. If an open biological treatment unit is used to comply with paragraph (f) or (g) of this section, the owner or operator shall comply with § 63.145(f) or § 63.145(g), respectively, of this subpart. Some biological treatment processes may not require a performance test. Refer to § 63.145(h) and table 36 of

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this subpart to determine whether the open biological treatment process meets the criteria that exempt the owner or operator from conducting a performance test.

(1) A design evaluation and supporting documentation that addresses the operating characteristics of the treatment process and that is based on operation at a representative wastewater stream flow rate and a concentration under which it would be most difficult to demonstrate compliance. For closed biological treatment processes, the actual mass removal shall be determined by a mass balance over the unit. The mass flow rate of Table 8 or Table 9 compounds exiting the treatment process shall be the sum of the mass flow rate of Table 8 or Table 9 compounds in the wastewater stream exiting the biological treatment process and the mass flow rate of the vented gas stream exiting the control device. The mass flow rate entering the treatment process minus the mass flow rate exiting the process determines the actual mass removal.

(2) Performance tests conducted using test methods and procedures that meet the applicable requirements specified in § 63.145 of this subpart.

(3) The provisions of <u>paragraphs (j)(1)</u> and (j)(2) of this section do not apply to design stream strippers which meet the requirements of <u>paragraph (d)</u> of this section.

(k) *Residuals*. For each residual removed from a Group 1 wastewater stream, the owner or operator shall control for air emissions by complying with  $\frac{\& 63.133-137 \text{ of this subpart}}{(k)(1)}$  and by complying with one of the provisions in <u>paragraphs</u> (k)(1) through (k)(4) of this section.

(1) Recycle the residual to a production process or sell the residual for the purpose of recycling. Once a residual is returned to a production process, the residual is no longer subject to this section.

(2) Return the residual to the treatment process.

(3) Treat the residual to destroy the total combined mass flow rate of Table 8 and/or Table 9 compounds by 99 percent or more, as determined by the procedures specified in  $\frac{63.145(c)}{c}$  or (d) of this subpart.

(4) Comply with the requirements for RCRA treatment options specified in  $\S$  63.138(h) of this subpart.

[62 FR 2757, Jan. 17, 1997, as amended at 66 FR 6933, Jan. 22, 2001; 89 FR 43202, May 16, 2024]

#### § 63.139 Process wastewater provisions—control devices.

(a) For each control device or combination of control devices used to comply with the provisions in  $\S$ <u>63.133</u> through <u>63.138 of this subpart</u>, the owner or operator shall operate and maintain the control device or combination of control devices in accordance with the requirements of <u>paragraphs</u> (b) through (f) of this section.

(b) Whenever organic hazardous air pollutants emissions are vented to a control device which is used to comply with the provisions of this subpart, such control device shall be operating.

(c) The control device shall be designed and operated in accordance with paragraph(c)(1), (2), (3), (4), or (5) of this section.

(1) An enclosed combustion device (including but not limited to a vapor incinerator, boiler, or process heater) shall meet the conditions in paragraph (c)(1)(i), (ii), or (iii) of this section, alone or in combination with other control devices. If a boiler or process heater is used as the control device, then the vent stream shall be introduced into the flame zone of the boiler or process heater.

(i) Reduce the total organic compound emissions, less methane and ethane, or total organic hazardous air pollutants emissions vented to the control device by 95 percent by weight or greater;

(ii) Achieve an outlet total organic compound concentration, less methane and ethane, or total organic hazardous air pollutants concentration of 20 parts per million by volume on a dry basis corrected to 3 percent oxygen. The owner or operator shall use either Method 18 of appendix A-6 to <u>part 60 of this chapter</u>, any other method or data that has been validated according to the applicable procedures in Method 301 of <u>appendix A of this part</u>, or ASTM D6420-18 (incorporated by reference, see § <u>63.14</u>) may also be used in lieu of Method 18, if the target compounds are all known and are all listed in <u>Section 1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method; or

(iii) Provide a minimum residence time of 0.5 seconds at a minimum temperature of 760 °C.

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(2) A vapor recovery system (including but not limited to a carbon adsorption system or condenser), alone or in combination with other control devices, shall reduce the total organic compound emissions, less methane and ethane, or total organic hazardous air pollutants emissions vented to the control device of 95 percent by weight or greater or achieve an outlet total organic compound concentration, less methane and ethane, or total organic hazardous air pollutants concentration of 20 parts per million by volume. The 20 parts per million by volume performance standard is not applicable to compliance with the provisions of  $\frac{63.134}{5}$ .

(3) Except as specified in <u>paragraph (a) of § 63.108</u>, a flare shall comply with the requirements of § 63.11(b).

(4) A scrubber, alone or in combination with other control devices, shall reduce the total organic compound emissions, less methane and ethane, or total organic hazardous air pollutants emissions in such a manner that 95 weight-percent is either removed, or destroyed by chemical reaction with the scrubbing liquid or achieve an outlet total organic compound concentration, less methane and ethane, or total organic hazardous air pollutants concentration of 20 parts per million by volume. The 20 parts per million by volume performance standard is not applicable to compliance with the provisions of § 63.134 or § 63.135.

(5) Any other control device used shall, alone or in combination with other control devices, reduce the total organic compound emissions, less methane and ethane, or total organic hazardous air pollutants emissions vented to the control device by 95 percent by weight or greater or achieve an outlet total organic compound concentration, less methane and ethane, or total organic hazardous air pollutants concentration of 20 parts per million by volume. The 20 parts per million by volume performance standard is not applicable to compliance with the provisions of  $\frac{63.134}{5}$  or  $\frac{63.135}{5}$ .

(d) Except as provided in <u>paragraphs (d)(4)</u> and (5) of this section, an owner or operator shall demonstrate that each control device or combination of control devices achieves the appropriate conditions specified in <u>paragraph (c)</u> of this section by using one or more of the methods specified in <u>paragraphs (d)(1), (2)</u>, or (3) of this section.

(1) Performance tests conducted using the test methods and procedures specified in  $\S$  <u>63.145(i)</u> for control devices other than flares; or

(2) A design evaluation that addresses the vent stream characteristics and control device operating parameters specified in <u>paragraphs (d)(2)(i)</u> through <u>(vii)</u> of this section.

(i) For a thermal vapor incinerator, the design evaluation shall consider the vent stream composition, constituent concentrations, and flow rate and shall establish the design minimum and average temperature in the combustion zone and the combustion zone residence time.

(ii) For a catalytic vapor incinerator, the design evaluation shall consider the vent stream composition, constituent concentrations, and flow rate and shall establish the design minimum and average temperatures across the catalyst bed inlet and outlet.

(iii) For a boiler or process heater, the design evaluation shall consider the vent stream composition, constituent concentrations, and flow rate; shall establish the design minimum and average flame zone temperatures and combustion zone residence time; and shall describe the method and location where the vent stream is introduced into the flame zone.

(iv) For a condenser, the design evaluation shall consider the vent stream composition, constituent concentrations, flow rate, relative humidity, and temperature and shall establish the design outlet organic compound concentration level, design average temperature of the condenser exhaust vent stream, and the design average temperatures of the coolant fluid at the condenser inlet and outlet.

(v) For a carbon adsorption system that regenerates the carbon bed directly on-site in the control device such as a fixed-bed adsorber, the design evaluation shall consider the vent stream composition, constituent concentrations, flow rate, relative humidity, and temperature and shall establish the design exhaust vent stream organic compound concentration level, adsorption cycle time, number and capacity of carbon beds, type and working capacity of activated carbon used for carbon beds, design total regeneration stream mass or volumetric flow over the period of each complete carbon bed regeneration cycle, design carbon bed temperature after regeneration, design carbon bed regeneration time, and design service life of carbon.

(vi) For a carbon adsorption system that does not regenerate the carbon bed directly on-site in the control device such as a carbon canister, the design evaluation shall consider the vent stream composition, constituent concentrations, mass or volumetric flow rate, relative humidity, and temperature and shall establish the design exhaust vent stream organic compound

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concentration level, capacity of carbon bed, type and working capacity of activated carbon used for carbon bed, and design carbon replacement interval based on the total carbon working capacity of the control device and source operating schedule.

(vii) For a scrubber, the design evaluation shall consider the vent stream composition; constituent concentrations; liquid-to-vapor ratio; scrubbing liquid flow rate and concentration; temperature; and the reaction kinetics of the constituents with the scrubbing liquid. The design evaluation shall establish the design exhaust vent stream organic compound concentration level and will include the additional information in <u>paragraphs (d)(2)(vii)(A)</u> and (<u>B)</u> of this section for trays and a packed column scrubber.

(A) Type and total number of theoretical and actual trays;

(B) Type and total surface area of packing for entire column, and for individual packed sections if column contains more than one packed section.

(3) For flares, except as specified in <u>paragraph (a) of § 63.108</u>, the compliance determination specified in § 63.11(b) and § 63.145(j) of this subpart.

(4) An owner or operator using any control device specified in <u>paragraphs (d)(4)(i)</u> through <u>(iv)</u> of this section is exempt from the requirements in <u>paragraphs (d)(1)</u> through <u>(3)</u> of this section and from the requirements in <u>§ 63.6(f)</u>, and from the requirements of <u>paragraph (e)</u> of this section.

(i) A boiler or process heater with a design heat input capacity of 44 megawatts or greater.

(ii) A boiler or process heater into which the emission stream is introduced with the primary fuel.

(iii) A boiler or process heater burning hazardous waste for which the owner or operator:

(A) Has been issued a final permit under <u>part 270 of this chapter</u> and complies with the requirements of <u>part 266, subpart H</u> of this chapter;

(B) Has certified compliance with the interim status requirements of part 266, subpart H of this chapter;

(C) Has submitted a Notification of Compliance under  $\S 63.1207(j)$  and complies with the requirements of subpart EEE of this part; or

(D) Complies with subpart EEE of this part and will submit a Notification of Compliance under  $\S$  63.1207(j) by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(iv) A hazardous waste incinerator for which the owner or operator:

(A) Has been issued a final permit under <u>part 270 of this chapter</u> and complies with the requirements of <u>part 264</u>, <u>subpart O</u> <u>of this chapter</u>;

(B) Has certified compliance with the interim status requirements of part 265, subpart O of this chapter;

(C) Has submitted a Notification of Compliance under  $\S$  <u>63.1207(j)</u> and complies with the requirements <u>subpart EEE of this</u> <u>part</u>; or

(D) Complies with the requirements subpart EEE of this part and will submit a Notification of Compliance under  $\S$  <u>63.1207(j)</u> by the date the owner or operator would have been required to submit the initial performance test report for this subpart.

(5) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), if the owner or operator vents emissions through a closed vent system to an adsorber(s) that cannot be regenerated or a regenerative adsorber(s) that is regenerated offsite, then the requirements specified in paragraphs (d)(1) and (2) of this section do not apply. Instead, the owner or operator must install a system of two or more adsorber units in series and comply with the requirements specified in paragraphs (d)(5)(i) through (iii) of this section.

(i) Conduct an initial performance test or design evaluation of the adsorber and establish the breakthrough limit and adsorber bed life.

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part 60, using methane, propane, isobutylene, or the primary HAP being controlled as the calibration gas or Method 25A of appendix A-7 to <u>40 CFR part 60</u>, using methane, propane, or the primary HAP being controlled as the calibration gas.

(iii) Comply with <u>paragraph (d)(5)(iii)(A)</u> of this section, and comply with the monitoring frequency according to <u>paragraph (d)(5)(iii)(B)</u> of this section.

(A) The first adsorber in series must be replaced immediately when breakthrough, as defined in § 63.101, is detected between the first and second adsorber. The original second adsorber (or a fresh canister) will become the new first adsorber and a fresh adsorber will become the second adsorber. For purposes of this paragraph, "immediately" means within 8 hours of the detection of a breakthrough for adsorbers of 55 gallons or less, and within 24 hours of the detection of a breakthrough for adsorber or operator must monitor at the outlet of the first adsorber within 3 days of replacement to confirm it is performing properly.

(B) Based on the adsorber bed life established according to paragraph (d)(5)(i) of this section and the date the adsorbent was last replaced, conduct monitoring to detect breakthrough at least monthly if the adsorbent has more than 2 months of life remaining, at least weekly if the adsorbent has between 2 months and 2 weeks of life remaining, and at least daily if the adsorbent has 2 weeks or less of life remaining.

(e) The owner or operator of a control device that is used to comply with the provisions of this section shall monitor the control device in accordance with  $\frac{63.143 \text{ of this subpart}}{14.000 \text{ subpart}}$ .

(f) Except as provided in <u>§ 63.140 of this subpart</u>, if gaps, cracks, tears, or holes are observed in ductwork, piping, or connections to covers and control devices during an inspection, a first effort to repair shall be made as soon as practical but no later than 5 calendar days after identification. Repair shall be completed no later than 15 calendar days after identification or discovery of the defect.

[62 FR 2760, Jan. 17, 1997, as amended at 64 FR 20192, Apr. 26, 1999; 89 FR 43203, May 16, 2024]

### § 63.140 Process wastewater provisions—delay of repair.

(a) Delay of repair of equipment for which a control equipment failure or a gap, crack, tear, or hole has been identified, is allowed if the repair is technically infeasible without a shutdown, as defined in  $\frac{63.101}{100}$  of subpart F of this part, or if the owner or operator determines that emissions of purged material from immediate repair would be greater than the emissions likely to result from delay of repair. Repair of this equipment shall occur by the end of the next shutdown.

(b) Delay of repair of equipment for which a control equipment failure or a gap, crack, tear, or hole has been identified, is allowed if the equipment is emptied or is no longer used to treat or manage Group 1 wastewater streams or residuals removed from Group 1 wastewater streams.

(c) Delay of repair of equipment for which a control equipment failure or a gap, crack, tear, or hole has been identified is also allowed if additional time is necessary due to the unavailability of parts beyond the control of the owner or operator. Repair shall be completed as soon as practical. The owner or operator who uses this provision shall comply with the requirements of  $\frac{63.147(b)(7)}{5}$  to document the reasons that the delay of repair was necessary.

[62 FR 2762, Jan. 17, 1997, as amended at 66 FR 6933, Jan. 22, 2001]

# §§ 63.141-63.142 [Reserved]

# § 63.143 Process wastewater provisions—inspections and monitoring of operations.

(a) For each wastewater tank, surface impoundment, container, individual drain system, and oil-water separator that receives, manages, or treats a Group 1 wastewater stream, a residual removed from a Group 1 wastewater stream, a recycled Group 1 wastewater stream, or a recycled residual removed from a Group 1 wastewater stream, the owner or operator shall comply with the inspection requirements specified in table 11 of this subpart.

(b) For each design steam stripper and biological treatment unit used to comply with  $\frac{63.138 \text{ of this subpart}}{63.138 \text{ of this subpart}}$ , the owner or operator shall comply with the monitoring requirements specified in table 12 of this subpart.

(c) If the owner or operator elects to comply with Item 1 in table 12 to this subpart, the owner or operator shall request approval to monitor appropriate parameters that demonstrate proper operation of the biological treatment unit. The request shall be submitted according to the procedures specified in  $\S 63.151(f)$ , and shall include a description of planned reporting and recordkeeping procedures. The owner or operator shall include as part of the submittal the basis for the selected

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monitoring frequencies and the methods that will be used. The Administrator will specify appropriate reporting and recordkeeping requirements as part of the review of the permit application or by other appropriate means.

(d) If the owner or operator elects to comply with Item 3 in table 12 of this subpart, the owner or operator shall request approval to monitor appropriate parameters that demonstrate proper operation of the selected treatment process. The request shall be submitted according to the procedures specified in  $\frac{63.151(f)}{1000}$  of this subpart, and shall include a description of planned reporting and recordkeeping procedures. The Administrator will specify appropriate reporting and recordkeeping requirements as part of the review of the permit application or by other appropriate means.

(e) Except as provided in <u>paragraphs (e)(4)</u> and (e)(5) of this section, for each control device used to comply with the requirements of  $\frac{88}{63.133}$  through  $\frac{63.139}{63.139}$  of this subpart, the owner or operator shall comply with the requirements in  $\frac{8}{53.139}$  (d) of this subpart, and with the requirements specified in <u>paragraph (e)(1)</u>, (e)(2), or (e)(3) of this section.

(1) The owner or operator shall comply with the monitoring requirements specified in table 13 of this subpart; or

(2) The owner or operator shall use an organic monitoring device installed at the outlet of the control device and equipped with a continuous recorder. Continuous recorder is defined in  $\S$  63.111 of this subpart; or

(3) The owner or operator shall request approval to monitor parameters other than those specified in <u>paragraphs</u> (e)(1) and (e)(2) of this section. The request shall be submitted according to the procedures specified in § 63.151(f) of this <u>subpart</u>, and shall include a description of planned reporting and recordkeeping procedures. The Administrator will specify appropriate reporting and recordkeeping requirements as part of the review of the permit application or by other appropriate means.

(4) For a boiler or process heater in which all vent streams are introduced with primary fuel, the owner or operator shall comply with the requirements in  $\S$  63.139(d) of this subpart but the owner or operator is exempt from the monitoring requirements specified in paragraphs (e)(1) through (e)(3) of this section.

(5) For a boiler or process heater with a design heat input capacity of 44 megawatts or greater, the owner or operator shall comply with the requirements in § 63.139(d) of this subpart but the owner or operator is exempt from the monitoring requirements specified in paragraphs (e)(1) through (e)(3) of this section.

(f) For each parameter monitored in accordance with <u>paragraph (c)</u>, (d), or (e) of this section, the owner or operator shall establish a range that indicates proper operation of the treatment process or control device. In order to establish the range, the owner or operator shall comply with the requirements specified in  $\frac{88}{63.146(b)(7)(ii)(A)}$  and (b)(8)(ii) of this subpart.

(g) Monitoring equipment shall be installed, calibrated, and maintained according to the manufacturer's specifications or other written procedures that provide adequate assurance that the equipment would reasonably be expected to monitor accurately.

[62 FR 2762, Jan. 17, 1997, as amended at 89 FR 43204, May 16, 2024]

# § 63.144 Process wastewater provisions—test methods and procedures for determining applicability and Group 1/Group 2 determinations (determining which wastewater streams require control).

(a) *Procedures to determine applicability*. An owner or operator shall comply with <u>paragraph (a)(1)</u> or <u>(a)(2)</u> of this section for each wastewater stream to determine which wastewater streams require control for Table 8 and/or Table 9 compounds. The owner or operator may use a combination of the approaches in <u>paragraphs (a)(1)</u> and <u>(a)(2)</u> of this section for different wastewater streams generated at the source.

(1) Determine Group 1 or Group 2 status. Determine whether a wastewater stream is a Group 1 or Group 2 wastewater stream in accordance with <u>paragraphs (b)</u> and (c) of this section.

(2) *Designate as Group 1*. An owner or operator may designate as a Group 1 wastewater stream a single wastewater stream or a mixture of wastewater streams. The owner or operator is not required to determine the concentration or flow rate for each designated Group 1 wastewater stream for the purposes of this section.

(b) Procedures to establish concentrations, when determining Group status under <u>paragraph (a)(1)</u> of this section. An owner or operator who elects to comply with the requirements of <u>paragraph (a)(1)</u> of this section shall determine the annual average concentration for Table 8 and/or Table 9 compounds according to <u>paragraph (b)(1)</u> of this section for existing sources or <u>paragraph (b)(2)</u> of this section for new sources. The annual average concentration shall be a flow weighted average

representative of actual or anticipated operation of the chemical manufacturing process unit generating the wastewater over a designated 12 month period. For flexible operation units, the owner or operator shall consider the anticipated production over the designated 12 month period and include all wastewater streams generated by the process equipment during this period. The owner/operator is not required to determine the concentration of Table 8 or Table 9 compounds that are not reasonably expected to be in the process.

(1) Existing sources. An owner or operator of an existing source who elects to comply with the requirements of paragraph (a)(1) of this section shall determine the flow weighted total annual average concentration for Table 9 compounds. For the purposes of this section, the term concentration, whether concentration is used alone or with other terms, may be adjusted by multiplying by the compound-specific fraction measured (Fm) factors listed in table 34 of this subpart unless determined by the methods in (63.144(b)(5)(i)(A)) and/or (B). When concentration is determined by Method 305 as specified in (6) 63.144(b)(5)(i)(B), concentration may be adjusted by dividing by the compound-specific Fm factors listed in table 34 of this subpart. When concentration is determined by Method 25D as specified in  $\frac{63.144(b)(5)(i)(A)}{(A)}$ , concentration may not be adjusted by the compound-specific Fm factors listed in table 34 of this subpart. Compound-specific Fm factors may be used only when concentrations of individual compounds are determined or when only one compound is in the wastewater stream. Flow weighted total annual average concentration for Table 9 compounds means the total mass of Table 9 compounds occurring in the wastewater stream during the designated 12-month period divided by the total mass of the wastewater stream during the same designated 12-month period. The total annual average concentration shall be determined for each wastewater stream either at the point of determination, or downstream of the point of determination with adjustment for concentration changes made according to paragraph (b)(6) of this section. The procedures specified in paragraphs (b)(3), (b)(4), and (b)(5) of this section are considered acceptable procedures for determining the annual average concentration. They may be used in combination, and no one procedure shall take precedence over another.

(2) New sources. An owner or operator of a new source who elects to comply with the requirements of paragraph (a)(1) of this section shall determine both the flow weighted total annual average concentration for Table 9 compounds and the flow weighted annual average concentration for each Table 8 compound. For the purposes of this section, the term concentration, whether concentration is used alone or with other terms, may be adjusted by multiplying by the compound-specific Fm factors listed in table 34 of this subpart unless determined by the methods in (63.144(b)(5)(i)(A)) and/or (B). When concentration is determined by Method 305 as specified in § 63.144(b)(5)(i)(B), concentration may be adjusted by dividing by the compound-specific Fm factors listed in table 34 of this subpart. When concentration is determined by Method 25D as specified in (63.144(b)(5)(i)(A)), concentration may not be adjusted by the compound-specific Fm factors listed in table 34 of this subpart. Compound-specific fraction measured factors are compound specific and shall be used only when concentration of individual compounds are determined or when only one compound is in the wastewater stream. The flow weighted annual average concentration of each Table 8 compound means the mass of each Table 8 compound occurring in the wastewater stream during the designated 12-month period divided by the total mass of the wastewater stream during the same designated 12-month period. Flow weighted total annual average concentration for Table 9 compounds means the total mass of Table 9 compounds occurring in the wastewater stream during the designated 12-month period divided by the total mass of the wastewater stream during the same designated 12-month period. The annual average concentration shall be determined for each wastewater stream either at the point of determination, or downstream of the point of determination with adjustment for concentration changes made according to paragraph (b)(6) of this section. Procedures specified in paragraphs (b)(3), (b)(4), and (b)(5) of this section are considered acceptable procedures for determining the annual average concentration. They may be used in combination, and no one procedure shall take precedence over another.

(3) *Knowledge of the wastewater*. Where knowledge is used to determine the annual average concentration, the owner or operator shall provide sufficient information to document the annual average concentration for wastewater streams determined to be Group 2 wastewater streams. Documentation to determine the annual average concentration is not required for Group 1 streams. Examples of acceptable documentation include material balances, records of chemical purchases, process stoichiometry, or previous test results. If test data are used, the owner or operator shall provide documentation describing the testing protocol and the means by which any losses of volatile compounds during sampling, and the bias and accuracy of the analytical method, were accounted for in the determination.

(4) *Bench-scale or pilot-scale test data.* Where bench-scale or pilot-scale test data are used to determine the annual average concentration, the owner or operator shall provide sufficient information to document that the data are representative of the actual annual average concentration, or are reliably indicative of another relevant characteristic of the wastewater stream that could be used to predict the annual average concentration. For concentration data, the owner or operator shall also provide

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documentation describing the testing protocol, and the means by which any losses of volatile compounds during sampling, and the bias and accuracy of the analytical method, were accounted for in the determination of annual average concentration.

(5) Test data from sampling at the point of determination or at a location downstream of the point of determination. Where an owner or operator elects to comply with paragraph (a)(1) of this section by measuring the concentration for the relevant Table 8 or Table 9 compounds, the owner or operator shall comply with the requirements of this paragraph. For each wastewater stream, measurements shall be made either at the point of determination, or downstream of the point of determination with adjustment for concentration changes made according to paragraph (b)(6) of this section. A minimum of three samples from each wastewater stream shall be taken. Samples may be grab samples or composite samples.

(i) *Methods*. The owner or operator shall use any of the methods specified in <u>paragraphs (b)(5)(i)(A)</u> through (b)(5)(i)(F) of this section.

(A) Method 25D. Use procedures specified in Method 25D of <u>40 CFR part 60, appendix A</u>.

(B) Method 305. Use procedures specified in Method 305 of 40 CFR part 63, appendix A.

(C) Methods 624 and 625. Use procedures specified in Methods 624 and 625 of  $\frac{40 \text{ CFR part 136}}{136, \text{ appendix A}}$  and comply with the sampling protocol requirements specified in paragraph (b)(5)(ii) of this section. If these methods are used to analyze one or more compounds that are not on the method's published list of approved compounds, the Alternative Test Procedure specified in  $\frac{40 \text{ CFR 136.4}}{136.5}$  shall be followed. For Method 625, make corrections to the compounds for which the analysis is being conducted based on the accuracy as recovery factors in Table 7 of the method.

(D) Method 1624 and Method 1625. Use procedures specified in Method 1624 and Method 1625 of  $\frac{40 \text{ CFR part 136}}{40 \text{ cFR part 136}}$ , appendix A and comply with the requirements specified in paragraph (b)(5)(ii) of this section. If these methods are used to analyze one or more compounds that are not on the method's published list of approved compounds, the Alternative Test Procedure specified in  $\frac{40 \text{ CFR 136.4}}{40 \text{ CFR 136.4}}$  and  $\frac{136.5}{40 \text{ shall be followed}}$ .

(E) Other EPA method(s). Use procedures specified in the method and comply with the requirements specified in paragraphs (b)(5)(ii) and either paragraph (b)(5)(iii)(A) or (b)(5)(iii)(B) of this section.

(F) *Method(s) other than EPA method.* Use procedures specified in the method and comply with the requirements specified in paragraphs (b)(5)(ii) and (b)(5)(iii)(A) of this section.

(G) Method 8260B. Use procedures specified in Method 8260B in the SW-846 Compendium of Methods.

(H) Method 316. Use Method 316 to determine formaldehyde concentration.

(I) Methods for ethylene oxide. Methods specified in  $\S 63.109(d)$  for analysis of ethylene oxide in wastewater.

(ii) *Sampling plan.* The owner or operator who is expressly referred to this paragraph by provisions of this subpart shall prepare a sampling plan. Wastewater samples shall be collected using sampling procedures which minimize loss of organic compounds during sample collection and analysis and maintain sample integrity. The sample plan shall include procedures for determining recovery efficiency of the relevant hazardous air pollutants listed in table 8 or table 9 of this subpart. An example of an acceptable sampling plan would be one that incorporates similar sampling and sample handling requirements to those of Method 25D of <u>40 CFR part 60, appendix A</u>. The sampling plan shall be maintained at the facility.

(iii) *Validation of methods*. The owner or operator shall validate EPA methods other than Methods 25D, 305, 624, 625, 1624, and 1625 using the procedures specified in paragraph (b)(5)(iii)(A) or (b)(5)(iii)(B) of this section. The owner or operator shall validate other methods as specified in paragraph (b)(5)(iii)(A) of this section.

(A) *Validation of EPA methods and other methods.* The method used to measure organic hazardous air pollutants concentrations in the wastewater shall be validated according to <u>section 5.1</u> or <u>5.3</u>, and the corresponding calculations in <u>section 6.1</u> or <u>6.3</u>, of Method 301 of <u>appendix A of this part</u>. The data are acceptable if they meet the criteria specified in <u>section 6.1.5</u> or <u>6.3.3</u> of Method 301 of <u>appendix A of this part</u>. If correction is required under <u>section 6.3.3</u> of Method 301 of <u>appendix A of this part</u>. If correction is required under <u>section 6.3.3</u> of Method 301 of <u>appendix A of this part</u>, the data are acceptable if the correction factor is within the range 0.7 to 1.30. Other sections of Method 301 of <u>appendix A of this part</u> are not required. The concentrations of the individual organic hazardous air pollutants measured in the water may be corrected to their concentrations had they been measured by Method 305 of <u>appendix A of this part</u>, by multiplying each concentration by the compound-specific fraction measured (Fm) factor listed in table 34 of this subpart.

(B) *Validation for EPA methods*. Follow the procedures as specified in "Alternative Validation Procedure for EPA Waste Methods" <u>40 CFR part 63, appendix D</u>.

(iv) *Calculations of average concentration*. The average concentration for each individually speciated Table 8 compound shall be calculated by adding the individual values determined for the specific compound in each sample and dividing by the number of samples. The total average concentration of Table 9 compounds shall be calculated by first summing the concentration of the individual compounds to obtain a total hazardous air pollutants concentration for the sample; add the sample totals and then divide by the number of samples in the run to obtain the sample average for the run. If the method used does not speciate the compounds, the sample results should be added and this total divided by the number of samples in the run to obtain the sample average for the run.

(6) Adjustment for concentrations determined downstream of the point of determination. The owner or operator shall make corrections to the annual average concentration or total annual average concentration when the concentration is determined downstream of the point of determination at a location where: two or more wastewater streams have been mixed; one or more wastewater streams have been treated; or, losses to the atmosphere have occurred. The owner or operator shall make the adjustments either to the individual data points or to the final annual average concentration.

(c) Procedures to determine flow rate, when evaluating Group status under paragraph (a)(1) of this section. An owner or operator who elects to comply with paragraph (a)(1) of this section shall determine the annual average flow rate of the wastewater stream either at the point of determination for each wastewater stream, or downstream of the point of determination with adjustment for flow rate changes made according to paragraph (c)(4) of this section. These procedures may be used in combination for different wastewater streams at the source. The annual average flow rate for the wastewater stream shall be representative of actual or anticipated operation of the chemical manufacturing process unit generating the wastewater over a designated 12-month period. The owner or operator shall consider the total annual wastewater volume generated by the chemical manufacturing process unit. If the chemical manufacturing process unit is a flexible operation unit, the owner or operator shall consider all anticipated production in the process equipment over the designated 12-month period. The procedures specified in paragraphs (c)(1), (c)(2), and (c)(3) of this section are considered acceptable procedures for determining the flow rate. They may be used in combination, and no one procedure shall take precedence over another.

(1) *Knowledge of the wastewater*. The owner or operator may use knowledge of the wastewater stream and/or the process to determine the annual average flow rate. The owner or operator shall use the maximum expected annual average production capacity of the process unit, knowledge of the process, and/or mass balance information to either: Estimate directly the annual average wastewater flow rate; or estimate the total annual wastewater volume and then divide total volume by 525,600 minutes in a year. Where knowledge is used to determine the annual average flow rate, the owner or operator shall provide sufficient information to document the flow rate for wastewater streams determined to be Group 2 wastewater streams. Documentation to determine the annual average flow rate is not required for Group 1 streams.

(2) *Historical records.* The owner or operator may use historical records to determine the annual average flow rate. Derive the highest annual average flow rate of wastewater from historical records representing the most recent 5 years of operation or, if the process unit has been in service for less than 5 years but at least 1 year, from historical records representing the total operating life of the process unit. Where historical records are used to determine the annual average flow rate, the owner or operator shall provide sufficient information to document the flow rate for wastewater streams determined to be Group 2 wastewater streams. Documentation to determine the annual average flow rate is not required for Group 1 streams.

(3) Measurements of flow rate. Where an owner or operator elects to comply with paragraph (a)(1) of this section by measuring the flow rate, the owner or operator shall comply with the requirements of this paragraph. Measurements shall be made at the point of determination, or at a location downstream of the point of determination with adjustments for flow rate changes made according to paragraph (c)(4) of this section. Where measurement data are used to determine the annual average flow rate, the owner or operator shall provide sufficient information to document the flow rate for wastewater streams determined to be Group 2 wastewater streams. Documentation to determine the annual average flow rate is not required for Group 1 streams.

(4) Adjustment for flow rates determined downstream of the point of determination. The owner or operator shall make corrections to the annual average flow rate of a wastewater stream when it is determined downstream of the point of determination at a location where two or more wastewater streams have been mixed or one or more wastewater streams have been treated. The owner or operator shall make corrections for such changes in the annual average flow rate.

[62 FR 2762, Jan. 17, 1997, as amended at 79 FR 11283, Feb. 27, 2014; 89 FR 43205, May 16, 2024]

# National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

# § 63.145 Process wastewater provisions—test methods and procedures to determine compliance.

(a) *General.* This section specifies the procedures for performance tests that are conducted to demonstrate compliance of a treatment process or a control device with the control requirements specified in § 63.138 of this subpart. Owners or operators conducting a design evaluation shall comply with the requirements of paragraph (a)(1) or (a)(2) of this section. Owners or operators conducting a performance test shall comply with the applicable requirements in paragraphs (a) through (i) of this section.

(1) Performance tests and design evaluations for treatment processes. If design steam stripper option ( $\S$  63.138(d)) or RCRA option ( $\S$  63.138(h)) is selected to comply with  $\S$  63.138, neither a design evaluation nor a performance test is required. For any other non-biological treatment process, the owner or operator shall conduct either a design evaluation as specified in  $\S$  63.138(j), or a performance test as specified in this section. For closed biological treatment processes, the owner or operator shall conduct either a design evaluation. For each open biological treatment process, the owner or operator shall conduct a performance test as specified in this section.

Note:

Some open biological treatment processes may not require a performance test. Refer to  $\frac{63.145(h)}{10}$  and table 36 of this subpart to determine whether the biological treatment process meets the criteria that exempt the owner or operator from conducting a performance test.

(2) Performance tests and design evaluations for control devices. The owner or operator shall conduct either a design evaluation as specified in  $\frac{63.139(d)}{10}$ , or a performance test as specified in <u>paragraph (i)</u> of this section for control devices other than flares and <u>paragraph (j)</u> of this section for flares.

(3) Representative process unit operating conditions. Except as specified in paragraph(a)(10) of this section, compliance shall be demonstrated for representative operating conditions. Operations during periods of startup, shutdown, or malfunction and periods of nonoperation shall not constitute representative conditions. The owner or operator shall record the process information that is necessary to document operating conditions during the test.

(4) Representative treatment process or control device operating conditions. Performance tests shall be conducted when the treatment process or control device is operating at a representative inlet flow rate and concentration. If the treatment process or control device will be operating at several different sets of representative operating conditions, the owner or operator shall comply with paragraphs (a)(4)(i) and (a)(4)(ii) of this section. The owner or operator shall record information that is necessary to document treatment process or control device operating conditions during the test.

(i) *Range of operating conditions*. If the treatment process or control device will be operated at several different sets of representative operating conditions, performance testing over the entire range is not required. In such cases, the performance test results shall be supplemented with modeling and/or engineering assessments to demonstrate performance over the operating range.

(ii) *Consideration of residence time.* If concentration and/or flow rate to the treatment process or control device are not relatively constant (i.e., comparison of inlet and outlet data will not be representative of performance), the owner or operator shall consider residence time, when determining concentration and flow rate.

(5) *Testing equipment*. All testing equipment shall be prepared and installed as specified in the applicable test methods, or as approved by the Administrator.

(6) Compounds not required to be considered in performance tests or design evaluations. Compounds that meet the requirements specified in paragraph (a)(6)(i), (a)(6)(ii), or (a)(6)(iii) of this section are not required to be included in the performance test. Concentration measurements based on Method 305 shall be adjusted by dividing each concentration by the compound-specific Fm factor listed in table 34 of this subpart. Concentration measurements based on methods other than Method 305 shall not be adjusted by the compound-specific Fm factor listed in table 34 of this subpart.

(i) Compounds not used or produced by the chemical manufacturing process unit; or

(ii) Compounds with concentrations at the point of determination that are below 1 part per million by weight; or

(iii) Compounds with concentrations at the point of determination that are below the lower detection limit where the lower detection limit is greater than 1 part per million by weight. The method shall be an analytical method for wastewater which has that compound as a target analyte.

(7) Treatment using a series of treatment processes. In all cases where the wastewater provisions in this subpart allow or require the use of a treatment process to comply with emissions limitations, the owner or operator may use multiple treatment processes. The owner or operator complying with the requirements of  $\frac{63.138(a)(7)(i)}{63.145(a)(7)(i)}$ , when wastewater is conveyed by hard-piping, shall comply with either  $\frac{68}{63.138(a)(7)(i)}$  or  $\frac{63.145(a)(7)(i)}{63.145(a)(7)(i)}$  of this subpart. The owner or operator complying with the requirements of  $\frac{63.138(a)(7)(i)}{63.145(a)(7)(i)}$  of this subpart shall comply with the requirements of  $\frac{63.145(a)(7)(i)}{63.145(a)(7)(i)}$  of this subpart.

(i) The owner or operator shall conduct the performance test across each series of treatment processes. For each series of treatment processes, inlet concentration and flow rate shall be measured either where the wastewater stream enters the first treatment process in a series of treatment processes, or prior to the first treatment process as specified in  $\S 63.145(a)(9)$  of this subpart. For each series of treatment processes, outlet concentration and flow rate shall be measured where the wastewater stream exits the last treatment process in the series of treatment processes, except when the last treatment process is an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process is either an open or a closed aerobic biological treatment process demonstrating compliance by using the procedures in  $\S 63.145$  (f) or (g) of this subpart, inlet and outlet concentrations and flow rates shall be measured as provided in paragraphs (a)(7)(i)(A) and (a)(7)(i)(B) of this section. The mass flow rates removed or destroyed by the series of treatment processes and by the biological treatment process are all used to calculate actual mass removal (AMR) as specified in  $\S 63.145$ (f)(5)(ii) of this subpart.

(A) The inlet and outlet to the series of treatment processes prior to the biological treatment process are the points at which the wastewater enters the first treatment process and exits the last treatment process in the series, respectively, except as provided in paragraph (a)(9)(ii) of this section.

(B) The inlet to the biological treatment process shall be the point at which the wastewater enters the biological treatment process or the outlet from the series of treatment processes identified in paragraph (a)(7)(i)(A) of this section, except as provided in paragraph (a)(9)(ii) of this section.

(ii) The owner or operator shall conduct the performance test across each treatment process in the series of treatment processes. The mass flow rate removed or destroyed by each treatment process shall be added together to determine whether compliance has been demonstrated using § 63.145 (c), (d), (e), (f), and (g), as applicable. If a biological treatment process is one of the treatment processes in the series of treatment processes, the inlet to the biological treatment process shall be the point at which the wastewater enters the biological treatment process, or the inlet to the equalization tank if all the criteria of paragraph (a)(9)(ii) of this section are met.

(8) When using a biological treatment process to comply with  $\S$  63.138 of this subpart, the owner or operator may elect to calculate the AMR using a subset of Table 8 and/or Table 9 compounds determined at the point of determination or downstream of the point of determination with adjustment for concentration and flowrate changes made according to  $\S$  63.144(b)(6) and  $\S$  63.144(c)(4) of this subpart, respectively. All Table 8 and/or Table 9 compounds measured to determine the RMR, except as provided by  $\S$  63.145(a)(6), shall be included in the RMR calculation.

(9) The owner or operator determining the inlet for purposes of demonstrating compliance with § 63.145 (e), (f), or (g) of this subpart may elect to comply with paragraph (a)(9)(i) or (a)(9)(ii) of this section.

(i) When wastewater is conveyed exclusively by hard-piping from the point of determination to a treatment process that is either the only treatment process or the first in a series of treatment processes (i.e., no treatment processes or other waste management units are used upstream of this treatment process to store, handle, or convey the wastewater), the inlet to the treatment process shall be at any location from the point of determination to where the wastewater stream enters the treatment process. When samples are taken upstream of the treatment process and before wastewater streams have converged, the owner or operator shall ensure that the mass flow rate of all Group 1 wastewater streams is accounted for when using  $\frac{63.138}{8}$  (e) or (f) to comply and that the mass flow rate of all Group 1 and Group 2 wastewater streams is accounted for when using  $\frac{8}{8}$  63.138(g) to comply, except as provided in  $\frac{8}{8}$  63.145(a)(6).

(ii) The owner or operator may consider the inlet to the equalization tank as the inlet to the biological treatment process if all the criteria in <u>paragraphs (a)(9)(ii)(A)</u> through (a)(9)(ii)(C) of this section are met. The outlet from the series of treatment processes prior to the biological treatment process is the point at which the wastewater exits the last treatment process in the series prior to the equalization tank, if the equalization tank and biological treatment process are part of a series of treatment processes. The owner or operator shall ensure that the mass flow rate of all Group 1 wastewater streams is accounted for

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when using § 63.138 (e) or (f) to comply and that the mass flow rate of all Group 1 and Group 2 wastewater streams is accounted for when using § 63.138(g) to comply, except as provided in § 63.145(a)(6).

(A) The wastewater is conveyed by hard-piping from either the last previous treatment process or the point of determination to the equalization tank.

(B) The wastewater is conveyed from the equalization tank exclusively by hard-piping to the biological treatment process and no treatment processes or other waste management units are used to store, handle, or convey the wastewater between the equalization tank and the biological treatment process.

(C) The equalization tank is equipped with a fixed roof and a closed vent system that routes emissions to a control device that meets the requirements of  $\frac{63.133(a)(2)(i)}{2}$  and  $\frac{63.133(b)(1)}{2}$  through (b)(4) of this subpart.

(10) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the requirement of paragraph (a)(3) of this section no longer applies. Instead, owners and operators must comply with the conditions specified in § 63.103(b)(3)(ii) of subpart F of this part.

(b) *Noncombustion treatment process—concentration limits.* This paragraph applies to performance tests that are conducted to demonstrate compliance of a noncombustion treatment process with the parts per million by weight wastewater stream concentration limits at the outlet of the treatment process. This compliance option is specified in  $\S$  63.138(b)(1) and  $\S$  63.138(c)(1). Wastewater samples shall be collected using sampling procedures which minimize loss of organic compounds during sample collection and analysis and maintain sample integrity per  $\S$  63.144(b)(5)(ii). Samples shall be collected and analyzed using the procedures specified in  $\S$  63.144 (b)(5)(i), (b)(5)(ii), and (b)(5)(iii) of this subpart. Samples may be grab samples or composite samples. Samples shall be taken at approximately equally spaced time intervals over a 1-hour period. Each 1-hour period constitutes a run, and the performance test shall consist of a minimum of 3 runs. Concentration measurements based on Method 305 may be adjusted by dividing each concentration by the compound-specific Fm factor listed in Table 34 of this subpart. Concentration measurements based on methods other than Method 305 may be adjusted by multiplying each concentration by the compound-specific Fm factor listed in table 34 of this subpart. (For wastewater streams that are Group 1 for both Table 8 and Table 9 compounds, compliance is demonstrated only if the sum of the concentrations of Table 9 compounds is less than 50 ppmw, and the concentration of each Table 8 compound is less than 10 ppmw.)

(c) Noncombustion, nonbiological treatment process: Percent mass removal/destruction option. This paragraph applies to performance tests that are conducted to demonstrate compliance of a noncombustion, nonbiological treatment process with the percent mass removal limits specified in § 63.138(e) (1) and (2) for Table 8 and/or Table 9 compounds. The owner or operator shall comply with the requirements specified in § 63.145 (c)(1) through (c)(6) of this subpart.

(1) Concentration. The concentration of Table 8 and/or Table 9 compounds entering and exiting the treatment process shall be determined as provided in this paragraph. Wastewater samples shall be collected using sampling procedures which minimize loss of organic compounds during sample collection and analysis and maintain sample integrity per § 63.144(b)(5)(ii). The method shall be an analytical method for wastewater which has that compound as a target analyte. Samples may be grab samples or composite samples. Samples shall be taken at approximately equally spaced time intervals over a 1-hour period. Each 1-hour period constitutes a run, and the performance test shall consist of a minimum of 3 runs. Concentration measurements based on Method 305 shall be adjusted by dividing each concentration by the compound-specific Fm factor listed in Table 34 of this subpart. Concentration measurements based on methods other than Method 305 shall not adjust by the compound-specific Fm factor listed in Table 34 of this subpart.

(2) *Flow rate.* The flow rate of the entering and exiting wastewater streams shall be determined using inlet and outlet flow measurement devices, respectively. Where the outlet flow is not greater than the inlet flow, a flow measurement device shall be used, and may be used at either the inlet or outlet. Flow rate measurements shall be taken at the same time as the concentration measurements.

(3) *Calculation of mass flow rate—for noncombustion, nonbiological treatment processes.* The mass flow rates of Table 8 and/or Table 9 compounds entering and exiting the treatment process are calculated as follows.

$$QMW_{a} = \frac{\rho}{p*10^{6}} \left( \sum_{k=1}^{p} Q_{a,k} C_{T,a,k} \right)$$
(Eqn WW1)  
$$QMW_{b} = \frac{\rho}{p*10^{6}} \left( \sum_{k=1}^{p} Q_{b,k} C_{T,b,k} \right)$$
(Eqn WW2)

Where:

 $QMW_a$ ,  $QMW_b = Mass$  flow rate of Table 8 or Table 9 compounds, average of all runs, in wastewater entering ( $QMW_a$ ) or exiting ( $QMW_b$ ) the treatment process, kilograms per hour.

 $\rho$  = Density of the wastewater, kilograms per cubic meter.

 $Q_{a, k}$ ,  $Qb_{b, k}$  = Volumetric flow rate of wastewater entering  $(Q_{a, k})$  or exiting  $(Q_{b, k})$  the treatment process during each run k, cubic meters per hour.

 $C_{T, a, k}$ ,  $C_{T, b, k}$  = Total concentration of Table 8 or Table 9 compounds in wastewater entering ( $C_{T, a, k}$ ) or exiting ( $C_{T, b, k}$ ) the treatment process during each run k, parts per million by weight.

p = Number of runs.

k = Identifier for a run.

 $10^6$  = conversion factor, mg/kg

(4) *Percent removal calculation for mass flow rate*. The percent mass removal across the treatment process shall be calculated as follows:

$$E = \frac{QMW_a - QMW_b}{QMW_a} \times 100$$
 (Eqn WW3)

Where:

E = Removal or destruction efficiency of the treatment process, percent.

 $QMW_a$ ,  $QMW_b = Mass$  flow rate of Table 8 or Table 9 compounds in wastewater entering ( $QMW_a$ ) and exiting ( $QMW_b$ ) the treatment process, kilograms per hour (as calculated using Equations WW1 and WW2).

(5) Calculation of flow-weighted average of Fr values. If complying with  $\S$  63.138(e)(2), use Equation WW8 to calculate the flow-weighted average of the Fr values listed in Table 9 of this subpart. When the term "combustion" is used in Equation WW8, the term "treatment process" shall be used for the purposes of this paragraph.

(6) Compare mass removal efficiency to required efficiency. Compare the mass removal efficiency (calculated in Equation WW3) to the required efficiency as specified in § 63.138(e) of this subpart. If complying with § 63.138(e)(1), compliance is demonstrated if the mass removal efficiency is 99 percent or greater. If complying with § 63.138(e)(2), compliance is demonstrated if the mass removal efficiency is greater than or equal to the flow-weighted average of the Fr values calculated in Equation WW8.

(d) Combustion treatment processes: percent mass removal/destruction option. This paragraph applies to performance tests that are conducted to demonstrate compliance of a combustion treatment process with the percent mass destruction limits specified in § 63.138(e) (1) and (2) for Table 9 compounds, and/or § 63.138(e)(1) for Table 8 compounds. The owner or operator shall comply with the requirements specified in § 63.145 (d)(1) through (d)(9) of this subpart. (Wastewater streams that are Group 1 for both Table 8 and Table 9 compounds need only do the compliance demonstration for Table 9 compounds.)

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(1) Concentration in wastewater stream entering the combustion treatment process. The concentration of Table 8 and/or Table 9 compounds entering the treatment process shall be determined as provided in this paragraph. Wastewater samples shall be collected using sampling procedures which minimize loss of organic compounds during sample collection and analysis and maintain sample integrity per  $\S$  63.144(b)(5)(ii). The method shall be an analytical method for wastewater which has that compound as a target analyte. Samples may be grab samples or composite samples. Samples shall be taken at approximately equally spaced time intervals over a 1-hour period. Each 1-hour period constitutes a run, and the performance test shall consist of a minimum of 3 runs. Concentration measurements based on Method 305 of appendix A of this part shall be adjusted by dividing each concentration by the compound-specific Fm factor listed in table 34 of this subpart. Concentration measurements based on methods other than Method 305 shall not adjust by the compound-specific Fm factor listed in table 34 of this subpart.

(2) *Flow rate of wastewater entering the combustion treatment process.* The flow rate of the wastewater stream entering the combustion treatment process shall be determined using an inlet flow meter. Flow rate measurements shall be taken at the same time as the concentration measurements.

(3) *Calculation of mass flow rate in wastewater stream entering combustion treatment processes.* The mass flow rate of Table 8 and/or Table 9 compounds entering the treatment process is calculated as follows:

QMW<sub>a</sub> = 
$$\frac{\rho}{p*10^6} \left( \sum_{k=1}^{p} Q_{a,k} * C_{T,a,k} \right)$$
 (Eqn WW4)

Where:

QMW<sub>a</sub> = Mass flow rate of Table 8 or Table 9 compounds entering the combustion unit, kilograms per hour.

 $\rho$  = Density of the wastewater stream, kilograms per cubic meter.

 $Q_{a,k}$  = Volumetric flow rate of wastewater entering the combustion unit during run k, cubic meters per hour.

 $C_{T, a, k}$  = Total concentration of Table 8 or Table 9 compounds in the wastewater stream entering the combustion unit during run k, parts per million by weight.

- p = Number of runs.
- k = Identifier for a run.

(4) Concentration in vented gas stream exiting the combustion treatment process. The concentration of table 8 and/or table 9 compounds exiting the combustion treatment process in any vented gas stream shall be determined as provided in this paragraph. Samples may be grab samples or composite samples. Samples shall be taken at approximately equally spaced time intervals over a 1-hour period. Each 1-hour period constitutes a run, and the performance test shall consist of a minimum of 3 runs. Concentration measurements shall be determined using Method 18 of appendix A-6 to <u>40 CFR part 60</u>. ASTM D6420-18 (incorporated by reference, see § <u>63.14</u>) may also be used in lieu of Method 18, if the target compounds are all known and are all listed in <u>Section 1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method. Alternatively, any other test method validated according to the procedures in Method 301 of appendix A to this part may be used.

(5) *Volumetric flow rate of vented gas stream exiting the combustion treatment process.* The volumetric flow rate of the vented gas stream exiting the combustion treatment process shall be determined using Method 2, 2A, 2C, or 2D of <u>40 CFR</u> part 60, appendix A, as appropriate. Volumetric flow rate measurements shall be taken at the same time as the concentration measurements.

(6) *Calculation of mass flow rate of vented gas stream exiting combustion treatment processes.* The mass flow rate of Table 8 and/or Table 9 compounds in a vented gas stream exiting the combustion treatment process shall be calculated as follows:

(Eqn WW5) [Reserved]

$$QMG_b = K_2 \left( \sum_{i=1}^{n} CG_{b,i} MW_i \right) QG_b$$
 (Eqn WW6)

Where:

 $CG_{a, i}$ ,  $CG_{b, i}$  = Concentration of total organic compounds (TOC) (minus methane and ethane) or total organic hazardous air pollutants, in vented gas stream, entering ( $CG_{a, i}$ ) and exiting ( $CG_{b, i}$ ) the control device, dry basis, parts per million by volume.

 $QMG_a$ ,  $QMG_b = Mass$  rate of TOC (minus methane and ethane) or total organic hazardous air pollutants, in vented gas stream, entering ( $QMG_a$ ) and exiting ( $QMG_b$ ) the control device, dry basis, kilograms per hour.

MW<sub>i</sub> = Molecular weight of a component, kilogram/kilogram-mole.

 $QG_a, QG_b = Flow$  rate of gas stream entering  $(QG_a)$  and exiting  $(QG_b)$  the control device, dry standard cubic meters per hour.

 $K_2 = Constant$ ,  $41.57 \times 10^{-9}$  (parts per million)<sup>-1</sup> (gram-mole per standard cubic meter) (kilogram/gram), where standard temperature (gram-mole per standard cubic meter) is 20 °Celsius.

i = Identifier for a compound.

n = Number of components in the sample.

(7) *Destruction efficiency calculation*. The destruction efficiency of the combustion unit for Table 8 and/or Table 9 compounds shall be calculated as follows:

$$E = \frac{QMW_s - QMG_{b} * 100}{QMW_s}$$
 (Eqn W

Where:

E = Destruction efficiency of Table 8 or Table 9 compounds for the combustion unit, percent.

QMW<sub>a</sub> = Mass flow rate of Table 8 or Table 9 compounds entering the combustion unit, kilograms per hour.

 $QMG_b$  = Mass flow rate of Table 8 or Table 9 compounds in vented gas stream exiting the combustion treatment process, kilograms per hour.

(8) Calculation of flow-weighted average of Fr values. Use Equation WW8 to calculate the flow-weighted average of the Fr values listed in table 9 of this subpart.

$$Fr_{avg} = \left[\frac{\sum_{i=1}^{n} \sum_{k=1}^{p} Fr_{i} * C_{i,a,k} * Q_{a,k}}{\sum_{k=1}^{p} \sum_{i=1}^{n} C_{i,a,k} * Q_{a,k}}\right] * 100 \quad (Eqn WW8)$$

Where:

 $Fr_{avg} = Flow$ -weighted average of the Fr values.

 $C_{i, a, k}$  = Concentration of Table 8 and/or Table 9 compounds in wastewater stream entering the combustion unit, during run k, parts per million by weight.

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 $Q_{a,k}$  = Volumetric flow rate of wastewater entering the combustion unit during run k, cubic meters per hour.

 $Fr_i$  = Compound-specific Fr value listed in table 9 of this subpart.

(9) Calculate flow-weighted average of Fr values and compare to mass destruction efficiency. Compare the mass destruction efficiency (calculated in Equation WW 7) to the required efficiency as specified in  $\S$  63.138(e)(1), compliance is demonstrated if the mass destruction efficiency is 99 percent or greater. If complying with  $\S$  63.138(e)(2), compliance is demonstrated if the mass destruction efficiency is greater than or equal to the flow-weighted average of the Fr value calculated in Equation WW8.

(e) *Non-combustion treatment processes including closed biological treatment processes: RMR option.* This paragraph applies to performance tests for non-combustion treatment processes other than open biological treatment processes to demonstrate compliance with the mass removal provisions for Table 8 and/or Table 9 compounds. Compliance options for noncombustion treatment processes are specified in  $\S$  63.138(f) of this subpart. Compliance options for closed aerobic or anaerobic biological treatment processes are specified in  $\S$  63.138(f) and  $\S$  63.138(g) of this subpart. When complying with  $\S$  63.138(f), the owner or operator shall comply with the requirements specified in  $\S$  63.145(e)(1) through (e)(6) of this subpart. Wastewater streams that are Group 1 for both Table 8 and Table 9 compounds need only do the compliance demonstration for Table 9 compounds.)

(1) Concentration in wastewater stream. The concentration of Table 8 and/or Table 9 compounds shall be determined as provided in this paragraph. Concentration measurements to determine RMR shall be taken at the point of determination or downstream of the point of determination with adjustment for concentration change made according to  $\frac{63.144(b)(6)}{63.144(b)(6)}$  of this subpart. Concentration measurements to determine AMR shall be taken at the inlet and outlet to the treatment process and as provided in  $\frac{63.145(a)(7)}{63.145(a)(7)}$  for a series of treatment processes. Wastewater samples shall be collected using sampling procedures which minimize loss of organic compounds during sample collection and analysis and maintain sample integrity per  $\frac{63.144(b)(5)(ii)}{63.144(b)(5)(ii)}$ . The method shall be an analytical method for wastewater which has that compound as a target analyte. Samples may be grab samples or composite samples. Samples shall be taken at approximately equally spaced time intervals over a 1-hour period. Each 1-hour period constitutes a run, and the performance test shall consist of a minimum of 3 runs. Concentration measurements based on Method 305 shall be adjusted by dividing each concentration by the compound-specific Fm factor listed in table 34 of this subpart. Concentration measurements based on methods other than Method 305 shall not adjust by the compound-specific Fm factor listed in table 34 of this subpart.

(2) *Flow rate*. Flow rate measurements to determine RMR shall be taken at the point of determination or downstream of the point of determination with adjustment for flow rate change made according to  $\frac{63.144(c)(4)}{63.144(c)(4)}$  of this subpart. Flow rate measurements to determine AMR shall be taken at the inlet and outlet to the treatment process and as provided in  $\frac{63.145(a)(7)}{63.145(a)(7)}$  for a series of treatment processes. Flow rate shall be determined using inlet and outlet flow measurement devices. Where the outlet flow is not greater than the inlet flow, a flow measurement device shall be used, and may be used at either the inlet or outlet. Flow rate measurements shall be taken at the same time as the concentration measurements.

(3) Calculation of RMR for non-combustion treatment processes including closed biological treatment processes. When using  $\frac{63.138(f)}{10}$  to comply, the required mass removal of Table 8 and/or Table 9 compounds for each Group 1 wastewater stream shall be calculated as specified in <u>paragraph (e)(3)(i)</u> of this section. When using  $\frac{63.138(g)}{10}$  to comply, the required mass removal shall be calculated as specified in <u>paragraph (e)(3)(i)</u> of this section.

(i) When using  $\S$  63.138(f) to comply, the required mass removal of Table 8 and/or Table 9 compounds for each Group 1 wastewater stream shall be calculated using Equation WW9.

$$RMR = \frac{\rho}{10^9} Q \sum_{i=1}^{n} (C_i * Fr_i) \qquad (Eqn WW9)$$

Where:

RMR = Required mass removal for treatment process or series of treatment processes, kilograms per hour.

 $\rho$  = Density of the Group 1 wastewater stream, kilograms per cubic meter.

Q = Volumetric flow rate of wastewater stream at the point of determination, liters per hour.

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i = Identifier for a compound.

n = Number of Table 8 or Table 9 compounds in stream.

C<sub>i</sub> = Concentration of Table 8 or Table 9 compounds at the point of determination, parts per million by weight.

Fr<sub>i</sub> = Fraction removal value of a Table 8 or Table 9 compound. Fr values are listed in table 9 of this subpart.

 $10^9 =$  Conversion factor, mg/kg \* l/m<sup>3</sup>.

(ii) When using  $\frac{63.138(g)}{10}$  to comply, the required mass removal is 95 percent of the mass flow rate for all Group 1 and Group 2 wastewater streams combined for treatment. The required mass removal of Table 8 and/or Table 9 compounds for all Group 1 and Group 2 wastewater streams combined for treatment when complying with  $\frac{63.138(g)}{10}$  shall be calculated using the following equation:

$$RMR = \frac{0.95\rho}{10^5} Q \sum_{i=1}^{n} (C_i) \qquad (Eqn WW9a)$$

Where:

RMR = Required mass removal for treatment process or series of treatment processes, kilograms per hour.

 $\rho$  = Density of the Group 1 wastewater stream, kilograms per cubic meter.

Q = Volumetric flow rate of wastewater stream at the point of determination, liters per hour.

i = Identifier for a compound.

n = Number of Table 8 or Table 9 compounds in stream.

C<sub>i</sub> = Concentration of Table 8 or Table 9 compounds at the point of determination, parts per million by weight.

 $10^9$  = Conversion factor, mg/kg \* l/m<sup>3</sup>

(4)

(i) The required mass removal is calculated by summing the required mass removal for each Group 1 wastewater stream to be combined for treatment when complying with  $\frac{63.138(f)}{10}$ .

(ii) The required mass removal is calculated by summing the required mass removal for all Group 1 and Group 2 wastewater streams combined for treatment when complying with  $\frac{63.138(g)}{2}$ .

(5) *The AMR calculation procedure for non-combustion treatment processes including closed biological treatment processes.* The AMR shall be calculated as follows:

$$AMR = (QMW_a - QMW_b)$$
 (Eqn WW10)

Where:

AMR = Actual mass removal of Table 8 or Table 9 compounds achieved by treatment process or series of treatment processes, kilograms per hour.

 $QMW_a = Mass$  flow rate of Table 8 or Table 9 compounds in wastewater entering the treatment process or first treatment process in a series of treatment processes, kilograms per hour.

 $QMW_b = Mass$  flow rate of Table 8 or Table 9 compounds in wastewater exiting the last treatment process in a series of treatment processes, kilograms per hour.

(6) Compare RMR to AMR. When complying with § 63.138(f), compare the RMR calculated in Equation WW9 to the AMR calculated in Equation WW10. Compliance is demonstrated if the AMR is greater than or equal to the RMR. When complying with § 63.138(g), compare the RMR calculated in Equation WW-9a to the AMR calculated in Equation WW10. Compliance is demonstrated if the AMR is greater than or equal to 95-percent mass removal.

(f) Open or closed aerobic biological treatment processes: Required mass removal (RMR) option. This paragraph applies to the use of performance tests that are conducted for open or closed aerobic biological treatment processes to demonstrate compliance with the mass removal provisions for Table 8 and/or Table 9 compounds. These compliance options are specified in § 63.138(f) of this subpart. The owner or operator shall comply with the requirements specified in § 63.145(f)(1) through (f)(6) of this subpart. Some compounds may not require a performance test. Refer to § 63.145(h) and table 36 of this subpart to determine which compounds may be exempt from the requirements of this paragraph.

(1) Concentration in wastewater stream. The concentration of Table 8 and/or Table 9 compounds shall be determined as provided in this paragraph. Concentration measurements to determine RMR shall be taken at the point of determination or downstream of the point of determination with adjustment for concentration change made according to  $\frac{63.144(b)(6)}{60}$  of this subpart. Concentration measurements to determine AMR shall be taken at the inlet and outlet to the treatment process and as provided in  $\frac{63.144(b)(5)}{60}$  for a series of treatment processes. Wastewater samples shall be collected using sampling procedures which minimize loss of organic compounds during sample collection and analysis and maintain sample integrity per  $\frac{63.144(b)(5)(ii)}{60}$ . The method shall be an analytical method for wastewater which has that compound as a target analyte. Samples may be grab samples or composite samples. Samples shall be taken at approximately equally spaced time intervals over a 1-hour period. Each 1-hour period constitutes a run, and the performance test shall consist of a minimum of 3 runs. Concentration measurements based on Method 305 shall be adjusted by dividing each concentration by the compound-specific Fm factor listed in table 34 of this subpart. Concentration measurements based on methods other than Method 305 shall not adjust by the compound-specific Fm factor listed in table 34 of this subpart.

(2) *Flow rate*. Flow rate measurements to determine RMR shall be taken at the point of determination or downstream of the point of determination with adjustment for flow rate change made according to  $\frac{63.144(c)(4)}{63.144(c)(4)}$  of this subpart. Flow rate measurements to determine AMR shall be taken at the inlet and outlet to the treatment process and as provided in  $\frac{63.145(a)(7)}{63.145(a)(7)}$  for a series of treatment processes. Flow rate shall be determined using inlet and outlet flow measurement devices. Where the outlet flow is not greater than the inlet flow, a flow measurement device shall be used, and may be used at either the inlet or outlet. Flow rate measurements shall be taken at the same time as the concentration measurements.

(3) *Calculation of RMR for open or closed aerobic biological treatment processes.* The required mass removal of Table 8 and/or Table 9 compounds for each Group 1 wastewater stream shall be calculated using the following equation:

RMR = 
$$\frac{\rho}{10^9} Q \sum_{i=1}^{n} (C_i * Fr_i)$$
 (Eqn WW11)

Where:

RMR = Required mass removal for treatment process or series of treatment processes, kilograms per hour.

 $\rho$  = Density of the Group 1 wastewater stream, kilograms per cubic meter.

Q = Volumetric flow rate of wastewater stream at the point of determination, liters per hour.

i = Identifier for a compound.

n = Number of Table 8 or Table 9 compounds in stream.

C<sub>i</sub> = Concentration of Table 8 or Table 9 compounds at the point of determination, parts per million by weight.

 $Fr_i = Fraction removal value of a Table 8 or Table 9 compound. Fr values are listed in table 9 of this subpart.$ 

 $10^9 =$  Conversion factor, mg/kg \* l/m<sup>3</sup>.

(4) The required mass removal is calculated by adding together the required mass removal for each Group 1 wastewater stream to be combined for treatment.

(5) Actual mass removal calculation procedure for open or closed aerobic biological treatment processes. The actual mass removal (AMR) shall be calculated using Equation WW12 as specified in paragraph (f)(5)(i) of this section when the performance test is performed across the open or closed aerobic biological treatment process only. If compliance is being demonstrated in accordance with § 63.145(a)(7)(i), the AMR for the series shall be calculated using Equation WW13 in § 63.145(f)(5)(ii). (This equation is for situations where treatment is performed in a series of treatment processes connected by

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hard-piping.) If compliance is being demonstrated in accordance with § 63.145(a)(7)(ii), the AMR for the biological treatment process shall be calculated using Equation WW12 in § 63.145(f)(5)(i). The AMR for the biological treatment process used in a series of treatment processes calculated using Equation WW12 shall be added to the AMR determined for each of the other individual treatment processes in the series of treatment processes.

(i) Calculate AMR for the open or closed aerobic biological treatment process as follows:

$$AMR = QMW_a * F_{bio}$$
 (Eqn WW12)

Where:

AMR = Actual mass removal of Table 8 or Table 9 compounds achieved by open or closed biological treatment process, kilograms per hour.

QMW<sub>a</sub> = Mass flow rate of Table 8 or Table 9 compounds in wastewater entering the treatment process, kilograms per hour.

 $F_{bio}$  = Site-specific fraction of Table 8 or Table 9 compounds biodegraded.  $F_{bio}$  shall be determined as specified in § 63.145(h) and appendix C of this subpart.

(ii) Calculate AMR across a series of treatment units where the last treatment unit is an open or closed aerobic biological treatment process as follows:

$$AMR = QMW_{a} - (QMW_{b})(1 - F_{bio}) \qquad (Eqn WW13)$$

Where:

AMR = Actual mass removal of Table 8 or Table 9 compounds achieved by a series of treatment processes, kilograms per hour.

 $QMW_a = Mass$  flow rate of Table 8 or Table 9 compounds in wastewater entering the first treatment process in a series of treatment processes, kilograms per hour.

 $QMW_b = Mass$  flow rate of Table 8 or Table 9 compounds in wastewater exiting the last treatment process in a series of treatment processes prior to the biological treatment process, kilograms per hour.

 $F_{bio}$  = Site-specific fraction of Table 8 or Table 9 compounds biodegraded.  $F_{bio}$  shall be determined as specified in <u>§</u> <u>63.145(h)</u> and appendix C of this subpart.

(6) *Compare RMR to AMR*. Compare the RMR calculated in Equation WW11 to the AMR calculated in either Equation WW12 or WW13, as applicable. Compliance is demonstrated if the AMR is greater than or equal to the RMR.

(g) Open or closed aerobic biological treatment processes: 95-percent mass removal option. This paragraph applies to performance tests that are conducted for open or closed aerobic biological treatment processes to demonstrate compliance with the 95-percent mass removal provisions for Table 8 and/or Table 9 compounds. This compliance option is specified in § 63.138(g) of this subpart. The RMR for this option is 95-percent mass removal. The owner or operator shall comply with the requirements specified in § 63.145(g)(1) to determine AMR, § 63.145(e)(3)(ii) and (e)(4)(ii) to determine RMR, and (g)(2) of this subpart to determine whether compliance has been demonstrated. Some compounds may not require a performance test. Refer to § 63.145(h) and table 36 of this subpart to determine which compounds may be exempt from the requirements of this paragraph. (Wastewater streams that are Group 1 for both Table 8 and Table 9 compounds need only do the compliance demonstration for Table 9 compounds.)

(1) The owner or operator shall comply with the requirements specified in <u>paragraphs (f)(1)</u>, (f)(2), and (f)(5) of this section to determine AMR. References to Group 1 wastewater streams shall be deemed Group 1 and Group 2 wastewater streams for the purposes of this paragraph.

(2) Compare RMR to AMR. Compliance is demonstrated if the AMR is greater than or equal to RMR.

(h) *Site-specific fraction biodegraded* ( $F_{bio}$ ). The compounds listed in table 9 of this subpart are divided into two sets for the purpose of determining whether  $F_{bio}$  must be determined, and if  $F_{bio}$  must be determined, which procedures may be used to determine compound-specific kinetic parameters. These sets are designated as lists 1 and 2 in table 36 of this subpart.

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(1) *Performance test exemption*. If a biological treatment process meets the requirements specified in <u>paragraphs</u> (h)(1)(i) and (h)(1)(ii) of this section, the owner or operator is not required to determine  $F_{bio}$  and is exempt from the applicable performance test requirements specified in § 63.138 of this subpart.

(i) The biological treatment process meets the definition of "enhanced biological treatment process" in § 63.111 of this subpart.

(ii) At least 99 percent by weight of all compounds on table 36 of this subpart that are present in the aggregate of all wastewater streams using the biological treatment process to comply with <u>§ 63.138 of this subpart</u> are compounds on list 1 of table 36 of this subpart.

(2)  $F_{bio}$  determination. If a biological treatment process does not meet the requirement specified in <u>paragraph (h)(1)(i)</u> of this section, the owner or operator shall determine  $F_{bio}$  for the biological treatment process using the procedures in appendix C to part 63, and <u>paragraph (h)(2)(ii)</u> of this section. If a biological treatment process meets the requirements of <u>paragraph (h)(1)(i)</u> of this section but does not meet the requirement specified in <u>paragraph (h)(1)(ii)</u> of this section, the owner or operator shall determine  $F_{bio}$  for the biological treatment process using the procedures in appendix C to part of a paragraph (h)(1)(i) of this section, the owner or operator shall determine  $F_{bio}$  for the biological treatment process using the procedures in appendix C to part 63, and <u>paragraph (h)(2)(i)</u> of this section.

(i) Enhanced biological treatment processes. If the biological treatment process meets the definition of "enhanced biological treatment process" in § 63.111 of this subpart and the wastewater streams include one or more compounds on list 2 of table 36 of this subpart that do not meet the criteria in paragraph (h)(1)(ii) of this section, the owner or operator shall determine  $f_{bio}$  for the list 2 compounds using any of the procedures specified in appendix C of 40 CFR part 63. (The symbol " $f_{bio}$ " represents the site specific fraction of an individual Table 8 or Table 9 compound that is biodegraded.) The owner or operator shall calculate  $f_{bio}$  for the list 1 compounds using the defaults for first order biodegradation rate constants (K<sub>1</sub>) in table 37 of subpart G and follow the procedure explained in form III of appendix C, <u>40 CFR part 63</u>, or any of the procedures specified in appendix C, <u>40 CFR part 63</u>.

(ii) *Biological treatment processes that are not enhanced biological treatment processes.* For biological treatment processes that do not meet the definition for "enhanced biological treatment process" in § 63.111 of this subpart, the owner or operator shall determine the  $f_{bio}$  for the list 1 and 2 compounds using any of the procedures in appendix C to part 63, except procedure 3 (inlet and outlet concentration measurements). (The symbol " $f_{bio}$ " represents the site specific fraction of an individual Table 8 or Table 9 compound that is biodegraded.)

(i) *Performance tests for control devices other than flares.* This paragraph applies to performance tests that are conducted to demonstrate compliance of a control device with the efficiency limits specified in § 63.139(c). If complying with the 95-percent reduction efficiency requirement, comply with the requirements specified in paragraphs (i)(1) through (i)(9) of this section. If complying with the 20 ppm by volume requirement, comply with the requirements specified in paragraphs (i)(1) through (6) and (9) of this section. The 20 ppm by volume limit or 95-percent reduction efficiency requirement shall be measured as either total organic hazardous air pollutants or as TOC minus methane and ethane. Performance tests must be conducted according to the schedule in § 63.103(b)(1) of subpart F of this part.

(1) *Sampling sites.* Sampling sites shall be selected using Method 1 or 1A of <u>40 CFR part 60, appendix A</u>, as appropriate. For determination of compliance with the 95 percent reduction requirement, sampling sites shall be located at the inlet and the outlet of the control device. For determination of compliance with the 20 parts per million by volume limit, the sampling site shall be located at the outlet of the control device.

(2) Concentration in gas stream entering or exiting the control device. The concentration of total organic hazardous air pollutants or TOC in a gas stream shall be determined as provided in this paragraph. Samples may be grab samples or composite samples (*i.e.*, integrated samples). Samples shall be taken at approximately equally spaced time intervals over a 1-hour period. Each 1-hour period constitutes a run, and the performance test shall consist of a minimum of 3 runs. Concentration measurements shall be determined using Method 18 of appendix A-6 to 40 CFR part 60. ASTM D6420-18 (incorporated by reference, see § 63.14) may also be used in lieu of Method 18, if the target compounds are all known and are all listed in Section 1.1 of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method. Alternatively, any other test method validated according to the procedures in Method 301 of appendix A to this part may be used.

(3) *Volumetric flow rate of gas stream entering or exiting the control device.* The volumetric flow rate of the gas stream shall be determined using Method 2, 2A, 2C, or 2D of <u>40 CFR part 60, appendix A</u>, as appropriate. Volumetric flow rate measurements shall be taken at the same time as the concentration measurements.

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(4) *Calculation of TOC concentration*. The TOC concentration (CG<sub>T</sub>) is the sum of the concentrations of the individual components. If compliance is being determined based on TOC, the owner or operator shall compute TOC for each run using the following equation:

$$CG_T = \frac{1}{m} \sum_{j=1}^{m} \left( \sum_{i=1}^{n} CGS_{i,j} \right)$$
 (Eqn WW14)

Where:

 $CG_T$  = Total concentration of TOC (minus methane and ethane) in vented gas stream, average of samples, dry basis, parts per million by volume.

CGS<sup>ij</sup> = Concentration of sample components in vented gas stream for sample j, dry basis, parts per million by volume.

i = Identifier for a compound.

n = Number of components in the sample.

j = Identifier for a sample.

m = Number of samples in the sample run.

(5) Calculation of total organic hazardous air pollutants concentration. The owner or operator determining compliance based on total organic hazardous air pollutants concentration ( $C_{HAP}$ ) shall compute  $C_{HAP}$  according to the Equation WW14, except that only Table 9 compounds shall be summed.

(6) Percent oxygen correction for combustion control devices. If the control device is a combustion device, comply with the requirements specified in paragraph (i)(6)(i) of this section to determine oxygen concentration, and in paragraph (i)(6)(ii) of this section to calculate the percent oxygen correction.

(i) Oxygen concentration. The concentration of TOC or total organic hazardous air pollutants shall be corrected to 3 percent oxygen if the control device is a combustion device. Method 3A of appendix A-2 to 40 CFR part 60 or the manual method in ANSI/ASME PTC 19.10-1981 (incorporated by reference, see § 63.14) shall be used to determine the actual oxygen concentration (%02d). The samples shall be taken during the same time that the TOC (minus methane or ethane) or total organic hazardous air pollutants samples are taken.

(ii) *3 percent oxygen calculation*. The concentration corrected to 3 percent oxygen (CG<sub>c</sub>), when required, shall be computed using the following equation:

$$CG_{C} = CG_{T} \left( \frac{17.9}{20.9 - \%0_{2d}} \right)$$
 (Eqn WW15)

Where:

 $CG_c$  = Concentration of TOC or organic hazardous air pollutants corrected to 3 percent oxygen, dry basis, parts per million by volume.

 $CG_T$  = Total concentration of TOC (minus methane and ethane) in vented gas stream, average of samples, dry basis, parts per million by volume.

 $\%0_{2d}$  = Concentration of oxygen measured in vented gas stream, dry basis, percent by volume.

(7) *Mass rate calculation*. The mass rate of either TOC (minus methane and ethane) or total organic hazardous air pollutants shall be calculated using the following equations. Where the mass rate of TOC is being calculated, all organic compounds (minus methane and ethane) measured by methods specified in <u>paragraph (i)(2)</u> of this section are summed using Equations WW16 and WW17. Where the mass rate of total organic hazardous air pollutants is being calculated, only Table 9 compounds shall be summed using Equations WW16 and WW17.

$$QMG_{a} = K_{2} \left( \sum_{i=1}^{n} CG_{a,i} MW_{i} \right) QG_{a} \qquad (Eqn WW16)$$
$$QMG_{b} = K_{2} \left( \sum_{i=1}^{n} CG_{b,i} MW_{i} \right) QG_{b} \qquad (Eqn WW17)$$

Where:

 $CG_{a, i}$ ,  $CG_{b, i}$  = Concentration of TOC (minus methane and ethane) or total organic hazardous air pollutants, in vented gas stream, entering ( $CG_{a, i}$ ) and exiting ( $CG_{b, i}$ ) the control device, dry basis, parts per million by volume.

 $QMG_a$ ,  $QMG_b$  = Mass rate of TOC (minus methane and ethane) or total organic hazardous air pollutants, in vented gas stream, entering ( $QMG_a$ ) and exiting ( $QMG_b$ ) the control device, dry basis, kilograms per hour.

MW<sub>i</sub> = Molecular weight of a component, kilogram/kilogram-mole.

 $QG_a$ ,  $QG_b$  = Flow rate of gas stream entering ( $QG_a$ ) and exiting ( $QG_b$ ) the control device, dry standard cubic meters per hour.

 $K_2 = Constant$ ,  $41.57 \times 10^{-9}$  (parts per million)<sup>-1</sup> (gram-mole per standard cubic meter) (kilogram/gram), where standard temperature (gram-mole per standard cubic meter) is 20 °Celsius.

i = Identifier for a compound.

n = Number of components in the sample.

(8) *Percent reduction calculation*. The percent reduction in TOC (minus methane and ethane) or total organic hazardous air pollutants shall be calculated as follows:

$$E = \frac{QMG_a - QMG_b}{QMG_a} (100\%) \qquad (Eqn WW18)$$

Where:

E = Destruction efficiency of control device, percent.

 $QMG_a$ ,  $QMG_b = Mass$  rate of TOC (minus methane and ethane) or total organic hazardous air pollutants, in vented gas stream entering and exiting ( $QMG_b$ ) the control device, dry basis, kilograms per hour.

(9) Compare mass destruction efficiency to required efficiency. If complying with the 95 percent reduction efficiency requirement, compliance is demonstrated if the mass destruction efficiency (calculated in Equation WW18) is 95 percent or greater. If complying with the 20 parts per million by volume limit in  $\S$  63.139 (c)(1)(ii) of this subpart, compliance is demonstrated if the outlet total organic compound concentration, less methane and ethane, or total organic hazardous air pollutants concentration is 20 parts per million by volume, or less. For combustion control devices, the concentration shall be calculated on a dry basis, corrected to 3 percent oxygen.

(j) Except as specified in <u>paragraph (a) of § 63.108</u>, when a flare is used to comply with <u>§ 63.139(c)</u>, the owner or operator shall comply with <u>paragraphs (j)(1)</u> through (<u>3</u>) of this section. The owner or operator is not required to conduct a performance test to determine percent emission reduction or outlet organic HAP or TOC concentration.

(1) Conduct a visible emission test using the techniques specified in  $\frac{63.11(b)(4)}{2}$ .

(2) Determine the net heating value of the gas being combusted using the techniques specified in  $\frac{63.11(b)(6)}{6}$ .

(3) Determine the exit velocity using the techniques specified in either  $\S 63.11(b)(7)(i)$  (and  $\S 63.11(b)(7)(iii)$ , where applicable) or  $\S 63.11(b)(8)$ , as appropriate.

[<u>62 FR 2765</u>, Jan. 17, 1997, as amended at <u>63 FR 67793</u>, Dec. 9, 1998; <u>64 FR 20192</u>, Apr. 26, 1999; <u>66 FR 6933</u>, Jan. 22, 2001; <u>89 FR 43205</u>, May 16, 2024]

# § 63.146 Process wastewater provisions—reporting.

(a) For each waste management unit, treatment process, or control device used to comply with <u>§§ 63.138</u> (b)(1), (c)(1), (d), (e), (f), or (g) of this subpart for which the owner or operator seeks to monitor a parameter other than those specified in table 11, table 12, or table 13 of this subpart, the owner or operator shall submit a request for approval to monitor alternative parameters according to the procedures specified in <u>§ 63.151(f)</u> or (g) of this subpart.

(b) The owner or operator shall submit the information specified in <u>paragraphs (b)(1)</u> through <u>(b)(9)</u> of this section as part of the Notification of Compliance Status required by  $\frac{\$ 63.152(b)}{\$ 63.152(b)}$  of this subpart.

(1) Requirements for Group 2 wastewater streams. This paragraph does not apply to Group 2 wastewater streams that are used to comply with  $\S$  63.138(g). For Group 2 wastewater streams, the owner or operator shall include the information specified in paragraphs (b)(1)(i) through (iv) of this section in the Notification of Compliance Status Report. This information may be submitted in any form. Table 15 of this subpart is an example.

(i) Process unit identification and description of the process unit.

(ii) Stream identification code.

(iii) For existing sources, concentration of table 9 compound(s) in parts per million, by weight. For new sources, concentration of table 8 and/or table 9 compound(s) in parts per million, by weight. Include documentation of the methodology used to determine concentration.

(iv) Flow rate in liter per minute.

(2) For each new and existing source, the owner or operator shall submit the information specified in table 15 of this subpart for Table 8 and/or Table 9 compounds.

(3) [Reserved]

(4) For each treatment process identified in table 15 of this subpart that receives, manages, or treats a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream, the owner or operator shall submit the information specified in table 17 of this subpart.

(5) For each waste management unit identified in table 15 of this subpart that receives or manages a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream, the owner or operator shall submit the information specified in table 18 of this subpart.

(6) For each residual removed from a Group 1 wastewater stream, the owner or operator shall report the information specified in table 19 of this subpart.

(7) For each control device used to comply with  $\underline{\$\$} \underline{\$\$} \underline{\$3.133}$  through  $\underline{63.139}$  of this subpart, the owner or operator shall report the information specified in paragraphs (b)(7)(i) and (b)(7)(ii) of this section.

(i) Except as specified in <u>paragraph (a) of § 63.108</u>, for each flare, the owner or operator shall submit the information specified in <u>paragraphs (b)(7)(i)(A)</u> through  $(\underline{b})(7)(i)(C)$  of this section.

(A) Flare design (i.e., steam-assisted, air-assisted, or non-assisted);

(B) All visible emission readings, heat content determinations, flow rate measurements, and exit velocity determinations made during the compliance determination required by  $\frac{63.139(c)(3)}{5.000}$  of this subpart; and

(C) Reports of the times and durations of all periods during the compliance determination when the pilot flame is absent or the monitor is not operating.

(ii) For each control device other than a flare, the owner or operator shall submit the information specified in <u>paragraph</u> (b)(7)(ii)(A) of this section and in either <u>paragraph (b)(7)(ii)(B)</u> or (b)(7)(ii)(C) of this section.

(A) The information on parameter ranges specified in  $\S$  63.152(b)(2) of this subpart for the applicable parameters specified in table 13 of this subpart, unless the parameter range has already been established in the operating permit; and either

(B) The design evaluation specified in  $\S 63.139(d)(2)$  of this subpart; or

(C) Results of the performance test specified in  $\S 63.139(d)(1)$  of this subpart. Performance test results shall include operating ranges of key process and control parameters during the performance test; the value of each parameter being monitored in accordance with  $\S 63.143$  of this subpart; and applicable supporting calculations. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with  $\S 63.152(h)$ , the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the notification of compliance status report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(8) For each treatment process used to comply with  $\S$  63.138(b)(1), (c)(1), (d), (e), (f), or (g) of this subpart, the owner or operator shall submit the information specified in paragraphs (b)(8)(i) and (b)(8)(ii) of this section.

(i) For Items 1 and 2 in table 12 of this subpart, the owner or operator shall submit the information specified in <u>paragraphs</u> (b)(8)(i)(A) and (b)(8)(i)(B) of this section. An owner or operator using the design steam stripper compliance option specified § 63.138(d) of this subpart does not have to submit the information specified in <u>paragraph</u> (b)(8)(i)(A) or (b)(8)(i)(B) of this section. However, the monitoring requirements specified in Item 2 of table 12 of this subpart still apply.

(A) The information on parameter ranges specified in  $\S$  63.152(b)(2) of this subpart for the parameters approved by the Administrator, unless the parameter range has already been established in the operating permit.

(B) Results of the initial measurements of the parameters approved by the Administrator and any applicable supporting calculations.

(ii) For Item 3 in table 12 of this subpart, the owner or operator shall submit the information on parameter ranges specified in  $\frac{63.152(b)(2)}{5}$  of this subpart for the parameters specified in Item 3 of table 12 of this subpart, unless the parameter range has already been established in the operating permit.

(9) For each waste management unit or treatment process used to comply with  $\S$  63.138(b)(1), (c)(1), (e), (f), or (g), the owner or operator shall submit the information specified in either paragraph (b)(9)(i) or (ii) of this section.

(i) The design evaluation and supporting documentation specified in  $\S 63.138(j)(1)$  of this subpart.

(ii) Results of the performance test specified in  $\S 63.138(j)(2)$  of this subpart. Performance test results shall include operating ranges of key process and control parameters during the performance test; the value of each parameter being monitored in accordance with  $\S 63.143$  of this subpart; and applicable supporting calculations. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with  $\S 63.152(h)$ , the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the notification of compliance status report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(c) For each waste management unit that receives, manages, or treats a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream, the owner or operator shall submit as part of the next Periodic Report required by  $\S 63.152(c)$  of this subpart the results of each inspection required by  $\S 63.143(a)$  of this subpart in which a control equipment failure was identified. Control equipment failure is defined for each waste management unit in \$ 63.133 through 63.137 of this subpart. Each Periodic Report shall include the date of the inspection, identification of each waste management unit in which a control equipment failure was detected, description of the failure, and description of the nature of and date the repair was made.

(d) Except as provided in paragraph (f) of this section, for each treatment process used to comply with  $\S$  <u>63.138(b)(1)</u>, (c)(1), (d), (e), (f), or (g), the owner or operator shall submit as part of the next Periodic Report required by  $\S$  <u>63.152(c)</u> the information specified in paragraphs (d)(1), (2), and (3) of this section for the monitoring required by  $\S$  <u>63.143(b)</u>, (c), and (d).

(1) For Item 1 in table 12, the owner or operator shall submit the results of measurements that indicate that the biological treatment unit is outside the range established in the Notification of Compliance Status or operating permit. Include the identification of the biological treatment unit, the parameter that was out of range and the date that the parameter is out of range.

(2) For Item 2 in table 12, the owner or operator shall submit the monitoring results for each operating day during which the daily average value of a continuously monitored parameter is outside the range established in the Notification of Compliance

Status or operating permit. Include the identification of the treatment process, the parameter that was out of range, and the date the parameter was out of range.

(3) For Item 3 in table 12 of this subpart, the owner or operator shall submit the monitoring results for each operating day during which the daily average value of any monitored parameter approved in accordance with  $\frac{63.151 (f)}{10}$  was outside the range established in the Notification of Compliance Status or operating permit. Include the identification of the treatment process, the parameter that was out of range, and the date the parameter was out of range.

(e) Except as provided in <u>paragraph (f)</u> of this section, for each control device used to comply with <u>§§ 63.133</u> through <u>63.139</u>, the owner or operator shall submit as part of the next Periodic Report required by <u>§ 63.152(c)</u> the information specified in either <u>paragraph (e)(1)</u> or <u>(e)(2)</u> of this section.

(1) The information specified in table 20 of this subpart, including the date of each occurrence, or

(2) If the owner or operator elects to comply with  $\S 63.143(e)(2)$  of this subpart, *i.e.*, an organic monitoring device installed at the outlet of the control device, the owner or operator shall submit the date and the monitoring results for each operating day during which the daily average concentration level or reading is outside the range established in the Notification of Compliance Status or operating permit.

(f) Where the owner or operator obtains approval to use a treatment process or control device other than one for which monitoring requirements are specified in § 63.143 of this subpart, or to monitor parameters other than those specified in table 12 or 13 of this subpart, the Administrator will specify appropriate reporting requirements.

(g) If an extension is utilized in accordance with  $\S$  63.133(e)(2) or  $\S$  63.133(h) of this subpart, the owner or operator shall include in the next periodic report the information specified in  $\S$  63.133 (e)(2) or  $\S$  63.133(h).

[<u>62 FR 2774</u>, Jan. 17, 1997, as amended at <u>64 FR 20192</u>, Apr. 26, 1999; <u>66 FR 6933</u>, Jan. 22, 2001; <u>89 FR 43206</u>, May 16, 2024]

# § 63.147 Process wastewater provisions—recordkeeping.

(a) The owner or operator transferring a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream in accordance with  $\frac{63.132(g)}{63.132(g)}$  of this subpart shall keep a record of the notice sent to the treatment operator stating that the wastewater stream or residual contains organic hazardous air pollutants which are required to be managed and treated in accordance with the provisions of this subpart.

(b) The owner or operator shall keep in a readily accessible location the records specified in paragraphs (b)(1) through (8) of the section.

(1) A record that each waste management unit inspection required by  $\frac{\$\$ 63.133}{\$}$  through  $\frac{63.137}{\$}$  of this subpart was performed.

(2) A record that each inspection for control devices required by § 63.139 of this subpart was performed.

(3) A record of the results of each seal gap measurement required by  $\underline{\$\$ 63.133(d)}$  and  $\underline{63.137(c)}$  of this subpart. The records shall include the date of the measurement, the raw data obtained in the measurement, and the calculations described in  $\underline{\$} \underline{63.120(b)(2)}$ , (3), and (4) of this subpart.

(4) For Item 1 and Item 3 of table 12 of this subpart, the owner or operator shall keep the records approved by the Administrator.

(5) Except as provided in paragraph (e) of this section, continuous records of the monitored parameters specified in Item 2 of table 12 and table 13 of this subpart, and in  $\S 63.143(e)(2)$  of this subpart.

(6) Documentation of a decision to use an extension, as specified in  $\S$  63.133(e)(2) or (h) of this subpart, which shall include a description of the failure, documentation that alternate storage capacity is unavailable, and specification of a schedule of actions that will ensure that the control equipment will be repaired or the vessel will be emptied as soon as practical.

(7) Documentation of a decision to use a delay of repair due to unavailability of parts, as specified in  $\S$  63.140(c), shall include a description of the failure, the reason additional time was necessary (including a statement of why replacement parts were not kept on site and when the manufacturer promised delivery), and the date when repair was completed.
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(8) Requirements for Group 2 wastewater streams. This paragraph (b)(8) does not apply to Group 2 wastewater streams that are used to comply with  $\S$  63.138(g). For all other Group 2 wastewater streams, the owner or operator shall keep in a readily accessible location the records specified in paragraphs (b)(8)(i) through (iv) of this section.

(i) Process unit identification and description of the process unit.

(ii) Stream identification code.

(iii) For existing sources, concentration of table 9 compound(s) in parts per million, by weight. For new sources, concentration of table 8 and/or table 9 compound(s) in parts per million, by weight. Include documentation of the methodology used to determine concentration.

(iv) Flow rate in liter per minute.

(c) For each boiler or process heater used to comply with  $\frac{\$\$ 63.133}{\$\$ 63.133}$  through  $\frac{63.139}{\$\$ 63.139}$  of this subpart, the owner or operator shall keep a record of any changes in the location at which the vent stream is introduced into the flame zone as required in  $\frac{\$}{\$}$   $\frac{63.139(c)(1)}{\$}$  of this subpart.

(d) The owner or operator shall keep records of the daily average value of each continuously monitored parameter for each operating day as specified in  $\frac{63.152(f)}{10}$ , except as provided in paragraphs (d)(1) through (4) of this section.

(1) For flares, except as specified in <u>paragraph (a) of § 63.108</u>, records of the times and duration of all periods during which the pilot flame is absent shall be kept rather than daily averages.

(2) Regenerative carbon adsorbers. Except as specified in paragraph (d)(4) of this section, for regenerative carbon adsorbers, the owner or operator shall keep the records specified in paragraphs (d)(2)(i) and (ii) of this section instead of daily averages.

(i) Records of the total regeneration stream mass flow for each carbon bed regeneration cycle.

(ii) Records of the temperature of the carbon bed after each regeneration cycle.

(3) Non-regenerative carbon adsorbers. Except as specified in paragraph (d)(4) of this section, for non-regenerative carbon adsorbers using organic monitoring equipment, the owner or operator shall keep the records specified in paragraph (d)(3)(i) of this section instead of daily averages. For non-regenerative carbon adsorbers replacing the carbon adsorption system with fresh carbon at a regular predetermined time interval that is less than the carbon replacement interval that is determined by the maximum design flow rate and organic concentration in the gas stream vented to the carbon adsorption system, the owner or operator shall keep the records specified in paragraph (d)(3)(ii) of this section instead of daily averages.

(i)

(A) Record of how the monitoring frequency, as specified in table 13 of this subpart, was determined.

(B) Records of when organic compound concentration of adsorber exhaust was monitored.

(C) Records of when the carbon was replaced.

(ii)

(A) Record of how the carbon replacement interval, as specified in table 13 of this subpart, was determined.

(B) Records of when the carbon was replaced.

(4) For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in  $\S$  <u>63.139(d)(5)</u>, the owner or operator must keep the applicable records specified in (d)(4)(i) through (d)(4)(iii) of this section.

(i) Breakthrough limit and bed life established according to  $\frac{63.139(d)(5)(i)}{5}$ .

(ii) Each outlet HAP or TOC concentration measured according to  $\frac{\$\$ 63.139(d)(5)(ii)}{\$}$  and  $\frac{(d)(5)(iii)}{\$}$ .

(iii) Date and time you last replaced the adsorbent.

(e) Where the owner or operator obtains approval to use a control device other than one for which monitoring requirements are specified in  $\S$  63.143 of this subpart, or to monitor parameters other than those specified in table 12 or table 13 of this subpart, the Administrator will specify appropriate recordkeeping requirements.

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(f) If the owner or operator uses process knowledge to determine the annual average concentration of a wastewater stream as specified in § 63.144(b)(3) of this subpart and/or uses process knowledge to determine the annual average flow rate as specified in § 63.144(c)(1) of this subpart, and determines that the wastewater stream is not a Group 1 wastewater stream, the owner or operator shall keep in a readily accessible location the documentation of how process knowledge was used to determine the annual average concentration and/or the annual average flow rate of the wastewater stream.

[<u>62 FR 2775</u>, Jan. 17, 1997, as amended at <u>64 FR 20192</u>, Apr. 26, 1999; <u>66 FR 6933</u>, Jan. 22, 2001; <u>89 FR 43206</u>, May 16, 2024]

# § 63.148 Leak inspection provisions.

(a) Except as provided in <u>paragraph (k)</u> of this section, for each vapor collection system, closed vent system, fixed roof, cover, or enclosure required to comply with this section, the owner or operator shall comply with the requirements of <u>paragraphs (b)</u> through (j) of this section.

(b) Except as provided in <u>paragraphs (g)</u> and (h) of this section, each vapor collection system and closed vent system shall be inspected according to the procedures and schedule specified in <u>paragraphs (b)(1)</u> and (b)(2) of this section and each fixed roof, cover, and enclosure shall be inspected according to the procedures and schedule specified in <u>paragraph (b)(3)</u> of this section.

(1) If the vapor collection system or closed vent system is constructed of hard-piping, the owner or operator shall:

(i) Conduct an initial inspection according to the procedures in paragraph (c) of this section, and

(ii) Conduct annual visual inspections for visible, audible, or olfactory indications of leaks.

(2) If the vapor collection system or closed vent system is constructed of ductwork, the owner or operator shall:

(i) Conduct an initial inspection according to the procedures in paragraph (c) of this section, and

(ii) Conduct annual inspections according to the procedures in paragraph (c) of this section.

(iii) Conduct annual visual inspections for visible, audible, or olfactory indications of leaks.

(3) For each fixed roof, cover, and enclosure, the owner or operator shall conduct initial visual inspections and semi-annual visual inspections for visible, audible, or olfactory indications of leaks as specified in <u> $\S$ </u> 63.133 through 63.137 of this subpart.

(c) Each vapor collection system and closed vent system shall be inspected according to the procedures specified in paragraphs (c)(1) through (c)(5) of this section.

(1) Inspections shall be conducted in accordance with Method 21 of <u>40 CFR part 60, appendix A</u>.

(2)

(ii) If no instrument is available at the plant site that will meet the performance criteria specified in <u>paragraph (c)(2)(i)</u> of this section, the instrument readings may be adjusted by multiplying by the average response factor of the process fluid, calculated on an inert-free basis as described in <u>paragraph (c)(2)(i)</u> of this section.

(3) The detection instrument shall be calibrated before use on each day of its use by the procedures specified in Method 21 of <u>40 CFR part 60</u>, appendix <u>A</u>.

(4) Calibration gases shall be as follows:

(i) Zero air (less than 10 parts per million hydrocarbon in air); and

(ii) Mixtures of methane in air at a concentration less than 10,000 parts per million. A calibration gas other than methane in air may be used if the instrument does not respond to methane or if the instrument does not meet the performance criteria

specified in <u>paragraph (c)(2)(i)</u> of this section. In such cases, the calibration gas may be a mixture of one or more of the compounds to be measured in air.

(5) An owner or operator may elect to adjust or not adjust instrument readings for background. If an owner or operator elects to not adjust readings for background, all such instrument readings shall be compared directly to the applicable leak definition to determine whether there is a leak. If an owner or operator elects to adjust instrument readings for background, the owner or operator shall measure background concentration using the procedures in \$ 63.180(b) and (c) of subpart H of this part. The owner or operator shall subtract background reading from the maximum concentration indicated by the instrument.

(6) The arithmetic difference between the maximum concentration indicated by the instrument and the background level shall be compared with 500 parts per million for determining compliance.

(d) Leaks, as indicated by an instrument reading greater than 500 parts per million above background or by visual inspections, shall be repaired as soon as practicable, except as provided in <u>paragraph (e)</u> of this section.

(1) A first attempt at repair shall be made no later than 5 calendar days after the leak is detected.

(2) Repair shall be completed no later than 15 calendar days after the leak is detected, except as provided in <u>paragraph</u>  $(\underline{d})(\underline{3})$  of this section.

(3) For leaks found in vapor collection systems used for transfer operations, repairs shall be completed no later than 15 calendar days after the leak is detected or at the beginning of the next transfer loading operation, whichever is later.

(e) Delay of repair of a vapor collection system, closed vent system, fixed roof, cover, or enclosure for which leaks have been detected is allowed if the repair is technically infeasible without a shutdown, as defined in  $\S$  63.101 of subpart F of this part, or if the owner or operator determines that emissions resulting from immediate repair would be greater than the fugitive emissions likely to result from delay of repair. Repair of such equipment shall be complete by the end of the next shutdown.

(f) For each vapor collection system or closed vent system that contains bypass lines that could divert a vent stream away from the control device and to the atmosphere, the owner or operator shall comply with the provisions of either <u>paragraph</u> (f)(1) or (f)(2), and (f)(4) of this section, except as provided in <u>paragraph (f)(3)</u> of this section.

(1) Install, calibrate, maintain, and operate a flow indicator that determines whether vent stream flow is present at least once every 15 minutes. Records shall be generated as specified in  $\S$  63.118(a)(3) of this subpart. The flow indicator shall be installed at the entrance to any bypass line; or

(2) Secure the bypass line valve in the closed position with a car-seal or a lock-and-key type configuration. A visual inspection of the seal or closure mechanism shall be performed at least once every month to ensure the valve is maintained in the closed position and the vent stream is not diverted through the bypass line.

(3) Except as specified in paragraph (f)(4) of this section, equipment such as low leg drains, high point bleeds, analyzer vents, open-ended valves or lines, and pressure relief valves needed for safety purposes are not subject to this paragraph.

(4) For each source as defined in  $\S$  63.101, beginning no later than the compliance dates specified in  $\S$  63.100(k)(10):

(i) The use of a bypass line at any time on a closed vent system to divert emissions (subject to the emission suppression requirements specified in <u>§§ 63.133</u> through <u>63.137</u>) to the atmosphere or to a control device not meeting the requirements specified in this subpart is an emissions standards violation.

(ii) <u>Paragraph (f)(3)</u> of this section no longer applies. Instead, the exemptions specified in <u>paragraphs</u> (f)(4)(ii)(A) and (f)(4)(ii)(B) of this section apply.

(A) Except for pressure relief devices subject to  $\S 63.165(e)(4)$ , equipment such as low leg drains and equipment subject to the requirements of subpart H of this part are not subject to this paragraph (f) of this section.

(B) Open-ended valves or lines that use a cap, blind flange, plug, or second valve and follow the requirements specified in  $\frac{40}{\text{CFR} 60.482-6(a)(2)}$ , (b), and (c) or follow requirements codified in another regulation that are the same as  $\frac{40 \text{ CFR} 60.482-6(a)(2)}{6(a)(2)}$ , (b), and (c) are not subject to this paragraph (f) of this section.

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(g) Any parts of the vapor collection system, closed vent system, fixed roof, cover, or enclosure that are designated, as described in <u>paragraph (i)(1)</u> of this section, as unsafe to inspect are exempt from the inspection requirements of <u>paragraphs</u> (b)(1), (b)(2), and (b)(3)(i) of this section if:

(1) The owner or operator determines that the equipment is unsafe to inspect because inspecting personnel would be exposed to an imminent or potential danger as a consequence of complying with <u>paragraphs (b)(1)</u>, (b)(2), or (b)(3)(i) of this section; and

(2) The owner or operator has a written plan that requires inspection of the equipment as frequently as practicable during safe-to-inspect times.

(h) Any parts of the vapor collection system, closed vent system, fixed roof, cover, or enclosure that are designated, as described in paragraph (i)(2) of this section, as difficult to inspect are exempt from the inspection requirements of paragraphs (b)(1), (b)(2), and (b)(3)(i) of this section if:

(1) The owner or operator determines that the equipment cannot be inspected without elevating the inspecting personnel more than 2 meters above a support surface; and

(2) The owner or operator has a written plan that requires inspection of the equipment at least once every 5 years.

(i) The owner or operator shall record the information specified in <u>paragraphs (i)(1)</u> through (i)(5) of this section.

(1) Identification of all parts of the vapor collection system, closed vent system, fixed roof, cover, or enclosure that are designated as unsafe to inspect, an explanation of why the equipment is unsafe to inspect, and the plan for inspecting the equipment.

(2) Identification of all parts of the vapor collection system, closed vent system, fixed roof, cover, or enclosure that are designated as difficult to inspect, an explanation of why the equipment is difficult to inspect, and the plan for inspecting the equipment.

(3) For each vapor collection system or closed vent system that contains bypass lines that could divert a vent stream away from the control device and to the atmosphere, the owner or operator shall keep a record of the information specified in either <u>paragraph (i)(3)(i)</u> or <u>(i)(3)(ii)</u> of this section in addition to the information specified in <u>paragraph (i)(3)(iii)</u> of this section.

(i) Hourly records of whether the flow indicator specified under <u>paragraph (f)(1)</u> of this section was operating and whether a diversion was detected at any time during the hour, as well as records of the times of all periods when the vent stream is diverted from the control device or the flow indicator is not operating.

(ii) Where a seal mechanism is used to comply with <u>paragraph (f)(2)</u> of this section, hourly records of flow are not required. In such cases, the owner or operator shall record whether the monthly visual inspection of the seals or closure mechanisms has been done, and shall record the occurrence of all periods when the seal mechanism is broken, the bypass line valve position has changed, or the key for a lock-and-key type configuration has been checked out, and records of any car-seal that has broken.

(iii) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in <u>paragraphs (i)(3)(i)</u> or (i)(3)(ii) of this section. For each flow event from a bypass line subject to the requirements in <u>paragraph (f)</u> of this section, the owner or operator must maintain records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requiring control that is released either directly to the atmosphere or to a control device not meeting the requirements in this subpart, the owner or operator must include an estimate of the volume of gas, the concentration of organic HAP in the gas and the resulting emissions of organic HAP that bypassed the control device using process knowledge and engineering estimates.

(4) For each inspection during which a leak is detected, a record of the information specified in <u>paragraphs</u> (i)(4)(i) through (i)(4)(viii) of this section.

(i) The instrument identification numbers; operator name or initials; and identification of the equipment.

(ii) The date the leak was detected and the date of the first attempt to repair the leak.

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(iii) Maximum instrument reading measured by the method specified in <u>paragraph (d)</u> of this section after the leak is successfully repaired or determined to be nonrepairable.

(iv) "Repair delayed" and the reason for the delay if a leak is not repaired within 15 calendar days after discovery of the leak.

(v) The name, initials, or other form of identification of the owner or operator (or designee) whose decision it was that repair could not be effected without a shutdown.

(vi) The expected date of successful repair of the leak if a leak is not repaired within 15 calendar days.

(vii) Dates of shutdowns that occur while the equipment is unrepaired.

(viii) The date of successful repair of the leak.

(5) For each inspection conducted in accordance with <u>paragraph (c)</u> of this section during which no leaks are detected, a record that the inspection was performed, the date of the inspection, and a statement that no leaks were detected.

(6) For each visual inspection conducted in accordance with <u>paragraph (b)(1)(ii)</u> or (b)(3)(ii) of this section during which no leaks are detected, a record that the inspection was performed, the date of the inspection, and a statement that no leaks were detected.

(j) The owner or operator shall submit with the reports required by  $\S 63.182(b)$  of subpart H of this part or with the reports required by  $\S 63.152(c)$  of this subpart, the information specified in paragraphs (j)(1) through (3) of this section and if applicable, the information in paragraph (j)(4) of this section.

(1) The information specified in <u>paragraph (i)(4)</u> of this section;

(2) Reports of the times of all periods recorded under <u>paragraph (i)(3)(i)</u> of this section when the vent stream is diverted from the control device through a bypass line, including the start date, start time, and duration in hours; and

(3) Reports of all periods recorded under <u>paragraph (i)(3)(ii)</u> of this section in which the seal mechanism is broken, the bypass line valve position has changed, or the key to unlock the bypass line valve was checked out. Include the start date, start time, and duration in hours for each period.

(4) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in <u>paragraphs (j)(1)</u> through (3) of this section. For bypass lines subject to the requirements in <u>paragraph (f)</u> of this section, the Periodic Report must include the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours.

(k) If a closed vent system subject to this section is also subject to  $\frac{63.172}{5}$ , the owner or operator shall comply with the provisions of  $\frac{63.172}{5}$  and is exempt from the requirements of this section.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>60 FR 63628</u>, Dec. 12, 1995; <u>62 FR 2775</u>, Jan. 17, 1997; <u>64 FR 20192</u>, Apr. 26, 1999; <u>89 FR 43206</u>, May 16, 2024]

# § 63.149 Control requirements for certain liquid streams in open systems within a chemical manufacturing process unit.

(a) The owner or operator shall comply with the provisions of table 35 of this subpart, for each item of equipment meeting all the criteria specified in paragraphs (b) through (d) and either <u>paragraph (e)(1)</u> or (e)(2) of this section.

(b) The item of equipment is of a type identified in table 35 of this subpart;

(c) The item of equipment is part of a chemical manufacturing process unit that meets the criteria of  $\S$  63.100(b) of subpart F of this part;

(d) The item of equipment is controlled less stringently than in table 35 and is not listed in § 63.100(f) of subpart F of this part, and the item of equipment is not otherwise exempt from controls by the provisions of subparts A, F, G, or H of this part; and

(e) The item of equipment:

(1) is a drain, drain hub, manhole, lift station, trench, pipe, or oil/water separator that conveys water with a total annual average concentration greater than or equal to 10,000 parts per million by weight of Table 9 compounds at any flowrate; or a total annual average concentration greater than or equal to 1,000 parts per million by weight of Table 9 compounds at an annual average flow rate greater than or equal to 10 liters per minute. At a chemical manufacturing process unit subject to the new source requirements of 40 CFR 63.100(1)(1) or 40 CFR 63.100(1)(2), the criteria of this paragraph are also met if the item of equipment conveys water with an annual average concentration greater than or equal to 10 parts per million by weight of any Table 8 compound at an annual average flow rate greater than or equal to 0.02 liter per minute, or

(2) Is a tank that receives one or more streams that contain water with a total annual average concentration greater than or equal to 1,000 ppm (by weight) of Table 9 compounds at an annual average flowrate greater than or equal to 10 liters per minute. At a chemical manufacturing process unit subject to the new source requirements of 40 CFR 63.100(1)(1) or 40 CFR 63.100(1)(2), the criteria of this paragraph are also met if the tank receives one or more streams that contain water with an annual average concentration greater than or equal to 10 parts per million by weight of any Table 8 compound at an annual average flow rate greater than or equal to 0.02 liter per minute. The owner or operator of the source shall determine the characteristics of the stream as specified in paragraphs (e)(2) (i) and (ii) of this section.

(i) The characteristics of the stream being received shall be determined at the inlet to the tank.

(ii) The characteristics shall be determined according to the procedures in § 63.144 (b) and (c).

[<u>62 FR 2776</u>, Jan. 17, 1997]

# § 63.150 Emissions averaging provisions.

(a) This section applies to owners or operators of existing sources who seek to comply with the emission standard in § <u>63.112(a) of this subpart</u> by using emissions averaging according to § <u>63.112(f) of this subpart</u> rather than following the provisions of §§ <u>63.113</u> through <u>63.148 of this subpart</u>. Notwithstanding the definition of process vent in § <u>63.101</u> and the sampling site designation in § <u>63.115(a)</u>, for purposes of this section the location of a process vent shall be defined, and the characteristics of its gas stream shall be determined, consistent with <u>paragraph (g)(2)(i)</u> of this section.

(b) Unless an operating permit application has been submitted, the owner or operator shall develop and submit for approval an Implementation Plan containing all of the information required in § 63.151(d) of this subpart for all points to be included in an emissions average. The Implementation Plan or operating permit application shall identify all emission points to be included in the emissions average. This must include any Group 1 emission points to which the reference control technology (defined in § 63.111 of this subpart) is not applied and all other emission points being controlled as part of the average.

(c) The following emission points can be used to generate emissions averaging credits, if control was applied after November 15, 1990 and if sufficient information is available to determine the appropriate value of credits for the emission point:

(1) Group 2 emission points.

(2) Group 1 emission points that are controlled by a technology that the Administrator or permitting authority agrees has a higher nominal efficiency than the reference control technology. Information on the nominal efficiencies for such technologies must be submitted and approved as provided in <u>paragraph (i)</u> of this section.

(3) Emission points from which emissions are reduced by pollution prevention measures. Percent reductions for pollution prevention measures shall be determined as specified in <u>paragraph (j)</u> of this section.

(i) For a Group 1 emission point, the pollution prevention measure must reduce emissions more than the reference control technology would have had the reference control technology been applied to the emission point instead of the pollution prevention measure except as provided in paragraph (c)(3)(ii) of this section.

(ii) If a pollution prevention measure is used in conjunction with other controls for a Group 1 emission point, the pollution prevention measure alone does not have to reduce emissions more than the reference control technology, but the combination of the pollution prevention measure and other controls must reduce emissions more than the reference control technology would have had it been applied instead.

(d) The following emission points cannot be used to generate emissions averaging credits:

(1) Emission points already controlled on or before November 15, 1990, unless the level of control is increased after November 15, 1990, in which case credit will be allowed only for the increase in control after November 15, 1990.

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(2) Group 1 emission points that are controlled by a reference control technology, unless the reference control technology has been approved for use in a different manner and a higher nominal efficiency has been assigned according to the procedures in <u>paragraph (i)</u> of this section. For example, it is not allowable to claim that an internal floating roof meeting the specifications of § 63.119(b) of this subpart applied to a storage vessel is achieving greater than 95 percent control.

(3) Emission points on shut-down process units. Process units that are shut down cannot be used to generate credits or debits.

(4) Wastewater that is not process wastewater or wastewater streams treated in biological treatment units. These two types of wastewater cannot be used to generate credits or debits. For the purposes of this section, the terms wastewater and wastewater stream are used to mean process wastewater.

(5) Emission points controlled to comply with a State or Federal rule other than this subpart, unless the level of control has been increased after November 15, 1990 above what is required by the other State or Federal rule. Only the control above what is required by the other State or Federal rule will be credited. However, if an emission point has been used to generate emissions averaging credit in an approved emissions average, and the point is subsequently made subject to a State or Federal rule other than this subpart, the point can continue to generate emissions averaging credit for the purpose of complying with the previously approved average.

(e) For all points included in an emissions average, the owner or operator shall:

(1) Calculate and record monthly debits for all Group 1 emission points that are controlled to a level less stringent than the reference control technology for those emission points. Equations in  $\frac{\text{paragraph}(g)}{\text{paragraph}(g)}$  of this section shall be used to calculate debits.

(2) Calculate and record monthly credits for all Group 1 or Group 2 emission points that are overcontrolled to compensate for the debits. Equations in <u>paragraph (h)</u> of this section shall be used to calculate credits. Emission points and controls that meet the criteria of <u>paragraph (c)</u> of this section may be included in the credit calculation, whereas those described in <u>paragraph</u> (d) of this section shall not be included.

(3) Demonstrate that annual credits calculated according to <u>paragraph (h)</u> of this section are greater than or equal to debits calculated for the same annual compliance period according to <u>paragraph (g)</u> of this section.

(i) The owner or operator may choose to include more than the required number of credit-generating emission points in an average in order to increase the likelihood of being in compliance.

(ii) The initial demonstration in the Implementation Plan or operating permit application that credit-generating emission points will be capable of generating sufficient credits to offset the debits from the debit-generating emission points must be made under representative operating conditions. After the compliance date, actual operating data will be used for all debit and credit calculations.

(4) Demonstrate that debits calculated for a quarterly (3-month) period according to <u>paragraph (g)</u> of this section are not more than 1.30 times the credits for the same period calculated according to <u>paragraph (h)</u> of this section. Compliance for the quarter shall be determined based on the ratio of credits and debits from that quarter, with 30 percent more debits than credits allowed on a quarterly basis.

(5) Record and report quarterly and annual credits and debits in the Periodic Reports as specified in  $\frac{\& 63.152(c) \text{ of this}}{\& \text{subpart}}$ . Every fourth Periodic Report shall include a certification of compliance with the emissions averaging provisions as required by  $\frac{\& 63.152(c)(5)(iv)(B)}{\& 0 \text{ of this subpart}}$ .

(f) Debits and credits shall be calculated in accordance with the methods and procedures specified in <u>paragraphs</u> (g) and (h) of this section, respectively, and shall not include emissions from the following:

(1) More than 20 individual Group 1 or Group 2 emission points. Where pollution prevention measures (as specified in paragraph (j)(1) of this section) are used to control emission points to be included in an emissions average, no more than 25 emission points may be included in the average. For example, if two emission points to be included in an emissions average are controlled by pollution prevention measures, the average may include up to 22 emission points.

(2) Periods of start-up, shutdown, and malfunction as described in the source's start-up, shutdown, and malfunction plan required by  $\frac{63.6(e)(3)}{2}$ . For each source as defined in  $\frac{63.101}{2}$ , on and after July 15, 2027, this paragraph no longer applies.

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(3) Periods of monitoring excursions as defined in  $\frac{63.152(c)(2)(ii)(A)}{(A)}$  of this subpart. For these periods, the calculation of monthly credits and debits shall be adjusted as specified in paragraphs (f)(3)(i) through (f)(3)(iii) of this section.

(i) No credits would be assigned to the credit-generating emission point.

(ii) Maximum debits would be assigned to the debit-generating emission point.

(iii) The owner or operator may demonstrate to the Administrator that full or partial credits or debits should be assigned using the procedures in <u>paragraph (1)</u> of this section.

(g) Debits are generated by the difference between the actual emissions from a Group 1 emission point that is uncontrolled or is controlled to a level less stringent than the reference control technology, and the emissions allowed for the Group 1 emission point. Debits shall be calculated as follows:

(1) The overall equation for calculating source-wide debits is:

$$Debits = \sum_{i=1}^{n} (EPV_{iACTUAL} - (0.02)EPV_{iu}) + \sum_{i=1}^{n} (ES_{iACTUAL} - (0.05)ES_{iu}) + \sum_{i=1}^{n} (ETR_{iACTUAL} - (0.02)ETR_{iu}) + \sum_{i=1}^{n} (EWW_{iACTUAL} - EWW_{ic})$$

where:

Debits and all terms of the equation are in units of megagrams per month, and

 $EPV_{iACTUAL} = Emissions$  from each Group 1 process vent i that is uncontrolled or is controlled to a level less stringent than the reference control technology. This is calculated according to paragraph (g)(2) of this section.

(0.02)  $EPV_{iu} = Emissions$  from each Group 1 vent i if the reference control technology had been applied to the uncontrolled emissions, calculated according to <u>paragraph (g)(2)</u> of this section.

 $ES_{iACTUAL} = Emissions$  from each Group 1 storage vessel i that is uncontrolled or is controlled to a level less stringent than the reference control technology. This is calculated according to paragraph (g)(3) of this section.

(0.05)  $ES_{iu} = Emissions$  from each Group 1 storage vessel i if the reference control technology had been applied to the uncontrolled emissions, calculated according to paragraph (g)(3) of this section.

 $ETR_{iACTUAL}$  = Emissions from each Group 1 transfer rack i that is uncontrolled or is controlled to a level less stringent than the reference control technology. This is calculated according to <u>paragraph (g)(4)</u> of this section.

(0.02)  $\text{ETR}_{iu}$  = Emissions from each Group 1 transfer rack i if the reference control technology had been applied to the uncontrolled emissions, calculated according to <u>paragraph (g)(4)</u> of this section.

 $EWW_{iACTUAL} = Emissions$  from each Group 1 wastewater stream i that is uncontrolled or is controlled to a level less stringent than the reference control technology. This is calculated according to <u>paragraph (g)(5)</u> of this section.

 $EWW_{ic} = Emissions$  from each Group 1 wastewater stream i if the reference control technology had been applied to the uncontrolled emissions. This is calculated according to paragraph (g)(5) of this section.

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n = The number of emission points being included in the emissions average. The value of n is not necessarily the same for process vents, storage vessels, transfer racks, and wastewater.

(2) Emissions from process vents shall be calculated according to <u>paragraphs (g)(2)(i)</u> through <u>(iii)</u> of this section.

(i) The location of a process vent shall be defined, and the characteristics of its gas stream shall be determined at a point that meets the conditions in either paragraph (g)(2)(i)(A) or (B) of this section and the conditions in paragraphs (g)(2)(i)(C) through (E) of this section.

(A) The point is after the final recovery device (if any recovery devices are present).

(B) If a gas stream included in an emissions average is combined with one or more other gas streams after a final recovery device (if any recovery devices are present), then for each gas stream, the point is at a representative point after any final recovery device and as near as feasible to, but before, the point of combination of the gas streams.

(C) The point is before any control device (for process vents, recovery devices shall not be considered control devices).

(D) The point is before discharge to the atmosphere.

(E) The measurement site for determination of the characteristics of the gas stream was selected using Method 1 or 1A of  $\underline{40}$  <u>CFR part 60, appendix A</u>.

(ii) The following equation shall be used for each process vent i to calculate  $\text{EPV}_{iu}$ :

$$EPV_{iu} = (2.494 \times 10^{-9}) Qh \left[ \sum_{j=1}^{n} C_j M_j \right]$$

Where:

EPV<sub>iu</sub> = Uncontrolled process vent emission rate from process vent i, megagrams per month.

Q = Vent stream flow rate, dry standard cubic meters per minute, measured using Method 2, 2A, 2C, or 2D of part 60, appendix A, as appropriate.

h = Monthly hours of operation during which positive flow is present in the vent, hours per month.

Cj = Concentration, parts per million by volume, dry basis, of organic HAP j as measured by Method 18 of part 60, appendix A, or ASTM D6420-18 (incorporated by reference, see  $\S$  63.14).

Mj = Molecular weight of organic HAP j, gram per gram-mole.

n = Number of organic HAP's.

(A) The values of Q, C<sub>j</sub>, and M<sub>j</sub> shall be determined during a performance test conducted under representative operating conditions as specified in <u>§ 63.103(b)(3)</u>. The values of Q, C<sub>j</sub>, and M<sub>j</sub> shall be established in the Notification of Compliance Status and must be updated as provided in <u>paragraph (g)(2)(ii)(B)</u> of this section.

(iii) The following procedures and equations shall be used to calculate EPV<sub>iACTUAL</sub>:

(A) If the vent is not controlled by a control device or pollution prevention measure,  $EPV_{iACTUAL} = EPV_{iu}$ , where  $EPV_{iu}$  is calculated according to the procedures in <u>paragraphs (g)(2)(i)</u> and <u>(g)(2)(ii)</u> of this section.

(B) If the vent is controlled using a control device or a pollution prevention measure achieving less than 98-percent reduction,

$$EPV_{iACTUAL} = EPV_{iu} \times \left(1 - \frac{Percent reduction}{100\%}\right)$$

(1) The percent reduction shall be measured according to the procedures in  $\S 63.116$  of this subpart if a combustion control device is used. For a flare meeting the criteria in  $\S 63.116(a)$  of this subpart, or a boiler or process heater meeting the criteria

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in  $\S$  63.116(b) of this subpart, the percent reduction shall be 98 percent. If a non-combustion control device is used, percent reduction shall be demonstrated by a performance test at the inlet and outlet of the device, or, if testing is not feasible, by a control design evaluation and documented engineering calculations.

(2) For determining debits from Group 1 process vents, recovery devices shall not be considered control devices and cannot be assigned a percent reduction in calculating  $EPV_{iACTUAL}$ . The sampling site for measurement of uncontrolled emissions is after the final recovery device. However, as provided in § 63.113(a)(3), except as specified in § 63.113(a)(4), a Group 1 process vent may add sufficient recovery to raise the TRE index value above 1.0, thereby becoming a Group 2 process vent.

(3) Procedures for calculating the percent reduction of pollution prevention measures are specified in <u>paragraph (j)</u> of this section.

(3) Emissions from storage vessels shall be calculated as follows:

(i) The following equation shall be used for each storage vessel i to calculate  $ES_{iu}$ :

$$\mathrm{ES}_{\mathrm{iu}} = \frac{\mathrm{L}_{\mathrm{B}} + \mathrm{L}_{\mathrm{W}}}{12}$$

where:

 $ES_{iu} = Uncontrolled$  emissions, defined as emissions from a fixed roof vessel having identical dimensions and vessel color as vessel i, megagrams per month.

 $L_B$  = Breathing loss emissions, megagrams per year, calculated according to <u>paragraph (g)(3)(i)(A)</u> of this section.

 $L_W$  = Working loss emissions, megagrams per year, calculated according to <u>paragraph (g)(3)(i)(B)</u> of this section.

12 =Constant, months per year.

(A) Breathing loss emissions shall be calculated using the following equation:

1

$$L_{\rm B} = 1.02 \times 10^{-5} \,\mathrm{M_v} \left(\frac{\mathrm{P}}{\mathrm{P_A} - \mathrm{P}}\right) 0.68_{\rm D} 1.73_{\rm H} 0.51_{\Delta \rm T} 0.50_{\mathrm{F_pC}\,\mathrm{K_C}}$$

where:

 $M_v$  = Molecular weight of vapor in storage vessel, pound per pound-mole.

 $P_A$  = Average atmospheric pressure, pounds per square inch absolute.

P = True vapor pressure of the HAP at liquid storage temperature, pounds per square inch absolute. See table 21 of this subpart.

D = Tank diameter, feet.

H = Average vapor space height, feet. Use vessel-specific values or an assumed value of one-half the height.

 $\Delta$  T = Average ambient diurnal temperature change, °F. A typical value of 20 °F may be used.

 $F_p$  = Paint factor, dimensionless, from table 22 of this subpart; use  $F_p$  = 1 for vessels located indoors.

C = Adjustment factor for small diameter tanks, dimensionless; use <math>C = 1 for diameter  $\ge 30$  feet; use  $C = 0.0771D - 0.0013D^2 - 0.1334$  for diameter  $\le 30$  feet.

 $K_C$  = Product factor, dimensionless. Use 1.0 for organic HAP's.

(B) Working losses shall be calculated using the following equation:

 $L_W = 1.089 \times 10^{-8} M_v (P)(V)(N) (K_N) (K_C)$ 

where:

V = Tank capacity, gallon.

N = Number of turnovers per year.

 $K_{\rm N}$  = Turnover factor, dimensionless, and

$$K_N = \frac{180 + N}{6N}$$
 for turnovers >36

$$K_N = 1$$
 for turnovers  $\leq 36$ .

 $M_v$ , P, and  $K_c$  as defined in <u>paragraph (g)(3)(i)(A)</u> of this section.

(C) The owner or operator may elect to calculate  $ES_{iu}$  in accordance with the methods described in American Petroleum Institute Publication 2518, Evaporative Loss from Fixed-Roof Tanks (incorporated by reference as specified in § 63.14 of this part).

(1) The owner or operator who elects to use these alternative methods must use them for all storage vessels included in the emissions average as debit or credit generating points.

(2) The equations of <u>paragraphs (g)(3)(i)(A)</u> and <u>(g)(3)(i)(B)</u> of this section shall not be used in conjunction with the alternative methods provided under <u>paragraph (g)(3)(i)(C)</u> of this section.

(ii) The following procedures and equations shall be used for each fixed roof storage vessel i that is not controlled with a floating roof to calculate  $ES_{iACTUAL}$ :

(A) If the vessel is not controlled,  $ES_{iACTUAL} = ES_{iu}$ , where  $ES_{iu}$  is calculated according to the procedures in <u>paragraph</u> (g)(3)(i) of this section.

(B) Except as provided in <u>paragraph (g)(3)(ii)(C)</u> of this section, if the vessel is controlled using a control device or pollution prevention measure achieving less than 95-percent reduction,

$$ES_{iACTUAL} = ES_{iu} * \left(\frac{1 - Percent reduction}{100}\right)$$

(1) The percent reduction for a control device shall be determined through a design evaluation according to the procedures specified in  $\S$  63.120(d) of this subpart.

(2) Procedures for calculating the percent reduction for pollution prevention measures are specified in <u>paragraph (j)</u> of this section.

(C) If the vessel is controlled according to the provisions of  $\S$  63.119(e)(2) of this section whereby the control device is only required to achieve at least 90-percent reduction, the vessel shall not be considered to be generating debits.

(iii) The following equation shall be used for each internal floating roof vessel i that does not meet the specifications of  $\S$  <u>63.119(b)</u> or <u>(d) of this subpart</u> to calculate ES<sub>iACTUAL</sub>:

$$\text{ES}_{\text{iACTUAL}} = \frac{L_{W} + L_{R} + L_{F} + L_{D}}{12}$$

where:

 $L_W$  = Withdrawal loss emissions, megagrams per year, calculated according to <u>paragraph (g)(3)(iii)(A)</u> of this section.

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- $L_R = Rim seal loss emissions$ , megagrams per year, calculated according to <u>paragraph (g)(3)(iii)(B)</u> of this section.
- $L_F$  = Fitting loss emissions, megagrams per year, calculated according to paragraph (g)(3)(iii)(C) of this section.
- $L_D$  = Deck seam loss emissions, megagrams per year, calculated according to <u>paragraph (g)(3)(iii)(D)</u> of this section.
- 12 =Constant, months per year.
- (A) Withdrawal loss emissions shall be calculated using the following equation:

$$L_{W} = \frac{1.018 \times 10^{-5} \text{QCW}_{L}}{\text{D}} \left[ 1 + \left( \frac{\text{N}_{c} \text{F}_{c}}{\text{D}} \right) \right]$$

where:

Q = Throughput, gallon per year; (gallon/turnover) \* (turnovers per year).

C = Shell clingage factor, barrel per 1,000 square foot, see table 23 of this subpart.

WL = Average liquid density, pound per gallon.

D = Tank diameter, feet.

 $N_c$  = Number of columns, dimensionless, see table 24 of this subpart.

 $F_c = Effective column diameter, feet [column perimeter (feet) ÷ 3.1416], see table 25 of this subpart.$ 

(B) Rim seal loss emissions shall be calculated using the following equation:

$$L_{R} = \frac{K_{s}V^{n}P^{*}DM_{v}K_{c}}{2.205}$$

where:

M<sub>v</sub> = Molecular weight of vapor in storage vessel, pound per pound-mole.

D = Tank diameter, feet.

 $K_c$  = Product factor, dimensionless; use 1.0 for organic HAP's.

 $K_s$  = Seal factor, pound-mole per [foot (miles per hour)<sup>n</sup> year], see table 26 of this subpart.

V = Average wind speed at the source, miles per hour. A value of 10 miles per hour may be assumed if source-specific data are not available.

n = Seal related wind speed exponent, dimensionless, see table 26 of this subpart.

2,205 = Constant, pounds per megagram.

P\* = Vapor pressure function, dimensionless, and

$$P^* = \frac{\frac{P}{P_A}}{\left[1 + \left(1 - \frac{P}{P_A}\right)0.5\right]^2}$$

where:

 $P_A$  = Average atmospheric pressure, pounds per square inch absolute.

P = True vapor pressure at liquid storage temperature, pounds per square inch absolute.

(C) Fitting loss emissions shall be calculated using the following equation:

$$L_{\rm F} = \frac{F_{\rm f} P^* M_v K_c}{2,205}$$

where:

 $F_f$  = The total deck fitting loss factor, pound-mole per year, and where:

$$F_{f} = \sum_{i=1}^{n} \left( N_{F_{i}} K_{F_{i}} \right) = \left[ \left( N_{F_{1}} K_{F_{1}} \right) + \left( N_{F_{2}} K_{F_{2}} \right) + \dots + \left( N_{F_{n}} K_{F_{n}} \right) \right]$$

 $N_{Fi}$  = Number of fittings of a particular type, dimensionless.  $N_{Fi}$  is determined for the specific tank or estimated from tables 24 and 27 of this subpart.

 $K_{Fi}$  = Deck fitting loss factor for a particular type fitting, pound-mole per year.  $K_{Fi}$  is determined for each fitting type from table 27 of this subpart.

n = Number of different types of fittings, dimensionless.

P\*, M<sub>v</sub>, K<sub>c</sub>, and 2,205 as defined in paragraph (g)(3)(iii)(B) of this section.

(D) Deck seam loss emissions shall be calculated using the following equation:

$$L_{\rm D} = \frac{K_{\rm D} S_{\rm D} D^2 P^* M_v K_c}{2,205}$$

where:

 $K_D$  = Deck seam loss factor, pound-mole per foot per year, and

 $K_D = 0.34$  for non-welded decks.

 $K_D = 0$  for welded decks.

 $S_D$  = Deck seam length factor, feet per square foot, see table 28 of this subpart.

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D, P\*, M<sub>v</sub>, K<sub>c</sub>, and 2,205 as defined in paragraph (g)(3)(iii)(B) of this section.

(iv) The following equation shall be used for each external floating roof vessel i that does not meet the specifications of  $\S$  <u>63.119(c) of this subpart</u> to calculate ES<sub>iACTUAL</sub>:

$$\mathrm{ES}_{\mathrm{iACTUAL}} = \frac{\mathrm{L}_{\mathrm{W}} + \mathrm{L}_{\mathrm{R}} + \mathrm{L}_{\mathrm{F}}}{12}$$

where:

 $L_W$  = Withdrawal loss emissions, megagrams per year, calculated according to <u>paragraph (g)(3)(iv)(A)</u> of this section.

 $L_R = Rim seal loss emissions$ , megagrams per year, calculated according to <u>paragraph (g)(3)(iv)(B)</u> of this section.

 $L_F$  = Fitting loss emissions, megagrams per year, calculated according to paragraph (g)(3)(iv)(C) of this section.

12 = Constant, months per year.

(A) Withdrawal loss emissions shall be calculated using the following equation:

$$L_{W} = \frac{4.28 \times 10^{-4} QCW_{L}}{D}$$

where:

Q = Throughput, gallons per year.

C = Shell clingage factor, barrel per 1,000 square foot, see table 23 of this subpart.

 $W_L$  = Average liquid density, pound per gallon.

D = Vessel diameter, feet.

(B) Rim seal loss emissions shall be calculated using the following equation:

$$L_{R} = \frac{K_{s}V^{N}P^{*}DM_{v}K_{c}}{2,205}$$

where:

 $K_s$  = Seal factor, pound-mole per [foot (miles per hour)<sup>N</sup> year], see table 29 of this subpart.

V = Average wind speed, miles per hour, at the source. A value of 10 miles per hour may be assumed if source-specific data are not available.

N = Seal wind speed exponent, dimensionless, see table 29 of this subpart.

 $P^* = Vapor pressure function, dimensionless, as defined in <u>paragraph (g)(3)(iii)(B)</u> of this section.$ 

D = Vessel diameter, feet.

 $M_V$  = Molecular weight of the HAP, pound per pound-mole.

 $K_c$  = Product factor, dimensionless; use 1.0 for organic HAP's.

2,205 = Constant, pounds per megagram.

(C) Fitting loss emissions shall be calculated using the following equation:

$$L_F = \frac{F_F P^* M_v K_c}{2,205}$$

where:

 $F_F$  = The total deck fitting loss factor, pound-mole per year, and

$$F_{F} = \sum_{i=1}^{n} \left( N_{F_{i}} K_{F_{i}} \right) = \left[ \left( N_{F_{i}} K_{F_{i}} \right) + \left( N_{F_{2}} K_{F_{2}} \right) + \dots + \left( N_{F_{n}} K_{F_{n}} \right) \right]$$

where:

 $N_{Fi}$  = Number of fittings of a particular type, dimensionless.  $N_{Fi}$  is determined for the specific tank or estimated from tables 30 through 32 of this subpart.

K<sub>Fi</sub> = Deck fitting loss factor for a particular type fitting, pound-mole per year, and

 $K_{Fi} = K_{Fai} + K_{Fbi} V^{mi}$ , pound-mole per year, see table 30 of this subpart for the appropriate values of  $K_{Fa}$ ,  $K_{Fb}$ , and m for each fitting type.

V, P\*,  $M_v$ , K<sub>c</sub>, and 2,205 as defined in <u>paragraph (g)(3)(iv)(B)</u> of this section.

- (4) Emissions from transfer racks shall be calculated as follows:
- (i) The following equation shall be used for each transfer rack i to calculate  $ETR_{iu}$ :

$$\text{ETR}_{\text{iu}} = \left(1.20 \times 10^{-7}\right) \frac{\text{SPMG}}{\text{T}}$$

where:

 $ETR_{iu}$  = Uncontrolled transfer HAP emission rate from transfer rack i, megagrams per month.

S = Saturation factor, dimensionless (see table 33 of this subpart).

P = Weighted average rack partial pressure of organic HAP's transferred at the rack during the month, kilopascals.

M = Weighted average molecular weight of organic HAP's transferred at the transfer rack during the month, gram per grammole.

G = Monthly volume of organic HAP's transferred, liters per month.

T = Weighted rack bulk liquid loading temperature during the month, Kelvin ( $^{\circ}C + 273$ ).

(ii) The following equation shall be used for each transfer rack i to calculate the weighted average rack partial pressure:

$$P = \frac{\sum_{j=n}^{j=n} (P_j)(G_j)}{G}$$

where:

 $P_j$  = Maximum true vapor pressure of individual organic HAP transferred at the rack, kilopascals.

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G = Monthly volume of organic HAP transferred, liters per month, and

$$G = \sum_{1}^{j=n} G_j$$

 $G_j$  = Monthly volume of individual organic HAP transferred at the transfer rack, liters per month.

n = Number of organic HAP's transferred at the transfer rack.

(iii) The following equation shall be used for each transfer rack i to calculate the weighted average rack molecular weight:

$$M = \frac{\sum_{j=n}^{j=n} (M_j)(G_j)}{G}$$

where:

 $M_j$  = Molecular weight of individual organic HAP transferred at the rack, gram per gram-mole.

G,  $G_j$ , and n as defined in <u>paragraph (g)(4)(ii)</u> of this section.

(iv) The following equation shall be used for each transfer rack i to calculate the monthly weighted rack bulk liquid loading temperature:

$$T = \frac{\sum_{j=n}^{j=n} (T_j)(G_j)}{G}$$

where:

 $T_j$  = Average annual bulk temperature of individual organic HAP loaded at the transfer rack, Kelvin ((°C + 273).

G,  $G_j$ , and n as defined in <u>paragraph (g)(4)(ii)</u> of this section.

(v) The following procedures and equations shall be used to calculate  $\text{ETR}_{iACTUAL}$ :

(A) If the transfer rack is not controlled,  $ETR_{iACTUAL} = ETR_{iu}$ , where  $ETR_{iu}$  is calculated using the equations specified in paragraphs (g)(4)(i) through (g)(4)(iv) of this section.

(B) If the transfer rack is controlled using a control device or a pollution prevention measure achieving less than the 98percent reduction,

$$ETR_{iACTUAL} = ETR_{iu} \left( \frac{1 - Percent reduction}{100\%} \right)$$

(1) The percent reduction for a control device shall be measured according to the procedures and test methods specified in § 63.128(a) of this subpart. For a flare meeting the criteria in § 63.128(b) of this subpart or a boiler or process heater meeting the criteria in § 63.128(c) of this subpart, the percent reduction shall be 98 percent. If testing is not feasible, percent reduction shall be determined through a design evaluation according to the procedures specified in § 63.128(b) of this subpart.

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(2) Procedures for calculating the percent reduction for pollution prevention measures are specified in <u>paragraph (j)</u> of this section.

- (5) Emissions from wastewater shall be calculated as follows:
- (i) The following equation shall be used for each wastewater stream i to calculate EWWic:

EWW<sub>ic</sub> = 
$$(6.0*10^{-8}) Q_i H_i \sum_{m=1}^{s} (1 - Fr_m) Fe_m HAP_{im}$$
  
+  $(0.05)(6.0*10^{-8}) Q_i H_i \sum_{m=1}^{s} (Fr_m HAP_{im})$ 

where:

 $EWW_{ic} = Monthly$  wastewater stream emission rate if wastewater stream i is controlled by the reference control technology, megagrams per month.

 $Q_i$  = Average flow rate for wastewater stream i, as determined by the procedure in <u>§ 63.144(c)(3)</u>, liters per minute.

H<sub>i</sub> = Number of hours during the month that wastewater stream i was generated, hours per month.

s = Total number of table 9 HAP in wastewater stream i.

 $Fr_m$  = Fraction removed of table 9 HAP m in wastewater, from table 9, dimensionless.

Fe<sub>m</sub> = Fraction emitted of table 9 HAP m in wastewater, from table 34, dimensionless.

HAP<sub>im</sub> = Average concentration of table 9 HAP m in wastewater stream i, parts per million by weight.

(A) HAP<sub>im</sub> shall be determined for the point of determination or, at a location downstream of the point of determination and adjusted according as specified in § 63.144(b)(6) of this subpart, by developing and using the sampling plan specified in § 63.144(b)(5)(ii) of this subpart. The samples collected may be analyzed by any of the methods specified in § 63.144(b)(5)(i)(B) through (b)(5)(i)(F) of this subpart. Concentration measurements based on Method 305 shall be adjusted by dividing each concentration by the compound-specific Fm factor listed on table 34 of this subpart. Concentration measurements other than Method 305 shall not be adjusted by the compound-specific Fm factor listed in table 34 of this subpart.

(B) Values for  $Q_i$ , HAP<sub>im</sub>, and  $C_{im}$  shall be determined during a performance test conducted under representative conditions as specified in § 63.145(a)(3) and (a)(4) of this subpart. The average value obtained from three test runs shall be used. The values of  $Q_i$ , HAP<sub>im</sub>, and  $C_{im}$  shall be established in the Notification of Compliance Status and must be updated as provided in paragraph (g)(5)(i)(C) of this section.

(C) If there is a change to the process or operation such that the previously measured values of  $Q_i$ , HAP<sub>im</sub>, and  $C_{im}$  are no longer representative, a new performance test shall be conducted to determine new representative values of  $Q_i$ , HAP<sub>im</sub>, and  $C_{im}$ . These new values shall be used to calculate debits and credits from the time of the change forward, and the new values shall be reported in the next Periodic Report.

(ii) The following equation shall be used to calculate  $EWW_{iACTUAL}$  for each wastewater stream i that is not managed according to the provisions for waste management units of <u>§§</u> 63.133 through <u>63.137 of this subpart</u>, as applicable, which specify equipment and work practices for suppressing and controlling vapors. Q<sub>i</sub>, H<sub>i</sub>, s, Fe<sub>m</sub>, and HAP<sub>im</sub> are as defined and determined according to <u>paragraph (g)(5)(i)</u> of this section.

$$EWW_{iACTUAL} = (6.0 \times 10^{-8}) Q_i H_i \sum_{m=1}^{s} Fe_m HAP_{im}$$

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Where:

 $EWW_{iACTUAL} =$  Monthly wastewater stream emission rate if wastewater stream i is uncontrolled or is controlled to a level less stringent than the reference control technology, megagrams per month.

(iii) The following equation shall be used to calculate EWW<sub>iACTUAL</sub> for each wastewater stream i that is managed according to the requirements of <u>§§ 63.133</u> through <u>63.137 of this subpart</u>, as applicable, and wastewater stream i is uncontrolled or is controlled to a level less stringent than the reference control technology (for the purposes of the wastewater emissions averaging provisions, the term control is used to mean treatment). Q<sub>i</sub>, H<sub>i</sub>, s, Fe<sub>m</sub>, and HAP<sub>im</sub> are as defined and determined according to <u>paragraph (g)(5)(i)</u> of this section.

EWW<sub>iACTUAL</sub> = 
$$(6.0 * 10^{-8}) Q_i H_i \sum_{m=1}^{s} [Fe_m HAP_{im} (1 - PR_{im})]$$
  
+  $(1 - \frac{R_i}{100\%}) (6.0 * 10^{-8}) Q_i H_i \sum_{m=1}^{s} (HAP_{im} PR_{im})$ 

Where:

 $EWW_{iACTUAL} =$  Monthly wastewater stream emission rate if wastewater stream i is uncontrolled or is controlled to a level less stringent than the reference control technology, megagrams per month.

 $PR_{im}$  = The efficiency of the treatment process, or series of treatment processes, which treat wastewater stream i, in reducing the emission potential of table 9 HAP m in wastewater, dimensionless, as calculated by:

$$PR_{im} = \frac{HAP_{im-in} - HAP_{im-out}}{HAP_{im-in}}$$

Where:

 $HAP_{im-in} = Average concentration of table 9 HAP m, parts per million by weight, as defined and determined according to paragraph (g)(5)(i) of this section, in the wastewater entering the first treatment process in the series.$ 

 $HAP_{im-out} = Average concentration of table 9 HAP m, parts per million by weight, as defined and determined according to paragraph (g)(5)(i) of this section, in the wastewater exiting the last treatment process in the series.$ 

 $R_i$  = Reduction efficiency of the device used to control any vapor streams emitted and collected from wastewater stream i during treatment, dimensionless, as determined according to the procedures in <u>§ 63.145(i)</u> or (j) of this subpart.

(h) Credits are generated by the difference between emissions that are allowed for each Group 1 and Group 2 emission point and the actual emissions from a Group 1 or Group 2 emission point that has been controlled after November 15, 1990 to a level more stringent than what is required by this subpart or any other State or Federal rule or statute. Credits shall be calculated as follows:

(1) The overall equation for calculating source-wide credits is:

$$Credits = D\sum_{i=1}^{n} ((0.02) EPV1_{iu} - EPV1_{iACTUAL}) + D\sum_{i=1}^{m} (EPV2_{iBASE} - EPV2_{iACTUAL}) + D\sum_{i=1}^{n} ((0.05) ES1_{iu} - ES1_{iACTUAL}) + D\sum_{i=1}^{m} (ES2_{iBASE} - ES2_{iACTUAL}) + D\sum_{i=1}^{n} ((0.02) ETR1_{iu} - ETR1_{iACTUAL}) + D\sum_{i=1}^{m} (ETR2_{iBASE} - ETR2_{iACTUAL}) + D\sum_{i=1}^{n} (EWW1_{ic} - EWW1_{iACTUAL}) + D\sum_{i=1}^{m} (EWW2_{iBASE} - EWW2_{iACTUAL}) + D\sum_{i=1}^{m} (EWZ2_{iACTUAL}) + D\sum_{i=1}^{m} (E$$

where:

Credits and all terms of the equation are in units of megagrams per month, the baseline date is November 15, 1990, and:

D = Discount factor = 0.9 for all credit generating emission points except those controlled by a pollution prevention measure, which will not be discounted.

 $EPV1_{iACTUAL}$  = Emissions for each Group 1 process vent i that is controlled to a level more stringent than the reference control technology, calculated according to <u>paragraph (h)(2)</u> of this section.

(0.02) EPV1<sub>iu</sub> = Emissions from each Group 1 process vent i if the reference control technology had been applied to the uncontrolled emissions. EPV1<sub>iu</sub> is calculated according to <u>paragraph (h)(2)</u> of this section.

 $EPV2_{iACTUAL}$  = Emissions from each Group 2 process vent i that is controlled, calculated according to <u>paragraph (h)(2)</u> of this section.

 $EPV2_{iBASE} = Emissions$  from each Group 2 process vent i at the baseline date, as calculated in <u>paragraph (h)(2)</u> of this section.

 $ES1_{iACTUAL}$  = Emissions from each Group 1 storage vessel i that is controlled to a level more stringent than the reference control technology, calculated according to paragraph (h)(3) of this section.

(0.05) ES1<sub>iu</sub> = Emissions from each Group 1 storage vessel i if the reference control technology had been applied to the uncontrolled emissions. ES1<sub>iu</sub> is calculated according to <u>paragraph (h)(3)</u> of this section.

 $ES2_{iACTUAL}$  = Emissions from each Group 2 storage vessel i that is controlled, calculated according to <u>paragraph (h)(3)</u> of this section.

 $ES2_{iBASE}$  = Emissions from each Group 2 storage vessel i at the baseline date, as calculated in <u>paragraph (h)(3)</u> of this section.

 $ETR1_{iACTUAL}$  = Emissions from each Group 1 transfer rack i that is controlled to a level more stringent than the reference control technology, calculated according to <u>paragraph (h)(4)</u> of this section.

(0.02)  $ETR1_{iu} = Emissions$  from each Group 1 transfer rack i if the reference control technology had been applied to the uncontrolled emissions.  $ETR1_{iu}$  is calculated according to paragraph (h)(4) of this section.

 $ETR2_{iACTUAL} = Emissions$  from each Group 2 transfer rack i that are controlled, calculated according to <u>paragraph (h)(4)</u> of this section.

 $ETR2_{iBASE}$  = Emissions from each Group 2 transfer rack i at the baseline date, as calculated in <u>paragraph (h)(4)</u> of this section.

 $EWW1_{iACTUAL} = Emissions$  from each Group 1 wastewater stream i that is controlled to a level more stringent than the reference control technology, calculated according to paragraph (h)(5) of this section.

 $EWW1_{ic} = Emissions$  from each Group 1 wastewater stream i if the reference control technology had been applied to the uncontrolled emissions, calculated according to paragraph (h)(5) of this section.

 $EWW2_{iACTUAL} = Emissions$  from each Group 2 wastewater stream i that is controlled, calculated according to <u>paragraph</u> (h)(5) of this section.

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 $EWW2_{iBASE} = Emissions$  from each Group 2 wastewater stream i at the baseline date, calculated according to <u>paragraph</u> (h)(5) of this section.

n = Number of Group 1 emission points included in the emissions average. The value of n is not necessarily the same for process vents, storage vessels, transfer racks, and wastewater.

m = Number of Group 2 emission points included in the emissions average. The value of m is not necessarily the same for process vents, storage vessels, transfer racks, and wastewater.

(i) For an emission point controlled using a reference control technology, the percent reduction for calculating credits shall be no greater than the nominal efficiency associated with the reference control technology, unless a higher nominal efficiency is assigned as specified in paragraph (h)(1)(ii) of this section.

(ii) For an emission point controlled to a level more stringent than the reference control technology, the nominal efficiency for calculating credits shall be assigned as described in <u>paragraph (i)</u> of this section. A reference control technology may be approved for use in a different manner and assigned a higher nominal efficiency according to the procedures in <u>paragraph</u> (i) of this section.

(iii) For an emission point controlled using a pollution prevention measure, the nominal efficiency for calculating credits shall be as determined as described in <u>paragraph (j)</u> of this section.

(2) Emissions from process vents shall be determined as follows:

(i) Uncontrolled emissions from Group 1 process vents,  $EPV1_{iu}$ , shall be calculated according to the procedures and equation for  $EPV_{iu}$  in <u>paragraphs (g)(2)(i)</u> and <u>(g)(2)(ii)</u> of this section.

(ii) Actual emissions from Group 1 process vents controlled using a technology with an approved nominal efficiency greater than 98 percent or a pollution prevention measure achieving greater than 98 percent emission reduction,  $EPV1_{iACTUAL}$ , shall be calculated according to the following equation:

$$EPV1_{iACTUAL} = EPV1_{iu} \left( 1 - \frac{Nominal efficiency \%}{100\%} \right)$$

(iii) The following procedures shall be used to calculate actual emissions from Group 2 process vents, EPV2<sub>iACTUAL</sub>:

(A) For a Group 2 process vent controlled by a control device, a recovery device applied as a pollution prevention project, or a pollution prevention measure, if the control achieves a percent reduction less than or equal to 98 percent reduction,

$$EPV2_{iACTUAL} = EPV2_{iu} \times \left(1 - \frac{Percent reduction}{100\%}\right)$$

(1) EPV2<sub>iu</sub> shall be calculated according to the equations and procedures for EPV<sub>iu</sub> in <u>paragraphs (g)(2)(i)</u> and <u>(g)(2)(ii)</u> of this section, except as provided in <u>paragraph (h)(2)(iii)(A)(3)</u> of this section.

(2) The percent reduction shall be calculated according to the procedures in <u>paragraphs</u> (g)(2)(iii)(B)(1) through (g)(2)(iii)(B)(3) of this section, except as provided in <u>paragraph (h)(2)(iii)(A)(4)</u> of this section.

(3) If a recovery device was added as part of a pollution prevention project,  $EPV2_{iu}$  shall be calculated prior to that recovery device. The equation for  $EPV_{iu}$  in <u>paragraph (g)(2)(ii)</u> of this section shall be used to calculate  $EPV2_{iu}$ ; however, the sampling site for measurement of vent stream flow rate and organic HAP concentration shall be at the inlet of the recovery device.

(4) If a recovery device was added as part of a pollution prevention project, the percent reduction shall be demonstrated by conducting a performance test at the inlet and outlet of that recovery device.

(B) For a Group 2 process vent controlled using a technology with an approved nominal efficiency greater than 98 percent or a pollution prevention measure achieving greater than 98 percent reduction,

$$EPV2_{iACTUAL} = EPV2_{iu} \left( 1 - \frac{Nominal efficiency \%}{100\%} \right)$$

(iv) Emissions from Group 2 process vents at baseline, EPV2<sub>iBASE</sub>, shall be calculated as follows:

(A) If the process vent was uncontrolled on November 15, 1990,  $EPV2_{iBASE} = EPV2_{iu}$  and shall be calculated according to the procedures and equation for  $EPV_{iu}$  in paragraphs (g)(2)(i) and (g)(2)(ii) of this section.

(B) If the process vent was controlled on November 15, 1990,

$$EPV2_{iBASE} = EPV2_{iu} \left( 1 - \frac{Percent reduction \%}{100\%} \right)$$

where  $EPV2_{iu}$  is calculated according to the procedures and equation for  $EPV_{iu}$  in <u>paragraphs (g)(2)(i)</u> and <u>(g)(2)(ii)</u> of this section. The percent reduction shall be calculated according to the procedures specified in <u>paragraphs</u> (g)(2)(iii)(B)(1) through (g)(2)(iii)(B)(3) of this section.

(C) If a recovery device was added to a process vent as part of a pollution prevention project initiated after November 15, 1990,  $EPV2_{iBASE} = EPV2_{iu}$ , where  $EPV2_{iu}$  is calculated according to paragraph (h)(2)(iii)(A)(3) of this section.

(3) Emissions from storage vessels shall be determined as follows:

(i) Uncontrolled emissions from Group 1 storage vessels,  $ES1_{iu}$ , shall be calculated according to the equations and procedures for  $ES_{iu}$  in <u>paragraph (g)(3)(i)</u> of this section.

(ii) Actual emissions from Group 1 storage vessels controlled using a technology with an approved nominal efficiency greater than 95 percent or a pollution prevention measure achieving greater than 95 percent emission reduction,  $ES1_{iACTUAL}$ , shall be calculated according to the following equation:

$$\text{ES1}_{\text{iACTUAL}} = \text{ES1}_{\text{iu}} \left( 1 - \frac{\text{Nominal efficiency \%}}{100\%} \right)$$

(iii) The following procedures shall be used to calculate actual emissions from Group 2 storage vessels, ES2<sub>iACTUAL</sub>:

(A) For a Group 2 storage vessel controlled using a control device or a pollution prevention measure (other than an internal or external floating roof) achieving a percent reduction less than or equal to 95-percent reduction,

$$ES2_{iACTUAL} = ES2_{iu} \times \left(1 - \frac{Percent reduction}{100\%}\right)$$

(1)  $ES2_{iu}$  is calculated according to the equations and procedures for  $ES_{iu}$  in <u>paragraph (g)(3)(i)</u> of this section.

(2) The percent reduction shall be calculated according to the procedures in paragraphs (g)(3)(ii)(B)(1) and (g)(3)(ii)(B)(2) of this section.

(3) If an internal or external floating roof meeting the specifications of  $\S$  63.119 (b), (c), or (d) of this subpart is used to control the vessel, the percent reduction shall be 95 percent.

(B) If a Group 2 storage vessel is controlled with an internal or external floating roof not meeting the specifications of § 63.119 (b), (c), or (d) of this subpart, ES2<sub>iACTUAL</sub> shall be calculated as specified for ES<sub>iACTUAL</sub> in paragraph (g)(3)(iii) or (g)(3)(iv) of this section.

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(C) For a Group 2 storage vessel controlled using a technology with an approved nominal efficiency greater than 95 percent or a pollution prevention measure achieving greater than 95 percent reduction,

$$\text{ES2}_{\text{iACTUAL}} = \text{ES2}_{\text{iu}} \left( 1 - \frac{\text{Nominal efficiency \%}}{100\%} \right)$$

(iv) Emissions from Group 2 storage vessels at baseline, ES2<sub>iBASE</sub>, shall be calculated as follows:

(A) If the fixed-roof vessel was uncontrolled on November 15, 1990,  $ES2_{iBASE} = ES2_{iu}$  and shall be calculated according to the procedures and equations for  $ES_{iu}$  in paragraph (g)(3)(i) of this section.

(B) If the storage vessel was controlled on November 15, 1990:

(1) The equations for  $\text{ES}_{iACTUAL}$  in paragraph (g)(3)(iii) of this section shall be used to calculate  $\text{ES2}_{iBASE}$  for vessels controlled with an internal floating roof that does not meet the specifications of § 63.119 (b) or (d) of this subpart.

(2) The equations for  $ES_{iACTUAL}$  in paragraph (g)(3)(iv) of this section shall be used to calculate  $ES2_{iBASE}$  for vessels controlled with an external floating roof that does not meet the specifications of § 63.119(c) of this subpart.

(3) The following equations shall be used to calculate ES2<sub>iBASE</sub> for vessels controlled with a control device,

$$ES2_{iBASE} = ES2_{iu} \left( 1 - \frac{Percent reduction \%}{100\%} \right)$$

where  $ES2_{iu}$  shall be calculated according to the equations for  $ES_{iu}$  in <u>paragraph (g)(3)(i)</u> of this section. The percent reduction shall be calculated according to the procedures in <u>paragraphs (g)(3)(ii)(B)(1)</u> and (g)(3)(ii)(B)(2) of this section.

(4) Emissions from transfer racks shall be determined as follows:

(i) Uncontrolled emissions from Group 1 transfer racks, ETR1<sub>iu</sub>, shall be calculated according to the procedures and equations for ETR<sub>iu</sub> as described in <u>paragraphs (g)(4)(i)</u> through (g)(4)(iv) of this section.

(ii) Actual emissions from Group 1 transfer racks controlled using a technology with an approved nominal efficiency greater than 98 percent or a pollution prevention measure achieving greater than 98 percent emission reduction, ETR<sub>iACTUAL</sub>, shall be calculated according to the following equation:

$$\text{ETR1}_{\text{iACTUAL}} = \text{ETR1}_{\text{iu}} \left( 1 - \frac{\text{Nominal efficiency}}{100\%} \right)$$

(iii) The following procedures shall be used to calculate actual emissions from Group 2 transfer racks, ETR2<sub>iACTUAL</sub>:

(A) For a Group 2 transfer rack controlled by a control device or a pollution prevention measure achieving a percent reduction less than or equal to 98 percent reduction,

$$ETR2_{iACTUAL} = ETR2_{iu} \left( 1 - \frac{Percent reduction}{100\%} \right)$$

(1) ETR2<sub>iu</sub> shall be calculated according to the equations and procedures for ETR<sub>iu</sub> in <u>paragraphs</u> (g)(4)(i) through (g)(4)(iv) of this section.

(2) The percent reduction shall be calculated according to the procedures in paragraph (g)(4)(v)(B)(1) and (g)(4)(v)(B)(2) of this section.

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(B) For a Group 2 transfer rack controlled using a technology with an approved nominal efficiency greater than 98 percent or a pollution prevention measure achieving greater than 98 percent reduction,

$$ETR2_{iACTUAL} = ETR2_{iu} \left( 1 - \frac{Nominal efficiency}{100\%} \right)$$

(iv) Emissions from Group 2 transfer racks at baseline, ETR2<sub>iBASE</sub>, shall be calculated as follows:

(A) If the transfer rack was uncontrolled on November 15, 1990,  $ETR2_{iBASE} = ETR2_{iu}$  and shall be calculated according to the procedures and equations for  $ETR_{iu}$  in paragraphs (g)(4)(i) through (g)(4)(iv) of this section.

(B) If the transfer rack was controlled on November 15, 1990,

$$ETR2_{iBASE} = ETR2_{iu} \left( 1 - \frac{Percent reduction}{100\%} \right)$$

where ETR2<sub>iu</sub> is calculated according to the procedures and equations for ETR<sub>iu</sub> in <u>paragraphs (g)(4)(i)</u> through (g)(4)(iv) of this section. Percent reduction shall be calculated according to the procedures in <u>paragraphs</u> (g)(4)(v)(B)(1) and (g)(4)(v)(B)(2) of this section.

(5) Emissions from wastewater shall be determined as follows:

(i) EWW1<sub>ic</sub> shall be calculated according to the equation for EWW<sub>ic</sub> in <u>paragraph (g)(5)(i)</u> of this section.

(ii) EWW2<sub>iBASE</sub> shall be calculated according to the equation for EWW<sub>iACTUAL</sub> in paragraph (g)(5)(ii) of this section for each Group 2 wastewater stream i, which on November 15, 1990, was not managed according to the requirements of <u>§§</u> 63.133 through 63.137 of this subpart, as applicable.

(iii) EWW2<sub>iBASE</sub> shall be calculated according to the equation for EWW<sub>iACTUAL</sub> in <u>paragraph (g)(5)(iii)</u> of this section for each Group 2 wastewater stream i, which on November 15, 1990, was managed according to the requirements of <u>§§</u> <u>63.133</u> through <u>63.137</u> of this subpart, as applicable, and was uncontrolled or controlled to a level less stringent than the reference control technology.

(iv) For Group 2 wastewater streams that are managed according to the requirements of  $\frac{8863.133}{500}$  through  $\frac{63.137}{500}$  of this subpart, as applicable, EWW2<sub>iACTUAL</sub> shall be calculated as follows:

(A) EWW2<sub>iACTUAL</sub> shall be calculated according to the equation for EWW<sub>iACTUAL</sub> in <u>paragraph (g)(5)(iii)</u> of this section for each Group 2 wastewater stream i that is controlled to a level less stringent than, or equivalent to, the reference control technology.

(B) EWW2<sub>iACTUAL</sub> shall be calculated according to the procedures for calculating EWW1<sub>iACTUAL</sub> in <u>paragraph (h)(5)(v)</u> of this section for each Group 2 wastewater stream that is controlled to a level more stringent than the reference control technology.

(v) The following equations for EWW1iACTUAL shall be used to calculate emissions from each Group 1 wastewater stream i that is managed according to the requirements of  $\frac{\$\$}{63.133}$  through  $\frac{63.137}{63.137}$  of this subpart, as applicable, and is controlled to a level more stringent than the reference control technology.

(A) If the Group 1 wastewater stream i is controlled using a treatment process or series of treatment processes with an approved nominal reduction efficiency in the concentration of table 9 HAP for stream i greater than that of the design steam stripper specified in § 63.138(d) of this subpart, and the control device used to reduce table 9 HAP emissions from the vapor stream(s) vented from the treatment process(es) achieves a percent reduction equal to 95 percent, the following equation shall be used. All terms in this equation are as defined and determined in paragraph (g)(5) of this section.

EWW1<sub>iACTUAL</sub> = 
$$(6.0 * 10^{-8}) Q_i H_i \sum_{m=1}^{s} [Fe_m HAP_{im} (1 - PR_{im})]$$
  
+ 0.05  $(6.0 * 10^{-8}) Q_i H_i \sum_{m=1}^{s} [HAP_{im} PR_{im}]$ 

(B) If the Group 1 wastewater stream i is not controlled using a treatment process or series of treatment processes with a nominal reduction efficiency in the table 9 HAP concentration greater than that of the design steam stripper specified in § 63.138(d) of this subpart, but the vapor stream(s) vented from the treatment process(es) are controlled using a device with an approved nominal efficiency greater than 95 percent, the following equation shall be used. All terms other than nominal efficiency are as defined and determined in paragraph (g)(5) of this section.

$$EWW1_{iACTUAL} = (6.0 * 10^{-8}) Q_i H_i \sum_{m=1}^{s} [Fe_m HAP_{im} (1 - Fr_m)] + \left(1 - \frac{Nominal efficiency\%}{100}\right) (6.0 * 10^{-8}) Q_i H_i \sum_{m=1}^{s} [HAP_{im} Fr_m]$$

(C) If the Group 1 wastewater stream i is controlled using a treatment process or series of treatment processes with an approved nominal reduction efficiency in the table 9 HAP concentration greater than that of the design steam stripper specified in  $\S$  63.138(d) of this subpart, and the vapor stream(s) vented from the treatment process are controlled using a device with an approved nominal efficiency greater than 95 percent, the following equation shall be used. All terms other than nominal efficiency are as defined and determined in paragraph (g)(5) of this section.

$$EWW1_{iACTUAL} = (6.0*10^{-8}) Q_i H_i \sum_{m=1}^{s} [Fe_m HAP_{im} (1 - PR_{im})] + (1 - \frac{Nominal efficiency\%}{100}) (6.0*10^{-8}) Q_i H_i \sum_{m=1}^{s} [HAP_{im} PR_{im}]$$

(i) The following procedures shall be followed to establish nominal efficiencies. The procedures in <u>paragraphs</u> (i)(1) through (i)(6) of this section shall be followed for control technologies that are different in use or design from the reference control technologies and achieve greater percent reductions than the percent efficiencies assigned to the reference control technologies in § 63.111 of this subpart.

(1) In those cases where the owner or operator is seeking permission to take credit for use of a control technology that is different in use or design from the reference control technology, and the different control technology will be used in more than three applications at a single plant-site, the owner or operator shall submit the information specified in <u>paragraphs</u> (i)(1)(i) through (i)(1)(iv) of this section to the Director of the EPA Office of Air Quality Planning and Standards in writing:

(i) Emission stream characteristics of each emission point to which the control technology is or will be applied including the kind of emission point, flow, organic HAP concentration, and all other stream characteristics necessary to design the control technology or determine its performance.

(ii) Description of the control technology including design specifications.

(iii) Documentation demonstrating to the Administrator's satisfaction the control efficiency of the control technology. This may include performance test data collected using an appropriate EPA method or any other method validated according to Method 301 of <u>appendix A of this part</u>. If it is infeasible to obtain test data, documentation may include a design evaluation

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and calculations. The engineering basis of the calculation procedures and all inputs and assumptions made in the calculations shall be documented.

(iv) A description of the parameter or parameters to be monitored to ensure that the control technology will be operated in conformance with its design and an explanation of the criteria used for selection of that parameter (or parameters).

(2) The Administrator shall determine within 120 calendar days whether an application presents sufficient information to determine nominal efficiency. The Administrator reserves the right to request specific data in addition to the items listed in paragraph (i)(1) of this section.

(3) The Administrator shall determine within 120 calendar days of the submittal of sufficient data whether a control technology shall have a nominal efficiency and the level of that nominal efficiency. If, in the Administrator's judgment, the control technology achieves a level of emission reduction greater than the reference control technology for a particular kind of emission point, the Administrator will publish a Federal Register notice establishing a nominal efficiency for the control technology.

(4) The Administrator may condition permission to take emission credits for use of the control technology on requirements that may be necessary to ensure operation and maintenance to achieve the specified nominal efficiency.

(5) In those cases where the owner or operator is seeking permission to take credit for use of a control technology that is different in use or design from the reference control technology and the different control technology will be used in no more than three applications at a single plant site, the information listed in paragraphs (i)(1)(i) through (i)(1)(iv) can be submitted to the permitting authority for the source for approval instead of the Administrator.

(i) In these instances, use and conditions for use of the control technology can be approved by the permitting authority as part of an operating permit application or modification. The permitting authority shall follow the procedures specified in <u>paragraphs (i)(2)</u> through (i)(4) of this section except that, in these instances, a Federal Register notice is not required to establish the nominal efficiency for the different technology.

(ii) If, in reviewing the application, the permitting authority believes the control technology has broad applicability for use by other sources, the permitting authority shall submit the information provided in the application to the Director of the EPA Office of Air Quality Planning and Standards. The Administrator shall review the technology for broad applicability and may publish a Federal Register notice; however, this review shall not affect the permitting authority's approval of the nominal efficiency of the control technology for the specific application.

(6) If, in reviewing an application for a control technology for an emission point, the Administrator or permitting authority determines the control technology is not different in use or design from the reference control technology, the Administrator or permitting authority shall deny the application.

(j) The following procedures shall be used for calculating the efficiency (percent reduction) of pollution prevention measures:

(1) A pollution prevention measure is any practice which meets the criteria of <u>paragraphs (j)(1)(i)</u> and <u>(j)(1)(ii)</u> of this section.

(i) A pollution prevention measure is any practice that results in a lesser quantity of organic HAP emissions per unit of product released to the atmosphere prior to out-of-process recycling, treatment, or control of emissions, while the same product is produced.

(ii) Pollution prevention measures may include: substitution of feedstocks that reduce HAP emissions; alterations to the production process to reduce the volume of materials released to the environment; equipment modifications; housekeeping measures; and in-process recycling that returns waste materials directly to production as raw materials. Production cutbacks do not qualify as pollution prevention.

(2) The emission reduction efficiency of pollution prevention measures implemented after November 15, 1990, can be used in calculating the actual emissions from an emission point in the debit and credit equations in <u>paragraphs (g)</u> and (<u>h</u>) of this section. When the term "organic HAP" is used in § 63.150(j)(2) in reference to wastewater emission points, the term "table 9 HAP" shall apply for the purposes of this paragraph.

(i) For pollution prevention measures, the percent reduction used in the equations in <u>paragraphs (g)(2)</u> through (g)(5) of this section and <u>paragraphs (h)(2)</u> through (h)(5) of this section is the percent difference between the monthly organic HAP emissions for each emission point after the pollution prevention measure for the most recent month versus monthly emissions

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from the same emission point before the pollution prevention measure, adjusted by the volume of product produced during the two monthly periods.

(ii) The following equation shall be used to calculate the percent reduction of a pollution prevention measure for each emission point.

Percent reduction = 
$$\frac{E_{B} - \frac{(E_{pp} \times P_{B})}{P_{pp}}}{E_{B}} \times 100\%$$

where:

Percent reduction = Efficiency of pollution prevention measure (percent organic HAP reduction).

 $E_B$  = Monthly emissions before the pollution prevention measure, megagrams per month, determined as specified in paragraphs (j)(2)(ii)(A), (j)(2)(ii)(B), and (j)(2)(ii)(C) of this section.

 $E_{pp}$  = Monthly emissions after the pollution prevention measure, megagrams per month, as determined for the most recent month, determined as specified in paragraphs (j)(2)(ii)(D) or (j)(2)(ii)(E) of this section.

 $P_B$  = Monthly production before the pollution prevention measure, megagrams per month, during the same period over which  $E_B$  is calculated.

 $P_{pp}$  = Monthly production after the pollution prevention measure, megagrams per month, as determined for the most recent month.

(A) The monthly emissions before the pollution prevention measure,  $E_B$ , shall be determined in a manner consistent with the equations and procedures in <u>paragraphs (g)(2)</u>, (g)(3), and (g)(4) of this section for process vents, storage vessels, and transfer operations.

(B) For wastewater,  $E_B$  shall be calculated as follows:

$$E_{B} = \sum_{i=1}^{n} \left[ (6.0 * 10^{-8}) Q_{Bi} H_{Bi} \sum_{m=1}^{s} Fe_{m} HAP_{Bim} \right]$$

Where:

n = Number of wastewater streams.

 $Q_{Bi}$  = Average flow rate for wastewater stream i before the pollution prevention measure, defined and determined according to <u>paragraph (g)(5)(i)</u> of this section, liters per minute, before implementation of the pollution prevention measure.

 $H_{Bi}$  = Number of hours per month that wastewater stream i was discharged before the pollution prevention measure, hours per month.

s = Total number of table 9 HAP in wastewater stream i.

 $Fe_m$  = Fraction emitted of table 9 HAP m in wastewater of this subpart, dimensionless.

 $HAP_{Bim}$  = Average concentration of table 9 HAP m in wastewater stream i, defined and determined according to <u>paragraph</u> (<u>g)(5)(i)</u> of this section, before the pollution prevention measure, parts per million by weight, as measured before the implementation of the pollution measure.

(C) If the pollution prevention measure was implemented prior to April 22, 1994, records may be used to determine E<sub>B</sub>.

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(D) The monthly emissions after the pollution prevention measure,  $E_{pp}$ , may be determined during a performance test or by a design evaluation and documented engineering calculations. Once an emissions-to-production ratio has been established, the ratio can be used to estimate monthly emissions from monthly production records.

(E) For wastewater,  $E_{pp}$  shall be calculated using the following equation:

$$E_{pp} = \sum_{i=1}^{n} \left[ (6.0*10^{-8}) Q_{ppi} H_{ppi} \sum_{m=1}^{s} Fe_m HAP_{ppim} \right]$$

where n,  $Q_{ppi}$ ,  $H_{ppi}$ , s,  $Fe_m$ , and  $HAP_{ppim}$  are defined and determined as described in <u>paragraph (j)(2)(ii)(B)</u> of this section except that  $Q_{ppi}$ ,  $H_{ppi}$ , and  $HAP_{ppim}$  shall be determined after the pollution prevention measure has been implemented.

(iii) All equations, calculations, test procedures, test results, and other information used to determine the percent reduction achieved by a pollution prevention measure for each emission point shall be fully documented.

(iv) The same pollution prevention measure may reduce emissions from multiple emission points. In such cases, the percent reduction in emissions for each emission point must be calculated.

(v) For the purposes of the equations in paragraphs (h)(2) through (h)(5) of this section, used to calculate credits for emission points controlled more stringently than the reference control technology, the nominal efficiency of a pollution prevention measure is equivalent to the percent reduction of the pollution prevention measure. When a pollution prevention measure is used, the owner or operator of a source is not required to apply to the Administrator for a nominal efficiency and is not subject to paragraph (i) of this section.

(k) The owner or operator must demonstrate that the emissions from the emission points proposed to be included in the average will not result in greater hazard or, at the option of the operating permit authority, greater risk to human health or the environment than if the emission points were controlled according to the provisions in  $\frac{\&\& 63.113}{\&\& 63.148}$ .

(1) This demonstration of hazard or risk equivalency shall be made to the satisfaction of the operating permit authority.

(i) The Administrator may require owners and operators to use specific methodologies and procedures for making a hazard or risk determination.

(ii) The demonstration and approval of hazard or risk equivalency shall be made according to any guidance that the Administrator makes available for use.

(2) Owners and operators shall provide documentation demonstrating the hazard or risk equivalency of their proposed emissions average in their operating permit application or in their Implementation Plan if an operating permit application has not yet been submitted.

(3) An emissions averaging plan that does not demonstrate hazard or risk equivalency to the satisfaction of the Administrator shall not be approved. The Administrator may require such adjustments to the emissions averaging plan as are necessary in order to ensure that the average will not result in greater hazard or risk to human health or the environment than would result if the emission points were controlled according to  $\frac{\xi\xi}{63.113}$  through  $\frac{63.148}{63.148}$  of this subpart.

(4) A hazard or risk equivalency demonstration must:

(i) Be a quantitative, bona fide chemical hazard or risk assessment;

(ii) Account for differences in chemical hazard or risk to human health or the environment; and

(iii) Meet any requirements set by the Administrator for such demonstrations.

(1) For periods of excursions, an owner or operator may request that the provisions of <u>paragraphs (1)(1)</u> through (1)(4) of this section be followed instead of the procedures in <u>paragraphs (f)(3)(i)</u> and (f)(3)(ii) of this section.

(1) The owner or operator shall notify the Administrator of excursions in the Periodic Reports as required in  $\S$  63.152 of this subpart.

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(2) The owner or operator shall demonstrate that other types of monitoring data or engineering calculations are appropriate to establish that the control device for the emission point was operating in such a fashion to warrant assigning full or partial credits and debits. This demonstration shall be made to the Administrator's satisfaction, and the Administrator may establish procedures of demonstrating compliance that are acceptable.

(3) The owner or operator shall provide documentation of the excursion and the other type of monitoring data or engineering calculations to be used to demonstrate that the control device for the emission point was operating in such a fashion to warrant assigning full or partial credits and debits.

(4) The Administrator may assign full or partial credit and debits upon review of the information provided.

(m) For each Group 1 or Group 2 emission point included in an emissions average, the owner or operator shall perform testing, monitoring, recordkeeping, and reporting equivalent to that required for Group 1 emission points complying with <u>§§</u> <u>63.113</u> through <u>63.148 of this subpart</u>. The specific requirements for process vents, storage vessels, transfer racks, and wastewater are identified in <u>paragraphs (m)(1)</u> through <u>(m)(6)</u> of this section.

(1) The source shall implement the following testing, monitoring, recordkeeping, and reporting procedures for each process vent equipped with a flare, incinerator, boiler, or process heater.

(i) Determine, consistent with <u>paragraph (g)(2)(i)</u> of this section, whether the process vent is Group 1 or Group 2 according to the procedures in  $\frac{63.115}{5}$ .

(ii) Conduct performance tests to determine percent reduction as specified in § 63.116 of this subpart;

(iii) Monitor the operating parameters, keep records, and submit reports specified in  $\S$  63.114,  $\S$  63.117(a), and  $\S$  63.118 (a), (f), and (g) of this subpart, as appropriate for the specific control device.

(2) The source shall implement the following procedures for each process vent equipped with a carbon adsorber, absorber, or condenser but not equipped with a control device:

(i) Except as specified in  $\frac{63.113(a)(4)}{63.113(a)(4)}$ , determine, consistent with paragraph (g)(2)(i) of this section, the flow rate, organic HAP concentration, and TRE index value using the methods specified in  $\frac{63.115}{5}$ ;

(ii) Monitor the operating parameters, keep records, and submit reports specified in § 63.114, § 63.117(a), and § 63.118(b), (f), and (g) of this subpart, as appropriate for the specific recovery device.

(3) The source shall implement the following procedures for each storage vessel controlled with an internal floating roof, external roof, or a closed vent system with a control device, as appropriate to the control technique:

(i) Perform the monitoring or inspection procedures in § 63.120 of this subpart,

(ii) Perform the reporting and recordkeeping procedures in <u>§§ 63.122</u> and <u>63.123 of this subpart</u>, and

(iii) For closed vent systems with control devices, conduct an initial design evaluation and submit an operating plan as specified in  $\S 63.120(d)$  and  $\S 63.122(a)(2)$  and (b) of this subpart.

(4) The source shall implement the following procedures for each transfer rack controlled with a vapor balancing system, or a vapor collection system and an incinerator, flare, boiler, process heater, adsorber, condenser, or absorber, as appropriate to the control technique:

(i) The monitoring and inspection procedures in § 63.127 of this subpart,

(ii) The testing and compliance procedures in § 63.128 of this subpart, and

(iii) The reporting and recordkeeping procedures in  $\S$  63.129 and  $\S$  63.130 of this subpart.

(5) The source shall implement the following procedures for wastewater emission points, as appropriate to the control techniques:

(i) For wastewater treatment processes, conduct tests as specified in § 63.138(j) of this subpart.

(ii) Conduct inspections and monitoring as specified in § 63.143 of this subpart.

(iii) A recordkeeping program as specified in § 63.147 of this subpart.

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(iv) A reporting program as specified in § 63.146 of this subpart.

(6) If an emission point in an emissions average is controlled using a pollution prevention measure or a device or technique for which no monitoring parameters or inspection procedures are specified in § 63.114, § 63.120, § 63.127, or § 63.143 of this subpart, the owner or operator shall submit the information specified in § 63.151(f) of this subpart in the Implementation Plan or operating permit application.

(n) Records of all information required to calculate emission debits and credits shall be retained for five years.

(o) Initial Notifications, Implementation Plans, Notifications of Compliance Status, Periodic Reports, and other reports shall be submitted as required by  $\S 63.151$  and  $\S 63.152$  of this subpart.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>60 FR 63628</u>, Dec. 12, 1995; <u>64 FR 20192</u>, Apr. 26, 1999; <u>66 FR 6934</u>, Jan. 22, 2001; <u>89 FR 43207</u>, May 16, 2024]

## § 63.151 Initial notification.

(a) Each owner or operator of a source subject to this subpart shall submit the reports listed in <u>paragraphs</u> (a)(1) through (a)(5) of this section. Owners or operators requesting an extension of compliance shall also submit the report listed in <u>paragraph (a)(6)</u> of this section.

(1) An Initial Notification described in paragraph (b) of this section, and

(2) An Implementation Plan for new sources subject to this subpart or for emission points to be included in an emissions average, unless an operating permit application has been submitted prior to the date the Implementation Plan is due and the owner or operator has elected to include the information specified in  $\S$  63.152(e) in that application. The submittal date and contents of the Implementation Plan are specified in paragraphs (c) and (d) of this section.

(3) A Notification of Compliance Status described in § 63.152 of this subpart,

(4) Periodic Reports described in § 63.152 of this subpart, and

(5) Other reports described in  $\S$  63.152 of this subpart.

(6) Pursuant to section 112(i)(3)(B) of the Act, an owner or operator may request an extension allowing the existing source up to 1 additional year to comply with section 112(d) standards.

(i) For purposes of this subpart, a request for an extension shall be submitted to the permitting authority as part of the operating permit application or as part of the Initial Notification or as a separate submittal. Requests for extensions shall be submitted no later than 120 days prior to the compliance dates specified in  $\S 63.100(k)(2)$ ,  $\S 63.100(1)(4)$ , and  $\S 63.100(m)$  of subpart F of this part, except as provided for in paragraph (a)(6)(iv) of this section. The dates specified in  $\S 63.6(i)$  of subpart A of this part for submittal of requests for extensions shall not apply to sources subject to this subpart G.

(ii) A request for an extension of compliance must include the data described in  $\S$  <u>63.6(i)(6)(i) (A)</u>, <u>(B)</u>, and <u>(D)</u> of <u>subpart A</u> <u>of this part</u>.

(iii) The requirements in  $\S$  63.6(i)(8) through (i)(14) of subpart A will govern the review and approval of requests for extensions of compliance with this subpart.

(iv) An owner or operator may submit a compliance extension request after the date specified in paragraph (a)(6)(i) of this section provided the need for the compliance extension arose after that date and before the otherwise applicable compliance date, and the need arose due to circumstances beyond reasonable control of the owner or operator. This request shall include, in addition to the information in paragraph (a)(6)(ii) of this section, a statement of the reasons additional time is needed and the date when the owner or operator first learned of the problem.

(7) The reporting requirements for storage vessels are located in  $\S$  63.122 of this subpart.

(b) Each owner or operator of an existing or new source subject to subpart G shall submit a written Initial Notification to the Administrator, containing the information described in <u>paragraph (b)(1)</u> of this section, according to the schedule in <u>paragraph (b)(2)</u> of this section. The Initial Notification provisions in § 63.9(b)(2), (b)(3), and (b)(6) of subpart A shall not apply to owners or operators of sources subject to subpart G.

(1) The Initial Notification shall include the following information:

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(i) The name and address of the owner or operator;

(ii) The address (physical location) of the affected source;

(iii) An identification of the kinds of emission points within the source that are subject to this subpart;

(iv) An identification of the chemical manufacturing processes subject to subpart G; and

(v) A statement of whether the source can achieve compliance by the relevant compliance date specified in  $\S$  63.100 of subpart F.

(2) The Initial Notification shall be submitted according to the schedule in <u>paragraph (b)(2)(i)</u>, (b)(2)(ii), or (b)(2)(iii) of this section, as applicable.

(i) For an existing source, the Initial Notification shall be submitted within 120 calendar days after the date of promulgation, or no later than 120 days after the source becomes subject to this subpart, whichever is later.

(ii) For a new source that has an initial start-up 90 calendar days after the date of promulgation of this subpart or later, the application for approval of construction or reconstruction required by  $\S$  <u>63.5(d)</u> of subpart A shall be submitted in lieu of the Initial Notification. The application shall be submitted as soon as practicable before construction or reconstruction is planned to commence (but it need not be sooner than 90 calendar days after the date of promulgation of this subpart). For a new source that reclassifies to major source status after January 19, 2021 and greater than 90 days after the initial start-up, the source shall submit the initial notification required by  $\S$  <u>63.9(b)</u> no later than 120 days after the source becomes subject to this subpart.

(iii) For a new source that has an initial start-up prior to 90 calendar days after the date of promulgation, the Initial Notification shall be submitted within 90 calendar days after the date of promulgation of this subpart, or no later than 120 days after the source becomes subject to this subpart, whichever is later. The application for approval of construction or reconstruction described in  $\S 63.5(d)$  of subpart A is not required for these sources.

(c) Each owner or operator of an existing source with emission points that will be included in an emissions average or new source subject to this subpart must submit an Implementation Plan to the Administrator by the dates specified in <u>paragraphs</u> (c)(1) and (c)(2) of this section, unless an operating permit application accompanied by the information specified in § 63.152(e) of this subpart has been submitted. The Implementation Plan for emissions averaging is subject to Administrator approval.

(1) Each owner or operator of an existing source subject to this subpart who elects to comply with § 63.112 of this subpart by using emissions averaging for any emission points, and who has not submitted an operating permit application accompanied by the information specified in § 63.152(e) of this subpart at least 18 months prior to the compliance dates specified in § 63.100 of subpart F of this part, shall develop an Implementation Plan for emissions averaging. For existing sources, the Implementation Plan for those emission points to be included in an emissions average shall be submitted no later than 18 months prior to the compliance dates in § 63.100 of subpart F of this part.

(2) Each owner or operator of a new source shall submit an Implementation Plan by the date specified in <u>paragraphs</u> (c)(2)(i) or (c)(2)(i) of this section, as applicable, unless an operating permit application containing the information in <u>paragraph (e)</u> of this section has been submitted by that date.

(i) For a new source that has an initial start-up 90 calendar days after the date of promulgation of this subpart or later, the Implementation Plan shall be submitted with the application for approval of construction or reconstruction by the date specified in paragraph (b)(2)(ii) of this section.

(ii) For a new source that has an initial start-up prior to 90 calendar days after the date of promulgation, the Implementation Plan shall be submitted within 90 calendar days after the date of promulgation of this subpart.

(3) The Administrator shall determine within 120 calendar days whether the Implementation Plan submitted by sources using emissions averaging presents sufficient information. The Administrator shall either approve the Implementation Plan, request changes, or request that the owner or operator submit additional information. Once the Administrator receives sufficient information, the Administrator shall approve, disapprove, or request changes to the plan within 120 calendar days.

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(d) Each owner or operator required to submit an Implementation Plan for emissions averaging shall include in the plan, for all emission points included in the emissions average, the information listed in <u>paragraphs (d)(1)</u> through  $(\underline{d})(\underline{8})$  of this section.

(1) The identification of all emission points in the planned emissions average and notation of whether each point is a Group 1 or Group 2 emission point as defined in § 63.111 of this subpart.

(2) The projected emission debits and credits for each emission point and the sum for the emission points involved in the average calculated according to  $\S 63.150$  of this subpart. The projected credits must be greater than the projected debits, as required under  $\S 63.150(e)(3)$  of this subpart.

(3) The specific control technology or pollution prevention measure that will be used for each emission point included in the average and date of application or expected date of application.

(5) A statement that the compliance demonstration, monitoring, inspection, recordkeeping, and reporting provisions in  $\S$  <u>63.150(m)</u>, (n), and (o) of this subpart that are applicable to each emission point in the emissions average will be implemented beginning on the date of compliance.

(6) Documentation of the information listed in <u>paragraph (d)(6)(i)</u> through  $(\underline{d})(\underline{6})(\underline{v})$  of this section for each process vent, storage vessel, or transfer rack included in the average.

(i) The values of the parameters used to determine whether the emission point is Group 1 or Group 2. Except as specified in  $\S$  <u>63.113(a)(4)</u>, where TRE index value is used for process vent group determination, the estimated or measured values of the parameters used in the TRE equation in  $\S$  <u>63.115(d)</u> (flow rate, organic HAP emission rate, TOC emission rate, and net heating value) and the resulting TRE index value shall be submitted.

(ii) The estimated values of all parameters needed for input to the emission debit and credit calculations in § 63.150 (g) and (h) of this subpart. These parameter values, or as appropriate, limited ranges for the parameter values, shall be specified in the source's Implementation Plan (or operating permit) as enforceable operating conditions. Changes to these parameters must be reported as required by paragraph (i)(2)(ii) of this section.

(iii) The estimated percent reduction if a control technology achieving a lower percent reduction than the efficiency of the reference control technology, as defined in  $\S$  63.111 of this subpart, is or will be applied to the emission point.

(iv) The anticipated nominal efficiency if a control technology achieving a greater percent emission reduction than the efficiency of the reference control technology is or will be applied to the emission point. The procedures in  $\S 63.150(i)$  of this subpart shall be followed to apply for a nominal efficiency.

(v) The operating plan required in  $\frac{63.122(a)(2)}{(2)}$  and  $\frac{(b)}{(b)}$  for each storage vessel controlled with a closed vent system with a control device other than a flare.

(7) The information specified in  $\S$  63.151(f) of this subpart shall be included in the Implementation Plan for:

(i) Each process vent or transfer rack controlled by a pollution prevention measure or control technique for which monitoring parameters or inspection procedures are not specified in § 63.114, § 63.126(b)(3), or § 63.127 of this subpart, and

(ii) Each storage vessel controlled by pollution prevention or a control technique other than an internal or external floating roof or a closed vent system with a control device.

(8) Documentation of the information listed in paragraph (d)(8)(i) through (d)(8)(iv) for each process wastewater stream included in the average.

(i) The information used to determine whether the wastewater stream is a Group 1 or Group 2 wastewater stream.

(ii) The estimated values of all parameters needed for input to the wastewater emission credit and debit calculations in § 63.150 (g)(5) and (h)(5) of this subpart.

(iii) The estimated percent reduction if:

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(A) A control technology that achieves an emission reduction less than or equal to the emission reduction achieved by the design steam stripper, as specified in  $\S$  63.138(g) of this subpart, is or will be applied to the wastewater stream, or

(B) A control technology achieving less than or equal to 95 percent emission reduction is or will be applied to the vapor stream(s) vented and collected from the treatment processes, or

(C) A pollution prevention measure is or will be applied.

(iv) The anticipated nominal efficiency if the owner or operator plans to apply for a nominal efficiency under  $\frac{63.150(i)}{100}$  of this subpart. A nominal efficiency shall be applied for if:

(A) A control technology is or will be applied to the wastewater stream and achieves an emission reduction greater than the emission reduction achieved by the design steam stripper as specified in  $\frac{\& 63.138(g) \text{ of this subpart}}{(g) \text{ of this subpart}}$ , or

(B) A control technology achieving greater than 95 percent emission reduction is or will be applied to the vapor stream(s) vented and collected from the treatment processes.

(v) For each pollution prevention measure, treatment process, or control device used to reduce air emissions of organic HAP's from wastewater and for which no monitoring parameters or inspection procedures are specified in  $\S$  63.143 of this subpart, the information specified in  $\S$  63.151(f) of this subpart shall be included in the Implementation Plan.

(e) An owner or operator expressly referred to this paragraph shall report, in an Implementation Plan, operating permit application, or as otherwise specified by the permitting authority, the information listed in <u>paragraphs (e)(1)</u> through (e)(5) of this section.

(1) A list designating each emission point complying with  $\frac{\$\$ 63.113}{10}$  through  $\frac{63.149}{100}$  and whether each emission point is Group 1 or Group 2, as defined in  $\frac{\$ 63.111}{100}$ . For each process vent within the source, provide the information listed in paragraphs (e)(1)(i) through (iv) of this section.

(i) The chemical manufacturing process unit(s) that is the origin of all or part of the vent stream that exits the process vent.

(ii) The type(s) of unit operations (i.e., an air oxidation reactor, distillation unit, or reactor) that creates the vent stream that exits the process vent.

(iii) For a Group 2 process vent, the last recovery device, if any.

(iv) For a Group 1 process vent, the control device, or other equipment used for compliance.

(2) The control technology or method of compliance that will be applied to each Group 1 emission point.

(3) A statement that the compliance demonstration, monitoring, inspection, recordkeeping, and reporting provisions in  $\frac{\$\$}{63.113}$  through  $\frac{63.149 \text{ of this subpart}}{63.113}$  that are applicable to each emission point will be implemented beginning on the date of compliance.

(4) The operating plan required in  $\S$  63.122(a)(2) and (b) of this subpart for each storage vessel controlled with a closed vent system with a control device other than a flare.

(5) The monitoring information in § 63.151(f) of this subpart if, for any emission point, the owner or operator of a source seeks to comply through use of a control technique other than those for which monitoring parameters are specified in § 63.114 for process vents, § 63.127 for transfer, and § 63.143 for process wastewater.

(f) The owner or operator who has been directed by any section of this subpart that expressly references this paragraph to set unique monitoring parameters or who requests approval to monitor a different parameter than those listed in  $\frac{63.114}{5}$  for process vents,  $\frac{63.127}{5}$  for transfer, or  $\frac{63.143}{5}$  for process wastewater of this subpart shall submit the information specified in paragraphs (f)(1), (f)(2), and (f)(3) of this section with the operating permit application or as otherwise specified by the permitting authority.

(1) A description of the parameter(s) to be monitored to ensure the control technology or pollution prevention measure is operated in conformance with its design and achieves the specified emission limit, percent reduction, or nominal efficiency, and an explanation of the criteria used to select the parameter(s).

(2) A description of the methods and procedures that will be used to demonstrate that the parameter indicates proper operation of the control device, the schedule for this demonstration, and a statement that the owner or operator will establish

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a range for the monitored parameter as part of the Notification of Compliance Status report required in  $\S 63.152(b)$  of this subpart, unless this information has already been included in the operating permit application.

(3) The frequency and content of monitoring, recording, and reporting if monitoring and recording is not continuous, or if reports of daily average values when the monitored parameter value is outside the range established in the operating permit or Notification of Compliance Status will not be included in Periodic Reports required under § 63.152(c) of this subpart. The rationale for the proposed monitoring, recording, and reporting system shall be included.

(g) An owner or operator may request approval to use alternatives to the continuous operating parameter monitoring and recordkeeping provisions listed in <u>§§ 63.114</u>, <u>63.117</u>, and <u>63.118</u> for process vents, <u>§§ 63.127</u>, <u>63.129</u>, and <u>63.130</u> for transfer operations, and <u>§§ 63.143</u>, <u>63.146</u>, and <u>63.147</u> for wastewater.

(1) Requests shall be included in the operating permit application or as otherwise specified by the permitting authority and shall contain the information specified in paragraphs (g)(3) through (g)(5) of this section, as applicable.

(2) The provisions in  $\S 63.8(f)(5)(i)$  of subpart A shall govern the review and approval of requests.

(3) An owner or operator of a source that does not have an automated monitoring and recording system capable of measuring parameter values at least once every 15 minutes and generating continuous records may request approval to use a non-automated system with less frequent monitoring.

(i) The requested system shall include manual reading and recording of the value of the relevant operating parameter no less frequently than once per hour. Daily average values shall be calculated from these hourly values and recorded.

(ii) The request shall contain:

(A) A description of the planned monitoring and recordkeeping system;

(B) Documentation that the source does not have an automated monitoring and recording system;

(C) Justification for requesting an alternative monitoring and recordkeeping system; and

(D) Demonstration to the Administrator's satisfaction that the proposed monitoring frequency is sufficient to represent control device operating conditions considering typical variability of the specific process and control device operating parameter being monitored.

(4) An owner or operator may request approval to use an automated data compression recording system that does not record monitored operating parameter values at a set frequency (for example once every 15 minutes) but records all values that meet set criteria for variation from previously recorded values.

(i) The requested system shall be designed to:

(A) Measure the operating parameter value at least once every 15 minutes.

(B) Record at least four values each hour during periods of operation.

(C) Record the date and time when monitors are turned off or on.

(D) Recognize unchanging data that may indicate the monitor is not functioning properly, alert the operator, and record the incident.

(E) Compute daily average values of the monitored operating parameter based on recorded data.

(F) If the daily average is not an excursion, as defined in  $\frac{63.152(c)(2)(ii)}{1000}$ , the data for that operating day may be converted to hourly average values and the four or more individual records for each hour in the operating day may be discarded.

(ii) The request shall contain a description of the monitoring system and data compression recording system, including the criteria used to determine which monitored values are recorded and retained, the method for calculating daily averages, and a demonstration that the system meets all criteria in paragraph (g)(4)(i) of this section.

(5) An owner or operator may request approval to use other alternative monitoring systems according to the procedures specified in  $\S$  63.8(f) of subpart A of this part.

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(h) The owner or operator required to prepare an Implementation Plan, or otherwise required to submit a report, under <u>paragraph (c), (d)</u>, or <u>(e)</u> of this section shall also submit a supplement for any additional alternative controls or operating scenarios that may be used to achieve compliance.

(i) The owner or operator of a source required to submit an Implementation Plan for emissions averaging under <u>paragraphs</u> (c) and (d) of this section shall also submit written updates of the Implementation Plan to the Administrator for approval under the circumstances described in <u>paragraphs (i)(1)</u> and (i)(2) of this section unless the relevant information has been included and submitted in an operating permit application or amendment.

(1) The owner or operator who plans to make a change listed in <u>paragraph (i)(1)(i)</u> or <u>(i)(1)(ii)</u> of this section shall submit an Implementation Plan update at least 120 calendar days prior to making the change.

(i) Whenever an owner or operator elects to achieve compliance with the emissions averaging provisions in  $\S$  63.150 of this subpart by using a control technique other than that specified in the Implementation Plan or plans to monitor a different parameter or operate a control device in a manner other than that specified in the Implementation Plan.

(ii) Whenever an emission point or a chemical manufacturing process unit is added to an existing source and is planned to be included in an emissions average, or whenever an emission point not included in the emissions average described in the Implementation Plan is to be added to an emissions average. The information in <u>paragraph (d)</u> of this section shall be updated to include the additional emission point.

(2) The owner or operator who has made a change listed in <u>paragraph (i)(2)(i)</u> or <u>(i)(2)(ii)</u> of this section shall submit an Implementation Plan update within 90 calendar days after the information regarding the change is known to the source. The update may be submitted in the next quarterly Periodic Report if the change is made after the date the Notification of Compliance status is due.

(i) Whenever a process change is made such that the group status of any emission point in an emissions average changes.

(ii) Whenever a value of a parameter in the emission credit or debit equations in  $\frac{63.150(g)}{10}$  or (h) changes such that it is outside the range specified in the Implementation Plan and causes a decrease in the projected credits or an increase in the projected debits.

(3) The Administrator shall approve or request changes to the Implementation Plan update within 120 calendar days of receipt of sufficient information regarding the change for emission points included in emissions averages.

(j) The owner or operator of a source subject to this subpart, for emission points that are not included in an emissions average, shall report to the Administrator under the circumstances described in <u>paragraphs (j)(1), (j)(2)</u>, and (j)(3) of this section unless the relevant information has been included and submitted in an operating permit application or amendment, or as otherwise specified by the permitting authority. The information shall be submitted within 180 calendar days after the change is made or the information regarding the change is known to the source. The update may be submitted in the next Periodic Report if the change is made after the date the Notification of Compliance Status is due.

(1) Whenever a deliberate change is made such that the group status of any emission point changes. The information submitted shall include a compliance schedule as specified in  $\S$  63.100 of subpart F of this part if the emission point becomes Group 1.

(2) Whenever an owner or operator elects to achieve compliance with this subpart by using a control technique other than that previously reported to the Administrator or to the permitting authority, or plans to monitor a different parameter, or operate a control device in a manner other than that previously reported.

(3) Whenever an emission point or a chemical manufacturing process unit is added to a source, written information specified under <u>paragraphs (e)(1)</u> through (e)(5) of this section, containing information on the new emission point(s) shall be submitted to the EPA regional office where the source is located.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>60 FR 63628</u>, Dec. 12, 1995; <u>61 FR 7718</u>, Feb. 29, 1996; <u>61 FR 64576</u>, Dec. 5, 1996; <u>64 FR 20195</u>, Apr. 26, 1999; <u>66 FR 6934</u>, Jan. 22, 2001; <u>85 FR 73887</u>, Nov. 19, 2020; <u>89 FR 43208</u>, May 16, 2024]

# § 63.152 General reporting and continuous records.

(a) The owner or operator of a source subject to this subpart shall submit the reports listed in <u>paragraphs</u> (a)(1) through (a)(5) of this section and keep continuous records of monitored parameters as specified in <u>paragraph (f)</u> of this

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section. Owners or operators requesting an extension of compliance shall also submit the report described in  $\frac{63.151(a)(6)}{60}$  of this subpart.

(1) An Initial Notification described in § 63.151(b) of this subpart.

(2) An Implementation Plan described in § 63.151(c), (d), and (e) of this subpart for existing sources with emission points that are included in an emissions average or for new sources.

(3) A Notification of Compliance Status described in <u>paragraph (b)</u> of this section.

(4) Periodic Reports described in paragraph (c) of this section.

(5) Other reports described in <u>paragraphs (d)</u> and <u>(e)</u> of this section.

(b) Each owner or operator of a source subject to this subpart shall submit a Notification of Compliance Status within 150 calendar days after the compliance dates specified in  $\frac{863.100}{5}$  of subpart F of this part.

(1) The notification shall include the results of any emission point group determinations, performance tests, inspections, continuous monitoring system performance evaluations, values of monitored parameters established during performance tests, and any other information used to demonstrate compliance or required to be included in the Notification of Compliance Status under  $\S 63.110$  (h) for regulatory overlaps, under  $\S 63.117$  for process vents,  $\S 63.122$  for storage vessels,  $\S 63.129$  for transfer operations,  $\S 63.146$  for process wastewater, and  $\S 63.150$  for emission points included in an emissions average.

(i) For performance tests and group determinations that are based on measurements, the Notification of Compliance Status shall include one complete test report for each test method used for a particular kind of emission point. For additional tests performed for the same kind of emission point using the same method, the results and any other information required in  $\S$  <u>63.117</u> for process vents,  $\S$  <u>63.129</u> for transfer, and  $\S$  <u>63.146</u> for process wastewater shall be submitted, but a complete test report is not required. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with <u>paragraph (h)</u> of this section, the process unit(s) tested, the pollutant(s) tested, and the date that such performance test results. The performance test results must be submitted to CEDRI by the date the notification of compliance status report is submitted.

(ii) A complete test report shall include a brief process description, sampling site description, description of sampling and analysis procedures and any modifications to standard procedures, quality assurance procedures, record of operating conditions during the test, record of preparation of standards, record of calibrations, raw data sheets for field sampling, raw data sheets for field and laboratory analyses, documentation of calculations, and any other information required by the test method.

(2) For each monitored parameter for which a range is required to be established under  $\frac{\$ 63.114}{10}$  for process vents,  $\frac{\$}{63.127}$  for transfer,  $\frac{\$ 63.143}{10}$  for process wastewater,  $\frac{\$ 63.150(m)}{100}$  for emission points in emissions averages, or  $\frac{\$ 63.151(f)}{100}$ , or  $\frac{\$ 63.152(e)}{100}$ , the Notification of Compliance Status shall include the information in paragraphs (b)(2)(i), (b)(2)(ii), and (b)(2)(iii) of this section, unless the range and the operating day definition have been established in the operating permit. The recordkeeping and reporting requirements applicable to storage vessels are located in  $\frac{\$ \$ 63.122}{\$ \$ 63.122}$  and  $\frac{63.123}{\$ 123}$ .

(i) The specific range of the monitored parameter(s) for each emission point;

(ii) The rationale for the specific range for each parameter for each emission point, including any data and calculations used to develop the range and a description of why the range indicates proper operation of the control device.

(A) If a performance test is required by this subpart for a control device, the range shall be based on the parameter values measured during the performance test and may be supplemented by engineering assessments and/or manufacturer's recommendations. Performance testing is not required to be conducted over the entire range of permitted parameter values.

(B) If a performance test is not required by this subpart for a control device, the range may be based solely on engineering assessments and/or manufacturer's recommendations.

(iii) A definition of the source's operating day for purposes of determining daily average values of monitored parameters. The definition shall specify the times at which an operating day begins and ends.

(3) For emission points included in an emissions average, the Notification of Compliance Status shall include the values of all parameters needed for input to the emission credit and debit equations in  $\frac{\& 63.150 (g)}{\& 63.150 (g)}$  and (h), calculated or measured

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according to the procedures in  $\S$  63.150 (g) and (h) of this subpart, and the resulting calculation of credits and debits for the first quarter of the year. The first quarter begins on the compliance date specified in  $\S$  63.100 of subpart F.

(4) If any emission point is subject to this subpart and to other standards as specified in § 63.110 of this subpart and if the provisions of § 63.110 of this subpart allow the owner or operator to choose which testing, monitoring, reporting, and recordkeeping provisions will be followed, then the Notification of Compliance Status shall indicate which rule's requirements will be followed for testing, monitoring, reporting, and recordkeeping.

(5) An owner or operator who transfers a Group 1 wastewater stream or residual removed from a Group 1 wastewater stream for treatment pursuant to  $\frac{63.132(g)}{100}$  shall include in the Notification of Compliance Status the name and location of the transferee and a description of the Group 1 wastewater stream or residual sent to the treatment facility.

(6) An owner or operator complying with  $\S$  63.113(i) shall include in the Notification of Compliance Status, or where applicable, a supplement to the Notification of Compliance Status, the name and location of the transferee, and the identification of the Group 1 process vent.

(7) For flares subject to the requirements in  $\S$  63.108, owners and operators must also submit the information in this paragraph in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date for flare monitoring. The supplement to the Notification of Compliance Status must include flare design (*e.g.*, steam-assisted, air-assisted, non-assisted, or pressure-assisted multi-point); all visible emission readings, heat content determinations, flow rate measurements, and exit velocity determinations made during the initial visible emissions demonstration required by  $\S$  63.670(h) of subpart CC of this part, as applicable; and all periods during the compliance determination when the pilot flame or flare flame is absent.

(8) For process vents and storage vessels subject to the requirements of  $\frac{63.124}{2}$ , owners and operators must also submit the information in this paragraph in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date. The supplement to the Notification of Compliance Status must identify all process vents and storage vessels that are in ethylene oxide service as defined in  $\frac{63.101}{2}$ , the method(s) used to control ethylene oxide emissions from each process vent and storage vessel (*i.e.*, use of a flare, scrubber, or other control device) and the information specified in paragraphs (b)(8)(i) and (b)(8)(ii) of this section, as applicable.

(i) For process vents, all uncontrolled, undiluted ethylene oxide concentration measurements, and the calculations used to determine the total uncontrolled ethylene oxide mass emission rate for the sum of all vent gas streams; and

(ii) For storage vessels, include the concentration of ethylene oxide of the fluid stored in each storage vessel.

(9) For adsorbers subject to the requirements of  $\frac{\&\& 63.114(a)(5)(v)}{(b)(2)(a)}$ ,  $\frac{63.120(d)(1)(iii)}{(b)(2)(a)}$ , and  $\frac{63.139(d)(5)}{(b)(2)(a)}$ , you must also submit the information listed in paragraphs (b)(9)(i) and (ii) of this section in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date.

(i) Whether the adsorber cannot be regenerated or is a regenerative adsorber(s) that is regenerated offsite.

(ii) The breakthrough limit and adsorber bed life established during the initial performance test or design evaluation of the adsorber.

(10) For Group 2 process vents subject to the requirements in § 63.113(1), owners and operators must also submit the information in this paragraph in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date. The supplement to the Notification of Compliance Status must identify each Group 2 process vent and include the data and calculations specified in § 63.115(g) that are used to demonstrate that the total organic HAP mass flow rate of each vent stream is less than 1.0 pound per hour.

(c) The owner or operator of a source subject to this subpart shall submit Periodic Reports. On and after July 15, 2027 or once the reporting template for this subpart has been available on the CEDRI website for 1 year, whichever date is later, owners and operators must submit all subsequent reports following the procedure specified in  $\S 63.9(k)$ , except any medium submitted through mail must be sent to the attention of the Hazardous Organic Chemical Manufacturing Sector Lead. Owners and operators must use the appropriate electronic report template on the CEDRI website (<u>https://www.epa.gov/electronic-reporting-air-emissions/cedri</u>) for this subpart. The date report templates become available will be listed on the CEDRI website. Unless the Administrator or delegated state agency or other authority has approved a different schedule for submission of reports under  $\S 63.9(i)$  and  $\S 63.10(a)$ , the report must be submitted by the deadline specified in this subpart, regardless of the method in which the report is submitted.
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(1) Except as specified under paragraphs (c)(5) and (c)(6) of this section, a report containing the information in paragraphs (c)(2), (c)(3), (c)(4), and (c)(7) of this section shall be submitted semiannually no later than 60 calendar days after the end of each 6-month period. The first report shall be submitted no later than 8 months after the date the Notification of Compliance Status is due and shall cover the 6-month period beginning on the date the Notification of Compliance Status is due. All periodic reports must contain the company name and address (including county), as well as the beginning and ending dates of the reporting period.

(2) Except as provided in paragraph (c)(2)(iv) of this section, for an owner or operator of a source complying with the provisions of  $\frac{\$}{\$} \frac{63.113}{63.113}$  through  $\frac{63.147}{63.122}$  for any emission points, Periodic Reports shall include all information specified in  $\frac{\$}{\$} \frac{63.117}{63.146}$  for process vents,  $\frac{\$}{\$} \frac{63.122}{63.122}$  for storage vessels,  $\frac{\$}{\$} \frac{63.129}{63.129}$  and  $\frac{63.130}{63.130}$  for transfer operations, and  $\frac{\$}{\$} \frac{63.146}{63.146}$  for process wastewater, including reports of each excursion (*i.e.*, each period when a monitored parameter is outside the established range and periods of insufficient monitoring data) using the procedures described in paragraphs (c)(2)(iv) of this section.

(i) Report the affected sources or equipment, the monitored parameter that was exceeded and the date of each excursion.

(ii) The parameter monitoring data for Group 1 emission points and emission points included in emissions averages that are required to perform continuous monitoring shall be used to determine compliance with the required operating conditions for the monitored control devices or recovery devices. For each excursion as specified in <u>paragraphs</u> (c)(2)(ii)(A) through (c)(2)(ii)(E) of this section, or <u>paragraph (g)(2)(iv)</u> of this section, except for excused excursions described therein, the owner or operator shall be deemed to have failed to have applied the control in a manner that achieves the required operating conditions and must report the information specified in <u>paragraph (c)(2)(ii)(F)</u> of this section.

(A) An excursion means any of the three cases listed in <u>paragraph (c)(2)(ii)(A)(1), (c)(2)(ii)(A)(2)</u>, or (c)(2)(ii)(A)(3) of this section. For a control device or recovery device where multiple parameters are monitored, if one or more of the parameters meets the excursion criteria in <u>paragraph (c)(2)(ii)(A)(1), (c)(2)(ii)(A)(2)</u>, or (c)(2)(ii)(A)(3) of this section, this is considered a single excursion for the control device or recovery device.

(1) When the daily average value of one or more monitored parameters is outside the permitted range.

(2) When the period of control device or recovery device operation is 4 hours or greater in an operating day and monitoring data are insufficient to constitute a valid hour of data for at least 75 percent of the operating hours.

(3) When the period of control device or recovery device operation is less than 4 hours in an operating day and more than one of the hours during the period of operation does not constitute a valid hour of data due to insufficient monitoring data.

(4) Monitoring data are insufficient to constitute a valid hour of data, as used in <u>paragraphs</u>

(c)(2)(ii)(A)(2) and (c)(2)(ii)(A)(3) of this section, if measured values are unavailable for any of the 15-minute periods within the hour. For data compression systems approved under § 63.151(g)(4), monitoring data are insufficient to calculate a valid hour of data if there are less than 4 data values recorded during the hour.

(B) The number of excused excursions for each control device or recovery device for each semiannual period is specified in <u>paragraphs (c)(2)(ii)(B)(1)</u> through (c)(2)(ii)(B)(6) of this section. This paragraph applies to sources required to submit Periodic Reports semiannually or quarterly. The first semiannual period is the 6-month period starting the date the Notification of Compliance Status is due.

- (1) For the first semiannual period—six excused excursions.
- (2) For the second semiannual period-five excused excursions.
- (3) For the third semiannual period—four excused excursions.
- (4) For the fourth semiannual period—three excused excursions.
- (5) For the fifth semiannual period—two excused excursions.
- (6) For the sixth and all subsequent semiannual periods—one excused excursion.

(C) A monitored parameter that is outside its established range or monitoring data that are not collected are excursions. However, if the conditions in <u>paragraph (c)(2)(ii)(C)(1)</u> or (c)(2)(ii)(C)(2) of this section are met, these excursions are not violations and do not count toward the number of excused excursions for determining compliance.

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(1) Periods of startup, shutdown, or malfunction. During periods of startup, shutdown, or malfunction when the source is operated during such periods in accordance with  $\frac{63.102(a)(4)}{2027}$ . For each source as defined in  $\frac{63.101}{2027}$ , on and after July 15, 2027, this paragraph no longer applies.

(2) *Periods of nonoperation*. During periods of nonoperation of the chemical manufacturing process unit, or portion thereof, that results in cessation of the emissions to which the monitoring applies.

(D) Nothing in <u>paragraph (c)(2)(ii)</u> of this section shall be construed to allow or excuse a monitoring parameter excursion caused by any activity that violates other applicable provisions of <u>subpart A</u>, <u>F</u>, or <u>G of this part</u>.

(E) <u>Paragraph (c)(2)(ii)</u> of this section, except <u>paragraph (c)(2)(ii)(C)</u> of this section, shall apply only to emission points and control devices or recovery devices for which continuous monitoring is required by <u>\$</u> 63.113 through 63.150.

(F) For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), for each excursion that is not an excused excursion, the report must include a list of the affected sources or equipment, the monitored parameter for which there was an excursion, the date of the excursion, an estimate of the quantity in pounds of each regulated pollutant emitted over any emission limit, a description of the method used to estimate the emissions, the cause of the excursion (including unknown cause, if applicable), as applicable, and the corrective action taken.

(iii) Periodic Reports shall include the daily average values of monitored parameters for both excused and unexcused excursions, as defined in <u>paragraph (c)(2)(ii)(A)</u> of this section. For excursions caused by lack of monitoring data, the affected equipment or source, the monitored parameter, the start date and duration in hours of periods when monitoring data were not collected shall be specified.

(iv) The provisions of <u>paragraphs (c)(2)</u> of this section, and (c)(2)(i) through (iii) of this section, do not apply to any storage vessel for which the owner or operator is not required, by the applicable monitoring plan established under § 63.120(d)(2), to keep continuous records. If continuous records are required, the owner or operator shall specify, in the monitoring plan, whether the provisions of <u>paragraphs (c)(2)</u> of this section, and (c)(2)(i) through (iii) of this section apply.

(3) Except as specified in <u>paragraph (c)(3)(iii)</u> of this section, if any performance tests are reported in a Periodic Report, the following information shall be included:

(i) One complete test report shall be submitted for each test method used for a particular kind of emission point tested. A complete test report shall contain the information specified in paragraph (b)(1)(ii) of this section.

(ii) For additional tests performed for the same kind of emission point using the same method, results and any other information required in  $\S 63.117$  for process vents,  $\S 63.129$  for transfer, and  $\S 63.146$  for process wastewater shall be submitted, but a complete test report is not required.

(iii) If the performance test report is submitted electronically through the EPA's CEDRI in accordance with <u>paragraph (h)</u> of this section, the process unit(s) tested, the pollutant(s) tested, and the date that such performance test was conducted may be submitted in the Periodic Report in lieu of the performance test results. The performance test results must be submitted to CEDRI by the date the Periodic Report is submitted.

(4) Periodic Reports shall include the information in paragraphs (c)(4)(i) through (iv) of this section, as applicable:

(i) For process vents, reports of process changes as required under § 63.118(g), (h), (i), and (j),

(ii) Any supplements required under § 63.151(i) and (j),

(iii) Notification if any Group 2 emission point becomes a Group 1 emission point, including a compliance schedule as required in  $\S$  63.100, and

(iv) For gas streams sent for disposal pursuant to  $\frac{63.113(i)}{10}$  or for process wastewater streams sent for treatment pursuant to  $\frac{63.132(g)}{10}$ , reports of changes in the identity of the transferee.

(5) The owner or operator of a source shall submit quarterly reports for all emission points included in an emissions average.

(i) The quarterly reports shall be submitted no later than 60 calendar days after the end of each quarter. The first report shall be submitted with the Notification of Compliance Status no later than 5 months after the compliance date specified in  $\frac{63.100}{5}$ .

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(ii) The quarterly reports shall include the information specified in this paragraph for all emission points included in an emissions average.

(A) The credits and debits calculated each month during the quarter;

(B) A demonstration that debits calculated for the quarter are not more than 1.30 times the credits calculated for the quarter, as required under  $\frac{63.150(e)(4)}{2}$ .

(C) The values of any inputs to the credit and debit equations in  $\S 63.150(g)$  and (h) that change from month to month during the quarter or that have changed since the previous quarter;

(D) Results of any performance tests conducted during the reporting period including one complete report for each test method used for a particular kind of emission point as described in paragraph (c)(3) of this section. If the performance test report is submitted electronically through the EPA's CEDRI in accordance with paragraph (h) of this section, the process unit(s) tested, the pollutant(s) tested, and the date that such performance test results must be submitted to CEDRI by the date the Periodic Report is submitted.;

(E) Reports of daily average values of monitored parameters for both excused and unexcused excursions as defined in paragraph (c)(2)(ii)(A) of this section. For excursions caused by lack of monitoring data, the duration of periods when monitoring data were not collected shall be specified. Include the affected sources or equipment, monitored parameter, and the date for each excursion.

(iii) <u>Paragraphs (c)(2)(i)</u> through (iii) of this section shall govern the use of monitoring data to determine compliance for Group 1 and Group 2 points included in emissions averages. For storage vessels to which the provisions of <u>paragraphs</u> (c)(2)(i) through (iii) of this section do not apply (as specified in <u>paragraph (c)(2)(iv)</u> of this section), the owner or operator is required to comply with the provisions of the applicable monitoring plan, and monitoring records may be used to determine compliance.

(iv) Every fourth quarterly report shall include the following:

(A) A demonstration that annual credits are greater than or equal to annual debits as required by  $\frac{63.150(e)(3)}{2}$ ; and

(B) A certification of compliance with all the emissions averaging provisions in  $\S$  63.150.

(6) The owner or operator of a source shall submit reports quarterly for particular emission points not included in an emissions average under the circumstances described in <u>paragraphs (c)(6)(i)</u> through (v) of this section.

(i) The owner or operator of a source subject to this subpart shall submit quarterly reports for a period of one year for an emission point that is not included in an emissions average if:

(A) The emission point has more excursions, as defined in <u>paragraph (c)(2)(ii)</u> of this section, than the number of excused excursions allowed under <u>paragraph (c)(2)(ii)(B)</u> of this section for a semiannual reporting period; and

(B) The Administrator requests the owner or operator to submit quarterly reports for the emission point.

(ii) The quarterly reports shall include all information in <u>paragraphs (c)(2)</u>, (3), and (4) of this section applicable to the emission point(s) for which quarterly reporting is required under <u>paragraph (c)(6)(i)</u> of this section. Information applicable to other emission points within the source shall be submitted in the semiannual reports required under <u>paragraph (c)(1)</u> of this section.

(iii) Quarterly reports shall be submitted no later than 60 calendar days after the end of each quarter.

(iv) After quarterly reports have been submitted for an emission point for one year, the owner or operator may return to semiannual reporting for the emission point unless the Administrator requests the owner or operator to continue to submit quarterly reports.

(v) <u>Paragraphs (c)(2)(i)</u> through (<u>iii)</u> of this section shall govern the use of monitoring data to determine compliance for Group 1 emission points. For storage vessels to which the provisions of <u>paragraphs (c)(2)(i)</u> through (<u>iii)</u> of this section do not apply (as specified in <u>paragraph (c)(2)(iv)</u> of this section), the owner or operator is required to comply with the provisions of the applicable monitoring plan, and monitoring records may be used to determine compliance.

(7) The information specified in  $\S 63.108(1)(2)$  of subpart F of this part.

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(d) Other reports shall be submitted as specified in subpart A of this part or in  $\S$  63.113 through 63.151 of this subpart. These reports are:

(1) Reports of start-up, shutdown, and malfunction required by  $\S 63.10(d)(5)$ . The start-up, shutdown and malfunction reports may be submitted on the same schedule as the Periodic Reports required under <u>paragraph (c)</u> of this section instead of the schedule specified in  $\S 63.10(d)(5)$ . For each source as defined in  $\S 63.101$ , on and after July 15, 2027, this paragraph no longer applies.

(2) For storage vessels, the notifications of inspections required by  $\S 63.122$  (h)(1) and (h)(2) of this subpart.

(3) For owners or operators of sources required to request approval for a nominal control efficiency for use in calculating credits for an emissions average, the information specified in  $\S$  63.150(i) of this subpart.

(4) If an owner or operator transfers for disposal a gas stream that has the characteristics specified in  $\S$ 

63.107(b) through (h) or meets the criteria specified in § 63.107(i) to an off-site location or an on-site location not owned or operated by the owner or operator of the source and the vent stream was not included in the information submitted with the Notification of Compliance Status or a previous periodic report, the owner or operator shall submit a supplemental report. The supplemental report shall be submitted no later than July 23, 2001 or with the next periodic report, whichever is later. The report shall provide the information listed in paragraphs (d)(4)(i) through (iv) of this section.

(i) The chemical manufacturing process unit(s) that is the origin of all or part of the vent stream that exits the process vent.

(ii) The type(s) of unit operations (i.e., an air oxidation reactor, distillation unit, or reactor) that creates the vent stream that exits the process vent.

(iii) For a Group 2 process vent, the last recovery device, if any.

(iv) For a Group 1 process vent, the identity of the transferee.

(e) An owner or operator subject to this subpart shall submit the information specified in paragraphs (e)(1) through (e)(4) of this section with the operating permit application or as otherwise specified by the permitting authority. The owner or operator shall submit written updates as amendments to the operating permit application on the schedule and under the circumstances described in § 63.151(j) of this subpart. Notwithstanding, if the owner or operator has an operating permit under 40 CFR part 70 or 71, the owner or operator shall follow the schedule and format required by the permitting authority.

(1) The information specified in  $\frac{63.151}{10}$  or (g) of this subpart for any emission points for which the owner or operator requests approval to monitor a unique parameter or use an alternative monitoring and recording system, and

(2) The information specified in § 63.151(d) of this subpart for points included in an emissions average.

(3) The information specified in § 63.151(e) of this subpart for points not included in an emissions average.

(4) The information specified in  $\S 63.151(h)$  as applicable.

(f) Owners or operators required to keep continuous records by §§ 63.118, 63.130, 63.147, 63.150, or other sections of this subpart shall keep records as specified in paragraphs (f)(1) through (f)(7) of this section, unless an alternative recordkeeping system has been requested and approved under § 63.151(f) or (g) or § 63.152(e) or under § 63.8(f), and except as provided in paragraph (c)(2)(ii)(C) of this section or in paragraph (g) of this section. If a monitoring plan for storage vessels pursuant to § 63.120(d)(2)(i) requires continuous records, the monitoring plan shall specify which provisions, if any, of paragraphs (f)(1) through (f)(7) of this section apply. Any records required to be maintained by this part that are submitted electronically via the EPA's CEDRI may be maintained in electronic format. This ability to maintain electronic copies does not affect the requirement for facilities to make records, data, and reports available upon request to a delegated air agency or the EPA as part of an on-site compliance evaluation.

(1) The monitoring system shall measure data values at least once every 15 minutes.

(2) The owner or operator shall record either:

(i) Each measured data value; or

(ii) Block average values for 15-minute or shorter periods calculated from all measured data values during each period or at least one measured data value per minute if measured more frequently than once per minute.

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(3) If the daily average value of a monitored parameter for a given operating day is within the range established in the Notification of Compliance Status or operating permit, the owner or operator shall either:

(i) Retain block hourly average values for that operating day for 5 years and discard, at or after the end of that operating day, the 15-minute or more frequent average values and readings recorded under paragraph (f)(2) of this section; or

(ii) Retain the data recorded in <u>paragraph (f)(2)</u> of this section for 5 years.

(4) If the daily average value of a monitored parameter for a given operating day is outside the range established in the Notification of Compliance Status or operating permit, the owner or operator shall retain the data recorded that operating day under paragraph (f)(2) of this section for 5 years.

(5) Daily average values of each continuously monitored parameter shall be calculated for each operating day, and retained for 5 years, except as specified in paragraphs (f)(6) and (f)(7) of this section.

(i) The daily average shall be calculated as the average of all values for a monitored parameter recorded during the operating day. The average shall cover a 24-hour period if operation is continuous, or the number of hours of operation per operating day if operation is not continuous.

(ii) The operating day shall be the period defined in the operating permit or the Notification of Compliance Status. It may be from midnight to midnight or another daily period.

(6) If all recorded values for a monitored parameter during an operating day are within the range established in the Notification of Compliance Status or operating permit, the owner or operator may record that all values were within the range and retain this record for 5 years rather than calculating and recording a daily average for that operating day. For these operating days, the records required in paragraph (f)(3) of this section shall also be retained for 5 years.

(7) Except as specified in paragraph (f)(7)(vi) of this section monitoring data recorded during periods identified in paragraphs (f)(7)(i) through (f)(7)(v) of this section shall not be included in any average computed under this subpart. Records shall be kept of the times and durations of all such periods and any other periods during process or control device operation when monitors are not operating.

(i) Monitoring system breakdowns, repairs, calibration checks, and zero (low-level) and high-level adjustments;

(ii) Start-ups;

(iii) Shutdowns;

(iv) Malfunctions;

(v) Periods of non-operation of the chemical manufacturing process unit (or portion thereof), resulting in cessation of the emissions to which the monitoring applies.

(vi) For each source as defined in  $\S$  63.101, on and after July 15, 2027, paragraphs (f)(7)(ii) through (f)(7)(iv) no longer apply.

(g) For any parameter with respect to any item of equipment, the owner or operator may implement the recordkeeping requirements in paragraph (g)(1) or (g)(2) of this section as alternatives to the continuous operating parameter monitoring and recordkeeping provisions listed in  $\frac{8}{63.114}$ ,  $\frac{63.117}{63.117}$ , and  $\frac{63.118}{63.118}$  for process vents,  $\frac{8}{63.127}$ ,  $\frac{63.129}{63.129}$ , and  $\frac{63.130}{63.130}$  for transfer operations,  $\frac{8}{5}$ ,  $\frac{63.143}{63.146}$ , and  $\frac{63.147}{63.147}$  for wastewater, and/or  $\frac{8}{5}$ ,  $\frac{63.152(f)}{63.152(f)}$ , except that  $\frac{8}{5}$ ,  $\frac{63.152(f)(7)}{63.103(c)}$  shall apply. The owner or operator shall retain each record required by paragraph (g)(1) or (g)(2) of this section as provided in  $\frac{8}{5}$ ,  $\frac{63.103(c)}{63.103(c)}$  of subpart F of this part, except as provided otherwise in paragraph (g)(1) or (g)(2) of this section.

(1) The owner or operator may retain only the daily average value, and is not required to retain more frequent monitored operating parameter values, for a monitored parameter with respect to an item of equipment, if the requirements of paragraphs (g)(1)(i) through (vi) of this section are met. An owner or operator electing to comply with the requirements of paragraph (g)(1) of this section shall notify the Administrator in the Notification of Compliance Status or, if the Notification of Compliance Status has already been submitted, in the periodic report immediately preceding implementation of the requirements of paragraph (g)(1) of this section.

(i) The monitoring system is capable of detecting unrealistic or impossible data during periods of operation other than startups, shutdowns, or malfunctions (*e.g.*, a temperature reading of -200 °C on a boiler), and will alert the operator by alarm

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or other means. The owner or operator shall record the occurrence. All instances of the alarm or other alert in an operating day constitute a single occurrence. For each source as defined in § 63.101, on and after July 15, 2027, the phrase "other than startups, shutdowns, or malfunctions (*e.g.*, a temperature reading of -200 °C on a boiler)," in this paragraph no longer applies.

(ii) The monitoring system generates, updated at least hourly throughout each operating day, a running average of the monitoring values that have been obtained during that operating day, and the capability to observe this average is readily available to the Administrator on-site during the operating day. The owner or operator shall record the occurrence of any period meeting the criteria in <u>paragraphs (g)(1)(ii)(A)</u> through (C) of this section. All instances in an operating day constitute a single occurrence.

(A) The running average is above the maximum or below the minimum established limits;

(B) The running average is based on at least 6 1-hour average values; and

(C) The running average reflects a period of operation other than a startup, shutdown, or malfunction. For each source as defined in  $\S$  63.101, on and after July 15, 2027, the phrase "other than a startup, shutdown, or malfunction" in this paragraph no longer applies.

(iii) The monitoring system is capable of detecting unchanging data during periods of operation other than startups, shutdowns, or malfunctions, except in circumstances where the presence of unchanging data is the expected operating condition based on past experience (*e.g.*, pH in some scrubbers), and will alert the operator by alarm or other means. The owner or operator shall record the occurrence. All instances of the alarm or other alert in an operating day constitute a single occurrence. For each source as defined in  $\S$  <u>63.101</u>, on and after July 15, 2027, the phrase "other than startups, shutdowns, or malfunctions" in this paragraph no longer applies.

(iv) The monitoring system will alert the owner or operator by an alarm or other means, if the running average parameter value calculated under <u>paragraph (g)(1)(ii)</u> of this section reaches a set point that is appropriately related to the established limit for the parameter that is being monitored.

(v) The owner or operator shall verify the proper functioning of the monitoring system, including its ability to comply with the requirements of <u>paragraph (g)(1)</u> of this section, at the times specified in <u>paragraphs (g)(1)(v)(A)</u> through (C) of this section. The owner or operator shall document that the required verifications occurred.

(A) Upon initial installation.

(B) Annually after initial installation.

(C) After any change to the programming or equipment constituting the monitoring system, which might reasonably be expected to alter the monitoring system's ability to comply with the requirements of this section.

(vi) The owner or operator shall retain the records identified in paragraphs (g)(1)(vi)(A) through (C) of this section.

(A) Identification of each parameter, for each item of equipment, for which the owner or operator has elected to comply with the requirements of <u>paragraph (g)</u> of this section.

(B) A description of the applicable monitoring system(s), and of how compliance will be achieved with each requirement of paragraph (g)(1)(i) through (g)(1)(v) of this section. The description shall include monitoring equipment manufacturer(s) and model number(s) and the pollutant or parameter monitored, and identify the location and format (*e.g.*, on-line storage; log entries) for each required record. If the description changes, the owner or operator shall retain both the current and the most recent superseded description. The description, and the most recent superseded description, shall be retained as provided in § 63.103(c) of subpart F of this part, except as provided in paragraph (g)(1)(v)(D) of this section.

(C) A description, and the date, of any change to the monitoring system that would reasonably be expected to affect its ability to comply with the requirements of paragraph (g)(1) of this section.

(D) Owners and operators subject to paragraph(g)(1)(vi)(B) of this section shall retain the current description of the monitoring system as long as the description is current, but not less than 5 years from the date of its creation. The current description shall, at all times, be retained on-site or be accessible from a central location by computer or other means that provides access within 2 hours after a request. The owner or operator shall retain the most recent superseded description at least until 5 years from the date of its creation. The superseded description shall be retained on-site (or accessible from a

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central location by computer that provides access within 2 hours after a request) at least 6 months after its creation. Thereafter, the superseded description may be stored off-site.

(2) If an owner or operator has elected to implement the requirements of paragraph(g)(1) of this section, and a period of 6 consecutive months has passed without an excursion as defined in paragraph(g)(2)(iv) of this section, the owner or operator is no longer required to record the daily average value for that parameter for that unit of equipment, for any operating day when the daily average value is less than the maximum, or greater than the minimum established limit. With approval by the Administrator, monitoring data generated prior to the compliance date of this subpart shall be credited toward the period of 6 consecutive months, if the parameter limit and the monitoring was required and/or approved by the Administrator.

(i) If the owner or operator elects not to retain the daily average values, the owner or operator shall notify the Administrator in the next periodic report. The notification shall identify the parameter and unit of equipment.

(ii) If, on any operating day after the owner or operator has ceased recording daily averages as provided in <u>paragraph</u> (g)(2) of this section, there is an excursion as defined in <u>paragraph</u> (g)(2)(iv) of this section, the owner or operator shall immediately resume retaining the daily average value for each day, and shall notify the Administrator in the next periodic report. The owner or operator shall continue to retain each daily average value until another period of 6 consecutive months has passed without an excursion as defined in <u>paragraph</u> (g)(2)(iv) of this section.

(iii) The owner or operator shall retain the records specified in paragraphs (g)(1) (i), (ii), (iii), (iv), (v), and (vi) of this section. For any calendar week, if compliance with paragraphs (g)(1) (i), (ii), (iii), and (iv) of this section does not result in retention of a record of at least one occurrence or measured parameter value, the owner or operator shall record and retain at least one parameter value during a period of operation other than a startup, shutdown, or malfunction. For each source as defined in § 63.101, on and after July 15, 2027, the phrase "other than a startup, shutdown, or malfunction" in this paragraph no longer applies.

(iv) For purposes of <u>paragraph (g)</u> of this section, an excursion means that the daily average value of monitoring data for a parameter is greater than the maximum, or less than the minimum established value, except as provided in <u>paragraphs</u> (g)(2)(iv)(A) and (B) of this section.

(A) The daily average value during any startup, shutdown, or malfunction shall not be considered an excursion for purposes of this paragraph (g)(2), if the owner or operator operates the source during such periods in accordance with  $\frac{63.102(a)(4)}{5}$ . For each source as defined in  $\frac{63.101}{5}$ , on and after July 15, 2027, this paragraph no longer applies.

(B) An excussion, as described in  $\S$  63.152(c)(2)(ii)(B) and (C), shall not be considered an excursion for purposes of this paragraph (g)(2).

(h) Beginning no later than July 15, 2024, owners and operators must submit performance test reports in accordance with this paragraph. Unless otherwise specified in this subpart, within 60 days after the date of completing each performance test required by this subpart, owners and operators must submit the results of the performance test following the procedures specified in § 63.9(k). Data collected using test methods supported by the EPA's Electronic Reporting Tool (ERT) as listed on the EPA's ERT website (https://www.epa.gov/electronic-reporting-air-emissions/electronic-reporting-tool-ert) at the time of the test must be submitted in a file format generated through the use of the EPA's ERT. Alternatively, owners and operators may submit an electronic file consistent with the extensible markup language (XML) schema listed on the EPA's ERT website. Data collected using test methods that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the test must be included as an attachment in the ERT or alternate electronic file.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>60 FR 63629</u>, Dec. 12, 1995; <u>61 FR 64577</u>, Dec. 5, 1996; <u>62 FR 2776</u>, Jan. 17, 1997; <u>64 FR 20195</u>, Apr. 26, 1999; <u>66 FR 6934</u>, Jan. 22, 2001; <u>71 FR 20456</u>, Apr. 20, 2006; <u>89 FR 43208</u>, May 16, 2024]

## § 63.153 Implementation and enforcement.

(a) This subpart can be implemented and enforced by the U.S. EPA, or a delegated authority such as the applicable State, local, or Tribal agency. If the U.S. EPA Administrator has delegated authority to a State, local, or Tribal agency, then that agency, in addition to the U.S. EPA, has the authority to implement and enforce this subpart. Contact the applicable U.S. EPA Regional Office to find out if implementation and enforcement of this subpart is delegated to a State, local, or Tribal agency.

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(b) In delegating implementation and enforcement authority of this subpart to a State, local, or Tribal agency under <u>subpart E</u> <u>of this part</u>, the authorities contained in <u>paragraph (c)</u> of this section are retained by the Administrator of U.S. EPA and cannot be transferred to the State, local, or Tribal agency.

(c) The authorities that cannot be delegated to State, local, or Tribal agencies are as specified in <u>paragraphs</u> (c)(1) through (5) of this section.

(1) Approval of alternatives to the requirements in  $\underline{\$\$}$ 

63.110, 63.112 through 63.113, 63.119, 63.126, 63.132 through 63.140, 63.148 through 63.149, and 63.150(i)(1) through (4). Follow the requirements in § 63.121 to request permission to use an alternative means of emission limitation for storage vessels. Where these standards reference another subpart, the cited provisions will be delegated according to the delegation provisions of the referenced subpart. Where these standards reference another subpart and modify the requirements, the requirements shall be modified as described in this subpart. Delegation of the modified requirements will also occur according to the delegation provisions of the referenced subpart.

(2) Approval of major alternatives to test methods under  $\frac{63.7(e)(2)(ii)}{2}$  and  $\frac{(f)}{2}$ , as defined in  $\frac{63.90}{2}$ , and as required in this subpart.

(3) Approval of major alternatives to monitoring under  $\S 63.8(f)$ , as defined in  $\S 63.90$ , and as required in this subpart.

(4) Approval of major alternatives to recordkeeping and reporting under  $\S 63.10(f)$ , as defined in  $\S 63.90$ , and as required in this subpart.

(5) Approval of an alternative to any electronic reporting to the EPA required by this subpart.

[68 FR 37344, June 23, 2003, as amended at 89 FR 43212, May 16, 2024]

# Table 1 to Subpart G of Part 63—Process Vents—Coefficients for Total Resource Effectiveness for Existing Source Nonhalogenated and Halogenated Vent Streams

Type of Streem	Control Device Basis	Values of Coefficients			
Type of Stream		a	b	c	d
Nonhalogenated	Flare	1.935	$3.660 \times 10^{-1}$	$-7.687 \times 10^{-3}$	$-7.333 \times 10^{-4}$
	Thermal Incinerator 0 Percent Heat Recovery	1.492	$6.267  imes 10^{-2}$	$3.177 \times 10^{-2}$	$-1.159 \times 10^{-3}$
	Thermal Incinerator 70 Percent Heat Recovery	2.519	$1.183 \times 10^{-2}$	$1.300 \times 10^{-2}$	$4.790 \times 10^{-2}$
Halogenated	Thermal Incinerator and Scrubber	3.995	$5.200 \times 10^{-2}$	$-1.769 \times 10^{-3}$	$9.700  imes 10^{-4}$

 Table 1A to Subpart G of Part 63—Applicable 40 CFR Part 63
 General Provisions

40 CFR part 63, subpart A, provisions applicable to subpart G
§ 63.1(a)(1), (a)(2), (a)(3), (a)(13), (a)(14), (b)(2) and (c)(4)
§ 63.2
63.5(a)(1), (a)(2), (b), (d)(1)(ii), (d)(3)(i), (d)(3)(iii) through (d)(3)(vi), (d)(4), (e), (f)(1), and (f)(2)
63.6(a), (b)(3), (c)(5), (i)(1), (i)(2), (i)(4)(i)(A), (i)(5) through (i)(14), (i)(16) and (j)
63.9(a)(2), (b)(4)(i), (b)(4)(ii), (b)(4)(iii), (b)(5), (c), (d), (j), and (k).
§ 63.10(d)(4)
§ 63.11 (c), (d), and (e)
§ 63.12(b)
<sup>a</sup> The notifications specified in $\S$ 63.9(b)(4)(i) and (b)(5) shall be submitted at the times specified in 40 CFR part 65.
[50 ED 104(9 A 22 1004 1 1 4 72 ED 70212 D 22 2009 95 ED 72997 N - 10 2020]

[59 FR 19468, Apr. 22, 1994, as amended at 73 FR 78213, Dec. 22, 2008; 85 FR 73887, Nov. 19, 2020]

 Table 2 to Subpart G of Part 63—Process Vents—Coefficients for Total Resource Effectiveness for New Source

 Nonhalogenated and Halogenated Vent Streams

## National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Turne of stream Control device basis		Values of Coefficients			
Type of stream	am Control device basis		b	c	d
Nonhalogenated	Flare	0.5276	0.0998	$^-2.096  imes 10^{-3}$	$-2.000  imes 10^{-4}$
	Thermal Incinerator 0 Percent Heat Recovery	0.4068	0.0171	$8.664 \times 10^{-3}$	$-3.162 \times 10^{-4}$
	Thermal Incinerator 70 Percent Heat Recovery	0.6868	$3.209 \times 10^{-3}$	$3.546 \times 10^{-3}$	$1.306 \times 10^{-2}$
Halogenated	Thermal Incinerator and Scrubber	1.0895	$1.417 \times 10^{-2}$	$-4.822 \times 10^{-4}$	$2.645 \times 10^{-4}$

# Table 3 to Subpart G of Part 63—Process Vents—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control Devices and Recapture Devices

Table 3 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control         Devices and Recapture Devices				
Control or recapture device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters		
Thermal incinerator, other than a thermal oxidizer used to comply with $\S 63.124$	Firebox temperature <sup>b</sup> [63.114(a)(1)(i)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the firebox temperature averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record the daily average firebox temperature for each operating day. <sup>e</sup>		
		4. Report all daily average temperatures that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>		
Thermal oxidizer used to comply with $\S$ 63.124	Combustion chamber temperature [63.124(b)(5)(i)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the combustion chamber temperature averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record each 1-hour block average firebox temperature for each operating day.		
		4. Report all 1-hour block temperatures that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>		
Thermal oxidizer used to comply with $\S$ 63.124 (Continued)	Flue gas flow rate [63.124(b)(5)(ii)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the flue gas flow rate averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record each 1-hour block average flue gas flow rate for each operating day.		
		4. Report all 1-hour block flue gas flow rates that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>		
Catalytic incinerator	Temperature upstream and downstream of the catalyst bed [63.114(a)(1)(ii)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the upstream and downstream temperatures and the temperature difference across the catalyst bed averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record the daily average upstream temperature and temperature difference across the catalyst bed for each		

Table 3 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control         Devices and Recapture Devices				
Control or recapture device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters		
		operating day. <sup>e</sup>		
		4. Report all daily average upstream temperatures that are outside the range established in the NCS or operating permit—PR.		
		5. Report all daily average temperature differences across the catalyst bed that are outside the range established in the NCS or operating permit—PR. <sup>g</sup>		
		6. Report all operating days when insufficient monitoring data are collected. <sup>f</sup>		
Flare (if meeting the requirements of $\frac{63.11(b)}{5}$ )	Presence of a flame at the pilot light $[\S 63.114(a)(2)]$	1. Hourly records of whether the monitor was continuously operating and whether the pilot flame was continuously present during each hour.		
		2. Record and report the presence of a flame at the pilot light over the full period of the compliance determination—NCS. <sup>d</sup>		
		3. Record the times and durations of all periods when all pilot flames are absent or the monitor is not operating.		
		4. Report the times and durations of all periods when all pilot flames of a flare are absent—PR. <sup>g</sup>		
Flare (if meeting the requirements of $\S$ 63.108)	The parameters are specified in $\S$ <u>63.108</u>	1. Records as specified in $\underline{\$ 63.108(m)}$ of subpart F of this part.		
		2. Report information as specified in <u>§</u> <u>63.108(1)</u> of <u>subpart F of this part</u> —PR. <sup>g</sup>		
Boiler or process heater with a design heat input capacity less than 44 megawatts and vent stream is <i>not</i> introduced with or as the primary fuel	Firebox temperature <sup>b</sup> [ $\underline{\$}$ <u>63.114(a)(3)</u> ]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the firebox temperature averaged over the full period of the performance test—NCS.<sup>d</sup></li> <li>Record the daily average firebox temperature for each operating day.<sup>e</sup></li> </ol>		
		4. Report all daily average firebox temperatures that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>		
Scrubber for halogenated vent streams ( <i>Note:</i> Controlled by a combustion device other than a flare)	pH of scrubber effluent [§ $63.114(a)(4)(i)$ ], and	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the pH of the scrubber effluent averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record the daily average pH of the scrubber effluent for each operating day. <sup>e</sup>		
		4. Report all daily average pH values of the scrubber effluent that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>		
Scrubber for halogenated vent	Scrubber liquid and gas flow rates [§	1. Continuous records of scrubber liquid flow rate. <sup>c</sup>		

Table 3 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control         Devices and Recapture Devices				
Control or recapture device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters		
streams ( <i>Note:</i> Controlled by a combustion device other than a flare) (Continued)	<u>63.114(a)(4)(ii)</u> ]	2. Record and report the scrubber liquid/gas ratio averaged over the full period of the performance test—NCS. <sup>d</sup>		
		3. Record the daily average scrubber liquid/gas ratio for each operating day. <sup>e</sup>		
		4. Report all daily average scrubber liquid/gas ratios that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>		
All control devices	Presence of flow diverted to the atmosphere from the control device $[\S 63.114(d)(1)]$ or	<ol> <li>Hourly records of whether the flow indicator was operating and whether diversion was detected at any time during each hour.</li> <li>Record and report the times and durations of all periods when the vent stream is diverted through a bypass line or the monitor is not operating—PR.<sup>g</sup></li> </ol>		
		3. For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), record and report the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours—PR. <sup>g</sup>		
All control devices (Continued)	Monthly inspections of sealed valves $[\frac{63.114(d)(2)}{3}]$	<ol> <li>Records that monthly inspections were performed.</li> <li>Record and report all monthly inspections that show the valves are moved to the diverting position or the seal has been changed—PR.<sup>g</sup></li> </ol>		
		3. For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), record and report the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours—PR. <sup>g</sup>		
All recapture devices (as an alternative to the below for absorbers, condensers, and carbon adsorbers)	Concentration level or reading indicated by an organic monitoring device at the outlet of the recovery device $[\S 63.114(a)(5)(i)]$	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the concentration level or reading averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record the daily average concentration level or reading for each operating day. <sup>e</sup>		
		4. Report all daily average concentration levels or		

Table 3 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control         Devices and Recapture Devices				
Control or recapture device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters		
		readings that are outside the range established in the NCS or operating permit—PR. <sup>g</sup>		
Absorber <sup>h</sup>	Exit temperature of the absorbing liquid [ $\frac{63.114(a)(5)(ii)}{3.114(a)(5)(ii)}$ ], and	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the exit temperature of the absorbing liquid averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record the daily average exit temperature of the absorbing liquid for each operating day. <sup>e</sup>		
		4. Report all the daily average exit temperatures of the absorbing liquid that are outside the range established in the NCS or operating permit—PR. <sup>g</sup>		
Absorber <sup>h</sup> (Continued)	Exit specific gravity [ <u>§</u> 63.114(a)(5)(ii)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the exit specific gravity averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record the daily average exit specific gravity for each operating day. <sup>e</sup>		
		4. Report all daily average exit specific gravity values that are outside the range established in the NCS or operating permit—PR. <sup>g</sup>		
Condenser <sup>h</sup>	Exit (product side) temperature [§ 63.114(a)(5)(iii)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the exit temperature averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Record the daily average exit temperature for each operating day <sup>e</sup> .		
		4. Report all daily average exit temperatures that are outside the range established in the NCS or operating permit—PR. <sup>g</sup>		
Carbon adsorber <sup>h</sup>	Total regeneration stream mass or volumetric flow during carbon bed regeneration cycle(s) [ $\S$ <u>63.114(a)(5)(iv)</u> ], and	<ol> <li>Record of total regeneration stream mass or volumetric flow for each carbon bed regeneration cycle.</li> <li>Record and report the total regeneration stream mass or volumetric flow during each carbon bed regeneration cycle during the period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Report all carbon bed regeneration cycles when the total regeneration stream mass or volumetric flow is outside the range established in the NCS or operating permit—PR. <sup>g</sup>		
Carbon adsorber <sup>h</sup> (Continued)	Temperature of the carbon bed after regeneration [and within 15 minutes of completing any cooling cycle(s)] [ $\S$ 63.114(a)(5)(iv)]	<ol> <li>Records of the temperature of the carbon bed after each regeneration.</li> <li>Record and report the temperature of the carbon bed after each regeneration during the period of the performance test—NCS.<sup>d</sup></li> </ol>		
		3. Report all carbon bed regeneration cycles during which temperature of the carbon bed after		

Table 3 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control         Devices and Recapture Devices			
Control or recapture device Parameters to be monitored <sup>a</sup>		Recordkeeping and reporting requirements for monitored parameters	
		regeneration is outside the range established in the NCS or operating permit—PR. <sup>g</sup>	
Carbon adsorber <sup>h</sup> (Continued)	Outlet HAP or TOC concentration [§ 63.114(a)(5)(v)]	For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in § $63.114(a)(5)(v)$ , the owner or operator must record each outlet HAP or TOC concentration measured according to §§ $63.114(a)(5)(v)(B)$ and (C).	
Carbon adsorber <sup>h</sup> (Continued)	Adsorbent replacement [§ 63.114(a)(5)(v)]	1. For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in $\S 63.114(a)(5)(v)$ , the owner or operator must record date and time the adsorbent was last replaced.	
Carbon adsorber <sup>h</sup> (Continued)	Breakthrough [ <u>§ 63.114(a)(5)(v)</u> ]	For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in § $63.114(a)(5)(v)$ , the owner or operator must:	
		1. Record breakthrough limit and bed life established according to $\frac{63.114(a)(5)(v)(A)}{2}$ .	
		2. Report the date of each instance when breakthrough, as defined in § 63.101, is detected between the first and second adsorber and the adsorber is not replaced according to § 63.114(a)(5)(v)(A)(I)—PR. <sup>g</sup>	
Scrubber with a reactant tank used to comply with $\S$ 63.124	Liquid-to-gas ratio [ <u>§</u> <u>63.124(b)(4)(i)</u> ]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the L/G of the scrubber averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>	
		3. Record each 1-hour block L/G of the scrubber for each operating day.	
		4. Report all 1-hour block L/G values of the scrubber that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>	
Scrubber with a reactant tank used to comply with $\S$ <u>63.124</u> (Continued)	In lieu of liquid-to-gas ratio, scrubber total liquid flow rate and gas flow rate through scrubber [ $\S$ <u>63.124(b)(4)(i)</u> ]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report both the total scrubber liquid flow rate and gas flow rate through the scrubber averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>	
		3. Record each 1-hour block total scrubber liquid flow rate and each 1-hour block gas flow rate through the scrubber for each operating day.	
		4. Report all 1-hour block total scrubber liquid flow rate values and all 1-hour block gas flow rate through the scrubber values that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are	

Table 3 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control         Devices and Recapture Devices			
Control or recapture device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters	
		collected <sup>f</sup> —PR. <sup>g</sup>	
Scrubber with a reactant tank used to comply with § 63.124 (Continued)	pH of liquid in reactant tank [§ 63.124(b)(4)(ii)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the pH of liquid in reactant tank averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>	
		3. Record each 1-hour block pH of liquid in reactant tank for each operating day.	
		4. Report all 1-hour block values of the pH of liquid in reactant tank that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>	
Scrubber with a reactant tank used to comply with $\S$ 63.124 (Continued)	Pressure drop [ <u>§ 63.124(b)(4)(iii)]</u>	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the pressure drop of the scrubber averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>	
		3. Record each 1-hour block pressure drop of the scrubber for each operating day.	
		4. Report all 1-hour block pressure drop values that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>	
Scrubber with a reactant tank used to comply with $\S$ 63.124 (Continued)	Temperature of scrubbing liquid entering column [ <u>§ 63.124(b)(4)(iv)</u> ]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the temperature of scrubbing liquid entering column averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>	
		3. Record each 1-hour block temperature of scrubbing liquid entering column for each operating day.	
		4. Report all 1-hour block values of the temperature of scrubbing liquid entering column that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>	
Scrubber with a reactant tank used to comply with $\S$ <u>63.124</u> (Continued)	Liquid feed pressure [ <u>§</u> 63.124(b)(4)(v)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the liquid feed pressure of the scrubber averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>	
		3. Record each 1-hour block liquid feed pressure of the scrubber for each operating day.	
		4. Report all 1-hour block liquid feed pressure values that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>	
Sorbent injection	Sorbent injection rate <sup>b</sup> [§ $63.114(a)(6)(i)$ ]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the sorbent injection rate</li> </ol>	

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Table 3 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Control         Devices and Recapture Devices			
Control or recapture device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters	
		averaged over the full period of the performance test—NCS. <sup>d</sup>	
		3. Record the daily average sorbent injection rate for each operating day. <sup>e</sup>	
		4. Report all daily average sorbent injection rates that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>	
Sorbent injection (Continued)	Carrier gas flow rate <sup>b</sup> [ <u>§</u> 63.114(a)(6)(ii)]	<ol> <li>Continuous records.<sup>c</sup></li> <li>Record and report the carrier gas flow rate averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>	
		3. Record the daily average carrier gas flow rate for each operating day. <sup>e</sup>	
		4. Report all daily average carrier gas flow rates that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR. <sup>g</sup>	

<sup>a</sup> Regulatory citations are listed in brackets.

<sup>b</sup> Monitor may be installed in the firebox or in the ductwork immediately downstream of the firebox before any substantial heat exchange is encountered.

<sup>c</sup> "Continuous records" is defined in <u>§ 63.111 of this subpart</u>.

<sup>d</sup> NCS = Notification of Compliance Status described in <u>§ 63.152 of this subpart</u>.

<sup>e</sup> The daily average is the average of all recorded parameter values for the operating day. If all recorded values during an operating day are within the range established in the NCS or operating permit, a statement to this effect can be recorded instead of the daily average.

<sup>f</sup> The periodic reports shall include the duration of periods when monitoring data is not collected for each excursion as defined in  $\frac{63.152(c)(2)(ii)(A)}{63.152(c)(2)(ii)(A)}$  of this subpart.

<sup>g</sup> PR = Periodic Reports described in  $\S$  63.152 of this subpart.

<sup>h</sup> Alternatively, these devices may comply with the organic monitoring device provisions listed at this table under "All recapture devices.".

[89 FR 43212, May 16, 2024]

## Table 4 to Subpart G of Part 63—Process Vents—Monitoring, Recordkeeping, and Reporting Requirements for Maintaining a TRE Index Value >1.0 and. ≤4.0 [No Longer Applicable in Accordance With <u>§ 63.113(a)(4)</u>]

Final recovery device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters
Absorber <sup>b</sup>	Exit temperature of the absorbing liquid [63.114(b)(1)], and	<ol> <li>Continuous records<sup>c</sup>.</li> <li>Record and report the exit temperature of the absorbing liquid averaged over the full period of the TRE determination—NCS.<sup>d</sup></li> </ol>
		3. Record the daily average exit temperature of the absorbing liquid for each operating day <sup>e</sup> .
		4. Report all the daily average exit temperatures of the

Final recovery device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters
		absorbing liquid that are outside the range established in the NCS or operating permit—PR <sup>f</sup> .
	Exit specific gravity [63.114(b)(1)]	<ol> <li>Continuous records.</li> <li>Record and report the exit specific gravity averaged over the full period of the TRE determination—NCS.</li> </ol>
		3. Record the daily average exit specific gravity for each operating day <sup>e</sup> .
		4. Report all daily average exit specific gravity values that are outside the range established in the NCS or operating permit—PR.
Condenser <sup>d</sup>	Exit (product side) temperature [63.114(b)(2)]	<ol> <li>Continuous records.</li> <li>Record and report the exit temperature averaged over the full period of the TRE determination—NCS.</li> </ol>
		3. Record the daily average exit temperature for each operating day <sup>e</sup> .
		4. Report all daily average exit temperatures that are outside the range established in the NCS or operating permit—PR.
Carbon adsorber <sup>d</sup>	Total regeneration stream mass or volumetric flow during carbon bed regeneration cycle(s) [63.114(b)(3)], and	<ol> <li>Record of total regeneration stream mass or volumetric flow for each carbon bed regeneration cycle.</li> <li>Record and report the total regeneration stream mass or volumetric flow during each carbon bed regeneration cycle during the period of the TRE determination—NCS.</li> </ol>
		3. Report all carbon bed regeneration cycles when the total regeneration stream mass or volumetric flow is outside the range established in the NCS or operating permit—PR.
	Temperature of the carbon bed after regeneration [and within 15 minutes of completing any cooling cycle(s)] [63.114(b)(3)]	<ol> <li>Records of the temperature of the carbon bed after each regeneration.</li> <li>Record and report the temperature of the carbon bed after each regeneration during the period of the TRE determination—NCS.</li> </ol>
		3. Report all carbon bed regeneration cycles during which temperature of the carbon bed after regeneration is outside the range established in the NCS or operating permit—PR.
All recovery devices (as an alternative to the above)	Concentration level or reading indicated by an organic monitoring device at the outlet of the recovery device [63.114 (b)]	<ol> <li>Continuous records.</li> <li>Record and report the concentration level or reading averaged over the full period of the TRE determination— NCS.</li> </ol>
		3. Record the daily average concentration level or reading for each operating day <sup>e</sup> .
		4. Report all daily average concentration levels or readings that are outside the range established in the NCS or operating permit—PR.
<sup>a</sup> Regulatory citations	are listed in brackets.	
<sup>o</sup> Alternatively, these o	devices may comply with the organic monito	ring device provisions listed at the end of this table under

National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Final recovery device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters
"All Recovery Device	s."	
<sup>c</sup> "Continuous records" is defined in <u>§ 63.111 of this subpart</u> .		
<sup>d</sup> NCS = Notification of Compliance Status described in <u>§ 63.152 of this subpart</u> .		f this subpart.
<sup>e</sup> The daily average is the average of all values recorded during the operating day. If all recorded values during an operating day are within the range established in the NCS or operating permit, a statement to this effect can be recorded instead of the		

daily average.

<sup>f</sup> PR= Periodic Reports described in § 63.152 of this subpart.

[59 FR 19453, Apr. 22, 1994, as amended at 89 FR 43215, May 16, 2024]

#### Table 5 to Subpart G of Part 63—Group 1 Storage Vessels at Existing Sources

Table 5 to Subpart G of Part 63—Group 1 Storage Vessels at Existing Sources		
Vessel capacity (cubic meters)	Vapor pressure <sup>a</sup> (kilopascals)	
$75 \le \text{capacity} < 151^{\text{b}}$	<sup>b</sup> ≥13.1	
$38 \le$ capacity $<151^{\circ}$	° ≥6.9	
151 ≤ capacity	≥5.2	
<sup>a</sup> Maximum true vapor pressure of total organic HAP at storage temperature.		
1		

<sup>b</sup> For each source as defined in  $\S$  <u>63.101</u>, beginning no later than the compliance dates specified in  $\S$  <u>63.100(k)(10)</u>, these vessel capacity and vapor pressure criterion no longer apply.

<sup>c</sup> For each source as defined in § <u>63.101</u>, beginning no later than the compliance dates specified in § <u>63.100(k)(10)</u>, these vessel capacity and vapor pressure criterion apply.

[<u>89 FR 43215</u>, May 16, 2024]

## Table 6 to Subpart G of Part 63—Group 1 Storage Vessels at New Sources

Table 6 to Subpart G of Part 63—Group 1 Storage Vessels at New Sources		
Vessel capacity (cubic meters)Vapor pressure <sup>a</sup> (kilopascals)		Vapor pressure <sup>a</sup> (kilopascals)
$38 \le \text{capacity} < 151^{\text{b}}$		≥13.1 <sup>b</sup>
$38 \le$ capacity $<151^{\circ}$		≥6.9 <sup>c</sup>
$151 \leq \text{capacity}$		≥0.7
<sup>a</sup> Maximum true vapor pressure of total organic HAP at storage temperature.		

<sup>b</sup> For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), these vessel capacity and vapor pressure criterion no longer apply.

<sup>c</sup> For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), these vessel capacity and vapor pressure criterion apply.

#### [89 FR 43216, May 16, 2024]

 Table 7 to Subpart G of Part 63—Transfer Operations—Monitoring, Recordkeeping, and Reporting Requirements

 for Complying With 98 Weight-Percent Reduction of Total Organic Hazardous Air Pollutants Emissions or a Limit of

 20 Parts per Million by Volume

Table 7 to Subpart G of Part 63—Transfer Operations—Monitoring, Recordkeeping, and Reporting Requirements for Complying With 98 Weight-Percent Reduction of Total Organic Hazardous Air Pollutants Emissions or a Limit of 20 Parts per Million by Volume

Control device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters
Thermal incinerator	Firebox temperature <sup>b</sup> [ <u>§</u> 63.127(a)(1)(i)]	<ol> <li>Continuous records<sup>c</sup> during loading.</li> <li>Record and report the firebox temperature averaged over the full period of the performance test—NCS.<sup>d</sup></li> </ol>
		<ul> <li>3. Record the daily average firebox temperature for each operating day.<sup>e</sup></li> <li>4. Report daily average temperatures that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected<sup>f</sup>—PR.<sup>g</sup></li> </ul>
Catalytic incinerator	Temperature upstream and downstream of the catalyst bed [ $\frac{63.127(a)(1)(ii)}{2}$ ]	<ol> <li>Continuous records during loading.</li> <li>Record and report the upstream and downstream temperatures and the temperature difference across the catalyst bed averaged over the full period of the performance test— NCS.</li> </ol>
		3. Record the daily average upstream temperature and temperature difference across catalyst bed for each operating day. <sup>e</sup>
		4. Report all daily average upstream temperatures that are outside the range established in the NCS or operating permit—PR.
		5. Report all daily average temperature differences across the catalyst bed that are outside the range established in the NCS or operating permit—PR.
		6. Report all operating days when insufficient monitoring data are collected. <sup>f</sup>
Boiler or process heater with a design heat input capacity less than 44 megawatts and vent stream is not introduced with or as the primary fuel	Firebox temperature <sup>b</sup> [§ 63.127(a)(3)]	<ol> <li>Continuous records during loading.</li> <li>Record and report the firebox temperature averaged over the full period of the performance test—NCS.</li> <li>Record the daily average firebox temperature for each operating day.<sup>e</sup></li> </ol>
		4. Report all daily average firebox temperatures that are outside the range established in the NCS or operating permit and all operating days when insufficient data are collected <sup>f</sup> —PR.
Flare (if meeting the requirements of $\S$ 63.126(b)(2)(i))	Presence of a flame at the pilot light [ <u>§ 63.127(a)(2)</u> ]	1. Hourly records of whether the monitor was continuously operating and whether the pilot flame was continuously present during each hour.
		2. Record and report the presence of a flame at the pilot light over the full period of the compliance determination—NCS.
		3. Record the times and durations of all periods when all pilot flames are absent or the monitor is not operating.
		4. Report the duration of all periods when all pilot flames of a flare are absent—PR.
Flare (if meeting the requirements of $\frac{\& 63.108}{\& 0.108}$ )	The parameters are specified in $\S 63.108$	<ol> <li>Records as specified in <u>§ 63.108(m)</u> of <u>subpart F of this part</u>.</li> <li>Report information as specified in <u>§ 63.108(l)</u> of <u>subpart F of this part</u>—PR.</li> </ol>
Scrubber for halogenated vent streams ( <i>Note:</i> Controlled by a combustion device other than	pH of scrubber effluent [ $\S$ 63.127(a)(4)(i)], and	<ol> <li>Continuous records during loading.</li> <li>Record and report the pH of the scrubber effluent averaged over the full period of the performance test—NCS.</li> </ol>

Table 7 to Subpart G of Part 63—Transfer Operations—Monitoring, Recordkeeping, and Reporting Requirements for Complying With 98 Weight-Percent Reduction of Total Organic Hazardous Air Pollutants Emissions or a Limit of 20 Parts per Million by Volume			
Control device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters	
a flare)			
		3. Record the daily average pH of the scrubber effluent for each operating day. <sup>e</sup>	
		4. Report all daily average pH values of the scrubber effluent that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR.	
	Scrubber liquid and gas flow rates [ <u>§</u> <u>63.127(a)(4)(ii)</u> ]	<ol> <li>Continuous records during loading of scrubber liquid flow rate.</li> <li>Record and report the scrubber liquid/gas ratio averaged over the full period of the performance test—NCS.</li> </ol>	
		3. Record the daily average scrubber liquid/gas ratio for each operating day. <sup>e</sup>	
		4. Report all daily average scrubber liquid/gas ratios that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR.	
Absorber <sup>h</sup>	Exit temperature of the absorbing liquid [ $\S$ <u>63.127(b)(1)</u> ], and	<ol> <li>Continuous records during loading.</li> <li>Record and report the exit temperature of the absorbing liquid averaged over the full period of the performance test—NCS.</li> </ol>	
		3. Record the daily average exit temperature of the absorbing liquid for each operating day. <sup>e</sup>	
		4. Report all daily average exit temperatures of the absorbing liquid that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR.	
	Exit specific gravity [§ 63.127(b)(1)]	<ol> <li>Continuous records during loading.</li> <li>Record and report the exit specific gravity averaged over the full period of the performance test—NCS.</li> </ol>	
		3. Record the daily average exit specific gravity for each operating day. <sup>e</sup>	
		4. Report all daily average exit specific gravity values that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR.	
Condenser <sup>h</sup>	Exit (product side) temperature [ <u>§</u> <u>63.127(b)(2)</u> ]	<ol> <li>Continuous records during loading.</li> <li>Record and report the exit temperature averaged over the full period of the performance test—NCS.</li> </ol>	
		3. Record the daily average exit temperature for each operating day. <sup>e</sup>	
		4. Report all daily average exit temperatures that are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR.	

Table 7 to Subpart G of Part 63—Transfer Operations—Monitoring, Recordkeeping, and Reporting Requirements for
Complying With 98 Weight-Percent Reduction of Total Organic Hazardous Air Pollutants Emissions or a Limit of 20 Parts
per Million by Volume

Control device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters
Carbon adsorber <sup>h</sup>	Total regeneration stream mass or volumetric or volumetric flow during carbon bed regeneration cycle(s) [ <u>§ 63.127(b)(3)</u> ], and	<ol> <li>Record of total regeneration stream mass or volumetric flow for each carbon bed regeneration cycle.</li> <li>Record and report the total regeneration stream mass or volumetric flow during each carbon bed regeneration cycle during the period of the performance test—NCS.</li> </ol>
		3. Report all carbon bed regeneration cycles when the total regeneration stream mass or volumetric flow is outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR.
	Temperature of the carbon bed after regeneration [and within 15 minutes of completing any cooling cycle(s)] [§ 63.127(b)(3)]	<ol> <li>Records of the temperature of the carbon bed after each regeneration.</li> <li>Record and report the temperature of the carbon bed after each regeneration during the period of the performance test— NCS.</li> </ol>
		3. Report all the carbon bed regeneration cycles during which the temperature of the carbon bed after regeneration is outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup><math>f</math></sup> —PR.
	Outlet HAP or TOC concentration [ <u>§</u> <u>63.127(b)(4)</u> ]	For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in $\S$ <u>63.127(b)(4)</u> , the owner or operator must record each outlet HAP or TOC concentration measured according to $\S$ <u>63.127(b)(4)(ii)</u> and <u>(iii)</u> .
	Adsorbent replacement [§ 63.127(b)(4)]	1. For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in $\S$ <u>63.127(b)(4)</u> , the owner or operator must record date and time the adsorbent was last replaced.
	Breakthrough [ <u>§</u> <u>63.127(b)(4)]</u>	For each nonregenerative adsorber and regenerative adsorber that is regenerated offsite subject to the requirements in $\S$ <u>63.127(b)(4)</u> , the owner or operator must:
		1. Record breakthrough limit and bed life established according to $\frac{63.127(b)(4)(i)}{2}$ .
		2. Report the date of each instance when breakthrough, as defined in § $63.101$ , is detected between the first and second adsorber and the adsorber is not replaced according to § $63.127(b)(4)(iii)(A)$ —PR.
All recovery devices (as an alternative to the above)	Concentration level or reading indicated by an organic monitoring device at the outlet of the recovery device [ $\S$ 63.127(b)]	<ol> <li>Continuous records during loading.</li> <li>Record and report the concentration level or reading averaged over the full period of the performance test—NCS.</li> <li>Record the daily average concentration level or reading for each operating day.<sup>d</sup></li> </ol>
		4. Report all daily average concentration levels or readings that

#### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Table 7 to Subpart G of Par Complying With 98 Weight-P	rt 63—Transfer Operations— Percent Reduction of Total Or per Millio	Monitoring, Recordkeeping, and Reporting Requirements for ganic Hazardous Air Pollutants Emissions or a Limit of 20 Parts on by Volume
Control device	Parameters to be monitored <sup>a</sup>	Recordkeeping and reporting requirements for monitored parameters
		are outside the range established in the NCS or operating permit and all operating days when insufficient monitoring data are collected <sup>f</sup> —PR.
All control devices and vapor balancing systems	Presence of flow diverted to the atmosphere from the control device [ $\S$ <u>63.127(d)(1)</u> ] or	<ol> <li>Hourly records of whether the flow indicator was operating and whether a diversion was detected at any time during each hour.</li> <li>Record and report the duration of all periods when the vent stream is diverted through a bypass line or the monitor is not operating—PR.</li> </ol>
		3. For each source as defined in § 63.101, beginning no later than the compliance dates specified in § 63.100(k)(10), record and report the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours—PR.
	Monthly inspections of sealed valves [§ 63.127(d)(2)]	<ol> <li>Records that monthly inspections were performed.</li> <li>Record and report all monthly inspections that show the valves are moved to the diverting position or the seal has been changed.</li> </ol>
		3. For each source as defined in $\S$ 63.101, beginning no later than the compliance dates specified in $\S$ 63.100(k)(10), record and report the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours—PR.

<sup>a</sup> Regulatory citations are listed in brackets.

<sup>b</sup> Monitor may be installed in the firebox or in the ductwork immediately downstream of the firebox before any substantial heat exchange is encountered.

<sup>c</sup> "Continuous records" is defined in <u>§ 63.111 of this subpart</u>.

<sup>d</sup> NCS = Notification of Compliance Status described in <u>§ 63.152 of this subpart</u>.

<sup>e</sup> The daily average is the average of all recorded parameter values for the operating day. If all recorded values during an operating day are within the range established in the NCS or operating permit, a statement to this effect can be recorded instead of the daily average.

<sup>f</sup> The periodic reports shall include the duration of periods when monitoring data are not collected for each excursion as defined in  $\frac{63.152(c)(2)(ii)(A)}{100}$  of this subpart.

<sup>g</sup> PR = Periodic Reports described in  $\S$  63.152 of this subpart.

<sup>h</sup> Alternatively, these devices may comply with the organic monitoring device provisions listed at the end of this table under "All Recovery Devices."

National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

### [<u>89 FR 43216</u>, May 16, 2024]

# Table 8 to Subpart G of Part 63—Organic HAP's Subject to the Wastewater Provisions for Process Units at New Sources

Chemical name	CAS No. <sup>a</sup>
Allyl chloride	107051
Benzene	71432
Butadiene (1,3-)	106990
Carbon disulfide	75150
Carbon tetrachloride	56235
Cumene	98828
Ethyl chloride (Chloroethane)	75003
Ethylbenzene	100414
Ethylene oxide	75218
Ethylidene dichloride	75343
(1,1-Dichloroethane).	
Hexachlorobutadiene	87683
Hexachloroethane	67721
Hexane	100543
Methyl bromide (Bromomethane)	74839
Methyl chloride (Chloromethane)	74873
Phosgene	75445
Tetrachloroethylene (Perchloroethylene)	127184
Toluene	108883
Trichloroethane (1,1,1-) (Methyl chloroform)	71556
Trichloroethylene	79016
Trimethylpentane (2,2,4-)	540841
Vinyl chloride (chloroethylene)	75014
Vinylidene chloride	75354
(1,1-Dichloroethylene).	
Xylene (m-)	108383
Xylene (p-)	106423
<sup>a</sup> CAS numbers refer to the Chemical Abstracts Service registry number assigned to sp mixtures of compounds.	pecific compounds, isomers, or

**Note.** The list of organic HAP's on table 8 is a subset of the list of organic HAP's on table 9 of this subpart.

[59 FR 19453, Apr. 22, 1994, as amended at 89 FR 43218, May 16, 2024]

## Table 9 to Subpart G of Part 63—Organic HAP's Subject to the Wastewater Provisions for Process Units at New and Existing Sources and Corresponding Fraction Removed (Fr) Values

Chemical name	CAS No. <sup>a</sup>	Fr
Acetaldehyde	75070	0.95
Acetonitrile	75058	0.62

Chemical name	CAS No. <sup>a</sup>	Fr
Acetophenone	98862	0.72
Acrolein	107028	0.96
Acrylonitrile	107131	0.96
Allyl chloride	107051	0.99
Benzene	71432	0.99
Benzyl chloride	100447	0.99
Biphenyl	92524	0.99
Bromoform	75252	0.99
Butadiene (1,3-)	106990	0.99
Carbon disulfide	75150	0.99
Carbon tetrachloride	56235	0.99
Chlorobenzene	108907	0.99
Chloroform	67663	0.99
Chloroprene (2-Chloro-1,3-butadiene)	126998	0.99
Cumene	98828	0.99
Dichlorobenzene (p-)	106467	0.99
Dichloroethane (1,2-) (Ethylene dichloride)	107062	0.99
Dichloroethyl ether (Bis(2-chloroethyl)ether)	111444	0.87
Dichloropropene (1,3-)	542756	0.99
Diethyl sulfate	64675	0.90
Dimethyl sulfate	77781	0.53
Dimethylaniline (N,N-)	121697	0.99
Dimethylhydrazine (1,1-)	57147	0.57
Dinitrophenol (2,4-)	51285	0.99
Dinitrotoluene (2,4-)	121142	0.38
Dioxane (1,4-) (1,4-Diethyleneoxide)	123911	0.37
Epichlorohydrin(1-Chloro-2,3-epoxypropane)	106898	0.91
Ethyl acrylate	140885	0.99
Ethylbenzene	100414	0.99
Ethyl chloride (Chloroethane)	75003	0.99
Ethylene dibromide (Dibromomethane)	106934	0.99
Ethylene glycol dimethyl ether	110714	0.90
Ethylene glycol monobutyl ether acetate	112072	0.76
Ethylene glycol monomethyl ether acetate	110496	0.28
Ethylene oxide	75218	0.98
Ethylidene dichloride (1,1-Dichloroethane)	75343	0.99
Hexachlorobenzene	118741	0.99
Hexachlorobutadiene	87683	0.99
Hexachloroethane	67721	0.99
Hexane	110543	0.99

#### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Isophorone         78591         0.60           Methanol         67561         0.31           Methyl bromide (Bromomethane)         74839         0.99           Methyl chloride (Chloromethane)         74873         0.99           Methyl isobutyl ketone (Hexone)         108101         0.99           Methyl methacrylate         80626         0.98           Methyl tert-butyl ether         1634044         0.99           Methyl methacrylate         80626         0.98           Methyl enchloride (Dichloromethane)         75092         0.99           Naphthalene         91203         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Styrene         100425         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Tetrachloroethylene (Perchloroethylene)         12784         0.44           Trichloroethare (1,1,2-) (Yinyl trichloride)         79005         0.99           Trichloroethare (1,2	Chemical name	CAS No. <sup>a</sup>	Fr
Methanol         67561         0.31           Methyl bromide (Bromomethane)         74839         0.99           Methyl chloride (Chloromethane)         74873         0.99           Methyl isobutyl ketone (Hexone)         108101         0.99           Methyl methacrylate         80626         0.98           Methyl methacrylate         1034044         0.99           Methyl ter-butyl ether         1634044         0.99           Methylene chloride (Dichloromethane)         75092         0.99           Naphthalene         91203         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Tichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroetha	Isophorone	78591	0.60
Methyl bromide (Bromomethane)         74839         0.99           Methyl chloride (Chloromethane)         74873         0.99           Methyl lisobutyl ketone (Hexone)         108101         0.99           Methyl methacrylate         80626         0.98           Methyl tert-butyl ether         1634044         0.99           Methyl tert-butyl ether         1634044         0.99           Methyl nethacrylate         80626         0.98           Methyl tert-butyl ether         1634044         0.99           Methyl nethacrylate         80923         0.80           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Trichloroethare (1,1,2-)         120821         0.99           Trichloroethare (1,1,2-)         120821         0.99           Trichloroethare (1,1,2-) (Vinyl trichloride)         7900	Methanol	67561	0.31
Methyl chloride (Chloromethane)         74873         0.99           Methyl isobutyl ketone (Hexone)         108101         0.99           Methyl methacrylate         80626         0.98           Methyl tert-butyl ether         1634044         0.99           Methyl tert-butyl ether         1634044         0.99           Methyl tert-butyl ether         1634044         0.99           Nitrobenzene         91203         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vi	Methyl bromide (Bromomethane)	74839	0.99
Methyl isobutyl ketone (Hexone)         108101         0.99           Methyl methacrylate         80626         0.98           Methyl tert-butyl ether         1634044         0.99           Methyl tert-butyl ether         1634044         0.99           Methylene chloride (Dichloromethane)         75092         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldchyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluene (1,1,2,2-)         79345         0.99           Toluene (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2,4-)         120821         0.99           Trichloroethane (1,1,2,0         19005         0.99           Trichloroethane (1,1,2,0         19016         0.99           Trichlorophenol (2,4,5-)	Methyl chloride (Chloromethane)	74873	0.99
Methyl methacrylate         80626         0.98           Methyl tert-butyl ether         1634044         0.99           Methyl tert-butyl ether         1634044         0.99           Methylene chloride (Dichloromethane)         75092         0.99           Naphthalene         91203         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Toluene         108883         0.99           Toluene (1,2,4-)         120821         0.99           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Tr	Methyl isobutyl ketone (Hexone)	108101	0.99
Methyl tert-butyl ether         1634044         0.99           Methylene chloride (Dichloromethane)         75092         0.99           Naphthalene         91203         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene xide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluidine (o-)         10883         0.99           Trichlorobenzene (1,2,4-)         120821         0.99           Trichlorobenzene (1,2,4-)         120821         0.99           Trichlorobethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichlorobethane (1,2,4-)         120821         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99	Methyl methacrylate	80626	0.98
Methylene chloride (Dichloromethane)         75092         0.99           Naphthalene         91203         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,2,4-)         120821         0.99           Trichloroethane (1,2,4-)         120821         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethylene         79016         0.99           Trichloroet	Methyl tert-butyl ether	1634044	0.99
Naphthalene         91203         0.99           Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,2,4-)         120821         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,2,4-)         120821         0.99           Trichloroethylene         79016         0.99           Trichloroethylene (1,2,5-)         95954         0.96           Trichlorophenol (2,4,	Methylene chloride (Dichloromethane)	75092	0.99
Nitrobenzene         98953         0.80           Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluine (o-)         95534         0.44           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99           Trichloroethylene         79016         0.99           Trichloroethylene (2,2,4-)         540841	Naphthalene	91203	0.99
Nitropropane (2-)         79469         0.98           Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,2-) (Vinyl trichloride)         71056         0.99           Trichloroethane (1,2,4-)         120821         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99           Trichlorophenol (2,4,5-)         95954         0.96           Trichlorophenol (2,4,5-)         540841         0.99           Vinyl acetate         108054         0.	Nitrobenzene	98953	0.80
Phosgene         75445         0.99           Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99           Trichloroethane (2,2,4-)         95954         0.96           Triethylamine         121448         0.99           Trimethylpentane (2,2,4-)         540841         0.99           Vinyl acetate         108054 <td>Nitropropane (2-)</td> <td>79469</td> <td>0.98</td>	Nitropropane (2-)	79469	0.98
Propionaldehyde         123386         0.99           Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79016         0.99           Trichlorophenol (2,4,5-)         95954         0.96           Triethylamine         121448         0.99           Trimethylpentane (2,2,4-)         540841         0.99           Vinyl acetate         108054         0.99           Vinyl chloride (Chloroethylene)         75014         0.99	Phosgene	75445	0.99
Propylene dichloride (1,2-Dichloropropane)         78875         0.99           Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethylene         79016         0.99           Trichlorophenol (2,4,5-)         95954         0.96           Triethylamine         121448         0.99           Trimethylpentane (2,2,4-)         540841         0.99           Vinyl acetate         108054         0.99	Propionaldehyde	123386	0.99
Propylene oxide         75569         0.99           Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,1,2-)         120821         0.99           Trichloroethane (1,1,1-)         (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-)         Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-)         Vinyl trichloride)         79005         0.99           Trichloroethane (1,1,2-)         Vinyl trichloride)         79016         0.99           Trichloroethane (1,1,2-)         Vinyl trichloride)         0.90         0.99           Trichloroethylene         79016         0.99         0.99         0.99           Trichlorophenol (2,4,5-)         95954         0.96         0.99           Trimethylpentane (2,2,4-)         540841         0.99         0.99         0.99         0.99         0.99         0.99         0.99         0.99         0.99         0.99         0.99         0.99 <td< td=""><td>Propylene dichloride (1,2-Dichloropropane)</td><td>78875</td><td>0.99</td></td<>	Propylene dichloride (1,2-Dichloropropane)	78875	0.99
Styrene         100425         0.99           Tetrachloroethane (1,1,2,2-)         79345         0.99           Tetrachloroethylene (Perchloroethylene)         127184         0.99           Toluene         108883         0.99           Toluidine (o-)         95534         0.44           Trichloroethane (1,2,4-)         120821         0.99           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         0.99           Trichloroethane (1,1,2-) (Vinyl trichloride)         79005         0.99           Trichloroethylene         79016         0.99           Trichlorophenol (2,4,5-)         95954         0.96           Triethylamine         121448         0.99           Vinyl acetate         108054         0.99           Vinyl chloride (Chloroethylene)         75014         0.99	Propylene oxide	75569	0.99
Tetrachloroethane (1,1,2,2-)       79345       0.99         Tetrachloroethylene (Perchloroethylene)       127184       0.99         Toluene       108883       0.99         Toluidine (o-)       95534       0.44         Trichloroethane (1,2,4-)       120821       0.99         Trichloroethane (1,1,1-) (Methyl chloroform)       71556       0.99         Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichloroethylene       79016       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Styrene	100425	0.99
Tetrachloroethylene (Perchloroethylene)       127184       0.99         Toluene       108883       0.99         Toluidine (o-)       95534       0.44         Trichlorobenzene (1,2,4-)       120821       0.99         Trichloroethane (1,1,1-) (Methyl chloroform)       71556       0.99         Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichloroethylene       79016       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Triethylamine       121448       0.99         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Tetrachloroethane (1,1,2,2-)	79345	0.99
Toluene       108883       0.99         Toluidine (o-)       95534       0.44         Trichlorobenzene (1,2,4-)       120821       0.99         Trichloroethane (1,1,1-) (Methyl chloroform)       71556       0.99         Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichloroethane (1,2,4-)       79005       0.99         Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Triethylamine       121448       0.99         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Tetrachloroethylene (Perchloroethylene)	127184	0.99
Toluidine (o-)       95534       0.44         Trichlorobenzene (1,2,4-)       120821       0.99         Trichloroethane (1,1,1-) (Methyl chloroform)       71556       0.99         Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichloroethylene       79016       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Toluene	108883	0.99
Trichlorobenzene (1,2,4-)       120821       0.99         Trichloroethane (1,1,1-) (Methyl chloroform)       71556       0.99         Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichloroethylene       79016       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Toluidine (o-)	95534	0.44
Trichloroethane (1,1,1-) (Methyl chloroform)       71556       0.99         Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichloroethylene       79016       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Triethylamine       121448       0.99         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Trichlorobenzene (1,2,4-)	120821	0.99
Trichloroethane (1,1,2-) (Vinyl trichloride)       79005       0.99         Trichloroethylene       79016       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Triethylamine       121448       0.99         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Trichloroethane (1,1,1-) (Methyl chloroform)	71556	0.99
Trichloroethylene       79016       0.99         Trichlorophenol (2,4,5-)       95954       0.96         Triethylamine       121448       0.99         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Trichloroethane (1,1,2-) (Vinyl trichloride)	79005	0.99
Trichlorophenol (2,4,5-)       95954       0.96         Triethylamine       121448       0.99         Trimethylpentane (2,2,4-)       540841       0.99         Vinyl acetate       108054       0.99         Vinyl chloride (Chloroethylene)       75014       0.99	Trichloroethylene	79016	0.99
Triethylamine         121448         0.99           Trimethylpentane (2,2,4-)         540841         0.99           Vinyl acetate         108054         0.99           Vinyl chloride (Chloroethylene)         75014         0.99	Trichlorophenol (2,4,5-)	95954	0.96
Trimethylpentane (2,2,4-)         540841         0.99           Vinyl acetate         108054         0.99           Vinyl chloride (Chloroethylene)         75014         0.99	Triethylamine	121448	0.99
Vinyl acetate1080540.99Vinyl chloride (Chloroethylene)750140.99	Trimethylpentane (2,2,4-)	540841	0.99
Vinyl chloride (Chloroethylene) 75014 0.99	Vinyl acetate	108054	0.99
	Vinyl chloride (Chloroethylene)	75014	0.99
Vinylidene chloride (1,1-Dichloroethylene)753540.99	Vinylidene chloride (1,1-Dichloroethylene)	75354	0.99
Xylene (m-) 108383 0.99	Xylene (m-)	108383	0.99
Xylene (o-)         95476         0.99	Xylene (o-)	95476	0.99
Xylene (p-) 106423 0.99	Xylene (p-)	106423	0.99

<sup>a</sup> CAS numbers refer to the Chemical Abstracts Service registry number assigned to specific compounds, isomers, or mixtures of compounds.

[59 FR 19468, Apr. 22, 1994, as amended at 71 FR 76615, Dec. 21, 2006]

## Table 10 to Subpart G of Part 63—Wastewater—Compliance Options for Wastewater Tanks

Capacity (m <sup>3</sup> )	Maximum true vapor pressure (kPa)	<b>Control requirements</b>
<75		§ 63.133(a)(1)

### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Capacity (m <sup>3</sup> )	Maximum true vapor pressure (kPa)	Control requirements
"75 and <151	<13.1 "13.1	§ 63.133(a)(1) § 63.133(a)(2)
"151	<5.2 "5.2	§ 63.133(a)(1) § 63.133(a)(2)

# Table 11 to Subpart G of Part 63—Wastewater—Inspection and Monitoring Requirements for Waste Management Units

To comply with	Inspection or monitoring requirement	Frequency of inspection or monitoring	Method
Tanks:			
63.133(b)(1)	Inspect fixed roof and all openings for leaks	Initially Semi-annually	Visual.
63.133(c)	Inspect floating roof in accordance with <u>§§</u> <u>63.120 (a)(2)</u> and <u>(a)(3)</u>	See $§ 63.120$ (a)(2) and (a)(3)	Visual.
63.133(d)	Measure floating roof seal gaps in accordance with $\S$ 63.120 (b)(2)(i) through (b)(4)		See $\frac{63.120}{(b)(2)(i)}$ through $(b)(4)$ .
	—Primary seal gaps	Once every 5 years Initially Annually	
	—Secondary seal gaps		
63.133(f) 63.133(g)	Inspect wastewater tank for control equipment failures and improper work practices	Initially Semi-annually	Visual.
Surface impoundments:			
63.134(b)(1)	Inspect cover and all openings for leaks	Initially Semi-annually	Visual.
63.134(c)	Inspect surface impoundment for control equipment failures and improper work practices	Initially Semi-annually	Visual.
Containers:			
63.135(b)(1), 63.135(b)(2) (ii)	Inspect cover and all openings for leaks	Initially Semi-annually	Visual.
63.135(d)(1)	Inspect enclosure and all openings for leaks	Initially Semi-annually	Visual.
63.135(e)	Inspect container for control equipment failures and improper work practices	Initially Semi-annually	Visual.
Individual Drain Systems <sup>a</sup> :			
63.136(b)(1)	Inspect cover and all openings to ensure there are no gaps, cracks, or holes	Initially Semi-annually	Visual.
63.136(c)	Inspect individual drain system for control equipment failures and improper work practices	Initially Semi-annually	Visual.
63.136(e)(1)	Verify that sufficient water is present to properly maintain integrity of water seals	Initially Semi-annually	Visual.
63.136(e)(2), 63.136(f)(1)	Inspect all drains using tightly-fitted caps or plugs to ensure caps and plugs are in place and properly installed	Initially Semi-annually	Visual.

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To comply with	Inspection or monitoring requirement	Frequency of inspection or monitoring	Method	
63.136(f)(2)	Inspect all junction boxes to ensure covers are in place and have no visible gaps, cracks, or holes	Initially Semi-annually	Visual or smoke test or other means as specified.	
63.136(f)(3)	Inspect unburied portion of all sewer lines for cracks and gaps	Initially Semi-annually	Visual.	
Oil-water separators:				
63.137(b)(1)	Inspect fixed roof and all openings for leaks	Initially Semi-annually	Visual.	
63.137(c)	Measure floating roof seal gaps in accordance with $40 \text{ CFR } 60.696(d)(1)$	Initially <sup>b</sup>	See <u>40 CFR 60.696(d)(1)</u> .	
	—Primary seal gaps	Once every 5 years		
63.137(c)	—Secondary seal gaps	Initially <sup>b</sup> Annually		
63.137(d) Inspect oil-water separator for control equipment failures and improper work practices Visual.				
<sup>a</sup> As specified in § 63.136(a), the owner or operator shall comply with either the requirements of § 63.136 (b) and (c) or § 63.136 (e) and (f).				
<sup>b</sup> Within 60 days of	installation as specified in $\S 63.137(c)$ .			

## Table 12 to Subpart G of Part 63—Monitoring Requirements for Treatment Processes

To comply with	Parameters to be monitored	Frequency	Methods
1. Required mass removal of Table 8 and/or Table 9 compound(s) from wastewater treated in a properly operated biological treatment unit, $\frac{63.138(f)}{63.138(g)}$	Appropriate parameters as specified in § 63.143(c) and approved by permitting authority	Appropriate frequency as specified in § 63.143 and approved by permitting authority	Appropriate methods as specified in $\S$ 63.143 and as approved by permitting authority.
2. Steam stripper	(i) Steam flow rate; and	Continuously	Integrating steam flow monitoring device equipped with a continuous recorder.
	(ii) Wastewater feed mass flow rate; and	Continuously	Liquid flow meter installed at stripper influent and equipped with a continuous recorder.
	(iii) Wastewater feed temperature; or (iv) Column operating temperature	Continuously	<ul> <li>(A) Liquid temperature monitoring device installed at stripper influent and equipped with a continuous or recorder; or</li> <li>(B) Liquid temperature monitoring device installed in the column top tray liquid phase (i.e., at the downcomer) and equipped with a continuous recorder.</li> </ul>
3. Other treatment processes or alternative monitoring parameters	Other parameters may be monitored upon approval		

## National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

To comply with	Parameters to be monitored	Frequency	Methods
to those listed in item 2 of this table	from the Administrator with		
	the requirements specified		
	in <u>§ 63.151(f)</u>		

#### Table 13 to Subpart G of Part 63—Wastewater—Monitoring Requirements for Control Devices

Table 13 to Subpart G of Part 63—Wastewater—Monitoring Requirements for Control D			or Control Devices
Control device	Monitoring equipment required	Parameters to be monitored	Frequency
All control devices	1. Flow indicator installed at all bypass lines to the atmosphere and equipped with continuous recorder <sup>b</sup> or	1. Presence of flow diverted from the control device to the atmosphere <i>or</i>	Hourly records of whether the flow indicator was operating and whether a diversion was detected at any time during each hour.
	2. Valves sealed closed with car- seal or lock-and-key configuration	2. Monthly inspections of sealed valves	Monthly.
Thermal Incinerator	Temperature monitoring device installed in firebox or in ductwork immediately downstream of firebox <sup>a</sup> and equipped with a continuous recorder <sup>b</sup>	Firebox temperature	Continuous.
Catalytic Incinerator	Temperature monitoring device installed in gas stream immediately before and after catalyst bed and equipped with a continuous recorder <sup>b</sup>	<ol> <li>Temperature upstream of catalyst bed <i>or</i></li> <li>Temperature difference across catalyst bed</li> </ol>	Continuous.
Flare (if meeting the requirements of $\S$ <u>63.139(c)(3)</u> )	Heat sensing device installed at the pilot light and equipped with a continuous recorder <sup>a</sup>	Presence of a flame at the pilot light	Hourly records of whether the monitor was continuously operating and whether the pilot flame was continuously present during each hour.
Flare (if meeting the requirements of $\frac{63.108}{5}$ )	The monitoring equipment is specified in $\frac{63.108}{2}$	The parameters are specified in $\S 63.108$	The frequency is specified in $\underline{\$}$ <u>63.108</u> .
Boiler or process heater <44 megawatts and vent stream is not mixed with the primary fuel	Temperature monitoring device installed in firebox <sup>a</sup> and equipped with continuous recorder <sup>b</sup>	Combustion temperature	Continuous.
Condenser	Temperature monitoring device installed at condenser exit and equipped with continuous recorder <sup>b</sup>	Condenser exit (product side) temperature	Continuous.
Carbon adsorber (regenerative, regenerated onsite)	Integrating regeneration stream flow monitoring device having an accuracy of $\pm 10$ percent, and	Total regeneration stream mass or volumetric flow during carbon bed regeneration cycle(s)	For each regeneration cycle, record the total regeneration stream mass or volumetric flow.
	Carbon bed temperature monitoring device	Temperature of carbon bed after regeneration [and within 15 minutes of completing any cooling cycle(s)]	For each regeneration cycle and within 15 minutes of completing any cooling cycle, record the carbon bed temperature.

### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Table 13 to Subpart G of Part 63—Wastewater—Monitoring Requirements for Control Devices				
Control device Monitoring equipment required		Parameters to be monitored	Frequency	
Carbon adsorber (Non- regenerative or regenerative, regenerated offsite)	Organic compound concentration monitoring device <sup>c</sup>	Organic compound concentration of adsorber exhaust	Daily or at intervals no greater than 20 percent of the design carbon replacement interval, whichever is greater.	
	The monitoring equipment is specified in $\S 63.139(d)(5)$	The parameters are specified in $\S 63.139(d)(5)$	The frequency is specified in $\S$ <u>63.139(d)(5)</u> .	
Organic monitoring device <sup>d</sup>	Organic monitoring device installed at the outlet of the control device	Organic compound concentration of control device exhaust	Continuous.	
Alternative monitoring parameters	Other parameters may be monitored upon approval from the Administrator in accordance with the requirements in § $63.143(e)(3)$			

<sup>a</sup> Monitor may be installed in the firebox or in the ductwork immediately downstream of the firebox before any substantial heat exchange is encountered.

<sup>b</sup> "Continuous recorder" is defined in <u>§ 63.111 of this subpart</u>.

<sup>c</sup> As an alternative to conducting this monitoring, an owner or operator may replace the carbon in the carbon adsorption system with fresh carbon at a regular predetermined time interval that is less than the carbon replacement interval that is determined by the maximum design flow rate and organic concentration in the gas stream vented to the carbon adsorption system. For each source as defined in § 63.101, on and after July 15, 2027, this footnote no longer applies.

<sup>d</sup> A continuous organic monitoring device may be used in lieu of the requirements outlined for thermal incinerators, catalytic incinerators, boilers, process heaters, condensers, and carbon adsorbers.

#### [89 FR 43218, May 16, 2024]

#### Tables 14-14b to Subpart G of Part 63 [Reserved]

 Table 15 to Subpart G of Part 63—Wastewater—Information on Table 8 and/or Table 9 Compounds To Be

 Submitted With Notification of Compliance Status for Process Units at New and/or Existing Sources<sup>a b</sup>

|--|

<sup>a</sup> The information specified in this table must be submitted; however, it may be submitted in any format. This table presents an example format.

<sup>b</sup> Other requirements for the NCS are specified in § 63.152(b) of this subpart.

<sup>c</sup> Also include a description of the process unit (e.g., benzene process unit).

<sup>d</sup> Except when  $\S$  <u>63.132(e)</u> is used, annual average concentration as specified in  $\S$  <u>63.132(c)</u> or <u>(d)</u> and  $\S$  <u>63.144</u>.

<sup>e</sup> When <u>§ 63.132(e)</u> is used, indicate the wastewater stream is a designated Group 1 wastewater stream.

<sup>f</sup> Except when  $\S 63.132(e)$  is used, annual average flow rate as specified in  $\S 63.132(c)$  or (d) and in  $\S 63.144$ .

<sup>g</sup> Indicate whether stream is Group 1 or Group 2. If Group 1, indica0te whether it is Group 1 for Table 8 or Table 9 compounds or for both Table 8 and Table 9 compounds.

<sup>h</sup> Cite <u>§ 63.138</u> compliance option used.

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#### Table 16 to Subpart G of Part 63 [Reserved]

# Table 17 to Subpart G of Part 63—Information for Treatment Processes To Be Submitted With Notification of Compliance Status<sup>a b</sup>

Treatment process identification <sup>c</sup>	Description <sup>d</sup>	Wastewater stream(s) treated <sup>e</sup>	Monitoring parameters <sup>f</sup>		
<sup>a</sup> The information specified in this table must be submitted; however, it may be submitted in any format. This table presents an example format.					
<sup>b</sup> Other requirements for the Notification	<sup>b</sup> Other requirements for the Notification of Compliance Status are specified in <u>§ 63.152(b) of this Subpart</u> .				
<sup>c</sup> Identification codes should correspond to those listed in Table 15.					
<sup>d</sup> Description of treatment process.					
<sup>e</sup> Stream identification code for each wastewater stream treated by each treatment unit. Identification codes should correspond to entries listed in Table 15.					
<sup>f</sup> Parameter(s) to be monitored or measured in accordance with Table 12 and $\$$ 63 143					

# Table 18 to Subpart G of Part 63—Information for Waste Management Units To Be Submitted With Notification of Compliance Status<sup>a b</sup>

Waste management unit identification <sup>c</sup>	Description <sup>d</sup>	Wastewater stream(s) received or managed <sup>e</sup>			
<sup>a</sup> The information specified in this table must be submitted; however, it may be submitted in any format. This table presents an example format.					
<sup>b</sup> Other requirements for the Notification of Compliance Status are specified in <u>§ 63.152(b) of this Subpart</u> .					
<sup>c</sup> Identification codes should correspond to those l	isted in Table 15.				
<sup>d</sup> Description of waste management unit.					

<sup>e</sup> Stream identification code for each wastewater stream received or managed by each waste management unit. Identification codes should correspond to entries listed in Table 15.

## Table 19 to Subpart G of Part 63—Wastewater—Information on Residuals To Be Submitted With Notification of Compliance Status<sup>a b</sup>

Residual identification <sup>c</sup>	Residual description <sup>d</sup>	Wastewater stream identification <sup>e</sup>	Treatment process <sup>f</sup>	Fate <sup>g</sup>	Control device identification code	Control device description <sup>h</sup>	Control device efficiency <sup>i</sup>
<sup>a</sup> The information specified in this table must be submitted; however, it may be submitted in any format. This table presents an example format.							

<sup>b</sup> Other requirements for the Notification of Compliance Status are specified in § 63.152(b) of this subpart.

<sup>c</sup> Name or identification code of residual removed from Group 1 wastewater stream.

<sup>d</sup> Description of residual (e.g., steam stripper A-13 overhead condensates).

<sup>e</sup> Identification of stream from which residual is removed.

<sup>f</sup> Treatment process from which residual originates.

<sup>g</sup> Indicate whether residual is sold, returned to production process, or returned to waste management unit or treatment process; or whether HAP mass of residual is destroyed by 99 percent.

<sup>h</sup> If the fate of the residual is such that the HAP mass is destroyed by 99 percent, give description of device used for HAP destruction.

<sup>i</sup> If the fate of the residual is such that the HAP mass is destroyed by 99 percent, provide an estimate of control device efficiency and attach substantiation in accordance with  $\S$  63.146(b)(9) of this subpart.

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Table 20 to Subpart G of Part 63—Wastewater—Periodic Reporting Requirements for Control Devices Subject to §63.139Used To Comply With §§ 63.13Through 63.139

Table 20 to Subpart G of Part 63—W $63.139$	Used To Comply With $\frac{\&\& 63.13}{\&\& 63.13}$ Through $\frac{63.139}{\&\& 63.13}$
Control device	Reporting requirements
(1) Thermal Incinerator. Report all daily a operating permit and all operating days w	average <sup>a</sup> temperatures that are outside the range established in the NCS <sup>b</sup> or hen insufficient monitoring data are collected. <sup>c</sup>
(2) Catalytic Incinerator	(i) Report all daily average <sup>a</sup> upstream temperatures that are outside the range established in the NCS <sup>b</sup> or operating permit.
	(ii) Report all daily average <sup>a</sup> temperature differences across the catalyst bed that are outside the range established in the NCS <sup>b</sup> or operating permit.
	(iii) Report all operating days when insufficient monitoring data are collected. <sup>c</sup>
(3) Boiler or Process Heater with a design heat input capacity less than 44 megawatts and vent stream is not mixed with the primary fuel	Report all daily average <sup>a</sup> firebox temperatures that are outside the range established in the NCS <sup>b</sup> or operating permit and all operating days when insufficient monitoring data are collected. <sup>c</sup>
(4a) Flare (if meeting the requirements of $\frac{63.139(c)(3)}{2}$ )	Report the duration of all periods when all pilot flames are absent.
(4b) Flare (if meeting the requirements of $\frac{\& 63.108}{3}$ )	The reporting requirements are specified in <u>§ 63.108(1)</u> of <u>subpart F of this part</u> .
(5) Condenser	Report all daily average <sup>a</sup> exit temperatures that are outside the range established in the NCS <sup>b</sup> or operating permit and all operating days when insufficient monitoring data are collected. <sup>c</sup>
(6) Carbon Adsorber (Regenerative)	(i) Report all carbon bed regeneration cycles when the total regeneration stream mass or volumetric flow is outside the range established in the NCS <sup>b</sup> or operating permit.
	(ii) Report all carbon bed regeneration cycles during which the temperature of the carbon bed after regeneration is outside the range established in the NCS <sup>b</sup> or operating permit.
	(iii) Report all operating days when insufficient monitoring data are collected <sup>c</sup> .
	(iv) For each regenerative adsorber that is regenerated offsite subject to the requirements in § $63.139(d)(5)$ report the date of each instance when breakthrough, as defined in § $63.101$ , is detected between the first and second adsorber and the adsorber is not replaced according to § $63.139(d)(5)(iii)(A)$ .
(7) Carbon Adsorber (Non-Regenerative)	(i) Report all operating days when inspections not done according to the schedule developed as specified in table 13 of this subpart.
	(ii) Report all operating days when carbon has not been replaced at the frequency specified in table 13 of this subpart.
	(iii) For each nonregenerative adsorber subject to the requirements in § $63.139(d)(5)$ , report the date of each instance when breakthrough, as defined in § $63.101$ , is detected between the first and second adsorber and the adsorber is not replaced according to § $63.139(d)(5)(iii)(A)$ .
(8) All Control Devices	(i) Report the times and durations of all periods when the vent stream is diverted through a bypass line or the monitor is not operating, or
	(ii) Report all monthly inspections that show the valves are moved to the diverting position or the seal has been changed.
	(iii) For each source as defined in $\S$ 63.101, beginning no later than the compliance

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Table 20 to Subpart G of Part 63—Wastewater—Periodic Reporting Requirements for Control Devices Subject to §63.139Used To Comply With §§ 63.13Through 63.139				
Control device Reporting requirements				
	dates specified in § $63.100(k)(10)$ , report the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours.			
<ul> <li>9) Thermal Incinerator, Catalytic ncinerator, Boiler, Process Heater, Condenser, or Carbon Adsorber using a continuous organic monitoring device as pecified in § 63.143(e)(2)</li> <li>(i) Report all daily average<sup>a</sup> concentration levels or readings that are outside the range established in the NCS or operating permit.<sup>c</sup></li> <li>(ii) Report all operating days when insufficient monitoring data are collected.<sup>c</sup></li> </ul>				
<sup>a</sup> The daily average is the average of all values recorded during the operating day, as specified in <u>§ 63.147(d)</u> .				
<sup>b</sup> NCS = Notification of Compliance Status described in $\S 63.152$ .				
<sup>c</sup> The periodic reports shall include the duration of periods when monitoring data are not collected for each excursion as defined in $\frac{63.152(c)(2)(ii)(A)}{2}$ .				

## [<u>89 FR 43219</u>, May 16, 2024]

## Table 21 to Subpart G of Part 63—Average Storage Temperature (Ts) as a Function of Tank Paint Color

Tank Color		Average Storage Temperature (Ts)
White	$T_A a = 0$	
Aluminum	$T_{\rm A} = 2.5$	
Gray	$T_{\rm A} = 3.5$	
Black	$T_{\rm A} = 5.0$	
$^{a}$ T <sub>A</sub> is the average annual a	mbient temperature in deg	grees Fahrenheit.

## Table 22 to Subpart G of Part 63—Paint Factors for Fixed Roof Tanks

Tank	Paint factors (F <sub>p</sub> ) Paint Condition		
Roof	Shell	Good	Poor
White	White	1.00	1.15
Aluminum (specular)	White	1.04	1.18
White	Aluminum (specular)	1.16	1.24
Aluminum (specular)	Aluminum (specular)	1.20	1.29
White	Aluminum (diffuse)	1.30	1.38
Aluminum (diffuse)	Aluminum (diffuse)	1.39	1.46
White	Gray	1.30	1.38
Light gray	Light gray	1.33	1.44
Medium gray	Medium gray	1.40	1.58

#### Table 23 to Subpart G of Part 63—Average Clingage Factors (c)<sup>a</sup>

Linuid	Shell condition			
Liquia	Light rust <sup>b</sup>	Dense rust	Gunite lined	

### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Liquid	Shell condition			
Liquia	Light rust <sup>b</sup>	Dense rust	Gunite lined	
Gasoline	0.0015	0.0075	0.15	
Single component stocks	0.0015	0.0075	0.15	
Crude oil	0.0060	0.030	0.60	
<sup>a</sup> Units for average clingage factors are barrels per 1,000 square feet.				

<sup>b</sup> If no specific information is available, these values can be assumed to represent the most common condition of tanks currently in use.

## Table 24 to Subpart G of Part 63—Typical Number of Columns as a Function of Tank Diameter for Internal Floating Roof Tanks With Column Supported Fixed Roofs<sup>a</sup>

Tank diameter range (D in feet)	Typical number of columns, (Nc)		
0 <d td="" ≤85<=""><td>1</td></d>	1		
85 <d td="" ≤100<=""><td>6</td></d>	6		
100 <d td="" ≤120<=""><td>7</td></d>	7		
120 <d td="" ≤135<=""><td>8</td></d>	8		
135 <d td="" ≤150<=""><td>9</td></d>	9		
150 <d td="" ≤170<=""><td>16</td></d>	16		
170 <d td="" ≤190<=""><td>19</td></d>	19		
190 <d td="" ≤220<=""><td>22</td></d>	22		
220 <d td="" ≤235<=""><td>31</td></d>	31		
235 <d td="" ≤270<=""><td>37</td></d>	37		
270 <d td="" ≤275<=""><td>43</td></d>	43		
275 <d td="" ≤290<=""><td>49</td></d>	49		
290 <d td="" ≤330<=""><td>61</td></d>	61		
330 <d td="" ≤360<=""><td>71</td></d>	71		
360 <d td="" ≤400<=""><td>81</td></d>	81		
<sup>a</sup> Data in this table should not supersede information on act	ual tanks.		

## Table 25 to Subpart G of Part 63—Effective Column Diameter (Fc)

Column type	Fc (feet)
9-inch by 7-inch built-up columns	1.1
8-inch-diameter pipe columns	0.7
No construction details known	1.0

## Table 26 to Subpart G of Part 63—Seal Related Factors for Internal Floating Roof Vessels

Seal type	Ks	n
Liquid mounted resilient seal:		
Primary seal only	3.0	0
With rim-mounted secondary seal <sup>a</sup>	1.6	0
Vapor mounted resilient seal:		
Primary seal only	6.7	0

#### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Seal type	Ks	n	
With rim-mounted secondary seal <sup>a</sup>	2.5	0	
<sup>a</sup> If vessel-specific information is not available about the secondary seal, assume only a primary seal is present.			

# Table 27 to Subpart G of Part 63—Summary of Internal Floating Deck Fitting Loss Factors (K<sub>F</sub>) and Typical Number of Fittings (N<sub>F</sub>)

Deck fitting type	Deck fitting loss factor (K <sub>F</sub> ) <sup>a</sup>	Typical number of fittings (N <sub>F</sub> )
Access hatch		1.
Bolted cover, gasketed	1.6	
Unbolted cover, gasketed	11	
Unbolted cover, ungasketed	<sup>b</sup> 25	
Automatic gauge float well		1.
Bolted cover, gasketed	5.1	
Unbolted cover, gasketed	15	
Unbolted cover, ungasketed	<sup>b</sup> 28	
Column well		(see Table 24).
Builtup column-sliding cover, gasketed	33	
Builtup column-sliding cover, ungasketed	<sup>b</sup> 47 10	
Pipe column-flexible fabric sleeve seal	19	
Pipe column-sliding cover, gasketed	32	
Pipe column-sliding cover, ungasketed		
Ladder well		1.
Sliding cover, gasketed	56	
Sliding cover, ungasketed	<sup>b</sup> 76	
Roof leg or hanger well		$(5 + D/10 + D^2/600)^{\circ}$ .
Adjustable	<sup>b</sup> 7.9	
Fixed	0	
Sample pipe or well		1.
Slotted pipe-sliding cover, gasketed	44	
Slotted pipe-sliding cover, ungasketed	57	
Sample well-slit fabric seal, 10 percent open area	<sup>b</sup> 12	
Stub drain, 1-in diameter <sup>d</sup>	1.2	(D <sup>2</sup> /125) <sup>c</sup> .
Vacuum breaker		1.
Weighted mechanical actuation, gasketed	<sup>b</sup> 0.7	
Weighted mechanical actuation, ungasketed	0.9	
<sup>a</sup> Units for K <sub>F</sub> are pound-moles per year.		
<sup>b</sup> If no specific information is available, this value ca currently used.	n be assumed to represent the most	common/typical deck fittings
<sup>c</sup> D = Tank diameter (feet).		
<sup>d</sup> Not used on welded contact internal floating decks.		

## Table 28 to Subpart G of Part 63—Deck Seam Length Factors<sup>a</sup> (S<sub>D</sub>) for Internal Floating Roof Tanks

### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Deck construction	Typical deck seam length factor			
Continuous sheet construction <sup>b</sup> :				
5-feet wide sheets	0.2°			
6-feet wide sheets	0.17			
7-feet wide sheets	0.14			
Panel construction <sup>d</sup> :				
$5 \times 7.5$ feet rectangular	0.33			
$5 \times 12$ feet rectangular	0.28			
<sup>a</sup> Deck seam loss applies to bolted decks only. Units for S <sup>D</sup> are feet per square feet.				

<sup>b</sup>  $S_D = 1/W$ , where W = sheet width (feet).

<sup>c</sup> If no specific information is available, these factors can be assumed to represent the most common bolted decks currently in use.

 $^{d}$  S<sub>D</sub> = (L + W)/LW, where W = panel width (feet), and L = panel length (feet).

## Table 29 to Subpart G of Part 63—Seal Related Factors for External Floating Roof Vessels

Seel torre	Weld	ed vessels	Riveted vessels	
Seal type	Ks	N	Ks	N
Metallic shoe seal:				
Primary seal only	1.2	1.5	1.3	1.5
With shoe-mounted secondary seal	0.8	1.2	1.4	1.2
With rim-mounted secondary seal	0.2	1.0	0.2	1.6
Liquid mounted resilient seal:				
Primary seal only	1.1	1.0	<sup>a</sup> NA	NA
With weather shield	0.8	0.9	NA	NA
With rim-mounted secondary seal	0.7	0.4	NA	NA
Vapor mounted resilient seal:				
Primary seal only	1.2	2.3	NA	NA
With weather shield	0.9	2.2	NA	NA
With rim-mounted secondary seal	0.2	2.6	NA	NA
<sup>a</sup> NA = Not applicable.				

## Table 30 to Subpart G of Part 63—Roof Fitting Loss Factors, KFa, KFb, and m,<sup>a</sup> and Typical Number of Fittings, NT

		Tunical number of		
Fitting type and construction details	K <sub>Fa</sub> (lb- mole/yr)	K <sub>Fb</sub> (lb- mole/[mi/hr] <sup>m</sup> -yr)	m (dimensionless)	fittings, N <sub>T</sub>
Access hatch (24-in-diameter well)				1.
Bolted cover, gasketed	0	0	° 0	
Unbolted cover, ungasketed	2.7	7.1	1.0	
Unbolted cover, gasketed	2.9	0.41	1.0	
Unslotted guide-pole well (8-in-diameter unslotted pole, 21-in-diameter well)				1.
Ungasketed sliding cover	0	67	° 0.98	

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Fitting type and construction details	K <sub>Fa</sub> (lb- mole/yr)	К <sub>Fb</sub> (lb- mole/[mi/hr] <sup>m</sup> -yr)	m (dimensionless)	fittings, N <sub>T</sub>	
Gasketed sliding cover	0	3.0	1.4		
Slotted guide-pole/sample well (8-in-diameter unslotted pole, 21-in-diameter well)				( <sup>d</sup> ).	
Ungasketed sliding cover, without float	0	310	1.2		
Ungasketed sliding cover, with float	0	29	2.0		
Gasketed sliding cover, without float	0	260	1.2		
Gasketed sliding cover, with float	0	8.5	1.4		
Gauge-float well (20-inch diameter)				1.	
Unbolted cover, ungasketed	2.3	5.9	° 1.0		
Unbolted cover, gasketed	2.4	0.34	1.0		
Bolted cover, gasketed	0	0	0		
Gauge-hatch/sample well (8-inch diameter)				1.	
Weighted mechanical actuation, gasketed	0.95	0.14	° 1.0		
Weighted mechanical actuation, ungasketed	0.91	2.4	1.0		
Vacuum breaker (10-in-diameter well)				N <sub>F6</sub> (Table 31).	
Weighted mechanical actuation, gasketed	1.2	0.17	° 1.0		
Weighted mechanical actuation, ungasketed	1.2	3.0	1.0		
Roof drain (3-in-diameter)				N <sub>F7</sub> (Table 31).	
Open	0	7.0	e 1.4	N <sub>F8</sub> (Table 32 <sup>f</sup> ).	
90 percent closed	0.51	0.81	1.0		
Roof leg (3-in-diameter)				N <sub>F8</sub> (Table 32 <sup>f</sup> ).	
Adjustable, pontoon area	1.5	0.20	° 1.0		
Adjustable, center area	0.25	0.067	° 1.0		
Adjustable, double-deck roofs	0.25	0.067	1.0		
Fixed	0	0	0		
Roof leg (21/2-in-diameter)				N <sub>F8</sub> (Table 32 <sup>f</sup> ).	
Adjustable, pontoon area	1.7	0	0		
Adjustable, center area	0.41	0	0		
Adjustable, double-deck roofs	0.41	0	0		
Fixed	0	0	0		
Rim vent (6-in-diameter)		_		1 <sup>g</sup> .	
Weighted mechanical actuation, gasketed	0.71	0.10	° 1.0		
Weighted mechanical actuation, ungasketed	0.68	1.8	1.0		
<sup>a</sup> The roof fitting loss factors, K <sub>Fa</sub> , K <sub>Fb</sub> , and m, n	nay only be us	ed for wind speeds from	m 2 to 15 miles per	hour.	
<sup>b</sup> Unit abbreviations are as follows: lb = pound;	mi = miles; hr	r = hour; yr = year.			
<sup>°</sup> If no specific information is available, this valucurrently in use.	ue can be assu	med to represent the m	ost common or typ	ical roof fittings	
<sup>d</sup> A slotted guide-pole/sample well is an optional fitting and is not typically used.					

<sup>e</sup> Roof drains that drain excess rainwater into the product are not used on pontoon floating roofs. They are, however, used on

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		T-mical number of		
Fitting type and construction details	K <sub>Fa</sub> (lb- mole/yr)	KFb (lb- mole/[mi/hr] <sup>m</sup> -yr)	m (dimensionless)	fittings, N <sub>T</sub>
double-deck floating roofs and are typically left of	open.			
<sup>f</sup> The most common roof leg diameter is 3 inches	The loss fact	ors for 21/2-inch diam	eter roof legs are n	provided for use if this

<sup>T</sup> The most common roof leg diameter is 3 inches. The loss factors for 21/2-inch diameter roof legs are provided for use if this smaller size roof is used on a particular floating roof.

<sup>g</sup> Rim vents are used only with mechanical-shoe primary seals.

## Table 31 to Subpart G of Part 63—Typical Number of Vacuum Breakers, NF6 and Roof Drains,<sup>a</sup> NF7

Tank diamatan D (faat)	No. of vacu	um breakers, N <sub>F6</sub>	No of your drains N - double deals your	
Tank ulameter D (leet)	Pontoon roof	Double-deck roof	No. of foot drains, N F7 double-deck foot	
50	1	1	1	
100	1	1	1	
150	2	2	2	
200	3	2	3	
250	4	3	5	
300	5	3	7	
350	6	4	d	
400	7	4	d	

<sup>a</sup> This table should not supersede information based on actual tank data.

<sup>b</sup> If the actual diameter is between the diameters listed, the closest diameter listed should be used. If the actual diameter is midway between the diameters listed, the next larger diameter should be used.

<sup>c</sup> Roof drains that drain excess rainwater into the product are not used on pontoon floating roofs. They are, however, used on double-deck floating roofs, and are typically left open.

<sup>d</sup> For tanks more than 300 feet in diameter, actual tank data or the manufacturer's recommendations may be needed for the number of roof drains.

## Table 32 to Subpart G of Part 63-Typical Number of Roof Legs,<sup>a</sup> NF8

Tank diamotor D (fast)	Pontoo	n roof	No of logs on double deals roof	
Tank diameter D (leet)	No. of pontoon legs	No. of center legs	No. of legs of double-deck fool	
30	4	2	6	
40	4	4	7	
50	6	6	8	
60	9	7	10	
70	13	9	13	
80	15	10	16	
90	16	12	20	
100	17	16	25	
110	18	20	29	
120	19	24	34	
130	20	28	40	
140	21	33	46	
150	23	38	52	
Tank diamatan D (faat)b	Pontoon roof		No. of long on double deals woof	
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Tank diameter D (feet)"	No. of pontoon legs	No. of center legs	No. of legs on double-deck roof	
160	26	42	58	
170	27	49	66	
180	28	56	74	
190	29	62	82	
200	30	69	90	
210	31	77	98	
220	32	83	107	
230	33	92	115	
240	34	101	127	
250	34	109	138	
260	36	118	149	
270	36	128	162	
280	37	138	173	
290	38	148	186	
300	38	156	200	
310	39	168	213	
320	39	179	226	
330	40	190	240	
340	41	202	255	
350	42	213	270	
360	44	226	285	
370	45	238	300	
380	46	252	315	
390	47	266	330	
400	48	281	345	

<sup>a</sup> This table should not supersede information based on actual tank data.

<sup>b</sup> If the actual diameter is between the diameters listed, the closest diameter listed should be used. If the actual diameter is midway between the diameters listed, the next larger diameter should be used.

# Table 33 to Subpart G of Part 63—Saturation Factors

Cargo carrier	Mode of operation	S factor
Tank trucks and rail tank cars	Submerged loading of a clean cargo tank	0.50
	Submerged loading: dedicated normal service	0.60
	Submerged loading: dedicated vapor balance service	1.00
	Splash loading of a clean cargo tank	1.45
	Splash loading: dedicated normal service	1.45
	Splash loading: dedicated vapor balance service	1.00

Table 34 to Subpart G of Part 63—Fraction Measured (Fm) and Fraction Emitted (Fe) For HAP Compounds in Wastewater Streams

Chemical name	CAS Number <sup>a</sup>	Fm	Fe
Acetaldehyde	75070	1.00	0.48
Acetonitrile	75058	0.99	0.36
Acetophenone	98862	0.31	0.14
Acrolein	107028	1.00	0.43
Acrylonitrile	107131	1.00	0.43
Allyl chloride	107051	1.00	0.89
Benzene	71432	1.00	0.80
Benzyl chloride	100447	1.00	0.47
Biphenyl	92524	0.86	0.45
Bromoform	75252	1.00	0.49
Butadiene (1,3-)	106990	1.00	0.98
Carbon disulfide	75150	1.00	0.92
Carbon tetrachloride	56235	1.00	0.94
Chlorobenzene	108907	1.00	0.73
Chloroform	67663	1.00	0.78
Chloroprene (2-Chloro-1,3-butadiene)	126998	1.00	0.68
Cumene	98828	1.00	0.88
Dichlorobenzene (p-)	106467	1.00	0.72
Dichloroethane (1,2-) (Ethylene dichloride)	107062	1.00	0.64
Dichloroethyl ether (Bis(2-Chloroethyl ether))	111444	0.76	0.21
Dichloropropene (1,3-)	542756	1.00	0.76
Diethyl sulfate	64675	0.0025	0.11
Dimethyl sulfate	77781	0.086	0.079
Dimethylaniline (N,N-)	121697	0.00080	0.34
Dimethylhydrazine (1,1-)	57147	0.38	0.054
Dinitrophenol (2,4-)	51285	0.0077	0.060
Dinitrotoluene (2,4-)	121142	0.085	0.18
Dioxane (1,4-) (1,4-Diethyleneoxide)	123911	0.87	0.18
Epichlorohydrin(1-Chloro-2,3-epoxypropane)	106898	0.94	0.35
Ethyl acrylate	140885	1.00	0.48
Ethylbenzene	100414	1.00	0.83
Ethyl chloride (Chloroethane)	75003	1.00	0.90
Ethylene dibromide (Dibromomethane)	106934	1.00	0.57
Ethylene glycol dimethyl ether	110714	0.86	0.32
Ethylene glycol monobutyl ether acetate	112072	0.043	0.067
Ethylene glycol monomethyl ether acetate	110496	0.093	0.048
Ethylene oxide	75218	1.00	0.50
Ethylidene dichloride (1,1-Dichloroethane)	75343	1.00	0.79
Hexachlorobenzene	118741	0.97	0.64
Hexachlorobutadiene	87683	0.88	0.86

Hexachloroethane         67721         0.50         0.85           Hexame         110543         1.00         1.00           Isophorone         78591         0.51         0.51           Methanol         67561         0.85         0.17           Methyl bromide (Bromomethane)         74839         1.00         0.85           Methyl chloride (Chloromethane)         74873         1.00         0.84           Methyl letherde (Hexone)         108101         0.98         0.53           Methyl tert-butyl ether         1634044         1.00         0.57           Methyl tert-butyl ether         1634044         1.00         0.57           Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Prosylene dichloride (1,2-Dichloropropane)         78875         1.00         0.60           Styrene         100425         1.00         0.60           Styrene         100425         1.00         0.60           Tetrachloroethane (1,1,2,2)         7345         1.00         0.64           Trichloroethane (1,1,2,2)         7345         1.00         0.60           Trichloroethane (1,1,2,2)         735	Chemical name	CAS Number <sup>a</sup>	Fm	Fe
Hexane         110543         1.00         1.00           Isophorone         78591         0.51         0.11           Methanol         67561         0.85         0.17           Methyl bromide (Bromomethane)         74839         1.00         0.85           Methyl nomide (Bromomethane)         74873         1.00         0.84           Methyl nethacrylate         80626         1.00         0.37           Methyl ter-butyl ether         1634044         1.00         0.57           Methylenchoride (Dichloromethane)         75092         1.00         0.77           Naphthalene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropopane (2-)         79469         0.90         0.44           Propionaldehyde         123386         1.00         0.41           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.60           Styrene         100425         1.00         0.61           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.62           Trichloroethane (1,1,2,2-)         102181         1.00         <	Hexachloroethane	67721	0.50	0.85
Isophorone         78591         0.51         0.11           Methanol         67561         0.85         0.17           Methyl bromide (Bromomethane)         74839         1.00         0.84           Methyl choride (Chloromethane)         74873         1.00         0.84           Methyl laboride (Chloromethane)         108101         0.98         0.53           Methyl ter-butyl etber         1634044         1.00         0.57           Methyl ter-butyl etber         1634044         1.00         0.57           Methyl ter-butyl etber         1634044         1.00         0.77           Maphthalene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Propionaldehyde         123386         1.00         0.41           Propoylene dichloride (1,2-Dichloropropane)         78875         1.00         0.60           Styrene         100425         1.00         0.60           Styrene         100425         1.00         0.60           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.60           Trichaloroethane (1,1,2,2-)	Hexane	110543	1.00	1.00
Methanol         67561         0.85         0.17           Methyl bromide (Bromomethane)         74839         1.00         0.85           Methyl chloride (Chloromethane)         74873         1.00         0.84           Methyl nebharcylate         80626         1.00         0.37           Methyl methacrylate         80626         1.00         0.37           Methyl methacrylate         1634044         1.00         0.57           Methyl methacrylate         1634044         1.00         0.57           Methyl methacrylate         1634044         1.00         0.57           Nitrobenzene         98953         0.39         0.23           Nitrobenzene         98953         0.39         0.24           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.60           Styrene         100425         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.64           Trichloroethylene (1,1.2) (Vinyl Trichloride)         79005	Isophorone	78591	0.51	0.11
Methyl bromide (Bromomethane)         74839         1.00         0.85           Methyl chloride (Choromethane)         74873         1.00         0.84           Methyl isobutyl ketone (Hexone)         108101         0.98         0.53           Methyl methacrylate         80626         1.00         0.37           Methyl methacrylate         1634044         1.00         0.57           Methyl ert-butyl ether         1634044         1.00         0.57           Nitrobenzene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropopane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.80           Styrene         100425         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethare (1,1,2,2-)         79354         1.00         0.80           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.80           Tolukne         101425         1.00         0.64           Trichloroethane (1,1,2-) (Vinyl Trichloride) <td>Methanol</td> <td>67561</td> <td>0.85</td> <td>0.17</td>	Methanol	67561	0.85	0.17
Methyl chloride (Chloromethane)         74873         1.00         0.84           Methyl isobutyl ketone (Hexone)         108101         0.98         0.53           Methyl methacrylate         80626         1.00         0.37           Methylen chloride (Dichloromethane)         75092         1.00         0.57           Naphthalene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Tolucane         108833         1.00         0.60           Trichlorobenzene (1,2,4-)         120821         1.00         0.64           Trichlorobenzene (1,2,4-)         120821         1.00         0.64 <td< td=""><td>Methyl bromide (Bromomethane)</td><td>74839</td><td>1.00</td><td>0.85</td></td<>	Methyl bromide (Bromomethane)	74839	1.00	0.85
Methyl isobutyl ketone (Hexone)         108101         0.98         0.53           Methyl methacrylate         80626         1.00         0.37           Methyl tert-butyl ether         1634044         1.00         0.57           Methyl tert-butyl ether         1634044         1.00         0.77           Naphthalene         91203         0.99         0.51           Nitrobenzene         98853         0.39         0.23           Nitropopane (2-)         79469         0.99         0.44           Propionaldehyde         123386         1.00         0.87           Propionaldehyde         123386         1.00         0.72           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.80           Styrene         100425         1.00         0.80           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.44           Toiluane         108833         1.00         0.80           Trichloroethare (1,1,2,2)         79345         1.00         0.46           Trichloroethare (1,2,4-)         120821         1.00         0.64           Trichloroethare (1,1,2) (Vinyl Trichloride)         79015         1.00         0.61	Methyl chloride (Chloromethane)	74873	1.00	0.84
Methyl methacrylate         80626         1.00         0.37           Methyl tert-butyl ether         1634044         1.00         0.57           Methylene chloride (Dichloromethane)         75092         1.00         0.77           Naphthalene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.60           Styrene         100425         1.00         0.60           Styrene         100425         1.00         0.46           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Toluene         108883         1.00         0.60           Trichloroethylene (Perchloroethylene)         127184         1.00         0.60           Trichloroethane (1,1,2,-)         120821         1.00         0.64           Trichloroethane (1,1,-) (Methyl chloroform)         71556         1.00         0.60           Trichloroethan	Methyl isobutyl ketone (Hexone)	108101	0.98	0.53
Methyl tert-butyl ether         1634044         1.00         0.57           Methylene chloride (Dichloromethane)         75092         1.00         0.77           Naphthalene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         12386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.60           Styrene         100425         1.00         0.60           Styrene         100425         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.64           Trichlorobenzene (1,2,4)         120821         1.00         0.64           Trichlorobethane (1,1,2) (Winyl Trichloride)         79005         1.00         0.61           Trichlorobethane (1,1,2) (Winyl Trichloride)         79055         1.00         0.61           Trichlorobenzene (1,2,4)         120821         1.00         0.83	Methyl methacrylate	80626	1.00	0.37
Methylene chloride (Dichloromethane)         75092         1.00         0.77           Naphthalene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.72           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.44           Toluen         108883         1.00         0.80           Toluine (o-)         95534         0.15         0.052           Trichloroethane (1,1,1-) (Methyl chloroform)         11556         1.00         0.91           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79016         1.00         0.80           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79015         1.00         0.91           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79016         1.00         0.87	Methyl tert-butyl ether	1634044	1.00	0.57
Naphthalene         91203         0.99         0.51           Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.72           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.46           Toluene         108883         1.00         0.64           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.69           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.60           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.60           Trichlorophenol (2,4,5-)         95954         0.11         0.88           Triechloroethylene         79016         1.00         0.38	Methylene chloride (Dichloromethane)	75092	1.00	0.77
Nitrobenzene         98953         0.39         0.23           Nitropropane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.41           Propylen dichloride (1,2-Dichloropropane)         78875         1.00         0.72           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.46           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Tolucne         108883         1.00         0.80           Tolidirie (o-)         95534         0.15         0.052           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.64           Trichloroethylene         79005         1.00         0.60           Trichloroethylene (1,2,4-)         120821         1.00         0.64           Trichloroethylene (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.60           Trichloroethylene (1,2,4-)         1.00         0.87         0.59	Naphthalene	91203	0.99	0.51
Nitropropane (2-)         79469         0.99         0.44           Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.72           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.64           Trichlorobenzene (1,2,4-)         10883         1.00         0.80           Trichlorobenzene (1,2,4-)         120821         1.00         0.64           Trichlorobenzene (1,2,4-)         1.00         0.66         1.00         0.87           Trichlorobenzene (1,2,4-)         100         0.86         1.00         0.87           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.87           Trichloroethane (2,4,5-)         99594         0.11         0.086           Trichlorophenol (2,4,5-)         540841         1.00	Nitrobenzene	98953	0.39	0.23
Phosgene         75445         1.00         0.87           Propionaldehyde         123386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.72           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.80           Trichlorobenzene (1,2,4-)         120821         1.00         0.64           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.91           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.60           Trichloroethylene         79016         1.00         0.87           Trichloroethylene         79016         1.00         0.87           Trichloroethylene         79016         1.00         0.88           Trichloroethylene         79016         1.00         0.87           Trichloroethylene         7554         0.11         0.86	Nitropropane (2-)	79469	0.99	0.44
Propionaldehyde         123386         1.00         0.41           Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.72           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.80           Trichlorobenzene (1,2,4-)         120821         1.00         0.64           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.64           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.64           Trichloroethylene         79016         1.00         0.64           Trichloroethylene         79016         1.00         0.60           Trichloroethylene         79016         1.00         0.87           Trichloroethylene         79016         1.00         0.88           Trichloroethylene         75014         1.00         0.38           Trichloroethylene         1.00         0.59         1.01         0.59 </td <td>Phosgene</td> <td>75445</td> <td>1.00</td> <td>0.87</td>	Phosgene	75445	1.00	0.87
Propylene dichloride (1,2-Dichloropropane)         78875         1.00         0.72           Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.80           Toluidine (o-)         95534         0.15         0.052           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.64           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.64           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.60           Trichloroethane (1,2,4-)         120821         1.00         0.87           Trichloroethane (1,2,-) (Vinyl Trichloride)         79005         1.00         0.87           Trichloroethylene         79016         1.00         0.87           Trichloroethylene         1.00         0.88           Trichloroethylene         75014         1.00         0.38           Trimethylpentate (2,2,4-)         540841         1.00	Propionaldehyde	123386	1.00	0.41
Propylene oxide         75569         1.00         0.60           Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.80           Toluidine (o-)         95534         0.15         0.052           Trichlorobenzene (1,2,4-)         120821         1.00         0.64           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.91           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.60           Trichloroethane (1,2,4-)         95954         0.11         0.086           Trichloroethylene         79016         1.00         0.87           Trichlorophenol (2,4,5-)         95954         0.11         0.086           Trimethylpentane (2,2,4-)         540841         1.00         0.38           Trimethylpentane (2,2,4-)         75014         1.00         0.97           Vinyl chloride (Chloroethylene)         7534         1.00         0.94           Xylene (m-)         108383         1.00         0.82	Propylene dichloride (1,2-Dichloropropane)	78875	1.00	0.72
Styrene         100425         1.00         0.80           Tetrachloroethane (1,1,2,2-)         79345         1.00         0.46           Tetrachloroethylene (Perchloroethylene)         127184         1.00         0.92           Toluene         108883         1.00         0.80           Toluidine (o-)         95534         0.15         0.052           Trichloroethane (1,2,4-)         120821         1.00         0.64           Trichloroethane (1,1,1-) (Methyl chloroform)         71556         1.00         0.91           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79005         1.00         0.60           Trichloroethane (1,1,2-) (Vinyl Trichloride)         79016         1.00         0.87           Trichloroethylene         79016         1.00         0.86           Trichlorophenol (2,4,5-)         95954         0.11         0.086           Trimethylpentane (2,2,4-)         540841         1.00         0.38           Vinyl acetate         108054         1.00         0.97           Vinylidene chloride (1,1-Dichloroethylene)         75354         1.00         0.94           Xylene (m-)         108383         1.00         0.82           Xylene (o-)         95476         1.00         <	Propylene oxide	75569	1.00	0.60
Tetrachloroethane (1,1,2,2-)793451.000.46Tetrachloroethylene (Perchloroethylene)1271841.000.92Toluene1088831.000.80Toluidine (o-)955340.150.052Trichloroethane (1,2,4-)1208211.000.64Trichloroethane (1,1,-) (Methyl chloroform)715561.000.91Trichloroethane (1,1,2-) (Vinyl Trichloride)790051.000.60Trichloroethane (1,2,5-)959540.110.086Trichlorophenol (2,4,5-)959540.110.086Trimethylpentane (2,2,4-)5408411.000.38Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Styrene	100425	1.00	0.80
Tetrachloroethylene (Perchloroethylene)1271841.000.92Toluene1088831.000.80Toluidine (o-)955340.150.052Trichlorobenzene (1,2,4-)1208211.000.64Trichloroethane (1,1,1-) (Methyl chloroform)715561.000.91Trichloroethane (1,1,2-) (Vinyl Trichloride)790051.000.60Trichloroethylene790161.000.87Trichlorophenol (2,4,5-)959540.110.086Trimethylpentane (2,2,4-)5408411.000.38Trimethylpentane (2,2,4-)5408411.000.59Vinyl acetate1080541.000.97Vinylidene chloride (1,1-Dichloroethylene)750141.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Tetrachloroethane (1,1,2,2-)	79345	1.00	0.46
Toluene1088831.000.80Toluidine (o-)955340.150.052Trichlorobenzene (1,2,4-)1208211.000.64Trichloroethane (1,1,1-) (Methyl chloroform)715561.000.91Trichloroethane (1,1,2-) (Vinyl Trichloride)790051.000.60Trichloroethylene790161.000.87Trichlorophenol (2,4,5-)959540.110.086Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.000.59Vinyl acetate1080541.000.97Vinylidene chloride (1,1-Dichloroethylene)750141.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Tetrachloroethylene (Perchloroethylene)	127184	1.00	0.92
Toluidine (o-)955340.150.052Trichlorobenzene (1,2,4-)1208211.000.64Trichloroethane (1,1,1-) (Methyl chloroform)715561.000.91Trichloroethane (1,1,2-) (Vinyl Trichloride)790051.000.60Trichloroethylene790161.000.87Trichlorophenol (2,4,5-)959540.110.0866Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.000.59Vinyl acetate1080541.000.97Vinyl chloride (Chloroethylene)750141.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Toluene	108883	1.00	0.80
Trichlorobenzene (1,2,4-)1208211.000.64Trichloroethane (1,1,1-) (Methyl chloroform)715561.000.91Trichloroethane (1,1,2-) (Vinyl Trichloride)790051.000.60Trichloroethylene790161.000.87Trichlorophenol (2,4,5-)959540.110.086Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.001.00Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.82Xylene (m-)1083831.000.82Xylene (p-)1064231.000.79	Toluidine (o-)	95534	0.15	0.052
Trichloroethane (1,1,1-) (Methyl chloroform)715561.000.91Trichloroethane (1,1,2-) (Vinyl Trichloride)790051.000.60Trichloroethylene790161.000.87Trichlorophenol (2,4,5-)959540.110.086Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.000.59Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.82Xylene (m-)1083831.000.82Xylene (p-)1064231.000.82	Trichlorobenzene (1,2,4-)	120821	1.00	0.64
Trichloroethane (1,1,2-) (Vinyl Trichloride)790051.000.60Trichloroethylene790161.000.87Trichlorophenol (2,4,5-)959540.110.086Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.001.00Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Trichloroethane (1,1,1-) (Methyl chloroform)	71556	1.00	0.91
Trichloroethylene790161.000.87Trichlorophenol (2,4,5-)959540.110.086Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.001.00Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Trichloroethane (1,1,2-) (Vinyl Trichloride)	79005	1.00	0.60
Trichlorophenol (2,4,5-)959540.110.086Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.001.00Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Trichloroethylene	79016	1.00	0.87
Triethylamine1214481.000.38Trimethylpentane (2,2,4-)5408411.001.00Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Trichlorophenol (2,4,5-)	95954	0.11	0.086
Trimethylpentane (2,2,4-)5408411.001.00Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Triethylamine	121448	1.00	0.38
Vinyl acetate1080541.000.59Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Trimethylpentane (2,2,4-)	540841	1.00	1.00
Vinyl chloride (Chloroethylene)750141.000.97Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Vinyl acetate	108054	1.00	0.59
Vinylidene chloride (1,1-Dichloroethylene)753541.000.94Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Vinyl chloride (Chloroethylene)	75014	1.00	0.97
Xylene (m-)1083831.000.82Xylene (o-)954761.000.79Xylene (p-)1064231.000.82	Vinylidene chloride (1,1-Dichloroethylene)	75354	1.00	0.94
Xylene (o-)       95476       1.00       0.79         Xylene (p-)       106423       1.00       0.82	Xylene (m-)	108383	1.00	0.82
Xylene (p-) 106423 1.00 0.82	Xylene (o-)	95476	1.00	0.79
	Xylene (p-)	106423	1.00	0.82

<sup>a</sup> CAS numbers refer to the Chemical Abstracts Service registry number assigned to specific compounds, isomers, or mixtures of compounds.

[59 FR 19468, Apr. 22, 1994, as amended at 71 FR 76615, Dec. 21, 2006]

# Table 35 to Subpart G of Part 63—Control Requirements for Items of Equipment That Meet the Criteria of §63.149of Subpart G

#### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

Item of equipment	Control requirement <sup>a</sup>	
Drain or drain hub	<ul> <li>(a) Tightly fitting solid cover (TFSC); or</li> <li>(b) TFSC with a vent to either a process, or to a fuel gas system, or to a control device meeting the requirements of <u>§ 63.139(c)</u>; or</li> <li>(c) Water seal with submerged discharge or barrier to protect discharge from wind.</li> </ul>	
Manhole <sup>b</sup>	<ul> <li>(a) TFSC; or</li> <li>(b) TSFC with a vent to either a process, or to a fuel gas system, or to a control device meeting the requirements of § 63.139(c); or</li> <li>(c) If the item is vented to the atmosphere, use a TFSC with a properly operating water seal at the entrance or exit to the item to restrict ventilation in the collection system. The vent pipe shall be at least 90 cm in length and not exceeding 10.2 cm in nominal inside diameter.</li> </ul>	
Lift station	<ul> <li>(a) TFSC; or</li> <li>(b) TFSC with a vent to either a process, or to a fuel gas system, or to a control device meeting the requirements of <u>§ 63.139(c)</u>; or</li> <li>(c) If the lift station is vented to the atmosphere, use a TFSC with a properly operating water seal at the entrance or exit to the item to restrict ventilation in the collection system. The vent pipe shall be at least 90 cm in length and not exceeding 10.2 cm in nominal inside diameter. The lift station shall be level controlled to minimize changes in the liquid level.</li> </ul>	
Trench	<ul> <li>(a) TFSC; or</li> <li>(b) TFSC with a vent to either a process, or to a fuel gas system, or to a control device meeting the requirements of § 63.139(c); or</li> <li>(c) If the item is vented to the atmosphere, use a TFSC with a properly operating water seal at the entrance or exit to the item to restrict ventilation in the collection system. The vent pipe shall be at least 90 cm in length and not exceeding 10.2 cm in nominal inside diameter.</li> </ul>	
Pipe	Each pipe shall have no visible gaps in joints, seals, or other emission interfaces.	
Oil/Water separator	(a) Equip with a fixed roof and route vapors to a process or to a fuel gas system, or equip with a closed vent system that routes vapors to a control device meeting the requirements of § $63.139(c)$ ; or (b) Equip with a floating roof that meets the equipment specifications of § $60.693$ (a)(1)(i), (a)(1)(ii), (a)(2), (a)(3), and (a)(4).	
Tank°	Maintain a fixed roof. <sup>d</sup> If the tank is sparged <sup>e</sup> or used for heating or treating by means of an exothermic reaction, a fixed roof and a system shall be maintained that routes the organic hazardous air pollutants vapors to other process equipment or a fuel gas system, or a closed vent system that routes vapors to a control device that meets the requirements of $\frac{40 \text{ CFR } \$ 63.119 \text{ (e)}(1)}{100000000000000000000000000000000000$	
<sup>a</sup> Where a tight of sampling,	ntly fitting solid cover is required, it shall be maintained with no visible gaps or openings, except during periods inspection, or maintenance.	
<sup>b</sup> Manhole includes sumps and other points of access to a conveyance system.		
<sup>c</sup> Applies to tanks with capacities of 38 m <sup>3</sup> or greater.		
<sup>a</sup> A fixed roof may have openings necessary for proper venting of the tank, such as pressure/vacuum vent, j-pipe vent.		
<sup>e</sup> The liquid in the tank is agitated by injecting compressed air or gas.		

# Table 36 to Subpart G of Part 63—Compound Lists Used for Compliance Demonstrations for Enhanced Biological Treatment Processes (See § 63.145(h))

List 1	List 2
Acetonitrile	Acetaldehyde.
Acetophenone	Acrolein.
Acrylonitrile	Allyl Chloride.
Biphenyl	Benzene.

List 1	List 2
Chlorobenzene	Benzyl Chloride,
Dichloroethyl Ether	Bromoform.
Diethyl Sulfate	Bromomethane.
Dimethyl Sulfate	Butadiene 1,3.
Dimethyl Hydrazine 1,1	Carbon Disulfide.
Dinitrophenol 2,4	Carbon Tetrachloride
Dinitrotoluene 2,4	Chloroethane (ethyl chloride).
Dioxane 1,4	Chloroform.
Ethylene Glycol Monobutyl Ether Acetate	Chloroprene.
Ethylene Glycol Monomethyl Ether Acetate	Cumene (isopropylbenzene).
Ethylene Glycol Dimethyl Ether	Dibromoethane 1,2.
Hexachlorobenzene	Dichlorobenzene 1,4.
Isophorone	Dichloroethane 1,2.
Methanol	Dichloroethane 1,1 (ethylidene dichloride).
Methyl Methacrylate	Dichloroethene 1,1 (vinylidene chloride).
Nitrobenzene	Dichloropropane 1,2.
Toluidine	Dichloropropene 1,3.
Trichlorobenzene 1,2,4.	Dimethylaniline N,N.
Trichlorophenol 2,4,6	Epichlorohydrin.
Triethylamine	Ethyl Acrylate.
	Ethylbenzene.
	Ethylene Oxide.
	Ethylene Dibromide.
	Hexachlorobutadiene.
	Hexachloroethane.
	Hexane-n.
	Methyl Isobutyl Ketone.
	Methyl Tertiary Butyl Ether.
	Methyl Chloride.
	Methylene Chloride (dichloromethane).
	Naphthalene.
	Nitropropane 2
	Phosgene.
	Propionaldehyde.
	Propylene Oxide.
	Styrene.
	Tetrachloroethane 1,1,2,2.
	TolueneTrichloroethane 1,1,1 (methyl chloroform).

## National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

List 1	List 2
	Trichloroethane 1,1,2.
	Trichloroethylene.
	Trimethylpentane 2,2,4.
	Vinyl Chloride.
	Vinyl Acetate.
	Xylene-m.
	Xylene-o.
	Xylene-p.

[59 FR 19468, Apr. 22, 1994, as amended at 71 FR 76615, Dec. 21, 2006]

## Table 37 to Subpart G of Part 63—Default Biorates for List 1 Compounds

Compound name	Biorate, K1 L/g MLVSS-hr
Acetonitrile	0.100
Acetophenone	0.538
Acrylonitrile	0.750
Biphenyl	5.643
Chlorobenzene	10.000
Dichloroethyl ether	0.246
Diethyl sulfate	0.105
Dimethyl hydrazine(1,1)	0.227
DIMethyl sulfate	0.178
Dinitrophenol 2,4	0.620
Dinitrotoluene(2,4)	0.784
Dioxane(1,4)	0.393
Ethylene glycol dimethyl ether	0.364
Ethylene glycol monomethyl ether acetate	0.159
Ethylene glycol monobutyl ether acetate	0.496
Hexachlorobenzene	16.179
ISophorone	0.598
Methanol	0.200
Methyl methacrylate	4.300
Nitrobenzene	2.300
Toluidine (-0)	0.859
Trichlorobenzene 1,2,4	4.393
Trichlorophenol 2,4,5	4.477
Triethylamine	1.064

#### Table 38 to Subpart G of Part 63—Toxic Equivalency Factors

Table 38 to Subpart G of Part 63—Toxic Equivalency Factors

Dioxin and furan congener	Toxic equivalency factor
1,2,3,7,8-pentachlorodibenzo-p-dioxin	1
1,2,3,4,7,8-hexachlorodibenzo-p-dioxin	0.1
1,2,3,7,8,9-hexachlorodibenzo-p-dioxin	0.1
1,2,3,6,7,8-hexachlorodibenzo-p-dioxin	0.1
1,2,3,4,6,7,8-heptachlorodibenzo-p-dioxin	0.01
octachlorodibenzo-p-dioxin	0.0003
2,3,7,8-tetrachlorodibenzofuran	0.1
2,3,4,7,8-pentachlorodibenzofuran	0.3
1,2,3,7,8-pentachlorodibenzofuran	0.03
1,2,3,4,7,8-hexachlorodibenzofuran	0.1
1,2,3,6,7,8-hexachlorodibenzofuran	0.1
1,2,3,7,8,9-hexachlorodibenzofuran	0.1
2,3,4,6,7,8-hexachlorodibenzofuran	0.1
1,2,3,4,6,7,8-heptachlorodibenzofuran	0.01
1,2,3,4,7,8,9-heptachlorodibenzofuran	0.01
Octachlorodibenzofuran	0.0003

[89 FR 43220, May 16, 2024]

# Figure 1 to Subpart G of Part 63—Definitions of Terms Used in Wastewater Equations

Main Terms

AMR = Actual mass removal of Table 8 and/or Table 9 compounds achieved by treatment process or a series of treatment processes, kg/hr.

C = Concentration of Table 8 and/or Table 9 compounds in wastewater, ppmw.

CG = Concentration of TOC (minus methane and ethane) or total organic hazardous air pollutants, in vented gas stream, dry basis, ppmv.

 $CG_c$  = Concentration of TOC or organic hazardous air pollutants corrected to 3-percent oxygen, in vented gas stream, dry basis, ppmv.

CGS = Concentration of sample compounds in vented gas stream, dry basis, ppmv.

E = Removal or destruction efficiency, percent.

 $F_{bio}$  = Site-specific fraction of Table 8 and/or Table 9 compounds biodegraded, unitless.

f<sup>bio</sup> = Site-specific fraction of an individual Table 8 or Table 9 compound biodegraded, unitless.

Fm = Compound-specific fraction measured factor, unitless (listed in table 34).

Fr = Fraction removal value for Table 8 and/or Table 9 compounds, unitless (listed in Table 9).

 $Fr_{avg} = Flow$ -weighted average of the Fr values.

i = Identifier for a compound.

j = Identifier for a sample.

k = Identifier for a run.

### National Emission Standards for Organic Hazardous Air Pollutants From the Synthetic Organic Chemical Manufacturing Industry for Process Vents, Storage Vessels, Transfer Operations, and Wastewater

 $K_2 = Constant$ , 41.57 \* 10<sup>-9</sup>, (ppm)<sup>-1</sup> (gram-mole per standard m<sup>3</sup>) (kg/g), where standard temperature (gram-mole per standard m<sup>3</sup>) is 20 °C.

m = Number of samples.

M = Mass, kg.

MW = Molecular weight, kg/kg-mole.

n = Number of compounds.

p = Number of runs.

 $O_{2d}$  = Concentration of oxygen, dry basis, percent by volume.

Q = Volumetric flowrate of wastewater, m<sup>3</sup>/hr.

QG = Volumetric flow rate of vented gas stream, dry standard, m<sup>3</sup>/min.

QMG = Mass flowrate of TOC (minus methane and ethane) or organic hazardous air pollutants, in vented gas stream, kg/hr.

QMW = Mass flowrate of Table 8 and/or Table 9 compounds in wastewater, kg/hr.

 $\rho = \text{Density}, \text{kg/m}^3.$ 

RMR = Required mass removal achieved by treatment process or a series of treatment processes, kg/hr.

 $t_T = Total time of all runs, hr.$ 

Subscripts

- a = Entering.
- b = Exiting.
- i = Identifier for a compound.
- j = Identifier for a sample.

k = Identifier for a run.

m = Number of samples.

n = Number of compounds.

p = Number of runs.

T = Total; sum of individual.

[<u>59 FR 19468</u>, Apr. 22, 1994, as amended at <u>59 FR 29201</u>, June 6, 1994; <u>61 FR 63629</u>, Dec. 12, 1995; <u>62 FR 2779</u>, Jan. 17, 1997; <u>63 FR 67793</u>, Dec. 9, 1998; <u>64 FR 20195</u>, Apr. 26, 1999; <u>65 FR 78284</u>, Dec. 14, 2000; <u>66 FR 6935</u>, Jan. 22, 2001]

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# Subpart H—National Emission Standards for Hazardous Air Pollutants for Equipment Leaks and Fenceline Monitoring for All Emission Sources

Source:

59 FR 19568, Apr. 22, 1994, unless otherwise noted.

# § 63.160 Applicability and designation of source.

(a) The provisions of this subpart apply to pumps, compressors, agitators, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, surge control vessels, bottoms receivers, instrumentation systems, and control devices or closed vent systems required by this subpart that are intended to operate in organic hazardous air pollutant service 300 hours or more during the calendar year within a source subject to the provisions of a specific subpart in <u>40 CFR part 63</u> that references this subpart.

(b) After the compliance date for a process unit, equipment to which this subpart applies that are also subject to the provisions of:

(1) <u>Part 60 of this chapter</u> will be required to comply only with the provisions of this subpart, except as specified in <u>§§</u> <u>60.480a(e)(2)(i)</u> and <u>60.480b(e)(2)(i)</u> of this chapter.

(2) <u>40 CFR part 61</u> will be required to comply only with the provisions of this subpart.

(c) If a process unit subject to the provisions of this subpart has equipment to which this subpart does not apply, but which is subject to a standard identified in paragraph (c)(1), (2), or (3) of this section, the owner or operator may elect to apply this subpart to all such equipment in the process unit. If the owner or operator elects this method of compliance, all VOC in such equipment shall be considered, for purposes of applicability and compliance with this subpart, as if it were organic hazardous air pollutant (HAP). Compliance with the provisions of this subpart, in the manner described in this paragraph, shall be deemed to constitute compliance with the standard identified in paragraph (c)(1), (2), or (3) of this section.

(1) Part 60, subpart VV, VVa, VVb, GGG, or KKK, of this chapter, except as specified in  $\underline{\$\$}$  <u>60.480a(e)(2)(i)</u> and <u>60.480b(e)(2)(i)</u> of this chapter;

(2) Part 61, subpart F or J of this chapter; or

(3) Part 264, subpart BB of this chapter or part 265, subpart BB of this chapter.

(d) The provisions in  $\frac{63.1(a)(3)}{2}$  of subpart A of this part do not alter the provisions in paragraph (b) of this section.

(e) Except as provided in any subpart that references this subpart, lines and equipment not containing process fluids are not subject to the provisions of this subpart. Utilities, and other non-process lines, such as heating and cooling systems which do not combine their materials with those in the processes they serve, are not considered to be part of a process unit.

(f) The provisions of this subpart do not apply to research and development facilities or to bench-scale batch processes, regardless of whether the facilities or processes are located at the same plant site as a process subject to the provisions of this subpart.

(g) Alternative means of compliance — For each source as defined in  $\S$  63.101, and for each source as defined in  $\S$  63.191, on and after July 15, 2027, this paragraph no longer applies.

(1) Option to comply with <u>40 CFR part 65</u>. Owners or operators of CMPU that are subject to <u>§ 63.100</u> may choose to comply with the provisions of <u>40 CFR part 65</u> for all Group 1 and Group 2 process vents, Group 1 storage vessels, Group 1 transfer operations, and equipment that are subject to <u>§ 63.100</u>, that are part of the CMPU. Other provisions applying to an owner or operator who chooses to comply with <u>40 CFR part 65</u> are provided in <u>40 CFR 65.1</u>.

(2) Part 65, subpart C or F. For owners or operators choosing to comply with  $\frac{40 \text{ CFR part 65}}{100}$ , each surge control vessel and bottoms receiver subject to  $\frac{63.100}{100}$  that meets the conditions specified in table 2 or table 3 of this subpart shall meet the requirements for storage vessels in  $\frac{40 \text{ CFR part 65}}{100}$ , subpart C; all other equipment subject to  $\frac{63.100}{100}$  shall meet the requirements in  $\frac{40 \text{ CFR part 65}}{100}$ , subpart F.

(3) Part 63, subpart A. Owners or operators who choose to comply with 40 CFR part 65, subpart C or <u>F</u>, for equipment subject to  $\frac{63.100}{5}$  must also comply with the applicable general provisions of this part 63 listed in table 4 of this subpart. All sections and paragraphs of <u>subpart A of this part</u> that are not mentioned in table 4 of this subpart do not apply to owners or operators of equipment subject to  $\frac{63.100}{563.100}$  of subpart F complying with 40 CFR part 65, subpart C or <u>F</u>, except that

provisions required to be met prior to implementing 40 CFR part 65 still apply. Owners and operators who choose to comply with 40 CFR part 65, subpart C or F, must comply with 40 CFR part 65, subpart A.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48176</u>, Sept. 20, 1994; <u>59 FR 53360</u>, Oct. 24, 1994; <u>60 FR 18029</u>, Apr. 10, 1995; <u>61 FR 31439</u>, June 20, 1996; <u>64 FR 20198</u>, Apr. 26, 1999; <u>65 FR 78285</u>, Dec. 14, 2000; <u>89 FR 43220</u>, May 16, 2024]

# § 63.161 Definitions.

All terms used in this subpart shall have the meaning given them in the Act and in <u>subpart F of this part</u>, except as provided in any subpart that references this subpart.

[<u>89 FR 43221</u>, May 16, 2024]

# § 63.162 Standards: General.

(a) Compliance with this subpart will be determined by review of the records required by  $\S$  63.181 of this subpart and the reports required by  $\S$  63.182 of this subpart, review of performance test results, and by inspections.

(b)

(1) An owner or operator may request a determination of alternative means of emission limitation to the requirements of  $\frac{\&\&}{63.163}$  through  $\frac{63.170}{63.170}$ , and  $\frac{\&\&}{63.172}$  through  $\frac{63.174}{63.174}$  of this subpart as provided in & 63.177.

(2) If the Administrator makes a determination that a means of emission limitation is a permissible alternative to the requirements of  $\frac{8}{63.163}$  through  $\frac{63.170}{63.172}$  through  $\frac{63.174}{63.174}$  of this subpart, the owner or operator shall comply with the alternative.

(c) Each piece of equipment in a process unit to which this subpart applies shall be identified such that it can be distinguished readily from equipment that is not subject to this subpart. Identification of the equipment does not require physical tagging of the equipment. For example, the equipment may be identified on a plant site plan, in log entries, or by designation of process unit boundaries by some form of weatherproof identification.

(d) Equipment that is in vacuum service is excluded from the requirements of this subpart.

(e) Equipment that is in organic HAP service less than 300 hours per calendar year is excluded from the requirements of  $\frac{\$\$}{63.163}$  through  $\frac{63.174 \text{ of this subpart}}{63.174 \text{ of this subpart}}$  and  $\frac{\$ 63.178 \text{ of this subpart}}{163.174 \text{ of this subpart}}$  if it is identified as required in  $\frac{\$ 63.181(j) \text{ of this subpart}}{163.181(j) \text{ of this subpart}}$ .

(f) When each leak is detected as specified in  $\S$  63.163 and 63.164;  $\S$  63.168 and 63.169; and  $\S$  63.172 through 63.174 of this subpart, the following requirements apply:

(1) Clearly identify the leaking equipment.

(2) The identification on a valve may be removed after it has been monitored as specified in  $\frac{\$\$ 63.168(f)(3)}{\$}$ , and  $\frac{63.175(e)(7)(i)(D)}{\$}$  of this subpart, and no leak has been detected during the follow-up monitoring. If the owner or operator elects to comply using the provisions of  $\frac{\$ 63.174(e)(1)(i)}{\$}$  of this subpart, the identification on a connector may be removed after it is monitored as specified in  $\frac{\$ 63.174(e)(1)(i)}{\$}$  and no leak is detected during that monitoring.

(g) Except as provided in paragraph (g)(1) of this section, all terms in this subpart that define a period of time for completion of required tasks (e.g., weekly, monthly, quarterly, annual), refer to the standard calendar periods unless specified otherwise in the section or subsection that imposes the requirement.

(1) If the initial compliance date does not coincide with the beginning of the standard calendar period, an owner or operator may elect to utilize a period beginning on the compliance date, or may elect to comply in accordance with the provisions of paragraphs (g)(2) or (g)(3) of this section.

(2) Time periods specified in this subpart for completion of required tasks may be changed by mutual agreement between the owner or operator and the Administrator, as specified in <u>subpart A of this part</u>. For each time period that is changed by agreement, the revised period shall remain in effect until it is changed. A new request is not necessary for each recurring period.

(3) Except as provided in <u>paragraph (g)(1)</u> or (g)(2) of this section, where the period specified for compliance is a standard calendar period, if the initial compliance date does not coincide with the beginning of the calendar period, compliance shall be required according to the schedule specified in <u>paragraphs (g)(3)(i)</u> or (g)(3)(ii) of this section, as appropriate.

(i) Compliance shall be required before the end of the standard calendar period within which the compliance deadline occurs, if there remain at least 3 days for tasks that must be performed weekly, at least 2 weeks for tasks that must be performed monthly, at least 1 month for tasks that must be performed each quarter, or at least 3 months for tasks that must be performed annually; or

(ii) In all other cases, compliance shall be required before the end of the first full standard calendar period after the period within which the initial compliance deadline occurs.

(4) In all instances where a provision of this subpart requires completion of a task during each of multiple successive periods, an owner or operator may perform the required task at any time during each period, provided the task is conducted at a reasonable interval after completion of the task during the previous period.

(h) In all cases where the provisions of this subpart require an owner or operator to repair leaks by a specified time after the leak is detected, it is a violation of this subpart to fail to take action to repair the leaks within the specified time. If action is taken to repair the leaks within the specified time, failure of that action to successfully repair the leak is not a violation of this subpart. However, if the repairs are unsuccessful, a leak is detected and the owner or operator shall take further action as required by applicable provisions of this subpart.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48176</u>, Sept. 20, 1994; <u>62 FR 2789</u>, Jan. 17, 1997; <u>68 FR 37345</u>, June 23, 2003]

# § 63.163 Standards: Pumps in light liquid service.

(a) The provisions of this section apply to each pump that is in light liquid service.

(1) The provisions are to be implemented on the dates specified in the specific subpart in  $\frac{40 \text{ CFR part } 63}{40 \text{ cFR part } 63}$  that references this subpart in the phases specified below:

(i) For each group of existing process units at existing sources subject to the provisions of subparts F or <u>I of this part</u>, the phases of the standard are:

- (A) Phase I, beginning on the compliance date;
- (B) Phase II, beginning no later than 1 year after the compliance date; and
- (C) Phase III, beginning no later than 21/2 years after the compliance date.
- (ii) For new sources subject to the provisions of <u>subparts F</u> or <u>L of this part</u>, the applicable phases of the standard are:
- (A) After initial start-up, comply with the Phase II requirements; and

(B) Beginning no later than 1 year after initial start-up, comply with the Phase III requirements.

(iii) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for each pump in ethylene oxide service, as defined in § 63.101, that is added to a CMPU, and for each pump in ethylene oxide service, that replaces a pump in ethylene oxide service, owners and operators must initially monitor for leaks within 5 days after initial startup of the equipment.

(2) The owner or operator of a source subject to the provisions of <u>subparts F</u> or <u>I of this part</u> may elect to meet the requirements of a later phase during the time period specified for an earlier phase.

(3) Sources subject to other subparts in <u>40 CFR part 63</u> that reference this subpart shall comply on the dates specified in the applicable subpart.

(b)

(1) The owner or operator of a process unit subject to this subpart shall monitor each pump monthly to detect leaks by the method specified in § 63.180(b) of this subpart and shall comply with the requirements of paragraphs (a) through (d) of this section, except as provided in § 63.162(b) of this subpart and paragraphs (e) through (j) of this section.

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(2) Except as specified in paragraph (b)(2)(iv) of this section, the instrument reading, as determined by the method as specified in  $\S$  63.180(b), that defines a leak in each phase of the standard is:

(i) For Phase I, an instrument reading of 10,000 parts per million or greater.

(ii) For Phase II, an instrument reading of 5,000 parts per million or greater.

(iii) For Phase III, an instrument reading of:

(A) 5,000 parts per million or greater for pumps handling polymerizing monomers;

(B) 2,000 parts per million or greater for pumps in food/medical service; and

(C) 1,000 parts per million or greater for all other pumps.

(iv) For each source as defined in  $\S$  63.101, and for each source as defined in  $\S$  63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for pumps in ethylene oxide service, as defined in § 63.101, the instrument reading that defines a leak for pumps is 500 parts per million or greater.

(3) Each pump shall be checked by visual inspection each calendar week for indications of liquids dripping from the pump seal. If there are indications of liquids dripping from the pump seal, a leak is detected.

(c)

(1) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in paragraph (c)(3) of this section or § 63.171 of this subpart.

(2) A first attempt at repair shall be made no later than 5 calendar days after the leak is detected. First attempts at repair include, but are not limited to, the following practices where practicable:

(i) Tightening of packing gland nuts.

(ii) Ensuring that the seal flush is operating at design pressure and temperature.

(3) Except as specified in paragraph (c)(4) of this section, for pumps in Phase III to which a 1.000 parts per million leak definition applies, repair is not required unless an instrument reading of 2,000 parts per million or greater is detected.

(4) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for pumps in ethylene oxide service, as defined in § 63.101, paragraph (c)(3) of this section is not applicable.

(d)

(1) The owner or operator shall decide no later than the first monitoring period whether to calculate percent leaking pumps on a process unit basis or on a source-wide basis. Once the owner or operator has decided, all subsequent percent calculations shall be made on the same basis.

(2) If, in Phase III, calculated on a 6-month rolling average, the greater of either 10 percent of the pumps in a process unit or three pumps in a process unit leak, the owner or operator shall implement a quality improvement program for pumps that complies with the requirements of § 63.176 of this subpart.

(3) The number of pumps at a process unit shall be the sum of all the pumps in organic HAP service, except that pumps found leaking in a continuous process unit within 1 month after start-up of the pump shall not count in the percent leaking pumps calculation for that one monitoring period only.

(4) Percent leaking pumps shall be determined by the following equation:

 $P_{\rm L} = ((P_{\rm L} - P_{\rm S})/(P_{\rm T} - P_{\rm S})) \times 100$ 

where:

 $%P_{L}$  = Percent leaking pumps

 $P_L$  = Number of pumps found leaking as determined through monthly monitoring as required in paragraphs (b)(1) and (b)(2) of this section.

 $P_T$  = Total pumps in organic HAP service, including those meeting the criteria in paragraphs (e) and (f) of this section.

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 $P_{S}$  = Number of pumps leaking within 1 month of start-up during the current monitoring period.

(e) Except as specified in <u>paragraph (e)(7)</u> of this section, each pump equipped with a dual mechanical seal system that includes a barrier fluid system is exempt from the requirements of <u>paragraphs (a)</u> through (d) of this section, provided the following requirements are met:

(1) Each dual mechanical seal system is:

(i) Operated with the barrier fluid at a pressure that is at all times greater than the pump stuffing box pressure; or

(ii) Equipped with a barrier fluid degassing reservoir that is routed to a process or fuel gas system or connected by a closed-vent system to a control device that complies with the requirements of  $\frac{63.172}{5}$  of this subpart; or

(iii) Equipped with a closed-loop system that purges the barrier fluid into a process stream.

(2) The barrier fluid is not in light liquid service.

(3) Each barrier fluid system is equipped with a sensor that will detect failure of the seal system, the barrier fluid system, or both.

(4) Each pump is checked by visual inspection each calendar week for indications of liquids dripping from the pump seal.

(i) If there are indications of liquids dripping from the pump seal at the time of the weekly inspection, the pump shall be monitored as specified in  $\S$  63.180(b) of this subpart to determine if there is a leak of organic HAP in the barrier fluid.

(ii) If an instrument reading of 1,000 parts per million or greater is measured, a leak is detected.

(5) Each sensor as described in <u>paragraph (e)(3)</u> of this section is observed daily or is equipped with an alarm unless the pump is located within the boundary of an unmanned plant site.

(6)

(i) The owner or operator determines, based on design considerations and operating experience, criteria applicable to the presence and frequency of drips and to the sensor that indicates failure of the seal system, the barrier fluid system, or both.

(ii) If indications of liquids dripping from the pump seal exceed the criteria established in <u>paragraph (e)(6)(i)</u> of this section, or if, based on the criteria established in <u>paragraph (e)(6)(i)</u> of this section, the sensor indicates failure of the seal system, the barrier fluid system, or both, a leak is detected.

(iii) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in  $\S$  63.171 of this subpart.

(iv) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(7) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for pumps in ethylene oxide service, as defined in § 63.101, paragraph (e) of this section is not applicable.

(f) Any pump that is designed with no externally actuated shaft penetrating the pump housing is exempt from the requirements of <u>paragraphs (a)</u> through (c) of this section.

(g) Any pump that is routed to a process or fuel gas system or equipped with a closed vent system capable of capturing and transporting leakage from the pump to a control device meeting the requirements of  $\S$  63.172 is exempt from the requirements of paragraphs (a)(1)(iii), and (b) through (e) of this section.

(h) Any pump that is located within the boundary of an unmanned plant site is exempt from the weekly visual inspection requirement of <u>paragraphs (b)(3)</u> and (e)(4) of this section, and the daily requirements of <u>paragraph (e)(5)</u> of this section, provided that each pump is visually inspected as often as practicable and at least monthly.

(i) If more than 90 percent of the pumps at a process unit meet the criteria in either <u>paragraph (e)</u> or <u>(f)</u> of this section, the process unit is exempt from the requirements of <u>paragraph (d)</u> of this section.

(j) Any pump that is designated, as described in  $\S$  63.181(b)(7)(i), as an unsafe-to-monitor pump is exempt from the requirements of paragraphs (a)(1)(iii), and (b) through (e) of this section if:

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(1) The owner or operator of the pump determines that the pump is unsafe to monitor because monitoring personnel would be exposed to an immediate danger as a consequence of complying with <u>paragraphs (a)(1)(iii)</u>, and (b) through (d) of this section; and

(2) The owner or operator of the pump has a written plan that requires monitoring of the pump as frequently as practical during safe-to-monitor times, but not more frequently than the periodic monitoring schedule otherwise applicable.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48176</u>, Sept. 20, 1994; <u>61 FR 31439</u>, June 20, 1996; <u>62 FR 2789</u>, Jan. 17, 1997; <u>64 FR 20198</u>, Apr. 26, 1999; <u>89 FR 43221</u>, May 16, 2024]

#### § 63.164 Standards: Compressors.

(a) Each compressor shall be equipped with a seal system that includes a barrier fluid system and that prevents leakage of process fluid to the atmosphere, except as provided in  $\S$  63.162(b) of this subpart and paragraphs (h) and (i) of this section.

(b) Each compressor seal system as required in <u>paragraph (a)</u> of this section shall be:

(1) Operated with the barrier fluid at a pressure that is greater than the compressor stuffing box pressure; or

(2) Equipped with a barrier fluid system degassing reservoir that is routed to a process or fuel gas system or connected by a closed-vent system to a control device that complies with the requirements of  $\frac{63.172}{5}$  of this subpart; or

(3) Equipped with a closed-loop system that purges the barrier fluid directly into a process stream.

(c) The barrier fluid shall not be in light liquid service.

(d) Each barrier fluid system as described in <u>paragraphs (a)</u> through (c) of this section shall be equipped with a sensor that will detect failure of the seal system, barrier fluid system, or both.

(e)

(1) Each sensor as required in <u>paragraph (d)</u> of this section shall be observed daily or shall be equipped with an alarm unless the compressor is located within the boundary of an unmanned plant site.

(2) The owner or operator shall determine, based on design considerations and operating experience, a criterion that indicates failure of the seal system, the barrier fluid system, or both.

(f) If the sensor indicates failure of the seal system, the barrier fluid system, or both based on the criterion determined under <u>paragraph (e)(2)</u> of this section, a leak is detected.

(g)

(1) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in  $\frac{63.171 \text{ of this subpart}}{1000 \text{ cm}}$ .

(2) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(h) A compressor is exempt from the requirements of <u>paragraphs (a)</u> through (g) of this section if it is equipped with a system to capture and transport leakage from the compressor drive shaft seal to a process or a fuel gas system or to a closed vent system that captures and transports leakage from the compressor to a control device meeting the requirements of § 63.172 of this subpart.

(i) Any compressor that is designated, as described in  $\frac{63.181(b)(2)(ii)}{63.181(b)(2)(ii)}$  of this subpart, to operate with an instrument reading of less than 500 parts per million above background, is exempt from the requirements of <u>paragraphs (a)</u> through (h) of this section if the compressor:

(1) Is demonstrated to be operating with an instrument reading of less than 500 parts per million above background, as measured by the method specified in  $\S$  63.180(c) of this subpart; and

(2) Is tested for compliance with <u>paragraph (i)(1)</u> of this section initially upon designation, annually, and at other times requested by the Administrator.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48176</u>, Sept. 20, 1994; <u>62 FR 2790</u>, Jan. 17, 1997; <u>64 FR 20198</u>, Apr. 26, 1999; <u>89 FR 43221</u>, May 16, 2024]

## § 63.165 Standards: Pressure relief devices in gas/vapor service or light liquid service.

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(a) Except during pressure releases, each pressure relief device in gas/vapor service shall be operated with an instrument reading of less than 500 parts per million above background except as provided in <u>paragraph (b)</u> of this section, as measured by the method specified in § 63.180(c). For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(10), this <u>paragraph (a)</u> no longer applies and instead the owner or operator must comply with <u>paragraph (e)</u> of this section.

(b) Except as specified in <u>paragraph (e)</u> of this section, comply with <u>paragraphs (b)(1)</u> and (b)(2) of this section.

(1) After each pressure release, the pressure relief device shall be returned to a condition indicated by an instrument reading of less than 500 parts per million above background, as soon as practicable, but no later than 5 calendar days after each pressure release, except as provided in  $\S$  63.171.

(2) No later than 5 calendar days after the pressure release and being returned to organic HAP service, the pressure relief device shall be monitored to confirm the condition indicated by an instrument reading of less than 500 parts per million above background, as measured by the method specified in  $\frac{63.180(c)}{c}$ .

(c) Except as specified in <u>paragraph (e)</u> of this section, any pressure relief device that is routed to a process or fuel gas system or equipped with a closed-vent system capable of capturing and transporting leakage from the pressure relief device to a control device as described in  $\S$  63.172 is exempt from the requirements of <u>paragraphs (a)</u> and <u>(b)</u> of this section.

(d) Except as specified in <u>paragraph (e)</u> of this section, comply with <u>paragraphs (d)(1)</u> and (d)(2) of this section.

(1) Any pressure relief device that is equipped with a rupture disk upstream of the pressure relief device is exempt from the requirements of <u>paragraphs (a)</u> and (b) of this section, provided the owner or operator complies with the requirements in <u>paragraph (d)(2)</u> of this section.

(2) After each pressure release, a rupture disk shall be installed upstream of the pressure relief device as soon as practicable, but no later than 5 calendar days after each pressure release, except as provided in  $\frac{63.171}{1.5}$ .

(e) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(10), except as specified in paragraph (e)(4) of this section, owners and operators must comply with the requirements specified in paragraphs (e)(1) and (2) of this section for pressure relief devices, such as relief valves or rupture disks, in organic HAP gas or vapor service instead of the pressure relief device requirements of paragraph (a) through (d) of this section. Except as specified in paragraphs (e)(4) and (5) of this section, owners and operators must also comply with the requirements specified in paragraphs (e)(3), (6), (7), and (8) of this section for all pressure relief devices in organic HAP service.

(1) Operating requirements. Except during a pressure release, operate each pressure relief device in organic HAP gas or vapor service with an instrument reading of less than 500 ppm above background as measured by the method in  $\S 63.180(c)$ .

(2) *Pressure release requirements*. For pressure relief devices in organic HAP gas or vapor service, owners and operators must comply with the applicable requirements <u>paragraphs (e)(2)(i)</u> through (iii) of this section following a pressure release.

(i) If the pressure relief device does not consist of or include a rupture disk, conduct instrument monitoring, as specified in  $\S$  <u>63.180(c)</u>, no later than 5 calendar days after the pressure relief device returns to organic HAP gas or vapor service following a pressure release to verify that the pressure relief device is operating with an instrument reading of less than 500 ppm.

(ii) If the pressure relief device includes a rupture disk, either comply with the requirements in <u>paragraph (e)(2)(i)</u> of this section (and do not replace the rupture disk) or install a replacement disk as soon as practicable after a pressure release, but no later than 5 calendar days after the pressure release.

(iii) If the pressure relief device consists only of a rupture disk, install a replacement disk as soon as practicable after a pressure release, but no later than 5 calendar days after the pressure release. Owners and operators must not initiate startup of the equipment served by the rupture disk until the rupture disc is replaced.

(3) *Pressure release management*. Except as specified in <u>paragraphs (e)(4)</u> and (5) of this section, owners and operators must comply with the requirements specified in <u>paragraphs (e)(3)(i)</u> through (v) of this section for all pressure relief devices in organic HAP service.

(i) Owners and operators must equip each affected pressure relief device with a device(s) or use a monitoring system that is capable of:

(A) Identifying the pressure release;

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(B) Recording the time and duration of each pressure release; and

(C) Notifying operators immediately that a pressure release is occurring. The device or monitoring system must be either specific to the pressure relief device itself or must be associated with the process system or piping, sufficient to indicate a pressure release to the atmosphere. Examples of these types of devices and systems include, but are not limited to, a rupture disk indicator, magnetic sensor, motion detector on the pressure relief valve stem, flow monitor, or pressure monitor.

(ii) Owners and operators must apply at least three redundant prevention measures to each affected pressure relief device and document these measures. Examples of prevention measures include:

(A) Flow, temperature, liquid level and pressure indicators with deadman switches, monitors, or automatic actuators. Independent, non-duplicative systems within this category count as separate redundant prevention measures.

(B) Documented routine inspection and maintenance programs and/or operator training (maintenance programs and operator training may count as only one redundant prevention measure).

(C) Inherently safer designs or safety instrumentation systems.

(D) Deluge systems.

(E) Staged relief system where the initial pressure relief device (with lower set release pressure) discharges to a flare or other closed vent system and control device.

(iii) If any affected pressure relief device releases to atmosphere as a result of a pressure release event, owners and operators must perform root cause analysis and corrective action analysis according to the requirement in <u>paragraph (e)(6)</u> of this section and implement corrective actions according to the requirements in <u>paragraph (e)(7)</u> of this section. Owners and operators must also calculate the quantity of organic HAP released during each pressure release event and report this quantity as required in <u>§ 63.182(d)(2)(xviii)</u>. Calculations may be based on data from the pressure relief device monitoring alone or in combination with process parameter monitoring data and process knowledge.

(iv) Owners and operators must determine the total number of release events that occurred during the calendar year for each affected pressure relief device separately.

(v) Except for pressure relief devices described in <u>paragraphs (e)(4)</u> and (5) of this section, the following release events from an affected pressure relief device are a violation of the pressure release management work practice standards.

(A) Except as specified in <u>paragraph (e)(3)(v)(D)</u> of this section, any release event for which the root cause of the event was determined to be operator error or poor maintenance.

(B) Except as specified in <u>paragraph (e)(3)(v)(D)</u> of this section, a second release event from a single pressure relief device in a 3 calendar year period for the same root cause for the same equipment.

(C) Except as specified in <u>paragraph (e)(3)(v)(D)</u> of this section, a third release event from a single pressure relief device in a 3 calendar year period for any reason.

(D) <u>Paragraphs (e)(3)(v)(A)</u> through (e)(3)(v)(C) of this section do not apply to pressure relief devices in ethylene oxide service, as defined in  $\S$  63.101; instead, any release event from an affected pressure relief device in ethylene oxide service is a violation of the pressure release management work practice standards.

(4) Pressure relief devices routed to a control device, process, fuel gas system, or drain system.

(i) If all releases and potential leaks from a pressure relief device are routed through a closed vent system to a control device, back into the process, to the fuel gas system, or to a drain system, then owners and operators are not required to comply with paragraph (e)(1), (2), or (3) of this section.

(ii) Both the closed vent system and control device (if applicable) referenced in <u>paragraph (e)(4)(i)</u> of this section must meet the applicable requirements specified in  $\frac{63.172}{2}$ .

(iii) The drain system (if applicable) referenced in <u>paragraph (e)(4)(i)</u> of this section must meet the applicable requirements specified in  $\S$  63.136(e).

(5) Pressure relief devices exempted from pressure release management requirements. The following types of pressure relief devices are not subject to the pressure release management requirements in <u>paragraph (e)(3)</u> of this section.

(i) Pressure relief devices in heavy liquid service, as defined in  $\S$  63.161.

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(ii) Thermal expansion relief valves.

(iii) Pressure relief devices on mobile equipment.

(iv) Pilot-operated pressure relief devices where the primary release valve is routed through a closed vent system to a control device or back into the process, to the fuel gas system, or to a drain system.

(v) Balanced bellows pressure relief devices where the primary release valve is routed through a closed vent system to a control device or back into the process, to the fuel gas system, or to a drain system.

(6) Root cause analysis and corrective action analysis. A root cause analysis and corrective action analysis must be completed as soon as possible, but no later than 45 days after a release event. Special circumstances affecting the number of root cause analyses and/or corrective action analyses are provided in paragraphs (e)(6)(i) through (iii) of this section.

(i) Owners and operators may conduct a single root cause analysis and corrective action analysis for a single emergency event that causes two or more pressure relief devices installed on the same equipment to release.

(ii) [Reserved]

(iii) Except as provided in <u>paragraph (e)(6)(i)</u> of this section, if more than one pressure relief device has a release during the same time period, an initial root cause analysis must be conducted separately for each pressure relief device that had a release. If the initial root cause analysis indicates that the release events have the same root cause(s), the initially separate root cause analyses may be recorded as a single root cause analysis and a single corrective action analysis may be conducted.

(7) Corrective action implementation. Owners and operators must conduct a root cause analysis and corrective action analysis as specified in paragraphs (e)(3)(iii) and (e)(6) of this section, and owners and operators must implement the corrective action(s) identified in the corrective action analysis in accordance with the applicable requirements in paragraphs (e)(7)(i) through (iii) of this section.

(i) All corrective action(s) must be implemented within 45 days of the event for which the root cause and corrective action analyses were required or as soon thereafter as practicable. If the owner or operator concludes that no corrective action should be implemented, the owner or operator must record and explain the basis for that conclusion no later than 45 days following the event.

(ii) For corrective actions that cannot be fully implemented within 45 days following the event for which the root cause and corrective action analyses were required, owners and operators must develop an implementation schedule to complete the corrective action(s) as soon as practicable.

(iii) No later than 45 days following the event for which a root cause and corrective action analyses were required, owners and operators must record the corrective action(s) completed to date, and, for action(s) not already completed, a schedule for implementation, including proposed commencement and completion dates.

(8) *Flowing pilot-operated pressure relief devices*. For affected sources that commenced construction or reconstruction on or before April 25, 2023, owners and operators are prohibited from installing a flowing pilot-operated pressure relief device or replacing any pressure relief device with a flowing pilot-operated pressure relief device after July 15, 2027. For affected sources that commenced construction or reconstruction after April 25, 2023, owners and operators are prohibited from installing and operating flowing pilot-operated pressure relief devices. For purpose of compliance with this paragraph, a flowing pilot-operated pressure relief device means the type of pilot-operated pressure relief device where the pilot discharge vent continuously releases emissions to the atmosphere when the pressure relief device is actuated.

[<u>89 FR 43221</u>, May 16, 2024]

## § 63.166 Standards: Sampling connection systems.

(a) Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent system, except as provided in  $\S$  63.162(b) of this subpart. Gases displaced during filling of the sample container are not required to be collected or captured.

(b) Each closed-purge, closed-loop, or closed-vent system as required in <u>paragraph (a)</u> of this section shall:

- (1) Return the purged process fluid directly to the process line; or
- (2) Collect and recycle the purged process fluid to a process; or

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(3) Be designed and operated to capture and transport the purged process fluid to a control device that complies with the requirements of  $\frac{63.172 \text{ of this subpart}}{1000 \text{ cm}}$ ; or

(4) Collect, store, and transport the purged process fluid to a system or facility identified in <u>paragraph (b)(4)(i)</u>, (ii), or (iii) of this section.

(i) A waste management unit as defined in § 63.111 of <u>subpart G of this part</u>, if the waste management unit is subject to, and operated in compliance with the provisions of <u>subpart G of this part</u> applicable to group 1 wastewater streams. If the purged process fluid does not contain any organic HAP listed in Table 9 of subpart G of part 63, the waste management unit need not be subject to, and operated in compliance with the requirements of <u>40 CFR part 63</u>, subpart <u>G</u> applicable to group 1 wastewater streams provided the facility has an NPDES permit or sends the wastewater to an NPDES permitted facility.

(ii) A treatment, storage, or disposal facility subject to regulation under <u>40 CFR part 262</u>, <u>264</u>, <u>265</u>, or <u>266</u>; or

(iii) A facility permitted, licensed, or registered by a State to manage municipal or industrial solid waste, if the process fluids are not hazardous waste as defined in <u>40 CFR part 261</u>.

(c) *In-situ* sampling systems and sampling systems without purges are exempt from the requirements of <u>paragraphs</u> (a) and (b) of this section.

[59 FR 19568, Apr. 22, 1994, as amended at 61 FR 31439, June 20, 1996]

# § 63.167 Standards: Open-ended valves or lines.

(a)

(1) Each open-ended valve or line shall be equipped with a cap, blind flange, plug, or a second valve, except as provided in  $\S$  <u>63.162(b) of this subpart</u> and <u>paragraphs (d)</u> and <u>(e)</u> of this section.

(2) The cap, blind flange, plug, or second valve shall seal the open end at all times except during operations requiring process fluid flow through the open-ended valve or line, or during maintenance or repair.

(b) Each open-ended valve or line equipped with a second valve shall be operated in a manner such that the valve on the process fluid end is closed before the second valve is closed.

(c) When a double block and bleed system is being used, the bleed valve or line may remain open during operations that require venting the line between the block valves but shall comply with <u>paragraph (a)</u> of this section at all other times.

(d) Open-ended valves or lines in an emergency shutdown system which are designed to open automatically in the event of a process upset are exempt from the requirements of <u>paragraphs (a)</u>, (b) and (c) of this section.

(e) Open-ended valves or lines containing materials which would autocatalytically polymerize or, would present an explosion, serious overpressure, or other safety hazard if capped or equipped with a double block and bleed system as specified in <u>paragraphs (a)</u> through (c) of this section are exempt from the requirements of <u>paragraph (a)</u> through (c) of this section.

[59 FR 19568, Apr. 22, 1994, as amended at <u>61 FR 31440</u>, June 20, 1996]

## § 63.168 Standards: Valves in gas/vapor service and in light liquid service.

(a) The provisions of this section apply to valves that are either in gas service or in light liquid service.

(1) The provisions are to be implemented on the dates set forth in the specific subpart in  $\frac{40 \text{ CFR part } 63}{40 \text{ CFR part } 63}$  that references this subpart as specified in paragraph (a)(1)(i), (a)(1)(ii), or (a)(1)(iii) of this section.

(i) For each group of existing process units at existing sources subject to the provisions of subpart F or <u>I of this part</u>, the phases of the standard are:

(A) Phase I, beginning on the compliance date;

- (B) Phase II, beginning no later than 1 year after the compliance date; and
- (C) Phase III, beginning no later than 21/2 years after the compliance date.
- (ii) For new sources subject to the provisions of subpart F or I of this part, the applicable phases of the standard are:

(A) After initial start-up, comply with the Phase II requirements; and

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(B) Beginning no later than 1 year after initial start-up, comply with the Phase III requirements.

(iii) Sources subject to other subparts in <u>40 CFR part 63</u> that reference this subpart shall comply on the dates specified in the applicable subpart.

(2) The owner or operator of a source subject to this subpart may elect to meet the requirements of a later phase during the time period specified for an earlier phase.

(3) The use of monitoring data generated before April 22, 1994 to qualify for less frequent monitoring is governed by the provisions of  $\frac{63.180(b)(6)}{5.180(b)(6)}$  of this subpart.

(b) The owner or operator of a source subject to this subpart shall monitor all valves, except as provided in § 63.162(b) of this subpart and paragraphs (h) and (i) of this section, at the intervals specified in paragraphs (c) and (d) of this section and shall comply with all other provisions of this section, except as provided in § 63.171, § 63.177, § 63.178, and § 63.179 of this subpart.

(1) The valves shall be monitored to detect leaks by the method specified in § 63.180(b) of this subpart.

(2) Except as specified in <u>paragraph (b)(2)(iv)</u> of this section, the instrument reading that defines a leak in each phase of the standard is:

(i) For Phase I, an instrument reading of 10,000 parts per million or greater.

(ii) For Phase II, an instrument reading of 500 parts per million or greater.

(iii) For Phase III, an instrument reading of 500 parts per million or greater.

(iv) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for valves in ethylene oxide service, as defined in § 63.101, that are either in gas service or in light liquid service the instrument reading that defines a leak is 100 parts per million or greater.

(c) In Phases I and II, each valve shall be monitored quarterly.

(d) Except as specified in paragraph (d)(5) of this section, in Phase III, the owner or

(1) At process units with 2 percent or greater leaking valves, calculated according to <u>paragraph (e)</u> of this section, the owner or operator shall either:

(i) Monitor each valve once per month; or

(ii) Within the first year after the onset of Phase III, implement a quality improvement program for valves that complies with the requirements of  $\frac{63.175}{0}$  or (e) of this subpart and monitor quarterly.

(2) At process units with less than 2 percent leaking valves, the owner or operator shall monitor each valve once each quarter, except as provided in <u>paragraphs (d)(3)</u> and (d)(4) of this section.

(3) At process units with less than 1 percent leaking valves, the owner or operator may elect to monitor each valve once every 2 quarters.

(4) At process units with less than 0.5 percent leaking valves, the owner or operator may elect to monitor each valve once every 4 quarters.

(5) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for valves in ethylene oxide service, as defined in § 63.101, that are either in gas service or in light liquid service the monitoring period is once per month.

(e)

(1) Percent leaking valves at a process unit shall be determined by the following equation:

$$V_{\rm L} = (V_{\rm L}/(V_{\rm T} + V_{\rm C})) \times 100$$

where:

 $%V_L$  = Percent leaking values as determined through periodic monitoring required in <u>paragraphs (b)</u> through <u>(d)</u> of this section.

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 $V_L$  = Number of valves found leaking excluding nonrepairables as provided in <u>paragraph (e)(3)(i)</u> of this section.

 $V_T$  = Total valves monitored, in a monitoring period excluding valves monitored as required by (f)(3) of this section.

 $V_C$  = Optional credit for removed valves = 0.67 × net number (i.e., total removed-total added) of valves in organic HAP service removed from process unit after the date set forth in § 63.100(k) of subpart F for existing process units, and after the date of initial start-up for new sources. If credits are not taken, then  $V_C = 0$ .

(2) For use in determining monitoring frequency, as specified in <u>paragraph (d)</u> of this section, the percent leaking valves shall be calculated as a rolling average of two consecutive monitoring periods for monthly, quarterly, or semiannual monitoring programs; and as an average of any three out of four consecutive monitoring periods for annual monitoring programs.

(3)

(i) Nonrepairable valves shall be included in the calculation of percent leaking valves the first time the valve is identified as leaking and nonrepairable and as required to comply with <u>paragraph (e)(3)(ii)</u> of this section. Otherwise, a number of nonrepairable valves (identified and included in the percent leaking calculation in a previous period) up to a maximum of 1 percent of the total number of valves in organic HAP service at a process unit may be excluded from calculation of percent leaking valves for subsequent monitoring periods.

(ii) If the number of nonrepairable valves exceeds 1 percent of the total number of valves in organic HAP service at a process unit, the number of nonrepairable valves exceeding 1 percent of the total number of valves in organic HAP service shall be included in the calculation of percent leaking valves.

(f)

(1) When a leak is detected, it shall be repaired as soon as practicable, but no later than 15 calendar days after the leak is detected, except as provided in  $\frac{63.171 \text{ of this subpart}}{1000 \text{ subpart}}$ .

(2) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(3) When a leak has been repaired, the valve shall be monitored at least once within the first 3 months after its repair.

(i) The monitoring shall be conducted as specified in  $\S$  63.180 (b) and (c), as appropriate, to determine whether the valve has resumed leaking.

(ii) Periodic monitoring required by <u>paragraphs (b)</u> through (d) of this section may be used to satisfy the requirements of this <u>paragraph (f)(3)</u>, if the timing of the monitoring period coincides with the time specified in this <u>paragraph (f)(3)</u>. Alternatively, other monitoring may be performed to satisfy the requirements of this <u>paragraph (f)(3)</u>, regardless of whether the timing of the monitoring period for periodic monitoring coincides with the time specified in this <u>paragraph (f)(3)</u>.

(iii) If a leak is detected by monitoring that is conducted pursuant to paragraph (f)(3) of this section, the owner or operator shall follow the provisions of paragraphs (f)(3)(iii)(A) and (f)(3)(iii)(B) of this section, to determine whether that valve must be counted as a leaking valve for purposes of § 63.168(e) of this subpart.

(A) If the owner or operator elected to use periodic monitoring required by <u>paragraphs (b)</u> through (d) of this section to satisfy the requirements of <u>paragraph (f)(3)</u> of this section, then the valve shall be counted as a leaking valve.

(B) If the owner or operator elected to use other monitoring, prior to the periodic monitoring required by <u>paragraphs</u> (b) through (d) of this section, to satisfy the requirements of <u>paragraph (f)(3)</u> of this section, then the valve shall be counted as a leaking valve unless it is repaired and shown by periodic monitoring not to be leaking.

(g) First attempts at repair include, but are not limited to, the following practices where practicable:

(1) Tightening of bonnet bolts,

(2) Replacement of bonnet bolts,

(3) Tightening of packing gland nuts, and

(4) Injection of lubricant into lubricated packing.

(h) Any valve that is designated, as described in  $\S$  63.181(b)(7)(i) of this subpart, as an unsafe-to-monitor valve is exempt from the requirements of paragraphs (b) through (f) of this section if:

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(1) The owner or operator of the valve determines that the valve is unsafe to monitor because monitoring personnel would be exposed to an immediate danger as a consequence of complying with <u>paragraphs (b)</u> through (d) of this section; and

(2) The owner or operator of the valve has a written plan that requires monitoring of the valve as frequently as practicable during safe-to-monitor times, but not more frequently than the periodic monitoring schedule otherwise applicable.

(i) Any value that is designated, as described in  $\S$  63.181(b)(7)(ii) of this subpart, as a difficult-to-monitor value is exempt from the requirements of paragraphs (b) through (d) of this section if:

(1) The owner or operator of the valve determines that the valve cannot be monitored without elevating the monitoring personnel more than 2 meters above a support surface or it is not accessible at anytime in a safe manner;

(2) The process unit within which the valve is located is an existing source or the owner or operator designates less than 3 percent of the total number of valves in a new source as difficult-to-monitor; and

(3) The owner or operator of the valve follows a written plan that requires monitoring of the valve at least once per calendar year.

(j) Any equipment located at a plant site with fewer than 250 valves in organic HAP service is exempt from the requirements for monthly monitoring and a quality improvement program specified in <u>paragraph (d)(1)</u> of this section. Instead, the owner or operator shall monitor each valve in organic HAP service for leaks once each quarter, or comply with <u>paragraph (d)(3)</u> or (d)(4) of this section except as provided in <u>paragraphs (h)</u> and (i) of this section.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48176</u>, Sept. 20, 1994; <u>61 FR 31440</u>, June 20, 1996; <u>62 FR 2790</u>, Jan. 17, 1997; <u>89 FR 43223</u>, May 16, 2024]

# § 63.169 Standards: Pumps, valves, connectors, and agitators in heavy liquid service; instrumentation systems; and pressure relief devices in liquid service.

(a) Pumps, valves, connectors, and agitators in heavy liquid service, pressure relief devices in light liquid or heavy liquid service, and instrumentation systems shall be monitored within 5 calendar days by the method specified in  $\S$  63.180(b) of this subpart if evidence of a potential leak to the atmosphere is found by visual, audible, olfactory, or any other detection method. If such a potential leak is repaired as required in paragraphs (c) and (d) of this section, it is not necessary to monitor the system for leaks by the method specified in  $\S$  63.180(b) of this subpart.

(b) If an instrument reading of 10,000 parts per million or greater for agitators, 5,000 parts per million or greater for pumps handling polymerizing monomers, 2,000 parts per million or greater for all other pumps (including pumps in food/medical service), or 500 parts per million or greater for valves, connectors, instrumentation systems, and pressure relief devices is measured, a leak is detected.

(c)

(1) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in  $\frac{63.171}{100}$  of this subpart.

(2) The first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(3) For equipment identified in <u>paragraph (a)</u> of this section that is not monitored by the method specified in <u>§ 63.180(b)</u>, repaired shall mean that the visual, audible, olfactory, or other indications of a leak to the atmosphere have been eliminated; that no bubbles are observed at potential leak sites during a leak check using soap solution; or that the system will hold a test pressure.

(d) First attempts at repair include, but are not limited to, the practices described under  $\frac{\$\$ 63.163(c)(2)}{\$$  and  $\frac{63.168(g)}{\$}$  of this subpart, for pumps and valves, respectively.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48177</u>, Sept. 20, 1994; <u>60 FR 18029</u>, Apr. 10, 1995; <u>62 FR 2790</u>, Jan. 17, 1997; <u>65 FR 78285</u>, Dec. 14, 2000]

## § 63.170 Standards: Surge control vessels and bottoms receivers.

(a) Except as specified in <u>paragraph (b)</u> of this section, each surge control vessel or bottoms receiver that is not routed back to the process and that meets the conditions specified in table 2 or table 3 of this subpart shall be equipped with a closed-vent system that routes the organic vapors vented from the surge control vessel or bottoms receiver back to the process or to a

control device that complies with the requirements in  $\S 63.172$ , except as provided in  $\S 63.162(b)$ , or comply with the requirements of  $\S 63.119(b)$  or (c).

(b) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(10), paragraph (a) of this section no longer applies. Instead, each surge control vessel and bottoms receiver that is not routed back to the process and emits greater than or equal to 1.0 lb/hr of total organic HAP must be equipped with a closed-vent system that routes the organic vapors vented from the surge control vessel or bottoms receiver back to the process or to a control device that complies with the requirements in § 63.172, except as provided in § 63.162(b), or comply with the requirements of § 63.113(a)(1) or (a)(2).

[89 FR 43224, May 16, 2024]

#### § 63.171 Standards: Delay of repair.

(a) Except as specified in <u>paragraph (f)</u> of this section, delay of repair of equipment for which leaks have been detected is allowed if repair within 15 days is technically infeasible without a process unit shutdown. Repair of this equipment shall occur by the end of the next process unit shutdown.

(b) Delay of repair of equipment for which leaks have been detected is allowed for equipment that is isolated from the process and that does not remain in organic HAP service.

(c) Except as specified in <u>paragraph (f)</u> of this section, delay of repair for valves, connectors, and agitators is also allowed if:

(1) The owner or operator determines that emissions of purged material resulting from immediate repair would be greater than the fugitive emissions likely to result from delay of repair, and

(2) When repair procedures are effected, the purged material is collected and destroyed or recovered in a control device complying with  $\S$  63.172 of this subpart.

(d) Except as specified in paragraph (f) of this section, delay of repair for pumps is also allowed if:

(1) Repair requires replacing the existing seal design with a new system that the owner or operator has determined under the provisions of  $\frac{63.176(d)}{1000}$  of this subpart will provide better performance or:

(i) A dual mechanical seal system that meets the requirements of § 63.163(e) of this subpart,

(ii) A pump that meets the requirements of § 63.163(f) of this subpart, or

(iii) A closed-vent system and control device that meets the requirements of § 63.163(g) of this subpart; and

(2) Repair is completed as soon as practicable, but not later than 6 months after the leak was detected.

(e) Except as specified in <u>paragraph (f)</u> of this section, delay of repair beyond a process unit shutdown will be allowed for a valve if valve assembly replacement is necessary during the process unit shutdown, valve assembly supplies have been depleted, and valve assembly supplies had been sufficiently stocked before the supplies were depleted. Delay of repair beyond the second process unit shutdown will not be allowed unless the third process unit shutdown occurs sooner than 6 months after the first process unit shutdown.

(f) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), delay of repair is not allowed for light liquid pumps in ethylene oxide service, gas/vapor and light liquid valves in ethylene oxide service, and connectors in ethylene oxide service.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48177</u>, Sept. 20, 1994; <u>65 FR 78285</u>, Dec. 14, 2000; <u>89 FR 43224</u>, May 16, 2024]

## § 63.172 Standards: Closed-vent systems and control devices.

(a) Owners or operators of closed-vent systems and control devices used to comply with provisions of this subpart shall comply with the provisions of this section, except as provided in  $\S$  63.162(b) of this subpart.

(b) Recovery or recapture devices (*e.g.*, condensers and absorbers) shall be designed and operated to recover the organic hazardous air pollutant emissions or volatile organic compounds emissions vented to them with an efficiency of 95 percent or greater, or to an exit concentration of 20 parts per million by volume, whichever is less stringent. The 20 parts per million by volume performance standard is not applicable to the provisions of  $\frac{6.3.179}{5}$ .

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(c) Enclosed combustion devices shall be designed and operated to reduce the organic hazardous air pollutant emissions or volatile organic compounds emissions vented to them with an efficiency of 95 percent or greater, or to an exit concentration of 20 parts per million by volume, on a dry basis, corrected to 3 percent oxygen, whichever is less stringent, or to provide a minimum residence time of 0.50 seconds at a minimum temperature of 760 °C.

(d) Except as specified in <u>paragraph (a) of § 63.108</u>, flares used to comply with this subpart shall comply with the requirements of  $\frac{\$ 63.11(b)}{10}$ .

(e) Owners or operators of control devices that are used to comply with the provisions of this subpart shall monitor these control devices to ensure that they are operated and maintained in conformance with their design.

Note:

The intent of this provision is to ensure proper operation and maintenance of the control device.

(f) Except as provided in <u>paragraphs (k)</u> and (<u>1</u>) of this section, each closed-vent system shall be inspected according to the procedures and schedule specified in <u>paragraphs (f)(1)</u> and (f)(2) of this section.

(1) If the closed-vent system is constructed of hard-piping, the owner or operator shall:

(i) Conduct an initial inspection according to the procedures in <u>paragraph (g)</u> of this section, and

(ii) Conduct annual visual inspections for visible, audible, or olfactory indications of leaks.

(2) If the vapor collection system or closed-vent system is constructed of duct work, the owner or operator shall:

(i) Conduct an initial inspection according to the procedures in paragraph (g) of this section, and

(ii) Conduct annual inspections according to the procedures in paragraph (g) of this section.

(g) Each closed-vent system shall be inspected according to the procedures in § 63.180(b) of this subpart.

(h) Leaks, as indicated by an instrument reading greater than 500 parts per million above background or by visual inspections, shall be repaired as soon as practicable, except as provided in <u>paragraph (i)</u> of this section.

(1) A first attempt at repair shall be made no later than 5 calendar days after the leak is detected.

(2) Repair shall be completed no later than 15 calendar days after the leak is detected, except as provided in <u>paragraph (i)</u> of this section.

(i) Delay of repair of a closed-vent system for which leaks have been detected is allowed if the repair is technically infeasible without a process unit shutdown or if the owner or operator determines that emissions resulting from immediate repair would be greater than the fugitive emissions likely to result from delay of repair. Repair of such equipment shall be complete by the end of the next process unit shutdown.

(j) For each closed-vent system that contains bypass lines that could divert a vent stream away from the control device and to the atmosphere, the owner or operator shall comply with the provisions of either <u>paragraphs (j)(1)</u> or (j)(2), and (j)(4) of this section, except as provided in <u>paragraph (j)(3)</u> of this section.

(1) Install, set or adjust, maintain, and operate a flow indicator that takes a reading at least once every 15 minutes. Records shall be generated as specified in  $\S 63.118(a)(3)$  of subpart G of this part. The flow indicator shall be installed at the entrance to any bypass line; or

(2) Secure the bypass line valve in the non-diverting position with a car-seal or a lock-and-key type configuration. A visual inspection of the seal or closure mechanism shall be performed at least once every month to ensure the valve is maintained in the non-diverting position and the vent stream is not diverted through the bypass line.

(3) Except as specified in <u>paragraph (j)(4)</u> of this section, equipment such as low leg drains, high point bleeds, analyzer vents, open-ended valves or lines, and pressure relief valves needed for safety purposes are not subject to this paragraph.

(4) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(10):

(i) The use of a bypass line at any time on a closed vent system (used to comply with the provisions of this subpart) to divert emissions to the atmosphere or to a control device not meeting the requirements specified in this subpart is an emissions standards violation.

(ii) <u>Paragraph (j)(3)</u> of this section does not apply. Instead, the exemptions specified in <u>paragraph</u> (j)(4)(ii)(A) and (j)(4)(ii)(B) of this section apply.

(A) Except for pressure relief devices subject to  $\frac{63.165(e)(4)}{2}$ , equipment such as low leg drains and equipment subject to the requirements specified in subpart H of this part are not subject to this paragraph (j) of this section.

(B) Open-ended valves or lines that use a cap, blind flange, plug, or second valve and follow the requirements specified in  $\frac{40}{\text{CFR} 60.482-6(a)(2)}$ , (b), and (c) or follow requirements codified in another regulation that are the same as  $\frac{40 \text{ CFR} 60.482-6(a)(2)}{6(a)(2)}$ , (b), and (c) are not subject to this <u>paragraph (j)</u> of this section.

(k) Any parts of the closed-vent system that are designated, as described in paragraph 63.181(b)(7)(i), as unsafe to inspect are exempt from the inspection requirements of <u>paragraphs (f)(1)</u> and <u>(f)(2)</u> of this section if:

(1) The owner or operator determines that the equipment is unsafe to inspect because inspecting personnel would be exposed to an imminent or potential danger as a consequence of complying with  $\frac{\text{paragraph}(f)(1)}{\text{paragraph}(f)(1)}$  or (f)(2) of this section; and

(2) The owner or operator has a written plan that requires inspection of the equipment as frequently as practicable during safe-to-inspect times, but not more frequently than annually.

(1) Any parts of the closed-vent system that are designated, as described in  $\S$  63.181 (b)(7)(i) of this subpart, as difficult to inspect are exempt from the inspection requirements of paragraphs (f)(1) and (f)(2) of this section if:

(1) The owner or operator determines that the equipment cannot be inspected without elevating the inspecting personnel more than 2 meters above a support surface; and

(2) The owner or operator has a written plan that requires inspection of the equipment at least once every 5 years.

(m) Whenever organic HAP emissions are vented to a closed-vent system or control device used to comply with the provisions of this subpart, such system or control device shall be operating.

(n) After the compliance dates specified in § 63.100 of subpart F of this part, the owner or operator of any control device subject to this subpart that is also subject to monitoring, recordkeeping, and reporting requirements in  $\frac{40 \text{ CFR part } 264}{40 \text{ CFR part } 264}$ , subpart BB, or is subject to monitoring and recordkeeping requirements in  $\frac{40 \text{ CFR part } 265}{40 \text{ CFR part } 265}$ , subpart BB, may elect to comply either with the monitoring, recordkeeping, and reporting requirements of this subpart, or with the monitoring, recordkeeping, and reporting requirements of this paragraph, which shall constitute compliance with the monitoring, recordkeeping and reporting requirements of this subpart. The owner or operator shall identify which option has been chosen, in the next periodic report required by § 63.182(d).

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48177</u>, Sept. 20, 1994; <u>61 FR 31440</u>, June 20, 1996; <u>62 FR 2790</u>, Jan. 17, 1997; <u>89 FR 43224</u>, May 16, 2024]

## § 63.173 Standards: Agitators in gas/vapor service and in light liquid service.

(a)

(1) Each agitator shall be monitored monthly to detect leaks by the methods specified in  $\S$  63.180(b) of this subpart, except as provided in  $\S$  63.162(b) of this subpart.

(2) If an instrument reading of 10,000 parts per million or greater is measured, a leak is detected.

(b)

(1) Each agitator shall be checked by visual inspection each calendar week for indications of liquids dripping from the agitator.

(2) If there are indications of liquids dripping from the agitator, a leak is detected.

(c)

(1) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in  $\frac{63.171 \text{ of this subpart}}{1000 \text{ subpart}}$ .

(2) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

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(d) Each agitator equipped with a dual mechanical seal system that includes a barrier fluid system is exempt from the requirements of <u>paragraph (a)</u> of this section, provided the requirements specified in <u>paragraphs (d)(1)</u> through  $(\underline{d})(\underline{6})$  of this section are met:

(1) Each dual mechanical seal system is:

(i) Operated with the barrier fluid at a pressure that is at all times greater than the agitator stuffing box pressure; or

(ii) Equipped with a barrier fluid degassing reservoir that is routed to a process or fuel gas system or connected by a closed-vent system to a control device that complies with the requirements of  $\frac{63.172 \text{ of this subpart}}{1000 \text{ subpart}}$ ; or

(iii) Equipped with a closed-loop system that purges the barrier fluid into a process stream.

(2) The barrier fluid is not in light liquid organic HAP service.

(3) Each barrier fluid system is equipped with a sensor that will detect failure of the seal system, the barrier fluid system, or both.

(4) Each agitator is checked by visual inspection each calendar week for indications of liquids dripping from the agitator seal.

(i) If there are indications of liquids dripping from the agitator seal at the time of the weekly inspection, the agitator shall be monitored as specified in § 63.180(b) of this subpart to determine the presence of organic HAP in the barrier fluid.

(ii) If an instrument reading of 10,000 parts per million or greater is measured, a leak is detected.

(5) Each sensor as described in <u>paragraph (d)(3)</u> of this section is observed daily or is equipped with an alarm unless the agitator is located within the boundary of an unmanned plant site.

(6)

(i) The owner or operator determines, based on design considerations and operating experience, criteria applicable to the presence and frequency of drips and to the sensor that indicates failure of the seal system, the barrier fluid system, or both.

(ii) If indications of liquids dripping from the agitator seal exceed the criteria established in <u>paragraph (d)(6)(i)</u> of this section, or if, based on the criteria established in <u>paragraph (d)(6)(i)</u> of this section, the sensor indicates failure of the seal system, the barrier fluid system, or both, a leak is detected.

(iii) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in <u>§ 63.171 of this subpart</u>.

(iv) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(e) Any agitator that is designed with no externally actuated shaft penetrating the agitator housing is exempt from <u>paragraphs</u> (a) through (c) of this section.

(f) Any agitator if it is equipped with a system to capture and transport leakage from the agitator to a process or a fuel gas system or to a closed vent system that captures and transports leakage from the agitator to a control device meeting the requirements of  $\frac{63.172}{5}$  is exempt from the requirements of paragraphs (a) through (c) of the section.

(g) Any agitator that is located within the boundary of an unmanned plant site is exempt from the weekly visual inspection requirement of paragraphs (b)(1) and (d)(4) of this section, and the daily requirements of paragraph (d)(5) of this section, provided that each agitator is visually inspected as often as practical and at least monthly.

(h) Any agitator that is difficult-to-monitor is exempt from the requirements of <u>paragraphs (a)</u> through (d) of this section if:

(1) The owner or operator determines that the agitator cannot be monitored without elevating the monitoring personnel more than two meters above a support surface or it is not accessible at anytime in a safe manner;

(2) The process unit within which the agitator is located is an existing source or the owner or operator designates less than three percent of the total number of agitators in a new source as difficult-to-monitor; and

(3) The owner or operator follows a written plan that requires monitoring of the agitator at least once per calendar year.

(i) Any agitator that is obstructed by equipment or piping that prevents access to the agitator by a monitor probe is exempt from the monitoring requirements of <u>paragraphs (a)</u> through (d) of this section.

(j) Any agitator that is designated, as described in  $\S$  <u>63.181(b)(7)(i) of this subpart</u>, as an unsafe-to-monitor agitator is exempt from the requirements of <u>paragraphs (a)</u> through (<u>d</u>) of this section if:

(1) The owner or operator of the agitator determines that the agitator is unsafe to monitor because monitoring personnel would be exposed to an immediate danger as a consequence of complying with <u>paragraphs (a)</u> through (d) of this section; and

(2) The owner or operator of the agitator has a written plan that requires monitoring of the agitator as frequently as practical during safe-to-monitor times, but not more frequently than the periodic monitoring schedule otherwise applicable.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>61 FR 31440</u>, June 20, 1996; <u>62 FR 2791</u>, Jan. 17, 1997; <u>64 FR 20198</u>, Apr. 26, 1999; <u>89 FR 43224</u>, May 16, 2024]

# § 63.174 Standards: Connectors in gas/vapor service and in light liquid service.

(a) The owner or operator of a process unit subject to this subpart shall monitor all connectors in gas/vapor and light liquid service, except as provided in  $\S$  63.162(b) of this subpart, and in paragraphs (f) through (h) of this section, at the intervals specified in paragraph (b) of this section.

(1) The connectors shall be monitored to detect leaks by the method specified in  $\S$  63.180(b) of this subpart.

(2) Except as specified in <u>paragraph (a)(3)</u> of this section, if an instrument reading greater than or equal to 500 parts per million is measured, a leak is detected.

(3) For each source as defined in  $\S$  63.101, and for each source as defined in  $\S$  63.191, beginning no later than the compliance dates specified in  $\S$  63.100(k)(11), for connectors in ethylene oxide service, as defined in  $\S$  63.101, the instrument reading that defines a leak for connectors is 100 parts per million or greater.

(b) The owner or operator shall monitor for leaks at the intervals specified in either <u>paragraph (b)(1)</u> or <u>(b)(2)</u> of this section and in <u>paragraphs (b)(3)</u> through <u>(b)(5)</u> of this section.

(1) For each group of existing process units within an existing source, by no later than 12 months after the compliance date, the owner or operator shall monitor all connectors, except as provided in <u>paragraphs (f)</u> through (h) of this section.

(2) For new sources, within the first 12 months after initial start-up or by no later than 12 months after the date of promulgation of a specific subpart that references this subpart, whichever is later, the owner or operator shall monitor all connectors, except as provided in <u>paragraphs (f)</u> through (<u>h</u>) of this section.

(3) After conducting the initial survey required in <u>paragraph (b)(1)</u> or (b)(2) of this section, the owner or operator shall perform all subsequent monitoring of connectors at the frequencies specified in <u>paragraphs (b)(3)(i)</u> through (b)(3)(v) of this section, except as provided in <u>paragraphs (b)(3)(vi)</u> and (c)(2) of this section:

(i) Once per year (i.e., 12-month period), if the percent leaking connectors in the process unit was 0.5 percent or greater during the last required annual or biennial monitoring period.

(ii) Once every 2 years, if the percent leaking connectors was less than 0.5 percent during the last required monitoring period. An owner or operator may comply with this paragraph by monitoring at least 40 percent of the connectors in the first year and the remainder of the connectors in the second year. The percent leaking connectors will be calculated for the total of all monitoring performed during the 2-year period.

(iii) If the owner or operator of a process unit in a biennial leak detection and repair program calculates less than 0.5 percent leaking connectors from the 2-year monitoring period, the owner or operator may monitor the connectors one time every 4 years. An owner or operator may comply with the requirements of this paragraph by monitoring at least 20 percent of the connectors each year until all connectors have been monitored within 4 years.

(iv) If a process unit complying with the requirements of <u>paragraph (b)</u> of this section using a 4-year monitoring interval program has greater than or equal to 0.5 percent but less than 1 percent leaking connectors, the owner or operator shall increase the monitoring frequency to one time every 2 years. An owner or operator may comply with the requirements of this paragraph by monitoring at least 40 percent of the connectors in the first year and the remainder of the connectors in the second year. The owner or operator may again elect to use the provisions of <u>paragraph (b)(3)(iii)</u> of this section when the percent leaking connectors decreases to less than 0.5 percent.

(v) If a process unit complying with requirements of <u>paragraph (b)(3)(iii)</u> of this section using a 4-year monitoring interval program has 1 percent or greater leaking connectors, the owner or operator shall increase the monitoring frequency to one

time per year. The owner or operator may again elect to use the provisions of <u>paragraph (b)(3)(iii)</u> of this section when the percent leaking connectors decreases to less than 0.5 percent.

(vi) For each source as defined in  $\S$  63.101, and for each source as defined in  $\S$  63.191, beginning no later than the compliance dates specified in  $\S$  63.100(k)(11), for connectors in ethylene oxide service, as defined in  $\S$  63.101, the monitoring period is once every month and paragraph (c)(2) of this section is not applicable.

(4) The use of monitoring data generated before April 22, 1994 to qualify for less frequent monitoring is governed by the provisions of  $\frac{63.180(b)(6)}{5}$ .

(5) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for each connector in ethylene oxide service, as defined in § 63.101, that is added to a CMPU, and for each connector in ethylene oxide service that replaces a connector in ethylene oxide service, owners and operators must initially monitor for leaks within 5 days after initial startup of the equipment.

(c)

(1)

(i) Except as provided in <u>paragraph (c)(1)(ii)</u> of this section, each connector that has been opened or has otherwise had the seal broken shall be monitored for leaks when it is reconnected or within the first 3 months after being returned to organic hazardous air pollutants service. If the monitoring detects a leak, it shall be repaired according to the provisions of <u>paragraph</u> (d) of this section, unless it is determined to be nonrepairable, in which case it is counted as a nonrepairable connector for the purposes of <u>paragraph (i)(2)</u> of this section.

(ii) As an alternative to the requirements in <u>paragraph (c)(1)(i)</u> of this section, an owner or operator may choose not to monitor connectors that have been opened or otherwise had the seal broken. In this case, the owner or operator may not count nonrepairable connectors for the purposes of <u>paragraph (i)(2)</u> of this section. The owner or operator shall calculate the percent leaking connectors for the monitoring periods described in <u>paragraph (b)</u> of this section, by setting the nonrepairable component,  $C_{AN}$ , in the equation in <u>paragraph (i)(2)</u> of this section to zero for all monitoring periods.

(iii) An owner or operator may switch alternatives described in <u>paragraphs (c)(1) (i)</u> and <u>(ii)</u> of this section at the end of the current monitoring period he is in, provided that it is reported as required in § 63.182 of this subpart and begin the new alternative in annual monitoring. The initial monitoring in the new alternative shall be completed no later than 12 months after reporting the switch.

(2) As an alternative to the requirements of <u>paragraph (b)(3)</u> of this section, each screwed connector 2 inches or less in nominal inside diameter installed in a process unit before the dates specified in <u>paragraph (c)(2)(iii)</u> or <u>(c)(2)(iv)</u> of this section may:

(i) Comply with the requirements of § 63.169 of this subpart, and

(ii) Be monitored for leaks within the first 3 months after being returned to organic hazardous air pollutants service after having been opened or otherwise had the seal broken. If that monitoring detects a leak, it shall be repaired according to the provisions of <u>paragraph (d)</u> of this section.

(iii) For sources subject to subparts F and I of this part, the provisions of paragraph (c)(2) of this section apply to screwed connectors installed before December 31, 1992.

(iv) For sources not identified in <u>paragraph (c)(2)(iii)</u> of this section, the provisions of <u>paragraph (c)(2)</u> of this section apply to screwed connectors installed before the date of proposal of the applicable subpart of this part that references this subpart.

(d) When a leak is detected, it shall be repaired as soon as practicable, but no later than 15 calendar days after the leak is detected, except as provided in <u>paragraph (g)</u> of this section and in § 63.171 of this subpart. A first attempt at repair shall be made no later than 5 calendar days after the leak is detected.

(e) [Reserved]

(f) Any connector that is designated, as described in  $\S$  63.181(b)(7)(i) of this subpart, as an unsafe-to-monitor connector is exempt from the requirements of paragraph (a) of this section if:

(1) The owner or operator determines that the connector is unsafe to monitor because personnel would be exposed to an immediate danger as a result of complying with <u>paragraphs (a)</u> through (e) of this section; and

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(2) The owner or operator has a written plan that requires monitoring of the connector as frequently as practicable during safe to monitor periods, but not more frequently than the periodic schedule otherwise applicable.

(g) Except as specified in <u>paragraph (g)(3)</u> of this section, any connector that is designated, as described in § 63.181(b)(7)(iii), as an unsafe-to-repair connector is exempt from the requirements of <u>paragraphs (a)</u>, (d), and (e) of this section if:

(1) The owner or operator determines that repair personnel would be exposed to an immediate danger as a consequence of complying with <u>paragraph (d)</u> of this section; and

(2) The connector will be repaired before the end of the next scheduled process unit shutdown.

(3) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(11), for connectors in ethylene oxide service, as defined in § 63.101, paragraph (g) of this section is no longer applicable.

(h)

(1) Any connector that is inaccessible or is ceramic or ceramic-lined (e.g., porcelain, glass, or glass-lined), is exempt from the monitoring requirements of <u>paragraphs (a)</u> and (c) of this section and from the recordkeeping and reporting requirements of § 63.181 and § 63.182 of this subpart. An inaccessible connector is one that is:

# (i) Buried;

(ii) Insulated in a manner that prevents access to the connector by a monitor probe;

(iii) Obstructed by equipment or piping that prevents access to the connector by a monitor probe;

(iv) Unable to be reached from a wheeled scissor-lift or hydraulic-type scaffold which would allow access to connectors up to 7.6 meters (25 feet) above the ground;

(v) Inaccessible because it would require elevating the monitoring personnel more than 2 meters above a permanent support surface or would require the erection of scaffold; or

(vi) Not able to be accessed at any time in a safe manner to perform monitoring. Unsafe access includes, but is not limited to, the use of a wheeled scissor-lift on unstable or uneven terrain, the use of a motorized man-lift basket in areas where an ignition potential exists, or access would require near proximity to hazards such as electrical lines, or would risk damage to equipment.

(2) If any inaccessible or ceramic or ceramic-lined connector is observed by visual, audible, olfactory, or other means to be leaking, the leak shall be repaired as soon as practicable, but no later than 15 calendar days after the leak is detected, except as provided in  $\frac{§ 63.171 \text{ of this subpart}}{2}$  and paragraph (g) of this section.

(3) A first attempt at repair shall be made no later than 5 calendar days after the leak is detected.

(i) For use in determining the monitoring frequency, as specified in <u>paragraph (b)</u> of this section, the percent leaking connectors shall be calculated as specified in <u>paragraphs (i)(1)</u> and <u>(i)(2)</u> of this section.

(1) For the first monitoring period, use the following equation:

%  $C_L = C_L / (C_t + C_C) \times 100$ 

where:

%  $C_L$  = Percent leaking connectors as determined through periodic monitoring required in <u>paragraphs (a)</u> and <u>(b)</u> of this section.

 $C_L$  = Number of connectors measured at 500 parts per million or greater, by the method specified in <u>§ 63.180(b) of this</u> subpart.

 $C_t$  = Total number of monitored connectors in the process unit.

 $C_C$  = Optional credit for removed connectors = 0.67 × net (i.e., total removed—total added) number of connectors in organic hazardous air pollutants service removed from the process unit after the compliance date set forth in the applicable subpart for existing process units, and after the date of initial start-up for new process units. If credits are not taken, then  $C_C = 0$ .

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(2) For subsequent monitoring periods, use the following equation:

% 
$$C_L = [(C_L - C_{AN})/(C_t + C_C)] \times 100$$

where:

%  $C_L$  = Percent leaking connectors as determined through periodic monitoring required in <u>paragraphs (a)</u> and <u>(b)</u> of this section.

 $C_L$  = Number of connectors, including nonrepairables, measured at 500 parts per million or greater, by the method specified in § 63.180(b) of this subpart.

 $C_{AN}$  = Number of allowable nonrepairable connectors, as determined by monitoring required in <u>paragraphs (b)(3)</u> and <u>(c)</u> of this section, not to exceed 2 percent of the total connector population,  $C_t$ .

 $C_t$  = Total number of monitored connectors, including nonrepairables, in the process unit.

 $C_C$  = Optional credit for removed connectors = 0.67 × net number (i.e., total removed—total added) of connectors in organic hazardous air pollutants service removed from the process unit after the compliance date set forth in the applicable subpart for existing process units, and after the date of initial start-up for new process units. If credits are not taken, then  $C_C = 0$ .

(j) Optional credit for removed connectors. If an owner or operator eliminates a connector subject to monitoring under <u>paragraph (b)</u> of this section, the owner or operator may receive credit for elimination of the connector, as described in <u>paragraph (i)</u> of this section, provided the requirements in paragraphs (j)(1) through (j)(4) are met.

(1) The connector was welded after the date of proposal of the specific subpart that references this subpart.

(2) The integrity of the weld is demonstrated by monitoring it according to the procedures in  $\S$  63.180(b) of this subpart or by testing using X-ray, acoustic monitoring, hydrotesting, or other applicable method.

(3) Welds created after the date of proposal but before the date of promulgation of a specific subpart that references this subpart are monitored or tested by 3 months after the compliance date specified in the applicable subpart.

(4) Welds created after promulgation of the subpart that references this subpart are monitored or tested within 3 months after being welded.

(5) If an inadequate weld is found or the connector is not welded completely around the circumference, the connector is not considered a welded connector and is therefore not exempt from the provisions of this subpart.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48177</u>, Sept. 20, 1994; <u>61 FR 31440</u>, June 20, 1996; <u>62 FR 2791</u>, Jan. 17, 1997; <u>89 FR 43224</u>, May 16, 2024]

## § 63.175 Quality improvement program for valves.

(a) In Phase III, an owner or operator may elect to comply with one of the alternative quality improvement programs specified in <u>paragraphs (d)</u> and (e) of this section. The decision to use one of these alternative provisions to comply with the requirements of  $\frac{63.168(d)(1)(ii)}{63.168(d)(1)(ii)}$  of this subpart must be made during the first year of Phase III for existing process units and for new process units.

(b) An owner or operator of a process unit subject to the requirements of <u>paragraph (d)</u> or (e) of this section shall comply with those requirements until the process unit has fewer than 2 percent leaking valves, calculated as a rolling average of 2 consecutive quarters, as specified in  $\S$  63.168(e) of this subpart.

(c) After the process unit has fewer than 2 percent leaking valves, the owner or operator may elect to comply with the requirements in  $\frac{63.168 \text{ of this subpart}}{1000 \text{ of this subpart}}$ , to continue to comply with the requirements in paragraph (e) (or (d), if appropriate) of this section, or comply with both the requirements in  $\frac{63.168}{50.168}$  and  $\frac{63.175}{5}$ .

(1) If the owner or operator elects to continue the quality improvement program, the owner or operator is exempt from the requirements for performance trials as specified in <u>paragraph (e)(6)</u> of this section, or further progress as specified in <u>paragraph (d)(4)</u> of this section, as long as the process unit has fewer than 2 percent leaking valves calculated according to  $\frac{63.168(e)}{2}$ .

(2) If the owner or operator elects to comply with both <u>paragraph (e)</u> of this section and  $\S$  <u>63.168 of this subpart</u>, he may also take advantage of the lower monitoring frequencies associated with lower leak rates in  $\S$  <u>63.168 (d)(2)</u>, (d)(3), and (d)(4) of <u>this subpart</u>.

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(3) If the owner or operator elects not to continue the quality improvement program, the program is no longer an option if the process unit again exceeds 2 percent leaking valves, and in such case, monthly monitoring will be required.

(d) The following requirements shall be met if an owner or operator elects to use a quality improvement program to demonstrate further progress:

(1) The owner or operator shall continue to comply with the requirements in  $\frac{63.168 \text{ of this subpart}}{1000 \text{ shall}}$  except each valve shall be monitored quarterly.

(2) The owner or operator shall collect the following data, and maintain records as required in § 63.181(h)(1) of this subpart, for each valve in each process unit subject to the quality improvement program:

(i) The maximum instrument reading observed in each monitoring observation before repair, the response factor for the stream if appropriate, the instrument model number, and date of the observation.

(ii) Whether the valve is in gas or light liquid service.

(iii) If a leak is detected, the repair methods used and the instrument readings after repair.

(3) The owner or operator shall continue to collect data on the valves as long as the process unit remains in the quality improvement program.

(4) The owner or operator must demonstrate progress in reducing the percent leaking valves each quarter the process unit is subject to the requirements of <u>paragraph (d)</u> of this section, except as provided in <u>paragraphs (d)(4)(ii)</u> and <u>(d)(4)(iii)</u> of this section.

(i) Demonstration of progress shall mean that for each quarter there is at least a 10-percent reduction in the percent leaking valves from the percent leaking valves determined for the preceding monitoring period. The percent leaking valves shall be calculated as a rolling average of two consecutive quarters of monitoring data. The percent reduction shall be calculated using the rolling average percent leaking valves, according to the following:

$$LV_{R} = (LV_{AVG1} - LV_{AVG2} / LV_{AVG1} \times 100)$$

where:

 $%LV_R$  = Percent leaking valve reduction.

 $V_{AVG1} = (V_{Li} + V_{V_{Li}=1})/2.$ 

 $% LV_{AVG2} = (% V_{Li=1} + % V_{Li=2})/2.$ 

where:

 $%V_{Li}, %V_{Li=1}, %V_{Li=2}$  are percent leaking valves calculated for subsequent monitoring periods, i, i + 1, i + 2.

(ii) An owner or operator who fails for two consecutive rolling averages to demonstrate at least a 10-percent reduction per quarter in percent leaking valves, and whose overall average percent reduction based on two or more rolling averages is less than 10 percent per quarter, shall either comply with the requirements in  $\frac{63.168(d)(1)(i)}{63.168(d)(1)(i)}$  of this subpart using monthly monitoring or shall comply using a quality improvement program for technology review as specified in <u>paragraph (e)</u> of this section. If the owner or operator elects to comply with the requirements of <u>paragraph (e)</u> of this section, the schedule for performance trials and valve replacements remains as specified in <u>paragraph (e)</u> of this section.

(iii) As an alternative to the provisions in paragraph (d)(4)(i), an owner or operator may use the procedure specified in paragraphs (d)(4)(iii)(A) and (d)(4)(iii)(B) of this section to demonstrate progress in reducing the percent leaking valves.

(A) The percent reduction that must be achieved each quarter shall be calculated as follows:

$$\% RR = \frac{\% V_L - 2\%}{0.10}$$

RR = percent reduction required each quarter, as calculated according to <u>§ 63.168(e)</u>

 $%V_L$  = percent leaking values, calculated according to  $\S 63.168(e)$ , at the time elected to use provisions of  $\S 63.168(d)(1)(ii)$ 

(B) The owner or operator shall achieve less than 2 percent leaking valves no later than 2 years after electing to use the demonstration of progress provisions in  $\S$  63.175(d) of this subpart.

(e) The following requirements shall be met if an owner or operator elects to use a quality improvement program of technology review and improvement:

(1) The owner or operator shall comply with the requirements in § 63.168 of this subpart except the requirement for monthly monitoring in § 63.168(d)(1)(i) of this subpart does not apply.

(2) The owner or operator shall collect the data specified below, and maintain records as required in  $\frac{63.181(h)(2)}{1000}$ , for each valve in each process unit subject to the quality improvement program. The data may be collected and the records may be maintained on a process unit or group of process units basis. The data shall include the following:

(i) Valve type (e.g., ball, gate, check); valve manufacturer; valve design (e.g., external stem or actuating mechanism, flanged body); materials of construction; packing material; and year installed.

(ii) Service characteristics of the stream such as operating pressure, temperature, line diameter, and corrosivity.

(iii) Whether the valve is in gas or light liquid service.

(iv) The maximum instrument readings observed in each monitoring observation before repair, response factor for the stream if adjusted, instrument model number, and date of the observation.

(v) If a leak is detected, the repair methods used and the instrument readings after repair.

(vi) If the data will be analyzed as part of a larger analysis program involving data from other plants or other types of process units, a description of any maintenance or quality assurance programs used in the process unit that are intended to improve emission performance.

(3) The owner or operator shall continue to collect data on the valves as long as the process unit remains in the quality improvement program.

(4) The owner or operator shall inspect all valves removed from the process unit due to leaks. The inspection shall determine which parts of the valve have failed and shall include recommendations, as appropriate, for design changes or changes in specifications to reduce leak potential.

(5)

(i) The owner or operator shall analyze the data collected to comply with the requirements of <u>paragraph (e)(2)</u> of this section to determine the services, operating or maintenance practices, and valve designs or technologies that have poorer than average emission performance and those that have better than average emission performance. The analysis shall determine if specific trouble areas can be identified on the basis of service, operating conditions or maintenance practices, equipment design, or other process specific factors.

(ii) The analysis shall also be used to identify any superior performing valve technologies that are applicable to the service(s), operating conditions, or valve designs associated with poorer than average emission performance. A superior performing valve technology is one for which a group of such valves has a leak frequency of less than 2 percent for specific applications in such a process unit. A candidate superior performing valve technology is one demonstrated or reported in the available literature or through a group study as having low emission performance and as being capable of achieving less than 2 percent leaking valves in the process unit.

(iii) The analysis shall include consideration of:

(A) The data obtained from the inspections of valves removed from the process unit due to leaks,

(B) Information from the available literature and from the experience of other plant sites that will identify valve designs or technologies and operating conditions associated with low emission performance for specific services, and

(C) Information on limitations on the service conditions for the valve design and operating conditions as well as information on maintenance procedures to ensure continued low emission performance.

(iv) The data analysis may be conducted through an inter- or intra-company program (or through some combination of the two approaches) and may be for a single process unit, a company, or a group of process units.

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(v) The first analysis of the data shall be completed no later than 18 months after the start of Phase III. The first analysis shall be performed using a minimum of two quarters of data. An analysis of the data shall be done each year the process unit is in the quality improvement program.

(6) A trial evaluation program shall be conducted at each plant site for which the data analysis does not identify superior performing valve designs or technologies that can be applied to the operating conditions and services identified as having poorer than average performance, except as provided in paragraph (e)(6)(v) of this section. The trial program shall be used to evaluate the feasibility of using in the process unit the valve designs or technologies that have been identified by others as having low emission performance.

(i) The trial program shall include on-line trials of valves or operating and maintenance practices that have been identified in the available literature or in analysis by others as having the ability to perform with leak rates below 2 percent in similar services, as having low probability of failure, or as having no external actuating mechanism in contact with the process fluid. If any of the candidate superior performing valve technologies is not included in the performance trials, the reasons for rejecting specific technologies from consideration shall be documented as required in  $\frac{63.181(h)(5)(ii)}{1000}$  of this subpart.

(ii) The number of valves in the trial evaluation program shall be the lesser of 1 percent or 20 valves for programs involving single process units and the lesser of 1 percent or 50 valves for programs involving groups of process units.

(iii) The trial evaluation program shall specify and include documentation of:

(A) The candidate superior performing valve designs or technologies to be evaluated, the stages for evaluating the identified candidate valve designs or technologies, including the estimated time period necessary to test the applicability;

(B) The frequency of monitoring or inspection of the equipment;

(C) The range of operating conditions over which the component will be evaluated; and

(D) Conclusions regarding the emission performance and the appropriate operating conditions and services for the trial valves.

(iv) The performance trials shall initially be conducted for, at least, a 6-month period beginning not later than 18 months after the start of Phase III. Not later than 24 months after the start of Phase III, the owner or operator shall have identified valve designs or technologies that, combined with appropriate process, operating, and maintenance practices, operate with low emission performance for specific applications in the process unit. The owner or operator shall continue to conduct performance trials as long as no superior performing design or technology has been identified, except as provided in paragraph (e)(6)(vi) of this section. The compilation of candidate and demonstrated superior emission performance valve designs or technologies shall be amended in the future, as appropriate, as additional information and experience is obtained.

(v) Any plant site with fewer than 400 valves and owned by a corporation with fewer than 100 total employees shall be exempt from trial evaluations of valves. Plant sites exempt from the trial evaluations of valves shall begin the program at the start of the fourth year of Phase III.

(vi) An owner or operator who has conducted performance trials on all candidate superior emission performance technologies suitable for the required applications in the process unit may stop conducting performance trials provided that a superior performing design or technology has been demonstrated or there are no technically feasible candidate superior technologies remaining. The owner or operator shall prepare an engineering evaluation documenting the physical, chemical, or engineering basis for the judgment that the superior emission performance technology is technically infeasible or demonstrating that it would not reduce emissions.

(7) Each owner or operator who elects to use a quality improvement program for technology review and improvement shall prepare and implement a valve quality assurance program that details purchasing specifications and maintenance procedures for all valves in the process unit. The quality assurance program may establish any number of categories, or classes, of valves as needed to distinguish among operating conditions and services associated with poorer than average emission performance as well as those associated with better than average emission performance. The quality assurance program shall be developed considering the findings of the data analysis required under paragraph (e)(5) of this section, if applicable, the findings of the trial evaluation required in paragraph (e)(6) of this section, and the operating conditions in the process unit. The quality assurance program shall be reviewed and, as appropriate, updated each year as long as the process unit has 2 percent or more leaking valves.

(i) The quality assurance program shall:

(A) Establish minimum design standards for each category of valves. The design standards shall specify known critical parameters such as tolerance, manufacturer, materials of construction, previous usage, or other applicable identified critical parameters;

(B) Require that all equipment orders specify the design standard (or minimum tolerances) for the valve;

(C) Include a written procedure for bench testing of valves that specifies performance criteria for acceptance of valves and specifies criteria for the precision and accuracy of the test apparatus. All valves repaired off-line after preparation of the quality assurance plan shall be bench-tested for leaks. This testing may be conducted by the owner or operator of the process unit, by the vendor, or by a designated representative. The owner or operator shall install only those valves that have been documented through bench-testing to be nonleaking.

(D) Require that all valves repaired on-line be monitored using the method specified in  $\frac{63.180(b)}{5.180(b)}$  of this subpart for leaks for 2 successive months, after repair.

(E) Provide for an audit procedure for quality control of purchased equipment to ensure conformance with purchase specifications. The audit program may be conducted by the owner or operator of the process unit or by a designated representative.

(F) Detail off-line valve maintenance and repair procedures. These procedures shall include provisions to ensure that rebuilt or refurbished valves will meet the design specifications for the valve type and will operate such that emissions are minimized.

(ii) The quality assurance program shall be established no later than the start of the third year of Phase III for plant sites with 400 or more valves or owned by a corporation with 100 or more employees; and no later than the start of the fourth year of Phase III for plant sites with less than 400 valves and owned by a corporation with less than 100 employees.

(8) Beginning at the start of the third year of Phase III for plant sites with 400 or more valves or owned by a corporation with 100 or more employees and at the start of the fourth year of Phase III for plant sites with less than 400 valves and owned by a corporation with less than 100 employees, each valve that is replaced for any reason shall be replaced with a new or modified valve that complies with the quality assurance standards for the valve category and that is identified as superior emission performance technology means valves or valve technologies identified with emission performance that, combined with appropriate process, operating, and maintenance practices, will result in less than 2 percent leaking valves for specific applications in a large population, except as provided in paragraph (e)(8)(ii) of this section.

(i) The valves shall be maintained as specified in the quality assurance program.

(ii) If a superior emission performance technology cannot be identified, then valve replacement shall be with one of (if several) the lowest emission performance technologies that has been identified for the specific application.

[59 FR 19568, Apr. 22, 1994, as amended at 60 FR 63631, Dec. 12, 1995]

## § 63.176 Quality improvement program for pumps.

(a) In Phase III, if, on a 6-month rolling average, the greater of either 10 percent of the pumps in a process unit (or plant site) or three pumps in a process unit (or plant site) leak, the owner or operator shall comply with the requirements of this section as specified below:

(1) Pumps that are in food/medical service or in polymerizing monomer service shall comply with all requirements except for those specified in <u>paragraph (d)(8)</u> of this section.

(2) Pumps that are not in food/medical or polymerizing monomer service shall comply with all requirements of this section.

(b) The owner or operator shall comply with the requirements of this section until the number of leaking pumps is less than the greater of either 10 percent of the pumps or three pumps, calculated as a 6-month rolling average, in the process unit (or plant site). Once the performance level is achieved, the owner or operator shall comply with the requirements in  $\S$  63.163 of this subpart.

(c) If in a subsequent monitoring period, the process unit (or plant site) has greater than 10 percent of the pumps leaking or three pumps leaking (calculated as a 6-month rolling average), the owner or operator shall resume the quality improvement program starting at performance trials.

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(d) The quality improvement program shall include the following:

(1) The owner or operator shall comply with the requirements in  $\S$  63.163 of this subpart.

(2) The owner or operator shall collect the following data, and maintain records as required in  $\S$  63.181(h)(3), for each pump in each process unit (or plant site) subject to the quality improvement program. The data may be collected and the records may be maintained on a process unit or plant site basis.

(i) Pump type (e.g., piston, horizontal or vertical centrifugal, gear, bellows); pump manufacturer; seal type and manufacturer; pump design (e.g., external shaft, flanged body); materials of construction; if applicable, barrier fluid or packing material; and year installed.

(ii) Service characteristics of the stream such as discharge pressure, temperature, flow rate, corrosivity, and annual operating hours.

(iii) The maximum instrument readings observed in each monitoring observation before repair, response factor for the stream if appropriate, instrument model number, and date of the observation.

(iv) If a leak is detected, the repair methods used and the instrument readings after repair.

(v) If the data will be analyzed as part of a larger analysis program involving data from other plants or other types of process units, a description of any maintenance or quality assurance programs used in the process unit that are intended to improve emission performance.

(3) The owner or operator shall continue to collect data on the pumps as long as the process unit (or plant site) remains in the quality improvement program.

(4) The owner or operator shall inspect all pumps or pump seals which exhibited frequent seal failures and were removed from the process unit due to leaks. The inspection shall determine the probable cause of the pump seal failure or of the pump leak and shall include recommendations, as appropriate, for design changes or changes in specifications to reduce leak potential.

(5)

(i) The owner or operator shall analyze the data collected to comply with the requirements of paragraph (d)(2) of this section to determine the services, operating or maintenance practices, and pump or pump seal designs or technologies that have poorer than average emission performance and those that have better than average emission performance. The analysis shall determine if specific trouble areas can be identified on the basis of service, operating conditions or maintenance practices, equipment design, or other process specific factors.

(ii) The analysis shall also be used to determine if there are superior performing pump or pump seal technologies that are applicable to the service(s), operating conditions, or pump or pump seal designs associated with poorer than average emission performance. A superior performing pump or pump seal technology is one with a leak frequency of less than 10 percent for specific applications in the process unit or plant site. A candidate superior performing pump or pump seal technology is one demonstrated or reported in the available literature or through a group study as having low emission performance and as being capable of achieving less than 10 percent leaking pumps in the process unit (or plant site).

(iii) The analysis shall include consideration of:

(A) The data obtained from the inspections of pumps and pump seals removed from the process unit due to leaks;

(B) Information from the available literature and from the experience of other plant sites that will identify pump designs or technologies and operating conditions associated with low emission performance for specific services; and

(C) Information on limitations on the service conditions for the pump seal technology operating conditions as well as information on maintenance procedures to ensure continued low emission performance.

(iv) The data analysis may be conducted through an inter- or intra-company program (or through some combination of the two approaches) and may be for a single process unit, a plant site, a company, or a group of process units.

(v) The first analysis of the data shall be completed no later than 18 months after the start of the quality improvement program. The first analysis shall be performed using a minimum of 6 months of data. An analysis of the data shall be done each year the process unit is in the quality improvement program.

(6) A trial evaluation program shall be conducted at each plant site for which the data analysis does not identify use of superior performing pump seal technology or pumps that can be applied to the areas identified as having poorer than average performance, except as provided in paragraph (d)(6)(v) of this section. The trial program shall be used to evaluate the feasibility of using in the process unit (or plant site) the pump designs or seal technologies, and operating and maintenance practices that have been identified by others as having low emission performance.

(i) The trial program shall include on-line trials of pump seal technologies or pump designs and operating and maintenance practices that have been identified in the available literature or in analysis by others as having the ability to perform with leak rates below 10 percent in similar services, as having low probability of failure, or as having no external actuating mechanism in contact with the process fluid. If any of the candidate superior performing pump seal technologies or pumps is not included in the performance trials, the reasons for rejecting specific technologies from consideration shall be documented as required in  $\frac{63.181(h)(5)(ii)}{10}$ .

(ii) The number of pump seal technologies or pumps in the trial evaluation program shall be the lesser of 1 percent or two pumps for programs involving single process units and the lesser of 1 percent or five pumps for programs involving a plant site or groups of process units. The minimum number of pumps or pump seal technologies in a trial program shall be one.

(iii) The trial evaluation program shall specify and include documentation of:

(A) The candidate superior performing pump seal designs or technologies to be evaluated, the stages for evaluating the identified candidate pump designs or pump seal technologies, including the time period necessary to test the applicability;

(B) The frequency of monitoring or inspection of the equipment;

(C) The range of operating conditions over which the component will be evaluated; and

(D) Conclusions regarding the emission performance and the appropriate operating conditions and services for the trial pump seal technologies or pumps.

(iv) The performance trials shall initially be conducted, at least, for a 6-month period beginning not later than 18 months after the start of the quality improvement program. No later than 24 months after the start of the quality improvement program, the owner or operator shall have identified pump seal technologies or pump designs that, combined with appropriate process, operating, and maintenance practices, operate with low emission performance for specific applications in the process unit. The owner or operator shall continue to conduct performance trials as long as no superior performing design or technology has been identified, except as provided in paragraph (d)(6)(vi) of this section. The initial list of superior emission performance pump designs or pump seal technologies shall be amended in the future, as appropriate, as additional information and experience is obtained.

(v) Any plant site with fewer than 400 valves and owned by a corporation with fewer than 100 employees shall be exempt from trial evaluations of pump seals or pump designs. Plant sites exempt from the trial evaluations of pumps shall begin the pump seal or pump replacement program at the start of the fourth year of the quality improvement program.

(vi) An owner or operator who has conducted performance trials on all alternative superior emission performance technologies suitable for the required applications in the process unit may stop conducting performance trials provided that a superior performing design or technology has been demonstrated or there are no technically feasible alternative superior technologies remaining. The owner or operator shall prepare an engineering evaluation documenting the physical, chemical, or engineering basis for the judgment that the superior emission performance technology is technically infeasible or demonstrating that it would not reduce emissions.

(7) Each owner or operator shall prepare and implement a pump quality assurance program that details purchasing specifications and maintenance procedures for all pumps and pump seals in the process unit. The quality assurance program may establish any number of categories, or classes, of pumps as needed to distinguish among operating conditions and services associated with poorer than average emission performance as well as those associated with better than average emission performance. The quality assurance program shall be developed considering the findings of the data analysis required under paragraph (d)(5) of this section, if applicable, the findings of the trial evaluation required in paragraph (d)(6) of this section, and the operating conditions in the process unit. The quality assurance program shall be updated each year as long as the process unit has the greater of either 10 percent or more leaking pumps or has three leaking pumps.

(i) The quality assurance program shall:

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(A) Establish minimum design standards for each category of pumps or pump seal technology. The design standards shall specify known critical parameters such as tolerance, manufacturer, materials of construction, previous usage, or other applicable identified critical parameters;

(B) Require that all equipment orders specify the design standard (or minimum tolerances) for the pump or the pump seal;

(C) Provide for an audit procedure for quality control of purchased equipment to ensure conformance with purchase specifications. The audit program may be conducted by the owner or operator of the plant site or process unit or by a designated representative; and

(D) Detail off-line pump maintenance and repair procedures. These procedures shall include provisions to ensure that rebuilt or refurbished pumps and pump seals will meet the design specifications for the pump category and will operate such that emissions are minimized.

(ii) The quality assurance program shall be established no later than the start of the third year of the quality improvement program for plant sites with 400 or more valves or 100 or more employees; and no later than the start of the fourth year of the quality improvement program for plant sites with less than 400 valves and less than 100 employees.

(8) Beginning at the start of the third year of the quality improvement program for plant sites with 400 or more valves or 100 or more employees and at the start of the fourth year of the quality improvement program for plant sites with less than 400 valves and less than 100 employees, the owner or operator shall replace, as described in <u>paragraphs (d)(8)(i)</u> and (d)(8)(ii) of this section, the pumps or pump seals that are not superior emission performance technology with pumps or pump seals that have been identified as superior emission performance technology and that comply with the quality assurance standards for the pump category. Superior emission performance technology is that category or design of pumps or pump seals with emission performance which, when combined with appropriate process, operating, and maintenance practices, will result in less than 10 percent leaking pumps for specific applications in the process unit or plant site. Superior emission performance technology includes material or design changes to the existing pump, pump seal, seal support system, installation of multiple mechanical seals or equivalent, or pump replacement.

(i) Pumps or pump seals shall be replaced at the rate of 20 percent per year based on the total number of pumps in light liquid service. The calculated value shall be rounded to the nearest nonzero integer value. The minimum number of pumps or pump seals shall be one. Pump replacement shall continue until all pumps subject to the requirements of § 63.163 of this subpart are pumps determined to be superior performance technology.

(ii) The owner or operator may delay replacement of pump seals or pumps with superior technology until the next planned process unit shutdown, provided the number of pump seals and pumps replaced is equivalent to the 20 percent or greater annual replacement rate.

(iii) The pumps shall be maintained as specified in the quality assurance program.

## § 63.177 Alternative means of emission limitation: General.

(a) Permission to use an alternative means of emission limitation under section 112(h)(3) of the Act shall be governed by the following procedures in <u>paragraphs (b)</u> through (c) of this section.

(b) Where the standard is an equipment, design, or operational requirement:

(1) Each owner or operator applying for permission to use an alternative means of emission limitation under  $\underline{\$}$  <u>63.6(g)</u> of <u>subpart A of this part</u> shall be responsible for collecting and verifying emission performance test data for an alternative means of emission limitation.

(2) The Administrator will compare test data for the means of emission limitation to test data for the equipment, design, and operational requirements.

(3) The Administrator may condition the permission on requirements that may be necessary to ensure operation and maintenance to achieve the same emission reduction as the equipment, design, and operational requirements.

(c) Where the standard is a work practice:

(1) Each owner or operator applying for permission shall be responsible for collecting and verifying test data for an alternative means of emission limitation.
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(2) For each kind of equipment for which permission is requested, the emission reduction achieved by the required work practices shall be demonstrated for a minimum period of 12 months.

(3) For each kind of equipment for which permission is requested, the emission reduction achieved by the alternative means of emission limitation shall be demonstrated.

(4) Each owner or operator applying for permission shall commit, in writing, for each kind of equipment to work practices that provide for emission reductions equal to or greater than the emission reductions achieved by the required work practices.

(5) The Administrator will compare the demonstrated emission reduction for the alternative means of emission limitation to the demonstrated emission reduction for the required work practices and will consider the commitment in paragraph (c)(4) of this section.

(6) The Administrator may condition the permission on requirements that may be necessary to ensure operation and maintenance to achieve the same or greater emission reduction as the required work practices of this subpart.

(d) An owner or operator may offer a unique approach to demonstrate the alternative means of emission limitation.

(e)

(1) Manufacturers of equipment used to control equipment leaks of an organic HAP may apply to the Administrator for permission for an alternative means of emission limitation that achieves a reduction in emissions of the organic HAP achieved by the equipment, design, and operational requirements of this subpart.

(2) The Administrator will grant permission according to the provisions of paragraphs (b), (c), and (d) of this section.

#### § 63.178 Alternative means of emission limitation: Batch processes.

(a) As an alternative to complying with the requirements of §§ 63.163 through 63.171 and §§ 63.173 through 63.176, an owner or operator of a batch process that operates in organic HAP service during the calendar year may comply with one of the standards specified in paragraphs (b) and (c) of this section, or the owner or operator may petition for approval of an alternative standard under the provisions of § 63.177 of this subpart. The alternative standards of this section provide the options of pressure testing or monitoring the equipment for leaks. The owner or operator may switch among the alternatives provided the change is documented as specified in § 63.181.

(b) The following requirements shall be met if an owner or operator elects to use pressure testing of batch product-process equipment to demonstrate compliance with this subpart. An owner or operator who complies with the provisions of this paragraph is exempt from the monitoring provisions of § 63.163, §§ 63.168 and 63.169, and §§ 63.173 through 63.176 of this subpart.

(1) Each time equipment is reconfigured for production of a different product or intermediate, the batch product-process equipment train shall be pressure-tested for leaks before organic HAP is first fed to the equipment and the equipment is placed in organic HAP service.

(i) When the batch product-process train is reconfigured to produce a different product, pressure testing is required only for the new or disturbed equipment.

(ii) Each batch product process that operates in organic HAP service during a calendar year shall be pressure tested at least once during that calendar year.

(iii) Pressure testing is not required for routine seal breaks, such as changing hoses or filters, which are not part of the reconfiguration to produce a different product or intermediate.

(2) The batch product process equipment shall be tested either using the procedures specified in  $\frac{63.180(f)}{100}$  of this subpart for pressure or vacuum loss or with a liquid using the procedures specified in  $\frac{63.180(g)}{100}$  of this subpart.

(3)

(i) For pressure or vacuum tests, a leak is detected if the rate of change in pressure is greater than 6.9 kilopascals (1 psig) in 1 hour or if there is visible, audible, or olfactory evidence of fluid loss.

(ii) For pressure tests using a liquid, a leak is detected if there are indications of liquids dripping or if there is other evidence of fluid loss.

(4)

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(i) If a leak is detected, it shall be repaired and the batch product-process equipment shall be retested before start-up of the process.

(ii) If a batch product-process fails the retest or the second of two consecutive pressure tests, it shall be repaired as soon as practicable, but not later than 30 calendar days after the second pressure test, provided the conditions specified in <u>paragraph</u> (d) of this section are met.

(c) The following requirements shall be met if an owner or operator elects to monitor the equipment to detect leaks by the method specified in  $\frac{63.180(b)}{5.000}$  of this subpart to demonstrate compliance with this subpart.

(1) The owner or operator shall comply with the requirements of  $\frac{\$\$ 63.163}{\$}$  through  $\frac{63.170}{\$\$ 63.172}$  through  $\frac{63.176}{\$\$ 63.172}$  through  $\frac{63.176}{\$\$ 83.172}$  through  $\frac{63.176}{\$\ast 83.172}$  through \frac{

(2) The equipment shall be monitored for leaks by the method specified in  $\S$  63.180(b) of this subpart when the equipment is in organic HAP service, in use with an acceptable surrogate volatile organic compound which is not an organic HAP, or is in use with any other detectable gas or vapor.

(3) The equipment shall be monitored for leaks as specified below:

(i) Each time the equipment is reconfigured for the production of a new product, the reconfigured equipment shall be monitored for leaks within 30 days of start-up of the process. This initial monitoring of reconfigured equipment shall not be included in determining percent leaking equipment in the process unit.

(ii) Connectors shall be monitored in accordance with the requirements in § 63.174 of this subpart.

(iii) Equipment other than connectors shall be monitored at the frequencies specified in table 1 of this subpart. The operating time shall be determined as the proportion of the year the batch product-process that is subject to the provisions of this subpart is operating.

(iv) The monitoring frequencies specified in table 1 of this subpart are not requirements for monitoring at specific intervals and can be adjusted to accommodate process operations. An owner or operator may monitor anytime during the specified monitoring period (e.g., month, quarter, year), provided the monitoring is conducted at a reasonable interval after completion of the last monitoring campaign. For example, if the equipment is not operating during the scheduled monitoring period, the monitoring can be done during the next period when the process is operating.

(4) If a leak is detected, it shall be repaired as soon as practicable but not later than 15 calendar days after it is detected, except as provided in <u>paragraph (d)</u> of this section.

(d) Delay of repair of equipment for which leaks have been detected is allowed if the replacement equipment is not available providing the following conditions are met:

(1) Equipment supplies have been depleted and supplies had been sufficiently stocked before the supplies were depleted.

(2) The repair is made no later than 10 calendar days after delivery of the replacement equipment.

#### § 63.179 Alternative means of emission limitation: Enclosed-vented process units.

Process units enclosed in such a manner that all emissions from equipment leaks are vented through a closed-vent system to a control device meeting the requirements of § 63.172 of this subpart are exempt from the requirements of § 63.163, through 63.171, and §§ 63.173 and 63.174 of this subpart. The enclosure shall be maintained under a negative pressure at all times while the process unit is in operation to ensure that all emissions are routed to a control device.

#### § 63.180 Test methods and procedures.

(a) Each owner or operator subject to the provisions of this subpart shall comply with the test methods and procedures requirements provided in this section.

(b) Monitoring, as required under this subpart, shall comply with the following requirements:

(1) Monitoring shall comply with Method 21 of 40 CFR part 60, appendix A.

(2)

(i) Except as provided for in <u>paragraph (b)(2)(ii)</u> of this section, the detection instrument shall meet the performance criteria of Method 21 of 40 CFR part 60, appendix A, except the instrument response factor criteria in <u>Section 3.1.2(a)</u> of Method 21

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shall be for the average composition of the process fluid not each individual VOC in the stream. For process streams that contain nitrogen, water, air, or other inerts which are not organic HAP's or VOC's, the average stream response factor may be calculated on an inert-free basis. The response factor may be determined at any concentration for which monitoring for leaks will be conducted.

(ii) If no instrument is available at the plant site that will meet the performance criteria specified in <u>paragraph (b)(2)(i)</u> of this section, the instrument readings may be adjusted by multiplying by the average response factor of the process fluid, calculated on an inert-free basis as described in <u>paragraph (b)(2)(i)</u> of this section.

(3) The instrument shall be calibrated before use on each day of its use by the procedures specified in Method 21 of  $\frac{40 \text{ CFR}}{21 \text{ part } 60, \text{ appendix A}}$ .

(4) Calibration gases shall be:

(i) Zero air (less than 10 parts per million of hydrocarbon in air); and

(ii) Mixtures of methane in air at the concentrations specified in paragraphs (b)(4)(ii)(A) through (b)(4)(ii)(C) of this section. A calibration gas other than methane in air may be used if the instrument does not respond to methane or if the instrument does not meet the performance criteria specified in paragraph (b)(2)(i) of this section. In such cases, the calibration gas may be a mixture of one or more of the compounds to be measured in air.

(A) For Phase I, a mixture of methane or other compounds, as applicable, in air at a concentration of approximately, but less than, 10,000 parts per million.

(B) For Phase II, a mixture of methane or other compounds, as applicable, and air at a concentration of approximately, but less than, 10,000 parts per million for agitators, 5,000 parts per million for pumps, and 500 parts per million for all other equipment, except as provided in paragraph (b)(4)(iii) of this section.

(C) For Phase III, a mixture of methane or other compounds, as applicable, and air at a concentration of approximately, but less than, 10,000 parts per million methane for agitators; 2,000 parts per million for pumps in food/medical service; 5,000 parts per million for pumps in polymerizing monomer service; 1,000 parts per million for all other pumps; and 500 parts per million for all other equipment, except as provided in paragraph (b)(4)(iii) of this section.

(iii) The instrument may be calibrated at a higher methane concentration than the concentration specified for that piece of equipment. The concentration of the calibration gas may exceed the concentration specified as a leak by no more than 2,000 parts per million. If the monitoring instrument's design allows for multiple calibration scales, then the lower scale shall be calibrated with a calibration gas that is no higher than 2,000 parts per million above the concentration specified as a leak and the highest scale shall be calibrated with a calibration gas that is approximately equal to 10,000 parts per million. If only one scale on an instrument will be used during monitoring, the owner or operator need not calibrate the scales that will not be used during that day's monitoring.

(5) Monitoring shall be performed when the equipment is in organic HAP service, in use with an acceptable surrogate volatile organic compound which is not an organic HAP, or is in use with any other detectable gas or vapor.

(6) Monitoring data that do not meet the criteria specified in <u>paragraphs (b)(1)</u> through (b)(5) of this section may be used to qualify for less frequent monitoring under the provisions in § 63.168(d)(2) and (d)(3) or § 63.174(b)(3)(ii) or (b)(3)(iii) of this subpart provided the data meet the conditions specified in <u>paragraphs (b)(6)(i)</u> and (b)(6)(ii) of this section.

(i) The data were obtained before April 22, 1994.

(ii) The departures from the criteria specified in <u>paragraphs (b)(1)</u> through (b)(5) of this section or from the specified monitoring frequency of § 63.168(c) are minor and do not significantly affect the quality of the data. Examples of minor departures are monitoring at a slightly different frequency (such as every six weeks instead of monthly or quarterly), following the performance criteria of section 3.1.2(a) of Method 21 of appendix A of 40 CFR part 60 instead of <u>paragraph</u> (b)(2) of this section, or monitoring at a different leak definition if the data would indicate the presence or absence of a leak at the concentration specified in this subpart. Failure to use a calibrated instrument is not considered a minor departure.

(c) When equipment is monitored for compliance as required in  $\frac{\$\$ 63.164(i)}{\$!}, \frac{63.165(a)}{\$!}$  or (e)(1), and  $\frac{63.172(f)}{\$!}$  or when equipment subject to a leak definition of 500 ppm is monitored for leaks as required by this subpart, the owner or operator may elect to adjust or not to adjust the instrument readings for background. If an owner or operator elects to not adjust instrument readings for background, the owner or operator shall monitor the equipment according to the procedures specified in paragraphs (b)(1) through (4) of this section. In such case, all instrument readings shall be compared directly to the

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applicable leak definition to determine whether there is a leak. If an owner or operator elects to adjust instrument readings for background, the owner or operator shall monitor the equipment according to the procedures specified in <u>paragraphs</u> (c)(1) through (c)(4) of this section.

(1) The requirements of <u>paragraphs (b) (1)</u> through (4) of this section shall apply.

(2) The background level shall be determined, using the same procedures that will be used to determine whether the equipment is leaking.

(3) The instrument probe shall be traversed around all potential leak interfaces as close to the interface as possible as described in Method 21 of  $\frac{40 \text{ CFR part } 60, \text{ appendix } A}{1000 \text{ A}}$ .

(4) The arithmetic difference between the maximum concentration indicated by the instrument and the background level is compared with 500 parts per million for determining compliance.

(d)

(1) Each piece of equipment within a process unit that can reasonably be expected to contain equipment in organic HAP service is presumed to be in organic HAP service unless an owner or operator demonstrates that the piece of equipment is not in organic HAP service. For a piece of equipment to be considered not in organic HAP service, it must be determined that the percent organic HAP content can be reasonably expected not to exceed 5 percent by weight on an annual average basis. For purposes of determining the percent organic HAP content of the process fluid that is contained in or contacts equipment, Method 18 of <u>40 CFR part 60, appendix A</u> shall be used. ASTM D6420-18 (incorporated by reference, see § <u>63.14</u>) may also be used in lieu of Method 18, if the target compounds are all known and are all listed in <u>Section 1.1</u> of ASTM D6420-18 as measurable; ASTM D6420-18 must not be used for methane and ethane; and ASTM D6420-18 may not be used as a total VOC method.

(2)

(i) An owner or operator may use good engineering judgment rather than the procedures in <u>paragraph (d)(1)</u> of this section to determine that the percent organic HAP content does not exceed 5 percent by weight. When an owner or operator and the Administrator do not agree on whether a piece of equipment is not in organic HAP service, however, the procedures in <u>paragraph (d)(1)</u> of this section shall be used to resolve the disagreement.

(ii) Conversely, the owner or operator may determine that the organic HAP content of the process fluid does not exceed 5 percent by weight by, for example, accounting for 98 percent of the content and showing that organic HAP is less than 3 percent.

(3) If an owner or operator determines that a piece of equipment is in organic HAP service, the determination can be revised after following the procedures in paragraph (d)(1) of this section, or by documenting that a change in the process or raw materials no longer causes the equipment to be in organic HAP service.

(4) Samples used in determining the percent organic HAP content shall be representative of the process fluid that is contained in or contacts the equipment.

(e) When a flare is used to comply with  $\S 63.172(d)$ , the owner or operator shall comply with <u>paragraphs (e)(1)</u> through (3) of this section, except as specified in <u>paragraph (a) of § 63.108</u>. The owner or operator is not required to conduct a performance test to determine percent emission reduction or outlet organic HAP or TOC concentration.

(1) Conduct a visible emission test using the techniques specified in  $\frac{63.11(b)(4)}{2}$ .

(2) Determine the net heating value of the gas being combusted using the techniques specified in  $\frac{63.11(b)(6)}{5}$ .

(3) Determine the exit velocity using the techniques specified in either  $\S 63.11(b)(7)(i)$  (and  $\S 63.11(b)(7)(iii)$ , where applicable) or  $\S 63.11(b)(8)$ , as appropriate.

(f) The following procedures shall be used to pressure test batch product-process equipment for pressure or vacuum loss to demonstrate compliance with the requirements of  $\frac{63.178(b)(3)(i)}{63.178(b)(3)(i)}$  of this subpart.

(1) The batch product-process equipment train shall be pressurized with a gas to a pressure less than the set pressure of any safety relief devices or valves or to a pressure slightly above the operating pressure of the equipment, or alternatively, the equipment shall be placed under a vacuum.

(2) Once the test pressure is obtained, the gas source or vacuum source shall be shut off.

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(3) The test shall continue for not less than 15 minutes unless it can be determined in a shorter period of time that the allowable rate of pressure drop or of pressure rise was exceeded. The pressure in the batch product-process equipment shall be measured after the gas or vacuum source is shut off and at the end of the test period. The rate of change in pressure in the batch product-process equipment shall be calculated using the following equation:

$$\Delta \frac{\mathbf{P}}{\mathbf{t}} = \frac{\left(\left|\mathbf{P}_{\mathrm{f}} - \mathbf{P}_{\mathrm{i}}\right|\right)}{\left(\mathbf{t}_{\mathrm{f}} - \mathbf{t}_{\mathrm{i}}\right)}$$

where:

 $\Delta P/t =$  Change in pressure, psig/hr.

 $P_f = Final pressure, psig.$ 

 $P_i$  = Initial pressure, psig.

 $t_f - t_i = Elapsed time, hours.$ 

(4) The pressure shall be measured using a pressure measurement device (gauge, manometer, or equivalent) which has a precision of  $\pm 2.5$  millimeter mercury in the range of test pressure and is capable of measuring pressures up to the relief set pressure of the pressure relief device. If such a pressure measurement device is not reasonably available, the owner or operator shall use a pressure measurement device with a precision of at least + 10 percent of the test pressure of the equipment and shall extend the duration of the test for the time necessary to detect a pressure loss or rise that equals a rate of one psig per hour.

(5) An alternative procedure may be used for leak testing the equipment if the owner or operator demonstrates the alternative procedure is capable of detecting a pressure loss or rise.

(g) The following procedures shall be used to pressure-test batch product-process equipment using a liquid to demonstrate compliance with the requirements of  $\frac{63.178(b)(3)(ii)}{5.000}$  of this subpart.

(1) The batch product-process equipment train, or section of the train, shall be filled with the test liquid (e.g., water, alcohol) until normal operating pressure is obtained. Once the equipment is filled, the liquid source shall be shut off.

(2) The test shall be conducted for a period of at least 60 minutes, unless it can be determined in a shorter period of time that the test is a failure.

(3) Each seal in the equipment being tested shall be inspected for indications of liquid dripping or other indications of fluid loss. If there are any indications of liquids dripping or of fluid loss, a leak is detected.

(4) An alternative procedure may be used for leak testing the equipment, if the owner or operator demonstrates the alternative procedure is capable of detecting losses of fluid.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48177</u>, Sept. 20, 1994; <u>61 FR 31440</u>, June 20, 1996; <u>62 FR 2792</u>, Jan. 17, 1997; <u>66 FR 6936</u>, Jan. 22, 2001; <u>89 FR 43225</u>, May 16, 2024]

# § 63.181 Recordkeeping requirements.

(a) An owner or operator of more than one process unit subject to the provisions of this subpart may comply with the recordkeeping requirements for these process units in one recordkeeping system if the system identifies each record by process unit and the program being implemented (e.g., quarterly monitoring, quality improvement) for each type of equipment. All records and information required by this section shall be maintained in a manner that can be readily accessed at the plant site. This could include physically locating the records at the plant site or accessing the records from a central location by computer at the plant site.

(b) Except as provided in <u>paragraph (e)</u> of this section, the following information pertaining to all equipment in each process unit subject to the requirements in <u>\$</u> 63.162 through 63.174 of this subpart shall be recorded:

(1)

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(i) A list of identification numbers for equipment (except connectors exempt from monitoring and recordkeeping identified in  $\frac{63.174}{5}$  of this subpart and instrumentation systems) subject to the requirements of this subpart. Connectors need not be individually identified if all connectors in a designated area or length of pipe subject to the provisions of this subpart are identified as a group, and the number of connectors subject is indicated. With respect to connectors, the list shall be complete no later than the completion of the initial survey required by  $\frac{63.174}{5}$  (b)(1) or (b)(2) of this subpart.

(ii) A schedule by process unit for monitoring connectors subject to the provisions of  $\S$  63.174(a) of this subpart and valves subject to the provisions of  $\S$  63.168(d) of this subpart.

(iii) Physical tagging of the equipment to indicate that it is in organic HAP service is not required. Equipment subject to the provisions of this subpart may be identified on a plant site plan, in log entries, or by other appropriate methods.

(2)

(i) A list of identification numbers for equipment that the owner or operator elects to equip with a closed-vent system and control device, under the provisions of  $\S$  63.163(g),  $\S$  63.164(h),  $\S$  63.165(c) or (e)(4), or  $\S$  63.173(f), as applicable.

(ii) A list of identification numbers for compressors that the owner or operator elects to designate as operating with an instrument reading of less than 500 parts per million above background, under the provisions of  $\S$  63.164(i) of this subpart.

(iii) Identification of surge control vessels or bottoms receivers subject to the provisions of this subpart that the owner or operator elects to equip with a closed-vent system and control device, under the provisions of  $\frac{63.170}{5.000}$  of this subpart.

(3)

(i) A list of identification numbers for pressure relief devices subject to the provisions in  $\S 63.165(a)$  or (e)(1), as applicable.

(ii) A list of identification numbers for pressure relief devices equipped with rupture disks, under the provisions of  $\S$  <u>63.165(d)</u>, (e)(2)(ii), or (e)(2)(iii), as applicable.

(4) Identification of instrumentation systems subject to the provisions of this subpart. Individual components in an instrumentation system need not be identified.

(5) Identification of screwed connectors subject to the requirements of  $\S$  63.174(c)(2) of this subpart. Identification can be by area or grouping as long as the total number within each group or area is recorded.

(6) The following information shall be recorded for each dual mechanical seal system:

(i) Design criteria required in  $\underline{\$\$} \underline{63.163(e)(6)(i)}, \underline{63.164(e)(2)}$ , and  $\underline{63.173(d)(6)(i)}$  of this subpart and an explanation of the design criteria; and

(ii) Any changes to these criteria and the reasons for the changes.

(7) The following information pertaining to all pumps subject to the provisions of  $\S$  <u>63.163(j)</u>, valves subject to the provisions of  $\S$  <u>63.168(h)</u> and <u>(i)</u> of this subpart</u>, agitators subject to the provisions of  $\S$  <u>63.173(h)</u> through <u>(j)</u>, and connectors subject to the provisions of  $\S$  <u>63.174(f)</u> and <u>(g)</u> of this subpart</u> shall be recorded:

(i) Identification of equipment designated as unsafe to monitor, difficult to monitor, or unsafe to inspect and the plan for monitoring or inspecting this equipment.

(ii) A list of identification numbers for the equipment that is designated as difficult to monitor, an explanation of why the equipment is difficult to monitor, and the planned schedule for monitoring this equipment.

(iii) A list of identification numbers for connectors that are designated as unsafe to repair and an explanation why the connector is unsafe to repair.

(8)

(i) A list of valves removed from and added to the process unit, as described in  $\S$  63.168(e)(1) of this subpart, if the net credits for removed valves is expected to be used.

(ii) A list of connectors removed from and added to the process unit, as described in  $\frac{63.174(i)(1)}{100}$  of this subpart, and documentation of the integrity of the weld for any removed connectors, as required in  $\frac{63.174(j)}{100}$  of this subpart. This is not required unless the net credits for removed connectors is expected to be used.

(9)

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(ii) Records demonstrating the proportion of the time during the calendar year the equipment is in use in a batch process that is subject to the provisions of this subpart. Examples of suitable documentation are records of time in use for individual pieces of equipment or average time in use for the process unit. These records are not required if the owner or operator does not adjust monitoring frequency by the time in use, as provided in  $\frac{§ 63.178(c)(3)(iii)}{5.000}$  of this subpart.

(10) For any leaks detected as specified in  $\frac{\$\$ 63.163}{\$\$ 63.164}$  and  $\frac{63.164}{\$\$ 63.168}$  and  $\frac{63.169}{\$\$ 63.172}$  through  $\frac{63.174 \text{ of this}}{\$\$ 83.174}$  and  $\frac{\$\$ 63.169}{\$\$ 83.172}$  through  $\frac{63.174 \text{ of this}}{\$\$ 83.174}$  and  $\frac{\$\$ 63.169}{\$\$ 83.172}$  through  $\frac{63.174 \text{ of this}}{\$\$ 83.174}$  of the equipment identification number, shall be attached to the leaking equipment.

(11) For each pressure relief device subject to the pressure release management work practice standards in § 63.165(e), owners and operators must keep the records specified in paragraphs (b)(11)(i) through (iii) of this section in addition to the records specified in paragraph (f) of this section.

(i) Records of the prevention measures implemented as required in § 63.165(e)(3)(ii).

(ii) Records of the number of releases during each calendar year. Keep these records for the current calendar year and the past 5 calendar years.

(iii) For each release to the atmosphere, owners and operators must keep the records specified in <u>paragraphs</u> (b)(11)(iii)(A) through (D) of this section.

(A) The start and end time and date of each pressure release to the atmosphere.

(B) Records of any data, assumptions, and calculations used to estimate of the mass quantity of each organic HAP released during the event.

(C) Records of the root cause analysis and corrective action analysis conducted as required in  $\frac{63.165(e)(3)(iii)}{1000}$ , including an identification of the affected facility, a statement noting whether the event resulted from the same root cause(s) identified in a previous analysis and either a description of the recommended corrective action(s) or an explanation of why corrective action is not necessary under  $\frac{63.165(e)(7)(i)}{1000}$ .

(D) For any corrective action analysis for which implementation of corrective actions are required in  $\S$  <u>63.165(e)(7)</u>, a description of the corrective action(s) completed within the first 45 days following the discharge and, for action(s) not already completed, a schedule for implementation, including proposed commencement and completion dates.

(12) For equipment in ethylene oxide service, as defined in  $\S$  63.101, records of the percent ethylene oxide content of the process fluid and the method used to determine it.

(c) For visual inspections of equipment subject to the provisions of this subpart (e.g.,  $\frac{63.163(b)(3)}{63.163(c)(4)(i)}$ ), the owner or operator shall document that the inspection was conducted and the date of the inspection. The owner or operator shall maintain records as specified in <u>paragraph (d)</u> of this section for leaking equipment identified in this inspection, except as provided in <u>paragraph (e)</u> of this section. These records shall be retained for 2 years.

(d) When each leak is detected as specified in  $\frac{\$\$ 63.163}{\$}$  and  $\frac{63.164}{\$\$ 63.168}$  and  $\frac{63.169}{\$}$ ; and  $\frac{\$\$ 63.172}{\$\$ 63.172}$  through  $\frac{63.174 \text{ of}}{\$1.174 \text{ of}}$  this subpart, the following information shall be recorded and kept for 2 years:

(1) The instrument and the equipment identification number and the operator name, initials, or identification number.

(2) The date the leak was detected and the date of first attempt to repair the leak.

(3) The date of successful repair of the leak.

(4) Maximum instrument reading measured by Method 21 of <u>40 CFR part 60, appendix A</u> after it is successfully repaired or determined to be nonrepairable.

(5) "Repair delayed" and the reason for the delay if a leak is not repaired within 15 calendar days after discovery of the leak.

(i) The owner or operator may develop a written procedure that identifies the conditions that justify a delay of repair. The written procedures may be included as part of the startup/shutdown/malfunction plan, required by  $\S$  <u>63.6(e)(3)</u>, for the source or may be part of a separate document that is maintained at the plant site. In such cases, reasons for delay of repair may be

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documented by citing the relevant sections of the written procedure. For each source as defined in § 63.101, and for each source as defined in § 63.191, on and after July 15, 2027, the sentence "The written procedures may be included as part of the startup/shutdown/malfunction plan, required by § 63.6(e)(3), for the source or may be part of a separate document that is maintained at the plant site." in this paragraph no longer applies.

(ii) If delay of repair was caused by depletion of stocked parts, there must be documentation that the spare parts were sufficiently stocked on-site before depletion and the reason for depletion.

(6) Dates of process unit shutdowns that occur while the equipment is unrepaired.

(7)

(i) Identification, either by list, location (area or grouping), or tagging of connectors that have been opened or otherwise had the seal broken since the last monitoring period required in § 63.174(b) of this subpart, as described in § 63.174(c)(1) of this subpart, unless the owner or operator elects to comply with the provisions of § 63.174(c)(1)(ii) of this subpart.

(ii) The date and results of monitoring as required in  $\S 63.174(c)$  of this subpart. If identification of connectors that have been opened or otherwise had the seal broken is made by location under paragraph (d)(7)(i) of this section, then all connectors within the designated location shall be monitored.

(8) The date and results of the monitoring required in  $\S 63.178(c)(3)(i)$  of this subpart for equipment added to a batch process unit since the last monitoring period required in  $\S 63.178(c)(3)(ii)$  and (c)(3)(iii) of this subpart. If no leaking equipment is found in this monitoring, the owner or operator shall record that the inspection was performed. Records of the actual monitoring results are not required.

(9) Copies of the periodic reports as specified in  $\S$  63.182(d) of this subpart, if records are not maintained on a computerized database capable of generating summary reports from the records.

(e) The owner or operator of a batch product process who elects to pressure test the batch product process equipment train to demonstrate compliance with this subpart is exempt from the requirements of <u>paragraphs (b)</u>, (c), (d), and (f) of this section. Instead, the owner or operator shall maintain records of the following information:

(1) The identification of each product, or product code, produced during the calendar year. It is not necessary to identify individual items of equipment in a batch product process equipment train.

(2) [Reserved]

(3) Physical tagging of the equipment to identify that it is in organic HAP service and subject to the provisions of this subpart is not required. Equipment in a batch product process subject to the provisions of this subpart may be identified on a plant site plan, in log entries, or by other appropriate methods.

(4) The dates of each pressure test required in  $\S$  63.178(b) of this subpart, the test pressure, and the pressure drop observed during the test.

(5) Records of any visible, audible, or olfactory evidence of fluid loss.

(6) When a batch product process equipment train does not pass two consecutive pressure tests, the following information shall be recorded in a log and kept for 2 years:

(i) The date of each pressure test and the date of each leak repair attempt.

(ii) Repair methods applied in each attempt to repair the leak.

(iii) The reason for the delay of repair.

(iv) The expected date for delivery of the replacement equipment and the actual date of delivery of the replacement equipment.

(v) The date of successful repair.

(f) The dates and results of each compliance test required for compressors subject to the provisions in  $\S 63.164(i)$  and the dates and results of the monitoring following a pressure release for each pressure relief device subject to the provisions in  $\S$   $\S$  63.165(a) and (b) of this subpart. The results shall include:

(1) The background level measured during each compliance test.

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(2) The maximum instrument reading measured at each piece of equipment during each compliance test.

(g) The owner or operator shall maintain records of the information specified in <u>paragraphs (g)(1)</u> through (g)(3) of this section for closed-vent systems and control devices subject to the provisions of § 63.172 of this subpart. The records specified in <u>paragraph (g)(1)</u> of this section shall be retained for the life of the equipment. The records specified in <u>paragraphs (g)(2)</u> and (g)(3) of this section shall be retained for 2 years.

(1) The design specifications and performance demonstrations specified in <u>paragraphs (g)(1)(i)</u> through (g)(1)(iv) of this section.

(i) Detailed schematics, design specifications of the control device, and piping and instrumentation diagrams.

(ii) The dates and descriptions of any changes in the design specifications.

(iii) Except as specified in paragraph (a) of § 63.108, the flare design (*i.e.*, steam-assisted, air-assisted, or non-assisted) and the results of the compliance demonstration required by § 63.11(b).

(iv) A description of the parameter or parameters monitored, as required in <u>§ 63.172(e) of this subpart</u>, to ensure that control devices are operated and maintained in conformance with their design and an explanation of why that parameter (or parameters) was selected for the monitoring.

(2) Records of operation of closed-vent systems and control devices, as specified in <u>paragraphs (g)(2)(i)</u> through (g)(2)(iii) of this section.

(i) Except as specified in paragraph (a) of § 63.108, dates and durations when the closed-vent systems and control devices required in §§ 63.163 through 63.166, and § 63.170 are not operated as designed as indicated by the monitored parameters, including periods when a flare pilot light system does not have a flame.

(ii) Dates and durations during which the monitoring system or monitoring device is inoperative.

(iii) Dates and durations of start-ups and shutdowns of control devices required in  $\frac{\$\$ 63.163}{\$$  through  $\underline{63.166}$ , and  $\underline{\$ 63.170}$  of this subpart.

(3) Records of inspections of closed-vent systems subject to the provisions of § 63.172, as specified in paragraphs (g)(3)(i) through (iii) of this section.

(i) For each inspection conducted in accordance with the provisions of  $\S 63.172(f)(1)$  or (f)(2) of this subpart during which no leaks were detected, a record that the inspection was performed, the date of the inspection, and a statement that no leaks were detected.

(ii) For each inspection conducted in accordance with the provisions of  $\S$  63.172(f)(1) or (f)(2) of this subpart during which leaks were detected, the information specified in paragraph (d) of this section shall be recorded.

(iii) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in paragraphs (g)(3)(i) and (ii) of this section. For each flow event from a bypass line subject to the requirements in § 63.172(i), the owner or operator must maintain records sufficient to determine whether or not the detected flow included flow requiring control. For each flow event from a bypass line requiring control that is released either directly to the atmosphere or to a control device not meeting the requirements in this subpart, the owner or operator must include an estimate of the volume of gas, the concentration of organic HAP in the gas and the resulting emissions of organic HAP that bypassed the control device using process knowledge and engineering estimates.

(h) Each owner or operator of a process unit subject to the requirements of  $\frac{\$\$ 63.175}{100}$  and  $\frac{63.176}{100}$  of this subpart shall maintain the records specified in paragraphs (h)(1) through (h)(9) of this section for the period of the quality improvement program for the process unit.

(1) For owners or operators who elect to use a reasonable further progress quality improvement program, as specified in  $\S$  <u>63.175(d) of this subpart</u>:

(i) All data required in § 63.175(d)(2) of this subpart.

(ii) The percent leaking valves observed each quarter and the rolling average percent reduction observed in each quarter.

(iii) The beginning and ending dates while meeting the requirements of  $\S$  63.175(d) of this subpart.

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(2) For owners or operators who elect to use a quality improvement program of technology review and improvement, as specified in  $\S$  63.175(e) of this subpart:

(i) All data required in § 63.175(e)(2) of this subpart.

(ii) The percent leaking valves observed each quarter.

(iii) Documentation of all inspections conducted under the requirements of  $\frac{63.175(e)(4)}{63.175(e)(4)}$  of this subpart, and any recommendations for design or specification changes to reduce leak frequency.

(iv) The beginning and ending dates while meeting the requirements of § 63.175(e) of this subpart.

(3) For owners or operators subject to the requirements of the pump quality improvement program as specified in  $\S$  63.176 of this subpart:

(i) All data required in § 63.176(d)(2) of this subpart.

(ii) The rolling average percent leaking pumps.

(iii) Documentation of all inspections conducted under the requirements of  $\frac{63.176(d)(4)}{63.176(d)(4)}$  of this subpart, and any recommendations for design or specification changes to reduce leak frequency.

(iv) The beginning and ending dates while meeting the requirements of § 63.176(d) of this subpart.

(4) If a leak is not repaired within 15 calendar days after discovery of the leak, the reason for the delay and the expected date of successful repair.

(5) Records of all analyses required in  $\frac{\$\$ 63.175(e)}{\$}$  and  $\frac{63.176(d)}{\$}$  of this subpart. The records will include the following:

(i) A list identifying areas associated with poorer than average performance and the associated service characteristics of the stream, the operating conditions and maintenance practices.

(ii) The reasons for rejecting specific candidate superior emission performing valve or pump technology from performance trials.

(iii) The list of candidate superior emission performing valve or pump technologies, and documentation of the performance trial program items required under  $\frac{\$\$ 63.175(e)(6)(iii)}{\$}$  and  $\frac{63.176(d)(6)(iii)}{\$}$  of this subpart.

(iv) The beginning date and duration of performance trials of each candidate superior emission performing technology.

(6) All records documenting the quality assurance program for valves or pumps as specified in <u>§§</u> <u>63.175(e)(7)</u> and <u>63.176(d)(7) of this subpart</u>.

(7) Records indicating that all values or pumps replaced or modified during the period of the quality improvement program are in compliance with the quality assurance requirements in  $\frac{63.175(e)(7)}{2}$  and  $\frac{63.175(e)$ 

(8) Records documenting compliance with the 20 percent or greater annual replacement rate for pumps as specified in § 63.176(d)(8) of this subpart.

(9) Information and data to show the corporation has fewer than 100 employees, including employees providing professional and technical contracted services.

(i) The owner or operator of equipment in heavy liquid service shall comply with the requirements of either <u>paragraph</u> (i)(1) or (i)(2) of this section, as provided in <u>paragraph</u> (i)(3) of this section.

(1) Retain information, data, and analyses used to determine that a piece of equipment is in heavy liquid service.

(2) When requested by the Administrator, demonstrate that the piece of equipment or process is in heavy liquid service.

(3) A determination or demonstration that a piece of equipment or process is in heavy liquid service shall include an analysis or demonstration that the process fluids do not meet the definition of "in light liquid service." Examples of information that could document this include, but are not limited to, records of chemicals purchased for the process, analyses of process stream composition, engineering calculations, or process knowledge.

(j) Identification, either by list, location (area or group) of equipment in organic HAP service less than 300 hours per year within a process unit subject to the provisions of this subpart under  $\frac{63.160}{5.160}$  of this subpart.

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(k) Owners and operators choosing to comply with the requirements of  $\S$  <u>63.179 of this subpart</u> shall maintain the following records:

(1) Identification of the process unit(s) and the organic HAP's they handle.

(2) A schematic of the process unit, enclosure, and closed-vent system.

(3) A description of the system used to create a negative pressure in the enclosure to ensure that all emissions are routed to the control device.

(1) For fenceline monitoring systems subject to  $\frac{63.184}{10}$ , each owner or operator must keep the records specified in <u>paragraphs (1)(1)</u> through (11) of this section.

(1) Coordinates of all passive tube and canister monitors, including co-located samplers and field blanks, and if applicable, the meteorological station. The owner or operator shall determine the coordinates using an instrument with an accuracy of at least 3 meters. The coordinates shall be in decimal degrees with at least five decimal places.

(2) The start and stop times and dates for each sample, as well as the tube or canister identifying information.

(3) Sampling period average temperature and barometric pressure measurements.

(4) For each outlier determined in accordance with <u>Section 9.2</u> of Method 325A of <u>appendix A of this part</u> the sampler location of and the concentration of the outlier and the evidence used to conclude that the result is an outlier. The evidence must include documentation of accidental contamination by the sample handler. High sample results attributed to unknown causes are not outliers if there is no evidence of sample contamination and the sample does not meet the requirements in <u>Section 9.2</u> of Method 325A of <u>appendix A of this part</u>.

(5) For samples that will be adjusted for offsite impacts, the location of and the concentration measured simultaneously by the additional sampler(s), and the perimeter samplers to which it applies.

(6) Individual sample results, the calculated  $\Delta c$  for each monitored compound for each sampling period and the two samples used to determine it, whether correction for offsite impacts was used, and the annual average  $\Delta c$  for each monitored compound calculated after each sampling period.

(7) Method detection limit for each sample, including co-located samples and blanks.

(8) Documentation of the root cause analysis and any resulting corrective action taken each time an action level is exceeded, including the dates the root cause analysis was initiated and the resulting correction action(s) were taken. If real-time sampling techniques are required under § 63.184(e)(3)(B), the location of the real-time monitors for each 48-hour period.

(9) Any corrective action plan developed under  $\frac{\& 63.184(f)}{\& 63.184(f)}$ .

(10) Other records as required by Methods 325A, 325B, and 327 of appendix A of this part.

(11) If monitoring is conducted using canisters in accordance with  $\S$  <u>63.184(b)</u>, if a near-field source correction is used as provided in  $\S$  <u>63.184(g)</u>, or if an alternative test method is used that provides time-resolved measurements, records of hourly meteorological data, including temperature, barometric pressure, wind speed and wind direction, calculated daily unit vector wind direction and daily sigma theta, and other records specified in the site-specific monitoring plan.

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48177</u>, Sept. 20, 1994; <u>60 FR 18030</u>, Apr. 10, 1995; <u>61 FR 31441</u>, June 20, 1996; <u>62 FR 2792</u>, Jan. 17, 1997; <u>64 FR 20198</u>, Apr. 26, 1999; <u>68 FR 37344</u>, June 23, 2003; <u>89 FR 43225</u>, May 16, 2024]

#### § 63.182 Reporting requirements.

(a) Each owner or operator of a source subject to this subpart shall submit the reports listed in <u>paragraphs</u> (a)(1) through (a)(5) of this section. Owners or operators requesting an extension of compliance shall also submit the report listed in <u>paragraph (a)(6)</u> of this section.

- (1) An Initial Notification described in paragraph (b) of this section, and
- (2) A Notification of Compliance Status described in paragraph (c) of this section,
- (3) Periodic Reports described in paragraph (d) of this section,
- (4) Fenceline Monitoring Reports described in paragraph (e) of this section, and

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(5) [Reserved]

(6) Pursuant to section 112(i)(3)(B) of the Act, an owner or operator may request an extension allowing an existing source up to 1 additional year beyond the compliance date specified in the subpart that references this subpart.

(i) For purposes of this subpart, a request for an extension shall be submitted to the operating permit authority as part of the operating permit application. If the State in which the source is located does not have an approved operating permit program, a request for an extension shall be submitted to the Administrator as a separate submittal. The dates specified in  $\S$  <u>63.6(i)</u> of <u>subpart A of this part</u> for submittal of requests for extensions shall not apply to sources subject to this subpart.

(ii) A request for an extension of compliance must include the data described in  $\S$  <u>63.6(i)(6)(i) (A)</u>, <u>(B)</u>, and <u>(D)</u> of <u>subpart A</u> <u>of this part</u>.

(iii) The requirements in  $\S$  63.6(i)(8) through (i)(14) of subpart A of this part will govern the review and approval of requests for extensions of compliance with this subpart.

(b) Each owner or operator of an existing or new source subject to the provisions of this subpart shall submit a written Initial Notification to the Administrator, containing the information described in paragraph (b)(1), according to the schedule in paragraph (b)(2) of this section. The Initial Notification provisions in § 63.9(b)(1) through (b)(3) of subpart A of this part shall not apply to owners or operators of sources subject to this subpart.

(1) The Initial Notification shall include the following information:

(i) The name and address of the owner or operator;

(ii) The address (physical location) of the affected source;

(iii) An identification of the chemical manufacturing processes subject to this subpart; and

(iv) A statement of whether the source can achieve compliance by the applicable compliance date specified in the subpart in <u>40 CFR part 63</u> that references this subpart.

(2) The Initial Notification shall be submitted according to the schedule in paragraph (b)(2)(i), (b)(2)(ii), or (b)(2)(iii) of this section, as applicable.

(i) For an existing source, the Initial Notification shall be submitted within 120 calendar days after the date of promulgation or no later than 120 calendar days after the source becomes subject to this subpart, whichever is later.

(ii) For a new source that has an initial start-up 90 days after the date of promulgation of this subpart or later, the application for approval of construction or reconstruction required by  $\S 63.5(d)$  of subpart A of this part shall be submitted in lieu of the Initial Notification. The application shall be submitted as soon as practicable before the construction or reconstruction is planned to commence (but it need not be sooner than 90 days after the date of promulgation of the subpart that references this subpart). For a new source that reclassifies to major source status after January 19, 2021 and greater than 90 days after the initial start-up, the source shall submit the initial notification required by  $\S 63.9(b)$  no later than 120 days after the source becomes subject to this subpart.

(iii) For a new source that has an initial start-up prior to 90 days after the date of promulgation of the applicable subpart, the Initial Notification shall be submitted within 90 days after the date of promulgation of the subpart that references this subpart, or no later than 120 calendar days after the source becomes subject to this subpart, whichever is later.

(c) Each owner or operator of a source subject to this subpart shall submit a Notification of Compliance Status within 90 days after the compliance dates specified in the subpart in this part 63 that references this subpart, except as provided in <u>paragraph</u> (c)(4) of this section. The owner or operator shall also submit a supplement to the Notification of Compliance Status as specified in <u>paragraphs</u> (c)(5) and (6) of this section, if applicable.

(1) The notification shall provide the information listed in <u>paragraphs (c)(1)(i)</u> through (c)(1)(iv) of this section for each process unit subject to the requirements of  $\S$  63.163 through  $\S$  63.174 of this subpart.

(i) Process unit identification.

(ii) Number of each equipment type (e.g., valves, pumps) excluding equipment in vacuum service.

(iii) Method of compliance with the standard (for example, "monthly leak detection and repair" or "equipped with dual mechanical seals").

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(iv) Planned schedule for each phase of the requirements in  $\S$  63.163 and  $\S$  63.168 of this subpart.

(2) The notification shall provide the information listed in <u>paragraphs (c)(2)(i)</u> and <u>(c)(2)(ii)</u> of this section for each process unit subject to the requirements of  $\S$  63.178(b) of this subpart.

(i) Batch products or product codes subject to the provisions of this subpart, and

(ii) Planned schedule for pressure testing when equipment is configured for production of products subject to the provisions of this subpart.

(3) The notification shall provide the information listed in <u>paragraphs (c)(3)(i)</u> and <u>(c)(3)(ii)</u> of this section for each process unit subject to the requirements in § 63.179 of this subpart.

(i) Process unit identification.

(ii) A description of the system used to create a negative pressure in the enclosure and the control device used to comply with the requirements of  $\frac{63.172 \text{ of this subpart}}{1000 \text{ subpart}}$ .

(4) For existing sources subject to subpart F of this part, the Notification of Compliance Status shall be submitted for the group of process units with the earliest compliance date specified in  $\frac{63.100(k)}{50.100(k)}$  of subpart F of this part, by no later than 90 days after the compliance date for that group. The Notification of Compliance Status for each subsequent group shall be submitted as part of the first periodic report that is due not less than 90 days after the compliance date for that group.

(5) For pressure relief devices subject to the pressure release management work practice standards in  $\S$  <u>63.165(e)</u>, owners and operators must also submit the information listed in <u>paragraphs (c)(5)(i)</u> and <u>(ii)</u> of this section in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date for pressure relief device monitoring.

(i) A description of the monitoring system to be implemented, including the relief devices and process parameters to be monitored, and a description of the alarms or other methods by which operators will be notified of a pressure release.

(ii) A description of the prevention measures to be implemented for each affected pressure relief device.

(6) For equipment that are in ethylene oxide service, as defined in  $\S 63.101$ , owners and operators must also submit the information in this paragraph in a supplement to the Notification of Compliance Status within 150 days after the first applicable compliance date. The supplement to the Notification of Compliance Status must identify all equipment that are in ethylene oxide service, and include the percent ethylene oxide content of the process fluid and the method used to determine it.

(d) The owner or operator of a source subject to this subpart shall submit Periodic Reports. On and after July 15, 2027 or once the reporting template for this subpart has been available on the CEDRI website for 1 year, whichever date is later, owners and operators must submit all subsequent reports following the procedure specified in § 63.9(k), except any medium submitted through mail must be sent to the attention of the Hazardous Organic Chemical Manufacturing Sector Lead. Owners and operators must use the appropriate electronic report template on the CEDRI website (<u>https://www.epa.gov/electronic-reporting-air-emissions/cedri</u>) for this subpart. The date report templates become available will be listed on the CEDRI website. Unless the Administrator or delegated state agency or other authority has approved a different schedule for submission of reports under § 63.9(i) and § 63.10(a), the report must be submitted by the deadline specified in this subpart, regardless of the method in which the report is submitted. All Periodic Reports must include the following general information: company name, address (including county), and beginning and ending dates of the reporting period.

(1) A report containing the information in <u>paragraphs (d)(2), (d)(3)</u>, and (d)(4) of this section shall be submitted semiannually starting 6 months after the Notification of Compliance Status, as required in <u>paragraph (c)</u> of this section. The first periodic report shall cover the first 6 months after the compliance date specified in § 63.100(k)(3) of subpart F. Each subsequent periodic report shall cover the 6 month period following the preceding period.

(2) For each process unit complying with the provisions of  $\S 63.163$  through  $\S 63.174$ , the summary information listed in paragraphs (d)(2)(i) through (xix) of this paragraph for each monitoring period during the 6-month period.

(i) The number of values for which leaks were detected as described in  $\S$  63.168(b) of this subpart, the percent leakers, and the total number of values monitored;

(ii) The number of valves for which leaks were not repaired as required in  $\S$  63.168(f) of this subpart, identifying the number of those that are determined nonrepairable;

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(iii) The number of pumps for which leaks were detected as described in  $\S$  63.163(b) of this subpart, the percent leakers, and the total number of pumps monitored;

(iv) The number of pumps for which leaks were not repaired as required in  $\S$  63.163(c) of this subpart;

(v) The number of compressors for which leaks were detected as described in  $\S$  63.164(f) of this subpart;

(vi) The number of compressors for which leaks were not repaired as required in § 63.164(g) of this subpart;

(vii) The number of agitators for which leaks were detected as described in § 63.173(a) and (b) of this subpart;

(viii) The number of agitators for which leaks were not repaired as required in § 63.173(c) of this subpart;

(ix) The number of connectors for which leaks were detected as described in  $\S$  63.174(a) of this subpart, the percent of connectors leaking, and the total number of connectors monitored;

(x) [Reserved]

(xi) The number of connectors for which leaks were not repaired as required in  $\S$  63.174(d) of this subpart, identifying the number of those that are determined nonrepairable;

(xii) [Reserved]

(xiii) The facts that explain any delay of repairs and, where appropriate, why a process unit shutdown was technically infeasible.

(xiv) The results of all monitoring to show compliance with  $\frac{\$\$ 63.164(i)}{63.165(a)}$ , and  $\frac{63.172(f)}{63.162(f)}$  of this subpart conducted within the semiannual reporting period.

(xv) If applicable, the initiation of a monthly monitoring program under  $\frac{63.168(d)(1)(i)}{63.168(d)(1)(i)}$  of this subpart, or a quality improvement program under either  $\frac{68}{63.175}$  or  $\frac{63.176}{63.176}$  of this subpart.

(xvi) If applicable, notification of a change in connector monitoring alternatives as described in  $\S$  63.174(c)(1) of this subpart.

(xvii) If applicable, the compliance option that has been selected under  $\frac{63.172(n)}{2}$ .

(xviii) Compliance reports for pressure relief devices subject to the requirements  $\S 63.165(e)$  must include the information specified in paragraphs (d)(2)(xviii)(A) through (C) of this section.

(A) For pressure relief devices in organic HAP gas or vapor service, pursuant to  $\frac{63.165(e)(1)}{10}$ , report the instrument readings and dates for all readings of 500 ppm or greater.

(B) For pressure relief devices in organic HAP gas or vapor service subject to  $\S 63.165(e)(2)$ , report the instrument readings and dates of instrument monitoring conducted.

(C) For pressure relief devices in organic HAP service subject to  $\S 63.165(e)(3)$ , report each pressure release to the atmosphere, including pressure relief device identification name or number, the start date, start time, and duration (in minutes) of the pressure release; an estimate of the mass quantity in pounds of each organic HAP released; the results of any root cause analysis and corrective action analysis completed during the reporting period, including the corrective actions implemented during the reporting period; and, if applicable, the implementation schedule for planned corrective actions to be implemented subsequent to the reporting period.

(xix) For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(10), the owner or operator must comply with this paragraph in addition to the requirements in paragraphs (d)(2)(i) through (d)(2)(xviii) of this section. For bypass lines subject to the requirements in § 63.172(j), the Periodic Report must include the start date, start time, duration in hours, estimate of the volume of gas in standard cubic feet, the concentration of organic HAP in the gas in parts per million by volume and the resulting mass emissions of organic HAP in pounds that bypass a control device. For periods when the flow indicator is not operating, report the start date, start time, and duration in hours.

(3) For owners or operators electing to meet the requirements of  $\frac{63.178(b)}{50.178(b)}$  of this subpart, the report shall include the information listed in paragraphs (i) through (v) of this paragraph for each process unit.

(i) Batch product process equipment train identification;

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(ii) The number of pressure tests conducted;

(iii) The number of pressure tests where the equipment train failed the pressure test;

(iv) The facts that explain any delay of repairs; and

(v) The results of all monitoring to determine compliance with § 63.172(f) of this subpart.

(4) The information listed in <u>paragraph (c)</u> of this section for the Notification of Compliance Status for process units with later compliance dates. Any revisions to items reported in earlier Notification of Compliance Status, if the method of compliance has changed since the last report.

(e) For fenceline monitoring systems subject to  $\frac{63.184}{63.184}$ , each owner or operator must submit Fenceline Monitoring Reports on a quarterly basis using the appropriate electronic report template on the CEDRI website (<u>https://www.epa.gov/electronic-reporting-air-emissions/cedri</u>) for this subpart and following the procedure specified in  $\frac{63.9(k)}{63.9(k)}$ , except any medium submitted through mail must be sent to the attention of the Hazardous Organic Chemical Manufacturing Sector Lead. The first quarterly report must be submitted once the owner or operator has obtained 12 months of data. The first quarterly report must cover the period beginning on the compliance date that is specified in  $\frac{63.100(k)(12)}{12}$  and ending on March 31, June 30, September 30 or December 31, whichever date is the first date that occurs after the owner or operator has obtained 12 months of data (*i.e.*, the first quarterly report will contain between 12 and 15 months of data). Each subsequent quarterly report must cover one of the following reporting periods: Quarter 1 from January 1 through March 31; Quarter 2 from April 1 through June 30; Quarter 3 from July 1 through September 30; and Quarter 4 from October 1 through December 31. Each quarterly report must be electronically submitted no later than 45 calendar days following the end of the reporting period.

(1) Facility name and address (including the county).

(2) Year and reporting quarter (*i.e.*, Quarter 1, Quarter 2, Quarter 3, or Quarter 4).

(3) For each passive tube or canister monitor: The latitude and longitude location coordinates; the sampler name; and identification of the type of sampler (*i.e.*, regular monitor, extra monitor, duplicate, field blank, inactive). Coordinates must be in decimal degrees with at least five decimal places.

(4) The beginning and ending dates for each sampling period.

(5) Individual sample results for each monitored compound, reported in units of  $\mu g/m3$ , for each monitor for each sampling period that ends during the reporting period. Results below the method detection limit must be flagged as below the detection limit and reported at the method detection limit.

(6) Data flags for each outlier determined in accordance with <u>Section 9.2</u> of Method 325A of <u>appendix A of this part</u>. For each outlier, the owner or operator must submit the individual sample result of the outlier, as well as the evidence used to conclude that the result is an outlier. The evidence must include documentation of accidental contamination by the sample handler. High sample results attributed to unknown causes are not outliers if there is no evidence of sample contamination and the sample does not meet the requirements in <u>Section 9.2</u> of Method 325A of <u>appendix A of this part</u>.

(7) The concentration difference ( $\Delta c$ ) for each monitored compound for each sampling period and the annual average  $\Delta c$  for each monitored compound for each sampling period.

(8) Indication of whether the owner or operator was required to develop a corrective action plan under  $\frac{63.184(f)}{10}$ .

(9) Data flags for each monitor for each analyte that was skipped for the sampling period, if the owner or operator uses an alternative sampling frequency under  $\frac{63.184(a)(3)(iii)}{63.184(b)(2)(iii)}$  or  $\frac{63.184(b)(2)(iii)}{63.184(b)(2)(iii)}$ .

[<u>59 FR 19568</u>, Apr. 22, 1994, as amended at <u>59 FR 48178</u>, Sept. 20, 1994; <u>60 FR 18030</u>, Apr. 10, 1995; <u>60 FR 63631</u>, Dec. 12, 1995; <u>62 FR 2792</u>, Jan. 17, 1997; <u>85 FR 73888</u>, Nov. 19, 2020; <u>89 FR 43226</u>, May 16, 2024]

#### § 63.183 Implementation and enforcement.

(a) This subpart can be implemented and enforced by the U.S. EPA, or a delegated authority such as the applicable State, local, or Tribal agency. If the U.S. EPA Administrator has delegated authority to a State, local, or Tribal agency, then that agency, in addition to the U.S. EPA, has the authority to implement and enforce this subpart. Contact the applicable U.S. EPA Regional Office to find out if implementation and enforcement of this subpart is delegated to a State, local, or Tribal agency.

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(b) In delegating implementation and enforcement authority of this subpart to a State, local, or Tribal agency under <u>subpart E</u> <u>of this part</u>, the authorities contained in <u>paragraph (c)</u> of this section are retained by the Administrator of U.S. EPA and cannot be transferred to the State, local, or Tribal agency.

(c) The authorities that cannot be delegated to State, local, or Tribal agencies are as specified in <u>paragraphs</u> (c)(1) through (5) of this section.

(1) Approval of alternatives to the requirements in  $\frac{\$}{63.160}$ ,  $\frac{63.162}{63.162}$  through  $\frac{63.176}{63.178}$  through  $\frac{63.179}{63.179}$ . Follow the applicable procedures of  $\frac{\$}{63.177}$  to request an alternative means of emission limitation for batch processes and enclosed-vented process units. Where these standards reference another subpart, the cited provisions will be delegated according to the delegation provisions of the referenced subpart. Where these standards reference another subpart and modify the requirements, the requirements shall be modified as described in this subpart. Delegation of the modified requirements will also occur according to the delegation provisions of the referenced subpart.

(2) Approval of major alternatives to test methods under  $\S 63.7(e)(2)(ii)$  and (f), as defined in  $\S 63.90$ , and as required in this subpart.

(3) Approval of major alternatives to monitoring under  $\frac{63.8(f)}{1000}$ , as defined in  $\frac{63.90}{1000}$ , and as required in this subpart.

(4) Approval of major alternatives to recordkeeping and reporting under  $\frac{63.10(f)}{10}$ , as defined in  $\frac{63.90}{10}$ , and as required in this subpart.

(5) Approval of an alternative to any electronic reporting to the EPA required by this subpart.

[68 FR 37345, June 23, 2003, as amended at 89 FR 43228, May 16, 2024]

# § 63.184 Fenceline monitoring provisions.

For each source as defined in § 63.101, and for each source as defined in § 63.191, beginning no later than the compliance dates specified in § 63.100(k)(12), the owner or operator must conduct sampling along the facility property boundary and analyze the samples in accordance with <u>paragraphs (a)</u> through (i) of this section. Sampling of benzene, 1,3-butadiene, chloroprene, and ethylene dichloride must be conducted in accordance with <u>paragraph (a)</u> of this section. Sampling of ethylene oxide and vinyl chloride must be conducted in accordance with <u>paragraph (b)</u> of this section. <u>Paragraphs</u> (c) through (i) of this section apply for any compound required to be sampled.

(a) The owner or operator must conduct sampling along the facility property boundary and analyze the samples in accordance with Methods 325A and 325B of appendix A to this part and <u>paragraphs (a)(1)</u> through (3) of this section. The monitoring perimeter may be located inside the facility, away from the facility property boundary. However, the monitoring perimeter must encompass all potential sources of the target analyte(s) specified in <u>paragraph (a)(1)</u> of this section that are located within the facility's property boundary.

(1) The owner or operator must monitor the target analyte(s), as specified in <u>paragraphs (a)(1)(i)</u> through (iv) of this section. The owner or operator must follow the procedure in <u>Section 9.6</u> of Method 325B of appendix A to this part to determine the detection limit of benzene, 1,3-butadiene, chloroprene, and ethylene dichloride for each sampler used to collect samples and blanks.

(i) If an affected source uses, produces, stores, or emits benzene, the owner or operator must include benzene as a target analyte.

(ii) If an affected source uses, produces, stores, or emits 1,3-butadiene, the owner or operator must include 1,3-butadiene as a target analyte.

(iii) If an affected source uses, produces, stores, or emits chloroprene, the owner or operator must include chloroprene as a target analyte.

(iv) If an affected source uses, produces, stores, or emits ethylene dichloride, the owner or operator must include ethylene dichloride as a target analyte.

(2) The owner or operator must determine passive monitor locations in accordance with <u>Section 8.2</u> of Method 325A of appendix A to this part.

(i) As it pertains to this subpart, known sources of VOCs, as used in <u>Section 8.2.1.3</u> in Method 325A of appendix A to this part for siting passive monitors, means a wastewater treatment unit, process unit, or any emission source requiring control

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according to the requirements of this subpart, including marine vessel loading operations. For marine vessel loading operations, one passive monitor should be sited on the shoreline adjacent to the dock. For this subpart, an additional monitor is not required if the only emission sources within 50 meters of the monitoring boundary are equipment leak sources satisfying all of the conditions in paragraphs (a)(2)(i)(A) through (C) of this section. If a leak is found, it must be repaired no later than 15 calendar days after it is detected with no provisions for delay of repair. If a repair is not completed within 15 calendar days, the additional passive monitor specified in Section 8.2.1.3 in Method 325A of appendix A to this part must be used.

(A) The equipment leak sources in organic HAP service within 50 meters of the monitoring boundary are limited to valves, pumps, connectors, sampling connections, and open-ended lines. If compressors, pressure relief devices, or agitators in organic HAP service are present within 50 meters of the monitoring boundary, the additional passive monitoring location specified in <u>Section 8.2.1.3</u> in Method 325A of appendix A to this part must be used.

(B) All equipment leak sources in gas or light liquid service (and in organic HAP service), including valves, pumps, connectors, sampling connections and open-ended lines, must be monitored using Method 21 of appendix A-7 to <u>40 CFR part</u> <u>60</u> no less frequently than quarterly with no provisions for skip period monitoring, or according to the provisions of § <u>63.11(c)</u> Alternative Work practice for monitoring equipment for leaks. For the purpose of this provision, a leak is detected if the instrument reading equals or exceeds the applicable limits in <u>paragraphs (a)(2)(i)(B)(1)</u> through <u>(5)</u> of this section:

(1) For valves, pumps or connectors at an existing source, an instrument reading of 10,000 ppmv.

(2) For valves or connectors at a new source, an instrument reading of 500 ppmv.

(3) For pumps at a new source, an instrument reading of 2,000 ppmv.

(4) For sampling connections or open-ended lines, an instrument reading of 500 ppmv above background.

(5) For equipment monitored according to the Alternative Work practice for monitoring equipment for leaks, the leak definitions contained in  $\S$  63.11(c)(6)(i) through (iii).

(C) All equipment leak sources in organic HAP service, including sources in gas, light liquid and heavy liquid service, must be inspected using visual, audible, olfactory, or any other detection method at least monthly. A leak is detected if the inspection identifies a potential leak to the atmosphere or if there are indications of liquids dripping.

(ii) If there are 19 or fewer monitoring locations, the owner or operator must collect at least one co-located duplicate sample per sampling period and at least one field blank per sampling period. If there are 20 or more monitoring locations, the owner or operator must collect at least two co-located duplicate samples per sampling period and at least one field blank per sampling period. The co-located duplicates may be collected at any of the perimeter sampling.

(iii) Samplers are not required to be placed along internal roads, waterways, or other right of ways that may bisect the facility. If a facility is bounded by a waterway on one or more sides, the shoreline is considered the facility property boundary.

(3) The owner or operator must use a sampling period and sampling frequency as specified in <u>paragraphs</u> (a)(3)(i) through (iii) of this section.

(i) Sampling period. A 14-day sampling period must be used, unless a shorter sampling period is determined to be necessary under <u>paragraph (e)</u> or (g) of this section. A sampling period is defined as the period during which sampling tube is deployed at a specific sampling location with the diffusive sampling end cap in-place and does not include the time required to analyze the sample. For the purpose of this subpart, a 14-day sampling period must be no shorter than 13 calendar days and no longer than 15 calendar days, but the routine sampling period must be 14 calendar days.

(ii) *Base sampling frequency*. Except as provided in <u>paragraph (a)(3)(iii)</u> of this section, the frequency of sample collection must be once each contiguous 14-day sampling period, such that the beginning of the next 14-day sampling period begins immediately upon the completion of the previous 14-day sampling period.

(iii) Alternative sampling frequency for burden reduction. When an individual monitor consistently achieves results for a particular analyte at or below the level specified in paragraph (a)(4) of this section, the owner or operator may elect to use the applicable minimum sampling frequency specified in paragraphs (a)(3)(iii)(A) through (E) of this section for that monitoring site for that analyte. When calculating  $\Delta c$  for the monitoring period when using this alternative for burden reduction, use zero for the lowest sampling result for each monitoring period where one or more samples was not taken and/or analyzed for the analyte(s) that qualifies for this alternative sampling frequency. This alternative for burden reduction is determined on an analyte specific basis. If an owner or operator is not required to sample for a particular analyte for a particular monitoring site

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in accordance with this <u>paragraph (a)(3)(iii)</u>, the owner or operator must still sample for any other analytes required by <u>paragraph (a)(1)</u> of this section at the frequency specified in <u>paragraph (a)(3)(ii)</u> of this section, unless the other analyte(s) also qualifies for this alternative for burden reduction.

(A) For the analyte of interest, if every sample at a monitoring site is at or below the level specified in <u>paragraph (a)(4)</u> of this section for 2 years (52 consecutive samples), every other sampling period can be skipped for that analyte for that monitoring site, *i.e.*, sampling will occur approximately once per month.

(B) For the analyte of interest, if every sample at a monitoring site that is monitored at the frequency specified in paragraph (a)(3)(iii)(A) of this section is at or below the level specified in paragraph (a)(4) of this section for 2 years (*i.e.*, 26 consecutive "monthly" samples), five 14-day sampling periods can be skipped for that analyte for that monitoring site following each period of sampling, *i.e.*, sampling will occur approximately once per quarter.

(C) For the analyte of interest, if every sample at a monitoring site that is monitored at the frequency specified in <u>paragraph</u> (a)(3)(iii)(B) of this section is at or below the level specified in <u>paragraph (a)(4)</u> of this section for 2 years (*i.e.*, 8 consecutive quarterly samples), twelve 14-day sampling periods can be skipped for that analyte for that monitoring site following each period of sampling, *i.e.*, sampling will occur twice a year.

(D) For the analyte of interest, if every sample at a monitoring site that is monitored at the frequency specified in <u>paragraph</u> (a)(3)(iii)(C) of this section is at or below the level specified in <u>paragraph</u> (a)(4) of this section for 2 years (*i.e.*, 4 consecutive semiannual samples), only one sample per year is required for that analyte for that monitoring site. For yearly sampling, samples shall occur at least 10 months but no more than 14 months apart.

(E) If at any time a sample for a monitoring site that is monitored for the analyte at the frequency specified in paragraph (a)(3)(iii)(A) through (D) of this section returns a result for the analyte that is above the level specified in paragraph (a)(4) of this section, the sampling site must return to the original sampling requirements for the analyte of contiguous 14-day sampling periods with no skip periods for one quarter (six 14-day sampling periods). If every sample collected for the analyte during this quarter is at or below the level specified in paragraph (a)(4) of this section, the owner or operator may revert back to the reduced monitoring schedule applicable for that analyte for that monitoring site prior to the sample reading exceeding the level specified in paragraph (a)(4) of this section. If any sample collected for the analyte during this quarter is above the level specified in paragraph (a)(4) of this section, that monitoring site must return to the original sampling requirements for that analyte of contiguous 14-day sampling requirements can be used again for that analyte for that monitoring site must return to the original sampling requirements of paragraph (a)(3)(iii)(A) of this section are met again, *i.e.*, after 52 contiguous 14-day samples with no results above the level specified in paragraph (a)(4) of this section.

(4) To use the alternative sampling frequency outlined in <u>paragraph (a)(3)</u> of this section, an individual monitor must consistently achieve results for the analyte at or below the level specified in <u>paragraphs (a)(4)(i)</u> through <u>(iii)</u> of this section.

(i) For benzene, the results must be consistently at or below  $0.9 \ \mu g/m^3$ .

(ii) For 1,3-butadiene, the results must be consistently at or below 0.3  $\mu$ g/m<sup>3</sup>.

(iii) For ethylene dichloride, the results must be consistently at or below  $0.4 \ \mu g/m^3$ .

(b) The owner or operator must conduct sampling along the facility property boundary and analyze the samples in accordance with Method 327 of appendix A to this part and <u>paragraphs (b)(1)</u> through  $(\underline{3})$  of this section.

(1) The owner or operator must monitor the target analyte(s), as specified in <u>paragraphs (b)(1)(i)</u> and (ii) of this section.

(i) If an affected source uses, produces, stores, or emits ethylene oxide, the owner or operator must include ethylene oxide as a target analyte.

(ii) If an affected source uses, produces, stores, or emits vinyl chloride, the owner or operator must include vinyl chloride as a target analyte.

(2) The owner or operator must use a sampling period and sampling frequency as specified in <u>paragraphs (b)(2)(i)</u> and <u>(ii)</u> of this section.

(i) Sampling period. A 24-hour sampling period must be used, unless a shorter sampling period is determined to be necessary under <u>paragraph (e)</u> or (g) of this section. A sampling period is defined as the period during which the canister is deployed at

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a specific sampling location and actively sampling and does not include the time required to analyze the sample. For the purpose of this subpart, a 24-hour sampling period may be no shorter than 23 hours and no longer than 25 hours.

(ii) *Base sampling frequency*. Except as provided in <u>paragraph (b)(2)(iii)</u> of this section, the frequency of sample collection must be once every 5 calendar days, such that the beginning of each sampling period begins approximately 96 hours ( $\pm$  24 hours) from the end of the previous sample.

(iii) Alternative sampling frequency for burden reduction. This alternative is only applicable for the measurement of vinyl chloride from sites with a monitoring perimeter less than or equal to 5,000 meters. When an individual sampling point consistently achieves results at or below  $0.3 \ \mu g/m^3$ , the owner or operator may elect to use the applicable minimum sampling frequency specified in paragraphs (b)(2)(iii)(A) through (E) of this section for that sampling site for vinyl chloride. If ethylene oxide is a required analyte, the owner or operator must continue to monitor ethylene oxide at the frequency specified in paragraph (b)(2)(ii) of this section. When calculating  $\Delta c$  for the monitoring period when using this alternative for burden reduction, use zero for the lowest sampling result for each monitoring period where one or more samples was not taken for vinyl chloride.

(A) If every sample at a monitoring site is at or below  $0.3 \ \mu g/m^3$  for 2 years (52 consecutive samples), every other sampling period can be skipped for that sampling site, *i.e.*, sampling will occur approximately once per month.

(B) If every sample at a sampling site that is monitored at the frequency specified in <u>paragraph (b)(2)(iii)(A)</u> of this section is at or below 0.3  $\mu$ g/m<sup>3</sup> for 2 years (*i.e.*, 26 consecutive "monthly" samples), five 14-day sampling periods can be skipped for that sampling site following each period of sampling, *i.e.*, sampling will occur approximately once per quarter.

(C) If every sample at a sampling site that is monitored at the frequency specified in <u>paragraph (b)(2)(iii)(B)</u> of this section is at or below 0.3  $\mu$ g/m<sup>3</sup> for 2 years (*i.e.*, 8 consecutive quarterly samples), twelve 14-day sampling periods can be skipped for that sampling site following each period of sampling, *i.e.*, sampling will occur twice a year.

(D) If every sample at a sampling site that is monitored at the frequency specified in <u>paragraph (b)(2)(iii)(C)</u> of this section is at or below 0.3  $\mu$ g/m<sup>3</sup> for 2 years (*i.e.*, 4 consecutive semiannual samples), only one sample per year is required for that sampling site. For yearly sampling, samples shall occur at least 10 months but no more than 14 months apart.

(E) If at any time a sample for a sampling site that is monitored at the frequency specified in <u>paragraphs</u>

(b)(2)(iii)(A) through (E) of this section returns a result that is above  $0.3 \ \mu g/m^3$ , the sampling site must return to the original sampling requirements of sampling every 5 calendar days with no skip periods for one quarter (18 5-day sampling periods). If every sample collected during this quarter is at or below  $0.3 \ \mu g/m^3$ , the owner or operator may revert back to the reduced monitoring schedule applicable for that sampling site prior to the sample reading exceeding  $0.3 \ \mu g/m^3$ . If any sample collected during this quarter is above  $0.3 \ \mu g/m^3$ , that sampling site must return to the original sampling requirements of sampling every 5 calendar days with no skip periods for a minimum of two years. The burden reduction requirements can be used again for that sampling site once the requirements of paragraph (b)(2)(ii)(A) of this section are met again, *i.e.*, after 146 consecutive samples with no results above  $0.3 \ \mu g/m^3$ .

(3) The owner or operator must determine canister sample locations in accordance with <u>paragraphs (b)(3)(i)</u> through (v) of this section.

(i) The monitoring perimeter must be located on or inside the facility property boundary. If the monitoring perimeter is located away from the facility property boundary, the monitoring perimeter must encompass all potential sources of the target analyte(s) specified in paragraph (b)(1) of this section that are located within the facility's property boundary. If the site contains process units that are disconnected (*i.e.*, one or more process areas are not within the boundary of the main facility), the owner or operator must follow the requirements in paragraph (b)(3)(v) of this section. Canisters are not required to be placed along internal roads, waterways, or other right of ways that may bisect the facility. If a facility is bounded by a waterway on one or more sides, the shoreline is considered the facility property boundary.

(ii) The owner or operator must place 8 canisters around the monitoring perimeter during each sampling period.

(iii) To determine sampling locations, measure the length of the monitoring perimeter.

(A) Locate the point on the monitoring perimeter that is closest to sources of the target analyte(s). If one of the target analytes is ethylene oxide, this point must be the point on the monitoring perimeter that is closest to the sources of ethylene oxide.

(B) If the monitoring perimeter is less than or equal to 5,000 meters, divide the monitoring perimeter into 8 evenly spaced sampling points, with one point located in accordance with the requirements of paragraph (b)(3)(iii)(A) of this section.

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(C) If the monitoring perimeter is greater than 5,000 meters, but less than or equal to 10,000 meters, divide the monitoring perimeter into 16 evenly spaced sampling points, with one point located in accordance with the requirements of paragraph (b)(3)(iii)(A) of this section.

(D) If the monitoring perimeter is greater than 10,000 meters, divide the monitoring perimeter into 24 evenly spaced sampling points, with one point located in accordance with the requirements of  $\frac{\text{paragraph}(b)(3)(\text{iii})(A)}{\text{paragraph}(b)(3)(\text{iii})(A)}$  of this section.

(iv) Place canisters on the monitoring perimeter at the sampling points as follows.

(A) If there are only 8 sampling points for the site, monitor each sampling point during each sampling period.

(B) If there are 16 sampling points for the site, number the sampling points consecutively along the monitoring perimeter. During the first sampling period, monitor the odd numbered sampling points. During the second sampling period, monitor the even numbered sampling points. Continue to alternate between the odd numbered and even numbered sampling points in subsequent sampling periods.

(C) If there are 24 sampling points for the site, number the sampling points consecutively along the monitoring perimeter. During the first sampling period, monitor every third sampling point starting with the first sampling point (*i.e.*, points 1, 4, 7, etc.). During the second sampling period, monitor every third sampling point starting with the second sampling point (*i.e.*, points 2, 5, 8, etc.). During the third sampling period, monitor every third sampling point starting with the second sampling point (*i.e.*, points 2, 5, 8, etc.). During the third sampling period, monitor every third sampling point starting with the third sampling point (*i.e.*, points 3, 6, 9, etc.). Continue to alternate between these placements for each subsequent sampling period (*i.e.*, the fourth sampling period will include every third sampling point starting with the first sampling point, the fifth sampling period will include every third sampling with the second sampling point, and so on).

(v) If the site consists of small areas disconnected from the main facility, additional monitors must be placed on these areas in accordance with <u>paragraphs (b)(3)(v)(A)</u> through (C) of this section. The monitoring perimeter for the disconnected area(s) must be located between the property boundary of the area and the process unit(s), such that the monitoring perimeter for the disconnected area encompasses all potential sources of the target analyte(s) specified in <u>paragraph (b)(1)</u> of this section.

(A) If the disconnected area is less than 50 acres, the owner or operator must sample at two locations each sampling period. One location must be placed in the expected prevailing wind direction for the sampling period, downwind of the main source of emissions of the target analyte(s). The other location must be located on the monitoring perimeter at 180 degrees from the first sample location.

(B) If the disconnected area is equal to or greater than 50 acres but less than or equal to 150 acres, the owner or operator must sample at four equally spaced locations. One sampling point must be located on the monitoring perimeter at the point that is closest to sources of the target analyte(s). If one of the target analytes is ethylene oxide, this point must be the point on the monitoring perimeter that is closest to the sources of ethylene oxide.

(C) If the disconnected area is greater than 150 acres, the sampling points for the disconnected area must be determined according to paragraphs (b)(3)(ii) through (iv) of this section.

(4) At least one co-located duplicate sample and at least one field blank must be collected per sampling period.

(5) The owner or operator must follow the procedures in Method 327 of appendix A to this part to determine the detection limit of the target analyte(s) and requirements for quality assurance samples.

(c) The owner or operator must collect and record meteorological data according to the applicable requirements in <u>paragraphs</u> (c)(1) through (3) of this section.

(1) If monitoring is conducted under <u>paragraph (b)</u> of this section, if a near-field source correction is used as provided in <u>paragraph (g)(2)</u> of this section, or if an alternative test method is used that provides time-resolved measurements, the owner or operator must use an on-site meteorological station in accordance with <u>Section 8.3</u> of Method 325A of appendix A to this part. Collect and record hourly average meteorological data, including temperature, barometric pressure, wind speed and wind direction and calculate daily unit vector wind direction and daily sigma theta.

(2) For cases other than those specified in <u>paragraph (c)(1)</u> of this section, the owner or operator must collect and record sampling period average temperature and barometric pressure using either an on-site meteorological station in accordance with <u>Section 8.3</u> of Method 325A of appendix A to this part or, alternatively, using data from a National Weather Service (NWS) meteorological station provided the NWS meteorological station is within 40 kilometers (25 miles) of the facility.

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(3) If an on-site meteorological station is used, the owner or operator must follow the calibration and standardization procedures for meteorological measurements in EPA-454/B-08-002 (incorporated by reference, see  $\frac{63.14}{10}$ ).

(d) Within 45 days of completion of each sampling period, the owner or operator must determine whether the results are above or below the action level for each measured compound as follows. If the owner or operator is required to monitor any small disconnected area(s) of the facility under paragraph (b)(3)(v) of this section, the procedure for determining whether the results are above or below the action level for each measured compound must be performed for the disconnected area(s) separately.

(1) The owner or operator must determine the facility impact on the concentration ( $\Delta c$ ) of each compound for each sampling period according to either paragraph (d)(1)(i) or (ii) of this section, as applicable.

(i) Except when near-field source correction is used as provided in paragraph (d)(1)(ii) of this section, the owner or operator must determine the highest and lowest sample results for each compound individually from the sample pool and calculate each compound's  $\Delta c$  as the difference in these concentrations. Co-located samples must be averaged together for the purposes of determining the concentration at a particular sampling location, and, if applicable, for determining  $\Delta c$ . The owner or operator must adhere to the following procedures when one or more samples for the sampling period are below the method detection limit for a particular compound:

(A) If the lowest detected value of a compound is below detection, the owner or operator must use zero as the lowest sample result when calculating  $\Delta c$ .

(B) If all sample results are below the method detection limit, the owner or operator must use the highest method detection limit for the sample set as the highest sample result and zero as the lowest sample result when calculating  $\Delta c$ .

(C) In the case of co-located samples, if one sample is above the method detection limit while the other sample is below the method detection limit, the owner or operator must use the method detection limit as the result for the sample that is below the method detection limit for purposes of averaging the results to determine the concentration at a particular sampling location, and, if applicable, for determining  $\Delta c$ .

(ii) When near-field source correction for a compound is used as provided in <u>paragraph (g)</u> of this section, the owner or operator must determine  $\Delta c$  using the calculation protocols outlined in <u>paragraph (d)(1)(i)</u> of this section, except as provided in this <u>paragraph (d)(1)(ii)</u>, and the additional requirements in <u>paragraph (g)(2)</u> of this section, as well as any additional requirements outlined in the approved site-specific monitoring plan. The  $\Delta c$  for the compound for the sampling period is equal to the higher of the values in <u>paragraphs (d)(1)(ii)(A)</u> and (<u>B)</u> of this section.

(A) The highest corrected sample result for the compound from a sampling location where near-field source correction for the compound is used during the sampling period.

(B) The difference in concentration between the highest sample result that was not corrected for a near-field source for the compound during the sampling period and the lowest sample result for the compound for the sampling period.

(2) The owner or operator must calculate the annual average  $\Delta c$  for each monitored compound as follows:

(i) For sampling conducted under <u>paragraph (a)</u> of this section, the annual average  $\Delta c$  for each compound is based on the average of the  $\Delta c$  values for the 26 most recent 14-day sampling periods. The owner or operator must update this annual average value after receiving the results of each subsequent 14-day sampling period.

(ii) For sampling conducted under <u>paragraph (b)</u> of this section, the annual average  $\Delta c$  for each compound is based on the average of the  $\Delta c$  values for the 73 most recent sampling periods. The owner or operator must update this annual average value after receiving the results of each subsequent sampling period.

(3) The action level for each compound is listed in <u>paragraphs (d)(3)(i)</u> through <u>(vi)</u> of this section. If the annual average  $\Delta c$  value for a compound is greater than the listed action level for the compound, the concentration is above the action level, and the owner or operator must conduct a root cause analysis and corrective action in accordance with <u>paragraph (e)</u> of this section.

(i) The action level for benzene is 9 micrograms per cubic meter  $(\mu g/m^3)$  on an annual average basis.

(ii) The action level for 1,3-butadiene is 3  $\mu$ g/m<sup>3</sup> on an annual average basis.

(iii) The action level for chloroprene is 0.8  $\mu$ g/m<sup>3</sup> on an annual average basis.

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(iv) The action level for ethylene oxide is  $0.2 \ \mu g/m^3$  on an annual average basis.

(v) The action level for vinyl chloride is 3  $\mu$ g/m<sup>3</sup> on an annual average basis.

(vi) The action level for ethylene dichloride is 4  $\mu$ g/m<sup>3</sup> on an annual average basis.

(e) Once any action level in <u>paragraph (d)(3)</u> of this section has been exceeded, the owner or operator must take the following actions to bring the annual average  $\Delta c$  back below the action level(s).

(1) Within 5 days of updating the annual average value as required in <u>paragraph (d)(2)</u> of this section and determining that any action level in <u>paragraph (d)(3)</u> of this section has been exceeded (*i.e.*, in no case longer than 50 days after completion of the sampling period), the owner or operator must initiate a root cause analysis to determine appropriate corrective action. A root cause analysis is an assessment conducted through a process of investigation to determine the primary underlying cause and all other contributing causes to an exceedance of an action level(s) set forth in <u>paragraph (d)(3)</u> of this section.

(i) The initial root cause analysis may include, but is not limited to:

(A) Leak inspection using Method 21 of appendix A-7 to <u>40 CFR part 60</u>, optical gas imaging, or handheld monitors.

(B) Visual inspection to determine the cause of the high emissions.

(C) Operator knowledge of process changes (e.g., a malfunction or release event).

(ii) If the initial root cause cannot be identified using the type of techniques described in <u>paragraph (e)(1)(i)</u> of this section, the owner or operator must employ more frequent sampling and analysis to determine the root cause of the exceedance.

(A) The owner or operator may first employ additional monitoring points and shorter sampling periods for Methods 325A and 325B of appendix A to this part for benzene, 1,3-butadiene, chloroprene, or ethylene dichloride or more frequent sampling with Method 327 of appendix A to this part for ethylene oxide or vinyl chloride to determine the root cause of the exceedance.

(B) If the owner or operator has not determined the root cause of the exceedance within 30 days of determining that the action level has been exceeded, the owner or operator must employ the appropriate real-time sampling techniques (*e.g.*, mobile gas chromatographs, optical spectroscopy instruments, sensors) to locate the cause of the exceedance. If the root cause is not identified after 48 hours, either the real-time monitor must be relocated or an additional real-time monitor must be added. Relocation or addition of extra real-time monitors must continue after each 48-hour period of nonidentification until the owner or operator cause of the exceedance.

(2) If the underlying primary and other contributing causes of the exceedance are deemed to be under the control of the owner or operator, the owner or operator must take appropriate corrective action as expeditiously as possible to bring annual average fenceline concentrations back below the action level(s) set forth in paragraph (d)(3) of this section. At a minimum, the corrective actions taken must address the underlying primary and other contributing cause(s) determined in the root cause analysis to prevent future exceedances from the same underlying cause(s).

(3) The root cause analysis must be completed and initial corrective actions taken no later than 45 days after determining there is an exceedance of an action level.

(4) Until the annual average  $\Delta c$  is below the action level again, following completion of the initial corrective action, the owner or operator must conduct a new root cause analysis according to this <u>paragraph (e)</u>, and if required, submit a corrective action plan under <u>paragraph (f)</u> of this section following any sampling period for which the sampling start time begins after the completion of the initial corrective actions and for which the  $\Delta c$  for the sampling period is greater than the level specified in <u>paragraphs (e)(4)(i)</u> through <u>(vi)</u> of this section for the compound(s) that initially exceeded the action level.

- (i) For benzene, a sampling period  $\Delta c$  of 9  $\mu g/m^3$ .
- (ii) For 1,3-butadiene, a sampling period  $\Delta c$  of 3  $\mu g/m^3$ .
- (iii) For chloroprene, a sampling period  $\Delta c$  of 0.8  $\mu$ g/m<sup>3</sup>.
- (iv) For ethylene dichloride, a sampling period  $\Delta c$  of 4  $\mu g/m^3$ .
- (v) For ethylene oxide, a sampling period  $\Delta c$  of 0.2  $\mu g/m^3$ .
- (vi) For vinyl chloride, a sampling period  $\Delta c$  of 3  $\mu g/m^3$ .

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(f) An owner or operator must develop a corrective action plan if the conditions in <u>paragraphs (f)(1), (2)</u>, or (3) of this section are met. The corrective action plan must describe the corrective action(s) completed to date, additional measures that the owner or operator proposes to employ to reduce annual average fenceline concentrations below the action level(s) set forth in <u>paragraph (d)(3)</u> of this section, and a schedule for completion of these measures. The corrective action plan does not need to be approved by the Administrator. However, if upon review, the Administrator disagrees with the additional measures outlined in the plan, the owner or operator must revise and resubmit the plan within 7 calendar days of receiving comments from the Administrator.

(1) If the compound that exceeded the action level was benzene, 1,3-butadiene, chloroprene, or ethylene dichloride, the owner or operator must develop a corrective action plan if, upon completion of the root cause analysis and initial corrective actions required in <u>paragraph (e)</u> of this section, the  $\Delta c$  value for the next sampling period, for which the sampling start time begins after the completion of the initial corrective actions, is greater than the level specified in <u>paragraphs</u> (f)(1)(i) through (iv) of this section for the compound(s) that initially exceeded the action level. The corrective action plan must include the implementation of real-time sampling techniques to locate the primary and other contributing causes of the exceedance. The owner or operator must submit the corrective action plan to the Administrator within 60 days after receiving the analytical results indicating that the  $\Delta c$  value for the sampling period following the completion of the initial corrective

action is greater than the level specified in <u>paragraphs (f)(1)(i)</u> through <u>(iv)</u> of this section.

(i) For benzene, a sampling period  $\Delta c$  of 9  $\mu g/m^3$ .

(ii) For 1,3-butadiene, a sampling period  $\Delta c$  of 3  $\mu g/m^3$ .

(iii) For chloroprene, a sampling period  $\Delta c$  of 0.8  $\mu$ g/m<sup>3</sup>.

(iv) For ethylene dichloride, a sampling period  $\Delta c$  of 4  $\mu g/m^3$ .

(2) If the compound that exceeded the action level was ethylene oxide or vinyl chloride, the owner or operator must develop a corrective action plan if, upon completion of the root cause analysis and initial corrective actions required in <u>paragraph (e)</u> of this section, the  $\Delta c$  value for any of the next three sampling periods, for which the sampling start time begins after the completion of the initial corrective actions, is greater than the level specified in <u>paragraphs (f)(2)(i)</u> and <u>(ii)</u> of this section for the compound(s) that initially exceeded the action level. The corrective action plan must include the implementation of real-time sampling techniques to locate the primary and other contributing causes of the exceedance. The owner or operator must submit the corrective action plan to the Administrator within 60 days after receiving the analytical results indicating that the  $\Delta c$  value for the sampling period following the completion of the initial corrective action is greater than the level specified in <u>paragraphs (f)(2)(i)</u> and <u>(ii)</u> of this section.

(i) For ethylene oxide, a sampling period  $\Delta c$  of 0.2  $\mu g/m^3$ .

(ii) For vinyl chloride, a sampling period  $\Delta c$  of 3  $\mu g/m^3$ .

(3) The owner or operator must develop a corrective action plan if complete implementation of all corrective measures identified in the root cause analysis required by <u>paragraph (e)</u> of this section will require more than 45 days. The owner or operator must submit the corrective action plan to the Administrator no later than 60 days following the completion of the root cause analysis required in <u>paragraph (e)</u> of this section.

(g) An owner or operator may request approval from the Administrator for a site-specific monitoring plan to account for offsite upwind sources according to the requirements in <u>paragraphs (g)(1)</u> through (4) of this section.

(1) The owner or operator must prepare and submit a site-specific monitoring plan and receive approval of the site-specific monitoring plan prior to using the near-field source alternative calculation for determining  $\Delta c$  provided in paragraph (g)(2) of this section. The site-specific monitoring plan must include, at a minimum, the elements specified in paragraphs (g)(1)(i) through (vi) of this section. The procedures in Section 12 of Method 325A of appendix A to this part are not required, but may be used, if applicable, when determining near-field source contributions.

(i) Identification of the near-field source or sources.

(ii) Location of the additional monitoring stations that will be used to determine the near-field source concentration contribution. The owner or operator must use additional monitoring stations to determine the near-field source contribution.

(iii) Identification of the fenceline monitoring locations impacted by the near-field source. If more than one near-field source is present, identify the near-field source or sources that are expected to contribute to the concentration at that monitoring location.

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(iv) A description of (including sample calculations illustrating) the planned data reduction; the treatment of invalid data, data below detection limits, and data collected during calm wind periods; and calculations to determine the near-field source concentration contribution for each monitoring location.

(v) A detailed description of the measurement technique, measurement location(s), the standard operating procedures, measurement frequency, recording frequency, measurement detection limit, and data quality indicators to ensure accuracy, precision, and validity of the data.

(vi) A detailed description of how data will be handled during periods of calm wind conditions (*i.e.*, less than 2 miles per hour).

(2) When an approved site-specific monitoring plan is used, the owner or operator must determine  $\Delta c$  for comparison with the action level according to <u>paragraph (d)</u> of this section. When determining the highest and lowest sample results for use in the  $\Delta c$  calculation, the concentration for any monitor that has been corrected using an approved site-specific monitoring plan will be corrected according to the procedures specified in <u>paragraphs (g)(2)(i)</u> and <u>(ii)</u> of this section.

(i) For each monitoring location corrected using the site-specific monitoring plan, the corrected fenceline concentration at that monitoring station will be equal to the fenceline concentration measured with Methods 325A and 325B or Method 327 of appendix A to this part minus the near-field source contributing concentration at the measurement location determined using the additional measurements and calculation procedures included in the site-specific monitoring plan.

(ii) If the fenceline concentration at the monitoring station is below the method detection limit for Methods 325A and 325B or Method 327 of appendix A to this part, no near-field source contribution can be subtracted from that monitoring station for that sampling period.

(3) The site-specific monitoring plan must be submitted and approved as described in <u>paragraphs (g)(3)(i)</u> through <u>(iv)</u> of this section.

(i) The site-specific monitoring plan must be submitted to the Administrator for approval.

 (ii) The site-specific monitoring plan must also be submitted to the following address: U.S. Environmental Protection Agency, Office of Air Quality Planning and Standards, Sector Policies and Programs Division, U.S. EPA Mailroom (E143-01), Attention: Hazardous Organic Chemical Manufacturing Sector Lead, 109 T.W. Alexander Drive, P.O. Box 12055, Research Triangle Park, NC 27711. Electronic copies in lieu of hard copies may also be submitted to <u>fencelineplan@epa.gov</u>.

(iii) The Administrator will approve or disapprove the plan in 90 days. The plan is considered approved if the Administrator either approves the plan in writing or fails to disapprove the plan in writing. The 90-day period begins when the Administrator receives the plan.

(iv) If the Administrator finds any deficiencies in the site-specific monitoring plan and disapproves the plan in writing, the owner or operator may revise and resubmit the site-specific monitoring plan following the requirements in <u>paragraphs</u> (g)(3)(i) and (ii) of this section. The 90-day period starts over with the resubmission of the revised monitoring plan.

(4) The approval by the Administrator of a site-specific monitoring plan will be based on the completeness, accuracy and reasonableness of the request for a site-specific monitoring plan. Factors that the Administrator will consider in reviewing the request for a site-specific monitoring plan include, but are not limited to, those described in <u>paragraphs</u> (g)(4)(i) through (v) of this section.

(i) The identification of the near-field source or sources and evidence of how the sources impact the fenceline concentrations.

(ii) The location(s) selected for additional monitoring to determine the near-field source concentration contribution.

(iii) The identification of the fenceline monitoring locations impacted by the near-field source or sources.

(iv) The appropriateness of the planned data reduction and calculations to determine the near-field source concentration contribution for each monitoring location, including the handling of invalid data, data below the detection limit, and data during calm periods.

(v) The adequacy of the description of and rationale for the measurement technique, measurement location(s), the standard operation procedure, measurement frequency, recording frequency, measurement detection limit, and data quality indicators to ensure accuracy, precision, and validity of the data.

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(h) The owner or operator must comply with the applicable recordkeeping and reporting requirements in  $\frac{\$\$}{63.181}$  and  $\frac{63.182}{63.182}$ .

(i) As outlined in  $\frac{63.7(f)}{10}$ , the owner or operator may submit a request for an alternative test method. At a minimum, the request must follow the requirements outlined in paragraphs (i)(1) through (7) of this section.

(1) The alternative method may be used in lieu of all or a partial number of passive samplers required in Method 325A of appendix A to this part or the canister sampling locations required under <u>paragraph (b)</u> of this section.

(2) The alternative method must be validated according to Method 301 in appendix A to this part or contain performancebased procedures and indicators to ensure self-validation.

(3) The method detection limit must nominally be at least one-third of the action level for the compound(s) that will be monitored with the alternative method. The alternate test method must describe the procedures used to provide field verification of the detection limit.

(4) If the alternative test method will be used to replace some or all passive samplers required under <u>paragraph (a)</u> of this section, the spatial coverage must be equal to or better than the spatial coverage provided in Method 325A of appendix A to this part. If the alternative test method will be used to replace some or all canisters required under <u>paragraph (b)</u> of this section, the spatial coverage must be equal to or better than the spatial coverage provided under <u>paragraph (b)</u> of this section, the spatial coverage must be equal to or better than the spatial coverage provided under <u>paragraph (b)</u> of this section.

(i) For path average concentration open-path instruments, the physical path length of the measurement must be no more than a passive sample footprint (the spacing that would be provided by the sorbent traps when following Method 325A of appendix A to this part) or canister sample footprint, as applicable. For example, if Method 325A requires spacing monitors A and B 610 meters (2,000 feet) apart, then the physical path length limit for the measurement at that portion of the fenceline must be no more than 610 meters (2,000 feet).

(ii) For range resolved open-path instrument or approach, the instrument or approach must be able to resolve an average concentration over each passive sampler footprint or canister sample footprint within the path length of the instrument.

(iii) The extra samplers required in Sections 8.2.1.3 of Method 325A of appendix A to this part may be omitted when they fall within the path length of an open-path instrument.

(5) At a minimum, non-integrating alternative test methods must provide a minimum of one cycle of operation (sampling, analyzing, and data recording) for each successive 15-minute period.

(6) For alternative test methods capable of real time measurements (less than a 5 minute sampling and analysis cycle), the alternative test method may allow for elimination of data points corresponding to outside emission sources for purpose of calculation of the high point for the two week average. The alternative test method approach must have wind speed, direction and stability class of the same time resolution and within the footprint of the instrument.

(7) For purposes of averaging data points to determine the  $\Delta c$  for the individual sampling period, all results measured under the method detection limit must use the method detection limit. For purposes of averaging data points for the individual sampling period low sample result, all results measured under the method detection limit must use zero.

#### [89 FR 43228, May 16, 2024]

#### Table 1 to Subpart H of Part 63—Batch Processes

[Monitoring frequency for equipment other than connectors]					
Operating time	Equivalent continuous process monitoring frequency time in use				
(% of year)	Monthly	Quarterly	Semiannually		
0 to <25	Quarterly	Annually	Annually.		
25 to <50	Quarterly	Semiannually	Annually.		
50 to <75	Bimonthly	Three times	Semiannually.		
75 to 100	Monthly	Quarterly	Semiannually.		

[89 FR 43234, May 16, 2024]

# Table 2 to Subpart H of Part 63—Surge Control Vessels and Bottoms Receivers at Existing Sources

# National Emission Standards for Organic Hazardous Air Pollutants for Equipment Leaks

Vessel capacity (cubic meters)	Vapor pressure <sup>1</sup> (kilopascals)
$75 \le$ capacity $<151$	≥13.1
151 ≤ capacity	<sup>a</sup> ≥5.2
<sup>1</sup> Maximum true vapor pressure of total organic HA	P at operating temperature as defined in subpart G of this part.

[<u>89 FR 43234</u>, May 16, 2024]

#### Table 3 to Subpart H of Part 63—Surge Control Vessels and Bottoms Receivers at New Sources

Vessel capacity (cubic meters)	Vapor pressure <sup>1</sup> (kilopascals)
$38 \le$ capacity <151	≥13.1
$151 \le \text{capacity}$	≥0.7

<sup>1</sup> Maximum true vapor pressure of total organic HAP at operating temperature as defined in subpart G of this part.

[89 FR 43234, May 16, 2024]

# Table 4 to Subpart H of Part 63—Applicable 40 CFR Part 63 General Provisions

40 CFR part 63, subpart A, provisions applicable to subpart H			
$\{$ 63.1(a)(1), (a)(2), (a)(3), (a)(13), (a)(14), (b)(2) and (c)(4).			
§ 63.2.			
§ 63.5(a)(1), (a)(2), (b), (d)(1)(ii), (d)(4), (e), (f)(1) and (f)(2).			
$\{$ 63.6(a), (b)(3), (c)(5), (i)(1), (i)(2), (i)(4)(i)(A), (i)(5) through (i)(14), (i)(16) and (j).			
§ 63.9(a)(2), (b)(4)(i), <sup>a</sup> (b)(4)(ii), (b)(4)(iii), (b)(5), <sup>a</sup> (c), (d), (j) and (k).			
§ 63.10(d)(4).			
§ 63.11 (c), (d), and (e).			
§ 63.12(b).			
<sup>a</sup> The notifications specified in $\frac{63.9(b)(4)(i)}{10}$ and $\frac{(b)(5)}{10}$ shall be submitted at the times specified in $\frac{40 \text{ CFR part } 65}{10}$ .			

[89 FR 43234, May 16, 2024]

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# Subpart ZZZZ—National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

Source:

<u>69 FR 33506</u>, June 15, 2004, unless otherwise noted.

#### What This Subpart Covers

#### § 63.6580 What is the purpose of subpart ZZZZ?

Subpart ZZZZ establishes national emission limitations and operating limitations for hazardous air pollutants (HAP) emitted from stationary reciprocating internal combustion engines (RICE) located at major and area sources of HAP emissions. This subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limitations and operating limitations.

#### [73 FR 3603, Jan. 18, 2008]

#### § 63.6585 Am I subject to this subpart?

You are subject to this subpart if you own or operate a stationary RICE at a major or area source of HAP emissions, except if the stationary RICE is being tested at a stationary RICE test cell/stand.

(a) A stationary RICE is any internal combustion engine which uses reciprocating motion to convert heat energy into mechanical work and which is not mobile. Stationary RICE differ from mobile RICE in that a stationary RICE is not a non-road engine as defined at <u>40 CFR 1068.30</u>, and is not used to propel a motor vehicle or a vehicle used solely for competition.

(b) A major source of HAP emissions is a plant site that emits or has the potential to emit any single HAP at a rate of 10 tons (9.07 megagrams) or more per year or any combination of HAP at a rate of 25 tons (22.68 megagrams) or more per year, except that for oil and gas production facilities, a major source of HAP emissions is determined for each surface site.

(c) An area source of HAP emissions is a source that is not a major source.

(d) If you are an owner or operator of an area source subject to this subpart, your status as an entity subject to a standard or other requirements under this subpart does not subject you to the obligation to obtain a permit under  $\frac{40 \text{ CFR part 70}}{1000 \text{ cFR part 70}}$  or  $\frac{71}{1000 \text{ c$ 

(e) If you are an owner or operator of a stationary RICE used for national security purposes, you may be eligible to request an exemption from the requirements of this subpart as described in <u>40 CFR part 1068, subpart C</u>.

(f) The emergency stationary RICE listed in <u>paragraphs (f)(1)</u> through (3) of this section are not subject to this subpart. The stationary RICE must meet the definition of an emergency stationary RICE in § 63.6675, which includes operating according to the provisions specified in § 63.6640(f).

(1) Existing residential emergency stationary RICE located at an area source of HAP emissions that do not operate for the purpose specified in  $\S 63.6640(f)(4)(ii)$ .

(3) Existing institutional emergency stationary RICE located at an area source of HAP emissions that do not operate for the purpose specified in  $\frac{63.6640(f)(4)(ii)}{10}$ .

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>73 FR 3603</u>, Jan. 18, 2008; <u>78 FR 6700</u>, Jan. 30, 2013; <u>87 FR 48607</u>, Aug. 10, 2022]

#### § 63.6590 What parts of my plant does this subpart cover?

This subpart applies to each affected source.

(a) *Affected source*. An affected source is any existing, new, or reconstructed stationary RICE located at a major or area source of HAP emissions, excluding stationary RICE being tested at a stationary RICE test cell/stand.

(1) Existing stationary RICE.

(i) For stationary RICE with a site rating of more than 500 brake horsepower (HP) located at a major source of HAP emissions, a stationary RICE is existing if you commenced construction or reconstruction of the stationary RICE before December 19, 2002.

(ii) For stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions, a stationary RICE is existing if you commenced construction or reconstruction of the stationary RICE before June 12, 2006.

(iii) For stationary RICE located at an area source of HAP emissions, a stationary RICE is existing if you commenced construction or reconstruction of the stationary RICE before June 12, 2006.

(iv) A change in ownership of an existing stationary RICE does not make that stationary RICE a new or reconstructed stationary RICE.

(2) New stationary RICE.

(i) A stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions is new if you commenced construction of the stationary RICE on or after December 19, 2002.

(ii) A stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions is new if you commenced construction of the stationary RICE on or after June 12, 2006.

(iii) A stationary RICE located at an area source of HAP emissions is new if you commenced construction of the stationary RICE on or after June 12, 2006.

# (3) *Reconstructed stationary RICE*.

(i) A stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions is reconstructed if you meet the definition of reconstruction in  $\S$  63.2 and reconstruction is commenced on or after December 19, 2002.

(ii) A stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions is reconstructed if you meet the definition of reconstruction in  $\S$  63.2 and reconstruction is commenced on or after June 12, 2006.

(iii) A stationary RICE located at an area source of HAP emissions is reconstructed if you meet the definition of reconstruction in  $\frac{\$ 63.2}{2}$  and reconstruction is commenced on or after June 12, 2006.

(b) Stationary RICE subject to limited requirements.

(1) An affected source which meets either of the criteria in <u>paragraphs (b)(1)(i)</u> through <u>(ii)</u> of this section does not have to meet the requirements of this subpart and of <u>subpart A of this part</u> except for the initial notification requirements of  $\underline{\$}$  <u>63.6645(f)</u>.

(i) The stationary RICE is a new or reconstructed emergency stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions.

(ii) The stationary RICE is a new or reconstructed limited use stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions.

(2) A new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis must meet the initial notification requirements of  $\frac{63.6645(f)}{10}$  and the requirements of  $\frac{863.6625(c)}{10}$ ,  $\frac{63.6655(c)}{10}$ . These stationary RICE do not have to meet the emission limitations and operating limitations of this subpart.

(3) The following stationary RICE do not have to meet the requirements of this subpart and of <u>subpart A of this part</u>, including initial notification requirements:

(i) Existing spark ignition 2 stroke lean burn (2SLB) stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions;

(ii) Existing spark ignition 4 stroke lean burn (4SLB) stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions;

(iii) Existing emergency stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions.

(iv) Existing limited use stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions;

(v) Existing stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis;

(c) *Stationary RICE subject to Regulations under <u>40 CFR Part 60</u>. An affected source that meets any of the criteria in <u>paragraphs (c)(1)</u> through (7) of this section must meet the requirements of this part by meeting the requirements of <u>40</u> <u>CFR part 60 subpart IIII</u>, for compression ignition engines or <u>40 CFR part 60 subpart JJJJ</u>, for spark ignition engines. No further requirements apply for such engines under this part.* 

(1) A new or reconstructed stationary RICE located at an area source;

(2) A new or reconstructed 2SLB stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions;

(3) A new or reconstructed 4SLB stationary RICE with a site rating of less than 250 brake HP located at a major source of HAP emissions;

(4) A new or reconstructed spark ignition 4 stroke rich burn (4SRB) stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions;

(5) A new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis;

(6) A new or reconstructed emergency or limited use stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions;

(7) A new or reconstructed compression ignition (CI) stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions.

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>73 FR 3604</u>, Jan. 18, 2008; <u>75 FR 9674</u>, Mar. 3, 2010; <u>75 FR 37733</u>, June 30, 2010; <u>75 FR 51588</u>, Aug. 20, 2010; <u>78 FR 6700</u>, Jan. 30, 2013; <u>87 FR 48607</u>, Aug. 10, 2022]

# § 63.6595 When do I have to comply with this subpart?

#### (a) Affected sources.

(1) If you have an existing stationary RICE, excluding existing non-emergency CI stationary RICE, with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the applicable emission limitations, operating limitations and other requirements no later than June 15, 2007. If you have an existing non-emergency CI stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, an existing stationary CI RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions, or an existing stationary CI RICE located at an area source of HAP emissions, you must comply with the applicable emission limitations, operating limitations, and other requirements no later than May 3, 2013. If you have an existing stationary SI RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions, or an existing stationary SI RICE located at an area source of HAP emissions, you must comply with the applicable emission limitations, operating limitations, and other requirements no later than May 3, 2013. If you have an existing stationary SI RICE located at an area source of HAP emissions, you must comply with the applicable emission limitations, operating limitations, and other requirements no later than October 19, 2013.

(2) If you start up your new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions before August 16, 2004, you must comply with the applicable emission limitations and operating limitations in this subpart no later than August 16, 2004.

(3) If you start up your new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions after August 16, 2004, you must comply with the applicable emission limitations and operating limitations in this subpart upon startup of your affected source.

(4) If you start up your new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions before January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart no later than January 18, 2008.

(5) If you start up your new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions after January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart upon startup of your affected source.

(6) If you start up your new or reconstructed stationary RICE located at an area source of HAP emissions before January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart no later than January 18, 2008.

(7) If you start up your new or reconstructed stationary RICE located at an area source of HAP emissions after January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart upon startup of your affected source.

(b) Area sources that become major sources. If you have an area source that increases its emissions or its potential to emit such that it becomes a major source of HAP, the compliance dates in <u>paragraphs (b)(1)</u> and (2) of this section apply to you.

(1) Any stationary RICE for which construction or reconstruction is commenced after the date when your area source becomes a major source of HAP must be in compliance with this subpart upon startup of your affected source.

(2) Any stationary RICE for which construction or reconstruction is commenced before your area source becomes a major source of HAP must be in compliance with the provisions of this subpart that are applicable to RICE located at major sources within 3 years after your area source becomes a major source of HAP.

(c) If you own or operate an affected source, you must meet the applicable notification requirements in  $\frac{\& 63.6645}{CFR \text{ part } 63, \text{ subpart } A}$ .

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>73 FR 3604</u>, Jan. 18, 2008; <u>75 FR 9675</u>, Mar. 3, 2010; <u>75 FR 51589</u>, Aug. 20, 2010; <u>78 FR 6701</u>, Jan. 30, 2013]

# **Emission and Operating Limitations**

# § 63.6600 What emission limitations and operating limitations must I meet if I own or operate a stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions?

Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in  $\frac{63.6620}{2}$  and Table 4 to this subpart.

(a) If you own or operate an existing, new, or reconstructed spark ignition 4SRB stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations in Table 1a to this subpart and the operating limitations in Table 1b to this subpart which apply to you.

(b) If you own or operate a new or reconstructed 2SLB stationary RICE with a site rating of more than 500 brake HP located at major source of HAP emissions, a new or reconstructed 4SLB stationary RICE with a site rating of more than 500 brake HP located at major source of HAP emissions, or a new or reconstructed CI stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations in Table 2a to this subpart and the operating limitations in Table 2b to this subpart which apply to you.

(c) If you own or operate any of the following stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the emission limitations in Tables 1a, 2a, 2c, and 2d to this subpart or operating limitations in Tables 1b and 2b to this subpart: an existing 2SLB stationary RICE; an existing 4SLB stationary RICE; a stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis; an emergency stationary RICE; or a limited use stationary RICE.

(d) If you own or operate an existing non-emergency stationary CI RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations in Table 2c to this subpart and the operating limitations in Table 2b to this subpart which apply to you.

[73 FR 3605, Jan. 18, 2008, as amended at 75 FR 9675, Mar. 3, 2010]

# § 63.6601 What emission limitations must I meet if I own or operate a new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 brake HP and less than or equal to 500 brake HP located at a major source of HAP emissions?

Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in § 63.6620 and Table 4 to this subpart. If you own or operate a new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at major source of HAP emissions manufactured on or after January 1, 2008, you must comply with the emission limitations in Table 2a to this subpart and the operating limitations in Table 2b to this subpart which apply to you.

[73 FR 3605, Jan. 18, 2008, as amended at 75 FR 9675, Mar. 3, 2010; 75 FR 51589, Aug. 20, 2010]

# § 63.6602 What emission limitations and other requirements must I meet if I own or operate an existing stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions?

If you own or operate an existing stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations and other requirements in Table 2c to this subpart which apply to you. Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in  $\S$  63.6620 and Table 4 to this subpart.

#### [<u>78 FR 6701</u>, Jan. 30, 2013]

# § 63.6603 What emission limitations, operating limitations, and other requirements must I meet if I own or operate an existing stationary RICE located at an area source of HAP emissions?

Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in  $\S$  63.6620 and Table 4 to this subpart.

(a) If you own or operate an existing stationary RICE located at an area source of HAP emissions, you must comply with the requirements in Table 2d to this subpart and the operating limitations in Table 2b to this subpart that apply to you.

(b) If you own or operate an existing stationary non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP that meets either paragraph (b)(1) or (2) of this section, you do not have to meet the numerical CO emission limitations specified in Table 2d of this subpart. Existing stationary non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP that meet either paragraph (b)(1) or (2) of this section must meet the management practices that are shown for stationary non-emergency CI RICE with a site rating of less than or equal to 300 HP in Table 2d of this subpart.

(1) The area source is located in an area of Alaska that is not accessible by the Federal Aid Highway System (FAHS).

(2) The stationary RICE is located at an area source that meets paragraphs (b)(2)(i), (ii), and (iii) of this section.

(i) The only connection to the FAHS is through the Alaska Marine Highway System (AMHS), or the stationary RICE operation is within an isolated grid in Alaska that is not connected to the statewide electrical grid referred to as the Alaska Railbelt Grid.

(ii) At least 10 percent of the power generated by the stationary RICE on an annual basis is used for residential purposes.

(iii) The generating capacity of the area source is less than 12 megawatts, or the stationary RICE is used exclusively for backup power for renewable energy.

(c) If you own or operate an existing stationary non-emergency CI RICE with a site rating of more than 300 HP located on an offshore vessel that is an area source of HAP and is a nonroad vehicle that is an Outer Continental Shelf (OCS) source as defined in <u>40 CFR 55.2</u>, you do not have to meet the numerical CO emission limitations specified in Table 2d of this subpart. You must meet all of the following management practices:

(1) Change oil every 1,000 hours of operation or within 1 year + 30 days of the previous change, whichever comes first. Sources have the option to utilize an oil analysis program as described in  $\frac{63.6625(i)}{10}$  in order to extend the specified oil change requirement.

(2) Inspect and clean air filters every 750 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary.

(3) Inspect fuel filters and belts, if installed, every 750 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary.

(4) Inspect all flexible hoses every 1,000 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary.

(d) If you own or operate an existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions that is certified to the Tier 1 or Tier 2 emission standards in Table 1 of 40 CFR 89.112 and that is subject to an enforceable state or local standard that requires the engine to be replaced no later than June 1, 2018, you may until January 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018, choose to comply with the management practices that are shown for stationary non-emergency CI RICE with a site rating of less than or equal to 300 HP in Table 2d of this subpart instead of the applicable emission limitations in Table 2d, operating limitations in Table 2b, and crankcase ventilation system requirements in § 63.6625(g). You must comply with the emission limitations in Table 2d and operating limitations in Table 2b that apply for non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions by January 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018. You must also comply with the crankcase ventilation system requirements in § 63.6625(g) by January 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018. You must also comply with the crankcase ventilation system requirements in § 63.6625(g) by January 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later

(e) If you own or operate an existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions that is certified to the Tier 3 (Tier 2 for engines above 560 kilowatt (kW)) emission standards in Table 1 of <u>40 CFR 89.112</u>, you may comply with the requirements under this part by meeting the requirements for Tier 3 engines (Tier 2 for engines above 560 kW) in <u>40 CFR part 60 subpart IIII</u> instead of the emission limitations and other requirements that would otherwise apply under this part for existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions.

(f) An existing non-emergency SI 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at area sources of HAP must meet the definition of remote stationary RICE in § 63.6675 on the initial compliance date for the engine, October 19, 2013, in order to be considered a remote stationary RICE under this subpart. Owners and operators of existing non-emergency SI 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at area sources of HAP that meet the definition of remote stationary RICE in § 63.6675 of this subpart as of October 19, 2013 must evaluate the status of their stationary RICE every 12 months. Owners and operators must keep records of the initial and annual evaluation of the status of the engine. If the evaluation indicates that the stationary RICE no longer meets the definition of remote stationary RICE in § 63.6675 of this subpart, the owner or operator must comply with all of the requirements for existing non-emergency SI 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at area sources of the status of the engine. If the evaluation indicates that the stationary RICE no longer meets the definition of remote stationary RICE in § 63.6675 of this subpart, the owner or operator must comply with all of the requirements for existing non-emergency SI 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at area sources of HAP that are not remote stationary RICE within 1 year of the evaluation.

[<u>75 FR 9675</u>, Mar. 3, 2010, as amended at <u>75 FR 51589</u>, Aug. 20, 2010; <u>76 FR 12866</u>, Mar. 9, 2011; <u>78 FR 6701</u>, Jan. 30, 2013; <u>89 FR 70515</u>, Aug. 30, 2024]

#### § 63.6604 What fuel requirements must I meet if I own or operate a stationary CI RICE?

(a) If you own or operate an existing non-emergency, non-black start CI stationary RICE with a site rating of more than 300 brake HP with a displacement of less than 30 liters per cylinder that uses diesel fuel, you must use diesel fuel that meets the requirements in <u>40 CFR 1090.305</u> for nonroad diesel fuel.

(b) Beginning January 1, 2015, if you own or operate an existing emergency CI stationary RICE with a site rating of more than 100 brake HP and a displacement of less than 30 liters per cylinder that uses diesel fuel and operates for the purpose specified in  $\S$  63.6640(f)(4)(ii), you must use diesel fuel that meets the requirements in 40 CFR 1090.305 for nonroad diesel fuel, except that any existing diesel fuel purchased (or otherwise obtained) prior to January 1, 2015, may be used until depleted.

#### (c) [Reserved]

(d) Existing CI stationary RICE located in Guam, American Samoa, the Commonwealth of the Northern Mariana Islands, at area sources in areas of Alaska that meet either  $\frac{63.6603(b)(1)}{63.6603(c)}$  or  $\frac{63.6603(b)(2)}{2}$ , or are on offshore vessels that meet  $\frac{63.6603(b)}{2}$  are exempt from the requirements of this section.

[78 FR 6702, Jan. 30, 2013, as amended at 85 FR 78463, Dec. 4, 2020; 87 FR 48607, Aug. 10, 2022]

#### **General Compliance Requirements**

#### § 63.6605 What are my general requirements for complying with this subpart?

(a) You must be in compliance with the emission limitations, operating limitations, and other requirements in this subpart that apply to you at all times.

(b) At all times you must operate and maintain any affected source, including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. The general duty to minimize emissions does not require you to make any further efforts to reduce emissions if levels required by this standard have been achieved. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator which may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.

[75 FR 9675, Mar. 3, 2010, as amended at 78 FR 6702, Jan. 30, 2013]

#### **Testing and Initial Compliance Requirements**

§ 63.6610 By what date must I conduct the initial performance tests or other initial compliance demonstrations if I own or operate a stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions?

If you own or operate a stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions you are subject to the requirements of this section.

(a) You must conduct the initial performance test or other initial compliance demonstrations in Table 4 to this subpart that apply to you within 180 days after the compliance date that is specified for your stationary RICE in § 63.6595 and according to the provisions in § 63.7(a)(2).

(b) If you commenced construction or reconstruction between December 19, 2002 and June 15, 2004 and own or operate stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must demonstrate initial compliance with either the proposed emission limitations or the promulgated emission limitations no later than February 10, 2005 or no later than 180 days after startup of the source, whichever is later, according to  $\frac{8}{63.7(a)(2)(ix)}$ .

(c) If you commenced construction or reconstruction between December 19, 2002 and June 15, 2004 and own or operate stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, and you chose to comply with the proposed emission limitations when demonstrating initial compliance, you must conduct a second performance test to demonstrate compliance with the promulgated emission limitations by December 13, 2007 or after startup of the source, whichever is later, according to  $\frac{\delta}{63.7(a)(2)(ix)}$ .

(d) An owner or operator is not required to conduct an initial performance test on units for which a performance test has been previously conducted, but the test must meet all of the conditions described in paragraphs (d)(1) through (5) of this section.

(1) The test must have been conducted using the same methods specified in this subpart, and these methods must have been followed correctly.

(2) The test must not be older than 2 years.

(3) The test must be reviewed and accepted by the Administrator.

(4) Either no process or equipment changes must have been made since the test was performed, or the owner or operator must be able to demonstrate that the results of the performance test, with or without adjustments, reliably demonstrate compliance despite process or equipment changes.

(5) The test must be conducted at any load condition within plus or minus 10 percent of 100 percent load.

[69 FR 33506, June 15, 2004, as amended at 73 FR 3605, Jan. 18, 2008]

#### 40 CFR 63 SUBPART ZZZZ

#### National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

# § 63.6611 By what date must I conduct the initial performance tests or other initial compliance demonstrations if I own or operate a new or reconstructed 4SLB SI stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at a major source of HAP emissions?

If you own or operate a new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at a major source of HAP emissions, you must conduct an initial performance test within 240 days after the compliance date that is specified for your stationary RICE in § 63.6595 and according to the provisions specified in Table 4 to this subpart, as appropriate.

[73 FR 3605, Jan. 18, 2008, as amended at 75 FR 51589, Aug. 20, 2010]

#### § 63.6612 By what date must I conduct the initial performance tests or other initial compliance demonstrations if I own or operate an existing stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions or an existing stationary RICE located at an area source of HAP emissions?

If you own or operate an existing stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions or an existing stationary RICE located at an area source of HAP emissions you are subject to the requirements of this section.

(a) You must conduct any initial performance test or other initial compliance demonstration according to Tables 4 and 5 to this subpart that apply to you within 180 days after the compliance date that is specified for your stationary RICE in  $\S$  <u>63.6595</u> and according to the provisions in  $\S$  <u>63.7(a)(2)</u>.

(b) An owner or operator is not required to conduct an initial performance test on a unit for which a performance test has been previously conducted, but the test must meet all of the conditions described in <u>paragraphs (b)(1)</u> through (4) of this section.

(1) The test must have been conducted using the same methods specified in this subpart, and these methods must have been followed correctly.

(2) The test must not be older than 2 years.

(3) The test must be reviewed and accepted by the Administrator.

(4) Either no process or equipment changes must have been made since the test was performed, or the owner or operator must be able to demonstrate that the results of the performance test, with or without adjustments, reliably demonstrate compliance despite process or equipment changes.

[75 FR 9676, Mar. 3, 2010, as amended at 75 FR 51589, Aug. 20, 2010]

#### § 63.6615 When must I conduct subsequent performance tests?

If you must comply with the emission limitations and operating limitations, you must conduct subsequent performance tests as specified in Table 3 of this subpart.

#### § 63.6620 What performance tests and other procedures must I use?

(a) You must conduct each performance test in Tables 3 and 4 of this subpart that applies to you.

(b) Each performance test must be conducted according to the requirements that this subpart specifies in Table 4 to this subpart. If you own or operate a non-operational stationary RICE that is subject to performance testing, you do not need to start up the engine solely to conduct the performance test. Owners and operators of a non-operational engine can conduct the performance test when the engine is started up again. The test must be conducted at any load condition within plus or minus 10 percent of 100 percent load for the stationary RICE listed in <u>paragraphs (b)(1)</u> through (4) of this section.

(1) Non-emergency 4SRB stationary RICE with a site rating of greater than 500 brake HP located at a major source of HAP emissions.

(2) New non-emergency 4SLB stationary RICE with a site rating of greater than or equal to 250 brake HP located at a major source of HAP emissions.

(3) New non-emergency 2SLB stationary RICE with a site rating of greater than 500 brake HP located at a major source of HAP emissions.

(4) New non-emergency CI stationary RICE with a site rating of greater than 500 brake HP located at a major source of HAP emissions.

(c) [Reserved]

(d) You must conduct three separate test runs for each performance test required in this section, as specified in  $\frac{63.7(e)(3)}{2}$ . Each test run must last at least 1 hour, unless otherwise specified in this subpart.

(e)

(1) You must use Equation 1 of this section to determine compliance with the percent reduction requirement:

$$\frac{C_i - C_o}{C_i} \times 100 = R \quad (Eq. 1)$$

Where:

C<sub>i</sub> = concentration of carbon monoxide (CO), total hydrocarbons (THC), or formaldehyde at the control device inlet,

 $C_o =$  concentration of CO, THC, or formaldehyde at the control device outlet, and

R = percent reduction of CO, THC, or formaldehyde emissions.

(2) You must normalize the CO, THC, or formaldehyde concentrations at the inlet and outlet of the control device to a dry basis and to 15 percent oxygen, or an equivalent percent carbon dioxide (CO<sub>2</sub>). If pollutant concentrations are to be corrected to 15 percent oxygen and CO<sub>2</sub> concentration is measured in lieu of oxygen concentration measurement, a CO<sub>2</sub> correction factor is needed. Calculate the CO<sub>2</sub> correction factor as described in <u>paragraphs (e)(2)(i)</u> through (<u>iii)</u> of this section.

(i) Calculate the fuel-specific  $F_o$  value for the fuel burned during the test using values obtained from Method 19, <u>Section 5.2</u>, and the following equation:

$$F_{O} = \frac{0.209 \ F_{d}}{F_{C}} (Eq. 2)$$

Where:

 $F_o =$  Fuel factor based on the ratio of oxygen volume to the ultimate  $CO_2$  volume produced by the fuel at zero percent excess air.

0.209 = Fraction of air that is oxygen, percent/100.

 $F_d$  = Ratio of the volume of dry effluent gas to the gross calorific value of the fuel from Method 19, dsm<sup>3</sup>/J (dscf/10<sup>6</sup> Btu).

 $F_c = Ratio of the volume of CO_2 produced to the gross calorific value of the fuel from Method 19, dsm<sup>3</sup>/J (dscf/10<sup>6</sup> Btu)$ 

(ii) Calculate the CO<sub>2</sub> correction factor for correcting measurement data to 15 percent O<sub>2</sub>, as follows:

$$X_{CO2} = \frac{5.9}{F_0}$$
 (Eq. 3)

Where:

 $X_{CO2} = CO_2$  correction factor, percent.

5.9 = 20.9 percent O<sub>2</sub>—15 percent O<sub>2</sub>, the defined O<sub>2</sub> correction value, percent.

(iii) Calculate the CO, THC, and formaldehyde gas concentrations adjusted to 15 percent O<sub>2</sub> using CO<sub>2</sub> as follows:

$$C_{adj} = C_d \frac{X_{CO2}}{%CO_2} \quad (Eq.4)$$

Where:

 $C_{adj}$  = Calculated concentration of CO, THC, or formaldehyde adjusted to 15 percent  $O_2$ .

 $C_d$  = Measured concentration of CO, THC, or formaldehyde, uncorrected.

 $X_{CO2} = CO_2$  correction factor, percent.

 $CO_2 =$  Measured CO<sub>2</sub> concentration measured, dry basis, percent.

(f) If you comply with the emission limitation to reduce CO and you are not using an oxidation catalyst, if you comply with the emission limitation to reduce formaldehyde and you are not using NSCR, or if you comply with the emission limitation to limit the concentration of formaldehyde in the stationary RICE exhaust and you are not using an oxidation catalyst or NSCR, you must petition the Administrator for operating limitations to be established during the initial performance test and continuously monitored thereafter; or for approval of no operating limitations. You must not conduct the initial performance test until after the petition has been approved by the Administrator.

(g) If you petition the Administrator for approval of operating limitations, your petition must include the information described in <u>paragraphs (g)(1)</u> through (5) of this section.

(1) Identification of the specific parameters you propose to use as operating limitations;

(2) A discussion of the relationship between these parameters and HAP emissions, identifying how HAP emissions change with changes in these parameters, and how limitations on these parameters will serve to limit HAP emissions;

(3) A discussion of how you will establish the upper and/or lower values for these parameters which will establish the limits on these parameters in the operating limitations;

(4) A discussion identifying the methods you will use to measure and the instruments you will use to monitor these parameters, as well as the relative accuracy and precision of these methods and instruments; and

(5) A discussion identifying the frequency and methods for recalibrating the instruments you will use for monitoring these parameters.

(h) If you petition the Administrator for approval of no operating limitations, your petition must include the information described in <u>paragraphs (h)(1)</u> through (7) of this section.

(1) Identification of the parameters associated with operation of the stationary RICE and any emission control device which could change intentionally (*e.g.*, operator adjustment, automatic controller adjustment, etc.) or unintentionally (*e.g.*, wear and tear, error, etc.) on a routine basis or over time;

(2) A discussion of the relationship, if any, between changes in the parameters and changes in HAP emissions;

(3) For the parameters which could change in such a way as to increase HAP emissions, a discussion of whether establishing limitations on the parameters would serve to limit HAP emissions;

(4) For the parameters which could change in such a way as to increase HAP emissions, a discussion of how you could establish upper and/or lower values for the parameters which would establish limits on the parameters in operating limitations;

(5) For the parameters, a discussion identifying the methods you could use to measure them and the instruments you could use to monitor them, as well as the relative accuracy and precision of the methods and instruments;

(6) For the parameters, a discussion identifying the frequency and methods for recalibrating the instruments you could use to monitor them; and

(7) A discussion of why, from your point of view, it is infeasible or unreasonable to adopt the parameters as operating limitations.
(i) The engine percent load during a performance test must be determined by documenting the calculations, assumptions, and measurement devices used to measure or estimate the percent load in a specific application. A written report of the average percent load determination must be included in the notification of compliance status. The following information must be included in the written report: the engine model number, the engine manufacturer, the year of purchase, the manufacturer's site-rated brake horsepower, the ambient temperature, pressure, and humidity during the performance test, and all assumptions that were made to estimate or calculate percent load during the performance test must be clearly explained. If measurement devices such as flow meters, kilowatt meters, beta analyzers, stain gauges, etc. are used, the model number of the measurement device, and an estimate of its accurate in percentage of true value must be provided.

(j) Beginning on February 26, 2025, within 60 days after the date of completing each performance test required by this subpart, you must submit the results of the performance test following the procedure specified in § 63.9(k). Data collected using test methods supported by the EPA's Electronic Reporting Tool (ERT) as listed on the EPA's ERT website (*https://www.epa.gov/electronic-reporting-air-emissions/electronic-reporting-tool-ert*) at the time of the test must be submitted in a file format generated using the EPA's ERT. Alternatively, you may submit an electronic file consistent with the extensible markup language (XML) schema listed on the EPA's ERT website. Data collected using test methods that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the test must be included as an attachment in the ERT or alternate electronic file.

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>75 FR 9676</u>, Mar. 3, 2010; <u>78 FR 6702</u>, Jan. 30, 2013; <u>89 FR 70516</u>, Aug. 30, 2024]

# § 63.6625 What are my monitoring, installation, collection, operation, and maintenance requirements?

(a) If you elect to install a CEMS as specified in Table 5 of this subpart, you must install, operate, and maintain a CEMS to monitor CO and either  $O_2$  or  $CO_2$  according to the requirements in <u>paragraphs (a)(1)</u> through (4) of this section. If you are meeting a requirement to reduce CO emissions, the CEMS must be installed at both the inlet and outlet of the control device. If you are meeting a requirement to limit the concentration of CO, the CEMS must be installed at the outlet of the control device.

(1) Each CEMS must be installed, operated, and maintained according to the applicable performance specifications of  $\frac{40}{CFR}$  part 60, appendix B.

(2) You must conduct an initial performance evaluation and an annual relative accuracy test audit (RATA) of each CEMS according to the requirements in § 63.8 and according to the applicable performance specifications of  $\frac{40 \text{ CFR part } 60}{40 \text{ CFR part } 60}$ , appendix B as well as daily and periodic data quality checks in accordance with  $\frac{40 \text{ CFR part } 60}{40 \text{ CFR part } 60}$ , appendix F, procedure 1.

(3) As specified in  $\frac{63.8(c)(4)(ii)}{1000}$ , each CEMS must complete a minimum of one cycle of operation (sampling, analyzing, and data recording) for each successive 15-minute period. You must have at least two data points, with each representing a different 15-minute period, to have a valid hour of data.

(4) The CEMS data must be reduced as specified in  $\S$  63.8(g)(2) and recorded in parts per million or parts per billion (as appropriate for the applicable limitation) at 15 percent oxygen or the equivalent CO<sub>2</sub> concentration.

(5) Beginning on February 26, 2025, within 60 days after the date of completing each continuous emissions monitoring system (CEMS) performance evaluation (as defined in § 63.2) that includes a relative accuracy test audit (RATA), you must submit the results of the performance evaluation following the procedures specified in § 63.9(k). The results of performance evaluations of CEMS measuring RATA pollutants that are supported by the EPA's ERT as listed on the EPA's ERT website at the time of the evaluation must be submitted in a file format generated using the EPA's ERT. Alternatively, you may submit an electronic file consistent with the XML schema listed on the EPA's ERT website. The results of performance evaluations of CEMS measuring RATA pollutants that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the evaluation must be included as an attachment in the ERT or alternate electronic file.

(b) If you are required to install a continuous parameter monitoring system (CPMS) as specified in Table 5 of this subpart, you must install, operate, and maintain each CPMS according to the requirements in <u>paragraphs (b)(1)</u> through (6) of this section. For an affected source that is complying with the emission limitations and operating limitations on March 9, 2011, the requirements in <u>paragraph (b)</u> of this section are applicable September 6, 2011.

(1) You must prepare a site-specific monitoring plan that addresses the monitoring system design, data collection, and the quality assurance and quality control elements outlined in <u>paragraphs (b)(1)(i)</u> through (v) of this section and in  $\frac{63.8(d)}{2}$ . As

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specified in  $\S$  <u>63.8(f)(4)</u>, you may request approval of monitoring system quality assurance and quality control procedures alternative to those specified in paragraphs (b)(1) through (5) of this section in your site-specific monitoring plan.

(i) The performance criteria and design specifications for the monitoring system equipment, including the sample interface, detector signal analyzer, and data acquisition and calculations;

(ii) Sampling interface (*e.g.*, thermocouple) location such that the monitoring system will provide representative measurements;

(iii) Equipment performance evaluations, system accuracy audits, or other audit procedures;

(iv) Ongoing operation and maintenance procedures in accordance with provisions in  $\frac{63.8(c)(1)(ii)}{2}$  and  $\frac{(c)(3)}{2}$ ; and

(v) Ongoing reporting and recordkeeping procedures in accordance with provisions in  $\S$  <u>63.10(c)</u>, <u>(e)(1)</u>, and <u>(e)(2)(i)</u>.

(2) You must install, operate, and maintain each CPMS in continuous operation according to the procedures in your site-specific monitoring plan.

(3) The CPMS must collect data at least once every 15 minutes (see also § 63.6635).

(4) For a CPMS for measuring temperature range, the temperature sensor must have a minimum tolerance of 2.8 degrees Celsius (5 degrees Fahrenheit) or 1 percent of the measurement range, whichever is larger.

(5) You must conduct the CPMS equipment performance evaluation, system accuracy audits, or other audit procedures specified in your site-specific monitoring plan at least annually.

(6) You must conduct a performance evaluation of each CPMS in accordance with your site-specific monitoring plan.

(c) If you are operating a new or reconstructed stationary RICE which fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, you must monitor and record your fuel usage daily with separate fuel meters to measure the volumetric flow rate of each fuel. In addition, you must operate your stationary RICE in a manner which reasonably minimizes HAP emissions.

(d) If you are operating a new or reconstructed emergency 4SLB stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at a major source of HAP emissions, you must install a non-resettable hour meter prior to the startup of the engine.

(e) If you own or operate any of the following stationary RICE, you must operate and maintain the stationary RICE and aftertreatment control device (if any) according to the manufacturer's emission-related written instructions or develop your own maintenance plan which must provide to the extent practicable for the maintenance and operation of the engine in a manner consistent with good air pollution control practice for minimizing emissions:

(1) An existing stationary RICE with a site rating of less than 100 HP located at a major source of HAP emissions;

(2) An existing emergency or black start stationary RICE with a site rating of less than or equal to 500 HP located at a major source of HAP emissions;

(3) An existing emergency or black start stationary RICE located at an area source of HAP emissions;

(4) An existing non-emergency, non-black start stationary CI RICE with a site rating less than or equal to 300 HP located at an area source of HAP emissions;

(5) An existing non-emergency, non-black start 2SLB stationary RICE located at an area source of HAP emissions;

(6) An existing non-emergency, non-black start stationary RICE located at an area source of HAP emissions which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis.

(7) An existing non-emergency, non-black start 4SLB stationary RICE with a site rating less than or equal to 500 HP located at an area source of HAP emissions;

(8) An existing non-emergency, non-black start 4SRB stationary RICE with a site rating less than or equal to 500 HP located at an area source of HAP emissions;

(9) An existing, non-emergency, non-black start 4SLB stationary RICE with a site rating greater than 500 HP located at an area source of HAP emissions that is operated 24 hours or less per calendar year; and

(10) An existing, non-emergency, non-black start 4SRB stationary RICE with a site rating greater than 500 HP located at an area source of HAP emissions that is operated 24 hours or less per calendar year.

(f) If you own or operate an existing emergency stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions or an existing emergency stationary RICE located at an area source of HAP emissions, you must install a non-resettable hour meter if one is not already installed.

(g) If you own or operate an existing non-emergency, non-black start CI engine greater than or equal to 300 HP that is not equipped with a closed crankcase ventilation system, you must comply with either paragraph (g)(1) or paragraph (2) of this section. Owners and operators must follow the manufacturer's specified maintenance requirements for operating and maintaining the open or closed crankcase ventilation systems and replacing the crankcase filters, or can request the Administrator to approve different maintenance requirements that are as protective as manufacturer requirements. Existing CI engines located at area sources in areas of Alaska that meet either  $\S$  63.6603(b)(1) or  $\S$  63.6603(b)(2) do not have to meet the requirements of this paragraph (g).

(1) Install a closed crankcase ventilation system that prevents crankcase emissions from being emitted to the atmosphere, or

(2) Install an open crankcase filtration emission control system that reduces emissions from the crankcase by filtering the exhaust stream to remove oil mist, particulates and metals.

(h) If you operate a new, reconstructed, or existing stationary engine, you must minimize the engine's time spent at idle during startup and minimize the engine's startup time to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the emission standards applicable to all times other than startup in Tables 1a, 2a, 2c, and 2d to this subpart apply.

(i) If you own or operate a stationary CI engine that is subject to the work, operation or management practices in items 1 or 2 of table 2c to this subpart or in items 1 or 4 of table 2d to this subpart, you have the option of utilizing an oil analysis program in order to extend the specified oil and filter change requirement in tables 2c and 2d to this subpart. The oil analysis must be performed at the same frequency specified for changing the oil and filter in table 2c or 2d to this subpart. The analysis program must at a minimum analyze the following three parameters: Total Base Number, viscosity, and percent water content. The condemning limits for these parameters are as follows: Total Base Number is less than 30 percent of the Total Base Number of the oil when new; viscosity of the oil has changed by more than 20 percent from the viscosity of the oil when new; or percent water content (by volume) is greater than 0.5. If all of these condemning limits are not exceeded, the engine owner or operator is not required to change the oil and filter. If any of the limits are exceeded, the engine owner or operator must change the oil and filter within 2 business days of receiving the results of the analysis; if the engine is not in operation when the results of the analysis are received, the engine owner or operator must change the oil and filter within 2 business days of receiving the results of the analysis; if the engine is not in operation when the results of the analysis are received, the engine owner or operator must change the oil and filter within 2 business days or before commencing operation, whichever is later. The owner or operator must keep records of the analyzed as part of the program, the results of the analysis, and the oil and filter changes for the engine. The analysis program must be part of the maintenance plan for the engine.

(j) If you own or operate a stationary SI engine that is subject to the work, operation or management practices in items 6, 7, or 8 of table 2c to this subpart or in items 5, 6, 7, 8, 10, 11, or 13 of table 2d to this subpart, you have the option of utilizing an oil analysis program in order to extend the specified oil and filter change requirement in tables 2c and 2d to this subpart. The oil analysis program must at a minimum analyze the following three parameters: Total Acid Number, viscosity, and percent water content. The condemning limits for these parameters are as follows: Total Acid Number increases by more than 3.0 milligrams of potassium hydroxide (KOH) per gram from Total Acid Number of the oil when new; viscosity of the oil has changed by more than 20 percent from the viscosity of the oil when new; or percent water content (by volume) is greater than 0.5. If all of these condemning limits are not exceeded, the engine owner or operator is not required to change the oil and filter. If any of the limits are exceeded, the engine is not in operation when the results of the analysis are received, the engine owner or operator must change the oil and filter within 2 business days or before commencing operation, whichever is later. The owner or operator must keep records of the parameters that are analyzed as part of the program, the results of the analysis, and the oil and filter changes for the engine. The analysis program must be part of the maintenance plan for the engine.

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[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>73 FR 3606</u>, Jan. 18, 2008; <u>75 FR 9676</u>, Mar. 3, 2010; <u>75 FR 51589</u>, Aug. 20, 2010; <u>76 FR 12866</u>, Mar. 9, 2011; <u>78 FR 6703</u>, Jan. 30, 2013; <u>89 FR 70516</u>, Aug. 30, 2024]

# § 63.6630 How do I demonstrate initial compliance with the emission limitations, operating limitations, and other requirements?

(a) You must demonstrate initial compliance with each emission limitation, operating limitation, and other requirement that applies to you according to Table 5 of this subpart.

(b) During the initial performance test, you must establish each operating limitation in Tables 1b and 2b of this subpart that applies to you.

(c) You must submit the Notification of Compliance Status containing the results of the initial compliance demonstration according to the requirements in  $\S$  63.6645.

(d) Non-emergency 4SRB stationary RICE complying with the requirement to reduce formaldehyde emissions by 76 percent or more can demonstrate initial compliance with the formaldehyde emission limit by testing for THC instead of formaldehyde. The testing must be conducted according to the requirements in Table 4 of this subpart. The average reduction of emissions of THC determined from the performance test must be equal to or greater than 30 percent.

(e) The initial compliance demonstration required for existing non-emergency 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year must be conducted according to the following requirements:

(1) The compliance demonstration must consist of at least three test runs.

(2) Each test run must be of at least 15 minute duration, except that each test conducted using the method in appendix A to this subpart must consist of at least one measurement cycle and include at least 2 minutes of test data phase measurement.

(3) If you are demonstrating compliance with the CO concentration or CO percent reduction requirement, you must measure CO emissions using one of the CO measurement methods specified in Table 4 of this subpart, or using appendix A to this subpart.

(4) If you are demonstrating compliance with the THC percent reduction requirement, you must measure THC emissions using Method 25A, reported as propane, of <u>40 CFR part 60, appendix A</u>.

(5) You must measure  $O_2$  using one of the  $O_2$  measurement methods specified in Table 4 of this subpart. Measurements to determine  $O_2$  concentration must be made at the same time as the measurements for CO or THC concentration.

(6) If you are demonstrating compliance with the CO or THC percent reduction requirement, you must measure CO or THC emissions and  $O_2$  emissions simultaneously at the inlet and outlet of the control device.

[69 FR 33506, June 15, 2004, as amended at 78 FR 6704, Jan. 30, 2013]

# **Continuous Compliance Requirements**

#### § 63.6635 How do I monitor and collect data to demonstrate continuous compliance?

(a) If you must comply with emission and operating limitations, you must monitor and collect data according to this section.

(b) Except for monitor malfunctions, associated repairs, required performance evaluations, and required quality assurance or control activities, you must monitor continuously at all times that the stationary RICE is operating. A monitoring malfunction is any sudden, infrequent, not reasonably preventable failure of the monitoring to provide valid data. Monitoring failures that are caused in part by poor maintenance or careless operation are not malfunctions.

(c) You may not use data recorded during monitoring malfunctions, associated repairs, and required quality assurance or control activities in data averages and calculations used to report emission or operating levels. You must, however, use all the valid data collected during all other periods.

[69 FR 33506, June 15, 2004, as amended at 76 FR 12867, Mar. 9, 2011]

§ 63.6640 How do I demonstrate continuous compliance with the emission limitations, operating limitations, and other requirements?

(a) You must demonstrate continuous compliance with each emission limitation, operating limitation, and other requirements in Tables 1a and 1b, Tables 2a and 2b, Table 2c, and Table 2d to this subpart that apply to you according to methods specified in Table 6 to this subpart.

(b) You must report each instance in which you did not meet each emission limitation or operating limitation in Tables 1a and 1b, Tables 2a and 2b, Table 2c, and Table 2d to this subpart that apply to you. These instances are deviations from the emission and operating limitations in this subpart. These deviations must be reported according to the requirements in  $\S$  63.6650. If you change your catalyst, you must reestablish the values of the operating parameters measured during the initial performance test. When you reestablish the values of your operating parameters, you must also conduct a performance test to demonstrate that you are meeting the required emission limitation applicable to your stationary RICE.

(c) The annual compliance demonstration required for existing non-emergency 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year must be conducted according to the following requirements:

(1) The compliance demonstration must consist of at least one test run.

(2) Each test run must be of at least 15 minute duration, except that each test conducted using the method in appendix A to this subpart must consist of at least one measurement cycle and include at least 2 minutes of test data phase measurement.

(3) If you are demonstrating compliance with the CO concentration or CO percent reduction requirement, you must measure CO emissions using one of the CO measurement methods specified in Table 4 of this subpart, or using appendix A to this subpart.

(4) If you are demonstrating compliance with the THC percent reduction requirement, you must measure THC emissions using Method 25A, reported as propane, of  $\frac{40 \text{ CFR part } 60, \text{ appendix } A}{40 \text{ CFR part } 60, \text{ appendix } A}$ .

(5) You must measure  $O_2$  using one of the  $O_2$  measurement methods specified in Table 4 of this subpart. Measurements to determine  $O_2$  concentration must be made at the same time as the measurements for CO or THC concentration.

(6) If you are demonstrating compliance with the CO or THC percent reduction requirement, you must measure CO or THC emissions and  $O_2$  emissions simultaneously at the inlet and outlet of the control device.

(7) If the results of the annual compliance demonstration show that the emissions exceed the levels specified in Table 6 of this subpart, the stationary RICE must be shut down as soon as safely possible, and appropriate corrective action must be taken (e.g., repairs, catalyst cleaning, catalyst replacement). The stationary RICE must be retested within 7 days of being restarted and the emissions must meet the levels specified in Table 6 of this subpart. If the retest shows that the emissions continue to exceed the specified levels, the stationary RICE must again be shut down as soon as safely possible, and the stationary RICE may not operate, except for purposes of startup and testing, until the owner/operator demonstrates through testing that the emissions do not exceed the levels specified in Table 6 of this subpart.

(d) For new, reconstructed, and rebuilt stationary RICE, deviations from the emission or operating limitations that occur during the first 200 hours of operation from engine startup (engine burn-in period) are not violations. Rebuilt stationary RICE means a stationary RICE that has been rebuilt as that term is defined in  $\frac{40 \text{ CFR 94.11}(a)}{40 \text{ CFR 94.11}(a)}$ .

(e) You must also report each instance in which you did not meet the requirements in Table 8 to this subpart that apply to you. If you own or operate a new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions (except new or reconstructed 4SLB engines greater than or equal to 250 and less than or equal to 500 brake HP), a new or reconstructed stationary RICE located at an area source of HAP emissions, or any of the following RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the requirements in Table 8 to this subpart: An existing 2SLB stationary RICE, an existing 4SLB stationary RICE, an existing emergency stationary RICE, an existing stationary RICE wich fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis. If you own or operate any of the following RICE with a site rating of more than 500 brake the located at a major source of HAP emissions, you do not need to comply with the requirements in Table 8 to this subpart. Subpart, except for the initial notification requirements: a new or reconstructed stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, a new or reconstructed emergency stationary RICE, or a new or reconstructed limited use stationary RICE, or a new or reconstructed stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, a new or reconstructed emergency stationary RICE, or a new or reconstructed limited use stationary RICE, or a new or reconstructed limited use stationary RICE, or a new or reconstructed limited use stationary RICE, or a new or reconstructed limited use stationary RICE.

(f) If you own or operate an emergency stationary RICE, you must operate the emergency stationary RICE according to the requirements in <u>paragraphs (f)(1)</u> through (4) of this section. In order for the engine to be considered an emergency stationary RICE under this subpart, any operation other than emergency operation, maintenance and testing, and operation in non-emergency situations for 50 hours per year, as described in paragraphs (f)(1) through (4), is prohibited. If you do not operate the engine according to the requirements in paragraphs (f)(1) through (4), the engine will not be considered an emergency engine under this subpart and must meet all requirements for non-emergency engines.

(1) There is no time limit on the use of emergency stationary RICE in emergency situations.

(2) You may operate your emergency stationary RICE for the purpose specified in <u>paragraph (f)(2)(i)</u> of this section for a maximum of 100 hours per calendar year. Any operation for non-emergency situations as allowed by <u>paragraphs</u> (f)(3) and (4) of this section counts as part of the 100 hours per calendar year allowed by this <u>paragraph (f)(2)</u>.

(i) Emergency stationary RICE may be operated for maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor, the regional transmission organization or equivalent balancing authority and transmission operator, or the insurance company associated with the engine. The owner or operator may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if the owner or operator maintains records indicating that federal, state, or local standards require maintenance and testing of emergency RICE beyond 100 hours per calendar year.

(ii)-(iii) [Reserved]

(3) Emergency stationary RICE located at major sources of HAP may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing provided in paragraph (f)(2) of this section. The 50 hours per year for non-emergency situations cannot be used for peak shaving or non-emergency demand response, or to generate income for a facility to supply power to an electric grid or otherwise supply power as part of a financial arrangement with another entity.

(4) Emergency stationary RICE located at area sources of HAP may be operated for up to 50 hours per calendar year in nonemergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing provided in <u>paragraph (f)(2)</u> of this section. Except as provided in <u>paragraphs</u> (f)(4)(i) and (ii) of this section, the 50 hours per year for non-emergency situations cannot be used for peak shaving or nonemergency demand response, or to generate income for a facility to an electric grid or otherwise supply power as part of a financial arrangement with another entity.

(i) Prior to May 3, 2014, the 50 hours per year for non-emergency situations can be used for peak shaving or non-emergency demand response to generate income for a facility, or to otherwise supply power as part of a financial arrangement with another entity if the engine is operated as part of a peak shaving (load management program) with the local distribution system operator and the power is provided only to the facility itself or to support the local distribution system.

(ii) The 50 hours per year for non-emergency situations can be used to supply power as part of a financial arrangement with another entity if all of the following conditions are met:

(A) The engine is dispatched by the local balancing authority or local transmission and distribution system operator.

(B) The dispatch is intended to mitigate local transmission and/or distribution limitations so as to avert potential voltage collapse or line overloads that could lead to the interruption of power supply in a local area or region.

(C) The dispatch follows reliability, emergency operation or similar protocols that follow specific NERC, regional, state, public utility commission or local standards or guidelines.

(D) The power is provided only to the facility itself or to support the local transmission and distribution system.

(E) The owner or operator identifies and records the entity that dispatches the engine and the specific NERC, regional, state, public utility commission or local standards or guidelines that are being followed for dispatching the engine. The local balancing authority or local transmission and distribution system operator may keep these records on behalf of the engine owner or operator.

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>71 FR 20467</u>, Apr. 20, 2006; <u>73 FR 3606</u>, Jan. 18, 2008; <u>75 FR 9676</u>, Mar. 3, 2010; <u>75 FR 51591</u>, Aug. 20, 2010; <u>78 FR 6704</u>, Jan. 30, 2013; <u>87 FR 48607</u>, Aug. 10, 2022]

## National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

# Notifications, Reports, and Records

# § 63.6645 What notifications must I submit and when?

(a) You must submit all of the notifications in  $\underline{\$\$ 63.7(b)}$  and (c),  $\underline{63.8(e)}$ , (f)(4) and (f)(6),  $\underline{63.9(b)}$  through (e), and (g) and (h) that apply to you by the dates specified if you own or operate any of the following;

(1) An existing stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions.

(2) An existing stationary RICE located at an area source of HAP emissions.

(3) A stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions.

(4) A new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 HP located at a major source of HAP emissions.

(5) This requirement does not apply if you own or operate an existing stationary RICE less than 100 HP, an existing stationary emergency RICE, or an existing stationary RICE that is not subject to any numerical emission standards.

(b) As specified in  $\frac{63.9(b)(2)}{10}$ , if you start up your stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions before the effective date of this subpart, you must submit an initial notification not later than December 13, 2004, or no later than 120 days after the source becomes subject to this subpart, whichever is later. Beginning on February 26, 2025, submit the notification electronically in portable document format (PDF) consistent with  $\frac{63.9(k)}{50.00}$ .

(c) If you start up your new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions on or after August 16, 2004, you must submit an initial notification not later than 120 days after you become subject to this subpart. Beginning on February 26, 2025, submit the notification electronically in PDF consistent with  $\frac{63.9(k)}{2}$ .

(d) As specified in § 63.9(b)(2), if you start up your stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions before the effective date of this subpart and you are required to submit an initial notification, you must submit an initial notification not later than July 16, 2008, or no later than 120 days after the source becomes subject to this subpart, whichever is later. Beginning on February 26, 2025, submit the notification electronically in PDF consistent with § 63.9(k).

(e) If you start up your new or reconstructed stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions on or after March 18, 2008, and you are required to submit an initial notification, you must submit an initial notification not later than 120 days after you become subject to this subpart. Beginning on February 26, 2025, submit the notification electronically in PDF consistent with  $\frac{\delta 63.9(k)}{\delta 20.000}$ .

(f) If you are required to submit an Initial Notification but are otherwise not affected by the requirements of this subpart, in accordance with § 63.6590(b), your notification should include the information in § 63.9(b)(2)(i) through (v), and a statement that your stationary RICE has no additional requirements and explain the basis of the exclusion (for example, that it operates exclusively as an emergency stationary RICE if it has a site rating of more than 500 brake HP located at a major source of HAP emissions).

(g) If you are required to conduct a performance test, you must submit a Notification of Intent to conduct a performance test at least 60 days before the performance test is scheduled to begin as required in  $\frac{63.7(b)(1)}{2}$ .

(h) If you are required to conduct a performance test or other initial compliance demonstration as specified in Tables 4 and 5 to this subpart, you must submit a Notification of Compliance Status according to  $\frac{\delta}{63.9(h)(2)(ii)}$ .

(1) For each initial compliance demonstration required in Table 5 to this subpart that does not include a performance test, you must submit the Notification of Compliance Status before the close of business on the 30th day following the completion of the initial compliance demonstration.

(2) Before February 26, 2025, for each initial compliance demonstration required in table 5 to this subpart that includes a performance test conducted according to the requirements in table 3 to this subpart, you must submit the Notification of Compliance Status, including the performance test results, before the close of business on the 60th day following the completion of the performance test according to  $\frac{63.10(d)(2)}{2}$ . Beginning on February 26, 2025, for each initial compliance demonstration required in table 5 to this subpart that includes a performance test conducted according to the requirements in

table 3 to this subpart, you must submit the Notification of Compliance Status, including a summary of the performance test results, in PDF to the EPA via the Compliance and Emissions Data Reporting Interface (CEDRI), before the close of business on the 60th day following the completion of the performance test following the procedure specified in  $\S$  63.9(k), except any Confidential Business Information (CBI) is to be submitted according to paragraphs (h)(2)(i) and (ii) of this section. Do not use CEDRI to submit information you claim as CBI. Although we do not expect persons to assert a claim of CBI, if you wish to assert a CBI claim for some of the information in the report, you must submit a complete file, including information claimed to be CBI, to the EPA following the procedures in paragraphs (h)(2)(i) and (ii) of this section. Clearly mark the part or all of the information marked as CBI will not be disclosed except in accordance with procedures set forth in <u>40</u> <u>CFR part 2</u>. All CBI claims must be asserted at the time of submission. Anything submitted using CEDRI cannot later be claimed CBI. Furthermore, under CAA section 114(c), emissions data is not entitled to confidential treatment, and the EPA is required to make emissions data available to the public. Thus, emissions data will not be protected as CBI and will be made publicly available. You must submit the same file submitted to the CBI office with the CBI omitted to the EPA via the EPA's CDX as described earlier in this paragraph (h)(2).

(i) The preferred method to receive CBI is for it to be transmitted electronically using email attachments, File Transfer Protocol, or other online file sharing services. Electronic submissions must be transmitted directly to the OAQPS CBI Office at the email address <u>oaqpscbi@epa.gov</u>, and as described in <u>paragraph (h)(2)</u> of this section, should include clear CBI markings and be flagged to the attention of the Reciprocating Internal Combustion Engine Sector Lead. If assistance is needed with submitting large electronic files that exceed the file size limit for email attachments, and if you do not have your own file sharing service, please email <u>oaqpscbi@epa.gov</u> to request a file transfer link.

(ii) If you cannot transmit the file electronically, you may send CBI information through the postal service to the following address: OAQPS Document Control Officer (C404-02), OAQPS, U.S. Environmental Protection Agency, 109 T.W. Alexander Drive, P.O. Box 12055, Research Triangle Park, North Carolina 27711, Attention Reciprocating Internal Combustion Engine Sector Lead. The mailed CBI material should be double wrapped and clearly marked. Any CBI markings should not show through the outer envelope.

(i) If you own or operate an existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions that is certified to the Tier 1 or Tier 2 emission standards in Table 1 of  $\frac{40 \text{ CFR } 89.112}{40 \text{ CFR } 89.112}$  and subject to an enforceable state or local standard requiring engine replacement and you intend to meet management practices rather than emission limits, as specified in § 63.6603(d), you must submit a notification by March 3, 2013, stating that you intend to use the provision in § 63.6603(d) and identifying the state or local regulation that the engine is subject to.

[<u>73 FR 3606</u>, Jan. 18, 2008, as amended at <u>75 FR 9677</u>, Mar. 3, 2010; <u>75 FR 51591</u>, Aug. 20, 2010; <u>78 FR 6705</u>, Jan. 30, 2013; <u>85 FR 73912</u>, Nov. 19, 2020; <u>89 FR 70516</u>, Aug. 30, 2024]

# § 63.6650 What reports must I submit and when?

(a) You must submit each report in Table 7 of this subpart that applies to you.

(b) Unless the Administrator has approved a different schedule for submission of reports under  $\frac{63.10(a)}{(b)(1)}$ , you must submit each report by the date in Table 7 of this subpart and according to the requirements in <u>paragraphs (b)(1)</u> through (b)(9) of this section.

(1) For semiannual Compliance reports, the first Compliance report must cover the period beginning on the compliance date that is specified for your affected source in  $\S$  63.6595 and ending on June 30 or December 31, whichever date is the first date following the end of the first calendar half after the compliance date that is specified for your source in  $\S$  63.6595.

(2) For semiannual Compliance reports, the first Compliance report must be postmarked or delivered no later than July 31 or January 31, whichever date follows the end of the first calendar half after the compliance date that is specified for your affected source in  $\frac{63.6595}{5}$ .

(3) For semiannual Compliance reports, each subsequent Compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31.

(4) For semiannual Compliance reports, each subsequent Compliance report must be postmarked or delivered no later than July 31 or January 31, whichever date is the first date following the end of the semiannual reporting period.

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(6) For annual Compliance reports, the first Compliance report must cover the period beginning on the compliance date that is specified for your affected source in  $\S$  63.6595 and ending on December 31.

(7) For annual Compliance reports, the first Compliance report must be postmarked or delivered no later than January 31 following the end of the first calendar year after the compliance date that is specified for your affected source in  $\frac{\& 63.6595}{\& 63.6595}$ .

(8) For annual Compliance reports, each subsequent Compliance report must cover the annual reporting period from January 1 through December 31.

(9) For annual Compliance reports, each subsequent Compliance report must be postmarked or delivered no later than January 31.

(c) The Compliance report must contain the information in <u>paragraphs (c)(1)</u> through (8) of this section.

(1) Company name and address.

(2) Statement by a responsible official, with that official's name, title, and signature, certifying the accuracy of the content of the report.

(3) Date of report and beginning and ending dates of the reporting period.

(4) If you had a malfunction during the reporting period, the compliance report must include the starting and ending date and time, the duration (in hours), and a brief description for each malfunction which occurred during the reporting period and which caused or may have caused any applicable emission limitation to be exceeded. The report must also include a description of actions taken by an owner or operator during a malfunction of an affected source to minimize emissions in accordance with  $\S$  <u>63.6605(b)</u>, including actions taken to correct a malfunction.

(5) If there are no deviations from any emission or operating limitations that apply to you, a statement that there were no deviations from the emission or operating limitations during the reporting period.

(6) If there were no periods during which the continuous monitoring system (CMS), including CEMS and CPMS, was out-of-control, as specified in  $\frac{63.8(c)(7)}{1000}$ , a statement that there were no periods during which the CMS was out-of-control during the reporting period.

(7) Engine site rating in brake HP, year construction of the engine commenced (as defined in <u>§ 63.2</u>, where the exact year is not known, provide the best estimate), and type of engine (CI, SI 2SLB, SI 4SLB, or SI 4SRB).

(8) Latitude and longitude of the engine in decimal degrees reported to the fifth decimal place.

(9) An engine can be claimed as exempt from reporting coordinates (latitude/longitude) via CEDRI if:

(i) During the reporting period, the engine will be owned by, or operated by or for, an agency of the Federal Government responsible for national defense; and

(ii) The agency determines that disclosing the coordinates to the general public would be a threat to national security.

(d) For each deviation from an emission or operating limitation that occurs for a stationary RICE where you are not using a CMS to comply with the emission or operating limitations in this subpart, the Compliance report must contain the information in <u>paragraphs (c)(1)</u> through (8) of this section and the information in <u>paragraphs (d)(1)</u> and (2) of this section.

(1) The total operating time (in hours) of the stationary RICE at which the deviation occurred during the reporting period.

(2) Information on the number, duration (in hours), and cause of deviations (including unknown cause, if applicable), as applicable, and the corrective action taken.

(3) A description of any changes in processes, or controls since the last reporting period.

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(e) For each deviation from an emission or operating limitation occurring for a stationary RICE where you are using a CMS to comply with the emission and operating limitations in this subpart, you must include information in <u>paragraphs</u> (c)(1) through (8) and (e)(1) through (13) of this section.

(1) The date and time that each malfunction started and stopped.

(2) The start and end date and time and the duration (in hours) that each CMS was inoperative, except for zero (low-level) and high-level checks.

(3) The start and end date and time and the duration (in hours) that each CMS was out-of-control, including the information in  $\frac{63.8(c)(8)}{2}$ .

(4) The date and time that each deviation started and stopped, and whether each deviation occurred during a period of malfunction or during another period.

(5) A summary of the total duration (in hours) of the deviation during the reporting period, and the total duration as a percent of the total source operating time during that reporting period.

(6) A breakdown of the total duration (in hours) of the deviations during the reporting period into those that are due to control equipment problems, process problems, other known causes, and other unknown causes.

(7) A summary of the total duration (in hours) of CMS downtime during the reporting period, and the total duration of CMS downtime as a percent of the total operating time of the stationary RICE at which the CMS downtime occurred during that reporting period.

(8) An identification of each parameter and pollutant (CO or formaldehyde) that was monitored at the stationary RICE.

(9) [Reserved]

(10) A brief description of the CMS.

(11) The date of the latest CMS certification or audit.

(12) A description of any changes in CMS, processes, or controls since the last reporting period.

(13) The total operating time of the stationary RICE at which the deviation occurred during the reporting period.

(f) Each affected source that has obtained a title V operating permit pursuant to 40 CFR part 70 or 71 must report all deviations as defined in this subpart in the semiannual monitoring report required by 40 CFR 70.6 (a)(3)(iii)(A) or 40 CFR 71.6(a)(3)(iii)(A). If an affected source submits a Compliance report pursuant to table 7 of this subpart along with, or as part of, the semiannual monitoring report required by 40 CFR 71.6(a)(3)(iii)(A), and the Compliance report includes all required information concerning deviations from any emission or operating limitation in this subpart, submission of the Compliance report shall be deemed to satisfy any obligation to report the same deviations in the semiannual monitoring report. However, submission of a Compliance report shall not otherwise affect any obligation the affected source may have to report deviations from permit requirements to the permit authority. Beginning on February 26, 2025, the semiannual and annual compliance report required in table 7 of this subpart must be submitted according to paragraph (i) of this section. Only those elements required under this subpart are required to be submitted according to paragraph (i) of this section.

(g) If you are operating as a new or reconstructed stationary RICE which fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, you must submit an annual report according to Table 7 of this subpart by the date specified unless the Administrator has approved a different schedule, according to the information described in <u>paragraphs (b)(1)</u> through (b)(5) of this section. You must report the data specified in (g)(1) through (g)(3) of this section.

(1) Fuel flow rate of each fuel and the heating values that were used in your calculations. You must also demonstrate that the percentage of heat input provided by landfill gas or digester gas is equivalent to 10 percent or more of the total fuel consumption on an annual basis.

(2) The operating limits provided in your federally enforceable permit, and any deviations from these limits.

(3) Any problems or errors suspected with the meters.

(h) If you own or operate an emergency stationary RICE with a site rating of more than 100 brake HP that operates for the purpose specified in § 63.6640(f)(4)(ii), you must submit an annual report according to the requirements in <u>paragraphs</u> (h)(1) through (3) of this section.

(1) The report must contain the following information:

(i) Company name and address where the engine is located.

(ii) Date of the report and beginning and ending dates of the reporting period.

(iii) Engine site rating in brake HP, year construction of the engine commenced (as defined in <u>§ 63.2</u>, where the exact year is not known, provide the best estimate), and type of engine (CI, SI 2SLB, SI 4SLB, or SI 4SRB).

(iv) Latitude and longitude of the engine in decimal degrees reported to the fifth decimal place.

(v)-(vi) [Reserved]

(vii) Hours spent for operation for the purpose specified in  $\S 63.6640(f)(4)(ii)$ , including the date, start time, and end time for engine operation for the purposes specified in  $\S 63.6640(f)(4)(ii)$ . The report must also identify the entity that dispatched the engine and the situation that necessitated the dispatch of the engine.

(viii) If there were no deviations from the fuel requirements in  $\S$  <u>63.6604</u> that apply to the engine (if any), a statement that there were no deviations from the fuel requirements during the reporting period.

(ix) If there were deviations from the fuel requirements in  $\S 63.6604$  that apply to the engine (if any), information on the number, duration (in hours), and cause of deviations, and the corrective action taken.

(2) The first annual report must cover the calendar year 2015 and must be submitted no later than March 31, 2016. Subsequent annual reports for each calendar year must be submitted no later than March 31 of the following calendar year.

(3) Before February 26, 2025, the annual report must be submitted electronically using the subpart specific reporting form in the Compliance and Emissions Data Reporting Interface (CEDRI) that is accessed through EPA's Central Data Exchange (CDX) (<u>https://cdx.epa.gov/</u>). However, if the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, the written report must be submitted to the Administrator at the appropriate address listed in <u>§ 63.13</u>. Beginning on February 26, 2025, the annual report must be submitted according to <u>paragraph (i)</u> of this section.

(i) Beginning on February 26, 2025 for the annual report specified in § 63.6650(h) and February 26, 2025 or one year after the report becomes available in CEDRI, whichever is later for all other semiannual or annual reports, submit all semiannual and annual subsequent compliance reports using the appropriate electronic report template on the CEDRI website (https://www.epa.gov/electronic-reporting-air-emissions/cedri) for this subpart and following the procedure specified in § 63.9(k), except any CBI must be submitted according to the procedures in § 63.6645(h). The date report templates become available will be listed on the CEDRI website. Unless the Administrator or delegated state agency or other authority has approved a different schedule for submission of reports, the report must be submitted by the deadline specified in this subpart, regardless of the method in which the report is submitted.

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>75 FR 9677</u>, Mar. 3, 2010; <u>78 FR 6705</u>, Jan. 30, 2013; <u>87 FR 48607</u>, Aug. 10, 2022; <u>89 FR 70517</u>, Aug. 30, 2024]

# § 63.6655 What records must I keep?

(a) If you must comply with the emission and operating limitations, you must keep the records described in <u>paragraphs</u> (a)(1) through (a)(5), (b)(1) through (b)(3) and (c) of this section.

(1) A copy of each notification and report that you submitted to comply with this subpart, including all documentation supporting any Initial Notification or Notification of Compliance Status that you submitted, according to the requirement in  $\frac{5}{63.10(b)(2)(xiv)}$ .

(2) Records of the occurrence and duration (in hours) of each malfunction of operation (*i.e.*, process equipment) or the air pollution control and monitoring equipment.

(3) Records of performance tests and performance evaluations as required in § 63.10(b)(2)(viii).

(4) Records of all required maintenance performed on the air pollution control and monitoring equipment.

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(5) Records of actions taken during periods of malfunction to minimize emissions in accordance with  $\S$  <u>63.6605(b)</u>, including corrective actions to restore malfunctioning process and air pollution control and monitoring equipment to its normal or usual manner of operation.

(b) For each CEMS or CPMS, you must keep the records listed in <u>paragraphs (b)(1)</u> through (3) of this section.

(1) Records described in  $\S 63.10(b)(2)(vi)$  through (xi).

(2) Previous (*i.e.*, superseded) versions of the performance evaluation plan as required in  $\frac{63.8(d)(3)}{2}$ .

(3) Requests for alternatives to the relative accuracy test for CEMS or CPMS as required in  $\frac{63.8(f)(6)(i)}{5.6}$ , if applicable.

(c) If you are operating a new or reconstructed stationary RICE which fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, you must keep the records of your daily fuel usage monitors.

(d) You must keep the records required in Table 6 of this subpart to show continuous compliance with each emission or operating limitation that applies to you.

(e) You must keep records of the maintenance conducted on the stationary RICE in order to demonstrate that you operated and maintained the stationary RICE and after-treatment control device (if any) according to your own maintenance plan if you own or operate any of the following stationary RICE;

(1) An existing stationary RICE with a site rating of less than 100 brake HP located at a major source of HAP emissions.

(2) An existing stationary emergency RICE.

(3) An existing stationary RICE located at an area source of HAP emissions subject to management practices as shown in Table 2d to this subpart.

(f) If you own or operate any of the stationary RICE in <u>paragraphs (f)(1)</u> through (2) of this section, you must keep records of the hours of operation of the engine that is recorded through the non-resettable hour meter. The owner or operator must document how many hours are spent for emergency operation, including what classified the operation as emergency and how many hours are spent for non-emergency operation. If the engine is used for the purpose specified in  $\frac{63.6640(f)(4)(ii)}{10}$ , the owner or operator must keep records of the notification of the emergency situation, and the date, start time, and end time of engine operation for these purposes.

(1) An existing emergency stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions that does not meet the standards applicable to non-emergency engines.

(2) An existing emergency stationary RICE located at an area source of HAP emissions that does not meet the standards applicable to non-emergency engines.

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>75 FR 9678</u>, Mar. 3, 2010; <u>75 FR 51592</u>, Aug. 20, 2010; <u>78 FR 6706</u>, Jan. 30, 2013; <u>87 FR 48607</u>, Aug. 10, 2022; <u>89 FR 70518</u>, Aug. 30, 2024]

# § 63.6660 In what form and how long must I keep my records?

(a) Your records must be in a form suitable and readily available for expeditious review according to  $\frac{63.10(b)(1)}{10.000}$ .

(b) As specified in  $\S$  63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.

(c) You must keep each record readily accessible in hard copy or electronic form for at least 5 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to  $\frac{63.10(b)(1)}{2}$ .

[69 FR 33506, June 15, 2004, as amended at 75 FR 9678, Mar. 3, 2010]

# **Other Requirements and Information**

# § 63.6665 What parts of the General Provisions apply to me?

Table 8 to this subpart shows which parts of the General Provisions in <u>§§ 63.1</u> through <u>63.15</u> apply to you. If you own or operate a new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions (except new or reconstructed 4SLB engines greater than or equal to 250 and less than or equal to 500 brake HP), a new or reconstructed stationary RICE located at an area source of HAP emissions, or any of the following

RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with any of the requirements of the General Provisions specified in Table 8: An existing 2SLB stationary RICE, an existing 4SLB stationary RICE, an existing stationary RICE that combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, an existing emergency stationary RICE, or an existing limited use stationary RICE. If you own or operate any of the following RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the requirements in the General Provisions specified in Table 8 except for the initial notification requirements: A new stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, a new emergency stationary RICE, or a new limited use stationary RICE.

# [<u>75 FR 9678</u>, Mar. 3, 2010]

# § 63.6670 Who implements and enforces this subpart?

(a) This subpart is implemented and enforced by the U.S. EPA, or a delegated authority such as your State, local, or tribal agency. If the U.S. EPA Administrator has delegated authority to your State, local, or tribal agency, then that agency (as well as the U.S. EPA) has the authority to implement and enforce this subpart. You should contact your U.S. EPA Regional Office to find out whether this subpart is delegated to your State, local, or tribal agency.

- (c) The authorities that will not be delegated to State, local, or tribal agencies are:
- (1) Approval of alternatives to the non-opacity emission limitations and operating limitations in  $\frac{63.6600}{2}$  under  $\frac{63.6600}{2}$ .
- (2) Approval of major alternatives to test methods under  $\S 63.7(e)(2)(ii)$  and (f) and as defined in  $\S 63.90$ .
- (3) Approval of major alternatives to monitoring under  $\frac{63.8(f)}{10}$  and as defined in  $\frac{63.90}{10}$ .
- (4) Approval of major alternatives to recordkeeping and reporting under  $\frac{63.10(f)}{10}$  and as defined in  $\frac{63.90}{10}$ .
- (5) Approval of a performance test which was conducted prior to the effective date of the rule, as specified in <u>§ 63.6610(b)</u>.
- (6) Approval of an alternative to any electronic reporting to the EPA required by this subpart.

[69 FR 33506, June 15, 2004, as amended at 89 FR 70518, Aug. 30, 2024]

# § 63.6675 What definitions apply to this subpart?

Terms used in this subpart are defined in the Clean Air Act (CAA); in <u>40 CFR 63.2</u>, the General Provisions of this part; and in this section as follows:

*Alaska Railbelt Grid* means the service areas of the six regulated public utilities that extend from Fairbanks to Anchorage and the Kenai Peninsula. These utilities are Golden Valley Electric Association; Chugach Electric Association; Matanuska Electric Association; Homer Electric Association; Anchorage Municipal Light & Power; and the City of Seward Electric System.

Area source means any stationary source of HAP that is not a major source as defined in part 63.

Associated equipment as used in this subpart and as referred to in section 112(n)(4) of the CAA, means equipment associated with an oil or natural gas exploration or production well, and includes all equipment from the well bore to the point of custody transfer, except glycol dehydration units, storage vessels with potential for flash emissions, combustion turbines, and stationary RICE.

*Backup power for renewable energy* means an engine that provides backup power to a facility that generates electricity from renewable energy resources, as that term is defined in Alaska Statute 42.45.045(l)(5) (incorporated by reference, see § 63.14).

Black start engine means an engine whose only purpose is to start up a combustion turbine.

CAA means the Clean Air Act (42 U.S.C. 7401 et seq., as amended by Public Law 101-549, 104 Stat. 2399).

*Commercial emergency stationary RICE* means an emergency stationary RICE used in commercial establishments such as office buildings, hotels, stores, telecommunications facilities, restaurants, financial institutions such as banks, doctor's offices, and sports and performing arts facilities.

Compression ignition means relating to a type of stationary internal combustion engine that is not a spark ignition engine.

*Custody transfer* means the transfer of hydrocarbon liquids or natural gas: After processing and/or treatment in the producing operations, or from storage vessels or automatic transfer facilities or other such equipment, including product loading racks, to pipelines or any other forms of transportation. For the purposes of this subpart, the point at which such liquids or natural gas enters a natural gas processing plant is a point of custody transfer.

Deviation means any instance in which an affected source subject to this subpart, or an owner or operator of such a source:

(1) Fails to meet any requirement or obligation established by this subpart, including but not limited to any emission limitation or operating limitation;

(2) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart and that is included in the operating permit for any affected source required to obtain such a permit; or

(3) Fails to meet any emission limitation or operating limitation in this subpart during malfunction, regardless or whether or not such failure is permitted by this subpart.

(4) Fails to satisfy the general duty to minimize emissions established by  $\frac{63.6(e)(1)(i)}{2}$ .

*Diesel engine* means any stationary RICE in which a high boiling point liquid fuel injected into the combustion chamber ignites when the air charge has been compressed to a temperature sufficiently high for auto-ignition. This process is also known as compression ignition.

*Diesel fuel* means any liquid obtained from the distillation of petroleum with a boiling point of approximately 150 to 360 degrees Celsius. One commonly used form is fuel oil number 2. Diesel fuel also includes any non-distillate fuel with comparable physical and chemical properties (*e.g.* biodiesel) that is suitable for use in compression ignition engines.

*Digester gas* means any gaseous by-product of wastewater treatment typically formed through the anaerobic decomposition of organic waste materials and composed principally of methane and CO<sub>2</sub>.

*Dual-fuel engine* means any stationary RICE in which a liquid fuel (typically diesel fuel) is used for compression ignition and gaseous fuel (typically natural gas) is used as the primary fuel.

*Emergency stationary RICE* means any stationary reciprocating internal combustion engine that meets all of the criteria in paragraphs (1) through (3) of this definition. All emergency stationary RICE must comply with the requirements specified in  $\S$  63.6640(f) in order to be considered emergency stationary RICE. If the engine does not comply with the requirements specified in  $\S$  63.6640(f), then it is not considered to be an emergency stationary RICE under this subpart.

(1) The stationary RICE is operated to provide electrical power or mechanical work during an emergency situation. Examples include stationary RICE used to produce power for critical networks or equipment (including power supplied to portions of a facility) when electric power from the local utility (or the normal power source, if the facility runs on its own power production) is interrupted, or stationary RICE used to pump water in the case of fire or flood, etc.

(2) The stationary RICE is operated under limited circumstances for situations not included in paragraph (1) of this definition, as specified in  $\S 63.6640(f)$ .

(3) The stationary RICE operates as part of a financial arrangement with another entity in situations not included in paragraph (1) of this definition only as allowed in  $\frac{63.6640(f)(4)(i)}{10}$  or (ii).

*Engine startup* means the time from initial start until applied load and engine and associated equipment reaches steady state or normal operation. For stationary engine with catalytic controls, engine startup means the time from initial start until applied load and engine and associated equipment, including the catalyst, reaches steady state or normal operation.

*Four-stroke engine* means any type of engine which completes the power cycle in two crankshaft revolutions, with intake and compression strokes in the first revolution and power and exhaust strokes in the second revolution.

*Gaseous fuel* means a material used for combustion which is in the gaseous state at standard atmospheric temperature and pressure conditions.

*Gasoline* means any fuel sold in any State for use in motor vehicles and motor vehicle engines, or nonroad or stationary engines, and commonly or commercially known or sold as gasoline.

*Glycol dehydration unit* means a device in which a liquid glycol (including, but not limited to, ethylene glycol, diethylene glycol, or triethylene glycol) absorbent directly contacts a natural gas stream and absorbs water in a contact tower or absorption column (absorber). The glycol contacts and absorbs water vapor and other gas stream constituents from the natural gas and becomes "rich" glycol. This glycol is then regenerated in the glycol dehydration unit reboiler. The "lean" glycol is then recycled.

Hazardous air pollutants (HAP) means any air pollutants listed in or pursuant to section 112(b) of the CAA.

*Institutional emergency stationary RICE* means an emergency stationary RICE used in institutional establishments such as medical centers, nursing homes, research centers, institutions of higher education, correctional facilities, elementary and secondary schools, libraries, religious establishments, police stations, and fire stations.

*ISO standard day conditions* means 288 degrees Kelvin (15 degrees Celsius), 60 percent relative humidity and 101.3 kilopascals pressure.

*Landfill gas* means a gaseous by-product of the land application of municipal refuse typically formed through the anaerobic decomposition of waste materials and composed principally of methane and CO<sub>2</sub>.

Lean burn engine means any two-stroke or four-stroke spark ignited engine that does not meet the definition of a rich burn engine.

Limited use stationary RICE means any stationary RICE that operates less than 100 hours per year.

*Liquefied petroleum gas* means any liquefied hydrocarbon gas obtained as a by-product in petroleum refining of natural gas production.

*Liquid fuel* means any fuel in liquid form at standard temperature and pressure, including but not limited to diesel, residual/crude oil, kerosene/naphtha (jet fuel), and gasoline.

Major Source, as used in this subpart, shall have the same meaning as in § 63.2, except that:

(1) Emissions from any oil or gas exploration or production well (with its associated equipment (as defined in this section)) and emissions from any pipeline compressor station or pump station shall not be aggregated with emissions from other similar units, to determine whether such emission points or stations are major sources, even when emission points are in a contiguous area or under common control;

(2) For oil and gas production facilities, emissions from processes, operations, or equipment that are not part of the same oil and gas production facility, as defined in  $\S$  63.1271 of subpart HHH of this part, shall not be aggregated;

(3) For production field facilities, only HAP emissions from glycol dehydration units, storage vessel with the potential for flash emissions, combustion turbines and reciprocating internal combustion engines shall be aggregated for a major source determination; and

(4) Emissions from processes, operations, and equipment that are not part of the same natural gas transmission and storage facility, as defined in <u>§ 63.1271</u> of <u>subpart HHH of this part</u>, shall not be aggregated.

*Malfunction* means any sudden, infrequent, and not reasonably preventable failure of air pollution control equipment, process equipment, or a process to operate in a normal or usual manner which causes, or has the potential to cause, the emission limitations in an applicable standard to be exceeded. Failures that are caused in part by poor maintenance or careless operation are not malfunctions.

*Natural gas* means a naturally occurring mixture of hydrocarbon and non-hydrocarbon gases found in geologic formations beneath the Earth's surface, of which the principal constituent is methane. Natural gas may be field or pipeline quality.

*Non-selective catalytic reduction (NSCR)* means an add-on catalytic nitrogen oxides (NO<sub>X</sub>) control device for rich burn engines that, in a two-step reaction, promotes the conversion of excess oxygen, NO<sub>X</sub>, CO, and volatile organic compounds (VOC) into CO<sub>2</sub>, nitrogen, and water.

*Oil and gas production facility* as used in this subpart means any grouping of equipment where hydrocarbon liquids are processed, upgraded (*i.e.*, remove impurities or other constituents to meet contract specifications), or stored prior to the point

of custody transfer; or where natural gas is processed, upgraded, or stored prior to entering the natural gas transmission and storage source category. For purposes of a major source determination, facility (including a building, structure, or installation) means oil and natural gas production and processing equipment that is located within the boundaries of an individual surface site as defined in this section. Equipment that is part of a facility will typically be located within close proximity to other equipment located at the same facility. Pieces of production equipment or groupings of equipment located on different oil and gas leases, mineral fee tracts, lease tracts, subsurface or surface unit areas, surface fee tracts, surface lease tracts, or separate surface sites, whether or not connected by a road, waterway, power line or pipeline, shall not be considered part of the same facility. Examples of facilities in the oil and natural gas production source category include, but are not limited to, well sites, satellite tank batteries, central tank batteries, a compressor station that transports natural gas to a natural gas processing plant, and natural gas processing plants.

Oxidation catalyst means an add-on catalytic control device that controls CO and VOC by oxidation.

Peaking unit or engine means any standby engine intended for use during periods of high demand that are not emergencies.

*Percent load* means the fractional power of an engine compared to its maximum manufacturer's design capacity at engine site conditions. Percent load may range between 0 percent to above 100 percent.

Potential to emit means the maximum capacity of a stationary source to emit a pollutant under its physical and operational design. Any physical or operational limitation on the capacity of the stationary source to emit a pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored, or processed, shall be treated as part of its design if the limitation or the effect it would have on emissions is federally enforceable. For oil and natural gas production facilities subject to subpart HH of this part, the potential to emit provisions in  $\frac{63.760(a)}{2}$  may be used. For natural gas transmission and storage facilities subject to subpart HHH of this part, the maximum annual facility gas throughput for storage facilities may be determined according to  $\frac{63.1270(a)(1)}{2}$ .

Production field facility means those oil and gas production facilities located prior to the point of custody transfer.

Production well means any hole drilled in the earth from which crude oil, condensate, or field natural gas is extracted.

Propane means a colorless gas derived from petroleum and natural gas, with the molecular structure C<sub>3</sub>H<sub>8</sub>.

*Remote stationary RICE* means stationary RICE meeting any of the following criteria:

(1) Stationary RICE located in an offshore area that is beyond the line of ordinary low water along that portion of the coast of the United States that is in direct contact with the open seas and beyond the line marking the seaward limit of inland waters.

(2) Stationary RICE located on a pipeline segment that meets both of the criteria in paragraphs (2)(i) and (ii) of this definition.

(i) A pipeline segment with 10 or fewer buildings intended for human occupancy and no buildings with four or more stories within 220 yards (200 meters) on either side of the centerline of any continuous 1-mile (1.6 kilometers) length of pipeline. Each separate dwelling unit in a multiple dwelling unit building is counted as a separate building intended for human occupancy.

(ii) The pipeline segment does not lie within 100 yards (91 meters) of either a building or a small, well-defined outside area (such as a playground, recreation area, outdoor theater, or other place of public assembly) that is occupied by 20 or more persons on at least 5 days a week for 10 weeks in any 12-month period. The days and weeks need not be consecutive. The building or area is considered occupied for a full day if it is occupied for any portion of the day.

(iii) For purposes of this <u>paragraph (2)</u>, the term pipeline segment means all parts of those physical facilities through which gas moves in transportation, including but not limited to pipe, valves, and other appurtenance attached to pipe, compressor units, metering stations, regulator stations, delivery stations, holders, and fabricated assemblies. Stationary RICE located within 50 yards (46 meters) of the pipeline segment providing power for equipment on a pipeline segment are part of the pipeline segment. Transportation of gas means the gathering, transmission, or distribution of gas by pipeline, or the storage of gas. A building is intended for human occupancy if its primary use is for a purpose involving the presence of humans.

(3) Stationary RICE that are not located on gas pipelines and that have 5 or fewer buildings intended for human occupancy and no buildings with four or more stories within a 0.25 mile radius around the engine. A building is intended for human occupancy if its primary use is for a purpose involving the presence of humans.

*Residential emergency stationary RICE* means an emergency stationary RICE used in residential establishments such as homes or apartment buildings.

Responsible official means responsible official as defined in 40 CFR 70.2.

*Rich burn engine* means any four-stroke spark ignited engine where the manufacturer's recommended operating air/fuel ratio divided by the stoichiometric air/fuel ratio at full load conditions is less than or equal to 1.1. Engines originally manufactured as rich burn engines, but modified prior to December 19, 2002 with passive emission control technology for NO<sub>X</sub> (such as pre-combustion chambers) will be considered lean burn engines. Also, existing engines where there are no manufacturer's recommendations regarding air/fuel ratio will be considered a rich burn engine if the excess oxygen content of the exhaust at full load conditions is less than or equal to 2 percent.

Site-rated HP means the maximum manufacturer's design capacity at engine site conditions.

*Spark ignition* means relating to either: A gasoline-fueled engine; or any other type of engine with a spark plug (or other sparking device) and with operating characteristics significantly similar to the theoretical Otto combustion cycle. Spark ignition engines usually use a throttle to regulate intake air flow to control power during normal operation. Dual-fuel engines in which a liquid fuel (typically diesel fuel) is used for CI and gaseous fuel (typically natural gas) is used as the primary fuel at an annual average ratio of less than 2 parts diesel fuel to 100 parts total fuel on an energy equivalent basis are spark ignition engines.

Stationary reciprocating internal combustion engine (RICE) means any reciprocating internal combustion engine which uses reciprocating motion to convert heat energy into mechanical work and which is not mobile. Stationary RICE differ from mobile RICE in that a stationary RICE is not a non-road engine as defined at <u>40 CFR 1068.30</u>, and is not used to propel a motor vehicle or a vehicle used solely for competition.

Stationary RICE test cell/stand means an engine test cell/stand, as defined in subpart PPPPP of this part, that tests stationary RICE.

Stoichiometric means the theoretical air-to-fuel ratio required for complete combustion.

Storage vessel with the potential for flash emissions means any storage vessel that contains a hydrocarbon liquid with a stock tank gas-to-oil ratio equal to or greater than 0.31 cubic meters per liter and an American Petroleum Institute gravity equal to or greater than 40 degrees and an actual annual average hydrocarbon liquid throughput equal to or greater than 79,500 liters per day. Flash emissions occur when dissolved hydrocarbons in the fluid evolve from solution when the fluid pressure is reduced.

Subpart means <u>40 CFR part 63, subpart ZZZZ</u>.

*Surface site* means any combination of one or more graded pad sites, gravel pad sites, foundations, platforms, or the immediate physical location upon which equipment is physically affixed.

*Two-stroke engine* means a type of engine which completes the power cycle in single crankshaft revolution by combining the intake and compression operations into one stroke and the power and exhaust operations into a second stroke. This system requires auxiliary scavenging and inherently runs lean of stoichiometric.

[<u>69 FR 33506</u>, June 15, 2004, as amended at <u>71 FR 20467</u>, Apr. 20, 2006; <u>73 FR 3607</u>, Jan. 18, 2008; <u>75 FR 9679</u>, Mar. 3, 2010; <u>75 FR 51592</u>, Aug. 20, 2010; <u>76 FR 12867</u>, Mar. 9, 2011; <u>78 FR 6706</u>, Jan. 30, 2013; <u>87 FR 48608</u>, Aug. 10, 2022]

# Table 1a to Subpart ZZZZ of Part 63—Emission Limitations for Existing, New, and Reconstructed Spark Ignition, 4SRB Stationary RICE >500 HP Located at a Major Source of HAP Emissions

As stated in <u>§§ 63.6600</u> and <u>63.6640</u>, you must comply with the following emission limitations at 100 percent load plus or minus 10 percent for existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions:

For each ·	You must meet the following emission limitation, except during periods of startup	During periods of startup you must
1. 4SRB	a. Reduce formaldehyde emissions by 76 percent or	Minimize the engine's time spent at idle and minimize
stationary	more. If you commenced construction or reconstruction	the engine's startup time at startup to a period needed
RICE	between December 19, 2002 and June 15, 2004, you	for appropriate and safe loading of the engine, not to

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For each	You must meet the following emission limitation, except during periods of startup	During periods of startup you must	
	may reduce formaldehyde emissions by 75 percent or more until June 15, 2007 or	exceed 30 minutes, after which time the non-startup emission limitations apply. <sup>1</sup>	
	b. Limit the concentration of formaldehyde in the stationary RICE exhaust to 350 ppbvd or less at 15 percent $O_2$		
<sup>1</sup> Sources can petition the Administrator pursuant to the requirements of $\frac{40 \text{ CFR } 63.6(\text{g})}{1000}$ for alternative work practices.			

[75 FR 9679, Mar. 3, 2010, as amended at 75 FR 51592, Aug. 20, 2010]

# Table 1b to Subpart ZZZZ of Part 63—Operating Limitations for Existing, New, and Reconstructed SI 4SRB Stationary RICE >500 HP Located at a Major Source of HAP Emissions

As stated in \$ 63.6600, 63.6603, 63.6630 and 63.6640, you must comply with the following operating limitations for existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions:

For each	You must meet the following operating limitation, except during periods of startup
1. existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to reduce formaldehyde emissions by 76 percent or more (or by 75 percent or more, if applicable) and using NSCR; or existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust to 350 ppbvd or less at 15 percent $O_2$ and using NSCR;	a. maintain your catalyst so that the pressure drop across the catalyst does not change by more than 2 inches of water at 100 percent load plus or minus 10 percent from the pressure drop across the catalyst measured during the initial performance test; and b. maintain the temperature of your stationary RICE exhaust so that the catalyst inlet temperature is greater than or equal to 750 °F and less than or equal to 1250 °F. <sup>1</sup>
2. existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to reduce formaldehyde emissions by 76 percent or more (or by 75 percent or more, if applicable) and not using NSCR; or	Comply with any operating limitations approved by the Administrator.
existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust to 350 ppbvd or less at 15 percent $O_2$ and not using NSCR.	

<sup>1</sup> Sources can petition the Administrator pursuant to the requirements of <u>40 CFR 63.8(f)</u> for a different temperature range.

[78 FR 6706, Jan. 30, 2013]

# Table 2a to Subpart ZZZZ of Part 63—Emission Limitations for New and Reconstructed 2SLB and Compression Ignition Stationary RICE >500 HP and New and Reconstructed 4SLB Stationary RICE ≥250 HP Located at a Major Source of HAP Emissions

As stated in <u>§§ 63.6600</u> and <u>63.6640</u>, you must comply with the following emission limitations for new and reconstructed lean burn and new and reconstructed compression ignition stationary RICE at 100 percent load plus or minus 10 percent:

For each	You must meet the following emission limitation, except during periods of startup	During periods of startup you must
1.2SLB	a. Reduce CO emissions by 58 percent or more; or	Minimize the engine's time spent at idle and
stationary	b. Limit concentration of formaldehyde in the stationary RICE	minimize the engine's startup time at startup to a

For each	You must meet the following emission limitation, except during periods of startup	During periods of startup you must
RICE	exhaust to 12 ppmvd or less at 15 percent O <sub>2</sub> . If you commenced construction or reconstruction between December 19, 2002 and June 15, 2004, you may limit concentration of formaldehyde to 17 ppmvd or less at 15 percent O <sub>2</sub> until June 15, 2007	period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply. <sup>1</sup>
2. 4SLB stationary RICE	a. Reduce CO emissions by 93 percent or more; or	
	b. Limit concentration of formaldehyde in the stationary RICE exhaust to 14 ppmvd or less at 15 percent $O_2$	
3. CI stationary RICE	a. Reduce CO emissions by 70 percent or more; or	
	b. Limit concentration of formal dehyde in the stationary RICE exhaust to 580 ppbvd or less at 15 percent $O_2$	
<sup>1</sup> Sources car	1 petition the Administrator pursuant to the requirements of $\frac{40}{40}$	CFR 63.6(g) for alternative work practices.

# [<u>75 FR 9680</u>, Mar. 3, 2010]

# Table 2b to Subpart ZZZZ of Part 63—Operating Limitations for New and Reconstructed 2SLB and CI Stationary RICE >500 HP Located at a Major Source of HAP Emissions, New and Reconstructed 4SLB Stationary RICE ≥250 HP Located at a Major Source of HAP Emissions, Existing CI Stationary RICE >500 HP

As stated in <u>§§ 63.6600</u>, <u>63.6601</u>, <u>63.6603</u>, <u>63.6630</u>, and <u>63.6640</u>, you must comply with the following operating limitations for new and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions; new and reconstructed 4SLB stationary RICE  $\geq$ 250 HP located at a major source of HAP emissions; and existing CI stationary RICE  $\geq$ 500 HP:

For each	You must meet the following operating limitation, except during periods of startup
1. New and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE $\geq$ 250 HP located at a major source of HAP emissions complying with the requirement to reduce CO emissions and using an oxidation catalyst; and New and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE $\geq$ 250 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust and using an oxidation catalyst.	a. maintain your catalyst so that the pressure drop across the catalyst does not change by more than 2 inches of water at 100 percent load plus or minus 10 percent from the pressure drop across the catalyst that was measured during the initial performance test; and b. maintain the temperature of your stationary RICE exhaust so that the catalyst inlet temperature is greater than or equal to 450 °F and less than or equal to 1350 °F. <sup>1</sup>
2. Existing CI stationary RICE >500 HP complying with the requirement to limit or reduce the concentration of CO in the stationary RICE exhaust and using an oxidation catalyst	a. maintain your catalyst so that the pressure drop across the catalyst does not change by more than 2 inches of water from the pressure drop across the catalyst that was measured during the initial performance test; and
	b. maintain the temperature of your stationary RICE exhaust so that the catalyst inlet temperature is greater than or equal to 450 °F and less than or equal to 1350 °F. <sup>1</sup>

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For each	You must meet the following operating limitation, except during periods of startup	
3. New and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE $\geq$ 250 HP located at a major source of HAP emissions complying with the requirement to reduce CO emissions and not using an oxidation catalyst; and	Comply with any operating limitations approved by the Administrator.	
New and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE $\geq$ 250 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust and not using an oxidation catalyst; and		
existing CI stationary RICE >500 HP complying with the requirement to limit or reduce the concentration of CO in the stationary RICE exhaust and not using an oxidation catalyst.		
<sup>1</sup> Sources can petition the Administrator pursuant to the requirements of 40 CFR 63.8(f) for a different temperature range.		

# [78 FR 6707, Jan. 30, 2013]

# Table 2c to Subpart ZZZZ of Part 63—Requirements for Existing Compression Ignition Stationary RICE Located at a Major Source of HAP Emissions and Existing Spark Ignition Stationary RICE ≤500 HP Located at a Major Source of HAP Emissions

As stated in <u>§§ 63.6600</u>, <u>63.6602</u>, and <u>63.6640</u>, you must comply with the following requirements for existing compression ignition stationary RICE located at a major source of HAP emissions and existing spark ignition stationary RICE  $\leq$  500 HP located at a major source of HAP emissions

For each	You must meet the following requirement, except during periods of startup	During periods of startup you must
1. Emergency stationary CI RICE and black start stationary CI RICE <sup>1</sup>	<ul> <li>a. Change oil and filter every 500 hours of operation or within 1 year + 30 days of the previous change, whichever comes first<sup>2</sup>.</li> <li>b. Inspect air cleaner every 1,000 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary;</li> </ul>	Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply. <sup>3</sup>
	c. Inspect all hoses and belts every 500 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary <sup>3</sup>	
2. Non-Emergency, non-black start stationary CI RICE <100 HP	a. Change oil and filter every 1,000 hours of operation or within 1 year + 30 days of the previous change, whichever comes first <sup>2</sup> .	
	b. Inspect air cleaner every 1,000 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace	

For each	You must meet the following requirement, except during periods of startup	During periods of startup you must
	as necessary;	
	c. Inspect all hoses and belts every 500 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary <sup>3</sup>	
3. Non-Emergency, non-black start CI stationary RICE 100≤HP≤300 HP	Limit concentration of CO in the stationary RICE exhaust to 230 ppmvd or less at 15 percent O <sub>2</sub>	
4. Non-Emergency, non-black start CI stationary RICE 300 <hp≤500< td=""><td>a. Limit concentration of CO in the stationary RICE exhaust to 49 ppmvd or less at 15 percent O<sub>2</sub>; or</td><td></td></hp≤500<>	a. Limit concentration of CO in the stationary RICE exhaust to 49 ppmvd or less at 15 percent O <sub>2</sub> ; or	
	b. Reduce CO emissions by 70 percent or more	
5. Non-Emergency, non-black start stationary CI RICE >500 HP	a. Limit concentration of CO in the stationary RICE exhaust to 23 ppmvd or less at 15 percent O <sub>2</sub> ; or	
	b. Reduce CO emissions by 70 percent or more	
6. Emergency stationary SI RICE and black start stationary SI RICE. <sup>1</sup>	a. Change oil and filter every 500 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>2</sup>	
	b. Inspect spark plugs every 1,000 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary;	
	c. Inspect all hoses and belts every 500 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary <sup>3</sup>	
7. Non-Emergency, non-black start stationary SI RICE <100 HP that are not 2SLB stationary RICE	a. Change oil and filter every 1,440 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>2</sup>	
	b. Inspect spark plugs every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
	c. Inspect all hoses and belts every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary <sup>3</sup>	

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For each	You must meet the following requirement, except during periods of startup	During periods of startup you must	
8. Non-Emergency, non-black start 2SLB stationary SI RICE <100 HP	a. Change oil and filter every 4,320 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>2</sup>		
	b. Inspect spark plugs every 4,320 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary;		
	c. Inspect all hoses and belts every 4,320 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary <sup>3</sup>		
9. Non-emergency, non-black start 2SLB stationary RICE 100≤HP≤500	Limit concentration of CO in the stationary RICE exhaust to 225 ppmvd or less at 15 percent O <sub>2</sub>		
10. Non-emergency, non-black start 4SLB stationary RICE 100≤HP≤500	Limit concentration of CO in the stationary RICE exhaust to 47 ppmvd or less at 15 percent O <sub>2</sub>		
11. Non-emergency, non-black start 4SRB stationary RICE 100≤HP≤500	Limit concentration of formaldehyde in the stationary RICE exhaust to 10.3 ppmvd or less at 15 percent O <sub>2</sub>		
12. Non-emergency, non-black start stationary RICE 100≤HP≤500 which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis	Limit concentration of CO in the stationary RICE exhaust to 177 ppmvd or less at 15 percent O <sub>2</sub>		
<sup>1</sup> If an emergency engine is operating d	<sup>1</sup> If an emergency engine is operating during an emergency and it is not possible to shut down the engine in order to perform		

<sup>1</sup> If an emergency engine is operating during an emergency and it is not possible to shut down the engine in order to perform the work practice requirements on the schedule required in table 2c of this subpart, or if performing the work practice on the required schedule would otherwise pose an unacceptable risk under Federal, state, or local law, the work practice can be delayed until the emergency is over or the unacceptable risk under Federal, state, or local law has abated. The work practice should be performed as soon as practicable after the emergency has ended or the unacceptable risk under Federal, state, or local law has abated. Sources must report any failure to perform the work practice on the schedule required and the Federal, state or local law under which the risk was deemed unacceptable.

<sup>2</sup> Sources have the option to utilize an oil analysis program as described in  $\S$  <u>63.6625(i)</u> or <u>(j)</u> in order to extend the specified oil change requirement in table 2c of this subpart.

<sup>3</sup> Sources can petition the Administrator pursuant to the requirements of <u>40 CFR 63.6(g)</u> for alternative work practices.

# [<u>89 FR 70518</u>, Aug. 30, 2024]

# Table 2d to Subpart ZZZZ of Part 63—Requirements for Existing Stationary RICE Located at Area Sources of HAP Emissions

As stated in \$ 63.6603 and 63.6640, you must comply with the following requirements for existing stationary RICE located at area sources of HAP emissions:

For each	You must meet the following requirement, except during periods of startup	During periods of startup you must
1. Non-Emergency, non-black start CI stationary RICE ≤300 HP	<ul> <li>a. Change oil and filter every 1,000 hours of operation or within 1 year + 30 days of the previous change, whichever comes first;<sup>1</sup></li> <li>b. Inspect air cleaner every 1,000 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary;</li> </ul>	Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply.
	c. Inspect all hoses and belts every 500 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
2. Non-Emergency, non-black start CI stationary RICE 300 <hp<500< td=""><td>a. Limit concentration of CO in the stationary RICE exhaust to 49 ppmvd at 15 percent <math>O_2</math>; or</td><td></td></hp<500<>	a. Limit concentration of CO in the stationary RICE exhaust to 49 ppmvd at 15 percent $O_2$ ; or	
	b. Reduce CO emissions by 70 percent or more	
3. Non-Emergency, non-black start CI stationary RICE >500 HP	a. Limit concentration of CO in the stationary RICE exhaust to 23 ppmvd at 15 percent $O_2$ ; or	
	b. Reduce CO emissions by 70 percent or more	
4. Emergency stationary CI RICE and black start stationary CI RICE. <sup>2</sup>	a. Change oil and filter every 500 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>1</sup>	
	b. Inspect air cleaner every 1,000 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and	
	c. Inspect all hoses and belts every 500 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
5. Emergency stationary SI RICE; black start stationary SI RICE; non-emergency, non-black start 4SLB stationary RICE >500 HP that operate 24 hours or less per calendar year; non- emergency, non-black start 4SRB stationary RICE >500 HP that operate 24 hours or less per	<ul> <li>a. Change oil and filter every</li> <li>500 hours of operation or within</li> <li>1 year + 30 days of the previous</li> <li>change, whichever comes first;<sup>1</sup></li> <li>b. Inspect spark plugs every</li> <li>1,000 hours of operation or</li> </ul>	

For each	You must meet the following requirement, except during periods of startup	During periods of startup you must
calendar year. <sup>2</sup>	within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and	
	c. Inspect all hoses and belts every 500 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
6. Non-emergency, non-black start 2SLB stationary RICE	a. Change oil and filter every 4,320 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>1</sup>	
	b. Inspect spark plugs every 4,320 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and	
	c. Inspect all hoses and belts every 4,320 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
7. Non-emergency, non-black start 4SLB stationary RICE ≤500 HP	a. Change oil and filter every 1,440 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>1</sup>	
	b. Inspect spark plugs every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and	
	c. Inspect all hoses and belts every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
8. Non-emergency, non-black start 4SLB remote stationary RICE >500 HP	a. Change oil and filter every 2,160 hours of operation or within 1 year + 30 days of the previous change, whichever	

For each	You must meet the following requirement, except during periods of startup	During periods of startup you must
	comes first; <sup>1</sup>	
	b. Inspect spark plugs every 2,160 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and	
	c. Inspect all hoses and belts every 2,160 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
9. Non-emergency, non-black start 4SLB stationary RICE >500 HP that are not remote stationary RICE and that operate more than 24 hours per calendar year	Install an oxidation catalyst to reduce HAP emissions from the stationary RICE	
10. Non-emergency, non-black start 4SRB stationary RICE ≤500 HP	a. Change oil and filter every 1,440 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>1</sup>	
	b. Inspect spark plugs every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and	
	c. Inspect all hoses and belts every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	
11. Non-emergency, non-black start 4SRB remote stationary RICE >500 HP	a. Change oil and filter every 2,160 hours of operation or within 1 year + 30 days of the previous change, whichever comes first; <sup>1</sup>	
	b. Inspect spark plugs every 2,160 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and	
	c. Inspect all hoses and belts every 2,160 hours of operation or within 1 year + 30 days of the	

For each	You must meet the following requirement, except during periods of startup	During periods of startup you must
	previous inspection, whichever comes first, and replace as necessary	
12. Non-emergency, non-black start 4SRB stationary RICE >500 HP that are not remote stationary RICE and that operate more than 24 hours per calendar year	Install NSCR to reduce HAP emissions from the stationary RICE	
13. Non-emergency, non-black start stationary RICE which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis	<ul> <li>a. Change oil and filter every 1,440 hours of operation or within 1 year + 30 days of the previous change, whichever comes first;<sup>1</sup></li> <li>b. Inspect spark plugs every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary; and</li> </ul>	
	c. Inspect all hoses and belts every 1,440 hours of operation or within 1 year + 30 days of the previous inspection, whichever comes first, and replace as necessary	

<sup>1</sup> Sources have the option to utilize an oil analysis program as described in  $\S$  <u>63.6625(i)</u> or <u>(j)</u> in order to extend the specified oil change requirement in table 2d of this subpart.

<sup>2</sup> If an emergency engine is operating during an emergency and it is not possible to shut down the engine in order to perform the management practice requirements on the schedule required in table 2d of this subpart, or if performing the management practice on the required schedule would otherwise pose an unacceptable risk under Federal, state, or local law, the management practice can be delayed until the emergency is over or the unacceptable risk under Federal, state, or local law has abated. The management practice should be performed as soon as practicable after the emergency has ended or the unacceptable risk under Federal, state, or local law has abated. Sources must report any failure to perform the management practice on the schedule required and the Federal, state or local law under which the risk was deemed unacceptable.

# [<u>89 FR 70520</u>, Aug. 30, 2024]

# Table 3 to Subpart ZZZZ of Part 63—Subsequent Performance Tests

As stated in <u>§§ 63.6615</u> and <u>63.6620</u>, you must comply with the following subsequent performance test requirements:

For each	Complying with the requirement to	You must
1. New or reconstructed 2SLB stationary RICE >500 HP located at major sources; new or reconstructed 4SLB stationary RICE >250 HP located at major sources; and new or reconstructed CI stationary RICE >500 HP located at major sources	Reduce CO emissions and not using a CEMS	Conduct subsequent performance tests semiannually. <sup>1</sup>
2. 4SRB stationary RICE $\geq$ 5,000 HP located at major sources	Reduce formaldehyde emissions	Conduct subsequent performance tests semiannually. <sup>1</sup>

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For each	Complying with the requirement to	You must
3. Stationary RICE >500 HP located at major sources and new or reconstructed 4SLB stationary RICE 250≤HP≤500 located at major sources	Limit the concentration of formaldehyde in the stationary RICE exhaust	Conduct subsequent performance tests semiannually. <sup>1</sup>
4. Existing non-emergency, non-black start CI stationary RICE >500 HP that are not limited use stationary RICE	Limit or reduce CO emissions and not using a CEMS	Conduct subsequent performance tests every 8,760 hours or 3 years, whichever comes first.
5. Existing non-emergency, non-black start CI stationary RICE >500 HP that are limited use stationary RICE	Limit or reduce CO emissions and not using a CEMS	Conduct subsequent performance tests every 8,760 hours or 5 years, whichever comes first.

<sup>1</sup> After you have demonstrated compliance for two consecutive tests, you may reduce the frequency of subsequent performance tests to annually. If the results of any subsequent annual performance test indicate the stationary RICE is not in compliance with the CO or formaldehyde emission limitation, or you deviate from any of your operating limitations, you must resume semiannual performance tests.

# [<u>78 FR 6711</u>, Jan. 30, 2013]

# Table 4 to Subpart ZZZZ of Part 63—Requirements for Performance Tests

As stated in  $\frac{\$\$ 63.6610}{63.6611}$ ,  $\frac{63.6620}{63.6620}$ , and  $\frac{63.6640}{63.6640}$ , you must comply with the following requirements for performance tests for stationary RICE:

For each	Complying with the requirement to	You must	Using	According to the following requirements
1. 2SLB, 4SLB, and CI stationary RICE	a. Reduce CO emissions	i. Select the sampling port location and the number/location of traverse points at the inlet and outlet of the control device; and		(a) For CO, O <sub>2</sub> , and moisture measurement, ducts $\leq 6$ inches in diameter may be sampled at a single point located at the duct centroid and ducts $\geq 6$ and $\leq 12$ inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is $\geq 12$ inches in diameter <i>and</i> the sampling port location meets the two and half- diameter criterion of section 11.1.1 of method 1 of <u>40 CFR part 60</u> , <u>appendix A</u> -1, the duct may be sampled at '3-point long line'; otherwise, conduct the stratification testing and select sampling points according to section 8.1.2 of method 7E of <u>40 CFR part 60</u> , <u>appendix A</u> -4.
		ii. Measure the O <sub>2</sub> at the inlet and outlet of the control device; and	(1) Method 3 or 3A or 3B of <u>40 CFR part 60, appendix</u> <u>A</u> -2, or ASTM D6522-00 (Reapproved 2005) <sup>13</sup> (heated probe not necessary)	(b) Measurements to determine $O_2$ must be made at the same time as the measurements for CO concentration.

For each ·	Complying with the requirement to	You must	Using	According to the following requirements
		iii. Measure the CO at the inlet and the outlet of the control device; and	(2) ASTM D6522-00 (Reapproved 2005) <sup>123</sup> (heated probe not necessary) or method 10 of <u>40 CFR part 60, appendix</u> <u>A</u> -4	(c) The CO concentration must be at 15 percent O <sub>2</sub> , dry basis.
		iv. Measure moisture content at the inlet and outlet of the control device as needed to determine CO and O <sub>2</sub> concentrations on a dry basis	(3) Method 4 of <u>40 CFR</u> part 60, appendix A-3, or method 320 of <u>40 CFR part</u> <u>63, appendix A</u> , or ASTM D6348-03 <sup>13</sup>	(d) Measurements to determine moisture content must be made at the same time and location as the measurements for CO concentration.
2. 4SRB stationary RICE	a. Reduce formaldehyde or THC emissions	i. Select the sampling port location and the number/location of traverse points at the inlet and outlet of the control device; and		(a) For formaldehyde, THC, O <sub>2</sub> , and moisture measurement, ducts $\leq 6$ inches in diameter may be sampled at a single point located at the duct centroid and ducts >6 and $\leq 12$ inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is >12 inches in diameter <i>and</i> the sampling port location meets the two and half-diameter criterion of section 11.1.1 of method 1 of <u>40 CFR part</u> <u>60, appendix A</u> , the duct may be sampled at '3-point long line'; otherwise, conduct the stratification testing and select sampling points according to section 8.1.2 of method 7E of <u>40 CFR part 60, appendix A</u> .
		ii. Measure $O_2$ at the inlet and outlet of the control device; and	(1) Method 3 or 3A or 3B of <u>40 CFR part 60, appendix</u> <u>A</u> -2, or ASTM D6522-00 (Reapproved 2005) <sup>13</sup> (heated probe not necessary)	(b) Measurements to determine O <sub>2</sub> concentration must be made at the same time as the measurements for formaldehyde or THC concentration.
		iii. Measure moisture content at the inlet and outlet of the control device as needed to determine formaldehyde or THC and $O_2$ concentrations on a dry basis; and	(2) Method 4 of <u>40 CFR</u> part 60, appendix <u>A</u> -3, or method 320 of <u>40 CFR part</u> <u>63, appendix A</u> , or ASTM D6348-03 <sup>13</sup>	(c) Measurements to determine moisture content must be made at the same time and location as the measurements for formaldehyde or THC concentration.
		iv. If demonstrating compliance with the formaldehyde percent	(3) Method 320 or 323 of <u>40</u> <u>CFR part 63, appendix A</u> ; or ASTM D6348-	(d) Formaldehyde concentration must be at 15 percent O <sub>2</sub> , dry basis. Results of this test consist of the

For each •	Complying with the requirement to	You must	Using	According to the following requirements
		reduction requirement, measure formaldehyde at the inlet and the outlet of the control device	03, <sup>13</sup> provided in ASTM D6348-03 Annex A5 (Analyte Spiking Technique), the percent R must be greater than or equal to 70 and less than or equal to 130	average of the three 1-hour or longer runs.
		v. If demonstrating compliance with the THC percent reduction requirement, measure THC at the inlet and the outlet of the control device	(4) (1) Method 25A, reported as propane, of <u>40</u> <u>CFR part 60, appendix A</u> -7	(e) THC concentration must be at 15 percent $O_2$ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
3. Stationary RICE	a. Limit the concentration of formaldehyde or CO in the stationary RICE exhaust	i. Select the sampling port location and the number/location of traverse points at the exhaust of the stationary RICE; and		(a) For formaldehyde, CO, O <sub>2</sub> , and moisture measurement, ducts $\leq 6$ inches in diameter may be sampled at a single point located at the duct centroid and ducts >6 and $\leq 12$ inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is >12 inches in diameter <i>and</i> the sampling port location meets the two and half-diameter criterion of section 11.1.1 of method 1 of <u>40 CFR part</u> <u>60, appendix A</u> , the duct may be sampled at '3-point long line'; otherwise, conduct the stratification testing and select sampling points according to section 8.1.2 of method 7E of <u>40 CFR part 60, appendix A</u> . If using a control device, the sampling site must be located at the outlet of the control device.
		ii. Determine the O <sub>2</sub> concentration of the stationary RICE exhaust at the sampling port location; and	(1) Method 3 or 3A or 3B of <u>40 CFR part 60, appendix</u> <u>A</u> -2, or ASTM D6522-00 (Reapproved 2005) <sup>13</sup> (heated probe not necessary)	(b) Measurements to determine $O_2$ concentration must be made at the same time and location as the measurements for formaldehyde or CO concentration.
		iii. Measure moisture content of the stationary RICE exhaust at the sampling port location as needed to determine formaldehyde or CO and O <sub>2</sub> concentrations on a	(2) Method 4 of <u>40 CFR</u> part 60, appendix A-3, or method 320 of <u>40 CFR part</u> <u>63, appendix A</u> , or ASTM D6348-03 <sup>13</sup>	(c) Measurements to determine moisture content must be made at the same time and location as the measurements for formaldehyde or CO concentration.

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For each	Complying with the requirement to	You must	Using	According to the following requirements
		dry basis; and		
		iv. Measure formaldehyde at the exhaust of the stationary RICE; or	(3) Method 320 or 323 of <u>40</u> <u>CFR part 63, appendix A</u> ; or ASTM D6348- 03, <sup>13</sup> provided in ASTM D6348-03 Annex A5 (Analyte Spiking Technique), the percent R must be greater than or equal to 70 and less than or equal to 130	(d) Formaldehyde concentration must be at 15 percent $O_2$ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
		v. Measure CO at the exhaust of the stationary RICE	(4) Method 10 of <u>40 CFR</u> part <u>60</u> , appendix <u>A</u> -4, ASTM D6522-00 (2005), <sup>13</sup> method 320 of <u>40</u> <u>CFR part 63</u> , appendix <u>A</u> , or ASTM D6348-03 <sup>13</sup>	(e) CO concentration must be at 15 percent O <sub>2</sub> , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
<sup>1</sup> You may a	lso use methods 3.	A and 10 as options to AST	M-D6522-00 (2005).	

<sup>2</sup> You may obtain a copy of ASTM-D6348-03 from at least one of the following addresses: American Society for Testing and Materials, 100 Barr Harbor Drive, West Conshohocken, PA 19428-2959, or University Microfilms International, 300 North Zeeb Road, Ann Arbor, MI 48106.

<sup>3</sup> Incorporated by reference, see  $\S$  <u>63.14</u>.

# [88 FR 18413, Mar. 29, 2023]

# Table 5 to Subpart ZZZZ of Part 63—Initial Compliance With Emission Limitations, Operating Limitations, and Other Requirements

As stated in  $\frac{\$\$ 63.6612}{63.6625}$  and  $\frac{63.6625}{63.6625}$ , you must initially comply with the emission and operating limitations as required by the following:

For each	Complying with the requirement to	You have demonstrated initial compliance if
1. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE $\geq$ 250 HP located at a major source of HAP, non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP located at an area source of HAP	a. Reduce CO emissions and using oxidation catalyst, and using a CPMS	i. The average reduction of emissions of CO determined from the initial performance test achieves the required CO percent reduction; and ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § $63.6625(b)$ ; and iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.
2. Non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non- emergency stationary CI RICE >500 HP located at an area source of HAP	a. Limit the concentration of CO, using oxidation catalyst, and using a CPMS	i. The average CO concentration determined from the initial performance test is less than or equal to the CO emission limitation; and
		ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according

For each	Complying with the requirement to	You have demonstrated initial compliance if
		to the requirements in $\S 63.6625(b)$ ; and
		iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.
3. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP located at an area source of HAP	a. Reduce CO emissions and not using oxidation catalyst	i. The average reduction of emissions of CO determined from the initial performance test achieves the required CO percent reduction; and ii. You have installed a CPMS to continuously monitor operating parameters approved by the Administrator (if any) according to the requirements in § 63.6625(b); and iii. You have recorded the approved operating parameters (if any) during the initial performance test.
4. Non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non- emergency stationary CI RICE >500 HP located at an area source of HAP	a. Limit the concentration of CO, and not using oxidation catalyst	i. The average CO concentration determined from the initial performance test is less than or equal to the CO emission limitation; and ii. You have installed a CPMS to continuously monitor operating parameters approved by the Administrator (if any) according to the requirements in § 63.6625(b); and
		iii. You have recorded the approved operating parameters (if any) during the initial performance test.
5. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP located at an area source of HAP	a. Reduce CO emissions, and using a CEMS	i. You have installed a CEMS to continuously monitor CO and either $O_2$ or $CO_2$ at both the inlet and outlet of the oxidation catalyst according to the requirements in § 63.6625(a); and ii. You have conducted a performance evaluation of your CEMS using PS 3 and 4A of 40 CFR part 60, appendix B; and
		iii. The average reduction of CO calculated using § 63.6620 equals or exceeds the required percent reduction. The initial test comprises the first 4-hour period after successful validation of the CEMS. Compliance is based on the average percent reduction achieved during the 4-hour period.
6. Non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non- emergency stationary CI RICE >500 HP located at an area source of HAP	a. Limit the concentration of CO, and using a CEMS	i. You have installed a CEMS to continuously monitor CO and either $O_2$ or $CO_2$ at the outlet of the oxidation catalyst according to the requirements in § 63.6625(a); and
		ii. You have conducted a performance evaluation of your CEMS using PS 3 and 4A of <u>40 CFR part 60, appendix B</u> ; and
		iii. The average concentration of CO calculated using $\S 63.6620$ is less than or

For each	Complying with the requirement to	You have demonstrated initial compliance if
		equal to the CO emission limitation. The initial test comprises the first 4-hour period after successful validation of the CEMS. Compliance is based on the average concentration measured during the 4-hour period.
7. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Reduce formaldehyde emissions and using NSCR	i. The average reduction of emissions of formaldehyde determined from the initial performance test is equal to or greater than the required formaldehyde percent reduction, or the average reduction of emissions of THC determined from the initial performance test is equal to or greater than 30 percent; and
		ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in $\S$ 63.6625(b); and
		iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.
8. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Reduce formaldehyde emissions and not using NSCR	i. The average reduction of emissions of formaldehyde determined from the initial performance test is equal to or greater than the required formaldehyde percent reduction or the average reduction of emissions of THC determined from the initial performance test is equal to or greater than 30 percent; and
		ii. You have installed a CPMS to continuously monitor operating parameters approved by the Administrator (if any) according to the requirements in § $63.6625(b)$ ; and
		iii. You have recorded the approved operating parameters (if any) during the initial performance test.
9. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE 250≤HP≤500 located at a major source of HAP, and existing non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Limit the concentration of formaldehyde in the stationary RICE exhaust and using oxidation catalyst or NSCR	i. The average formaldehyde concentration, corrected to 15 percent $O_2$ , dry basis, from the three test runs is less than or equal to the formaldehyde emission limitation; and ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b); and
		iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.
10. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE 250≤HP≤500 located at a major source of HAP, and existing non-emergency 4SRB stationary RICE >500 HP located at a major source	a. Limit the concentration of formaldehyde in the stationary RICE exhaust and not using oxidation catalyst or NSCR	i. The average formaldehyde concentration, corrected to 15 percent O <sub>2</sub> , dry basis, from the three test runs is less than or equal to the formaldehyde emission limitation; and ii. You have installed a CPMS to continuously monitor operating parameters approved by the

For each	Complying with the requirement to	You have demonstrated initial compliance if
of HAP		Administrator (if any) according to the requirements in $\S$ 63.6625(b); and
		iii. You have recorded the approved operating parameters (if any) during the initial performance test.
11. Existing non-emergency stationary RICE 100≤HP≤500 located at a major source of HAP, and existing non-emergency stationary CI RICE 300 <hp≤500 an="" area="" at="" hap<="" located="" of="" source="" td=""><td>a. Reduce CO emissions</td><td>i. The average reduction of emissions of CO or formaldehyde, as applicable determined from the initial performance test is equal to or greater than the required CO or formaldehyde, as applicable, percent reduction.</td></hp≤500>	a. Reduce CO emissions	i. The average reduction of emissions of CO or formaldehyde, as applicable determined from the initial performance test is equal to or greater than the required CO or formaldehyde, as applicable, percent reduction.
12. Existing non-emergency stationary RICE 100≤HP≤500 located at a major source of HAP, and existing non-emergency stationary CI RICE 300 <hp≤500 an="" area="" at="" hap<="" located="" of="" source="" td=""><td>a. Limit the concentration of formaldehyde or CO in the stationary RICE exhaust</td><td>i. The average formaldehyde or CO concentration, as applicable, corrected to 15 percent <math>O_2</math>, dry basis, from the three test runs is less than or equal to the formaldehyde or CO emission limitation, as applicable.</td></hp≤500>	a. Limit the concentration of formaldehyde or CO in the stationary RICE exhaust	i. The average formaldehyde or CO concentration, as applicable, corrected to 15 percent $O_2$ , dry basis, from the three test runs is less than or equal to the formaldehyde or CO emission limitation, as applicable.
13. Existing non-emergency 4SLB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year	a. Install an oxidation catalyst	i. You have conducted an initial compliance demonstration as specified in § $63.6630(e)$ to show that the average reduction of emissions of CO is 93 percent or more, or the average CO concentration is less than or equal to 47 ppmvd at 15 percent O <sub>2</sub> ;
		ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b), or you have installed equipment to automatically shut down the engine if the catalyst inlet temperature exceeds 1350 °F.
14. Existing non-emergency 4SRB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year	a. Install NSCR	i. You have conducted an initial compliance demonstration as specified in § $63.6630(e)$ to show that the average reduction of emissions of CO is 75 percent or more, the average CO concentration is less than or equal to 270 ppmvd at 15 percent O <sub>2</sub> , or the average reduction of emissions of THC is 30 percent or more;
		ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in $\S$ 63.6625(b), or you have installed equipment to automatically shut down the engine if the catalyst inlet temperature exceeds 1250 °F.

[<u>78 FR 6712</u>, Jan. 30, 2013]

# Table 6 to Subpart ZZZZ of Part 63—Continuous Compliance With Emission Limitations, and Other Requirements

As stated in <u>§ 63.6640</u>, you must continuously comply with the emissions and operating limitations and work or management practices as required by the following:

For each	Complying with the requirement to	You must demonstrate continuous compliance by

For each	Complying with the requirement to	You must demonstrate continuous compliance by
1. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, and new or reconstructed non-emergency CI stationary RICE >500 HP located at a major source of HAP	a. Reduce CO emissions and using an oxidation catalyst, and using a CPMS	<ul> <li>i. Conducting semiannual performance tests for CO to demonstrate that the required CO percent reduction is achieved<sup>a</sup>; and</li> <li>ii. Collecting the catalyst inlet temperature data according to § 63.6625(b); and</li> <li>iii. Reducing these data to 4-hour rolling averages; and</li> </ul>
		iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and
		v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.
2. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE $\geq$ 250 HP located at a major source of HAP, and new or reconstructed non-emergency CI stationary RICE >500 HP located at a major source of HAP	a. Reduce CO emissions and not using an oxidation catalyst, and using a CPMS	i. Conducting semiannual performance tests for CO to demonstrate that the required CO percent reduction is achieved <sup>a</sup> ; and ii. Collecting the approved operating parameter (if any) data according to § <u>63.6625(b)</u> ; and iii. Reducing these data to 4-hour rolling averages; and
		iv. Maintaining the 4-hour rolling averages within the operating limitations for the operating parameters established during the performance test.
3. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, new or reconstructed non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP	a. Reduce CO emissions or limit the concentration of CO in the stationary RICE exhaust, and using a CEMS	i. Collecting the monitoring data according to $\S$ 63.6625(a), reducing the measurements to 1-hour averages, calculating the percent reduction or concentration of CO emissions according to $\S$ 63.6620; and ii. Demonstrating that the catalyst achieves the required percent reduction of CO emissions over the 4-hour averaging period, or that the emission remain at or below the CO concentration limit; and
		iii. Conducting an annual RATA of your CEMS using PS 3 and 4A of <u>40 CFR part 60</u> , <u>appendix B</u> , as well as daily and periodic data quality checks in accordance with <u>40 CFR</u> <u>part 60</u> , <u>appendix F</u> , procedure 1.
4. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Reduce formaldehyde emissions and using NSCR	i. Collecting the catalyst inlet temperature data according to $\frac{63.6625(b)}{5}$ ; and
		ii. Reducing these data to 4-hour rolling averages; and
		iii. Maintaining the 4-hour rolling averages within the operating limitations for the

For each	Complying with the requirement to	You must demonstrate continuous compliance by
		catalyst inlet temperature; and
		iv. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.
5. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Reduce formaldehyde emissions and not using NSCR	i. Collecting the approved operating parameter (if any) data according to $\underline{\$}$ <u>63.6625(b)</u> ; and
		ii. Reducing these data to 4-hour rolling averages; and
		iii. Maintaining the 4-hour rolling averages within the operating limitations for the operating parameters established during the performance test.
6. Non-emergency 4SRB stationary RICE with a brake HP ≥5,000 located at a major source of HAP	a. Reduce formaldehyde emissions	Conducting semiannual performance tests for formaldehyde to demonstrate that the required formaldehyde percent reduction is achieved, or to demonstrate that the average reduction of emissions of THC determined from the performance test is equal to or greater than 30 percent. <sup>a</sup>
7. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP and new or reconstructed non-emergency 4SLB stationary RICE 250≤HP≤500 located at a major source of HAP	a. Limit the concentration of formaldehyde in the stationary RICE exhaust and using oxidation catalyst or NSCR	i. Conducting semiannual performance tests for formaldehyde to demonstrate that your emissions remain at or below the formaldehyde concentration limit <sup>a</sup> ; and ii. Collecting the catalyst inlet temperature data according to $\S$ 63.6625(b); and
		iii. Reducing these data to 4-hour rolling averages; and
		iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and
		v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.
8. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP and new or reconstructed non-emergency 4SLB stationary RICE 250≤HP≤500 located at a major source of HAP	a. Limit the concentration of formaldehyde in the stationary RICE exhaust and not using oxidation catalyst or NSCR	i. Conducting semiannual performance tests for formaldehyde to demonstrate that your emissions remain at or below the formaldehyde concentration limit <sup>a</sup> ; and ii. Collecting the approved operating parameter (if any) data according to § 63.6625(b); and
		iii. Reducing these data to 4-hour rolling averages; and
		iv. Maintaining the 4-hour rolling averages

For each	Complying with the requirement to	You must demonstrate continuous compliance by
		within the operating limitations for the operating parameters established during the performance test.
9. Existing emergency and black start stationary RICE $\leq$ 500 HP located at a major source of HAP, existing non-emergency stationary RICE <100 HP located at a major source of HAP, existing emergency and black start stationary RICE located at an area source of HAP, existing non-emergency stationary CI RICE $\leq$ 300 HP located at an area source of HAP, existing non-emergency 2SLB stationary RICE located at an area source of HAP, existing non-emergency stationary SI RICE located at an area source of HAP which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, existing non- emergency 4SLB and 4SRB stationary RICE $\leq$ 500 HP located at an area source of HAP, existing non- emergency 4SLB and 4SRB stationary RICE $\geq$ 500 HP located at an area source of HAP that operate 24 hours or less per calendar year, and existing non- emergency 4SLB and 4SRB stationary RICE $\geq$ 500 HP located at an area source of HAP that are remote stationary RICE	a. Work or Management practices	i. Operating and maintaining the stationary RICE according to the manufacturer's emission-related operation and maintenance instructions; or ii. Develop and follow your own maintenance plan which must provide to the extent practicable for the maintenance and operation of the engine in a manner consistent with good air pollution control practice for minimizing emissions.
10. Existing stationary CI RICE >500 HP that are not limited use stationary RICE	a. Reduce CO emissions, or limit the concentration of CO in the stationary RICE exhaust, and using oxidation catalyst	i. Conducting performance tests every 8,760 hours or 3 years, whichever comes first, for CO or formaldehyde, as appropriate, to demonstrate that the required CO or formaldehyde, as appropriate, percent reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and
		ii. Collecting the catalyst inlet temperature data according to $\frac{63.6625(b)}{2}$ ; and
		iii. Reducing these data to 4-hour rolling averages; and
		iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and
		v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.
11. Existing stationary CI RICE >500 HP that are not limited use stationary RICE	a. Reduce CO emissions, or limit the concentration of CO in the stationary RICE exhaust, and not using	i. Conducting performance tests every 8,760 hours or 3 years, whichever comes first, for CO or formaldehyde, as appropriate, to demonstrate that the required CO or formaldehyde, as appropriate, percent
For each	Complying with the requirement to	You must demonstrate continuous compliance by
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	oxidation catalyst	reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and
		ii. Collecting the approved operating parameter (if any) data according to $\underline{\$}$ <u>63.6625(b)</u> ; and
		iii. Reducing these data to 4-hour rolling averages; and
		iv. Maintaining the 4-hour rolling averages within the operating limitations for the operating parameters established during the performance test.
12. Existing limited use CI stationary RICE >500 HP	a. Reduce CO emissions or limit the concentration of CO in the stationary RICE exhaust, and using an oxidation catalyst	i. Conducting performance tests every 8,760 hours or 5 years, whichever comes first, for CO or formaldehyde, as appropriate, to demonstrate that the required CO or formaldehyde, as appropriate, percent reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and
		ii. Collecting the catalyst inlet temperature data according to $\S$ 63.6625(b); and
		iii. Reducing these data to 4-hour rolling averages; and
		iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and
		v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.
13. Existing limited use CI stationary RICE >500 HP	a. Reduce CO emissions or limit the concentration of CO in the stationary RICE exhaust, and not using an oxidation catalyst	i. Conducting performance tests every 8,760 hours or 5 years, whichever comes first, for CO or formaldehyde, as appropriate, to demonstrate that the required CO or formaldehyde, as appropriate, percent reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and
		ii. Collecting the approved operating parameter (if any) data according to $\underline{\$}$ <u>63.6625(b)</u> ; and
		iii. Reducing these data to 4-hour rolling averages; and
		iv. Maintaining the 4-hour rolling averages within the operating limitations for the operating parameters established during the

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For each	Complying with the requirement to	You must demonstrate continuous compliance by
		performance test.
14. Existing non-emergency 4SLB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year	a. Install an oxidation catalyst	i. Conducting annual compliance demonstrations as specified in § 63.6640(c) to show that the average reduction of emissions of CO is 93 percent or more, or the average CO concentration is less than or equal to 47 ppmvd at 15 percent O <sub>2</sub> ; and either ii. Collecting the catalyst inlet temperature data according to § 63.6625(b), reducing these data to 4-hour rolling averages; and maintaining the 4-hour rolling averages within the limitation of greater than 450 °F and less than or equal to 1350 °F for the catalyst inlet temperature; or iii. Immediately shutting down the engine if the catalyst inlet temperature exceeds 1350 °F.
15. Existing non-emergency 4SRB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year	a. Install NSCR	i. Conducting annual compliance demonstrations as specified in § 63.6640(c) to show that the average reduction of emissions of CO is 75 percent or more, the average CO concentration is less than or equal to 270 ppmvd at 15 percent $O_2$ , or the average reduction of emissions of THC is 30 percent or more; and either ii. Collecting the catalyst inlet temperature data according to § 63.6625(b), reducing these data to 4-hour rolling averages; and maintaining the 4-hour rolling averages within the limitation of greater than or equal to 750 °F and less than or equal to 1250 °F for the catalyst inlet temperature; or iii. Immediately shutting down the engine if the catalyst inlet temperature exceeds 1250 °F.

<sup>a</sup> After you have demonstrated compliance for two consecutive tests, you may reduce the frequency of subsequent performance tests to annually. If the results of any subsequent annual performance test indicate the stationary RICE is not in compliance with the CO or formaldehyde emission limitation, or you deviate from any of your operating limitations, you must resume semiannual performance tests.

[78 FR 6715, Jan. 30, 2013]

#### Table 7 to Subpart ZZZZ of Part 63—Requirements for Reports

As stated in <u>§ 63.6650</u>, you must comply with the following requirements for reports:

For each	You must submit a	The report must contain	You must submit the report
1. Existing non-emergency, non- black start stationary RICE 100≤HP≤500 located at a major	Compliance report	a. If there are no deviations from any emission limitations or operating limitations that apply to	i. Semiannually according to the requirements in $\frac{63.6650(b)(1)}{(5)}$ and (i) for engines that are not

For each	You must submit a	The report must contain	You must submit the report
source of HAP; existing non- emergency, non-black start stationary CI RICE >500 HP located at a major source of HAP; existing non- emergency 4SRB stationary RICE >500 HP located at a major source of HAP; existing non-emergency, non- black start stationary CI RICE >300 HP located at an area source of HAP; new or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP; and new or reconstructed non-emergency 4SLB stationary RICE 250≤HP≤500 located at a major source of HAP		you, a statement that there were no deviations from the emission limitations or operating limitations during the reporting period. If there were no periods during which the CMS, including CEMS and CPMS, was out-of-control, as specified in § 63.8(c)(7), a statement that there were not periods during which the CMS was out-of-control during the reporting period; or b. If you had a deviation from any emission limitation or operating limitation during the reporting period, the information in § 63.6650(d). If there were periods during which the CMS, including CEMS and CPMS, was out-of- control, as specified in § $63.8(c)(7)$ , the information in § $63.6650(c)$ ; or	limited use stationary RICE subject to numerical emission limitations; and ii. Annually according to the requirements in § 63.6650(b)(6)- (9) and (i) for engines that are limited use stationary RICE subject to numerical emission limitations. i. Semiannually according to the requirements in § 63.6650(b) and (i).
		c. If you had a malfunction during the reporting period, the information in $\S.63.6650(c)(4)$	i. Semiannually according to the requirements in § $63.6650(b)$ and (i).
2. New or reconstructed non- emergency stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis	Report	a. The fuel flow rate of each fuel and the heating values that were used in your calculations, and you must demonstrate that the percentage of heat input provided by landfill gas or digester gas, is equivalent to 10 percent or more of the gross heat input on an annual basis; and	i. Annually, according to the requirements in $\S 63.6650$ .
		b. The operating limits provided in your federally enforceable permit, and any deviations from these limits; and	i. See item 2.a.i.
		c. Any problems or errors suspected with the meters	i. See item 2.a.i.
3. Existing non-emergency, non- black start 4SLB and 4SRB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that operate more than 24 hours per calendar year	Compliance report	a. The results of the annual compliance demonstration, if conducted during the reporting period	i. Semiannually according to the requirements in $\S 63.6650(b)(1)$ -(5) and (i).
4. Emergency stationary RICE that operate for the purposes specified in $\frac{63.6640(f)(4)(ii)}{100}$	Report	a. The information in <u>§</u> 63.6650(h)(1)	i. Annually according to the requirements in $\S$ 63.6650(h)(2)-(3) and (i).

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# [89 FR 70522, Aug. 30, 2024]

# Table 8 to Subpart ZZZZ of Part 63—Applicability of General Provisions to Subpart ZZZZ

As stated in § 63.6665, you must comply with the following applicable general provisions.

General provisions citation	Subject of citation	Applies to subpart	Explanation
§ 63.1	General applicability of the General Provisions	Yes	
§ 63.2	Definitions	Yes	Additional terms defined in § 63.6675.
§ 63.3	Units and abbreviations	Yes	
§ 63.4	Prohibited activities and circumvention	Yes	
§ 63.5	Construction and reconstruction	Yes	
§ 63.6(a)	Applicability	Yes	
§ 63.6(b)(1)-(4)	Compliance dates for new and reconstructed sources	Yes	
§ 63.6(b)(5)	Notification	Yes	
§ 63.6(b)(6)	[Reserved]		
§ 63.6(b)(7)	Compliance dates for new and reconstructed area sources that become major sources	Yes	
§ 63.6(c)(1)-(2)	Compliance dates for existing sources	Yes	
§ 63.6(c)(3)-(4)	[Reserved]		
§ 63.6(c)(5)	Compliance dates for existing area sources that become major sources		
§ 63.6(d)	[Reserved]		
§ 63.6(e)	Operation and maintenance	No	
§ 63.6(f)(1)	Applicability of standards	No	
§ 63.6(f)(2)	Methods for determining compliance	Yes	
§ 63.6(f)(3)	Finding of compliance	Yes	
§ 63.6(g)(1)-(3)	Use of alternate standard	Yes	
§ 63.6(h)	Opacity and visible emission standards	No	Subpart ZZZZ does not contain opacity or visible emission standards.
§ 63.6(i)	Compliance extension procedures and criteria	Yes	
§ 63.6(j)	Presidential compliance exemption	Yes	
§ 63.7(a)(1)-(2)	Performance test dates	Yes	Subpart ZZZZ contains performance test dates at $\S$ <u>63.6610</u> , <u>63.6611</u> , and <u>63.6612</u> .
§ 63.7(a)(3)	CAA section 114 authority	Yes	
§ 63.7(b)(1)	Notification of performance test	Yes	Except that $\S 63.7(b)(1)$ only applies as specified in $\S 63.6645$ .
§ 63.7(b)(2)	Notification of rescheduling	Yes	Except that $\S 63.7(b)(2)$ only applies as specified in $\S$

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General provisions citation	Subject of citation	Applies to subpart	Explanation
			<u>63.6645</u> .
§ 63.7(c)	Quality assurance/test plan	Yes	Except that $\S 63.7(c)$ only applies as specified in $\S 63.6645$ .
§ 63.7(d)	Testing facilities	Yes	
§ 63.7(e)(1)	Conditions for conducting performance tests	No	Subpart ZZZZ specifies conditions for conducting performance tests at $\S$ 63.6620.
§ 63.7(e)(2)	Conduct of performance tests and reduction of data	Yes	Subpart ZZZZ specifies test methods at $\S$ 63.6620.
§ 63.7(e)(3)	Test run duration	Yes	
§ 63.7(e)(4)	Administrator may require other testing under section 114 of the CAA	Yes	
§ 63.7(f)	Alternative test method provisions	Yes	
§ 63.7(g)	Performance test data analysis, recordkeeping, and reporting	Yes	
§ 63.7(h)	Waiver of tests	Yes	
§ 63.8(a)(1)	Applicability of monitoring requirements	Yes	Subpart ZZZZ contains specific requirements for monitoring at $\frac{63.6625}{2}$ .
§ 63.8(a)(2)	Performance specifications	Yes	
§ 63.8(a)(3)	[Reserved]		
§ 63.8(a)(4)	Monitoring for control devices	No	
§ 63.8(b)(1)	Monitoring	Yes	
§ 63.8(b)(2)-(3)	Multiple effluents and multiple monitoring systems	Yes	
§ 63.8(c)(1)	Monitoring system operation and maintenance	Yes	
§ 63.8(c)(1)(i)	Routine and predictable SSM	No	
§ 63.8(c)(1)(ii)	SSM not in Startup Shutdown Malfunction Plan	Yes	
§ 63.8(c)(1)(iii)	Compliance with operation and maintenance requirements	No	
§ 63.8(c)(2)-(3)	Monitoring system installation	Yes	
§ 63.8(c)(4)	Continuous monitoring system (CMS) requirements	Yes	Except that subpart ZZZZ does not require Continuous Opacity Monitoring System (COMS).
§ 63.8(c)(5)	COMS minimum procedures	No	Subpart ZZZZ does not require COMS.
§ 63.8(c)(6)-(8)	CMS requirements	Yes	Except that subpart ZZZZ does not require COMS.
§ 63.8(d)	CMS quality control	Yes	
§ 63.8(e)	CMS performance evaluation	Yes	Except for <u>§ 63.8(e)(5)(ii)</u> , which applies to COMS.
			Except that $\S 63.8(e)$ only applies as specified in $\S 63.6645$ .
§ 63.8(f)(1)-(5)	Alternative monitoring method	Yes	Except that $\S 63.8(f)(4)$ only applies as specified in $\S 63.6645$ .

General provisions citation	General provisions Subject of citation citation		Explanation
§ 63.8(f)(6)	Alternative to relative accuracy test	Yes	Except that $\S 63.8(f)(6)$ only applies as specified in $\S 63.6645$ .
§ 63.8(g)	Data reduction	Yes	Except that provisions for COMS are not applicable. Averaging periods for demonstrating compliance are specified at $\underline{\$\$}$ 63.6635 and 63.6640.
§ 63.9(a)	Applicability and State delegation of notification requirements	Yes	
§ 63.9(b)(1)-(5)	Initial notifications	Yes	Except that § 63.9(b)(3) is reserved.
			Except that $\S$ <u>63.9(b)</u> only applies as specified in $\S$ <u>63.6645</u> .
§ 63.9(c)	Request for compliance extension	Yes	Except that $\S$ 63.9(c) only applies as specified in $\S$ 63.6645.
§ 63.9(d)	Notification of special compliance requirements for new sources	Yes	Except that $\S$ 63.9(d) only applies as specified in $\S$ 63.6645.
§ 63.9(e)	Notification of performance test	Yes	Except that $\S 63.9(e)$ only applies as specified in $\S 63.6645$ .
§ 63.9(f)	Notification of visible emission (VE)/opacity test	No	Subpart ZZZZ does not contain opacity or VE standards.
§ 63.9(g)(1)	Notification of performance evaluation	Yes	Except that $\S 63.9(g)$ only applies as specified in $\S 63.6645$ .
§ 63.9(g)(2)	Notification of use of COMS data	No	Subpart ZZZZ does not contain opacity or VE standards.
§ 63.9(g)(3)	Notification that criterion for alternative to RATA is exceeded	Yes	If alternative is in use. Except that $\S 63.9(g)$ only applies as specified in $\S 63.6645$ .
§ 63.9(h)(1)-(6)	Notification of compliance status	Yes	Except that notifications for sources using a CEMS are due 30 days after completion of performance evaluations. $\frac{63.9(h)(4)}{10}$ is reserved.
			Except that $\S 63.9(h)$ only applies as specified in $\S 63.6645$ .
§ 63.9(i)	Adjustment of submittal deadlines	Yes	
§ 63.9(j)	Change in previous information	Yes	
§ 63.9(k)	Electronic reporting procedures	Yes	Only as specified in <u>§§</u> <u>63.9(j)</u> , <u>63.6620</u> , <u>63.6625</u> , <u>63.6645</u> , and <u>63.6650</u> .
§ 63.10(a)	Administrative provisions for recordkeeping/reporting	Yes	
§ 63.10(b)(1)	Record retention	Yes	Except that the most recent 2 years of data do not have to be retained on site.
§ 63.10(b)(2)(i)- (v)	Records related to SSM	No	
§ 63.10(b)(2)(vi)- (xi)	Records	Yes	
§ 63.10(b)(2)(xii)	Record when under waiver	Yes	
§ 63.10(b)(2)(xiii)	Records when using alternative to	Yes	For CO standard if using RATA alternative.

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General provisions citation	Subject of citation	Applies to subpart	Explanation
	RATA		
§ 63.10(b)(2)(xiv)	Records of supporting documentation	Yes	
§ 63.10(b)(3)	Records of applicability determination	Yes	
§ 63.10(c)	Additional records for sources using CEMS	Yes	Except that $\S 63.10(c)(2)-(4)$ and $(9)$ are reserved.
§ 63.10(d)(1)	General reporting requirements	Yes	
§ 63.10(d)(2)	Report of performance test results	Yes	
§ 63.10(d)(3)	Reporting opacity or VE observations	No	Subpart ZZZZ does not contain opacity or VE standards.
§ 63.10(d)(4)	Progress reports	Yes	
§ 63.10(d)(5)	) Startup, shutdown, and malfunction reports		
§ 63.10(e)(1) and (2)(i)	(1) and Additional CMS Reports		
§ 63.10(e)(2)(ii)	COMS-related report	No	Subpart ZZZZ does not require COMS.
§ 63.10(e)(3)	Excess emission and parameter exceedances reports		Excess emissions and exceedance reporting is specified in $\frac{63.6650}{2}$ .
§ 63.10(e)(4)	Reporting COMS data	No	Subpart ZZZZ does not require COMS.
§ 63.10(f)	Waiver for recordkeeping/reporting	Yes	
§ 63.11	Flares	No	
§ 63.12	State authority and delegations	Yes	
§ 63.13	Addresses	Yes	
§ 63.14	Incorporation by reference	Yes	
§ 63.15	Availability of information	Yes	

[89 FR 70522, Aug. 30, 2024]

# Appendix A to Subpart ZZZZ of Part 63—Protocol for Using an Electrochemical Analyzer to Determine Oxygen and Carbon Monoxide Concentrations From Certain Engines

1.0 Scope and Application. What is this Protocol?

This protocol is a procedure for using portable electrochemical (EC) cells for measuring carbon monoxide (CO) and oxygen  $(O_2)$  concentrations in controlled and uncontrolled emissions from existing stationary 4-stroke lean burn and 4-stroke rich burn reciprocating internal combustion engines as specified in the applicable rule.

1.1 Analytes. What does this protocol determine?

This protocol measures the engine exhaust gas concentrations of carbon monoxide (CO) and oxygen (O<sub>2</sub>).

Analyte	CAS No.	Sensitivity
Carbon monoxide (CO)	630-08-0	Minimum detectable limit should be 2 percent of the nominal range or 1 ppm, whichever is less restrictive.
Oxygen (O <sub>2</sub> )	7782-44- 7	

## 40 CFR 63 SUBPART ZZZZ

## National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

1.2 Applicability. When is this protocol acceptable?

This protocol is applicable to <u>40 CFR part 63</u>, <u>subpart ZZZZ</u>. Because of inherent cross sensitivities of EC cells, you must not apply this protocol to other emissions sources without specific instruction to that effect.

1.3 Data Quality Objectives. How good must my collected data be?

Refer to Section 13 to verify and document acceptable analyzer performance.

1.4 Range. What is the targeted analytical range for this protocol?

The measurement system and EC cell design(s) conforming to this protocol will determine the analytical range for each gas component. The nominal ranges are defined by choosing up-scale calibration gas concentrations near the maximum anticipated flue gas concentrations for CO and O<sub>2</sub>, or no more than twice the permitted CO level.

1.5 Sensitivity. What minimum detectable limit will this protocol yield for a particular gas component?

The minimum detectable limit depends on the nominal range and resolution of the specific EC cell used, and the signal to noise ratio of the measurement system. The minimum detectable limit should be 2 percent of the nominal range or 1 ppm, whichever is less restrictive.

2.0 Summary of Protocol

In this protocol, a gas sample is extracted from an engine exhaust system and then conveyed to a portable EC analyzer for measurement of CO and  $O_2$  gas concentrations. This method provides measurement system performance specifications and sampling protocols to ensure reliable data. You may use additions to, or modifications of vendor supplied measurement systems (e.g., heated or unheated sample lines, thermocouples, flow meters, selective gas scrubbers, etc.) to meet the design specifications of this protocol. Do not make changes to the measurement system from the as-verified configuration (Section 3.12).

3.0 Definitions

*3.1 Measurement System.* The total equipment required for the measurement of CO and O<sub>2</sub> concentrations. The measurement system consists of the following major subsystems:

3.1.1 Data Recorder. A strip chart recorder, computer or digital recorder for logging measurement data from the analyzer output. You may record measurement data from the digital data display manually or electronically.

3.1.2 Electrochemical (EC) Cell. A device, similar to a fuel cell, used to sense the presence of a specific analyte and generate an electrical current output proportional to the analyte concentration.

3.1.3 Interference Gas Scrubber. A device used to remove or neutralize chemical compounds that may interfere with the selective operation of an EC cell.

3.1.4 Moisture Removal System. Any device used to reduce the concentration of moisture in the sample stream so as to protect the EC cells from the damaging effects of condensation and to minimize errors in measurements caused by the scrubbing of soluble gases.

3.1.5 Sample Interface. The portion of the system used for one or more of the following: sample acquisition; sample transport; sample conditioning or protection of the EC cell from any degrading effects of the engine exhaust effluent; removal of particulate matter and condensed moisture.

*3.2 Nominal Range*. The range of analyte concentrations over which each EC cell is operated (normally 25 percent to 150 percent of up-scale calibration gas value). Several nominal ranges can be used for any given cell so long as the calibration and repeatability checks for that range remain within specifications.

3.3 Calibration Gas. A vendor certified concentration of a specific analyte in an appropriate balance gas.

*3.4 Zero Calibration Error*. The analyte concentration output exhibited by the EC cell in response to zero-level calibration gas.

*3.5 Up-Scale Calibration Error*. The mean of the difference between the analyte concentration exhibited by the EC cell and the certified concentration of the up-scale calibration gas.

*3.6 Interference Check.* A procedure for quantifying analytical interference from components in the engine exhaust gas other than the targeted analytes.

*3.7 Repeatability Check.* A protocol for demonstrating that an EC cell operated over a given nominal analyte concentration range provides a stable and consistent response and is not significantly affected by repeated exposure to that gas.

*3.8 Sample Flow Rate.* The flow rate of the gas sample as it passes through the EC cell. In some situations, EC cells can experience drift with changes in flow rate. The flow rate must be monitored and documented during all phases of a sampling run.

3.9 Sampling Run. A timed three-phase event whereby an EC cell's response rises and plateaus in a sample conditioning phase, remains relatively constant during a measurement data phase, then declines during a refresh phase. The sample conditioning phase exposes the EC cell to the gas sample for a length of time sufficient to reach a constant response. The measurement data phase is the time interval during which gas sample measurements can be made that meet the acceptance criteria of this protocol. The refresh phase then purges the EC cells with CO-free air. The refresh phase replenishes requisite  $O_2$  and moisture in the electrolyte reserve and provides a mechanism to de-gas or desorb any interference gas scrubbers or filters so as to enable a stable CO EC cell response. There are four primary types of sampling runs: pre- sampling calibrations; stack gas sampling; post-sampling calibration checks; and measurement system repeatability checks. Stack gas sampling runs can be chained together for extended evaluations, providing all other procedural specifications are met.

*3.10 Sampling Day.* A time not to exceed twelve hours from the time of the pre-sampling calibration to the post-sampling calibration check. During this time, stack gas sampling runs can be repeated without repeated recalibrations, providing all other sampling specifications have been met.

*3.11 Pre-Sampling Calibration/Post-Sampling Calibration Check.* The protocols executed at the beginning and end of each sampling day to bracket measurement readings with controlled performance checks.

3.12 Performance-Established Configuration. The EC cell and sampling system configuration that existed at the time that it initially met the performance requirements of this protocol.

4.0 Interferences.

When present in sufficient concentrations, NO and  $NO_2$  are two gas species that have been reported to interfere with CO concentration measurements. In the likelihood of this occurrence, it is the protocol user's responsibility to employ and properly maintain an appropriate CO EC cell filter or scrubber for removal of these gases, as described in Section 6.2.12.

5.0 Safety. [Reserved]

6.0 Equipment and Supplies.

6.1 What equipment do I need for the measurement system?

The system must maintain the gas sample at conditions that will prevent moisture condensation in the sample transport lines, both before and as the sample gas contacts the EC cells. The essential components of the measurement system are described below.

6.2 Measurement System Components.

*6.2.1 Sample Probe.* A single extraction-point probe constructed of glass, stainless steel or other non-reactive material, and of length sufficient to reach any designated sampling point. The sample probe must be designed to prevent plugging due to condensation or particulate matter.

6.2.2 Sample Line. Non-reactive tubing to transport the effluent from the sample probe to the EC cell.

6.2.3 Calibration Assembly (optional). A three-way valve assembly or equivalent to introduce calibration gases at ambient pressure at the exit end of the sample probe during calibration checks. The assembly must be designed such that only stack gas or calibration gas flows in the sample line and all gases flow through any gas path filters.

6.2.4 Particulate Filter (optional). Filters before the inlet of the EC cell to prevent accumulation of particulate material in the measurement system and extend the useful life of the components. All filters must be fabricated of materials that are non-reactive to the gas mixtures being sampled.

6.2.5 Sample Pump. A leak-free pump to provide undiluted sample gas to the system at a flow rate sufficient to minimize the response time of the measurement system. If located upstream of the EC cells, the pump must be constructed of a material that is non-reactive to the gas mixtures being sampled.

6.2.8 Sample Flow Rate Monitoring. An adjustable rotameter or equivalent device used to adjust and maintain the sample flow rate through the analyzer as prescribed.

*6.2.9 Sample Gas Manifold (optional).* A manifold to divert a portion of the sample gas stream to the analyzer and the remainder to a by-pass discharge vent. The sample gas manifold may also include provisions for introducing calibration gases directly to the analyzer. The manifold must be constructed of a material that is non-reactive to the gas mixtures being sampled.

 $6.2.10 \ EC \ cell$ . A device containing one or more EC cells to determine the CO and O<sub>2</sub> concentrations in the sample gas stream. The EC cell(s) must meet the applicable performance specifications of Section 13 of this protocol.

6.2.11 Data Recorder. A strip chart recorder, computer or digital recorder to make a record of analyzer output data. The data recorder resolution (i.e., readability) must be no greater than 1 ppm for CO; 0.1 percent for O<sub>2</sub>; and one degree (either °C or °F) for temperature. Alternatively, you may use a digital or analog meter having the same resolution to observe and manually record the analyzer responses.

6.2.12 Interference Gas Filter or Scrubber. A device to remove interfering compounds upstream of the CO EC cell. Specific interference gas filters or scrubbers used in the performance-established configuration of the analyzer must continue to be used. Such a filter or scrubber must have a means to determine when the removal agent is exhausted. Periodically replace or replenish it in accordance with the manufacturer's recommendations.

7.0 Reagents and Standards. What calibration gases are needed?

7.1 Calibration Gases. CO calibration gases for the EC cell must be CO in nitrogen or CO in a mixture of nitrogen and  $O_2$ . Use CO calibration gases with labeled concentration values certified by the manufacturer to be within ±5 percent of the label value. Dry ambient air (20.9 percent  $O_2$ ) is acceptable for calibration of the  $O_2$  cell. If needed, any lower percentage  $O_2$  calibration gas must be a mixture of  $O_2$  in nitrogen.

7.1.1 Up-Scale CO Calibration Gas Concentration. Choose one or more up-scale gas concentrations such that the average of the stack gas measurements for each stack gas sampling run are between 25 and 150 percent of those concentrations. Alternatively, choose an up-scale gas that does not exceed twice the concentration of the applicable outlet standard. If a measured gas value exceeds 150 percent of the up-scale CO calibration gas value at any time during the stack gas sampling run, the run must be discarded and repeated.

# 7.1.2 Up-Scale O<sub>2</sub> Calibration Gas Concentration.

Select an  $O_2$  gas concentration such that the difference between the gas concentration and the average stack gas measurement or reading for each sample run is less than 15 percent  $O_2$ . When the average exhaust gas  $O_2$  readings are above 6 percent, you may use dry ambient air (20.9 percent  $O_2$ ) for the up-scale  $O_2$  calibration gas.

7.1.3 Zero Gas. Use an inert gas that contains less than 0.25 percent of the up-scale CO calibration gas concentration. You may use dry air that is free from ambient CO and other combustion gas products (e.g.,  $CO_2$ ).

8.0 Sample Collection and Analysis

# 8.1 Selection of Sampling Sites.

8.1.1 Control Device Inlet. Select a sampling site sufficiently downstream of the engine so that the combustion gases should be well mixed. Use a single sampling extraction point near the center of the duct (e.g., within the 10 percent centroidal area), unless instructed otherwise.

8.1.2 Exhaust Gas Outlet. Select a sampling site located at least two stack diameters downstream of any disturbance (e.g., turbocharger exhaust, crossover junction or recirculation take-off) and at least one-half stack diameter upstream of the gas discharge to the atmosphere. Use a single sampling extraction point near the center of the duct (e.g., within the 10 percent centroidal area), unless instructed otherwise.

8.2 Stack Gas Collection and Analysis. Prior to the first stack gas sampling run, conduct that the pre-sampling calibration in accordance with Section 10.1. Use Figure 1 to record all data. Zero the analyzer with zero gas. Confirm and record that the

scrubber media color is correct and not exhausted. Then position the probe at the sampling point and begin the sampling run at the same flow rate used during the up-scale calibration. Record the start time. Record all EC cell output responses and the flow rate during the "sample conditioning phase" once per minute until constant readings are obtained. Then begin the "measurement data phase" and record readings every 15 seconds for at least two minutes (or eight readings), or as otherwise required to achieve two continuous minutes of data that meet the specification given in Section 13.1. Finally, perform the "refresh phase" by introducing dry air, free from CO and other combustion gases, until several minute-to-minute readings of consistent value have been obtained. For each run use the "measurement data phase" readings to calculate the average stack gas CO and  $O_2$  concentrations.

8.3 EC Cell Rate. Maintain the EC cell sample flow rate so that it does not vary by more than  $\pm 10$  percent throughout the presampling calibration, stack gas sampling and post-sampling calibration check. Alternatively, the EC cell sample flow rate can be maintained within a tolerance range that does not affect the gas concentration readings by more than  $\pm 3$  percent, as instructed by the EC cell manufacturer.

9.0 Quality Control (Reserved)

10.0 Calibration and Standardization

10.1 Pre-Sampling Calibration. Conduct the following protocol once for each nominal range to be used on each EC cell before performing a stack gas sampling run on each field sampling day. Repeat the calibration if you replace an EC cell before completing all of the sampling runs. There is no prescribed order for calibration of the EC cells; however, each cell must complete the measurement data phase during calibration. Assemble the measurement system by following the manufacturer's recommended protocols including for preparing and preconditioning the EC cell. Assure the measurement system has no leaks and verify the gas scrubbing agent is not depleted. Use Figure 1 to record all data.

10.1.1 Zero Calibration. For both the  $O_2$  and CO cells, introduce zero gas to the measurement system (e.g., at the calibration assembly) and record the concentration reading every minute until readings are constant for at least two consecutive minutes. Include the time and sample flow rate. Repeat the steps in this section at least once to verify the zero calibration for each component gas.

10.1.2 Zero Calibration Tolerance. For each zero gas introduction, the zero level output must be less than or equal to  $\pm 3$  percent of the up-scale gas value or  $\pm 1$  ppm, whichever is less restrictive, for the CO channel and less than or equal to  $\pm 0.3$  percent O<sub>2</sub> for the O<sub>2</sub> channel.

10.1.3 Up-Scale Calibration. Individually introduce each calibration gas to the measurement system (e.g., at the calibration assembly) and record the start time. Record all EC cell output responses and the flow rate during this "sample conditioning phase" once per minute until readings are constant for at least two minutes. Then begin the "measurement data phase" and record readings every 15 seconds for a total of two minutes, or as otherwise required. Finally, perform the "refresh phase" by introducing dry air, free from CO and other combustion gases, until readings are constant for at least two consecutive minutes. Then repeat the steps in this section at least once to verify the calibration for each component gas. Introduce all gases to flow through the entire sample handling system (i.e., at the exit end of the sampling probe or the calibration assembly).

10.1.4 Up-Scale Calibration Error. The mean of the difference of the "measurement data phase" readings from the reported standard gas value must be less than or equal to  $\pm 5$  percent or  $\pm 1$  ppm for CO or  $\pm 0.5$  percent O<sub>2</sub>, whichever is less restrictive, respectively. The maximum allowable deviation from the mean measured value of any single "measurement data phase" reading must be less than or equal to  $\pm 2$  percent or  $\pm 1$  ppm for CO or  $\pm 0.5$  percent O<sub>2</sub>, whichever is less restrictive, respectively.

10.2 Post-Sampling Calibration Check. Conduct a stack gas post-sampling calibration check after the stack gas sampling run or set of runs and within 12 hours of the initial calibration. Conduct up-scale and zero calibration checks using the protocol in Section 10.1. Make no changes to the sampling system or EC cell calibration until all post-sampling calibration checks have been recorded. If either the zero or up-scale calibration error exceeds the respective specification in Sections 10.1.2 and 10.1.4 then all measurement data collected since the previous successful calibrations are invalid and re-calibration and re-sampling are required. If the sampling system is disassembled or the EC cell calibration is adjusted, repeat the calibration check before conducting the next analyzer sampling run.

11.0 Analytical Procedure

The analytical procedure is fully discussed in Section 8.

12.0 Calculations and Data Analysis

Determine the CO and  $O_2$  concentrations for each stack gas sampling run by calculating the mean gas concentrations of the data recorded during the "measurement data phase".

13.0 Protocol Performance

Use the following protocols to verify consistent analyzer performance during each field sampling day.

13.1 Measurement Data Phase Performance Check. Calculate the mean of the readings from the "measurement data phase". The maximum allowable deviation from the mean for each of the individual readings is  $\pm 2$  percent, or  $\pm 1$  ppm, whichever is less restrictive. Record the mean value and maximum deviation for each gas monitored. Data must conform to Section 10.1.4. The EC cell flow rate must conform to the specification in Section 8.3.

# **Example:**

A measurement data phase is invalid if the maximum deviation of any single reading comprising that mean is greater than  $\pm 2$  percent *or*  $\pm 1$  ppm (the default criteria). For example, if the mean = 30 ppm, single readings of below 29 ppm and above 31 ppm are disallowed).

13.2 Interference Check. Before the initial use of the EC cell and interference gas scrubber in the field, and semi-annually thereafter, challenge the interference gas scrubber with NO and  $NO_2$  gas standards that are generally recognized as representative of diesel-fueled engine NO and  $NO_2$  emission values. Record the responses displayed by the CO EC cell and other pertinent data on Figure 1 or a similar form.

*13.2.1 Interference Response.* The combined NO and NO<sub>2</sub> interference response should be less than or equal to  $\pm 5$  percent of the up-scale CO calibration gas concentration.

*13.3 Repeatability Check.* Conduct the following check once for each nominal range that is to be used on the CO EC cell within 5 days prior to each field sampling program. If a field sampling program lasts longer than 5 days, repeat this check every 5 days. Immediately repeat the check if the EC cell is replaced or if the EC cell is exposed to gas concentrations greater than 150 percent of the highest up-scale gas concentration.

13.3.1 Repeatability Check Procedure. Perform a complete EC cell sampling run (all three phases) by introducing the CO calibration gas to the measurement system and record the response. Follow Section 10.1.3. Use Figure 1 to record all data. Repeat the run three times for a total of four complete runs. During the four repeatability check runs, do not adjust the system except where necessary to achieve the correct calibration gas flow rate at the analyzer.

13.3.2 Repeatability Check Calculations. Determine the highest and lowest average "measurement data phase" CO concentrations from the four repeatability check runs and record the results on Figure 1 or a similar form. The absolute value of the difference between the maximum and minimum average values recorded must not vary more than  $\pm 3$  percent or  $\pm 1$  ppm of the up-scale gas value, whichever is less restrictive.

14.0 Pollution Prevention (Reserved)

15.0 Waste Management (Reserved)

16.0 Alternative Procedures (Reserved)

17.0 References

(1) "Development of an Electrochemical Cell Emission Analyzer Test Protocol", Topical Report, Phil Juneau, Emission Monitoring, Inc., July 1997.

(2) "Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Emissions from Natural Gas-Fired Engines, Boilers, and Process Heaters Using Portable Analyzers", EMC Conditional Test Protocol 30 (CTM-30), Gas Research Institute Protocol GRI-96/0008, Revision 7, October 13, 1997.

(3) "ICAC Test Protocol for Periodic Monitoring", EMC Conditional Test Protocol 34 (CTM-034), The Institute of Clean Air Companies, September 8, 1999.

(4) "Code of Federal Regulations", Protection of Environment, <u>40 CFR</u>, Part 60, Appendix A, Methods 1-4; 10.

Table 1: Appendix A-Sampling Run Data.

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# National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

Facil	ity	Engine	e I.D		Da	ate							
Run '	Туре:	$\bigcirc$			(	)		(	)			$\bigcirc$	
(X)		Pre-Sa	mple Ca	libratio	n S	tack Gas	s Sample	P	ost-Samp	le Cal. Check		Repe	atability Check
	Run #	1	1	2	2	3	3	4	4	Time	Scrub OK	).	Flow- Rate
	Gas	O <sub>2</sub>	СО	O <sub>2</sub>	CO	O <sub>2</sub>	CO	<b>O</b> <sub>2</sub>	СО				
	Sample Cond. Phase												
	"												
	"												
	"												
	"												
	Measurement Data Phase												
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	"												
	"												
	"												
	Mean												
	Refresh Phase												
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	"												
	"												
	"												

[<u>78 FR 6721</u>, Jan. 30, 2013]

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# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

## Subpart A—General Provisions

## § 60.1 Applicability.

(a) Except as provided in <u>subparts B</u>, <u>Ba</u>, and <u>C of this part</u>, the provisions of this part apply to the owner or operator of any stationary source which contains an affected facility, the construction or modification of which is commenced after the date of publication in this part of any standard (or, if earlier, the date of publication of any proposed standard) applicable to that facility.

(b) Any new or revised standard of performance promulgated pursuant to section 111(b) of the Act shall apply to the owner or operator of any stationary source which contains an affected facility, the construction or modification of which is commenced after the date of publication in this part of such new or revised standard (or, if earlier, the date of publication of any proposed standard) applicable to that facility.

(c) In addition to complying with the provisions of this part, the owner or operator of an affected facility may be required to obtain an operating permit issued to stationary sources by an authorized State air pollution control agency or by the Administrator of the U.S. Environmental Protection Agency (EPA) pursuant to Title V of the Clean Air Act (Act) as amended November 15, 1990 (<u>42 U.S.C. 7661</u>). For more information about obtaining an operating permit see <u>part 70 of this chapter</u>.

(d) Site-specific standard for Merck & Co., Inc.'s Stonewall Plant in Elkton, Virginia.

(1) This paragraph applies only to the pharmaceutical manufacturing facility, commonly referred to as the Stonewall Plant, located at Route 340 South, in Elkton, Virginia ("site").

(2) Except for compliance with 40 CFR 60.49b(u), the site shall have the option of either complying directly with the requirements of this part, or reducing the site-wide emissions caps in accordance with the procedures set forth in a permit issued pursuant to 40 CFR 52.2454. If the site chooses the option of reducing the site-wide emissions caps in accordance with the procedures set forth in such permit, the requirements of such permit shall apply in lieu of the otherwise applicable requirements of this part.

(3) Notwithstanding the provisions of <u>paragraph (d)(2)</u> of this section, for any provisions of this part except for Subpart Kb, the owner/operator of the site shall comply with the applicable provisions of this part if the Administrator determines that compliance with the provisions of this part is necessary for achieving the objectives of the regulation and the Administrator notifies the site in accordance with the provisions of the permit issued pursuant to  $\frac{40 \text{ CFR 52.2454}}{2.2454}$ .

[<u>40 FR 53346</u>, Nov. 17, 1975, as amended at <u>55 FR 51382</u>, Dec. 13, 1990; <u>59 FR 12427</u>, Mar. 16, 1994; <u>62 FR 52641</u>, Oct. 8, 1997; <u>88 FR 80542</u>, Nov. 17, 2023]

# § 60.2 Definitions.

The terms used in this part are defined in the Act or in this section as follows:

Act means the Clean Air Act (<u>42 U.S.C. 7401</u> et seq.)

Administrator means the Administrator of the Environmental Protection Agency or his authorized representative.

Affected facility means, with reference to a stationary source, any apparatus to which a standard is applicable.

*Alternative method* means any method of sampling and analyzing for an air pollutant which is not a reference or equivalent method but which has been demonstrated to the Administrator's satisfaction to, in specific cases, produce results adequate for his determination of compliance.

*Approved permit program* means a State permit program approved by the Administrator as meeting the requirements of <u>part</u> <u>70 of this chapter</u> or a Federal permit program established in this chapter pursuant to Title V of the Act (<u>42 U.S.C. 7661</u>).

*Capital expenditure* means an expenditure for a physical or operational change to an existing facility which exceeds the product of the applicable "annual asset guideline repair allowance percentage" specified in the latest edition of Internal Revenue Service (IRS) Publication 534 and the existing facility's basis, as defined by section 1012 of the Internal Revenue Code. However, the total expenditure for a physical or operational change to an existing facility must not be reduced by any "excluded additions" as defined in IRS Publication 534, as would be done for tax purposes.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

*Clean coal technology demonstration project* means a project using funds appropriated under the heading 'Department of Energy-Clean Coal Technology', up to a total amount of \$2,500,000,000 for commercial demonstrations of clean coal technology, or similar projects funded through appropriations for the Environmental Protection Agency.

*Commenced* means, with respect to the definition of *new source* in section 111(a)(2) of the Act, that an owner or operator has undertaken a continuous program of construction or modification or that an owner or operator has entered into a contractual obligation to undertake and complete, within a reasonable time, a continuous program of construction or modification.

Construction means fabrication, erection, or installation of an affected facility.

*Continuous monitoring system* means the total equipment, required under the emission monitoring sections in applicable subparts, used to sample and condition (if applicable), to analyze, and to provide a permanent record of emissions or process parameters.

*Electric utility steam generating unit* means any steam electric generating unit that is constructed for the purpose of supplying more than one-third of its potential electric output capacity and more than 25 MW electrical output to any utility power distribution system for sale. Any steam supplied to a steam distribution system for the purpose of providing steam to a steam-electric generator that would produce electrical energy for sale is also considered in determining the electrical energy output capacity of the affected facility.

*Equivalent method* means any method of sampling and analyzing for an air pollutant which has been demonstrated to the Administrator's satisfaction to have a consistent and quantitatively known relationship to the reference method, under specified conditions.

*Excess Emissions and Monitoring Systems Performance Report* is a report that must be submitted periodically by a source in order to provide data on its compliance with stated emission limits and operating parameters, and on the performance of its monitoring systems.

*Existing facility* means, with reference to a stationary source, any apparatus of the type for which a standard is promulgated in this part, and the construction or modification of which was commenced before the date of proposal of that standard; or any apparatus which could be altered in such a way as to be of that type.

*Force majeure* means, for purposes of  $\S$  60.8, an event that will be or has been caused by circumstances beyond the control of the affected facility, its contractors, or any entity controlled by the affected facility that prevents the owner or operator from complying with the regulatory requirement to conduct performance tests within the specified timeframe despite the affected facility's best efforts to fulfill the obligation. Examples of such events are acts of nature, acts of war or terrorism, or equipment failure or safety hazard beyond the control of the affected facility.

*Isokinetic sampling* means sampling in which the linear velocity of the gas entering the sampling nozzle is equal to that of the undisturbed gas stream at the sample point.

*Issuance* of a part 70 permit will occur, if the State is the permitting authority, in accordance with the requirements of <u>part 70</u> <u>of this chapter</u> and the applicable, approved State permit program. When the EPA is the permitting authority, issuance of a Title V permit occurs immediately after the EPA takes final action on the final permit.

*Malfunction* means any sudden, infrequent, and not reasonably preventable failure of air pollution control equipment, process equipment, or a process to operate in a normal or usual manner. Failures that are caused in part by poor maintenance or careless operation are not malfunctions.

*Modification* means any physical change in, or change in the method of operation of, an existing facility which increases the amount of any air pollutant (to which a standard applies) emitted into the atmosphere by that facility or which results in the emission of any air pollutant (to which a standard applies) into the atmosphere not previously emitted.

*Monitoring device* means the total equipment, required under the monitoring of operations sections in applicable subparts, used to measure and record (if applicable) process parameters.

Nitrogen oxides means all oxides of nitrogen except nitrous oxide, as measured by test methods set forth in this part.

One-hour period means any 60-minute period commencing on the hour.

*Opacity* means the degree to which emissions reduce the transmission of light and obscure the view of an object in the background.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

*Owner or operator* means any person who owns, leases, operates, controls, or supervises an affected facility or a stationary source of which an affected facility is a part.

Part 70 permit means any permit issued, renewed, or revised pursuant to part 70 of this chapter.

*Particulate matter* means any finely divided solid or liquid material, other than uncombined water, as measured by the reference methods specified under each applicable subpart, or an equivalent or alternative method.

*Permit program* means a comprehensive State operating permit system established pursuant to title V of the Act (<u>42 U.S.C.</u> <u>7661</u>) and regulations codified in <u>part 70 of this chapter</u> and applicable State regulations, or a comprehensive Federal operating permit system established pursuant to title V of the Act and regulations codified in this chapter.

*Permitting authority* means:

(1) The State air pollution control agency, local agency, other State agency, or other agency authorized by the Administrator to carry out a permit program under <u>part 70 of this chapter</u>; or

(2) The Administrator, in the case of EPA-implemented permit programs under title V of the Act (<u>42 U.S.C. 7661</u>).

Proportional sampling means sampling at a rate that produces a constant ratio of sampling rate to stack gas flow rate.

*Reactivation of a very clean coal-fired electric utility steam generating unit* means any physical change or change in the method of operation associated with the commencement of commercial operations by a coal-fired utility unit after a period of discontinued operation where the unit:

(1) Has not been in operation for the two-year period prior to the enactment of the Clean Air Act Amendments of 1990, and the emissions from such unit continue to be carried in the permitting authority's emissions inventory at the time of enactment;

(2) Was equipped prior to shut-down with a continuous system of emissions control that achieves a removal efficiency for sulfur dioxide of no less than 85 percent and a removal efficiency for particulates of no less than 98 percent;

(3) Is equipped with low-NO<sub>X</sub> burners prior to the time of commencement of operations following reactivation; and

(4) Is otherwise in compliance with the requirements of the Clean Air Act.

Reference method means any method of sampling and analyzing for an air pollutant as specified in the applicable subpart.

*Repowering* means replacement of an existing coal-fired boiler with one of the following clean coal technologies: atmospheric or pressurized fluidized bed combustion, integrated gasification combined cycle, magnetohydrodynamics, direct and indirect coal-fired turbines, integrated gasification fuel cells, or as determined by the Administrator, in consultation with the Secretary of Energy, a derivative of one or more of these technologies, and any other technology capable of controlling multiple combustion emissions simultaneously with improved boiler or generation efficiency and with significantly greater waste reduction relative to the performance of technology in widespread commercial use as of November 15, 1990. Repowering shall also include any oil and/or gas-fired unit which has been awarded clean coal technology demonstration funding as of January 1, 1991, by the Department of Energy.

*Run* means the net period of time during which an emission sample is collected. Unless otherwise specified, a run may be either intermittent or continuous within the limits of good engineering practice.

Shutdown means the cessation of operation of an affected facility for any purpose.

Six-minute period means any one of the 10 equal parts of a one-hour period.

Standard means a standard of performance proposed or promulgated under this part.

Standard conditions means a temperature of 293 K (68F) and a pressure of 101.3 kilopascals (29.92 in Hg).

Startup means the setting in operation of an affected facility for any purpose.

*State* means all non-Federal authorities, including local agencies, interstate associations, and State-wide programs, that have delegated authority to implement:

(1) The provisions of this part; and/or

(2) the permit program established under part 70 of this chapter. The term State shall have its conventional meaning where clear from the context.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Stationary source means any building, structure, facility, or installation which emits or may emit any air pollutant.

*Title V permit* means any permit issued, renewed, or revised pursuant to Federal or State regulations established to implement title V of the Act (<u>42 U.S.C. 7661</u>). A title V permit issued by a State permitting authority is called a part 70 permit in this part.

*Volatile Organic Compound* means any organic compound which participates in atmospheric photochemical reactions; or which is measured by a reference method, an equivalent method, an alternative method, or which is determined by procedures specified under any subpart.

[<u>44 FR 55173</u>, Sept. 25, 1979, as amended at <u>45 FR 5617</u>, Jan. 23, 1980; <u>45 FR 85415</u>, Dec. 24, 1980; <u>54 FR 6662</u>, Feb. 14, 1989; <u>55 FR 51382</u>, Dec. 13, 1990; <u>57 FR 32338</u>, July 21, 1992; <u>59 FR 12427</u>, Mar. 16, 1994; <u>72 FR 27442</u>, May 16, 2007]

#### § 60.3 Units and abbreviations.

Used in this part are abbreviations and symbols of units of measure. These are defined as follows:

(a) System International (SI) units of measure:

- A—ampere
- g—gram
- Hz-hertz
- J—joule
- K-degree Kelvin
- kg-kilogram
- m—meter
- m<sup>3</sup>—cubic meter
- mg—milligram—10<sup>-3</sup> gram
- mm—millimeter—10<sup>-3</sup> meter
- Mg—megagram—10<sup>6</sup> gram
- mol-mole
- N-newton
- ng—nanogram—10<sup>-9</sup> gram
- nm—nanometer—10<sup>-9</sup> meter
- Pa-pascal
- s—second
- V—volt
- W-watt
- $\Omega$ —ohm
- µg—microgram—10<sup>-6</sup> gram
- (b) Other units of measure:
- Btu—British thermal unit
- °C—degree Celsius (centigrade)
- cal-calorie
- cfm—cubic feet per minute

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

cu ft-cubic feet dcf-dry cubic feet dcm-dry cubic meter dscf-dry cubic feet at standard conditions dscm-dry cubic meter at standard conditions eq-equivalent °F-degree Fahrenheit ft-feet gal-gallon gr-grain g-eq-gram equivalent hr-hour in-inch k-1,000 l-liter lpm-liter per minute lb-pound meq-milliequivalent min-minute ml-milliliter mol. wt.-molecular weight ppb-parts per billion ppm-parts per million psia-pounds per square inch absolute psig-pounds per square inch gage °R-degree Rankine scf—cubic feet at standard conditions scfh-cubic feet per hour at standard conditions scm-cubic meter at standard conditions sec-second sq ft-square feet std-at standard conditions (c) Chemical nomenclature: CdS-cadmium sulfide CO-carbon monoxide CO<sub>2</sub>-carbon dioxide

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

HCl-hydrochloric acid

Hg-mercury

H<sub>2</sub>O-water

H<sub>2</sub>S-hydrogen sulfide

H<sub>2</sub>SO<sub>4</sub>—sulfuric acid

N<sub>2</sub>—nitrogen

NO—nitric oxide

NO2-nitrogen dioxide

NO<sub>X</sub>—nitrogen oxides

O<sub>2</sub>—oxygen

SO<sub>2</sub>—sulfur dioxide

SO<sub>3</sub>—sulfur trioxide

SO<sub>X</sub>—sulfur oxides

(d) Miscellaneous:

A.S.T.M.—American Society for Testing and Materials

[<u>42 FR 37000</u>, July 19, 1977; <u>42 FR 38178</u>, July 27, 1977]

## § 60.4 Address.

(a) All requests, reports, applications, submittals, and other communications to the Administrator pursuant to this part shall be submitted in duplicate to the appropriate Regional Office of the U.S. Environmental Protection Agency to the attention of the Director of the Division indicated in the following table.

	Table 1 to Paragraph (a)					
Region	Address	State				
I	Director, Enforcement and Compliance Assurance Division, U.S. EPA Region I, 5 Post Office Square—Suite 100 (04-2), Boston, MA 02109-3912, Attn: Air Compliance Clerk	Connecticut, Maine, Massachusetts, New Hampshire, Rhode Island, Vermont.				
п	Director, Air and Waste Management Division, U.S. Environmental Protection Agency, Federal Office Building, 26 Federal Plaza (Foley Square), New York, NY 10278	New Jersey, New York, Puerto Rico, Virgin Islands.				
III	Director, Air Protection Division, Mail Code 3AP00, 1650 Arch Street, Philadelphia, PA 19103-2029	Delaware, District of Columbia, Maryland, Pennsylvania, Virginia, West Virginia.				
IV	Director, Air and Radiation Division, 61 Forsyth Street SW, Atlanta, Georgia 30303-8960	Alabama, Florida, Georgia, Kentucky, Mississippi, North Carolina, South Carolina, Tennessee.				
V	Director, Air and Radiation Division, U.S. Environmental Protection Agency, 77 West Jackson Boulevard, Chicago, IL 60604-3590	Illinois, Indiana, Michigan, Minnesota, Ohio, Wisconsin.				
VI	Director; Enforcement and Compliance	Arkansas, Louisiana, New Mexico, Oklahoma, Texas.				

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

	Table 1 to Paragraph (a)					
Region	Address	State				
	Assurance Division; U.S. Environmental Protection Agency, 1201 Elm Street, Suite 500, Mail Code 6ECD, Dallas, Texas 75270-2102					
VII	Director, Air and Waste Management Division, 11201 Renner Boulevard, Lenexa, Kansas 66219	Iowa, Kansas, Missouri, Nebraska.				
VIII	Director, Air and Toxics Technical Enforcement Program, Office of Enforcement, Compliance and Environmental Justice, Mail Code 8ENF- AT, 1595 Wynkoop Street, Denver, CO 80202-1129	Colorado, Montana, North Dakota, South Dakota, Utah, Wyoming.				
IX	Director, Enforcement and Compliance Assurance Division (ENF 2-1), U.S. Environmental Protection Agency Region IX, 75 Hawthorne Street, San Francisco, CA 94105	Arizona, California, Hawaii and Nevada; the territories of American Samoa and Guam; the Commonwealth of the Northern Mariana Islands; the territories of Baker Island, Howland Island, Jarvis Island, Johnston Atoll, Kingman Reef, Midway Atoll, Palmyra Atoll, and Wake Islands; and certain U.S. Government activities in the freely associated states of the Republic of the Marshall Islands, the Federated States of Micronesia, and the Republic of Palau.				
x	Director, Air and Waste Management Division, U.S. Environmental Protection Agency, 1200 Sixth Avenue, Seattle, WA 98101	Alaska, Oregon, Idaho, Washington.				

(b) Section 111(c) directs the Administrator to delegate to each State, when appropriate, the authority to implement and enforce standards of performance for new stationary sources located in such State. All information required to be submitted to EPA under <u>paragraph (a)</u> of this section, must also be submitted to the appropriate State Agency of any State to which this authority has been delegated (provided, that each specific delegation may except sources from a certain Federal or State reporting requirement). The appropriate mailing address for those States whose delegation request has been approved is as follows:

(1) [Reserved]

(2) State of Alabama: Alabama Department of Environmental Management, P.O. Box 301463, Montgomery, Alabama 36130-1463.

(3) State of Alaska, Department of Environmental Conservation, Pouch O, Juneau, AK 99811.

(4) Arizona:

Arizona Department of Environmental Quality, Suite #160, 1110 West Washington Street, Phoenix, AZ 85007.

Maricopa County Air Quality Department, 301 West Jefferson Street, Phoenix, AZ 85003.

Pima County Department of Environmental Quality, 33 North Stone Avenue, Suite 700, Tucson, AZ 85701.

Pinal County Air Quality Department, 31 North Pinal Street, Building F, Florence, AZ 85132.

Note 1 to paragraph (b)(4):

For tables listing the delegation status of agencies in Region IX, see <u>paragraph (d)</u> of this section.

(5) State of Arkansas: Chief, Division of Air Pollution Control, Arkansas Department of Pollution Control and Ecology, 8001 National Drive, P.O. Box 9583, Little Rock, AR 72209.

(6) California:

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Amador Air District, 810 Court Street, Jackson, CA 95642. Antelope Valley Air Quality Management District, 2551 W Avenue H, Lancaster, CA 93536. Bay Area Air Quality Management District, 375 Beale Street, Suite 600, San Francisco, CA 94105. Butte County Air Quality Management District, 629 Entler Avenue, Suite 15, Chico, CA 95928. Calaveras County Air Pollution Control District, 891 Mountain Ranch Road, Building E, San Andreas, CA 95249. Colusa County Air Pollution Control District, 100 Sunrise Blvd., Suite A, Colusa, CA 95932-3246. El Dorado County Air Quality Management District, 330 Fair Lane, Placerville, CA 95667-4100. Eastern Kern Air Pollution Control District, 2700 "M" Street, Suite 302, Bakersfield, CA 93301-2370. Feather River Air Quality Management District, 541 Washington Avenue, Yuba City, CA 95991. Glenn County Air Pollution Control District, 720 N Colusa Street, P.O. Box 351, Willows, CA 95988-0351. Great Basin Unified Air Pollution Control District, 157 Short Street, Bishop, CA 93514-3537. Imperial County Air Pollution Control District, 150 South Ninth Street, El Centro, CA 92243-2839. Lake County Air Quality Management District, 2617 S Main St., Lakeport, CA 95453-5405. Lassen County Air Pollution Control District, 720 South St., Susanville, CA 96130. Mariposa County Air Pollution Control District, P.O. Box 5, Mariposa, CA 95338. Mendocino County Air Quality Management District, 306 E Gobbi Street, Ukiah, CA 95482-5511. Modoc County Air Pollution Control District, 202 W 4th Street, Alturas, CA 96101. Mojave Desert Air Quality Management District, 14306 Park Avenue, Victorville, CA 92392-2310. Monterey Bay Air Resources District, 24580 Silver Cloud Court, Monterey, CA 93940. North Coast Unified Air Quality Management District, 707 L Street, Eureka, CA 95501-3327. Northern Sierra Air Quality Management District, 200 Litton Drive, Suite 320, Grass Valley, CA 95945-2509. Northern Sonoma County Air Pollution Control District, 150 Matheson Street, Healdsburg, CA 95448-4908. Placer County Air Pollution Control District, 110 Maple Street, Auburn, CA 95603. Sacramento Metropolitan Air Quality Management District, 777 12th Street, Suite 300, Sacramento, CA 95814-1908. San Diego County Air Pollution Control District, 10124 Old Grove Road, San Diego, CA 92131-1649. San Joaquin Valley Air Pollution Control District, 1990 E Gettysburg, Fresno, CA 93726. San Luis Obispo County Air Pollution Control District, 3433 Roberto Court, San Luis Obispo, CA 93401-7126. Santa Barbara County Air Pollution Control District, 260 North San Antonio Road, Suite A, Santa Barbara, CA 93110-1315. Shasta County Air Quality Management District, 1855 Placer Street, Suite 101, Redding, CA 96001-1759. Siskiyou County Air Pollution Control District, 525 So. Foothill Drive, Yreka, CA 96097-3036. South Coast Air Quality Management District, 21865 Copley Drive, Diamond Bar, CA 91765-4182. Tehama County Air Pollution Control District, P.O. Box 1169 (1834 Walnut Street), Red Bluff, CA 96080-0038. Tuolumne County Air Pollution Control District, 2 South Green St., Sonora, CA 95370-4618. Ventura County Air Pollution Control District, 4567 Telephone Road, 2nd Floor, Ventura, CA 93003-5417. Yolo-Solano Air Quality Management District, 1947 Galileo Court, Suite 103, Davis, CA 95618. Note 2 to paragraph (b)(6):

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

For tables listing the delegation status of agencies in Region IX, see <u>paragraph (d)</u> of this section.

(7) State of Colorado, Department of Public Health and Environment, 4300 Cherry Creek Drive South, Denver, CO 80222-1530.

Note:

For a table listing Region VIII's NSPS delegation status, see paragraph (c) of this section.

(8) State of Connecticut, Compliance Analysis and Coordination Unit, Bureau of Air Management, Department of Energy and Environmental Protection, 79 Elm Street, 5th Floor, Hartford, CT 06106-5127.

(9) State of Delaware, Department of Natural Resources & Environmental Control, 89 Kings Highway, P.O. Box 1401, Dover, Delaware 19903.

(10) District of Columbia, Department of Public Health, Air Quality Division, 51 N Street, NE., Washington, DC 20002.

(11) State of Florida: Florida Department of Environmental Protection, Division of Air Resources Management, 2600 Blair Stone Road, MS 5500, Tallahassee, Florida 32399-2400.

(12) State of Georgia: Georgia Department of Natural Resources, Environmental Protection Division, Air Protection Branch, 4244 International Parkway, Suite 120, Atlanta, Georgia 30354.

(13) Hawaii:

Clean Air Branch, Hawaii Department of Health, 2827 Waimano Home Road, #130 Pearl City, HI 96782.

Note 4 to paragraph (b)(13):

For tables listing the delegation status of agencies in Region IX, see <u>paragraph (d)</u> of this section.

(14) State of Idaho, Department of Health and Welfare, Statehouse, Boise, ID 83701.

(15) State of Illinois: Illinois Environmental Protection Agency, 1021 North Grand Avenue East, Springfield, Illinois 62794.

(16) State of Indiana: Indiana Department of Environmental Management, Office of Air Quality, 100 North Senate Avenue, Indianapolis, Indiana 46204.

(17) State of Iowa: Iowa Department of Natural Resources, Environmental Protection Division, Air Quality Bureau, 7900 Hickman Road, Suite 1, Urbandale, IA 50322.

(18) State of Kansas: Kansas Department of Health and Environment, Bureau of Air and Radiation, 1000 S.W. Jackson, Suite 310, Topeka, KS 66612-1366.

(19) Commonwealth of Kentucky: Kentucky Department for Environmental Protection, Division for Air Quality, 300 Sower Boulevard, 2nd Floor, Frankfort, Kentucky 40601 or local agency, Louisville Metro Air Pollution Control District, 701 W. Ormsby Ave., Suite 303, Louisville, Kentucky 40203.

(20) State of Louisiana: Louisiana Department of Environmental Quality, P.O. Box 4301, Baton Rouge, Louisiana 70821-4301.

Note:

For a list of delegated standards for Louisiana (excluding Indian country), see paragraph (e)(2) of this section.

(21) State of Maine, Maine Department of Environmental Protection, Bureau of Air Quality, 17 State House Station, Augusta, ME 04333-0017.

(22) State of Maryland, Department of the Environment, 1800 Washington Boulevard, Suite 705, Baltimore, Maryland 21230.

(23) Commonwealth of Massachusetts, Massachusetts Department of Environmental Protection, Division of Air and Climate Programs, One Winter Street, Boston, MA 02108.

(24) State of Michigan: Michigan Department of Natural Resources and Environment, Air Quality Division, P.O. Box 30028, Lansing, Michigan 48909.

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(25) State of Minnesota: Minnesota Pollution Control Agency, Division of Air Quality, 520 Lafayette Road North, St. Paul, Minnesota 55155.

(26) State of Mississippi: Hand Deliver or Courier: Mississippi Department of Environmental Quality, Office of Pollution Control, Air Division, 515 East Amite Street, Jackson, Mississippi 39201, Mailing Address: Mississippi Department of Environmental Quality, Office of Pollution Control, Air Division, P.O. Box 2261, Jackson, Mississippi 39225.

(27) State of Missouri: Missouri Department of Natural Resources, Division of Environmental Quality, P.O. Box 176, Jefferson City, MO 65102.

(28) State of Montana, Department of Environmental Quality, 1520 E. 6th Ave., PO Box 200901, Helena, MT 59620-0901.

Note:

For a table listing Region VIII's NSPS delegation status, see <u>paragraph (c)</u> of this section.

(29) State of Nebraska, Nebraska Department of Environmental Control, P.O. Box 94877, State House Station, Lincoln, NE 68509.

Lincoln-Lancaster County Health Department, Division of Environmental Health, 2200 St. Marys Avenue, Lincoln, NE 68502

(30) Nevada:

Nevada Division of Environmental Protection, 901 South Stewart Street, Suite 4001, Carson City, NV 89701-5249.

Clark County Division of Air Quality, 500 S Grand Central Parkway, 1st Floor, P.O. Box 555210, Las Vegas, NV 89155-5210.

Northern Nevada Public Health, Air Quality Management Division, 1001 E 9th Street, Building B, Reno, NV 89512.

Note 7 to paragraph (b)(30):

For tables listing the delegation status of agencies in Region IX, see <u>paragraph (d)</u> of this section.

(31) State of New Hampshire, New Hampshire Department of Environmental Services, Air Resources Division, 29 Hazen Drive, P.O. Box 95, Concord, NH 03302-0095.

(32) State of New Jersey: New Jersey Department of Environmental Protection, Division of Environmental Quality, Enforcement Element, John Fitch Plaza, CN-027, Trenton, NJ 08625.

(1) The following table lists the specific source and pollutant categories that have been delegated to the states in Region II. The (X) symbol is used to indicate each category that has been delegated.

		State				
	Subpart	New Jersey	New York	Puerto Rico	Virgin Islands	
D	Fossil-Fuel Fired Steam Generators for Which Construction Commenced After August 17, 1971 (Steam Generators and Lignite Fired Steam Generators)	X	Х	X	X	
Da	Electric Utility Steam Generating Units for Which Construction Commenced After September 18, 1978	X		X		
Db	Industrial-Commercial-Institutional Steam Generating Units	X	Х	Х	X	
E	Incinerators	X	Х	Х	X	
F	Portland Cement Plants	X	Х	Х	Х	
G	Nitric Acid Plants	X	Х	Х	X	
Η	Sulfuric Acid Plants	X	Х	Х	X	
Ι	Asphalt Concrete Plants	X	Х	Х	X	
J	Petroleum Refineries—(All Categories)	X	Х	Х	X	
K	Storage Vessels for Petroleum Liquids Constructed After June 11, 1973, and	X	Х	Х	X	

		State					
	Subpart	New Jersey	New York	Puerto Rico	Virgin Islands		
	prior to May 19, 1978						
Ka	Storage Vessels for Petroleum Liquids Constructed After May 18, 1978	Х	Х	Х			
L	Secondary Lead Smelters	Х	Х	Х	X		
М	Secondary Brass and Bronze Ingot Production Plants	X	Х	Х	X		
N	Iron and Steel Plants	X	X	Х	X		
0	Sewage Treatment Plants	X	X	Х	X		
Р	Primary Copper Smelters	X	Х	Х	X		
Q	Primary Zinc Smelters	X	Х	Х	X		
R	Primary Lead Smelters	X	X	Х	X		
S	Primary Aluminum Reduction Plants	X	X	X	X		
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	X	X	X	X		
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	X	X	X	X		
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	X	X	X	X		
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	X	X	X	X		
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate	X	X	X	X		
Y	Coal Preparation Plants	X	X	X	X		
Z	Ferroally Production Facilities	X	X	X	X		
AA	Steel Plants: Electric Arc Furnaces	X	X	X	X		
AAa	Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels in Steel Plants	X	X	X			
BB	Kraft Pulp Mills	X	X	X			
CC	Glass Manufacturing Plants	X	X	X			
DD	Grain Elevators	X	X	X	-		
EE	Surface Coating of Metal Furniture	X	X	X	-		
GG	Stationary Gas Turbines	X	X	X	-		
HH	Lime Plants	X	X	X	-		
КК	Lead Acid Battery Manufacturing Plants	X	X	1	-		
LL	Metallic Mineral Processing Plants	X	X	X	-		
MM	Automobile and Light-Duty Truck Surface Coating Operations	X	X		-		
NN	Phosphate Rock Plants	X	X		-		
PP	Ammonium Sulfate Manufacturing Plants	X	X		-		
00	Graphic Art Industry Publication Rotograyure Printing	X	x	X	X		
RR	Pressure Sensitive Tape and Label Surface Coating Operations	X	X	X	-		
SS	Industrial Surface Coating: Large Appliances	X	X	X	-		
TT	Metal Coil Surface Coating	X	X	X	-		
UU	Asphalt Processing and Asphalt Roofing Manufacture	X	X	X	-		
VV	Equipment Leaks of Volatile Organic Compounds in Synthetic Organic Chemical Manufacturing Industry	X		X			
WW	Beverage Can Surface Coating Industry	X	X	X			

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			State					
	Subpart	New Jersey	New York	Puerto Rico	Virgin Islands			
XX	Bulk Gasoline Terminals	Х	Х	Х				
FFF	Flexible Vinyl and Urethane Coating and Printing	Х	X	X				
GGG	Equipment Leaks of VOC in Petroleum Refineries	Х		X				
HHH	Synthetic Fiber Production Facilities	Х		X				
JJJ	Petroleum Dry Clearners	X	Х	Х				
KKK	Equipment Leaks of VOC from Onshore Natural Gas Processing Plants	K						
LLL	Onshore Natural Gas Processing Plants; SO <sub>2</sub> Emissions		Х					
000	Nonmetallic Mineral Processing Plants		X	Х				
PPP	Wool Fiberglass Insulation Manufacturing Plants		X	X				

(33) State of New Mexico: New Mexico Environment Department, P.O. Box 5469, Santa Fe, New Mexico 87502-5469. Note: For a list of delegated standards for New Mexico (excluding Bernalillo County and Indian country), see <u>paragraph</u> (e)(1) of this section.

(34) New York: New York State Department of Environmental Conservation, 50 Wolf Road Albany, New York 12233, attention: Division of Air Resources.

(35) State of North Carolina: North Carolina Department of Environmental Quality, Division of Air Quality, 1641 Mail Service Center, Raleigh, North Carolina 27699-1641 or local agencies, Forsyth County Office of Environmental Assistance and Protection, 201 North Chestnut Street, Winston-Salem, North Carolina 27101-4120; Mecklenburg County Land Use and Environmental Services Agency, Air Quality, 2145 Suttle Avenue, Charlotte, North Carolina 28208; Western North Carolina Regional Air Quality Agency, 125 S. Lexington Ave., Suite 101, Asheville, North Carolina 28801-3661.

(36) State of North Dakota, North Dakota Department of Environmental Quality, 918 East Divide Avenue, Bismarck, ND 58501-1947.

Note:

For a table listing Region VIII's NSPS delegation status, see <u>paragraph (c)</u> of this section.

(37) State of Ohio:

(i) Medina, Summit and Portage Counties; Director, Akron Regional Air Quality Management District, 146 South High Street, Room 904, Akron, OH 44308.

(ii) Stark County; Director, Canton City Health Department, Air Pollution Control Division, 420 Market Avenue North, Canton, Ohio 44702-1544.

(iii) Butler, Clermont, Hamilton, and Warren Counties; Director, Hamilton County Department of Environmental Services, 250 William Howard Taft Road, Cincinnati, Ohio 45219-2660.

(iv) Cuyahoga County; Commissioner, Cleveland Department of Public Health, Division of Air Quality, 75 Erieview Plaza 2nd Floor, Cleveland, Ohio 44114.

(v) Clark, Darke, Greene, Miami, Montgomery, and Preble Counties; Director, Regional Air Pollution Control Agency, 117 South Main Street, Dayton, Ohio 45422-1280.

(vi) Lucas County and the City of Rossford (in Wood County); Director, City of Toledo, Division of Environmental Services, 348 South Erie Street, Toledo, OH 43604.

(vii) Adams, Brown, Lawrence, and Scioto Counties; Portsmouth Local Air Agency, 605 Washington Street, Third Floor, Portsmouth, OH 45662.

(viii) Allen, Ashland, Auglaize, Crawford, Defiance, Erie, Fulton, Hancock, Hardin, Henry, Huron, Marion, Mercer, Ottawa, Paulding, Putnam, Richland, Sandusky, Seneca, Van Wert Williams, Wood (Except City of Rossford), and Wyandot

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Counties; Ohio Environmental Protection Agency, Northwest District Office, Air Pollution Control, 347 North Dunbridge Road, Bowling Green, Ohio 43402.

(ix) Ashtabula, Caroll, Colombiana, Holmes, Lorain, and Wayne Counties; Ohio Environmental Protection Agency, Northeast District Office, Air Pollution Unit, 2110 East Aurora Road, Twinsburg, OH 44087.

(x) Athens, Belmont, Coshocton, Gallia, Guemsey, Harrison, Hocking, Jackson, Jefferson, Meigs, Monroe, Morgan, Muskingum, Noble, Perry, Pike, Ross, Tuscarawas, Vinton, and Washington Counties; Ohio Environmental Protection Agency, Southeast District Office, Air Pollution Unit, 2195 Front Street, Logan, OH 43138.

(xi) Champaign, Clinton, Highland, Logan, and Shelby Counties; Ohio Environmental Protection Agency, Southwest District Office, Air Pollution Unit, 401 East Fifth Street, Dayton, Ohio 45402-2911.

(xii) Delaware, Fairfield, Fayette, Franklin, Knox, Licking, Madison, Morrow, Pickaway, and Union Counties; Ohio Environmental Protection Agency, Central District Office, Air Pollution control, 50 West Town Street, Suite 700, Columbus, Ohio 43215.

(xiii) Geauga and Lake Counties; Lake County General Health District, Air Pollution Control, 33 Mill Street, Painesville, OH 44077.

(xiv) Mahoning and Trumbull Counties; Mahoning-Trumbull Air Pollution Control Agency, 345 Oak Hill Avenue, Suite 200, Youngstown, OH 44502.

(38) State of Oklahoma, Oklahoma State Department of Health, Air Quality Service, P.O. Box 53551, Oklahoma City, OK 73152.

(i) Oklahoma City and County: Director, Oklahoma City-County Health Department, 921 Northeast 23rd Street, Oklahoma City, OK 73105.

(ii) Tulsa County: Tulsa City-County Health Department, 4616 East Fifteenth Street, Tulsa, OK 74112.

(39) State of Oregon.

(i) Oregon Department of Environmental Quality (ODEQ), 811 SW Sixth Avenue, Portland, OR 97204-1390, <u>http://www.deg.state.or.us</u>.

(ii) Lane Regional Air Pollution Authority (LRAPA), 1010 Main Street, Springfield, Oregon 97477, <u>http://www.lrapa.org</u>.

(40)

(i) City of Philadelphia, Department of Public Health, Air Management Services, 321 University Avenue, Philadelphia, Pennsylvania 19104.

(ii) Commonwealth of Pennsylvania, Department of Environmental Protection, Bureau of Air Quality Control, P.O. Box 8468, 400 Market Street, Harrisburg, Pennsylvania 17105.

(iii) Allegheny County Health Department, Bureau of Environmental Quality, Division of Air Quality, 301 39th Street, Pittsburgh, Pennsylvania 15201.

(41) State of Rhode Island, Rhode Island Department of Environmental Management, Office of Air Resources, 235 Promenade Street, Providence, RI 02908.

(42) State of South Carolina: South Carolina Department of Health and Environmental Control, 2600 Bull Street, Columbia, South Carolina 29201.

(43) State of South Dakota, Air Quality Program, Department of Agriculture and Natural Resources, Joe Foss Building, 523 East Capitol, Pierre, SD 57501-3181.

(44) State of Tennessee: Tennessee Department of Environment and Conservation, Division of Air Pollution Control, William R. Snodgrass Tennessee Tower, 312 Rosa L. Parks Avenue, 15th Floor, Nashville, Tennessee 37243, or local agencies, Knox County Air Quality Management—Department of Public Health, 140 Dameron Avenue, Knoxville, Tennessee 37917; Metro Public Health Department, Pollution Control Division, 2500 Charlotte Ave., Nashville, Tennessee 37209; Chattanooga-Hamilton County Air Pollution Control Bureau, 6125 Preservation Drive, Chattanooga, Tennessee 37416; Shelby County Health Department, Pollution Control Section, 814 Jefferson Avenue, Memphis, Tennessee 38105.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(45) State of Texas, Texas Air Control Board, 6330 Highway 290 East, Austin, TX 78723.

(46) State of Utah, Division of Air Quality, Department of Environmental Quality, P.O. Box 144820, Salt Lake City, UT 84114-4820.

Note:

For a table listing Region VIII's NSPS delegation status, see paragraph (c) of this section.

(47) State of Vermont, Agency of Natural Resources, Department of Environmental Conservation, Air Quality and Climate Division, Davis 2, One National Life Drive, Montpelier, VT 05620-3802.

(48) Commonwealth of Virginia, Department of Environmental Quality, 629 East Main Street, Richmond, Virginia 23219.

(49) State of Washington.

(i) Washington State Department of Ecology (Ecology), P.O. Box 47600, Olympia, WA 98504-7600, <u>http://www.ecy.wa.gov/</u>

(ii) Benton Clean Air Authority (BCAA), 650 George Washington Way, Richland, WA 99352-4289, http://www.bcaa.net/

(iii) Northwest Air Pollution Control Authority (NWAPA), 1600 South Second St., Mount Vernon, WA 98273-5202, <u>http://www.nwair.org/</u>

(iv) Olympic Regional Clean Air Agency (ORCAA), 909 Sleater-Kinney Road S.E., Suite 1, Lacey, WA 98503-1128, <u>http://www.orcaa.org/</u>

(v) Puget Sound Clean Air Agency (PSCAA), 110 Union Street, Suite 500, Seattle, WA 98101-2038, <u>http://www.pscleanair.org/</u>

(vi) Spokane County Air Pollution Control Authority (SCAPCA), West 1101 College, Suite 403, Spokane, WA 99201, <u>http://www.scapca.org/</u>

(vii) Southwest Clean Air Agency (SWCAA), 1308 NE. 134th St., Vancouver, WA 98685-2747, http://www.swcleanair.org/

(viii) Yakima Regional Clean Air Authority (YRCAA), 6 South 2nd Street, Suite 1016, Yakima, WA 98901, <u>http://co.yakima.wa.us/cleanair/default.htm</u>

(ix) The following table lists the delegation status of the New Source Performance Standards for the State of Washington. An "X" indicates the subpart has been delegated, subject to all the conditions and limitations set forth in Federal law and the letters granting delegation. Some authorities cannot be delegated and are retained by EPA. Refer to the letters granting delegation for a discussion of these retained authorities. The dates noted at the end of the table indicate the effective dates of Federal rules that have been delegated. Authority for implementing and enforcing any amendments made to these rules after these effective dates are not delegated.

NSPS Subparts Delegated to Washington Air Agencies									
Subnart	Washington								
Subpart	Ecology <sup>2</sup>	BCAA <sup>3</sup>	NWAPA <sup>4</sup>	ORCAA <sup>5</sup>	PSCAA <sup>6</sup>	SCAPCA <sup>7</sup>	SWCAA <sup>8</sup>	YRCAA <sup>9</sup>	
A General Provisions	Х	Х	Х	Х	Х	Х	Х	Х	
B Adoption and Submittal of State Plans for Designated Facilities									
C Emission Guidelines and Compliance Times									
Cb Large Municipal Waste Combustors that are Constructed on or before September 20, 1994 (Emission Guidelines and Compliance Times)									
Cc Municipal Solid Waste Landfills (Emission Guidelines and Compliance Times)									

NSPS	Subparts	Delegate	d to Washin	ngton Air A	Agencies				
Sechar and	Washington								
Subpart <sup>2</sup>	Ecology <sup>2</sup>	BCAA <sup>3</sup>	NWAPA <sup>4</sup>	ORCAA <sup>5</sup>	PSCAA <sup>6</sup>	SCAPCA <sup>7</sup>	SWCAA <sup>8</sup>	YRCAA <sup>9</sup>	
Cd Sulfuric Acid Production Units (Emission Guidelines and Compliance Times)									
Ce Hospital/Medical/Infectious Waste Incinerators (Emission Guidelines and Compliance Times)									
D Fossil-Fuel-Fired Steam Generators for which Construction is Commenced after August 17, 1971	X	Х	Х	х	x	X	Х	Х	
Da Electric Utility Steam Generating Units for which Construction is Commenced after September 18, 1978	X	Х	х	x	х	Х	х	Х	
Db Industrial-Commercial-Institutional Steam Generating Units	X	X	X	X	X	X	X	X	
Dc Small Industrial-Commercial- Institutional Steam Generating Units	Х	Х	Х	x	х	Х	X	Х	
E Incinerators	Х	Х	Х	Х	X	Х	Х	Х	
Ea Municipal Waste Combustors for which Construction is Commenced after December 20, 1989 and on or before September 20, 1994	x	x	X	X	х	X	Х	Х	
Eb—Large Municipal Waste Combustors		X		X	x	X			
Ec—Hospital/Medical/Infectious Waste Incinerators	X	Х	X	X	X	X			
F Portland Cement Plants	X	Х	X	Х	Х	Х	Х	Х	
G Nitric Acid Plants	X	Х	X	Х	Х	Х	Х	Х	
H Sulfuric Acid Plants	X	Х	X	Х	Х	X	Х	Х	
I Hot Mix Asphalt Facilities	X	X	Х	Х	Х	Х	Х	Х	
J Petroleum Refineries	X	X	Х	Х	Х	Х	Х	Х	
K Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced after June 11, 1973 and prior to May 19, 1978	х	Х	х	Х	X	X	х	х	
Ka Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced after May 18, 1978 and prior to July 23, 1984	X	X	X	X	X	X	X	X	
Kb VOC Liquid Storage Vessels (including Petroleum Liquid Storage Vessels) for which Construction, Reconstruction, or Modification Commenced after July 23, 1984	X	х	X	X	X	X	X	X	

NSPS Subparts Delegated to Washington Air Agencies									
Sector and				Was	hington				
Subpart <sup>.</sup>	Ecology <sup>2</sup>	BCAA <sup>3</sup>	NWAPA <sup>4</sup>	ORCAA <sup>5</sup>	PSCAA <sup>6</sup>	SCAPCA <sup>7</sup>	SWCAA <sup>8</sup>	YRCAA <sup>9</sup>	
L Secondary Lead Smelters	X	Х	Х	Х	Х	Х	Х	Х	
M Secondary Brass and Bronze Production Plants	Х	Х	Х	Х	X	Х	X	X	
N Primary Emissions from Basic Oxygen Process Furnaces for which Construction is Commenced after June 11, 1973	X	x	X	X	X	X	X	Х	
Na Secondary Emissions from Basic Oxygen Process Steel-making Facilities for which Construction is Commenced after January 20, 1983	X	x	Х	X	x	X	X	X	
O Sewage Treatment Plants	Х	X	Х	X	Х	X	X	Х	
P Primary Copper Smelters	Х	X	X	Х	X	Х	Х	Х	
Q Primary Zinc Smelters	X	X	X	X	X	X	X	X	
R Primary Lead Smelters	X	X	X	X	X	X	X	X	
S Primary Aluminum Reduction Plants <sup>10</sup>	X								
T Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	X	X	X	X	x	X	X	X	
U Phosphate Fertilizer Industry: Superphosphoric Acid Plants	X	X	X	X	x	X	X	X	
V Phosphate Fertilizer Industry: Diammonium Phosphate Plants	X	X	X	X	X	X	X	X	
W Phosphate Fertilizer Industry: Triple Superphosphate Plants	X	X	X	X	X	X	X	X	
X Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities	X	X	X	X	x	X	X	X	
Y Coal Preparation Plants	X	X	X	X	X	X	X	X	
Z Ferroalloy Production Facilities	X	X	X	X	X	X	X	X	
AA Steel Plants: Electric Arc Furnaces Constructed after October 21, 1974 and on or before August 17, 1983	x	X	X	X	X	X	X	Х	
AAa Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed after August 7, 1983	x	x	X	х	x	X	X	Х	
BB Kraft Pulp Mills <sup>11</sup>	Х								
CC Glass Manufacturing Plants	Х	Х	Х	Х	Х	Х	Х	Х	
DD Grain Elevators	Х	Х	Х	Х	Х	Х	Х	Х	
EE Surface Coating of Metal Furniture	Х	Х	Х	Х	Х	Х	Х	Х	
GG Stationary Gas Turbines	Х	Х	X	Х	Х	Х	X	X	
HH Lime Manufacturing Plants	X	X	X	X	X	X	X	X	

NSPS	S Subparts	Delegate	d to Washi	ngton Air A	Agencies			
Subnartl				Was	hington			
Subpart	Ecology <sup>2</sup>	BCAA <sup>3</sup>	NWAPA <sup>4</sup>	ORCAA <sup>5</sup>	PSCAA <sup>6</sup>	SCAPCA <sup>7</sup>	SWCAA <sup>8</sup>	YRCAA9
KK Lead-Acid Battery Manufacturing Plants	X	Х	Х	Х	Х	Х	Х	Х
LL Metallic Mineral Processing Plants	X	X	Х	X	X	Х	Х	X
MM Automobile and Light Duty Truck Surface Coating Operations	X	Х	X	X	x	X	X	X
NN Phosphate Rock Plants	X	X	Х	X	X	X	Х	Х
PP Ammonium Sulfate Manufacture	X	X	Х	Х	X	Х	Х	X
QQ Graphic Arts Industry: Publication Rotogravure Printing	X	X	X	X	x	X	X	X
RR Pressure Sensitive Tape and Label Surface Coating Standards	X	X	X	X	X	X	X	X
SS Industrial Surface Coating: Large Appliances	X	X	X	X	X	X	X	X
TT Metal Coil Surface Coating	X	X	Х	X	X	X	X	X
UU Asphalt Processing and Asphalt Roof Manufacture	X	X	X	X	x	X	X	X
VV Equipment Leaks of VOC in Synthetic Organic Chemical Manufacturing Industry	X	X	X	x	x	X	X	X
WW Beverage Can Surface Coating Industry	X	X	Х	X	X	X	X	X
XX Bulk Gasoline Terminals	X	Х	Х	X	X	Х	Х	Х
AAA New Residential Wood Heaters								
BBB Rubber Tire Manufacturing Industry	X	Х	X	X	X	X	X	Х
DDD VOC Emissions from Polymer Manufacturing Industry	X	X	X	X	X	X	X	X
FFF Flexible Vinyl and Urethane Coating and Printing	X	X	X	X	X	X	X	X
GGG Equipment Leaks of VOC in Petroleum Refineries	x	Х	X	X	X	x	X	X
HHH Synthetic Fiber Production Facilities	X	X	X	X	X	X	X	X
III VOC Emissions from Synthetic Organic Chemical Manufacturing Industry Air Oxidation Unit Processes	X	х	X	X	x	X	X	x
JJJ Petroleum Dry Cleaners	X	X	Х	X	X	Х	Х	Х
KKK Equipment Leaks of VOC from Onshore Natural Gas Processing Plants	X	Х	X	X	X	X	X	Х
LLL Onshore Natural Gas Processing: SO <sub>2</sub> Emissions	X	X	X	X	X	X	X	X
NNN VOC Emissions from Synthetic Organic Chemical Manufacturing	X	X	Х	Х	X	Х	X	X

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

NSPS	Subparts	Delegate	d to Washii	ngton Air A	gencies					
Sector and				Was	Washington					
Subpart	Ecology <sup>2</sup>	BCAA <sup>3</sup>	NWAPA <sup>4</sup>	ORCAA <sup>5</sup>	PSCAA <sup>6</sup>	SCAPCA <sup>7</sup>	SWCAA <sup>8</sup>	YRCAA <sup>9</sup>		
Industry Distillation Operations										
OOO Nonmetallic Mineral Processing Plants			X		X		Х			
PPP Wool Fiberglass Insulation Manufacturing Plants	X	X	X	X	X	X	Х	X		
QQQ VOC Emissions from Petroleum Refinery Wastewater Systems	Х	Х	X	X	X	Х	Х	X		
RRR VOCs from Synthetic Organic Chemical Manufacturing Industry Reactor Processes	х	Х	Х	х	х	X	Х	Х		
SSS Magnetic Tape Coating Facilities	Х	Х	Х	X	Х	X	Х	Х		
TTT Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines	х	Х	Х	х	X	Х	Х	Х		
UUU Calciners and Dryers in Mineral Industries	Х	Х	Х	Х	х	Х	Х	Х		
VVV Polymeric Coating of Supporting Substrates Facilities	Х	X	X	Х	Х	Х	Х	Х		
WWW Municipal Solid Waste Landfills	Х	X	X	Х	X	Х	Х	X		
AAAA Small Municipal Waste Combustion Units for which Construction is Commenced after August 30, 1999 or for which Modification or Reconstruction is Commenced after June 6, 2001	X	X	K	x	X	X		X		
BBBB Small Municipal Waste Combustion Units Constructed on or before August 30, 1999 (Emission Guidelines and Compliance Times)										
CCCC Commercial and Industrial Solid Waste Incineration Units for which Construction is Commenced after November, 30, 1999 or for which Modification or Reconstruction is Commenced on or after June 1, 2001	x	x		X	X	X		x		
DDDD Commercial and Industrial Solid Waste Incineration Units that Commenced Construction on or before November 30, 1999 (Emission Guidelines and Compliance Times)										

<sup>1</sup> Any authority within any subpart of this part that is not delegable, is not delegated. Please refer to Attachment B to the delegation letters for a listing of the NSPS authorities excluded from delegation.

<sup>2</sup> Washington State Department of Ecology, for <u>40 CFR 60.17(h)(1)</u>, (h)(2), (h)(3) and <u>40 CFR part 60</u>, subpart AAAA, as in effect on June 6, 2001; for <u>40 CFR part 60</u>, subpart CCCC, as in effect on June 1, 2001; and for all other NSPS delegated, as in effect February 20, 2001.

NSPS	Subparts Delegated to Washington Air Agencies
Subnart <sup>1</sup>	Washington
	Ecology <sup>2</sup> BCAA <sup>3</sup> NWAPA <sup>4</sup> ORCAA <sup>5</sup> PSCAA <sup>6</sup> SCAPCA <sup>7</sup> SWCAA <sup>8</sup> YRCAA <sup>9</sup>
<sup>3</sup> Benton Clean Air Authority, for <u>40 CF</u> June 6, 2001; for <u>40 CFR part 60, subpar</u> February 20, 2001.	<u>R 60.17(h)(1)</u> , ( <u>h)(2</u> ), ( <u>h)(3</u> ) and <u>40 CFR part 60</u> , <u>subpart AAAA</u> , as in effect on <u>t CCCC</u> , as in effect on June 1, 2001; and for all other NSPS delegated, as in effect
<sup>4</sup> Northwest Air Pollution Authority, for	all NSPS delegated, as in effect on July 1, 2000.
<sup>5</sup> Olympic Regional Clean Air Authority effect on June 6, 2001; for <u>40 CFR part 6</u> in effect February 20, 2001.	, for <u>40 CFR 60.17(h)(1)</u> , <u>(h)(2)</u> , <u>(h)(3)</u> and <u>40 CFR part 60</u> , <u>subpart AAAA</u> , as in <u>50</u> , <u>subpart CCCC</u> , as in effect on June 1, 2001; and for all other NSPS delegated, as
<sup>6</sup> Puget Sound Clean Air Authority, for a	ll NSPS delegated, as in effect on July 1, 2002.
<sup>7</sup> Spokane County Air Pollution Control <u>AAAA</u> , as in effect on June 6, 2001; for delegated, as in effect February 20, 2001	Authority, for <u>40 CFR 60.17(h)(1), (h)(2)</u> , ( <u>h)(3)</u> and <u>40 CFR part 60, subpart</u> <u>40 CFR part 60, subpart CCCC</u> , as in effect on June 1, 2001; and for all other NSPS
<sup>8</sup> Southwest Clean Air Agency, for all N	SPS delegated, as in effect on July 1, 2000.
<sup>9</sup> Yakima Regional Clean Air Authority, effect on June 6, 2001; for <u>40 CFR part 6</u> in effect February 20, 2001.	for <u>40 CFR 60.17(h)(1)</u> , (h)(2), (h)(3) and <u>40 CFR part 60, subpart AAAA</u> , as in <u>50, subpart CCCC</u> , as in effect on June 1, 2001; and for all other NSPS delegated, as
<sup>10</sup> <u>Subpart S of this part</u> is not delegated Ecology retains sole authority to regulate 010.	to local agencies in Washington because the Washington State Department of e Primary Aluminum Plants, pursuant to Washington Administrative Code 173-415-
<sup>11</sup> <u>Subpart BB of this part</u> is not delegate Ecology retains sole authority to regulate 173-405-012 and 173-410-012.	d to local agencies in Washington because the Washington State Department of e Kraft and Sulfite Pulping Mills, pursuant to Washington State Administrative Code
(50) State of West Virginia, Department Charleston, West Virginia 25304.	of Environmental Protection, Division of Air Quality, 601 57th Street, SE.,
(51) State of Wisconsin: Wisconsin Depa Wisconsin 53707-7921.	artment of Natural Resouces, 101 South Webster St., P.O. Box 7921, Madison,
(52) State of Wyoming, Department of E Street, Cheyenne, WY 82002.	nvironmental Quality, Air Quality Division, Herschler Building, 122 West 25th
Note:	
For a table listing Region VIII's NSPS de	elegation status, see <u>paragraph (c)</u> of this section.
(53) Territory of Guam: Guam Environm	nental Protection Agency, P.O. Box 22439 GMF, Barrigada, Guam 96921.
Note:	
For tables listing the delegation status of	agencies in Region IX, see paragraph (d) of this section.
(54) Commonwealth of Puerto Rico: Cor Santurce, PR 00910, Attention: Air Qual	nmonwealth of Puerto Rico Environmental Quality Board, P.O. Box 11488, ity Area Director (see table under <u>§ 60.4(b)(FF)(1)</u> ).
(55) U.S. Virgin Islands: U.S. Virgin Isla Amalie, St. Thomas, VI 00801.	ands Department of Conservation and Cultural Affairs, P.O. Box 578, Charlotte
(56) American Samoa: American Samoa 96799.	Environmental Protection Agency, P.O. Box PPA, Pago Pago, American Samoa
Note:	
For tables listing the delegation status of	agencies in Region IX, see paragraph (d) of this section.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(57) Commonwealth of the Northern Mariana Islands: CNMI Division of Environmental Quality, P.O. Box 501304, Saipan, MP 96950.

Note:

For tables listing the delegation status of agencies in Region IX, see <u>paragraph (d)</u> of this section.

(c) The delegation status table for New Source Performance Standards for Region VIII can be found online at <u>http://www2.epa.gov/region8/air-program</u>.

(d) The following tables list the specific part 60 standards that have been delegated unchanged to the air pollution control agencies in Region IX. The (X) symbol is used to indicate each standard that has been delegated. The following provisions of this subpart are not delegated: <u>§§ 60.4(b)</u>, <u>60.8(b)</u>, <u>60.9</u>, <u>60.11(b)</u>, <u>60.11(e)</u>, <u>60.13(a)</u>, <u>60.13(d)(2)</u>, <u>60.13(g)</u>, <u>60.13(j)</u>.

(1) Arizona. The following table identifies delegations for Arizona:

Table 3 to Paragraph (d)(1)—Delegation Status for New Source Performance Standards for Arizona									
		Air p	Air pollution contro						
	Subpart	Arizona DEQ	Maricopa County	Pima County	Pinal County				
A	General Provisions	X	Х	Х	Х				
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	Х	X	Х	X				
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978	X	X	X	X				
Db	Industrial-Commercial-Institutional Steam Generating Units	X	X	X	X				
Dc	Small Industrial-Commercial-Institutional Steam Generating Units	X	Х	X	Х				
Е	Incinerators	X	X	X	X				
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994	X	X	X	X				
Eb	Large Municipal Waste Combustors Constructed After September 20, 1994	X	X	X					
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996	x	X	X					
F	Portland Cement Plants	X		X	X				
G	Nitric Acid Plants	X	X	X	X				
Ga	Nitric Acid Plants For Which Construction, Reconstruction or Modification Commenced After October 14, 2011		X	Х					
Н	Sulfuric Acid Plant	X	X	X	X				
Ι	Hot Mix Asphalt Facilities	X	X	X	X				
J	Petroleum Refineries	X		X	Х				
Ja	Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After May 14, 2007			X					
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	X	Х	X	X				
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	Х	Х	X	X				
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	Х	Х	X	X				

		Air pollution control agency					
	Subpart	Arizona DEQ	Maricopa County	Pima County	Pinal County		
L	Secondary Lead Smelters	Х		X	X		
М	Secondary Brass and Bronze Production Plants	Х	X	X	X		
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973	x	X	X	X		
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983	x	Х	Х	X		
0	Sewage Treatment Plants	X	X	X	X		
Р	Primary Copper Smelters	X		X	X		
Q	Primary Zinc Smelters	Х		X	X		
R	Primary Lead Smelters	Х		X	X		
S	Primary Aluminum Reduction Plants	Х	Х	X	X		
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	X	X	X	X		
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	X	X	X	X		
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	X	X	X	X		
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	X	X	X	X		
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities	X	X	X	X		
Y	Coal Preparation and Processing Plants	X	X	X	X		
Ζ	Ferroalloy Production Facilities	X	X	X	X		
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983	X	X	X	X		
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983	X	X	X	X		
BB	Kraft Pulp Mills	Х	X	X	X		
BBa	Kraft Pulp Mill Sources for which Construction, Reconstruction or Modification Commenced after May 23, 2013		X	X			
CC	Glass Manufacturing Plants	X	X	X	X		
DD	Grain Elevators	X	X	X	X		
EE	Surface Coating of Metal Furniture	X	X	X	X		
FF	(Reserved)						
GG	Stationary Gas Turbines	X	X	X	X		
HH	Lime Manufacturing Plants	X	X	X	X		
KK	Lead-Acid Battery Manufacturing Plants	X	X	X	X		
LL	Metallic Mineral Processing Plants	X	X	X	X		
MM	Automobile and Light Duty Trucks Surface Coating Operations	X	X	X	X		
NN	Phosphate Rock Plants	X	X	X	X		
PP	Ammonium Sulfate Manufacture	X	X	X	X		
QQ	Graphic Arts Industry: Publication Rotogravure Printing	X	X	X	X		
RR	Pressure Sensitive Tape and Label Surface Coating Operations	X	X	X	X		

		Air pollution control agency					
	Subpart	Arizona DEQ	Maricopa County	Pima County	Pinal County		
SS	Industrial Surface Coating: Large Appliances	Х	Х	X	X		
TT	Metal Coil Surface Coating	Х	Х	X	X		
UU	Asphalt Processing and Asphalt Roofing Manufacture	X	X	X	X		
VV	Equipment Leaks of VOC in the Synthetic Organic Industry Chemicals Manufacturing	x	X	X	X		
VVa	Equipment Leaks of VOC in the Synthetic Organic Industry for Which Construction, Reconstruction, or Chemicals Manufacturing Modification Commenced After November 7, 2006	X	X	X			
WW	Beverage Can Surface Coating Industry	Х	X	X	Х		
XX	Bulk Gasoline Terminals	Х	X	X	X		
AAA	New Residential Wood Heaters	X	X	X	X		
BBB	Rubber Tire Manufacturing Industry	X	X	X	X		
CCC	(Reserved)		Ţ,				
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry	X	X	X	X		
EEE	(Reserved)						
FFF	Flexible Vinyl and Urethane Coating and Printing	X	X	X	X		
GGG	Equipment Leaks of VOC in Petroleum Refineries	X		X	X		
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006	X		X			
HHH	Synthetic Fiber Production Facilities	X	Х	X	X		
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes	X	X	X	X		
JJJ	Petroleum Dry Cleaners	X	X	X	X		
KKK	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants	X	X	X	X		
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions	X	X	X	X		
MMM	(Reserved)						
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations	X	X	X	X		
000	Nonmetallic Mineral Processing Plants	Х	Х	X	Х		
PPP	Wool Fiberglass Insulation Manufacturing Plants	X	X	X	X		
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems	X		X	X		
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes	X	X	X			
SSS	Magnetic Tape Coating Facilities	X	X	X	Х		
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines	X	X	X	X		
UUU	Calciners and Dryers in Mineral Industries	X	Х	X			
VVV	Polymeric Coating of Supporting Substrates Facilities	X	X	X	X		
WWW	Municipal Solid Waste Landfills	X	Х	X			

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A - GENERAL PROVISIONS.

Table 3 to Paragraph (d)(1)—Delegation Status for New Source Performance Standards for Arizona								
	Subpart	Air pollution control agency						
		Arizona DEQ	Maricopa County	Pima County	Pinal County			
xxx	Municipal Solid Waste Landfills that Commenced Construction, Reconstruction, or Modification After July 17, 2014		X	X				
AAAA	Small Municipal Waste Combustion Units for Which Construction is Commenced After August 30, 1999 or for Which Modification or Reconstruction is Commended After June 6, 2001	x	X	X				
CCCC	Commercial and Industrial Solid Waste Incineration Units for Which Construction Is Commenced After November 30, 1999 or for Which Modification or Reconstruction Is Commenced on or After June 1, 2001	x	X	X				
EEEE	Other Solid Waste Incineration Units for Which Construction is Commenced After December 9, 2004, or for Which Modification or Reconstruction is Commenced on or After June 16, 2006	X	X	X				
GGGG	(Reserved)							
HHHH	(Reserved)							
IIII	Stationary Compression Ignition Internal Combustion Engines	X	X	X				
JJJJ	Stationary Spark Ignition Internal Combustion Engines		Х	X				
КККК	Stationary Combustion Turbines	X	Х	X				
LLLL	New Sewage Sludge Incineration Units			X				
MMMM	Emissions Guidelines and Compliance Times for Existing Sewage Sludge Incineration Units	х						
0000	Crude Oil and Natural Gas Production, Transmission, and Distribution		Х	Х				
OOOOa	Standards of Performance for Crude Oil and Natural Gas Facilities for Which Construction, Modification or Reconstruction Commenced After September 18, 2015		x	X				
QQQQ	Standards of Performance for New Residential Hydronic Heaters and Forced-Air Furnaces		X	X				
TTTT	Standards of Performance for Greenhouse Gas Emissions for Electric Generating Units		X	X				

(2) California. The following tables identify delegations for each of the local air pollution control agencies of California.

(i) Delegations for Amador County Air Pollution Control District, Antelope Valley Air Quality Management District, Bay Area Air Quality Management District, and Butte County Air Quality Management District are shown in the following table:

Table 4 to Paragraph (d)(2)(i)—Delegation Status for New Source Performance Standards for Amador County APCD, Antelope Valley AQMD, Bay Area AQMD, and Butte County AQMD								
		Air pollution control agency						
	Subpart	Amador County APCD	Antelope Valley AQMD	Bay Area AQMD	Butte County AQMD			
А	General Provisions		Х					
Ba	Adoption and Submittal of State Plans for Designated Facilities		Х					
Cf	Emission Guidelines and Compliance Times for Municipal Solid Waste Landfills		Х					
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971		Х	X				
Table 4 to Paragraph (d)(2)(i)-Delegation Status for New Source Performance Standards for	Amador County APCD,							
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Antelope Valley AQMD, Bay Area AQMD, and Butte County AQMD								

		Air pollution control agency				
	Subpart	Amador County APCD	Antelope Valley AQMD	Bay Area AQMD	Butte County AQMD	
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978		X	Х		
Db	Industrial-Commercial-Institutional Steam Generating Units		Х	X		
Dc	Small Industrial-Commercial-Institutional Steam Generating Units	K	Х	X		
E	Incinerators		Х	X		
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994		Х	Х		
Eb	Large Municipal Waste Combustors Constructed After September 20, 1994		Х			
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996		х			
F	Portland Cement Plants		Х	Х		
G	Nitric Acid Plants		Х	Х		
Ga	Nitric Acid Plants For Which Construction, Reconstruction or Modification Commenced After October 14, 2011		Х			
Н	Sulfuric Acid Plant		Х	Х		
Ι	Hot Mix Asphalt Facilities		Х	Х		
J	Petroleum Refineries		Х	Х		
Ja	Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After May 14, 2007		Х			
К	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978		Х	Х		
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984		Х	Х		
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984		Х	X		
L	Secondary Lead Smelters		Х	Х		
М	Secondary Brass and Bronze Production Plants		Х	X		
Ν	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973		Х	Х		
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983		Х	Х		
0	Sewage Treatment Plants		Х	X		
Р	Primary Copper Smelters		X	X		
Q	Primary Zinc Smelters		X	X		
R	Primary Lead Smelters		X	X		
S	Primary Aluminum Reduction Plants		X	X		
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants		X			

Table 4 to Paragraph (d)(2)(i)—Delegation Status for New Source Performance Standards for Amador County APCD,
Antelope Valley AQMD, Bay Area AQMD, and Butte County AQMD

		Air pollution control agency				
	Subpart	Amador County APCD	Antelope Valley AQMD	Bay Area AQMD	Butte County AQMD	
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants		X	X		
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants		X	X		
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants		Х	X		
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities		X	Х		
Y	Coal Preparation and Processing Plants		X	X		
Z	Ferroalloy Production Facilities		X	X		
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983		x	x		
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983		X	х		
BB	Kraft Pulp Mills		Х	Х		
BBa	Kraft Pulp Mill Sources for which Construction, Reconstruction or Modification Commenced after May 23, 2013		X			
CC	Glass Manufacturing Plants		Х	Х		
DD	Grain Elevators		Х	Х		
EE	Surface Coating of Metal Furniture		Х	Х		
FF	(Reserved)					
GG	Stationary Gas Turbines		Х	Х		
HH	Lime Manufacturing Plants		Х	X		
KK	Lead-Acid Battery Manufacturing Plants		Х	Х		
LL	Metallic Mineral Processing Plants		Х	X		
MM	Automobile and Light Duty Trucks Surface Coating Operations		Х	Х		
NN	Phosphate Rock Plants		Х	Х		
PP	Ammonium Sulfate Manufacture		Х	Х		
QQ	Graphic Arts Industry: Publication Rotogravure Printing		Х	Х		
RR	Pressure Sensitive Tape and Label Surface Coating Operations		X	X		
SS	Industrial Surface Coating: Large Appliances		X	X		
TT	Metal Coil Surface Coating		Х	Х		
UU	Asphalt Processing and Asphalt Roofing Manufacture		Х	Х		
VV	Equipment Leaks of VOC in the Synthetic Organic Industry Chemicals Manufacturing		X	Х		
VVa	Equipment Leaks of VOC in the Synthetic Organic Industry for Which Construction, Reconstruction, or Chemicals Manufacturing Modification Commenced After November 7, 2006		X			
WW	Beverage Can Surface Coating Industry		X	X		
XX	Bulk Gasoline Terminals					
AAA	New Residential Wood Heaters		Х	Х		

Table 4 to Paragraph (d)(2)(i)—Delegation Status for New Source Performance Standards for Amador County APCD,
Antelope Valley AQMD, Bay Area AQMD, and Butte County AQMD

		Air pollution control agency				
	Subpart	Amador County APCD	Antelope Valley AQMD	Bay Area AQMD	Butte County AQMD	
BBB	Rubber Tire Manufacturing Industry		X	X		
CCC	(Reserved)					
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry		X	Х		
EEE	(Reserved)					
FFF	Flexible Vinyl and Urethane Coating and Printing		Х	Х		
GGG	Equipment Leaks of VOC in Petroleum Refineries		X	X		
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006		X			
HHH	Synthetic Fiber Production Facilities		X	X		
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes		X	P		
]]]	Petroleum Dry Cleaners		X	X		
ККК	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants		X	X		
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions		Х			
MMM	(Reserved)					
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations		X	X		
000	Nonmetallic Mineral Processing Plants		X	X		
PPP	Wool Fiberglass Insulation Manufacturing Plants		X	Х		
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems		X			
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes		X			
SSS	Magnetic Tape Coating Facilities		X	X		
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines		X	x		
UUU	Calciners and Dryers in Mineral Industries		X	X		
VVV	Polymeric Coating of Supporting Substrates Facilities		X	X		
WWW	Municipal Solid Waste Landfills		X			
XXX	Municipal Solid Waste Landfills that Commenced Construction, Reconstruction, or Modification After July 17, 2014		X			
AAAA	Small Municipal Waste Combustion Units for Which Construction is Commenced After August 30, 1999 or for Which Modification or Reconstruction is Commended After June 6, 2001		X			
CCCC	Commercial and Industrial Solid Waste Incineration Units for Which Construction Is Commenced After November 30, 1999 or for Which Modification or Reconstruction Is Commenced on or After June 1, 2001		х			
DDDD	Emissions Guidelines and Compliance Times for Commercial and Industrial Solid Waste Incineration Units		X			

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Table	4 to Paragraph (d)(2)(i)—Delegation Status for New Source Performance Sta Antelope Valley AQMD, Bay Area AQMD, and Butte Cour	ndards for nty AQMI	Amador ( )	County Al	PCD,
	Air pollution control				
	Subpart	Amador County APCD	Antelope Valley AQMD	Bay Area AQMD	Butte County AQMD
EEEE	Other Solid Waste Incineration Units for Which Construction is Commenced After December 9, 2004, or for Which Modification or Reconstruction is Commenced on or After June 16, 2006		х		
GGGG	(Reserved)				
HHHH	(Reserved)				
IIII	Stationary Compression Ignition Internal Combustion Engines		X		
<b>J</b> ]]]]	Stationary Spark Ignition Internal Combustion Engines		Х		
KKKK	Stationary Combustion Turbines		Х		
LLLL	New Sewage Sludge Incineration Units		X		
MMMM	Emissions Guidelines and Compliance Times for Existing Sewage Sludge Incineration Units		Х		
0000	Crude Oil and Natural Gas Production, Transmission, and Distribution		Х		
OOOOa	Standards of Performance for Crude Oil and Natural Gas Facilities for Which Construction, Modification or Reconstruction Commenced After September 18, 2015		Х		
TTTT	Standards of Performance for Greenhouse Gas Emissions for Electric Generating Units		X		
UUUUa	Emission Guidelines for Greenhouse Gas Emissions From Existing Electric Utility Generating Units		X		

## (ii) [Reserved]

(iii) Delegations for Glenn County Air Pollution Control District, Great Basin Unified Air Pollution Control District, Imperial County Air Pollution Control District, and Kern County Air Pollution Control District are shown in the following table:

Delegation Status for New Source	Performance Standards for G	lenn County APCD, Great Ba	sin Unified APCD, Imperial
	County APCD, and Ker	rn County APCD	_

		Air pollution control agency				
	Subpart	Glenn County APCD	Great Basin Unified APCD	Imperial County APCD	Kern County APCD	
А	General Provisions		Х		Х	
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971		X		X	
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978		X		X	
Db	Industrial-Commercial-Institutional Steam Generating Units		Х		Х	
Dc	Small Industrial Steam Generating Units		Х		Х	
E	Incinerators		Х		Х	
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994		X			
Eb	Municipal Waste Combustors Constructed After September 20,					

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Dele	gation Status for New Source Performance Standards for Glenn Cou County APCD, and Kern Count	inty APCI y APCD	), Great Basin U	Unified APCI	D, Imperial
		Air pollution control agency			
	Subpart	Glenn County APCD	Great Basin Unified APCD	Imperial County APCD	Kern County APCD
	1994				
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996				
F	Portland Cement Plants		X		X
G	Nitric Acid Plants		X		X
Н	Sulfuric Acid Plants		X		
Ι	Hot Mix Asphalt Facilities		X		X
J	Petroleum Refineries		X		X
к	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978		x		X
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984		X		X
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984		x		X
L	Secondary Lead Smelters		X		Х
М	Secondary Brass and Bronze Production Plants		X		X
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973		X		X
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983		x		X
0	Sewage Treatment Plants		X		X
Р	Primary Copper Smelters		X		X
Q	Primary Zinc Smelters		X		X
R	Primary Lead Smelters		X		X
S	Primary Aluminum Reduction Plants		X		X
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants		X		X
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants		X		X
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants		X		X
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants		Х		X
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities		X		X
Y	Coal Preparation Plants		X		X
Z	Ferroalloy Production Facilities		X		X
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983		X		X

		Air pollution control agency				
	Subpart	Glenn County APCD	Great Basin Unified APCD	Imperial County APCD	Kern County APCD	
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983		X		Х	
BB	Kraft pulp Mills		X		Х	
CC	Glass Manufacturing Plants		X		Х	
DD	Grain Elevators		X		Х	
EE	Surface Coating of Metal Furniture		X		Х	
FF	(Reserved)					
GG	Stationary Gas Turbines		X		Х	
HH	Lime Manufacturing Plants		X		X	
KK	Lead-Acid Battery Manufacturing Plants		X		X	
LL	Metallic Mineral Processing Plants		X		X	
MM	Automobile and Light Duty Trucks Surface Coating Operations		X		X	
NN	Phosphate Rock Plants		X		X	
PP	Ammonium Sulfate Manufacture		X		X	
QQ	Graphic Arts Industry: Publication Rotogravure Printing		X		X	
RR	Pressure Sensitive Tape and Label Surface Coating Operations		X		X	
SS	Industrial Surface Coating: Large Appliances		X		X	
TT	Metal Coil Surface Coating		X		X	
UU	Asphalt Processing and Asphalt Roofing Manufacture		X		X	
vv	Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry		X		X	
WW	Beverage Can Surface Coating Industry		X		X	
XX	Bulk Gasoline Terminals					
AAA	New Residential Wool Heaters		X		X	
BBB	Rubber Tire Manufacturing Industry		X		X	
CCC	(Reserved)					
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry		X		X	
EEE	(Reserved)					
FFF	Flexible Vinyl and Urethane Coating and Printing		X		X	
GGG	Equipment Leaks of VOC in Petroleum Refineries		X		X	
HHH	Synthetic Fiber Production Facilities		X		X	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes		X		X	
JJJ	Petroleum Dry Cleaners		Х		Х	
ккк	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants		X		X	

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

	County APCD, and Kern County APCD						
		Air pollution control agency					
	Subpart	Glenn County APCD	Great Basin Unified APCD	Imperial County APCD	Kern County APCD		
LLL	Onshore Natural Gas Processing: SO2 Emissions				Х		
MMM	(Reserved)						
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations		x		Х		
000	Nonmetallic Mineral Processing Plants		Х		Х		
PPP	Wool Fiberglass Insulation Manufacturing Plants		Х		Х		
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems		Х		Х		
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes				X		
SSS	Magnetic Tape Coating Facilities		Х		Х		
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines		X	X			
UUU	Calciners and Dryers in Mineral Industries		Х		Х		
VVV	Polymeric Coating of Supporting Substrates Facilities		X		Х		
WWW	Municipal Solid Waste Landfills				Х		

(iv) Delegations for Lake County Air Quality Management District, Lassen County Air Pollution Control District, Mariposa County Air Pollution Control District, and Mendocino County Air Pollution Control District are shown in the following table:

Delegation Status for New Source Performance Standards for Lake County Air Quality Management District, Lassen County Air Pollution Control District, Mariposa County Air Pollution Control District, and Mendocino County Air Pollution Control

District

		Air pollution control agency				
	Subpart	Lake County AQMD	Lassen County APCD	Mariposa County AQMD	Mendocino County AQMD	
A	General Provisions	Х			X	
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	Х			Х	
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978	Х			Х	
Db	Industrial-Commercial-Institutional Steam Generating Units	Х				
Dc	Small Industrial Steam Generating Units	Х			Х	
E	Incinerators	Х			Х	
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994	Х			Х	
Eb	Municipal Waste Combustors Constructed After September 20, 1994					
Ec	Hospital/Medical/Infectious Waste Incinerators for Which					

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Delegation Status for New Source Performance Standards for Lake County Air Quality Management District, Lassen County Air Pollution Control District, Mariposa County Air Pollution Control District, and Mendocino County Air Pollution Control District

		Air pollution control agency				
	Subpart	Lake County AQMD	Lassen County APCD	Mariposa County AQMD	Mendocino County AQMD	
	Construction is Commenced After June 20, 1996					
F	Portland Cement Plants	Х			X	
G	Nitric Acid Plants	X			X	
Н	Sulfuric Acid Plants	Х			X	
Ι	Hot Mix Asphalt Facilities	X			X	
J	Petroleum Refineries	X			X	
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	Х			X	
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	X			X	
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	X			Х	
L	Secondary Lead Smelters	X			X	
М	Secondary Brass and Bronze Production Plants	X			X	
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973	X			X	
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983	X			X	
0	Sewage Treatment Plants	Х			X	
Р	Primary Copper Smelters	Х			X	
Q	Primary Zinc Smelters	Х			X	
R	Primary Lead Smelters	Х			Х	
S	Primary Aluminum Reduction Plants	Х			X	
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	Х			Х	
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	Х			X	
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	X			X	
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	Х			Х	
Х	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities	Х			X	
Y	Coal Preparation Plants	Х			Х	
Ζ	Ferroalloy Production Facilities	Х			X	
AA	Steel Plants: Electric Arc Furnaces Constructed After	Х			X	

Delegation Status for New Source Performance Standards for Lake County Air Quality Management District, Lassen County Air Pollution Control District, Mariposa County Air Pollution Control District, and Mendocino County Air Pollution Control District

		Air polluti	llution control agency			
	Subpart	Lake County AQMD	Lassen County APCD	Mariposa County AQMD	Mendocino County AQMD	
	October 21, 1974 and On or Before August 17, 1983					
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983	X			X	
BB	Kraft Pulp Mills	Х			X	
CC	Glass Manufacturing Plants	X			X	
DD	Grain Elevators	Х			X	
EE	Surface Coating of Metal Furniture	X			X	
FF	(Reserved)					
GG	Stationary Gas Turbines	X			X	
HH	Lime Manufacturing Plants	X			X	
KK	Lead-Acid Battery Manufacturing Plants	X			X	
LL	Metallic Mineral Processing Plants	Х			X	
MM	Automobile and Light Duty Trucks Surface Coating Operations	Х			X	
NN	Phosphate Rock Plants	X			X	
РР	Ammonium Sulfate Manufacture	X			X	
QQ	Graphic Arts Industry: Publication Rotogravure Printing	X			X	
RR	Pressure Sensitive Tape and Label Surface Coating Operations	X			X	
SS	Industrial Surface Coating: Large Appliances	X			X	
TT	Metal Coil Surface Coating	X			X	
UU	Asphalt Processing and Asphalt Roofing Manufacture	Х			X	
VV	Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry	X			X	
WW	Beverage Can Surface Coating Industry	X			X	
XX	Bulk Gasoline Terminals					
AAA	New Residential Wool Heaters	X			X	
BBB	Rubber Tire Manufacturing Industry	X			X	
CCC	(Reserved)					
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry	X			X	
EEE	(Reserved)					
FFF	Flexible Vinyl and Urethane Coating and Printing	Х			X	
GGG	Equipment Leaks of VOC in Petroleum Refineries	X			X	
HHH	Synthetic Fiber Production Facilities	Х			X	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry	Х			X	

Delegation Status for New Source Performance Standards for Lake County Air Quality Management District, Lassen County Air Pollution Control District, Mariposa County Air Pollution Control District, and Mendocino County Air Pollution Control District

		Air pollution control agency					
	Subpart	Lake County AQMD	Lassen County APCD	Mariposa County AQMD	Mendocino County AQMD		
	(SOCMI) Air Oxidation Unit Processes						
JJJ	Petroleum Dry Cleaners	Х			X		
ккк	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants	X			X		
LLL	Onshore Natural Gas Processing: SO2 Emissions	Х			X		
MMM	(Reserved)						
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations	x			X		
000	Nonmetallic Mineral Processing Plants	X			X		
PPP	Wool Fiberglass Insulation Manufacturing Plants	X			X		
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems	X			X		
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes	X					
SSS	Magnetic Tape Coating Facilities	X			X		
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines						
UUU	Calciners and Dryers in Mineral Industries	Х			X		
VVV	Polymeric Coating of Supporting Substrates Facilities	X			X		
WWW	Municipal Solid Waste Landfills	X					

(v) Delegations for Modoc Air Pollution Control District, Mojave Desert Air Quality Management District, Monterey Bay Unified Air Pollution Control District and North Coast Unified Air Quality Management District are shown in the following table:

 Table 7 to Paragraph (d)(2)(v)—Delegation Status for New Source Performance Standards for Modoc County APCD,

 Mojave Desert AQMD, Monterey Bay Unified APCD, and North Coast Unified AQMD

			Air pollution control agency				
	Subpart	Modoc County APCD	Mojave Desert AQMD	Monterey Bay Unified APCD	North Coast Unified AQMD		
А	General Provisions	X	Х	Х	Х		
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	Х	Х	Х	Х		
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978	X	Х	Х	Х		
Db	Industrial-Commercial-Institutional Steam Generating Units	X	Х	Х	Х		
Dc	Small Industrial-Commercial-Institutional Steam Generating Units		Х	Х			
Е	Incinerators	X	Х	Х	X		

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

# Table 7 to Paragraph (d)(2)(v)—Delegation Status for New Source Performance Standards for Modoc County APCD,Mojave Desert AQMD, Monterey Bay Unified APCD, and North Coast Unified AQMD

		Air pollution co		control agency	
	Subpart	Modoc County APCD	Mojave Desert AQMD	Monterey Bay Unified APCD	North Coast Unified AQMD
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994		X		
Eb	Large Municipal Waste Combustors Constructed After September 20, 1994		X		
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996		X		
F	Portland Cement Plants	X	X	Х	Х
G	Nitric Acid Plants	Х	Х	Х	X
Ga	Nitric Acid Plants For Which Construction, Reconstruction or Modification Commenced After October 14, 2011				
Н	Sulfuric Acid Plant	X	X	X	Х
Ι	Hot Mix Asphalt Facilities	Х	X	X	X
J	Petroleum Refineries	X	X	Х	X
Ja	Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After May 14, 2007		X		
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	X	X	Х	X
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	X	Х	Х	Х
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	X	X	X	X
L	Secondary Lead Smelters	X	X	X	X
М	Secondary Brass and Bronze Production Plants	X	X	Х	X
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973	X	X	X	X
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983	X	X	X	X
0	Sewage Treatment Plants	X	X	Х	X
Р	Primary Copper Smelters	X	X	Х	X
Q	Primary Zinc Smelters	X	X	Х	X
R	Primary Lead Smelters	X	X	Х	X
S	Primary Aluminum Reduction Plants	X	X	Х	Х
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	X	Х	Х	Х
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	Х	Х	Х	Х
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	Х	Х	X	Х
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	Х	Х	Х	Х
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage	X	X	X	X

Table 7 to Paragraph (d)(2)(v)-Delegation Status for New Source Performance Standards for Modoc County APC	D,
Mojave Desert AQMD, Monterey Bay Unified APCD, and North Coast Unified AQMD	

		Air pollution co		control agency	
	Subpart	Modoc County APCD	Mojave Desert AQMD	Monterey Bay Unified APCD	North Coast Unified AQMD
	Facilities				
Y	Coal Preparation and Processing Plants	X	X	X	X
Ζ	Ferroalloy Production Facilities	X	X	X	X
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983	X	Х	X	Х
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983	X	X	X	Х
BB	Kraft Pulp Mills	Х	X	X	Х
CC	Glass Manufacturing Plants	Х	Х	Х	Х
DD	Grain Elevators	Х	X	X	X
EE	Surface Coating of Metal Furniture	X	X	Х	Х
FF	(Reserved)				
GG	Stationary Gas Turbines	X	X	Х	X
HH	Lime Manufacturing Plants	X	X	X	X
KK	Lead-Acid Battery Manufacturing Plants	X	X	X	X
LL	Metallic Mineral Processing Plants	X	X	X	X
MM	Automobile and Light Duty Trucks Surface Coating Operations	X	X	Х	X
NN	Phosphate Rock Plants	X	X	X	X
PP	Ammonium Sulfate Manufacture	X	X	Х	X
QQ	Graphic Arts Industry: Publication Rotogravure Printing	X	X	X	X
RR	Pressure Sensitive Tape and Label Surface Coating Operations	X	X	Х	X
SS	Industrial Surface Coating: Large Appliances	X	X	X	X
TT	Metal Coil Surface Coating	X	X	X	X
UU	Asphalt Processing and Asphalt Roofing Manufacture	X	X	X	X
VV	Equipment Leaks of VOC in the Synthetic Organic Industry Chemicals Manufacturing	Х	X	X	X
VVa	Equipment Leaks of VOC in the Synthetic Organic Industry for Which Construction, Reconstruction, or Chemicals Manufacturing Modification Commenced After November 7, 2006		X		
WW	Beverage Can Surface Coating Industry	Х	X	Х	Х
XX	Bulk Gasoline Terminals				
AAA	New Residential Wood Heaters	X	Х	Х	Х
BBB	Rubber Tire Manufacturing Industry	X	X	Х	X
CCC	(Reserved)				
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry	Х	Х	Х	
EEE	(Reserved)				

#### NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

# Table 7 to Paragraph (d)(2)(v)—Delegation Status for New Source Performance Standards for Modoc County APCD,Mojave Desert AQMD, Monterey Bay Unified APCD, and North Coast Unified AQMD

		Air	pollution	control ag	ency
	Subpart	Modoc County APCD	Mojave Desert AQMD	Monterey Bay Unified APCD	North Coast Unified AQMD
FFF	Flexible Vinyl and Urethane Coating and Printing	X	Х	Х	Х
GGG	Equipment Leaks of VOC in Petroleum Refineries	X	Х	Х	Х
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006		х		
HHH	Synthetic Fiber Production Facilities	X	Х	Х	Х
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes		х		
JJJ	Petroleum Dry Cleaners	X	X	X	Х
KKK	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants	Х	X	X	Х
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions	X	X	Х	X
MMM	(Reserved)				
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations	X	X	X	
000	Nonmetallic Mineral Processing Plants	X	Х	Х	Х
PPP	Wool Fiberglass Insulation Manufacturing Plants	X	Х	Х	X
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems	X	Х	Х	X
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes		Х		
SSS	Magnetic Tape Coating Facilities	X	Х	Х	X
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines	X	Х	X	X
UUU	Calciners and Dryers in Mineral Industries		Х	Х	
VVV	Polymeric Coating of Supporting Substrates Facilities		Х	Х	Х
WWW	Municipal Solid Waste Landfills		Х	Х	
AAAA	Small Municipal Waste Combustion Units for Which Construction is Commenced After August 30, 1999 or for Which Modification or Reconstruction is Commended After June 6, 2001		X		
СССС	Commercial and Industrial Solid Waste Incineration Units for Which Construction Is Commenced After November 30, 1999 or for Which Modification or Reconstruction Is Commenced on or After June 1, 2001		Х		
EEEE	Other Solid Waste Incineration Units for Which Construction is Commenced After December 9, 2004, or for Which Modification or Reconstruction is Commenced on or After June 16, 2006		Х		
GGGG	(Reserved)				
HHHH	(Reserved)				
IIII	Stationary Compression Ignition Internal Combustion Engines		X	Х	
JJJJ	Stationary Spark Ignition Internal Combustion Engines		Х	X	
KKKK	Stationary Combustion Turbines		X	X	

 Table 7 to Paragraph (d)(2)(v)—Delegation Status for New Source Performance Standards for Modoc County APCD,

 Mojave Desert AQMD, Monterey Bay Unified APCD, and North Coast Unified AQMD

	Subpart	Air pollution control agency				
		Modoc County APCD	Mojave Desert AQMD	Monterey Bay Unified APCD	North Coast Unified AQMD	
LLLL	New Sewage Sludge Incineration Units					
0000	Crude Oil and Natural Gas Production, Transmission, and Distribution					

(vi) Delegations for Northern Sierra Air Quality Management District, Northern Sonoma County Air Pollution Control District, Placer County Air Pollution Control District, and Sacramento Metropolitan Air Quality Management District are shown in the following table:

Delegation Status for New Source Performance Standards for Northern Sierra Air Quality Management District, Northern Sonoma County Air Pollution Control District, Placer County Air Pollution Control District, and Sacramento Metropolitan Air Quality Management District

		Air pollution control agency					
	Subpart	Northern Sierra AQMD	Northern Sonoma County APCD	Placer County APCD	Sacramento Metropolitan AQMD		
А	General Provisions		X		Х		
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971		X		X		
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978		X		X		
Db	Industrial-Commercial-Institutional Steam Generating Units				X		
Dc	Small Industrial Steam Generating Units				X		
E	Incinerators		Х		Х		
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994				X		
Eb	Municipal Waste Combustors Constructed After September 20, 1994				X		
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996				X		
F	Portland Cement Plants		Х		Х		
G	Nitric Acid Plants		Х		X		
Н	Sulfuric Acid Plants		Х		Х		
Ι	Hot Mix Asphalt Facilities		Х		X		
J	Petroleum Refineries		Х		Х		
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978		X		X		
Ka	Storage Vessels for Petroleum Liquids for Which		X		X		

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Delegation Status for New Source Performance Standards for Northern Sierra Air Quality Management District, Northern Sonoma County Air Pollution Control District, Placer County Air Pollution Control District, and Sacramento Metropolitan Air Quality Management District

		Air pollution control agency					
	Subpart	Northern Sierra AQMD	Northern Sonoma County APCD	Placer County APCD	Sacramento Metropolitan AQMD		
	Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984						
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984				X		
L	Secondary Lead Smelters		X		X		
М	Secondary Brass and Bronze Production Plants		X		X		
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973		X	4	X		
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983				X		
0	Sewage Treatment Plants		X		X		
Р	Primary Copper Smelters		X		Х		
Q	Primary Zinc Smelters		X		X		
R	Primary Lead Smelters		X		X		
S	Primary Aluminum Reduction Plants		X		X		
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants		X		X		
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants		X		X		
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants		X		X		
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants		X		X		
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities		X		X		
Y	Coal Preparation Plants		X		X		
Ζ	Ferroalloy Production Facilities		X		X		
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983		X		X		
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983				Х		
BB	Kraft pulp Mills		Х		X		
CC	Glass Manufacturing Plants		X		X		

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Delegation Status for New Source Performance Standards for Northern Sierra Air Quality Management District, Northern Sonoma County Air Pollution Control District, Placer County Air Pollution Control District, and Sacramento Metropolitan Air Quality Management District

		Air pollution control agency				
	Subpart	Northern Sierra AQMD	Northern Sonoma County APCD	Placer County APCD	Sacramento Metropolitan AQMD	
DD	Grain Elevators		X		X	
EE	Surface Coating of Metal Furniture				Х	
FF	(Reserved)					
GG	Stationary Gas Turbines		X		Х	
HH	Lime Manufacturing Plants		X		X	
KK	Lead-Acid Battery Manufacturing Plants				Х	
LL	Metallic Mineral Processing Plants				X	
MM	Automobile and Light Duty Trucks Surface Coating Operations		X		X	
NN	Phosphate Rock Plants				Х	
PP	Ammonium Sulfate Manufacture		X		Х	
QQ	Graphic Arts Industry: Publication Rotogravure Printing				Х	
RR	Pressure Sensitive Tape and Label Surface Coating Operations				X	
SS	Industrial Surface Coating: Large Appliances				X	
TT	Metal Coil Surface Coating				X	
UU	Asphalt Processing and Asphalt Roofing Manufacture	-			Х	
VV	Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry				X	
WW	Beverage Can Surface Coating Industry				Х	
XX	Bulk Gasoline Terminals					
AAA	New Residential Wool Heaters				X	
BBB	Rubber Tire Manufacturing Industry				X	
CCC	(Reserved)					
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry				X	
EEE	(Reserved)					
FFF	Flexible Vinyl and Urethane Coating and Printing				Х	
GGG	Equipment Leaks of VOC in Petroleum Refineries				X	
HHH	Synthetic Fiber Production Facilities				Х	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes				X	
JJJ	Petroleum Dry Cleaners				Х	
ккк	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants				X	
LLL	Onshore Natural Gas Processing: SO2 Emissions				X	

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Delegation Status for New Source Performance Standards for Northern Sierra Air Quality Management District, Northern Sonoma County Air Pollution Control District, Placer County Air Pollution Control District, and Sacramento Metropolitan Air Quality Management District

			Air pollution	control age	ency
	Subpart	Northern Sierra AQMD	Northern Sonoma County APCD	Placer County APCD	Sacramento Metropolitan AQMD
MMM	(Reserved)				
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations				X
000	Nonmetallic Mineral Processing Plants				X
PPP	Wool Fiberglass Insulation Manufacturing Plants				X
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems				X
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes				х
SSS	Magnetic Tape Coating Facilities				Х
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines				X
UUU	Calciners and Dryers in Mineral Industries				Х
VVV	Polymeric Coating of Supporting Substrates Facilities				X
WWW	Municipal Solid Waste Landfills				X

(vii) Delegations for San Diego County Air Pollution Control District, San Joaquin Valley Unified Air Pollution Control District, San Luis Obispo County Air Pollution Control District, and Santa Barbara County Air Pollution Control District are shown in the following table:

Table 9 to Paragraph (d)(2)(vii)—Delegation Status for New Source Performance Standards for San Diego County APCD,<br/>San Joaquin Valley Unified APCD, San Luis Obispo County APCD, and Santa Barbara County APCD

			Air pollution control agency				
	Subpart	San Diego County APCD	San Joaquin Valley Unified APCD	San Luis Obispo County APCD	Santa Barbara County APCD		
А	General Provisions	Х	Х	X	Х		
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	X	Х	Х	Х		
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978	Х	Х	Х	Х		
Db	Industrial-Commercial-Institutional Steam Generating Units	Х	Х	Х	Х		
Dc	Small Industrial-Commercial-Institutional Steam Generating Units	Х	Х	Х	X		
E	Incinerators	X	Х	X	X		
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994	X	X	Х			
Eb	Large Municipal Waste Combustors Constructed After September 20, 1994	X	Х		X		
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is	X			X		

		Air	Air pollution control age		
	Subpart	San Diego County APCD	San Joaquin Valley Unified APCD	San Luis Obispo County APCD	Santa Barbara County APCD
	Commenced After June 20, 1996				
F	Portland Cement Plants	X	X	Х	
G	Nitric Acid Plants	X	X	Х	
Ga	Nitric Acid Plants For Which Construction, Reconstruction or Modification Commenced After October 14, 2011				
Н	Sulfuric Acid Plant	X	X	X	
Ι	Hot Mix Asphalt Facilities	X	X	X	X
J	Petroleum Refineries	X	X	X	X
Ja	Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After May 14, 2007				X
К	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	X	X	X	X
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	x	X	X	X
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	X	X	X	X
L	Secondary Lead Smelters	X	X	X	X
М	Secondary Brass and Bronze Production Plants	X	X	X	X
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973	X	X	X	
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983	X	X	X	
0	Sewage Treatment Plants	X	X	Х	X
Р	Primary Copper Smelters	X	X	X	
Q	Primary Zinc Smelters	X	X	X	
R	Primary Lead Smelters	X	X	Х	
S	Primary Aluminum Reduction Plants	X	X	X	
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	X	X	Х	
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	Х	X	X	
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	Х	X	X	
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	X	X	X	
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities	Х	Х	Х	
Y	Coal Preparation and Processing Plants	Х	X	X	
Ζ	Ferroalloy Production Facilities	Х	Х	Х	

		Air	Air pollution control ag		
	Subpart	San Diego County APCD	San Joaquin Valley Unified APCD	San Luis Obispo County APCD	Santa Barbara County APCD
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983	x	X	X	
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983	X	Х	х	
BB	Kraft Pulp Mills	X	Х	Х	
CC	Glass Manufacturing Plants	X	X	X	X
DD	Grain Elevators	X	X	X	Х
EE	Surface Coating of Metal Furniture	Х	X	X	
FF	(Reserved)				
GG	Stationary Gas Turbines	Х	X	X	Х
HH	Lime Manufacturing Plants	X	X	X	
KK	Lead-Acid Battery Manufacturing Plants	Х	X	X	
LL	Metallic Mineral Processing Plants	X	X	X	
MM	Automobile and Light Duty Trucks Surface Coating Operations	X	X	X	
NN	Phosphate Rock Plants	X	X	X	
PP	Ammonium Sulfate Manufacture	Х	X	X	
QQ	Graphic Arts Industry: Publication Rotogravure Printing	Х	X	X	
RR	Pressure Sensitive Tape and Label Surface Coating Operations	Х	X	X	
SS	Industrial Surface Coating: Large Appliances	Х	X	X	
TT	Metal Coil Surface Coating	Х	X	Х	
UU	Asphalt Processing and Asphalt Roofing Manufacture	Х	X	X	
VV	Equipment Leaks of VOC in the Synthetic Organic Industry Chemicals Manufacturing	X	X	X	
VVa	Equipment Leaks of VOC in the Synthetic Organic Industry for Which Construction, Reconstruction, or Chemicals Manufacturing Modification Commenced After November 7, 2006				x
WW	Beverage Can Surface Coating Industry	Х	X	X	
XX	Bulk Gasoline Terminals				
AAA	New Residential Wood Heaters	X	X	X	Х
BBB	Rubber Tire Manufacturing Industry	Х	X	X	
CCC	(Reserved)				
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry	Х	Х		
EEE	(Reserved)				
FFF	Flexible Vinyl and Urethane Coating and Printing	Х	X	X	
GGG	Equipment Leaks of VOC in Petroleum Refineries	x	X	X	

		Air J	Air pollution control age		
	Subpart	San Diego County APCD	San Joaquin Valley Unified APCD	San Luis Obispo County APCD	Santa Barbara County APCD
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006				X
HHH	Synthetic Fiber Production Facilities	X	X	Х	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes	X	х		
JJJ	Petroleum Dry Cleaners	Х	X	Х	
KKK	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants	X	X	X	
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions	Х	X	X	
MMM	(Reserved)				
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations	X	X		
000	Nonmetallic Mineral Processing Plants	X	X	X	X
PPP	Wool Fiberglass Insulation Manufacturing Plants	X	X	X	
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems	X	X	X	
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes	X	X	Х	
SSS	Magnetic Tape Coating Facilities	Х	X	X	
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines	X	X	X	
UUU	Calciners and Dryers in Mineral Industries	Х	X	X	X
VVV	Polymeric Coating of Supporting Substrates Facilities	X	X	X	X
WWW	Municipal Solid Waste Landfills	Х	X	X	X
АААА	Small Municipal Waste Combustion Units for Which Construction is Commenced After August 30, 1999 or for Which Modification or Reconstruction is Commended After June 6, 2001	X			X
сссс	Commercial and Industrial Solid Waste Incineration Units for Which Construction Is Commenced After November 30, 1999 or for Which Modification or Reconstruction Is Commenced on or After June 1, 2001	Х			Х
EEEE	Other Solid Waste Incineration Units for Which Construction is Commenced After December 9, 2004, or for Which Modification or Reconstruction is Commenced on or After June 16, 2006	X			x
GGGG	(Reserved)				
HHHH	(Reserved)				
IIII	Stationary Compression Ignition Internal Combustion Engines	Х			X
JJJJ	Stationary Spark Ignition Internal Combustion Engines	Х			X
КККК	Stationary Combustion Turbines	Х			X
LLLL	New Sewage Sludge Incineration Units				
0000	Crude Oil and Natural Gas Production, Transmission, and Distribution				

Table 9 to Paragraph (d)(2)(vii)—Delegation Status for New Source Performance Standards for San Diego County APCD,						
	San Joaquin Valley Unified APCD, San Luis Obispo County APCD, and Sar	ita Barba	ra County	APCD		
		Air pollution control agency				
	Subpart	San Diego County APCD	San Joaquin Valley Unified APCD	San Luis Obispo County APCD	Santa Barbara County APCD	
QQQQ	Standards of Performance for New Residential Hydronic Heaters and Forced- Air Furnaces	x				
TTTT	Standards of Performance for Greenhouse Gas Emissions for Electric Generating Units	Х				

(viii) Delegations for Shasta County Air Quality Management District, Siskiyou County Air Pollution Control District, South Coast Air Quality Management District, and Tehama County Air Pollution Control District are shown in the following table:

Deleg	AQMD, and Tehama County A	PCD			Julii Coust		
		Air pollution control agency					
	Subpart	Shasta County AQMD	Siskiyou County APCD	South Coast AQMD	Tehama County APCD		
А	General Provisions	Х	Х	Х			
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	x		Х			
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978			Х			
Db	Industrial-Commercial-Institutional Steam Generating Units			Х			
Dc	Small Industrial-Commercial-Institutional Steam Generating Units			Х			
E	Incinerators	Х		Х			
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994			Х			
Eb	Large Municipal Waste Combustors Constructed After September 20, 1994			X			
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996			X			
F	Portland Cement Plants	Х		Х			
G	Nitric Acid Plants	Х		Х			
Ga	Nitric Acid Plants For Which Construction, Reconstruction or Modification Commenced After October 14, 2011						
Н	Sulfuric Acid Plant	X		Х			
Ι	Hot Mix Asphalt Facilities	Х		Х			
J	Petroleum Refineries	Х		Х			
Ja	Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After May 14, 2007			Х			
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	X		X			

Delegation Status for New Source Performance Standards for Shasta County AQMD, Siskiyou County APCD, Sout	h Coast
AQMD, and Tehama County APCD	

		Air pollution control agenc			Air pollution control agency	cy
	Subpart	Shasta County AQMD	Siskiyou County APCD	South Coast AQMD	Tehama County APCD	
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984			X		
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984			X		
L	Secondary Lead Smelters	Х		Х		
М	Secondary Brass and Bronze Production Plants	Х		X		
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973	X		X		
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983			X		
0	Sewage Treatment Plants	Х		Х		
Р	Primary Copper Smelters	Х		Х		
Q	Primary Zinc Smelters	Х		Х		
R	Primary Lead Smelters	X	P	Х		
S	Primary Aluminum Reduction Plants	X		Х		
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	X		Х		
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	Х		Х		
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	Х		Х		
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	Х		Х		
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities	X		X		
Y	Coal Preparation and Processing Plants	Х		Х		
Ζ	Ferroalloy Production Facilities	Х		Х		
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983	X		X		
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983			X		
BB	Kraft Pulp Mills	Х		Х		
CC	Glass Manufacturing Plants			Х		
DD	Grain Elevators	Х		Х		
EE	Surface Coating of Metal Furniture			Х		
FF	(Reserved)					
GG	Stationary Gas Turbines			Х		
HH	Lime Manufacturing Plants	Х		Х		
KK	Lead-Acid Battery Manufacturing Plants			Х		
LL	Metallic Mineral Processing Plants			X		

Delegation Status for New Source Performance Standards for Shasta County AQMD, Siskiyou County APCD, South Coast
AQMD, and Tehama County APCD

		Ai	ir pollution c	ontrol agen	cy
	Subpart	Shasta County AQMD	Siskiyou County APCD	South Coast AQMD	Tehama County APCD
MM	Automobile and Light Duty Trucks Surface Coating Operations			Х	
NN	Phosphate Rock Plants			Х	
PP	Ammonium Sulfate Manufacture			Х	
QQ	Graphic Arts Industry: Publication Rotogravure Printing			Х	
RR	Pressure Sensitive Tape and Label Surface Coating Operations			Х	
SS	Industrial Surface Coating: Large Appliances			Х	
TT	Metal Coil Surface Coating			Х	
UU	Asphalt Processing and Asphalt Roofing Manufacture			X	
VV	Equipment Leaks of VOC in the Synthetic Organic Industry Chemicals Manufacturing			X	
VVa	Equipment Leaks of VOC in the Synthetic Organic Industry for Which Construction, Reconstruction, or Chemicals Manufacturing Modification Commenced After November 7, 2006			X	
WW	Beverage Can Surface Coating Industry			Х	
XX	Bulk Gasoline Terminals				
AAA	New Residential Wood Heaters		X	Х	
BBB	Rubber Tire Manufacturing Industry		Х	Х	
CCC	(Reserved)				
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry			X	
EEE	(Reserved)				
FFF	Flexible Vinyl and Urethane Coating and Printing			Х	
GGG	Equipment Leaks of VOC in Petroleum Refineries			Х	
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006			X	
HHH	Synthetic Fiber Production Facilities			Х	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes			X	
JJJ	Petroleum Dry Cleaners			Х	
ккк	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants			X	
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions			X	
MMM	(Reserved)				
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations			Х	
000	Nonmetallic Mineral Processing Plants			X	

#### NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Delega	AQMD, and Tehama County AI	Y AQIVID, S PCD	iskiyou Coun	iy APCD, So	Julii Coast
		Ai	Air pollution control agency		
	Subpart	Shasta County AQMD	Siskiyou County APCD	South Coast AQMD	Tehama County APCD
PPP	Wool Fiberglass Insulation Manufacturing Plants			Х	
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems		X	Х	
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes			X	
SSS	Magnetic Tape Coating Facilities		X	Х	
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines		X	X	
UUU	Calciners and Dryers in Mineral Industries			X	
VVV	Polymeric Coating of Supporting Substrates Facilities			X	
WWW	Municipal Solid Waste Landfills			Х	
АААА	Small Municipal Waste Combustion Units for Which Construction is Commenced After August 30, 1999 or for Which Modification or Reconstruction is Commended After June 6, 2001	X	X	X	
СССС	Commercial and Industrial Solid Waste Incineration Units for Which Construction Is Commenced After November 30, 1999 or for Which Modification or Reconstruction Is Commenced on or After June 1, 2001			X	
EEEE	Other Solid Waste Incineration Units for Which Construction is Commenced After December 9, 2004, or for Which Modification or Reconstruction is Commenced on or After June 16, 2006			X	
GGGG	(Reserved)				
HHHH	(Reserved)				
IIII	Stationary Compression Ignition Internal Combustion Engines			Х	
JJJJ	Stationary Spark Ignition Internal Combustion Engines			Х	
KKKK	Stationary Combustion Turbines			Х	
LLLL	New Sewage Sludge Incineration Units				
0000	Crude Oil and Natural Gas Production, Transmission, and Distribution				

(ix) Delegations for Tuolumne County Air Pollution Control District, Ventura County Air Pollution Control District, and Yolo-Solano Air Quality Management District are shown in the following table:

Table	11 to Paragraph (d)(2)(ix)—Delegation Status for New Source Performance Standards f	for Tuolumn	e County	APCD,
	Ventura County ATCD, and Tolo-Solano AQMD	Air pollution control agency		
	Subpart	Tuolumne County APCD	Ventura County APCD	Yolo- Solano AQMD
А	General Provisions		X	X
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971		Х	Х

		Air pol	lution con agency	ntrol
	Subpart	Tuolumne County APCD	Ventura County APCD	Yolo- Solano AQMD
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978		Х	
Db	Industrial-Commercial-Institutional Steam Generating Units		Х	X
Dc	Small Industrial-Commercial-Institutional Steam Generating Units		X	
Е	Incinerators		Х	
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994		X	
Eb	Large Municipal Waste Combustors Constructed After September 20, 1994			
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996			
F	Portland Cement Plants		X	
G	Nitric Acid Plants		Х	
Н	Sulfuric Acid Plant		X	
Ι	Hot Mix Asphalt Facilities		Х	X
J	Petroleum Refineries		Х	X
К	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978		X	X
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984		X	
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984		х	
L	Secondary Lead Smelters		X	
М	Secondary Brass and Bronze Production Plants		X	
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973		X	
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983		X	
0	Sewage Treatment Plants		Х	
Р	Primary Copper Smelters		Х	
Q	Primary Zinc Smelters		Х	
R	Primary Lead Smelters		Х	
S	Primary Aluminum Reduction Plants		Х	
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants		Х	
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants		X	
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants		X	
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants		Х	
Χ	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities		Х	
Y	Coal Preparation and Processing Plants		X	

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Table	11 to Paragraph (d)(2)(ix)—Delegation Status for New Source Performance Standards f Ventura County APCD, and Yolo-Solano AQMD	òr Tuolumn	e County	APCD,
		Air pol	itrol	
	Subpart	Tuolumne County APCD	Ventura County APCD	Yolo- Solano AQMD
Ζ	Ferroalloy Production Facilities		X	
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983		X	Х
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983		Х	
BB	Kraft Pulp Mills		X	
CC	Glass Manufacturing Plants		X	
DD	Grain Elevators		X	
EE	Surface Coating of Metal Furniture		X	
FF	(Reserved)			
GG	Stationary Gas Turbines		X	
HH	Lime Manufacturing Plants		X	
KK	Lead-Acid Battery Manufacturing Plants		X	
LL	Metallic Mineral Processing Plants		X	
MM	Automobile and Light Duty Trucks Surface Coating Operations		X	
NN	Phosphate Rock Plants		X	
PP	Ammonium Sulfate Manufacture		X	
QQ	Graphic Arts Industry: Publication Rotogravure Printing		X	
RR	Pressure Sensitive Tape and Label Surface Coating Operations		X	
SS	Industrial Surface Coating: Large Appliances		X	
TT	Metal Coil Surface Coating		X	
UU	Asphalt Processing and Asphalt Roofing Manufacture		X	
VV	Equipment Leaks of VOC in the Synthetic Organic Industry Chemicals Manufacturing		X	
WW	Beverage Can Surface Coating Industry		X	
XX	Bulk Gasoline Terminals			
AAA	New Residential Wood Heaters		X	
BBB	Rubber Tire Manufacturing Industry		X	
CCC	(Reserved)			
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry		X	
EEE	(Reserved)			
FFF	Flexible Vinyl and Urethane Coating and Printing		Х	
GGG	Equipment Leaks of VOC in Petroleum Refineries		Х	
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006			
HHH	Synthetic Fiber Production Facilities		Х	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical		Х	

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Table	11 to Paragraph (d)(2)(ix)—Delegation Status for New Source Performance Standards f Ventura County APCD, and Yolo-Solano AQMD	for Tuolumn	e County	APCD,	
			Air pollution contro agency		
	Subpart	Tuolumne County APCD	Ventura County APCD	Yolo- Solano AQMD	
	Manufacturing Industry (SOCMI) Air Oxidation Unit Processes				
JJJ	Petroleum Dry Cleaners		Х		
KKK	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants		Х		
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions		Х		
MMM	(Reserved)				
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations		Х		
000	Nonmetallic Mineral Processing Plants		Х	Х	
PPP	Wool Fiberglass Insulation Manufacturing Plants		X		
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems		Х		
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes		Х		
SSS	Magnetic Tape Coating Facilities		Х		
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines		Х		
UUU	Calciners and Dryers in Mineral Industries		Х		
VVV	Polymeric Coating of Supporting Substrates Facilities		Х		
WWW	Municipal Solid Waste Landfills	Х	Х		

(3) Hawaii. The following table identifies delegations for Hawaii:

Delegation Status for New Source Performance Standards for Hawaii:

Delegation Status for New Source Performance Standards for Hawaii				
	Subpart	Hawaii		
А	General Provisions	Х		
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	X		
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978	Х		
Db	Industrial-Commercial-Institutional Steam Generating Units	X		
Dc	Small Industrial Steam Generating Units	X		
E	Incinerators	X		
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994	Х		
Eb	Municipal Waste Combustors Constructed After September 20, 1994	X		
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996	X		
F	Portland Cement Plants	X		
G	Nitric Acid Plants			
Н	Sulfuric Acid Plants			
Ι	Hot Mix Asphalt Facilities	Х		
J	Petroleum Refineries	Х		

	Delegation Status for New Source Performance Standards for Hawaii	
	Subpart	Hawaii
Ja	Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After May 14, 2007	
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	X
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	X
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	Х
L	Secondary Lead Smelters	
М	Secondary Brass and Bronze Production Plants	
N	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973	
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983	
0	Sewage Treatment Plants	X
Р	Primary Copper Smelters	
Q	Primary Zinc Smelters	
R	Primary Lead Smelters	
S	Primary Aluminum Reduction Plants	
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants	
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	
Х	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities	
Y	Coal Preparation Plants	Х
Ζ	Ferroalloy Production Facilities	
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983	Х
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983	X
BB	Kraft pulp Mills	
CC	Glass Manufacturing Plants	
DD	Grain Elevators	
EE	Surface Coating of Metal Furniture	
FF	(Reserved)	
GG	Stationary Gas Turbines	X
HH	Lime Manufacturing Plants	
KK	Lead-Acid Battery Manufacturing Plants	
LL	Metallic Mineral Processing Plants	
MM	Automobile and Light Duty Trucks Surface Coating Operations	
NN	Phosphate Rock Plants	
PP	Ammonium Sulfate Manufacture	

	Delegation Status for New Source Performance Standards for Hawaii	
	Subpart	Hawaii
QQ	Graphic Arts Industry: Publication Rotogravure Printing	
RR	Pressure Sensitive Tape and Label Surface Coating Operations	
SS	Industrial Surface Coating: Large Appliances	
TT	Metal Coil Surface Coating	
UU	Asphalt Processing and Asphalt Roofing Manufacture	
VV	Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry	X
VVa	Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006	
WW	Beverage Can Surface Coating Industry	X
XX	Bulk Gasoline Terminals	X
AAA	New Residential Wool Heaters	
BBB	Rubber Tire Manufacturing Industry	
CCC	(Reserved)	
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry	
EEE	(Reserved)	
FFF	Flexible Vinyl and Urethane Coating and Printing	
GGG	Equipment Leaks of VOC in Petroleum Refineries	X
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006	
HHH	Synthetic Fiber Production Facilities	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes	
JJJ	Petroleum Dry Cleaners	X
KKK	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants	
LLL	Onshore Natural Gas Processing: SO2 Emissions	
MMM	(Reserved)	
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations	X
000	Nonmetallic Mineral Processing Plants	X
PPP	Wool Fiberglass Insulation Manufacturing Plants	
QQQ	VOC Emissions From Petroleum Refinery Wastewater	X
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes	
SSS	Magnetic Tape Coating Facilities	
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines	
UUU	Calciners and Dryers in Mineral Industries	X
VVV	Polymeric Coating of Supporting Substrates Facilities	X
WWW	Municipal Solid Waste Landfills	X
AAAA	Small Municipal Waste Combustion Units for Which Construction is Commenced After August 30, 1999 or for Which Modification or Reconstruction is Commenced After June 6, 2001	X
CCCC	Commercial and Industrial Solid Waste Incineration Units for Which Construction Is Commenced After	X

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Delegation Status for New Source Performance Standards for Hawaii				
	Subpart	Hawaii		
	November 30, 1999 or for Which Modification or Reconstruction Is Commenced on or After June 1, 2001			
EEEE	Other Solid Waste Incineration Units for Which Construction is Commenced After December 9, 2004, or for Which Modification or Reconstruction is Commenced on or After June 16, 2006			
GGGG	(Reserved)			
IIII	Stationary Compression Ignition Internal Combustion Engines			
JJJJ	Stationary Spark Ignition Internal Combustion Engines			
КККК	Stationary Combustion Turbines			

(4) Nevada. The following table identifies delegations for Nevada:

	Table 12 to Paragraph (d)(4)—Delegation Status for New Source Performance Standards for Nevada					
	Subpart	Air pollution c agency		ontrol		
	Subpart	Nevada DEP	Clark County	Washoe County		
А	General Provisions	X	X	X		
Cf	Emission Guidelines and Compliance Times for Municipal Solid Waste Landfills	Х				
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	X	X	Х		
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978	X	X			
Db	Industrial-Commercial-Institutional Steam Generating Units	X	X			
Dc	Small Industrial-Commercial-Institutional Steam Generating Units	X	X			
Е	Incinerators	X	X	Х		
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994	X	X			
Eb	Large Municipal Waste Combustors Constructed After September 20, 1994	X	X			
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996	X	Х			
F	Portland Cement Plants	X	X	Х		
G	Nitric Acid Plants	X	X			
Ga	Nitric Acid Plants For Which Construction, Reconstruction or Modification Commenced After October 14, 2011	X				
Η	Sulfuric Acid Plant	X	X			
Ι	Hot Mix Asphalt Facilities	X	X	Х		
J	Petroleum Refineries	X	X			
Ja	Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After May 14, 2007	X				
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	X	X	X		
Ka	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	X	Х	X		
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	x	X			

	Table 12 to Paragraph (d)(4)—Delegation Status for New Source Performance Stand	dards for N	Jevada	
	Subpart	Air p	ontrol	
	Subpart	Nevada DEP	Clark County	Washoe County
L	Secondary Lead Smelters	Х	X	Х
М	Secondary Brass and Bronze Production Plants	Х	Х	
Ν	Primary Emissions from Basic Oxygen Process Furnaces for Which Construction is Commenced After June 11, 1973	Х	Х	
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities for Which Construction is Commenced After January 20, 1983	X	Х	
0	Sewage Treatment Plants	X	X	X
Р	Primary Copper Smelters	X	X	Х
Q	Primary Zinc Smelters	X	X	Х
R	Primary Lead Smelters	X	X	X
S	Primary Aluminum Reduction Plants	X	X	
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Acid Plants		Х	
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants		Х	
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants		Х	
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants		Х	
Х	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities		Х	
Y	Coal Preparation and Processing Plants	X	Х	Х
Ζ	Ferroalloy Production Facilities	X	X	
AA	Steel Plants: Electric Arc Furnaces Constructed After October 21, 1974 and On or Before August 17, 1983	X	Х	
AAa	Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983	X	Х	
BB	Kraft Pulp Mills		Х	
CC	Glass Manufacturing Plants	X	X	
DD	Grain Elevators	X	X	X
EE	Surface Coating of Metal Furniture	X	X	Х
FF	(Reserved)			
GG	Stationary Gas Turbines	Х	Х	Х
HH	Lime Manufacturing Plants	X	X	X
KK	Lead-Acid Battery Manufacturing Plants	X	X	Х
LL	Metallic Mineral Processing Plants	Х	Х	Х
MM	Automobile and Light Duty Trucks Surface Coating Operations	X	X	Х
NN	Phosphate Rock Plants	X	X	Х
PP	Ammonium Sulfate Manufacture	Х	Х	
QQ	Graphic Arts Industry: Publication Rotogravure Printing	Х	Х	Х
RR	Pressure Sensitive Tape and Label Surface Coating Operations	X	X	
SS	Industrial Surface Coating: Large Appliances	Х	Х	Х
TT	Metal Coil Surface Coating	Х	Х	Х

	Table 12 to Paragraph (d)(4)—Delegation Status for New Source Performance Stand	lards for N	levada	
	Subnart	Air p	ollution c agency	ontrol
	Subpart	Nevada DEP	Clark County	Washoe County
UU	Asphalt Processing and Asphalt Roofing Manufacture	Х	Х	Х
VV	Equipment Leaks of VOC in the Synthetic Organic Industry Chemicals Manufacturing	Х	Х	Х
VVa	Equipment Leaks of VOC in the Synthetic Organic Industry for Which Construction, Reconstruction, or Chemicals Manufacturing Modification Commenced After November 7, 2006	X	X	
WW	Beverage Can Surface Coating Industry	Х	Х	
XX	Bulk Gasoline Terminals	X	X	
AAA	New Residential Wood Heaters		X	
BBB	Rubber Tire Manufacturing Industry	X	Х	
CCC	(Reserved)			
DDD	Volatile Organic Compounds (VOC) Emissions from the Polymer Manufacturing Industry	X	x	
EEE	(Reserved)			
FFF	Flexible Vinyl and Urethane Coating and Printing	X	X	
GGG	Equipment Leaks of VOC in Petroleum Refineries	X	X	
GGGa	Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006	X	x	
HHH	Synthetic Fiber Production Facilities	X	X	
III	Volatile Organic Compound (VOC) Emissions From the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes	X	X	
JJJ	Petroleum Dry Cleaners	Х	Х	Х
KKK	Equipment Leaks of VOC From Onshore Natural Gas Processing Plants	X	X	
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions	Х	Х	
MMM	(Reserved)			
NNN	Volatile Organic Compound (VOC) Emissions From Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations	X	Х	
000	Nonmetallic Mineral Processing Plants	Х	X	
PPP	Wool Fiberglass Insulation Manufacturing Plants	Х	X	
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems	Х	Х	
RRR	Volatile Organic Compound Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes	X	Х	
SSS	Magnetic Tape Coating Facilities	X	X	
TTT	Industrial Surface Coating: Surface Coating of Plastic Parts for Business Machines	Х	X	Х
UUU	Calciners and Dryers in Mineral Industries	Х	Х	Х
VVV	Polymeric Coating of Supporting Substrates Facilities	Х	X	Х
WWW	Municipal Solid Waste Landfills	Х	Х	Х
XXX	Municipal Solid Waste Landfills that Commenced Construction, Reconstruction, or Modification after July 17, 2014	X		
AAAA	Small Municipal Waste Combustion Units for Which Construction is Commenced After	Х	X	Х

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Table 12 to Paragraph (d)(4)—Delegation Status for New Source Performance Standards for Nevada				
	Subnart	Air po	ollution control agency	
	Subpart	Nevada DEP	Clark County	Washoe County
	August 30, 1999 or for Which Modification or Reconstruction is Commended After June 6, 2001			
CCCC	Commercial and Industrial Solid Waste Incineration Units for Which Construction Is Commenced After November 30, 1999 or for Which Modification or Reconstruction Is Commenced on or After June 1, 2001	X	X	х
EEEE	Other Solid Waste Incineration Units for Which Construction is Commenced After December 9, 2004, or for Which Modification or Reconstruction is Commenced on or After June 16, 2006	х	Х	х
GGGG	(Reserved)			
HHHH	(Reserved)			
IIII	Stationary Compression Ignition Internal Combustion Engines	X	X	Х
JJJJ	Stationary Spark Ignition Internal Combustion Engines	X	X	Х
KKKK	Stationary Combustion Turbines	Х	Х	Х
LLLL	New Sewage Sludge Incineration Units		X	
0000	Crude Oil and Natural Gas Production, Transmission, and Distribution	X		

(5) Guam. The following table identifies delegations as of June 15, 2001:

	Delegation Status for New Source Performance Standards for Guam		
	Subpart	Guam	
Α	General Provisions	Х	
D	Fossil-Fuel Fired Steam Generators Constructed After August 17, 1971	Х	
Da	Electric Utility Steam Generating Units Constructed After September 18, 1978		
Db	Industrial-Commercial-Institutional Steam Generating Units		
Dc	Small Industrial Steam Generating Units		
E	Incinerators		
Ea	Municipal Waste Combustors Constructed After December 20, 1989 and On or Before September 20, 1994		
Eb	Municipal Waste Combustors Constructed After September 20, 1994		
Ec	Hospital/Medical/Infectious Waste Incinerators for Which Construction is Commenced After June 20, 1996		
F	Portland Cement Plants	X	
G	Nitric Acid Plants		
Η	Sulfuric Acid Plants		
Ι	Hot Mix Asphalt Facilities	Х	
J	Petroleum Refineries	Х	
K	Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	X	

(e) The following lists the specific part 60 standards that have been delegated unchanged to the air pollution control agencies in Region 6.

(1) *New Mexico*. The New Mexico Environment Department has been delegated all part 60 standards promulgated by the EPA, except subpart AAA—Standards of Performance for New Residential Wood Heaters; and subpart QQQQ—Standards

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of Performance for New Residential Hydronic Heaters and Forced-Air Furnaces, as amended in the Federal Register through January 15, 2017.

(2) *Louisiana*. The Louisiana Department of Environmental Quality has been delegated all part 60 standards promulgated by EPA, except subpart AAA—Standards of Performance for New Residential Wood Heaters, as amended in the Federal Register through July 1, 2013.

Delegation Status for Part 60 Standards—State of Louisiana [Excluding Indian Country]		
Subpart	Source category	LDEQ <sup>1</sup>
A	General Provisions	Yes
Ce	Emission Guidelines and Compliance Times for Hospital/Medical/Infectious Waste Incinerators	Yes
D	Fossil Fueled Steam Generators (>250 MM BTU/hr)	Yes
Da	Electric Utility Steam Generating Units (>250 MM BTU/hr)	Yes
Db	Industrial-Commercial-Institutional Steam Generating Units (100 to 250 MM BTU/hr)	Yes
Dc	Industrial-Commercial-Institutional Small Steam Generating Units (10 to 100 MM BTU/hr)	Yes
Е	Incinerators (>50 tons per day)	Yes
Ea	Municipal Waste Combustors	Yes
Eb	Large Municipal Waste Combustors	Yes
Ec	Hospital/Medical/Infectious Waste Incinerators	Yes
F	Portland Cement Plants	Yes
G	Nitric Acid Plants	Yes
Ga	Nitric Acid Plants (after October 14, 2011)	Yes
Н	Sulfuric Acid Plants	Yes
Ι	Hot Mix Asphalt Facilities	Yes
J	Petroleum Refineries	Yes
Ja	Petroleum Refineries (After May 14, 2007)	Yes
K	Storage Vessels for Petroleum Liquids (After 6/11/73 & Before 5/19/78)	Yes
Ka	Storage Vessels for Petroleum Liquids (After 6/11/73 & Before 5/19/78)	Yes
Kb	Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Stg/Vessels) After 7/23/84	Yes
L	Secondary Lead Smelters Yes	Yes
М	Secondary Brass and Bronze Production Plants	Yes
N	Primary Emissions from Basic Oxygen Process Furnaces (Construction Commenced After June 11, 1973)	Yes
Na	Secondary Emissions from Basic Oxygen Process Steelmaking Facilities Construction is Commenced After January 20, 1983	Yes
0	Sewage Treatment Plants	Yes
Р	Primary Copper Smelters	Yes
Q	Primary Zinc Smelters	Yes
R	Primary Lead Smelters	Yes
S	Primary Aluminum Reduction Plants	Yes
Т	Phosphate Fertilizer Industry: Wet Process Phosphoric Plants	Yes
U	Phosphate Fertilizer Industry: Superphosphoric Acid Plants	Yes
V	Phosphate Fertilizer Industry: Diammonium Phosphate Plants	Yes
W	Phosphate Fertilizer Industry: Triple Superphosphate Plants	Yes

Delegation Status for Part 60 Standards—State of Louisiana [Excluding Indian Country]		
Subpart	Source category	LDEQ <sup>1</sup>
X	Phosphate Fertilizer Industry: Granular Triple Superphosphate Storage Facilities	Yes
Y	Coal Preparation Plants	Yes
Z	Ferroalloy Production Facilities	Yes
AA	Steel Plants: Electric Arc Furnaces After 10/21/74 & On or Before 8/17/83	Yes
AAa	Steel Plants: Electric Arc Furnaces & Argon-Oxygen Decarburization Vessels After 8/07/83	Yes
BB	Kraft Pulp Mills	Yes
CC	Glass Manufacturing Plants	Yes
DD	Grain Elevators	Yes
EE	Surface Coating of Metal Furniture	Yes
GG	Stationary Gas Turbines	Yes
HH	Lime Manufacturing Plants	Yes
KK	Lead-Acid Battery Manufacturing Plants	Yes
LL	Metallic Mineral Processing Plants	Yes
MM	Automobile & Light Duty Truck Surface Coating Operations	Yes
NN	Phosphate Manufacturing Plants	Yes
PP	Ammonium Sulfate Manufacture	Yes
QQ	Graphic Arts Industry: Publication Rotogravure Printing	Yes
RR	Pressure Sensitive Tape and Label Surface Coating Operations	Yes
SS	Industrial Surface Coating: Large Appliances	Yes
TT	Metal Coil Surface Coating	Yes
UU	Asphalt Processing and Asphalt Roofing Manufacture	Yes
VV	VOC Equipment Leaks in the SOCMI Industry	Yes
VVa	VOC Equipment Leaks in the SOCMI Industry (After November 7, 2006)	Yes
XX	Bulk Gasoline Terminals	Yes
AAA	New Residential Wood Heaters	No
BBB	Rubber Tire Manufacturing Industry	Yes
DDD	Volatile Organic Compound (VOC) Emissions from the Polymer Manufacturing Industry	Yes
FFF	Flexible Vinyl and Urethane Coating and Printing	Yes
GGG	VOC Equipment Leaks in Petroleum Refineries	Yes
HHH	Synthetic Fiber Production	Yes
III	VOC Emissions from the SOCMI Air Oxidation Unit Processes	Yes
JJJ	Petroleum Dry Cleaners	Yes
KKK	VOC Equipment Leaks From Onshore Natural Gas Processing Plants	Yes
LLL	Onshore Natural Gas Processing: SO <sub>2</sub> Emissions	Yes
NNN	VOC Emissions from SOCMI Distillation Operations	Yes
000	Nonmetallic Mineral Processing Plants	Yes
PPP	Wool Fiberglass Insulation Manufacturing Plants	Yes
QQQ	VOC Emissions From Petroleum Refinery Wastewater Systems	Yes
RRR	VOC Emissions from SOCMI Reactor Processes	Yes

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Delegation Status for Part 60 Standards—State of Louisiana	
[Excluding Indian Country]	

Subpart	Source category	LDEQ <sup>1</sup>
SSS	Magnetic Tape Coating Operations	Yes
TTT	Industrial Surface Coating: Plastic Parts for Business Machines	Yes
UUU	Calciners and Dryers in Mineral Industries	Yes
VVV	Polymeric Coating of Supporting Substrates Facilities	Yes
WWW	Municipal Solid Waste Landfills	Yes
AAAA	Small Municipal Waste Combustion Units (Construction is Commenced After 8/30/99 or Modification/Reconstruction is Commenced After 6/06/2001)	Yes
CCCC	Commercial & Industrial Solid Waste Incineration Units (Construction is Commenced After 11/30/1999 or Modification/Reconstruction is Commenced on or After 6/01/2001)	Yes
DDDD	Emission Guidelines & Compliance Times for Commercial & Industrial Solid Waste Incineration Units (Commenced Construction On or Before 11/30/1999)	Yes
EEEE	Other Solid Waste Incineration Units (Constructed after 12/09/2004 or Modification/Reconstruction is commenced on or after 06/16/2004)	Yes
IIII	Stationary Compression Ignition Internal Combustion Engines	Yes
JJJJ	Stationary Spark Ignition Internal Combustion Engines	Yes
КККК	Stationary Combustion Turbines (Construction Commenced After 02/18/2005)	Yes
LLLL	New Sewage Sludge Incineration Units	Yes
MMMM	Emission Guidelines and Compliance Times for Existing Sewage Sludge Incineration Units	Yes
0000	Crude Oil and Natural Gas Production, Transmission and Distribution	Yes
<sup>1</sup> The Louisiana Department of Environmental Quality (LDEQ) has been delegated all Part 60 standards promulgated by EPA, except subpart AAA—Standards of Performance for New Residential Wood Heaters—as amended in the Federal Register through July 1, 2013.		

(3) *Albuquerque-Bernalillo County Air Quality Control Board*. The Albuquerque-Bernalillo County Air Quality Control Board has been delegated all part 60 standards promulgated by the EPA, except <u>subpart AAA of this part</u> and <u>subpart QQQQ</u> of this part as amended through January 23, 2017.

[<u>40 FR 18169</u>, Apr. 25, 1975]

#### **Editorial Note**

## **Editorial Note:**

For Federal Register citations affecting  $\S$  60.4, see the List of CFR Sections Affected, which appears in the Finding Aids section of the printed volume and at <u>www.govinfo.gov</u>.

#### § 60.5 Determination of construction or modification.

(a) When requested to do so by an owner or operator, the Administrator will make a determination of whether action taken or intended to be taken by such owner or operator constitutes construction (including reconstruction) or modification or the commencement thereof within the meaning of this part.

(b) The Administrator will respond to any request for a determination under <u>paragraph (a)</u> of this section within 30 days of receipt of such request.

[<u>40 FR 58418</u>, Dec. 16, 1975]

#### § 60.6 Review of plans.

(a) When requested to do so by an owner or operator, the Administrator will review plans for construction or modification for the purpose of providing technical advice to the owner or operator.
## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(b)

(1) A separate request shall be submitted for each construction or modification project.

(2) Each request shall identify the location of such project, and be accompanied by technical information describing the proposed nature, size, design, and method of operation of each affected facility involved in such project, including information on any equipment to be used for measurement or control of emissions.

(c) Neither a request for plans review nor advice furnished by the Administrator in response to such request shall

(1) relieve an owner or operator of legal responsibility for compliance with any provision of this part or of any applicable State or local requirement, or

(2) prevent the Administrator from implementing or enforcing any provision of this part or taking any other action authorized by the Act.

[<u>36 FR 24877</u>, Dec. 23, 1971, as amended at <u>39 FR 9314</u>, Mar. 8, 1974]

## § 60.7 Notification and record keeping.

(a) Any owner or operator subject to the provisions of this part shall furnish the Administrator written notification or, if acceptable to both the Administrator and the owner or operator of a source, electronic notification, as follows:

(1) A notification of the date construction (or reconstruction as defined under  $\frac{60.15}{100}$ ) of an affected facility is commenced postmarked no later than 30 days after such date. This requirement shall not apply in the case of mass-produced facilities which are purchased in completed form.

(2) [Reserved]

(3) A notification of the actual date of initial startup of an affected facility postmarked within 15 days after such date.

(4) A notification of any physical or operational change to an existing facility which may increase the emission rate of any air pollutant to which a standard applies, unless that change is specifically exempted under an applicable subpart or in  $\S$  <u>60.14(e)</u>. This notice shall be postmarked 60 days or as soon as practicable before the change is commenced and shall include information describing the precise nature of the change, present and proposed emission control systems, productive capacity of the facility before and after the change, and the expected completion date of the change. The Administrator may request additional relevant information subsequent to this notice.

(5) A notification of the date upon which demonstration of the continuous monitoring system performance commences in accordance with  $\frac{60.13(c)}{1.000}$ . Notification shall be postmarked not less than 30 days prior to such date.

(6) A notification of the anticipated date for conducting the opacity observations required by  $\S$  60.11(e)(1) of this part. The notification shall also include, if appropriate, a request for the Administrator to provide a visible emissions reader during a performance test. The notification shall be postmarked not less than 30 days prior to such date.

(7) A notification that continuous opacity monitoring system data results will be used to determine compliance with the applicable opacity standard during a performance test required by  $\S$  60.8 in lieu of Method 9 observation data as allowed by  $\S$  60.11(e)(5) of this part. This notification shall be postmarked not less than 30 days prior to the date of the performance test.

(b) Any owner or operator subject to the provisions of this part shall maintain records of the occurrence and duration of any startup, shutdown, or malfunction in the operation of an affected facility; any malfunction of the air pollution control equipment; or any periods during which a continuous monitoring system or monitoring device is inoperative.

(c) Each owner or operator required to install a continuous monitoring device shall submit excess emissions and monitoring systems performance report (excess emissions are defined in applicable subparts) and-or summary report form (see <u>paragraph</u> (d) of this section) to the Administrator semiannually, except when: more frequent reporting is specifically required by an applicable subpart; or the Administrator, on a case-by-case basis, determines that more frequent reporting is necessary to accurately assess the compliance status of the source. All reports shall be postmarked by the 30th day following the end of each six-month period. Written reports of excess emissions shall include the following information:

(1) The magnitude of excess emissions computed in accordance with  $\S$  60.13(h), any conversion factor(s) used, and the date and time of commencement and completion of each time period of excess emissions. The process operating time during the reporting period.

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(2) Specific identification of each period of excess emissions that occurs during startups, shutdowns, and malfunctions of the affected facility. The nature and cause of any malfunction (if known), the corrective action taken or preventative measures adopted.

(3) The date and time identifying each period during which the continuous monitoring system was inoperative except for zero and span checks and the nature of the system repairs or adjustments.

(4) When no excess emissions have occurred or the continuous monitoring system(s) have not been inoperative, repaired, or adjusted, such information shall be stated in the report.

(d) The summary report form shall contain the information and be in the format shown in figure 1 unless otherwise specified by the Administrator. One summary report form shall be submitted for each pollutant monitored at each affected facility.

(1) If the total duration of excess emissions for the reporting period is less than 1 percent of the total operating time for the reporting period and CMS downtime for the reporting period is less than 5 percent of the total operating time for the reporting period, only the summary report form shall be submitted and the excess emission report described in § 60.7(c) need not be submitted unless requested by the Administrator.

(2) If the total duration of excess emissions for the reporting period is 1 percent or greater of the total operating time for the reporting period or the total CMS downtime for the reporting period is 5 percent or greater of the total operating time for the reporting period, the summary report form and the excess emission report described in § 60.7(c) shall both be submitted.

Figure 1-Summary Report-Gaseous and Opacity Excess Emission and Monitoring System Performance

Pollutant (Circle One—SO<sub>2</sub>/NO<sub>X</sub>/TRS/H<sub>2</sub>S/CO/Opacity)

Reporting period dates: From to

Company:

**Emission Limitation** 

Address:

Monitor Manufacturer and Model No.

Date of Latest CMS Certification or Audit

Process Unit(s) Description:

Total source operating time in reporting period<sup>1</sup>

Emission data summary <sup>1</sup>		CMS performance summary <sup>1</sup>		
1. Duration of excess emissions in reporting period due to:		1. CMS downtime in reporting period due to:		
a. Startup/shutdown		a. Monitor equipment malfunctions		
b. Control equipment problems		b. Non-Monitor equipment malfunctions		
c. Process problems		c. Quality assurance calibration		
d. Other known causes		d. Other known causes		
e. Unknown causes		e. Unknown causes		
2. Total duration of excess emission		2. Total CMS Downtime		
3. Total duration of excess emissions × (100) [Total source operating time]	% <sup>2</sup>	3. [Total CMS Downtime] × (100) [Total source operating time]	9⁄0 <sup>2</sup>	
<sup>1</sup> For opacity, record all times in minutes. For gases, record all times in hours.				

 $^{2}$  For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in  $\S$  60.7(c) shall be submitted.

On a separate page, describe any changes since last quarter in CMS, process or controls. I certify that the information contained in this report is true, accurate, and complete.

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Name

Signature

Title

Date

(e)

(1) Notwithstanding the frequency of reporting requirements specified in <u>paragraph (c)</u> of this section, an owner or operator who is required by an applicable subpart to submit excess emissions and monitoring systems performance reports (and summary reports) on a quarterly (or more frequent) basis may reduce the frequency of reporting for that standard to semiannual if the following conditions are met:

(i) For 1 full year (e.g., 4 quarterly or 12 monthly reporting periods) the affected facility's excess emissions and monitoring systems reports submitted to comply with a standard under this part continually demonstrate that the facility is in compliance with the applicable standard;

(ii) The owner or operator continues to comply with all recordkeeping and monitoring requirements specified in this subpart and the applicable standard; and

(iii) The Administrator does not object to a reduced frequency of reporting for the affected facility, as provided in <u>paragraph</u> ( $\underline{e}$ )(2) of this section.

(2) The frequency of reporting of excess emissions and monitoring systems performance (and summary) reports may be reduced only after the owner or operator notifies the Administrator in writing of his or her intention to make such a change and the Administrator does not object to the intended change. In deciding whether to approve a reduced frequency of reporting, the Administrator may review information concerning the source's entire previous performance history during the required recordkeeping period prior to the intended change, including performance test results, monitoring data, and evaluations of an owner or operator's conformance with operation and maintenance requirements. Such information may be used by the Administrator to make a judgment about the source's potential for noncompliance in the future. If the Administrator disapproves the owner or operator's request to reduce the frequency of reporting, the Administrator will notify the owner or operator in writing within 45 days after receiving notice of the owner or operator's intention. The notification from the Administrator to the owner or operator will specify the grounds on which the disapproval is based. In the absence of a notice of disapproval within 45 days, approval is automatically granted.

(3) As soon as monitoring data indicate that the affected facility is not in compliance with any emission limitation or operating parameter specified in the applicable standard, the frequency of reporting shall revert to the frequency specified in the applicable standard, and the owner or operator shall submit an excess emissions and monitoring systems performance report (and summary report, if required) at the next appropriate reporting period following the noncomplying event. After demonstrating compliance with the applicable standard for another full year, the owner or operator may again request approval from the Administrator to reduce the frequency of reporting for that standard as provided for in paragraphs (e)(1) and (e)(2) of this section.

(f) Any owner or operator subject to the provisions of this part shall maintain a file of all measurements, including continuous monitoring system, monitoring device, and performance testing measurements; all continuous monitoring system performance evaluations; all continuous monitoring system or monitoring device calibration checks; adjustments and maintenance performed on these systems or devices; and all other information required by this part recorded in a permanent form suitable for inspection. The file shall be retained for at least two years following the date of such measurements, maintenance, reports, and records, except as follows:

(1) This paragraph applies to owners or operators required to install a continuous emissions monitoring system (CEMS) where the CEMS installed is automated, and where the calculated data averages do not exclude periods of CEMS breakdown or malfunction. An automated CEMS records and reduces the measured data to the form of the pollutant emission standard through the use of a computerized data acquisition system. In lieu of maintaining a file of all CEMS subhourly measurements as required under <u>paragraph (f)</u> of this section, the owner or operator shall retain the most recent consecutive three averaging periods of subhourly measurements and a file that contains a hard copy of the data acquisition system algorithm used to reduce the measured data into the reportable form of the standard.

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(2) This paragraph applies to owners or operators required to install a CEMS where the measured data is manually reduced to obtain the reportable form of the standard, and where the calculated data averages do not exclude periods of CEMS breakdown or malfunction. In lieu of maintaining a file of all CEMS subhourly measurements as required under paragraph (f) of this section, the owner or operator shall retain all subhourly measurements for the most recent reporting period. The subhourly measurements shall be retained for 120 days from the date of the most recent summary or excess emission report submitted to the Administrator.

(3) The Administrator or delegated authority, upon notification to the source, may require the owner or operator to maintain all measurements as required by <u>paragraph (f)</u> of this section, if the Administrator or the delegated authority determines these records are required to more accurately assess the compliance status of the affected source.

(g) If notification substantially similar to that in <u>paragraph (a)</u> of this section is required by any other State or local agency, sending the Administrator a copy of that notification will satisfy the requirements of <u>paragraph (a)</u> of this section.

(h) Individual <u>subparts of this part</u> may include specific provisions which clarify or make inapplicable the provisions set forth in this section.

[<u>36 FR 24877</u>, Dec. 28, 1971, as amended at <u>40 FR 46254</u>, Oct. 6, 1975; <u>40 FR 58418</u>, Dec. 16, 1975; <u>45 FR 5617</u>, Jan. 23, 1980; <u>48 FR 48335</u>, Oct. 18, 1983; <u>50 FR 53113</u>, Dec. 27, 1985; <u>52 FR 9781</u>, Mar. 26, 1987; <u>55 FR 51382</u>, Dec. 13, 1990; <u>59 FR 12428</u>, Mar. 16, 1994; <u>59 FR 47265</u>, Sep. 15, 1994; <u>64 FR 7463</u>, Feb. 12, 1999]

## § 60.8 Performance tests.

(a) Except as specified in paragraphs (a)(1),(a)(2), (a)(3), and (a)(4) of this section, within 60 days after achieving the maximum production rate at which the affected facility will be operated, but not later than 180 days after initial startup of such facility, or at such other times specified by this part, and at such other times as may be required by the Administrator under section 114 of the Act, the owner or operator of such facility shall conduct performance test(s) and furnish the Administrator a written report of the results of such performance test(s).

(1) If a force majeure is about to occur, occurs, or has occurred for which the affected owner or operator intends to assert a claim of force majeure, the owner or operator shall notify the Administrator, in writing as soon as practicable following the date the owner or operator first knew, or through due diligence should have known that the event may cause or caused a delay in testing beyond the regulatory deadline, but the notification must occur before the performance test deadline unless the initial force majeure or a subsequent force majeure event delays the notice, and in such cases, the notification shall occur as soon as practicable.

(2) The owner or operator shall provide to the Administrator a written description of the force majeure event and a rationale for attributing the delay in testing beyond the regulatory deadline to the force majeure; describe the measures taken or to be taken to minimize the delay; and identify a date by which the owner or operator proposes to conduct the performance test. The performance test shall be conducted as soon as practicable after the force majeure occurs.

(3) The decision as to whether or not to grant an extension to the performance test deadline is solely within the discretion of the Administrator. The Administrator will notify the owner or operator in writing of approval or disapproval of the request for an extension as soon as practicable.

(4) Until an extension of the performance test deadline has been approved by the Administrator under <u>paragraphs (a)(1), (2)</u>, and (3) of this section, the owner or operator of the affected facility remains strictly subject to the requirements of this part.

(b) Performance tests shall be conducted and data reduced in accordance with the test methods and procedures contained in each applicable subpart unless the Administrator

(1) specifies or approves, in specific cases, the use of a reference method with minor changes in methodology,

(2) approves the use of an equivalent method,

(3) approves the use of an alternative method the results of which he has determined to be adequate for indicating whether a specific source is in compliance,

(4) waives the requirement for performance tests because the owner or operator of a source has demonstrated by other means to the Administrator's satisfaction that the affected facility is in compliance with the standard, or

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(5) approves shorter sampling times and smaller sample volumes when necessitated by process variables or other factors. Nothing in this paragraph shall be construed to abrogate the Administrator's authority to require testing under section 114 of the Act.

(c) Performance tests shall be conducted under such conditions as the Administrator shall specify to the plant operator based on representative performance of the affected facility. The owner or operator shall make available to the Administrator such records as may be necessary to determine the conditions of the performance tests. Operations during periods of startup, shutdown, and malfunction shall not constitute representative conditions for the purpose of a performance test nor shall emissions in excess of the level of the applicable emission limit during periods of startup, shutdown, and malfunction be considered a violation of the applicable emission limit unless otherwise specified in the applicable standard.

(d) The owner or operator of an affected facility shall provide the Administrator at least 30 days prior notice of any performance test, except as specified under other subparts, to afford the Administrator the opportunity to have an observer present. If after 30 days notice for an initially scheduled performance test, there is a delay (due to operational problems, etc.) in conducting the scheduled performance test, the owner or operator of an affected facility shall notify the Administrator (or delegated State or local agency) as soon as possible of any delay in the original test date, either by providing at least 7 days prior notice of the rescheduled date of the performance test, or by arranging a rescheduled date with the Administrator (or delegated State or local agency) by mutual agreement.

(e) The owner or operator of an affected facility shall provide, or cause to be provided, performance testing facilities as follows:

(1) Sampling ports adequate for test methods applicable to such facility. This includes

(i) constructing the air pollution control system such that volumetric flow rates and pollutant emission rates can be accurately determined by applicable test methods and procedures and

(ii) providing a stack or duct free of cyclonic flow during performance tests, as demonstrated by applicable test methods and procedures.

(2) Safe sampling platform(s).

(3) Safe access to sampling platform(s).

(4) Utilities for sampling and testing equipment.

(f) Unless otherwise specified in the applicable subpart, each performance test shall consist of three separate runs using the applicable test method.

(1) Each run shall be conducted for the time and under the conditions specified in the applicable standard. For the purpose of determining compliance with an applicable standard, the arithmetic means of results of the three runs shall apply. In the event that a sample is accidentally lost or conditions occur in which one of the three runs must be discontinued because of forced shutdown, failure of an irreplaceable portion of the sample train, extreme meteorological conditions, or other circumstances, beyond the owner or operator's control, compliance may, upon the Administrator's approval, be determined using the arithmetic mean of the results of the two other runs.

(2) Contents of report (electronic or paper submitted copy). Unless otherwise specified in a relevant standard or test method, or as otherwise approved by the Administrator in writing, the report for a performance test shall include the elements identified in paragraphs ( $f_{2}(2)(i)$ ) through (vi) of this section.

(i) General identification information for the facility including a mailing address, the physical address, the owner or operator or responsible official (where applicable) and his/her email address, and the appropriate Federal Registry System (FRS) number for the facility.

(ii) Purpose of the test including the applicable regulation(s) requiring the test, the pollutant(s) and other parameters being measured, the applicable emission standard and any process parameter component, and a brief process description.

(iii) Description of the emission unit tested including fuel burned, control devices, and vent characteristics; the appropriate source classification code (SCC); the permitted maximum process rate (where applicable); and the sampling location.

(iv) Description of sampling and analysis procedures used and any modifications to standard procedures, quality assurance procedures and results, record of process operating conditions that demonstrate the applicable test conditions are met, and values for any operating parameters for which limits were being set during the test.

(v) Where a test method requires you record or report, the following shall be included: Record of preparation of standards, record of calibrations, raw data sheets for field sampling, raw data sheets for field and laboratory analyses, chain-of-custody documentation, and example calculations for reported results.

(vi) Identification of the company conducting the performance test including the primary office address, telephone number, and the contact for this test program including his/her email address.

(g) The performance testing shall include a test method performance audit (PA) during the performance test. The PAs consist of blind audit samples supplied by an accredited audit sample provider and analyzed during the performance test in order to provide a measure of test data bias. Gaseous audit samples are designed to audit the performance of the sampling system as well as the analytical system and must be collected by the sampling system during the compliance test just as the compliance samples are collected. If a liquid or solid audit sample is designed to audit the sampling system, it must also be collected by the sampling system during the compliance test. If multiple sampling systems or sampling trains are used during the compliance test for any of the test methods, the tester is only required to use one of the sampling systems per method to collect the audit sample. The audit sample must be analyzed by the same analyst using the same analytical reagents and analytical system and at the same time as the compliance samples. Retests are required when there is a failure to produce acceptable results for an audit sample. However, if the audit results do not affect the compliance or noncompliance status of the affected facility, the compliance authority may waive the reanalysis requirement, further audits, or retests and accept the results of the compliance test. Acceptance of the test results shall constitute a waiver of the reanalysis requirement, further audits, or retests. The compliance authority may also use the audit sample failure and the compliance test results as evidence to determine the compliance or noncompliance status of the affected facility. A blind audit sample is a sample whose value is known only to the sample provider and is not revealed to the tested facility until after they report the measured value of the audit sample. For pollutants that exist in the gas phase at ambient temperature, the audit sample shall consist of an appropriate concentration of the pollutant in air or nitrogen that can be introduced into the sampling system of the test method at or near the same entry point as a sample from the emission source. If no gas phase audit samples are available, an acceptable alternative is a sample of the pollutant in the same matrix that would be produced when the sample is recovered from the sampling system as required by the test method. For samples that exist only in a liquid or solid form at ambient temperature, the audit sample shall consist of an appropriate concentration of the pollutant in the same matrix that would be produced when the sample is recovered from the sampling system as required by the test method. An accredited audit sample provider (AASP) is an organization that has been accredited to prepare audit samples by an independent, third party accrediting body.

(1) The source owner, operator, or representative of the tested facility shall obtain an audit sample, if commercially available, from an AASP for each test method used for regulatory compliance purposes. No audit samples are required for the following test methods: Methods 3A and 3C of appendix A-3 of part 60, Methods 6C, 7E, 9, and 10 of appendix A-4 of part 60, Methods 18 and 19 of appendix A-6 of part 60, Methods 20, 22, and 25A of appendix A-7 of part 60, Methods 30A and 30B of appendix A-8 of part 60, and Methods 303, 318, 320, and 321 of appendix A of part 63 of this chapter. If multiple sources at a single facility are tested during a compliance test event, only one audit sample is required for each method used during a compliance test. The compliance authority responsible for the compliance test may waive the requirement to include an audit sample if they believe that an audit sample is not necessary. "Commercially available" means that two or more independent AASPs have blind audit samples available for purchase. If the source owner, operator, or representative cannot find an audit sample for a specific method, the owner, operator, or representative shall consult the EPA Web site at the following URL, www.epa.gov/ttn/emc, to confirm whether there is a source that can supply an audit sample for that method. If the EPA Web site does not list an available audit sample at least 60 days prior to the beginning of the compliance test, the source owner, operator, or representative shall not be required to include an audit sample as part of the quality assurance program for the compliance test. When ordering an audit sample, the source owner, operator, or representative shall give the sample provider an estimate for the concentration of each pollutant that is emitted by the source or the estimated concentration of each pollutant based on the permitted level and the name, address, and phone number of the compliance authority. The source owner, operator, or representative shall report the results for the audit sample along with a summary of the emission test results for the audited pollutant to the compliance authority and shall report the results of the audit sample to the AASP. The source owner, operator, or representative shall make both reports at the same time and in the same manner or shall report to the compliance authority first and then report to the AASP. If the method being audited is a method that allows the samples to be analyzed in the field and the tester plans to analyze the samples in the field, the tester may analyze the audit samples prior to collecting the emission samples provided a representative of the compliance authority is present at the testing site. The tester may request and the compliance authority may grant a waiver to the requirement that a representative of the compliance authority must be present at the testing site during the field analysis of an audit sample. The source owner, operator, or representative may report the results of the audit sample to the compliance authority and report the results of the

audit sample to the AASP prior to collecting any emission samples. The test protocol and final test report shall document whether an audit sample was ordered and utilized and the pass/fail results as applicable.

(2) An AASP shall have and shall prepare, analyze, and report the true value of audit samples in accordance with a written technical criteria document that describes how audit samples will be prepared and distributed in a manner that will ensure the integrity of the audit sample program. An acceptable technical criteria document shall contain standard operating procedures for all of the following operations:

(i) Preparing the sample;

(ii) Confirming the true concentration of the sample;

(iii) Defining the acceptance limits for the results from a well qualified tester. This procedure must use well established statistical methods to analyze historical results from well qualified testers. The acceptance limits shall be set so that there is 95 percent confidence that 90 percent of well qualified labs will produce future results that are within the acceptance limit range.

(iv) Providing the opportunity for the compliance authority to comment on the selected concentration level for an audit sample;

(v) Distributing the sample to the user in a manner that guarantees that the true value of the sample is unknown to the user;

(vi) Recording the measured concentration reported by the user and determining if the measured value is within acceptable limits;

(vii) The AASP shall report the results from each audit sample in a timely manner to the compliance authority and then to the source owner, operator, or representative. The AASP shall make both reports at the same time and in the same manner or shall report to the compliance authority first and then report to the source owner, operator, or representative. The results shall include the name of the facility tested, the date on which the compliance test was conducted, the name of the company performing the sample collection, the name of the company that analyzed the compliance samples including the audit sample, the measured result for the audit sample, and whether the testing company passed or failed the audit. The AASP shall report the true value of the audit sample to the compliance authority. The AASP may report the true value to the source owner, operator, or representative if the AASP's operating plan ensures that no laboratory will receive the same audit sample twice.

(viii) Evaluating the acceptance limits of samples at least once every two years to determine in cooperation with the voluntary consensus standard body if they should be changed;

(ix) Maintaining a database, accessible to the compliance authorities, of results from the audit that shall include the name of the facility tested, the date on which the compliance test was conducted, the name of the company performing the sample collection, the name of the company that analyzed the compliance samples including the audit sample, the measured result for the audit sample, the true value of the audit sample, the acceptance range for the measured value, and whether the testing company passed or failed the audit.

(3) The accrediting body shall have a written technical criteria document that describes how it will ensure that the AASP is operating in accordance with the AASP technical criteria document that describes how audit samples are to be prepared and distributed. This document shall contain standard operating procedures for all of the following operations:

(i) Checking audit samples to confirm their true value as reported by the AASP;

(ii) Performing technical systems audits of the AASP's facilities and operating procedures at least once every two years;

(iii) Providing standards for use by the voluntary consensus standard body to approve the accrediting body that will accredit the audit sample providers.

(4) The technical criteria documents for the accredited sample providers and the accrediting body shall be developed through a public process guided by a voluntary consensus standards body (VCSB). The VCSB shall operate in accordance with the procedures and requirements in the Office of Management and Budget Circular A-119. A copy of Circular A-119 is available upon request by writing the Office of Information and Regulatory Affairs, Office of Management and Budget, 725 17th Street, NW., Washington, DC 20503, by calling (202) 395-6880 or downloading online

at <u>http://standards.gov/standards\_gov/a119.cfm</u>. The VCSB shall approve all accrediting bodies. The Administrator will review all technical criteria documents. If the technical criteria documents do not meet the minimum technical requirements in <u>paragraphs (g)(2)</u> through (4) of this section, the technical criteria documents are not acceptable and the proposed audit

sample program is not capable of producing audit samples of sufficient quality to be used in a compliance test. All acceptable technical criteria documents shall be posted on the EPA Web site at the following URL, <u>http://www.epa.gov/ttn/emc</u>.

(h) Unless otherwise specified in the applicable subpart, each test location must be verified to be free of cyclonic flow and evaluated for the existence of emission gas stratification and the required number of sampling traverse points. If other procedures are not specified in the applicable subpart to the regulations, use the appropriate procedures in Method 1 to check for cyclonic flow and Method 7E to evaluate emission gas stratification and selection of sampling points.

(i) Whenever the use of multiple calibration gases is required by a test method, performance specification, or quality assurance procedure in a part 60 standard or appendix, Method 205 of <u>40 CFR part 51, appendix M</u> of this chapter, "Verification of Gas Dilution Systems for Field Instrument Calibrations," may be used.

[<u>36 FR 24877</u>, Dec. 23, 1971, as amended at <u>39 FR 9314</u>, Mar. 8, 1974; <u>42 FR 57126</u>, Nov. 1, 1977; <u>44 FR 33612</u>, June 11, 1979; <u>54 FR 6662</u>, Feb. 14, 1989; <u>54 FR 21344</u>, May 17, 1989; <u>64 FR 7463</u>, Feb. 12, 1999; <u>72 FR 27442</u>, May 16, 2007; <u>75 FR 55646</u>, Sept. 13, 2010; <u>79 FR 11241</u>, Feb. 27, 2014; <u>81 FR 59809</u>, Aug. 30, 2016]

## § 60.9 Availability of information.

The availability to the public of information provided to, or otherwise obtained by, the Administrator under this part shall be governed by <u>part 2 of this chapter</u>. (Information submitted voluntarily to the Administrator for the purposes of <u>§§</u> <u>60.5</u> and <u>60.6</u> is governed by <u>§§ 2.201</u> through <u>2.213 of this chapter</u> and not by <u>§ 2.301 of this chapter</u>.)

## § 60.10 State authority.

The provisions of this part shall not be construed in any manner to preclude any State or political subdivision thereof from:

(a) Adopting and enforcing any emission standard or limitation applicable to an affected facility, provided that such emission standard or limitation is not less stringent than the standard applicable to such facility.

(b) Requiring the owner or operator of an affected facility to obtain permits, licenses, or approvals prior to initiating construction, modification, or operation of such facility.

## § 60.11 Compliance with standards and maintenance requirements.

(a) Compliance with standards in this part, other than opacity standards, shall be determined in accordance with performance tests established by  $\S 60.8$ , unless otherwise specified in the applicable standard.

(b) Compliance with opacity standards in this part shall be determined by conducting observations in accordance with Method 9 in <u>appendix A of this part</u>, any alternative method that is approved by the Administrator, or as provided in <u>paragraph (e)(5)</u> of this section. For purposes of determining initial compliance, the minimum total time of observations shall be 3 hours (30 6-minute averages) for the performance test or other set of observations (meaning those fugitive-type emission sources subject only to an opacity standard).

(c) The opacity standards set forth in this part shall apply at all times except during periods of startup, shutdown, malfunction, and as otherwise provided in the applicable standard.

(d) At all times, including periods of startup, shutdown, and malfunction, owners and operators shall, to the extent practicable, maintain and operate any affected facility including associated air pollution control equipment in a manner consistent with good air pollution control practice for minimizing emissions. Determination of whether acceptable operating and maintenance procedures are being used will be based on information available to the Administrator which may include, but is not limited to, monitoring results, opacity observations, review of operating and maintenance procedures, and inspection of the source.

(e)

(1) For the purpose of demonstrating initial compliance, opacity observations shall be conducted concurrently with the initial performance test required in  $\S$  60.8 unless one of the following conditions apply. If no performance test under  $\S$  60.8 is required, then opacity observations shall be conducted within 60 days after achieving the maximum production rate at which the affected facility will be operated but no later than 180 days after initial startup of the facility. If visibility or other conditions prevent the opacity observations from being conducted concurrently with the initial performance test required under  $\S$  60.8, the source owner or operator shall reschedule the opacity observations as soon after the initial performance test as possible, but not later than 30 days thereafter, and shall advise the Administrator of the rescheduled date. In these cases, the 30-day prior notification to the Administrator required in  $\S$  60.7(a)(6) shall be waived. The rescheduled opacity

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observations shall be conducted (to the extent possible) under the same operating conditions that existed during the initial performance test conducted under § 60.8. The visible emissions observer shall determine whether visibility or other conditions prevent the opacity observations from being made concurrently with the initial performance test in accordance with procedures contained in Method 9 of <u>appendix B of this part</u>. Opacity readings of portions of plumes which contain condensed, uncombined water vapor shall not be used for purposes of determing compliance with opacity standards. The owner or operator of an affected facility shall make available, upon request by the Administrator, such records as may be necessary to determine the conditions under which the visual observations were made and shall provide evidence indicating proof of current visible observer emission certification. Except as provided in <u>paragraph (e)(5)</u> of this section, the results of continuous monitoring by transmissometer which indicate that the opacity at the time visual observations were made was not in excess of the standard are probative but not conclusive evidence of the actual opacity of an emission, provided that the source shall meet the burden of proving that the instrument used meets (at the time of the alleged violation) Performance Specification 1 in <u>appendix B of this part</u>, has been properly maintained and (at the time of the alleged violation) that the resulting data have not been altered in any way.

(2) Except as provided in <u>paragraph (e)(3)</u> of this section, the owner or operator of an affected facility to which an opacity standard in this part applies shall conduct opacity observations in accordance with <u>paragraph (b)</u> of this section, shall record the opacity of emissions, and shall report to the Administrator the opacity results along with the results of the initial performance test required under  $\frac{60.8}{1000}$ . The inability of an owner or operator to secure a visible emissions observer shall not be considered a reason for not conducting the opacity observations concurrent with the initial performance test.

(3) The owner or operator of an affected facility to which an opacity standard in this part applies may request the Administrator to determine and to record the opacity of emissions from the affected facility during the initial performance test and at such times as may be required. The owner or operator of the affected facility shall report the opacity results. Any request to the Administrator to determine and to record the opacity of emissions from an affected facility shall be included in the notification required in  $\frac{60.7(a)(6)}{10}$ . If, for some reason, the Administrator cannot determine and record the opacity of emissions from the affected facility during the performance test, then the provisions of <u>paragraph (e)(1)</u> of this section shall apply.

(4) An owner or operator of an affected facility using a continuous opacity monitor (transmissometer) shall record the monitoring data produced during the initial performance test required by  $\S 60.8$  and shall furnish the Administrator a written report of the monitoring results along with Method 9 and  $\S 60.8$  performance test results.

(5) An owner or operator of an affected facility subject to an opacity standard may submit, for compliance purposes, continuous opacity monitoring system (COMS) data results produced during any performance test required under  $\frac{60.8}{60.8}$  in lieu of Method 9 observation data. If an owner or operator elects to submit COMS data for compliance with the opacity standard, he shall notify the Administrator of that decision, in writing, at least 30 days before any performance test required under  $\frac{60.8}{60.8}$  is conducted. Once the owner or operator of an affected facility has notified the Administrator to that effect, the COMS data results will be used to determine opacity compliance during subsequent tests required under  $\frac{60.8}{60.8}$  until the owner or operator notifies the Administrator, in writing, to the contrary. For the purpose of determining compliance with the opacity standard during a performance test required under  $\frac{60.8}{60.8}$  using COMS data, the minimum total time of COMS data collection shall be averages of all 6-minute continuous periods within the duration of the mass emission performance test. Results of the COMS opacity determinations shall be submitted along with the results of the performance test required under  $\frac{60.8}{60.8}$ . The owner or operator of an affected facility using a COMS for compliance purposes is responsible for demonstrating that the COMS meets the requirements specified in  $\frac{60.13(c)}{60.8}$  of this part, that the COMS has been properly maintained and operated, and that the resulting data have not been altered in any way. If COMS data results are submitted for compliance with the opacity standard for a period of time during which Method 9 data indicates noncompliance, the Method 9 data will be used to determine compliance with the opacity standard.

(6) Upon receipt from an owner or operator of the written reports of the results of the performance tests required by  $\S$  60.8, the opacity observation results and observer certification required by  $\S$  60.11(e)(1), and the COMS results, if applicable, the Administrator will make a finding concerning compliance with opacity and other applicable standards. If COMS data results are used to comply with an opacity standard, only those results are required to be submitted along with the performance test results required by  $\S$  60.8. If the Administrator finds that an affected facility is in compliance with all applicable standards for which performance tests are conducted in accordance with  $\S$  60.8 of this part but during the time such performance tests are being conducted fails to meet any applicable opacity standard, he shall notify the owner or operator and advise him that he may petition the Administrator within 10 days of receipt of notification to make appropriate adjustment to the opacity standard for the affected facility.

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(7) The Administrator will grant such a petition upon a demonstration by the owner or operator that the affected facility and associated air pollution control equipment was operated and maintained in a manner to minimize the opacity of emissions during the performance tests; that the performance tests were performed under the conditions established by the Administrator; and that the affected facility and associated air pollution control equipment were incapable of being adjusted or operated to meet the applicable opacity standard.

(8) The Administrator will establish an opacity standard for the affected facility meeting the above requirements at a level at which the source will be able, as indicated by the performance and opacity tests, to meet the opacity standard at all times during which the source is meeting the mass or concentration emission standard. The Administrator will promulgate the new opacity standard in the Federal Register.

(f) Special provisions set forth under an applicable subpart shall supersede any conflicting provisions in paragraphs (a) through (e) of this section.

(g) For the purpose of submitting compliance certifications or establishing whether or not a person has violated or is in violation of any standard in this part, nothing in this part shall preclude the use, including the exclusive use, of any credible evidence or information, relevant to whether a source would have been in compliance with applicable requirements if the appropriate performance or compliance test or procedure had been performed.

[38 FR 28565, Oct. 15, 1973, as amended at 39 FR 39873, Nov. 12, 1974; 43 FR 8800, Mar. 3, 1978; 45 FR 23379, Apr. 4, 1980; 48 FR 48335, Oct. 18, 1983; 50 FR 53113, Dec. 27, 1985; 51 FR 1790, Jan. 15, 1986; 52 FR 9781, Mar. 26, 1987; 62 FR 8328, Feb. 24, 1997; 65 FR 61749, Oct. 17, 2000]

## § 60.12 Circumvention.

No owner or operator subject to the provisions of this part shall build, erect, install, or use any article, machine, equipment or process, the use of which conceals an emission which would otherwise constitute a violation of an applicable standard. Such concealment includes, but is not limited to, the use of gaseous diluents to achieve compliance with an opacity standard or with a standard which is based on the concentration of a pollutant in the gases discharged to the atmosphere.

## [<u>39 FR 9314</u>, Mar. 8, 1974]

## § 60.13 Monitoring requirements.

(a) For the purposes of this section, all continuous monitoring systems required under applicable subparts shall be subject to the provisions of this section upon promulgation of performance specifications for continuous monitoring systems under appendix B to this part and, if the continuous monitoring system is used to demonstrate compliance with emission limits on a continuous basis, appendix F to this part, unless otherwise specified in an applicable subpart or by the Administrator. Appendix F is applicable December 4, 1987.

(b) All continuous monitoring systems and monitoring devices shall be installed and operational prior to conducting performance tests under § 60.8. Verification of operational status shall, as a minimum, include completion of the manufacturer's written requirements or recommendations for installation, operation, and calibration of the device.

(c) If the owner or operator of an affected facility elects to submit continous opacity monitoring system (COMS) data for compliance with the opacity standard as provided under  $\frac{60.11(e)(5)}{5}$ , he shall conduct a performance evaluation of the COMS as specified in Performance Specification 1, appendix B, of this part before the performance test required under § 60.8 is conducted. Otherwise, the owner or operator of an affected facility shall conduct a performance evaluation of the COMS or continuous emission monitoring system (CEMS) during any performance test required under § 60.8 or within 30 days thereafter in accordance with the applicable performance specification in appendix B of this part, The owner or operator of an affected facility shall conduct COMS or CEMS performance evaluations at such other times as may be required by the Administrator under section 114 of the Act.

(1) The owner or operator of an affected facility using a COMS to determine opacity compliance during any performance test required under  $\frac{60.8}{60.8}$  and as described in  $\frac{60.11(e)(5)}{5}$  shall furnish the Administrator two or, upon request, more copies of a written report of the results of the COMS performance evaluation described in paragraph (c) of this section at least 10 days before the performance test required under  $\S$  60.8 is conducted.

(2) Except as provided in paragraph (c)(1) of this section, the owner or operator of an affected facility shall furnish the Administrator within 60 days of completion two or, upon request, more copies of a written report of the results of the performance evaluation.

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(d)

(1) Owners and operators of a CEMS installed in accordance with the provisions of this part, must check the zero (or low level value between 0 and 20 percent of span value) and span (50 to 100 percent of span value) calibration drifts at least once each operating day in accordance with a written procedure. The zero and span must, at a minimum, be adjusted whenever either the 24-hour zero drift or the 24-hour span drift exceeds two times the limit of the applicable performance specification in <u>appendix B of this part</u>. The system must allow the amount of the excess zero and span drift to be recorded and quantified whenever specified. Owners and operators of a COMS installed in accordance with the provisions of this part must check the zero and upscale (span) calibration drifts at least once daily. For a particular COMS, the acceptable range of zero and upscale calibration materials is defined in the applicable version of PS-1 in <u>appendix B of this part</u>. For a COMS, the optical surfaces, exposed to the effluent gases, must be cleaned before performing the zero and upscale drift adjustments, except for systems using automatic zero adjustments. The optical surfaces must be cleaned when the cumulative automatic zero compensation exceeds 4 percent opacity.

(2) Unless otherwise approved by the Administrator, the following procedures must be followed for a COMS. Minimum procedures must include an automated method for producing a simulated zero opacity condition and an upscale opacity condition using a certified neutral density filter or other related technique to produce a known obstruction of the light beam. Such procedures must provide a system check of all active analyzer internal optics with power or curvature, all active electronic circuitry including the light source and photodetector assembly, and electronic or electro-mechanical systems and hardware and or software used during normal measurement operation.

(e) Except for system breakdowns, repairs, calibration checks, and zero and span adjustments required under <u>paragraph (d)</u> of this section, all continuous monitoring systems shall be in continuous operation and shall meet minimum frequency of operation requirements as follows:

(1) All continuous monitoring systems referenced by <u>paragraph (c)</u> of this section for measuring opacity of emissions shall complete a minimum of one cycle of sampling and analyzing for each successive 10-second period and one cycle of data recording for each successive 6-minute period.

(2) All continuous monitoring systems referenced by <u>paragraph (c)</u> of this section for measuring emissions, except opacity, shall complete a minimum of one cycle of operation (sampling, analyzing, and data recording) for each successive 15-minute period.

(f) All continuous monitoring systems or monitoring devices shall be installed such that representative measurements of emissions or process parameters from the affected facility are obtained. Additional procedures for location of continuous monitoring systems contained in the applicable Performance Specifications of <u>appendix B of this part</u> shall be used.

(g) When the effluents from a single affected facility or two or more affected facilities subject to the same emission standards are combined before being released to the atmosphere, the owner or operator may install applicable continuous monitoring systems on each effluent or on the combined effluent. When the affected facilities are not subject to the same emission standards, separate continuous monitoring systems shall be installed on each effluent. When the effluent from one affected facility is released to the atmosphere through more than one point, the owner or operator shall install an applicable continuous monitoring system on each separate effluent unless the installation of fewer systems is approved by the Administrator. When more than one continuous monitoring system is used to measure the emissions from one affected facility (e.g., multiple breechings, multiple outlets), the owner or operator shall report the results as required from each continuous monitoring system.

(h)

(1) Owners or operators of all continuous monitoring systems for measurement of opacity shall reduce all data to 6-minute averages and for continuous monitoring systems other than opacity to 1-hour averages for time periods as defined in  $\S$  60.2. Six-minute opacity averages shall be calculated from 36 or more data points equally spaced over each 6-minute period.

(2) For continuous monitoring systems other than opacity, 1-hour averages shall be computed as follows, except that the provisions pertaining to the validation of partial operating hours are only applicable for affected facilities that are required by the applicable subpart to include partial hours in the emission calculations:

(i) Except as provided under <u>paragraph (h)(2)(iii)</u> of this section, for a full operating hour (any clock hour with 60 minutes of unit operation), at least four valid data points are required to calculate the hourly average, *i.e.*, one data point in each of the 15-minute quadrants of the hour.

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(ii) Except as provided under <u>paragraph (h)(2)(iii)</u> of this section, for a partial operating hour (any clock hour with less than 60 minutes of unit operation), at least one valid data point in each 15-minute quadrant of the hour in which the unit operates is required to calculate the hourly average.

(iii) For any operating hour in which required maintenance or quality-assurance activities are performed:

(A) If the unit operates in two or more quadrants of the hour, a minimum of two valid data points, separated by at least 15 minutes, is required to calculate the hourly average; or

(B) If the unit operates in only one quadrant of the hour, at least one valid data point is required to calculate the hourly average.

(iv) If a daily calibration error check is failed during any operating hour, all data for that hour shall be invalidated, unless a subsequent calibration error test is passed in the same hour and the requirements of <u>paragraph (h)(2)(iii)</u> of this section are met, based solely on valid data recorded after the successful calibration.

(v) For each full or partial operating hour, all valid data points shall be used to calculate the hourly average.

(vi) Except as provided under <u>paragraph (h)(2)(vii)</u> of this section, data recorded during periods of continuous monitoring system breakdown, repair, calibration checks, and zero and span adjustments shall not be included in the data averages computed under this paragraph.

(vii) Owners and operators complying with the requirements of  $\S 60.7(f)(1)$  or (2) must include any data recorded during periods of monitor breakdown or malfunction in the data averages.

(viii) When specified in an applicable subpart, hourly averages for certain partial operating hours shall not be computed or included in the emission averages (e.g., hours with < 30 minutes of unit operation under  $\frac{60.47b(d)}{20}$ ).

(ix) Either arithmetic or integrated averaging of all data may be used to calculate the hourly averages. The data may be recorded in reduced or nonreduced form (e.g., ppm pollutant and percent  $O_2$  or ng/J of pollutant).

(3) All excess emissions shall be converted into units of the standard using the applicable conversion procedures specified in the applicable subpart. After conversion into units of the standard, the data may be rounded to the same number of significant digits used in the applicable subpart to specify the emission limit.

(i) After receipt and consideration of written application, the Administrator may approve alternatives to any monitoring procedures or requirements of this part including, but not limited to the following:

(1) Alternative monitoring requirements when installation of a continuous monitoring system or monitoring device specified by this part would not provide accurate measurements due to liquid water or other interferences caused by substances in the effluent gases.

(2) Alternative monitoring requirements when the affected facility is infrequently operated.

(3) Alternative monitoring requirements to accommodate continuous monitoring systems that require additional measurements to correct for stack moisture conditions.

(4) Alternative locations for installing continuous monitoring systems or monitoring devices when the owner or operator can demonstrate that installation at alternate locations will enable accurate and representative measurements.

(5) Alternative methods of converting pollutant concentration measurements to units of the standards.

(6) Alternative procedures for performing daily checks of zero and span drift that do not involve use of span gases or test cells.

(7) Alternatives to the A.S.T.M. test methods or sampling procedures specified by any subpart.

(8) Alternative continuous monitoring systems that do not meet the design or performance requirements in Performance Specification 1, appendix B, but adequately demonstrate a definite and consistent relationship between its measurements and the measurements of opacity by a system complying with the requirements in Performance Specification 1. The Administrator may require that such demonstration be performed for each affected facility.

(9) Alternative monitoring requirements when the effluent from a single affected facility or the combined effluent from two or more affected facilities is released to the atmosphere through more than one point.

(j) An alternative to the relative accuracy (RA) test specified in Performance Specification 2 of appendix B may be requested as follows:

(1) An alternative to the reference method tests for determining RA is available for sources with emission rates demonstrated to be less than 50 percent of the applicable standard. A source owner or operator may petition the Administrator to waive the RA test in Section 8.4 of Performance Specification 2 and substitute the procedures in Section 16.0 if the results of a performance test conducted according to the requirements in § 60.8 of this subpart or other tests performed following the criteria in § 60.8 demonstrate that the emission rate of the pollutant of interest in the units of the applicable standard is less than 50 percent of the applicable standard. For sources subject to standards expressed as control efficiency levels, a source owner or operator may petition the Administrator to waive the RA test and substitute the procedures in Section 16.0 of Performance Specification 2 if the control device exhaust emission rate is less than 50 percent of the level needed to meet the control efficiency requirement. The alternative procedures do not apply if the continuous emission monitoring system is used to determine compliance continuously with the applicable standard. The petition to waive the RA test shall include a detailed description of the procedures to be applied. Included shall be location and procedure for conducting the alternative, the concentration or response levels of the alternative RA materials, and the other equipment checks included in the alternative procedure. The Administrator will review the petition for completeness and applicability. The determination to grant a waiver will depend on the intended use of the CEMS data (e.g., data collection purposes other than NSPS) and may require specifications more stringent than in Performance Specification 2 (e.g., the applicable emission limit is more stringent than NSPS).

(2) The waiver of a CEMS RA test will be reviewed and may be rescinded at such time, following successful completion of the alternative RA procedure, that the CEMS data indicate that the source emissions are approaching the level. The criterion for reviewing the waiver is the collection of CEMS data showing that emissions have exceeded 70 percent of the applicable standard for seven, consecutive, averaging periods as specified by the applicable regulation(s). For sources subject to standards expressed as control efficiency levels, the criterion for reviewing the waiver is the collection of CEMS data showing that exhaust emissions have exceeded 70 percent of the level needed to meet the control efficiency requirement for seven, consecutive, averaging periods as specified by the applicable regulation(s) [e.g., §§ 60.45(g) (2) and (3), 60.73(e), and 60.84(e)]. It is the responsibility of the source operator to maintain records and determine the level of emissions relative to the criterion on the waiver of RA testing. If this criterion is exceeded, the owner or operator must notify the Administrator within 10 days of such occurrence and include a description of the nature and cause of the increasing emissions. The Administrator will review the notification and may rescind the waiver and require the owner or operator to conduct a RA test of the CEMS as specified in <u>Section 8.4</u> of Performance Specification 2.

[40 FR 46255, Oct. 6, 1975]

## **Editorial Note**

## **Editorial Note:**

For Federal Register citations affecting § 60.13, see the List of CFR Sections Affected, which appears in the Finding Aids section of the printed volume and at <u>www.govinfo.gov</u>.

## § 60.14 Modification.

(a) Except as provided under <u>paragraphs (e)</u> and (f) of this section, any physical or operational change to an existing facility which results in an increase in the emission rate to the atmosphere of any pollutant to which a standard applies shall be considered a modification within the meaning of section 111 of the Act. Upon modification, an existing facility shall become an affected facility for each pollutant to which a standard applies and for which there is an increase in the emission rate to the atmosphere.

(b) Emission rate shall be expressed as kg/hr of any pollutant discharged into the atmosphere for which a standard is applicable. The Administrator shall use the following to determine emission rate:

(1) Emission factors as specified in the latest issue of "Compilation of Air Pollutant Emission Factors," EPA Publication No. AP-42, or other emission factors determined by the Administrator to be superior to AP-42 emission factors, in cases where utilization of emission factors demonstrates that the emission level resulting from the physical or operational change will either clearly increase or clearly not increase.

(2) Material balances, continuous monitor data, or manual emission tests in cases where utilization of emission factors as referenced in <u>paragraph (b)(1)</u> of this section does not demonstrate to the Administrator's satisfaction whether the emission level resulting from the physical or operational change will either clearly increase or clearly not increase, or where an owner

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

or operator demonstrates to the Administrator's satisfaction that there are reasonable grounds to dispute the result obtained by the Administrator utilizing emission factors as referenced in <u>paragraph (b)(1)</u> of this section. When the emission rate is based on results from manual emission tests or continuous monitoring systems, the procedures specified in <u>appendix C of this</u> <u>part</u> shall be used to determine whether an increase in emission rate has occurred. Tests shall be conducted under such conditions as the Administrator shall specify to the owner or operator based on representative performance of the facility. At least three valid test runs must be conducted before and at least three after the physical or operational change. All operating parameters which may affect emissions must be held constant to the maximum feasible degree for all test runs.

(c) The addition of an affected facility to a stationary source as an expansion to that source or as a replacement for an existing facility shall not by itself bring within the applicability of this part any other facility within that source.

(d) [Reserved]

(e) The following shall not, by themselves, be considered modifications under this part:

(1) Maintenance, repair, and replacement which the Administrator determines to be routine for a source category, subject to the provisions of paragraph (c) of this section and  $\S 60.15$ .

(2) An increase in production rate of an existing facility, if that increase can be accomplished without a capital expenditure on that facility.

(3) An increase in the hours of operation.

(4) Use of an alternative fuel or raw material if, prior to the date any standard under this part becomes applicable to that source type, as provided by  $\S$  60.1, the existing facility was designed to accommodate that alternative use. A facility shall be considered to be designed to accommodate an alternative fuel or raw material if that use could be accomplished under the facility's construction specifications as amended prior to the change. Conversion to coal required for energy considerations, as specified in section 111(a)(8) of the Act, shall not be considered a modification.

(5) The addition or use of any system or device whose primary function is the reduction of air pollutants, except when an emission control system is removed or is replaced by a system which the Administrator determines to be less environmentally beneficial.

(6) The relocation or change in ownership of an existing facility.

(f) Special provisions set forth under an applicable subpart of this part shall supersede any conflicting provisions of this section.

(g) Within 180 days of the completion of any physical or operational change subject to the control measures specified in <u>paragraph (a)</u> of this section, compliance with all applicable standards must be achieved.

(h) No physical change, or change in the method of operation, at an existing electric utility steam generating unit shall be treated as a modification for the purposes of this section provided that such change does not increase the maximum hourly emissions of any pollutant regulated under this section above the maximum hourly emissions achievable at that unit during the 5 years prior to the change.

(i) Repowering projects that are awarded funding from the Department of Energy as permanent clean coal technology demonstration projects (or similar projects funded by EPA) are exempt from the requirements of this section provided that such change does not increase the maximum hourly emissions of any pollutant regulated under this section above the maximum hourly emissions achievable at that unit during the five years prior to the change.

(j)

(1) Repowering projects that qualify for an extension under section 409(b) of the Clean Air Act are exempt from the requirements of this section, provided that such change does not increase the actual hourly emissions of any pollutant regulated under this section above the actual hourly emissions achievable at that unit during the 5 years prior to the change.

(2) This exemption shall not apply to any new unit that:

(i) Is designated as a replacement for an existing unit;

(ii) Qualifies under section 409(b) of the Clean Air Act for an extension of an emission limitation compliance date under section 405 of the Clean Air Act; and

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(iii) Is located at a different site than the existing unit.

(k) The installation, operation, cessation, or removal of a temporary clean coal technology demonstration project is exempt from the requirements of this section. A *temporary clean coal control technology demonstration project*, for the purposes of this section is a clean coal technology demonstration project that is operated for a period of 5 years or less, and which complies with the State implementation plan for the State in which the project is located and other requirements necessary to attain and maintain the national ambient air quality standards during the project and after it is terminated.

(l) The reactivation of a very clean coal-fired electric utility steam generating unit is exempt from the requirements of this section.

[<u>40 FR 58419</u>, Dec. 16, 1975, as amended at <u>43 FR 34347</u>, Aug. 3, 1978; <u>45 FR 5617</u>, Jan. 23, 1980; <u>57 FR 32339</u>, July 21, 1992; <u>65 FR 61750</u>, Oct. 17, 2000]

## § 60.15 Reconstruction.

(a) An existing facility, upon reconstruction, becomes an affected facility, irrespective of any change in emission rate.

(b) "Reconstruction" means the replacement of components of an existing facility to such an extent that:

(1) The fixed capital cost of the new components exceeds 50 percent of the fixed capital cost that would be required to construct a comparable entirely new facility, and

(2) It is technologically and economically feasible to meet the applicable standards set forth in this part.

(c) "Fixed capital cost" means the capital needed to provide all the depreciable components.

(d) If an owner or operator of an existing facility proposes to replace components, and the fixed capital cost of the new components exceeds 50 percent of the fixed capital cost that would be required to construct a comparable entirely new facility, he shall notify the Administrator of the proposed replacements. The notice must be postmarked 60 days (or as soon as practicable) before construction of the replacements is commenced and must include the following information:

(1) Name and address of the owner or operator.

(2) The location of the existing facility.

(3) A brief description of the existing facility and the components which are to be replaced.

(4) A description of the existing air pollution control equipment and the proposed air pollution control equipment.

(5) An estimate of the fixed capital cost of the replacements and of constructing a comparable entirely new facility.

(6) The estimated life of the existing facility after the replacements.

(7) A discussion of any economic or technical limitations the facility may have in complying with the applicable standards of performance after the proposed replacements.

(e) The Administrator will determine, within 30 days of the receipt of the notice required by <u>paragraph (d)</u> of this section and any additional information he may reasonably require, whether the proposed replacement constitutes reconstruction.

(f) The Administrator's determination under paragraph (e) shall be based on:

(1) The fixed capital cost of the replacements in comparison to the fixed capital cost that would be required to construct a comparable entirely new facility;

(2) The estimated life of the facility after the replacements compared to the life of a comparable entirely new facility;

(3) The extent to which the components being replaced cause or contribute to the emissions from the facility; and

(4) Any economic or technical limitations on compliance with applicable standards of performance which are inherent in the proposed replacements.

(g) Individual <u>subparts of this part</u> may include specific provisions which refine and delimit the concept of reconstruction set forth in this section.

[<u>40 FR 58420</u>, Dec. 16, 1975]

## § 60.16 Priority list.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

	Prioritized Major Source Categories		
Priority Number <sup>1</sup>	Source Category		
1.	Synthetic Organic Chemical Manufacturing Industry (SOCMI) and Volatile Organic Liquid Storage Vessels and Handling Equipment		
	(a) SOCMI unit processes		
	(b) Volatile organic liquid (VOL) storage vessels and handling equipment		
	(c) SOCMI fugitive sources		
	(d) SOCMI secondary sources		
2.	Industrial Surface Coating: Cans		
3.	Petroleum Refineries: Fugitive Sources		
4.	Industrial Surface Coating: Paper		
5.	Dry Cleaning		
	(a) Perchloroethylene		
	(b) Petroleum solvent		
6.	Graphic Arts		
7.	Polymers and Resins: Acrylic Resins		
8.	Mineral Wool (Deleted)		
9.	Stationary Internal Combustion Engines		
10.	Industrial Surface Coating: Fabric		
11.	Industrial-Commercial-Institutional Steam Generating Units.		
12.	Incineration: Non-Municipal (Deleted)		
13.	Non-Metallic Mineral Processing		
14.	Metallic Mineral Processing		
15.	Secondary Copper (Deleted)		
16.	Phosphate Rock Preparation		
17.	Foundries: Steel and Gray Iron		
18.	Polymers and Resins: Polyethylene		
19.	Charcoal Production		
20.	Synthetic Rubber		
	(a) Tire manufacture		
	(b) SBR production		
21.	Vegetable Oil		
22.	Industrial Surface Coating: Metal Coil		
23.	Petroleum Transportation and Marketing		
24.	By-Product Coke Ovens		
25.	Synthetic Fibers		
26.	Plywood Manufacture		
27.	Industrial Surface Coating: Automobiles		
28.	Industrial Surface Coating: Large Appliances		
29.	Crude Oil and Natural Gas Production		
30.	Secondary Aluminum		

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

Prioritized Major Source Categories		
Priority Number <sup>1</sup>	Source Category	
31.	Potash (Deleted)	
32.	Lightweight Aggregate Industry: Clay, Shale, and Slate <sup>2</sup>	
33.	Glass	
34.	Gypsum	
35.	Sodium Carbonate	
36.	Secondary Zinc (Deleted)	
37.	Polymers and Resins: Phenolic	
38.	Polymers and Resins: Urea-Melamine	
39.	Ammonia (Deleted)	
40.	Polymers and Resins: Polystyrene	
41.	Polymers and Resins: ABS-SAN Resins	
42.	Fiberglass	
43.	Polymers and Resins: Polypropylene	
44.	Textile Processing	
45.	Asphalt Processing and Asphalt Roofing Manufacture	
46.	Brick and Related Clay Products	
47.	Ceramic Clay Manufacturing (Deleted)	
48.	Ammonium Nitrate Fertilizer	
49.	Castable Refractories (Deleted)	
50.	Borax and Boric Acid (Deleted)	
51.	Polymers and Resins: Polyester Resins	
52.	Ammonium Sulfate	
53.	Starch	
54.	Perlite	
55.	Phosphoric Acid: Thermal Process (Deleted)	
56.	Uranium Refining	
57.	Animal Feed Defluorination (Deleted)	
58.	Urea (for fertilizer and polymers)	
59.	Detergent (Deleted)	
Other Source Categories		
Lead acid battery manufacture <sup>3</sup>		
Organic solven	t cleaning <sup>3</sup>	
Industrial surface coating: metal furniture <sup>3</sup>		
Stationary gas turbines <sup>4</sup>		
Municipal solid waste landfills <sup>4</sup>		
<sup>1</sup> Low numbers have highest priority, e.g., No. 1 is high priority, No. 59 is low priority.		
<sup>2</sup> Formerly titled "Sintering: Clay and Fly Ash".		
<sup>3</sup> Minor source category, but included on list since an NSPS is being developed for that source category.		
<sup>4</sup> Not prioritized, since an NSPS for this major source category has already been promulgated.		

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[<u>47 FR 951</u>, Jan. 8, 1982, as amended at <u>47 FR 31876</u>, July 23, 1982; <u>51 FR 42796</u>, Nov. 25, 1986; <u>52 FR 11428</u>, Apr. 8, 1987; <u>61 FR 9919</u>, Mar. 12, 1996]

## § 60.17 Incorporations by reference.

(a)

(1) Certain material is incorporated by reference into this part with the approval of the Director of the Federal Register under <u>5 U.S.C. 552(a)</u> and <u>1 CFR part 51</u>. To enforce any edition other than that specified in this section, the U.S. Environmental Protection Agency (EPA) must publish a document in the Federal Register and the material must be available to the public. All approved incorporation by reference (IBR) material is available for inspection at the EPA and at the National Archives and Records Administration (NARA). Contact the EPA at: EPA Docket Center, Public Reading Room, EPA WJC West, Room 3334, 1301 Constitution Ave. NW, Washington, DC; phone: (202) 566-1744. For information on the availability of this material at NARA, visit <u>www.archives.gov/federal-register/cfr/ibr-locations</u> or email <u>fr.inspection@nara.gov</u>.

(2) The IBR material may be obtained from the sources in the following paragraphs of this section or from one or more private resellers listed in this <u>paragraph (a)(2)</u>. For material that is no longer commercially available, contact: the EPA (see <u>paragraph (a)(1)</u> of this section).

(i) Accuris Standards Store, 321 Inverness Drive, South Englewood, CO 80112; phone: (800) 332-6077; website: <u>https://store.accuristech.com</u>.

(ii) American National Standards Institute (ANSI), see <u>paragraph (d)</u> of this section.

(iii) GlobalSpec, 257 Fuller Road, Suite NFE 1100, Albany, NY 12203-3621; phone: (800) 261-2052; website: <u>https://standards.globalspec.com</u>.

(iv) Nimonik Document Center, 401 Roland Way, Suite 224, Oakland, CA 94624; phone (650) 591-7600; email: <u>info@document-center.com</u>; website: <u>www.document-center.com</u>.

(v) Techstreet, phone: (855) 999-9870; email: <u>store@techstreet.com</u>; website: <u>www.techstreet.com</u>.

(b) American Gas Association, available through ILI Infodisk, 610 Winters Avenue, Paramus, New Jersey 07652:

(1) American Gas Association Report No. 3: Orifice Metering for Natural Gas and Other Related Hydrocarbon Fluids, Part 1: General Equations and Uncertainty Guidelines (1990), IBR approved for <u>§ 60.107a(d)</u>.

(2) American Gas Association Report No. 3: Orifice Metering for Natural Gas and Other Related Hydrocarbon Fluids, Part 2: Specification and Installation Requirements (2000), IBR approved for <u>§ 60.107a(d)</u>.

(3) American Gas Association Report No. 11: Measurement of Natural Gas by Coriolis Meter (2003), IBR approved for § 60.107a(d).

(4) American Gas Association Transmission Measurement Committee Report No. 7: Measurement of Gas by Turbine Meters (Revised February 2006), IBR approved for <u>§ 60.107a(d)</u>.

(c) American Hospital Association (AHA) Service, Inc., Post Office Box 92683, Chicago, Illinois 60675-2683.

(1) An Ounce of Prevention: Waste Reduction Strategies for Health Care Facilities. American Society for Health Care Environmental Services of the American Hospital Association. Chicago, Illinois. 1993. AHA Catalog No. 057007. ISBN 0-87258-673-5. IBR approved for <u>§§ 60.35e</u> and <u>60.55c</u>.

(2) [Reserved]

(d) American National Standards Institute (ANSI), 25 West 43rd Street, Fourth Floor, New York, NY 10036-7417; phone: (212) 642-4980; email: *info@ansi.org*; website: *www.ansi.org*.

(1) ANSI No. C12.20-2010 American National Standard for Electricity Meters—0.2 and 0.5 Accuracy Classes (Approved August 31, 2010); IBR approved for <u>§§ 60.5535(d)</u>; <u>60.5535a(d)</u>; <u>60.5860b(a)</u>.

(2) [Reserved]

(e) American Petroleum Institute (API), 200 Massachusetts Ave. NW, Suite 1100, Washington, DC 20001; phone: (202) 682-8000; website: <u>www.api.org</u>.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(1) API Publication 2517, Evaporation Loss from External Floating Roof Tanks, Second Edition, February 1980, IBR approved for  $\frac{\$ 60.111(i)}{100}$ ,  $\frac{60.111a(f)}{100}$ , and  $\frac{60.116b(e)}{100}$ .

(2) API Manual of Petroleum Measurement Standards, Chapter 14—Natural Gas Fluids Measurement, Section 1—Collecting and Handling of Natural Gas Samples for Custody Transfer, 7th Edition, May 2016, IBR approved for <u>§ 60.4415(a)</u>.

(3) API Manual of Petroleum Measurement Standards, Chapter 22—Testing Protocol, Section 2—Differential Pressure Flow Measurement Devices, First Edition, August 2005, IBR approved for  $\frac{\& 60.107a(d)}{\& 60.107a(d)}$ .

(f) American Public Health Association, 1015 18th Street NW., Washington, DC 20036.

(1) "Standard Methods for the Examination of Water and Wastewater," 16th edition, 1985. Method 303F: "Determination of Mercury by the Cold Vapor Technique." Incorporated by reference for appendix A-8 to part 60, Method 29, §§ 9.2.3, 10.3, and 11.1.3.

(2) 2540 G. Total, Fixed, and Volatile Solids in Solid and Semisolid Samples, in Standard Methods for the Examination of Water and Wastewater, 20th Edition, 1998, IBR approved for  $\frac{60.154(b)}{2}$ .

(g) American Society of Mechanical Engineers (ASME), Two Park Avenue, New York, NY 10016-5990; phone: (800) 843-2763; email: <u>*CustomerCare@asme.org*</u>; website: <u>www.asme.org</u>.

(1) ASME Interim Supplement 19.5 on Instruments and Apparatus: Application, Part II of Fluid Meters, 6th Edition (1971), IBR approved for <u>§§ 60.58a(h)</u>, <u>60.58b(i)</u>, <u>60.1320(a)</u>, and <u>60.1810(a)</u>.

(2) ASME MFC-3M-2004, Measurement of Fluid Flow in Pipes Using Orifice, Nozzle, and Venturi, IBR approved for <u>§</u> <u>60.107a(d)</u>.

(3) ASME/ANSI MFC-4M-1986 (Reaffirmed 2008), Measurement of Gas Flow by Turbine Meters, IBR approved for <u>§</u> <u>60.107a(d)</u>.

(4) ASME/ANSI MFC-5M-1985 (Reaffirmed 2006), Measurement of Liquid Flow in Closed Conduits Using Transit-Time Ultrasonic Flowmeters, IBR approved for <u>§ 60.107a(d)</u>.

(5) ASME MFC-6M-1998 (Reaffirmed 2005), Measurement of Fluid Flow in Pipes Using Vortex Flowmeters, IBR approved for <u>§ 60.107a(d)</u>.

(6) ASME/ANSI MFC-7M-1987 (Reaffirmed 2006), Measurement of Gas Flow by Means of Critical Flow Venturi Nozzles, IBR approved for <u>§ 60.107a(d)</u>.

(7) ASME/ANSI MFC-9M-1988 (Reaffirmed 2006), Measurement of Liquid Flow in Closed Conduits by Weighing Method, IBR approved for <u>§ 60.107a(d)</u>.

(8) ASME MFC-11M-2006, Measurement of Fluid Flow by Means of Coriolis Mass Flowmeters, IBR approved for <u>§</u> <u>60.107a(d)</u>.

(9) ASME MFC-14M-2003, Measurement of Fluid Flow Using Small Bore Precision Orifice Meters, IBR approved for <u>§</u> <u>60.107a(d)</u>.

(10) ASME MFC-16-2007, Measurement of Liquid Flow in Closed Conduits with Electromagnetic Flowmeters, IBR approved for  $\frac{60.107a(d)}{100}$ .

(11) ASME MFC-18M-2001, Measurement of Fluid Flow Using Variable Area Meters, IBR approved for § 60.107a(d).

(12) ASME MFC-22-2007, Measurement of Liquid by Turbine Flowmeters, IBR approved for § 60.107a(d).

(13) ASME PTC 4.1-1964 (Reaffirmed 1991), Power Test Codes: Test Code for Steam Generating Units (with 1968 and 1969 Addenda), IBR approved for  $\underline{\$\$ 60.46b}, \underline{60.58a(h)}, \underline{60.58b(i)}, \underline{60.1320(a)}, and \underline{60.1810(a)}$ .

(14) ASME/ANSI PTC 19.10-1981, Flue and Exhaust Gas Analyses [Part 10, Instruments and Apparatus], Issued August 31, 1981; IBR approved for  $\S$  60.56c(b); 60.63(f); 60.106(e); 60.104a(d), (h), (i), and (j); 60.105a(b), (d), (f), and (g); 60.106a(a); 60.107a(a), (c), and (d); 60.275(e); 60.275a(e); 60.275b(e); tables 1 and 3 to subpart EEEE; tables 2 and 4 to subpart FFFF; table 2 to subpart JJJJ;  $\S$ 

<u>60.285a(f);</u> <u>60.396(a);</u> <u>60.614a(b);</u> <u>60.664a(b);</u> <u>60.704(b);</u> <u>60.704a(b);</u> <u>60.2145(s)</u> and <u>(t);</u> <u>60.2710(s)</u> and <u>(t);</u> <u>60.2730(q);</u> <u>60.415(a);</u> <u>60.4900(b);</u> <u>60.5220(b);</u> tables 1 and 2 to subpart LLLL; tables 2 and 3 to subpart MMMM; <u>§§</u>

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<u>60.5406(c)</u>; <u>60.5406a(c)</u>; <u>60.5406b(c)</u>; <u>60.5407a(g)</u>; <u>60.5407b(g)</u>; <u>60.5413(b)</u>; <u>60.5413a(b)</u> and <u>(d)</u>; <u>60.5413</u>b(d) and (d); 60.5413c(b) and (d).

(15) ASME PTC 22-2014, Gas Turbines: Performance Test Codes, (Issued December 31, 2014); IBR approved for §§ 60.5580; 60.5580a.

(16) ASME PTC 46-1996, Performance Test Code on Overall Plant Performance, (Issued October 15,1997); IBR approved for <u>§§ 60.5580</u>; <u>60.5580a</u>.

(17) ASME QRO-1-1994, Standard for the Qualification and Certification of Resource Recovery Facility Operators, IBR approved for  $\frac{880.54b(a)}{100}$  and  $\frac{(b)}{100}$ ,  $\frac{60.56}{100}$ ,  $\frac{60.56}{100}$ ,  $\frac{60.1185(a)}{100}$  and  $\frac{(c)}{100}$ , and  $\frac{(c)}{100}$ .

(h) ASTM International, 100 Barr Harbor Drive, P.O. Box CB700, West Conshohocken, Pennsylvania 19428-2959; phone: (800) 262-1373; website: <u>www.astm.org</u>.

(1) ASTM A99-76, Standard Specification for Ferromanganese, IBR approved for <u>§ 60.261</u>.

(2) ASTM A99-82 (Reapproved 1987), Standard Specification for Ferromanganese, IBR approved for <u>§ 60.261</u>.

(3) ASTM A100-69, Standard Specification for Ferrosilicon, IBR approved for <u>§ 60.261</u>.

(4) ASTM A100-74, Standard Specification for Ferrosilicon, IBR approved for § 60.261.

(5) ASTM A100-93, Standard Specification for Ferrosilicon, IBR approved for § 60.261.

(6) ASTM A101-73, Standard Specification for Ferrochromium, IBR approved for § 60.261.

(7) ASTM A101-93, Standard Specification for Ferrochromium, IBR approved for <u>§ 60.261</u>.

(8) ASTM A482-76, Standard Specification for Ferrochromesilicon, IBR approved for § 60.261.

(9) ASTM A482-93, Standard Specification for Ferrochromesilicon, IBR approved for <u>§ 60.261</u>.

(10) ASTM A483-64, Standard Specification for Silicomanganese, IBR approved for § 60.261.

(11) ASTM A483-74 (Reapproved 1988), Standard Specification for Silicomanganese, IBR approved for <u>§ 60.261</u>.

(12) ASTM A495-76, Standard Specification for Calcium-Silicon and Calcium Manganese-Silicon, IBR approved for <u>§</u> 60.261.

(13) ASTM A495-94, Standard Specification for Calcium-Silicon and Calcium Manganese-Silicon, IBR approved for § 60.261.

(14) ASTM D86-78, Distillation of Petroleum Products, IBR approved for <u>§§ 60.562-2(d)</u>, <u>60.593(d)</u>, <u>60.593</u>(d), 60.633(h).

(15) ASTM D86-82, Distillation of Petroleum Products, IBR approved for <u>§§ 60.562-2(d)</u>, <u>60.593(d)</u>, <u>60.593</u>(d), 60.633(h).

(16) ASTM D86-90, Distillation of Petroleum Products, IBR approved for <u>§§ 60.562-2(d)</u>, <u>60.593(d)</u>, <u>60.593</u>a(d), 60.633(h).

(17) ASTM D86-93, Distillation of Petroleum Products, IBR approved for <u>§§ 60.562-2(d)</u>, <u>60.593(d)</u>, <u>60.593</u>(d), 60.633(h).

(18) ASTM D86-95, Distillation of Petroleum Products, IBR approved for <u>§§ 60.562-2(d)</u>, <u>60.593(d)</u>, <u>60.593</u>a(d), 60.633(h).

(19) ASTM D86-96, Distillation of Petroleum Products, approved April 10, 1996; IBR approved for <u>§§ 60.562-2(d)</u>. 60.593(d). 60.593a(d); 60.633(h); 60.5401(f); 60.5401a(f); 60.5402b(d); 60.5402c(d).

(20) ASTM D129-64, Standard Test Method for Sulfur in Petroleum Products (General Bomb Method), IBR approved for <u>§§</u> <u>60.106(j)</u> and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(21) ASTM D129-78, Standard Test Method for Sulfur in Petroleum Products (General Bomb Method), IBR approved for <u>§§</u> <u>60.106(j)</u> and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(22) ASTM D129-95, Standard Test Method for Sulfur in Petroleum Products (General Bomb Method), IBR approved for <u>§§</u> <u>60.106(j)</u> and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(23) ASTM D129-00, Standard Test Method for Sulfur in Petroleum Products (General Bomb Method), IBR approved for § 60.335(b).

(24) ASTM D129-00 (Reapproved 2005), Standard Test Method for Sulfur in Petroleum Products (General Bomb Method), IBR approved for  $\frac{60.4415(a)}{2}$ .

(25) ASTM D240-76, Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter, IBR approved for <u>§§ 60.46(c)</u>, <u>60.296(b)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(26) ASTM D240-92, Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter, IBR approved for <u>§§ 60.46(c)</u>, <u>60.296(b)</u>, and appendix A-7: Method 19, <u>Section 12.5.2.2.3</u>.

(27) ASTM D240-02 (Reapproved 2007), Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter, (Approved May 1, 2007), IBR approved for  $\S 60.107a(d)$ .

(28) ASTM D240-19, Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter, approved November 1, 2019; IBR approved for  $\frac{\& 60.485b(g)}{\& 60.485b(g)}$ .

(29) ASTM D270-65, Standard Method of Sampling Petroleum and Petroleum Products, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.1</u>.

(30) ASTM D270-75, Standard Method of Sampling Petroleum and Petroleum Products, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.1</u>.

(31) ASTM D323-82, Test Method for Vapor Pressure of Petroleum Products (Reid Method), IBR approved for <u>&&</u> <u>60.111(1)</u>, <u>60.111a(g)</u>, <u>60.111b</u>, and <u>60.116b(f)</u>.

(32) ASTM D323-94, Test Method for Vapor Pressure of Petroleum Products (Reid Method), IBR approved for  $\underline{\$\$}$ <u>60.111(1)</u>, <u>60.111a(g)</u>, <u>60.111b</u>, and <u>60.116b(f)</u>.

(33) ASTM D388-77, Standard Specification for Classification of Coals by Rank, IBR approved for <u>§§</u> <u>60.41</u>, <u>60.45(f)</u>, <u>60.41Da</u>, <u>60.41b</u>, <u>60.41c</u>, and <u>60.251</u>.

(34) ASTM D388-90, Standard Specification for Classification of Coals by Rank, IBR approved for <u>§§</u> <u>60.41</u>, <u>60.45(f)</u>, <u>60.41Da</u>, <u>60.41b</u>, <u>60.41c</u>, and <u>60.251</u>.

(35) ASTM D388-91, Standard Specification for Classification of Coals by Rank, IBR approved for <u>§§</u> <u>60.41</u>, <u>60.45(f)</u>, <u>60.41Da</u>, <u>60.41b</u>, <u>60.41c</u>, and <u>60.251</u>.

(36) ASTM D388-95, Standard Specification for Classification of Coals by Rank, IBR approved for <u>§§</u> <u>60.41</u>, <u>60.45(f)</u>, <u>60.41Da</u>, <u>60.41b</u>, <u>60.41c</u>, and <u>60.251</u>.

(37) ASTM D388-98a, Standard Specification for Classification of Coals by Rank, IBR approved for <u>§§</u> <u>60.41</u>, <u>60.45(f)</u>, <u>60.41Da</u>, <u>60.41b</u>, <u>60.41c</u>, and <u>60.251</u>.

(38) ASTM D388-99 (Reapproved 2004)<sup> $\epsilon$ 1</sup>(ASTM D388-99R04), Standard Classification of Coals by Rank, (Approved June 1, 2004); IBR approved for <u>§§ 60.41; 60.45(f); 60.41Da; 60.41b; 60.41c; 60.251; 60.5580; 60.5580a</u>.

(39) ASTM D396-78, Standard Specification for Fuel Oils, IBR approved for <u>§§ 60.41b</u>, <u>60.41c</u>, <u>60.111(b)</u>, and <u>60.111a(b)</u>.

(40) ASTM D396-89, Standard Specification for Fuel Oils, IBR approved for <u>§§ 60.41b</u>, <u>60.41c</u>, <u>60.111(b)</u>, and <u>60.111a(b)</u>.

(41) ASTM D396-90, Standard Specification for Fuel Oils, IBR approved for <u>§§ 60.41b</u>, <u>60.41c</u>, <u>60.111(b)</u>, and <u>60.111a(b)</u>.

(42) ASTM D396-92, Standard Specification for Fuel Oils, IBR approved for <u>§§ 60.41b</u>, <u>60.41c</u>, <u>60.111(b)</u>, and <u>60.111a(b)</u>.

(43) ASTM D396-98, Standard Specification for Fuel Oils, (Approved April 10, 1998); IBR approved for <u>§§</u> <u>60.41b</u>; <u>60.41c</u>; <u>60.111a(b)</u>; <u>60.5580</u>; <u>60.5580a</u>.

(44) ASTM D975-78, Standard Specification for Diesel Fuel Oils, IBR approved for <u>§§ 60.111(b)</u> and <u>60.111a(b)</u>.

- (45) ASTM D975-96, Standard Specification for Diesel Fuel Oils, IBR approved for <u>§§ 60.111(b)</u> and <u>60.111a(b)</u>.
- (46) ASTM D975-98a, Standard Specification for Diesel Fuel Oils, IBR approved for <u>§§ 60.111(b)</u> and <u>60.111a(b)</u>.

(47) ASTM D975-08a, Standard Specification for Diesel Fuel Oils, (Approved October 1, 2008); IBR approved for <u>§§</u> <u>60.41b</u>; <u>60.41c</u>; <u>60.5580</u>; <u>60.5580a</u>.

(48) ASTM D1072-80, Standard Test Method for Total Sulfur in Fuel Gases, IBR approved for § 60.335(b).

(49) ASTM D1072-90 (Reapproved 1994), Standard Test Method for Total Sulfur in Fuel Gases, IBR approved for <u>§</u> <u>60.335(b)</u>.

(50) ASTM D1072-90 (Reapproved 1999), Standard Test Method for Total Sulfur in Fuel Gases, IBR approved for § 60.4415(a).

(51) ASTM D1137-53, Standard Method for Analysis of Natural Gases and Related Types of Gaseous Mixtures by the Mass Spectrometer, IBR approved for  $\frac{60.45(f)}{10}$ .

(52) ASTM D1137-75, Standard Method for Analysis of Natural Gases and Related Types of Gaseous Mixtures by the Mass Spectrometer, IBR approved for  $\S 60.45(f)$ .

(53) ASTM D1193-77, Standard Specification for Reagent Water, IBR approved for appendix A-3 to part 60: Method 5, <u>Section 7.1.3</u>; Method 5E, <u>Section 7.2.1</u>; Method 5F, <u>Section 7.2.1</u>; appendix A-4 to part 60: Method 6, <u>Section 7.1.1</u>; Method 7C, <u>Section 7.1.1</u>; Method 7D, <u>Section 7.1.1</u>; Method 10A, <u>Section 7.1.1</u>; appendix A-5 to part 60: Method 11, <u>Section 7.1.3</u>; Method 12, <u>Section 7.1.3</u>; Method 13A, <u>Section 7.1.2</u>; appendix A-8 to part 60: Method 26, <u>Section 7.1.2</u>; and Method 29, <u>Section 7.2.2</u>.

(54) ASTM D1193-91, Standard Specification for Reagent Water, IBR approved for appendix A-3 to part 60: Method 5, <u>Section 7.1.3</u>; Method 5E, <u>Section 7.2.1</u>; Method 5F, <u>Section 7.2.1</u>; appendix A-4 to part 60: Method 6, <u>Section 7.1.1</u>; Method 7C, <u>Section 7.1.1</u>; Method 7D, <u>Section 7.1.1</u>; Method 10A, <u>Section 7.1.1</u>; appendix A-5 to part 60: Method 11, <u>Section 7.1.3</u>; Method 12, <u>Section 7.1.3</u>; Method 13A, <u>Section 7.1.2</u>; appendix A-8 to part 60: Method 26, <u>Section 7.1.2</u>; and Method 29, <u>Section 7.2.2</u>.

(55) ASTM D1266-87, Standard Test Method for Sulfur in Petroleum Products (Lamp Method), IBR approved for  $\underline{\$\$}$  <u>60.106(j)</u> and <u>60.335(b)</u>.

(56) ASTM D1266-91, Standard Test Method for Sulfur in Petroleum Products (Lamp Method), IBR approved for  $\underline{\$\$}$ <u>60.106(j)</u> and <u>60.335(b)</u>.

(57) ASTM D1266-98, Standard Test Method for Sulfur in Petroleum Products (Lamp Method), IBR approved for <u>§§</u> <u>60.106(j)</u> and <u>60.335(b)</u>.

(58) ASTM D1266-98 (Reapproved 2003)<sup> $\epsilon$ , 1</sup> Standard Test Method for Sulfur in Petroleum Products (Lamp Method), IBR approved for <u>§ 60.4415(a)</u>.

(59) ASTM D1475-60 (Reapproved 1980), Standard Test Method for Density of Paint, Varnish Lacquer, and Related Products, IBR approved for <u>§ 60.435(d)</u>, appendix A-7 to part 60: Method 24, <u>Section 6.1</u>; and Method 24A, Sections 6.5 and 7.1.

(60) ASTM D1475-90, Standard Test Method for Density of Paint, Varnish Lacquer, and Related Products, IBR approved for  $\frac{60.435(d)}{1000}$ , appendix A-7 to part 60: Method 24, Section 6.1; and Method 24A,  $\frac{88}{1000}$  6.5 and  $\frac{7.1}{1000}$ .

(61) ASTM D1475-13, Standard Test Method for Density of Liquid Coatings, Inks, and Related Products, Approved November 1, 2013; IBR approved for  $\S 60.393a(f)$ .

(62) ASTM D1552-83, Standard Test Method for Sulfur in Petroleum Products (High-Temperature Method), IBR approved for <u>§§ 60.106(j)</u>, <u>60.335(b)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(63) ASTM D1552-95, Standard Test Method for Sulfur in Petroleum Products (High-Temperature Method), IBR approved for <u>§§ 60.106(j)</u>, <u>60.335(b)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(64) ASTM D1552-01, Standard Test Method for Sulfur in Petroleum Products (High-Temperature Method), IBR approved for <u>§§ 60.106(j)</u>, <u>60.335(b)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(65) ASTM D1552-03, Standard Test Method for Sulfur in Petroleum Products (High-Temperature Method), IBR approved for <u>§ 60.4415(a)</u>.

(66) ASTM D1826-77, Standard Test Method for Calorific Value of Gases in Natural Gas Range by Continuous Recording Calorimeter, IBR approved for <u>§§ 60.45(f)</u>, <u>60.46(c)</u>, <u>60.296(b)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.3.2.4</u>.

(67) ASTM D1826-94, Standard Test Method for Calorific Value of Gases in Natural Gas Range by Continuous Recording Calorimeter, IBR approved for <u>§§ 60.45(f)</u>, <u>60.46(c)</u>, <u>60.296(b)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.3.2.4</u>.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(68) ASTM D1826-94 (Reapproved 2003), Standard Test Method for Calorific (Heating) Value of Gases in Natural Gas Range by Continuous Recording Calorimeter, (Approved May 10, 2003), IBR approved for <u>§ 60.107a(d)</u>.

(69) ASTM D1835-87, Standard Specification for Liquefied Petroleum (LP) Gases, IBR approved for <u>§§ 60.41Da</u>, <u>60.41b</u>, and <u>60.41c</u>.

(70) ASTM D1835-91, Standard Specification for Liquefied Petroleum (LP) Gases, IBR approved for <u>§§ 60.41Da</u>, <u>60.41b</u>, and <u>60.41c</u>.

(71) ASTM D1835-97, Standard Specification for Liquefied Petroleum (LP) Gases, IBR approved for <u>§§ 60.41Da</u>, <u>60.41b</u>, and <u>60.41c</u>.

(72) ASTM D1835-03a, Standard Specification for Liquefied Petroleum (LP) Gases, IBR approved for <u>§§ 60.41Da</u>, <u>60.41b</u>, and <u>60.41c</u>.

(73) ASTM D1945-64, Standard Method for Analysis of Natural Gas by Gas Chromatography, IBR approved for § 60.45(f).

(74) ASTM D1945-76, Standard Method for Analysis of Natural Gas by Gas Chromatography, IBR approved for § 60.45(f).

(75) ASTM D1945-91, Standard Method for Analysis of Natural Gas by Gas Chromatography, IBR approved for § 60.45(f).

(76) ASTM D1945-96, Standard Method for Analysis of Natural Gas by Gas Chromatography, IBR approved for <u>§ 60.45(f)</u>.

(77) ASTM D1945-03 (Reapproved 2010), Standard Method for Analysis of Natural Gas by Gas Chromatography, approved January 1, 2010; IBR approved for <u>§§ 60.107a(d)</u>; <u>60.5413(d)</u>; <u>60.5413(d)</u>; <u>60.5413(d)</u>; <u>60.5413c(d)</u>.

(78) ASTM D1945-14 (Reapproved 2019), Standard Test Method for Analysis of Natural Gas by Gas Chromatography, approved December 1, 2019; IBR approved for  $\frac{60.485b(g)}{2}$ .

(79) ASTM D1946-77, Standard Method for Analysis of Reformed Gas by Gas Chromatography, IBR approved for  $\underline{\$\$}$  <u>60.18(f)</u>, <u>60.45(f)</u>, <u>60.564(f)</u>, <u>60.614(e)</u>, <u>60.664(e)</u>, and <u>60.704(d)</u>.

(80) ASTM D1946-90 (Reapproved 1994), Standard Method for Analysis of Reformed Gas by Gas Chromatography, IBR approved for  $\frac{88\ 60.18(f)\ 60.45(f)\ 60.564(f)\ 60.614(e)\ 60.664(e)\ and\ 60.704(d)}{60.704(d)}$ .

(81) ASTM D1946-90 (Reapproved 2006), Standard Method for Analysis of Reformed Gas by Gas Chromatography, (Approved June 1, 2006), IBR approved for <u>§ 60.107a(d)</u>.

(82) ASTM D2013-72, Standard Method of Preparing Coal Samples for Analysis, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(83) ASTM D2013-86, Standard Method of Preparing Coal Samples for Analysis, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(84) ASTM D2015-77 (Reapproved 1978), Standard Test Method for Gross Calorific Value of Solid Fuel by the Adiabatic Bomb Calorimeter, IBR approved for  $\frac{\$\$ 60.45(f)}{60.46(c)}$ , and appendix A-7 to part 60: Method 19, Section 12.5.2.1.3.

(85) ASTM D2015-96, Standard Test Method for Gross Calorific Value of Solid Fuel by the Adiabatic Bomb Calorimeter, IBR approved for <u>§§ 60.45(f)</u>, <u>60.46(c)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(86) ASTM D2016-74, Standard Test Methods for Moisture Content of Wood, IBR approved for appendix A-8 to part 60: Method 28, Section 16.1.1.

(87) ASTM D2016-83, Standard Test Methods for Moisture Content of Wood, IBR approved for appendix A-8 to part 60: Method 28, <u>Section 16.1.1</u>.

(88) ASTM D2234-76, Standard Methods for Collection of a Gross Sample of Coal, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.1</u>.

(89) ASTM D2234-96, Standard Methods for Collection of a Gross Sample of Coal, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.1</u>.

(90) ASTM D2234-97b, Standard Methods for Collection of a Gross Sample of Coal, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.1</u>.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(91) ASTM D2234-98, Standard Methods for Collection of a Gross Sample of Coal, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.1</u>.

(92) ASTM D2369-81, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.2</u>.

(93) ASTM D2369-87, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.2</u>.

(94) ASTM D2369-90, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.2</u>.

(95) ASTM D2369-92, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.2</u>.

(96) ASTM D2369-93, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.2</u>.

(97) ASTM D2369-95, Standard Test Method for Volatile Content of Coatings, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.2</u>.

(98) ASTM D2369-10 (Reapproved 2015)e1, Standard Test Method for Volatile Content of Coatings, (Approved June 1, 2015); IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.2</u>.

(99) ASTM D2369-20, Standard Test Method for Volatile Content of Coatings, Approved June 1, 2020; IBR approved for <u>§§</u> <u>60.393a(f)</u>; <u>60.723(b)</u>; <u>60.724(a)</u>; <u>60.725(b)</u>; <u>60.723a(b)</u>; <u>60.724a(a)</u>; <u>60.725a(b)</u>.

(100) ASTM D2382-76, Heat of Combustion of Hydrocarbon Fuels by Bomb Calorimeter (High-Precision Method), IBR approved for  $\frac{880.18(f)}{0.485(g)}$ ,  $\frac{60.485(g)}{0.485(g)}$ ,  $\frac{60.564(f)}{0.614(e)}$ ,  $\frac{60.664(e)}{0.604(d)}$ , and  $\frac{60.704(d)}{0.004(d)}$ .

(101) ASTM D2382-88, Heat of Combustion of Hydrocarbon Fuels by Bomb Calorimeter (High-Precision Method), IBR approved for  $\frac{880.18(f)}{60.485(g)}$ ,  $\frac{60.485(g)}{60.485(g)}$ ,  $\frac{60.564(f)}{60.614(e)}$ ,  $\frac{60.664(e)}{60.664(e)}$ , and  $\frac{60.704(d)}{60.704(d)}$ .

(102) ASTM D2504-67, Noncondensable Gases in C3 and Lighter Hydrocarbon Products by Gas Chromatography, IBR approved for  $\frac{\& 60.485(g)}{\& 60.485(g)}$  and  $\frac{60.485a(g)}{\& 60.485a(g)}$ .

(103) ASTM D2504-77, Noncondensable Gases in C3 and Lighter Hydrocarbon Products by Gas Chromatography, IBR approved for  $\frac{\& 0.485(g)}{2}$  and  $\frac{60.485(g)}{2}$ .

(104) ASTM D2504-88 (Reapproved 1993), Noncondensable Gases in C3 and Lighter Hydrocarbon Products by Gas Chromatography, IBR approved for  $\frac{88\ 60.485(g)}{60.485(g)}$  and  $\frac{60.485a(g)}{60.485a(g)}$ .

(105) ASTM D2584-68(Reapproved 1985), Standard Test Method for Ignition Loss of Cured Reinforced Resins, IBR approved for <u>§ 60.685(c)</u>.

(106) ASTM D2584-94, Standard Test Method for Ignition Loss of Cured Reinforced Resins, IBR approved for <u>§ 60.685(c)</u>.

(107) ASTM D2597-94 (Reapproved 1999), Standard Test Method for Analysis of Demethanized Hydrocarbon Liquid Mixtures Containing Nitrogen and Carbon Dioxide by Gas Chromatography, IBR approved for <u>§ 60.335(b)</u>.

(108) ASTM D2622-87, Standard Test Method for Sulfur in Petroleum Products by Wavelength Dispersive X-Ray Fluorescence Spectrometry, IBR approved for  $\frac{88}{60.106(j)}$  and  $\frac{60.335(b)}{60.335(b)}$ .

(109) ASTM D2622-94, Standard Test Method for Sulfur in Petroleum Products by Wavelength Dispersive X-Ray Fluorescence Spectrometry, IBR approved for  $\frac{88}{60.106(j)}$  and  $\frac{60.335(b)}{60.335(b)}$ .

(110) ASTM D2622-98, Standard Test Method for Sulfur in Petroleum Products by Wavelength Dispersive X-Ray Fluorescence Spectrometry, IBR approved for  $\frac{88}{60.106(j)}$  and  $\frac{60.335(b)}{60.335(b)}$ .

(111) ASTM D2622-05, Standard Test Method for Sulfur in Petroleum Products by Wavelength Dispersive X-Ray Fluorescence Spectrometry, IBR approved for  $\S$  60.4415(a).

(112) ASTM D2697-22, Standard Test Method for Volume Nonvolatile Matter in Clear or Pigmented Coatings, Approved July 1, 2022; IBR approved for  $\underline{\$\$} \underbrace{60.393a(g); 60.723(b); 60.724(a); 60.725(b); 60.723a(b); 60.724a(a); 60.725a(b)}_{60.725a(b)}$ .

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(113) ASTM D2879-83, Test Method for Vapor Pressure-Temperature Relationship and Initial Decomposition Temperature of Liquids by Isoteniscope, approved 1983; IBR approved for <u>§§ 60.111b(f)</u>; <u>60.116b(e)</u> and <u>(f)</u>; <u>60.485(e)</u>; <u>60.485</u>a(e); 60.5403b(d); 60.5406c(d).

(114) ASTM D2879-96, Test Method for Vapor Pressure-Temperature Relationship and Initial Decomposition Temperature of Liquids by Isoteniscope, approved 1996; IBR approved for  $\underline{\$\$ 60.111b(f)}$ ;  $\underline{60.116b(e)}$  and  $\underline{(f)}$ ;  $\underline{60.485(e)}$ ;  $\underline{60.485}a(e)$ ;  $\underline{60.5403b(d)}$ ;  $\underline{60.5406c(d)}$ .

(115) ASTM D2879-97, Test Method for Vapor Pressure-Temperature Relationship and Initial Decomposition Temperature of Liquids by Isoteniscope, approved 1997; IBR approved for <u>§§ 60.111b(f)</u>; <u>60.116b(e)</u> and <u>(f)</u>; <u>60.485(e)</u>; <u>60.485</u>a(e); 60.5403b(d); 60.5406c(d).

(116) ASTM D2879-23, Standard Test Method for Vapor Pressure-Temperature Relationship and Initial Decomposition Temperature of Liquids by Isoteniscope, approved December 1, 2019; IBR approved for <u>§ 60.485b(e)</u>.

(117) ASTM D2880-78, Standard Specification for Gas Turbine Fuel Oils, IBR approved for  $\frac{\&\& 60.111(b)}{60.111a(b)}$ , and  $\frac{60.335(d)}{60.335(d)}$ .

(118) ASTM D2880-96, Standard Specification for Gas Turbine Fuel Oils, IBR approved for  $\frac{\$\$ 60.111(b)}{60.111a(b)}$ , and  $\frac{60.335(d)}{60.335(d)}$ .

(119) ASTM D2908-74, Standard Practice for Measuring Volatile Organic Matter in Water by Aqueous-Injection Gas Chromatography, IBR approved for  $\S 60.564(j)$ .

(120) ASTM D2908-91, Standard Practice for Measuring Volatile Organic Matter in Water by Aqueous-Injection Gas Chromatography, IBR approved for  $\S 60.564(j)$ .

(121) ASTM D2986-71, Standard Method for Evaluation of Air, Assay Media by the Monodisperse DOP (Dioctyl Phthalate) Smoke Test, IBR approved for appendix A-3 to part 60: Method 5, <u>Section 7.1.1</u>; appendix A-5 to part 60: Method 12, <u>Section 7.1.1</u>; and Method 13A, <u>Section 7.1.12</u>.

(122) ASTM D2986-78, Standard Method for Evaluation of Air, Assay Media by the Monodisperse DOP (Dioctyl Phthalate) Smoke Test, IBR approved for appendix A-3 to part 60: Method 5, <u>Section 7.1.1</u>; appendix A-5 to part 60: Method 12, <u>Section 7.1.1</u>; and Method 13A, <u>Section 7.1.12</u>.

(123) ASTM D2986-95a, Standard Method for Evaluation of Air, AssaMedia by the Monodisperse DOP (Dioctyl Phthalate) Smoke Test, IBR approved for appendix A-3 to part 60: Method 5, <u>Section 7.1.1</u>; appendix A-5 to part 60: Method 12, <u>Section 7.1.1</u>; and Method 13A, <u>Section 7.1.12</u>.

(124) ASTM D3173-73, Standard Test Method for Moisture in the Analysis Sample of Coal and Coke, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(125) ASTM D3173-87, Standard Test Method for Moisture in the Analysis Sample of Coal and Coke, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(126) ASTM D3176-74, Standard Method for Ultimate Analysis of Coal and Coke, IBR approved for  $\S 60.45(f)(5)(i)$  and appendix A-7 to part 60: Method 19, Section 12.3.2.3.

(127) ASTM D3176-89, Standard Method for Ultimate Analysis of Coal and Coke, IBR approved for  $\frac{60.45(f)(5)(i)}{12.3.2.3}$  and appendix A-7 to part 60: Method 19, Section 12.3.2.3.

(128) ASTM D3177-75, Standard Test Method for Total Sulfur in the Analysis Sample of Coal and Coke, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(129) ASTM D3177-89, Standard Test Method for Total Sulfur in the Analysis Sample of Coal and Coke, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(130) ASTM D3178-73 (Reapproved 1979), Standard Test Methods for Carbon and Hydrogen in the Analysis Sample of Coal and Coke, IBR approved for  $\frac{60.45(f)}{10}$ .

(131) ASTM D3178-89, Standard Test Methods for Carbon and Hydrogen in the Analysis Sample of Coal and Coke, IBR approved for  $\frac{60.45(f)}{10}$ .

(132) ASTM D3246-81, Standard Test Method for Sulfur in Petroleum Gas by Oxidative Microcoulometry, IBR approved for <u>§ 60.335(b)</u>.

(133) ASTM D3246-92, Standard Test Method for Sulfur in Petroleum Gas by Oxidative Microcoulometry, IBR approved for <u>§ 60.335(b)</u>.

(134) ASTM D3246-96, Standard Test Method for Sulfur in Petroleum Gas by Oxidative Microcoulometry, IBR approved for <u>§ 60.335(b)</u>.

(135) ASTM D3246-05, Standard Test Method for Sulfur in Petrolum Gas by Oxidative Microcoulometry, IBR approved for  $\frac{60.4415(a)(1)}{2}$ .

(136) ASTM D3270-73T, Standard Test Methods for Analysis for Fluoride Content of the Atmosphere and Plant Tissues (Semiautomated Method), IBR approved for appendix A-5 to part 60: Method 13A, <u>Section 16.1</u>.

(137) ASTM D3270-80, Standard Test Methods for Analysis for Fluoride Content of the Atmosphere and Plant Tissues (Semiautomated Method), IBR approved for appendix A-5 to part 60: Method 13A, <u>Section 16.1</u>.

(138) ASTM D3270-91, Standard Test Methods for Analysis for Fluoride Content of the Atmosphere and Plant Tissues (Semiautomated Method), IBR approved for appendix A-5 to part 60: Method 13A, <u>Section 16.1</u>.

(139) ASTM D3270-95, Standard Test Methods for Analysis for Fluoride Content of the Atmosphere and Plant Tissues (Semiautomated Method), IBR approved for appendix A-5 to part 60: Method 13A, <u>Section 16.1</u>.

(140) ASTM D3286-85, Standard Test Method for Gross Calorific Value of Coal and Coke by the Isoperibol Bomb Calorimeter, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(141) ASTM D3286-96, Standard Test Method for Gross Calorific Value of Coal and Coke by the Isoperibol Bomb Calorimeter, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(142) ASTM D3370-76, Standard Practices for Sampling Water, IBR approved for § 60.564(j).

(143) ASTM D3370-95a, Standard Practices for Sampling Water, IBR approved for § 60.564(j).

(144) ASTM D3588-98 (Reapproved 2003), Standard Practice for Calculating Heat Value, Compressibility Factor, and Relative Density of Gaseous Fuels, approved May 10, 2003; IBR approved for <u>§§</u> 60.107a(d); 60.5413(d); 60.5413a(d); 60.5413b(d); 60.5413c(d).

(145) ASTM D3699-08, Standard Specification for Kerosine, including Appendix X1, (Approved September 1, 2008); IBR approved for <u>§§ 60.41b</u>; <u>60.41c</u>; <u>60.5580</u>; <u>60.5580a</u>.

(146) ASTM D3792-79, Standard Test Method for Water Content of Water-Reducible Paints by Direct Injection into a Gas Chromatograph, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.3</u>.

(147) ASTM D3792-91, Standard Test Method for Water Content of Water-Reducible Paints by Direct Injection into a Gas Chromatograph, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.3</u>.

(148) ASTM D4017-81, Standard Test Method for Water in Paints and Paint Materials by the Karl Fischer Titration Method, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.4</u>.

(149) ASTM D4017-90, Standard Test Method for Water in Paints and Paint Materials by the Karl Fischer Titration Method, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.4</u>.

(150) ASTM D4017-96a, Standard Test Method for Water in Paints and Paint Materials by the Karl Fischer Titration Method, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.4</u>.

(151) ASTM D4057-81, Standard Practice for Manual Sampling of Petroleum and Petroleum Products, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(152) ASTM D4057-95, Standard Practice for Manual Sampling of Petroleum and Petroleum Products, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.3</u>.

(153) ASTM D4057-95 (Reapproved 2000), Standard Practice for Manual Sampling of Petroleum and Petroleum Products, IBR approved for <u>§ 60.4415(a)</u>.

# NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(154) ASTM D4084-82, Standard Test Method for Analysis of Hydrogen Sulfide in Gaseous Fuels (Lead Acetate Reaction Rate Method), IBR approved for  $\frac{60.334(h)}{1000}$ .

(155) ASTM D4084-94, Standard Test Method for Analysis of Hydrogen Sulfide in Gaseous Fuels (Lead Acetate Reaction Rate Method), IBR approved for  $\S 60.334(h)$ .

(156) ASTM D4084-05, Standard Test Method for Analysis of Hydrogen Sulfide in Gaseous Fuels (Lead Acetate Reaction Rate Method), IBR approved for  $\frac{\$\$ 60.4360}{60.4415(a)}$  and  $\frac{60.4415(a)}{60.4415(a)}$ .

(157) ASTM D4177-95, Standard Practice for Automatic Sampling of Petroleum and Petroleum Products, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.2.1</u>.

(158) ASTM D4177-95 (Reapproved 2000), Standard Practice for Automatic Sampling of Petroleum and Petroleum Products, IBR approved for  $\frac{\$ 60.4415(a)}{100}$ .

(159) ASTM D4239-85, Standard Test Methods for Sulfur in the Analysis Sample of Coal and Coke Using High Temperature Tube Furnace Combustion Methods, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(160) ASTM D4239-94, Standard Test Methods for Sulfur in the Analysis Sample of Coal and Coke Using High Temperature Tube Furnace Combustion Methods, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(161) ASTM D4239-97, Standard Test Methods for Sulfur in the Analysis Sample of Coal and Coke Using High Temperature Tube Furnace Combustion Methods, IBR approved for appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(162) ASTM D4294-02, Standard Test Method for Sulfur in Petroleum and Petroleum Products by Energy-Dispersive X-Ray Fluorescence Spectrometry, IBR approved for  $\frac{60.335(b)}{2}$ .

(163) ASTM D4294-03, Standard Test Method for Sulfur in Petroleum and Petroleum Products by Energy-Dispersive X-Ray Fluorescence Spectrometry, IBR approved for  $\frac{60.4415(a)}{2}$ .

(164) ASTM D4442-84, Standard Test Methods for Direct Moisture Content Measurement in Wood and Wood-base Materials, IBR approved for appendix A-8 to part 60: Method 28, <u>Section 16.1.1</u>.

(165) ASTM D4442-92, Standard Test Methods for Direct Moisture Content Measurement in Wood and Wood-base Materials, IBR approved for appendix A-8 to part 60: Method 28, <u>Section 16.1.1</u>.

(166) ASTM D4444-92, Standard Test Methods for Use and Calibration of Hand-Held Moisture Meters, IBR approved for appendix A-8 to part 60: Method 28, <u>Section 16.1.1</u>.

(167) ASTM D4457-85 (Reapproved 1991), Test Method for Determination of Dichloromethane and 1,1,1-Trichloroethane in Paints and Coatings by Direct Injection into a Gas Chromatograph, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.5</u>.

(168) ASTM D4468-85 (Reapproved 2000), Standard Test Method for Total Sulfur in Gaseous Fuels by Hydrogenolysis and Rateometric Colorimetry, IBR approved for  $\frac{\$\ 60.335(b)}{\$\ 60.335(b)}$  and  $\frac{60.4415(a)}{\$\ 60.335(b)}$ .

(169) ASTM D4468-85 (Reapproved 2006), Standard Test Method for Total Sulfur in Gaseous Fuels by Hydrogenolysis and Rateometric Colorimetry, (Approved June 1, 2006), IBR approved for  $\frac{60.107a(e)}{2}$ .

(170) ASTM D4629-02, Standard Test Method for Trace Nitrogen in Liquid Petroleum Hydrocarbons by Syringe/Inlet Oxidative Combustion and Chemiluminescence Detection, IBR approved for  $\frac{\$\$ 60.49b(e)}{\$\$ 60.49b(e)}$  and  $\frac{60.335(b)}{\$\$}$ .

(171) ASTM D4809-95, Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter (Precision Method), IBR approved for <u>§§ 60.18(f)</u>, <u>60.485(g)</u>, <u>60.485a(g)</u>, <u>60.564(f)</u>, <u>60.614(d)</u>, <u>60.664(e)</u>, and <u>60.704(d)</u>.

(172) ASTM D4809-06, Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter (Precision Method), (Approved December 1, 2006), IBR approved for  $\frac{\S 60.107a(d)}{S}$ .

(173) ASTM D4809-18, Standard Test Method for Heat of Combustion of Liquid Hydrocarbon Fuels by Bomb Calorimeter (Precision Method), approved July 1, 2018; IBR approved for  $\frac{60.485b(g)}{2}$ .

(174) ASTM D4810-88 (Reapproved 1999), Standard Test Method for Hydrogen Sulfide in Natural Gas Using Length of Stain Detector Tubes, IBR approved for  $\frac{\&\& 60.4360}{60.4415(a)}$  and  $\frac{60.4415(a)}{60.4415(a)}$ .

(175) ASTM D4840-99(2018)e1 Standard Guide for Sample Chain-of-Custody Procedures, approved August 2018; IBR approved for Appendix A-7: Method 23.

(176) ASTM D4891-89 (Reapproved 2006), Standard Test Method for Heating Value of Gases in Natural Gas Range by Stoichiometric Combustion, approved June 1, 2006; IBR approved for <u>§§</u> <u>60.107a(d)</u>; <u>60.5413(d)</u>; <u>60.5413a(d)</u>; <u>60.5413b(d)</u>; <u>60.5413c(d)</u>.

(177) ASTM D5066-91, Standard Test Method for Determination of the Transfer Efficiency Under Production Conditions for Spray Application of Automotive Paints—Weight Basis, Approved June 1, 2017; IBR approved for  $\S 60.393a(h)$ .

(178) ASTM D5087-02 (Reapproved 2021), Standard Test Method for Determining Amount of Volatile Organic Compound (VOC) Released from Solventborne Automotive Coatings and Available for Removal in a VOC Control Device (Abatement), Approved February 1, 2021; IBR approved for <u>§ 60.397a(e)</u>; appendix A to subpart MMa.

(179) ASTM D5287-97 (Reapproved 2002), Standard Practice for Automatic Sampling of Gaseous Fuels, IBR approved for  $\frac{60.4415(a)}{2}$ .

(180) ASTM D5403-93, Standard Test Methods for Volatile Content of Radiation Curable Materials, IBR approved for appendix A-7 to part 60: Method 24, <u>Section 6.6</u>.

(181) ASTM D5453-00, Standard Test Method for Determination of Total Sulfur in Light Hydrocarbons, Motor Fuels and Oils by Ultraviolet Fluorescence, IBR approved for  $\frac{60.335(b)}{2}$ .

(182) ASTM D5453-05, Standard Test Method for Determination of Total Sulfur in Light Hydrocarbons, Motor Fuels and Oils by Ultraviolet Fluorescence, IBR approved for  $\frac{60.4415(a)}{2}$ .

(183) ASTM D5504-01, Standard Test Method for Determination of Sulfur Compounds in Natural Gas and Gaseous Fuels by Gas Chromatography and Chemiluminescence, IBR approved for  $\frac{\&\& 60.334(h)}{\&\& 60.334(h)}$  and  $\frac{60.4360}{\&\& 60.4360}$ .

(184) ASTM D5504-08, Standard Test Method for Determination of Sulfur Compounds in Natural Gas and Gaseous Fuels by Gas Chromatography and Chemiluminescence, (Approved June 15, 2008), IBR approved for  $\frac{88}{60.107a(e)}$  and  $\frac{60.5413(d)}{60.5413(d)}$ .

(185) ASTM D5623-19, Standard Test Method for Sulfur Compounds in Light Petroleum Liquids by Gas Chromatography and Sulfur Selective Detection, (Approved July 1, 2019); IBR approved for  $\frac{60.4415(a)}{2}$ .

(186) ASTM D5762-02, Standard Test Method for Nitrogen in Petroleum and Petroleum Products by Boat-Inlet Chemiluminescence, IBR approved for  $\S 60.335(b)$ .

(187) ASTM D5865-98, Standard Test Method for Gross Calorific Value of Coal and Coke, IBR approved for <u>§§</u> <u>60.45(f)</u> and <u>60.46(c)</u>, and appendix A-7 to part 60: Method 19, <u>Section 12.5.2.1.3</u>.

(188) ASTM D5865-10, Standard Test Method for Gross Calorific Value of Coal and Coke, (Approved January 1, 2010), IBR approved for <u>§§ 60.45(f)</u>, <u>60.46(c)</u>, and appendix A-7 to part 60: Method 19, <u>section 12.5.2.1.3</u>.

(189) ASTM D5965-02 (Reapproved 2013), Standard Test Methods for Specific Gravity of Coating Powders, Approved June 1, 2013; IBR approved for <u>§ 60.393a(f)</u>.

(190) ASTM D6093-97 (Reapproved 2016), Standard Test Method for Percent Volume Nonvolatile Matter in Clear or Pigmented Coatings Using a Helium Gas Pycnometer, Approved December 1, 2016; IBR approved for <u>§§</u> <u>60.393a(g)</u>; <u>60.723(b)</u>; <u>60.724(a)</u>; <u>60.725(b)</u>; <u>60.723a(b)</u>; <u>60.725a(b)</u>.

(191) ASTM D6216-20, Standard Practice for Opacity Monitor Manufacturers to Certify Conformance with Design and Performance Specifications, approved September 1, 2020; IBR approved for appendix B to part 60.

(192) ASTM D6228-98, Standard Test Method for Determination of Sulfur Compounds in Natural Gas and Gaseous Fuels by Gas Chromatography and Flame Photometric Detection, IBR approved for  $\frac{\delta}{60.334(h)}$ .

(193) ASTM D6228-98 (Reapproved 2003), Standard Test Method for Determination of Sulfur Compounds in Natural Gas and Gaseous Fuels by Gas Chromatography and Flame Photometric Detection, IBR approved for  $\frac{\$\$ 60.4360}{\$\$ 60.4360}$  and  $\frac{60.4415}{\$\$ 60.4360}$ .

(194) ASTM D6266-00a (Reapproved 2017), Standard Test Method for Determining the Amount of Volatile Organic Compound (VOC) Released From Waterborne Automotive Coatings and Available for Removal in a VOC Control Device (Abatement), Approved July 1, 2017; IBR approved for <u>§ 60.397a(e)</u>.

(195) ASTM D6348-03, Standard Test Method for Determination of Gaseous Compounds by Extractive Direct Interface Fourier Transform Infrared (FTIR) Spectroscopy, (Approved October 1, 2003), IBR approved for  $\S$  60.73a(b), table 7 to subpart IIII, table 2 to subpart JJJJ, and  $\S$  60.4245(d).

(196) ASTM D6348-12e1, Standard Test Method for Determination of Gaseous Compounds by Extractive Direct Interface Fourier Transform Infrared (FTIR) Spectroscopy, approved February 1, 2012; IBR approved for <u>§ 60.5413c(b)</u>.

(197) ASTM D6366-99, Standard Test Method for Total Trace Nitrogen and Its Derivatives in Liquid Aromatic Hydrocarbons by Oxidative Combustion and Electrochemical Detection, IBR approved for  $\S 60.335(b)(9)$ .

(198) ASTM D6377-20, Standard Test Method for Determination of Vapor Pressure of Crude Oil: VPCR<sub>X</sub> (Expansion Method), (Approved June 1, 2020); IBR approved for  $\frac{\& 60.113c}{\& 60.113c}$ .

(199) ASTM-D6378-22, Standard Test Method for Determination of Vapor Pressure (VPX) of Petroleum Products, Hydrocarbons, and Hydrocarbon-Oxygenate Mixtures (Triple Expansion Method), (Approved July 1, 2022); IBR approved for <u>§ 60.113c</u>.

(200) ASTM D6420-99 (Reapproved 2004), Standard Test Method for Determination of Gaseous Organic Compounds by Direct Interface Gas Chromatography-Mass Spectrometry, (Approved October 1, 2004), IBR approved for  $\S$  60.107a(d) and table 2 to subpart JJJJ.

(201) ASTM D6420-18, Standard Test Method for Determination of Gaseous Organic Compounds by Direct Interface Gas Chromatography-Mass Spectrometry, approved November 1, 2018, IBR approved for <u>§§</u> <u>60.485a(g)</u>; <u>60.485b(g)</u>; <u>60.611a</u>; <u>60.614(b)</u> and <u>(e)</u>; <u>60.614</u>a(b) and (e), 60.664(b) and (e); 60.664a(b) and (f); 60.700(c); 60.704(b) (d), and (h); 60.705(l); 60.704a(b) and (f).

(202) ASTM D6522-00, Standard Test Method for Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Concentrations in Emissions from Natural Gas-Fired Reciprocating Engines, Combustion Turbines, Boilers, and Process Heaters Using Portable Analyzers, IBR approved for  $\S$  60.335(a).

(203) ASTM D6522-00 (Reapproved 2005), Standard Test Method for Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Concentrations in Emissions from Natural Gas-Fired Reciprocating Engines, Combustion Turbines, Boilers, and Process Heaters Using Portable Analyzers, (Approved October 1, 2005), IBR approved for table 2 to subpart JJJJ, <u>§§</u> <u>60.5413(b)</u> and <u>(d)</u>, and <u>60.5413(a)</u>.

(204) ASTM D6522-11 Standard Test Method for Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Concentrations in Emissions from Natural Gas-Fired Reciprocating Engines, Combustion Turbines, Boilers, and Process Heaters Using Portable Analyzers (Approved December 1, 2011), IBR approved for <u>§ 60.37f(a)</u>, <u>60.766(a)</u>.

(205) ASTM D6522-20, Standard Test Method for Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Concentrations in Emissions from Natural Gas-Fired Reciprocating Engines, Combustion Turbines, Boilers, and Process Heaters Using Portable Analyzers, approved June 1, 2020; IBR approved for <u>§§ 60.5413b(b)</u>; <u>60.5413c(b)</u>.

(206) ASTM D6667-01, Standard Test Method for Determination of Total Volatile Sulfur in Gaseous Hydrocarbons and Liquefied Petroleum Gases by Ultraviolet Fluorescence, IBR approved for  $\frac{60.335(b)}{2}$ .

(207) ASTM D6667-04, Standard Test Method for Determination of Total Volatile Sulfur in Gaseous Hydrocarbons and Liquefied Petroleum Gases by Ultraviolet Fluorescence, IBR approved for  $\frac{\& 60.4415(a)}{\& 60.4415(a)}$ .

(208) ASTM D6751-11b, Standard Specification for Biodiesel Fuel Blend Stock (B100) for Middle Distillate Fuels, including Appendices X1 through X3, (Approved July 15, 2011), IBR approved for <u>§§ 60.41b</u>, <u>60.41c</u>, <u>60.5580</u>, and <u>60.5580a</u>.

(209) ASTM D6784-02, Standard Test Method for Elemental, Oxidized, Particle-Bound and Total Mercury in Flue Gas Generated from Coal-Fired Stationary Sources (Ontario Hydro Method), IBR approved for <u>§ 60.56c(b)</u> and appendix B to part 60: Performance Specification 12A, <u>Section 8.6.2</u>.

(210) ASTM D6784-02 (Reapproved 2008), Standard Test Method for Elemental, Oxidized, Particle-Bound and Total Mercury in Flue Gas Generated from Coal-Fired Stationary Sources (Ontario Hydro Method), approved April 1, 2008; IBR approved for <u>§ 60.56c(b)</u>.

(211) ASTM D6784-16, Standard Test Method for Elemental, Oxidized, Particle-Bound and Total Mercury in Flue Gas Generated from Coal-Fired Stationary Sources (Ontario Hydro Method), approved March 1, 2016; IBR approved for appendix B to part 60.

(212) ASTM D6911-15 Standard Guide for Packaging and Shipping Environmental Samples for Laboratory Analysis, approved January 15, 2015; IBR approved for Appendix A-7: Method 23; Appendix A-8: Method 30B.

(213) ASTM D7039-15a, Standard Test Method for Sulfur in Gasoline, Diesel Fuel, Jet Fuel, Kerosine, Boideisel, Biodiesel Blends, and Gasoline-Ethanol Blends by Monochromatic Wavelength Dispersive X-ray Fluorescence Spectrometry, (Approved July 1, 2015); IBR approved for <u>§ 60.4415(a)</u>.

(214) ASTM D7467-10, Standard Specification for Diesel Fuel Oil, Biodiesel Blend (B6 to B20), including Appendices X1 through X3, (Approved August 1, 2010), IBR approved for <u>§§ 60.41b</u>, <u>60.41c</u>, <u>60.5580</u>, and <u>60.5580a</u>.

(215) ASTM D7520-16, Standard Test Method for Determining the Opacity of a Plume in the Outdoor Ambient Atmosphere, approved April 1, 2016; IBR approved for <u>§§</u>

 $\frac{60.123(c)(6)}{60.123(c)(6)}; \frac{60.123(c)(6)(i)}{60.123(c)(6)(ii)}; \frac{60.123(c)(6)(v)}{60.123(c)(6)(v)}; \frac{60.123a(c)(6)(ii)}{60.123a(c)(6)(ii)(A)}; \frac{60.123a(c)(6)(ii)(B)}{60.273(c)}; \frac{60.271(a)}{60.273(c)}; \frac{60.271(a)}{60.273(c)}; \frac{60.272(a)}{60.273(c)}; \frac{60.273(a)}{60.273(c)}; \frac{60.272(a)}{60.273(c)}; \frac{60.272(a)}{60.273(c)}; \frac{60.272(a)}{60.273(c)}; \frac{60.273(a)}{60.273(c)}; \frac{60.272(a)}{60.273(c)}; \frac{60.273(a)}{60.273(c)}; \frac{60.273$ 

(216) ASTM E168-67, General Techniques of Infrared Quantitative Analysis, IBR approved for  $\underline{\$\$}$  <u>60.485a(d)</u>, <u>60.593(b)</u>, <u>60.593a(b)</u>, and <u>60.632(f)</u>.

(217) ASTM E168-77, General Techniques of Infrared Quantitative Analysis, IBR approved for  $\underline{\$\$}$  <u>60.485a(d)</u>, <u>60.593(b)</u>, <u>60.593a(b)</u>, and <u>60.632(f)</u>.

(218) ASTM E168-92, General Techniques of Infrared Quantitative Analysis, IBR approved for <u>§§</u> <u>60.485a(d)</u>, <u>60.593(b)</u>, <u>60.593a(b)</u>, <u>60.632(f)</u>, <u>60.5400a</u>, <u>60.5400a(f)</u>.

(219) ASTM E168-16 (Reapproved 2023), Standard Practices for General Techniques of Infrared Quantitative Analysis, approved January 1, 2023; IBR approved for <u>§ 60.485b(d)</u>.

(220) ASTM E169-63, General Techniques of Ultraviolet Quantitative Analysis, IBR approved for  $\underline{\$\$}$  60.485a(d), 60.593(b), 60.593a(b), and 60.632(f).

(221) ASTM E169-77, General Techniques of Ultraviolet Quantitative Analysis, IBR approved for <u>§§ 60.485a(d)</u>, <u>60.593(b)</u>, and <u>60.593a(b)</u>, <u>60.632(f)</u>.

(222) ASTM E169-93, General Techniques of Ultraviolet Quantitative Analysis, (Approved May 15, 1993), IBR approved for  $\underline{\$\$ 60.485a(d), 60.593(b), 60.593a(b), 60.632(f), 60.5400(f), and 60.5400a(f).$ 

(223) ASTM E169-16 (Reapproved 2022), Standard Practices for General Techniques of Ultraviolet-Visible Quantitative Analysis, approved November 1, 2022; IBR approved for <u>§ 60.485b(d)</u>.

(224) ASTM E260-73, General Gas Chromatography Procedures, IBR approved for  $\frac{60.593(b)}{60.593(b)}$ ,  $\frac{60.593(b)}{60.593(b)}$ 

(225) ASTM E260-91, General Gas Chromatography Procedures, (IBR approved for  $\frac{\&\& 60.485a(d)}{60.593(b)}$ ,  $\frac{60.593(b)}{60.593a(b)}$ , and  $\frac{60.632(f)}{60.632(f)}$ .

(226) ASTM E260-96, General Gas Chromatography Procedures, approved April 10, 1996; IBR approved for <u>§§</u> <u>60.485a(d)</u>, <u>60.593(b)</u>, <u>60.593a(b)</u>, <u>60.632(f)</u>, <u>60.5400(f)</u>, <u>60.5400a(f)</u>, <u>60.5406(b)</u>, <u>60.5406a(b)(3)</u>, <u>60.5400b(a)(2)</u>, <u>60.5401b(a)(2)</u>, <u>60.5406b(b)(3)</u>, <u>60.5400b(a)(2)</u>, <u>60.5401b(a)(2)</u>, <u>60.5406b(b)(3)</u>, <u>60.5400b(a)(2)</u>, <u>60.5401b(a)(2)</u>, <u>60.5401b(a)(2)</u>, <u>60.5406b(b)(3)</u>, <u>60.5400b(a)(2)</u>, <u>60.5401b(a)(2)</u>, <u>60.5401b(a)(2)</u>, <u>60.5400b(a)(2)</u>, <u>60.5400b(a)(2)}, <u>60.5400b(a)(2)</u>, <u>60.5400b(a)(2)}, <u>60.5400b(a)(2)</u>, <u>60.5400b(a)(2)</u>, <u>60.5400b(a)(2)}, <u>60.5400b(a)(2)}, <u>60.5400b(a)(2)}, <u>60.5400b(a)(2)}, <u>60.5400b(a)(2)}, <u>60.540</u></u></u></u></u></u></u></u></u></u></u></u></u></u></u></u></u>

(227) ASTM E260-96 (Reapproved 2019), Standard Practice for Packed Column Gas Chromatography, approved September 1, 2029; IBR approved for  $\S 60.485b(d)$ .

(228) ASTM E617-13, Standard Specification for Laboratory Weights and Precision Mass Standards, approved May 1, 2013, IBR approved for appendix A-3: Methods 4, 5, 5H, 5I, and appendix A-8: Method 29.

(229) ASTM E871-82 (Reapproved 2013), Standard Test Method for Moisture Analysis of Particulate Wood Fuels, (Approved August 15, 2013), IBR approved for appendix A-8: method 28R.

(230) ASTM E1584-11, Standard Test Method for Assay of Nitric Acid, (Approved August 1, 2011), IBR approved for <u>§</u> <u>60.73a(c)</u>.

(231) ASTM E2515-11, Standard Test Method for Determination of Particulate Matter Emissions Collected by a Dilution Tunnel, (Approved November 1, 2011), IBR approved for  $\frac{60.534}{2000}$  and  $\frac{60.5476}{2000}$ .

(232) ASTM E2618-13 Standard Test Method for Measurement of Particulate Matter Emissions and Heating Efficiency of Outdoor Solid Fuel-Fired Hydronic Heating Appliances, (Approved September 1, 2013), IBR approved for <u>§ 60.5476</u>.

(233) ASTM E2779-10, Standard Test Method for Determining Particulate Matter Emissions from Pellet Heaters, (Approved October 1, 2010), IBR approved for  $\S$  60.534.

(234) ASTM E2780-10, Standard Test Method for Determining Particulate Matter Emissions from Wood Heaters, (Approved October 1, 2010), IBR approved for appendix A: method 28R.

(235) ASTM UOP539-97, Refinery Gas Analysis by Gas Chromatography, (Copyright 1997), IBR approved for <u>§</u> <u>60.107a(d)</u>.

(i) Association of Official Analytical Chemists, 1111 North 19th Street, Suite 210, Arlington, VA 22209; phone: (301) 927-7077; website: <u>https://www.aoac.org/</u>.

(1) AOAC Method 9, Official Methods of Analysis of the Association of Official Analytical Chemists (AOAC), 11th edition, 1970, pp. 11-12, IBR approved for  $\frac{\$\$ 60.204(b)}{60.214(b)}$ ,  $\frac{60.224(b)}{60.224(b)}$ , and  $\frac{60.234(b)}{60.234(b)}$ .

(2) [Reserved]

(j) CSA Group (CSA) (formerly Canadian Standards Association), 178 Rexdale Boulevard, Toronto, Ontario, Canada; phone: (800) 463-6727; website: <u>https://shop.csa.ca</u>.

(1) CSA B415.1-10, Performance Testing of Solid-fuel-burning Heating Appliances, (March 2010), IBR approved for <u>§§</u> <u>60.534</u>; <u>60.5476</u>.

(2) [Reserved]

(k) U.S. Environmental Protection Agency (EPA), 1200 Pennsylvania Avenue NW, Washington, DC 20460; phone: (202) 272-0167; website: <u>www.epa.gov/aboutepa/forms/contact-epa</u>.

(1) EPA-453/R-08-002, Protocol for Determining the Daily Volatile Organic Compound Emission Rate of Automobile and Light-Duty Truck Primer-Surfacer and Topcoat Operations, September 2008, Office of Air Quality Planning and Standards (OAQPS); IBR approved for <u>§§ 60.393a(e)</u> and <u>(h)</u>; <u>60.395</u>a(k); 60.397a(e); appendix A to subpart MMa.

(2) EPA-454/B-08-002, Quality Assurance Handbook for Air Pollution Measurement Systems; Volume IV: Meteorological Measurements, Version 2.0 (Final), March 2008; IBR approved for appendix K to this part.

(3) EPA-454/R-98-015, Office of Air Quality Planning and Standards (OAQPS), Fabric Filter Bag Leak Detection Guidance, September 1997; IBR approved for <u>§§</u>

<u>60.124(f); 60.124a(f); 60.273(e); 60.273a(e); 60.273b(e); 60.373a(b); 60.2145(r); 60.2710(r); 60.4905(b); 60.5225(b)</u>. (Available from: <u>https://nepis.epa.gov/Exe/ZyPDF.cgi?Dockey=2000D5T6.pdf</u>).

(4) EPA-600/R-12/531, EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards, May 2012; IBR approved for <u>§§ 60.5413(d)</u>; <u>60.5413(d)</u>; <u>60.5413(d)</u>; <u>60.5413(d)</u>; <u>60.5413(d)</u>.

(5) In EPA Publication No. SW-846, Test Methods for Evaluating Solid Waste, Physical/Chemical Methods (Available from: <u>www.epa.gov/hw-sw846/sw-846-compendium</u>):

(i) SW-846-6010D, Inductively Coupled Plasma-Optical Emission Spectrometry, Revision 5, July 2018; IBR approved for appendix A-5 to this part.

(ii) SW-846-6020B, Inductively Coupled Plasma-Mass Spectrometry, Revision 2, July 2014; IBR approved for appendix A-5 to this part.

(l) European Standards (EN), European Committee for Standardization, Management Centre, Avenue Marnix 17, B-1000 Brussels, Belgium; phone: + 32 2 550 08 11; website: <u>https://www.en-standard.eu</u>.

(1) DIN EN 303-5:2012E (EN 303-5), Heating boilers—Part 5: Heating boilers for solid fuels, manually and automatically stoked, nominal heat output of up to 500 kW—Terminology, requirements, testing and marking, (October 2012), IBR approved for <u>§ 60.5476</u>.

(2) [Reserved]

(m) GPA Midstream Association, 6060 American Plaza, Suite 700, Tulsa, OK 74135; phone: (918) 493-3872; website: *www.gpamidstream.org*.

(1) GPA Midstream Standard 2140-17 (GPA 2140-17), Liquefied Petroleum Gas Specifications and Test Methods, (Revised 2017), IBR approved for <u>§ 60.4415(a)</u>.

(2) GPA Midstream Standard 2166-17 (GPA 2166-17), Obtaining Natural Gas Samples for Analysis by Gas Chromatography, (Reaffirmed 2017), IBR approved for  $\S 60.4415(a)$ .

(3) Gas Processors Association Standard 2172-09, Calculation of Gross Heating Value, Relative Density, Compressibility and Theoretical Hydrocarbon Liquid Content for Natural Gas Mixtures for Custody Transfer (2009), IBR approved for  $\S$  <u>60.107a(d)</u>.

(4) GPA Standard 2174-14 (GPA 2174-14), Obtaining Liquid Hydrocarbon Samples for Analysis by Gas Chromatography, (Revised 2014), IBR approved for <u>§ 60.4415(a)</u>.

(5) GPA Standard 2261-19 (GPA 2261-19), Analysis for Natural Gas and Similar Gaseous Mixtures by Gas Chromatography, (Revised 2019), IBR approved for <u>§ 60.4415(a)</u>.

(6) Gas Processors Association Standard 2377-86, Test for Hydrogen Sulfide and Carbon Dioxide in Natural Gas Using Length of Stain Tubes, 1986 Revision, IBR approved for  $\frac{\$\$ 60.105(b)}{\$\$ 60.105(b)}$ ,  $\frac{60.107a(b)}{\$0.334(h)}$ ,  $\frac{60.4360}{\$0.4360}$ , and  $\frac{60.4415(a)}{\$0.4360}$ .

(n) International Organization for Standardization (ISO), 1, ch. de la Voie-Creuse, Case postale 56, CH-1211 Geneva 20, Switzerland; phone: + 41 22 749 01 11; website: <u>www.iso.org</u>.

(1) ISO 8178-4: 1996(E), Reciprocating Internal Combustion Engines—Exhaust Emission Measurement—part 4: Test Cycles for Different Engine Applications, IBR approved for <u>§ 60.4241(b)</u>.

(2) ISO 2314:2009(E), Gas turbines-Acceptance tests, Third edition (December 15, 2009), IBR approved for <u>§§</u> <u>60.5580;</u> <u>60.5580a</u>.

(3) ISO 8316: Measurement of Liquid Flow in Closed Conduits—Method by Collection of the Liquid in a Volumetric Tank (1987-10-01)—First Edition, IBR approved for  $\S 60.107a(d)$ .

(4) ISO 10715:1997(E), Natural gas—Sampling guidelines, (First Edition, June 1, 1997), IBR approved for § 60.4415(a).

(o) National Technical Information Services (NTIS), 5285 Port Royal Road, Springfield, Virginia 22161.

(1) OMB Bulletin No. 93-17: Revised Statistical Definitions for Metropolitan Areas. Office of Management and Budget, June 30, 1993. NTIS No. PB 93-192-664. IBR approved for <u>§ 60.31e</u>.

(2) [Reserved]

(p) North American Electric Reliability Corporation, 1325 G Street NW., Suite 600, Washington, DC 20005-3801, <u>http://www.nerc.com</u>.

(1) North American Electric Reliability Corporation Reliability Standard EOP-002-3, Capacity and Energy Emergencies, updated November 19, 2012, IBR approved for <u>§§ 60.4211(f)</u> and <u>60.4243(d)</u>. Also available online: <u>http://www.nerc.com/files/EOP-002-3\_\_1.pdf</u>.

## (2) [Reserved]

(q) Pacific Lumber Inspection Bureau (formerly West Coast Lumber Inspection Bureau), 1010 South 336th Street #210, Federal Way, WA 98003; phone: (253) 835.3344; website: <u>www.plib.org</u>.

(1) West Coast Lumber Standard Grading Rules No. 16, pages 5-21, 90 and 91, September 3, 1970, revised 1984, IBR approved for appendix A-8 to part 60.

(2) [Reserved]

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(r) Technical Association of the Pulp and Paper Industry (TAPPI), 15 Technology Parkway South, Suite 115, Peachtree Corners, GA 30092; phone (800) 332-8686; website: <u>www.tappi.org</u>.

(1) TAPPI Method T 624 cm-11, (Copyright 2011), IBR approved, for <u>§§ 60.285(d)</u> and <u>60.285a(d)</u>.

(2) [Reserved]

(s) Underwriter's Laboratories, Inc. (UL), 333 Pfingsten Road, Northbrook, IL 60062.

(1) UL 103, Sixth Edition revised as of September 3, 1986, Standard for Chimneys, Factory-built, Residential Type and Building Heating Appliance, IBR approved for appendix A-8 to part 60.

(2) [Reserved]

(t) Water Pollution Control Federation (WPCF), 2626 Pennsylvania Avenue NW., Washington, DC 20037.

(1) Method 209A, Total Residue Dried at 103-105 °C, in Standard Methods for the Examination of Water and Wastewater, 15th Edition, 1980, IBR approved for  $\frac{\$ 60.683(b)}{100}$ .

(2) [Reserved]

[<u>79 FR 11242</u>, Feb. 27, 2014]

## **Editorial Note**

## **Editorial Note:**

For Federal Register citations affecting <u>§ 60.17</u>, see the List of CFR Sections Affected, which appears in the Finding Aids section of the printed volume and at <u>www.govinfo.gov</u>.

## § 60.18 General control device and work practice requirements.

(a) Introduction.

(1) This section contains requirements for control devices used to comply with applicable subparts of <u>40 CFR parts</u> <u>60</u> and <u>61</u>. The requirements are placed here for administrative convenience and apply only to facilities covered by subparts referring to this section.

(2) This section also contains requirements for an alternative work practice used to identify leaking equipment. This alternative work practice is placed here for administrative convenience and is available to all subparts in  $\frac{40 \text{ CFR parts}}{1000 \text{ CFR part}}$  60, 61, 63, and 65 that require monitoring of equipment with a  $\frac{40 \text{ CFR part}}{1000 \text{ CFR part}}$  60, appendix A-7, Method 21 monitor.

(b) Flares. Paragraphs (c) through (f) apply to flares.

(c)

(1) Flares shall be designed for and operated with no visible emissions as determined by the methods specified in paragraph (f), except for periods not to exceed a total of 5 minutes during any 2 consecutive hours.

(2) Flares shall be operated with a flame present at all times, as determined by the methods specified in paragraph (f).

(3) An owner/operator has the choice of adhering to either the heat content specifications in <u>paragraph (c)(3)(ii)</u> of this section and the maximum tip velocity specifications in <u>paragraph (c)(4)</u> of this section, or adhering to the requirements in <u>paragraph (c)(3)(i)</u> of this section.

(i)

(A) Flares shall be used that have a diameter of 3 inches or greater, are nonassisted, have a hydrogen content of 8.0 percent (by volume), or greater, and are designed for and operated with an exit velocity less than 37.2 m/sec (122 ft/sec) and less than the velocity,  $V_{max}$ , as determined by the following equation:

 $V_{max} = (X_{H2} - K_1) * K_2$ 

Where:

V<sub>max</sub> = Maximum permitted velocity, m/sec.

 $K_1 = Constant, 6.0$  volume-percent hydrogen.

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 $K_2 = Constant, 3.9(m/sec)/volume-percent hydrogen.$ 

 $X_{H2}$  = The volume-percent of hydrogen, on a wet basis, as calculated by using the American Society for Testing and Materials (ASTM) Method D1946-77. (Incorporated by reference as specified in § 60.17).

(B) The actual exit velocity of a flare shall be determined by the method specified in paragraph (f)(4) of this section.

(ii) Flares shall be used only with the net heating value of the gas being combusted being 11.2 MJ/scm (300 Btu/scf) or greater if the flare is steam-assisted or air-assisted; or with the net heating value of the gas being combusted being 7.45 MJ/scm (200 Btu/scf) or greater if the flare is nonassisted. The net heating value of the gas being combusted shall be determined by the methods specified in paragraph (f)(3) of this section.

(4)

(i) Steam-assisted and nonassisted flares shall be designed for and operated with an exit velocity, as determined by the methods specified in <u>paragraph (f)(4)</u> of this section, less than 18.3 m/sec (60 ft/sec), except as provided in <u>paragraphs (c)(4)</u> (ii) and (iii) of this section.

(ii) Steam-assisted and nonassisted flares designed for and operated with an exit velocity, as determined by the methods specified in paragraph (f)(4), equal to or greater than 18.3 m/sec (60 ft/sec) but less than 122 m/sec (400 ft/sec) are allowed if the net heating value of the gas being combusted is greater than 37.3 MJ/scm (1,000 Btu/scf).

(iii) Steam-assisted and nonassisted flares designed for and operated with an exit velocity, as determined by the methods specified in paragraph (f)(4), less than the velocity,  $V_{max}$ , as determined by the method specified in paragraph (f)(5), and less than 122 m/sec (400 ft/sec) are allowed.

(5) Air-assisted flares shall be designed and operated with an exit velocity less than the velocity,  $V_{max}$ , as determined by the method specified in paragraph (f)(6).

(6) Flares used to comply with this section shall be steam-assisted, air-assisted, or nonassisted.

(d) Owners or operators of flares used to comply with the provisions of this subpart shall monitor these control devices to ensure that they are operated and maintained in conformance with their designs. Applicable subparts will provide provisions stating how owners or operators of flares shall monitor these control devices.

(e) Flares used to comply with provisions of this subpart shall be operated at all times when emissions may be vented to them.

(f)

(1) Method 22 of appendix A to this part shall be used to determine the compliance of flares with the visible emission provisions of this subpart. The observation period is 2 hours and shall be used according to Method 22.

(2) The presence of a flare pilot flame shall be monitored using a thermocouple or any other equivalent device to detect the presence of a flame.

(3) The net heating value of the gas being combusted in a flare shall be calculated using the following equation:



where:

 $H_T$  = Net heating value of the sample, MJ/scm; where the net enthalpy per mole of offgas is based on combustion at 25 °C and 760 mm Hg, but the standard temperature for determining the volume corresponding to one mole is 20 °C;

# $K = Constant, -7 \quad (\frac{1}{ppm}) \quad (\frac{g \text{ mole}}{scm}) \quad (\frac{MJ}{kcal})$

# where the standard temperature for $(\frac{g \text{ mole}}{scm})$ is 20°C;

 $C_i$  = Concentration of sample component i in ppm on a wet basis, as measured for organics by Reference Method 18 and measured for hydrogen and carbon monoxide by ASTM D1946-77 or 90 (Reapproved 1994) (Incorporated by reference as specified in § 60.17); and

 $H_i$  = Net heat of combustion of sample component i, kcal/g mole at 25 °C and 760 mm Hg. The heats of combustion may be determined using ASTM D2382-76 or 88 or D4809-95 (incorporated by reference as specified in § 60.17) if published values are not available or cannot be calculated.

(4) The actual exit velocity of a flare shall be determined by dividing the volumetric flowrate (in units of standard temperature and pressure), as determined by Reference Methods 2, 2A, 2C, or 2D as appropriate; by the unobstructed (free) cross sectional area of the flare tip.

(5) The maximum permitted velocity,  $V_{max}$ , for flares complying with paragraph (c)(4)(iii) shall be determined by the following equation.

 $Log_{10}(V_{max}) = (H_T + 28.8)/31.7$ 

 $V_{max} = Maximum permitted velocity, M/sec$ 

28.8 = Constant

31.7 = Constant

 $H_T$  = The net heating value as determined in paragraph (f)(3).

(6) The maximum permitted velocity,  $V_{max}$ , for air-assisted flares shall be determined by the following equation.

 $V_{max} = 8.706 + 0.7084 (H_T)$ 

 $V_{max}$  = Maximum permitted velocity, m/sec

8.706 = Constant

0.7084 = Constant

 $H_T$  = The net heating value as determined in paragraph (f)(3).

(g) Alternative work practice for monitoring equipment for leaks. Paragraphs (g), (h), and (i) of this section apply to all equipment for which the applicable subpart requires monitoring with a 40 CFR part 60, appendix A-7, Method 21 monitor, except for closed vent systems, equipment designated as leakless, and equipment identified in the applicable subpart as having no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background. An owner or operator may use an optical gas imaging instrument instead of a 40 CFR part 60, appendix A-7, Method 21 monitor. Requirements in the existing subparts that are specific to the Method 21 instrument do not apply under this section. All other requirements in the applicable subpart that are not addressed in paragraphs (g), (h), and (i) of this section apply to this standard. For example, equipment specification requirements, and non-Method 21 instrument recordkeeping and reporting requirements in the applicable subpart continue to apply. The terms defined in paragraphs (g), (h), and (i) of this section have meanings that are specific to the alternative work practice standard in paragraphs (g), (h), and (i) of this section.

(1) Applicable subpart means the subpart in <u>40 CFR parts 60</u>, <u>61</u>, <u>63</u>, or <u>65</u> that requires monitoring of equipment with a <u>40 CFR part 60</u>, <u>appendix A</u>-7, Method 21 monitor.

(2) *Equipment* means pumps, valves, pressure relief valves, compressors, open-ended lines, flanges, connectors, and other equipment covered by the applicable subpart that require monitoring with a <u>40 CFR part 60, appendix A</u>-7, Method 21 monitor.

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(3) *Imaging* means making visible emissions that may otherwise be invisible to the naked eye.

(4) *Optical gas imaging instrument* means an instrument that makes visible emissions that may otherwise be invisible to the naked eye.

(5) Repair means that equipment is adjusted, or otherwise altered, in order to eliminate a leak.

(6) *Leak* means:

(i) Any emissions imaged by the optical gas instrument;

(ii) Indications of liquids dripping;

(iii) Indications by a sensor that a seal or barrier fluid system has failed; or

(iv) Screening results using a <u>40 CFR part 60, appendix A</u>-7, Method 21 monitor that exceed the leak definition in the applicable subpart to which the equipment is subject.

(h) The alternative work practice standard for monitoring equipment for leaks is available to all subparts in  $\frac{40 \text{ CFR parts}}{60, 61, 63}$ , and  $\frac{65}{5}$  that require monitoring of equipment with a  $\frac{40 \text{ CFR part } 60, \text{ appendix } A}{10 \text{ CFR part } 60, \text{ appendix } A}$ . 7, Method 21 monitor.

(1) An owner or operator of an affected source subject to CFR parts 60, 61, 63, or 65 can choose to comply with the alternative work practice requirements in <u>paragraph (i)</u> of this section instead of using the <u>40 CFR part 60, appendix A</u>-7, Method 21 monitor to identify leaking equipment. The owner or operator must document the equipment, process units, and facilities for which the alternative work practice will be used to identify leaks.

(2) Any leak detected when following the leak survey procedure in <u>paragraph (i)(3)</u> of this section must be identified for repair as required in the applicable subpart.

(3) If the alternative work practice is used to identify leaks, re-screening after an attempted repair of leaking equipment must be conducted using either the alternative work practice or the  $\frac{40 \text{ CFR part } 60, \text{ appendix } A}{1000 \text{ CFR part } 60, \text{ appendix } A}$ -7, Method 21 monitor at the leak definition required in the applicable subpart to which the equipment is subject.

(4) The schedule for repair is as required in the applicable subpart.

(5) When this alternative work practice is used for detecting leaking equipment, choose one of the monitoring frequencies listed in Table 1 to <u>subpart A of this part</u> in lieu of the monitoring frequency specified for regulated equipment in the applicable subpart. Reduced monitoring frequencies for good performance are not applicable when using the alternative work practice.

(6) When this alternative work practice is used for detecting leaking equipment the following are not applicable for the equipment being monitored:

(i) Skip period leak detection and repair;

(ii) Quality improvement plans; or

(iii) Complying with standards for allowable percentage of valves and pumps to leak.

(7) When the alternative work practice is used to detect leaking equipment, the regulated equipment in paragraph (h)(1)(i) of this section must also be monitored annually using a <u>40 CFR part 60, appendix A</u>-7, Method 21 monitor at the leak definition required in the applicable subpart. The owner or operator may choose the specific monitoring period (for example, first quarter) to conduct the annual monitoring. Subsequent monitoring must be conducted every 12 months from the initial period. Owners or operators must keep records of the annual Method 21 screening results, as specified in paragraph (i)(4)(vii) of this section.

(i) An owner or operator of an affected source who chooses to use the alternative work practice must comply with the requirements of <u>paragraphs (i)(1)</u> through (i)(5) of this section.

(1) Instrument Specifications. The optical gas imaging instrument must comply with the requirements in  $(\underline{i})(\underline{1})(\underline{i})$  and  $(\underline{i})(\underline{1})(\underline{i})$  of this section.

(i) Provide the operator with an image of the potential leak points for each piece of equipment at both the detection sensitivity level and within the distance used in the daily instrument check described in paragraph(i)(2) of this section. The detection sensitivity level depends upon the frequency at which leak monitoring is to be performed.
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(ii) Provide a date and time stamp for video records of every monitoring event.

(2) Daily Instrument Check. On a daily basis, and prior to beginning any leak monitoring work, test the optical gas imaging instrument at the mass flow rate determined in <u>paragraph (i)(2)(i)</u> of this section in accordance with the procedure specified in <u>paragraphs (i)(2)(ii)</u> through (i)(2)(iv) of this section for each camera configuration used during monitoring (for example, different lenses used), unless an alternative method to demonstrate daily instrument checks has been approved in accordance with <u>paragraph (i)(2)(v)</u> of this section.

(i) Calculate the mass flow rate to be used in the daily instrument check by following the procedures in <u>paragraphs</u>  $(\underline{i})(2)(\underline{i})(\underline{A})$  and  $(\underline{i})(2)(\underline{i})(\underline{B})$  of this section.

(A) For a specified population of equipment to be imaged by the instrument, determine the piece of equipment in contact with the lowest mass fraction of chemicals that are detectable, within the distance to be used in <u>paragraph (i)(2)(iv)(B)</u> of this section, at or below the standard detection sensitivity level.

(B) Multiply the standard detection sensitivity level, corresponding to the selected monitoring frequency in Table 1 of <u>subpart</u> <u>A of this part</u>, by the mass fraction of detectable chemicals from the stream identified in <u>paragraph (i)(2)(i)(A)</u> of this section to determine the mass flow rate to be used in the daily instrument check, using the following equation.

$$E_{dic} = (E_{sds}) \sum_{i=1}^{k} x_i$$

Where:

 $E_{dic}$  = Mass flow rate for the daily instrument check, grams per hour

 $x_i = Mass$  fraction of detectable chemical(s) i seen by the optical gas imaging instrument, within the distance to be used in <u>paragraph (i)(2)(iv)(B)</u> of this section, at or below the standard detection sensitivity level,  $E_{sds}$ .

 $E_{sds}$  = Standard detection sensitivity level from Table 1 to subpart A, grams per hour

k = Total number of detectable chemicals emitted from the leaking equipment and seen by the optical gas imaging instrument.

(ii) Start the optical gas imaging instrument according to the manufacturer's instructions, ensuring that all appropriate settings conform to the manufacturer's instructions.

(iii) Use any gas chosen by the user that can be viewed by the optical gas imaging instrument and that has a purity of no less than 98 percent.

(iv) Establish a mass flow rate by using the following procedures:

(A) Provide a source of gas where it will be in the field of view of the optical gas imaging instrument.

(B) Set up the optical gas imaging instrument at a recorded distance from the outlet or leak orifice of the flow meter that will not be exceeded in the actual performance of the leak survey. Do not exceed the operating parameters of the flow meter.

(C) Open the valve on the flow meter to set a flow rate that will create a mass emission rate equal to the mass rate specified in paragraph (i)(2)(i) of this section while observing the gas flow through the optical gas imaging instrument viewfinder. When an image of the gas emission is seen through the viewfinder at the required emission rate, make a record of the reading on the flow meter.

(v) Repeat the procedures specified in <u>paragraphs (i)(2)(ii)</u> through  $(\underline{i})(\underline{2})(\underline{iv})$  of this section for each configuration of the optical gas imaging instrument used during the leak survey.

(vi) To use an alternative method to demonstrate daily instrument checks, apply to the Administrator for approval of the alternative under  $\frac{60.13(i)}{1.000}$ .

(3) Leak Survey Procedure. Operate the optical gas imaging instrument to image every regulated piece of equipment selected for this work practice in accordance with the instrument manufacturer's operating parameters. All emissions imaged by the optical gas imaging instrument are considered to be leaks and are subject to repair. All emissions visible to the naked eye are also considered to be leaks and are subject to repair.

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(4) Recordkeeping. You must keep the records described in <u>paragraphs (i)(4)(i)</u> through  $(\underline{i})(4)(\underline{vii})$  of this section:

(i) The equipment, processes, and facilities for which the owner or operator chooses to use the alternative work practice.

(ii) The detection sensitivity level selected from Table 1 to subpart A of this part for the optical gas imaging instrument.

(iii) The analysis to determine the piece of equipment in contact with the lowest mass fraction of chemicals that are detectable, as specified in paragraph (i)(2)(i)(A) of this section.

(iv) The technical basis for the mass fraction of detectable chemicals used in the equation in  $\frac{\text{paragraph}(i)(2)(i)(B)}{|B|}$  of this section.

(v) The daily instrument check. Record the distance, per <u>paragraph (i)(2)(iv)(B)</u> of this section, and the flow meter reading, per <u>paragraph (i)(2)(iv)(C)</u> of this section, at which the leak was imaged. Keep a video record of the daily instrument check for each configuration of the optical gas imaging instrument used during the leak survey (for example, the daily instrument check must be conducted for each lens used). The video record must include a time and date stamp for each daily instrument check. The video record must be kept for 5 years.

(vi) Recordkeeping requirements in the applicable subpart. A video record must be used to document the leak survey results. The video record must include a time and date stamp for each monitoring event. A video record can be used to meet the recordkeeping requirements of the applicable subparts if each piece of regulated equipment selected for this work practice can be identified in the video record. The video record must be kept for 5 years.

(vii) The results of the annual Method 21 screening required in <u>paragraph (h)(7)</u> of this section. Records must be kept for all regulated equipment specified in <u>paragraph (h)(1)</u> of this section. Records must identify the equipment screened, the screening value measured by Method 21, the time and date of the screening, and calibration information required in the existing applicable subpart.

(5) Reporting. Submit the reports required in the applicable subpart. Submit the records of the annual Method 21 screening required in <u>paragraph (h)(7)</u> of this section to the Administrator via e-mail to <u>CCG-AWP@EPA.GOV</u>.

[<u>51 FR 2701</u>, Jan. 21, 1986, as amended at <u>63 FR 24444</u>, May 4, 1998; <u>65 FR 61752</u>, Oct. 17, 2000; <u>73 FR 78209</u>, Dec. 22, 2008]

### § 60.19 General notification and reporting requirements.

(a) For the purposes of this part, time periods specified in days shall be measured in calendar days, even if the word "calendar" is absent, unless otherwise specified in an applicable requirement.

(b) For the purposes of this part, if an explicit postmark deadline is not specified in an applicable requirement for the submittal of a notification, application, report, or other written communication to the Administrator, the owner or operator shall postmark the submittal on or before the number of days specified in the applicable requirement. For example, if a notification must be submitted 15 days before a particular event is scheduled to take place, the notification shall be postmarked on or before 15 days preceding the event; likewise, if a notification must be submitted 15 days after a particular event takes place, the notification shall be delivered or postmarked on or before 15 days following the end of the event. The use of reliable non-Government mail carriers that provide indications of verifiable delivery of information required to be submitted to the Administrator, similar to the postmark provided by the U.S. Postal Service, or alternative means of delivery, including the use of electronic media, agreed to by the permitting authority, is acceptable.

(c) Notwithstanding time periods or postmark deadlines specified in this part for the submittal of information to the Administrator by an owner or operator, or the review of such information by the Administrator, such time periods or deadlines may be changed by mutual agreement between the owner or operator and the Administrator. Procedures governing the implementation of this provision are specified in <u>paragraph (f)</u> of this section.

(d) If an owner or operator of an affected facility in a State with delegated authority is required to submit periodic reports under this part to the State, and if the State has an established timeline for the submission of periodic reports that is consistent with the reporting frequency(ies) specified for such facility under this part, the owner or operator may change the dates by which periodic reports under this part shall be submitted (without changing the frequency of reporting) to be consistent with the State's schedule by mutual agreement between the owner or operator and the State. The allowance in the previous sentence applies in each State beginning 1 year after the affected facility is required to be in compliance with the applicable subpart in this part. Procedures governing the implementation of this provision are specified in paragraph (f) of this section.

## NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART A – GENERAL PROVISIONS.

(e) If an owner or operator supervises one or more stationary sources affected by standards set under this part and standards set under part 61, part 63, or both such parts of this chapter, he/she may arrange by mutual agreement between the owner or operator and the Administrator (or the State with an approved permit program) a common schedule on which periodic reports required by each applicable standard shall be submitted throughout the year. The allowance in the previous sentence applies in each State beginning 1 year after the stationary source is required to be in compliance with the applicable subpart in this part, or 1 year after the stationary source is required to be in compliance with the applicable <u>40 CFR part 61</u> or <u>part 63 of this chapter</u> standard, whichever is latest. Procedures governing the implementation of this provision are specified in <u>paragraph</u> (f) of this section.

(f)

(1)

(i) Until an adjustment of a time period or postmark deadline has been approved by the Administrator under <u>paragraphs</u>  $(\underline{f})(2)$  and  $(\underline{f})(3)$  of this section, the owner or operator of an affected facility remains strictly subject to the requirements of this part.

(ii) An owner or operator shall request the adjustment provided for in <u>paragraphs (f)(2)</u> and <u>(f)(3)</u> of this section each time he or she wishes to change an applicable time period or postmark deadline specified in this part.

(2) Notwithstanding time periods or postmark deadlines specified in this part for the submittal of information to the Administrator by an owner or operator, or the review of such information by the Administrator, such time periods or deadlines may be changed by mutual agreement between the owner or operator and the Administrator. An owner or operator who wishes to request a change in a time period or postmark deadline for a particular requirement shall request the adjustment in writing as soon as practicable before the subject activity is required to take place. The owner or operator shall include in the request whatever information he or she considers useful to convince the Administrator that an adjustment is warranted.

(3) If, in the Administrator's judgment, an owner or operator's request for an adjustment to a particular time period or postmark deadline is warranted, the Administrator will approve the adjustment. The Administrator will notify the owner or operator in writing of approval or disapproval of the request for an adjustment within 15 calendar days of receiving sufficient information to evaluate the request.

(4) If the Administrator is unable to meet a specified deadline, he or she will notify the owner or operator of any significant delay and inform the owner or operator of the amended schedule.

[59 FR 12428, Mar. 16, 1994, as amended at 64 FR 7463, Feb. 12, 1998]

### Table 1 to Subpart A of Part 60—Detection Sensitivity Levels (grams per hour)

Monitoring frequency per subpart <sup>a</sup>	Detection sensitivity level
Bi-Monthly	60
Semi-Quarterly	85
Monthly	100

<sup>a</sup> When this alternative work practice is used to identify leaking equipment, the owner or operator must choose one of the monitoring frequencies listed in this table in lieu of the monitoring frequency specified in the applicable subpart. Bi-monthly means every other month. Semi-quarterly means twice per quarter. Monthly means once per month.

[<u>73 FR 78211</u>, Dec. 22, 2008]

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## Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984

Subpart Kb—Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984, and On or Before October 4, 2023

Source:

52 FR 11429, Apr. 8, 1987, unless otherwise noted.

## § 60.110b Applicability and designation of affected facility.

(a) Except as provided in paragraph (b) of this section, the affected facility to which this subpart applies is each storage vessel with a capacity greater than or equal to 75 cubic meters (m<sup>3</sup>) that is used to store volatile organic liquids (VOL) for which construction, reconstruction, or modification is commenced after July 23, 1984, and on or before October 4, 2023.

(b) This subpart does not apply to storage vessels with a capacity greater than or equal to 151 m<sup>3</sup> storing a liquid with a maximum true vapor pressure less than 3.5 kilopascals (kPa) or with a capacity greater than or equal to 75 m<sup>3</sup> but less than 151 m<sup>3</sup> storing a liquid with a maximum true vapor pressure less than 15.0 kPa.

(c) [Reserved]

(d) This subpart does not apply to the following:

(1) Vessels at coke oven by-product plants.

(2) Pressure vessels designed to operate in excess of 204.9 kPa and without emissions to the atmosphere.

(3) Vessels permanently attached to mobile vehicles such as trucks, railcars, barges, or ships.

(4) Vessels with a design capacity less than or equal to  $1.589.874 \text{ m}^3$  used for petroleum or condensate stored, processed, or treated prior to custody transfer.

(5) Vessels located at bulk gasoline plants.

(6) Storage vessels located at gasoline service stations.

(7) Vessels used to store beverage alcohol.

(8) Vessels subject to subpart GGGG of 40 CFR part 63.

(e) Alternative means of compliance —

(1) Option to comply with part 65. Owners or operators may choose to comply with 40 CFR part 65, subpart C, to satisfy the requirements of §§ 60.112b through 60.117b for storage vessels that are subject to this subpart that meet the specifications in paragraphs (e)(1)(i) and (ii) of this section. When choosing to comply with 40 CFR part 65, subpart C, the monitoring requirements of  $\S$  60.116b(c), (e), (f)(1), and (g) still apply. Other provisions applying to owners or operators who choose to comply with 40 CFR part 65 are provided in 40 CFR 65.1.

(i) A storage vessel with a design capacity greater than or equal to 151 m<sup>3</sup> containing a VOL that, as stored, has a maximum true vapor pressure equal to or greater than 5.2 kPa; or

(ii) A storage vessel with a design capacity greater than 75 m<sup>3</sup> but less than 151 m<sup>3</sup> containing a VOL that, as stored, has a maximum true vapor pressure equal to or greater than 27.6 kPa.

(2) Part 60, subpart A. Owners or operators who choose to comply with 40 CFR part 65, subpart C, must also comply with <u>§§ 60.1, 60.2, 60.5, 60.6, 60.7(a)(1)</u> and <u>(4), 60.14, 60.15</u>, and <u>60.16</u> for those storage vessels. All sections and paragraphs of subpart A of this part that are not mentioned in this paragraph (e)(2) do not apply to owners or operators of storage vessels complying with 40 CFR part 65, subpart C, except that provisions required to be met prior to implementing <u>40 CFR part 65</u> still apply. Owners and operators who choose to comply with <u>40 CFR part 65</u>, subpart C, must comply with 40 CFR part 65, subpart A.

(3) Internal floating roof report. If an owner or operator installs an internal floating roof and, at initial startup, chooses to comply with 40 CFR part 65, subpart C, a report shall be furnished to the Administrator stating that the control equipment meets the specifications of 40 CFR 65.43. This report shall be an attachment to the notification required by 40 CFR 65.5(b).

## Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984

(4) *External floating roof report.* If an owner or operator installs an external floating roof and, at initial startup, chooses to comply with <u>40 CFR part 65</u>, <u>subpart C</u>, a report shall be furnished to the Administrator stating that the control equipment meets the specifications of <u>40 CFR 65.44</u>. This report shall be an attachment to the notification required by <u>40 CFR 65.5(b)</u>.

(5) Option to comply with part 63, subpart WW, of this chapter. Except as specified in paragraphs (e)(5)(i) through (iv) of this section, owners or operators may choose to comply with 40 CFR part 63, subpart WW, to satisfy the requirements of  $\frac{88}{50.112b}$  through 60.117b for storage vessels either with a design capacity greater than or equal to 151 m<sup>3</sup> containing a VOL that, as stored, has a maximum true vapor pressure equal to or greater than 5.2 kPa but less than 76.6 kPa, or with a design capacity greater than or equal to 75 m<sup>3</sup> but less than 151 m<sup>3</sup> containing a VOL that, as stored, has a maximum true vapor pressure equal to 76 kPa.

(i) The general provisions in <u>subpart A of this part</u> apply instead of the general provisions in <u>subpart A of part 63 of this</u> <u>chapter</u>.

(ii) Where terms are defined in both this subpart and <u>40 CFR part 63, subpart WW</u>, the definitions in this subpart apply.

(iii) Owners or operators who choose to comply with  $\underline{40 \text{ CFR part 63, subpart WW}}$ , also must comply with the monitoring requirements of § 60.116b(a), (c), (e), and (f)(1), except as specified in paragraphs (e)(5)(iii)(A) through (C) of this section.

(A) The reference to all records applies only to the records required by  $\frac{60.116b(c)}{2}$ ;

(B) The reference to  $\S 60.116b(b)$  does not apply; and

(C) The reference to  $\S 60.116b(g)$  does not apply.

(iv) Owners or operators who choose to comply with <u>40 CFR part 63</u>, <u>subpart WW</u>, <u>must</u> also keep records and furnish reports as specified in <u>paragraphs (e)(5)(iv)(A)</u> through  $(\underline{F})$  of this section.

(A) For each affected facility, the owner or operator must notify the Administrator at least 30 days before the first inspection is conducted under <u>40 CFR part 63</u>, <u>subpart WW</u>. After this notification is submitted to the Administrator, the owner or operator must continue to comply with the alternative standard described in this <u>paragraph (e)(5)</u> until the owner or operator submits another notification to the Administrator indicating the affected facility is using the requirements of <u>§§</u> <u>60.112b</u> through <u>60.117b</u> instead of the alternative standard described in this <u>paragraph (e)(5)</u>. The compliance schedule for events does not reset upon switching between compliance with this subpart and <u>40 CFR part 63</u>, <u>subpart WW</u>.

(B) Keep a record of each affected facility using the alternative standard described in this <u>paragraph (e)(5)</u> when conducting an inspection required by  $\frac{63.1063(c)(1)}{5}$  of this chapter.

(C) Keep a record of each affected facility using the alternative standard described in this <u>paragraph (e)(5)</u> when conducting an inspection required by  $\S 63.1063(c)(2)$  of this chapter.

(E) Copies of all records and reports kept pursuant to  $\frac{63.1065}{5}$  of this chapter that have not met the 5-year record retention required by the introductory text of  $\frac{63.1065}{5}$  must be kept for an additional 5 years after the date of submittal of the notification specified in <u>paragraph (e)(5)(iv)(A)</u> of this section, indicating the affected facility is using the requirements of  $\frac{86.1065}{5}$  through  $\frac{60.112b}{5}$  through  $\frac{60.117b}{5}$ .

(F) The following exceptions to the reporting requirements of § 63.1066 of this chapter apply:

(1) The notification of initial startup required under  $\S 63.1066(a)(1)$  and (2) of this chapter must be submitted as an attachment to the notification required by  $\S \$ 60.7(a)(3)$  and 60.115b(a)(1);

(2) The reference in § 63.1066(b)(2) of this chapter to periodic reports "when inspection failures occur" means to submit inspections results within 60 days of the initial gap measurements required by § 63.1063(c)(2)(i) of this chapter and within 30 days of all other inspections required by § 63.1063(c)(1) and (2) of this chapter.

[52 FR 11429, Apr. 8, 1987, as amended at 54 FR 32973, Aug. 11, 1989; 65 FR 78275, Dec. 14, 2000; 68 FR 59332, Oct. 15, 2003; 86 FR 5019, Jan. 19, 2021; 89 FR 83317, Oct. 15, 2024]

## Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984

## § 60.111b Definitions.

Terms used in this subpart are defined in the Act, in subpart A of this part, or in this subpart as follows:

*Bulk gasoline plant* means any gasoline distribution facility that has a gasoline throughput less than or equal to 75,700 liters per day. Gasoline throughput shall be the maximum calculated design throughput as may be limited by compliance with an enforceable condition under Federal requirement or Federal, State or local law, and discoverable by the Administrator and any other person.

*Condensate* means hydrocarbon liquid separated from natural gas that condenses due to changes in the temperature or pressure, or both, and remains liquid at standard conditions.

*Custody transfer* means the transfer of produced petroleum and/or condensate, after processing and/or treatment in the producing operations, from storage vessels or automatic transfer facilities to pipelines or any other forms of transportation.

Fill means the introduction of VOL into a storage vessel but not necessarily to complete capacity.

Gasoline service station means any site where gasoline is dispensed to motor vehicle fuel tanks from stationary storage tanks.

*Maximum true vapor pressure* means the equilibrium partial pressure exerted by the volatile organic compounds (as defined in <u>40 CFR 51.100</u>) in the stored VOL at the temperature equal to the highest calendar-month average of the VOL storage temperature for VOL's stored above or below the ambient temperature or at the local maximum monthly average temperature as reported by the National Weather Service for VOL's stored at the ambient temperature, as determined:

(1) In accordance with methods described in American Petroleum institute Bulletin 2517, Evaporation Loss From External Floating Roof Tanks, (incorporated by reference—see  $\frac{60.17}{3}$ ; or

(2) As obtained from standard reference texts; or

(3) As determined by ASTM D2879-83, 96, or 97 (incorporated by reference—see § 60.17);

(4) Any other method approved by the Administrator.

Petroleum means the crude oil removed from the earth and the oils derived from tar sands, shale, and coal.

*Petroleum liquids* means petroleum, condensate, and any finished or intermediate products manufactured in a petroleum refinery.

*Process tank* means a tank that is used within a process (including a solvent or raw material recovery process) to collect material discharged from a feedstock storage vessel or equipment within the process before the material is transferred to other equipment within the process, to a product or by-product storage vessel, or to a vessel used to store recovered solvent or raw material. In many process tanks, unit operations such as reactions and blending are conducted. Other process tanks, such as surge control vessels and bottoms receivers, however, may not involve unit operations.

*Reid vapor pressure* means the absolute vapor pressure of volatile crude oil and volatile nonviscous petroleum liquids except liquified petroleum gases, as determined by ASTM D323-82 or 94 (incorporated by reference—see  $\frac{60.17}{10}$ ).

Storage vessel means each tank, reservoir, or container used for the storage of volatile organic liquids but does not include:

(1) Frames, housing, auxiliary supports, or other components that are not directly involved in the containment of liquids or vapors;

(2) Subsurface caverns or porous rock reservoirs; or

(3) Process tanks.

*Volatile organic liquid (VOL)* means any organic liquid which can emit volatile organic compounds (as defined in <u>40 CFR</u> <u>51.100</u>) into the atmosphere.

*Waste* means any liquid resulting from industrial, commercial, mining or agricultural operations, or from community activities that is discarded or is being accumulated, stored, or physically, chemically, or biologically treated prior to being discarded or recycled.

[52 FR 11429, Apr. 8, 1987, as amended at 54 FR 32973, Aug. 11, 1989; 65 FR 61756, Oct. 17, 2000; 68 FR 59333, Oct. 15, 2003]

## Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984

## § 60.112b Standard for volatile organic compounds (VOC).

(a) The owner or operator of each storage vessel either with a design capacity greater than or equal to  $151 \text{ m}^3$  containing a VOL that, as stored, has a maximum true vapor pressure equal to or greater than 5.2 kPa but less than 76.6 kPa or with a design capacity greater than or equal to 75 m<sup>3</sup> but less than 151 m<sup>3</sup> containing a VOL that, as stored, has a maximum true vapor pressure equal to or greater than 27.6 kPa but less than 76.6 kPa, shall equip each storage vessel with one of the following:

(1) A fixed roof in combination with an internal floating roof meeting the following specifications:

(i) The internal floating roof shall rest or float on the liquid surface (but not necessarily in complete contact with it) inside a storage vessel that has a fixed roof. The internal floating roof shall be floating on the liquid surface at all times, except during initial fill and during those intervals when the storage vessel is completely emptied or subsequently emptied and refilled. When the roof is resting on the leg supports, the process of filling, emptying, or refilling shall be continuous and shall be accomplished as rapidly as possible.

(ii) Each internal floating roof shall be equipped with one of the following closure devices between the wall of the storage vessel and the edge of the internal floating roof:

(A) A foam- or liquid-filled seal mounted in contact with the liquid (liquid-mounted seal). A liquid-mounted seal means a foam- or liquid-filled seal mounted in contact with the liquid between the wall of the storage vessel and the floating roof continuously around the circumference of the tank.

(B) Two seals mounted one above the other so that each forms a continuous closure that completely covers the space between the wall of the storage vessel and the edge of the internal floating roof. The lower seal may be vapor-mounted, but both must be continuous.

(C) A mechanical shoe seal. A mechanical shoe seal is a metal sheet held vertically against the wall of the storage vessel by springs or weighted levers and is connected by braces to the floating roof. A flexible coated fabric (envelope) spans the annular space between the metal sheet and the floating roof.

(iii) Each opening in a noncontact internal floating roof except for automatic bleeder vents (vacuum breaker vents) and the rim space vents is to provide a projection below the liquid surface.

(iv) Each opening in the internal floating roof except for leg sleeves, automatic bleeder vents, rim space vents, column wells, ladder wells, sample wells, and stub drains is to be equipped with a cover or lid which is to be maintained in a closed position at all times (i.e., no visible gap) except when the device is in actual use. The cover or lid shall be equipped with a gasket. Covers on each access hatch and automatic gauge float well shall be bolted except when they are in use.

(v) Automatic bleeder vents shall be equipped with a gasket and are to be closed at all times when the roof is floating except when the roof is being floated off or is being landed on the roof leg supports.

(vi) Rim space vents shall be equipped with a gasket and are to be set to open only when the internal floating roof is not floating or at the manufacturer's recommended setting.

(vii) Each penetration of the internal floating roof for the purpose of sampling shall be a sample well. The sample well shall have a slit fabric cover that covers at least 90 percent of the opening.

(viii) Each penetration of the internal floating roof that allows for passage of a column supporting the fixed roof shall have a flexible fabric sleeve seal or a gasketed sliding cover.

(ix) Each penetration of the internal floating roof that allows for passage of a ladder shall have a gasketed sliding cover.

(2) An external floating roof. An external floating roof means a pontoon-type or double-deck type cover that rests on the liquid surface in a vessel with no fixed roof. Each external floating roof must meet the following specifications:

(i) Each external floating roof shall be equipped with a closure device between the wall of the storage vessel and the roof edge. The closure device is to consist of two seals, one above the other. The lower seal is referred to as the primary seal, and the upper seal is referred to as the secondary seal.

(A) The primary seal shall be either a mechanical shoe seal or a liquid-mounted seal. Except as provided in  $\S$  60.113b(b)(4), the seal shall completely cover the annular space between the edge of the floating roof and tank wall.

## Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984

(B) The secondary seal shall completely cover the annular space between the external floating roof and the wall of the storage vessel in a continuous fashion except as allowed in  $\frac{60.113b(b)(4)}{2}$ .

(ii) Except for automatic bleeder vents and rim space vents, each opening in a noncontact external floating roof shall provide a projection below the liquid surface. Except for automatic bleeder vents, rim space vents, roof drains, and leg sleeves, each opening in the roof is to be equipped with a gasketed cover, seal, or lid that is to be maintained in a closed position at all times (i.e., no visible gap) except when the device is in actual use. Automatic bleeder vents are to be closed at all times when the roof is floating except when the roof is being floated off or is being landed on the roof leg supports. Rim vents are to be set to open when the roof is being floated off the roof legs supports or at the manufacturer's recommended setting. Automatic bleeder vents and rim space vents are to be gasketed. Each emergency roof drain is to be provided with a slotted membrane fabric cover that covers at least 90 percent of the area of the opening.

(iii) The roof shall be floating on the liquid at all times (i.e., off the roof leg supports) except during initial fill until the roof is lifted off leg supports and when the tank is completely emptied and subsequently refilled. The process of filling, emptying, or refilling when the roof is resting on the leg supports shall be continuous and shall be accomplished as rapidly as possible.

(3) A closed vent system and control device meeting the following specifications:

(i) The closed vent system shall be designed to collect all VOC vapors and gases discharged from the storage vessel and operated with no detectable emissions as indicated by an instrument reading of less than 500 ppm above background and visual inspections, as determined in part 60, subpart VV,  $\frac{60.485(b)}{2}$ .

(ii) The control device shall be designed and operated to reduce inlet VOC emissions by 95 percent or greater. If a flare is used as the control device, it shall meet the specifications described in the general control device requirements ( $\frac{60.18}{50.18}$ ) of the General Provisions.

(4) A system equivalent to those described in <u>paragraphs (a)(1)</u>, (a)(2), or (a)(3) of this section as provided in § 60.114b of this subpart.

(b) The owner or operator of each storage vessel with a design capacity greater than or equal to 75  $m^3$  which contains a VOL that, as stored, has a maximum true vapor pressure greater than or equal to 76.6 kPa shall equip each storage vessel with one of the following:

(1) A closed vent system and control device as specified in  $\S 60.112b(a)(3)$ .

(2) A system equivalent to that described in paragraph (b)(1) as provided in  $\S$  60.114b of this subpart.

(c) *Site-specific standard for Merck & Co., Inc.'s Stonewall Plant in Elkton, Virginia.* This paragraph applies only to the pharmaceutical manufacturing facility, commonly referred to as the Stonewall Plant, located at Route 340 South, in Elkton, Virginia ("site").

(1) For any storage vessel that otherwise would be subject to the control technology requirements of <u>paragraphs (a)</u> or (b) of this section, the site shall have the option of either complying directly with the requirements of this subpart, or reducing the site-wide total criteria pollutant emissions cap (total emissions cap) in accordance with the procedures set forth in a permit issued pursuant to 40 CFR 52.2454. If the site chooses the option of reducing the total emissions cap in accordance with the procedures set forth in such permit, the requirements of such permit shall apply in lieu of the otherwise applicable requirements of this subpart for such storage vessel.

(2) For any storage vessel at the site not subject to the requirements of  $\frac{40 \text{ CFR } 60.112 \text{ (a)}}{\text{ cFR } 60.116 \text{ (b)}}$  and  $\frac{\text{(c)}}{\text{ cm}}$  and the General Provisions (subpart A of this part) shall not apply.

[52 FR 11429, Apr. 8, 1987, as amended at <u>62 FR 52641</u>, Oct. 8, 1997]

### § 60.113b Testing and procedures.

The owner or operator of each storage vessel as specified in  $\S 60.112b(a)$  shall meet the requirements of <u>paragraph (a)</u>, (b), or (c) of this section. The applicable paragraph for a particular storage vessel depends on the control equipment installed to meet the requirements of  $\S 60.112b$ .

(a) After installing the control equipment required to meet  $\S 60.112b(a)(1)$  (permanently affixed roof and internal floating roof), each owner or operator shall:

## Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984

(1) Visually inspect the internal floating roof, the primary seal, and the secondary seal (if one is in service), prior to filling the storage vessel with VOL. If there are holes, tears, or other openings in the primary seal, the secondary seal, or the seal fabric or defects in the internal floating roof, or both, the owner or operator shall repair the items before filling the storage vessel.

(2) For Vessels equipped with a liquid-mounted or mechanical shoe primary seal, visually inspect the internal floating roof and the primary seal or the secondary seal (if one is in service) through manholes and roof hatches on the fixed roof at least once every 12 months after initial fill. If the internal floating roof is not resting on the surface of the VOL inside the storage vessel, or there is liquid accumulated on the roof, or the seal is detached, or there are holes or tears in the seal fabric, the owner or operator shall repair the items or empty and remove the storage vessel from service within 45 days. If a failure that is detected during inspections required in this paragraph cannot be repaired within 45 days and if the vessel cannot be emptied within 45 days, a 30-day extension may be requested from the Administrator in the inspection report required in  $\S$  schedule of actions the company will take that will assure that the control equipment will be repaired or the vessel will be emptied as soon as possible.

(i) Visually inspect the vessel as specified in <u>paragraph (a)(4)</u> of this section at least every 5 years; or

(ii) Visually inspect the vessel as specified in <u>paragraph (a)(2)</u> of this section.

(4) Visually inspect the internal floating roof, the primary seal, the secondary seal (if one is in service), gaskets, slotted membranes and sleeve seals (if any) each time the storage vessel is emptied and degassed. If the internal floating roof has defects, the primary seal has holes, tears, or other openings in the seal or the seal fabric, or the secondary seal has holes, tears, or other openings in the seal or the seal of the liquid surfaces from the atmosphere, or the slotted membrane has more than 10 percent open area, the owner or operator shall repair the items as necessary so that none of the conditions specified in this paragraph exist before refilling the storage vessel with VOL. In no event shall inspections conducted in accordance with this provision occur at intervals greater than 10 years in the case of vessels conducting the annual visual inspection as specified in paragraphs (a)(2) and (a)(3)(i) of this section and at intervals no greater than 5 years in the case of vessels specified in paragraph (a)(3)(i) of this section.

(5) Notify the Administrator in writing at least 30 days prior to the filling or refilling of each storage vessel for which an inspection is required by <u>paragraphs (a)(1)</u> and (a)(4) of this section to afford the Administrator the opportunity to have an observer present. If the inspection required by <u>paragraph (a)(4)</u> of this section is not planned and the owner or operator could not have known about the inspection 30 days in advance of refilling the tank, the owner or operator shall notify the Administrator at least 7 days prior to the refilling of the storage vessel. Notification shall be made by telephone immediately followed by written documentation demonstrating why the inspection was unplanned. Alternatively, this notification including the written documentation may be made in writing and sent by express mail so that it is received by the Administrator at least 7 days prior to the refilling.

(b) After installing the control equipment required to meet  $\frac{60.112b(a)(2)}{60.112b(a)(2)}$  (external floating roof), the owner or operator shall:

(1) Determine the gap areas and maximum gap widths, between the primary seal and the wall of the storage vessel and between the secondary seal and the wall of the storage vessel according to the following frequency.

(i) Measurements of gaps between the tank wall and the primary seal (seal gaps) shall be performed during the hydrostatic testing of the vessel or within 60 days of the initial fill with VOL and at least once every 5 years thereafter.

(ii) Measurements of gaps between the tank wall and the secondary seal shall be performed within 60 days of the initial fill with VOL and at least once per year thereafter.

(iii) If any source ceases to store VOL for a period of 1 year or more, subsequent introduction of VOL into the vessel shall be considered an initial fill for the purposes of paragraphs (b)(1)(i) and (b)(1)(i) of this section.

(2) Determine gap widths and areas in the primary and secondary seals individually by the following procedures:

(i) Measure seal gaps, if any, at one or more floating roof levels when the roof is floating off the roof leg supports.

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(ii) Measure seal gaps around the entire circumference of the tank in each place where a 0.32-cm diameter uniform probe passes freely (without forcing or binding against seal) between the seal and the wall of the storage vessel and measure the circumferential distance of each such location.

(iii) The total surface area of each gap described in <u>paragraph (b)(2)(ii)</u> of this section shall be determined by using probes of various widths to measure accurately the actual distance from the tank wall to the seal and multiplying each such width by its respective circumferential distance.

(3) Add the gap surface area of each gap location for the primary seal and the secondary seal individually and divide the sum for each seal by the nominal diameter of the tank and compare each ratio to the respective standards in paragraph (b)(4) of this section.

(4) Make necessary repairs or empty the storage vessel within 45 days of identification in any inspection for seals not meeting the requirements listed in (b)(4) (i) and (ii) of this section:

(i) The accumulated area of gaps between the tank wall and the mechanical shoe or liquid-mounted primary seal shall not exceed 212  $cm^2$  per meter of tank diameter, and the width of any portion of any gap shall not exceed 3.81 cm.

(A) One end of the mechanical shoe is to extend into the stored liquid, and the other end is to extend a minimum vertical distance of 61 cm above the stored liquid surface.

(B) There are to be no holes, tears, or other openings in the shoe, seal fabric, or seal envelope.

(ii) The secondary seal is to meet the following requirements:

(A) The secondary seal is to be installed above the primary seal so that it completely covers the space between the roof edge and the tank wall except as provided in paragraph (b)(2)(iii) of this section.

(B) The accumulated area of gaps between the tank wall and the secondary seal shall not exceed 21.2 cm<sup>2</sup> per meter of tank diameter, and the width of any portion of any gap shall not exceed 1.27 cm.

(C) There are to be no holes, tears, or other openings in the seal or seal fabric.

(iii) If a failure that is detected during inspections required in paragraph (b)(1) of § 60.113b(b) cannot be repaired within 45 days and if the vessel cannot be emptied within 45 days, a 30-day extension may be requested from the Administrator in the inspection report required in § 60.115b(b)(4). Such extension request must include a demonstration of unavailability of alternate storage capacity and a specification of a schedule that will assure that the control equipment will be repaired or the vessel will be emptied as soon as possible.

(5) Notify the Administrator 30 days in advance of any gap measurements required by <u>paragraph (b)(1)</u> of this section to afford the Administrator the opportunity to have an observer present.

(6) Visually inspect the external floating roof, the primary seal, secondary seal, and fittings each time the vessel is emptied and degassed.

(i) If the external floating roof has defects, the primary seal has holes, tears, or other openings in the seal or the seal fabric, or the secondary seal has holes, tears, or other openings in the seal or the seal fabric, the owner or operator shall repair the items as necessary so that none of the conditions specified in this paragraph exist before filling or refilling the storage vessel with VOL.

(ii) For all the inspections required by <u>paragraph (b)(6)</u> of this section, the owner or operator shall notify the Administrator in writing at least 30 days prior to the filling or refilling of each storage vessel to afford the Administrator the opportunity to inspect the storage vessel prior to refilling. If the inspection required by <u>paragraph (b)(6)</u> of this section is not planned and the owner or operator could not have known about the inspection 30 days in advance of refilling the tank, the owner or operator shall notify the Administrator at least 7 days prior to the refilling of the storage vessel. Notification shall be made by telephone immediately followed by written documentation demonstrating why the inspection was unplanned. Alternatively, this notification including the written documentation may be made in writing and sent by express mail so that it is received by the Administrator at least 7 days prior to the refilling.

(c) The owner or operator of each source that is equipped with a closed vent system and control device as required in § 60.112b(a)(3) or (b)(2) (other than a flare) is exempt from § 60.8 of the General Provisions and shall meet the following requirements.

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(1) Submit for approval by the Administrator as an attachment to the notification required by  $\frac{60.7(a)(1)}{2}$  or, if the facility is exempt from  $\frac{60.7(a)(1)}{2}$ , as an attachment to the notification required by  $\frac{60.7(a)(2)}{2}$ , an operating plan containing the information listed below.

(i) Documentation demonstrating that the control device will achieve the required control efficiency during maximum loading conditions. This documentation is to include a description of the gas stream which enters the control device, including flow and VOC content under varying liquid level conditions (dynamic and static) and manufacturer's design specifications for the control device. If the control device or the closed vent capture system receives vapors, gases, or liquids other than fuels from sources that are not designated sources under this subpart, the efficiency demonstration is to include consideration of all vapors, gases, and liquids received by the closed vent capture system and control device. If an enclosed combustion device with a minimum residence time of 0.75 seconds and a minimum temperature of 816 °C is used to meet the 95 percent requirement, documentation that those conditions will exist is sufficient to meet the requirements of this paragraph.

(ii) A description of the parameter or parameters to be monitored to ensure that the control device will be operated in conformance with its design and an explanation of the criteria used for selection of that parameter (or parameters).

(2) Operate the closed vent system and control device and monitor the parameters of the closed vent system and control device in accordance with the operating plan submitted to the Administrator in accordance with  $\frac{\text{paragraph}(c)(1)}{\text{plan}}$  of this section, unless the plan was modified by the Administrator during the review process. In this case, the modified plan applies.

(d) The owner or operator of each source that is equipped with a closed vent system and a flare to meet the requirements in § 60.112b (a)(3) or (b)(2) shall meet the requirements as specified in the general control device requirements, § 60.18 (c) and (f).

[52 FR 11429, Apr. 8, 1987, as amended at 54 FR 32973, Aug. 11, 1989]

### § 60.114b Alternative means of emission limitation.

(a) If, in the Administrator's judgment, an alternative means of emission limitation will achieve a reduction in emissions at least equivalent to the reduction in emissions achieved by any requirement in  $\S$  60.112b, the Administrator will publish in the Federal Register a notice permitting the use of the alternative means for purposes of compliance with that requirement.

(b) Any notice under <u>paragraph (a)</u> of this section will be published only after notice and an opportunity for a hearing.

(c) Any person seeking permission under this section shall submit to the Administrator a written application including:

(1) An actual emissions test that uses a full-sized or scale-model storage vessel that accurately collects and measures all VOC emissions from a given control device and that accurately simulates wind and accounts for other emission variables such as temperature and barometric pressure.

(2) An engineering evaluation that the Administrator determines is an accurate method of determining equivalence.

(d) The Administrator may condition the permission on requirements that may be necessary to ensure operation and maintenance to achieve the same emissions reduction as specified in  $\S 60.112b$ .

### § 60.115b Reporting and recordkeeping requirements.

The owner or operator of each storage vessel as specified in  $\S 60.112b(a)$  shall keep records and furnish reports as required by <u>paragraphs (a)</u>, (b), or (c) of this section depending upon the control equipment installed to meet the requirements of  $\S 60.112b$ . The owner or operator shall keep copies of all reports and records required by this section, except for the record required by (c)(1), for at least 2 years. The record required by (c)(1) will be kept for the life of the control equipment.

(a) After installing control equipment in accordance with  $\frac{60.112b(a)(1)}{60.112b(a)(1)}$  (fixed roof and internal floating roof), the owner or operator shall meet the following requirements.

(1) Furnish the Administrator with a report that describes the control equipment and certifies that the control equipment meets the specifications of  $\S 60.112b(a)(1)$  and  $\S 60.113b(a)(1)$ . Prior to October 15, 2024, this report shall be an attachment to the notification required by  $\S 60.7(a)(3)$ . Beginning October 15, 2024, the owner or operator must submit all subsequent reports in PDF format following the procedures specified in paragraph (e) of this section.

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(2) Keep a record of each inspection performed as required by  $\S 60.113b(a)(1)$ , (a)(2), (a)(3), and (a)(4). Each record shall identify the storage vessel on which the inspection was performed and shall contain the date the vessel was inspected and the observed condition of each component of the control equipment (seals, internal floating roof, and fittings).

(3) If any of the conditions described in  $\S 60.113b(a)(2)$  are detected during the annual visual inspection required by  $\S 60.113b(a)(2)$ , a report shall be furnished to the Administrator within 30 days of the inspection. Each report shall identify the storage vessel, the nature of the defects, and the date the storage vessel was emptied or the nature of and date the repair was made. Beginning October 15, 2024, all subsequent reports must be submitted in PDF format following the procedures in paragraph (e) of this section.

(4) After each inspection required by  $\S 60.113b(a)(3)$  that finds holes or tears in the seal or seal fabric, or defects in the internal floating roof, or other control equipment defects listed in  $\S 60.113b(a)(3)(ii)$ , a report shall be furnished to the Administrator within 30 days of the inspection. The report shall identify the storage vessel and the reason it did not meet the specifications of  $\S 60.112b(a)(1)$  or  $\S 60.113b(a)(3)$  and list each repair made. Beginning October 15, 2024, all subsequent reports must be submitted in PDF format following the procedures in paragraph (e) of this section.

(b) After installing control equipment in accordance with  $\frac{60.112b(a)(2)}{2}$  (external floating roof), the owner or operator shall meet the following requirements.

(1) Furnish the Administrator with a report that describes the control equipment and certifies that the control equipment meets the specifications of  $\S$  60.112b(a)(2) and  $\S$  60.113b(b)(2), (b)(3), and (b)(4). Prior to October 15, 2024, this report shall be an attachment to the notification required by  $\S$  60.7(a)(3). Beginning October 15, 2024, the owner or operator must submit all subsequent reports in PDF format following the procedures specified in paragraph (e) of this section.

(2) Within 60 days of performing the seal gap measurements required by  $\S 60.113b(b)(1)$ , furnish the Administrator with a report that contains the following information. Beginning October 15, 2024, all subsequent reports must be submitted in PDF format following the procedures in paragraph (e) of this section.

- (i) The date of measurement;
- (ii) The raw data obtained in the measurement; and
- (iii) The calculations described in  $\S 60.113b(b)(2)$  and (b)(3).

(3) Keep a record of each gap measurement performed as required by  $\S 60.113b(b)$ . Each record shall identify the storage vessel in which the measurement was performed and shall contain:

- (i) The date of measurement;
- (ii) The raw data obtained in the measurement; and
- (iii) The calculations described in  $\S 60.113b(b)(2)$  and (b)(3).

(4) After each seal gap measurement that detects gaps exceeding the limitations specified by  $\frac{60.113b(b)(4)}{2}$ , submit a report to the Administrator within 30 days of the inspection. The report will identify the vessel and contain the information specified in <u>paragraph (b)(2)</u> of this section and the date the vessel was emptied or the repairs made and date of repair. Beginning October 15, 2024, all subsequent reports must be submitted in PDF format following the procedures in <u>paragraph (e)</u> of this section.

(c) After installing control equipment in accordance with  $\frac{60.112b}{a}(a)(3)$  or  $\frac{b}{1}$  (closed vent system and control device other than a flare), the owner or operator shall keep the following records.

- (1) A copy of the operating plan.
- (2) A record of the measured values of the parameters monitored in accordance with  $\S 60.113b(c)(2)$ .

(d) After installing a closed vent system and flare to comply with  $\frac{60.112b}{50.112b}$ , the owner or operator shall meet the following requirements.

(1) A report containing the measurements required by  $\S 60.18(f)(1)$  through (6) shall be furnished to the Administrator as required by  $\S 60.8$  of the General Provisions. This report shall be submitted within 6 months of the initial start-up date. Beginning October 15, 2024, all subsequent reports must be submitted in PDF format following the procedures in paragraph (c) of this section.

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(2) Records shall be kept of all periods of operation during which the flare pilot flame is absent.

(3) Semiannual reports of all periods recorded under  $\S 60.115b(d)(2)$  in which the pilot flame was absent shall be furnished to the Administrator. Beginning October 15, 2024, all subsequent reports must be submitted in PDF format following the procedures specified in paragraph (e) of this section.

(e) An owner or operator required to submit notifications or reports following the procedures specified in this <u>paragraph</u> (e) must submit notifications or reports to the EPA via the Compliance and Emissions Data Reporting Interface (CEDRI), which can be accessed through the EPA's Central Data Exchange (CDX) (<u>https://cdx.epa.gov/</u>). The EPA will make all the information submitted through CEDRI available to the public without further notice to the owner or operator. Do not use CEDRI to submit information the owner or operator claims as CBI. Although the EPA does not expect persons to assert a claim of CBI, if an owner or operator wishes to assert a CBI claim for some of the information in the report or notification, the owner or operator must submit a complete file in the format specified in this subpart, including information claimed to be CBI, to the EPA following the procedures in <u>paragraphs (e)(1)</u> and (2) of this section. Clearly mark the part or all of the information marked as CBI will not be disclosed except in accordance with procedures set forth in 40 CFR part 2. All CBI claims must be asserted at the time of submission. Anything submitted using CEDRI cannot later be claimed CBI. Furthermore, under CAA section 114(c), emissions data is not entitled to confidential treatment, and the EPA is required to make emissions data available to the public. Thus, emissions data will not be protected as CBI and will be made publicly available. The owner or operator must submit the same file submitted to the CBI office with the CBI omitted to the EPA via the EPA's CDX as described earlier in this <u>paragraph (e)</u>.

(1) The preferred method to receive CBI is for it to be transmitted electronically using email attachments, File Transfer Protocol, or other online file sharing services. Electronic submissions must be transmitted directly to the OAQPS CBI Office at the email address <u>oaqpscbi@epa.gov</u>, and as described above, should include clear CBI markings, and be flagged to the attention of the NSPS Kb Lead. Owners and operators who do not have their own file sharing service and who require assistance with submitting large electronic files that exceed the file size limit for email attachments should email <u>oaqpscbi@epa.gov</u> to request a file transfer link.

(2) If an owner or operator cannot transmit the file electronically, the owner or operator may send CBI information through the postal service to the following address: U.S. EPA, Attn: OAQPS Document Control Officer and NSPS Kb Lead, Mail Drop: C404-02, 109 T.W. Alexander, P.O. Box 12055, RTP, NC 27711. The mailed CBI material should be double wrapped and clearly marked. Any CBI markings should not show through the outer envelope.

(f) Owners and operators required to electronically submit notifications or reports through CEDRI in the EPA's CDX may assert a claim of EPA system outage for failure to timely comply with the electronic submittal requirement. To assert a claim of EPA system outage, owners and operators must meet the requirements outlined in <u>paragraphs (f)(1)</u> through (7) of this section.

(1) The owner or operator must have been or will be precluded from accessing CEDRI and submitting a required report within the time prescribed due to an outage of either the EPA's CEDRI or CDX systems.

(2) The outage must have occurred within the period of time beginning 5 business days prior to the date that the submission is due.

(3) The outage may be planned or unplanned.

(4) The owner or operator must submit notification to the Administrator in writing as soon as possible following the date the owner or operator first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

(5) The owner or operator must provide to the Administrator a written description identifying:

(i) The date(s) and time(s) when CDX or CEDRI was accessed and the system was unavailable;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to EPA system outage;

(iii) A description of measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which the owner or operator proposes to report, or if the owner or operator has already met the reporting requirement at the time of the notification, the date the report was submitted.

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(6) The decision to accept the claim of EPA system outage and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(7) In any circumstance, the report must be submitted electronically as soon as possible after the outage is resolved.

(g) Owners and operators required to electronically submit notifications or reports through CEDRI in the EPA's CDX may assert a claim of force majeure for failure to timely comply with the electronic submittal requirement. To assert a claim of force majeure, you must meet the requirements outlined in <u>paragraphs (g)(1)</u> through (5) of this section.

(1) An owner or operator may submit a claim if a force majeure event is about to occur, occurs, or has occurred or there are lingering effects from such an event within the period of time beginning 5 business days prior to the date the submission is due. For the purposes of this section, a force majeure event is defined as an event that will be or has been caused by circumstances beyond the control of the affected facility, its contractors, or any entity controlled by the affected facility that prevents the owner or operator from complying with the requirement to submit a report electronically within the time period prescribed. Examples of such events are acts of nature (*e.g.*, hurricanes, earthquakes, or floods), acts of war or terrorism, or equipment failure or safety hazard beyond the control of the affected facility (*e.g.*, large scale power outage).

(2) The owner or operator must submit notification to the Administrator in writing as soon as possible following the date the owner or operator first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

(3) The owner or operator must provide to the Administrator:

(i) A written description of the force majeure event;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to the force majeure event;

(iii) A description of measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which the owner or operator proposes to report, or if the owner or operator has already met the reporting requirement at the time of the notification, the date the report was submitted.

(4) The decision to accept the claim of force majeure and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(5) In any circumstance, the reporting must occur as soon as possible after the force majeure event occurs.

[52 FR 11429, Apr. 8, 1987, as amended at 86 FR 5019, Jan. 19, 2021; 89 FR 83317, Oct. 15, 2024]

### § 60.116b Monitoring of operations.

(a) The owner or operator shall keep copies of all records required by this section, except for the record required by <u>paragraph (b)</u> of this section, for at least 2 years. The record required by <u>paragraph (b)</u> of this section will be kept for the life of the source.

(b) The owner or operator of each storage vessel as specified in  $\S 60.110b(a)$  shall keep readily accessible records showing the dimension of the storage vessel and an analysis showing the capacity of the storage vessel.

(c) Except as provided in paragraphs (f) and (g) of this section, the owner or operator of each storage vessel either with a design capacity greater than or equal to  $151 \text{ m}^3$  storing a liquid with a maximum true vapor pressure greater than or equal to 3.5 kPa or with a design capacity greater than or equal to  $75 \text{ m}^3$  but less than  $151 \text{ m}^3$  storing a liquid with a maximum true vapor pressure greater than or equal to 15.0 kPa shall maintain a record of the VOL stored, the period of storage, and the maximum true vapor pressure of that VOL during the respective storage period.

(d) Except as provided in paragraph (g) of this section, the owner or operator of each storage vessel either with a design capacity greater than or equal to  $151 \text{ m}^3$  storing a liquid with a maximum true vapor pressure that is normally less than 5.2 kPa or with a design capacity greater than or equal to 75 m<sup>3</sup> but less than 151 m<sup>3</sup> storing a liquid with a maximum true vapor pressure that is normally less than 27.6 kPa shall notify the Administrator within 30 days when the maximum true vapor pressure of the liquid exceeds the respective maximum true vapor pressure values for each volume range. Beginning October 15, 2024, all subsequent notifications must be submitted in PDF format following the procedures specified in  $\frac{60.115b(e)}{2}$ .

(e) Available data on the storage temperature may be used to determine the maximum true vapor pressure as determined below.

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(1) For vessels operated above or below ambient temperatures, the maximum true vapor pressure is calculated based upon the highest expected calendar-month average of the storage temperature. For vessels operated at ambient temperatures, the maximum true vapor pressure is calculated based upon the maximum local monthly average ambient temperature as reported by the National Weather Service.

(2) For crude oil or refined petroleum products the vapor pressure may be obtained by the following:

(i) Available data on the Reid vapor pressure and the maximum expected storage temperature based on the highest expected calendar-month average temperature of the stored product may be used to determine the maximum true vapor pressure from nomographs contained in API Bulletin 2517 (incorporated by reference—see § 60.17), unless the Administrator specifically requests that the liquid be sampled, the actual storage temperature determined, and the Reid vapor pressure determined from the sample(s).

(ii) The true vapor pressure of each type of crude oil with a Reid vapor pressure less than 13.8 kPa or with physical properties that preclude determination by the recommended method is to be determined from available data and recorded if the estimated maximum true vapor pressure is greater than 3.5 kPa.

(3) For other liquids, the vapor pressure:

(i) May be obtained from standard reference texts, or

(ii) Determined by ASTM D2879-83, 96, or 97 (incorporated by reference—see § 60.17); or

(iii) Measured by an appropriate method approved by the Administrator; or

(iv) Calculated by an appropriate method approved by the Administrator.

(f) The owner or operator of each vessel storing a waste mixture of indeterminate or variable composition shall be subject to the following requirements.

(1) Prior to the initial filling of the vessel, the highest maximum true vapor pressure for the range of anticipated liquid compositions to be stored will be determined using the methods described in paragraph (e) of this section.

(2) For vessels in which the vapor pressure of the anticipated liquid composition is above the cutoff for monitoring but below the cutoff for controls as defined in (60.112b(a)), an initial physical test of the vapor pressure is required; and a physical test at least once every 6 months thereafter is required as determined by the following methods:

(i) ASTM D2879-83, 96, or 97 (incorporated by reference—see § 60.17); or

(ii) ASTM D323-82 or 94 (incorporated by reference—see § 60.17); or

(iii) As measured by an appropriate method as approved by the Administrator.

(g) The owner or operator of each vessel equipped with a closed vent system and control device meeting the specification of (60.112b) or with emissions reductions equipment as specified in 40 CFR (65.42(b)(4), (b)(5), (b)(6), (c)) is exempt from the requirements of paragraphs (c) and (d) of this section.

[52 FR 11429, Apr. 8, 1987, as amended at 65 FR 61756, Oct. 17, 2000; 65 FR 78276, Dec. 14, 2000; 68 FR 59333, Oct. 15, 2003; 89 FR 83319, Oct. 15, 2024]

### § 60.117b Delegation of authority.

(a) In delegating implementation and enforcement authority to a State under section 111(c) of the Act, the authorities contained in paragraph (b) of this section shall be retained by the Administrator and not transferred to a State.

(b) Authorities which will not be delegated to States: \$ 60.111b(f)(4), 60.114b, 60.116b(e)(3)(iii), 60.116b(e)(3)(iv), and 60.116b(f)(2)(iii), and approval of an alternative to any electronic reporting to the EPA required by this subpart.

[52 FR 11429, Apr. 8, 1987, as amended at 52 FR 22780, June 16, 1987; 89 FR 83319, Oct. 15, 2024]

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## Subpart IIII—Standards of Performance for Stationary Compression Ignition Internal Combustion Engines

### Source:

71 FR 39172, July 11, 2006, unless otherwise noted.

## What This Subpart Covers

## § 60.4200 Am I subject to this subpart?

(a) The provisions of this subpart are applicable to manufacturers, owners, and operators of stationary compression ignition (CI) internal combustion engines (ICE) and other persons as specified in <u>paragraphs (a)(1)</u> through (4) of this section. For the purposes of this subpart, the date that construction commences is the date the engine is ordered by the owner or operator.

(1) Manufacturers of stationary CI ICE with a displacement of less than 30 liters per cylinder where the model year is:

(i) 2007 or later, for engines that are not fire pump engines;

(ii) The model year listed in Table 3 to this subpart or later model year, for fire pump engines.

(2) Owners and operators of stationary CI ICE that commence construction after July 11, 2005, where the stationary CI ICE are:

(i) Manufactured after April 1, 2006, and are not fire pump engines, or

(ii) Manufactured as a certified National Fire Protection Association (NFPA) fire pump engine after July 1, 2006.

(3) Owners and operators of any stationary CI ICE that are modified or reconstructed after July 11, 2005 and any person that modifies or reconstructs any stationary CI ICE after July 11, 2005.

(4) The provisions of  $\S$  60.4208 of this subpart are applicable to all owners and operators of stationary CI ICE that commence construction after July 11, 2005.

(b) The provisions of this subpart are not applicable to stationary CI ICE being tested at a stationary CI ICE test cell/stand.

(c) If you are an owner or operator of an area source subject to this subpart, you are exempt from the obligation to obtain a permit under  $\frac{40 \text{ CFR part 70}}{10 \text{ CFR 70.3(a)}}$  or  $\frac{40 \text{ CFR part 71}}{10 \text{ CFR 71.3(a)}}$  for a reason other than your status as an area source under this subpart. Notwithstanding the previous sentence, you must continue to comply with the provisions of this subpart applicable to area sources.

(d) Stationary CI ICE may be eligible for exemption from the requirements of this subpart as described in <u>40 CFR part 1068</u>, <u>subpart C</u>, except that owners and operators, as well as manufacturers, may be eligible to request an exemption for national security.

(e) Owners and operators of facilities with CI ICE that are acting as temporary replacement units and that are located at a stationary source for less than 1 year and that have been properly certified as meeting the standards that would be applicable to such engine under the appropriate nonroad engine provisions, are not required to meet any other provisions under this subpart with regard to such engines.

[71 FR 39172, July 11, 2006, as amended at 76 FR 37967, June 28, 2011; 86 FR 34357, June 29, 2021]

### **Emission Standards for Manufacturers**

## § 60.4201 What emission standards must I meet for non-emergency engines if I am a stationary CI internal combustion engine manufacturer?

(a) Stationary CI internal combustion engine manufacturers must certify their 2007 model year and later non-emergency stationary CI ICE with a maximum engine power less than or equal to 2,237 kilowatt (KW) (3,000 horsepower (HP)) and a displacement of less than 10 liters per cylinder to the certification emission standards for new nonroad CI engines in <u>40 CFR</u> <u>1039.101</u>, <u>1039.102</u>, <u>1039.104</u>, <u>1039.105</u>, <u>1039.107</u>, and <u>1039.115</u> and <u>40 CFR part 1039</u>, <u>appendix I</u>, as applicable, for all pollutants, for the same model year and maximum engine power.

(b) Stationary CI internal combustion engine manufacturers must certify their 2007 through 2010 model year non-emergency stationary CI ICE with a maximum engine power greater than 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder to the emission standards in table 1 to this subpart, for all pollutants, for the same maximum engine power.

(c) Stationary CI internal combustion engine manufacturers must certify their 2011 model year and later non-emergency stationary CI ICE with a maximum engine power greater than 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder to the certification emission standards for new nonroad CI engines in <u>40 CFR 1039.101</u>, <u>40 CFR 1039.102</u>, <u>40 CFR 1039.105</u>, <u>40 CFR 1039.107</u>, and <u>40 CFR 1039.115</u>, as applicable, for all pollutants, for the same maximum engine power.

(d) Stationary CI internal combustion engine manufacturers must certify the following non-emergency stationary CI ICE to the appropriate Tier 2 emission standards for new marine CI engines as described in <u>40 CFR part 1042, appendix I</u>, for all pollutants, for the same displacement and rated power:

(1) Their 2007 model year through 2012 non-emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder;

(2) Their 2013 model year non-emergency stationary CI ICE with a maximum engine power greater than or equal to 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder; and

(3) Their 2013 model year non-emergency stationary CI ICE with a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder.

(e) Stationary CI internal combustion engine manufacturers must certify the following non-emergency stationary CI ICE to the certification emission standards and other requirements for new marine CI engines in <u>40 CFR 1042.101</u>, <u>40 CFR 1042.101</u>, <u>40 CFR 1042.115</u>, <u>40 CFR 1042.120</u>, and <u>40 CFR 1042.145</u>, as applicable, for all pollutants, for the same displacement and maximum engine power:

(1) Their 2013 model year non-emergency stationary CI ICE with a maximum engine power less than 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder; and

(2) Their 2014 model year and later non-emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder.

(f) Notwithstanding the requirements in <u>paragraphs (a)</u> through (c) of this section, stationary non-emergency CI ICE identified in <u>paragraphs (a)</u> and (c) of this section may be certified to the provisions of 40 CFR part 1042 for commercial engines that are applicable for the engine's model year, displacement, power density, and maximum engine power if the engines will be used solely in either or both of the following locations:

(1) Remote areas of Alaska; and

(2) Marine offshore installations.

(g) Notwithstanding the requirements in <u>paragraphs (a)</u> through (f) of this section, stationary CI internal combustion engine manufacturers are not required to certify reconstructed engines; however manufacturers may elect to do so. The reconstructed engine must be certified to the emission standards specified in <u>paragraphs (a)</u> through (e) of this section that are applicable to the model year, maximum engine power, and displacement of the reconstructed stationary CI ICE.

(h) Stationary CI ICE certified to the standards in  $\frac{40 \text{ CFR part 1039}}{1000 \text{ CFR part 1039}}$  and equipped with auxiliary emission control devices (AECDs) as specified in  $\frac{40 \text{ CFR 1039.665}}{1000 \text{ CFR part 1039}}$  must meet the Tier 1 certification emission standards for new nonroad CI engines in  $\frac{40 \text{ CFR part 1039}}{1000 \text{ cFR 1039.665}}$ . When the AECD is activated during a qualified emergency situation. A qualified emergency situation has ended and the AECD is deactivated, the engine must resume meeting the otherwise applicable emission standard specified in this section.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>76 FR 37967</u>, June 28, 2011; <u>81 FR 44219</u>, July 7, 2016; <u>86 FR 34357</u>, June 29, 2021]

## § 60.4202 What emission standards must I meet for emergency engines if I am a stationary CI internal combustion engine manufacturer?

(a) Stationary CI internal combustion engine manufacturers must certify their 2007 model year and later emergency stationary CI ICE with a maximum engine power less than or equal to 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder that are not fire pump engines to the emission standards specified in <u>paragraphs (a)(1)</u> through (2) of this section.

(1) For engines with a maximum engine power less than 37 KW (50 HP):

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(i) The Tier 2 emission standards for new nonroad CI engines for the appropriate rated power as described in <u>40 CFR part</u> <u>1039, appendix I</u>, for all pollutants and the smoke standards as specified in <u>40 CFR 1039.105</u> for model year 2007 engines; and

(2) For engines with a rated power greater than or equal to 37 KW (50 HP), the Tier 2 or Tier 3 emission standards for new nonroad CI engines for the same rated power as described in <u>40 CFR part 1039, appendix I</u>, for all pollutants and the smoke standards as specified in <u>40 CFR 1039.105</u> beginning in model year 2007.

(b) Stationary CI internal combustion engine manufacturers must certify their 2007 model year and later emergency stationary CI ICE with a maximum engine power greater than 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder that are not fire pump engines to the emission standards specified in <u>paragraphs (b)(1)</u> through (2) of this section.

(1) For 2007 through 2010 model years, the emission standards in table 1 to this subpart, for all pollutants, for the same maximum engine power.

(2) For 2011 model year and later, the Tier 2 emission standards as described in <u>40 CFR part 1039</u>, appendix I, for all pollutants and the smoke standards as specified in <u>40 CFR 1039.105</u>.

(c) [Reserved]

(d) Beginning with the model years in table 3 to this subpart, stationary CI internal combustion engine manufacturers must certify their fire pump stationary CI ICE to the emission standards in table 4 to this subpart, for all pollutants, for the same model year and NFPA nameplate power.

(e) Stationary CI internal combustion engine manufacturers must certify the following emergency stationary CI ICE that are not fire pump engines to the appropriate Tier 2 emission standards for new marine CI engines as described in <u>40 CFR part</u> <u>1042</u>, <u>appendix I</u>, for all pollutants, for the same displacement and rated power:

(1) Their 2007 model year through 2012 emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder;

(2) Their 2013 model year and later emergency stationary CI ICE with a maximum engine power greater than or equal to 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder;

(3) Their 2013 model year emergency stationary CI ICE with a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder; and

(4) Their 2014 model year and later emergency stationary CI ICE with a maximum engine power greater than or equal to 2,000 KW (2,682 HP) and a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder.

(f) Stationary CI internal combustion engine manufacturers must certify the following emergency stationary CI ICE to the certification emission standards and other requirements applicable to Tier 3 new marine CI engines in <u>40 CFR 1042.101</u>, <u>40</u> <u>CFR 1042.107</u>, <u>40 CFR 1042.115</u>, <u>40 CFR 1042.120</u>, and <u>40 CFR 1042.145</u>, for all pollutants, for the same displacement and maximum engine power:

(1) Their 2013 model year and later emergency stationary CI ICE with a maximum engine power less than 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder; and

(2) Their 2014 model year and later emergency stationary CI ICE with a maximum engine power less than 2,000 KW (2,682 HP) and a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder.

(g) Notwithstanding the requirements in <u>paragraphs (a)</u> through (d) of this section, stationary emergency CI ICE identified in <u>paragraphs (a)</u> and (c) of this section may be certified to the provisions of <u>40 CFR part 1042</u> for commercial engines that are applicable for the engine's model year, displacement, power density, and maximum engine power if the engines will be used solely in either or both of the locations identified in <u>paragraphs (g)(1)</u> and (2) of this section. Engines that would be subject to the Tier 4 standards in <u>40 CFR part 1042</u> that are used solely in either or both of the locations identified in <u>paragraphs (g)(1)</u> and (2) of this section may instead continue to be certified to the previous tier of standards in <u>40 CFR</u> <u>part 1042</u>. The previous tier is Tier 3 in most cases; however, the previous tier is Tier 2 if there are no Tier 3 standards specified for engines of a certain size or power rating.

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(1) Remote areas of Alaska; and

(2) Marine offshore installations.

(h) Notwithstanding the requirements in <u>paragraphs (a)</u> through (f) of this section, stationary CI internal combustion engine manufacturers are not required to certify reconstructed engines; however manufacturers may elect to do so. The reconstructed engine must be certified to the emission standards specified in <u>paragraphs (a)</u> through (f) of this section that are applicable to the model year, maximum engine power and displacement of the reconstructed emergency stationary CI ICE.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>76 FR 37968</u>, June 28, 2011; <u>81 FR 44219</u>, July 7, 2016; <u>86 FR 34358</u>, June 29, 2021; <u>88 FR 4471</u>, Jan. 24, 2023]

## § 60.4203 How long must my engines meet the emission standards if I am a manufacturer of stationary CI internal combustion engines?

Engines manufactured by stationary CI internal combustion engine manufacturers must meet the emission standards as required in  $\frac{8860.4201}{1000}$  and  $\frac{60.4202}{10000}$  during the certified emissions life of the engines.

[<u>76 FR 37968</u>, June 28, 2011]

### **Emission Standards for Owners and Operators**

## § 60.4204 What emission standards must I meet for non-emergency engines if I am an owner or operator of a stationary CI internal combustion engine?

(a) Owners and operators of pre-2007 model year non-emergency stationary CI ICE with a displacement of less than 10 liters per cylinder must comply with the emission standards in table 1 to this subpart. Owners and operators of pre-2007 model year non-emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder must comply with the Tier 1 emission standards in <u>40 CFR part 1042, appendix I</u>.

(b) Owners and operators of 2007 model year and later non-emergency stationary CI ICE with a displacement of less than 30 liters per cylinder must comply with the emission standards for new CI engines in  $\S$  60.4201 for their 2007 model year and later stationary CI ICE, as applicable.

(c) Owners and operators of non-emergency stationary CI engines with a displacement of greater than or equal to 30 liters per cylinder must meet the following requirements:

(1) For engines installed prior to January 1, 2012, limit the emissions of  $NO_X$  in the stationary CI internal combustion engine exhaust to the following:

(i) 17.0 grams per kilowatt-hour (g/KW-hr) (12.7 grams per horsepower-hr (g/HP-hr)) when maximum engine speed is less than 130 revolutions per minute (rpm);

(ii)  $45 \cdot n^{-0.2}$  g/KW-hr ( $34 \cdot n^{-0.2}$  g/HP-hr) when maximum engine speed is 130 or more but less than 2,000 rpm, where n is maximum engine speed; and

(iii) 9.8 g/KW-hr (7.3 g/HP-hr) when maximum engine speed is 2,000 rpm or more.

(2) For engines installed on or after January 1, 2012 and before January 1, 2016, limit the emissions of  $NO_X$  in the stationary CI internal combustion engine exhaust to the following:

(i) 14.4 g/KW-hr (10.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii)  $44 \cdot n^{-0.23}$  g/KW-hr (33  $\cdot n^{-0.23}$  g/HP-hr) when maximum engine speed is greater than or equal to 130 but less than 2,000 rpm and where n is maximum engine speed; and

(iii) 7.7 g/KW-hr (5.7 g/HP-hr) when maximum engine speed is greater than or equal to 2,000 rpm.

(3) For engines installed on or after January 1, 2016, limit the emissions of  $NO_X$  in the stationary CI internal combustion engine exhaust to the following:

(i) 3.4 g/KW-hr (2.5 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii)  $9.0 \cdot n^{-0.20}$  g/KW-hr ( $6.7 \cdot n^{-0.20}$  g/HP-hr) where n (maximum engine speed) is 130 or more but less than 2,000 rpm; and

(iii) 2.0 g/KW-hr (1.5 g/HP-hr) where maximum engine speed is greater than or equal to 2,000 rpm.

(4) Reduce particulate matter (PM) emissions by 60 percent or more, or limit the emissions of PM in the stationary CI internal combustion engine exhaust to 0.15 g/KW-hr (0.11 g/HP-hr).

(d) Owners and operators of non-emergency stationary CI ICE with a displacement of less than 30 liters per cylinder who conduct performance tests in-use must meet the not-to-exceed (NTE) standards as indicated in  $\frac{\& 60.4212}{\& 60.4212}$ .

(e) Owners and operators of any modified or reconstructed non-emergency stationary CI ICE subject to this subpart must meet the emission standards applicable to the model year, maximum engine power, and displacement of the modified or reconstructed non-emergency stationary CI ICE that are specified in <u>paragraphs (a)</u> through (d) of this section.

(f) Owners and operators of stationary CI ICE certified to the standards in <u>40 CFR part 1039</u> and equipped with AECDs as specified in <u>40 CFR 1039.665</u> must meet the Tier 1 certification emission standards for new nonroad CI engines in <u>40 CFR part 1039</u>, appendix I, while the AECD is activated during a qualified emergency situation. A qualified emergency situation is defined in <u>40 CFR 1039.665</u>. When the qualified emergency situation has ended and the AECD is deactivated, the engine must resume meeting the otherwise applicable emission standard specified in this section.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>76 FR 37968</u>, June 28, 2011; <u>81 FR 44219</u>, July 7, 2016; <u>86 FR 34358</u>, June 29, 2021]

## § 60.4205 What emission standards must I meet for emergency engines if I am an owner or operator of a stationary CI internal combustion engine?

(a) Owners and operators of pre-2007 model year emergency stationary CI ICE with a displacement of less than 10 liters per cylinder that are not fire pump engines must comply with the emission standards in Table 1 to this subpart. Owners and operators of pre-2007 model year emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder that are not fire pump engines must comply with the Tier 1 emission standards in <u>40 CFR part 1042</u>, appendix I.

(b) Owners and operators of 2007 model year and later emergency stationary CI ICE with a displacement of less than 30 liters per cylinder that are not fire pump engines must comply with the emission standards for new nonroad CI engines in  $\S$  <u>60.4202</u>, for all pollutants, for the same model year and maximum engine power for their 2007 model year and later emergency stationary CI ICE.

(c) Owners and operators of fire pump engines with a displacement of less than 30 liters per cylinder must comply with the emission standards in table 4 to this subpart, for all pollutants.

(d) Owners and operators of emergency stationary CI engines with a displacement of greater than or equal to 30 liters per cylinder must meet the requirements in this section.

(1) For engines installed prior to January 1, 2012, limit the emissions of  $NO_X$  in the stationary CI internal combustion engine exhaust to the following:

(i) 17.0 g/KW-hr (12.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii)  $45 \cdot n^{-0.2}$  g/KW-hr ( $34 \cdot n^{-0.2}$  g/HP-hr) when maximum engine speed is 130 or more but less than 2,000 rpm, where n is maximum engine speed; and

(iii) 9.8 g/kW-hr (7.3 g/HP-hr) when maximum engine speed is 2,000 rpm or more.

(2) For engines installed on or after January 1, 2012, limit the emissions of  $NO_X$  in the stationary CI internal combustion engine exhaust to the following:

(i) 14.4 g/KW-hr (10.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii)  $44 \cdot n^{-0.23}$  g/KW-hr (33  $\cdot n^{-0.23}$  g/HP-hr) when maximum engine speed is greater than or equal to 130 but less than 2,000 rpm and where n is maximum engine speed; and

(iii) 7.7 g/KW-hr (5.7 g/HP-hr) when maximum engine speed is greater than or equal to 2,000 rpm.

(3) Limit the emissions of PM in the stationary CI internal combustion engine exhaust to 0.40 g/KW-hr (0.30 g/HP-hr).

(e) Owners and operators of emergency stationary CI ICE with a displacement of less than 30 liters per cylinder who conduct performance tests in-use must meet the NTE standards as indicated in  $\frac{60.4212}{2}$ .

(f) Owners and operators of any modified or reconstructed emergency stationary CI ICE subject to this subpart must meet the emission standards applicable to the model year, maximum engine power, and displacement of the modified or reconstructed CI ICE that are specified in <u>paragraphs (a)</u> through (<u>e</u>) of this section.

[71 FR 39172, July 11, 2006, as amended at 76 FR 37969, June 28, 2011; 86 FR 34358, June 29, 2021]

## § 60.4206 How long must I meet the emission standards if I am an owner or operator of a stationary CI internal combustion engine?

Owners and operators of stationary CI ICE must operate and maintain stationary CI ICE that achieve the emission standards as required in  $\frac{8860.4204}{0.000}$  and  $\frac{60.4205}{0.0000}$  over the entire life of the engine.

### [<u>76 FR 37969</u>, June 28, 2011]

### **Fuel Requirements for Owners and Operators**

# § 60.4207 What fuel requirements must I meet if I am an owner or operator of a stationary CI internal combustion engine subject to this subpart?

### (a) [Reserved]

(b) Beginning October 1, 2010, owners and operators of stationary CI ICE subject to this subpart with a displacement of less than 30 liters per cylinder that use diesel fuel must use diesel fuel that meets the requirements of <u>40 CFR 1090.305</u> for nonroad diesel fuel, except that any existing diesel fuel purchased (or otherwise obtained) prior to October 1, 2010, may be used until depleted.

### (c) [Reserved]

(d) Beginning June 1, 2012, owners and operators of stationary CI ICE subject to this subpart with a displacement of greater than or equal to 30 liters per cylinder must use diesel fuel that meets a maximum per-gallon sulfur content of 1,000 parts per million (ppm).

(e) Stationary CI ICE that have a national security exemption under  $\S 60.4200(d)$  are also exempt from the fuel requirements in this section.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>76 FR 37969</u>, June 28, 2011; <u>78 FR 6695</u>, Jan. 30, 2013; <u>85 FR 78463</u>, Dec. 4, 2020]

### Other Requirements for Owners and Operators

### § 60.4208 What is the deadline for importing or installing stationary CI ICE produced in previous model years?

(a) After December 31, 2008, owners and operators may not install stationary CI ICE (excluding fire pump engines) that do not meet the applicable requirements for 2007 model year engines.

(b) After December 31, 2009, owners and operators may not install stationary CI ICE with a maximum engine power of less than 19 KW (25 HP) (excluding fire pump engines) that do not meet the applicable requirements for 2008 model year engines.

(c) After December 31, 2014, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 19 KW (25 HP) and less than 56 KW (75 HP) that do not meet the applicable requirements for 2013 model year non-emergency engines.

(d) After December 31, 2013, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 56 KW (75 HP) and less than 130 KW (175 HP) that do not meet the applicable requirements for 2012 model year non-emergency engines.

(e) After December 31, 2012, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 130 KW (175 HP), including those above 560 KW (750 HP), that do not meet the applicable requirements for 2011 model year non-emergency engines.

(f) After December 31, 2016, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 560 KW (750 HP) that do not meet the applicable requirements for 2015 model year non-emergency engines.

(g) After December 31, 2018, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power greater than or equal to 600 KW (804 HP) and less than 2,000 KW (2,680 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder that do not meet the applicable requirements for 2017 model year non-emergency engines.

(h) In addition to the requirements specified in \$ 60.4201, 60.4202, 60.4204, and 60.4205, it is prohibited to import stationary CI ICE with a displacement of less than 30 liters per cylinder that do not meet the applicable requirements specified in paragraphs (a) through (g) of this section after the dates specified in paragraphs (a) through (g) of this section.

(i) The requirements of this section do not apply to owners or operators of stationary CI ICE that have been modified, reconstructed, and do not apply to engines that were removed from one existing location and reinstalled at a new location.

[71 FR 39172, July 11, 2006, as amended at 76 FR 37969, June 28, 2011]

### § 60.4209 What are the monitoring requirements if I am an owner or operator of a stationary CI internal combustion engine?

If you are an owner or operator, you must meet the monitoring requirements of this section. In addition, you must also meet the monitoring requirements specified in  $\S$  60.4211.

(a) If you are an owner or operator of an emergency stationary CI internal combustion engine that does not meet the standards applicable to non-emergency engines, you must install a non-resettable hour meter prior to startup of the engine.

(b) If you are an owner or operator of a stationary CI internal combustion engine equipped with a diesel particulate filter to comply with the emission standards in  $\S$  60.4204, the diesel particulate filter must be installed with a backpressure monitor that notifies the owner or operator when the high backpressure limit of the engine is approached.

[71 FR 39172, July 11, 2006, as amended at 76 FR 37969, June 28, 2011]

### **Compliance Requirements**

## § 60.4210 What are my compliance requirements if I am a stationary CI internal combustion engine manufacturer?

(a) Stationary CI internal combustion engine manufacturers must certify their stationary CI ICE with a displacement of less than 10 liters per cylinder to the emission standards specified in  $\frac{8}{60.4201(a)}$  through (c) and  $\frac{60.4202(a)}{(a)}$ , (b), and (d) using the certification procedures required in 40 CFR part 1039, subpart C, and must test their engines as specified in 40 CFR part 1039. For the purposes of this subpart, engines certified to the standards in Table 1 to this subpart shall be subject to the same certification procedures required for engines certified to the Tier 1 standards in 40 CFR part 1039, appendix I. For the purposes of this subpart, engines certified to the standards in Table 4 to this subpart shall be subject to the same certification procedures required for engines certified to the Tier 1 standards in 40 CFR part 1039, appendix I, except that engines with NFPA nameplate power of less than 37 KW (50 HP) certified to model year 2011 or later standards shall be subject to the same requirements as engines certified to the standards in 40 CFR part 1039.

(b) Stationary CI internal combustion engine manufacturers must certify their stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder to the emission standards specified in §§ 60.4201(d) and (e) and 60.4202(e) and (f) using the certification procedures required in 40 CFR part 1042, subpart C, and must test their engines as specified in 40 CFR part 1042.

(c) Stationary CI internal combustion engine manufacturers must meet the requirements of 40 CFR

1039.120, 1039.125, 1039.130, and 1039.135 and 40 CFR part 1068 for engines that are certified to the emission standards in 40 CFR part 1039. Stationary CI internal combustion engine manufacturers must meet the corresponding provisions of 40 CFR part 1042 for engines that would be covered by that part if they were nonroad (including marine) engines. Labels on such engines must refer to stationary engines, rather than or in addition to nonroad or marine engines, as appropriate. Stationary CI internal combustion engine manufacturers must label their engines according to paragraphs (c)(1) through (3) of this section.

(1) Stationary CI internal combustion engines manufactured from January 1, 2006 to March 31, 2006 (January 1, 2006 to June 30, 2006 for fire pump engines), other than those that are part of certified engine families under the nonroad CI engine regulations, must be labeled according to 40 CFR 1039.20.

(2) Stationary CI internal combustion engines manufactured from April 1, 2006 to December 31, 2006 (or, for fire pump engines, July 1, 2006 to December 31 of the year preceding the year listed in table 3 to this subpart) must be labeled according to paragraphs (c)(2)(i) through (iii) of this section:

(i) Stationary CI internal combustion engines that are part of certified engine families under the nonroad regulations must meet the labeling requirements for nonroad CI engines, but do not have to meet the labeling requirements in <u>40 CFR 1039.20</u>.

(ii) Stationary CI internal combustion engines that meet Tier 1 requirements (or requirements for fire pumps) under this subpart, but do not meet the requirements applicable to nonroad CI engines must be labeled according to <u>40 CFR 1039.20</u>. The engine manufacturer may add language to the label clarifying that the engine meets Tier 1 requirements (or requirements for fire pumps) of this subpart.

(iii) Stationary CI internal combustion engines manufactured after April 1, 2006 that do not meet Tier 1 requirements of this subpart, or fire pumps engines manufactured after July 1, 2006 that do not meet the requirements for fire pumps under this subpart, may not be used in the U.S. If any such engines are manufactured in the U.S. after April 1, 2006 (July 1, 2006 for fire pump engines), they must be exported or must be brought into compliance with the appropriate standards prior to initial operation. The export provisions of  $\frac{40 \text{ CFR } 1068.230}{40 \text{ CFR } 1068.230}$  would apply to engines for export and the manufacturers must label such engines according to  $\frac{40 \text{ CFR } 1068.230}{40 \text{ CFR } 1068.230}$ .

(3) Stationary CI internal combustion engines manufactured after January 1, 2007 (for fire pump engines, after January 1 of the year listed in table 3 to this subpart, as applicable) must be labeled according to <u>paragraphs (c)(3)(i)</u> through <u>(iii)</u> of this section.

(i) Stationary CI internal combustion engines that meet the requirements of this subpart and the corresponding requirements for nonroad (including marine) engines of the same model year and HP must be labeled according to the provisions in  $\frac{40}{CFR \text{ part } 1039}$  or  $\frac{1042}{2}$ , as appropriate.

(ii) Stationary CI internal combustion engines that meet the requirements of this subpart, but are not certified to the standards applicable to nonroad (including marine) engines of the same model year and HP must be labeled according to the provisions in  $\frac{40 \text{ CFR part } 1039}{1042}$ , as appropriate, but the words "stationary" must be included instead of "nonroad" or "marine" on the label. In addition, such engines must be labeled according to  $\frac{40 \text{ CFR } 1039.20}{1042}$ .

(iii) Stationary CI internal combustion engines that do not meet the requirements of this subpart must be labeled according to  $\frac{40 \text{ CFR } 1068.230}{40 \text{ CFR } 1068.230}$  and must be exported under the provisions of  $\frac{40 \text{ CFR } 1068.230}{40 \text{ CFR } 1068.230}$ .

(d) An engine manufacturer certifying an engine family or families to standards under this subpart that are identical to standards applicable under <u>40 CFR part 1039</u> or <u>1042</u> for that model year may certify any such family that contains both nonroad (including marine) and stationary engines as a single engine family and/or may include any such family containing stationary engines in the averaging, banking, and trading provisions applicable for such engines under those parts.

(e) Manufacturers of engine families discussed in <u>paragraph (d)</u> of this section may meet the labeling requirements referred to in <u>paragraph (c)</u> of this section for stationary CI ICE by either adding a separate label containing the information required in <u>paragraph (c)</u> of this section or by adding the words "and stationary" after the word "nonroad" or "marine," as appropriate, to the label.

(f) Starting with the model years shown in table 5 to this subpart, stationary CI internal combustion engine manufacturers must add a permanent label stating that the engine is for stationary emergency use only to each new emergency stationary CI internal combustion engine greater than or equal to 19 KW (25 HP) that meets all the emission standards for emergency engines in  $\frac{60.4202}{50.4201}$  but does not meet all the emission standards for non-emergency engines in  $\frac{60.4201}{50.4201}$ . The label must be added according to the labeling requirements specified in  $\frac{40 \text{ CFR } 1039.135(b)}{50.135(b)}$ . Engine manufacturers must specify in the owner's manual that operation of emergency engines is limited to emergency operations and required maintenance and testing.

(g) Manufacturers of fire pump engines may use the test cycle in table 6 to this subpart for testing fire pump engines and may test at the NFPA certified nameplate HP, provided that the engine is labeled as "Fire Pump Applications Only".

(h) Engine manufacturers, including importers, may introduce into commerce uncertified engines or engines certified to earlier standards that were manufactured before the new or changed standards took effect until inventories are depleted, as long as such engines are part of normal inventory. For example, if the engine manufacturers' normal industry practice is to keep on hand a one-month supply of engines based on its projected sales, and a new tier of standards starts to apply for the 2009 model year, the engine manufacturer may manufacture engines based on the normal inventory requirements late in the

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2008 model year, and sell those engines for installation. The engine manufacturer may not circumvent the provisions of § 60.4201 or § 60.4202 by stockpiling engines that are built before new or changed standards take effect. Stockpiling of such engines beyond normal industry practice is a violation of this subpart.

(i) The replacement engine provisions of <u>40 CFR 1068.240</u> are applicable to stationary CI engines replacing existing equipment that is less than 15 years old.

(j) Stationary CI ICE manufacturers may equip their stationary CI internal combustion engines certified to the emission standards in <u>40 CFR part 1039</u> with AECDs for qualified emergency situations according to the requirements of <u>40 CFR 1039.665</u>. Manufacturers of stationary CI ICE equipped with AECDs as allowed by <u>40 CFR 1039.665</u> must meet all the requirements in <u>40 CFR 1039.665</u> that apply to manufacturers. Manufacturers must document that the engine complies with the Tier 1 standard in <u>40 CFR part 1039</u>, appendix I, when the AECD is activated. Manufacturers must provide any relevant testing, engineering analysis, or other information in sufficient detail to support such statement when applying for certification (including amending an existing certificate) of an engine equipped with an AECD as allowed by <u>40 CFR 1039.665</u>.

(k) Manufacturers of any size may certify their emergency stationary CI internal combustion engines under this section using assigned deterioration factors established by EPA, consistent with <u>40 CFR 1039.240</u> and <u>1042.240</u>.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>76 FR 37969</u>, June 28, 2011; <u>81 FR 44219</u>, July 7, 2016; <u>86 FR 34358</u>, June 29, 2021]

## § 60.4211 What are my compliance requirements if I am an owner or operator of a stationary CI internal combustion engine?

(a) If you are an owner or operator and must comply with the emission standards specified in this subpart, you must do all of the following, except as permitted under <u>paragraph (g)</u> of this section:

(1) Operate and maintain the stationary CI internal combustion engine and control device according to the manufacturer's emission-related written instructions;

(2) Change only those emission-related settings that are permitted by the manufacturer; and

(3) Meet the requirements of <u>40 CFR part 1068</u>, as they apply to you.

(b) If you are an owner or operator of a pre-2007 model year stationary CI internal combustion engine and must comply with the emission standards specified in § 60.4204(a) or § 60.4205(a), or if you are an owner or operator of a CI fire pump engine that is manufactured prior to the model years in table 3 to this subpart and must comply with the emission standards specified in § 60.4205(c), you must demonstrate compliance according to one of the methods specified in paragraphs (b)(1) through (5) of this section.

(1) Purchasing an engine certified to emission standards for the same model year and maximum engine power as described in <u>40 CFR parts 1039</u> and <u>1042</u>, as applicable. The engine must be installed and configured according to the manufacturer's specifications.

(2) Keeping records of performance test results for each pollutant for a test conducted on a similar engine. The test must have been conducted using the same methods specified in this subpart and these methods must have been followed correctly.

(3) Keeping records of engine manufacturer data indicating compliance with the standards.

(4) Keeping records of control device vendor data indicating compliance with the standards.

(5) Conducting an initial performance test to demonstrate compliance with the emission standards according to the requirements specified in  $\S$  60.4212, as applicable.

(c) If you are an owner or operator of a 2007 model year and later stationary CI internal combustion engine and must comply with the emission standards specified in § 60.4204(b) or § 60.4205(b), or if you are an owner or operator of a CI fire pump engine that is manufactured during or after the model year that applies to your fire pump engine power rating in table 3 to this subpart and must comply with the emission standards specified in § 60.4204(b), or § 60.4205(c), you must comply by purchasing an engine certified to the emission standards in § 60.4204(b), or § 60.4205(b) or (c), as applicable, for the same model year and maximum (or in the case of fire pumps, NFPA nameplate) engine power. The engine must be installed and configured according to the manufacturer's emission-related specifications, except as permitted in paragraph (g) of this section.

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(d) If you are an owner or operator and must comply with the emission standards specified in  $\S$  60.4204(c) or  $\S$  60.4205(d), you must demonstrate compliance according to the requirements specified in paragraphs (d)(1) through (3) of this section.

(1) Conducting an initial performance test to demonstrate initial compliance with the emission standards as specified in  $\S$  <u>60.4213</u>.

(2) Establishing operating parameters to be monitored continuously to ensure the stationary internal combustion engine continues to meet the emission standards. The owner or operator must petition the Administrator for approval of operating parameters to be monitored continuously. The petition must include the information described in <u>paragraphs</u> (d)(2)(i) through (v) of this section.

(i) Identification of the specific parameters you propose to monitor continuously;

(ii) A discussion of the relationship between these parameters and  $NO_X$  and PM emissions, identifying how the emissions of these pollutants change with changes in these parameters, and how limitations on these parameters will serve to limit  $NO_X$  and PM emissions;

(iii) A discussion of how you will establish the upper and/or lower values for these parameters which will establish the limits on these parameters in the operating limitations;

(iv) A discussion identifying the methods and the instruments you will use to monitor these parameters, as well as the relative accuracy and precision of these methods and instruments; and

(v) A discussion identifying the frequency and methods for recalibrating the instruments you will use for monitoring these parameters.

(3) For non-emergency engines with a displacement of greater than or equal to 30 liters per cylinder, conducting annual performance tests to demonstrate continuous compliance with the emission standards as specified in  $\frac{60.4213}{1000}$ .

(e) If you are an owner or operator of a modified or reconstructed stationary CI internal combustion engine and must comply with the emission standards specified in § 60.4204(e) or § 60.4205(f), you must demonstrate compliance according to one of the methods specified in paragraphs (e)(1) or (2) of this section.

(1) Purchasing, or otherwise owning or operating, an engine certified to the emission standards in  $\S$  60.4204(e) or  $\S$  60.4205(f), as applicable.

(2) Conducting a performance test to demonstrate initial compliance with the emission standards according to the requirements specified in § 60.4212 or § 60.4213, as appropriate. The test must be conducted within 60 days after the engine commences operation after the modification or reconstruction.

(f) If you own or operate an emergency stationary ICE, you must operate the emergency stationary ICE according to the requirements in <u>paragraphs (f)(1)</u> through (3) of this section. In order for the engine to be considered an emergency stationary ICE under this subpart, any operation other than emergency operation, maintenance and testing, and operation in nonemergency situations for 50 hours per year, as described in paragraphs (f)(1) through (3), is prohibited. If you do not operate the engine according to the requirements in paragraphs (f)(1) through (3), the engine will not be considered an emergency engine under this subpart and must meet all requirements for non-emergency engines.

(1) There is no time limit on the use of emergency stationary ICE in emergency situations.

(2) You may operate your emergency stationary ICE for the purpose specified in <u>paragraph (f)(2)(i)</u> of this section for a maximum of 100 hours per calendar year. Any operation for non-emergency situations as allowed by <u>paragraph (f)(3)</u> of this section counts as part of the 100 hours per calendar year allowed by this <u>paragraph (f)(2)</u>.

(i) Emergency stationary ICE may be operated for maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor, the regional transmission organization or equivalent balancing authority and transmission operator, or the insurance company associated with the engine. The owner or operator may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if the owner or operator maintains records indicating that federal, state, or local standards require maintenance and testing of emergency ICE beyond 100 hours per calendar year.

(ii)-(iii) [Reserved]

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(3) Emergency stationary ICE may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing provided in paragraph (f)(2) of this section. Except as provided in paragraph (f)(3)(i) of this section, the 50 hours per calendar year for non-emergency situations cannot be used for peak shaving or non-emergency demand response, or to generate income for a facility to an electric grid or otherwise supply power as part of a financial arrangement with another entity.

(i) The 50 hours per year for non-emergency situations can be used to supply power as part of a financial arrangement with another entity if all of the following conditions are met:

(A) The engine is dispatched by the local balancing authority or local transmission and distribution system operator;

(B) The dispatch is intended to mitigate local transmission and/or distribution limitations so as to avert potential voltage collapse or line overloads that could lead to the interruption of power supply in a local area or region.

(C) The dispatch follows reliability, emergency operation or similar protocols that follow specific NERC, regional, state, public utility commission or local standards or guidelines.

(D) The power is provided only to the facility itself or to support the local transmission and distribution system.

(E) The owner or operator identifies and records the entity that dispatches the engine and the specific NERC, regional, state, public utility commission or local standards or guidelines that are being followed for dispatching the engine. The local balancing authority or local transmission and distribution system operator may keep these records on behalf of the engine owner or operator.

#### (ii) [Reserved]

(g) If you do not install, configure, operate, and maintain your engine and control device according to the manufacturer's emission-related written instructions, or you change emission-related settings in a way that is not permitted by the manufacturer, you must demonstrate compliance as follows:

(1) If you are an owner or operator of a stationary CI internal combustion engine with maximum engine power less than 100 HP, you must keep a maintenance plan and records of conducted maintenance to demonstrate compliance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions. In addition, if you do not install and configure the engine and control device according to the manufacturer's emission-related written instructions, or you change the emission-related settings in a way that is not permitted by the manufacturer, you must conduct an initial performance test to demonstrate compliance with the applicable emission standards within 1 year of such action.

(2) If you are an owner or operator of a stationary CI internal combustion engine greater than or equal to 100 HP and less than or equal to 500 HP, you must keep a maintenance plan and records of conducted maintenance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions. In addition, you must conduct an initial performance test to demonstrate compliance with the applicable emission standards within 1 year of startup, or within 1 year after an engine and control device is no longer installed, configured, operated, and maintained in accordance with the manufacturer's emission-related written instructions, or within 1 year after you change emission-related settings in a way that is not permitted by the manufacturer.

(3) If you are an owner or operator of a stationary CI internal combustion engine greater than 500 HP, you must keep a maintenance plan and records of conducted maintenance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions. In addition, you must conduct an initial performance test to demonstrate compliance with the applicable emission standards within 1 year of startup, or within 1 year after an engine and control device is no longer installed, configured, operated, and maintained in accordance with the manufacturer's emission-related written instructions, or within 1 year after you change emission-related settings in a way that is not permitted by the manufacturer. You must conduct subsequent performance testing every 8,760 hours of engine operation or 3 years, whichever comes first, thereafter to demonstrate compliance with the applicable emission standards.

(h) The requirements for operators and prohibited acts specified in <u>40 CFR 1039.665</u> apply to owners or operators of stationary CI ICE equipped with AECDs for qualified emergency situations as allowed by <u>40 CFR 1039.665</u>.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>76 FR 37970</u>, June 28, 2011; <u>78 FR 6695</u>, Jan. 30, 2013; <u>81 FR 44219</u>, July 7, 2016; <u>86 FR 34359</u>, June 29, 2021; <u>87 FR 48605</u>, Aug. 10, 2022]

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## Testing Requirements for Owners and Operators

# § 60.4212 What test methods and other procedures must I use if I am an owner or operator of a stationary CI internal combustion engine with a displacement of less than 30 liters per cylinder?

Owners and operators of stationary CI ICE with a displacement of less than 30 liters per cylinder who conduct performance tests pursuant to this subpart must do so according to paragraphs (a) through (e) of this section.

(a) The performance test must be conducted according to the in-use testing procedures in <u>40 CFR part 1039</u>, <u>subpart F</u>, for stationary CI ICE with a displacement of less than 10 liters per cylinder, and according to <u>40 CFR part 1042</u>, <u>subpart F</u>, for stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder. Alternatively, stationary CI ICE that are complying with Tier 2 or Tier 3 emission standards as described in <u>40 CFR part 1042</u>, <u>appendix I</u>, may follow the testing procedures specified in <u>§ 60.4213</u>, as appropriate.

(c) Exhaust emissions from stationary CI ICE subject to Tier 2 or Tier 3 emission standards as described in  $\frac{40 \text{ CFR part}}{1039, \text{ appendix I}}$ , or Tier 2 emission standards as described in  $\frac{40 \text{ CFR part }1042, \text{ appendix I}}{1042, \text{ appendix I}}$ , must not exceed the NTE numerical requirements, rounded to the same number of decimal places as the applicable standard, determined from the following equation:

# NTE requirement for each pollutant = $(1.25) \times (STD)$ (Eq. 1)

Where:

STD = The standard specified for that pollutant in  $\frac{40 \text{ CFR part } 1039}{1042}$ , as applicable.

(d) Exhaust emissions from stationary CI ICE that are complying with the emission standards for pre-2007 model year engines in  $\S$  60.4204(a),  $\S$  60.4205(a), or  $\S$  60.4205(c) must not exceed the NTE numerical requirements, rounded to the same number of decimal places as the applicable standard in  $\S$  60.4204(a),  $\S$  60.4205(a), or  $\S$  60.4205(c), determined from the equation in paragraph (c) of this section.

Where:

STD = The standard specified for that pollutant in  $\S 60.4204(a)$ ,  $\S 60.4205(a)$ , or  $\S 60.4205(c)$ .

Alternatively, stationary CI ICE that are complying with the emission standards for pre-2007 model year engines in § 60.4204(a), § 60.4205(a), or § 60.4205(c) may follow the testing procedures specified in § 60.4213, as appropriate.

(e) Exhaust emissions from stationary CI ICE that are complying with the emission standards for new CI engines in  $\frac{40 \text{ CFR}}{1042}$  must not exceed the NTE standards for the same model year and maximum engine power as required in  $\frac{40 \text{ CFR}}{1042.101(c)}$ .

[71 FR 39172, July 11, 2006, as amended at 76 FR 37971, June 28, 2011; 86 FR 34359, June 29, 2021]

## § 60.4213 What test methods and other procedures must I use if I am an owner or operator of a stationary CI internal combustion engine with a displacement of greater than or equal to 30 liters per cylinder?

Owners and operators of stationary CI ICE with a displacement of greater than or equal to 30 liters per cylinder must conduct performance tests according to <u>paragraphs (a)</u> through <u>(f)</u> of this section.

(a) Each performance test must be conducted according to the requirements in  $\S 60.8$  and under the specific conditions that this subpart specifies in table 7. The test must be conducted within 10 percent of 100 percent peak (or the highest achievable) load.

(b) You may not conduct performance tests during periods of startup, shutdown, or malfunction, as specified in  $\frac{60.8(c)}{2}$ .

(c) You must conduct three separate test runs for each performance test required in this section, as specified in  $\frac{60.8(f)}{1000}$ . Each test run must last at least 1 hour.

(d) To determine compliance with the percent reduction requirement, you must follow the requirements as specified in paragraphs (d)(1) through (3) of this section.

(1) You must use Equation 2 of this section to determine compliance with the percent reduction requirement:

$$\frac{C_i - C_o}{C_i} \times 100 = R \qquad (Eq. 2)$$

Where:

 $C_i$  = concentration of NO<sub>X</sub> or PM at the control device inlet,

 $C_o$  = concentration of NO<sub>X</sub> or PM at the control device outlet, and

R = percent reduction of NO<sub>X</sub> or PM emissions.

(2) You must normalize the NO<sub>X</sub> or PM concentrations at the inlet and outlet of the control device to a dry basis and to 15 percent oxygen (O<sub>2</sub>) using Equation 3 of this section, or an equivalent percent carbon dioxide (CO<sub>2</sub>) using the procedures described in paragraph (d)(3) of this section.

$$C_{adj} = C_d \frac{5.9}{20.9 - \% O_2}$$
 (Eq. 3)

Where:

 $C_{adj}$  = Calculated NO<sub>X</sub> or PM concentration adjusted to 15 percent O<sub>2</sub>.

 $C_d$  = Measured concentration of NO<sub>X</sub> or PM, uncorrected.

5.9 = 20.9 percent O<sub>2</sub>-15 percent O<sub>2</sub>, the defined O<sub>2</sub> correction value, percent.

 $O_2 = Measured O_2$  concentration, dry basis, percent.

(3) If pollutant concentrations are to be corrected to 15 percent  $O_2$  and  $CO_2$  concentration is measured in lieu of  $O_2$  concentration measurement, a  $CO_2$  correction factor is needed. Calculate the  $CO_2$  correction factor as described in <u>paragraphs (d)(3)(i)</u> through <u>(iii)</u> of this section.

(i) Calculate the fuel-specific  $F_0$  value for the fuel burned during the test using values obtained from Method 19, <u>Section 5.2</u>, and the following equation:

$$F_{o} = \frac{0.209_{F_{d}}}{F_{c}}$$
 (Eq. 4)

Where:

 $F_o =$  Fuel factor based on the ratio of O<sub>2</sub> volume to the ultimate CO<sub>2</sub> volume produced by the fuel at zero percent excess air. 0.209 = Fraction of air that is O<sub>2</sub>, percent/100.

 $F_d$  = Ratio of the volume of dry effluent gas to the gross calorific value of the fuel from Method 19, dsm<sup>3</sup>/J (dscf/10<sup>6</sup> Btu).

 $F_c$  = Ratio of the volume of CO<sub>2</sub> produced to the gross calorific value of the fuel from Method 19, dsm<sup>3</sup>/J (dscf/10<sup>6</sup> Btu).

(ii) Calculate the CO<sub>2</sub> correction factor for correcting measurement data to 15 percent O<sub>2</sub>, as follows:

$$X_{CO_2} = \frac{5.9}{F_0}$$
 (Eq. 5)

Where:

 $X_{CO2} = CO_2$  correction factor, percent.

5.9 = 20.9 percent O<sub>2</sub>-15 percent O<sub>2</sub>, the defined O<sub>2</sub> correction value, percent.

(iii) Calculate the NO<sub>X</sub> and PM gas concentrations adjusted to 15 percent O<sub>2</sub> using CO<sub>2</sub> as follows:

$$C_{adj} = C_d \frac{X_{CO_2}}{\% CO_2}$$
 (Eq. 6)

Where:

 $C_{adj}$  = Calculated NO<sub>X</sub> or PM concentration adjusted to 15 percent O<sub>2</sub>.

 $C_d$  = Measured concentration of NO<sub>X</sub> or PM, uncorrected.

 $CO_2$  = Measured CO<sub>2</sub> concentration, dry basis, percent.

(e) To determine compliance with the  $NO_X$  mass per unit output emission limitation, convert the concentration of  $NO_X$  in the engine exhaust using Equation 7 of this section:

$$ER = \frac{C_{d} \times 1.912 \times 10^{-3} \times Q \times T}{KW\text{-hour}}$$
(Eq. 7)

Where:

ER = Emission rate in grams per KW-hour.

 $C_d$  = Measured NO<sub>X</sub> concentration in ppm.

 $1.912 \times 10^{-3}$  = Conversion constant for ppm NO<sub>X</sub> to grams per standard cubic meter at 25 degrees Celsius.

Q = Stack gas volumetric flow rate, in standard cubic meter per hour.

T = Time of test run, in hours.

KW-hour = Brake work of the engine, in KW-hour.

(f) To determine compliance with the PM mass per unit output emission limitation, convert the concentration of PM in the engine exhaust using Equation 8 of this section:

$$ER = \frac{C_{adj} \times Q \times T}{KW-hour} \qquad (Eq. 8)$$

Where:

ER = Emission rate in grams per KW-hour.

 $C_{adj}$  = Calculated PM concentration in grams per standard cubic meter.

Q = Stack gas volumetric flow rate, in standard cubic meter per hour.

T = Time of test run, in hours.

KW-hour = Energy output of the engine, in KW.

[71 FR 39172, July 11, 2006, as amended at 76 FR 37971, June 28, 2011]

## Notification, Reports, and Records for Owners and Operators

# § 60.4214 What are my notification, reporting, and recordkeeping requirements if I am an owner or operator of a stationary CI internal combustion engine?

(a) Owners and operators of non-emergency stationary CI ICE that are greater than 2,237 KW (3,000 HP), or have a displacement of greater than or equal to 10 liters per cylinder, or are pre-2007 model year engines that are greater than 130 KW (175 HP) and not certified, must meet the requirements of <u>paragraphs (a)(1)</u> and (2) of this section.

(1) Submit an initial notification as required in  $\S 60.7(a)(1)$ . The notification must include the information in <u>paragraphs</u> (a)(1)(i) through (v) of this section. Beginning on February 26, 2025, submit the notification electronically according to <u>paragraph (g)</u> of this section.

(i) Name and address of the owner or operator;

(ii) The address of the affected source;

(iii) Engine information including make, model, engine family, serial number, model year, maximum engine power, and engine displacement;

(iv) Emission control equipment; and

(v) Fuel used.

(2) Keep records of the information in <u>paragraphs (a)(2)(i)</u> through (iv) of this section.

(i) All notifications submitted to comply with this subpart and all documentation supporting any notification.

(ii) Maintenance conducted on the engine.

(iii) If the stationary CI internal combustion is a certified engine, documentation from the manufacturer that the engine is certified to meet the emission standards.

(iv) If the stationary CI internal combustion is not a certified engine, documentation that the engine meets the emission standards.

(b) If the stationary CI internal combustion engine is an emergency stationary internal combustion engine, the owner or operator is not required to submit an initial notification. Starting with the model years in table 5 to this subpart, if the emergency engine does not meet the standards applicable to non-emergency engines in the applicable model year, the owner or operator must keep records of the operation of the engine in emergency and non-emergency service that are recorded through the non-resettable hour meter. The owner must record the time of operation of the engine and the reason the engine was in operation during that time.

(c) If the stationary CI internal combustion engine is equipped with a diesel particulate filter, the owner or operator must keep records of any corrective action taken after the backpressure monitor has notified the owner or operator that the high backpressure limit of the engine is approached.

(d) If you own or operate an emergency stationary CI ICE with a maximum engine power more than 100 HP that operates for the purpose specified in § 60.4211(f)(3)(i), you must submit an annual report according to the requirements in <u>paragraphs</u> (d)(1) through (3) of this section.

- (1) The report must contain the following information:
- (i) Company name and address where the engine is located.
- (ii) Date of the report and beginning and ending dates of the reporting period.
- (iii) Engine site rating and model year.
- (iv) Latitude and longitude of the engine in decimal degrees reported to the fifth decimal place.

(v)-(vi) [Reserved]

(vii) Hours spent for operation for the purposes specified in  $\S$  60.4211(f)(3)(i), including the date, start time, and end time for engine operation for the purposes specified in  $\S$  60.4211(f)(3)(i). The report must also identify the entity that dispatched the engine and the situation that necessitated the dispatch of the engine.

(2) The first annual report must cover the calendar year 2015 and must be submitted no later than March 31, 2016. Subsequent annual reports for each calendar year must be submitted no later than March 31 of the following calendar year.

(3) The annual report must be submitted electronically using the subpart specific reporting form in the Compliance and Emissions Data Reporting Interface (CEDRI) that is accessed through EPA's Central Data Exchange (CDX) (<u>https://cdx.epa.gov/</u>). However, if the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, the written report must be submitted to the Administrator at the appropriate address listed in § 60.4. Beginning on February 26, 2025, submit annual report electronically according to <u>paragraph (g)</u> of this section.

(e) Owners or operators of stationary CI ICE equipped with AECDs pursuant to the requirements of 40 CFR 1039.665 must report the use of AECDs as required by 40 CFR 1039.665(e).

(f) Beginning on February 26, 2025, within 60 days after the date of completing each performance test required by this subpart, you must submit the results of the performance test required under this section following the procedures specified in <u>paragraphs (f)(1)</u> and (2) of this section.

(1) Data collected using test methods supported by the EPA's Electronic Reporting Tool (ERT) as listed on the EPA's ERT website (<u>https://www.epa.gov/electronic-reporting-air-emissions/electronic-reporting-tool-ert</u>) at the time of the test. Submit the results of the performance test to the EPA via the Compliance and Emissions Data Reporting Interface (CEDRI), according to <u>paragraph (g)</u> of this section. The data must be submitted in a file format generated using the EPA's ERT. Alternatively, you may submit an electronic file consistent with the extensible markup language (XML) schema listed on the EPA's ERT website.

(2) Data collected using test methods that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the test. The results of the performance test must be included as an attachment in the ERT or an alternate electronic file consistent with the XML schema listed on the EPA's ERT website. Submit the ERT generated package or alternative file to the EPA via CEDRI according to paragraph (g) of this section.

(g) If you are required to submit notifications or reports following the procedure specified in this <u>paragraph (g)</u>, you must submit notifications or reports to the EPA via the Compliance and Emissions Data Reporting Interface (CEDRI), which can be accessed through the EPA's Central Data Exchange (CDX) (<u>https://cdx.epa.gov/</u>). The EPA will make all the information submitted through CEDRI available to the public without further notice to you. Do not use CEDRI to submit information you claim as CBI. Although we do not expect persons to assert a claim of CBI, if you wish to assert a CBI claim for some of the information rot notification, you must submit a complete file in the format specified in this subpart, including information claimed to be CBI, to the EPA following the procedures in <u>paragraphs (g)(1)</u> and (2) of this section. Clearly mark the part or all of the information marked as CBI will not be disclosed except in accordance with procedures set forth in <u>40 CFR part 2</u>. All CBI claims must be asserted at the time of submission. Anything submitted using CEDRI cannot later be claimed CBI. Furthermore, under CAA section 114(c), emissions data is not entitled to confidential treatment, and the EPA is required to make emissions data available to the public. Thus, emissions data will not be protected as CBI and will be made publicly available. You must submit the same file submitted to the CBI office with the CBI omitted to the EPA via the EPA's CDX as described earlier in this <u>paragraph (g)</u>.

(1) The preferred method to receive CBI is for it to be transmitted electronically using email attachments, File Transfer Protocol, or other online file sharing services. Electronic submissions must be transmitted directly to the OAQPS CBI Office at the email address <u>oaqpscbi@epa.gov</u>, and as described in <u>paragraph (g)</u> of this section, should include clear CBI markings. ERT files should be flagged to the attention of the Group Leader, Measurement Policy Group; all other files should be flagged to the attention of the Stationary Compression Ignition Internal Combustion Engine Sector Lead. If assistance is needed with submitting large electronic files that exceed the file size limit for email attachments, and if you do not have your own file sharing service, please email <u>oaqpscbi@epa.gov</u> to request a file transfer link.

(2) If you cannot transmit the file electronically, you may send CBI information through the postal service to the following address: OAQPS Document Control Officer (C404-02), OAQPS, U.S. Environmental Protection Agency, 109 T.W. Alexander Drive, P.O. Box 12055, Research Triangle Park, North Carolina 27711. ERT files should be sent to the attention of the Group Leader, Measurement Policy Group, and all other files should be sent to the attention of the Stationary

Compression Ignition Internal Combustion Engine Sector Lead. The mailed CBI material should be double wrapped and clearly marked. Any CBI markings should not show through the outer envelope.

(h) If you are required to electronically submit a report through CEDRI in the EPA's CDX, you may assert a claim of EPA system outage for failure to timely comply with that reporting requirement. To assert a claim of EPA system outage, you must meet the requirements outlined in paragraphs (h)(1) through (7) of this section.

(1) You must have been or will be precluded from accessing CEDRI and submitting a required report within the time prescribed due to an outage of either the EPA's CEDRI or CDX systems.

(2) The outage must have occurred within the period of time beginning five business days prior to the date that the submission is due.

(3) The outage may be planned or unplanned.

(4) You must submit notification to the Administrator in writing as soon as possible following the date you first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

(5) You must provide to the Administrator a written description identifying:

(i) The date(s) and time(s) when CDX or CEDRI was accessed and the system was unavailable;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to EPA system outage;

(iii) A description of measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which you propose to report, or if you have already met the reporting requirement at the time of the notification, the date you reported.

(6) The decision to accept the claim of EPA system outage and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(7) In any circumstance, the report must be submitted electronically as soon as possible after the outage is resolved.

(i) If you are required to electronically submit a report through CEDRI in the EPA's CDX, you may assert a claim of force majeure for failure to timely comply with that reporting requirement. To assert a claim of force majeure, you must meet the requirements outlined in paragraphs (i)(1) through (5) of this section.

(1) You may submit a claim if a force majeure event is about to occur, occurs, or has occurred or there are lingering effects from such an event within the period of time beginning five business days prior to the date the submission is due. For the purposes of this section, a force majeure event is defined as an event that will be or has been caused by circumstances beyond the control of the affected facility, its contractors, or any entity controlled by the affected facility that prevents you from complying with the requirement to submit a report electronically within the time period prescribed. Examples of such events are acts of nature (*e.g.*, hurricanes, earthquakes, or floods), acts of war or terrorism, or equipment failure or safety hazard beyond the control of the affected facility (*e.g.*, large scale power outage).

(2) You must submit notification to the Administrator in writing as soon as possible following the date you first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

(3) You must provide to the Administrator:

(i) A written description of the force majeure event;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to the force majeure event;

(iii) A description of measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which you propose to report, or if you have already met the reporting requirement at the time of the notification, the date you reported.

(4) The decision to accept the claim of force majeure and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(5) In any circumstance, the reporting must occur as soon as possible after the force majeure event occurs.

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(j) Any records required to be maintained by this subpart that are submitted electronically via the EPA's CEDRI may be maintained in electronic format. This ability to maintain electronic copies does not affect the requirement for facilities to make records, data, and reports available upon request to a delegated air agency or the EPA as part of an on-site compliance evaluation.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>78 FR 6696</u>, Jan. 30, 2013; <u>81 FR 44219</u>, July 7, 2016; <u>87 FR 48606</u>, Aug. 10, 2022; <u>89 FR 70512</u>, Aug. 30, 2024]

## Special Requirements

# § 60.4215 What requirements must I meet for engines used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands?

(a) Stationary CI ICE with a displacement of less than 30 liters per cylinder that are used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands are required to meet the applicable emission standards in  $\frac{\$\$}{60.4202}$  and  $\frac{60.4205}{60.4205}$ .

(b) Stationary CI ICE that are used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands are not required to meet the fuel requirements in  $\S 60.4207$ .

(c) Stationary CI ICE with a displacement of greater than or equal to 30 liters per cylinder that are used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands are required to meet the following emission standards:

(1) For engines installed prior to January 1, 2012, limit the emissions of  $NO_X$  in the stationary CI internal combustion engine exhaust to the following:

(i) 17.0 g/KW-hr (12.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii)  $45 \cdot n^{-0.2}$  g/KW-hr ( $34 \cdot n^{-0.2}$  g/HP-hr) when maximum engine speed is 130 or more but less than 2,000 rpm, where n is maximum engine speed; and

(iii) 9.8 g/KW-hr (7.3 g/HP-hr) when maximum engine speed is 2,000 rpm or more.

(2) For engines installed on or after January 1, 2012, limit the emissions of  $NO_X$  in the stationary CI internal combustion engine exhaust to the following:

(i) 14.4 g/KW-hr (10.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii)  $44 \cdot n^{-0.23}$  g/KW-hr (33  $\cdot n^{-0.23}$  g/HP-hr) when maximum engine speed is greater than or equal to 130 but less than 2,000 rpm and where n is maximum engine speed; and

(iii) 7.7 g/KW-hr (5.7 g/HP-hr) when maximum engine speed is greater than or equal to 2,000 rpm.

(3) Limit the emissions of PM in the stationary CI internal combustion engine exhaust to 0.40 g/KW-hr (0.30 g/HP-hr).

[71 FR 39172, July 11, 2006, as amended at 76 FR 37971, June 28, 2011]

## § 60.4216 What requirements must I meet for engines used in Alaska?

(a) Prior to December 1, 2010, owners and operators of stationary CI ICE with a displacement of less than 30 liters per cylinder located in areas of Alaska not accessible by the FAHS should refer to <u>40 CFR part 69</u> to determine the diesel fuel requirements applicable to such engines.

(b) Except as indicated in paragraph (c) of this section, manufacturers, owners and operators of stationary CI ICE with a displacement of less than 10 liters per cylinder located in remote areas of Alaska may meet the requirements of this subpart by manufacturing and installing engines meeting the Tier 2 or Tier 3 emission standards described in  $\frac{40 \text{ CFR part } 1042}{40 \text{ CFR part } 1042}$  for the same model year, displacement, and maximum engine power, as appropriate, rather than the otherwise applicable requirements of  $\frac{40 \text{ CFR part } 1039}{40 \text{ CFR part } 1039}$ , as indicated in  $\frac{88 60.4201(f)}{40 \text{ CFR part } 1039}$ .

(c) Manufacturers, owners, and operators of stationary CI ICE that are located in remote areas of Alaska may choose to meet the applicable emission standards for emergency engines in <u>§§ 60.4202</u> and <u>60.4205</u>, and not those for non-emergency engines in <u>§§ 60.4201</u> and <u>60.4204</u>, except that for 2014 model year and later nonemergency CI ICE, the owner or operator of any such engine must have that engine certified as meeting at least the Tier 3 PM standards identified in appendix I of <u>40</u> <u>CFR part 1039</u> or in <u>40 CFR 1042.101</u>.

(d) The provisions of  $\frac{60.4207}{2}$  do not apply to owners and operators of pre-2014 model year stationary CI ICE subject to this subpart that are located in remote areas of Alaska.

(e) The provisions of  $\frac{60.4208(a)}{2000}$  do not apply to owners and operators of stationary CI ICE subject to this subpart that are located in areas of Alaska not accessible by the FAHS until after December 31, 2009.

(f) The provisions of this section and  $\frac{\& 60.4207}{U}$  do not prevent owners and operators of stationary CI ICE subject to this subpart that are located in remote areas of Alaska from using fuels mixed with used lubricating oil, in volumes of up to 1.75 percent of the total fuel. The sulfur content of the used lubricating oil must be less than 200 parts per million. The used lubricating oil must meet the on-specification levels and properties for used oil in  $\frac{40 \text{ CFR } 279.11}{U}$ .

[76 FR 37971, June 28, 2011, as amended at <u>81 FR 44219</u>, July 7, 2016; <u>86 FR 34359</u>, June 29, 2021]

## § 60.4217 What emission standards must I meet if I am an owner or operator of a stationary internal combustion engine using special fuels?

Owners and operators of stationary CI ICE that do not use diesel fuel may petition the Administrator for approval of alternative emission standards, if they can demonstrate that they use a fuel that is not the fuel on which the manufacturer of the engine certified the engine and that the engine cannot meet the applicable standards required in  $\S$  60.4204 or  $\S$  60.4205 using such fuels and that use of such fuel is appropriate and reasonably necessary, considering cost, energy, technical feasibility, human health and environmental, and other factors, for the operation of the engine.

[76 FR 37972, June 28, 2011]

### **General Provisions**

### § 60.4218 What General Provisions and confidential information provisions apply to me?

(a) Table 8 to this subpart shows which parts of the General Provisions in  $\frac{8860.1}{1000}$  through  $\frac{60.19}{1000}$  apply to you.

(b) The provisions of  $\frac{40 \text{ CFR } 1068.10}{(\text{CBI})}$  and  $\frac{1068.11}{2000}$  and  $\frac{1068.11}{2000}$  apply for engine manufacturers. For others, the general confidential business information (CBI) provisions apply as described in  $\frac{40 \text{ CFR } \text{part } 2}{2}$ .

[<u>88 FR 4471</u>, Jan. 24, 2023]

#### Definitions

### § 60.4219 What definitions apply to this subpart?

As used in this subpart, all terms not defined herein shall have the meaning given them in the CAA and in <u>subpart A of this</u> <u>part</u>.

*Alaska Railbelt Grid* means the service areas of the six regulated public utilities that extend from Fairbanks to Anchorage and the Kenai Peninsula. These utilities are Golden Valley Electric Association; Chugach Electric Association; Matanuska Electric Association; Homer Electric Association; Anchorage Municipal Light & Power; and the City of Seward Electric System.

*Certified emissions life* means the period during which the engine is designed to properly function in terms of reliability and fuel consumption, without being remanufactured, specified as a number of hours of operation or calendar years, whichever comes first. The values for certified emissions life for stationary CI ICE with a displacement of less than 10 liters per cylinder are given in <u>40 CFR 1039.101(g)</u>. The values for certified emissions life for stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder are given in <u>40 CFR 1042.101(e)</u>.

*Combustion turbine* means all equipment, including but not limited to the turbine, the fuel, air, lubrication and exhaust gas systems, control systems (except emissions control equipment), and any ancillary components and sub-components comprising any simple cycle combustion turbine, any regenerative/recuperative cycle combustion turbine, the combustion turbine portion of any cogeneration cycle combustion system, or the combustion turbine portion of any combined cycle steam/electric generating system.

Compression ignition means relating to a type of stationary internal combustion engine that is not a spark ignition engine.

Date of manufacture means one of the following things:

(1) For freshly manufactured engines and modified engines, date of manufacture means the date the engine is originally produced.

(2) For reconstructed engines, date of manufacture means the date the engine was originally produced, except as specified in paragraph (3) of this definition.

(3) Reconstructed engines are assigned a new date of manufacture if the fixed capital cost of the new and refurbished components exceeds 75 percent of the fixed capital cost of a comparable entirely new facility. An engine that is produced from a previously used engine block does not retain the date of manufacture of the engine in which the engine block was previously used if the engine is produced using all new components except for the engine block. In these cases, the date of manufacture is the date of reconstruction or the date the new engine is produced.

*Diesel fuel* means any liquid obtained from the distillation of petroleum with a boiling point of approximately 150 to 360 degrees Celsius. One commonly used form is number 2 distillate oil.

*Diesel particulate filter* means an emission control technology that reduces PM emissions by trapping the particles in a flow filter substrate and periodically removes the collected particles by either physical action or by oxidizing (burning off) the particles in a process called regeneration.

*Emergency stationary internal combustion engine* means any stationary reciprocating internal combustion engine that meets all of the criteria in paragraphs (1) through (3) of this definition. All emergency stationary ICE must comply with the requirements specified in § 60.4211(f) in order to be considered emergency stationary ICE. If the engine does not comply with the requirements specified in § 60.4211(f), then it is not considered to be an emergency stationary ICE under this subpart.

(1) The stationary ICE is operated to provide electrical power or mechanical work during an emergency situation. Examples include stationary ICE used to produce power for critical networks or equipment (including power supplied to portions of a facility) when electric power from the local utility (or the normal power source, if the facility runs on its own power production) is interrupted, or stationary ICE used to pump water in the case of fire or flood, etc.

(2) The stationary ICE is operated under limited circumstances for situations not included in paragraph (1) of this definition, as specified in  $\S$  60.4211(f).

Engine manufacturer means the manufacturer of the engine. See the definition of "manufacturer" in this section.

*Fire pump engine* means an emergency stationary internal combustion engine certified to NFPA requirements that is used to provide power to pump water for fire suppression or protection.

*Freshly manufactured engine* means an engine that has not been placed into service. An engine becomes freshly manufactured when it is originally produced.

Installed means the engine is placed and secured at the location where it is intended to be operated.

*Manufacturer* has the meaning given in section 216(1) of the Act. In general, this term includes any person who manufactures a stationary engine for sale in the United States or otherwise introduces a new stationary engine into commerce in the United States. This includes importers who import stationary engines for sale or resale.

Maximum engine power means maximum engine power as defined in 40 CFR 1039.801.

Model year means the calendar year in which an engine is manufactured (see "date of manufacture"), except as follows:

(1) Model year means the annual new model production period of the engine manufacturer in which an engine is manufactured (see "date of manufacture"), if the annual new model production period is different than the calendar year and includes January 1 of the calendar year for which the model year is named. It may not begin before January 2 of the previous calendar year and it must end by December 31 of the named calendar year.

(2) For an engine that is converted to a stationary engine after being placed into service as a nonroad or other non-stationary engine, model year means the calendar year or new model production period in which the engine was manufactured (see "date of manufacture").

*Other internal combustion engine* means any internal combustion engine, except combustion turbines, which is not a reciprocating internal combustion engine or rotary internal combustion engine.

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*Reciprocating internal combustion engine* means any internal combustion engine which uses reciprocating motion to convert heat energy into mechanical work.

Remote areas of Alaska means areas of Alaska that meet either paragraph (1) or (2) of this definition.

(1) Areas of Alaska that are not accessible by the Federal Aid Highway System (FAHS).

(2) Areas of Alaska that meet all of the following criteria:

(i) The only connection to the FAHS is through the Alaska Marine Highway System, or the stationary CI ICE operation is within an isolated grid in Alaska that is not connected to the statewide electrical grid referred to as the Alaska Railbelt Grid.

(ii) At least 10 percent of the power generated by the stationary CI ICE on an annual basis is used for residential purposes.

(iii) The generating capacity of the source is less than 12 megawatts, or the stationary CI ICE is used exclusively for backup power for renewable energy.

*Rotary internal combustion engine* means any internal combustion engine which uses rotary motion to convert heat energy into mechanical work.

*Spark ignition* means relating to a gasoline, natural gas, or liquefied petroleum gas fueled engine or any other type of engine with a spark plug (or other sparking device) and with operating characteristics significantly similar to the theoretical Otto combustion cycle. Spark ignition engines usually use a throttle to regulate intake air flow to control power during normal operation. Dual-fuel engines in which a liquid fuel (typically diesel fuel) is used for CI and gaseous fuel (typically natural gas) is used as the primary fuel at an annual average ratio of less than 2 parts diesel fuel to 100 parts total fuel on an energy equivalent basis are spark ignition engines.

Stationary internal combustion engine means any internal combustion engine, except combustion turbines, that converts heat energy into mechanical work and is not mobile. Stationary ICE differ from mobile ICE in that a stationary internal combustion engine is not a nonroad engine as defined at <u>40 CFR 1068.30</u> (excluding paragraph (2)(ii) of that definition), and is not used to propel a motor vehicle, aircraft, or a vehicle used solely for competition. Stationary ICE include reciprocating ICE, rotary ICE, and other ICE, except combustion turbines.

Subpart means 40 CFR part 60, subpart IIII.

[<u>71 FR 39172</u>, July 11, 2006, as amended at <u>76 FR 37972</u>, June 28, 2011; <u>78 FR 6696</u>, Jan. 30, 2013; <u>81 FR 44219</u>, July 7, 2016; <u>86 FR 34360</u>, June 29, 2021; <u>87 FR 48606</u>, Aug. 10, 2022]

Table 1 to Subpart IIII of Part 60—Emission Standards for Stationary Pre-2007 Model Year Engines With a Displacement of <10 Liters per Cylinder and 2007-2010 Model Year Engines >2,237 KW (3,000 HP) and With a Displacement of <10 Liters per Cylinder

[As stated in <u>§§ 60.4201(b)</u> , <u>60.4202(b)</u> , <u>60.4204(a)</u> , and <u>60.4205(a)</u> , you must comply with the following emission standards]						
Maximum engine power	Emission standards for stationary pre-2007 model year engines with a displacement of <10 liters per cylinder and 2007-2010 model year engines >2,237 KW (3,000 HP) and with a displacement of <10 liters per cylinder in g/KW-hr (g/HP-hr)					
	NMHC + NO <sub>X</sub>	НС	NOx	CO	PM	
KW<8 (HP<11)	10.5 (7.8)			8.0 (6.0)	1.0 (0.75)	
8≤KW<19 (11≤HP<25)	9.5 (7.1)			6.6 (4.9)	0.80 (0.60)	
19≤KW<37 (25≤HP<50)	9.5 (7.1)			5.5 (4.1)	0.80 (0.60)	
37≤KW<56 (50≤HP<75)			9.2 (6.9)			
56≤KW<75 (75≤HP<100)			9.2 (6.9)			
75 <u>≤</u> KW<130 (100 <u>≤</u> HP<175)			9.2 (6.9)			
[As stated in §§ 60.4201(b), 60.4202(b), 60.4204(a), and 60.4205(a), you must comply with the following emission standards]						
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Maximum engine power	Emission standards for stationary pre-2007 model year engines with a displacement of <10 liters per cylinder and 2007-2010 model year engines >2,237 KW (3,000 HP) and with a displacement of <10 liters per cylinder in g/KW-hr (g/HP-hr)					
	NMHC + NO <sub>X</sub>	НС	NOx	СО	PM	
130≤KW<225 (175≤HP<300)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)	
225≤KW<450 (300≤HP<600)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)	
450≤KW≤560 (600≤HP≤750)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)	
KW>560 (HP>750)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)	

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## Table 2 to Subpart IIII of Part 60—Emission Standards for 2008 Model Year and Later Emergency Stationary CIICE <37 KW (50 HP) With a Displacement of <10 Liters per Cylinder</td>

[As stated in $\S$ 60.4202(a)(1), you must comply with the following emission standards]							
Engine power	Emission standards for 2008 model year and later emergency stationary CI ICE <37 KW (50 HP) with a displacement of <10 liters per cylinder in g/KW-hr (g/HP-hr)						
	Model year(s)	NO <sub>x</sub> + NMHC	СО	PM			
KW<8 (HP<11)	2008 +	7.5 (5.6)	8.0 (6.0)	0.40 (0.30)			
8≤KW<19 (11≤HP<25)	2008 +	7.5 (5.6)	6.6 (4.9)	0.40 (0.30)			
19≤KW<37 (25≤HP<50)	2008 +	7.5 (5.6)	5.5 (4.1)	0.30 (0.22)			

## Table 3 to Subpart IIII of Part 60—Certification Requirements for Stationary Fire Pump Engines

As stated in <u>§ 60.4202(d)</u> , you must certify new stationary fire pump engines beginning with the following model years:					
Engine power	Starting model year engine manufacturers must certify new stationary fire pump engines according to § 60.4202(d) <sup>1</sup>				
KW<75 (HP<100)	2011				
75≤KW<130 (100≤HP<175)	2010				
130≤KW≤560 (175≤HP≤750)	2009				
KW>560 (HP>750)	2008				

<sup>1</sup> Manufacturers of fire pump stationary CI ICE with a maximum engine power greater than or equal to 37 kW (50 HP) and less than 450 KW (600 HP) and a rated speed of greater than 2,650 revolutions per minute (rpm) are not required to certify such engines until three model years following the model year indicated in this Table 3 for engines in the applicable engine power category.

[71 FR 39172, July 11, 2006, as amended at 76 FR 37972, June 28, 2011]

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### Table 4 to Subpart IIII of Part 60—Emission Standards for Stationary Fire Pump Engines

[As stated in  $\S$  60.4202(d) and 60.4205(c), you must comply with the following emission standards for stationary fire pump engines]

Maximum engine power	Model year(s)	Emission standards for stationary fire pump engines in g/KW-hr (g/HP-hr)		
		NMHC + NO <sub>X</sub>	CO	PM
KW<8 (HP<11)	2010 and earlier	10.5 (7.8)	8.0 (6.0)	1.0 (0.75)
KW<8 (HP<11)	2011 +	7.5 (5.6)	8.0 (6.0)	0.40 (0.30)
8≤KW<19 (11≤HP<25)	2010 and earlier	9.5 (7.1)	6.6 (4.9)	0.80 (0.60)
8≤KW<19 (11≤HP<25)	2011 +	7.5 (5.6)	6.6 (4.9)	0.40 (0.30)
19≤KW<37 (25≤HP<50)	2010 and earlier	9.5 (7.1)	5.5 (4.1)	0.80 (0.60)
19≤KW<37 (25≤HP<50)	2011 +	7.5 (5.6)	5.5 (4.1)	0.30 (0.22)
37≤KW<56 (50≤HP<75)	2010 and earlier	10.5 (7.8)	5.0 (3.7)	0.80 (0.60)
37≤KW<56 (50≤HP<75)	2011 +1	4.7 (3.5)	5.0 (3.7)	0.40 (0.30)
56≤KW<75 (75≤HP<100)	2010 and earlier	10.5 (7.8)	5.0 (3.7)	0.80 (0.60)
56≤KW<75 (75≤HP<100)	2011 +1	4.7 (3.5)	5.0 (3.7)	0.40 (0.30)
75≤KW<130 (100≤HP<175)	2009 and earlier	10.5 (7.8)	5.0 (3.7)	0.80 (0.60)
75≤KW<130 (100≤HP<175)	2010 +2	4.0 (3.0)	5.0 (3.7)	0.30 (0.22)
130≤KW<225 (175≤HP<300)	2008 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
130≤KW<225 (175≤HP<300)	2009 + 3	4.0 (3.0)	3.5 (2.6)	0.20 (0.15)
225≤KW<450 (300≤HP<600)	2008 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
225≤KW<450 (300≤HP<600)	2009 +3	4.0 (3.0)	3.5 (2.6)	0.20 (0.15)
450≤KW≤560 (600≤HP≤750)	2008 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
450≤KW≤560 (600≤HP≤750)	2009 +	4.0 (3.0)	3.5 (2.6)	0.20 (0.15)
KW>560 (HP>750)	2007 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
KW>560 (HP>750)	2008 +	6.4 (4.8)	3.5 (2.6)	0.20 (0.15)

<sup>1</sup> For model years 2011-2013, manufacturers, owners and operators of fire pump stationary CI ICE in this engine power category with a rated speed of greater than 2,650 revolutions per minute (rpm) may comply with the emission limitations for 2010 model year engines.

<sup>2</sup> For model years 2010-2012, manufacturers, owners and operators of fire pump stationary CI ICE in this engine power category with a rated speed of greater than 2,650 rpm may comply with the emission limitations for 2009 model year engines.

<sup>3</sup> In model years 2009-2011, manufacturers of fire pump stationary CI ICE in this engine power category with a rated speed of greater than 2,650 rpm may comply with the emission limitations for 2008 model year engines.

### [<u>89 FR 70513</u>, Aug. 30, 2024]

## Table 5 to Subpart IIII of Part 60—Labeling and Recordkeeping Requirements for New Stationary Emergency Engines

[You must comply with the labeling requirements in $\frac{60.4210(f)}{100}$ and the record keeping requirements in $\frac{60.4214(b)}{100}$ for				
new emergency stationary CI ICE beginning in the following model years:				
Engine power	Starting model year			
19≤KW<56 (25≤HP<75)	2013			
56≤KW<130 (75≤HP<175)	2012			

## Standards of Performance for Stationary Compression Ignition Internal Combustion Engines

[You must comply with the labeling requirements in § 60.4210(f) and the recordkeeping requirements in § 60.4214(b) for new emergency stationary CI ICE beginning in the following model years:]

Engine power	Starting model year
KW≥130 (HP≥175)	2011

#### Table 6 to Subpart IIII of Part 60—Optional 3-Mode Test Cycle for Stationary Fire Pump Engines

[As stated in <u>§ 60.4210</u>	)(g), manufacturers of fire pump engeng	ngines may use the following te gines:]	est cycle for testing fire pump		
Mode No.	Engine speed <sup>1</sup>	Torque (percent) <sup>2</sup>	Weighting factors		
1	Rated	100	0.30		
2	Rated	75	0.50		
3	Rated	50	0.20		
<sup>1</sup> Engine speed: ±2 percent of point.					

<sup>2</sup> Torque: NFPA certified nameplate HP for 100 percent point. All points should be  $\pm 2$  percent of engine percent load value.

## Table 7 to Subpart IIII of Part 60—Requirements for Performance Tests for Stationary CI ICE With a Displacement of ≥30 Liters per Cylinder

As stated in § 60.4213, you must comply with the following requirements for performance tests for stationary CI ICE with a displacement of  $\geq$  30 liters per cylinder:

Each	Complying with the requirement to	You must	Using	According to the following requirements
1. Stationary CI internal combustion engine with a displacement of ≥ 30 liters per cylinder	a. Reduce NO <sub>x</sub> emissions by 90 percent or more;	i. Select the sampling port location and number/location of traverse points at the inlet and outlet of the control device;		(a) For NO <sub>X</sub> , O <sub>2</sub> , and moisture measurement, ducts $\leq 6$ inches in diameter may be sampled at a single point located at the duct centroid and ducts >6 and $\leq 12$ inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is >12 inches in diameter <i>and</i> the sampling port location meets the two and half- diameter criterion of Section 11.1.1 of Method 1 of <u>40 CFR part 60</u> , appendix <u>A</u> -1, the duct may be sampled at '3- point long line'; otherwise, conduct the stratification testing and select sampling points according to Section 8.1.2 of Method 7E of <u>40 CFR part 60</u> , <u>appendix A</u> -4.
		ii. Measure O <sub>2</sub> at the inlet and outlet of the control device;	(1) Method 3, 3A, or 3B of <u>40 CFR part</u> <u>60, appendix A</u> -2	(b) Measurements to determine $O_2$ concentration must be made at the same time as the measurements for $NO_X$ concentration.
		iii. If necessary, measure moisture content at the inlet and outlet of the control device; and	(2) Method 4 of <u>40</u> <u>CFR part 60</u> , <u>appendix A</u> -3, Method 320 of <u>40</u>	(c) Measurements to determine moisture content must be made at the same time as the measurements for NO <sub>X</sub> concentration.

## Standards of Performance for Stationary Compression Ignition Internal Combustion Engines

Each	Complying with the requirement to	You must	Using	According to the following requirements
			$\frac{\text{CFR part 63,}}{\text{appendix A, or}}$ ASTM D 6348-03 (incorporated by reference, see § 60.17)	
		iv. Measure $NO_X$ at the inlet and outlet of the control device.	(3) Method 7E of <u>40</u> <u>CFR part 60,</u> <u>appendix A-4,</u> Method 320 of <u>40</u> <u>CFR part 63,</u> <u>appendix A, or</u> ASTM D 6348-03 (incorporated by reference, see <u>§</u> <u>60.17</u> )	(d) NO <sub>X</sub> concentration must be at 15 percent $O_2$ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
	b. Limit the concentration of NO <sub>X</sub> in the stationary CI internal combustion engine exhaust.	i. Select the sampling port location and number/location of traverse points at the exhaust of the stationary internal combustion engine;		(a) For NO <sub>X</sub> , O <sub>2</sub> , and moisture measurement, ducts $\leq 6$ inches in diameter may be sampled at a single point located at the duct centroid and ducts $\geq 6$ and $\leq 12$ inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is $\geq 12$ inches in diameter <i>and</i> the sampling port location meets the two and half- diameter criterion of Section 11.1.1 of Method 1 of <u>40 CFR part 60</u> , appendix <u>A</u> -1, the duct may be sampled at '3- point long line'; otherwise, conduct the stratification testing and select sampling points according to Section 8.1.2 of Method 7E of <u>40 CFR part 60</u> , <u>appendix A</u> -4.
		<ul> <li>ii. Determine the</li> <li>O<sub>2</sub> concentration of the stationary internal combustion engine</li> <li>exhaust at the sampling port location;</li> </ul>	(1) Method 3, 3A, or 3B of <u>40 CFR part</u> <u>60, appendix A</u> -2	(b) Measurements to determine $O_2$ concentration must be made at the same time as the measurement for $NO_X$ concentration.
		iii. If necessary, measure moisture content of the stationary internal combustion engine exhaust at the sampling port location; and	(2) Method 4 of <u>40</u> <u>CFR part 60</u> , <u>appendix A-3</u> , Method 320 of <u>40</u> <u>CFR part 63</u> , <u>appendix A</u> , or ASTM D 6348-03 (incorporated by reference, see §	(c) Measurements to determine moisture content must be made at the same time as the measurement for $NO_X$ concentration.

## Standards of Performance for Stationary Compression Ignition Internal Combustion Engines

Each	Each Complying with the requirement You must to		Using	According to the following requirements
			<u>60.17</u> )	
		iv. Measure $NO_X$ at the exhaust of the stationary internal combustion engine; if using a control device, the sampling site must be located at the outlet of the control device.	(3) Method 7E of $40$ <u>CFR part 60.</u> <u>appendix A-4</u> , Method 320 of $40$ <u>CFR part 63.</u> <u>appendix A</u> , or ASTM D 6348-03 (incorporated by reference, see § <u>60.17</u> )	(d) NO <sub>X</sub> concentration must be at 15 percent $O_2$ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
	c. Reduce PM emissions by 60 percent or morei. Select the sampling port location and the number of traverse points;ii. Measure O2 at the inlet and outlet of the control device;		(1) Method 1 or 1A of <u>40 CFR part 60,</u> <u>appendix A</u> -1	(a) Sampling sites must be located at the inlet and outlet of the control device.
			(2) Method 3, 3A, or 3B of <u>40 CFR part</u> <u>60, appendix A</u> -2	(b) Measurements to determine O <sub>2</sub> concentration must be made at the same time as the measurements for PM concentration.
iii. If necessary, measure moisture content at the inlet and outlet of the control device; and		(3) Method 4 of <u>40</u> <u>CFR part 60,</u> <u>appendix A</u> -3	(c) Measurements to determine and moisture content must be made at the same time as the measurements for PM concentration.	
		iv. Measure PM at the inlet and outlet of the control device.	(4) Method 5 of <u>40</u> <u>CFR part 60,</u> <u>appendix A</u> -3	(d) PM concentration must be at 15 percent $O_2$ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
	d. Limit the concentration of PM in the stationary CI internal combustion engine exhaust	i. Select the sampling port location and the number of traverse points;	(1) Method 1 or 1A of <u>40 CFR part 60,</u> <u>appendix A</u> -1	(a) If using a control device, the sampling site must be located at the outlet of the control device.
ii. Determine th O <sub>2</sub> concentration stationary inter combustion eng exhaust at the s port location;		<ul> <li>Determine the</li> <li>O<sub>2</sub> concentration of the stationary internal combustion engine exhaust at the sampling port location;</li> </ul>	(2) Method 3, 3A, or 3B of <u>40 CFR part</u> <u>60, appendix A</u> -2	(b) Measurements to determine $O_2$ concentration must be made at the same time as the measurements for PM concentration.
		iii. If necessary, measure moisture content of the stationary internal combustion engine exhaust at the sampling port location; and	(3) Method 4 of <u>40</u> <u>CFR part 60,</u> <u>appendix A</u> -3	(c) Measurements to determine moisture content must be made at the same time as the measurements for PM concentration.
		iv. Measure PM at the exhaust of the stationary internal combustion	(4) Method 5 of <u>40</u> <u>CFR part 60,</u> <u>appendix A</u> -3	(d) PM concentration must be at 15 percent $O_2$ , dry basis. Results of this test consist of the average of the three

## Standards of Performance for Stationary Compression Ignition Internal Combustion Engines

Each	Complying with the requirement to	You must	Using	According to the following requirements
		engine.		1-hour or longer runs.

#### [<u>79 FR 11251</u>, Feb. 27, 2014]

### Table 8 to Subpart IIII of Part 60—Applicability of General Provisions to Subpart IIII

	[As stated in § 60.4218, you must	t comply v	with the following applicable General Provisions:]
General Provisions citation	Subject of citation	Applies to subpart	Explanation
§ 60.1	General applicability of the General Provisions	Yes	
§ 60.2	Definitions	Yes	Additional terms defined in $\S 60.4219$ .
§ 60.3	Units and abbreviations	Yes	
§ 60.4	Address	Yes	
§ 60.5	Determination of construction or modification	Yes	
§ 60.6	Review of plans	Yes	
§ 60.7	Notification and Recordkeeping	Yes	Except that $\S 60.7$ only applies as specified in $\S 60.4214(a)$ .
§ 60.8	Performance tests	Yes	Except that $\frac{60.8}{2}$ only applies to stationary CI ICE with a displacement of ( $\geq$ 30 liters per cylinder and engines that are not certified.
§ 60.9	Availability of information	Yes	
§ 60.10	State Authority	Yes	
§ 60.11	Compliance with standards and maintenance requirements	No	Requirements are specified in subpart IIII.
§ 60.12	Circumvention	Yes	
§ 60.13	Monitoring requirements	Yes	Except that $\S 60.13$ only applies to stationary CI ICE with a displacement of ( $\geq$ 30 liters per cylinder.
§ 60.14	Modification	Yes	
§ 60.15	Reconstruction	Yes	
§ 60.16	Priority list	Yes	
§ 60.17	Incorporations by reference	Yes	
§ 60.18	General control device requirements	No	
§ 60.19	General notification and reporting requirements	Yes	

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# Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006

Subpart VVa—Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006, and on or Before April 25, 2023

Source:

72 FR 64883, Nov. 16, 2007, unless otherwise noted.

### § 60.480a Applicability and designation of affected facility.

(a)

(1) The provisions of this subpart apply to affected facilities in the synthetic organic chemicals manufacturing industry.

(2) The group of all equipment (defined in  $\S 60.481a$ ) within a process unit is an affected facility.

(b) Any affected facility under <u>paragraph (a)</u> of this section that commences construction, reconstruction, or modification after November 7, 2006, and on or before April 25, 2023, shall be subject to the requirements of this subpart.

(c) Addition or replacement of equipment for the purpose of process improvement which is accomplished without a capital expenditure shall not by itself be considered a modification under this subpart.

(d)

(1) If an owner or operator applies for one or more of the exemptions in this paragraph, then the owner or operator shall maintain records as required in  $\frac{60.486a(i)}{10}$ .

(2) Any affected facility that has the design capacity to produce less than 1,000 Mg/yr (1,102 ton/yr) of a chemical listed in § 60.489 is exempt from §§ 60.482-1a through 60.482-10a.

(3) If an affected facility produces heavy liquid chemicals only from heavy liquid feed or raw materials, then it is exempt from  $\frac{88\ 60.482-1a}{82-1a}$  through  $\frac{60.482-10a}{82-10a}$ .

(4) Any affected facility that produces beverage alcohol is exempt from  $\frac{8860.482-1a}{1000}$  through  $\frac{60.482-10a}{1000}$ .

(5) Any affected facility that has no equipment in volatile organic compounds (VOC) service is exempt from  $\frac{\&\& 60.482-1}{1a}$  through  $\frac{60.482-10a}{1a}$ .

(e) Alternative means of compliance —

(1) Option to comply with part 65.

(i) Owners or operators may choose to comply with the provisions of <u>40 CFR part 65</u>, <u>subpart F</u>, to satisfy the requirements of <u>§§ 60.482-1a</u> through <u>60.487a</u> for an affected facility. When choosing to comply with <u>40 CFR part 65</u>, <u>subpart</u> <u>F</u>, <u>the</u> requirements of <u>§§ 60.485a(d)</u>, (e), and (f), and <u>60.486a(i)</u> and (j) still apply. Other provisions applying to an owner or operator who chooses to comply with 40 CFR part 65 are provided in 40 CFR 65.1.

(ii) Part 60, subpart A. Owners or operators who choose to comply with 40 CFR part 65, subpart F must also comply with  $\underline{\$\$}$  60.1, 60.2, 60.5, 60.6, 60.7(a)(1) and (4), 60.14, 60.15, and 60.16 for that equipment. All sections and paragraphs of subpart A of this part that are not mentioned in this paragraph (e)(1)(ii) do not apply to owners or operators of equipment subject to this subpart complying with 40 CFR part 65, subpart F, except that provisions required to be met prior to implementing 40 CFR part 65 still apply. Owners and operators who choose to comply with 40 CFR part 65, subpart F, must comply with 40 CFR part 65, subpart A.

### (2) Part 63, subpart H.

(i) Owners or operators may choose to comply with the provisions of <u>40 CFR part 63, subpart H</u>, to satisfy the requirements of <u>§§ 60.482-1a</u> through <u>60.487a</u> for an affected facility. When choosing to comply with <u>40 CFR part 63, subpart</u> <u>H</u>, the requirements of <u>§ 60.485a(d)</u>, (e), and (f), and <u>§ 60.486a(i)</u> and (j) still apply.

(ii) Part 60, subpart A. Owners or operators who choose to comply with 40 CFR part 63, subpart H must also comply with  $\underline{\$\$}$ 60.1, 60.2, 60.5, 60.6, 60.7(a)(1) and (4), 60.14, 60.15, and 60.16 for that equipment. All sections and paragraphs of subpart A of this part that are not mentioned in this paragraph (e)(2)(ii) do not apply to owners or operators of equipment subject to this subpart complying with 40 CFR part 63, subpart H, except that provisions required to be met prior to implementing 40

### Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006

CFR part 63 still apply. Owners and operators who choose to comply with 40 CFR part 63, subpart H, must comply with 40 CFR part 63, subpart A.

(f) Owners and operators of flares that are subject to the flare related requirements of this subpart and flare related requirements of any other regulation in this part or 40 CFR part 61 or 63, may elect to comply with the requirements in § 60.619a, § 60.669a, or § 60.709a, in lieu of all flare related requirements in any other regulation in this part or 40 CFR part <u>61</u> or <u>63</u>.

[72 FR 64883, Nov. 16, 2007, as amended at 73 FR 31375, June 2, 2008; 89 FR 43070, May 16, 2024]

### § 60.481a Definitions.

As used in this subpart, all terms not defined herein shall have the meaning given them in the Clean Air Act (CAA) or in subpart A of part 60, and the following terms shall have the specific meanings given them.

*Capital expenditure* means, in addition to the definition in § 60.2, an expenditure for a physical or operational change to an existing facility that:

(1) Exceeds P, the product of the facility's replacement cost, R, and an adjusted annual asset guideline repair allowance, A, as reflected by the following equation:  $P = R \times A$ , where:

(i) The adjusted annual asset guideline repair allowance, A, is the product of the percent of the replacement cost, Y, and the applicable basic annual asset guideline repair allowance, B, divided by 100 as reflected by the following equation:

Equation 1 to Capital Expenditure Paragraph (1)(i)

 $A = Y \times (B \div 100);$ 

(ii) The percent Y is determined from the following equation:  $Y = 1.0 - 0.575 \log X$ , where X is:

(A) 2006 minus the year of construction if the physical or operational change to the existing facility was on or after November 16, 2007, or

(B) 1982 minus the year of construction if the physical or operational change to the existing facility was prior to November 16, 2007; and

(iii) The applicable basic annual asset guideline repair allowance, B, is selected from the following table consistent with the applicable subpart:

Table 1 to Capital Expenditure Paragraph (1)(iii)—Determining Applicable Value for B			
Subpart applicable to facility	Value of B to be used in equation		
(A) VVa	12.5		
(B) GGGa	7.0		

Closed-loop system means an enclosed system that returns process fluid to the process.

Closed-purge system means a system or combination of systems and portable containers to capture purged liquids. Containers for purged liquids must be covered or closed when not being filled or emptied.

Closed vent system means a system that is not open to the atmosphere and that is composed of hard-piping, ductwork, connections, and, if necessary, flow-inducing devices that transport gas or vapor from a piece or pieces of equipment to a control device or back to a process.

Connector means flanged, screwed, or other joined fittings used to connect two pipe lines or a pipe line and a piece of process equipment or that close an opening in a pipe that could be connected to another pipe. Joined fittings welded completely around the circumference of the interface are not considered connectors for the purpose of this regulation.

*Control device* means an enclosed combustion device, vapor recovery system, or flare.

Distance piece means an open or enclosed casing through which the piston rod travels, separating the compressor cylinder from the crankcase.

# Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006

*Double block and bleed system* means two block valves connected in series with a bleed valve or line that can vent the line between the two block valves.

*Duct work* means a conveyance system such as those commonly used for heating and ventilation systems. It is often made of sheet metal and often has sections connected by screws or crimping. Hard-piping is not ductwork.

*Equipment* means each pump, compressor, pressure relief device, sampling connection system, open-ended valve or line, valve, and flange or other connector in VOC service and any devices or systems required by this subpart.

*First attempt at repair* means to take action for the purpose of stopping or reducing leakage of organic material to the atmosphere using best practices.

Fuel gas means gases that are combusted to derive useful work or heat.

*Fuel gas system* means the offsite and onsite piping and flow and pressure control system that gathers gaseous stream(s) generated by onsite operations, may blend them with other sources of gas, and transports the gaseous stream for use as fuel gas in combustion devices or in-process combustion equipment, such as furnaces and gas turbines, either singly or in combination.

*Hard-piping* means pipe or tubing that is manufactured and properly installed using good engineering judgment and standards such as ASME B31.3, Process Piping (available from the American Society of Mechanical Engineers, P.O. Box 2300, Fairfield, NJ 07007-2300).

In gas/vapor service means that the piece of equipment contains process fluid that is in the gaseous state at operating conditions.

In heavy liquid service means that the piece of equipment is not in gas/vapor service or in light liquid service.

In light liquid service means that the piece of equipment contains a liquid that meets the conditions specified in § 60.485a(e).

In-situ sampling systems means nonextractive samplers or in-line samplers.

*In vacuum service* means that equipment is operating at an internal pressure which is at least 5 kilopascals (kPa) (0.7 psia) below ambient pressure.

*In VOC service* means that the piece of equipment contains or contacts a process fluid that is at least 10 percent VOC by weight. (The provisions of  $\frac{60.485a(d)}{2}$  specify how to determine that a piece of equipment is not in VOC service.)

*Initial calibration value* means the concentration measured during the initial calibration at the beginning of each day required in  $\frac{60.485a(b)(1)}{1}$ , or the most recent calibration if the instrument is recalibrated during the day (i.e., the calibration is adjusted) after a calibration drift assessment.

Liquids dripping means any visible leakage from the seal including spraying, misting, clouding, and ice formation.

*Open-ended valve or line* means any valve, except safety relief valves, having one side of the valve seat in contact with process fluid and one side open to the atmosphere, either directly or through open piping.

*Pressure release means* the emission of materials resulting from system pressure being greater than set pressure of the pressure relief device.

*Process improvement* means routine changes made for safety and occupational health requirements, for energy savings, for better utility, for ease of maintenance and operation, for correction of design deficiencies, for bottleneck removal, for changing product requirements, or for environmental control.

*Process unit* means components assembled to produce, as intermediate or final products, one or more of the chemicals listed in  $\frac{60.489a}{1000}$ . A process unit can operate independently if supplied with sufficient feed or raw materials and sufficient storage facilities for the product.

*Process unit shutdown* means a work practice or operational procedure that stops production from a process unit or part of a process unit during which it is technically feasible to clear process material from a process unit or part of a process unit consistent with safety constraints and during which repairs can be accomplished. The following are not considered process unit shutdowns:

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(1) An unscheduled work practice or operational procedure that stops production from a process unit or part of a process unit for less than 24 hours.

(2) An unscheduled work practice or operational procedure that would stop production from a process unit or part of a process unit for a shorter period of time than would be required to clear the process unit or part of the process unit of materials and start up the unit, and would result in greater emissions than delay of repair of leaking components until the next scheduled process unit shutdown.

(3) The use of spare equipment and technically feasible bypassing of equipment without stopping production.

*Quarter* means a 3-month period; the first quarter concludes on the last day of the last full month during the 180 days following initial startup.

*Repaired* means that equipment is adjusted, or otherwise altered, in order to eliminate a leak as defined in the applicable sections of this subpart and, except for leaks identified in accordance with  $\frac{\$\$ 60.482}{2a(b)(2)(ii)}$  and (d)(6)(iii),  $\frac{60.482}{2}-3a(f)$ , and  $\frac{60.482}{2}-10a(f)(1)(ii)$ , is re-monitored as specified in  $\frac{\$ 60.485a(b)}{2}$  to

 $\frac{2a(b)(2)(ii)}{2a(b)(2)(ii)}$  and  $\frac{(d)(6)(ii)}{2a(b)(2)(ii)}$ ,  $\frac{60.482}{2}$ -3a(f), and 60.482-10a(f)(1)(ii), is re-monitored as specified in  $\frac{8}{2}$  60.485a(b) to verify that emissions from the equipment are below the applicable leak definition.

Replacement cost means the capital needed to purchase all the depreciable components in a facility.

*Sampling connection system* means an assembly of equipment within a process unit used during periods of representative operation to take samples of the process fluid. Equipment used to take nonroutine grab samples is not considered a sampling connection system.

*Sensor* means a device that measures a physical quantity or the change in a physical quantity such as temperature, pressure, flow rate, pH, or liquid level.

*Storage vessel* means a tank or other vessel that is used to store organic liquids that are used in the process as raw material feedstocks, produced as intermediates or final products, or generated as wastes. Storage vessel does not include vessels permanently attached to motor vehicles, such as trucks, railcars, barges or ships.

Synthetic organic chemicals manufacturing industry means the industry that produces, as intermediates or final products, one or more of the chemicals listed in  $\S$  60.489.

*Transfer rack* means the collection of loading arms and loading hoses, at a single loading rack, that are used to fill tank trucks and/or railcars with organic liquids.

*Volatile organic compounds* or VOC means, for the purposes of this subpart, any reactive organic compounds as defined in  $\S$  <u>60.2</u> Definitions.

[72 FR 64883, Nov. 16, 2007, as amended at 89 FR 43070, May 16, 2024; 89 FR 55522, July 5, 2024]

### § 60.482-1a Standards: General.

(a) Each owner or operator subject to the provisions of this subpart shall demonstrate compliance with the requirements of  $\frac{\&\&}{60.482-1a}$  through  $\frac{60.482-10a}{60.482-10a}$  or  $\frac{\& 60.480a(e)}{60.482-1a}$  for all equipment within 180 days of initial startup.

(b) Compliance with  $\frac{\$}{60.482-1a}$  to  $\frac{60.482-10a}{60.482-10a}$  will be determined by review of records and reports, review of performance test results, and inspection using the methods and procedures specified in  $\frac{\$}{60.485a}$ .

(c)

(1) An owner or operator may request a determination of equivalence of a means of emission limitation to the requirements of  $\frac{860.482-2a}{60.482-3a}$ ,  $\frac{60.482-5a}{60.482-5a}$ ,  $\frac{60.482-6a}{60.482-6a}$ ,  $\frac{60.482-7a}{60.482-8a}$ , and  $\frac{60.482-10a}{60.482-10a}$  as provided in  $\frac{8}{60.484a}$ .

(2) If the Administrator makes a determination that a means of emission limitation is at least equivalent to the requirements of  $\S$  60.482-2a,  $\S$  60.482-3a,  $\S$  60.482-5a,  $\S$  60.482-6a,  $\S$  60.482-7a,  $\S$  60.482-8a, or  $\S$  60.482-10a, an owner or operator shall comply with the requirements of that determination.

(d) Equipment that is in vacuum service is excluded from the requirements of  $\frac{60.482-2a}{60.482-2a}$  through  $\frac{60.482-10a}{60.482-10a}$  if it is identified as required in  $\frac{60.482-10a}{60.486a(e)(5)}$ .

## Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006

(e) Equipment that an owner or operator designates as being in VOC service less than 300 hr/yr is excluded from the requirements of  $\frac{8}{60.482-2a}$  through  $\frac{60.482-10a}{60.482-10a}$  if it is identified as required in  $\frac{8}{60.486a(e)(6)}$  and it meets any of the conditions specified in paragraphs (e)(1) through (3) of this section.

(1) The equipment is in VOC service only during startup and shutdown, excluding startup and shutdown between batches of the same campaign for a batch process.

(2) The equipment is in VOC service only during process malfunctions or other emergencies.

(3) The equipment is backup equipment that is in VOC service only when the primary equipment is out of service.

(f)

(1) If a dedicated batch process unit operates less than 365 days during a year, an owner or operator may monitor to detect leaks from pumps, valves, and open-ended valves or lines at the frequency specified in the following table instead of monitoring as specified in  $\frac{88}{60.482-2a}$ ,  $\frac{60.482-2a}{60.482-7a}$ , and  $\frac{60.483.2}{a}$ :

Operating time (percent of hours during year)	Equivalent monitoring frequency time in use		
	Monthly	Quarterly	Semiannually
0 to <25	Quarterly	Annually	Annually.
25 to <50	Quarterly	Semiannually	Annually.
50 to <75	Bimonthly	Three quarters	Semiannually.
75 to 100	Monthly	Quarterly	Semiannually.

(2) Pumps and values that are shared among two or more batch process units that are subject to this subpart may be monitored at the frequencies specified in paragraph (f)(1) of this section, provided the operating time of all such process units is considered.

(3) The monitoring frequencies specified in <u>paragraph (f)(1)</u> of this section are not requirements for monitoring at specific intervals and can be adjusted to accommodate process operations. An owner or operator may monitor at any time during the specified monitoring period (e.g., month, quarter, year), provided the monitoring is conducted at a reasonable interval after completion of the last monitoring campaign. Reasonable intervals are defined in <u>paragraphs (f)(3)(i)</u> through <u>(iv)</u> of this section.

(i) When monitoring is conducted quarterly, monitoring events must be separated by at least 30 calendar days.

(ii) When monitoring is conducted semiannually (*i.e.*, once every 2 quarters), monitoring events must be separated by at least 60 calendar days.

(iii) When monitoring is conducted in 3 quarters per year, monitoring events must be separated by at least 90 calendar days.

(iv) When monitoring is conducted annually, monitoring events must be separated by at least 120 calendar days.

[<u>72 FR 64883</u>, Nov. 16, 2007, as amended at <u>89 FR 43070</u>, May 16, 2024; <u>89 FR 55522</u>, July 5, 2024; <u>89 FR 74136</u>, Sept. 12, 2024]

## § 60.482-2a Standards: Pumps in light liquid service.

(a)

(1) Each pump in light liquid service shall be monitored monthly to detect leaks by the methods specified in  $\S 60.485a(b)$ , except as provided in  $\S 60.482-1a(c)$  and (f) and paragraphs (d), (e), and (f) of this section. A pump that begins operation in light liquid service after the initial startup date for the process unit must be monitored for the first time within 30 days after the end of its startup period, except for a pump that replaces a leaking pump and except as provided in  $\S 60.482-1a(c)$  and (f) of this section.

(2) Each pump in light liquid service shall be checked by visual inspection each calendar week for indications of liquids dripping from the pump seal, except as provided in  $\frac{60.482-1a(f)}{10}$ .

(b)

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(1) The instrument reading that defines a leak is specified in paragraphs (b)(1)(i) and (ii) of this section.

(i) 5,000 parts per million (ppm) or greater for pumps handling polymerizing monomers;

(ii) 2,000 ppm or greater for all other pumps.

(2) If there are indications of liquids dripping from the pump seal, the owner or operator shall follow the procedure specified in either paragraph (b)(2)(i) or (ii) of this section. This requirement does not apply to a pump that was monitored after a previous weekly inspection and the instrument reading was less than the concentration specified in paragraph (b)(1)(i) or (ii) of this section, whichever is applicable.

(i) Monitor the pump within 5 days as specified in  $\S 60.485a(b)$ . A leak is detected if the instrument reading measured during monitoring indicates a leak as specified in paragraph (b)(1)(i) or (ii) of this section, whichever is applicable. The leak shall be repaired using the procedures in paragraph (c) of this section.

(ii) Designate the visual indications of liquids dripping as a leak, and repair the leak using either the procedures in <u>paragraph</u> (c) of this section or by eliminating the visual indications of liquids dripping.

(c)

(1) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in  $\frac{60.482-9a}{2}$ .

(2) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected. First attempts at repair include, but are not limited to, the practices described in <u>paragraphs (c)(2)(i)</u> and <u>(ii)</u> of this section, where practicable.

(i) Tightening the packing gland nuts;

(ii) Ensuring that the seal flush is operating at design pressure and temperature.

(d) Each pump equipped with a dual mechanical seal system that includes a barrier fluid system is exempt from the requirements of <u>paragraph (a)</u> of this section, provided the requirements specified in <u>paragraphs (d)(1)</u> through <u>(6)</u> of this section are met.

(1) Each dual mechanical seal system is:

(i) Operated with the barrier fluid at a pressure that is at all times greater than the pump stuffing box pressure; or

(ii) Equipped with a barrier fluid degassing reservoir that is routed to a process or fuel gas system or connected by a closed vent system to a control device that complies with the requirements of  $\frac{60.482-10a}{5}$ , or

(iii) Equipped with a system that purges the barrier fluid into a process stream with zero VOC emissions to the atmosphere.

(2) The barrier fluid system is in heavy liquid service or is not in VOC service.

(3) Each barrier fluid system is equipped with a sensor that will detect failure of the seal system, the barrier fluid system, or both.

(4)

(i) Each pump is checked by visual inspection, each calendar week, for indications of liquids dripping from the pump seals.

(ii) If there are indications of liquids dripping from the pump seal at the time of the weekly inspection, the owner or operator shall follow the procedure specified in either paragraph (d)(4)(ii)(A) or (B) of this section prior to the next required inspection.

(A) Monitor the pump within 5 days as specified in  $\S$  60.485a(b) to determine if there is a leak of VOC in the barrier fluid. If an instrument reading of 2,000 ppm or greater is measured, a leak is detected.

(B) Designate the visual indications of liquids dripping as a leak.

(5)

(i) Each sensor as described in paragraph (d)(3) is checked daily or is equipped with an audible alarm.

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(ii) The owner or operator determines, based on design considerations and operating experience, a criterion that indicates failure of the seal system, the barrier fluid system, or both.

(iii) If the sensor indicates failure of the seal system, the barrier fluid system, or both, based on the criterion established in paragraph (d)(5)(ii) of this section, a leak is detected.

(6)

(i) When a leak is detected pursuant to  $\underline{\text{paragraph } (d)(4)(ii)(A)}$  of this section, it shall be repaired as specified in  $\underline{\text{paragraph }}(\underline{c})$  of this section.

(ii) A leak detected pursuant to paragraph (d)(5)(iii) of this section shall be repaired within 15 days of detection by eliminating the conditions that activated the sensor.

(iii) A designated leak pursuant to <u>paragraph (d)(4)(ii)(B)</u> of this section shall be repaired within 15 days of detection by eliminating visual indications of liquids dripping.

(e) Any pump that is designated, as described in  $\S 60.486a(e)(1)$  and (2), for no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background, is exempt from the requirements of paragraphs (a), (c), and (d) of this section if the pump:

(1) Has no externally actuated shaft penetrating the pump housing;

(2) Is demonstrated to be operating with no detectable emissions as indicated by an instrument reading of less than 500 ppm above background as measured by the methods specified in  $\S 60.485a(c)$ ; and

(3) Is tested for compliance with <u>paragraph (e)(2)</u> of this section initially upon designation, annually, and at other times requested by the Administrator.

(f) If any pump is equipped with a closed vent system capable of capturing and transporting any leakage from the seal or seals to a process or to a fuel gas system or to a control device that complies with the requirements of  $\S$  60.482-10a, it is exempt from paragraphs (a) through (e) of this section.

(g) Any pump that is designated, as described in  $\S 60.486a(f)(1)$ , as an unsafe-to-monitor pump is exempt from the monitoring and inspection requirements of <u>paragraphs (a)</u> and (d)(4) through (6) of this section if:

(1) The owner or operator of the pump demonstrates that the pump is unsafe-to-monitor because monitoring personnel would be exposed to an immediate danger as a consequence of complying with <u>paragraph (a)</u> of this section; and

(2) The owner or operator of the pump has a written plan that requires monitoring of the pump as frequently as practicable during safe-to-monitor times, but not more frequently than the periodic monitoring schedule otherwise applicable, and repair of the equipment according to the procedures in <u>paragraph (c)</u> of this section if a leak is detected.

(h) Any pump that is located within the boundary of an unmanned plant site is exempt from the weekly visual inspection requirement of <u>paragraphs (a)(2)</u> and (d)(4) of this section, and the daily requirements of <u>paragraph (d)(5)</u> of this section, provided that each pump is visually inspected as often as practicable and at least monthly.

## § 60.482-3a Standards: Compressors.

(a) Each compressor shall be equipped with a seal system that includes a barrier fluid system and that prevents leakage of VOC to the atmosphere, except as provided in  $\S 60.482-1a(c)$  and paragraphs (h), (i), and (j) of this section.

(b) Each compressor seal system as required in <u>paragraph (a)</u> of this section shall be:

(1) Operated with the barrier fluid at a pressure that is greater than the compressor stuffing box pressure; or

(2) Equipped with a barrier fluid system degassing reservoir that is routed to a process or fuel gas system or connected by a closed vent system to a control device that complies with the requirements of  $\frac{60.482-10a}{5}$ , or

(3) Equipped with a system that purges the barrier fluid into a process stream with zero VOC emissions to the atmosphere.

(c) The barrier fluid system shall be in heavy liquid service or shall not be in VOC service.

(d) Each barrier fluid system as described in paragraph (a) shall be equipped with a sensor that will detect failure of the seal system, barrier fluid system, or both.

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(e)

(1) Each sensor as required in <u>paragraph (d)</u> of this section shall be checked daily or shall be equipped with an audible alarm.

(2) The owner or operator shall determine, based on design considerations and operating experience, a criterion that indicates failure of the seal system, the barrier fluid system, or both.

(f) If the sensor indicates failure of the seal system, the barrier system, or both based on the criterion determined under <u>paragraph (e)(2)</u> of this section, a leak is detected.

(g)

(1) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in  $\frac{60.482-9a}{2}$ .

(2) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(h) A compressor is exempt from the requirements of <u>paragraphs (a)</u> and (b) of this section, if it is equipped with a closed vent system to capture and transport leakage from the compressor drive shaft back to a process or fuel gas system or to a control device that complies with the requirements of  $\frac{60.482-10a}{60.482-10a}$ , except as provided in <u>paragraph (i)</u> of this section.

(i) Any compressor that is designated, as described in  $\S 60.486a(e)(1)$  and (2), for no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background, is exempt from the requirements of paragraphs (a) through (h) of this section if the compressor:

(1) Is demonstrated to be operating with no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background, as measured by the methods specified in  $\S$  60.485a(c); and

(2) Is tested for compliance with <u>paragraph (i)(1)</u> of this section initially upon designation, annually, and at other times requested by the Administrator.

(j) Any existing reciprocating compressor in a process unit which becomes an affected facility under provisions of  $\S$  60.14 or  $\S$  60.15 is exempt from paragraphs (a) through (e) and (h) of this section, provided the owner or operator demonstrates that recasting the distance piece or replacing the compressor are the only options available to bring the compressor into compliance with the provisions of paragraphs (a) through (e) and (h) of this section.

### § 60.482-4a Standards: Pressure relief devices in gas/vapor service.

(a) Except during pressure releases, each pressure relief device in gas/vapor service shall be operated with no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background, as determined by the methods specified in  $\S$  60.485a(c).

(b)

(1) After each pressure release, the pressure relief device shall be returned to a condition of no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background, as soon as practicable, but no later than 5 calendar days after the pressure release, except as provided in  $\frac{8}{50.482-9a}$ .

(2) No later than 5 calendar days after the pressure release, the pressure relief device shall be monitored to confirm the conditions of no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background, by the methods specified in  $\frac{\& 60.485a(c)}{2}$ .

(c) Any pressure relief device that is routed to a process or fuel gas system or equipped with a closed vent system capable of capturing and transporting leakage through the pressure relief device to a control device as described in  $\S$  60.482-10a is exempted from the requirements of paragraphs (a) and (b) of this section.

(d)

(1) Any pressure relief device that is equipped with a rupture disk upstream of the pressure relief device is exempt from the requirements of <u>paragraphs (a)</u> and (b) of this section, provided the owner or operator complies with the requirements in <u>paragraph (d)(2)</u> of this section.

(2) After each pressure release, a new rupture disk shall be installed upstream of the pressure relief device as soon as practicable, but no later than 5 calendar days after each pressure release, except as provided in  $\frac{60.482-9a}{2}$ .

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### § 60.482-5a Standards: Sampling connection systems.

(a) Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent system, except as provided in  $\S 60.482-1a(c)$  and paragraph (c) of this section.

(b) Each closed-purge, closed-loop, or closed-vent system as required in <u>paragraph (a)</u> of this section shall comply with the requirements specified in <u>paragraphs (b)(1)</u> through (4) of this section.

(1) Gases displaced during filling of the sample container are not required to be collected or captured.

(2) Containers that are part of a closed-purge system must be covered or closed when not being filled or emptied.

(3) Gases remaining in the tubing or piping between the closed-purge system valve(s) and sample container valve(s) after the valves are closed and the sample container is disconnected are not required to be collected or captured.

(4) Each closed-purge, closed-loop, or closed-vent system shall be designed and operated to meet requirements in either paragraph (b)(4)(i), (ii), (iii), or (iv) of this section.

(i) Return the purged process fluid directly to the process line.

(ii) Collect and recycle the purged process fluid to a process.

(iii) Capture and transport all the purged process fluid to a control device that complies with the requirements of  $\frac{60.482}{10a}$ .

(iv) Collect, store, and transport the purged process fluid to any of the following systems or facilities:

(A) A waste management unit as defined in <u>40 CFR 63.111</u>, if the waste management unit is subject to and operated in compliance with the provisions of <u>40 CFR part 63</u>, subpart <u>6</u>, applicable to Group 1 wastewater streams;

(B) A treatment, storage, or disposal facility subject to regulation under <u>40 CFR part 262, 264, 265</u>, or <u>266</u>;

(C) A facility permitted, licensed, or registered by a state to manage municipal or industrial solid waste, if the process fluids are not hazardous waste as defined in <u>40 CFR part 261</u>;

(D) A waste management unit subject to and operated in compliance with the treatment requirements of  $\frac{40 \text{ CFR } 61.348(a)}{40 \text{ CFR } 61.348}$ , provided all waste management units that collect, store, or transport the purged process fluid to the treatment unit are subject to and operated in compliance with the management requirements of  $\frac{40 \text{ CFR } 61.343}{40 \text{ CFR } 61.343}$  through  $\frac{40 \text{ CFR } 61.347}{40 \text{ CFR } 61.347}$ ; or

(E) A device used to burn off-specification used oil for energy recovery in accordance with <u>40 CFR part 279, subpart G</u>, provided the purged process fluid is not hazardous waste as defined in <u>40 CFR part 261</u>.

(c) In-situ sampling systems and sampling systems without purges are exempt from the requirements of <u>paragraphs</u> (a) and (b) of this section.

### § 60.482-6a Standards: Open-ended valves or lines.

(a)

(1) Each open-ended valve or line shall be equipped with a cap, blind flange, plug, or a second valve, except as provided in  $\S$  <u>60.482-1a(c)</u> and <u>paragraphs (d)</u> and <u>(e)</u> of this section.

(2) The cap, blind flange, plug, or second valve shall seal the open end at all times except during operations requiring process fluid flow through the open-ended valve or line.

(b) Each open-ended valve or line equipped with a second valve shall be operated in a manner such that the valve on the process fluid end is closed before the second valve is closed.

(c) When a double block-and-bleed system is being used, the bleed valve or line may remain open during operations that require venting the line between the block valves but shall comply with <u>paragraph (a)</u> of this section at all other times.

(d) Open-ended valves or lines in an emergency shutdown system which are designed to open automatically in the event of a process upset are exempt from the requirements of <u>paragraphs (a)</u>, (b), and (c) of this section.

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(e) Open-ended valves or lines containing materials which would autocatalytically polymerize or would present an explosion, serious overpressure, or other safety hazard if capped or equipped with a double block and bleed system as specified in <u>paragraphs (a)</u> through (c) of this section are exempt from the requirements of <u>paragraphs (a)</u> through (c) of this section.

## § 60.482-7a Standards: Valves in gas/vapor service and in light liquid service.

(a)

(1) Each valve shall be monitored monthly to detect leaks by the methods specified in  $\frac{60.485a(b)}{10}$  and shall comply with <u>paragraphs (b)</u> through (c) of this section, except as provided in <u>paragraphs (f)</u>, (g), and (h) of this section,  $\frac{60.482-1a}{10}$  and (f), and  $\frac{860.483-1a}{10}$  and  $\frac{60.483-2a}{10}$ .

(2) A valve that begins operation in gas/vapor service or light liquid service after the initial startup date for the process unit must be monitored according to paragraphs (a)(2)(i) or (ii), except for a valve that replaces a leaking valve and except as provided in <u>paragraphs (f), (g)</u>, and (<u>h</u>) of this section, § 60.482-1a(c), and §§ 60.483-1a and 60.483-2a.

(i) Monitor the value as in <u>paragraph (a)(1)</u> of this section. The value must be monitored for the first time within 30 days after the end of its startup period to ensure proper installation.

(ii) If the existing values in the process unit are monitored in accordance with  $\S 60.483-1a$  or  $\S 60.483-2a$ , count the new value as leaking when calculating the percentage of values leaking as described in  $\S 60.483-2a(b)(5)$ . If less than 2.0 percent of the values are leaking for that process unit, the value must be monitored for the first time during the next scheduled monitoring event for existing values in the process unit or within 90 days, whichever comes first.

(b) If an instrument reading of 500 ppm or greater is measured, a leak is detected.

(c)

(1)

(i) Any valve for which a leak is not detected for 2 successive months may be monitored the first month of every quarter, beginning with the next quarter, until a leak is detected.

(ii) As an alternative to monitoring all of the valves in the first month of a quarter, an owner or operator may elect to subdivide the process unit into two or three subgroups of valves and monitor each subgroup in a different month during the quarter, provided each subgroup is monitored every 3 months. The owner or operator must keep records of the valves assigned to each subgroup.

(2) If a leak is detected, the valve shall be monitored monthly until a leak is not detected for 2 successive months.

(d)

(1) When a leak is detected, it shall be repaired as soon as practicable, but no later than 15 calendar days after the leak is detected, except as provided in  $\frac{60.482-9a}{2}$ .

(2) A first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(e) First attempts at repair include, but are not limited to, the following best practices where practicable:

(1) Tightening of bonnet bolts;

(2) Replacement of bonnet bolts;

(3) Tightening of packing gland nuts;

(4) Injection of lubricant into lubricated packing.

(f) Any valve that is designated, as described in  $\S$  60.486a(e)(2), for no detectable emissions, as indicated by an instrument reading of less than 500 ppm above background, is exempt from the requirements of <u>paragraph (a)</u> of this section if the valve:

(1) Has no external actuating mechanism in contact with the process fluid,

(2) Is operated with emissions less than 500 ppm above background as determined by the method specified in  $\S$  60.485a(c), and

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(3) Is tested for compliance with <u>paragraph (f)(2)</u> of this section initially upon designation, annually, and at other times requested by the Administrator.

(g) Any valve that is designated, as described in  $\S 60.486a(f)(1)$ , as an unsafe-to-monitor valve is exempt from the requirements of paragraph (a) of this section if:

(1) The owner or operator of the valve demonstrates that the valve is unsafe to monitor because monitoring personnel would be exposed to an immediate danger as a consequence of complying with <u>paragraph (a)</u> of this section, and

(2) The owner or operator of the valve adheres to a written plan that requires monitoring of the valve as frequently as practicable during safe-to-monitor times.

(h) Any valve that is designated, as described in  $\S 60.486a(f)(2)$ , as a difficult-to-monitor valve is exempt from the requirements of paragraph (a) of this section if:

(1) The owner or operator of the valve demonstrates that the valve cannot be monitored without elevating the monitoring personnel more than 2 meters above a support surface.

(2) The process unit within which the valve is located either:

(i) Becomes an affected facility through § 60.14 or § 60.15 and was constructed on or before January 5, 1981; or

(ii) Has less than 3.0 percent of its total number of valves designated as difficult-to-monitor by the owner or operator.

(3) The owner or operator of the valve follows a written plan that requires monitoring of the valve at least once per calendar year.

## § 60.482-8a Standards: Pumps, valves, and connectors in heavy liquid service and pressure relief devices in light liquid or heavy liquid service.

(a) If evidence of a potential leak is found by visual, audible, olfactory, or any other detection method at pumps, valves, and connectors in heavy liquid service and pressure relief devices in light liquid or heavy liquid service, the owner or operator shall follow either one of the following procedures:

(1) The owner or operator shall monitor the equipment within 5 days by the method specified in  $\S 60.485a(b)$  and shall comply with the requirements of <u>paragraphs (b)</u> through (d) of this section.

(2) The owner or operator shall eliminate the visual, audible, olfactory, or other indication of a potential leak within 5 calendar days of detection.

(b) If an instrument reading of 10,000 ppm or greater is measured, a leak is detected.

(c)

(1) When a leak is detected, it shall be repaired as soon as practicable, but not later than 15 calendar days after it is detected, except as provided in  $\frac{60.482-9a}{2}$ .

(2) The first attempt at repair shall be made no later than 5 calendar days after each leak is detected.

(d) First attempts at repair include, but are not limited to, the best practices described under  $\frac{\$\$ 60.482-2a(c)(2)}{7a(e)}$  and  $\frac{60.482}{7a(e)}$ .

### § 60.482-9a Standards: Delay of repair.

(a) Delay of repair of equipment for which leaks have been detected will be allowed if repair within 15 days is technically infeasible without a process unit shutdown. Repair of this equipment shall occur before the end of the next process unit shutdown. Monitoring to verify repair must occur within 15 days after startup of the process unit.

(b) Delay of repair of equipment will be allowed for equipment which is isolated from the process and which does not remain in VOC service.

(c) Delay of repair for valves and connectors will be allowed if:

(1) The owner or operator demonstrates that emissions of purged material resulting from immediate repair are greater than the fugitive emissions likely to result from delay of repair, and

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(2) When repair procedures are effected, the purged material is collected and destroyed or recovered in a control device complying with  $\frac{60.482-10a}{2}$ .

(d) Delay of repair for pumps will be allowed if:

(1) Repair requires the use of a dual mechanical seal system that includes a barrier fluid system, and

(2) Repair is completed as soon as practicable, but not later than 6 months after the leak was detected.

(e) Delay of repair beyond a process unit shutdown will be allowed for a valve, if valve assembly replacement is necessary during the process unit shutdown, valve assembly supplies have been depleted, and valve assembly supplies had been sufficiently stocked before the supplies were depleted. Delay of repair beyond the next process unit shutdown will not be allowed unless the next process unit shutdown occurs sooner than 6 months after the first process unit shutdown.

(f) When delay of repair is allowed for a leaking pump, valve, or connector that remains in service, the pump, valve, or connector may be considered to be repaired and no longer subject to delay of repair requirements if two consecutive monthly monitoring instrument readings are below the leak definition.

## § 60.482-10a Standards: Closed vent systems and control devices.

(a) Owners or operators of closed vent systems and control devices used to comply with provisions of this subpart shall comply with the provisions of this section.

(b) Vapor recovery systems (for example, condensers and absorbers) shall be designed and operated to recover the VOC emissions vented to them with an efficiency of 95 percent or greater, or to an exit concentration of 20 parts per million by volume (ppmv), whichever is less stringent.

(c) Enclosed combustion devices shall be designed and operated to reduce the VOC emissions vented to them with an efficiency of 95 percent or greater, or to an exit concentration of 20 ppmv, on a dry basis, corrected to 3 percent oxygen, whichever is less stringent or to provide a minimum residence time of 0.75 seconds at a minimum temperature of 816 °C.

(d) Flares used to comply with this subpart shall comply with the requirements of  $\frac{60.18}{5}$ .

(e) Owners or operators of control devices used to comply with the provisions of this subpart shall monitor these control devices to ensure that they are operated and maintained in conformance with their designs.

(f) Except as provided in <u>paragraphs (i)</u> through (k) of this section, each closed vent system shall be inspected according to the procedures and schedule specified in <u>paragraphs (f)(1)</u> and (2) of this section.

(1) If the vapor collection system or closed vent system is constructed of hard-piping, the owner or operator shall comply with the requirements specified in <u>paragraphs (f)(1)(i)</u> and <u>(ii)</u> of this section:

(i) Conduct an initial inspection according to the procedures in  $\S 60.485a(b)$ ; and

(ii) Conduct annual visual inspections for visible, audible, or olfactory indications of leaks.

(2) If the vapor collection system or closed vent system is constructed of ductwork, the owner or operator shall:

(i) Conduct an initial inspection according to the procedures in  $\S 60.485a(b)$ ; and

(ii) Conduct annual inspections according to the procedures in  $\frac{60.485a(b)}{2}$ .

(g) Leaks, as indicated by an instrument reading greater than 500 ppmv above background or by visual inspections, shall be repaired as soon as practicable except as provided in <u>paragraph (h)</u> of this section.

(1) A first attempt at repair shall be made no later than 5 calendar days after the leak is detected.

(2) Repair shall be completed no later than 15 calendar days after the leak is detected.

(h) Delay of repair of a closed vent system for which leaks have been detected is allowed if the repair is technically infeasible without a process unit shutdown or if the owner or operator determines that emissions resulting from immediate repair would be greater than the fugitive emissions likely to result from delay of repair. Repair of such equipment shall be complete by the end of the next process unit shutdown.

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(i) If a vapor collection system or closed vent system is operated under a vacuum, it is exempt from the inspection requirements of <u>paragraphs (f)(1)(i)</u> and <u>(f)(2)</u> of this section.

(j) Any parts of the closed vent system that are designated, as described in <u>paragraph (1)(1)</u> of this section, as unsafe to inspect are exempt from the inspection requirements of <u>paragraphs (f)(1)(i)</u> and <u>(f)(2)</u> of this section if they comply with the requirements specified in <u>paragraphs (j)(1)</u> and <u>(2)</u> of this section:

(1) The owner or operator determines that the equipment is unsafe to inspect because inspecting personnel would be exposed to an imminent or potential danger as a consequence of complying with <u>paragraphs (f)(1)(i)</u> or (f)(2) of this section; and

(2) The owner or operator has a written plan that requires inspection of the equipment as frequently as practicable during safe-to-inspect times.

(k) Any parts of the closed vent system that are designated, as described in <u>paragraph (1)(2)</u> of this section, as difficult to inspect are exempt from the inspection requirements of <u>paragraphs (f)(1)(i)</u> and <u>(f)(2)</u> of this section if they comply with the requirements specified in <u>paragraphs (k)(1)</u> through (3) of this section:

(1) The owner or operator determines that the equipment cannot be inspected without elevating the inspecting personnel more than 2 meters above a support surface; and

(2) The process unit within which the closed vent system is located becomes an affected facility through  $\frac{\$\$ 60.14}{\$\$}$  or  $\frac{60.15}{\$}$ , or the owner or operator designates less than 3.0 percent of the total number of closed vent system equipment as difficult to inspect; and

(3) The owner or operator has a written plan that requires inspection of the equipment at least once every 5 years. A closed vent system is exempt from inspection if it is operated under a vacuum.

(1) The owner or operator shall record the information specified in <u>paragraphs (1)(1)</u> through (5) of this section.

(1) Identification of all parts of the closed vent system that are designated as unsafe to inspect, an explanation of why the equipment is unsafe to inspect, and the plan for inspecting the equipment.

(2) Identification of all parts of the closed vent system that are designated as difficult to inspect, an explanation of why the equipment is difficult to inspect, and the plan for inspecting the equipment.

(3) For each inspection during which a leak is detected, a record of the information specified in  $\S 60.486a(c)$ .

(4) For each inspection conducted in accordance with  $\S 60.485a(b)$  during which no leaks are detected, a record that the inspection was performed, the date of the inspection, and a statement that no leaks were detected.

(5) For each visual inspection conducted in accordance with <u>paragraph (f)(1)(ii)</u> of this section during which no leaks are detected, a record that the inspection was performed, the date of the inspection, and a statement that no leaks were detected.

(m) Closed vent systems and control devices used to comply with provisions of this subpart shall be operated at all times when emissions may be vented to them.

#### § 60.483-1a Alternative standards for valves—allowable percentage of valves leaking.

(a) An owner or operator may elect to comply with an allowable percentage of valves leaking of equal to or less than 2.0 percent.

(b) The following requirements shall be met if an owner or operator wishes to comply with an allowable percentage of valves leaking:

(1) An owner or operator must notify the Administrator that the owner or operator has elected to comply with the allowable percentage of valves leaking before implementing this alternative standard, as specified in  $\frac{60.487a(d)}{10}$ .

(2) A performance test as specified in <u>paragraph (c)</u> of this section shall be conducted initially upon designation, annually, and at other times requested by the Administrator.

(3) If a valve leak is detected, it shall be repaired in accordance with  $\S 60.482-7a(d)$  and (e).

(c) Performance tests shall be conducted in the following manner:

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(1) All valves in gas/vapor and light liquid service within the affected facility shall be monitored within 1 week by the methods specified in  $\frac{60.485a(b)}{100}$ .

(2) If an instrument reading of 500 ppm or greater is measured, a leak is detected.

(3) The leak percentage shall be determined by dividing the number of valves for which leaks are detected by the number of valves in gas/vapor and light liquid service within the affected facility.

(d) Owners and operators who elect to comply with this alternative standard shall not have an affected facility with a leak percentage greater than 2.0 percent, determined as described in  $\S 60.485a(h)$ .

## § 60.483-2a Alternative standards for valves—skip period leak detection and repair.

(a)

(1) An owner or operator may elect to comply with one of the alternative work practices specified in <u>paragraphs</u> (b)(2) and (3) of this section.

(2) An owner or operator must notify the Administrator before implementing one of the alternative work practices, as specified in  $\S 60.487(d)a$ .

(b)

(1) An owner or operator shall comply initially with the requirements for valves in gas/vapor service and valves in light liquid service, as described in  $\frac{60.482-7a}{2}$ .

(2) After 2 consecutive quarterly leak detection periods with the percent of valves leaking equal to or less than 2.0, an owner or operator may begin to skip 1 of the quarterly leak detection periods for the valves in gas/vapor and light liquid service.

(3) After 5 consecutive quarterly leak detection periods with the percent of valves leaking equal to or less than 2.0, an owner or operator may begin to skip 3 of the quarterly leak detection periods for the valves in gas/vapor and light liquid service.

(4) If the percent of valves leaking is greater than 2.0, the owner or operator shall comply with the requirements as described in  $\frac{60.482-7a}{10}$  but can again elect to use this section.

(5) The percent of valves leaking shall be determined as described in § 60.485a(h).

(6) An owner or operator must keep a record of the percent of valves found leaking during each leak detection period.

(7) A valve that begins operation in gas/vapor service or light liquid service after the initial startup date for a process unit following one of the alternative standards in this section must be monitored in accordance with  $\S 60.482$ -7a(a)(2)(i) or (ii) before the provisions of this section can be applied to that valve.

### § 60.484a Equivalence of means of emission limitation.

(a) Each owner or operator subject to the provisions of this subpart may apply to the Administrator for determination of equivalence for any means of emission limitation that achieves a reduction in emissions of VOC at least equivalent to the reduction in emissions of VOC achieved by the controls required in this subpart.

(b) Determination of equivalence to the equipment, design, and operational requirements of this subpart will be evaluated by the following guidelines:

(1) Each owner or operator applying for an equivalence determination shall be responsible for collecting and verifying test data to demonstrate equivalence of means of emission limitation.

(2) The Administrator will compare test data for demonstrating equivalence of the means of emission limitation to test data for the equipment, design, and operational requirements.

(3) The Administrator may condition the approval of equivalence on requirements that may be necessary to assure operation and maintenance to achieve the same emission reduction as the equipment, design, and operational requirements.

(c) Determination of equivalence to the required work practices in this subpart will be evaluated by the following guidelines:

(1) Each owner or operator applying for a determination of equivalence shall be responsible for collecting and verifying test data to demonstrate equivalence of an equivalent means of emission limitation.

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(2) For each affected facility for which a determination of equivalence is requested, the emission reduction achieved by the required work practice shall be demonstrated.

(3) For each affected facility, for which a determination of equivalence is requested, the emission reduction achieved by the equivalent means of emission limitation shall be demonstrated.

(4) Each owner or operator applying for a determination of equivalence shall commit in writing to work practice(s) that provide for emission reductions equal to or greater than the emission reductions achieved by the required work practice.

(5) The Administrator will compare the demonstrated emission reduction for the equivalent means of emission limitation to the demonstrated emission reduction for the required work practices and will consider the commitment in paragraph (c)(4) of this section.

(6) The Administrator may condition the approval of equivalence on requirements that may be necessary to assure operation and maintenance to achieve the same emission reduction as the required work practice.

(d) An owner or operator may offer a unique approach to demonstrate the equivalence of any equivalent means of emission limitation.

(e)

(1) After a request for determination of equivalence is received, the Administrator will publish a notice in the Federal Register and provide the opportunity for public hearing if the Administrator judges that the request may be approved.

(2) After notice and opportunity for public hearing, the Administrator will determine the equivalence of a means of emission limitation and will publish the determination in the Federal Register.

(3) Any equivalent means of emission limitations approved under this section shall constitute a required work practice, equipment, design, or operational standard within the meaning of section 111(h)(1) of the CAA.

(f)

(1) Manufacturers of equipment used to control equipment leaks of VOC may apply to the Administrator for determination of equivalence for any equivalent means of emission limitation that achieves a reduction in emissions of VOC achieved by the equipment, design, and operational requirements of this subpart.

(2) The Administrator will make an equivalence determination according to the provisions of <u>paragraphs (b)</u>, (c), (d), and (e) of this section.

### § 60.485a Test methods and procedures.

(a) In conducting the performance tests required in  $\S 60.8$ , the owner or operator shall use as reference methods and procedures the test methods in <u>appendix A of this part</u> or other methods and procedures as specified in this section, except as provided in  $\S 60.8$ (b).

(b) The owner or operator shall determine compliance with the standards in  $\frac{8860.482-1a}{60.482-1a}$  through  $\frac{60.482-10a}{60.483a}$ , and  $\frac{60.484a}{60.484a}$  as follows:

(1) Method 21 shall be used to determine the presence of leaking sources. The instrument shall be calibrated before use each day of its use by the procedures specified in Method 21 of appendix A-7 of this part. The following calibration gases shall be used:

(i) Zero air (less than 10 ppm of hydrocarbon in air); and

(ii) A mixture of methane or n-hexane and air at a concentration no more than 2,000 ppm greater than the leak definition concentration of the equipment monitored. If the monitoring instrument's design allows for multiple calibration scales, then the lower scale shall be calibrated with a calibration gas that is no higher than 2,000 ppm above the concentration specified as a leak, and the highest scale shall be calibrated with a calibration gas that is approximately equal to 10,000 ppm. If only one scale on an instrument will be used during monitoring, the owner or operator need not calibrate the scales that will not be used during that day's monitoring.

(2) A calibration drift assessment shall be performed, at a minimum, at the end of each monitoring day. Check the instrument using the same calibration gas(es) that were used to calibrate the instrument before use. Follow the procedures specified in

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Method 21 of appendix A-7 to this part, <u>section 10.1</u>, except do not adjust the meter readout to correspond to the calibration gas value. Record the instrument reading for each scale used as specified in  $\frac{60.486a(e)(8)}{60.486a(e)(8)}$ . Divide the arithmetic difference of the initial and post-test calibration response by the corresponding calibration gas value for each scale and multiply by 100 to express the calibration drift as a percentage.

(i) If a calibration drift assessment shows a negative drift of more than 10 percent, then all equipment with instrument readings between the appropriate leak definition and the leak definition multiplied by (100 minus the percent of negative drift/divided by 100) that was monitored since the last calibration must be re-monitored.

(ii) If any calibration drift assessment shows a positive drift of more than 10 percent from the initial calibration value, then, at the owner/operator's discretion, all equipment with instrument readings above the appropriate leak definition and below the leak definition multiplied by (100 plus the percent of positive drift/divided by 100) monitored since the last calibration may be re-monitored.

(c) The owner or operator shall determine compliance with the no-detectable-emission standards in  $\frac{\$\$ 60.482-2a(e)}{60.482-3a(i)}$ ,  $\frac{60.482-2a(e)}{60.482-7a(f)}$ , and  $\frac{60.482-10a(e)}{60.482-10a(e)}$  as follows:

(1) The requirements of paragraph (b) shall apply.

(2) Method 21 of appendix A-7 of this part shall be used to determine the background level. All potential leak interfaces shall be traversed as close to the interface as possible. The arithmetic difference between the maximum concentration indicated by the instrument and the background level is compared with 500 ppm for determining compliance.

(d) The owner or operator shall test each piece of equipment unless he demonstrates that a process unit is not in VOC service, i.e., that the VOC content would never be reasonably expected to exceed 10 percent by weight. For purposes of this demonstration, the following methods and procedures shall be used:

(1) Procedures that conform to the general methods in ASTM E260-73, 91, or 96, E168-67, 77, or 92, E169-63, 77, or 93 (incorporated by reference—see  $\S$  60.17) shall be used to determine the percent VOC content in the process fluid that is contained in or contacts a piece of equipment.

(2) Organic compounds that are considered by the Administrator to have negligible photochemical reactivity may be excluded from the total quantity of organic compounds in determining the VOC content of the process fluid.

(3) Engineering judgment may be used to estimate the VOC content, if a piece of equipment had not been shown previously to be in service. If the Administrator disagrees with the judgment, paragraphs (d)(1) and (2) of this section shall be used to resolve the disagreement.

(e) The owner or operator shall demonstrate that a piece of equipment is in light liquid service by showing that all the following conditions apply:

(1) The vapor pressure of one or more of the organic components is greater than 0.3 kPa at 20 °C (1.2 in. H<sub>2</sub>O at 68 °F). Standard reference texts or ASTM D2879-83, 96, or 97 (incorporated by reference—see § 60.17) shall be used to determine the vapor pressures.

(2) The total concentration of the pure organic components having a vapor pressure greater than 0.3 kPa at 20 °C (1.2 in.  $H_2O$  at 68 °F) is equal to or greater than 20 percent by weight.

(3) The fluid is a liquid at operating conditions.

(f) Samples used in conjunction with <u>paragraphs (d)</u>, (e), and (g) of this section shall be representative of the process fluid that is contained in or contacts the equipment or the gas being combusted in the flare.

(g) The owner or operator shall determine compliance with the standards of flares as follows:

(1) Method 22 of appendix A-7 of this part shall be used to determine visible emissions.

(2) A thermocouple or any other equivalent device shall be used to monitor the presence of a pilot flame in the flare.

(3) The maximum permitted velocity for air assisted flares shall be computed using the following equation:

 $V_{max} = K_1 + K_2 H_T$ 

Where:

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V<sub>max</sub> = Maximum permitted velocity, m/sec (ft/sec).

 $H_T$  = Net heating value of the gas being combusted, MJ/scm (Btu/scf).

 $K_1 = 8.706$  m/sec (metric units) = 28.56 ft/sec (English units).

 $K_2 = 0.7084 \text{ m}^4/(\text{MJ-sec}) \text{ (metric units)} = 0.087 \text{ ft}^4/(\text{Btu-sec}) \text{ (English units)}.$ 

(4) The net heating value (HT) of the gas being combusted in a flare shall be computed using the following equation:

$$H_1 = K \sum_{i=1}^{n} C_i H_i$$

Where:

K = Conversion constant,  $1.740 \times 10^{-7}$  (g-mole)(MJ)/(ppm-scm-kcal) (metric units) =  $4.674 \times 10^{-6}$  [(g-mole)(Btu)/(ppm-scf-kcal)] (English units).

 $C_i$  = Concentration of sample component "i," ppm

H<sub>i</sub> = net heat of combustion of sample component "i" at 25 °C and 760 mm Hg (77 °F and 14.7 psi), kcal/g-mole.

(5) Method 18 of appendix A-6 to this part and ASTM D2504-67, 77, or 88 (Reapproved 1993) (incorporated by reference, see § 60.17) shall be used to determine the concentration of sample component "i." ASTM D6420-18 (incorporated by reference, see § 60.17) may be used in lieu of Method 18, under the conditions specified in <u>paragraphs</u> (g)(5)(i) through (iii) of this section.

(i) If the target compounds are all known and are all listed in <u>Section 1.1</u> of ASTM D6420-18 as measurable.

(ii) ASTM D6420-18 may not be used for methane and ethane.

(iii) ASTM D6420-18 may not be used as a total VOC method.

(6) ASTM D2382-76 or 88 or D4809-95 (incorporated by reference-see  $\S$  60.17) shall be used to determine the net heat of combustion of component "i" if published values are not available or cannot be calculated.

(7) Method 2, 2A, 2C, or 2D of appendix A-7 of this part, as appropriate, shall be used to determine the actual exit velocity of a flare. If needed, the unobstructed (free) cross-sectional area of the flare tip shall be used.

(h) The owner or operator shall determine compliance with  $\frac{60.483-1a}{2}$  or  $\frac{60.483-2a}{2}$  as follows:

(1) The percent of valves leaking shall be determined using the following equation:

 $V_{\rm L} = (V_{\rm L} / V_{\rm T}) * 100$ 

Where:

 $%V_L$  = Percent leaking values.

 $V_L$  = Number of valves found leaking.

 $V_T$  = The sum of the total number of valves monitored.

(2) The total number of valves monitored shall include difficult-to-monitor and unsafe-to-monitor valves only during the monitoring period in which those valves are monitored.

(3) The number of valves leaking shall include valves for which repair has been delayed.

(4) Any new valve that is not monitored within 30 days of being placed in service shall be included in the number of valves leaking and the total number of valves monitored for the monitoring period in which the valve is placed in service.

(5) If the process unit has been subdivided in accordance with  $\S 60.482-7a(c)(1)(ii)$ , the sum of valves found leaking during a monitoring period includes all subgroups.

(6) The total number of valves monitored does not include a valve monitored to verify repair.

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[72 FR 64883, Nov. 16, 2007, as amended at 89 FR 43070, May 16, 2024]

## § 60.486a Recordkeeping requirements.

(a)

(1) Each owner or operator subject to the provisions of this subpart shall comply with the recordkeeping requirements of this section.

(2) An owner or operator of more than one affected facility subject to the provisions of this subpart may comply with the recordkeeping requirements for these facilities in one recordkeeping system if the system identifies each record by each facility.

(3) The owner or operator shall record the information specified in <u>paragraphs (a)(3)(i)</u> through (v) of this section for each monitoring event required by <u> $\S$ </u> 60.482-2a, 60.482-3a, 60.482-7a, 60.482-8a, and 60.483-2a.

(i) Monitoring instrument identification.

- (ii) Operator identification.
- (iii) Equipment identification.
- (iv) Date of monitoring.

(v) Instrument reading.

(b) When each leak is detected as specified in  $\S$  60.482-2a, 60.482-3a, 60.482-7a, 60.482-8a, and 60.483-2a, the following requirements apply:

(1) A weatherproof and readily visible identification, marked with the equipment identification number, shall be attached to the leaking equipment.

(2) The identification on a valve may be removed after it has been monitored for 2 successive months as specified in  $\S$  <u>60.482-7a(c)</u> and no leak has been detected during those 2 months.

(3) [Reserved]

(4) The identification on equipment, except on a valve or connector, may be removed after it has been repaired.

(c) When each leak is detected as specified in <u>§§ 60.482-2a</u>, <u>60.482-3a</u>, <u>60.482-7a</u>, <u>60.482-8a</u>, and <u>60.483-2a</u>, the following information shall be recorded in a log and shall be kept for 2 years in a readily accessible location:

(1) The instrument and operator identification numbers and the equipment identification number, except when indications of liquids dripping from a pump are designated as a leak.

(2) The date the leak was detected and the dates of each attempt to repair the leak.

(3) Repair methods applied in each attempt to repair the leak.

(4) Maximum instrument reading measured by Method 21 of appendix A-7 of this part at the time the leak is successfully repaired or determined to be nonrepairable, except when a pump is repaired by eliminating indications of liquids dripping.

(5) "Repair delayed" and the reason for the delay if a leak is not repaired within 15 calendar days after discovery of the leak.

(6) The signature of the owner or operator (or designate) whose decision it was that repair could not be effected without a process shutdown.

(7) The expected date of successful repair of the leak if a leak is not repaired within 15 days.

(8) Dates of process unit shutdowns that occur while the equipment is unrepaired.

(9) The date of successful repair of the leak.

(d) The following information pertaining to the design requirements for closed vent systems and control devices described in  $\S$  60.482-10a shall be recorded and kept in a readily accessible location:

(1) Detailed schematics, design specifications, and piping and instrumentation diagrams.

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(2) The dates and descriptions of any changes in the design specifications.

(3) A description of the parameter or parameters monitored, as required in  $\S 60.482-10a(e)$ , to ensure that control devices are operated and maintained in conformance with their design and an explanation of why that parameter (or parameters) was selected for the monitoring.

(4) Periods when the closed vent systems and control devices required in  $\frac{88}{60.482-2a}$ ,  $\frac{60.482-3a}{60.482-3a}$ ,  $\frac{60.482-4a}{60.482-4a}$ , and  $\frac{60.482-3a}{60.482-4a}$ .

(5) Dates of startups and shutdowns of the closed vent systems and control devices required in  $\frac{8860.482-2a}{60.482-5a}$ .

(1) A list of identification numbers for equipment subject to the requirements of this subpart.

(2)

(i) A list of identification numbers for equipment that are designated for no detectable emissions under the provisions of  $\underline{\$\$}$ <u>60.482-2a(e)</u>, <u>60.482</u>-3a(i), and 60.482-7a(f).

(ii) The designation of equipment as subject to the requirements of  $\S 60.482-2a(e)$ ,  $\S 60.482-3a(i)$ , or  $\S 60.482-7a(f)$  shall be signed by the owner or operator. Alternatively, the owner or operator may establish a mechanism with their permitting authority that satisfies this requirement.

(3) A list of equipment identification numbers for pressure relief devices required to comply with § 60.482-4a.

(4)

(i) The dates of each compliance test as required in <u>§§ 60.482-2a(e)</u>, <u>60.482</u>-3a(i), 60.482-4a, and 60.482-7a(f).

(ii) The background level measured during each compliance test.

(iii) The maximum instrument reading measured at the equipment during each compliance test.

(5) A list of identification numbers for equipment in vacuum service.

(6) A list of identification numbers for equipment that the owner or operator designates as operating in VOC service less than 300 hr/yr in accordance with  $\S$  60.482-1a(e), a description of the conditions under which the equipment is in VOC service, and rationale supporting the designation that it is in VOC service less than 300 hr/yr.

(7) The date and results of the weekly visual inspection for indications of liquids dripping from pumps in light liquid service.

(8) Records of the information specified in paragraphs (e)(8)(i) through (vi) of this section for monitoring instrument calibrations conducted according to sections 8.1.2 and 10 of Method 21 of appendix A-7 of this part and  $\S 60.485a(b)$ .

(i) Date of calibration and initials of operator performing the calibration.

(ii) Calibration gas cylinder identification, certification date, and certified concentration.

(iii) Instrument scale(s) used.

(iv) A description of any corrective action taken if the meter readout could not be adjusted to correspond to the calibration gas value in accordance with section 10.1 of Method 21 of appendix A-7 of this part.

(v) Results of each calibration drift assessment required by  $\frac{60.485a(b)(2)}{60.485a(b)(2)}$  (i.e., instrument reading for calibration at end of monitoring day and the calculated percent difference from the initial calibration value).

(vi) If an owner or operator makes their own calibration gas, a description of the procedure used.

(9) [Reserved]

(10) Records of each release from a pressure relief device subject to  $\S 60.482-4a$ .

(f) The following information pertaining to all valves subject to the requirements of  $\S 60.482-7a(g)$  and (h), and all pumps subject to the requirements of  $\S 60.482-2a(g)$  shall be recorded in a log that is kept in a readily accessible location:

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(1) A list of identification numbers for valves, pumps, and connectors that are designated as unsafe-to-monitor, an explanation for each valve, pump, or connector stating why the valve, pump, or connector is unsafe-to-monitor, and the plan for monitoring each valve, pump, or connector.

(2) A list of identification numbers for valves that are designated as difficult-to-monitor, an explanation for each valve stating why the valve is difficult-to-monitor, and the schedule for monitoring each valve.

(g) The following information shall be recorded for valves complying with  $\frac{60.483-2a}{2}$ :

(1) A schedule of monitoring.

(2) The percent of valves found leaking during each monitoring period.

(h) The following information shall be recorded in a log that is kept in a readily accessible location:

(1) Design criterion required in §§ 60.482-2a(d)(5) and 60.482-3a(e)(2) and explanation of the design criterion; and

(2) Any changes to this criterion and the reasons for the changes.

(i) The following information shall be recorded in a log that is kept in a readily accessible location for use in determining exemptions as provided in  $\frac{60.480a(d)}{2}$ :

(1) An analysis demonstrating the design capacity of the affected facility,

(2) A statement listing the feed or raw materials and products from the affected facilities and an analysis demonstrating whether these chemicals are heavy liquids or beverage alcohol, and

(3) An analysis demonstrating that equipment is not in VOC service.

(j) Information and data used to demonstrate that a piece of equipment is not in VOC service shall be recorded in a log that is kept in a readily accessible location.

(k) The provisions of  $\frac{60.7(b)}{2}$  and  $\frac{(d)}{(d)}$  do not apply to affected facilities subject to this subpart.

(1) Any records required to be maintained by this subpart that are submitted electronically via the EPA's Compliance and Emissions Data Reporting Interface (CEDRI) may be maintained in electronic format. This ability to maintain electronic copies does not affect the requirement for facilities to make records, data, and reports available upon request to a delegated air agency or the EPA as part of an on-site compliance evaluation.

[72 FR 64883, Nov. 16, 2007, as amended at 89 FR 43071, May 16, 2024]

### § 60.487a Reporting requirements.

(a) Each owner or operator subject to the provisions of this subpart shall submit semiannual reports to the Administrator beginning 6 months after the initial startup date. Beginning on July 15, 2025, or once the report template for this subpart has been available on the CEDRI website (*https://www.epa.gov/electronic-reporting-air-emissions/cedri*) for 1 year, whichever date is later, submit all subsequent reports using the appropriate electronic report template on the CEDRI website for this subpart and following the procedure specified in <u>paragraph (g)</u> of this section. The date report templates become available will be listed on the CEDRI website. Unless the Administrator or delegated state agency or other authority has approved a different schedule for submission of reports, the report must be submitted by the deadline specified in this subpart, regardless of the method in which the report is submitted.

(b) The initial semiannual report to the Administrator shall include the following information:

(1) Process unit identification.

(2) Number of valves subject to the requirements of  $\S 60.482$ -7a, excluding those valves designated for no detectable emissions under the provisions of  $\S 60.482$ -7a(f).

(3) Number of pumps subject to the requirements of  $\S 60.482-2a$ , excluding those pumps designated for no detectable emissions under the provisions of  $\S 60.482-2a(e)$  and those pumps complying with  $\S 60.482-2a(f)$ .

(4) Number of compressors subject to the requirements of  $\S 60.482-3a$ , excluding those compressors designated for no detectable emissions under the provisions of  $\S 60.482-3a(i)$  and those compressors complying with  $\S 60.482-3a(h)$ .

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(c) All semiannual reports to the Administrator shall include the following information, summarized from the information in  $\frac{60.486a}{2}$ :

(1) Process unit identification.

(2) For each month during the semiannual reporting period,

(i) Number of values for which leaks were detected as described in  $\frac{60.482-7a(b)}{5}$  or  $\frac{60.483-2a}{5}$ ,

(ii) Number of values for which leaks were not repaired as required in  $\S 60.482-7a(d)(1)$ ,

(iii) Number of pumps for which leaks were detected as described in  $\S 60.482-2a(b)$ , (d)(4)(ii)(A) or (B), or (d)(5)(iii),

(iv) Number of pumps for which leaks were not repaired as required in  $\S 60.482-2a(c)(1)$  and (d)(6),

(v) Number of compressors for which leaks were detected as described in § 60.482-3a(f),

(vi) Number of compressors for which leaks were not repaired as required in § 60.482-3a(g)(1), and

(vii)-(x) [Reserved]

(xi) The facts that explain each delay of repair and, where appropriate, why a process unit shutdown was technically infeasible.

(3) Dates of process unit shutdowns which occurred within the semiannual reporting period.

(4) Revisions to items reported according to <u>paragraph (b)</u> of this section if changes have occurred since the initial report or subsequent revisions to the initial report.

(d) An owner or operator electing to comply with the provisions of  $\frac{\$\$ 60.483-1a}{\$}$  or  $\frac{60.483-2a}{\$}$  shall notify the Administrator of the alternative standard selected 90 days before implementing either of the provisions.

(e) An owner or operator shall report the results of all performance tests in accordance with  $\frac{60.8}{0.8}$  of the General Provisions. The provisions of  $\frac{60.8(d)}{0}$  do not apply to affected facilities subject to the provisions of this subpart except that an owner or operator must notify the Administrator of the schedule for the initial performance tests at least 30 days before the initial performance tests.

(f) The requirements of <u>paragraphs (a)</u> through (c) of this section remain in force until and unless EPA, in delegating enforcement authority to a state under section 111(c) of the CAA, approves reporting requirements or an alternative means of compliance surveillance adopted by such state. In that event, affected sources within the state will be relieved of the obligation to comply with the requirements of <u>paragraphs (a)</u> through (c) of this section, provided that they comply with the requirements established by the state. The EPA will not approve a waiver of electronic reporting to the EPA in delegating enforcement authority. Thus, electronic reporting to the EPA cannot be waived, and as such, the provisions of this paragraph cannot be used to relieve owners or operators of affected facilities of the requirement to submit the electronic reports required in this section to the EPA.

(g) If an owner or operator is required to submit notifications or reports following the procedure specified in this <u>paragraph</u> (g), the owner or operator must submit notifications or reports to the EPA via CEDRI, which can be accessed through the EPA's Central Data Exchange (CDX) (<u>https://cdx.epa.gov/</u>). The EPA will make all the information submitted through CEDRI available to the public without further notice to the owner or operator. Do not use CEDRI to submit information the owner or operator claims as CBI. Although the EPA does not expect persons to assert a claim of CBI, if you an owner or operator wishes to assert a CBI claim for some of the information in the report or notification, the owner or operator must submit a complete file in the format specified in this subpart, including information claimed to be CBI, to the EPA following the procedures in <u>paragraphs (g)(1)</u> and (<u>2</u>) of this section. Clearly mark the part or all of the information marked as CBI will not be disclosed except in accordance with procedures set forth in <u>40 CFR part 2</u>. All CBI claims must be asserted at the time of submission. Anything submitted using CEDRI cannot later be claimed CBI. Furthermore, under CAA section 114(c), emissions data is not entitled to confidential treatment, and the EPA is required to make emissions data available to the public. Thus, emissions data will not be CBI office with the CBI omitted to the EPA via the EPA's CDX as described earlier in this <u>paragraph (g)</u>.

## Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006

(1) The preferred method to receive CBI is for it to be transmitted electronically using email attachments, File Transfer Protocol, or other online file sharing services. Electronic submissions must be transmitted directly to the OAQPS CBI Office at the email address <u>oaqpscbi@epa.gov</u>, and as described above, should include clear CBI markings. ERT files should be flagged to the attention of the Group Leader, Measurement Policy Group; all other files should be flagged to the attention of the SOCMI NSPS Sector Lead. Owners and operators who do not have their own file sharing service and who require assistance with submitting large electronic files that exceed the file size limit for email attachments should email <u>oaqpscbi@epa.gov</u> to request a file transfer link.

(2) If an owner or operator cannot transmit the file electronically, the owner or operator may send CBI information through the postal service to the following address: OAQPS Document Control Officer (C404-02), OAQPS, U.S. Environmental Protection Agency, 109 T.W. Alexander Drive, P.O. Box 12055, Research Triangle Park, North Carolina 27711. ERT files should be sent to the attention of the Group Leader, Measurement Policy Group, and all other files should be sent to the attention of the SOCMI NSPS Sector Lead. The mailed CBI material should be double wrapped and clearly marked. Any CBI markings should not show through the outer envelope.

(h) Owners and operators required to electronically submit notifications or reports through CEDRI in the EPA's CDX may assert a claim of EPA system outage for failure to timely comply with that reporting requirement. To assert a claim of EPA system outage, owners and operators must meet the requirements outlined in <u>paragraphs (h)(1)</u> through (7) of this section.

(1) The owner or operator must have been or will be precluded from accessing CEDRI and submitting a required report within the time prescribed due to an outage of either the EPA's CEDRI or CDX systems.

(2) The outage must have occurred within the period of time beginning five business days prior to the date that the submission is due.

(3) The outage may be planned or unplanned.

(4) The owner or operator must submit notification to the Administrator in writing as soon as possible following the date the owner or operator first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

(5) The owner or operator must provide to the Administrator a written description identifying:

(i) The date(s) and time(s) when CDX or CEDRI was accessed and the system was unavailable;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to EPA system outage;

(iii) A description of measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which the owner or operator proposes to report, or if the owner or operator has already met the reporting requirement at the time of the notification, the date the report was submitted.

(6) The decision to accept the claim of EPA system outage and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(7) In any circumstance, the report must be submitted electronically as soon as possible after the outage is resolved.

(i) Owners and operators required to electronically submit notifications or reports through CEDRI in the EPA's CDX may assert a claim of *force majeure* for failure to timely comply with that reporting requirement. To assert a claim of *force majeure*, owners and operators must meet the requirements outlined in <u>paragraphs (i)(1)</u> through (5) of this section.

(1) An owner or operator may submit a claim if a *force majeure* event is about to occur, occurs, or has occurred or there are lingering effects from such an event within the period of time beginning five business days prior to the date the submission is due. For the purposes of this section, a *force majeure* event is defined as an event that will be or has been caused by circumstances beyond the control of the affected facility, its contractors, or any entity controlled by the affected facility that prevents the owner or operator from complying with the requirement to submit a report electronically within the time period prescribed. Examples of such events are acts of nature (*e.g.*, hurricanes, earthquakes, or floods), acts of war or terrorism, or equipment failure or safety hazard beyond the control of the affected facility (*e.g.*, large scale power outage).

(2) The owner or operator must submit notification to the Administrator in writing as soon as possible following the date the owner or operator first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

## Standards of Performance for Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry for Which Construction, Reconstruction, or Modification Commenced After November 7, 2006

(3) The owner or operator must provide to the Administrator:

(i) A written description of the *force majeure* event;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to the *force majeure* event;

(iii) A description of measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which the owner or operator proposes to report, or if the owner or operator has already met the reporting requirement at the time of the notification, the date the report was submitted.

(4) The decision to accept the claim of *force majeure* and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(5) In any circumstance, the reporting must occur as soon as possible after the *force majeure* event occurs.

[72 FR 64883, Nov. 16, 2007, as amended at 89 FR 43071, May 16, 2024]

#### § 60.488a Reconstruction.

For the purposes of this subpart:

(a) The cost of the following frequently replaced components of the facility shall not be considered in calculating either the "fixed capital cost of the new components" or the "fixed capital costs that would be required to construct a comparable new facility" under  $\S$  60.15: Pump seals, nuts and bolts, rupture disks, and packings.

(b) Under <u>§ 60.15</u>, the "fixed capital cost of new components" includes the fixed capital cost of all depreciable components (except components specified in <u>§ 60.488a(a)</u>) which are or will be replaced pursuant to all continuous programs of component replacement which are commenced within any 2-year period following the applicability date for the appropriate subpart. (See the "Applicability and designation of affected facility" section of the appropriate subpart.) For purposes of this paragraph, "commenced" means that an owner or operator has undertaken a continuous program of component replacement or that an owner or operator has entered into a contractual obligation to undertake and complete, within a reasonable time, a continuous program of component replacement.

### § 60.489a List of chemicals produced by affected facilities.

Process units that produce, as intermediates or final products, chemicals listed in  $\frac{60.489}{2}$  are covered under this subpart. The applicability date for process units producing one or more of these chemicals is November 8, 2006.

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#### FACILITY-WIDE REPORTING REQUIREMENTS (Version Dated 8/8/2019)

**RR1.** <u>Reporting Schedule</u>. This table summarizes information for convenience purposes only. It does not supersede any of the terms or conditions of this permit.

Report	Reporting Deadline(s)	Related Condition(s)
Plant Problems/Permit Deviations	Immediately upon occurrence (See RR2.d.)	RR2, RR3
Malfunction Excess Emissions Report	Quarterly (if requested)	RR3
Semi-Annual Monitoring Report	Every 6 months	RR4
Annual Operating Report	April 1	RR5
EAOR Title V Annual Emissions Fee Invoice and Fee Payment	April 1	RR6
Annual Statement of Compliance	Within 60 days after the end of each calendar year (or more frequently if specified by Rule 62-213.440(2), F.A.C., or by any other applicable requirement); and Within 60 days after submittal of a written agreement for transfer of responsibility, or Within 60 days after permanent shutdown.	RR7
Notification of Administrative Permit Corrections	As needed	RR8
Notification of Startup after Shutdown for More than One Year	Minimum of 60 days prior to the intended startup date or, if emergency startup, as soon as possible after the startup date is ascertained	RR9
Permit Renewal Application	225 days prior to the expiration date of permit	TV18
Test Reports	Maximum 45 days following compliance tests	TR9

{*Permitting Note: See permit Section III. Emissions Units and Specific Conditions, for any additional Emission Unit-specific reporting requirements.*}

#### RR2. <u>Reports of Problems</u>.

- a. Plant Operation Problems. If the permittee is temporarily unable to comply with any of the conditions of the permit due to breakdown of equipment or destruction by hazard of fire, wind or by other cause, the permittee shall immediately notify the Department. Notification shall include pertinent information as to the cause of the problem, and what steps are being taken to correct the problem and to prevent its recurrence, and where applicable, the owner's intent toward reconstruction of destroyed facilities. Such notification does not release the permittee from any liability for failure to comply with Department rules.
- b. If, for any reason, the permittee does not comply with or will be unable to comply with any condition or limitation specified in this permit, the permittee shall immediately provide the Department with the following information:
  - (1) A description of and cause of noncompliance; and
  - (2) The period of noncompliance, including dates and times; or, if not corrected, the anticipated time the noncompliance is expected to continue, and steps being taken to reduce, eliminate, and prevent recurrence of the noncompliance. The permittee shall be responsible for any and all damages which may result and may be subject to enforcement action by the Department for penalties or for revocation of this permit.
- c. When requested by the Department, the permittee shall within a reasonable time furnish any information required by law which is needed to determine compliance with the permit. If the permittee becomes aware the relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly.
- d. "Immediately" shall mean the same day, if during a workday (i.e., 8:00 a.m. 5:00 p.m.), or the first business day after the incident, excluding weekends and holidays; and, for purposes of Rule 62-4.160(15) and 40 CFR 70.6(a)(3)(iii)(B), "promptly" or "prompt" shall have the same meaning as "immediately".

[Rules 62-4.130, 62-4.160(8), 62-4.160(15) & 62-213.440(1)(b)3.c., F.A.C.; and, 40 CFR 70.6(a)(3)(iii)(B)]

## FACILITY-WIDE REPORTING REQUIREMENTS

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**RR3.** <u>Reports of Deviations from Permit Requirements</u>. The permittee shall report in accordance with the requirements of Rule 62-210.700(5), F.A.C. (below), and Rule 62-4.130, F.A.C. (condition RR2.), deviations from permit requirements, including those attributable to upset conditions as defined in the permit. Reports shall include the probable cause of such deviations, and any corrective actions or preventive measures taken.

*Rule 62-210.700(5)*: In case of excess emissions resulting from malfunctions, each owner or operator shall notify the Department or the appropriate Local Program in accordance with Rule 62-4.130, F.A.C. (See condition RR2.). A full written report on the malfunctions shall be submitted in a quarterly report, if requested by the Department.

[Rules 62-213.440(1)(b)3.b., and 62-210.700(5)F.A.C.]

- **RR4.** <u>Semi-Annual Monitoring Reports</u>. The permittee shall submit reports of any required monitoring at least every six (6) months. All instances of deviations from permit requirements must be clearly identified in such reports. [Rule 62-213.440(1)(b)3.a., F.A.C.]
- RR5. <u>Annual Operating Report</u>. The information required by the Annual Operating Report for Air Pollutant Emitting Facility [Including Title V Source Emissions Fee Calculation] (DEP Form No. 62-210.900(5)) shall be submitted by April 1 of each year, for the previous calendar year, to the Department of Environmental Protection's Division of Air Resource Management. Each Title V source shall submit the annual operating report using the DEP's Electronic Annual Operating Report (EAOR) software, unless the Title V source claims a technical or financial hardship by submitting DEP Form No. 62-210.900(5) to the DEP Division of Air Resource Management instead of using the reporting software. Emissions shall be computed in accordance with the provisions of subsection 62-210.370(2), F.A.C. [Rules 62-210.370(2) & (3), 62-210.900 and 62-213.440(3)(a)2., F.A.C.]
- **RR6.** <u>EAOR Title V Annual Emissions Fee Invoice and Fee Payment</u>. Each Title V source permitted to operate in Florida must pay between January 15 and April 1 of each year, an annual emissions fee in an amount determined as set forth in Rule 62-213.205(1), F.A.C.
  - a. If the Department has not received the fee by March 1 of the year following the calendar year for which the fee is calculated, the Department will send the primary responsible official of the Title V source a written warning of the consequences for failing to pay the fee by April 1. If the fee is not postmarked or electronically submitted by April 1 of the year due, the Department shall impose, in addition to the fee, a penalty of 50 percent of the amount of the fee unpaid plus interest on such amount computed in accordance with Section 220.807, F.S. If the Department determines that a submitted fee was inaccurately calculated, the Department shall either refund to the permittee any amount overpaid or notify the permittee of any amount underpaid. The Department shall not impose a penalty or interest on any amount underpaid, provided that the permittee has timely remitted payment of at least 90 percent of the amount underpaid. The Department shall waive the collection of underpayment and shall not refund overpayment of the fee, if the amount is less than one percent of the fee due, up to \$50.00. The Department shall make every effort to provide a timely assessment of the adequacy of the submitted fee. Failure to pay timely any required annual emissions fee, penalty, or interest constitutes grounds for permit revocation pursuant to Rule 62-4.100, F.A.C.
  - b. Any documentation of actual hours of operation, actual material or heat input, actual production amount, or actual emissions used to calculate the annual emissions fee shall be retained by the owner for a minimum of five years and shall be made available to the Department upon request.
  - c. A copy of the EAOR Title V Annual Emissions Fee Invoice generated by the electronic annual operating report (EAOR) application, must be submitted along with the annual emissions fee payment.

[Rules 62-210.370(3), 62-210.900 and 62-213.205, F.A.C.]

### **RR7.** <u>Annual Statement of Compliance</u>.

a. The permittee shall submit a Statement of Compliance with all terms and conditions of the permit that includes all the provisions of 40 CFR 70.6(c)(5)(iii), incorporated by reference at Rule 62-204.800, F.A.C., using DEP Form No. 62-213.900(2). Such statement shall be accompanied by a certification in accordance with Rule 62-213.420(4), F.A.C., for Title V requirements and with Rule 62-214.350, F.A.C., for Acid Rain requirements. Such statements shall be submitted (postmarked) to the Department and EPA:

### FACILITY-WIDE REPORTING REQUIREMENTS

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- (1) Annually, within 60 days after the end of each calendar year during which the Title V permit was effective, or more frequently if specified by Rule 62-213.440(2), F.A.C., or by any other applicable requirement; and
- (2) Within 60 days after submittal of a written agreement for transfer of responsibility as required pursuant to 40 CFR 70.7(d)(1)(iv), adopted and incorporated by reference at Rule 62-204.800, F.A.C., or within 60 days after permanent shutdown of a facility permitted under Chapter 62-213, F.A.C.; provided that, in either such case, the reporting period shall be the portion of the calendar year the permit was effective up to the date of transfer of responsibility or permanent facility shutdown, as applicable.
- b. In lieu of individually identifying all applicable requirements and specifying times of compliance with, noncompliance with, and deviation from each, the responsible official may use DEP Form No. 62-213.900(2) as such statement of compliance so long as the responsible official identifies all reportable deviations from and all instances of non-compliance with any applicable requirements and includes all information required by the federal regulation relating to each reportable deviation and instance of non-compliance.
- c. The responsible official may treat compliance with all other applicable requirements as a surrogate for compliance with Rule 62-296.320(2), Objectionable Odor Prohibited.

[Rules 62-213.440(3)(a)2. & 3. and (b), F.A.C.]

#### RR8. <u>Notification of Administrative Permit Corrections</u>.

A facility owner shall notify the Department by letter of minor corrections to information contained in a permit. Such notifications shall include:

- a. Typographical errors noted in the permit;
- b. Name, address or phone number change from that in the permit;
- c. A change requiring more frequent monitoring or reporting by the permittee;
- d. A change in ownership or operational control of a facility, subject to the following provisions:
  - (1) The Department determines that no other change in the permit is necessary;
    - (2) The permittee and proposed new permittee have submitted an Application for Transfer of Air Permit, and the Department has approved the transfer pursuant to Rule 62-210.300(7), F.A.C.; and
  - (3) The new permittee has notified the Department of the effective date of sale or legal transfer.
- e. Changes listed at 40 CFR 72.83(a)(1), (2), (6), (9) and (10), adopted and incorporated by reference at Rule 62-204.800, F.A.C., and changes made pursuant to Rules 62-214.340(1) and (2), F.A.C., to Title V sources subject to emissions limitations or reductions pursuant to 42 USC ss. 7651-76510;
- f. Changes listed at 40 CFR 72.83(a)(11) and (12), adopted and incorporated by reference at Rule 62-204.800, F.A.C., to Title V sources subject to emissions limitations or reductions pursuant to 42 USC ss. 7651-76510, provided the notification is accompanied by a copy of any EPA determination concerning the similarity of the change to those listed at Rule 62-210.360(1)(e), F.A.C.; and
- g. Any other similar minor administrative change at the source.

[Rule 62-210.360, F.A.C.]

- **RR9.** <u>Notification of Startup</u>. The owners or operator of any emissions unit or facility which has a valid air operation permit which has been shut down more than one year, shall notify the Department in writing of the intent to start up such emissions unit or facility, a minimum of 60 days prior to the intended startup date.
  - a. The notification shall include information as to the startup date, anticipated emission rates or pollutants released, changes to processes or control devices which will result in changes to emission rates, and any other conditions which may differ from the valid outstanding operation permit.
  - b. If, due to an emergency, a startup date is not known 60 days prior thereto, the owner shall notify the Department as soon as possible after the date of such startup is ascertained.

[Rule 62-210.300(5), F.A.C.]

**RR10.** <u>Report Submission</u>. Except as provided in Rule 62-297.310(10), F.A.C., the permittee shall submit all compliance related notifications and reports required of this permit to the Compliance Authority. {See front of permit for address and phone number.} [Rules 62-4.130, 62-4.160 and 62-213.440, F.A.C.]

#### FACILITY-WIDE REPORTING REQUIREMENTS (Version Dated 8/8/2019)

- **RR11.** <u>EPA Report Submission</u>. Any reports, data, notifications, certifications, and requests required to be sent to the United States Environmental Protection Agency, Region 4, should be sent to: Air, Pesticides & Toxics Management Division, United States Environmental Protection Agency, Region 4, Sam Nunn Atlanta Federal Center, 61 Forsyth Street SW, Atlanta, GA 30303-8960. Phone: 404/562-9077.
- RR12. <u>Acid Rain Report Submission</u>. Acid Rain Program Information shall be submitted, as necessary, to: Department of Environmental Protection, 2600 Blair Stone Road, Mail Station #5505, Tallahassee, Florida 32399-2400. Phone: 850/717-9000 Email: <u>DARM Permitting@dep.state.fl.us</u>.
- **RR13.** <u>Report Certification</u>. All reports shall be accompanied by a certification by a responsible official, pursuant to Rule 62-213.420(4), F.A.C. [Rule 62-213.440(1)(b)3.c, F.A.C.]
- **RR14.** <u>Certification by Responsible Official (RO)</u>. In addition to the professional engineering certification required for applications by Rule 62-4.050(3), F.A.C., any application form, report, compliance statement, compliance plan and compliance schedule submitted pursuant to Chapter 62-213, F.A.C., shall contain a certification signed by a responsible official that, based on information and belief formed after reasonable inquiry, the statements and information in the document are true, accurate, and complete. Any responsible official who fails to submit any required information or who has submitted incorrect information shall, upon becoming aware of such failure or incorrect submittal, promptly submit such supplementary information or correct information. [Rule 62-213.420(4), F.A.C.]
- **RR15.** <u>Confidential Information</u>. Whenever an applicant submits information under a claim of confidentiality pursuant to Section 403.111, F.S., the applicant shall also submit a copy of all such information and claim directly to EPA. Any permittee may claim confidentiality of any data or other information by complying with this procedure. [Rules 62-213.420(2), and 62-213.440(1)(d)6., F.A.C.]
- RR16. Forms and Instructions. The forms used by the Department in the Title V source operation program are adopted and incorporated by reference in Rule 62-213.900, F.A.C. The forms are listed by rule number, which is also the form number, and with the subject, title, and effective date. Copies of forms may be obtained by writing to the Department of Environmental Protection, Division of Air Resource Management, 2600 Blair Stone Road, Tallahassee, Florida 32399-2400, by contacting the appropriate permitting authority or by accessing the Department's web site at: <a href="http://www.dep.state.fl.us/air/rules/forms.htm">http://www.dep.state.fl.us/air/rules/forms.htm</a>.
  - a. Annual Operating Report for Air Pollutant Emitting Facility [Including Title V Source Emissions Fee Calculation] (DEP Form No. 62-210.900(5)) (Effective 12/31/2013)
  - b. Statement of Compliance Form (Effective 06/02/2002).
  - c. Responsible Official Notification Form (Effective 06/02/2002).

[Rule 62-213.900, F.A.C.: Forms (1), (7) and (8)]

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## FACILITY-WIDE TESTING REQUIREMENTS

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Unless otherwise specified in a specific rule, this permit, or other order, the following testing requirements apply to each emissions unit for which testing is required. An emissions test is an emissions rate test, a concentration test, or an opacity test.

- TR1. <u>Required Number of Test Runs</u>. For emission rate or concentration limitations, an emissions test shall consist of three valid test runs to determine the total air pollutant emission rate or concentration through the test section of the stack or duct. A valid test run is a test run that meets all requirements of the applicable test method. An emissions test shall also consist of three distinct determinations of any applicable process parameters corresponding to the three distinct test run time periods during which the emission rate or concentration was measured when such data are needed in conjunction with emissions data to compare the emissions test results with the applicable emission limiting standards. Such data shall be obtained pursuant to condition TR5. [subsection 62-297.310(6), F.A.C.]. The three required test runs shall be completed within one consecutive five-day period. In the event that a sample is lost or one of the three runs must be discontinued because of circumstances beyond the control of the owner or operator, and a valid third run cannot be obtained within the five day period allowed for the test, results of the two valid runs shall be accepted, provided that the arithmetic mean of the results of the two valid runs is at least 20% below the allowable emission limiting standard. [Rule 62-297.310(2), F.A.C.]
- **TR2.** <u>Operating Conditions during Emissions Testing</u>. Testing of emissions shall be conducted with the emissions unit operating at the testing capacity as defined below. If it is impracticable to test at the testing capacity, an emissions unit may be tested at less than the testing capacity. If an emissions unit is tested at less than the testing capacity, another emissions test shall be conducted and completed no later than 60 days after the emissions unit operation exceeds 110% of the capacity at which its most recent emissions test was conducted.
  - a. Combustion Turbines. (Reserved)
  - b. All Other Sources. Testing capacity is defined as at least 90 percent of the maximum operation rate specified by the permit.

[Rule 62-297.310(3), F.A.C.]

- **TR3.** <u>Calculation of Emission Rate or Concentration</u>. The emission rate or concentration used for comparison with the relevant standard shall be the arithmetic average of the emission rate or concentration determined by each of the three valid test runs unless otherwise specified in an applicable rule or test method. Data collected during periods of soot blowing shall not be excluded from any calculation of emission rate or concentration. [Rule 62-297.310(4), F.A.C.]
- **TR4.** <u>Required Sampling Times and Observation Periods</u>. Unless otherwise specified in an applicable test method, rule, permit, or other order, the owner or operator shall conduct emissions tests in accordance with the following procedures:
  - a. *Emission Rate or Concentration Tests.* The required sampling time for each test run shall be no less than one hour and no greater than four hours, and the sampling time at each sampling point shall be of equal intervals of at least two minutes, except that for operations that are typically completed within less than the minimum required sampling time, the duration of each test run shall include each occurrence of the operation during the minimum required sampling time. The test period shall include the period of typical operation during which the highest representative emissions are expected to occur.
  - b. *Opacity Tests.* When EPA Method 9 is specified as the applicable opacity test method, the required minimum period of observation for a visible emissions test shall be 60 minutes for emissions units that are subject to a multiple-valued opacity standard, and 30 minutes for all other emissions units, except that for batch, cyclical processes, or other operations that are typically completed within less than the minimum observation period, the period of observation shall include each occurrence of the operation during the minimum observation period. The opacity test observation period shall include the period during which the highest opacity emissions can reasonably be expected to occur.

[Rule 62-297.310(5), F.A.C.]

- TR5. <u>Determination of Process Parameters</u>.
  - a. *Required Process Equipment*. The owner or operator of an emissions unit for which emissions tests are required shall install, operate, and maintain equipment or instruments necessary to determine process parameters, when such

#### FACILITY-WIDE TESTING REQUIREMENTS

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data are needed in conjunction with emissions data to compare emissions test results with applicable emission limiting standards.

b. Accuracy of Process Measurement Equipment. Equipment or instruments used to directly or indirectly determine process parameters shall be calibrated and adjusted so as to determine the value of the process parameter to within 10 percent of its true value.

[Rule 62-297.310(6), F.A.C.]

- TR6. <u>Required Emissions Testing Facilities</u>.
  - a. The owner or operator of an emissions unit, for which an emissions test other than a visible emissions test is required, shall provide emissions testing facilities that meet the requirements of 40 CFR 60.8(e), adopted and incorporated in Rule 62-204.800, F.A.C.
  - b. *Permanent Emissions Testing Facilities.* The owner or operator of an emissions unit, for which an emissions test other than a visible emissions test is required on at least an annual basis, shall install and maintain permanent emissions testing facilities.
  - c. *Temporary Emissions Testing Facilities*. The owner or operator of an emissions unit that is not required to conduct an emissions test on at least an annual basis may use permanent or temporary emissions testing facilities. If the owner or operator chooses to use temporary emissions testing facilities on an emissions unit, and the Department elects to test the unit, such temporary facilities shall be installed on the emissions unit within 5 days of a request by the Department and remain on the emissions unit until the test is completed.

[Rule 62-297.310(7), F.A.C.]

- **TR7.** <u>Frequency of Emissions Tests</u>. The following provisions apply only to those emissions units that are subject to an emissions-limiting standard for which emissions testing is required.
  - a. Annual Emissions Tests Required.
    - (1) Where used in Rules 62-210.310, 62-297.310, or Chapter 62-296, F.A.C., to refer to frequency of required emissions tests, the terms "annual", "annually", and "annually thereafter" shall mean no less frequently than once every calendar year (January 1 December 31).
    - (2) Unless exempted by paragraph a.(5), below [subparagraph 62-297.310(8)(a)5., F.A.C.], the owner or operator shall have an emissions unit tested annually for each of the following pollutants that has an emissions-limiting standard for which emissions testing is required:
      - (a) Each hazardous air pollutant regulated by 40 CFR Part 61, adopted and incorporated by reference at Rule 62-204.800, F.A.C.; and
      - (b) Any other regulated air pollutant, as defined at Rule 62-210.200, F.A.C., or a pollutant designated as a surrogate to a regulated air pollutant by an applicable rule or order, if allowable emissions equal or exceed 100 tons per year.
    - (3) Unless exempted by paragraph a.(5), below [subparagraph 62-297.310(8)(a)5., F.A.C.], the owner or operator shall have an emissions unit tested annually for visible emissions, if there is an applicable standard other than the general opacity standard of subparagraph 62-296.320(4)(b)1., F.A.C.
    - (4) Unless exempted by paragraph a.(5), below [subparagraph 62-297.310(8)(a)5., F.A.C.], the owner or operator shall have an emissions unit tested annually if a rule, permit or other order issued after March 9, 2015, requires an initial emissions test but is silent as to the frequency of additional testing. A rule, permit, or other order that states that no further testing is required after an initial test, or which expressly lists or describes the tests that shall be conducted annually, is not considered silent as to the frequency of additional testing. Annual testing is not required where a permit or other order issued prior to March 9, 2015, is silent as to the frequency of additional testing.
    - (5) Exemptions from paragraphs a.(2), (3) and (4), above [subparagraphs 62-297.310(8)(a)2., 3., and 4., F.A.C.].

#### FACILITY-WIDE TESTING REQUIREMENTS

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- (a) An annual emissions test shall not be required for any pollutant for which a rule, permit, or other order requires emissions testing at some other specific frequency. If multiple applicable rules, permits, or other orders, other than paragraphs a.(2), (3) and (4), above [subparagraphs 62-297.310(8)(a)2., 3., and 4., F.A.C.], require different testing frequencies, testing must comply with the frequency requirements of each such rule, permit, or order.
- (b) An annual emissions test shall not be required for any pollutant for which a rule, permit, or other order requires that the pollutant emissions be measured by a continuous emission monitoring system and, either that system meets the performance specifications and quality assurance and quality control measures of 40 CFR part 60, adopted and incorporated in Rule 62-204.800, F.A.C., or that system meets the performance specifications and quality control measures of 40 CFR part 75, adopted and incorporated in Rule 62-204.800, F.A.C.
- (c) An annual emissions test shall not be required for visible emissions for which a rule, permit, or other order requires that emissions be measured by a continuous opacity monitoring system, and that system meets the performance specifications and quality assurance and quality control measures of 40 CFR part 60, adopted and incorporated in Rule 62-204.800, F.A.C., and the manufacturer's recommended quality assurance and quality control measures.
- (d) An annual emissions test shall not be required for any emissions unit that operated for 400 hours or less (including during startup and shutdown) during the calendar year. If an emission unit operates for more than 400 hours during the calendar year, an emissions test shall be completed no later than 60 days after the emissions unit's annual operation exceeds 400 hours, or by the end of the calendar year, whichever is later.
- (e) An annual emissions test shall not be required for any emissions unit with emissions generated solely from the combustion of fuel, provided that the emissions unit does not burn any liquid fuel or solid fuel or fuel blend for more than 400 hours combined, other than during startup, during the calendar year. If an emissions unit's liquid fuel or solid fuel or fuel blend burning exceeds 400 hours combined during the calendar year, other than during startup, an emissions test shall be completed no later than 60 days after the emissions unit's liquid fuel or solid fuel or fuel blend burning exceeds 400 hours combined, or by the end of the calendar year, whichever is later.
- (f) An annual emissions test shall not be required for each fuel-specific emissions limit, provided the fuel or fuel blend subject to a fuel-specific limit was not burned for more than 400 hours, other than during startup, during the calendar year. If an emissions unit burns a fuel or fuel blend subject to a fuel-specific emission limit for more than 400 hours, other than during startup, during the calendar year, an emissions test for that fuel or fuel blend shall be completed no later than 60 days after the unit's burning of that fuel or fuel blend exceeds 400 hours, or by the end of the calendar year, whichever is later.
- (g) An emissions unit shall not be required to start up for the sole purpose of conducting an emissions test to meet the frequency requirements of this condition **TR7.** [subsection 62-297.310(8), F.A.C.]. In such a case, an emissions test shall be completed no later than 60 days after the emissions unit next starts up.
- (h) An emissions unit permitted to burn multiple fuels or fuel blends shall not be required to switch fuels for the sole purpose of conducting an annual emissions test to meet the frequency requirements of this condition TR7. [subsection 62-297.310(8), F.A.C.]. In such a case, an emissions test shall be completed no later than 60 days after a switch is made to burn the fuel or fuel blend for which testing is required.
- (i) An annual emissions test for visible emissions shall not be required for emissions units exempted from air permitting pursuant to paragraphs 62-210.300(3)(a) or (b), F.A.C.; emissions units determined to be insignificant pursuant to paragraph 62-213.430(6)(b), F.A.C.; or, emissions units authorized pursuant to the general permit provisions in subsection 62-210.300(4), F.A.C., unless the general permit specifically requires such testing.

### b. Emissions Tests Prior to Obtaining an Air Operation Permit.

(1) Unless exempted by paragraph b.(3), below [subparagraph 62-297.310(8)(b)3., F.A.C.], prior to obtaining an initial or renewal air operation permit for any emissions unit that is subject to any emission-limiting standard, the owner or operator shall have an emissions test conducted for each such standard to assist in providing reasonable assurance, per Rule 62-4.070, F.A.C., that the emission-limiting standard can be met and shall submit the test report as specified in subsection 62-297.310(10), F.A.C. For an emissions unit at a Title V source, such prior emissions testing is not required provided that an emissions testing compliance plan is included in the Title V permit.
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- (2) For the purpose of renewal of an air operation permit, the owner or operator may satisfy the requirements of paragraph b.(1), above [subparagraph 62-297.310(8)(b)1., F.A.C.], for any emissions unit by submitting the most recent emissions test, as specified in condition **TR9.** [subsection 62-297.310(10), F.A.C.], provided such test occurred within the term of the current operation permit.
- (3) Exemptions from paragraph b.(1), above [subparagraph 62-297.310(8)(b)1., F.A.C.].
  - (a) An emissions test shall not be required for any pollutant for which a rule, permit, or other order requires that the emissions be measured by a continuous emission monitoring system and, either that system meets the performance specifications and quality assurance and quality control measures of 40 CFR part 60, adopted and incorporated in Rule 62-204.800, F.A.C., or that system meets the performance specifications and quality control measures of 40 CFR part 75, adopted and incorporated in Rule 62-204.800, F.A.C.
  - (b) An emissions test shall not be required for visible emissions for which a rule, permit, or other order requires that emissions be measured by a continuous opacity monitoring system, and that system meets the performance specifications and quality assurance and quality control measures of 40 CFR part 60, adopted and incorporated in Rule 62-204.800, F.A.C., and the manufacturer's recommended quality assurance and quality control measures.
  - (c) For the purpose of renewal of an air operation permit, an emissions test shall not be required for any emissions unit that, in the previous five-year period of permitted operation, operated for 400 hours or less (including during startup and shutdown) during each calendar year included in the five-year period of permitted operation. The first time an emissions unit subsequently exceeds 400 hours of operation during a calendar year, emissions must be tested no later than 60 days after 400 hours of operation is exceeded in that calendar year, or by the end of that calendar year, whichever is later.
  - (d) For the purpose of renewal of an air operation permit, an emissions test shall not be required for any emissions unit with emissions generated solely from the combustion of fuel provided that, in the previous five-year period of permitted operation, the emissions unit did not burn any liquid fuel or solid fuel or fuel blend for more than 400 hours combined, other than during startup, during each calendar year included in the five-year period of permitted operation. The first time an emissions unit subsequently burns any liquid fuel or solid fuel or fuel blend for more than 400 hours combined during a calendar year, emissions must be tested no later than 60 days after the emissions unit's combined burning of any liquid fuel or solid fuel or fuel blend exceeds 400 hours in that calendar year, or by the end of that calendar year, whichever is later.
  - (e) An emissions test shall not be required for each fuel-specific emissions limit prior to the renewal of an air operation permit for an emissions unit provided that, in the previous five-year period of permitted operation, the fuel or fuel blend subject to a fuel-specific limit was not burned for more than 400 hours, other than during startup, during each calendar year included in the five-year period of permitted operation. The first time an emissions unit subsequently burns a fuel or fuel blend subject to a fuel-specific emission limit for more than 400 hours, other than during startup, during any calendar year, an emissions test for that fuel or fuel blend must be completed no later than 60 days after the emissions unit's burning of that fuel or fuel blend exceeds 400 hours in that calendar year, or by the end of that calendar year, whichever is later.
  - (f) An emissions unit shall not be required to start up for the sole purpose of conducting an emissions test to meet the frequency requirements of this condition **TR7.** [subsection 62-297.310(8), F.A.C.]. In such a case, an emissions test shall be completed no later than 60 days after the emissions unit starts up.
  - (g) An emissions unit permitted to burn multiple fuels or fuel blends shall not be required to switch fuels for the sole purpose of conducting the emissions test to meet the frequency requirements of this condition TR7. [subsection 62-297.310(8), F.A.C.]. In such a case, an emissions test shall be completed no later than 60 days after a switch is made to burn the fuel or fuel blend for which testing is required.
  - (h) An emissions test for visible emissions shall not be required for emissions units exempted from air permitting pursuant to paragraphs 62-210.300(3)(a) or (b), F.A.C.; emissions units determined to be insignificant pursuant to paragraph 62-213.430(6)(b), F.A.C.; or emissions units authorized pursuant to the general permit provisions in subsection 62-210.300(4), F.A.C., unless the general permit specifically requires such testing.
- c. *Special Compliance Tests.* When the Department, after investigation, has good reason (such as complaints, increased visible emissions or questionable maintenance of control equipment) to believe that any applicable emission standard contained in a Department rule or in a permit issued pursuant to those rules is being violated, it shall require the owner or operator of the emissions unit to conduct compliance tests which identify the nature and

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quantity of pollutant emissions from the emissions unit, unless the Department obtains other information sufficient to demonstrate compliance. The owner or operator of the emissions unit shall provide a report on the results of said tests to the Department in accordance with the provisions of condition **TR9**. [subsection 62-297.310(10), F.A.C.].

#### [Rule 62-297.310(8), F.A.C.]

**TR8.** <u>Scheduling and Notification</u>. At least 15 days prior to the date on which each required emissions test is to begin, the owner or operator shall notify the air compliance program identified by permit, unless shorter notice is agreed to by the appropriate air compliance program. The notification shall include the date, time, place of each such test, Facility ID Number, Emission Unit ID Number(s) and description(s), Emission Point Number(s) and description(s), test method(s), pollutant(s) to be tested, along with the name and telephone number of the person who will be responsible for conducting such test(s) for the owner or operator. If a scheduled emissions test needs to be re-scheduled, the owner or operator shall submit to the appropriate air compliance program a revised notification at least seven days prior to the re-scheduled emissions test date or arrange a re-scheduled test date with the appropriate air compliance program by mutual agreement. [Rule 62-297.310(9), F.A.C.]

{Permitting Note: Air compliance test notifications can now be completed online in the Department's Business Portal. To access this online process, go to <u>http://www.fldepportal.com/go/home</u> and sign in (or register if you're a new user) from the link in the upper right corner of the page. On the Welcome page select the Submit option, then select Registration/Notification, and then click on Air Compliance Test Notifications. Once in the process, just carefully read the instructions on each screen (and under the Help tabs) to complete the notification.}

#### TR9. <u>Test Reports</u>.

- a. The owner or owner's authorized agent of an emissions unit for which an emissions test is required shall submit a written test report to the compliance authority specified by permit, on the results of each such test as soon as practicable but no later than 45 days after the last run of each test is completed. Test reports may be submitted electronically.
- b. If the owner or owner's authorized agent of an emissions unit for which an emissions test is required submits the results of each such test electronically using the EPA Electronic Reporting Tool (ERT) (<u>http://www.epa.gov/ttnchiel/ert/</u>), the written report specified in paragraph a., above [paragraph 62-297.310(10)(a), F.A.C.], need not be submitted, provided the conditions of paragraphs (1) (3), below [subparagraphs 62-297.310(10)(b)1. through 3., F.A.C.], are met:
  - (1) The owner or owner's authorized agent shall submit the test information using the ERT as soon as practicable but no later than 45 days after the last run of each test is completed;
  - (2) The test information shall provide, as a minimum, the information specified in paragraphs c.(1) (24), below [subparagraphs 62-297.310(10)(c)1. through 24., F.A.C.]; and
  - (3) The compliance authority specified by permit must receive written notification, no later than 45 days after the last run of each test is completed, of the date that the test data was submitted using the ERT.
- c. The test report shall provide sufficient detail on the emissions unit tested and the test procedures used to allow the Department to determine if the test was properly conducted and the test results properly computed. As a minimum, the test report, other than for an EPA Method 9 test, shall provide the following information:
  - (1) The type, location, and identification number of the emissions unit tested.
  - (2) The facility at which the emissions unit is located.
  - (3) The owner and, if other than the owner, operator of the emissions unit.
  - (4) The type and amount of fuels and materials typically used and processed, and the actual types and amounts of fuels used and material processed during each test run.
  - (5) If necessary, in order to compare the emissions test results with an applicable emission limiting standard, the means, raw data, and computations used to determine the amount of fuels used and materials processed.
  - (6) The type of air pollution control devices installed on the emissions unit, their general condition, their typical operating parameters, and their actual operating parameters during each test run.
  - (7) A diagram of the sampling location, including the distance to any upstream and downstream bends or other flow disturbances.
  - (8) The date, starting time, and duration of each sampling run.
  - (9) The test procedures, including any authorized alternative procedures, used.

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- (10) The number of points sampled, and the configuration and location of the sampling plane.
- (11) For each sampling point for each run, the dry gas meter reading, velocity head, pressure drop across the stack or duct, temperatures, average meter temperatures, and sample time per point.
- (12) The type, manufacturer, and configuration of the sampling equipment used.
- (13) Data related to the required calibration of the test equipment.
- (14) Data on the identification, processing, and weights of all filters used.
- (15) Data on the types and amounts of any chemical solutions used.
- (16) For each sampling run, data on the amount of pollutant collected from each sampling probe.
- (17) For each sampling run, data on the amount of pollutant collected from the filters.
- (18) For each sampling run, data on the amount of pollutant collected from the impingers.
- (19) The names of individuals who furnished the process variable data, conducted the test, analyzed the samples and prepared the report.
- (20) All measured and calculated data required to be determined by each applicable test procedure for each run.
- (21) The detailed calculations for one run that relate the collected data to the calculated emission rate or concentration, as applicable.
- (22) The applicable emission standard, and the resulting maximum allowable emission rate or concentration for the emissions unit, as applicable, plus the test result in the same form and unit of measure.
- (23) When an emissions test is conducted for the Department or its agent, the person who conducts the test shall provide the certification with respect to the test procedures used. The owner or owner's authorized agent shall certify that all data required and provided to the person conducting the test are true and correct to his or her knowledge.
- (24) For non-Title V sources, a certification by the owner or owner's authorized agent that, to his or her knowledge, all data submitted are true and correct.
- (25) Any report submitted for a Title V source shall contain certification by a responsible official. This certification shall state that, based on information and belief formed after reasonable inquiry, the statements and information in the document are true, accurate, and complete.

[Rule 62-297.310(10), F.A.C.]

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#### **Operation**

- **TV1.** <u>General Prohibition</u>. A permitted installation may only be operated, maintained, constructed, expanded or modified in a manner that is consistent with the terms of the permit. [Rule 62-4.030, Florida Administrative Code (F.A.C.)]
- **TV2.** <u>Validity</u>. This permit is valid only for the specific processes and operations applied for and indicated in the approved drawings or exhibits. Any unauthorized deviation from the approved drawings, exhibits, specifications, or conditions of this permit may constitute grounds for revocation and enforcement action by the Department. [Rule 62-4.160(2), F.A.C.]
- **TV3.** <u>Proper Operation and Maintenance</u>. The permittee shall properly operate and maintain the facility and systems of treatment and control (and related appurtenances) that are installed and used by the permittee to achieve compliance with the conditions of this permit, as required by Department rules. This provision includes the operation of backup or auxiliary facilities or similar systems when necessary to achieve compliance with the conditions of the permit and when required by Department rules. [Rule 62-4.160(6), F.A.C.]
- **TV4.** Not Federally Enforceable. <u>Health, Safety and Welfare</u>. To ensure protection of public health, safety, and welfare, any construction, modification, or operation of an installation which may be a source of pollution, shall be in accordance with sound professional engineering practices pursuant to Chapter 471, F.S. [Rule 62-4.050(3), F.A.C.]
- **TV5.** <u>Continued Operation</u>. An applicant making timely and complete application for permit, or for permit renewal, shall continue to operate the source under the authority and provisions of any existing valid permit or Florida Electrical Power Plant Siting Certification, and in accordance with applicable requirements of the Acid Rain Program, applicable requirements of the CAIR Program, and applicable requirements of the Hg Budget Trading Program, until the conclusion of proceedings associated with its permit application or until the new permit becomes effective, whichever is later, provided the applicant complies with all the provisions of subparagraphs 62-213.420(1)(b)3., F.A.C. [Rules 62-213.420(1)(b)2., F.A.C.]
- **TV6**. <u>Changes Without Permit Revision</u>. Title V sources having a valid permit issued pursuant to Chapter 62-213, F.A.C., may make the following changes without permit revision, provided that sources shall maintain source logs or records to verify periods of operation:
  - a. Permitted sources may change among those alternative methods of operation allowed by the source's permit as provided by the terms of the permit;
  - b. A permitted source may implement operating changes, as defined in Rule 62-210.200, F.A.C., after the source submits any forms required by any applicable requirement and provides the Department and EPA with at least 7 days written notice prior to implementation. The source and the Department shall attach each notice to the relevant permit;
    - (1) The written notice shall include the date on which the change will occur, and a description of the change within the permitted source, the pollutants emitted and any change in emissions, and any term or condition becoming applicable or no longer applicable as a result of the change;
    - (2) The permit shield described in Rule 62-213.460, F.A.C., shall not apply to such changes;
  - c. Permitted sources may implement changes involving modes of operation only in accordance with Rule 62-213.415, F.A.C.

[Rule 62-213.410, F.A.C.]

**TV7.** <u>Circumvention</u>. No person shall circumvent any air pollution control device, or allow the emission of air pollutants without the applicable air pollution control device operating properly. [Rule 62-210.650, F.A.C.]

#### **Compliance**

**TV8.** <u>Compliance with Chapter 403, F.S., and Department Rules</u>. Except as provided at Rule 62-213.460, Permit Shield, F.A.C., the issuance of a permit does not relieve any person from complying with the requirements of Chapter 403, F.S., or Department rules. [Rule 62-4.070(7), F.A.C.]

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- **TV9**. <u>Compliance with Federal, State and Local Rules</u>. Except as provided at Rule 62-213.460, F.A.C., issuance of a permit does not relieve the owner or operator of a facility or an emissions unit from complying with any applicable requirements, any emission limiting standards or other requirements of the air pollution rules of the Department or any other such requirements under federal, state, or local law. [Rule 62-210.300, F.A.C.]</u>
- **TV10.** <u>Binding and enforceable</u>. The terms, conditions, requirements, limitations and restrictions set forth in this permit, are "permit conditions" and are binding and enforceable pursuant to Sections 403.141, 403.727, or 403.859 through 403.861, F.S. The permittee is placed on notice that the Department will review this permit periodically and may initiate enforcement action for any violation of these conditions. [Rule 62-4.160(1), F.A.C.]
- **TV11.** <u>Timely information</u>. When requested by the Department, the permittee shall within a reasonable time furnish any information required by law which is needed to determine compliance with the permit. If the permittee becomes aware the relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly. [Rule 62-4.160(15), F.A.C.]
- **TV12.** <u>Halting or reduction of source activity</u>. It shall not be a defense for a permittee in an enforcement action that maintaining compliance with any permit condition would necessitate halting of or reduction of the source activity. [Rule 62-213.440(1)(d)3., F.A.C.]
- **TV13.** <u>Final permit action</u>. Any Title V source shall comply with all the terms and conditions of the existing permit until the Department has taken final action on any permit renewal or any requested permit revision, except as provided at Rule 62-213.412(2), F.A.C. [Rule 62-213.440(1)(d)4., F.A.C.]
- **TV14.** <u>Sudden and unforeseeable events beyond the control of the source</u>. A situation arising from sudden and unforeseeable events beyond the control of the source which causes an exceedance of a technology-based emissions limitation because of unavoidable increases in emissions attributable to the situation and which requires immediate corrective action to restore normal operation, shall be an affirmative defense to an enforcement action in accordance with the provisions and requirements of 40 CFR 70.6(g)(2) and (3), hereby adopted and incorporated by reference. [Rule 62-213.440(1)(d)5., F.A.C.]</u>
- **TV15.** <u>Permit Shield</u>. Except as provided in Chapter 62-213, F.A.C., compliance with the terms and conditions of a permit issued pursuant to Chapter 62-213, F.A.C., shall, as of the effective date of the permit, be deemed compliance with any applicable requirements in effect, provided that the source included such applicable requirements in the permit <u>application</u>. Nothing in this condition or in any permit shall alter or affect the ability of EPA or the Department to deal with an emergency, the liability of an owner or operator of a source for any violation of applicable requirements prior to or at the time of permit issuance, or the requirements of the Federal Acid Rain Program, the CAIR Program. [Rule 62-213.460, F.A.C.]
- TV16. Compliance With Federal Rules. A facility or emissions unit subject to any standard or requirement of 40 CFR, Part 60, 61, 63 or 65, adopted and incorporated by reference at Rule 62-204.800, F.A.C., shall comply with such standard or requirement. Nothing in this chapter shall relieve a facility or emissions unit from complying with such standard or requirement, provided, however, that where a facility or emissions unit is subject to a standard established in Rule 62-296, F.A.C., such standard shall also apply. [Rule 62-296.100(3), F.A.C.]

#### Permit Procedures

- **TV17.** <u>Permit Revision Procedures</u>. The permittee shall revise its permit as required by Rules 62-213.400, 62-213.412, 62-213.420, 62-213.430 & 62-4.080, F.A.C.; and, in addition, the Department shall revise permits as provided in Rule 62-4.080, F.A.C. & 40 CFR 70.7(f).
- TV18. <u>Permit Renewal</u>. The permittee shall renew its permit as required by Rules 62-4.090, 62.213.420(1) and 62-213.430(3), F.A.C. Permits being renewed are subject to the same requirements that apply to permit issuance at the time of application for renewal. Permit renewal applications shall contain that information identified in Rules 62-210.900(1) [Application for Air Permit Long Form], 62-213.420(3) [Required Information], 62-213.420(6) [CAIR Part Form], F.A.C. Unless a Title V source submits a timely and complete application for permit renewal in accordance with the requirements this rule, the existing permit shall expire and the source's right to operate shall terminate. For purposes of a permit renewal, a timely application is one that is submitted 225 days before the expiration of a permit that expires on or

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after June 1, 2009. No Title V permit will be issued for a new term except through the renewal process. [Rules 62-213.420 & 62-213.430, F.A.C.]

- **TV19.** <u>Insignificant Emissions Units or Pollutant-Emitting Activities</u>. The permittee shall identify and evaluate insignificant emissions units and activities as set forth in Rule 62-213.430(6), F.A.C.
- **TV20.** <u>Savings Clause</u>. If any portion of the final permit is invalidated, the remainder of the permit shall remain in effect. [Rule 62-213.440(1)(d)1., F.A.C.]
- TV21. Suspension and Revocation.
  - a. Permits shall be effective until suspended, revoked, surrendered, or expired and shall be subject to the provisions of Chapter 403, F.S., and rules of the Department.
  - b. Failure to comply with pollution control laws and rules shall be grounds for suspension or revocation.
  - c. A permit issued pursuant to Chapter 62-4, F.A.C., shall not become a vested property right in the permittee. The Department may revoke any permit issued by it if it finds that the permit holder or his agent:
    - (1) Submitted false or inaccurate information in his application or operational reports.
    - (2) Has violated law, Department orders, rules or permit conditions.
    - (3) Has failed to submit operational reports or other information required by Department rules.
    - (4) Has refused lawful inspection under Section 403.091, F.S.
  - d. No revocation shall become effective except after notice is served by personal services, certified mail, or newspaper notice pursuant to Section 120.60(7), F.S., upon the person or persons named therein and a hearing held if requested within the time specified in the notice. The notice shall specify the provision of the law, or rule alleged to be violated, or the permit condition or Department order alleged to be violated, and the facts alleged to constitute a violation thereof.

[Rule 62-4.100, F.A.C.]

- **TV22.** Not federally enforceable. <u>Financial Responsibility</u>. The Department may require an applicant to submit proof of financial responsibility and may require the applicant to post an appropriate bond to guarantee compliance with the law and Department rules. [Rule 62-4.110, F.A.C.]
- TV23. Emissions Unit Reclassification.
  - a. Any emissions unit whose operation permit has been revoked as provided for in Chapter 62-4, F.A.C., shall be deemed permanently shut down for purposes of Rule 62-212.500, F.A.C. Any emissions unit whose permit to operate has expired without timely renewal or transfer may be deemed permanently shut down, provided, however, that no such emissions unit shall be deemed permanently shut down if, within 20 days after receipt of written notice from the Department, the emissions unit owner or operator demonstrates that the permit expiration resulted from inadvertent failure to comply with the requirements of Rule 62-4.090, F.A.C., and that the owner or operator intends to continue the emissions unit in operation, and either submits an application for an air operation permit or complies with permit transfer requirements, if applicable.
  - b. If the owner or operator of an emissions unit which is so permanently shut down, applies to the Department for a permit to reactivate or operate such emissions unit, the emissions unit will be reviewed and permitted as a new emissions unit.

[Rule 62-210.300(6), F.A.C.]

**TV24.** <u>Transfer of Permits</u>. Per Rule 62-4.160(11), F.A.C., this permit is transferable only upon Department approval in accordance with Rule 62-4.120, F.A.C., as applicable. The permittee shall be liable for any non-compliance of the permitted activity until the transfer is approved by the Department. The permittee transferring the permit shall remain liable for corrective actions that may be required as a result of any violations occurring prior to the sale or legal transfer of the facility. The permittee shall also comply with the requirements of Rule 62-210.300(7), F.A.C., and use DEP Form No. 62-210.900(7). [Rules 62-4.160(11), 62-4.120, and 62-210.300(7), F.A.C.]

#### **Rights, Title, Liability, and Agreements**

**TV25.** <u>Rights</u>. As provided in Subsections 403.087(6) and 403.722(5), F.S., the issuance of this permit does not convey any vested rights or any exclusive privileges. Neither does it authorize any injury to public or private property or any

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invasion of personal rights, nor any infringement of federal, state, or local laws or regulations. This permit is not a waiver of or approval of any other Department permit that may be required for other aspects of the total project which are not addressed in this permit. [Rule 62-4.160(3), F.A.C.]

- **TV26**. <u>Title</u>. This permit conveys no title to land or water, does not constitute State recognition or acknowledgment of title, and does not constitute authority for the use of submerged lands unless herein provided and the necessary title or leasehold interests have been obtained from the State. Only the Trustees of the Internal Improvement Trust Fund may express State opinion as to title. [Rule 62-4.160(4), (F.A.C.]
- **TV27.** <u>Liability</u>. This permit does not relieve the permittee from liability for harm or injury to human health or welfare, animal, or plant life, or property caused by the construction or operation of this permitted source, or from penalties therefore; nor does it allow the permittee to cause pollution in contravention of F.S. and Department rules, unless specifically authorized by an order from the Department. [Rule 62-4.160(5), F.A.C.]

#### TV28. Agreements.

- a. The permittee, by accepting this permit, specifically agrees to allow authorized Department personnel, upon presentation of credentials or other documents as may be required by law and at reasonable times, access to the premises where the permitted activity is located or conducted to:
  - (1) Have access to and copy any records that must be kept under conditions of the permit;
  - (2) Inspect the facility, equipment, practices, or operations regulated or required under this permit; and,
  - (3) Sample or monitor any substances or parameters at any location reasonably necessary to assure compliance with this permit or Department rules. Reasonable time may depend on the nature of the concern being investigated.
- b. In accepting this permit, the permittee understands and agrees that all records, notes, monitoring data and other information relating to the construction or operation of this permitted source which are submitted to the Department may be used by the Department as evidence in any enforcement case involving the permitted source arising under the Florida Statutes or Department rules, except where such use is prescribed by Sections 403.111 and 403.73, F.S. Such evidence shall only be used to the extent it is consistent with the Florida Rules of Civil Procedure and appropriate evidentiary rules.
- c. The permittee agrees to comply with changes in Department rules and Florida Statutes after a reasonable time for compliance; provided, however, the permittee does not waive any other rights granted by Florida Statutes or Department rules.

[Rules 62-4.160(7), (9), and (10), F.A.C.]

#### **Recordkeeping and Emissions Computation**

- **TV29.** <u>Permit</u>. The permittee shall keep this permit or a copy thereof at the work site of the permitted activity. [Rule 62-4.160(12), F.A.C.]
- TV30. <u>Recordkeeping</u>.
  - a. Upon request, the permittee shall furnish all records and plans required under Department rules. During enforcement actions, the retention period for all records will be extended automatically unless otherwise stipulated by the Department.
  - b. The permittee shall hold at the facility or other location designated by this permit records of all monitoring information (including all calibration and maintenance records and all original strip chart recordings for continuous monitoring instrumentation) required by the permit, copies of all reports required by this permit, and records of all data used to complete the application for this permit. These materials shall be retained at least five (5) years from the date of the sample, measurement, report, or application unless otherwise specified by Department rule.
  - c. Records of monitoring information shall include:
    - (1) The date, exact place, and time of sampling or measurements, and the operating conditions at the time of sampling or measurement;
    - (2) The person responsible for performing the sampling or measurements;
    - (3) The dates analyses were performed;
    - (4) The person and company that performed the analyses;
    - (5) The analytical techniques or methods used;

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(6) The results of such analyses.

[Rules 62-4.160(14) and 62-213.440(1)(b)2., F.A.C.]

**TV31.** Emissions Computation. Pursuant to Rule 62-210.370, F.A.C., the following required methodologies are to be used by the owner or operator of a facility for computing actual emissions, baseline actual emissions, and net emissions increase, as defined at Rule 62-210.200, F.A.C., and for computing emissions for purposes of the reporting requirements of subsection 62-210.370(3) and paragraph 62-212.300(1)(e), F.A.C., or of any permit condition that requires emissions be computed in accordance with Rule 62-210.370, F.A.C. Rule 62-210.370, F.A.C., is not intended to establish methodologies for determining compliance with the emission limitations of any air permit.

For any of the purposes specified above, the owner or operator of a facility shall compute emissions in accordance with the requirements set forth in this subsection.

- a. *Basic Approach*. The owner or operator shall employ, on a pollutant-specific basis, the most accurate of the approaches set forth below to compute the emissions of a pollutant from an emissions unit; provided, however, that nothing in this rule shall be construed to require installation and operation of any continuous emissions monitoring system (CEMS), continuous parameter monitoring system (CPMS), or predictive emissions monitoring system (PEMS) not otherwise required by rule or permit, nor shall anything in this rule be construed to require performance of any stack testing not otherwise required by rule or permit.
  - (1) If the emissions unit is equipped with a CEMS meeting the requirements of paragraph 62-210.370(2)(b), F.A.C., the owner or operator shall use such CEMS to compute the emissions of the pollutant, unless the owner or operator demonstrates to the department that an alternative approach is more accurate because the CEMS represents still-emerging technology.
  - (2) If a CEMS is not available or does not meet the requirements of paragraph 62-210.370(2)(b), F.A.C, but emissions of the pollutant can be computed pursuant to the mass balance methodology of paragraph 62-210.370(2)(c), F.A.C., the owner or operator shall use such methodology, unless the owner or operator demonstrates to the department that an alternative approach is more accurate.
  - (3) If a CEMS is not available or does not meet the requirements of paragraph 62-210.370(2)(b), F.A.C., and emissions cannot be computed pursuant to the mass balance methodology, the owner or operator shall use an emission factor meeting the requirements of paragraph 62-210.370(2)(d), F.A.C., unless the owner or operator demonstrates to the department that an alternative approach is more accurate.
- b. Continuous Emissions Monitoring System (CEMS).
  - (1) An owner or operator may use a CEMS to compute emissions of a pollutant for purposes of this rule provided:
    - (a) The CEMS complies with the applicable certification and quality assurance requirements of 40 CFR Part 60, Appendices B and F, or, for an acid rain unit, the certification and quality assurance requirements of 40 CFR Part 75, all adopted by reference at Rule 62-204.800, F.A.C.; or,
    - (b) The owner or operator demonstrates that the CEMS otherwise represents the most accurate means of computing emissions for purposes of this rule.
  - (2) Stack gas volumetric flow rates used with the CEMS to compute emissions shall be obtained by the most accurate of the following methods as demonstrated by the owner or operator:
    - (a) A calibrated flowmeter that records data on a continuous basis, if available; or
    - (b) The average flow rate of all valid stack tests conducted during a five-year period encompassing the period over which the emissions are being computed, provided all stack tests used shall represent the same operational and physical configuration of the unit.
  - (3) The owner or operator may use CEMS data in combination with an appropriate f-factor, heat input data, and any other necessary parameters to compute emissions if such method is demonstrated by the owner or operator to be more accurate than using a stack gas volumetric flow rate as set forth at subparagraph 62-210.370(2)(b)2., F.A.C., above.
- c. Mass Balance Calculations.
  - (1) An owner or operator may use mass balance calculations to compute emissions of a pollutant for purposes of this rule provided the owner or operator:
    - (a) Demonstrates a means of validating the content of the pollutant that is contained in or created by all materials or fuels used in or at the emissions unit; and,
    - (b) Assumes that the emissions unit emits all of the pollutant that is contained in or created by any material or fuel used in or at the emissions unit if it cannot otherwise be accounted for in the process or in the capture and destruction of the pollutant by the unit's air pollution control equipment.

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#### TITLE V GENERAL CONDITIONS

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- (2) Where the vendor of a raw material or fuel which is used in or at the emissions unit publishes a range of pollutant content from such material or fuel, the owner or operator shall use the highest value of the range to compute the emissions, unless the owner or operator demonstrates using site-specific data that another content within the range is more accurate.
- (3) In the case of an emissions unit using coatings or solvents, the owner or operator shall document, through purchase receipts, records and sales receipts, the beginning and ending VOC inventories, the amount of VOC purchased during the computational period, and the amount of VOC disposed of in the liquid phase during such period.
- d. Emission Factors.
  - (1) An owner or operator may use an emission factor to compute emissions of a pollutant for purposes of this rule provided the emission factor is based on site-specific data such as stack test data, where available, unless the owner or operator demonstrates to the department that an alternative emission factor is more accurate. An owner or operator using site-specific data to derive an emission factor, or set of factors, shall meet the following requirements.
    - (a) If stack test data are used, the emission factor shall be based on the average emissions per unit of input, output, or gas volume, whichever is appropriate, of all valid stack tests conducted during at least a five-year period encompassing the period over which the emissions are being computed, provided all stack tests used shall represent the same operational and physical configuration of the unit.
    - (b) Multiple emission factors shall be used as necessary to account for variations in emission rate associated with variations in the emissions unit's operating rate or operating conditions during the period over which emissions are computed.
    - (c) The owner or operator shall compute emissions by multiplying the appropriate emission factor by the appropriate input, output or gas volume value for the period over which the emissions are computed. The owner or operator shall not compute emissions by converting an emission factor to pounds per hour and then multiplying by hours of operation, unless the owner or operator demonstrates that such computation is the most accurate method available.
  - (2) If site-specific data are not available to derive an emission factor, the owner or operator may use a published emission factor directly applicable to the process for which emissions are computed. If no directly-applicable emission factor is available, the owner or operator may use a factor based on a similar, but different, process.
- e. Accounting for Emissions During Periods of Missing Data from CEMS, PEMS, or CPMS. In computing the emissions of a pollutant, the owner or operator shall account for the emissions during periods of missing data from CEMS, PEMS, or CPMS using other site-specific data to generate a reasonable estimate of such emissions.
- f. Accounting for Emissions During Periods of Startup and Shutdown. In computing the emissions of a pollutant, the owner or operator shall account for the emissions during periods of startup and shutdown of the emissions unit.
- g. *Fugitive Emissions*. In computing the emissions of a pollutant from a facility or emissions unit, the owner or operator shall account for the fugitive emissions of the pollutant, to the extent quantifiable, associated with such facility or emissions unit.
- h. *Recordkeeping*. The owner or operator shall retain a copy of all records used to compute emissions pursuant to this rule for a period of five years from the date on which such emissions information is submitted to the department for any regulatory purpose.

[Rule 62-210.370(1) & (2), F.A.C.]

#### **Responsible Official**

**TV32**. <u>Designation and Update</u>. The permittee shall designate and update a responsible official as required by Rule 62-213.202, F.A.C.

#### **Prohibitions and Restrictions**

**TV33.** <u>Asbestos</u>. This permit does not authorize any demolition or renovation of the facility or its parts or components which involves asbestos removal. This permit does not constitute a waiver of any of the requirements of Chapter 62-257, F.A.C., and 40 CFR 61, Subpart M, National Emission Standard for Asbestos, adopted and incorporated by reference in Rule 62-204.800, F.A.C. Compliance with Chapter 62-257, F.A.C., and 40 CFR 61, Subpart M, Section 61.145, is required for any asbestos demolition or renovation at the source. [40 CFR 61; Rule 62-204.800, F.A.C.; and, Chapter 62-257, F.A.C.]

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- **TV34.** <u>Refrigerant Requirements</u>. Any facility having refrigeration equipment, including air conditioning equipment, which uses a Class I or II substance (listed at 40 CFR 82, Subpart A, Appendices A and B), and any facility which maintains, services, or repairs motor vehicles using a Class I or Class II substance as refrigerant must comply with all requirements of 40 CFR 82, Subparts B and F, and with Chapter 62-281, F.A.C.
- **TV35.** <u>Open Burning Prohibited</u>. Unless otherwise authorized by Rule 62-296.320(3) or Chapter 62-256, F.A.C., open burning is prohibited.

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#### APPENDIX U

#### LIST OF UNREGULATED EMISSIONS UNITS AND/OR ACTIVITIES.

<u>Unregulated Emissions Units and/or Activities</u>. An emissions unit which emits no "emissions-limited pollutant" and which is subject to no unit-specific work practice standard, though it may be subject to regulations applied on a facility-wide basis (e.g., unconfined emissions, odor, general opacity) or to regulations that require only that it be able to prove exemption from unit-specific emissions or work practice standards.

The below listed emissions units and/or activities are neither 'regulated emissions units' nor 'insignificant emissions units'

#### Brief Description of Unregulated Emissions Units and/or Activity

Emission Units/Activities Associated with the Boilers Area

1. Fugitive equipment leaks. [EU062]

Emission Units/Activities Associated with the Methylamines Plants No. 1 and No. 4

- 1. Methylamines Plants No. 1 and No. 4 non-HON, non-NSPS fugitives. [EU062]
- 2. Methylamines Plants No. 1 and No. 4 non-NESHAP Cooling Towers (do not use chromium-based water treatment chemicals) [CT-67102 and CT-67103, CT- 67038 and CT-67039]. [EU063]
- 3. Methylamines Plants No. 1 and No. 4 unregulated process equipment used to produce methylamines not regulated under HON (such as distillation, separation columns, hot water recycle loop, dehydration bottoms coolers E-67073A/B/C, hot water loop trim cooler E-67072).
- Methylamines Plants No. 1 and No. 4 Non-Regulated Storage Tanks [D-67001; D-67101; D-67102; D-67103; D-67105A, B; D-67106A, B; D-67107A, B; D-67110A, B; D-67112A, B; D-67116A, B, C, D, R, S; D-67117; D-67134A, C; D-67137A, B; D-67203A, B, C, D; D-67204A, B, C, D, E; D-67205; D-67207; D-67215; D-67216A, B; D-67600A, B; D-67601; D-67604; D-67611A, B].
- Methylamines Plant No. 1 and No. 4 Non-Product Tanks [D-67102; D-67130; TK-67004; TK-671128; D- 24101B].

Emission Units/Activities Associated with the Higher Amines Plant and Batch Still (Plant No. 2 and No. 3)

- 1. Higher Amines Plant and Batch Still fugitives. [EU062]
- Higher Amines and Batch Still Plants No. 2 and No. 3 non-NESHAP Cooling Tower (does not use chromium- based water treatment chemicals) [CT-32000 (Note: also services the Utilities and Ammonia Recovery areas)].[EU063]
- Higher Amines non-regulated storage tanks vent to flare except for TK-69102 and D-68214 [D-67116F, G, J, K, L, N, P, T; D-68109; D-68201; D-68202, D-68205; D-68206; D-68209; D-68211; D-68213; D-68142; D-69101A, B, C, D; TK-69102]
- Higher Amines and Batch Still Plants No. 2 and No. 3 Non-Product Tanks [D-68101\*; D-68121A, B; D-68122A, B; D-68123; D-24109; D-69102\*; D-68102\*; D-68103\*; D-68111\*; D-68141\*; D-68106A\*, B\*; D-68110A\*, B\*; TK-68100; D-24109]. \*Note: These tanks vent to flare.
- Unregulated Loading Racks for Higher Amines and Batch Still Plants No. 2 and No. 3 vent to flare or vapor balanced [South 10, SouthMiddle, North Middle, East Side, South Alcohol, and North Alcohol Loading Racks].
- 6. Higher Amines Unregulated Process Equipment used to produce higher amines not regulated under MON (such as distillation, separation columns).
- 7. Batch Still Vent. [EU055]
- 8. Low Pressure Absorber (T-68104) Vent to flare
- 9. High Pressure Absorber (T-68106) Vent to flare
- 10. Railcar Cleaning vents to flare

Emissions Units/Activities Associated with the DIMLA Plant

- DIMLA Plant Non-Regulated Storage Tanks and Loading [(TK-62101, TK-62102, TK-62103), (TK-62090, TK-62091, TK-62092), TK-62190, TK-62191, TK-62192, TK-62193, TK-62194), and TK-62168] [EU076]
- 2. DIMLA Unregulated Process Equipment used to produce DIMLA not regulated under MON

#### **APPENDIX U**

#### LIST OF UNREGULATED EMISSIONS UNITS AND/OR ACTIVITIES.

(such as distillation, separation columns, waste water tank TK- 62099).

3. DIMLA non-MON and non-NSPS fugitive leaks. [EU062]

Emission Units/Activities Associated with General Plant Emission Units

- 1. Painting application of coatings for maintenance or aesthetic purposes using spray, brush or roller.
- 2. Wastewater treatment air emissions from chemical sewers, neutralization, equalization, biological oxidation and facultative ponds. [EU075]
- 3. Use of aerosol canned products and aerosol can-punching for disposal.
- 4. Facility-wide Equipment Leak Fugitives. [EU062]

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#### ATTACHMENTS

## (INCLUDED FOR CONVENIENCE)

The following attachments are included for convenient reference:

Figure 1, Summary Report-Gaseous and Opacity Excess Emission and Monitoring System Performance (40 CFR 60, July, 1996).

Table H, Permit History.

Time Sensitive Action Chart.

<u>Table 1 – Summary of Applicable Requirements and Compliance Procedures.</u>

Figure 2 - Project Emissions Increase Report - Example Format.

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#### FIGURE 1 SUMMARY REPORT - GASEOUS AND OPACITY EXCESS EMISSION AND MONITORING SYSTEM PERFORMANCE

[Note: This form is refe	renced in 40 CFR	60.7, Sub	part A-Ge	eneral Provis	sions]	
Pollutant (Circle One):	SO <sub>2</sub>	NO <sub>X</sub>	TRS	$H_2S$	СО	Opacity
Reporting period dates:	From			to		
Company:						
Emission Limitation: _						
Address:						
Monitor Manufacturer:						
Model No.:						
Date of Latest CMS Cer	rtification or Audit	:				
Process Unit(s) Description	tion:					
Total source operating t	ime in reporting po	eriod <sup>1</sup> : _				
Emission data summa	ary <sup>1</sup>	,		CMS per	formance summa	<b>ry</b> <sup>1</sup>
<ul> <li>to:         <ul> <li>a. Startup/shutdown</li> <li>b. Control equipmen</li> <li>c. Process problems</li> <li>d. Other known cause</li> <li>e. Unknown causes .</li> </ul> </li> <li>Total duration of ex</li> <li>Total duration of f</li> <li>source operating time]</li> </ul> <sup>1</sup> For opacity, record For the reporting the total CMS do excess emission reports and the total CMS do excess emis do excess emission reports a	t problems es es es emissions excess emissions d all times in minu period: If the tota owntime is 5 perc eport described in	s x (100) ttes. For g l duration ent or gro 40 CFR 6	/ [Total %2 gases, reco of excess eater of t 0.7(c) sh	<ul> <li>a. Moni</li> <li>b. Non-</li> <li>c. Quali</li> <li>d. Other</li> <li>e. Unkn</li> <li>2. Total C</li> <li>3. [Total</li> <li>time]</li> <li>ord all times</li> <li>s emissions</li> <li>he total ope</li> <li>all be submit</li> </ul>	itor equipment mal Monitor equipmen ity assurance calibi r known causes cown causes CMS Downtime CMS Downtime] : in hours. is 1 percent or gree rating time, both t	functions
<u>Note</u> : On a separate pa	ge, describe any c	hanges si	nce the la	st in CMS, p	process or controls.	
I <u>certify</u> that the informa	ation contained in	this repor	t is true, a	occurate, and	complete.	
Name:						
Signature:					Date:	
Title:						
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# TABLE HPERMIT HISTORY

For convenience purposes only, this table summarizes the history of air construction and Title V air operation permits.

EU No.	Description	Permit No.	Effective Date	<b>Expiration Date</b>	Project Type
Amines	Amines Plant #1 & Flare	1130004-001-AC	09/12/1995	06/15/1996	Construction
Amines	Methanol Loading Scrubber	1130004-002-AC	01/10/1996	12/01/1996	Construction
Amines	Methanol Storage Tanks	1130004-003-AC	03/26/1996	03/26/2001	Construction
Amines	Methanol Crude Storage Tk	1130004-004-AC	05/17/1996	05/17/2001	Construction
All	Facility	1130004-005-AV	12/02/1999	12/02/2004	Initial Issue
Amines	#4 MA Plant and Cogen	1130004-006-AC	10/22/1996	10/22/2001	Construction
Amines	#1 MA Plant Inc Heat Input	1130004-008-AC	02/01/1997	02/01/2002	Construction
Amines	#1 MA Plant Inc Heat Input	1130004-009-AC	02/01/1997	02/01/2002	Construction
Amines	Mod Nitric Acid Plants 1&2	1130004-010-AC	01/23/2004	01/24/2006	Construction
All	Facility	1130004-011-AV	08/25/2005	08/22/2010	Renewal
67	Higher Amines Plant LDAR	1130004-012-AC	08/08/2006	08/08/2011	Construction
Amines	Air Products and Chemicals	1130004-013-AC	N/A	N/A	Construction
All	Air Products to Taminco	1130004-013-AO	10/25/2006	8/22/2010	Transfer
All	Facility	1130004-014-AV	02/01/2008	08/22/2010	Revision
Boiler	Boiler AC (Part of 017-AC)	1130004-015-AC	N/A	N/A	Construction
Amines	Triazine (Part of 017-AC)	1130004-016-AC	N/A	N/A	Construction
Amines/Triazine/BLR	Amines, Triazine, Boiler	1130004-017-AC	07/29/2008	12/17/2010	Construction
All	Facility	1130004-018-AV	07/13/2011	07/13/2016	Renewal
DIMLA	DIMLA Plant (new)	1130004-019-AC	03/07/2011	03/07/2016	Construction
Amines	No. 4 MA Plant Expansion	1130004-020-AC	11/29/2012	11/29/2017	Construction
DIMLA	DIMLA Plant (Incorp)	1130004-021-AV	06/20/2013	07/13/2016	Revision
Amines	Replace TMA Column	1130004-022-AC	04/14/2014	N/A	Exemption
005	Temporary Flare Alteration	1130004-023-AC	05/14/2014	N/A	Exemption
Amines	Extend 020-AC due date	1130004-024-AC	11/17/2014	N/A	Modification
All	No. 4 MA Plant Exp. (Incorp)	1130004-025-AV	05/22/2015	07/13/2016	Revision
001,003,006,007,033,060,079	Boilers and Process Heaters	1130004-026-AC	3/22/2016	3/22/2017	Construction
All	Facility	1130004-027-AV	4/22/2016	4/22/2021	Renewal
All	Admin Correction to Appendices	1130004-028-AC	5/22/2017	5/22/2017	Admin
					Correction
001, 003, 005, 074, 080, 081	Riley Boiler Fuel Switch	1130004-029-AC	9/25/2018	9/28/2019	Construction
001, 003, 005, 074, 080, 081	Riley Boiler (Incorp 029-AC)	1130004-030-AV	10/26/2018	4/22/2021	Revision
001 & 003	Temporary Increase in Steam Flow to DIMLA	1130004-031-AC	9/1/2018	N/A	Exemption
001 & 003	Temporary Increase in Steam Flow to DIMLA	1130004-032-AC	11/29/2018	N/A	Exemption
001 & 003	Temporary Increase in Steam Flow to DIMLA	1130004-033-AC	1/29/2019	N/A	Exemption
001 & 003	Temporary Increase in Steam Flow to DIMLA	1130004-034-AC	4/10/2020	N/A	Exemption

# TABLE HPERMIT HISTORY

EU No.	Description	Permit No.	Effective Date	<b>Expiration Date</b>	Project Type
All	Facility	1130004-035-AV	01/21/2021	01/21/2026	Renewal
005	Install Calorimeters at the Amines Plants Flare	1130004-036-AC	11/12/2020	11/12/2025	Construction
001 & 003	Remove Duplicative DIMLA PSD	1130004-037-AC	12/01/2020	12/31/2021	Construction
	Requirements				
001,003,005,006,058,071,072,060,077,078,	DIMLA Expansion	1130004-038-AC	06/04/2021	06/03/2026	Construction
079,062,063,075,076					
001 & 003	Incorporate Permit No. 1130004-037-AC	1130004-039-AV	09/21/2021	01/21/2026	Revision
001,003,005,007,055,056,057,058,059,062,	Higher Amines Expansion	1130004-040-AC	10/21/2021	10/21/2026	Construction
063,066,070,071,072,073,074,075					
078	Change the material of construction for three	1130004-041-AC	10/06/2021	N/A	Exemption
	existing heat exchangers in the DIMLA Plant				
001,003,005,006,007,055,056,057,058,059,	Incorporate Phase One Construction activities	1130004-042-AV	12/02/2022	01/21/2026	Revision
060,062,063,066,070,071,072,073,074,075,	for Permits 038-AC & 040-AC				
076,077,078,079					
Unregulated Storage Tanks	Fugitive Component Replacement	1130004-043-AC	11/29/2022	N/A	Exemption
001,003,005,006,007,055,056,057,058,059,	Incorporate Phase Two Construction activities	1130004-044-AV	08/06/2024	01/21/2026	Revision
060,062,063,066,070,071,072,073,074,075,	for Permits 038-AC & 040-AC				
076,077,078,079					
001, 003, 005, 006, 029, 033, 034, 049,	DIMLA Expansion II, supersedes 1130004-	1130004-045-AC	01/29/2025	01/29/2030	Construction
050, 053, 058, 060, 062, 063, 071, 072,	038-AC and replaces Phase Three with five				
075, 076, 077, 078, 079	new phases.	*			
All	Facility	1130004-046-AV	Pending	Pending	Renewal

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# TABLE 1 SUMMARY OF AIR POLLUTANT STANDARDS AND TERMS

# Air Permit

Time Sensitive Action Chart

[If any of the time deadlines in the Air Permit Action Chart are inconsistent with a time deadline in a permit condition, the time deadline in the permit condition shall be followed.]

SOURCE	ACTION	DUE DATE
Facility-Wide	EAOR Title V Annual Emissions Fee Invoice and Fee Payment [Rules 62-210.370(3), 62-210.900 & 62-213.205, F.A.C.; and, §403.0872(11), Florida Statutes (2013)]	April 1 - annually
Facility-Wide	Annual Statement of Compliance [Rules 62-213.440(3)(a)2. & 3. and (b), F.A.C.]	Before March 1 - annually
Facility-Wide	Plant Problems/Permit Deviations	Immediately upon occurrence
Facility-Wide	Malfunction Excess Emissions Report	Quarterly (if requested)
Facility-Wide	Semiannual Report [40 CFR 63.864(k)(1) or (2)]	As agreed with Administrator. See Permit Section II – Facility- Wide Conditions and Appendix RR – Facility-Wide Reporting Requirements.
Facility-Wide	Permit Renewal Application	On or before <b>Application Due</b> <b>Date</b>
All Emissions Units	See <u>Table 1</u> : Summary of Applicable Requirements a complete list time sensitive actions and due dates for	and Compliance Procedures, for each emissions unit

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For convenience purposes only, this table summarizes applicable requirements and compliance procedures related to the facility. It does not supersede any of the terms or conditions of the permit.

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 029	Methylamines Plant Nos. 1 and 4 Group 1 HON Storage Tanks: TK- 53407, TK- 53405, TK- 53401B	Each floating roof shall be equipped with a metallic shoe seal. [62-204.800(11)(b), F.A.C.] [40 CFR 63.119(a)(1), (b)(3)]	Must visually inspect the internal floating roofs and the secondary seals through manholes and roof hatches on each fixed roof at least once every12 months after January 27, 1998. Visually inspect each internal floating roof, the primary and secondary seals, gaskets, slotted membranes, and holes, tears sleeve seals (if any) each time the storage vessel is emptied and degassed, and at least once every 10 years after April 22, 1997. If during an inspection, an internal floating roof is not resting on the surface of the liquid inside the storage vessel and is not resting on the leg supports; or there is liquid on the floating roof; or the seal is detached; or there are holes or tears in the seal fabric; or there are visible gaps between the seal and the wall of the storage vessel, repairs shall be made to the equipment within 45 calendar days. If a failure is detacted that cannot be repaired within 45 calendar days and if the vessel cannot be emptied within 45 calendar days of up to 30 additional calendar days each provided that documentation of a decision to utilize an extension is maintained that includes a description of the failure, that alternate storage capacity is unavailable, and that specifies a schedule of actions that will ensure that the equipment will be repaired or the vessel will be emptied as soon as possible. If during the inspections, the internal floating roof has defects; or the gaskets no longer close off the liquid surface from the atmosphere; or the slotted membrane has more than 10 percent open area, the repairs shall be made	<ul> <li>(1) Periodic reports are to include a summary of the results of each internal or external inspection conducted in which a failure was detected with the date of the inspection, identification of the storage vessel in which a failure was detected and a description of the failure. Also, the nature of and date the repair was made or the date the storage vessel was emptied is to be documented. The Department shall be notified in writing at least 30 calendar days prior to the refilling of a storage vessel that has been emptied and degassed. If the facility could not have known about the refilling 30 calendar days in advance, the facility shall notify the Department at least 7 calendar days prior to the refilling of the storage vessel. Notification made by telephone shall be immediately followed by written documentation demonstrating why the inspection was unplanned. Documentation pertaining to the utilization of any extensions is to be included.</li> <li>[62-204.800(11)(b), F.A.C.] [40 CFR 63.122, (a)(4), (a)(5), (d)] [40 CFR 63.120(a)(5) and (6)][40 CFR 63.123 (g)]</li> </ul>

	before the vessel is refilled with organic HAP.	(2) Records showing each tank's
		dimensions and capacities and records
	[62-204.800(11)(b), F.A.C.] [40 CFR 63.120(a)(2), (4) and (7)]	of each inspection shall be maintained
	<u>STERP</u> .	as long as the tank retains Group 1 or
	Visually inspect the deck fitting for the slotted	Group 2 status under the HON and is
	guidepole at least once every 10 years and each time	in operation.
	the vessel is emptied and	[62-204.800(11)(b), F.A.C.] [40 CFR
	degassed. If the slotted guidepole deck fitting or control	63.123(a) and (c)]
	devices have defects, or if a gap of more than 0.32	
	centimeters (1/8 inch) exists between any gasket	
	required for control of the slotted guidepole deck fitting	
	and any surface that is intended to seal, such items shall	
	be repaired before filling or refilling the storage vessel	
	with regulated material.	
	[Federal Register Notice 19891 (April 13, 2000)]	

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 046	Sitewide HON Heat Exchangers	All sitewide heat exchange systems not meeting the conditions specified in 40 CFR 63.104(a)(1) through (6), shall be monitored by (a) inspecting the cooling water for the presence of one or more organic HAPs or other representative substance whose presence in cooling water indicates a leak as specified in 40 CFR 63.104(b)(1) through (6); or by using a surrogate indicator of heat exchanger system leaks as specified in 40 CFR 63.104(c)(1) through (3). [62-204.800(11)(b), F.A.C.] [40 CFR 63.104(a), (b), and (c)]	<ul> <li>Beginning April 22, 1999, any leaks that are detected shall be repaired as soon as practical but not later than 45 days after the Permittee receives results of monitoring tests indicating a leak. After repair, the Permittee shall confirm that the heat exchange system has been repaired within 7 calendar days of the repair or startup, whichever is later. Repairs may be delayed beyond 45 days if the criteria specified in 40 CFR 63.104(e) are met.</li> <li>[62-204.800(11)(b), F.A.C.] [40 CFR 63.104(d) and (e)]</li> </ul>	<ul> <li>Beginning April 22, 1999, the Permittee shall maintain records of required monitoring, leaks detected, the dates of efforts to repair leaks, and the method or procedures used to confirm repair of a leak and the date the repair was confirmed.</li> <li>Periodic reports are required only if the Permittee invokes the delay of repair. Periodic reports shall include information required by 40 CFR 63.104(f)(2).</li> <li>[62-204.800(11)(b), F.A.C.] [40 CFR 63.104(f)]</li> </ul>
EU 047	Methanol Storage HON- Maintenance Wastewater	Permittee shall prepare a description of maintenance procedures for management of wastewaters containing those organic HAPs listed in Table 9 of 40CFR Subpart G which are generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance- turnaround) and during periods which are not shutdown (i.e., routine maintenance). The descriptions shall: (1) specify process equipment or maintenance tasks anticipated to create wastewater during maintenance activities, (2) specify procedures that will be followed	<ul> <li>The Permittee shall maintain a record of the required information as part of the startup, shutdown, and malfunction plan required under 40 CFR 63.6(e)(3).</li> <li>Plans shall be maintained and kept readily available for inspection for the life of the source, or until 40 CFR Part 63 standards no longer apply to the source. No notification or periodic reporting of maintenance wastewater activities is required.</li> <li>[62-204.800(11)(b), F.A.C.] [40 CFR 63.105(d) and (e)]</li> </ul>	See requirements specified in "Compliance Testing/Demonstration Requirement(s)" column.

to properly mana and control organic the atmosphere procedures to be fol materials from pr Permittee shall m maintenance proc	e the wastewater HAP emissions to and (3) specify owed when clearing ocess equipment. dify and update edures as needed.		
[62-204.800(11)(b) 63.105(b)	F.A.C.] [40 CFR and (c)]		

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 048	Methylamines Plants Sample Points	Sampling points in organic HAP service shall meet the criteria set forth in 40 CFR 63.166. [62-204.800(11)(b), F.A.C.] [40 CFR 63.166]	Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent system. Gases displaced during filling of the sample container are not required to be collected or captured. Each sampling system shall meet one of the specifications specified in 40 CFR 63.166(b). [62-204.800(11)(b), F.A.C.][40 CFR 63.166]	The Permittee shall maintain records specified in 40 CFR 63.181(b)(1)(i) and no periodic reporting is required under 40 CFR 63.182. Notwithstanding, Title V semi-annual progress reports shall be submitted that identify any instances of non- compliance and annual Title V compliance certification reports must certify whether or not compliance with applicable requirements has been achieved. [62-204.800(11)(b), F.A.C.][40 CFR 63.181]
EU 001	Riley Stoker Boiler	The maximum allowable operating rate of the Riley Stoker Boiler is 128 MMBtu/hour heat input, averaged daily. [62-213.440(1), F.A.C.]		The Permittee shall maintain records of operation.
EU 001	Riley Stoker Boiler	The boiler may operate using natural gas and process off-gases. [Rule 62-210.200(PTE), F.A.C.; and Permit No. 1130004-019-AC]		
EU 001	Riley Stoker Boiler	Visible emissions shall not exceed 20% opacity except for one six-minute period per one-hour period during which opacity shall not exceed 27%. [62-296.406(1), F.A.C.]	EPA Method 9 testing shall be conducted shall be conducted once within the final twelve months of the Title V permit at 90 to 100 percent of the maximum capacity. [62-297.310(3)(b)]	Results of testing reported to the Department within 45 days after testing and must contain, at a minimum, information required in [62- 297.310(8), F.A.C.].

#### Permit **Compliance Testing/Demonstration Recordkeeping/ Reporting** Section / Description **Condition/Limitation Requirement(s)** Requirement(s) EU No. EU 001 Riley Stoker Annual compliance reports must cover the period from Permittee must submit a compliance The permittee must keep records Boiler report with the information in paragraphs January 1 to December 31. Annual compliance reports according to paragraphs (a)(1) & (2) of (c)(5)(i) through (iii), (xiv) & (xvii) of 40 must be postmarked or submitted no later than January 31. 40 CFR 63.7555. CFR 63.7550. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7550(b)] [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7555(a)] [Rule 62-204.800(11), F.A.C. and 40 CFR 63.7550(c)] Permittee shall maintain records of compliance information in accordance with 40 CFR 63.7560. As specified in 40 CFR 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record. [Rule 62-204.800(11), F.A.C; and 40 CFR 63.75601 EU 003 B & W Boiler The maximum allowable operating rate The annual production rate of steam shall be calculated The Permittee shall maintain records of the B & W Boiler is 128 from daily records. of operation. The annual production MMBtu/hour heat input, averaged daily. rate of steam shall be calculated from the monthly measured steam [62-213.440(1), F.A.C.] production. Visible emissions shall not exceed 20% EPA Method 9 testing shall be conducted prior to Results of testing reported to the EU 003 B & W Boiler obtaining a renewed operation at 90 to 100 percent of Department within 45 days after opacity except for one six-minute period the maximum boilerplate capacity, which is 90,000 testing (and included in submission of per one-hour period during which opacity shall not exceed 27%. pounds per hour of steam. the application) and must contain, at a minimum, information required in [62-296.406(1), F.A.C.] [62-297.310, F.A.C.] [62- 297.310(10), F.A.C.]. B & W Boiler Permittee shall conduct an initial fuel specification EU 003 Permittee shall demonstrate that all Maintain records as specified in 40 analyses for mercury according to the procedures in 40 gaseous fuels other than natural gas or CFR 63.7555(g) and in refinery gas qualifies as an "Other gas CFR 63.7521(f) through (i) and according to the accordance with 40 CFR 63.7560. 1" fuel, as defined in §63.7575. frequency listed in 40 CFR 63.7540(c). [62-204.800(11)(b), F.A.C.] [40 CFR [62-204.800(11)(b), F.A.C.] [40 CFR 63.7530(g)] [40 CFR 63.7560] [62-204.800(11)(b), F.A.C.] [40 CFR 63.7530(g)]

	63.7530(g)]	

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 003	B & W Boiler	Permittee shall conduct an annual tune-up of the boiler. [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)] [Table 3 (Item 3) to Subpart DDDDD of part 63]	Permittee shall perform tune-ups according to the criteria specified in 40 CFR 63.7540(a)(10)(i) through (v). [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)] [Table 3 (Item 3) to Subpart DDDDD of part 63]	Maintain and submit, if requested by the Administrator, an annual report containing the information in 40 CFR 63.7540(a)(10)(vi)(A) through (C). [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)(vi)]
EU 003	B & W Boiler	Permittee must submit a compliance report with the information in paragraphs (c)(5)(i) through (iii), (xiv) & (xvii) of 40 CFR 63.7550. [Rule 62-204.800(11), F.A.C. and 40 CFR 63.7550(c)]	Annual compliance reports must cover the period from January 1 to December 31. Annual compliance reports must be postmarked or submitted no later than January 31. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7550(b)]	The permittee must keep records according to paragraphs (a)(1) & (2) of 40 CFR 63.7555. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.7555(a)] Permittee shall maintain records of compliance information in accordance with 40 CFR 63.7560. As specified in 40 CFR 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record. [Rule 62-204.800(11), F.A.C; and 40 CFR 63.7560]

## Permit **Recordkeeping/ Reporting** Section / Description **Condition/Limitation Compliance Testing/Demonstration Requirement(s)** Requirement(s) FU NL

EU NO.				
EU 005	Amines Plants Flare	During periods of flare startup, shutdown, malfunction, and maintenance, or other such periods that the Permittee may choose, the Permittee may divert emissions from the flare to the Fuel Gas System Boilers. [62-204.800(11)(b), F.A.C.] [40 CFR 63.6(e)(3]	The Permittee shall demonstrate compliance with this requirement by maintaining compliance with 40 CFR Part 63 requirements pertaining to startup, shutdown, malfunction, and reporting of maintenance activities in accordance with other permit conditions set forth in this permit that pertain to emission units that emit organic hazardous air pollutants to the Amines Flare and that are regulated under 40 CFR 63 Subparts F, G, H and FFFF. [62-204.800(11)(b), F.A.C.] [40 CFR 63.10(d)(5)]	See "Compliance Testing" column.
EU 005	Amines Plants Flare	<ul> <li>The Amines Plants Flare, a non-assisted flare, shall:</li> <li>Be operated at all times when HON or MON- regulated emissions may be vented to it and shall maintain a minimum net heating value of the gas being combusted at 7.45 MJ/scm (200 Btu/scf) when emission units subject to 40 CFR 63 Parts G, H, or FFFF are venting to the flare</li> <li>Be operated with a flame present at all times. The presence of a flare pilot flame shall be monitored, at least once each hour, using a thermocouple or any other equivalent device to detect the presence of a flame; and</li> <li>Maintain the exit velocity of gas from the flare at less than or equal to 60 ft/sec (18.3 m/sec).</li> </ul>	<ul> <li>Compliance with the minimum net heating value requirement shall be demonstrated by maintaining a vent gas to natural gas fuel input ratio sufficient to maintain a minimum net heating value of 7.45 MJ/scm (200 Btu/scf). Approved alternate monitoring allows use of the Honeywell control system that continuously monitors the natural gas and process gas flow rate at the flare in lieu of collecting samples of gas ducted to the flare tip for heating value analysis and testing to measure the velocity at the flare tip;</li> <li>The presence of a flare pilot plant flame shall be measured using a thermocouple or other equivalent device.</li> <li>Utilize a high velocity alarm to ensure that the maximum allowable flare exit velocity 60 ft/sec (18.3 m/sec) will not be exceeded.</li> <li>[62-204.800(11)(b), F.A.C.] [40 CFR 63.11(b)(3), (5), (6) and (7); and 40 CFR 60.18]</li> </ul>	<ul> <li>The Permittee shall maintain records of the following information:</li> <li>Identification of the dates and durations of periods during which the minimum heating value, pilot flame, and exit velocity requirements were not maintained and the reasons why these requirements were not met.</li> <li>Identification of the dates and durations during which flare control and monitoring systems were inoperative.</li> <li>The Permittee shall submit periodic reports that identify each occurrence during which heating value, pilot flame, and exit velocity requirements were not maintained. Periodic reports shall also specify periods during which the control and monitoring systems were inoperative. The lack of monitoring data shall not constitute an excursion if other process data is available that</li> </ul>

		[62-204.800(8)(d) and (11)(b) & (d), F.A.C.] [40 CFR 63.11(b)(3), (5), (6) and (7)]		adequately demonstrates that the flare was operating normally. [62-204.800(11)(b) and (d), F.A.C.] [40 CFR 63.118(a)(1)] [40 CFR
				63.122(g)(3)] [40CFR 63.130(a)(2)(i)] [40 CFR 63.130(a)(1)] [40 CFR 152(c)(4)(E)(iii)] [40 CFR 60.115b] [40 CFR 63.172]
EU 005	Amines Plants Flare	<ul> <li>The Amines Plants Flare shall be operated with no visible emissions, except for periods not to exceed a total of five minutes in any two consecutive hours.</li> <li>[Rules 62-204.800(8) and (11), F.A.C.; 40 CFR 63.11(b)(4), and 40 CFR 60.18(c)(1) and (f)(1)]</li> </ul>	<ul> <li>Permittee shall conduct a flare compliance assessment using EPA Method 22 during operations at a time when either the MA Plant No. 1 or No. 4 and the DIMLA Plant are operating. The test shall be conducted within the 12 months prior to the submittal of and included with the Title V permit Renewal Application. The observation period shall be at least two hours.</li> <li>[Rules 62-204.800(8) &amp; (11), F.A.C.; 40 CFR 63.11(b)(4), 40 CFR 60.18(c)(1) and (f)(1); and Permit No. 1130004-019-AC]</li> </ul>	Results of testing must be reported to the Department within 45 days after testing and must contain, at a minimum, information required in Rule 62- 297.310(10)(c), F.A.C. Periodic reports will only specify that EPA Method 22 testing was conducted and indicate any deviations from the visible emissions requirement. [Rule 62-297.310(10), F.A.C.]

#### Permit **Recordkeeping/ Reporting** Section / Description **Condition/Limitation Compliance Testing/Demonstration Requirement(s) Requirement(s)** EU No. EU 006 Methylamines The maximum allowable operating rate The actual gas-fired heater heat input will be calculated on The Permittee shall maintain records Plant No. 1 of the Methylamines Gas-Fired Heater a semi-annual basis as the sum of the previous 12 months of operation. The annual gas-fired is 10 million Btu/hr heat input. total measured flow of natural gas to the heater and the heater heat capacity will be calculated Gas-Fired average higher heating value of the natural gas. on a semi-annual basis as the sum of Heater the previous 12 months total [62-213.440(1),F.A.C.] measured flow of natural gas to the heater and the average higher heating value of natural gas. [62-213.440(1), F.A.C.] EU 006 Permittee shall conduct an annual Permittee shall perform tune-ups according to the criteria Maintain and submit, if requested by Methylamines specified in 40 CFR 63.7540(a)(10)(i) through (v). the Administrator, an annual report tune-up of the boiler. Plant No. 1 containing the information in 40 Gas-Fired [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)] [62-204.800(11)(b), F.A.C.] [40 CFR CFR 63.7540(a)(10)(vi)(A) through Heater 63.7540(a)(10)] [Table 3 (Item 3) to (C). Subpart DDDDD of part 63] [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)(vi)] Periodic reports on flare operation will be Intermittent organic hazardous air pollutant EU 049 Methylamines The Permittee shall reduce emissions submitted (see "Amines Plant Flare"). emissions from Methylamines Plant No. 1 Process Vents Plant No. 1 of organic hazardous air pollutants (i.e., chemicals listed in Table 2 of 40 shall be vented to the Amines Plants Flare, which shall Process Vents [62-204.800(8)(d) and (11)(b), CFR Part 60 Subpart F) using a vapor meet the general control device requirements of 40 CFR F.A.C.] [40 CFR 63.118] [40 CFR collection system and flare meeting the 63.11(b). Specific permit conditions applicable to the 63. 152(c)(4)] criteria of 40 CFR 63.11(b). Amines Plants Flare are specified elsewhere in this permit. [62-204.800(11)(b), F.A.C.] [40 CFR 63.113(a)(1)] [62-204.800(11)(b), F.A.C.] [40 CFR 63.113(a)(1)]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 050	Methylamines Plant No. 1 Wastewater	The Permittee shall comply with requirements set forth in 40 CFR 63.132(a)(1) through (a)(3), which requires that the Permittee determine whether a wastewater emission source is a Group 1 or Group 2 stream. For Group 2 streams, the Permittee shall comply with the recordkeeping requirements of 40 CFR 63.146. [62-204.800(11)(b), F.A.C.] [40 CFR 63.132(a)] [40 CFR 63.146]	If the Permittee uses process knowledge to determine the annual average concentration of a wastewater stream and/or the annual average flowrate and thereby concludes that a wastewater stream is not a Group 1 stream, the Permittee shall keep in a readily accessible location the documentation of how process knowledge was used. [62-204.800(11)(b), F.A.C.] [40 CFR 63.147(f)]	Maintain records of information specified in "Compliance Demonstration" Column.
EU 051	Methylamines Plant No. 1 HON Maintenance Wastewater	The Permittee shall maintain a description of maintenance procedures for management of wastewaters containing those organic HAPs listed in Table 9 of 40 CFR Subpart G which are generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdown (i.e., routine maintenance). The descriptions shall: (1) specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities, (2) specify procedures that will be followed to properly manage the wastewater and control organic HAP emissions to the	See requirements specified in "Condition/Limitation" column.	The Permittee shall maintain a record of the required information as part of the startup, shutdown, and malfunction plan required under 40 CFR 63.6(e)(3). Plans shall be maintained and kept readily available for inspection for the life of the source, or until 40 CFR Part 63 standards no longer apply to the source. No notification or periodic reporting of maintenance wastewater activities is required. [62-204.800(11)(b), F.A.C.] [40 CFR 63.105(d)]

		atmosphere, and (3) specify the procedures to be followed when clearing materials from process equipment. Permittee shall modify and update the maintenance procedures as needed. [62-204.800(11)(b), F.A.C.] [40 CFR 63.105(b) and (c)]		
EU 053	Methylamines Plants Nos. 1&4 HON Group 2 Storage Tanks	For the Group 2 storage vessels (D- 68127, D- 68146, D-671160, D- 67134B and D-67043 in the common service of both MA Plants 1 and 4), the Permittee shall comply with the recordkeeping requirements of 40 CFR 63.123(a). [62-204.800(11)(b), F.A.C.] [40 CFR 63.119(a)(3)]	See requirements specified in "Condition/Limitation" column.	The Permittee shall keep records showing the dimensions of the storage vessel and an analysis showing the capacity of the vessel. The Permittee is not required to comply with any other provisions of 40 CFR 63.119 through 40 CFR 63.123. [62-204.800(11)(b), F.A.C.] [40 CFR 63.123(a)]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 054	Methylamines Plant Nos. 1&4 NSPS Storage Tanks	The Methylamines Plant Nos. 1&4 NSPS Storage Tanks (D-67204E, D- 67216A, D-67216B and D- 67044, used in the common service of both MA Plants 1 and 4) shall vent through a closed loop vent system followed by a control device designed and operated to reduce inlet emissions of VOC by 95 percent. The closed loop vent system shall be designed to collect all VOC vapors and gases discharged from the storage vessel and shall be operated with no detectable emissions as indicated by an instrument reading of less than 500 ppm above background and visual inspections as determined by 40 CFR 60.485(b). [62-204.800(8)(b)18, F.A.C.] [40 CFR 60.112b(a)(3)(i)&(ii)]	Emissions from the storage tanks shall be vented to the Amines Plants Flare, which shall meet the general control device requirements of 40 CFR 60.18(e) & (f). Specific permit conditions applicable to the Amines Plants Flare are specified elsewhere in this permit. [62-204.800(8)(b)18, F.A.C.] [40 CFR 60.113b(d)]	Continuous records of flare operation shall be maintained and periodic reports on flare operation shall be submitted (see "Amines Plant Flare"). Records showing the dimension of the storage vessel and an analysis showing the capacity of the storage vessel shall be kept readily accessible for each storage tank subject to 40 CFR 60 Subpart Kb. [Rule 62-204.800(8)(b)(18), F.A.C. and 40 CFR 60.116b(b)]
EU 007	Higher Amines Plant Gas- Fired Heater	The maximum allowable operating rate of the Methylamines Gas-Fired Heater 8.4 MM Btu/hr.	The gas-fired heater heat capacity will be calculated from the measured flow of natural gas to the heater and the average higher heating value of natural gas.	The Permittee shall maintain records of operation. The annual gas-fired heater heat capacity will be calculated on a semi-annual basis as the sum of the previous 12 months total measured flow of natural gas to the heater and the average higher heating value of natural gas. [62-213.440(1), F.A.C.]

EU 007Higher Amines Plant Gas- Fired HeaterPermittee shall conduct a biennial tune-up of the boiler. [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(11)] [Table 3 (Item 2) to Subpart DDDDD of part 63]Permittee shall perform tune-ups according to the criteria specified in 40 CFR 63.7540(a)(10)(i) through (v). [62-204.800(11)(b), F.A.C.] [40 CFR [62-204.800(11)(b), F.A.C.] [40 CFR [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(11)]	Maintain and submit, if requested by the Administrator, an annual report containing the information in 40 CFR 63.7540(a)(10)(vi)(A) through (C). [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)(vi)]
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Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 058	DIMLA MON Group 2 Storage Tanks	For each Group 2 storage vessel DIMLA; Formalin Tank, TK-6214, the Permittee shall comply with the recordkeeping requirements of 40 CFR 63.123(a [62- 204.800(11)(b), F.A.C.] [40 CFR 63.119(a)(3)]	See requirements specified in "Condition/Limitation" column.	The Permittee shall keep records showing the dimensions of each storage vessel and an analysis showing the capacity of each vessel. The Permittee is not required to comply with any other provisions of 40 CFR 63.119 through 40 CFR 63.123. [62-204.800(11)(b), F.A.C.] [40 CFR 63.123(a)] [62-212.300(1)(e)2, F.A.C.]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 060	Methylamines Plant No. 4 Gas-Fired Heater	The maximum allowable operating rate of the Methylamines Plant 4 Gas-Fired Heater is 10 MM Btu/hr.	The gas-fired heater heat capacity will be calculated from the measured flow of natural gas to the heater and the average higher heating value of natural gas.	The Permittee shall maintain records of operation. The annual gas-fired heater heat capacity will be calculated on a semi-annual basis as the sum of the previous 12 months total measured flow of natural gas to the heater and the average higher heating value of natural gas. [62-213.440(1), F.A.C.]
EU 060	Methylamines Plant No. 4 Gas-Fired Heater	Permittee shall conduct an annual tune-up of the boiler. [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)] [Table 3 (Item 3) to Subpart DDDDD of part 63]	Permittee shall perform tune-ups according to the criteria specified in 40 CFR 63.7540(a)(10)(i) through (v). [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)]	Maintain and submit, if requested by the Administrator, an annual report containing the information in 40 CFR 63.7540(a)(10)(vi)(A) through (C). [62-204.800(11)(b), F.A.C.] [40 CFR 63.7540(a)(10)(vi)]

#### Permit **Recordkeeping/ Reporting** Section / Description **Condition/Limitation Compliance Testing/Demonstration Requirement(s) Requirement(s)** EU No. EU 033 Methylamines The Permittee shall reduce emissions Intermittent organic hazardous air pollutant emissions from Continuous records of flare operation Methylamines Plant No. 4 Process Vents shall be vented to Plant No. 4 of organic hazardous air pollutants shall be maintained and periodic the Amines Plants Flare, which shall meet the general Process Vents (i.e., chemicals listed in Table 2 of 40 reports on flare operation shall be CFR Part 60 Subpart F) using a vapor control device requirements of 40 CFR 63.11(b). submitted (see "Amines Plant Flare"). collection system and flare meeting the Specific permit conditions applicable to the Amines [62-204.800(11)(b), F.A.C.] [40 CFR criteria of 40 CFR 63.11(b) [62-Plants Flare are specified elsewhere in this permit. 63.118] [40 CFR 63.152(c)(4)] 204.800(11)(b), F.A.C.] [40 CFR [62-204.800(11)(b), F.A.C.] [40 CFR 63.113(a)(1)] 63.113(a)(1)] After the compliance date specified in 40 CFR 63.100 of subpart F of this part, a Group 1 process vent that is also subject to the provisions of 40 CFR part 60, subpart NNN is required only to comply with the provisions of this subpart [G]. EU 033 Methylamines Intermittent organic hazardous air pollutant emissions from Continuous records of flare operation Methylamines Plant No. 4 Process Vents shall be vented to Plant No. 4 shall be maintained and periodic Process Vents the Amines Plants Flare, which shall meet the general reports on flare operation shall be control device requirements of 40 CFR 63.11(b). submitted (see "Amines Plant Flare"). Specific permit conditions applicable to the Amines [62-204.800(11)(b), F.A.C.] [40 CFR Plants Flare are specified elsewhere in this permit. [40 CFR 63.110(d)(4)] 63.118] [40 CFR 63.152(c)(4)] [62-204.800(11)(b), F.A.C.] [40 CFR 63.113(a)(1)] After the compliance date specified in 40 CFR 63.100 of subpart F of this part, a Group 1 process vent that is also subject to the provisions of 40 CFR part 60, subpart RRR is required only to comply with the provisions of this subpart [G]. EU 033 Intermittent organic hazardous air pollutant emissions from Continuous records of flare operation Methylamines Plant No. 4 Methylamines Plant No. 4 Process Vents shall be vented to shall be maintained and periodic the Amines Plants Flare, which shall meet the general reports on flare operation shall be Process Vents submitted (see "Amines Plant Flare"). control device requirements of 40 CFR 63.11(b). Specific permit conditions applicable to the Amines [62-204.800(11)(b), F.A.C.] [40 CFR Plants Flare are specified elsewhere in this permit. [40 CFR 63.110(d)(4)] 63.118] [40 CFR 63.152(c)(4)] [62-204.800(11)(b), F.A.C.] [40 CFR 63.113(a)(1)]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 034	Methylamines Plant No. 4 Wastewater No.4 Dehydration Column Bottoms)	The Permittee shall comply with requirements set forth in 40 CFR 63.132(a)(1) through (a)(3), which requires that the Permittee determine whether a wastewater emission source is a Group 1 or Group 2 stream. For Group 2 streams, the Permittee shall comply with the recordkeeping requirements of 40 CFR 63.146. [62-204.800(11)(b), F.A.C.] [40 CFR 63.132(a)]	If the Permittee uses process knowledge to determine the annual average concentration of a wastewater stream and/or the annual average flowrate used to determine that a wastewater stream is not a Group 1 stream, the Permittee shall keep in a readily accessible location the documentation of how process knowledge was used. [62-204.800(11)(b), F.A.C.] [40 CFR 63.147]	Maintain records of information specified in "Compliance Demonstration" Column.
EU 035	Methylamines Plant No. 4 HON Maintenance Wastewater	The Permittee shall maintain a description of maintenance procedures for management of wastewaters containing those organic HAPs listed in Table 9 of 40 CFR 63 Subpart G which are generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdown (i.e., routine maintenance). The descriptions shall: (1) specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities, (2) specify procedures that will be followed to properly manage the wastewater and control organic HAP emissions to the atmosphere, and (3) specify the procedures to be	See requirements specified in "Condition/Limitation" column.	The Permittee shall maintain a record of the required information as part of the startup, shutdown, and malfunction plan required under 40 CFR 63.6(e)(3). Plans shall be maintained and kept readily available for inspection for the life of the source, or until 40 CFR Part 63 standards no longer apply to the source. No notification or periodic reporting of maintenance wastewater activities is required. [62-204.800(8)(d) and (11)(b), F.A.C.] [40 CFR 63.105(d) and 63.6(e)(3)]

followed when clearing main from process equipment. Permittee shall modify and the maintenance procedure needed.	erials The update s as			
[62-204.800(11)(b), F.A.C.] [ 63.105(b) and (c)]	0 CFR			
Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
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EU 036	Methylamines Plant No. 1 and No. 4 HON Equipment Leaks	<u>Pumps</u> . The Permittee shall meet the criteria set forth in 40 CFR 63.163 for pumps in light liquid service that have been designated by the Permittee to be in organic hazardous air pollutant light liquid service for 300 or more hours per year. [62- 204. 800(11)(b), F.A. C.] [40 CFR 63.163]	In order to comply with the requirements of 40 CFR 63.163, the Permittee shall either: (1) Comply with the Phase III leak detection and repair requirements specified in 40 CFR 63.163, or (2) Alternately, the Permittee may comply with the requirements specified in 40 CFR 63.163 using methods specified in 40 CFR 63.163(e), (f), or (g). [62- 204. 800(11)(b), F.A. C.] [40 CFR 63.163]	If the Permittee elects to demonstrate compliance with the requirements of 40 CFR 63.163 by implementing a leak detection and repair program, records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i), (b)(7), (c), (d), and if a quality improvement plan is implemented, records required under paragraph (h) shall also be maintained. If the Permittee elects to demonstrate compliance using methods specified in 40 CFR 63.163(e), (f), or (g), other relevant records specified in 40 CFR 63.163 shall be maintained. Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [62- 204. 800(11)(b), F.A. C.] [40 CFR 63.181 and 63.182]
EU 036	Methylamines Plant No. 1 and No. 4 HON Equipment Leaks	<u>Pressure relief devices</u> . The Permittee shall comply with the requirements set forth in 40 CFR 63.165 for pressure relief devices in gas/vapor service that have been designated by the Permittee to be in organic hazardous air pollutant gas/vapor service for 300 or more hours per year. Pressure relief devices that are routed to a process or fuel gas system are exempt. [62-204.800(11)(b), F.A.C.] [40 CFR 63.165]	After pressure releases from pressure relief valves that are not equipped with upstream rupture disks, the pressure relief device shall be returned to less than 500 ppmv above background, as confirmed by the method specified in 40 CFR 63.180(c), as soon as practicable, but no later than 5 days after the release. Any pressure relief device with an upstream rupture disk is exempt from monitoring, provided that in the event that a release ruptures the disk, the disk is replaced as soon as practicable, but no later than 5 days after the release. [62-204.800(11)(b), F.A.C.] [40 CFR 63.165] [40 CFR 63.180]	Records shall be maintained in accordance with 40 CFR 63.1 81(b)(1)(i), (b)(3), and (f). Periodic reports meeting the specifications of 40 CFR 63.182(d)(xiv) shall be submitted to the Department. [62-204.800(11)(b), F.A.C.] [40 CFR 63.181 and 63.182]

EU 036Methylamines Plant No. 1 and No. 4 HON Equipment LeaksOpen-ended valves or lines. The Permittee shall comply with requirements set forth in 40 CFR 63.167 for open-ended lines that have been designated by the Permittee to be in organic hazardous air pollutant service for 300 or more hours per year.Each open-ended valve or line shall be equipped with a cap, blind flange, plug, or a second valve, except for open- ended valves specified in 40 CFR 63.167(d) and (e), which are exempt. The Permittee shall also comply with work and operating practices specified in 40 CFR 63.167(a)(2), (b), and (c).[62-204.800(11)(b), F.A.C.] [40 CFR 63.167][62-204.800(11)(b), F.A.C.] [40 CFR 63.167]	The Permittee shall maintain records specified in 40 CFR 63.181 (b)(1)(i) and no periodic reporting shall be required under 40 CFR 63.182. Notwithstanding, Title V semi-annual progress reports shall be submitted that identify any instances of non- compliance and annual Title V compliance certification reports must certify whether or not compliance with applicable requirements has been achieved [62- 204.800(11)(b), F.A.C.][40 CFR 63.181 and 63.182]
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Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 036	Methylamines Plant No. 1 and No. 4 HON Equipment Leaks	<u>Valves</u> . The Permittee shall comply with Phase III leak detection and repair criteria set forth in 40 CFR 63.168 for valves in light liquid and gas service that have been designated by the Permittee to be in organic hazardous air pollutant light liquid/gas service for 300 or more hours per year. [62-204.800(11)(b), F.A.C.] [40 CFR 63.168]	The Permittee shall inspect and repair valves according to the criteria specified in 40 CFR 63.168. [62-204.800(11)(b), F.A.C.] [40 CFR 63.168] [40 CFR 63.180]	Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i) and (ii), (b)(7), (d), and if a quality improvement plan is implemented, records required under paragraph (i) shall also be required. Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [62-204.800(11)(b), F.A.C.] [40 CFR 63.181 and 63.182]
EU 036	Methylamines Plant No. 1 and No. 4 HON Equipment Leaks	<u>Connectors</u> . The Permittee shall comply with Phase III leak detection and repair criteria set forth in 40 CFR 63.174 for connectors in light liquid and gas service that have been designated by the Permittee to be in organic hazardous air pollutant light liquid/gas service for 300 or more hours per year. [62-204.800(11)(b), F.A.C.] [40 CFR 63.174]	The Permittee shall inspect and repair connectors according to the criteria specified in 40 CFR 63.174. [62-204.800(11)(b), F.A.C.] [40 CFR 63.174]	Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i) and (ii), (b)(5), (b)(7), and (d). Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [62-204.800(11)(b), F.A.C.] [40 CFR 63.181 and 63.182]
EU 036	Methylamines Plant No. 1 and No. 4 HON Equipment Leaks	Sampling Points. The Permittee shall meet the criteria set forth in 40 CFR 63.166 for sampling points in organic hazardous service that have been designated by the Permittee to be in organic hazardous air pollutant service for 300 or more hours per year. [62-204.800(11)(b), F.A.C.] [40 CFR	Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent system. Gases displaced during filling of the sample container are not required to be collected or captured. Each sampling system shall meet one of the specifications specified in 40 CFR 63.166(b). [62-204.800(11)(b), F.A.C.][40 CFR 63.166]	<ul> <li>The Permittee shall maintain records specified in 40 CFR 63.181(b)(1)(i) and no periodic reporting shall be required.</li> <li>[62-204.800(11)(b), F.A.C.][40 CFR 63.181]</li> </ul>

		63.166]		
EU 037	Methylamines Plant No. 4 VOC Equipment Leaks	Pressure relief devices.The Permitteeshall comply with the requirements setforth in 40 CFR 63.165 for pressurerelief devices in gas/vapor service.The Permittee shall comply with therequirements set forth in 40 CFR63.169 for pressure relief devices inlight liquid service.Pressure relief devices that are routed toa process or fuel gas system areexempt.[Rule 62-204.800 (11)(b), F.A.C.; 40 CFR63.165 and 63.169]	<u>Pressure relief devices</u> . After pressure releases from pressure relief valves, the pressure relief device shall be returned to less than 500 ppmv above background, as confirmed by the method specified in 40 CFR 63.180(c), as soon as practicable, but no later than 5 days after the release. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR 63.165 and 63.180(c)]	Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i), 63.181(b)(3), and 63.181(d). Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR 63.181 and 63.182(d)]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 037	Methylamines Plant No. 4 VOC Equipment Leaks	<u>Open-ended valves or lines</u> . The Permittee shall comply with requirements set forth in 40 CFR 63.167 for open-ended lines that have been designated by the Permittee to be in organic hazardous air pollutant service for 300 or more hours per year. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR 63.167] <u>Valves</u> . The Permittee shall comply	<u>Open-ended valves or lines</u> . Each open-ended valve or line shall be equipped with a cap, blind flange, plug, or a second valve. The Permittee shall also comply with work and operating practices specified in 40 CFR 63.167(a)(2), (b) and (c). [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR63.167(a)(2), (b) and (c)] <u>Valves</u> . The Permittee shall inspect and repair valves in	Open-ended valves or lines. Records shall be maintained in accordance with 40 CFR 63.181(b) and 63.181(d). Periodic reports containing relevant information specified in 40 CFR 60.487(c) shall be submitted to the Department. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR 60.486] <u>Valves</u> . Records shall be maintained
EU 037	Methylamines Plant No. 4 VOC Equipment Leaks	with the requirements set forth in 40 CFR 60.482-7 for valves in light liquid or gas/vapor service. [Rule 62-204.800 (11)(b) F.A.C.; 40 CFR 63.168]	light liquid or gas/vapor service according to the criteria specified in 40 CFR 63.168. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR63.168]	<ul> <li>in accordance with 40 CFR</li> <li>63.181(b)(1)(i and ii). Records shall also be maintained in accordance with 40 CFR 63.181 (7 and 8) for every valve subject to the requirements of §63.168(g and h). Periodic reports containing relevant information specified in 40 CFR</li> <li>63.182(d) shall be submitted to the Department.</li> <li>[Rule 62-204.800 (11)(b), F.A.C.; 40 CFR63.168, 63.181, 63.182(d)]</li> </ul>
EU 037	Methylamines Plant No. 4 VOC Equipment Leaks	<u>Flanges and Connectors</u> . The Permittee shall comply with the requirements set forth in 40 CFR 63.174 for flanges and connectors. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR 63.174]	Connectors. The Permittee shall inspect and repair connectors according to the criteria specified in 40 CFR 63.174. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR63.174]	<u>Connectors</u> Records shall be maintained in accordance with 40 CFR 63.181(b)(1)(i and ii), 63.181(b)(5,7, and 8) and 63.181(d). Periodic reports containing relevant information specified in 40 CFR 63.182(d) shall be submitted to the Department. [Rule 62-204.800 (11)(b), F.A.C.; 40 CFR 63.181 and 63.182(d)]

EU 037	Methylamines Plant No. 4	Sampling Points. The Permittee shall meet the criteria set forth in 40 CFR	Sampling Points. Each sampling connection system shall be equipped with a closed-purge, closed-loop, or closed-vent	
	VOC	63.166 for sampling points.	system. Each sampling system shall meet one of the	
	Equipment Leaks	[Rule 62-204.800 (11)(b),	specifications specified in 40 CFR 63.166(b).	
		F.A.C.; 40 CFR63.166]	[Rule 62-204.800(11)(b), F.A.C.; 40 CFR63.166]	

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 037	Methylamines Plant No. 4 VOC Equipment Leaks		<ul> <li>Testing. The owner or operator shall test each piece of equipment in accordance with 60.485a(d) unless he demonstrates that a process unit is not in VOC service, i.e., that the VOC content would never be reasonably expected to exceed 10 percent by weight.</li> <li>[Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.486a(d)]</li> <li>Testing. The owner or operator shall demonstrate that a piece of equipment is in light liquid service by demonstrating that the conditions in 60.485a(e) apply.</li> <li>[Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.486a(e)]</li> <li>(f) Samples used in conjunction with 60.486a(d), (e), and (g) shall be representative of the process fluid that is contained in or contacts the equipment or the gas being combusted in the flare.</li> <li>[Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.486a(f)]</li> </ul>	Components Not in VOC Service. The Permittee shall maintain records specified in 40 CFR         60.486a(i and j) for any equipment considered not in VOC service.         [Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.486a(i and j)]         Performance Test Reporting. The Permittee shall report the results of all performance tests in accordance with 40 CFR 63.182(c).         [Rule 62-204.800(11)(b), F.A.C.; 40 CFR 63.182(c)]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 071	DIMLA MON Maintenance Wastewater	The Permittee shall prepare a description of maintenance procedures for management of wastewaters containing those organic HAPs listed in Table 8 or Table 9 of 40 CFR Subpart FFFF which are generated from the emptying and purging of equipment in the process during temporary shutdowns for inspections, maintenance, and repair (i.e., a maintenance-turnaround) and during periods which are not shutdown (i.e., routine maintenance). The descriptions shall: (1) specify the process equipment or maintenance tasks that are anticipated to create wastewater during maintenance activities, (2) specify procedures that will be followed to properly manage the wastewater and control organic HAP emissions to the atmosphere, and (3) specify the process equipment. The Permittee shall modify and update the maintenance procedures as needed. [62-204.800(11)(b), F.A.C.] [40 CFR 63.105(b) referenced by 40 CFR 63.2485(a) and (b)]	<ul> <li>The Permittee shall maintain a record of the required information as part of the startup, shutdown, and malfunction plan required under 40 CFR 63.6(e)(3).</li> <li>Plans shall be maintained and kept readily_available for inspection for the life of the source, or until 40 CFR Part 63 standards no longer apply to the source. No notification or periodic reporting of maintenance wastewater activities is required.</li> <li>[62-204.800(11)(b), F.A.C.] [40 CFR 63.105(d) referenced by 40 CFR 63.2485(a) and (b)]]</li> </ul>	See requirements specified in "Compliance Testing/Demonstration Requirement(s)" column.

EU 072	DIMLA MON Wastewater	Permittee shall comply with the requirements in 63.132 through 63.148 and the requirements referenced therein, except as specified in 63.2485. The compounds in table 8 and 9 of Subpart FFFF apply. Permittee shall comply with the requirements in 40 CFR 63.132(a)(1) through (a)(3), except as specified in 63.2485(c), which requires that Permittee determine whether each wastewater stream is Group 1 or Group 2 stream. For Group 2 streams, Permittee shall comply with recordkeeping requirements of 40 CFR 63.1467(b)(8)(i) through (iv).	Permittee shall maintain records of all Group 1/Group 2 determinations, and the Notification of Compliance Status available for Department inspection. [62-204.800(11)(b), F.A.C.] [40 CFR 63.152(f) and 40 CFR 63.2485]
		[62-204.800(11)(b), F.A.C.] [40 CFR 63.2485]	

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 077	DIMLA MON Equipment Leaks	Standards for Equipment Leak Detection. The permittee shall comply with the following equipment leak standards as applicable:	Compliance Tests. Compliance tests shall be conducted using instruments or sensory methods as specified in the standards for instrument and sensory monitoring for leaks specified in 40 CFR 63.1023. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1023 referenced by 40 CFR 63.2480]	Reporting Requirements. For the equipment specified in the "Compliance Testing/Demonstration Requirement(s)" column, the permittee shall report in a summary format by equipment type, the
		Standards for Valves in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1025 referenced by 40 CFR 63.2480]	Test Methods. Required tests shall be performed in accordance with the following reference methods.21 and sensory.	number of components for which leaks were detected and for valves, pumps and connectors show the percent leakers, and the total number of components
		<ul> <li>Standards for Pumps in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1026 and 63.1035 referenced by 40 CFR 63.2480]</li> <li>Standards for Connectors in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1027</li> </ul>	Monitoring shall comply with Method 21 of 40 CFR part 60, Appendix A, as specified by, and, except as otherwise provided in 40 CFR 63.1023. The above methods are described in 40 CFR 60, Appendix A, and adopted by reference in Rule 62-204.800, F.A.C. No other methods may be used unless prior written approval is received from the Department. [Rule 62-204.800, F.A.C.] Equipment to be Monitored. The permittee shall monitor the	monitored. Also include the number of leaking components that were not repaired as required by 40 CFR 63.1024, and for valves and connectors, identify the number of components that are determined by 40 CFR 63.1025(c)(3) to be nonrepairable. [Rule 62-204.800(11).
		referenced by 40 CFR 63.2480] Standards for Agitators in gas and vapor service and in light liquid service. [Rule	equipment comprising this emissions unit routinely as follows:	F.A.C.; 40 CFR 63.1039(b) referenced by 40 CFR 63.2480]
		62-204.800(11), F.A.C.; 40 CFR 63.1028 referenced by 40 CFR 63.2480]	Valves in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1025(b) and (c) referenced by 40 CFR 63.2480]	Reports. Periodic compliance reports required by 40 CFR 63.2520(d) shall be
		Standards for Pumps, Valves, Connectors, and Agitators in heavy liquid service; pressure relief devices in liquid service;	Pumps in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1026(b)-(e) referenced by 40 CFR 63.2480]	submitted semiannually according to the schedule specified in 40 CFR 63.2520(b) as follows:
		and instrumentation systems. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1029 and 63.1035 referenced by 40 CFR 63.2480]	Connectors in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1027(b) and (c) referenced by 40 CFR 63.2480]	Each subsequent compliance report must cover the semiannual reporting period from January 1 through June 30 or the
		Standards for Pressure relief devices in gas and vapor service. [Rule 62-204.800(11), F A C : 40 CFR 63 1030 referenced by 40	Agitators in gas and vapor service and in light liquid service. [Rule 62-204.800(11), F.A.C.; 40 CFR 63.1028(c) referenced by 40 CFR 63 2480]	semiannual reporting period from July 1 through December 31.
		CFR 63.2480] Standard for Compressors standards. [Rule	Pumps, valves, connectors, and agitators in heavy liquid	Each subsequent compliance report must be postmarked or delivered no later than August 31 or February 28, whichever

Permit No. 1130004-046-AV

Title V Air Operation Permit Renewal





EU 078	DIMLA VOC	Pressure relief devices. The Permittee shall	Pressure relief devices. After pressure releases from pressure	Records shall be maintained in
	Equipment Leaks	comply with the requirements set forth in	relief valves, the pressure relief device shall be returned to	accordance with 40 CFR486a(b)(1) and
		40 CFR 60.482-4a for pressure relief	less than 500 ppmv above background, as confirmed by the	(c).
		devices in gas/vapor service. The Permittee	method specified in 40 CFR 60.485a, as soon as practicable,	Periodic reports containing relevant
		shall comply with the requirements set	but no later than 5 days after the release.	information specified in 40 CFR
		forth in 40 CFR 482-8a for pressure relief	[Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.482-4a(b)	60.487a(c) shall be submitted to the
		devices in light liquid service.	and 60.485a]	Department.
		Pressure relief devices that are routed to a		[Rule 62-204.800(8)(b)(54), F.A.C.; 40
		process or fuel gas system are exempt.		CFR 60.486a]]
		[Rule 62-204.800(8)(b)(54), F.A.C.; 40		
		CFR 60.482-4a]]		

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 078	DIMLA VOC Equipment Leaks	<u>Open-ended valves or lines</u> . The Permittee shall comply with requirements set forth in 40 CFR 60.482-6a for open-ended lines that have been designated by the Permittee to be in organic hazardous air pollutant service for 300 or more hours per year. [Rule 62-204.800(8)(b)(54), F.A.C.: 40 CFR 60.482-6a]	<u>Open-ended valves or lines</u> . Each open-ended valve or line shall be equipped with a cap, blind flange, plug, or a second valve. The Permittee shall also comply with work and operating practices specified in 40 CFR 60.482- 6a(a)(2), (b), and (c). [Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.482-6a]	Open-ended valves or lines. Periodic reports containing relevant information specified in 40 CFR 60.487a(c) shall be submitted to the Department. [Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.486a]
EU 078	DIMLA VOC Equipment Leaks	Valves. The Permittee shall comply         with the requirements set forth in 40         CFR 60.482-7a for valves in light         liquid or gas/vapor service.         [Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR         60.482-7a]	Valves.The Permittee shall inspect and repair valves in light liquid or gas/vapor service according to the criteria specified in 40 CFR 60.482-7a.The Permittee may elect to reduce the frequency of inspection in accordance with 40 CFR 60.483-2a(b) after providing the Department with the appropriate notification as defined in 40 CFR 60.483-2a(a) and 487a(b).The Permittee shall inspect and repair valves in heavy liquid service according to the criteria specified in 40 CFR 60.482-8a[Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.482-7a, 60.482-8a and 60.483-2a]	Valves.Records shall bemaintained in accordance with40 CFR 60.486a(b)(1) and (c).Records shall also be maintainedin accordance with 40 CFR60.486a(f) for every valve subjectto the requirements of § 60.482-7a(g) and (h).Periodic reportscontaining relevant informationspecified in 40 CFR 60.487a(c)shall be submitted to theDepartment.[Rule 62-204.800(8)(b)(54)F.A.C.; 40 CFR 60.486a]
EU 078	DIMLA VOC Equipment Leaks	<u>Flanges and Connectors</u> . The Permittee shall comply with the requirements set forth in 40 CFR 60.482-8a for flanges and connectors. [Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.482-8a]	<u>Connectors</u> . The Permittee shall inspect and repair connectors according to the criteria specified in 40 CFR 60.482-8a. [Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR60.482-8a]	<u>Connectors</u> Records shall be maintained in accordance with 40 CFR 60.486a(b)(1) and (c). Periodic reports containing relevant information specified in 40 CFR 60.487a(c) shall be submitted to the Department. [Rule 62-204.800(8)(b)(54) F.A.C.; 40 CFR 60.486a]

EU 078	DIMLA VOC	<u>Sampling Points</u> . The Permittee shall	Sampling Points. Each sampling connection system shall be	
	Equipment Leaks	meet the criteria set forth in 40 CFR	equipped with a closed-purge, closed-loop, or closed-vent	
		60.482-5a for sampling points.	system. Each sampling system shall meet one of the	
		[Rule 62-204.800(8)(b)(54),	specifications specified in 40 CFR 60.482-5a(b).	
		F.A.C.; 40 CFR 60.482-5a]	[Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR60.482-5a]	



		[Rule 62-204.800(8)(b)(54), F.A.C.; 40 CFR 60.487a]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU 079	DIMLA Scrubber	The DIMLA scrubber shall be operated with a minimum water flow of 1 GPM based on a 24-hr block average [midnight to midnight], excluding periods of non-operation of the source. [F.A.C.; Rules 62-210.200PTE and 62-4.070(3)]	<ul> <li><u>Bypass Monitoring:</u> Except for equipment needed for safety purposes such as pressure relief devices, low leg drains, high point bleeds, analyzer vents, and open-ended valves or lines, the owner or operator shall comply with one of the follow for each closed vent system that contains bypass lines that could divert a vent stream to the atmosphere: <ul> <li>(1) Properly install, maintain, and operate a flow indicator that is capable of taking readings at least once every 15 minutes. The flow indicator shall be installed at the entrance to any bypass line. [40 CFR 63.983(a)(3)(i) and (b)(4)(i), referenced by 40 CFR 63.2450(e) via 63.982(c)]</li> </ul> </li> <li>(2) Secure the bypass line valve in the non-diverting position with a car-seal or lock-and-key type configuration and visually inspect the seal or closure mechanism at least monthly to verify that the valve is maintained in the non-diverting position, and the vent stream is not diverted through the bypass line. [40 CFR 63.983(a)(3)(ii) and (b)(4)(ii), referenced by 40 CFR 63.982(c)]</li> </ul>	Bypass monitoring records: The Permittee shall maintain the records specified in 40 CFR 63.998(d)(1)(ii)A or B, as appropriate to document that the DIMLA scrubber is not bypassed. [40 CFR 63.983(a)(3), referenced by 40 CFR 63.2450(e) via 63.982(c)]
EU 079	DIMLA Scrubber			Leak Repair Records: The Permittee shall maintain leak detection and repair records for the piping connecting the DIMLA Purification Tower overhead vacuum system discharge to the DIMLA Scrubber as specified in 40 CFR 63.998(d)(1)(iii)(A)-(F). These records shall be maintained for five years. [40 CFR 983(a)(3), referenced by 40 CFR 63.2450(e) via 63.982(c)]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU080	Five Emergency Reciprocating Internal Combustion Engines (RICE) <sup>a</sup>	Hours of Operation. Operate for the purpose of maintenance checks and readiness testing, provided that the tests are recommended by Federal, State or local government, the manufacturer, the vendor, or the insurance company associated with the engine. Limit maintenance checks and readiness testing to 100 hours per year. Operate up to 50 hours per year in non- emergency situations, but count those 50 hours towards the 100 hours per year provided for maintenance and testing per 40 CFR 63.6640(f)(2) and (3). For owners and operators of emergency engines, any operation other than emergency operation, maintenance and testing, and operation in non-emergency situations for 50 hours per year is prohibited. [[40 CFR 60.4243(d) and 62- 210.200(PTE), F.A.C.]	Install a non-resettable hour meter. [40 CFR 63.6625(f)] Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes. [40 CFR 63.6602 and 63.6625(h)]	Keep records of the hours of operation of the engine that is recorded through the non- resettable hour meter. Document how many hours are spent for emergency operation, including what classified the operation as emergency and how many hours are spent for non- emergency operation. [40 CFR 63.6655(f)]

Permit Section / EU No.	Description	Condition/Limitation	Compliance Testing/Demonstration Requirement(s)	Recordkeeping/ Reporting Requirement(s)
EU080	Five Emergency Reciprocating Internal Combustion Engines <sup>a</sup>	<ul> <li><u>Emission Limits and Standards</u>: Comply with the applicable emission limitations and operating limitations in Table 2C to 40 CFR Subpart ZZZZ which apply to emergency stationary CI RICE.</li> <li>Change oil and filter every 500 hours of operation or annually, whichever comes first.</li> <li>Inspect air cleaner every 1,000 hours of operation or annually, whichever comes first.</li> <li>Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary.</li> <li>Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes. [40 CFR 63.6602]</li> </ul>	NA	Keep records of the maintenance conducted on the stationary RICE in order to demonstrate that you operated and maintained the stationary RICE and after-treatment control device (if any) according to your own maintenance plan if you own or operate any of the following stationary RICE Keep records of the occurrence and duration of each malfunction of operation (i.e., process equipment) or the air pollution control and monitoring equipment (if any) Keep records of all required maintenance performed on the air pollution control and monitoring equipment Keep records of actions taken during periods of malfunction to minimize emissions in accordance with §63.6605(b), including corrective actions to restore malfunctioning process and air pollution control and monitoring equipment to its normal or usual manner of operation. [40 CFR 63.6655(a)(2, 4, and 5) and 63.6655(e) and (f)] Report each instance in which you did not meet each operating limitation in Table 2c. [63.6640(b), 63.6650]

EU081	New	Firewater pump shall comply with all	Operate for the purpose of maintenance checks and	The Permittee must keep records of the
	Emergency	applicable requirements of 40 CFR	readiness testing checks to 100 hours per year. Emergency	operation of the engine in emergency
	Reciprocating	60.4205(c) for the same model year and	operation does not have a limit but non-emergency hours	and non-emergency service that are
	Internal	maximum engine power as per Table 4.	shall be limited to 50 hours per year and are counted as part	recorded through the non-resettable
	Combustion	[62-204.800(8)(b)82., F.A.C., 40 CFR	of the 100 hours per calendar year for maintenance and	hour meter. The owner must record the
	Engine <sup>b</sup>	60.4205(c)]	testing.	time of operation of the engine and the
		Use only diesel fuel that meets the	[62-204.800(8)(b)82., F.A.C., 40 CFR 60.4211(f)]	reason the engine was in operation
		requirements of 40 CFR 80.510(b) for	Change only those emission-related settings that are	during that time.
		non-road diesel fuel.	permitted by the manufacturer.	[Rule 62-204.800(8), F.A.C. and 40
		[62-204.800(8)(b)82., F.A.C., 40 CFR	[62-204.800(8)(b)82.,	CFR 60.4214(b)]
		60.4207(b)]		
		Compliance with all applicable	F.A.C., 40 CFR	
		requirements of 40 CFR 60 Subpart IIII	60 4211(a)]	
		has been determined to be compliance	00.1211(d)]	
		with all applicable requirements of		
		Subpart ZZZZ.		
		[62-204.800(11)(b)82., F.A.C., 40		
		CFR 63.6590(c)]		

Notes: In the case of conflict between this table and the permit, the permit shall take precedence over the table

<sup>a</sup> Existing Emergency Reciprocating Internal Combustion Engines: B-area emergency fire water pump and No. 2 well water pump (each at 234 hp), plant emergency generator (330 hp), and south foxtrot (340 hp)

<sup>b</sup> New Emergency Reciprocating Internal Combustion Engine: main fire water pump (268 hp)

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#### FIGURE 2 **PROJECT EMISSIONS INCREASE REPORT – EXAMPLE FORMAT**

Emissions Year\*: (This is year No. of  $\Box 5$  or  $\Box 10$  required reports.)

Facility Information					
ARMS	ARMS ID No. Facility/Site Name:				
		Air Construction	Permit Informa	ation	
Perm	nit No.	Date Issued:	Date Construction	on Completed: Date Regular Operation Resumed:	
EU ID No.	]	EU Description	EU ID No.	EU Description	

Tracked			Annual Emissions, Tons per Year			PSD? Yes/No <sup>6</sup>
PSD Ponutant	RAE <sup>1</sup>	DG <sup>2</sup>	BAE <sup>3</sup>	Increase <sup>4</sup>	SER <sup>5</sup>	

Report Deadline: This report must be submitted to the Compliance Authority within 60 days after the end of each calendar year during which records must be generated under subparagraph 62-212.300(1)(e)1., F.A.C.

"RAE" means reported annual emissions for the given year (or PAE for year zero). 1.

- "DG" means the annual emissions resulting from production demand growth that could have been accommodated during 2. the baseline years and that are unrelated to the project. Please provide supporting information and a discussion that describes: how the emissions were related to demand growth, how the emissions could have been accommodated previously and how the emissions are unrelated to the project. This will not change from year to year.
- 3. "BAE" means baseline actual emissions as determined in the original air construction permit. BAE will remain the same for each reporting year.
- "Increase" is the annual emissions increase related to the project (Increase = RAE DG BAE). 4.
- "SER" means the "significant emissions rate" as defined for the PSD pollutant in Rule 62-210.200, F.A.C. 5.
- If RAE-DG-BAE is greater than the "SER", then the project is subject to PSD preconstruction review as though 6. construction had not yet commenced. **A** Back to Table of Contents

Title V Air Operation Permit Renewal Permit No. 1130004-046-AV

# APPLICANT

The applicant for this project is Taminco US LLC. The applicant's responsible official and mailing address are: Shane Fowler, Site Manager, Taminco US LLC, Taminco Pace Plant, 4575 Highway 90 East, Pace, Florida 32571-0467.

# FACILITY DESCRIPTION

The applicant operates the existing Taminco Pace Plant, which is located in Santa Rosa County at 4575 Highway 90 East, Pace, Florida.

Taminco Pace Plant is an existing Chemical Processing Plant, which is categorized under Standard Industrial Classification Code No. 2869. The existing Taminco Pace Plant is comprised of five chemical manufacturing units. Plant Nos. 1 and 4 produce methylamines; Plant No. 2 produces a variety of higher amines, including alkylamines and amylamines; Plant No. 3 processes higher amines; and the DIMLA Plant produces dimethyl laurylamine (DIMLA12), dimethyl myristylamine (DIMLA14), dimethyl hexadecylamine (DIMLA16) and a blend of DIMLA12, DIMLA14 and/or DIMLA16 (e.g. DIMLA1214). The Utilities area contains two boilers and three cogeneration units. The cogeneration units are owned by Florida Power & Light Company but operated by Taminco and permitted separately under Facility ID No. 1130173.

### Methylamines Plant Nos. 1 and 4

At Methylamines (MA) Plants Nos. 1 and 4, methanol is continuously reacted with ammonia to yield methylamines. A natural gas-fired preheater is used to reach reaction temperature. Volatile off-gases from the low-pressure absorbers are controlled with the Amines Plants Flare (EU 005) or the boilers (EU 001 and EU 003). Process gases from the high-pressure absorber vents can be routed to the boilers or to the Amines Plants Flare. Visible emissions from the gas-fired heater and the flare are controlled by proper combustion. Wastewater generated is treated in the wastewater treatment system.

# Higher Amines Plant Nos. 2 and 3

At Higher Amines Plants Nos. 2 and 3, alcohols, ammonia, ethers, aldehydes, ketones and other amines are reacted to yield various alkylamines and amylamines. A natural gas-fired preheater is used to bring the mixture to reaction temperature. The volatile off-gases from the low-pressure absorbers are controlled by the Amines Plants Flare or the boilers. Process gases from the high-pressure absorber vent in Higher Amines Plant No. 2 can be routed to the boilers or to the Amines Plants Flare. Visible emissions from the gas-fired heater and the flare are controlled by proper combustion. Wastewater generated is treated in the wastewater treatment system.

#### **Amines Plants Flare**

The Amines Plants Flare is a non-assisted flare with a natural gas pilot. Off-gases from the product absorbers at MA Plants, the Higher Amines Plants and the DIMLA Plant, as well as other process vents at the facility, are continuously released to the flare for destruction. An infra-red and a flame strength camera are utilized to continuously monitor the flame. The flame strength will alarm the control room operator if the flame goes out. The flare pilot will not relight itself. An alarm delay is built into the computer logic to avoid false alarms during brief instances when weather conditions may disrupt the flame viewed by the camera. Natural gas is fed with process gas in a ratio of 0.3:1 for streams that do not have direct BTU measurement to ensure that the minimum net heating value of gas being combusted by the flare is maintained, and a high flow alarm on the gas flow to the flare ensures that the maximum allowable flare exit velocity is not exceeded.

# **DIMLA Plant**

At the DIMLA Plant, Dimethyl Laurylamine is manufactured from a C12 alcohol (lauryl alcohol), a C14 alcohol (myristyl alcohol), a C16 straight chain alcohol (Hexadecyl alcohol) or a mixture of the C12, C14, and/or C16

alcohols. The alcohol feed (ROH) is reacted with dimethylamine (DMA) in a catalyzed reaction with hydrogen present. Vent streams from the amines absorption column, the amines reactor and the amines desorption column are sent to the low-pressure absorber in the MA Plant No. 1 or in the MA Plant No. 4 or directly to the flare header. Wastewater from the amines desorption column can go to the wastewater treatment system. The water phase from the decanters is also sent to the wastewater treatment system via the wastewater recycle tank TK-62057 or the wastewater tank TK-62099. Residue from the ROH evaporator and a portion of the DIMLA purification column residue are sold or disposed of offsite. Off-gases from the vacuum system are recovered using an atmospheric scrubber that feeds the amines absorption column.

# Boilers

The Riley Stoker boiler (EU 001) and B&W boiler (EU 003) are designed to burn natural gas and off gases from the amines and dimethyl laurylamine processes. The vent gases are fed through annular burners with natural gas to ensure complete combustion. Each boiler is designed for a maximum firing rate of 130 million British thermal units per hour (MMBtu/hr) and is capable of producing about 90,000 pounds per hour (lb/hr) of 600 pounds per square inch gauge (psig) steam. Flue Gas Recirculation (FGR) has been added to the Riley Stoker boiler for control of NOx emissions. An estimated 50% control of NOx is expected; however, the Riley Stoker Boiler is not required to operate the FGR to stay in compliance because emissions calculations were done without taking the FGR NOx reduction into account.

Florida Power & Light Company owns three cogeneration units located within the Taminco Pace Plant boundaries. Taminco personnel operate the units, but the Florida Power & Light Company maintains compliance with a separate Title V air operation permit under Facility No. 1130173.

# **Reciprocating Internal Combustion Engines**

The Taminco Pace Plant operates four *existing* stationary emergency, diesel fueled, compression ignition, reciprocating internal combustion engines (CI RICE):

Equip. I.D.	Area/Location	Existing or New	Construction Commenced Date	Brake hp	Fuel Type
PG24101C	B-Area well water pump	Existing	04/19/1994	234	Diesel
PG24101B	No. 2 well water pump	Existing	04/06/1994	234	Diesel
D24018	Plant emergency generator	Existing	06/07/1991	330	Diesel
PG24121	South Foxtrot fire water pump	Existing	04/15/1994	340	Diesel

These engines are *existing* stationary reciprocating internal combustion engines [per 40 CFR 63.6590(a)(1)(ii)] with a rating of less than 500 brake horsepower (Hp), located at a major source of hazardous air pollutants (HAP) and constructed before June 12, 2006. These stationary CI RICE are subject to 40 CFR 63, Subpart ZZZZ, National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines and must comply with the applicable emission limitations in Table 2c to 40 CFR 63, Subpart ZZZZ for Emergency Stationary CI RICE.

Taminco also operates one *new* stationary emergency, diesel fueled, compression ignition, reciprocating internal combustion engine:

Equip. I.D.	Area/Location	Existing or New	Construction Commenced Date	Brake hp	Fuel Type
PG24114	Main fire water pump	New	06/2016	268	Diesel

This new CI RICE is regulated by 40 CFR 60, Subpart IIII, Standards of Performance for Stationary Compression Ignition Internal Combustion Engines. The fire pump engine is a "new" stationary emergency CI RICE with a displacement of less than 30 liters per cylinder, located at a major source of HAP, commenced construction on or after 6/12/2006, and has a post-2007 model year.

# **REGULATED EMISSIONS UNIT IDENTIFICATION NUMBERS AND DESCRIPTIONS**

EU No.	Brief Description
Regulated	Emissions Units
, in the second s	Methanol Storage:
029	Methylamines Plants Nos. 1 and 4 HON Group 1 Storage Tanks (Methanol)
047	Methanol Storage HON Maintenance Wastewater
048	Methylamines Plants Sample Points (HON)
	Boilers:
001	Riley Stoker Boiler
003	B & W Boiler
	Methylamines Plant No. 1:
005	Amines Plants Flare
006	Methylamines Plant No. 1 Gas Fired Heater
036	Methylamines Plants Nos. 1 and 4 HON Equipment Leaks
046	Sitewide HON Heat Exchangers
049	Methylamines Plant No. 1 Process Vents
050	Methylamines Plant No. 1 Wastewater
051	Methylamines Plant No. 1 HON Maintenance Wastewater
054	Methylamines Plants Nos. 1 and 4 NSPS Storage Tanks
	Higher Amines Plants:
007	Higher Amines Plant No. 2 Gas-Fired Heater
055	72-inch Batch Column Process Vent
056	72-inch Batch Column Maintenance Wastewater
059	72-inch Batch Column Wastewater
070	Higher Amines Plant Process Vents
- (0	Methylamines Plant No. 4:
060	Methylamines Plant No. 4 Gas-Fired Heater
033	Methylamines Plant No. 4 Process Vents
034	Methylamines Plant No. 4 Wastewater
035	Methylamines Plant No. 4 HON Maintenance Wastewater
037	Methylamines Plant No. 4 VOC Equipment Leaks
053	Methylamines Plants Nos. 1 and 4 HON Group 2 Storage Tanks
050	DIMLA Plant:
058	DIMLA MON Group 2 Storage Tanks
071	DIMLA MON Maintenance Wastewater
072	DIMLA MON Wastewater
077	DIMLA MON Equipment Leaks
070	DIMLA VOC Equipment Leaks
0/9	
080	Plant Wide:
080	Existing Emergency Reciprocating Internal Combustion Engines (Defore 2000)
U01	New Emergency Reciprocating internal Combustion Engine (After 2007)
Unregulate	ed Emissions Units and Activities (see Appendix U, List of Unregulated Emissions Units and/or Activities)
062	Facility-Wide Equipment Leak Fugitives
063	Cooling Towers (4) (that do not use chromium-based water treatment chemicals)
075	Wastewater Treatment Plant Fugitives
076	DIMLA Storage Tanks and Loading

Also included in this permit are miscellaneous insignificant emissions units and/or activities (see Appendix I, List of Insignificant Emissions Units and/or Activities).

# **APPLICABLE REGULATIONS**

Based on the Title V air operation permit renewal application received on February 24, 2025, this facility is a major source of hazardous air pollutants (HAP). The existing facility is a prevention of significant deterioration (PSD) major source of air pollutants in accordance with Rule 62-212.400, F.A.C. A summary of applicable regulations is shown in the following table:

Regulation	EU No(s).
Federal Rule Cit	rations
40 CFR 60, Subpart A, NSPS General Provisions	005, 054
40 CFR 60, Subpart Kb, NSPS for Volatile Organic Liquid Storage Vessels After July 23, 1984	054
40 CFR 60, Subpart VVa, NSPS for Equipment Leaks of VOC After November 7, 2006	037, 078
40 CFR 60, Subpart IIII, Standards of Performance for Stationary CI RICE	081
40 CFR 63, Subpart A, NESHAP General Provisions	005, 029
40 CFR 63, Subpart F, NESHAP for the Synthetic Organic Chemical Manufacturing Industry	005, 029, 033, 034, 035, 046, 047, 049, 050, 051, 053
40 CFR 63, Subpart G, NESHAP for Process Vents-Stg Vessels- Transfer Ops-Wastewater	005, 029, 033, 034, 035, 046, 047, 049, 050, 051, 053
40 CFR 63, Subpart H, NESHAP for Equipment Leaks	005, 036, 037, 048
40 CFR 63, Subpart SS	005
40 CFR 63, Subpart FFFF, NESHAP for Miscellaneous Organic Chemical Manufacturing	005, 058, 071, 072, 077, 079
40 CFR 63, Subpart ZZZZ, NESHAP for Stationary Reciprocating Internal Combustion Engines	080
40 CFR 63, Subpart DDDDD, NESHAP for Boilers and Process Heaters	001, 003, 006, 007, 060
State Rule Cita	tions
Rule 62-210.200(Definitions), F.A.C.	Facility-Wide
Rule 62-210.370, F.A.C., Emissions Computation and Reporting	Facility-Wide
Rule 62-210.900, F.A.C., Forms and Instructions	Facility-Wide
Rule 62-212.400(12), F.A.C., Source Obligation	Facility-Wide
Rule 62-213.205, F.A.C., Annual Emissions Fee	Facility-Wide
Rule 62-296.320(1), (2) & (4), F.A.C., General Pollutant Emission Limiting Standards	Facility-Wide
Rule 62-210.370(3), F.A.C., Annual Operating Report (AOR)	Facility-Wide
Rule 62-213.440, F.A.C., Permit Content	Facility-Wide
Rule 62-210.300(2)(a), F.A.C., Minimum Requirements for All Air Operation Permits	001, 003
Rule 62-210.700, F.A.C., Excess Emissions	054
Rule 62-212.300(1)(e), F.A.C., Actual Emissions Recordkeeping and Reporting Requirements	029, 001, 003

## STATEMENT OF BASIS

Regulation	EU No(s).
Rule 62-213.440(1), F.A.C., Standard Permit Requirements	029, 001, 003, 006, 007, 060
Rule 62-4.070(3), F.A.C., Reasonable Assurance	029, 001, 003, 005, 006, 007, 035, 058, 060, 077, 078, 079
Rule 62-204.800, F.A.C., Compliance Assurance, Standards Adopted: NSPS and NESHAP	001, 003, 005, 006, 007, 029, 033, 034, 035, 036, 037, 046, 047, 048, 049, 050, 051, 053, 054, 058, 060, 071, 072, 077, 078, 079, 080
Rule 62-296.406(1), F.A.C., Visible Emissions Requirement for Fossil Fuel Steam Generators with Less Than 250 Million Btu Per Hour Heat Input	001, 003
Rule 62-297.310, F.A.C., General Emissions Test Requirements	001, 003

### **Definitions:**

'<u>HON</u>' is an abbreviation for Hazardous Organic NESHAP (National Emission Standards for Hazardous Air Pollutants).

'MON' is an abbreviation for Miscellaneous Organic NESHAP.

'<u>Group 1 wastewater stream</u>' means a wastewater stream consisting of process wastewater at an existing or new source that meets the criteria for Group 1 status in 40 CFR 63.2485(c) for compounds in Tables 8 and 9 of 40 CFR 63, Subpart FFFF and/or a wastewater stream consisting of process wastewater at a new source that meets the criteria for Group 1 status in 40 CFR 63.132(d) for compounds in Table 8 of 40 CFR 63, Subpart G.

'Group 2 wastewater stream' means any process wastewater stream that does not meet the definition of a Group 1 wastewater stream.

'<u>The MON Rule</u>': 40 CFR 63, Subpart FFFF, National Emissions Standards for Hazardous Air Pollutants, applies to new and existing Miscellaneous Organic Chemical (MON) manufacturers. This regulation indicates that all pressure relief devices (PRDs) in HAP service (except as specified in in <u>paragraphs (e)(4)</u> and <u>(5)</u> of 40 CFR 63.2480) must be equipped with a monitoring device by August 12, 2023.

The regulation applies to all existing and new Miscellaneous Organic Chemicals manufacturing process units that have the possibility of emitting Hazardous Air Pollutants. The list of HAPs emitted from the DIMLA MON manufacturing facility includes (but is not limited to) methanol and formaldehyde.

# **PROJECT DESCRIPTION**

The purpose of this permitting project is to renew the existing Title V permit for the above referenced facility. This project renews Title V air operation permit No. 1130004-035-AV, which was effective on January 21, 2021.

# PROCESSING SCHEDULE AND RELATED DOCUMENTS

Renewed Title V Air Operation Permit issued January 21, 2021 Revised Title V Air Operation Permit issued September 21, 2021 Revised Title V Air Operation Permit issued December 2, 2022 Revised Title V Air Operation Permit issued August 6, 2024 Application for a Title V Air Operation Permit Renewal received February 24, 2025

# PRIMARY REGULATORY REQUIREMENTS

Standard Industrial Classification (SIC) Code: 2869 - Industrial Organic Chemicals, Not Elsewhere Classified.

<u>North American Industry Classification System (NAICS)</u>: 325199 – All Other Basic Organic Chemical Manufacturing.

## STATEMENT OF BASIS

HAP: The facility is identified as a major source of hazardous air pollutants (HAP).

<u>Title IV</u>: The facility does not operate units subject to the acid rain provisions of the Clean Air Act.

<u>Title V</u>: The facility is a Title V major source of air pollution in accordance with Chapter 62-213, Florida Administrative Code (F.A.C.).

<u>PSD</u>: The facility is a Prevention of Significant Deterioration (PSD)-major source of air pollution in accordance with Rule 62-212.400, F.A.C.

<u>NSPS</u>: The facility operates units subject to the New Source Performance Standards (NSPS) of 40 Code of Federal Regulations (CFR) 60.

<u>NESHAP</u>: The facility operates units subject to the National Emissions Standards for Hazardous Air Pollutants (NESHAP) of 40 CFR 63.

CAIR: The facility is subject to the Clean Air Interstate Rule (CAIR) set forth in Rule 62-296.470, F.A.C.

CAM: Compliance Assurance Monitoring (CAM) does not apply to any of the units at the facility.

<u>GHG</u>: The facility is not identified as a major source of greenhouse gas (GHG) pollutants.

### **PROJECT REVIEW**

This project renews Title V air operation permit No. 1130004-035-AV, issued on January 21, 2021. Administrative changes were made to specific conditions throughout the permit for clarity and consistency with current permitting templates.

### **Changes Since the Last Title V Air Operation Permit Renewal**

**Permit No. 1130004-037-AC:** This project authorized removal of a duplicative prevention of significant deterioration (PSD) tracking requirement, specifically, the limit on the amount of steam fed to the Dimethyl Laurylamine (DIMLA) Plant. No actual construction was authorized by this project.

**Permit No. 1130004-038-AC:** This project authorized the expansion of the DIMLA Plant to increase the production of dimethyl laurylamine (DIMLA) at the facility. Construction work for the DIMLA Plant expansion project will be allowed to proceed in phases (project milestones) as described in Administrative Requirement 9. of this permit.

*{Permitting Note: Phase 3 construction authorized by this permit was not completed as permitted, see Permit No. 1130004-045-AC for revised phases}* 

**Permit No. 1130004-039-AV:** This project revised the existing Title V Permit for the above referenced facility and incorporated air construction Permit No. 1130004-037-AC. Issue Date: September 21, 2021. Expiration Date: January 21, 2026.

**Permit No. 1130004-040-AC:** This project authorized the expansion of the Higher Amines Plants to increase the production of higher amines at the facility.

**Permit No. 1130004-041-AC:** Exemption from permitting pursuant to Rule 62-4.040(1)(b), F.A.C., to change the material of construction for three existing heat exchangers (E-62015A-C) from *carbon steel* to *stainless steel* in the DIMLA Plant.

**Permit No. 1130004-042-AV:** This project revised the Title V air operation permit for the above referenced facility and incorporated the Phase 1 construction activities that were authorized by Permit Nos. 1130004-038-AC and 1130004-040-AC. Issue Date: December 2, 2022. Expiration Date: January 21, 2026.

**Permit No. 1130004-043-AC**: Exemption from permitting pursuant to Rule 62-4.040(1)(b), F.A.C., to replace several fugitive components (valves, relief valves, a pump, and associated piping and instrumentation) associated with methylamines crude storage tank (D-67134C).

**Permit No. 1130004-044-AV:** This project revised the Title V air operation permit for the above referenced facility and incorporated the Phase 2 construction activities authorized by Permit Nos. 1130004-038-AC and 1130004-040-AC. Issue Date: August 6, 2024. Expiration Date: January 21, 2026.

**Permit No. 1130004-045-AC:** This project authorized additional expansions to the Dimethyl Laurylamine (DIMLA) Plant to increase the production of DIMLA at the facility (Project). This air construction permit superseded Permit No. 1130004-038-AC and replaced the Phase 3 construction work that is authorized by Permit No. 1130004-038-AC with five new construction phases to further expand the DIMLA Plan.

*{Permitting Note: This permit is not incorporated into the Title V air operation permit as of this renewal}* 

# CONCLUSION

This project renews Title V air operation Permit No. 1130004-035-AV, which was effective on January 21, 2021. This Title V air operation permit renewal is issued under the provisions of Chapter 403, Florida Statues (F.S.), and Chapters 62-4, 62-210, and 62-213, F.A.C.